

MATHEMATICAL MODEL FOR MULTIPLE COOLING TOWER PLUMES

by

Frank H. Y. Wu
Robert C. Y. Koh

W. M. Keck Laboratory of Hydraulics and Water Resources
Division of Engineering and Applied Science
CALIFORNIA INSTITUTE OF TECHNOLOGY
Pasadena, California

MATHEMATICAL MODEL FOR MULTIPLE COOLING TOWER PLUMES

by

Frank H. Y. Wu
Robert C. Y. Koh

Final Report

to

U.S. Environmental Protection Agency
Corvallis Environmental Research Laboratory
Corvallis, Oregon 97330

EPA Grant No. (5) R-803989-01-1

W. M. Keck Laboratory of Hydraulics and Water Resources
Division of Engineering and Applied Science
California Institute of Technology
Pasadena, California

ACKNOWLEDGEMENTS

The writers would like to express their gratitude to Professors Norman H. Brooks and John F. Kennedy for providing valuable comments and suggestions during the investigation. They would also like to thank Drs. Mostafa Shirazi and Larry Winianski for several stimulating discussions on the project.

The work reported herein was supported by EPA Grant Number (5) R-803989-01-1.

ABSTRACT

A mathematical model is developed resulting in a computer program for the prediction of the behavior of plumes from multiple cooling towers with multiple cells. A general integral method based on the conservation of mass, momentum, energy (heat), and moisture fluxes (before and after plume merging), were employed in the prediction scheme. The effects of ambient stratifications of temperature, moisture, and wind are incorporated in the model.

An axisymmetric round plume is assumed to be emitted from each individual cell before interference with neighboring plumes. A finite length slot plume in the central part and two half round plumes at both ends of the merged plume were used to approximate the plume after merging. The entrainment and drag functions are calculated based on the modified merged plume shape.

The computer output provides the predicted plume properties such as excess plume temperature, humidity and liquid phase moisture (water droplet), plume trajectory, width, and dilution at the merging locations and the beginning and ending points of the visible part of the plumes. Detailed printout and contour plots of excess temperature and moisture distribution can also be obtained if desired.

Based on comparison with laboratory data this model gives good predictions for the case of dry plumes (no moisture involved). It should be noted that several empirical coefficients are as yet not accurately known. Verification of this model for the wet plume (such as for prototype cooling tower plumes) and the determination of the values for these empirical coefficients to be used in prototype applications must await detailed comparison with field data.

TABLE OF CONTENTS

<u>Chapter</u>		<u>Page</u>
1.	INTRODUCTION	1
2.	THEORETIC MODEL	4
	2.1 Formulation	5
	2.2 Entrainment	13
	2.3 Merging Process	17
3.	COMPUTER PROGRAM	28
4.	RESULTS, COMPARISONS AND DISCUSSIONS	31
5.	CONCLUSIONS AND RECOMMENDATIONS	57
	REFERENCES	59
	APPENDIX A: COMPUTER PROGRAM	
	APPENDIX B: EXPLANATIONS OF THE IMPORTANT SYMBOLS IN THE PROGRAM MTP	
	APPENDIX C: LISTING OF PROGRAM	

LIST OF FIGURES

<u>Figure</u>		<u>Page</u>
2.1	Top View of the Coordinate System Associated with the Cooling Tower Configuration	6
2.2	Side View of the Coordinate System Associated with the Cooling Tower Configuration	6
2.3	Merged Plume Shape	19
2.4	Definition Sketch	20 21
2.5	Modified Merged Plume Shape	24
2.6	Correction of Δy for the Merged Plume	26
3.1	Flow Chart of the Computer Program	30
4.1	Excess Temperature Distribution for the Case of 4 Towers in Linear Array and 0° to Wind Direction	32
4.2	Excess Humidity Distribution for the Case of 4 Towers in Linear Array and 0° to Wind Direction	33
4.3	Excess Liquid Phase Moisture Distribution for the Case of 4 Towers in Linear Array and 0° to Wind Direction	34
4.4	Excess Temperature Distribution for the Case of 4 Towers in Linear Array and 90° to Wind Direction	35
4.5	Excess Humidity Distribution for the Case of 4 Towers in Linear Array and 90° to Wind Direction	36
4.6	Excess Liquid Phase Moisture Distribution for the Case of 4 Towers in Linear Array and 90° to Wind Direction	37
4.7	Excess Temperature Distribution for the Case of 4 Towers in Linear Array and 135° to Wind Direction	38
4.8	Excess Humidity Distribution for the Case of 4 Towers in Linear Array and 135° to Wind Direction	39
4.9	Excess Liquid Phase Distribution for the Case of 4 Towers in Linear Array and 135° to Wind Direction	40

LIST OF FIGURES (Continued)

<u>Figure</u>		<u>Page</u>
4.10	Excess Temperature Distribution for the Case of 5 Towers in Round Array	41
4.11	Excess Humidity Distribution for the Case of 5 Towers in Round Array	42
4.12	Excess Liquid Phase Moisture Distribution for the Case of 5 Towers in Round Array	43
4.13	Comparisons of Plume Trajectory, Width and Dilution Between the Present Theory and Fan's (1967) Experiments for $F = 20$ and $K = 8$	45
4.14	Comparisons of Plume Trajectory, Width and Dilution Between the Present Theory and Fan's (1967) Experiments for $F = 40$ and $K = 8$	46
4.15	Comparisons of Plume Trajectory, Width and Dilution Between the Present Theory and Fan's (1967) Experiments for $F = 80$ and $K = 16$	47
4.16	Comparisons of Plume Excess Temperature Between the Present Theory and Chan et al.'s (1974) Experiments for $F = 4$ and $K = 1.02$	48
4.17	Comparisons of Plume Trajectories Between the Present Theory and TVA (1968, TVA-11, single tower) Field Data in a Stable Atmospheric Condition ($\partial\theta/\partial z = 0.59^\circ\text{K}/100\text{ m}$)	50
4.18	Comparisons of Plume Trajectories Between the Present Theory and TVA (1968, TVA-14, two towers) Field Data in an Atmosphere with an Inversion ($\partial\theta/\partial z = 1.42^\circ\text{K}/100\text{ m}$)	51

LIST OF TABLES

<u>Table</u>		<u>Page</u>
4.1	Input Data Cards for Example Cases (Different Wind Directions to a Line Array (3 cases) and Round Array (one case) of Towers)	52
4.2	Input Data Cards for Three Cases of Fan's (1967) Experiments with $F = 20$, $K = 8$; $F = 40$, $K = 8$; and $F = 80$, $K = 16$	53
4.3	Input Data Cards for Chan et al.'s (1974) Experiment with $F = 4$, $K = 1.02$	54
4.4	Input Data Cards for TVA (1968, TVA-11, single tower) Field Data in a Stable Atmospheric Condition ($\partial\theta/\partial z = 0.59^\circ\text{K}/100\text{ m}$)	55
4.5	Input Data Cards for TVA (1968, TVA-14, two towers) Field Data in an Atmosphere with an Inversion ($\partial\theta/\partial z = 1.42^\circ\text{K}/100\text{ m}$)	56

LIST OF SYMBOLS

a_1	Entrainment coefficient associated with jet type entrainment
a_2	Entrainment coefficient associated with the effect of buoyancy
a_3	Entrainment coefficient associated with thermal type entrainment
a_4	Entrainment coefficient associated with ambient turbulence
a	Finite length of the slot plume in the central part of the merged plume
A	Finite length of the slot plume in the central part of the modified merged plume
b	Plume radius
b_{r1}, b_{r2}	Plume radii at the ends of the merged plume
b_s	Plume width of the slot plume in the central part of the merged plume
$B1, B2$	Plume radii at the ends of the modified merged plume
BXZ	Plume half height of the cross-section normal to s-axis
BY	Plume half width
C	Tracer concentration
C_d	Drag coefficient
C_{pa}	Specific heat at constant pressure
e_s	Saturation vapor pressure
E	Volume rate of entrainment
E_{1r}	Volume rate of entrainment associated with the effects of momentum and buoyancy for a round plume
E_{1s}	Volume rate of entrainment associated with jet type entrainment for slot plume
E_2	Volume rate of entrainment associated with thermal type entrainment

LIST OF SYMBOLS (Continued)

E_3	Volume rate of entrainment associated with ambient turbulence
F	Sum of excess vapor and liquid phase moisture fluxes (H+W)
F^2	Densimetric Froude number ($m^{5/2}/\mu^2\beta$)
Fr_L	Local densimetric Froude number ($U_p^2 / [(\rho_a - \rho_p)bg/\rho_o]$)
Fr_{LC}	Critical local densimetric Froude number
g	Acceleration of gravity
G	$T - L_v W/C_{pa}$
H	Excess vapor phase (humidity) moisture flux
HT	Total height of the merged plume
L_v	Latent heat of evaporation or condensation
m	Kinematic momentum flux ($\int_A u_p^2 dA$)
M	Excess kinematic momentum flux
p_d	Dry air absolute pressure
p_t	Total absolute pressure ($p_d + e_s$)
P	Plume periphery
q	Specific vapor phase moisture (humidity)
Q	Plume volume flux
s	Plume trajectory
t	Temperature
t_s	Steam point temperature
T	Excess temperature flux
U	Velocity
U_a'	Measure of ambient turbulent fluctuation
U_{r1}, U_{r2}	Plume velocities at both ends of merged plumes

LIST OF SYMBOLS (Continued)

U_s	Plume velocity at central part of merged plume
W	Excess liquid phase moisture flux
W_d	Plume width
WD	Total width of the merged plume
x	x-coordinate (parallel to wind direction)
y	y-coordinate (normal to x-axis)
z	z-coordinate (vertical coordinate)
α_j	Entrainment coefficient for pure jet ($F_1 \rightarrow \infty$)
α_p	Entrainment coefficient for pure plume
β	Buoyancy flux ($\int_A g U_p (\rho_a - \rho_p) / \rho_a dA$)
Γ	Adiabatic lapse rate
θ	Angle between the tangent of s and x-axis
ρ	Density
σ	Liquid phase moisture
ϕ	Angle between the centerline of the (inclined) plume cross-section and the horizontal line parallel to y-axis
μ	Volume flux ($\int_A U_p dA$)
$()_a$	in ambient
$()_o$	at tower exit
$()_p$	in plume

CHAPTER 1

INTRODUCTION

The use of multiple cooling towers is a common means of disposal of waste heat from large power plants. A better understanding of the behavior and interaction of plumes from multiple towers would be useful not only to cooling tower design and operation, but also in the assessment of their environmental impact. Due to the relatively close proximity of neighboring tower exits, the individual plumes from multiple cooling towers rapidly interfere with one another, thus changing the overall plume shape and its mixing characteristics. In addition, the ambient stability (temperature profile), humidity, wind velocity and wind direction to the tower array also influence the plume behavior. In this report a mathematical model resulting in a computer program is developed which will provide the framework to allow reasonable predictions to be made of the characteristics of plumes from multiple cooling towers under various ambient conditions.

Throughout this report, no distinction will be made between a plume and a jet. Neither will the distinction be made between the multiple plumes from the several cells of a tower and the multiple plumes from several individual towers.

The plume from a cooling tower is a buoyant jet which has been studied in the past by numerous investigators, such as Morton, et al. (1956), Morton (1957), Slawson and Csanady (1967,1971), Koh and Brooks (1975). Several existing single tower plume models, including dry and wet plumes, were developed by Briggs (1969), Hoult et al. (1969), Abraham (1970), Fox (1970), Csanady (1971), Wigley and Slawson (1971,1972),

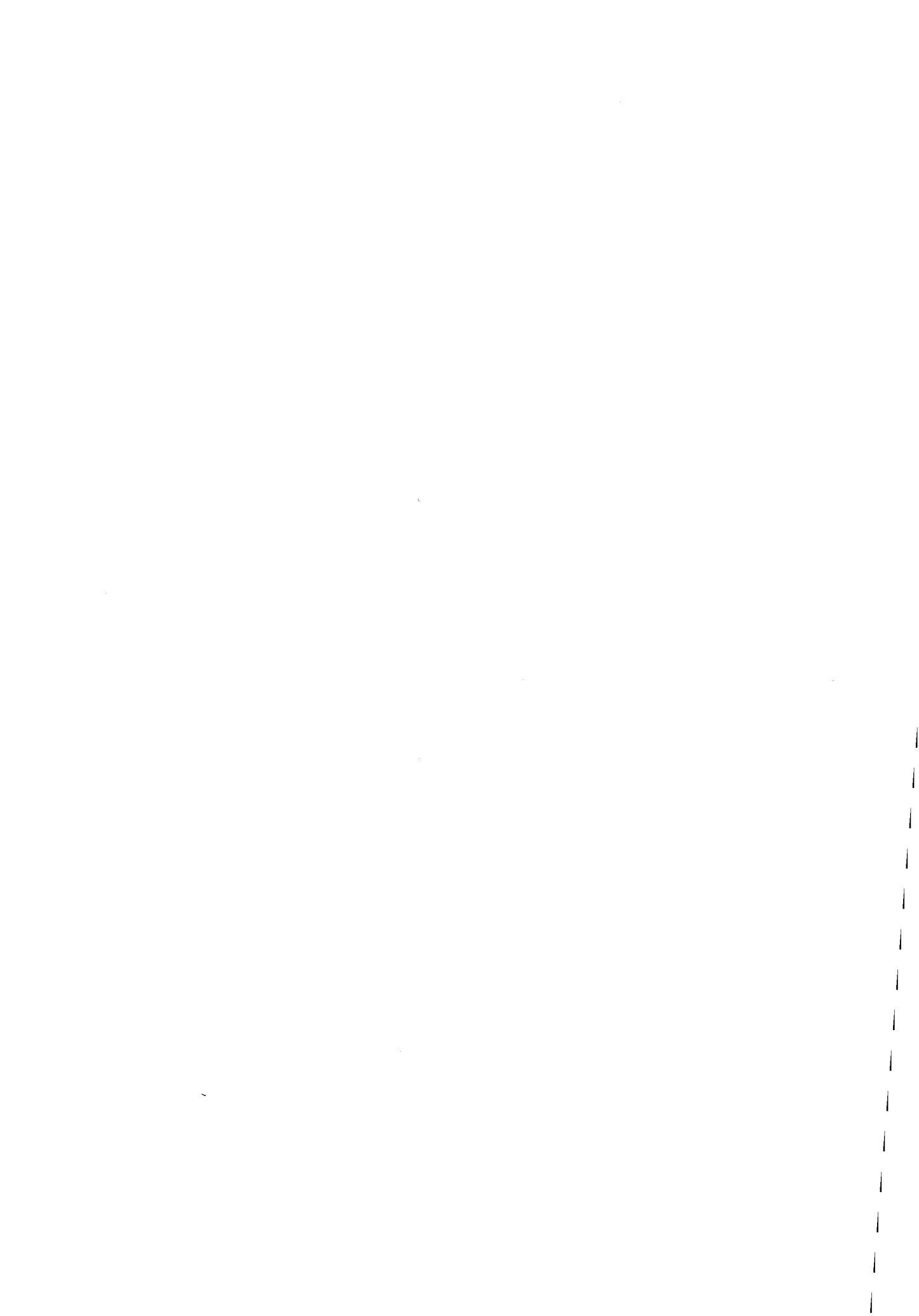
Hirst (1971), Hanna (1972), Weil (1974), Wigley (1975a,b), and Schatzmann (1977).

A model for multiple plumes was first developed by Koh and Fan (1970) in analysing the analogous problem of disposal of waste heat into the ocean by multiple port diffusers. The integral method was used and the individual round buoyant jets were approximated by a two-dimensional slot jet after interference. A transition region during merging was considered. Although a discontinuous centerline temperature resulted at the point of merging, the overall predictions of the plume properties were quite satisfactory. Jirka and Harleman (1974) approached the multiple port diffuser problem by replacing it with an equivalent slot jet having the same mass and momentum fluxes as the multi-port discharge. As expected this method generally over-estimates dilution except for those instances when the plumes are very close to each other initially. Briggs (1974) added an enhancement factor to his single tower equation for plume rise by considering the effects of number of towers and tower spacing. Meyer et al. (1974) modified Briggs' equation and used a "peak factor" to develop a model which can give a fairly good prediction of visible plume length. However, the prediction of the plume trajectory is less accurate. Davis (1975) developed a mathematical model for calculating plume rise and dilution from multiple cell mechanical draft cooling towers with the wind normal to the tower array. The entrainment function used includes the effects of plume interference and the changing entrainment surfaces during merging. The model also provides calculation techniques for various modes of plume development. The plume properties remain continuous when the calculations proceed

smoothly from one zone to another. The values of the coefficients in his entrainment function still need to be determined from suitable laboratory and field experiments.

Data from multiple towers are very scarce. Chan et al. (1974) made laboratory simulations of plumes from multiple towers using water as the fluid medium. Two sets of normalized excess temperature distributions were presented. These are useful for model comparisons. The studies by Carpenter et al. (1968) and Slawson et al. (1975) at TVA gave field data on plume trajectory and some plume properties. More complete data including plume trajectory, width, dilution, and ambient conditions (i.e. temperature, humidity and wind velocity profiles, wind direction to tower array, tower configuration, etc.) however are required for proper verification.

The model developed in this report is based on a general integral method applied to the conservation equations for mass, momentum, energy, and moisture fluxes. An axisymmetric round plume is assumed initially for each tower exit. As the plumes merge, combinations of round and slot plumes are employed to simulate the shape of the resulting merged plumes. The merging criteria, merging processes, changes of plume shape and entrainment functions are a part of the model and are discussed in Chapter 2. Some results of model predictions and comparisons with laboratory and field data are presented and discussed in Chapter 4. A computer program has been written to perform the calculations and is included in Chapter 3 and Appendices A and C.



CHAPTER 2

THEORETICAL MODEL

The present mathematical model is developed for the prediction of plume properties from multiple cooling towers. These include plume temperature, moisture (vapor and liquid phases), excess temperature, excess moisture, velocity, width, dilution, trajectory and visible plume length. For ease of application to practical situations, this model is capable of handling rather arbitrary vertical profiles of ambient temperature, humidity, and velocity; arbitrary but steady wind direction to the tower array; and randomly arranged tower configurations.

The assumptions made in developing this model are as follows:

1. The flow is fully turbulent. Molecular transport can be neglected in comparison with turbulent transport so that there is no Reynolds number dependence.
2. Longitudinal turbulent transport is small compared with longitudinal advective transport.
3. Pressure is hydrostatic throughout the flow field.
4. The cross-plume profiles are similar for plume velocity, temperature, density, humidity and liquid phase moisture.
5. The Boussinesq assumption is valid. This implies that the variations of fluid density throughout the flow field are small compared with the reference density chosen. The variations in density are only considered in the buoyancy term.

Using these assumptions, a general integral model for multiple cooling tower plumes based on the conservation of mass, momentum, energy and moisture fluxes along the plume trajectory is developed. By providing

the ambient conditions and the empirical equations for entrainment and drag, the conservation equations are integrated stepwise for the center line properties along the plume trajectory. Before interference the plumes are assumed to be individual, axisymmetric, round buoyant jets. During the merging process, a combination of a finite slot jet in the central part and two half round jets at both ends is assumed to be the cross-sectional shape of the merged plume as an approximation but only for the calculation of entrainment and drag. Finally, the completely merged plume gradually tends to become round in cross section again, whereupon the individual axisymmetric analysis is reapplied. The formulations of the basic plume conservation equations, entrainment function, merging criterion and merging process are presented in the following sections.

2.1 Formulation

The coordinate system chosen with a typical cooling tower configuration is shown in Figures 2.1 and 2.2. The x-axis is parallel to the steady ambient wind direction. s is the coordinate along the plume path and θ is the angle between the tangent to s and the x-axis. The individual plumes from the cooling tower cells are presumed to be discharged vertically into a stratified atmosphere, and bent over due to the effect of ambient wind. The plume properties are defined as velocity U , density ρ , temperature t , specific humidity q , and liquid phase moisture σ . Here, the specific humidity (vapor phase moisture) q and liquid phase moisture σ are defined as the ratio of mass of vapor (or liquid) phase moisture to the total mass of the mixture in a unit volume. The subscripts o , p , and a are used for the values at tower

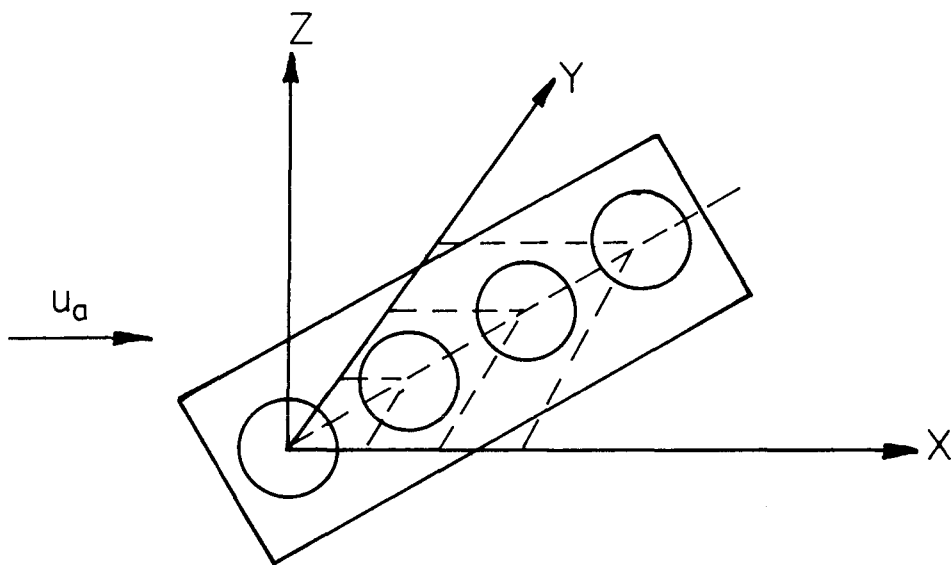


Figure 2.1 Top View of the Coordinate System Associated with the Cooling Tower Configuration

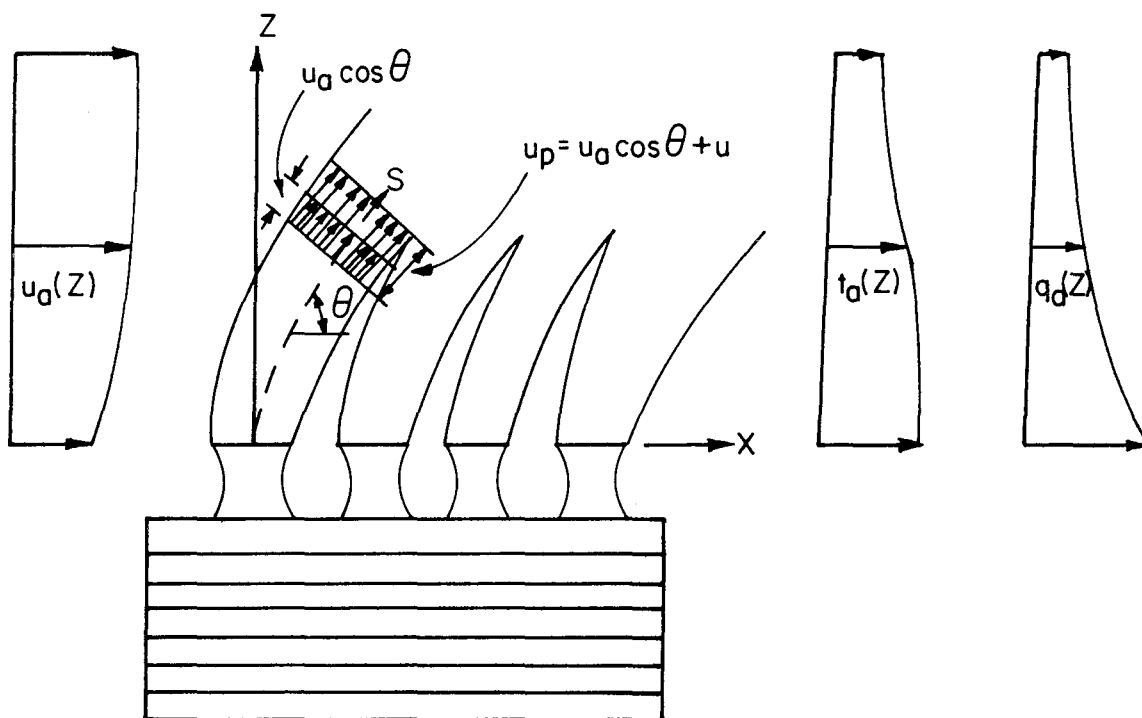


Figure 2.2 Side View of the Coordinate System Associated with the Cooling Tower Configuration

exit, in the plume, and in the ambient atmosphere, respectively. The plume volume flux Q , kinematic momentum flux M , temperature deficiency flux T , vapor phase moisture (or humidity) deficiency flux H , and liquid phase moisture deficiency flux W are defined as follows:

$$Q = \int_A U_p \, dA \quad (2.1)$$

$$M = \int_A U_p^2 \, dA \quad (2.2)$$

$$T = \int_A (t_p - t_a) U_p \, dA \quad (2.3)$$

$$H = \int_A (q_p - q_a) U_p \, dA \quad (2.4)$$

$$W = \int_A (\sigma_p - \sigma_a) U_p \, dA \quad (2.5)$$

Any 'rainout' of liquid droplets in the ambient atmosphere will be neglected so that σ_a is equal to zero.

The conservation of mass equation is:

$$\frac{d}{ds} \left\{ \int_A \rho_p U_p \, dA \right\} = \rho_a E \quad (2.6)$$

where E is the volume rate of entrainment of ambient fluid. The function used for E is an empirical expression including the effects of plume geometry, local mean velocity, buoyancy and ambient turbulence. The detailed form of E is presented in Section 2.2.

The conservation equation for horizontal momentum flux is:

$$\frac{d}{ds} \left\{ \int_A \rho_p U_p^2 \, dA \cdot \cos \theta \right\} = \rho_a U_a E + \frac{1}{2} \rho_a U_a^2 \sin^2 \theta C_d W_d |\sin \theta| \quad (2.7)$$

where the first term on the right hand side of equation (2.7) is due to the momentum of the entrained ambient fluid and the second term is due to the horizontal drag force (Fan, 1967) on the plume; C_d is a drag coefficient to be determined empirically and W_d is the width of the plume; the absolute value of $\sin\theta$ is used in order to account for both the ascending and descending parts of the plume.

The conservation equation for vertical momentum flux is:

$$\frac{d}{ds} \left\{ \int_A \rho_p U_p^2 dA \cdot \sin\theta \right\} = g \int_A (\rho_a - \rho_p) dA - g \int_A \rho_p \sigma_p dA \mp \frac{1}{2} \rho_a U_a^2 \cdot \sin^2 \theta C_d W_d \cos\theta \quad (2.8)$$

where the first term on the right hand side of equation (2.8) is the buoyancy force due to the density difference between the plume and ambient fluid; the second term is the effect of the weight of liquid droplets suspended in the plume; the third term is the vertical drag force on the plume with the negative and positive signs corresponding to $0 \leq \theta \leq \pi/2$ and $-\pi/2 \leq \theta < 0$, respectively.

Koh and Fan (1970) have shown that the governing equation for the flux of a tracer quantity C is as follows:

$$\frac{d}{ds} \int_A (C_p - C_a) U_p dA = - \frac{dC_a}{ds} \int_A U_p dA \quad (2.9)$$

where C_p and C_a are the tracer concentrations in the plume and the ambient, respectively. Now considering the temperature flux and also taking into account the effects of atmospheric adiabatic lapse rate Γ

and the liberation of latent heat due to condensation of water vapor inside the plume (Csanady, 1971), the conservation equation for energy (or heat) flux is derived as follows:

$$\frac{d}{ds} \int_A (t_p - t_a) U_p dA = - \left(\frac{dT_a}{dz} + \Gamma \right) \sin\theta \int_A U_p dA + \frac{d}{ds} \int_A \frac{L_v}{C_{pa}} \sigma_p U_p dA \quad (2.10)$$

where L_v is the latent heat of evaporation (or condensation) i.e.,
 $L_v(t) = [597.31 - 0.57x(t^\circ\text{C})] \times 4.1868 \text{ Jg}^{-1}$ for $t \geq 0^\circ\text{C}$ and
 $L_v = [677 + 0.622 \times (t^\circ\text{C})] \times 4.1868$ for $t < 0^\circ\text{C}$, and C_{pa} is the specific heat of air at constant pressure.

The conservation equation for (vapor and liquid phase) moisture flux is:

$$\frac{d}{ds} \int_A (q_p - q_a) U_p dA + \frac{d}{ds} \int_A \sigma_p U_p dA = - \frac{dq_a}{dz} \sin\theta \int_A U_p dA \quad (2.11)$$

We assume a top-hat distribution of plume properties across the plume. Therefore, U_p , T_p , ρ_p , q_p , and σ_p are constants inside the plume. In particular, U_p is defined as follows:

$$U_p = U_a \cos\theta + U \quad (2.12)$$

where U is the 'net' plume velocity relative to the ambient wind.

Applying the relationship between temperature and density for a constant pressure process (pressure variations in the plume cross section is neglected) we can write:

$$\frac{\rho_a}{\rho_p} = \frac{t_p}{t_a} ; \text{ and } \frac{\rho_{a-p}}{\rho_p} = \frac{t_p - t_a}{t_a} \quad (2.13)$$

The conservation equations may now be rewritten as:

$$\frac{dQ}{ds} = \frac{t_p}{t_a} E \quad (2.14)$$

$$\frac{d}{ds} \{M \cos\theta\} = \frac{t_p}{t_a} \{U_a E + 0.5 U_a^2 \sin^2\theta C_d W_d |\sin\theta|\} \quad (2.15)$$

$$\frac{d}{ds} \{M \sin\theta\} = g \left\{ \frac{t_p - t_a}{t_a} - \sigma_p \right\} \int_A dA + \frac{t_p}{t_a} 0.5 U_a^2 \sin^2\theta C_d W_d \cos\theta \quad (2.16)$$

$$\frac{d}{ds} \left\{ T - \frac{L_v}{C_{pa}} W \right\} = - \left(\frac{d t_a}{dz} + \Gamma \right) \cdot \sin\theta \cdot Q \quad (2.17)$$

$$\frac{d}{ds} \{H + W\} = - \frac{dq_a}{dz} \cdot \sin\theta \cdot Q \quad (2.18)$$

In addition, the equations for the geometrical relations yield

$$\frac{dx}{ds} = \cos\theta \quad (2.19)$$

$$\frac{dz}{ds} = \sin\theta \quad (2.20)$$

Since U_p , t_p , σ_p and W_d can be written in terms of M , Q , T and W (Koh and Fan, 1970); for instance, $U_p = 2M/Q$ for round plume, the system of equations (2.14) to (2.20) constitute seven ordinary differential equations for the eight unknowns, Q , M , θ , T , H , W , x and z as functions of s . For closure, one more equation is needed. This extra condition is:

$$\sigma_p = 0 \quad \text{for } q_p < q_{sp} \text{ (dry plume)} \quad (2.21)$$

$$q_p = q_{sp}(t_p) \quad \text{for } q_p \geq q_{sp} \text{ (wet plume)}$$

where q_{sp} is the plume saturation specific humidity.

Equation (2.21) implies that when the plume is unsaturated, no liquid phase moisture due to condensation need be considered and when the plume is saturated, the plume humidity is equal to the plume saturation specific humidity. To calculate the saturated specific humidity, thermodynamic equilibrium between liquid and vapor is assumed. The Clausius-Clapeyron equation (or tabulated values) can then be used to calculate the saturated humidity. The equation used in the model to calculate the saturated specific humidity q_s is (Linsley et al., 1975):

$$q_s(t,p) = \frac{0.622e_s(t)}{P_t - 0.378 e_s(t)} = \frac{0.622 e_s(t)}{P_d(z) + e_s(t) - 0.378 e_s(t)} \quad (2.22)$$

where t and p are absolute temperature and pressure, respectively; P_t is the total pressure which is the sum of the dry air pressure $P_d(z)$ and the saturated vapor pressure $e_s(t)$.

Since the variation of pressure is small (for instance, $\Delta P = 1\%$ of P corresponding to $\Delta z \approx 100M$), the absolute pressure at sea level (i.e., $P_d = 1013.25$ mb) is used in equation (2.22), which becomes:

$$q_s(t) = \frac{0.622 e_s(t)}{1013.25 + 0.622 e_s(t)} \quad (2.23)$$

An approximate expression of $e_s(t)$ was developed by Richards (1971)

as

$$e_s(t) = 1013.25 \times \exp(13.3185 t_v - 1.9760 t_v^2 - 0.6445 t_v^3 - 0.1299 t_v^4)$$

where

$$t_v = 1 - \frac{t_s}{t}$$

and t_s is the steam point temperature ($^{\circ}\text{K}$). The result from this equation is very accurate (to within 0.1%) over the wide range of temperature -50°C to 140°C (Wigley, 1974). Within the range 0° to 100°C it is accurate to within the limits of accuracy of the accepted Goff-Gratch formula. In this study t_s is equal to 373.16°K . Because both q_s and t are unknown in the governing equations, the implicit form of equation (2.23) would require an iteration scheme in the calculation. In the model, the Newton method was adopted for this iteration.

With the additional equation (2.23) and the Newton iteration method, the system of equations (2.14) to (2.21) may now be solved given the initial values of the unknowns at tower exit (or $s=0$). The initial values are as follows;

$$\begin{aligned} Q_o &= \int_A U_p \, dA = \frac{\pi}{4} D_o^2 U_o \\ \theta_o &= 90^{\circ} \\ M_o \cos \theta_o &= 0 \\ M_o \sin \theta_o &= \int_A U_p^2 \, dA = \frac{\pi}{4} D_o^2 U_o^2 = Q_o U_o \\ G_o &= T_o - \frac{L_v}{C_{pa}} W_o = \frac{\pi}{4} D_o^2 U_o \left(t_o - t_{ao} - \frac{L_v}{C_{pa}} \sigma_o \right) \\ &= Q_o \left(t_o - t_{ao} - \frac{L_v}{C_{pa}} \sigma_o \right) \end{aligned} \quad (2.24)$$

$$\begin{aligned} F_o &= H_o + W_o = \frac{\pi}{4} D_o^2 U_o (q_o - q_{ao} + \sigma_o) \\ &= Q_o (q_o - q_{ao} + \sigma_o) \end{aligned}$$

$$x_o = 0$$

$$z_o = 0$$

where the subscripts o and ao are associated with the values at tower exit (or initial values) and the ambient at the same level, and

$$L_v(t) = [597.31 - 0.57 \times t_o (^{\circ}\text{C})] \times 4.1868 \text{ Jg}^{-1}, \text{ and } C_{pa} = 1.005 \text{ Jg}^{-1}\text{K}^{-1}.$$

2.2 Entrainment

The entrainment of ambient fluid into the plume is a function of plume geometry, local mean velocity, buoyancy, and ambient turbulence. The entrainment function first proposed by Morton et al. (1956) is:

$$E_{1r} = \alpha 2\pi b U_p \quad (2.25)$$

where α is entrainment coefficient determined from experiments; b is the round jet radius; and U_p is the jet centerline velocity.

Based on the integral conservation equations of mass, momentum, energy, and mechanical energy, and assuming similar profiles, Fox (1970) and Hirst (1971) derived an entrainment function for round jets which includes the effect of buoyancy to the entrainment. It reads as follows:

$$E_{1r} = (a_1 + \frac{a_2}{Fr_L} \sin\theta) 2\pi b U_p \quad (2.26)$$

where a_1 and a_2 are entrainment coefficients, and Fr_L is the local densimetric Froude number defined as $Fr_L = U_p^2 / [(\rho_a - \rho_p) b g / \rho_o] = U_p^2 / [(t_p - t_a) t_o b g / t_p t_a]$, and g is gravitational acceleration. Based on experimental results, a_1 was determined to be 0.057 for pure round jet with Gaussian profile distribution (i.e., $Fr_L \rightarrow \infty$). Hirst (1971) suggested the value of $a_2 = 0.97$. This appears to be too large when his results are compared with experiments. A better estimate of the value of

a_2 can be made from the work of List and Imberger (1973), who, based on dimensional analysis and experimental data, derived a similar expression for E_{1r} for round jets (Koh and Brooks, 1975)

$$E_{1r} = (0.057 + \frac{0.083}{F^2}) 2\pi b U_p \quad (2.27)$$

where $F^2 = m^{5/2}/\mu^2\beta$ with m being the kinematic momentum flux
 $= \int_A U_p^2 dA$, μ the volume flux $= \int_A U_p dA$, and β the buoyancy flux
 $= \int_A gU_p \frac{\rho_a - \rho_p}{\rho_a} dA$.

Comparing equations (2.26) and (2.27) in a quiescent ambient (i.e. $\sin\theta = 1$) and calculating F^2 by using the Gaussian similarity profiles for U_p and ρ_p , one finds $a_2 = 0.083 Fr_L/F^2 \approx 0.4775$. Hence equation (2.26) becomes

$$E_{1r} = (0.057 + \frac{0.4775}{Fr_L} \sin\theta) 2\pi b U_p \quad (2.28)$$

The entrainment coefficient α in equation (2.25) has the extreme values for pure jet (i.e., $Fr_L \rightarrow \infty$) $\alpha_j = 0.057$ and pure plume (i.e., $Fr_L \rightarrow 0$) $\alpha_p = 0.082$ in a quiescent ambient. A critical value of Fr_L may be determined from

$$0.082 = 0.057 + \frac{0.4775}{Fr_{LC}}$$

which gives

$$Fr_{LC} = 19.1$$

For Gaussian similarity profiles of plume properties it will be assumed that

$$\begin{aligned} E_{1r} &= (0.057 + \frac{0.4775}{Fr_L} \sin\theta) 2\pi b U_p \quad \text{for } Fr_L > 19.1 \\ &= 0.082 \cdot 2\pi b U_p \quad \text{for } Fr_L \leq 19.1 \end{aligned} \quad (2.29)$$

which implies that $Fr_L = 19.1$ was considered a small number below which the entrainment of a buoyant jet is similar to that of a pure plume.

Experimental results for two-dimensional slot jet are not sufficiently comprehensive to obtain a similar entrainment expression [i.e., equation (2.29)] (Koh and Brooks, 1975). Therefore, based on the experimentally determined entrainment coefficient, the following form will be used for the slot jet with Gaussian profile distribution, viz.,

$$E_{1s} = 0.14 \cdot 2A \cdot U_p \quad (2.30)$$

where A is the length of the slot jet.

The entrainment functions embodied in equations (2.29) and (2.30) are based on Gaussian profiles of plume properties. In this study, top-hat similarity profiles are assumed. The difference in the resulting entrainment functions [equations (2.29) and (2.30)] due to this is a factor of $\sqrt{2}$. Therefore, equations (2.29) and (2.30) can be rewritten as follows:

$$\begin{aligned} E_{1r} &= \left(0.0806 + \frac{0.6753}{Fr_L} \sin\theta\right) 2\pi b U_p \quad \text{for } Fr_L > 19.1 \\ &= 0.1160 \quad 2\pi b U_p \quad \text{for } Fr_L \leq 19.1 \end{aligned} \quad (2.31)$$

$$E_{1s} = 0.198 \cdot 2AU_p \quad (2.32)$$

As the plume bends over towards the direction of the ambient wind, the plume velocity is about equal to the wind velocity. Then the entrainment should be nearly as if the plume were a two-dimensional thermal in a stagnant atmosphere. This entrainment is proportional to the jet periphery and the velocity of the thermal. Abraham (1970) proposed the

following form

$$E_2 = a_3 P U_a \sin\theta \cos\theta \quad (2.33)$$

where P is the jet periphery, $\cos\theta$ is arbitrarily chosen to diminish the thermal type of entrainment closed to the initial stage of the vertical jet, and a_3 is the entrainment coefficient for a line thermal. For large Reynolds number, the experimentally determined value of a_3 is 0.5 (Richards, 1963). But a better value suggested by Koh and Chang (1973) from their plume measurements and numerical model is 0.3536, which will be used in this present model. Thus

$$E_2 = 0.3536 P U_a \sin\theta \cos\theta \quad (2.34)$$

Another type of entrainment is associated with ambient turbulence, and expressed as

$$E_3 = a_4 P U'_a \quad (2.35)$$

where a_4 and U'_a are the entrainment coefficient and a measure of turbulent velocity fluctuations. Based on dimensional analysis, Briggs (1969) found that U'_a is associated with eddy energy dissipation in the inertial subrange and gave an estimate of $a_4 = 1$. In practice, the root-mean-square value of the ambient wind velocity fluctuation may be used to approximate U'_a , which is equal to a few percent of the mean wind velocity under normal atmospheric conditions.

Finally, we may combine equations (2.31), (2.32), (2.34) and (2.35) to construct a complete entrainment function as

$$E = P \{ \alpha |U| + 0.3536 U_a |\sin\theta \cos\theta + 1.0 U'_a \} \quad (2.36)$$

where for a round jet,

$$P = 2\pi b$$

$$\alpha = 0.0806 + \frac{0.6753}{Fr_L} |\sin\theta| \quad \text{for } Fr_L > 19.1$$

$$= 0.1160 \quad \text{for } Fr_L \leq 19.1$$

and for a slot jet,

$$P = 2A$$

$$\alpha = 0.198$$

Here U is the net velocity in the plume relative to the ambient velocity; the absolute value is used here to account for both the ascending and descending parts of the plume.

In the literature on buoyant jets, various investigators employing the integral approach have devised differing entrainment functions. A recent survey for the round jet can be found in Wright (1977). The entrainment function expressed in equation (2.36) and incorporated in the present model is but one possible expression. Should a different form be shown to be superior in the future, the model can readily be modified.

2.3 Merging Process

The individual plumes from the multiple cells of a cooling tower typically merge within a relatively short distance from the exits. Before the plumes merge, equations for individual round buoyant jets are applied in this model to calculate the plume behavior. When several individual plumes are merged, the resulting plume cross-section is no longer round, but rather tends to be elliptical in shape. In this model,

this merged plume is approximated by a slot jet in the central part and two half round jets at the two ends of the merged plume as shown by the solid lines in Figure 2.3. The nonuniform size of the plume is due to the effect of the wind direction with respect to the tower configuration. In general, it is necessary to consider all types of plume merging including all the possible combinations between individual round plumes and modified merged plumes as shown in Figure 2.4. The basic merging criterion considered here is that the plume cross-sections are in contact with each other. An additional criterion is incorporated for the merging between two individual round plumes: the area of the trapezoid should be equal to the sum of the areas of the two half round plumes as circled by the dashed lines in Figure 2.3. When the plumes satisfy these merging criteria, they are merged. The fluxes of the merged plumes are summed to maintain the conservation of fluxes. Moreover, the new shape and the new centroids of the merged plumes are determined, and the integration of the equations is continued. Upon merging, the entrainment and drag functions are altered due to the change in plume shape. The merged plume shape is characterized by the radii B_1 and B_2 of the two half round plumes, length of the slot jet A , and the angle ϕ (shown in Figure 2.3) between the centerline of the (inclined) plume cross-section and the horizontal line parallel to the y -axis. As the plumes merge a new set of B_1 , B_2 , A and ϕ should be determined in order to calculate the entrainment and drag and to check if any other new plume merging occurred. To determine B_1 , B_2 , A and ϕ the plumes are classified into two categories: one will be called horizontal for which the total width (WD) of the new merged plume is larger than the total

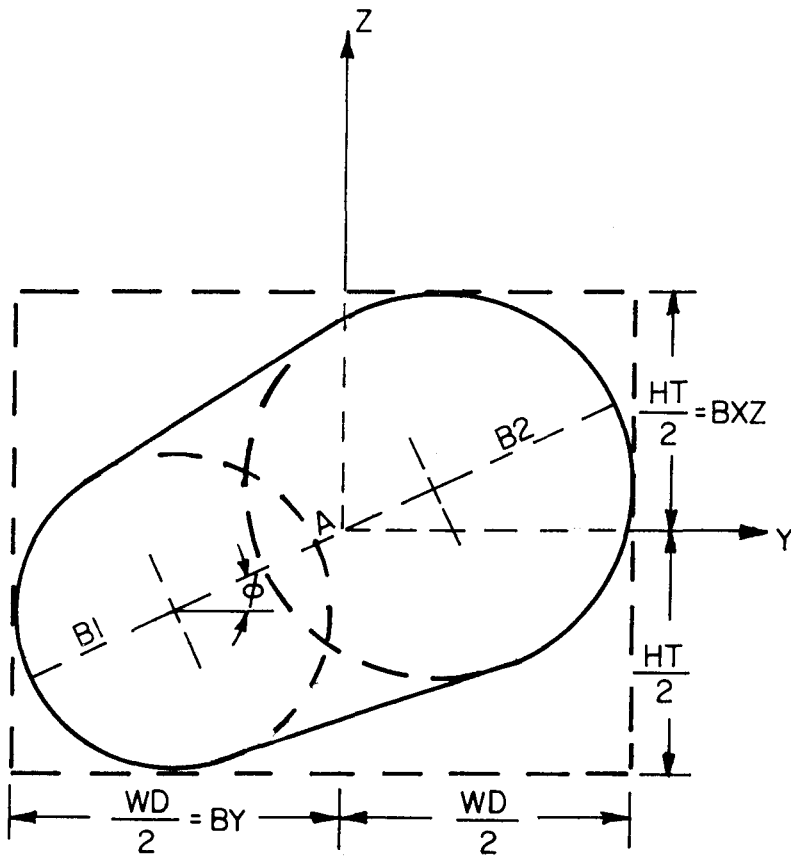


Figure 2.3 Merged Plume Shape

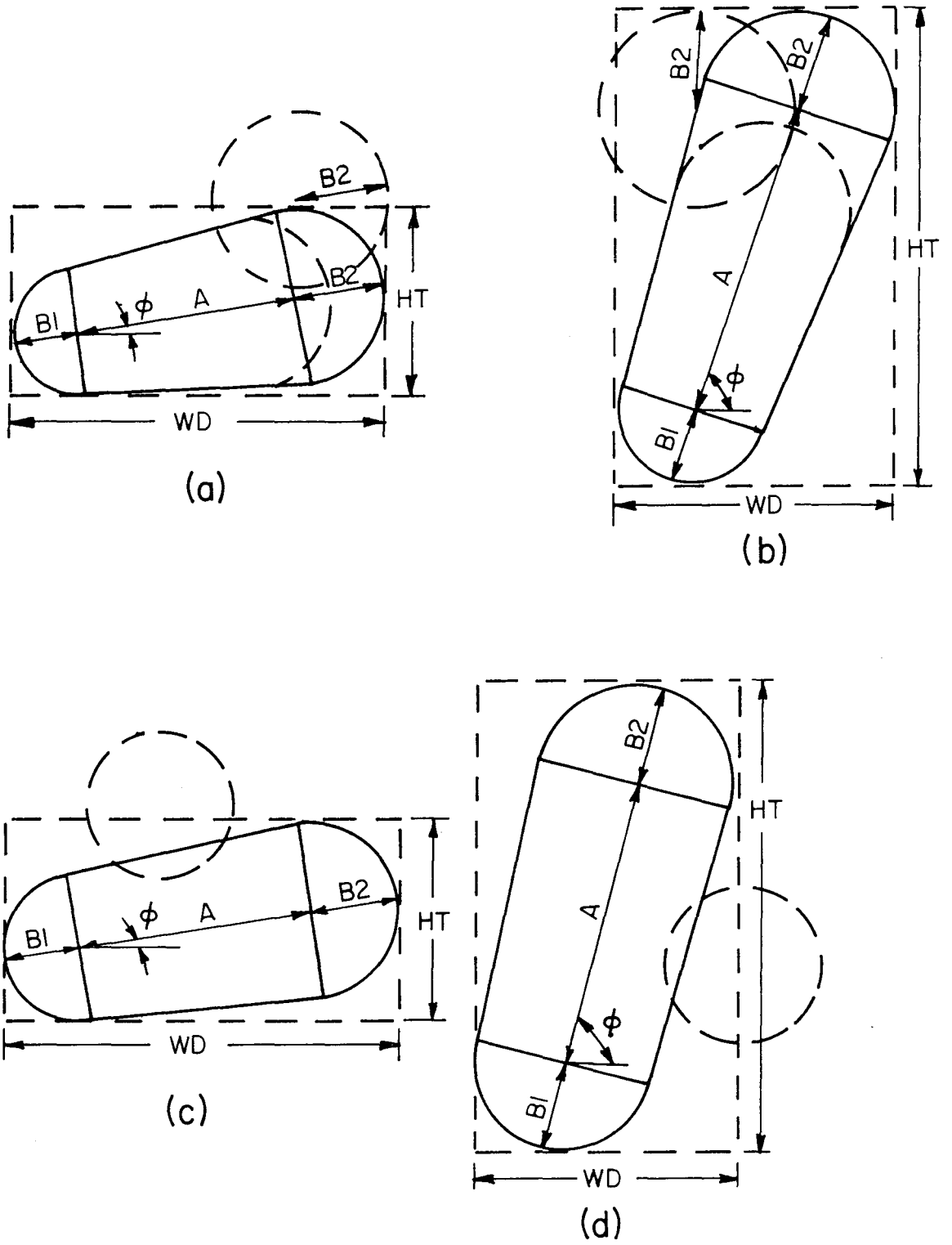


Figure 2.4 Definition Sketch

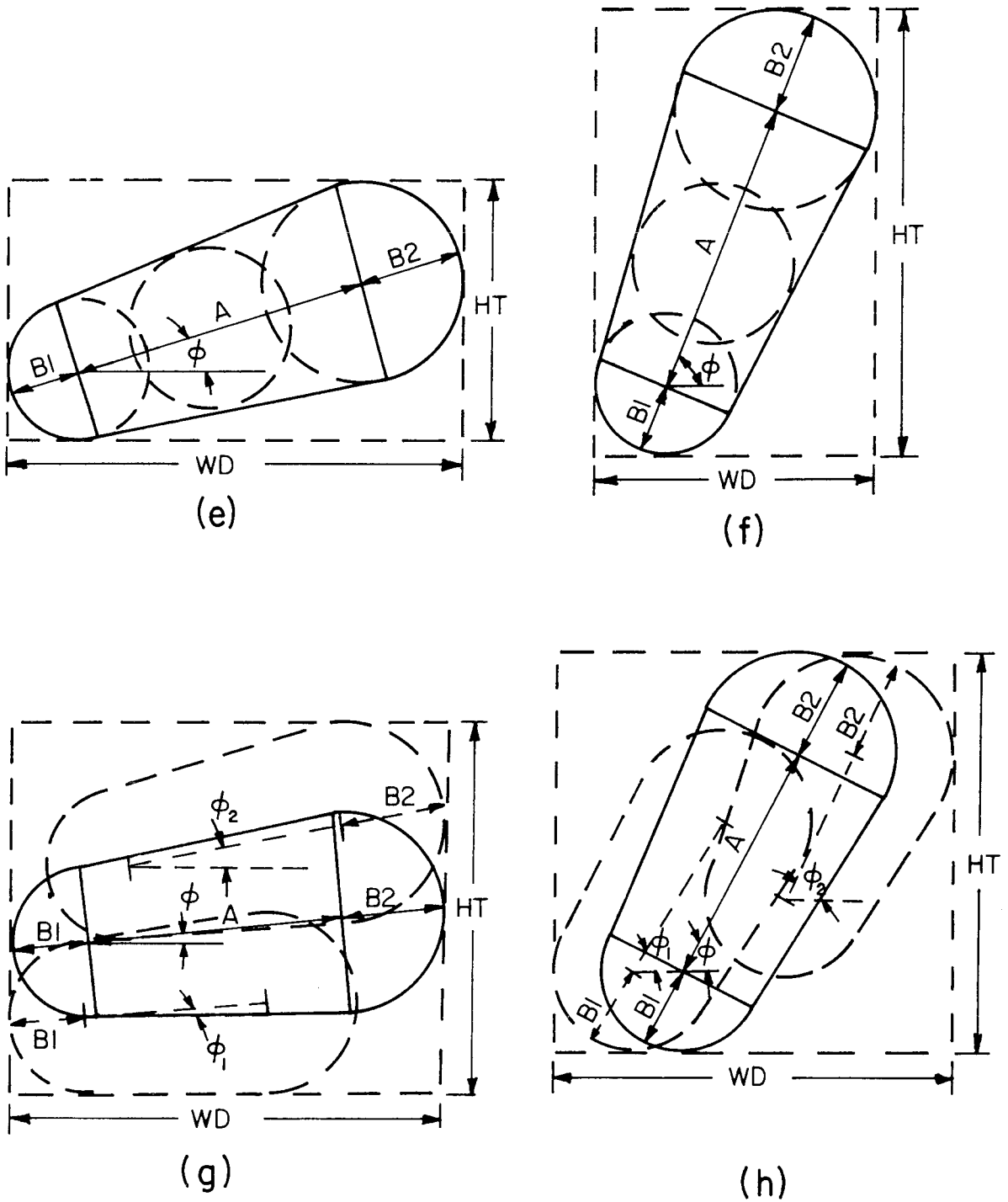


Figure 2.4 Definition Sketch

height (HT), otherwise, it will be called vertical. Both types are illustrated by Figures 2.4(a), (c) and (e); and (b), (d) and (f), respectively. These two categories are not different in substance and the distinction is made primarily for coding convenience in the computer program. B1 and B2 are chosen to be the radii of the left end (or lowest end) and the right end (or highest end) of the horizontal (or vertical) plumes, respectively. The left end of the plume is the end closer to the x-axis. For the cases of merging among individual round plumes as shown by Figure 2.4(a) and (b), ϕ is the angle between the horizontal line and the line connecting the two centers of the merged ending plumes. For the cases of merging between merged plumes, ϕ is the average of angles ϕ_1 and ϕ_2 of the merging plumes 1 and 2, respectively, as shown in Figures 2.4(c) and (d). For the cases of individual round plume 2 joining the merged plume 1 as shown in Figures 2.4(e), (f), (g) and (h), ϕ is assumed to maintain the original value of the merged plume 2 since the resulting merged plume is envisioned to be dominated by the merged plume 2. After B1, B2 and ϕ are determined, A can be calculated by the following equations.

For horizontal plumes:

$$A = (WD-B1-B2)/\cos\phi \quad \text{for } \cos\phi \neq 0$$

$$A = HT-B1-B2 \quad \text{for } \cos\phi = 0$$

For vertical plumes:

$$A = (HT-B1-B2)/\sin\phi \quad \text{for } \sin\phi \neq 0$$

$$A = WD-B1-B2 \quad \text{for } \sin\phi = 0 \quad (2.37)$$

When the new shape of the merged plume is determined, then the calculation can be performed forward one integration step for the round jets at

the ends and the slot jet (with unit fluxes found by dividing the total fluxes of the slot jet by the finite length A) in the central part. This will result in new values for the radii of the round jets at the ends of the merged plumes, b_{r1} and b_{r2} and the half width and length of the central part slot jet b_s and a . Because of the different entrainment rates for round and slot jets, the calculated plume cross-section determined by b_{r1} , b_{r2} , b_s and a may not be smooth enough to represent a realistic shape. The discontinuities occurring at the junctions of the round and slot jets are demonstrated by the dashed line curve in Figure 2.5. In order to eliminate the discontinuity and to obtain a modified smooth plume cross-section described by $B1$, $B2$, and A , the following set of equations is proposed:

$$0.5\pi (b_{r1}^2 U_{r1} + b_{r2}^2 U_{r2}) + 2b_s a U_s =$$
$$[0.5\pi (B1^2 + B2^2) + A (B1 + B2)] \cdot U \quad (2.38)$$

$$a + b_{r1} + b_{r2} = A + B1 + B2 \quad (2.39)$$

$$B1/B2 = b_{r1}/b_{r2} \quad (2.40)$$

where U_{r1} , U_{r2} , U_s and U are the plume velocities corresponding to the half round jets with radii b_{r1} and b_{r2} , the slot jet with half width b_s , and the overall merged plume defined by $B1$, $B2$ and A , respectively.

Equation (2.38) describes the redistribution of the volume flux from the calculated merged plume to the proposed modified plume. Equation (2.39) maintains the same plume length between the calculated and modified plumes. Equation (2.40) keeps the same ratios of the radii of the two half round plumes between calculated and modified plumes.

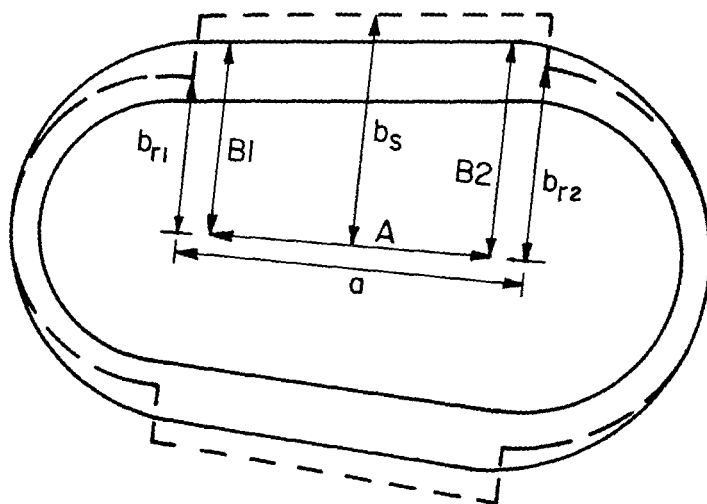


Figure 2.5 Modified Merged Plume Shape

After the modified plume shape is determined, the half width, BY and the half height, BXZ of the merged plume, indicated in Figure 2.3, can be determined by the following equations for the purpose of checking plume merging at the next step:

$$\begin{aligned}
 BY &= 0.5x (A \cdot \cos\phi + B1 + B2) && \text{for } \cos\phi \neq 0 \\
 &= B1 && \text{for } \cos\phi = 0 \text{ and } B1 \geq B2 \\
 &= B2 && \text{for } \cos\phi = 0 \text{ and } B2 > B1 \\
 BXZ &= 0.5x (A \cdot \sin\phi + B1 + B2) && \text{for } \sin\phi \neq 0 \\
 &= B1 && \text{for } \sin\phi = 0 \text{ and } B1 \geq B2 \\
 &= B2 && \text{for } \sin\phi = 0 \text{ and } B2 > B1
 \end{aligned}
 \tag{2.41}$$

Due to the uneven change of B1, B2 and A for each integration step, the y-coordinate of the plume centroid also needs to be readjusted.

The amount of adjustment Δy noted in Figure 2.6 is

$$\begin{aligned}
 \Delta y &= \left[\frac{A_j + B1_j + B2_j}{2} \times \frac{A_{j+1}}{A_j} + B2_{j+1} - \frac{A_{j+1} + B1_{j+1} + B2_{j+1}}{2} \right] \cdot |\cos\phi| \\
 &= 0.5x |\cos\phi| \times \left[(B1_j - B2_j) \times \frac{A_{j+1}}{A_j} + B2_{j+1} - B1_{j+1} \right]
 \end{aligned}$$

where j and j+1 refer to the calculation steps.

With the modified merged plume cross-sectional shape, the entrainment and drag force can be determined and the conservation equations integrated. During the calculation, barring further merging, the length of the slot jet A generally will be reduced and the radii of the two ending round plumes will be increased. Finally, when A diminishes to zero, the shape of the merged plume cross-section becomes practically

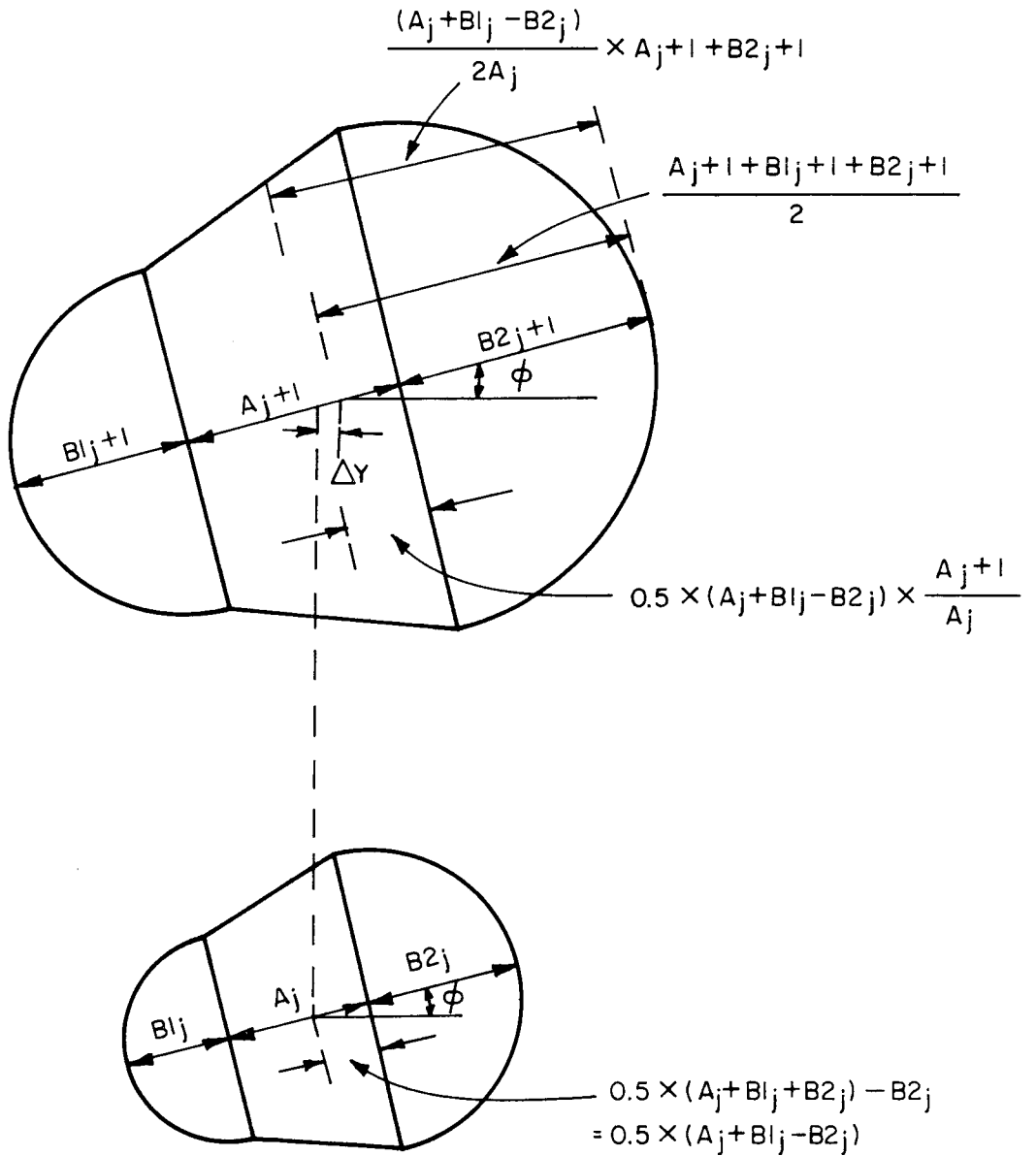


Figure 2.6 Correction of Δy for the Merged Plume

round. At that point, a round plume is again adopted to carry through the final stage of plume calculation.

CHAPTER 3

COMPUTER PROGRAM

The governing equations for predicting the dynamic behavior of multiple cooling tower plumes were presented in Chapter 2. No analytical solution can be obtained due to their complexity as well as the arbitrary ambient conditions in the governing equations. Therefore, a computer program written in Fortran IV language was developed to solve these equations. A standard fourth order Runge-Kutta method was employed in the solution. The inputs to the program include tower exit conditions, ambient conditions, tower configuration, entrainment and drag coefficients, and some control parameters. The basic routine of the computer program begins with inputting data, setting initial conditions (subroutine SETIC) and calculating the first plume (from the tower with the smallest value of x) by setting an indicator $IND(I) = 1$ for i^{th} individual round plume (subroutines RUNGS and DERIVR). As the calculation continues, the subroutines CHKNWP, ALIGN and PLMERG are called to check for the appearance of any new plumes, to align the existing plumes at approximately the same x -coordinate, and to check for the merging among the existing plumes, respectively, along the direction of the plume trajectory. If new plumes appear (whenever x exceeds the x -location of downstream tower exits), the results for such new plumes are calculated stepwise until the stage is reached to necessitate the checking of the merging criterion. If the plumes merge, the indicator of the i^{th} and the j^{th} plumes are changed to $IND(I) = 2$ and $IND(J) = 0$ ($J > I$). In the subroutine RESETI, the fluxes of the merged plumes are added together, and the initial conditions for the merged plumes are

reset. The subroutines DERIVR and DERIVS are called to calculate the plume half widths and velocities of the round and slot jets in order to determine the shape of the modified merged plume. Then, subroutine DERIVE is used to calculate the dynamic properties of the modified merged plume. The calculation stops when the integration step number is equal to the desired (input) step number. The outputs include the input information, and the calculated plume properties such as temperature, excess temperature, moisture, excess moisture, half width and trajectory at visible, merging and final stages of the plumes. The detailed listings and examples of the input and output are presented in Appendix A. The general structure of the computer program is described by the flow chart shown in Figure 3.1. Some important variables in the text and program are compiled and listed in Appendix B. The complete computer program is presented in Appendix C.

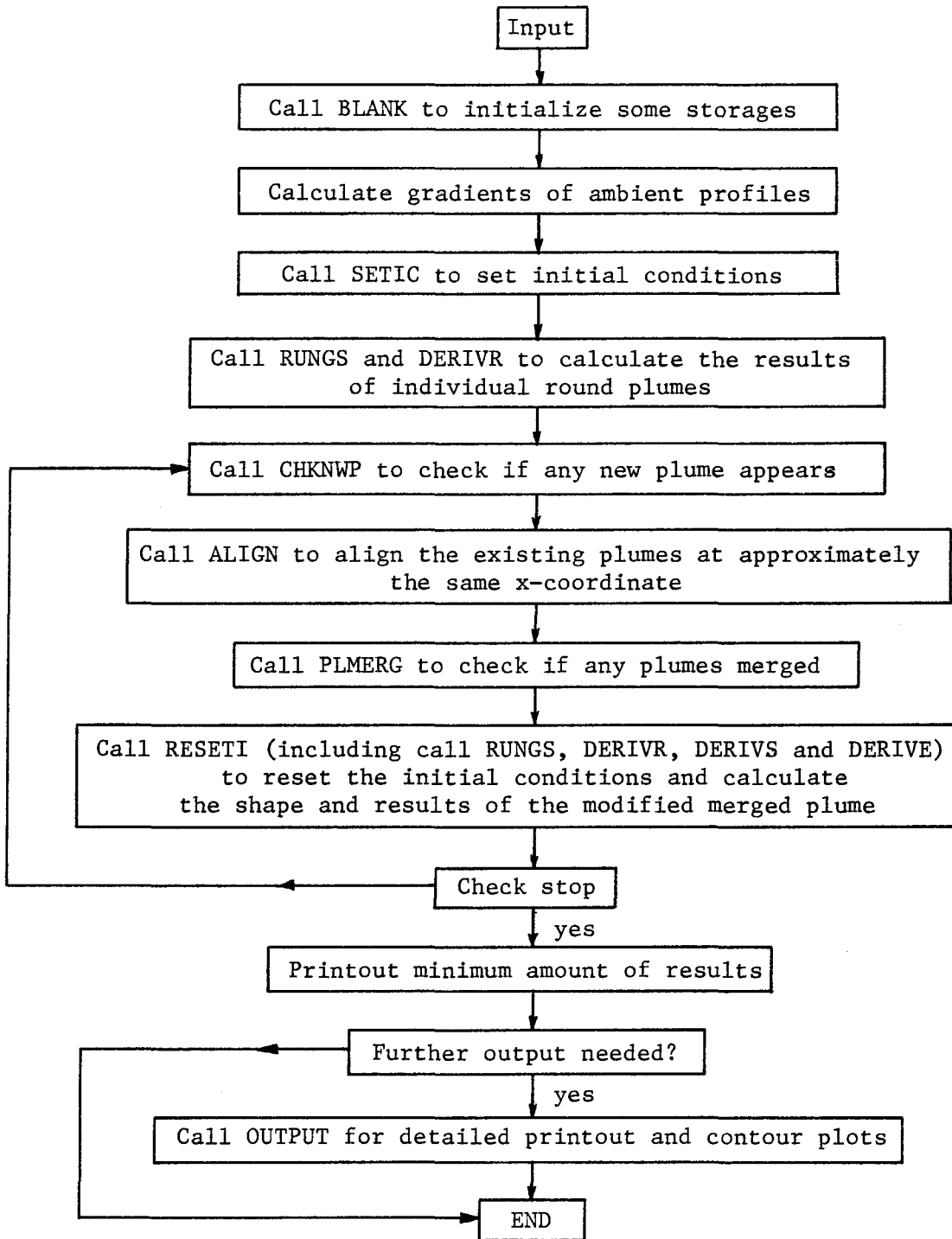


Figure 3.1 Flow Chart of the Computer Program

CHAPTER 4

RESULTS, COMPARISONS AND DISCUSSIONS

In this chapter, four example cases are presented. The results of the present theory are also compared with the laboratory results of Fan (1967), Chan et al. (1974), and field data from TVA (Carpenter et al., 1968).

In the example runs, a line array of four cooling towers and a round array of five cooling towers are considered. For the cases with the line array, three wind directions (i.e. 0° , 90° , and 135° with respect to the tower array) are chosen. The input data cards are shown in Table 4.1, which include the number of towers, the desired number of calculation steps, control parameters, tower configuration, ambient levels, temperature profile, humidity profile, wind velocity profile, tower exit conditions, coefficients of contour plots and heading of plots. Normally, the outputs consist only of the input information, the results at the merging points, and those at the beginning and ending points of the visible phases of plumes. However, detailed printouts and/or contour plots can also be provided by the program upon request. The contour plots of excess temperature, humidity and liquid phase moisture for these examples are shown in Figures 4.1 through 4.12. The plots represent the distribution of the highest values projected onto the X-Z plane. Detailed explanations of the input and output parameters are presented in Appendix A.

Three sets of data from Fan (1967) for a single jet, one set from Chan et al. (1974) for six towers and two sets from Carpenter et al. (1968) for a single tower and multiple towers are chosen for comparison with the model.

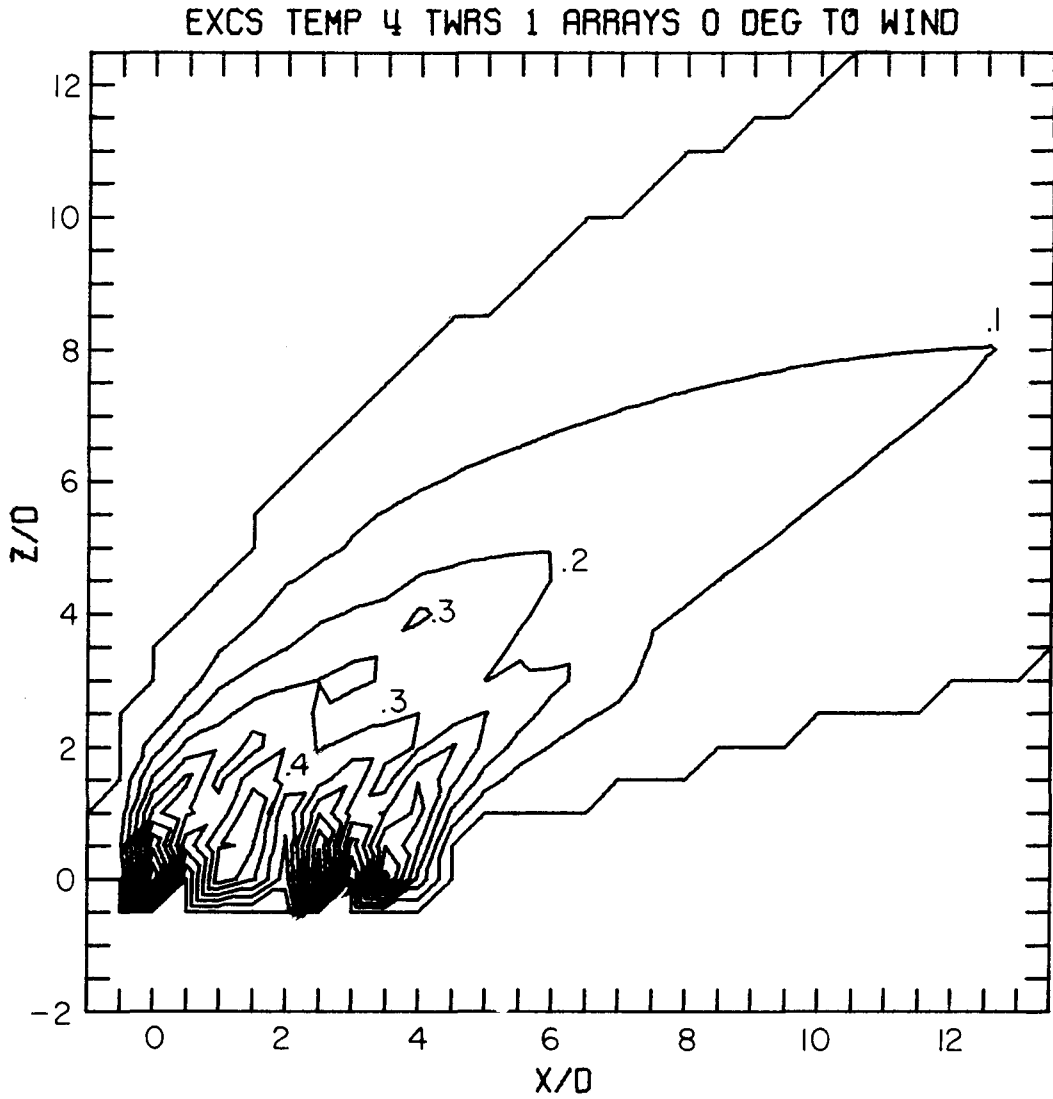


Figure 4.1 Excess Temperature Distribution for the Case of 4 Towers in Linear Array and 0° to Wind Direction

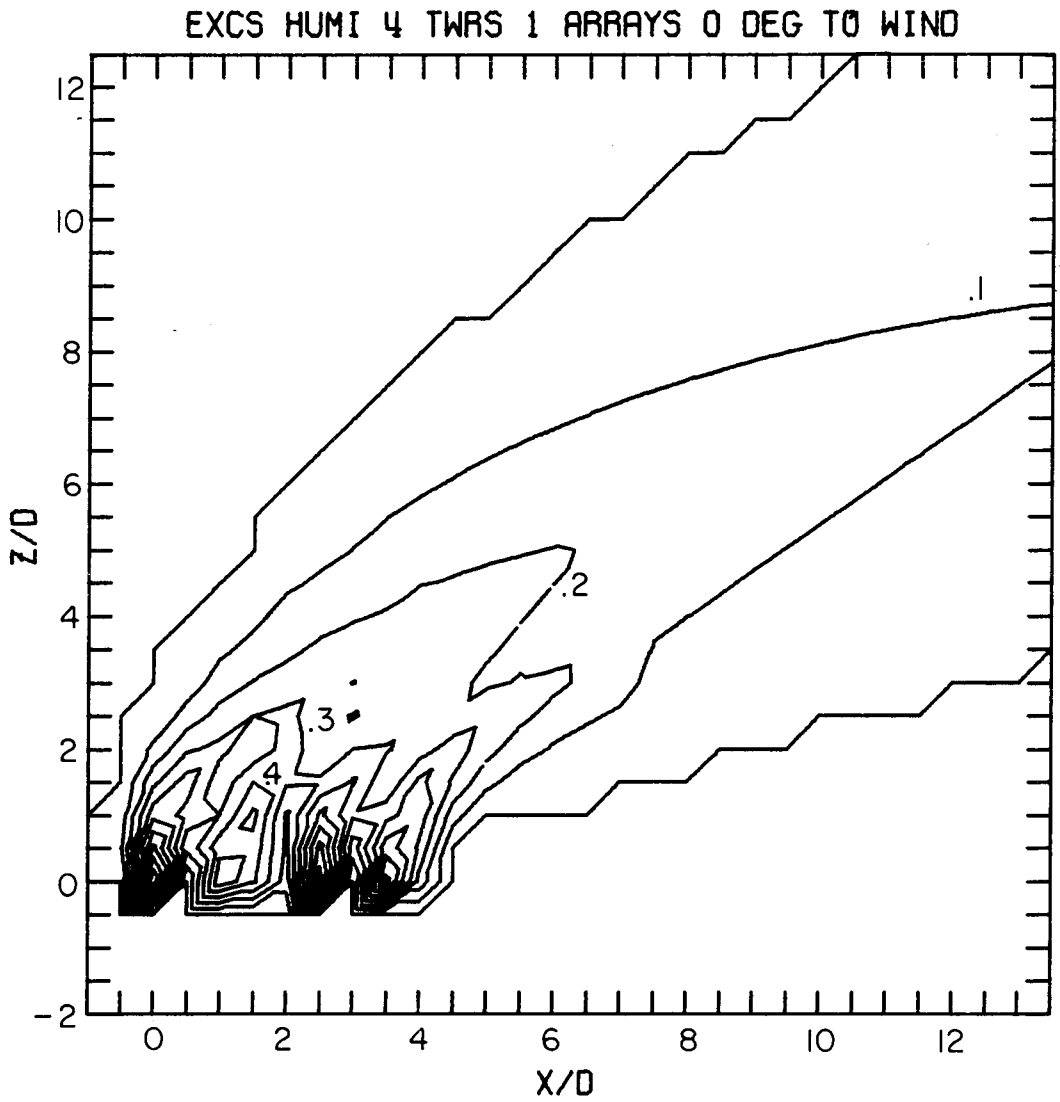


Figure 4.2 Excess Humidity Distribution for the Case of 4 Towers in Linear Array and 0° to Wind Direction

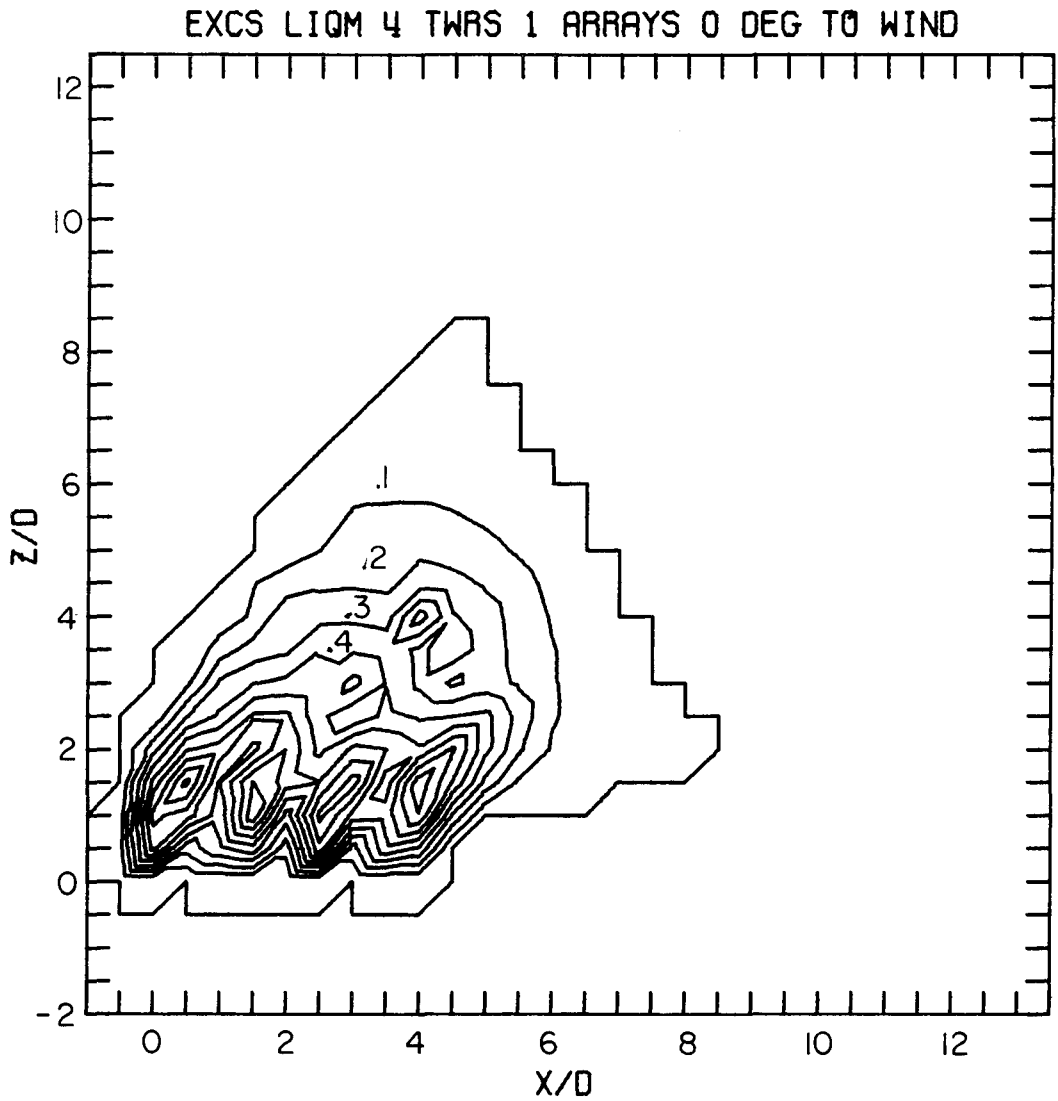


Figure 4.3 Excess Liquid Phase Moisture Distribution for the Case of 4 Towers in Linear Array and 0° to Wind Direction

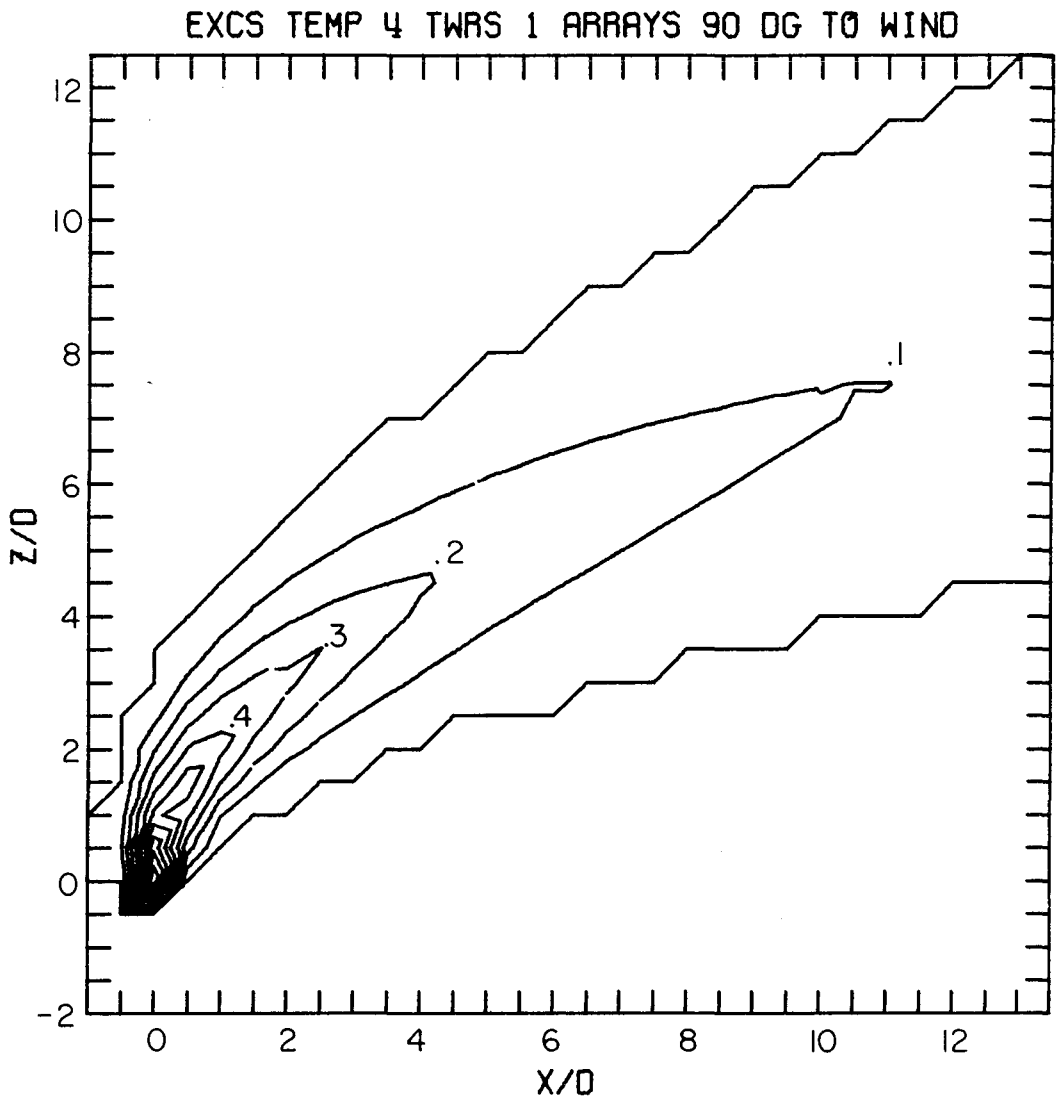


Figure 4.4 Excess Temperature Distribution for the Case of 4 Towers in Linear Array and 90° to Wind Direction

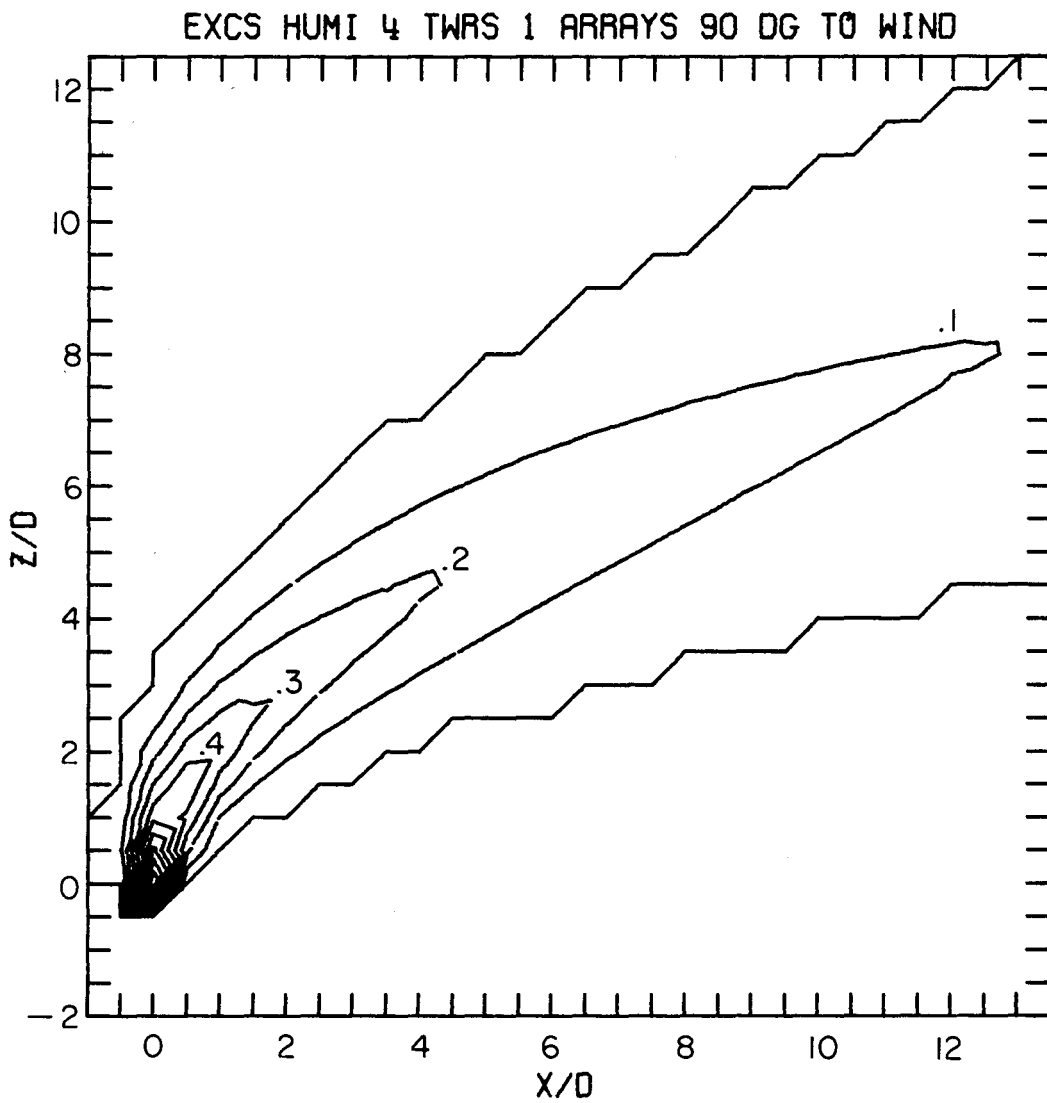


Figure 4.5 Excess Humidity Distribution for the Case of 4 Towers in Linear Array and 90° to Wind Direction

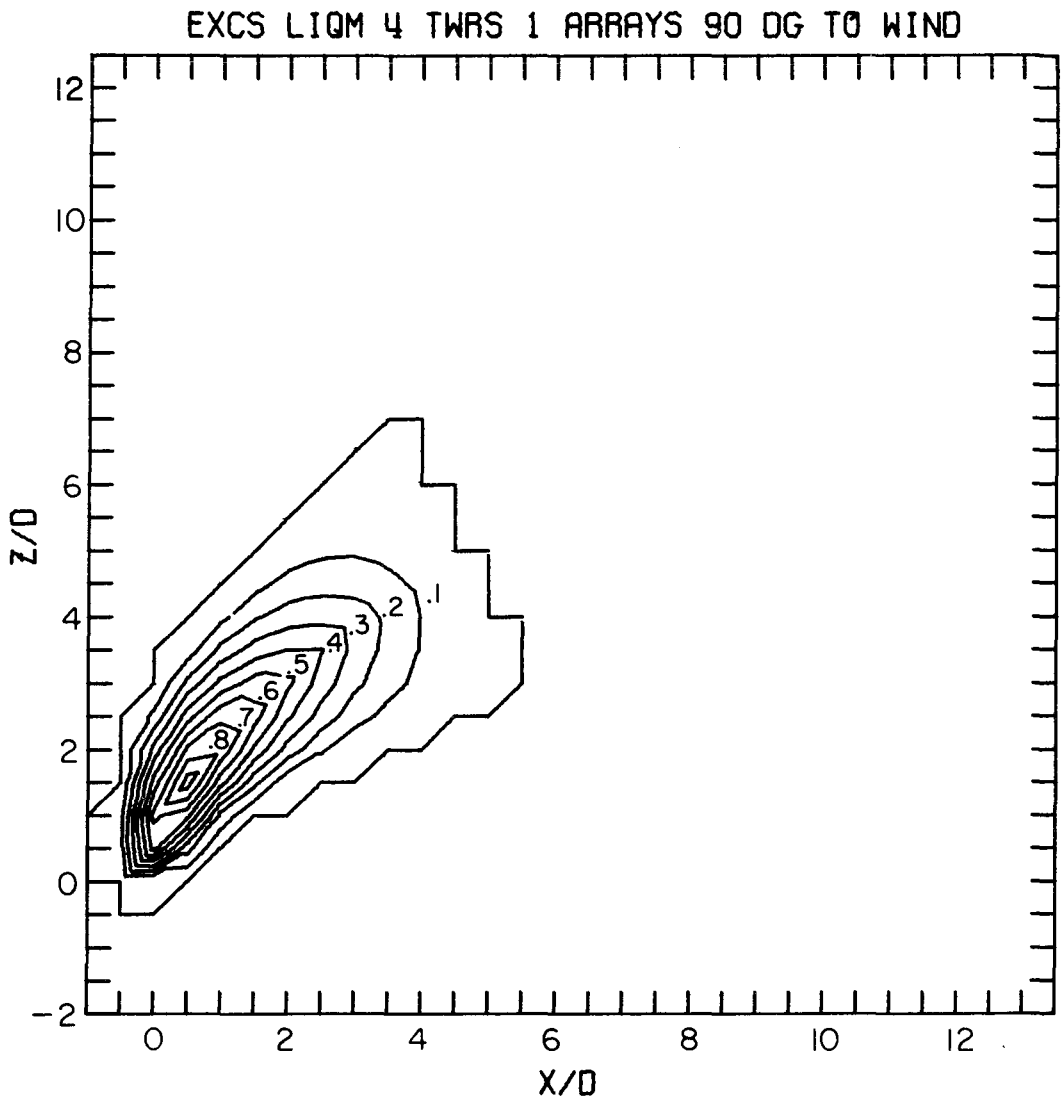


Figure 4.6 Excess Liquid Phase Moisture Distribution for the Case of 4 Towers in Linear Array and 90° to Wind Direction

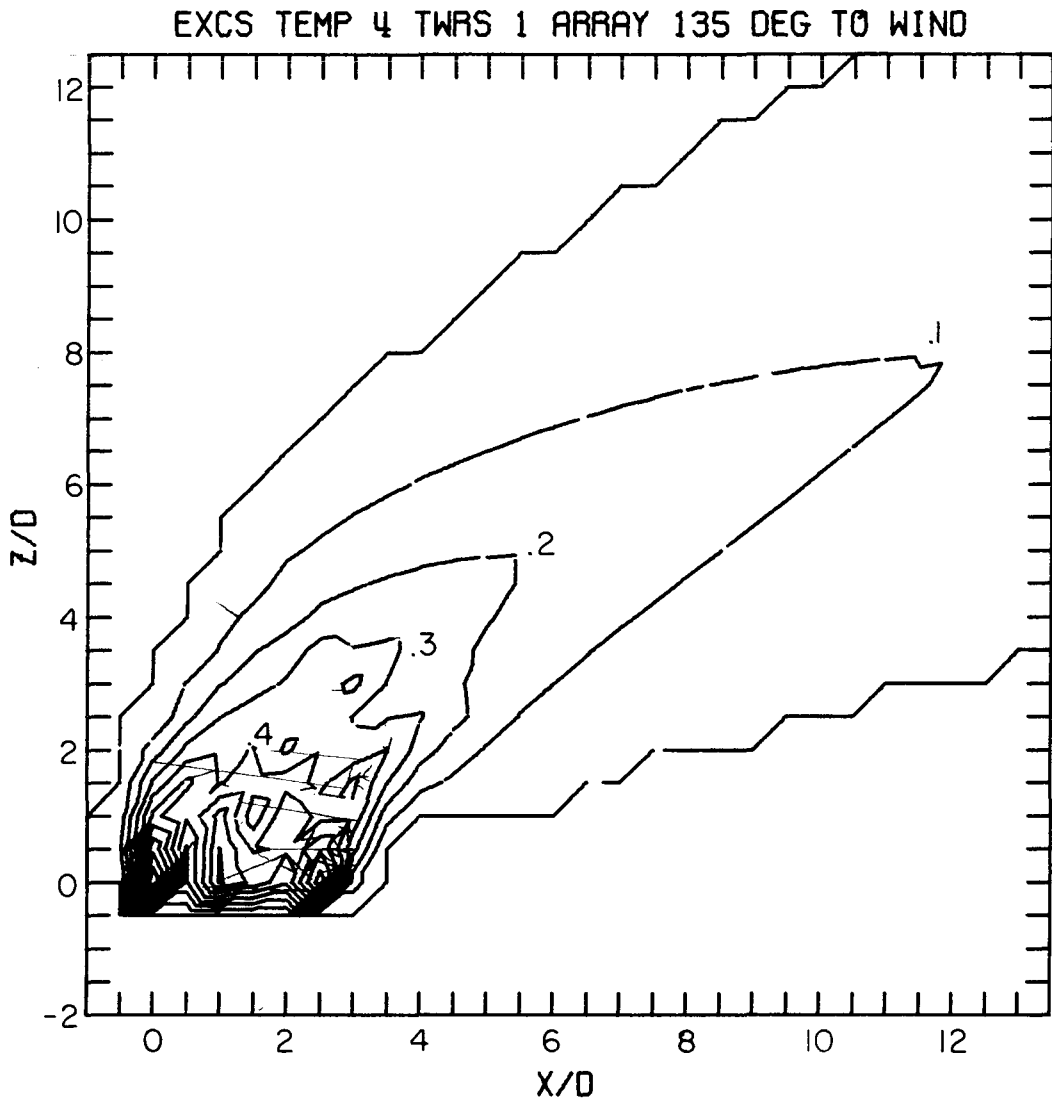


Figure 4.7 Excess Temperature Distribution for the Case of 4 Towers in Linear Array and 135° to Wind Direction

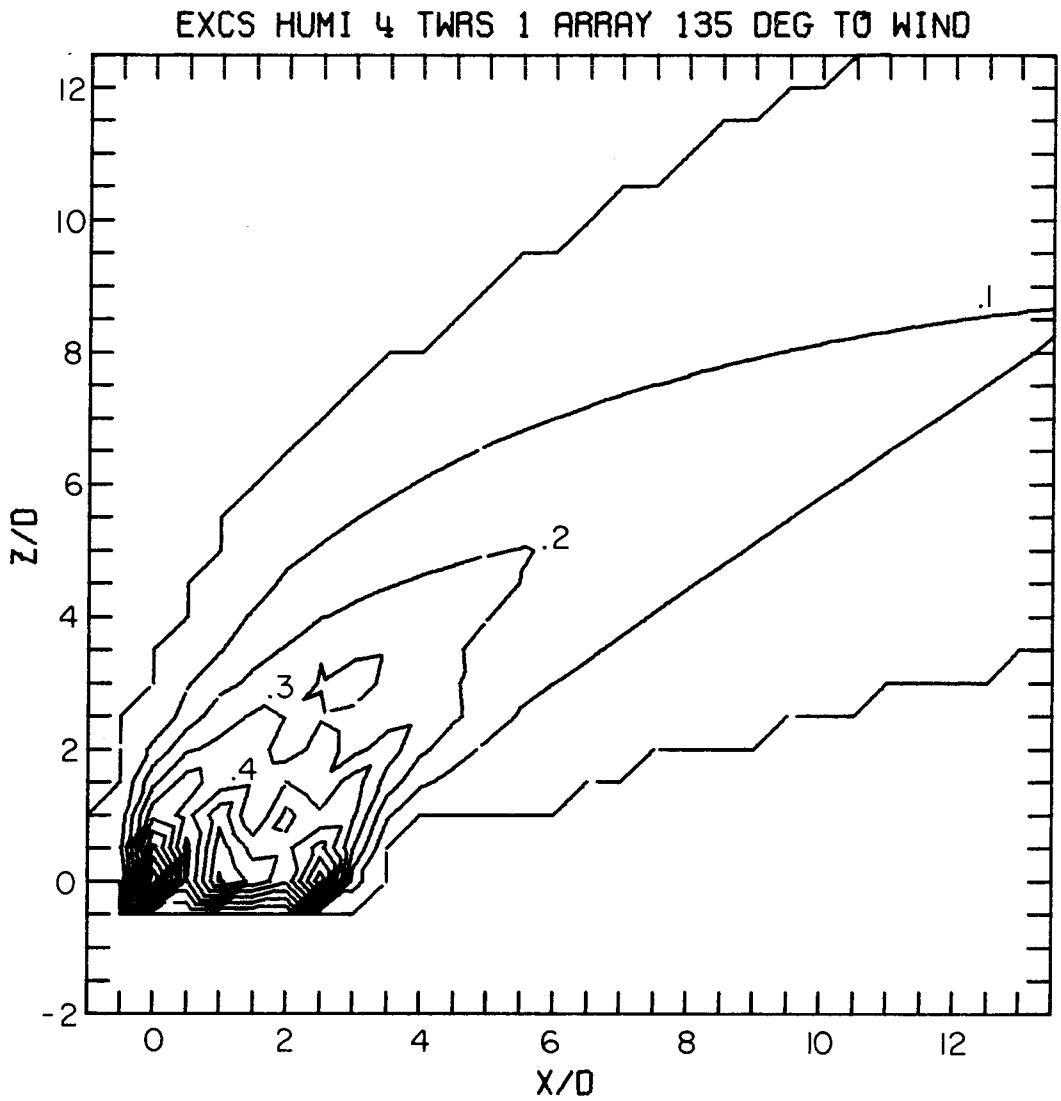


Figure 4.8 Excess Humidity Distribution for the Case of 4 Towers in Linear Array and 135° to Wind Direction

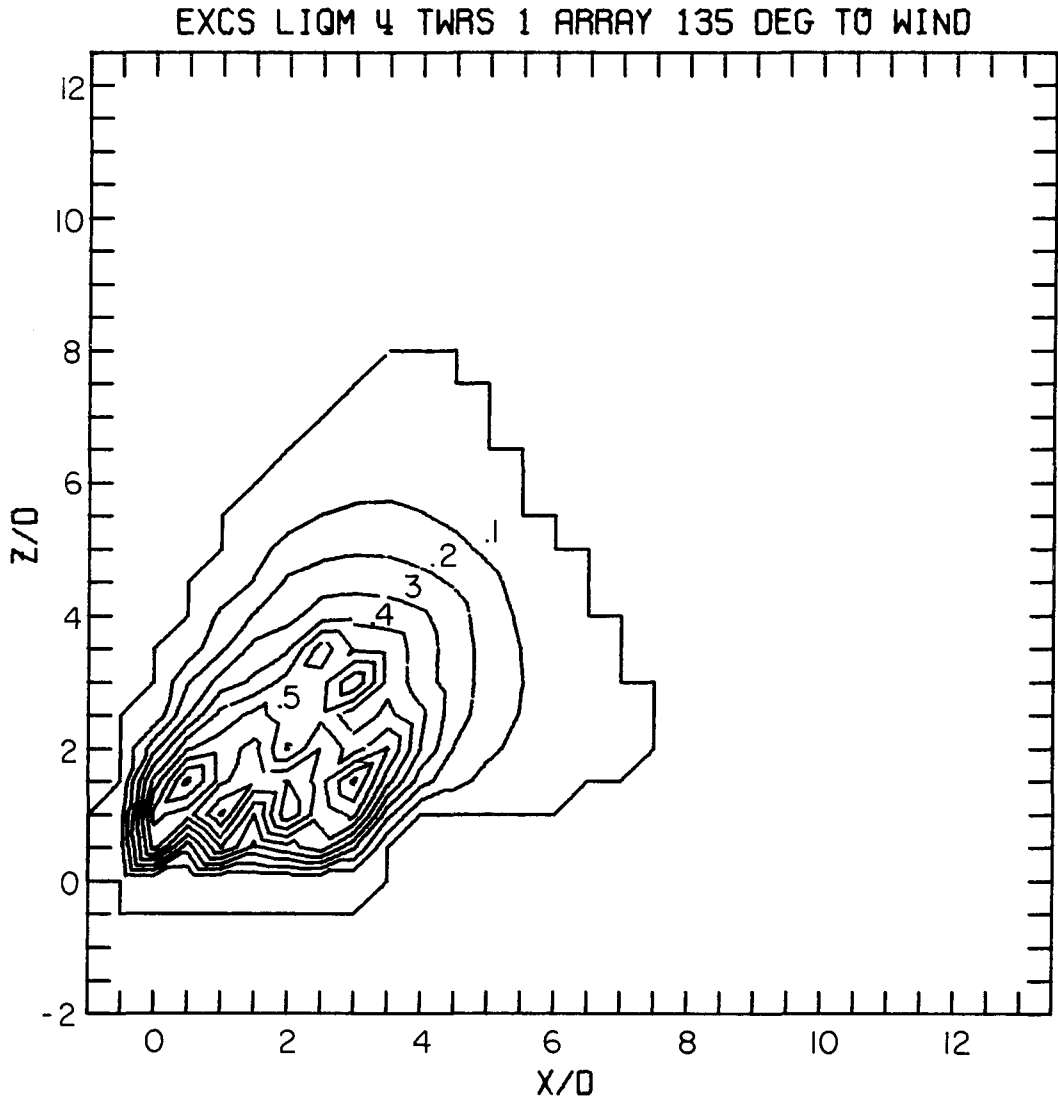


Figure 4.9 Excess Liquid Phase Moisture Distribution for the Case of 4 Towers in Linear Array and 135° to Wind Direction

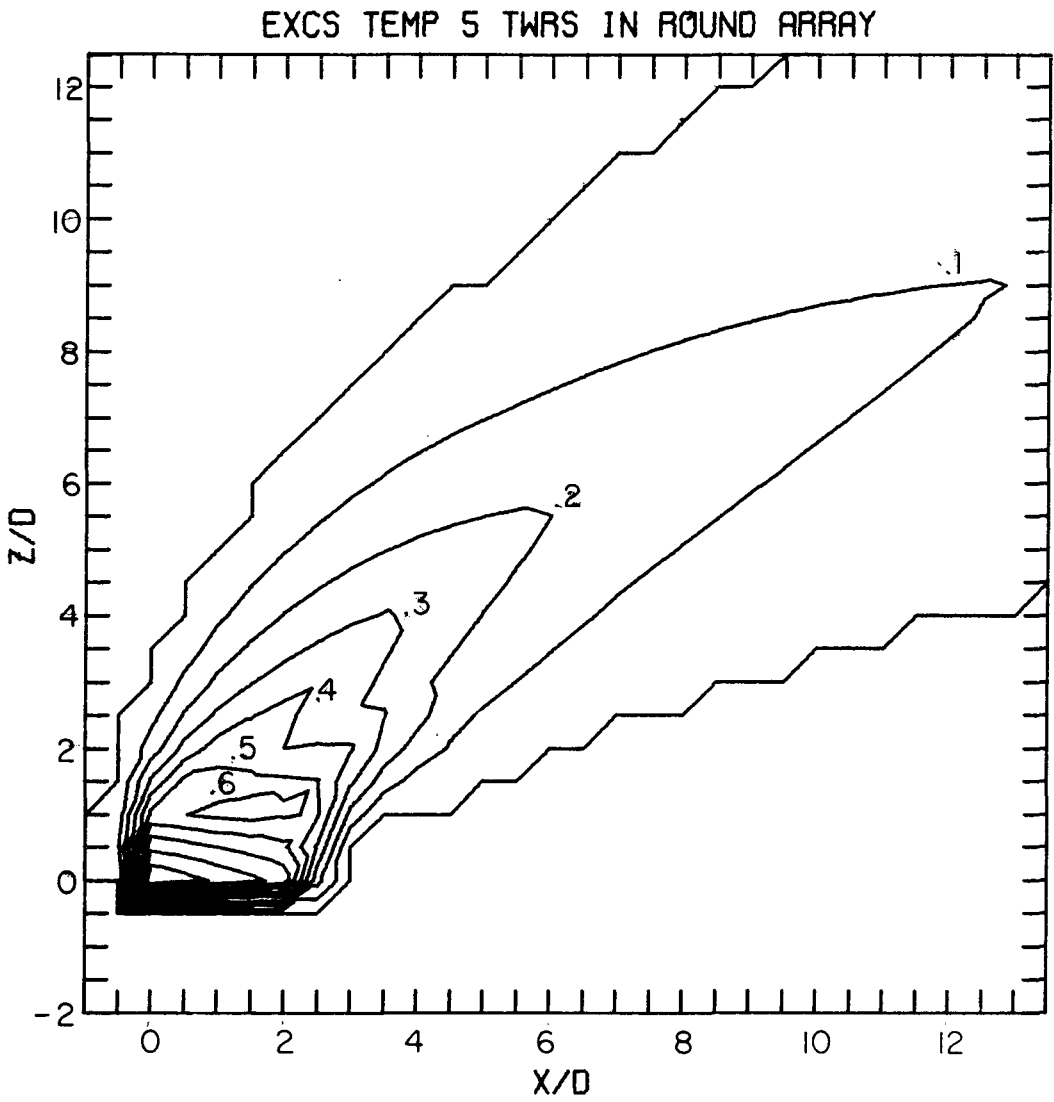


Figure 4.10 Excess Temperature Distribution for the Case of 5 Towers in Round Array

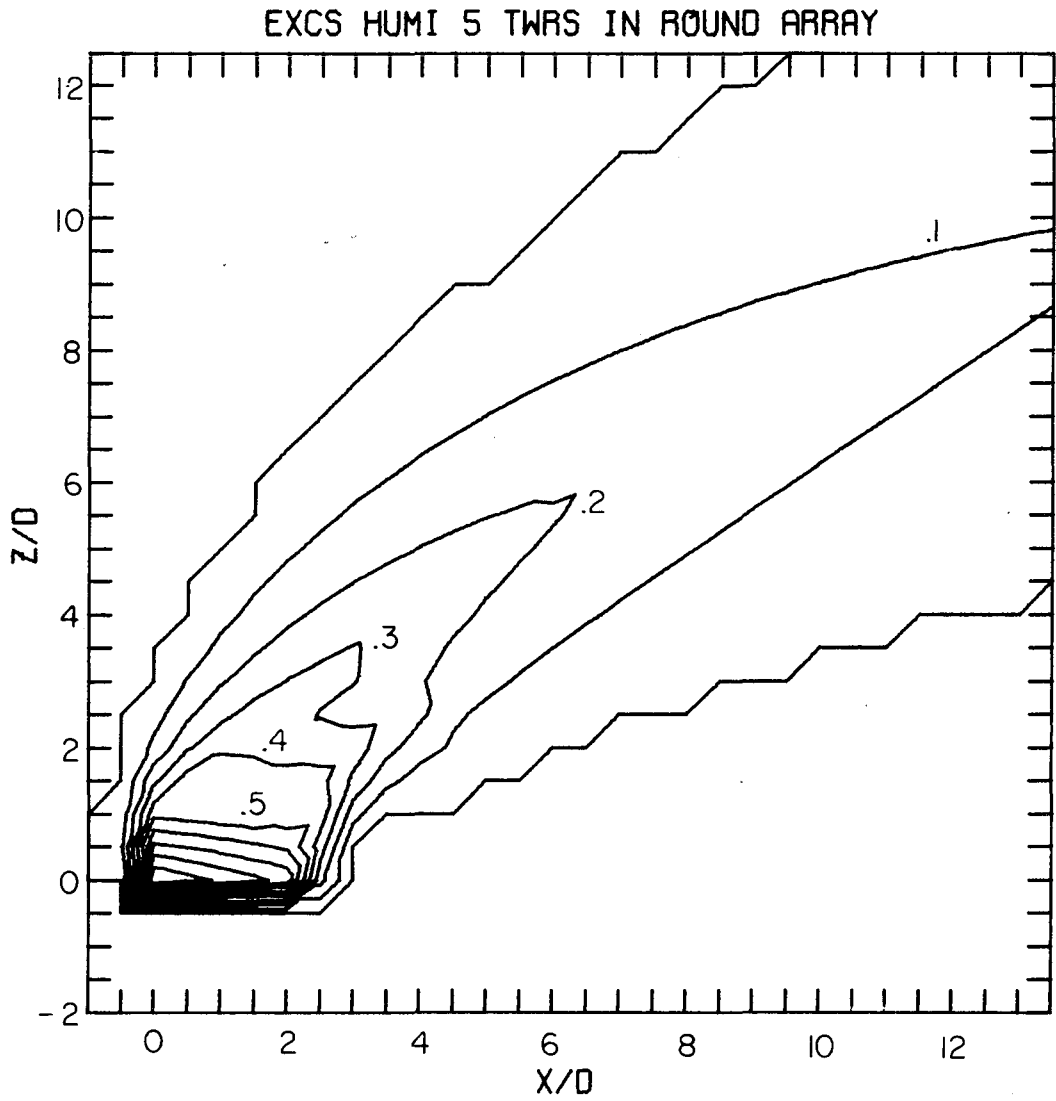


Figure 4.11 Excess Humidity Distribution for the Case of 5 Towers in Round Array

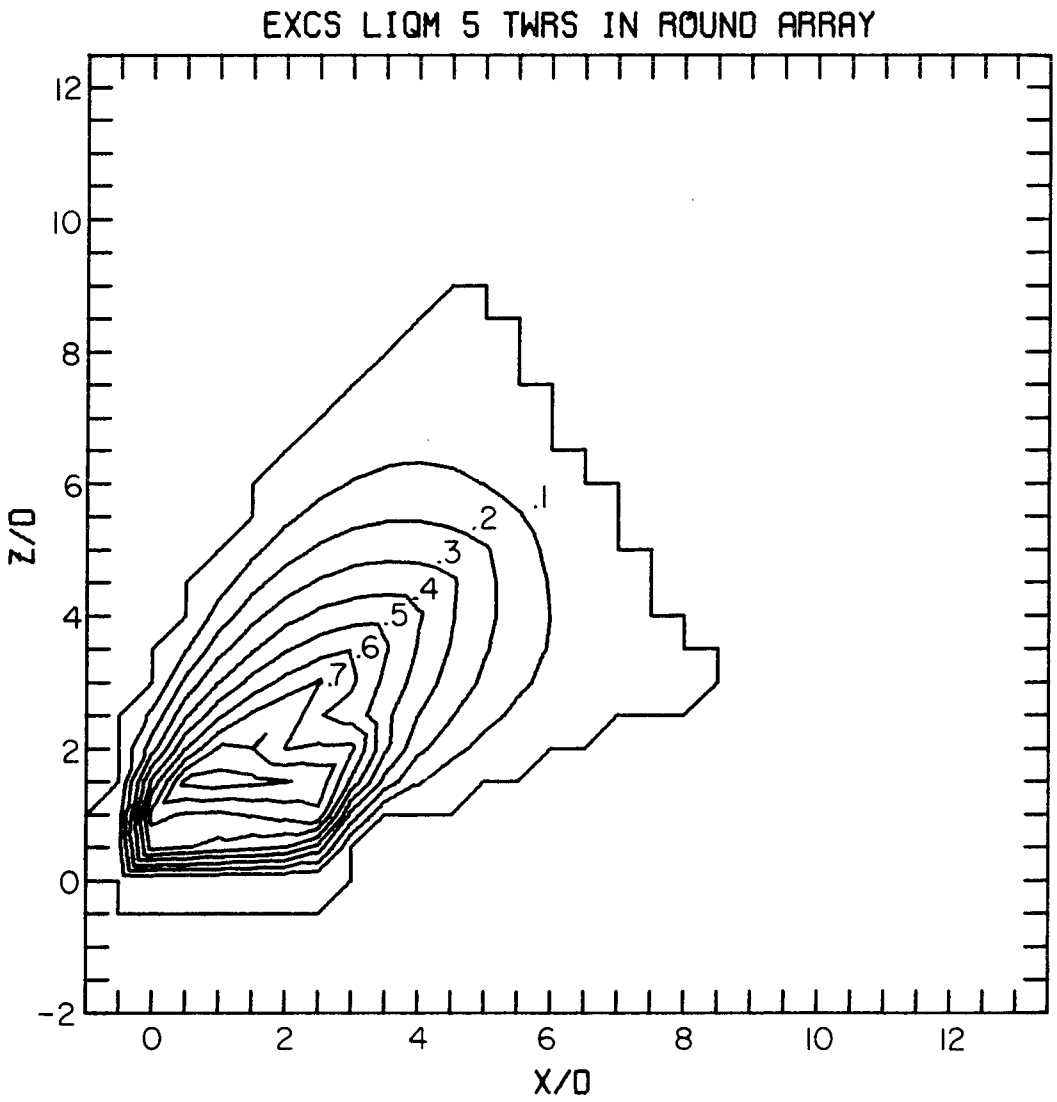
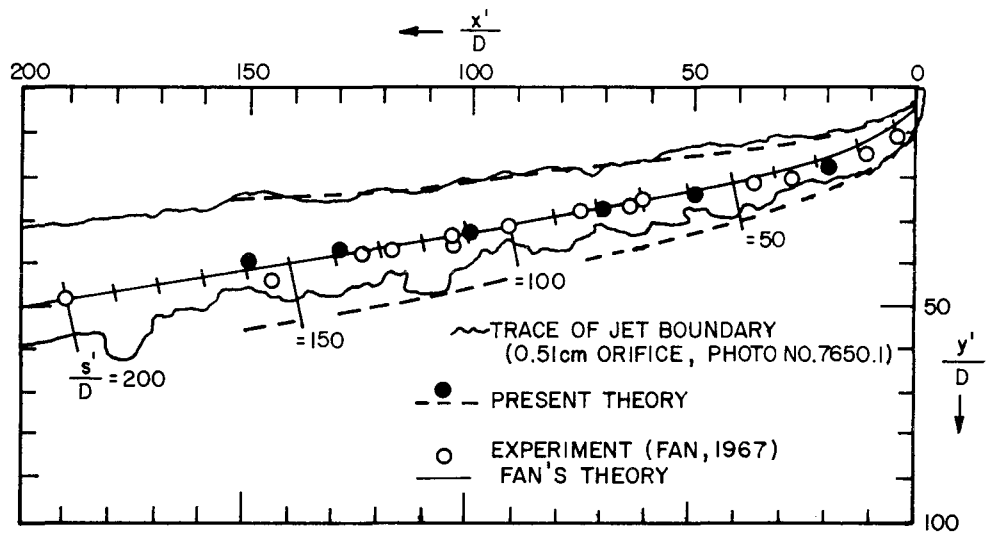


Figure 4.12 Excess Liquid Phase Moisture Distribution for the Case of 5 Towers in Round Array

The input data cards for these cases are shown in Tables 4.2 through 4.5. The ambient conditions for the data from Fan and Chan et al. are uniform. The velocity and temperature at the tower exit and ambient are chosen to satisfy the given values of densimetric Froude number F and velocity ratio K . The predicted results of dilution, plume trajectory and width for Fan's cases are shown in Figures 4.13, 4.14 and 4.15, and are compared with his experimental results. The comparisons are generally good. The predicted excess temperature distribution for the six tower case from Chan et al. is shown in Figure 4.16, together with the experimental results. In this case the six towers are in one line array and the ambient flow to it is normal. The contour plot is for the distribution of values in the central x - z plane. It seems that the present model tends to overpredict the excess temperature. The main reason might be because of the neglect of the effect of the mixing in the plume wake zone in the present model. However it should also be noted that the experimental results of Chan et al. may have been influenced by the blockage of the flow by the model towers due to the finite width of the experimental flume.

The field results from TVA at the Paradise power plant include two cases. One is for a single tower in a stable ambient (TVA-11, potential temperature gradient $\frac{\partial \theta}{\partial z} = 0.59 \text{ } ^\circ\text{k}/100\text{m}$, $0 < \frac{\partial \theta}{\partial z} \leq 1.0 \text{ } ^\circ\text{k}/\text{m}$). The other is for two towers in an ambient with a temperature inversion (TVA-14, $\frac{\partial \theta}{\partial z} = 1.42 \text{ } ^\circ\text{k}/100\text{m} > 1.0 \text{ } ^\circ\text{k}/\text{m}$). Since only the average temperature gradient and average wind velocities at a few levels were available only rough estimates of ambient temperature and wind velocity profiles were constructed based on the limited data.



F=20 k=8 60(d)

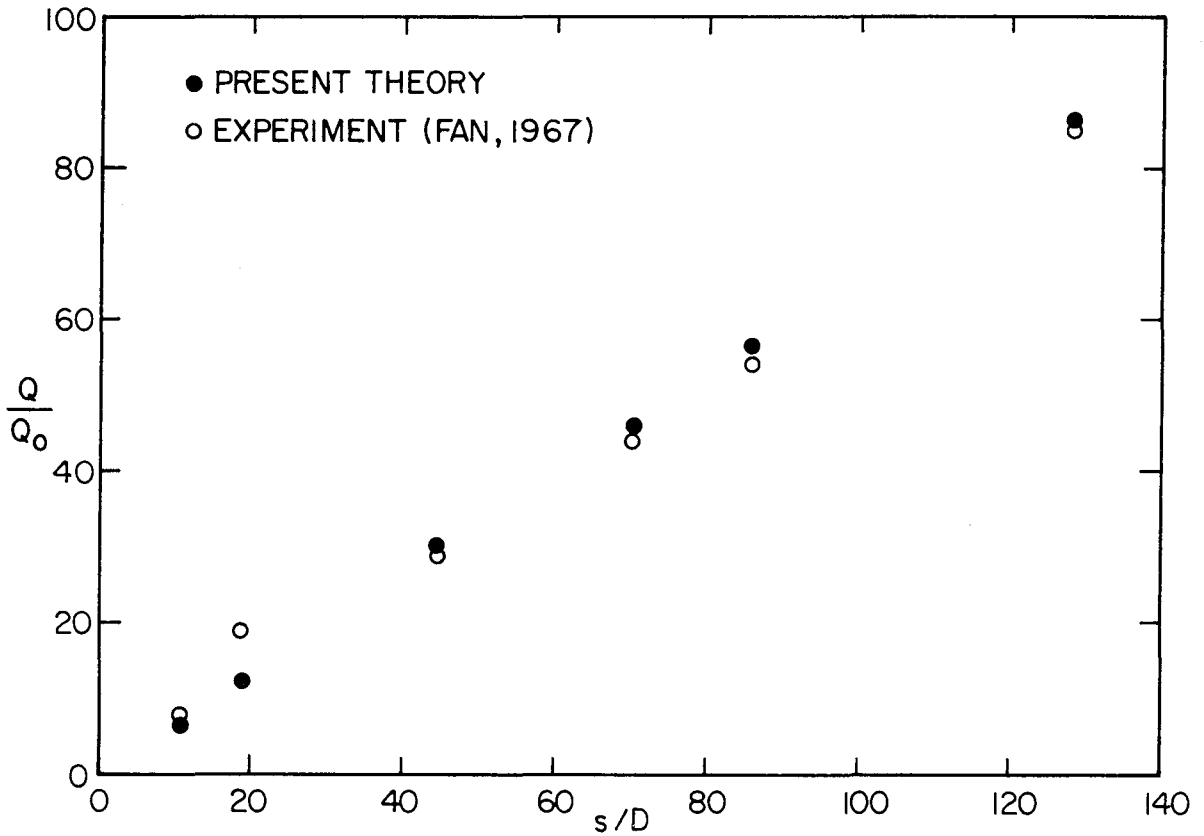
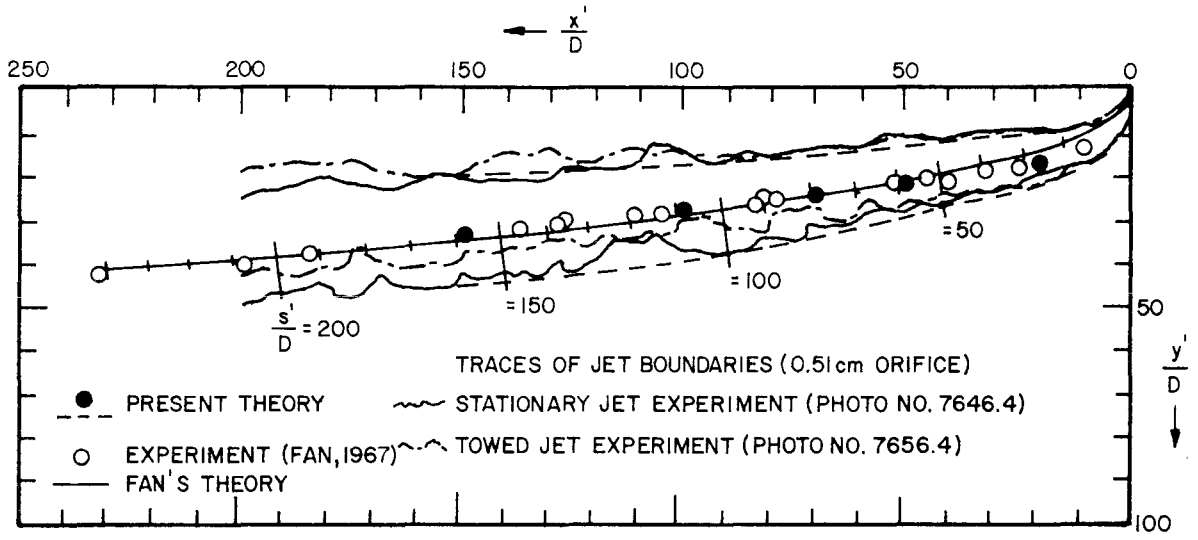


Figure 4.13 Comparisons of Plume Trajectory, Width and Dilution Between the Present Theory and Fan's (1967) Experiments for F = 20 and K = 8



F=40 k=8 60(g)

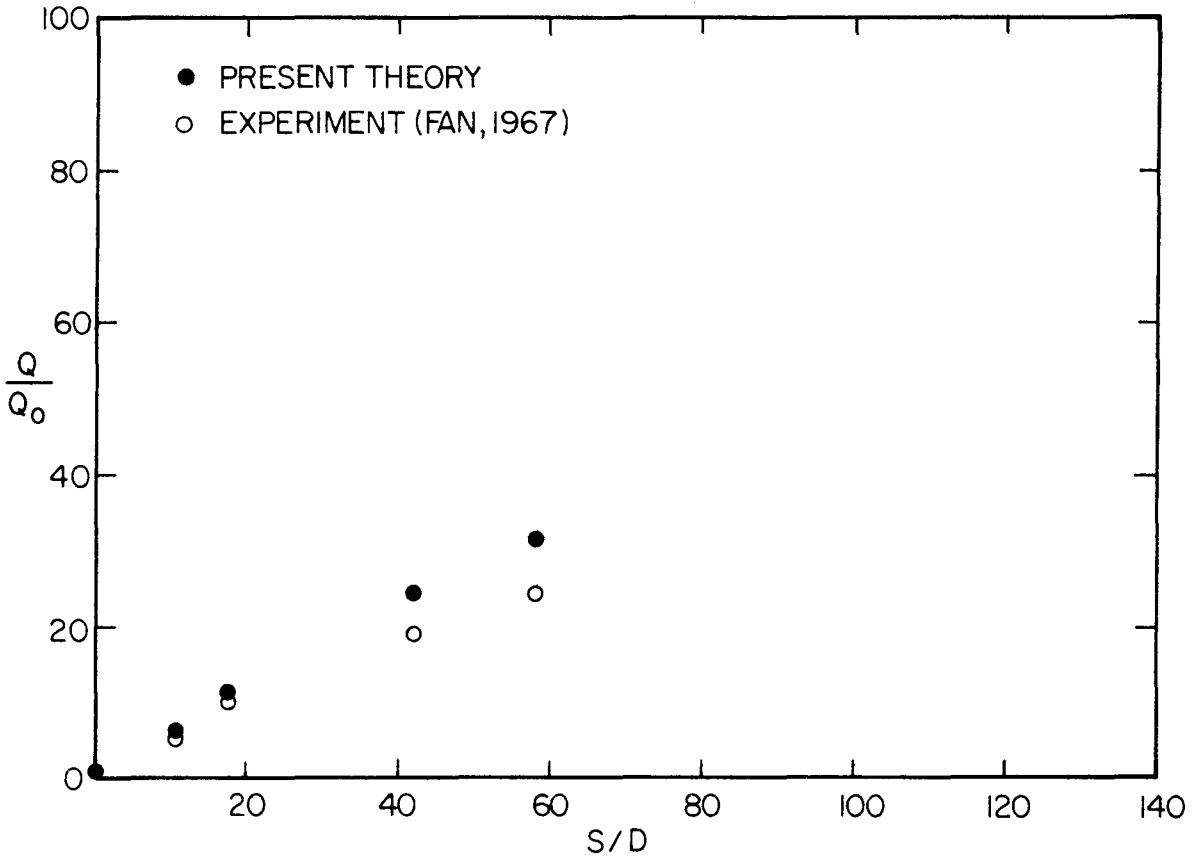


Figure 4.14 Comparisons of Plume Trajectory, Width and Dilution Between the Present Theory and Fan's (1967) Experiments for F = 40 and K = 8

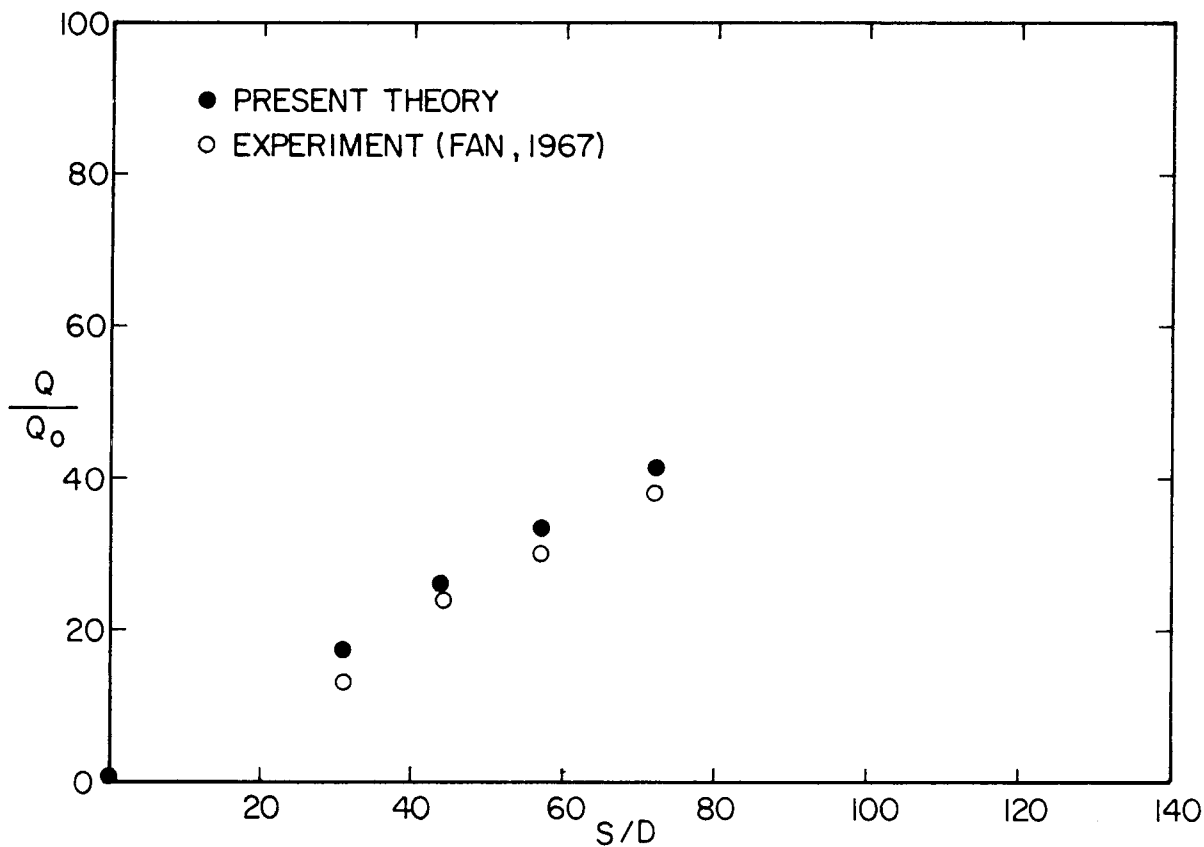
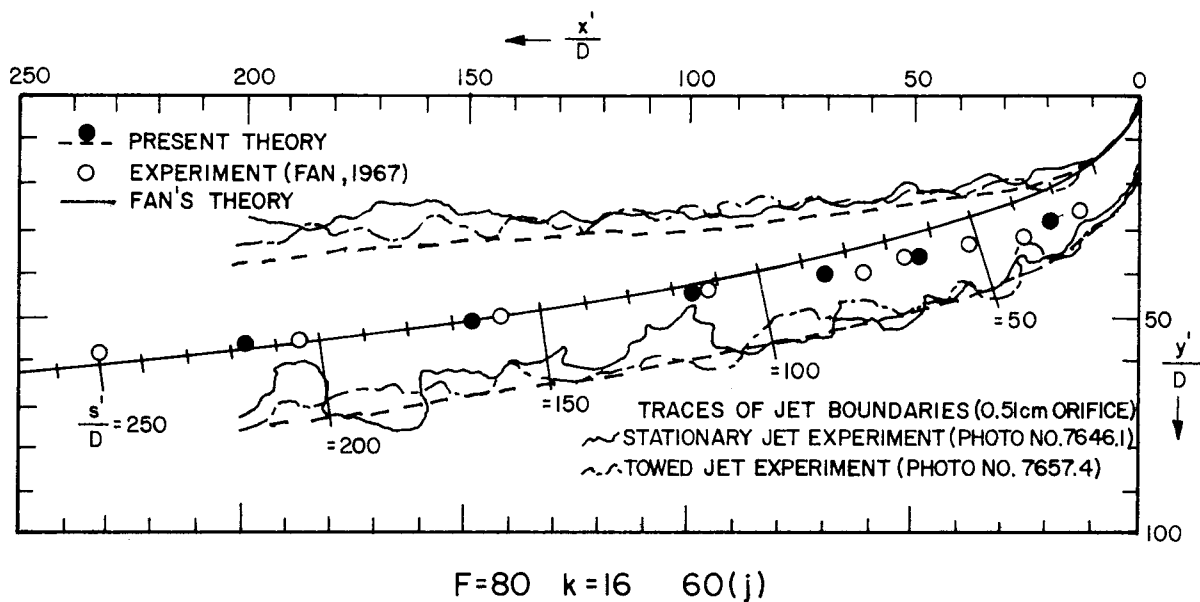


Figure 4.15 Comparisons of Plume Trajectory, Width and Dilution Between the Present Theory and Fan's (1967) Experiments for $F = 80$ and $k = 16$

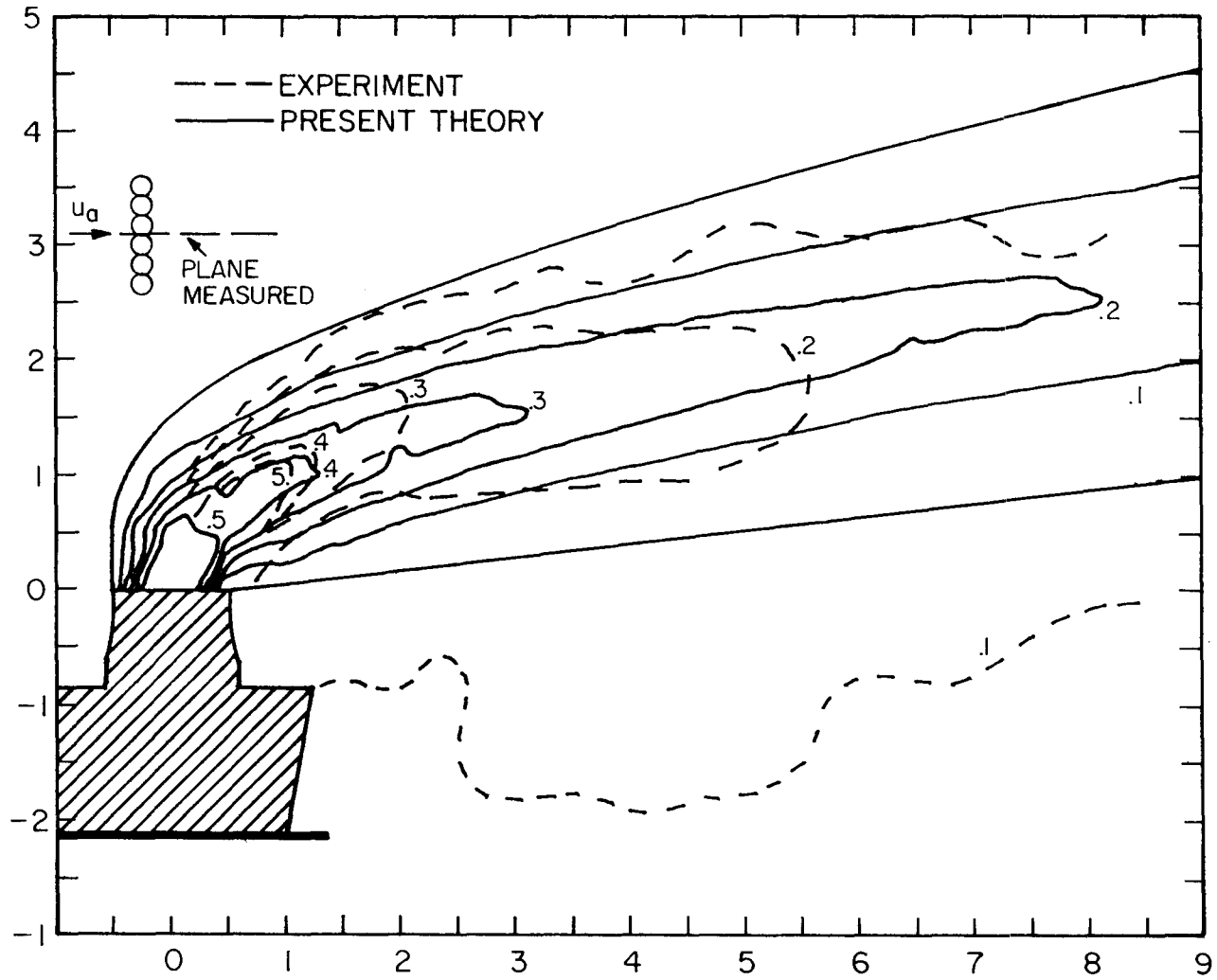


Figure 4.16 Comparisons of Plume Excess Temperature Between the Present Theory and Chan et al.'s (1974) Experiments for $F = 4$ and $K = 1.02$

Three ambient relative humidity profiles (100%, 70%, 0%) associated with the relative temperature profiles were generated and tested. The exit plume humidities were assumed 100% (saturated) except for one dry plume case which is 0% for ambient and exit humidities. The input data cards are presented in Tables 4.4 and 4.5. The predicted results and the comparisons are shown in Figures 4.17 and 4.18. From the variations of plume trajectory for different ambient humidity conditions, the effect of the ambient humidity can be seen to be quite significant. Similar conclusions could be drawn for the effect of ambient temperature and wind velocity. The present model overpredicts the plume trajectories for TVA's cases. This could be due to the incomplete information of the ambient conditions and the neglect of drift in the tower initial conditions. Adequate ambient and source conditions are mandatory for proper model validation.

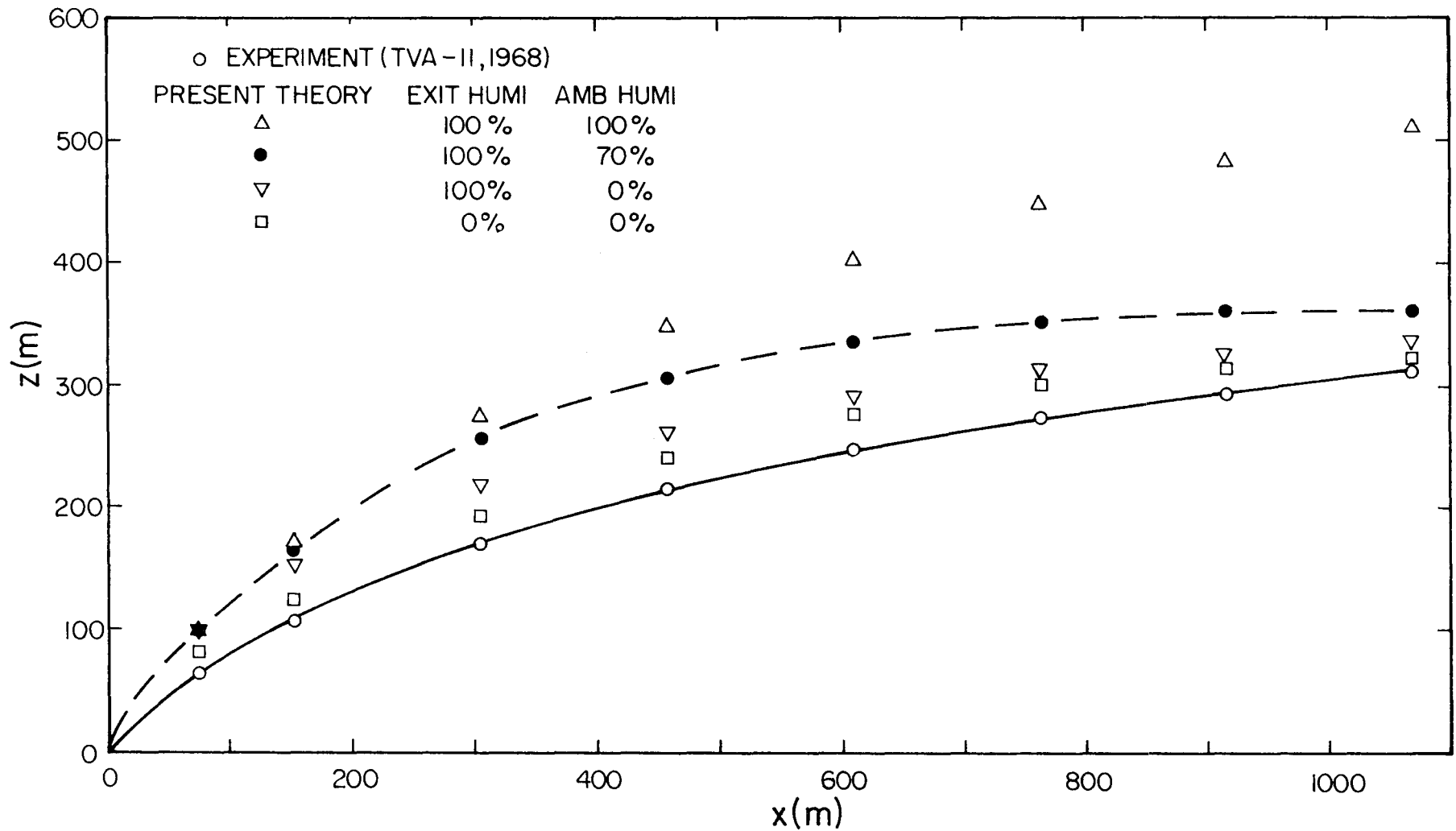


Figure 4.17 Comparisons of Plume Trajectories Between the Present Theory and TVA (1968, TVA-11, single tower) Field Data in a Stable Atmospheric Condition ($\partial\theta/\partial z=0.59^\circ\text{K}/100\text{ m}$)

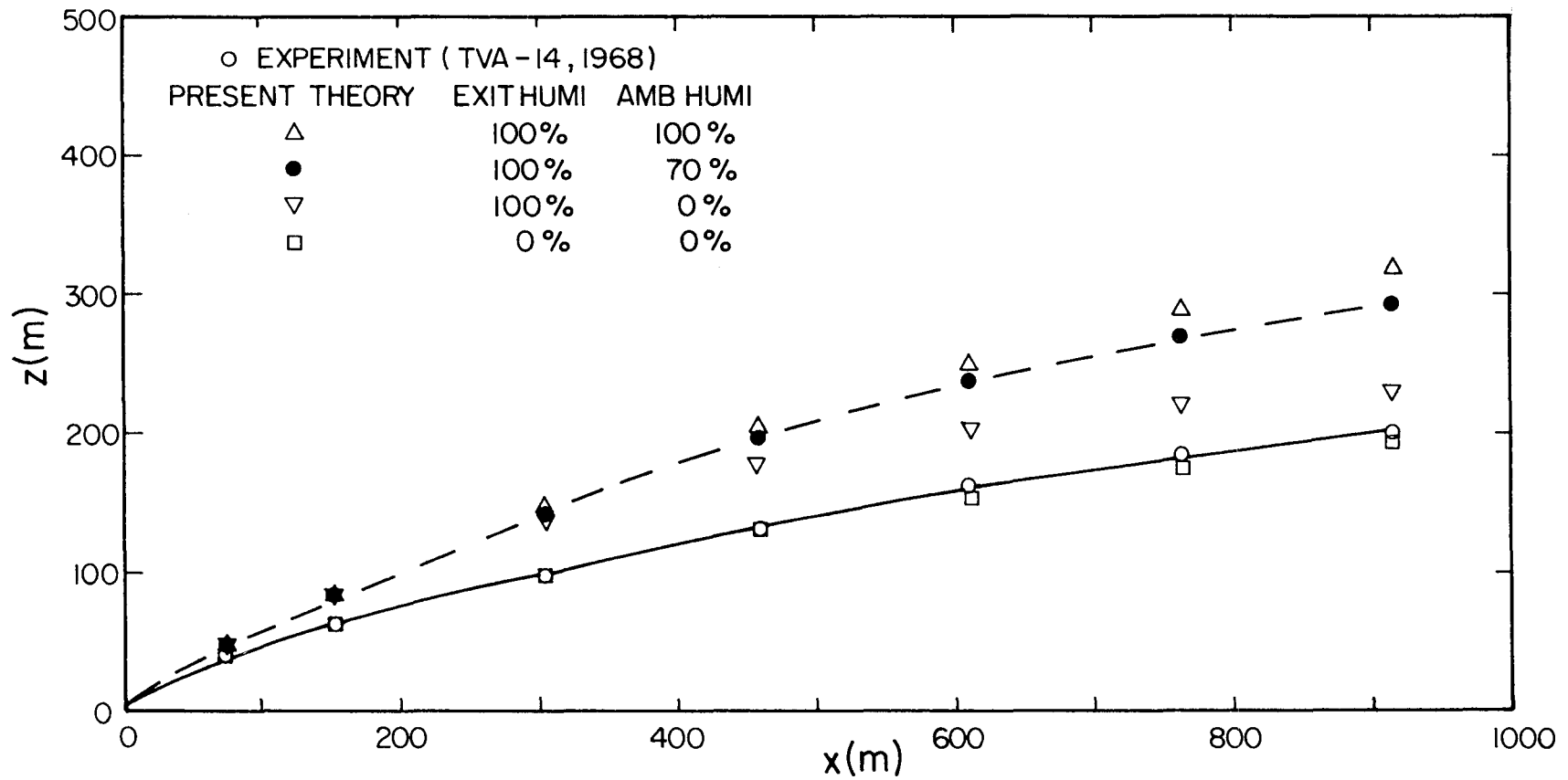


Figure 4.18 Comparisons of Plume Trajectories Between the Present Theory and TVA (1968, TVA, two towers) Field Data in an Atmosphere with an Inversion ($\partial\theta/\partial z=1.42^\circ\text{K}/100\text{ m}$)

Table 4.1 Input Data Cards for Example Cases (Different Wind Directions to a Line Array (3 cases) and Round Array (one case) of Towers)

CASE (1) 4 TOWERS IN ONE ARRAY 0 DEGREES TO WIND										
4	120	30	30	11						
0	0	0	3	10	0	1	1	1	1	1
.00000	11.45000	22.90000	34.35000							
.00000	.00000	.00000	.00000							
.00000	100.00000	200.00000								
10.50000	10.30000	10.10000								
70.00000	70.00000	70.00000								
4.10000	5.22504	5.76969	4.10000	5.22504	5.76969	4.10000	5.22504			
5.76969	4.10000	5.22504	5.76969							
9.44880	10.26800	31.90000	.02821	.00000						
5.00000	5.00000	0	0	0	0					
EXCS TEMP	4	TWRS	1	ARRAYS	0	DEG	TO	WIND	Z/D	X/D
EXCS HUMI	4	TWRS	1	ARRAYS	0	DEG	TO	WIND	Z/D	X/D
EXCS LIQM	4	TWRS	1	ARRAYS	0	DEG	TO	WIND	Z/D	X/D
CASE (2) 4 TOWERS IN ONE ARRAY 90 DEGREES TO WIND										
4	120	30	30	11						
0	0	0	3	10	0	1	1	1	1	1
.00000	.00000	.00000	.00000							
.00000	11.45000	22.90000	34.35000							
.00000	100.00000	200.00000								
10.50000	10.30000	10.10000								
70.00000	70.00000	70.00000								
4.10000	5.22504	5.76969	4.10000	5.22504	5.76969	4.10000	5.22504			
5.76969	4.10000	5.22504	5.76969							
9.44880	10.26800	31.90000	.02821	.00000						
5.00000	5.00000	0	0	0	0					
EXCS TEMP	4	TWRS	1	ARRAYS	90	DEG	TO	WIND	Z/D	X/D
EXCS HUMI	4	TWRS	1	ARRAYS	90	DEG	TO	WIND	Z/D	X/D
EXCS LIQM	4	TWRS	1	ARRAYS	90	DEG	TO	WIND	Z/D	X/D
CASE (3) 4 TOWERS IN ONE ARRAY 135 DEGREES TO WIND										
4	120	30	30	11						
0	0	0	3	10	0	1	1	1	1	1
.00000	8.10000	16.19000	24.29000							
.00000	8.10000	16.19000	24.29000							
.00000	100.00000	200.00000								
10.50000	10.30000	10.10000								
70.00000	70.00000	70.00000								
4.10000	5.22504	5.76969	4.10000	5.22504	5.76969	4.10000	5.22504			
5.76969	4.10000	5.22504	5.76969							
9.44880	10.26800	31.90000	.02821	.00000						
5.00000	5.00000	0	0	0	0					
EXCS TEMP	4	TWRS	1	ARRAY	135	DEG	TO	WIND	Z/D	X/D
EXCS HUMI	4	TWRS	1	ARRAY	135	DEG	TO	WIND	Z/D	X/D
EXCS LIQM	4	TWRS	1	ARRAY	135	DEG	TO	WIND	Z/D	X/D
CASE (4) 5 TOWERS IN ROUND ARRAY										
5	100	30	30	11						
0	0	0	3	10	0	0	1	1	1	1
.00000	5.00000	10.00000	15.00000	20.00000						
10.00000	.00000	20.00000	2.00000	12.00000						
.00000	100.00000	200.00000								
10.50000	10.30000	10.10000								
70.00000	70.00000	70.00000								
4.10000	5.22504	5.76969	4.10000	5.22504	5.76969	4.10000	5.22504			
5.76969	4.10000	5.22504	5.76969	4.10000	5.22504	5.76969				
9.44880	10.26800	31.90000	.02821	.00000						
5.00000	5.00000	0	0	0	0					
EXCS TEMP	5	TWRS	IN	ROUND	ARRAY			Z/D		X/D
EXCS HUMI	5	TWRS	IN	ROUND	ARRAY			Z/D		X/D
EXCS LIQM	5	TWRS	IN	ROUND	ARRAY			Z/D		X/D

Table 4.2 Input Data Cards for Three Cases of Fan's (1967) Experiments with
F = 20, K = 8; F = 40, K = 8; and F = 80, K = 16

CASE (1) 60(D) F=20 K=8

```
1 350 1 1 1
0 0 0 2 1 0 0 0 0 0 0
.0
.0
.00000 -50.00000
31.87000 31.87000
.00000 .00000
.13700 .13700
.00760 -1.10000 20.00000 .00000 .00000
```

CASE (2) 60(G) F=40 K=8

```
1 350 1 1 1
0 0 0 2 1 0 0 0 0 0 0
.0
.0
.00000 -50.00000
26.57000 26.57000
.00000 .00000
.20400 .20400
.00760 -1.63000 20.00000 .00000 .00000
```

CASE (3) 60(J) F=80 K=16

```
1 350 1 1 1
0 0 0 2 1 0 0 0 0 0 0
.0
.0
.00000 -50.00000
23.31000 23.31000
.00000 .00000
.14600 .14600
.00760 -2.32000 20.00000 .00000 .00000
```

Table 4.3 Input Data Cards for Chan et al.'s (1974) Experiment
with F = 4, K = 1.02

Case (1) 6 Towers in One Array 90 Degrees to Wind F=4, K=1.02

```
6 100 21 17 11
0 0 1 2 0 0 1 1 0 0 1
.00000 .00000 .00000 .00000 .00000 .00000
.00000 .06501 .13003 .19504 .26006 .32507
.00000 900.00000
25.00000 25.00000
.00000 .00000
.37621 .37621 .37621 .37621 .37621 .37621 .37621 .37621
.37621 .37621 .37621 .37621
.05690 .38374 30.00000 .00000 .00000
.50000 .50000 1.00000 3.00000
6.31250 5.06250 0 0 0 0
EXCS TEMP 6 TWRS 1 ARRAY 90 DEG TO WIND Z/D X/D A3=0.3536 CD=1.5
```

Table 4.4 Input Data Cards for TVA (1968, TVA-11, single tower) Field Data in a Stable Atmospheric Condition ($\partial\theta/\partial z=0.59^\circ\text{K}/100\text{ m}$)

CASE (1) 100% EXIT HUMID & 100% AMB HUMID

1	300	1	1	1							
0	0	0	8	1	0	0	0	0	0	0	0
.00000											
.00000											
.00000	100.00000	150.00000	200.00000	250.00000	300.00000	350.00000	400.00000				
20.00000	20.16000	20.24000	20.32000	20.40000	20.48000	20.56000	20.64000				
100.00000	100.00000	100.00000	100.00000	100.00000	100.00000	100.00000	100.00000				
4.10000	4.10000	4.10000	4.70000	5.30000	5.90000	6.50000	7.10000				
7.90000	17.10000	139.00000	.67883	.00000							

CASE (2) 100% EXIT HUMID & 70% AMB HUMID

1	300	1	1	1							
0	0	0	8	1	0	0	0	0	0	0	0
.00000											
.00000											
.00000	100.00000	150.00000	200.00000	250.00000	300.00000	350.00000	400.00000				
20.00000	19.61000	19.42000	19.23000	19.04000	18.84000	18.65000	18.46000				
70.00000	70.00000	70.00000	70.00000	70.00000	70.00000	70.00000	70.00000				
4.10000	4.10000	4.10000	4.70000	5.30000	5.90000	6.50000	7.10000				
7.90000	17.10000	139.00000	.67883	.00000							

CASE (3) 100% EXIT HUMID & 0% AMB HUMID

1	300	1	1	1							
0	0	0	8	1	0	0	0	0	0	0	0
.00000											
.00000											
.00000	100.00000	150.00000	200.00000	250.00000	300.00000	350.00000	400.00000				
20.00000	19.61000	19.42000	19.23000	19.04000	18.84000	18.65000	18.46000				
.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000				
4.10000	4.10000	4.10000	4.70000	5.30000	5.90000	6.50000	7.10000				
7.90000	17.10000	139.00000	.67883	.00000							

CASE (4) 0% EXIT HUMID & 0% AMB HUMID

1	300	1	1	1							
0	0	0	8	1	0	0	0	0	0	0	0
.00000											
.00000											
.00000	100.00000	150.00000	200.00000	250.00000	300.00000	350.00000	400.00000				
20.00000	19.61000	19.42000	19.23000	19.04000	18.84000	18.65000	18.46000				
.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000				
4.10000	4.10000	4.10000	4.70000	5.30000	5.90000	6.50000	7.10000				
7.90000	17.10000	139.00000	.00000	.00000							

CHAPTER 5

CONCLUSIONS AND RECOMMENDATIONS

In this study, a mathematical model and corresponding computer program have been developed for the prediction of plume behavior from multiple cooling towers. Some comparisons between the predictions based on the present model and the measured results from laboratories and the field are made in order to test the model. The following conclusions and recommendations are made based on this study.

(1) The model is developed for arbitrary vertical profiles of ambient temperature, humidity, wind velocity, and arbitrary tower arrangement. The velocity defect for the downstream towers due to the effect of the upstream towers and plumes can be included by specifying different ambient velocity profiles for each plume. A general expression for the velocity defect of the downstream towers might be developed in the future.

(2) The temperature range for which this model is valid is -50°C to 140°C , because of the accuracy associated with the calculation of the saturation humidity.

(3) A set of suggested values of entrainment and drag coefficients have been incorporated in the computer program. Because of the rapid merging and usually rapid bending over of the plumes, the coefficients a_3 , α_s and C_d are the most important ones. Better estimates of their values are needed such as by further experimental study or field program.

(4) The merging criteria and processes (defined in this model by equations (2.38) (2.39) and (2.40)) could also be improved when further

research results on plume interaction are available.

(5) The blockage and recirculation effects in the wake zone of the towers and plumes have not been incorporated in the present model. Future effort could be made to include these effects.

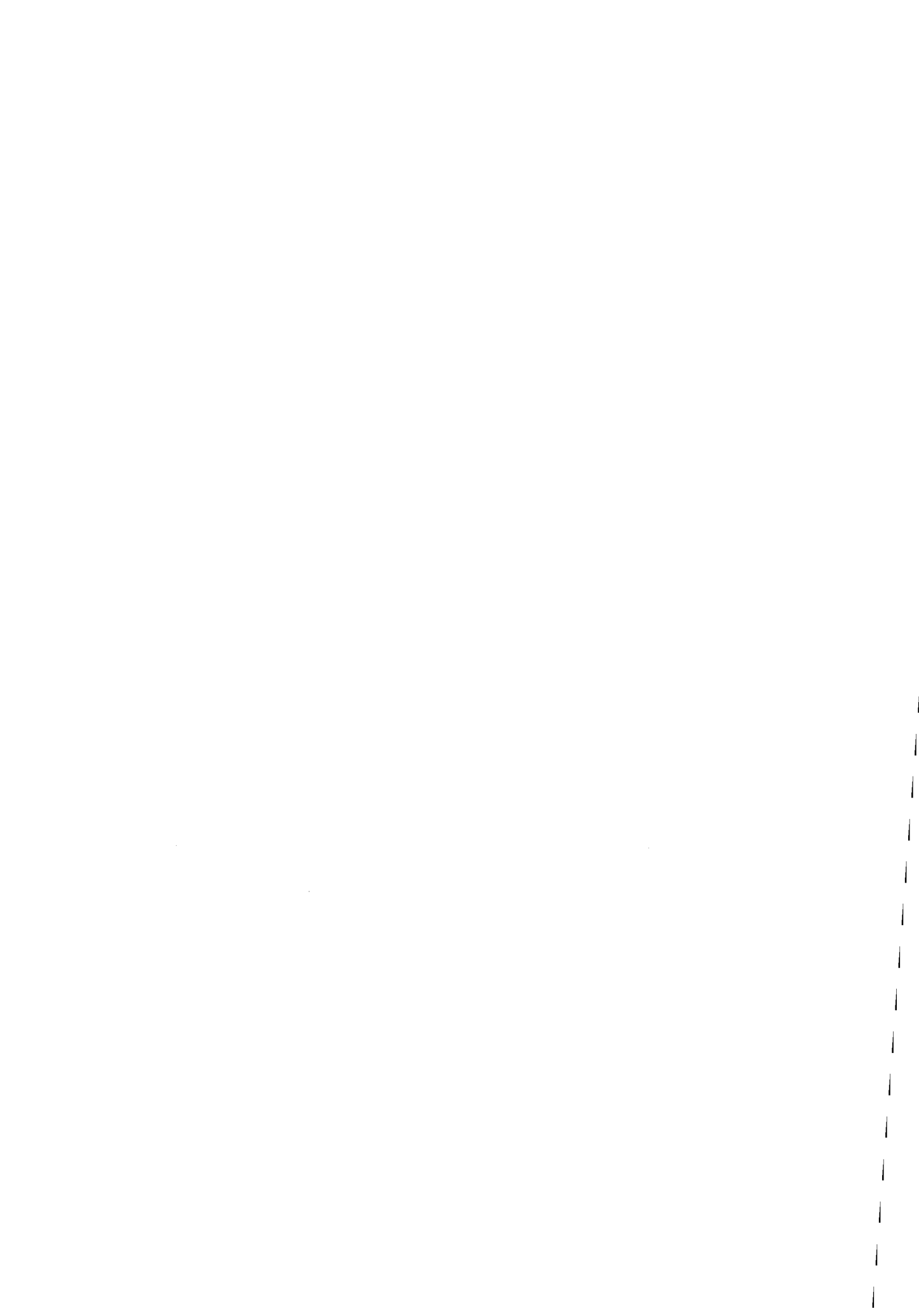
(6) Based on comparisons between model and laboratory results (Fan, and Chan et al.), good predictions of dry plume behavior can be obtained. In order to verify the model for actual cooling tower plumes, a more complete set of experimental data (including the plume width, trajectory, dilution and detailed ambient profiles of temperature, humidity and wind velocity) are required. Therefore, a complete set of field measurement are strongly recommended for validation of the model.

REFERENCES

- Abraham, G. (1970), "The Flow of Round Buoyant Jets Issuing Vertically into Ambient Fluid Flowing in a Horizontal Direction," *Advan. Water Poll. Res. Proc. Int. Conf. Water Poll. Res.* 5th Paper III-15.
- Briggs, G. A. (1969), "Plume Rise," AEC Critical Review Series Report. Report number TID-25075.
- Briggs, G. A. (1974), "Plume Rise from Multiple Sources," *Cooling Tower Environment-74*. CONF-74032, ERDA Symposium Series. National Technical Exchange Service. U.S. Dept. of Commerce, Springhill, VA., pp. 161-179.
- Carpenter, S. R., F. W. Thomas, and R. E. Gartrell (1968), "Full-Scale Study of Plume Rise at Large Electric Generating Stations," TVA, Muscle Shoals. Alabama.
- Chan, T. L., S.-T. Hsu, J.-T. Lin, K.-H. Hsu, N.-S. Huang, S. C. Jain, C. E. Tsai, T. E. Croley II, H. Fordyce and J. F. Kennedy, "Plume Recirculation and Interference in Mechanical Draft Cooling Towers," *Iowa Inst. Hyd. Res. Rep. No. 160*, 41 pp.
- Csanady, G. T. (1971), "Bent-Over Vapor Plume," *J. Appl. Meteor.*, 10, 34-42.
- Davis, L. R. (1975), "Analysis of Multiple Cell Mechanical Draft Cooling Towers," *Environ. Prot. Agency Rep. Office of Research and Development, Ecological Research Series*, EPA-66013-75-039.
- Fan, L. N. (1967), "Turbulent Buoyant Jets into Stratified or Flowing Ambient Fluid," *California Institute of Technology, W. M. Keck Laboratory of Hydraulics and Water Resources*, Rep. No. KH-R-15.
- Fox, D. G. (1970), "Forced Plume in a Stratified Fluid," *J. Geophys. Res.*, 75 (33), 6818-35.
- Hanna, S. R. (1972), "Rise and Condensation of Large Cooling Tower Plumes," *J. Appl. Meteor.*, 11, 793-799.
- Hirst, E. A. (1971), "Analysis of Round, Turbulent, Buoyant Jets Discharged to Flowing Stratified Ambients," *Oak Ridge National Laboratory, Report Number ORNL-4685*.
- Hoult, D. P., J. A. Fay, and L. J. Forney (1969), "A Theory of Plume Rise Compared with Field Observations," *J. Air Pollut. Contr. Assoc.* 19(9), 585-90.
- Jirka, G. and D.R.F. Harleman (1974), "The Mechanics of Submerged Multiport Diffusers for Buoyant Discharges in Shallow Water," *MIT Ralph M. Parsons Lab. for Water Resources and Hydraulics*, Report Number 169.

- Koh, R.C.Y. and N. H. Brooks (1975), "Fluid Mechanics of Waste-Water Disposal in the Ocean," *Ann. Rev. Fluid Mech.*, 7:187-211.
- Koh, R.C.Y. and Y. C. Chang (1973), "Mathematical Model for Barged Ocean Disposal of Wastes," *Environ. Prot. Agency, Office of Research and Development, Environ. Prot. Tech. Series, EPA-660/2-73-029.*
- Koh, R.C.Y. and L. N. Fan (1970), "Mathematical Models for the Prediction of Temperature Distributions Resulting from the Discharge of Heated Water into Large Bodies of Water," *Environ. Prot. Agency Rep. 16130 DWO 10/70, 219 pp.* (Also Tetra Tech, Inc., Rep. TC-170).
- Linsley, Jr., R. K., M. A. Kohler, and J.L.H. Paulhus (1975), Hydrology for Engineers, McGraw-Hill Book Company, Inc., New York, NY.
- List, E. J. and J. Imberger (1973), "Turbulent Entrainment in Buoyant Jets and Plumes," *J. Hydraul. Div., Proc. ASCE*, 99:1461-74.
- Meyer, J. H., T. W. Eagles, L. C. Kohlenstein, J. A. Kagan, and W. D. Stanbro (1974), "Mechanical Draft Cooling Tower Visible Plume Behavior: Measurements, Models, Predictions," *Cooling Tower Environment-74. CONF-74032, ERDA Symposium Series. National Technical Exchange Service, U.S. Dept. of Commerce, Springhill, VA, pp. 307-352.*
- Morton, B. R. (1957), "Buoyant Plumes in a Moist Atmosphere," *J. Fluid Mech.*, 2, 127-144.
- Morton, B. R., G. I. Taylor and J. S. Turner (1956), "Turbulent Gravitational Convection from Maintained and Instantaneous Sources," *Proc. Roy. Soc. London, Ser. A* 234:1-23.
- Richards, J. M. (1963), "Experiments on the Motion of Isolated Cylindrical Thermals through Unstratified Surroundings," *Intern. J. of Air and Water Pollut.*, 7, pp. 17-34.
- Richards, J. M. (1971), "Simple Expression for the Saturation Vapor Pressure of Water in the Range -50° to 140°C ," *Brit. J. Appl. Phys.*, 4, L15-L18.
- Schatzmann, M. (1977), "A Mathematical Model for the Prediction of Plume Rise in Stratified Flows," *Sonderforschungsbereich 80, University of Karlsruhe, W. Germany.*
- Slawson, P. R. and G. T. Csanady (1967), "On the Mean Path of Buoyant, Bent-Over Chimney Plumes," *J. Fluid Mech.*, 28, 311-322.
- Slawson, P. R. and G. T. Csanady (1971), "The Effect of Atmospheric Conditions on Plume Rise," *J. Fluid Mech.*, 47, 33-39.

- Slawson, P. R., J. H. Coleman, and J. W. Frey (1975), "Some Observations on Cooling-Tower Plume Behavior at the Paradise Steam Plant," Cooling Tower Environment--1974 (ERDA Symp. Series: CONF-740302), 147-160.
- Weil, J. C. (1974), "The Rise of Moist, Buoyant Plumes," J. Appl. Meteor., 13, 435-443.
- Wigley, T. M. L. (1974), Comments on "A Simple but Accurate Formula for the Saturation Vapor Pressure over Liquid Water," J. Appl. Meteor., 13, 608.
- Wigley, T. M. L. (1975), "A Numerical Analysis of the Effect of Condensation on Plume Rise," J. Appl. Meteor., 14, 1105-1109.
- Wigley, T. M. L. (1975), "Condensation in Jets, Industrial Plumes and Cooling Tower Plumes," J. Appl. Meteor., 14, 78-86.
- Wigley, T. M. L. and P. R. Salwson (1971), "On the Condensation of Buoyant, Moist Bent-Over Plumes," J. Appl. Meteor., 10, 253-259.
- Wigley, T. M. L. and P. R. Salwson (1972), "A Comparison of Wet and Dry Bent-Over Plumes," J. Appl. Meteor., 11, 335-340.
- Wright, S. J. (1977), "Effects of Ambient Crossflows and Density Stratification of the Characteristic Behavior of Round, Turbulent Buoyant Jets," California Institute of Technology, W. M. Keck Laboratory of Hydraulics and Water Resources, Report No. KH-R-36, 254 pp.



APPENDIX A

COMPUTER PROGRAM

The computer program based on the model and listed in Appendix C was tested on an IBM 370/158. The detailed input and output information are listed in this Appendix. The input ambient wind velocity profiles (AU(NP, MG)) for each tower are designed to allow consideration of the velocity defect in the wake of upstream towers (i.e., the tower array parallel to the ambient wind direction). In addition, some suggested input values are listed below for reference:

NS = 300

NX = 40

NY = 40

NCONT = 11

IX(3) = IX(6) = IX(11) = 0

In this Appendix, the input sequence as well as the input and output variables are tabulated, explained and related to the symbols used in the text of this report.

INPUT SEQUENCE

Symbol	Parameter	Format	Subroutine
NP,NS,NX,NY,NCONT		514	CTPS
(IX(I),I=1,11)		11I4	MTP
(CX(I),I=1,NP)		8F10.5	MTP
(CY(I),I=1,NP)		8F10.5	MTP
(AZ(I),I=1,MG)		8F10.5	MTP
(AT(I),I=1,MG)		8F10.5	MTP
(AH(I),I=1,MG)		8F10.5	MTP
((AU(I,J),J=1,MG),I=1,NP)		8F10.5	MTP
DI(1),UO(1), TO(1),HO(1),WO(1)	IX(1)=0 ⁺	8F10.5	MTP
(DI(I),I=1,NP)	IX(1)=1*	8F10.5	MTP
(UO(I),I=1,NP)	IX(1)=1*	8F10.5	MTP
(TO(I),I=1,NP)	IX(1)=1*	8F10.5	MTP
(HO(I),I=1,NP)	IX(1)=1*	8F10.5	MTP
(WO(I),I=1,NP)	IX(1)=1*	8F10.5	MTP
A1,A2,A3,A4,CD,TURBF	IX(2)=1*	8F10.5	MTP
DX,DZ,X0,Z0	IX(3)=1*	4F10.5	OUTPUT
WIDTH, HITE,MORE,NOMAP,ICENT NOTICK	IX(11)=1*	2F10.5 414	OUTPUT
(HEDN(k),k=1,10),(LABY(L),L=1,5),(LABX(M),M=1,5)	IX(8)=1*	20A4	OUTPUT
(HEDN(k),k=1,10),(LABY(L),L=1,5),(LABX(M),M=1,5)	IX(9)=1*	20A4	OUTPUT
(HEDN(k),k=1,10),(LABY(L),L=1,5),(LABX(M),M=1,5)	IX(10)=1*	20A4	OUTPUT

+ Skip card if IX(1)=1

* Skip card if the corresponding IX(I)=0, (I=1,2,3,11,8,9,10)

EXPLANATION OF THE INPUT SYMBOLS

<u>In Program</u>	<u>In Text</u>	<u>Remarks</u>
NP		Total number of towers
NS		Desired number of calculation steps
NX, NY [CONTA(NX,NY)]		Horizontal and vertical grid sizes, respectively (for contour plot)
NCONT [CONTB(NCONT)]		Desired contour levels for plotting
IX(1)	IX(1)=0	Same exit conditions of all the plumes (Input one card only)
	IX(1)=1	Different exit conditions of the plumes
IX(2)	IX(2)=0	No input card of entrainment and drag coefficients is needed
	IX(2)=1	Input the desired entrainment and drag coefficients
IX(3)	IX(3)=0	No input card of DX, DZ, XO and ZO is needed
	IX(3)=1	Input the desired values of DX, DZ, XO and ZO
	IX(3)=-1	No plot needed
IX(4)	MG	Number of vertical levels for ambient conditions
IX(5)	INRPR	Interval of detailed printout for plume 1
IX(6)	IPNT=0	For contour plot (always use IPNT=0)
IX(7)	LC=0	For cluster array (round array) of towers
	LC=1	For line or random array of towers
IX(8)	IX(8)=0	No contour map plotted for plume excess temperature
	IX(8)=1	Contour map plotted for plume excess temperature
IX(9)	IX(9)=0	No contour map plotted for plume excess humidity
	IX(9)=1	Contour map plotted for plume excess humidity
IX(10)	IX(10)=0	No contour map plotted for plume excess liquid moisture
	IX(10)=1	Contour map plotted for plume excess liquid moisture
IX(11)	IX(11)=0	No input card of WIDTH, HITE, MORE, NOMAP, ICENT, and NOTICK is needed
	IX(11)=1	Input the desired values of WIDTH, HITE, MORE, NOMAP, ICENT and NOTICK

<u>In Program</u>	<u>In Text</u>	<u>Remarks</u>
CX(NP)	x	x-coordinates of towers (in m)
CY(NP)	y	y-coordinates of towers (in m)
AZ(MG)	z	Ambient levels (in m)
AT(MG)	ta	Ambient temperature profile corresponding to AZ(I) (in °C)
AH(MG)	q _a	Ambient relative humidity profile corresponding to AZ(I) (in percentage of the saturation humidity)
AU(NP, MG)	U _a	Ambient wind velocity profile corresponding to AZ(I) for each tower (in m/sec)
DI(NP)	D _o	Diameter of each tower (in m)
UO(NP)	U _o	Exit velocity of each plume (in m/sec)
TO(NP)	t _o	Exit temperature of each plume (in °C)
HO(NP)	q _o	Exit specific humidity of each plume (in kg/kg)
WO(NP)	σ _o	Exit liquid phase moisture of each plume (in kg/kg)
A1, A2, A3 and A4	a ₁ , a ₂ , a ₃ and a ₄	Entrainment coefficients (Default: A1=0.0806, A2=0.4775, A3=0.3536, A4=0.)
CD	C _d	Drag coefficient (Default: CD=1.5)
TURBF	U' _a	Intensity of ambient turbulent fluctuations (in percentage, decimal; Default: TURBF=0.)
DX, DZ		Increments of grid size in x and z directions, respectively (Normalized by the diameter of the first tower; Default: DX=0.5, DZ=0.5)
XO, ZO		Location of the center of the top of the first tower in the grid (Normalized by the diameter of the first tower; Default: XO=1, ZO=2.)
WIDTH, HITE		Width and height of contour map, respectively (Inches; Default: 8", 8")
MORE		MORE=1 Do not finish off the map (Default: MORE=0)
NOMAP		NOMAP=1 Do not force grid to be square (Default: NOMAP=0)
ICENT		ICENT=1 Do not center the title (Default: ICENT=0)
NOTICK		NOCITK=1 Do not draw tick marks (Default: NOTICK=0)

<u>In Program</u>	<u>In Text</u>	<u>Remarks</u>
HEDN(10)		40 characters to plot as title on top (Default: Blank)
LABY(5)		20 characters to plot as label on vertical left (Default: Blank)
LABX(5)		20 characters to plot as label on horizontal bottom (Default: Blank)

EXPLANATIONS OF THE OUTPUT SYMBOLS

<u>In Program</u>	<u>In Text</u>	<u>Remarks</u>
EXIT, COEF, TWLC, AMBL, INPR, IPNT, LC, ETPL, EHPL, EMPL, COPL		Correspond to IX(1) to IX(11) respectively
A1, A2, A3, A4, CD, TURBF	$a_1, a_2, a_3, a_4,$ C_d, U'_a	Same as input symbols
NTHP		The N th plume
CX, CY [(CX(I), CY(I))]		Same as input symbols
DIA, VELO, TEMP, HUMI, LPMO [DI(I), UO(I), HO(I)WO(I)]	$D_o, U_o, t_o,$ q_o, σ_o	Tower diameter, exit values of plume velocity, temperature, specific humidity and liquid phase moisture, respectively
NSTEP*		The N th step of calculation referred to each tower
X, Y, Z [PX(NP, NS), PY(NP, NS), PZ(NP, NS)]	x, y, z	The horizontal, lateral and vertical coordinates of plume center
PTEMP, PHUMI, PLQEMOIST [PT(NP, NS), PH(NP, NS), PW(NP, NS)]	t_p, q_p, σ_p	Plume temperature, specific humidity and liquid phase moisture respectively
EXCEST, EXCESH [PET(NP, NS), PEH (NP, NS)]	$\Delta t, \Delta q$	Excess plume temperature and specific humidity
PCROSEC [BXZ(I)]	HT/2	Half height of plume cross-section
SLOTLEN[A(I)]	A	Finite length of slot jet of the merged plume
PANGLE [PCOS(NP, NS) PSIN(NP, NS)]	θ	The angle between the tangent of plume trajectory and the horizontal line
DILUTN [PDIL(NP, NS)]	Q/Q_o	Plume dilution
PVELO [PU(NP, NS)]	U_p	Plume velocity

* NSTEP refers to the number of calculation step of plume 1 when each plume first appeared

APPENDIX B

EXPLANATION OF THE IMPORTANT SYMBOLS IN THE PROGRAM MTP

<u>In Program</u>	<u>In Text</u>	<u>Remarks</u>
PX(NP,NS)	x	*
PY(NP,NS)	y	*
PZ(NP,NS)	z	*
PS(NP,NS)	s	*
PCOS(NP,NS)	$\cos\theta$	*
PSIN(NP,NS)	$\sin\theta$	*
PQ(NP,NS)	Q	*
PMX(NP,NS)	M_x	*
PMZ(NP,NS)	M_z	*
PF(NP,NS)	F^z	*
PG(NP,NS)	G	*
PH(NP,NS)	H	*
PW(NP,NS)	W	*
PT(NP,NS)	T	*
PET(NP,NS)	$t_p - t_a$	Excess temperature
PEH(NP,NS)	$q_p - q_a$	Excess humidity
PAN(NP,NS)	θ	*
PU(NP,NS)	U	Net plume velocity
PENT(NP,NS)	E	*
PA(NP,NS)	A	*
PB(NP,NS)	b or $(B1+B2)/2$	Average plume width
PC(NP,NS)	BXZ	*
PDIL(NP,NS)	Q/Q_0	Plume dilution
CONTA(NX,NY)		Normalized PET,PEH & PW (or PEW)
CONTB(NCONT)		Contour levels
IND(I)		Indication of the status of each plume
	IND(I)=5	Plume which has not been started
	IND(I)=1	Single plume
	IND(I)=2	Merged plume
	IND(I)=3	All plumes are merged
IS(I)		Beginning step number for each plume
MP(I)		Merged plume pair
MS(I)		Merged plume step numbers associated with MP(I)
A(I)	A	*
B1(I)	B1	*
B2(I)	B2	*
BXZ(I)	BXZ	*
BY(I)	BY	*
PMCOS(I)	$\cos\phi$	*
PMSIN(I)	$\sin\phi$	*
DW(I)	$2 \cdot BY$	*
NBV(I)		Beginning step number for visible plume
NEV(I)		Ending step number for visible plume
PAI	π	3.1415926
GRA	g	*
A1	a_1	*
A2	a_2	*
A3	a_3	*
A4	a_4	*

<u>In Program</u>	<u>In Text</u>	<u>Remarks</u>
CD	C_d	*
TURBF	U_a	*
UC	U_p	*
B		Plume width
TP	t_p	*
HP	q_p	*
WP	σ_p	*
ET	$t_p - t_a$	Excess temperature
EH	$q_p - q_a$	Excess humidity
MG		Elevation level
CFRL	Fr_{LC}	*
ALV	L_v	*
CPA	C_{pa}	*
ANG	θ	*
ITHP		i^{th} plume
ENTRAN	E	*
IQ		<3 All the plumes have not been completely merged
		=3 All the plumes have merged
		>3 All the plumes have merged and become a round plume again
IL		Number of merged pairs
IK		Plume step number
KE(I)		Ending step number of each plume
Y(I)	$Y(1)=Q$	*
	$Y(2)=M\cos\theta$	*
	$Y(3)=M\sin\theta$	*
	$Y(4)=G$	*
	$Y(5)=F$	*
	$Y(6)=x$	*
	$Y(7)=z$	*
YP(I)		Derivatives of Y(I) with respect to s
YR1(I), YR2(I), & YS(I)		Y(I) associated with the two half round plumes and the central slot plume for the merged plume
YR1P(I), YR2P(I), & YSP(I)		YP(I) associated with the two half round plumes and the central slot plume for the merged plume

* Refer to "List of Symbols"

C-1

APPENDIX C

LISTING OF PROGRAM

```
FORTRAN IV G LEVEL 20.7 VS          MAIN          DATE = 6/07/77 14:32:
0001          DIMENSION IA(2),I(26)
          C      NP=NUMBER_OF_PLUME,NS=NUMBER_OF_CALCULATION_STEP, NX,NY=DESIRED
          C      GRID OF CONTOUR PLOT, NCCNT=DESIRED CONTOUR LEVELS
0002          3  READ(5,2,END=9) NP,NS,NX,NY,NCONT
0003          2  FORMAT(5I4)
0004          N4=MAX0(NX,NY)
0005          NTOTAL=NP*NS
0006          IA(2)=NTOTAL*23+NX*NY+NCCNT+N4
0007          CALL GETVEC(IA)
0008          I(1)=IA(3)
0009          DO 1 J=2,24
0010          1  I(J)=I(J-1)+NTOTAL
0011          I(25)=I(24)+NX*NY
0012          I(26)=I(25)+NCONT
0013          CALL MTP(IA(I(1)),IA(I(2)),IA(I(3)),IA(I(4)),IA(I(5)),IA(I(6)),
          1IA(I(7)),IA(I(8)),IA(I(9)),IA(I(10)),IA(I(11)),IA(I(12)),IA(I(13)),
          2,IA(I(14)),IA(I(15)),IA(I(16)),IA(I(17)),IA(I(18)),IA(I(19)),
          3IA(I(20)),IA(I(21)),IA(I(22)),IA(I(23)),IA(I(24)),IA(I(25)),
          4IA(I(26)),NP,NS,NX,NY,NCCNT,N4)
0014          CALL FREEUP(IA)
0015          GO TO 3
0016          9  STOP
0017          END
```

FORTRAN IV G LEVEL 20.7 VS

MTP

DATE = 6/07/77

14:32

```

0001      SUBROUTINE MTP(PX,PZ,PQ,PMX,FMZ,PG,PF,PCOS,PSIN,PENT,PU,PS,PB,PA,
          1PT,PET,PH,PEH,PW,PAN,PDIL,PY,PC,CCNTA,CCNTB,CONTC,NP,NS,NX,NY,
          2NCONT,N4)
0002      EXTERNAL DERIVE,DERIVS,DERIVF
0003      DOUBLE PRECISION AQ,BQ,CQ,DQ
0004      COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
          1 /STORE2/MP(30),MS(30),IIP(30)
          2 /STORE3/AH(30),AT(30),AZ(30),AHG(30),ATG(30),AU(30,30),
          A AUG(30,30)
          3 /STORE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
          4 PMSIN(30),DW(30),NBV(30),NEV(30),NCV(30)
          5 /CONST1/PA1,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WP,
          6 MG,MG1,CFRL,ALV,CPA,ANG,IQ,ITHP,ENTRAN
          7 /CCNST2/IL,NII,IK,NI,NIP1
          8 /CCNST3/AQ,BQ,CQ,DQ
          9 /CCNTUU/WIDTH,HITE,MORE,NQMAP,ICENT,NOTICK,HEDN(10),
          * LABY(5),LABX(5)
          B /STORE5/DI(30),UO(30),TO(30),HC(30),WO(30)
0005      DIMENSION PX(NP,NS),PZ(NP,NS),PQ(NP,NS),PMX(NP,NS),PMZ(NP,NS),
          1PB(NP,NS),PU(NP,NS),PF(NP,NS),PG(NP,NS),PCOS(NP,NS),PSIN(NP,NS),
          2PENT(NP,NS),PH(NP,NS),PW(NP,NS),PEH(NP,NS),CX(30),CY(30),KE(30),
          3PT(NP,NS),PS(NP,NS),PA(NP,NS),PET(NP,NS),PAN(NP,NS),PY(NP,NS),
          4Y(8),YP(8),YS(8),YSP(8),YR1(8),YR1P(8),YR2(8),YR2P(8),PDIL(NP,NS),
          5CONTA(NX,NY),CONTB(NCONT),CONTC(N4),IX(12),MGPA2(30),MGST1(30),
          6PC(NP,NS),LCHK(30),AHP(30)
          C INITIALIZE STORAGES
0006      CALL BLANK(PX,PZ,PQ,PMX,PMZ,PB,PU,PF,PG,PCOS,PSIN,PENT,PT,PS,PA,
          1PET,PEH,PAN,PY,PDIL,PH,PW,PC,NP,NS,NX,NY,NCONT,N4,CONTA,CONTB,
          2CONTC,MGPA2,MGST1,DX,DZ,XO,ZC,IPNT,KE,LCHK,AHP)
          C INPUT CONTROL PARAMETERS
0007      READ(5,2) (IX(I),I=1,11)
0008      MG=IX(4)
0009      INTPR=IX(5)
0010      IPNT=IX(6)
0011      LC=IX(7)
          C INPUT TOWER CONFIGURATION
0012      READ(5,1) (CX(I),I=1,NP)
0013      READ(5,1) (CY(I),I=1,NP)
          C INPUT AMBIENT CONDITIONS
0014      READ(5,1) (AZ(I),I=1,MG)
0015      READ(5,1) (AT(I),I=1,MG)
0016      READ(5,1) (AHP(I),I=1,MG)
0017      READ(5,1) ((AU(I,J),J=1,MG),I=1,NP)
0018      IF(IX(1).GT.0) GO TO 34
          C INPUT TOWER EXIT CONDITIONS;DI=DIA., UC=VELO., TO=TEMP., HO=HUMID
          C WO=LIQUID PHASE MOISTURE
0019      READ(5,1)DI(1),UC(1),TO(1),HC(1),WO(1)
0020      DO 24 I=2,NP
0021      CI(I)=DI(1)
0022      UC(I)=LC(1)
0023      TO(I)=TO(1)
0024      HO(I)=HC(1)
0025      24 WO(I)=WO(1)
0026      GO TO 35
0027      34 READ(5,1) (DI(I),I=1,NP)
0028      READ(5,1) (UO(I),I=1,NP)

```

```

FORTRAN IV G LEVEL 20.7 VS                MTP                DATE =    6/07/77    14:32
-----
0029      READ(5,1) (TO(I),I=1,NP)
0030      READ(5,1) (HO(I),I=1,NP)
0031      READ(5,1) (WO(I),I=1,NP)
0032      35 IF(IX(2) .LE. 0) GO TO 32
          C      INPUT COEFFICIENTS OF ENTRAINMENT AND DRAG ;TURBF=TURB. FLUCT.
          C      TURBF=%(IN DECIMAL) OF AMBIENT WIND VELOCITY
0033      READ(5,1)A1,A2,A3,A4,CD,TURBF
0034      CFR1=A2/(0.116-A1)
-----
0035      1 FORMAT(8F10.5)
0036      2 FORMAT(12I4)
0037      32 WRITE(6,555)
0038      555 FORMAT(1H1)
0039      WRITE(6,3)
0040      3 FORMAT(1X,'UNITS OF THE VARIABLES')
0041      WRITE(6,4)
0042      4 FORMAT(1X,'LENGTH:M,  TEMP:C,  MOISTURE:KG/KG,  VELO:M/SEC,  ANGL
          1:DEG')
0043      WRITE(6,50)NP,NS,NX,NY,NCGNT
0044      WRITE(6,49)
0045      WRITE(6,36)
0046      WRITE(6,48) (IX(J),J=1,11)
0047      50 FORMAT(1X,'NO. OF TOWERS=',I4,' NO. OF CALCULATION STEPS=',I4,
          1' GRID SIZE (X,Y)=' ,I4,' X',I4,' CCNTOUR LEVELS=' ,I4//)
0048      49 FORMAT(1X,'CONTROL PARAMETERS')
0049      36 FORMAT(' EXIT COEF TWLC AMBL INPR IPNT LC ETPL EHPL '
          1'EMPL COPL')
-----
0050      48 FORMAT(1X,11(I4,2X)//)
0051      WRITE(6,5)
0052      5 FORMAT(1X,'COEFFICIENTS OF ENTRAINMENT AND DRAG')
0053      WRITE(6,6)A1,A2,A3,A4,CD,TURBF
0054      6 FORMAT(1X,'A1=' ,F8.5,5X,'A2=' ,F8.5,5X,'A3=' ,F8.5,5X,'A4=' ,F8.5,5
          1'CD=' ,F8.5,5X,'TURBF=' ,F8.5//)
0055      WRITE(6,7)
0056      7 FORMAT(1X,'AMBIENT PROFILES')
0057      WRITE(6,8)
0058      8 FORMAT(3X,'HEIGHT',7X,'TEMP',12X,'HUMIDITY',9X,'VELOCITY')
0059      DO 556 I=1,MG
0060      TK=AT(I)+273.16
0061      T=1.-373.16/TK
0062      EST=EXP((13.3185-(1.576+(0.6445+0.1229*T)*T)*T)*T)
0063      ES=0.622*1013.25*EST
0064      FSH=ES/(1013.25+ES)
0065      556 AH(I)=AHP(I)*0.01*FSH
0066      DO 9 I=1,MG
0067      9 WRITE(6,10)AZ(I),AT(I),AH(I),AHP(I),AU(1,I)
0068      10 FORMAT(1X,2(F10.5,2X),F10.6,1X,'( ',F6.2,'% )',2X,F10.5)
0069      WRITE(6,11)
0070      11 FORMAT(/)
0071      WRITE(6,12)
0072      12 FORMAT(1X,'TOWER CONFIGURATION AND EXIT CONDITIONS')
0073      WRITE(6,18)
0074      18 FORMAT(2X,'NTHP',6X,'CX',8X,'CY',8X,'DIA',4X,'VELO',6X,'TEMP',9)
          1'HUMI',9X,'LPMO')
0075      DO 17 I=1,NP
0076      17 WRITE(6,13)I,CX(I),CY(I),DI(I),UO(I),TO(I),HO(I),WO(I)
0077      13 FORMAT(1X,I5,3X,F7.2,3X,F7.2,3X,F6.2,3X,F6.2,3X,F8.3,3X,F12.8,3)

```

FORTRAN IV G LEVEL 20.7 VS

MTP

DATE = 6/07/77

14:32

```

1F12.8)
0078 WRITE(6,242)
      C CALCULATION OF TEMPERATURE,HUMIDITY AND VELOCITY GRADIENTS
0079 MG1=MG-1
0080 DO 14 I=1, MG1
0081 II=I+1
0082 DV=AZ(II)-AZ(I)
0083 ATG(I)=(AT(II)-AT(I))/DV
0084 14 AHG(I)=(AH(II)-AH(I))/DV
0085 DO 47 J=1, NP
0086 DO 47 I=1, MG1
0087 II=I+1
0088 DV=AZ(II)-AZ(I)
0089 47 AUG(J,I)=(AU(J,II)-AU(J,I))/DV
0090 DO 148 I=1, NP
0091 DO2=DI(I)/2.
0092 BXZ(I)=DC2
0093 BY(I)=DO2
0094 B1(I)=DO2
0095 148 B2(I)=DO2
0096 WRITE(6,15)
0097 15 FORMAT(1X,'PLUME 1 APPEARS AT NSTEP= 1',/)
      C SET INITIAL CONDITIONS
0098 TP=TD(1)
0099 ALV=FALV(TP)
0100 CALL SETIC(Y,IHP,CX)
      C INTEGRATION BY RUNGE-KUTTA METHOD
0101 L=0
0102 S=0.
0103 IKT=1
0104 DS=DI(IHP)/20.
0105 GO TO 598
0106 86 IF(NIP1 .GT. NP) GO TO 19
      C CHECK IF ANY NEW PLUME APPEARS
0107 CALL CHKNWP(PX,PZ,PQ,PMX,PMZ,PG,PF,PCCS,PSIN,PENT,PU,PS,PB,PA,PT,
1PET,PH,PEH,PW,PAN,PY,PDIL,PC,CX,NP,NS,DERIVR,CY,KE)
0108 19 IF(NII-1)16,105,105
0109 357 IKT=IK+NOVIK(1)
0110 IHP=1
0111 ALV=FALV(TP)
0112 DS=0.1*PB(1,IKT-1)
0113 598 CALL RUNGS(S,DS,7,Y,YP,L,DERIVR)
0114 B1(1)=B
0115 B2(1)=B
0116 BXZ(1)=B
0117 BY(1)=B
      C SOLUTIONS FOR SINGLE PLUME
0118 CALL SCLUTN(PX,PY,PZ,PQ,PMX,PMZ,PG,PF,PU,PENT,PS,PA,PB,PCOS,PSIN
1PT,PET,PH,PEH,PW,PAN,PDIL,PC,CY,Y,YP,S,IHP,IKT,NP,NS)
GO TO 78
      C CHECK IF ANY NEW PLUME MERGING OCCURS
0120 105 CALL ALIGN(PX,PY,PZ,PQ,PMX,PMZ,PG,PF,PU,PENT,PS,PA,PB,PC,PCOS,
1PSIN,PT,PET,PH,PEH,PW,PAN,PDIL,CY,Y,YP,YS,YSP,YR1,YR1P,YR2,YR2P,
2DERIVE,DERIVS,DERIVR,S,LC,NP,NS,KE)
0121 CALL PLMERG(PX,PY,PZ,PT,PET,PH,PEH,PW,PA,PB,PAN,PDIL,PCCS,PSIN,
1CY,NP,NS,KE,MGPA2,MGST1,PC,LCHK,PU)

```



```

FORTRAN IV G LEVEL 20.7 VS                MTP                DATE = 6/07/77    14:32:
-----
0122          16 DO 23 I=1,NI
0123          IJHP=I
0124          IKT=IK+NCV(IK(I))-IS(I)+1
0125          IF(IND(I) .LT.1) GO TO 23
0126          DS=0.1*PB(I,IKT-1)
-----
C          RESET INITIAL CONDITIONS AND CALCULATE PLUME PROPERTIES FOR SINGLE
C          AND MERGED PLUMES
0127          CALL RESETI(I,IKT,DS,S,NP,NS,CY,Y,YP,YS,YSP,YR1,YR1P,YR2,YR2P,
1 DERIVE,DERIVS,DERIVR,PX,PZ,PQ,PMX,PMZ,PG,PF,PCOS,PSIN,PENT,PU,PB,
2 PA,PJ,PET,PEH,PW,LC)
-----
C          SOLUTIONS OF PLUMES INCLUDING SINGLE & MERGED PLUMES
0128          CALL SOLUTN(PX,PY,PZ,PQ,PMX,PMZ,PG,PF,PU,PENT,PS,PA,PB,PCOS,PSIN,
1 PT,PET,PH,PEH,PW,PAN,PDIL,PC,CY,Y,YP,S,I,IKT,NP,NS)
-----
0129          23 CONTINUE
0130          IL=0
0131          78 DO 77 I=1,NP
0132          IF((IK+NOV(IK(I))) .LT. NS) GO TO 77
0133          IND(I)=0
0134          77 CONTINUE
0135          DC 75 I=1,NP
0136          IF(IND(I) .GT. 0) GO TO 79
0137          75 CONTINUE
0138          GC TO 80
0139          75 IK=IK+1
0140          IF(IQ-3)86,16,397
0141          80 DC 81 I=1,NP
0142          IF(KE(I) .LE. 0) GO TO 82
0143          IF(LCHK(I) .LT. 1) GO TO 81
0144          KE(I)=KE(I)+1
0145          J=KE(I)
0146          K=MGPA2(I)
0147          L=MGST1(I)+1
0148          PX(I,J)=PX(K,L)
0149          PZ(I,J)=PZ(K,L)
0150          PB(I,J)=PB(K,L)
0151          PC(I,J)=PC(K,L)
0152          PCOS(I,J)=PCOS(K,L)
0153          PSIN(I,J)=PSIN(K,L)
0154          PET(I,J)=PET(K,L)
0155          PEH(I,J)=PEH(K,L)
0156          PW(I,J)=PW(K,L)
0157          GO TO 81
0158          82 KE(I)=NS
0159          81 CONTINUE
0160          WRITE(6,808)
0161          808 FORMAT(1X,'RESULTS OF THE VISIBLE PLUMES')
0162          WRITE(6,225)
0163          CH=0.
0164          DO 807 I=1,NP
0165          KEN=KE(I)
0166          DO 803 J=1,KEN
0167          IF(PW(I,J) .GT. 0.) GO TO 802
0168          IF(NCV(I) .EQ. 0.) GO TO 803
0169          NEV(I)=J
0170          NCV(I)=0
0171          CH=2.
-----

```

```

FORTRAN IV G LEVEL 20.7 VS                MTP                DATE =    6/07/77    14:32:
0172          WRITE(6,809)J,I,PX(I,J),PZ(I,J),PY(I,J),PT(I,J),PET(I,J),PH(I,J),
             1PEH(I,J),PW(I,J),PB(I,J),PC(I,J),PA(I,J),PAN(I,J),PDIL(I,J),
             2PU(I,J)
0173          809 FORMAT(1X,2(I5,1X),3(F8.2,1X),2(F7.2,1X),3(F8.5,1X),6(F7.2,1X),/)
0174          GO TO 803
0175          802 IF(NCV(I).NE.0)GO TO 803
0176          NBV(I)=J
0177          NCV(I)=1
0178          CH=1.
0179          WRITE(6,241)J,I,PX(I,J),PZ(I,J),PY(I,J),PT(I,J),PET(I,J),PH(I,J),
             1PEH(I,J),PW(I,J),PB(I,J),PC(I,J),PA(I,J),PAN(I,J),PDIL(I,J),
             2PU(I,J)
0180          241 FORMAT(1X,2(I5,1X),3(F8.2,1X),2(F7.2,1X),3(F8.5,1X),6(F7.2,1X))
0181          803 CONTINUE
0182          IF(CH-1.) 804,805,807
0183          804 WRITE(6,233)I
0184          233 FORMAT(1X,'NO VISIBLE PART OF PLUME FOR PLUME',I4/)
0185          GO TO 807
0186          805 WRITE(6,243)I,J
0187          243 FORMAT(1X,'PLUME',I4,' STILL VISIBLE AT THE TERMINATION STEP',I4/)
0188          807 CONTINUE
0189          WRITE(6,242)
0190          242 FORMAT(//)
0191          WRITE(6,224)
0192          224 FORMAT(1X,'RESULTS AT THE LAST STEP OF CALCULATION')
0193          WRITE(6,225)
0194          225 FORMAT(1X,'NSTEP  NTHP  X      Z      Y      PTEMP  EXCEST
             1,' PHUMI  EXCESH  PLQDMOIST  PAVHFWD  PCROSEC  SLOTLN  PANGLE  ',
             2'DILUTN  PVELO')
             NTHP=1
0195          WRITE(6,226)NS,NTHP,PX(1,NS),PZ(1,NS),PY(1,NS),PT(1,NS),PET(1,NS)
0196          1PH(1,NS),PEH(1,NS),PW(1,NS),PB(1,NS),PC(1,NS),PA(1,NS),PAN(1,NS),
             2PDIL(1,NS),PU(1,NS)
0197          226 FORMAT(1X,2(I5,1X),3(F8.2,1X),2(F7.2,1X),3(F8.5,1X),6(F7.2,1X),//)
0198          CALL OUTPUT(PX,PY,PZ,PT,PET,PH,PEH,PW,PA,PC,PAN,PDIL,PSIN,PCOS,
             1CONTA,CONTB,CCNTC,KE,INTPR,IPNT,NX,NY,NCONT,N4,NP,NS,IX,DX,DZ,XC,
             2ZC,PB,PS,PU)
0199          RETURN
0200          END

```


FORTRAN IV G LEVEL 20.7 VS

BLANK

DATE = 6/07/77

14:32

```

0040          PT(I,J)=0.
0041          PS(I,J)=0.
0042          PA(I,J)=0.
0043          PH(I,J)=0.
0044          PY(I,J)=0.
0045          PAN(I,J)=0.
0046          PDIL(I,J)=C.
0047          1 PW(I,J)=0.
0048          DO 2 I=1,NX
0049          DO 2 J=1,NY
0050          2 CCNTA(I,J)=0.
0051          DO 3 I=1,NCONT
0052          3 CCNTB(I)=0.
0053          DO 5 I=1,N4
0054          5 CONTC(I)=0.
0055          DO 6 I=1,30
0056          DO 6 J=1,30
0057          AUG(I,J)=0.
0058          6 AU(I,J)=0.
0059          DO 7 I=1,30
0060          KE(I)=0
0061          AZ(I)=0.
0062          AT(I)=0.
0063          AHP(I)=0.
0064          AH(I)=0.
0065          AIG(I)=0.
0066          7 AHG(I)=0.
0067          AQ=0.000009153132
0068          BQ=0.0002112502
0069          CQ=0.003660244
0070          DQ=0.009494118
0071          CPA=1.005
0072          PAI=3.14159265
0073          GRA=9.8066
0074          A1=0.0806
0075          A2=0.6753
0076          A3=0.3536
0077          A4=0.
0078          CD=1.5
0079          TLRBF=0.
0080          DX=0.5
0081          CZ=0.5
0082          XD=1.
0083          ZQ=2.
0084          IPNT=0
0085          CFRL=A2/(0.116-A1)
0086          IL=0
0087          NII=0
0088          IK=1
0089          IQ=1
0090          NI=1
0091          NIP1=2
0092          ITHP=1
0093          IND(1)=1
0094          IS(1)=1
0095          RETURN

```

FORTRAN IV G LEVEL 20.7 VS

BLANK

DATE = 6/07/77

14:

0096

END

FORTRAN IV G LEVEL 20.7 VS

FALV

DATE = 6/07/77

14:32

```
0001      FUNCTION FALV(TC)
          C      TO DETERMINE LATENT HEAT ALV
0002      IF(TC .LT. 0.) GO TO 1
0003      FALV=(597.31-0.57*TC)*4.1868
0004      GO TO 2
0005      1 FALV=(677.01+0.622*TC)*4.1868
0006      2 RETURN
0007      END
```

FORTRAN IV G LEVEL 20.7 VS

SETIC

DATE = 6/07/77

14:0

```
0001      SUBROUTINE SETIC(Y,I,CX)
0002      COMMON /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WP,
          1          MG,MG1,CFRL,ALV,CPA,ANG,IQ,ITHP,ENTRAN
          2          /STORE3/AH(30),AT(30),AZ(30),AHG(30),ATG(30),AU(30,30),
          *          AUG(30,30)
          3          /STORE5/DI(30),UO(30),TO(30),HO(30),WO(30)
0003      DIMENSION Y(8),CX(30)
0004      Y(1)=PAI*DI(I)*DI(I)*ABS(UO(I))/4.
0005      Y(2)=0.
0006      Y(3)=Y(1)*UO(I)
0007      Y(4)=Y(1)*(TO(I)-AT(I)-WO(I)*ALV/CPA)
0008      Y(5)=Y(1)*(HO(I)-AH(I)+WO(I))
0009      Y(6)=CX(I)
0010      Y(7)=0.
0011      RETURN
0012      END
```

FORTRAN IV G LEVEL 20.7 VS

RUNGS

DATE = 6/07/77

14:32

```

0001      SUBROUTINE RUNGS(X,H,N,Y,YPRIME,INDEX,DERIV)
0002      DIMENSION Y(8),YPRIME(8),Z(8),W1(8),W2(8),W3(8),W4(8)
      C      RUNGS-RUNGE-KUTTA SOLUTION OF SET OF FIRST ORDER O.D.E. FORTRAN I
      C      DIMENSIONS MUST BE SET FOR EACH PROGRAM
      C      X      INDEPENDENT VARIABLE
      C      H      INCREMENT DELTA X, MAY BE CHANGED IN VALUE
      C      N      NUMBER OF EQUATIONS
      C      Y      DEPENDENT VARIABLE BLOCK      ONE DIMENSIONAL ARRAY
      C      YPRIME  DERIVATIVE BLOCK      ONE DIMENSIONAL ARRAY
      C      THE PROGRAMMER MUST SUPPLY INITIAL VALUES OF Y(1) TO Y(N)
      C      INDEX   IS A VARIABLE WHICH SHOULD BE SET TO ZERO BEFORE EACH
      C      INITIAL ENTRY TO THE SUBROUTINE, I.E., TO SOLVE A DIFFERENT
      C      SET OF EQUATIONS OR TO START WITH NEW INITIAL CONDITIONS.
      C      THE PROGRAMMER MUST WRITE A SUBROUTINE CALLED DERIVE WHICH
      C      COMPUTES THE DERIVATIVES AND STORES THEM
      C      THE ARGUMENT LIST IS SUBROUTINE DERIVE(X,N,Y,YPRIME)
0003      IF(INDEX) 5,5,1
0004      1 DO 2 I=1,N
0005      W1(I)=H*YPRIME(I)
0006      2 Z(I)=Y(I)+(W1(I)*.5)
0007      A=X+0.5*H
0008      CALL DERIV(A,N,Z,YPRIME)
0009      DC 3 I=1,N
0010      W2(I)=H*YPRIME(I)
0011      3 Z(I)=Y(I)+.5*W2(I)
0012      A=X+0.5*H
0013      CALL DERIV(A,N,Z,YPRIME)
0014      DO 4 I=1,N
0015      W3(I)=H*YPRIME(I)
0016      4 Z(I)=Y(I)+W3(I)
0017      A=X+H
0018      CALL DERIV(A,N,Z,YPRIME)
0019      DO 7 I=1,N
0020      W4(I)=H*YPRIME(I)
0021      7 Y(I)=Y(I)+(((2.*(W2(I)+W3(I)))+W1(I)+W4(I))/6.)
0022      X=X+H
0023      CALL DERIV(X,N,Y,YPRIME)
0024      GO TO 6
0025      5 CALL DERIV(X,N,Y,YPRIME)
0026      INDEX=1
0027      6 RETURN
0028      END

```


FORTRAN IV G LEVEL 20.7 VS

DERIVR

DATE = 6/07/77

15:27:

```

0001      SUBROUTINE DERIVR(S,A,Y,YP)
0002      DOUBLE PRECISION AQ,BQ,CQ,DQ
0003      COMMON /STORE1/INC(30),INDT(30),NOVIK(30),IS(30)
           1      /STORE3/AH(30),AT(30),AZ(30),AHG(30),ATG(30),AU(30),
           A      AUG(30,30)
           3      /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,IP,EH,WP,
           4      MG,MG1,CFRL,ALV,CPA,ANG,IC,ITHP,ENTRAN
           5      /CCNST3/AQ,BQ,CQ,DQ
           6      /STORE5/DI(30),UD(30),TO(30),HO(30),WO(30)
0004      DIMENSION Y(8),YP(8)
           C      DETERMINE AMBIENT CONDITIONS
0005      TPK=TP+273.16
0006      TOK=TO(ITHP)+273.16
0007      DO 88 I=2, MG
0008      IF(Y(7) .GT. AZ(I)) GO TO 88
0009      II=I-1
0010      DZZ=Y(7)-AZ(II)
0011      TA=AT(II)+ATG(II)*DZZ
0012      HA=AH(II)+AHG(II)*DZZ
0013      UA=AU(ITHP,II)+AUG(ITHP,II)*DZZ
0014      TG=ATG(II)
0015      HG=AHG(II)
0016      GO TO 90
0017      88 CONTINUE
0018      DZ1=Y(7)-AZ(MG1)
0019      TA=AT(MG1)+ATG(MG1)*DZ1
0020      HA=AH(MG1)+AHG(MG1)*DZ1
0021      UA=AU(ITHP,MG1)+AUG(ITHP,MG1)*DZ1
0022      HG=AHG(MG1)
0023      TG=ATG(MG1)
0024      90 TAK=TA+273.16
0025      UP=UA*TURBF
           C      DETERMINE MOMENTUM,TRAJECTORY AND VELOCITY OF PLUME
0026      PM=SQRT(Y(2)*Y(2)+Y(3)*Y(3))
0027      PCCS=Y(2)/PM
0028      PSIN=Y(3)/PM
0029      IF(PCOS .NE. 0.) GO TO 86
0030      ANG=90.
0031      GO TO 85
0032      86 ANG=ATAN(PSIN/PCCS)*180./PAI
0033      85 SIGN=1.
0034      IF(PSIN .LT. 0.) SIGN=-1.
0035      APSIN=ABS(PSIN)
0036      SY=PSIN*Y(1)
0037      UC=PM/Y(1)
0038      U=UC-UA*PCCS
0039      SPM=SQRT(PAI*PM)
0040      B=Y(1)/SPM
0041      USU=UC*PAI*B*B
0042      PMC=CD*B*UA*UA*PSIN*PSIN
0043      Y4=Y(4)/LSU
0044      Y5=Y(5)/LSU
0045      C1=ALV/CPA
0046      C2=Y4+TA+C1*(Y5+T)
0047      C3=Y5+HA
           C      TO ASSUME THE PLUME IS SATURATED AND CALCULATE THE SATURATED PLL

```

```

FORTRAN IV G LEVEL 20.7 VS                DERIVR                DATE = 6/07/77    15:27:

0048      C    HUMIDITY AND TEMPERATURE
          CALL ITER(TPK,HP,EST,C1,C2)
0049      C    TO DETERMINE THE PLUME LIQUID PHASE MOISTURE
          WP=C3-HP
0050      C    IF(WP .GT. 0.) GO TO 79
          DRY PLUME
0051      C    WP=0.
0052      C    HP=C3
0053      C    TP=TA+Y4
0054      C    TPK=TP+273.16
0055      C    GO TO 178
          WET PLUME
0056      C    79 TP=TPK-273.16
0057      C    178 ET=TP-TA
0058      C    EH=HP-HA
          TO DETERMINE ADIABATIC LAPSE RATE
0059      C    GAMA=FGAMA(TAK,TA)
          DETERMINE PLUME ENTRAINMENT
0060      C    RT=TPK/TAK
0061      C    PER=2.*PAI*B
0062      C    IF(RT .EQ. 1.) GO TO 99
0063      C    FRL=UC*UC*TPK/(GRA*TCK*ABS(RT-1.)*B)
0064      C    IF(FRL .GT. CFRL) GO TO 9
0065      C    A12=0.116
0066      C    GO TO 10
0067      C    9 A12=A1+A2*APSIN/FRL
0068      C    GO TO 10
0069      C    99 A12=A1
0070      C    10 ENTRAN=PER*(A12*ABS(U)+A3*UA*APSIN*PCOS+A4*UP)
          EQUATIONS OF CONSERVATION OF VOLUME, MOM., ENERGE AND MOIST. FLUXES
0071      C    YP(1)=ENTRAN*RT
0072      C    YP(2)=(UA*ENTRAN+PMC*APSIN)*RT
0073      C    YP(3)=(RT-1.-WP)*GRA*LSL/UC-SIGN*PMC*PCOS*RT
0074      C    YP(4)=- (TG+GAMA)*SY
0075      C    YP(5)=-HG*SY
0076      C    YP(6)=PCCS
0077      C    YP(7)=PSIN
0078      C    RETURN
0079      C    END

```

```

FORTRAN IV G LEVEL 20.7 VS          DERIVS          DATE = 6/07/77 15:27#

0001      SUBROUTINE DERIVS(S,N,Y,YP)
0002      DOUBLE PRECISION AQ,BQ,CQ,DQ
0003      COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
           1      /STORE3/AH(30),AT(30),AZ(30),AHG(30),ATG(30),AU(30,30),
           A      ALG(30,30)
           3      /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WF,
           4      MG,MG1,CFRL,ALV,CPA,ANG,IC,ITHP,ENTRAN
           5      /CCNST3/AG,BQ,CQ,DQ
           6      /STORE5/DI(30),UC(30),TO(20),HO(30),WO(30)

0004      DIMENSION Y(8),YP(8)
0005      TPK=TP+273.16
           C      DETERMINE AMBIENT CONDITIONS
0006      TOK=TO(ITHP)+273.16
0007      DO 88 I=2,MG
0008      IF(Y(7) .GT. AZ(I)) GC TO 88
0009      II=I-1
0010      DZZ=Y(7)-AZ(II)
0011      TA=AT(II)+ATG(II)*DZZ
0012      HA=AH(II)+AHG(II)*DZZ
0013      UA=AU(ITHP,II)+AUG(ITHP,II)*DZZ
0014      TG=ATG(II)
0015      HG=AHG(II)
0016      GO TO 90
0017      88 CONTINUE
0018      DZ1=Y(7)-AZ(MG1)
0019      TA=AT(MG1)+ATG(MG1)*DZ1
0020      HA=AH(MG1)+AHG(MG1)*DZ1
0021      UA=AU(ITHP,MG1)+AUG(ITHP,MG1)*DZ1
0022      TG=ATG(MG1)
0023      HG=AHG(MG1)
0024      90 TAK=TA+273.16
           C      UP=UA*TURBF
           C      DETERMINE MOMENTUM,TRAJECTORY AND VELOCITY OF PLUME
0026      PM=SQRT(Y(2)*Y(2)+Y(3)*Y(3))
0027      PCOS=Y(2)/PM
0028      PSIN=Y(3)/PM
0029      85 SIGN=1.
0030      IF(PSIN .LT. 0.) SIGN=-1.
0031      APSIN=ABS(PSIN)
0032      SY=PSIN*Y(1)
0033      UC=PM/Y(1)
0034      U=UC-UA*PCOS
0035      B=Y(1)*Y(1)/(2.*PM)
0036      USU=2.*B*UC
0037      PMC=CD*UA*UA*PSIN*PSIN*.5
0038      Y4=Y(4)/LSU
0039      Y5=Y(5)/LSU
0040      C1=ALV/CPA
0041      C2=Y4+TA+C1*(Y5+TA)
0042      C3=Y5+HA
           C      TO ASSUME THE PLUME IS SATURATED AND CALCULATE THE SATURATED PLUME
           C      HUMIDITY AND TEMPERATURE
0043      CALL ITER(TPK,HP,EST,C1,C2)
           C      TO DETERMINE THE PLUME LIQUID PHASE MOISTURE
0044      WP=C3-HP
0045      IF(WP .GT. 0.) GO TO 79

```

FORTRAN IV G LEVEL 20.7 VS

DERIVS

DATE = 6/07/77

15:27:

```

      C      DRY PLUME
0046      WP=0.
0047      HP=C3
0048      TP=TA+Y4
0049      TPK=TP+273.16
0050      GO TO 178
      C      WET PLUME
0051      79 TP=TPK-273.16
0052      178 ET=TP-TA
0053      EH=HP-HA
      C      TO DETERMINE ADIABATIC LAPSE RATE
0054      GAMA=FGAMA(TAK,FA)
      C      DETERMINE PLUME ENTRAINMENT
0055      TPK=TP+273.16
0056      RT=TPK/TAK
0057      ENTRAN=2.*(0.198*ABS(U)+A3*UA*PSIN*PCOS+A4*UP)
      C      EQUATIONS OF CONSERVATION OF VOLUME, MOM., ENERGY AND MOIST. FLUXES
0058      YP(1)=ENTRAN*RT
0059      YP(2)=(UA*ENTRAN+PMC*PSIN)*RT
0060      YP(3)=(RT-1.-WP)*GRA*LSL/UC-SIGN*PMC*PCOS*RT
0061      YP(4)=- (TG+GAMA)*SY
0062      YP(5)=-HG*SY
0063      YP(6)=PCCS
0064      YP(7)=PSIN
0065      RETURN
0066      END

```

FORTRAN IV G LEVEL 20.7 VS

DERIVE

DATE = 6/07/77

15:27:

```

0001      SUBROUTINE DERIVE(S,N,Y,YP)
0002      DOUBLE PRECISION AQ,BC,CQ,CQ
0003      COMMON /STORE1/INC(30),INDT(30),NOVIK(30),IS(30)
          1      /STORE3/AF(30),AT(30),AZ(30),AHG(30),ATG(30),AU(30,30),
          A      AUG(30,30)
          2      /STORE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
          3      PMSIN(30),Dw(30),NEV(30),NEV(30),NCV(30)
          4      /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,EF,EH,WF,
          5      MG,MG1,CFRL,ALV,CPA,ANG,IC,ITHP,ENTRAN
          6      /CCNST3/AC,BQ,CQ,CQ
          7      /STORE5/DI(30),UC(30),TO(30),HO(30),WO(30)

0004      DIMENSION Y(8),YP(8)
0005      TPK=TP+273.16
          C      DETERMINE AMBIENT CONDITIONS
0006      TOK=TO(ITHP)+273.16
0007      DO 88 I=2,MG
0008      IF(Y(7) .GT. AZ(I)) GO TO 88
0009      II=I-1
0010      DZZ=Y(7)-AZ(II)
0011      TA=AT(II)+ATG(II)*DZZ
0012      HA=AH(II)+AHG(II)*DZZ
0013      UA=AU(ITHP,II)+AUG(ITHP,II)*DZZ
0014      TG=ATG(II)
0015      HG=AHG(II)
0016      GO TO 90
0017      88 CONTINUE
0018      DZ1=Y(7)-AZ(MG1)
0019      TA=AT(MG1)+ATG(MG1)*DZ1
0020      HA=AH(MG1)+AHG(MG1)*DZ1
0021      UA=AU(ITHP,MG1)+AUG(ITHP,MG1)*DZ1
0022      TG=ATG(MG1)
0023      HG=AHG(MG1)
0024      90 TAK=TA+273.16
          C      UP=UA*TURBF
          C      DETERMINE MOMENTUM,TRAJECTORY AND VELOCITY OF PLUME
0026      PM=SQRT(Y(2)*Y(2)+Y(3)*Y(3))
0027      PCOS=Y(2)/PM
0028      PSIN=Y(3)/PM
0029      IF(PCOS .NE. 0.) GO TO 86
0030      ANG=90.
0031      GO TO 85
0032      86 ANG=ATAN(PSIN/PCOS)*180./PAI
0033      85 SIGN=1.
0034      IF(PSIN .LT. 0.) SIGN=-1.
0035      APSIN=ABS(PSIN)
0036      SY=PSIN*Y(1)
0037      UC=PM/Y(1)
0038      U=UC-UA*PCCS
0039      USU=UC*(A(ITHP)+(B1(ITHP)+B2(ITHP))+0.5*PAI*(B1(ITHP)*B1(ITHP)+
          1B2(ITHP)*B2(ITHP)))
0040      PMC=0.5*CD*UA*UA*PSIN*PSIN*Dw(ITHP)
0041      Y4=Y(4)/USU
0042      Y5=Y(5)/LSU
0043      C1=ALV/CPA
0044      C2=Y4+TA+C1*(Y5+TAK)
0045      C3=Y5+HA

```

```

FORTRAN IV G LEVEL 20.7 VS                DERIVE                DATE = 6/07/77    15:27:
C      TO ASSUME THE PLUME IS SATURATED AND CALCULATE THE SATURATED PLUME
C      HUMIDITY AND TEMPERATURE
0046  CALL ITER(TPK,HP,EST,C1,C2)
C      TO DETERMINE THE PLUME LIQUID PHASE MOISTURE
0047  WP=C3-HP
0048  IF(WP .GT. 0.) GC TO 79
C      DRY PLUME
0049  WP=0.
0050  HP=C3
0051  TP=TA+Y4
0052  TPK=TP+273.16
0053  GO TO 178
C      WET PLUME
0054  79 TP=TPK-273.16
0055  178 ET=TP-TA
0056  EH=HP-HA
C      TO DETERMINE ADIABATIC LAPSE RATE
0057  GAMA=FGAMA(TAK,FA)
C      DETERMINE PLUME ENTRAINMENT
0058  TPK=TP+273.16
0059  RT=TPK/TAK
0060  PER=2.*A(ITHP)
0061  A12=0.198
0062  IF(RT .EQ. 1.) GO TO 99
0063  FRC=UC*UC*TPK/(GRA*UC*ABS(RT-1.))
0064  FRL=FRC/B1(ITHP)
0065  IF(FRL .GT. CFRL) GO TO 106
0066  B12=0.116
0067  GO TO 108
0068  106 B12=A1+A2*AP SIN/FRL
0069  108 FRL=FRC/B2(ITHP)
0070  IF(FRL .GT. CFRL) GO TO 104
0071  C12=0.116
0072  GO TO 107
0073  104 C12=A1+A2*AP SIN/FRL
0074  GO TO 107
0075  99 B12=A1
0076  C12=A1
C      ENTRAINMENT OF TWO HALF ROUND ENDING PLUMES
0077  107 ENTR=PAI*(ABS(U)*(B1(ITHP)*B12+B2(ITHP)*C12)+(B1(ITHP)+B2(ITHP))
      I*(A3*UA*AP SIN*PCOS+A4*UF))
C      ENTRAINMENT OF TWO HALF ROUND PLUMES AND SLOT JET
0078  ENTRAN=PER*(A12*ABS(U)+A3*UA*AP SIN*PCOS+A4*UP)+ENTR
C      EQUATIONS OF CONSERVATION OF VOLUME, MOM., ENERGE AND MOIST. FLUXES
0079  YP(1)=ENTRAN*RT
0080  YP(2)=(UA*ENTRAN+PMC*AP SIN)*RT
0081  YP(3)=(RT-1.-WP)*GRA*USL/UC-SIGN*PMC*PCOS*RT
0082  YP(4)=- (TG+GAMA)*SY
0083  YP(5)=-HG*SY
0084  YP(6)=PCOS
0085  YP(7)=PSIN
0086  RETURN
0087  END

```

```

FORTRAN IV G LEVEL 20.7 VS          PHI          DATE = 6/07/77 14:32
0001          SUBROUTINE PHI(I,JR,M,CY,PZ,NP,NS,IKQ,IKP)
0002          COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
           1      /STORE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
           2      PMSIN(30),DW(30),NBV(30),NEV(30),NCV(30)
0003          DIMENSION PZ(NP,NS),CY(30)
           C      TO CALCULATE THE ANGLE OF THE INCLINATION OF MERGED PLUME (PHI)
0004          IJR=INDT(JR)
0005          IM=INDT(M)
0006          IF(IJR .NE. IM) GO TO 1
0007          IF(IJR .EQ. 1 .AND. IM .EQ. 1) GO TO 2
0008          IF(JR .EQ. M) GO TO 6
0009          IF(IJR .EQ. 2 .AND. IM .EQ. 2) GO TO 4
0010          2  DY=ABS(CY(JR)-CY(M))
0011          DZ=ABS(PZ(JR,IKP)-PZ(M,IKQ))
0012          DS=SQRT(DY*DY+DZ*DZ)
0013          PMCOS(I)=DY/DS
0014          PMSIN(I)=DZ/DS
0015          GO TO 5
0016          1  IF(IJR .NE. 1) GO TO 6
0017          7  PMCOS(I)=PMCOS(M)
0018          PMSIN(I)=PMSIN(M)
0019          GO TO 5
0020          6  PMCOS(I)=PMCOS(JR)
0021          PMSIN(I)=PMSIN(JR)
0022          GO TO 5
0023          4  COSS=PMCOS(JR)*PMCOS(M)-PMSIN(JR)*PMSIN(M)
0024          PMCOS(I)=SQRT(0.5*(1.+COSS))
0025          PMSIN(I)=SQRT(0.5*(1.-COSS))
0026          5  RETURN
0027          END

```

```
FORTRAN IV G LEVEL 20.7 VS          ITER          DATE = 6/07/77 14:32
0001      SUBROUTINE ITER(TPK,HP,EST,C1,C2)
0002      1 JS=373.16/IPK
0003      T=1.-TS
0004      EST=1013.25*EXP((13.3185-(1.976+(0.6445+0.1299*T)*T)*T)*T)
0005      ES=0.622*EST
0006      HP=ES/(1013.25+ES)
0007      FTPK=C2-C1*HP+273.16-TPK
0008      IF(ABS(FTPK) .LT. 0.01) RETURN
0009      DST=(13.3185-(3.952+(1.9335+0.5196*T)*T)*T)*TS/TPK
0010      FTPKD=-1.+C1*HP*DST*(HP-1.)
0011      TPK=TPK-FTPK/FTPDK
0012      GO TO 1
0013      END
```



```
FORTRAN IV G LEVEL 20.7 VS          FGAMA          DATE = 6/07/77 14:32
0001          FUNCTION FGAMA(TAK,HA)
          C      TO DETERMINE ADIABATIC LAPSE RATE
0002          T=1.-373.16/TAK
0003          EST=EXP(((13.3185-(1.976+(0.6445+0.1229*T))*T)*T)*T)
0004          ES=0.622*1013.25*EST
0005          HAS=0.99*ES/(1013.25+ES)
0006          IF(HA .GE. HAS) GO TO 1
          C      DRY ADIABATIC LAPSE RATE
0007          FGAMA=0.00976
0008          GO TO 2
0009          1 RESP=EST/TAK
          C      SATURATED ADIABATIC LAPSE RATE
0010          FGAMA=0.00976*(1.+5420.*RESP)/(1.+839000.*RESP/TAK)
0011          2 RETURN
0012          END
```

```

FORTRAN IV G LEVEL 20.7 VS          SOLUTN          DATE = 6/07/77 14:32:
0001          SUBROUTINE SOLUTN(PX,PY,PZ,PQ,PMX,FMZ,PG,PF,PU,PENT,PS,PA,PB,PCOS,
          1PSIN,PI,PET,PH,PEH,PH,PAN,PDIL,PC,CY,Y,YP,S,I,J,NP,NS)
0002          COMMON /STORE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
          1          FMSIN(30),DW(30),NBV(30),NEV(30),NCV(30)
          2          /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WP,
          3          MG,MG1,CFRL,ALV,CPA,ANG,IQ,ITHP,ENTRAN
          4          /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
0003          DIMENSION PX(NP,NS),PY(NP,NS),PZ(NP,NS),PQ(NP,NS),PMX(NP,NS),
          1PMZ(NP,NS),PG(NP,NS),PF(NP,NS),PU(NP,NS),PENT(NP,NS),PS(NP,NS),
          2PA(NP,NS),PB(NP,NS),PCOS(NP,NS),PSIN(NP,NS),PT(NP,NS),PET(NP,NS),
          3PH(NP,NS),PEH(NP,NS),PW(NP,NS),PAN(NP,NS),PDIL(NP,NS),CY(30),Y(8),
          4YP(8),FC(NP,NS)
0004          PX(I,J)=Y(6)
0005          PZ(I,J)=Y(7)
0006          PY(I,J)=CY(I)
0007          PQ(I,J)=Y(1)
0008          PMX(I,J)=Y(2)
0009          PMZ(I,J)=Y(3)
0010          PG(I,J)=Y(4)
0011          PF(I,J)=Y(5)
0012          PU(I,J)=UC
0013          PENT(I,J)=ENTRAN
0014          PS(I,J)=S
0015          PA(I,J)=A(I)
0016          PC(I,J)=BXZ(I)
0017          PB(I,J)=B
0018          PCOS(I,J)=YP(6)
0019          PSIN(I,J)=YP(7)
0020          PT(I,J)=TP
0021          PET(I,J)=ET
0022          PH(I,J)=HP
0023          PEH(I,J)=EH
0024          PW(I,J)=WP
0025          PAN(I,J)=ANG
0026          PDIL(I,J)=Y(1)/PQ(I,1)
0027          RETURN
0028          END

```

```

FORTRAN IV G LEVEL 20.7 VS          CHKNWP          DATE = 6/07/77 14:32:
0001          SUBROUTINE CHKNWP(PX,PZ,PQ,PMX,PMZ,PG,PF,PCOS,PSIN,PENT,PU,PS,PB,
          1PA,PT,PET,PH,PEH,PW,FAN,PY,PDIL,PC,CX,NP,NS,DERIVR,CY,KE)
0002          EXTERNAL DERIVR
0003          COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
          1 /STORE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
          2 PMSIN(30),DW(30),NBV(30),NEV(30),NCV(30)
          3 /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WP,
          4 MG,MG1,CFRL,ALV,CPA,ANG,IQ,ITHP,ENTRAN
          5 /CONST2/IL,NII,IK,NI,NIP1
          6 /STORE5/DI(30),UO(30),TO(30),HC(30),WO(30)
0004          DIMENSION PX(NP,NS),PZ(NP,NS),PQ(NP,NS),PMX(NP,NS),PMZ(NP,NS),
          1PB(NP,NS),PU(NP,NS),PF(NP,NS),PG(NP,NS),PCOS(NP,NS),PSIN(NP,NS),
          2PENT(NP,NS),PA(NP,NS),PT(NP,NS),CX(30),Y(8),YP(8),PS(NP,NS),
          3PH(NP,NS),PW(NP,NS),PET(NP,NS),PEH(NP,NS),PAN(NP,NS),PY(NP,NS),
          4PDIL(NP,NS),CY(30),KE(30),PC(NP,NS)
          C CHECK IF ANY NEW PLUME APPEARS
0005          IKK=IK+NOVIK(1)-IS(1)
0006          IF(PX(1,IKK) .LT. CX(NIP1)) GO TO 19
0007          NIPP=NIP1
0008          DO 22 J=NIPP,NP
0009          DS=DI(J)/20.
0010          IF(ABS(CX(NIPP)-CX(J)) .GE. DS) GO TO 22
0011          NI=NI+1
0012          WRITE(6,40)J,IKK
0013          40 FORMAT(1X,'PLUME',2X,I3,' APPEARS AT NSTEP=',I5//)
0014          NII=1
0015          IS(J)=IKK
0016          NOVIK(J)=NOVIK(1)
0017          NIP1=J+1
0018          INDI(J)=1
0019          IKS=1
          C SET INITIAL CCNDITICNS
0020          TP=TO(J)
0021          ALV=FALV(TP)
0022          CALL SETIC(Y,J,CX)
0023          L=0
0024          S=0.
0025          ITHP=J
0026          30 CALL RUNGS(S,DS,7,Y,YP,L,DERIVR)
0027          BXZ(J)=B
          C SOLUTICNS FOR UNMERGED SINGLE ROUND PLUME
0028          CALL SOLUTN(PX,PY,PZ,PQ,PMX,PMZ,PG,PF,PU,PENT,PS,PA,PB,PCOS,PSIN,
          1PT,PET,PH,PEH,PW,PAN,PDIL,PC,CY,Y,YP,S,J,IKS,NP,NS)
          C CHECKING THE CRITERION FOR STOPPING THE CALCULATION OF THE NEW
          C ISSUED SINGLE PLUME
0029          IF(PZ(J,IKS) .GE. PZ(1,IKK)) GO TO 23
0030          IF(IKS .GE. NS) GO TO 22
0031          IKS=IKS+1
0032          DS=B*0.1
0033          ALV=FALV(TP)
0034          GO TO 30
0035          23 KE(J)=IKS
0036          22 CONTINUE
0037          19 RETURN
0038          END

```

```

FORTRAN IV G LEVEL 20.7 VS                ALIGN                DATE =      6/07/77      14:32
0001      SUBROUTINE ALIGN(PX,PY,PZ,PQ,PMX,PMZ,PG,PF,PU,PENT,PS,PA,PB,PC,
        1PCOS,PSIN,PI,PET,PH,FEH,PW,PAN,PDIL,CY,Y,YP,YS,YSP,YR1,YR1P,YR2,
        2YR2P,DERIVE,DERIVS,DERIVR,S,LC,NP,NS,KE)
0002      EXTERNAL DERIVE,DERIVS,DERIVR
0003      COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
        1      /CCNST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WP,
        2      MG,MG1,CFRL,ALV,CPA,ANG,IQ,ITHP,ENTRAN
        3      /CCNST2/IL,NII,IK,NI,API
        4      /STORE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
        5      PMSIN(30),DW(30),NBV(30),NEV(30),NCV(30)
0004      DIMENSION PX(NP,NS),PY(NP,NS),PZ(NP,NS),PQ(NP,NS),PMX(NP,NS),
        1PMZ(NP,NS),PG(NP,NS),PF(NP,NS),PU(NP,NS),PENT(NP,NS),PS(NP,NS),
        2PA(NP,NS),PB(NP,NS),PC(NP,NS),PCOS(NP,NS),PSIN(NP,NS),PT(NP,NS),
        3PET(NP,NS),PH(NP,NS),PEH(NP,NS),PW(NP,NS),PAN(NP,NS),PDIL(NP,NS),
        4CY(30),Y(8),YP(8),YS(8),YSP(8),YR1(8),YR1P(8),YR2(8),YR2P(8),
        5KE(30)
0005      I1=IK+NOVIK(1)-1
0006      PXMAX=PX(1,I1)
0007      DO 1 I=1,NI
0008      IM=IK+NOVIK(I)-IS(I)
0009      IF(PXMAX .LT. PX(I,IM)) PXMAX=PX(I,IM)
0010      1 CCNTINLE
0011      DO 2 I=1,NI
0012      IF(IND(I) .LT. 1) GO TO 2
0013      IM=IK+NOVIK(I)-IS(I)
0014      11 IF(IM .GE. NS) GO TO 2
0015      DS=PB(I,IM)*0.1
0016      IF((PXMAX-PX(I,IM)-DS) .LT. 0.) GO TO 2
0017      IM=IM+1
0018      IF(IND(I) .GT. 1) GO TO 8
0019      IF(IM .GT. KE(I)) GO TO 8
0020      B1(I)=PB(I,IM)
0021      B2(I)=PB(I,IM)
0022      BXZ(I)=PB(I,IM)
0023      BY(I)=PB(I,IM)
0024      PC(I,IM)=PB(I,IM)
0025      GO TO 9
0026      8 ITHP=I
0027      IKT=IM
0028      CALL RESETI(I,IKT,DS,S,NP,NS,CY,Y,YP,YS,YSP,YR1,YR1P,YR2,YR2P,
        1DERIVE,DERIVS,DERIVR,PX,PZ,PC,PMX,FMZ,PG,PF,PCOS,PSIN,PENT,PU,PB,
        2PA,PI,PEI,PEH,PW,LC)
0029      CALL SOLUTN(PX,PY,PZ,PJ,PMX,PMZ,PG,PF,PU,PENT,PS,PA,PB,PCOS,PSIN,
        1PI,PEI,PH,PEH,PW,PAN,PDIL,PC,CY,Y,YP,S,I,IKT,NP,NS)
0030      9 NOVIK(I)=NOVIK(I)+1
0031      GO TO 11
0032      2 CONTINUE
0033      RETURN
0034      END

```

FORTRAN IV G LEVEL 20.7 VS

FLMERG

DATE = 6/07/77

14:32:

```

0001      SUBROUTINE PLMERG(PX,PY,PZ,PT,PET,PH,PEH,PW,PA,PB,PAN,PDIL,PCOS,
1PSIN,CY,NP,NS,KE,MGPA2,MGST1,PC,LCHK,PU)
0002      COMMON /STCRE1/IND(30),INDT(30),NOVIK(30),IS(30)
1          /STORE2/MP(30),MS(30),IIP(30)
2          /STCRE4/A(30),B1(30),B2(30),BXZ(30),BY(30),PMCOS(30),
3              PMSIN(30),DW(30),NBV(30),NEV(30),NCV(30)
4          /CONST1/PAI,GRA,A1,A2,A3,A4,CD,TURBF,UC,B,TP,ET,HP,EH,WP,
5              MG,MG1,CFRL,ALV,CPA,ANG,IQ,ITHP,ENTRAN
6          /CONST2/IL,NII,IK,NI,NIP1
0003      DIMENSION PX(NP,NS),PZ(NP,NS),PB(NP,NS),PCOS(NP,NS),PXI(30),
1PYI(30),PZI(30),PBI(30),PCOSI(30),CY(30),IRE(30),PSIN(NP,NS),
2PSINI(30),KE(30),PY(NP,NS),PT(NP,NS),PET(NP,NS),PH(NP,NS),
3PEH(NP,NS),PW(NP,NS),PA(NP,NS),PAN(NP,NS),PDIL(NP,NS),MGPA2(30),
4MGST1(30),PC(NP,NS),B1I(30),B2I(30),BXZI(30),BYI(30),AI(30),
5LCHK(30),PU(NP,NS)
C          REARRANGE THE TRAJECTORIES OF THE EXISTING PLUMES
0004      NJ=0
0005      DO 101 I=1,NI
0006          IF(IND(I)-1)101,102,102
0007      102  ISC=IK+NOVIK(I)-IS(I)
0008          NJ=NJ+1
0009          PXI(NJ)=PX(I,ISC)
0010          PYI(NJ)=CY(I)
0011          PZI(NJ)=PZ(I,ISC)
0012          PBI(NJ)=PB(I,ISC)
0013          PCOSI(NJ)=PCOS(I,ISC)
0014          PSINI(NJ)=PSIN(I,ISC)
0015          AI(NJ)=A(I)
0016          B1I(NJ)=B1(I)
0017          B2I(NJ)=B2(I)
0018          BXZI(NJ)=BXZ(I)
0019          BYI(NJ)=BY(I)
0020          IRE(NJ)=I
0021      101  CONTINUE
C          CHECK PLUME MERGING
0022      IL=0
0023      NII=NJ-1
0024      DO 103 I=1,NII
0025          JI=I+1
0026          DO 103 J=JI,NJ
0027          PYD=ABS(PYI(I)-PYI(J))
0028          PZD=ABS(PZI(I)-PZI(J))
0029          PYZ=SQRT(PZD*PZD+PYD*PYD)
0030          SR=BXZI(I)*PCOSI(I)+BXZI(J)*PCOSI(J)
0031          SR2=BYI(I)+BYI(J)
0032          IF(SR-PZD)103,10,10
0033      10  IF(SR2-PYD)103,104,104
0034      104  IF(AI(I).EQ.0..AND. AI(J).EQ.0.) GO TO 1
0035          GO TO 106
0036      1  AREA1=C.5*PAI*(B1I(I)*B1I(I)+B1I(J)*B1I(J))
0037          AREA2=PYZ*(B1I(I)+B1I(J))
0038          IF(AREA1-AREA2)103,106,106
0039      106  IL=IL+1
C          RECORD THE PAIRS OF THE MERGED PLUMES
0040          MP(IL)=IRE(I)
0041          MS(IL)=IRE(J)

```

```

FORTRAN IV G LEVEL 20.7 VS          PLMERG          DATE = 6/07/77 14:32:
0042          II=IRE(I)
0043          JJ=IRE(J)
0044          IND(JJ)=IND(JJ)
0045          IND(I)=IND(I)
          C    RESET IND(II)=2,IND(JJ)=0 FOR JJ>II WHEN PLUMES II AND JJ MERGED
0046          IND(JJ)=0
0047          IIP(JJ)=IK+NOVIK(JJ)-IS(JJ)
0048          IF(IND(II)-1) 103,111,113
0049          111 IND(II)=2
0050          113 IIP(II)=IK+NOVIK(II)-IS(II)
0051          103 CCNTINUE
0052          IF(IL-1)16,107,205
0053          205 K=1
0054          206 II=K+1
0055          DO 200 I=II,IL
0056          IF(MS(K).NE.MS(I))GO TO 20C
0057          IF(MP(I)-MP(K))204,200,203
0058          203 IF(IND(I).EQ.0)GO TO 200
0059          IND(I)=0
0060          IIP(I)=IK+NOVIK(I)-IS(I)
0061          GO TO 20C
0062          204 IF(IND(K).EQ.0)GO TO 200
0063          IND(K)=0
0064          IIP(K)=IK+NOVIK(K)-IS(K)
0065          200 CCNTINUE
0066          K=K+1
0067          IF(K.LT.IL)GO TO 206
          C    PLUME MERGING OCCURS
0068          107 WRITE(6,108)
0069          108 FORMAT(1X,'RESULTS OF THE PAIRS OF MERGED PLUMES AT MERGING PLACE'
          1)
0070          WRITE(6,112)
0071          112 FORMAT(1X,'NSTEP  NTHP  X      Z      Y      PTEMP  EXCEST'
          1,' PHUMI  EXCESH  PLQDMCIST  PAVHFW  PCROSEC  SLOTLN  PANGLE  ',
          2'DILUTN  PVELO')
0072          DO 109 I=1,IL
0073          INDX=1
0074          LP=MP(I)
0075          LS=MS(I)
0076          MT=IIP(LP)
0077          NT=IIP(LS)
0078          MGPA2(LS)=LP
0079          MGST1(LS)=MT
0080          IF(KE(LS).GT. NT) GO TO 116
0081          LCHK(LS)=1
0082          KE(LS)=NT
0083          116 WRITE(6,110)MT,LP,PX(LP,MT),PZ(LP,MT),PY(LP,MT),PT(LP,MT),
          1PET(LP,MT),PH(LP,MT),PEH(LP,MT),PW(LP,MT),PB(LP,MT),PC(LP,MT),
          2PA(LP,MT),PAN(LP,MT),PDIL(LP,MT),PU(LP,MT)
0084          110 FORMAT(1X,2(I5,1X),3(F8.2,1X),2(F7.2,1X),3(F8.5,1X),6(F7.2,1X))
0085          IF(INDX-1)117,117,118
0086          117 INDX=2
0087          LP=LS
0088          MT=NT
0089          GO TO 116
0090          118 WRITE(6,119)

```

FORTRAN IV G LEVEL 20.7 VS

PLMERG

DATE = 6/07/77

14:32;

```
0091      119 FORMAT(/)
0092      109 CONTINUE
0093          DO 777 I=2,NI
0094          IF(IND(I)-1) 777,779,779
0095      777 CONTINUE
0096          NII=0
0097          ITHP=1
0098      779 DO 400 I=2,NP
0099          IF(IND(I))16,400,16
0100      400 CONTINUE
          C    ALL THE PLUMES ARE MERGED WHEN IND(I)=0 FOR 1<I<NP+1
0101          IND(I)=3
0102          IQ=3
0103          NI=1
0104          ITHP=1
0105      16 RETURN
0106      END
```

```

FORTRAN IV G LEVEL 20.7 VS                RESETI                DATE = 6/07/77    19:42:
0001      SUBROUTINE RESETI(I, IKT, DS, S, NP, NS, CY, Y, YP, YS, YSP, YR1, YR1P, YR2,
1YR2P, DERIVE, DERIVS, DERIVR, FX, PZ, PQ, PMX, PMZ, PG, PF, PCCS, PSIN, PENT,
2PU, PB, PA, PT, PET, PEH, PW, LC)
0002      EXTERNAL DERIVE, DERIVS, DERIVR
0003      COMMON /STCRE1/INC(30), INDT(30), NOVIK(30), IS(30)
1          /STORE2/MP(30), MS(30), IIP(30)
2          /STCRE4/A(30), B1(30), B2(30), BXZ(30), BY(30), PMCJS(30),
3          PMSIN(30), GW(30), NEV(30), NEV(30), NCV(30)
4          /CONST1/PAI, GRA, A1, A2, A3, A4, CD, TURBF, UC, B, TP, ET, HF, EH, WP,
5          MG, MG1, CFRL, ALV, CPA, ANG, IC, ITHP, ENTRAN
6          /CONST2/IL, NII, IK, NI, NIP1
0004      DIMENSION FX(NP, NS), PZ(NP, NS), PQ(NP, NS), FMX(NP, NS), FMZ(NP, NS),
1PB(NP, NS), PF(NP, NS), PG(NP, NS), PENT(NP, NS), IRP(30), COB(30), Y(8),
2YP(8), CY(30), PT(NP, NS), PET(NP, NS), PU(NP, NS), YS(8), YSP(8),
3PA(NP, NS), PCOS(NP, NS), PSIN(NP, NS), YR1(8), YR1P(8), YR2(8), YR2P(8),
4PEH(NP, NS), PW(NP, NS), IH(30)
0005      IK1=IKT-1
0006      Y(1)=PQ(I, IK1)
0007      Y(2)=PMX(I, IK1)
0008      Y(3)=PMZ(I, IK1)
0009      Y(4)=PG(I, IK1)
0010      Y(5)=PF(I, IK1)
0011      Y(6)=PX(I, IK1)
0012      Y(7)=PZ(I, IK1)
0013      APT=PT(I, IK1)
0014      IF(INDT(I)-2)29,30,30
0015      30 IF(IL)32,32,33
1          C RESET INITIAL CONDITIONS WHEN ANY NEW PLUME MERGING OCCURS
0016      33 IRP(1)=I
0017      IJK=1
0018      MM=1
0019      JR=I
0020      M=I
0021      JRZ=I
0022      MZ=I
0023      CYMANI=CY(I)+BY(I)
0024      CYMINI=CY(I)-BY(I)
0025      PZMANI=PZ(I, IK1)+BXZ(I)
0026      PZMINI=PZ(I, IK1)-BXZ(I)
0027      CYMAN=CYMANI
0028      CYMIN=CYMINI
0029      PZMAN=PZMANI
0030      PZMIN=PZMINI
0031      60 DO 34 J=1, IL
0032      IF(IRP(MM)-MP(J))34,35,34
0033      35 JJ=MS(J)
0034      DO 86 NR=1, IJK
0035      IF(JJ-IRP(NR))86,34,86
0036      86 CONTINUE
1          C SUMMING UP VOLUME, MOMENTUM, ENERGY AND MOISTURE FLUXES OF THE
2          C MERGED PLUMES
0037      IKP=IK+NCVIK(JJ)-IS(JJ)
0038      Y(1)=Y(1)+PQ(JJ, IKP)
0039      Y(2)=Y(2)+PMX(JJ, IKP)
0040      Y(3)=Y(3)+PMZ(JJ, IKP)
0041      Y(4)=Y(4)+PG(JJ, IKP)

```


FORTRAN IV G LEVEL 20.7 VS

RESETI

DATE = 6/07/77

19:42:

```

0042      Y(5)=Y(5)+PF(JJ,IKP)
0043      PQ(I,1)=PQ(I,1)+PQ(JJ,1)
0044      APT=APT+PT(JJ,IKP)
0045      IJK=IJK+1
0046      IRP(IJK)=JJ
0047      CYMANC=CX(JJ)+BY(JJ)
0048      CYMINC=CX(JJ)-BY(JJ)
0049      PZMANC=PZ(JJ,IKP)+BXZ(JJ)
0050      PZMINC=PZ(JJ,IKP)-BXZ(JJ)
0051      IF(INDT(JJ).GT.1) GO TO 401
0052      IF(INDT(I)-2) 401,400,4C1
0053      400 IF(IH(I).GT.2) GO TO 404
0054      IF(CYMANI .GE. CYMANC .AND. CYMINI .LE. CYMINC) GO TO 3+
0055      GO TO 401
0056      404 IF(PZMANI .GE. PZMANC .AND. PZMINI .LE. PZMINC) GO TO 3+
0057      401 IF(CYMAN .GE. CYMANC) GO TO 244
0058      CYMAN=CYMANC
0059      JR=JJ
0060      244 IF(CYMIN .LE. CYMINC) GO TO 28
0061      CYMIN=CYMINC
0062      M=JJ
0063      28 IF(PZMAN .GE. PZMANC) GO TO 26
0064      PZMAN=PZMANC
0065      JRZ=JJ
0066      26 IF(PZMIN .LE. PZMINC) GO TO 34
0067      PZMIN=PZMINC
0068      MZ=JJ
0069      34 CONTINUE
0070      IF(MM-IJK) 58,59,59
0071      58 MM=MM+1
0072      GO TO 60
0073      59 IF(MM-1) 32,32,555
0074      859 APT=APT/FLCAT(IJK)
0075      Y(7)=0.5*(PZMAN+PZMIN)
      C      LC=C MEANS CLUSTER OF TOWERS; LC=1 MEANS LINE TOWER ARRAY
0076      IF(LC-1)575,572,575
0077      575 CY(I)=0.5*(CYMAN+CYMIN)
0078      GO TO 571
0079      572 IKQ=IK+NCVIK(M)-IS(M)
0080      IKP=IK+NCVIK(JR)-IS(JR)
0081      DCYAI=CYMAN-CYMIN
0082      DPZAI=PZMAN-PZMIN
0083      IF(DCYAI .LT. DPZAI) GO TO 402
0084      IF(-(CYMAN-CYMIN) .LT. -(PZMAN-PZMIN)) GO TO 402
0085      IF(CY(M) .EQ. CY(JR)) GO TO 407
0086      CYDZ=ABS(PZ(M,IKC)-PZ(JR,IKP))
      C      TO CALCULATE THE ANGLE OF THE INCLINATION OF MERGED PLUME (PHI)
0087      CALL PHI(I,JR,M,CY,PZ,NF,NS,IKQ,IKP)
0088      IF(CYDZ.NE.0.) GO TO 408
0089      IH(I)=2
0090      GO TO 409
0091      408 IH(I)=1
0092      409 B1(I)=PB(M,IKQ)
0093      B2(I)=PB(JR,IKP)
0094      IF(PMCOS(I) .EQ. 0.) GO TO 988
0095      A(I)=(DCYAI-B1(I)-B2(I))/PMCCS(I)

```

```

FORTRAN IV G LEVEL 20.7 VS                RESETI                DATE = 6/07/77    19:42:
0096          GO TO 573
0097          988 A(I)=DPZAI-B1(I)-B2(I)
0098          GO TO 573
0099          402 JR=JRZ
0100          M=MZ
0101          IKQ=IK+NOVIK(M)-IS(M)
0102          IKP=IK+NCVIK(JR)-IS(JR)
0103          IF(PZ(JR,IKP).EQ.PZ(M,IKQ)) GO TO 407
0104          PZY=ABS(CY(JR)-CY(M))
C          TO CALCULATE THE ANGLE OF THE INCLINATION OF MERGED PLUME (PHI)
0105          CALL PHI(I,JR,M,CY,PZ,NF,NS,IKQ,IKP)
0106          IF(PZY.NE.0.)GO TO 431
0107          IH(I)=3
0108          GO TO 432
0109          431 IH(I)=1
0110          432 B1(I)=PB(M,IKQ)
0111          B2(I)=PB(JR,IKP)
0112          IF(PMSIN(I).EQ.0.) GO TO 989
0113          A(I)=(DPZAI-B1(I)-B2(I))/FMSIN(I)
0114          GO TO 573
0115          989 A(I)=DCYAI-B1(I)-B2(I)
0116          GO TO 573
0117          407 A(I)=A(JR)
0118          B1(I)=B1(JR)
0119          B2(I)=B2(JR)
0120          PMCCS(I)=PMCCS(JR)
0121          PMSIN(I)=PMSIN(JR)
0122          IH(I)=IH(JR)
0123          573 CY(I)=0.5*(CYMAN+CYMIN)
0124          IF(A(I).EQ.0.)GO TO 38
0125          GO TO 574
0126          32 IF(LC-I)571,570,571
0127          571 IF(IND(I)-3)29,41,29
0128          570 IF(A(I))38,38,39
0129          38 A(I)=0.
0130          IF(IND(I)-3)40,41,40
0131          41 IQ=4
0132          IND(I)=4
0133          GO TO 29
0134          40 IND(I)=1
0135          GO TO 29
0136          39 JR=I
0137          IKP=IK1
0138          M=I
0139          IKQ=IK1
C          RESET I.C. FOR THE HALF ROUND PLUME
0140          574 BBB=PAI*B1(I)*B1(I)*ABS(PU(M,IKQ))
0141          ALV1=FALV(PT(M,IKQ))
0142          ALV2=FALV(PT(JR,IKP))
0143          YR1(1)=BBB
0144          YR1(2)=BBB*PU(M,IKQ)*PCCS(M,IKQ)
0145          YR1(3)=BBB*PU(M,IKQ)*PSIN(M,IKQ)
0146          YR1(4)=BBB*(PET(M,IKQ)-ALV1*PW(M,IKQ))
0147          YR1(5)=BBB*(PEH(M,IKQ)+FW(M,IKQ))
0148          YR1(6)=PX(M,IKQ)
0149          YR1(7)=PZ(M,IKQ)

```

FORTRAN IV G LEVEL 20.7 VS

RESETI

DATE = 6/07/77

19:42:

```

C      RESET I.C. FOR THE HALF ROUND PLUME
0150      BBB=PAI*B2(I)*B2(I)*ABS(PU(JR,IKP))
0151      YR2(1)=BBB
0152      YR2(2)=BBB*PU(JR,IKP)*PCOS(JR,IKP)
0153      YR2(3)=BBB*PU(JR,IKP)*PSIN(JR,IKP)
0154      YR2(4)=BBB*(PET(JR,IKP)-ALV2*PW(JR,IKP))
0155      YR2(5)=BBB*(PEH(JR,IKP)+PW(JR,IKP))
0156      YR2(6)=PX(JR,IKP)
0157      YR2(7)=PZ(JR,IKP)
C      RESET I.C. FOR THE CENTRAL SLOT JET
0158      YS(1)=(Y(1)-0.5*(YR1(1)+YR2(1)))/A(I)
0159      YS(2)=(Y(2)-0.5*(YR1(2)+YR2(2)))/A(I)
0160      YS(3)=(Y(3)-0.5*(YR1(3)+YR2(3)))/A(I)
0161      YS(4)=(Y(4)-0.5*(YR1(4)+YR2(4)))/A(I)
0162      YS(5)=(Y(5)-0.5*(YR1(5)+YR2(5)))/A(I)
0163      YS(6)=Y(6)
0164      YS(7)=Y(7)
C      CALCULATE NEW HALF WIDTH AND VELO. OF THE HALF ROUND PLUME
0165      L=0
0166      ALV=ALV1
0167      CALL RUNGS(S,DS,5,YR1,YR1P,L,DERIVR)
0168      CALL RUNGS(S,DS,5,YR1,YR1P,L,DERIVR)
0169      BR1=B
0170      UR1=UC
0171      S=S-DS
C      CALCULATE NEW HALF WIDTH AND VELO. OF THE HALF ROUND PLUME
0172      L=0
0173      ALV=ALV2
0174      CALL RUNGS(S,DS,5,YR2,YR2P,L,DERIVR)
0175      CALL RUNGS(S,DS,5,YR2,YR2P,L,DERIVR)
0176      BR2=B
0177      UR2=UC
0178      S=S-DS
C      CALCULATE NEW HALF WIDTH AND VELO. OF THE SLCT JET
0179      L=0
0180      ALV=FALV(APT)
0181      CALL RUNGS(S,DS,5,YS,YSF,L,DERIVS)
0182      CALL RUNGS(S,DS,5,YS,YSF,L,DERIVS)
0183      BS=B
0184      US=UC
0185      S=S-DS
C      CALCULATE MERGED PLUME WITH THE MODIFIED PLUME SHAPE DETERMINED C
C      THE PREVIOUS STEP
0186      L=0
0187      CALL RUNGS(S,DS,7,Y,YP,L,DERIVE)
0188      CALL RUNGS(S,DS,7,Y,YF,L,DERIVE)
C      DETERMINE B1,B2 AND A CF THE MODIFIED PLUME SHAPE FOR CALCULATING
C      ENTRAINMENT AND DRAG FOR NEXT STEP
0189      UU=UC
0190      W=A(I)
0191      CB1=BR2/BR1
0192      CB2=W+BR1+BR2
0193      CB3=(1.5707963*(BR1*BR1*UR1+BR2*BR2*UR2)+2.*BS*W*US)/JU
0194      CB4=1.+CB1
0195      API=1.5707963*(1.+CB1*CB1)-CB4*CB4
0196      BP1=CB2*CB4

```

```

FORTRAN IV G LEVEL 20.7 VS                RESETI                DATE = 6/07/77    19:42:
0197          CP1=-CB3
0198          B1P=B1(I)
0199          B2P=B2(I)
0200          AP=A(I)
          C    THE DETERMINED B1,B2 AND A
0201          B1(I)=(-BP1+SQRT(EP1*BP1-4.*AP1*CP1))/(.2.*AP1)
0202          B2(I)=CB1*B1(I)
0203          A(I)=CB2-CB4*B1(I)
0204          B=(B1(I)+B2(I))*0.5
0205          IF(A(I))418,418,419
0206          418 A(I)=0.
0207          IF(IND(I)-3) 420,421,420
0208          421 IQ=4
0209          IND(I)=4
0210          GO TO 31
0211          420 IND(I)=1
0212          GO TO 31
0213          419 DY=0.5*(B2(I)-B1(I)+(B1F-B2P)*A(I)/AP)*ABS(PMCCS(I))
0214          CY(I)=CY(I)+DY
          C    DETERMINE SOME LENGTH SCALES FOR THE USE OF MERGING CRITERION
0215          AL=0.5*(B1(I)+B2(I))
0216          ALC=AL+0.5*PMCCS(I)*A(I)
0217          ALS=AL+0.5*PMSIN(I)*A(I)
0218          LQ=IH(I)
0219          GO TO (411,412,413),LQ
0220          411 BY(I)=ALC
0221          BXZ(I)=ALS
0222          GO TO 416
0223          412 BY(I)=ALC
0224          BXZ(I)=AMAX1(B1(I),B2(I))
0225          GO TO 416
0226          413 BXZ(I)=ALS
0227          BY(I)=AMAX1(B1(I),B2(I))
0228          416 DW(I)=2.*BY(I)
0229          GO TO 31
          C    CALCULATE SINGLE ROUND FLUME
0230          29 L=0
0231          ALV=FALV(PT(I,IK1))
0232          CALL RUNGS(S,DS,7,Y,YF,L,DERIVR)
0233          CALL RUNGS(S,DS,7,Y,YF,L,DERIVR)
0234          B1(I)=B
0235          B2(I)=B
0236          BXZ(I)=B
0237          BY(I)=B
0238          31 RETURN
0239          END

```

```

FORTRAN IV G LEVEL 20.7 VS          OUTPUT          DATE = 6/07/77 19:42:
0001          SUBROUTINE OUTPUT(PX,PY,PZ,PT,PET,PH,PEH,PW,PA,PC,PAN,PJ,IL,PSIN,
1PCGS,CONTA,CONTB,CONTC,KE,INTPR,IFNT,NX,NY,NCONT,N4,NP,NS,IX,DX,
2DZ,XO,ZO,PB,PS,PU)
0002          COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
1          /CCNTUU/WIDTH,HITE,MORE,NCMAP,ICENT,NOTICK,HEDN(10),
2          LABY(5),LABX(5)
3          /STORE5/DI(30),UO(30),TO(30),HO(30),WO(30)
0003          DIMENSION PX(NP,NS),PY(NP,NS),PZ(NP,NS),PT(NP,NS),PET(NP,NS),
1PH(NP,NS),PEH(NP,NS),PW(NP,NS),PA(NP,NS),PC(NP,NS),PAN(NP,NS),
2PDIL(NP,NS),PSIN(NP,NS),PCGS(NP,NS),CONTA(NX,NY),CONTB(NCONT),
3CONTC(N4),KE(30),IX(12),PB(NP,NS),PS(NP,NS),PU(NP,NS)
0004          IF(INTPR.LE.0) GO TO 10
0005          WRITE(6,1)
0006          1 FORMAT(1X,'DETAILED RESULTS OF PLUME 1')
0007          WRITE(6,2)
0008          2 FORMAT(1X,'NSTEP  NTP  X  Z  Y  PTEMP EXCESS
1,' PHUMI  EXCESH PLQDMOIST PAVHFD PRCSEC SLOTLN PANGLE ',
2'DILUTN PVELO')
0009          I=1
0010          DO 3 J=1,NS,INTPR
0011          3 WRITE(6,241)J,I,PX(I,J),PZ(I,J),PY(I,J),PT(I,J),PET(I,J),PH(I,J),
1PEH(I,J),PW(I,J),PB(I,J),PC(I,J),PA(I,J),PAN(I,J),PDIL(I,J),
2PU(I,J)
0012          241 FORMAT(1X,2(I5,1X),3(F8.2,1X),2(F7.2,1X),3(F8.5,1X),6(F7.2,1X))
0013          10 IF(IX(3))15,21,20
0014          20 READ(5,22)CX,DZ,XC,ZC
0015          22 FORMAT(4F10.5)
0016          21 IF(IX(11).LE.0) GO TO 26
0017          READ(5,28)WIDTH,HITE,MORE,NOMAP,ICENT,NOTICK
0018          28 FORMAT(2F10.5,4I4)
0019          NCONB=-NCONT
0020          26 PETO=PMAX(PET,NP,NS,KE)
0021          PEHC=PMAX(PEH,NP,NS,KE)
0022          PEWC=PMAX(PW,NP,NS,KE)
0023          IF(PETO.GT.0.) GO TO 14
0024          IX(8)=0
0025          PETO=1.
0026          WRITE(6,40)
0027          40 FORMAT(1X,'NO EXCESS TEMP PLOT DUE TO ZERO OR NEGATIVE EXCESS',
1' TEMPERATURE')
0028          14 IF(PEHC.GT.0.) GO TO 42
0029          IX(9)=0
0030          PEHC=1.
0031          WRITE(6,43)
0032          43 FORMAT(1X,'NO EXCESS HUMI PLOT DUE TO ZERO OR NEGATIVE EXCESS',
1' HUMIDITY')
0033          42 IF(PEWC.GT.0.) GO TO 47
0034          IX(10)=0
0035          PEWC=1.
0036          WRITE(6,46)
0037          46 FORMAT(1X,'NO EXCESS LIQUID PHASE MOISTURE PLOT DUE TO ZERO OR',
1' NEGATIVE EXCESS LIQUID PHASE MOISTURE')
C          DETERMINE GRID DISTRIBUTION
0038          47 DO 11 I=1,NP
0039          DO 11 J=1,NS
0040          PX(I,J)=PX(I,J)/EI(I)

```

```

FORTRAN IV G LEVEL 20.7 VS                OUTPUT                DATE =    6/07/77    19:42:
0041          PZ(I,J)=PZ(I,J)/DI(I)
0042          PB(I,J)=PB(I,J)/DI(I)
0043          PC(I,J)=PC(I,J)/DI(I)
0044          PS(I,J)=PS(I,J)/DI(I)
0045          PW(I,J)=PW(I,J)/PEWO
0046          PEH(I,J)=PEH(I,J)/PEHC
0047          11 PET(I,J)=PET(I,J)/PETC
0048          I=8
0049          IF(IX(I) .LE. 0) GO TO 5
0050          CALL GRD2(CONTA,DX,DZ,PX,PZ,PC,PET,PCOS,PSIN,NP,NS,KE,XJ,ZO,NX,NY)
0051          WRITE(6,31)
0052          31 FORMAT(1X,'EXCESS TEMPERATURE PLOT',//)
0053          GO TO 37
0054          8 CALL GRD2(CONTA,DX,DZ,PX,PZ,PC,PEH,PCOS,PSIN,NP,NS,KE,XJ,ZO,NX,NY)
0055          WRITE(6,32)
0056          32 FORMAT(1X,'EXCESS SPECIFIC HUMIDITY PLOT',//)
0057          GO TO 37
0058          9 CALL GRD2(CONTA,DX,DZ,PX,PZ,PC,PW,PCOS,PSIN,NP,NS,KE,XJ,ZO,NX,NY)
0059          WRITE(6,33)
0060          33 FORMAT(1X,'EXCESS LIQUID PHASE MOISTURE PLOT',//)
0061          37 READ(5,30) (HEDN(K),K=1,10), (LABY(L),L=1,5), (LABX(M),M=1,5)
0062          30 FORMAT(20A4)
0063          7 CALL CCNTU(CCNTA,CCNTE,CONTC,NX,NY,NCONB,IFNT)
0064          5 I=I+1
0065          IF(I-10)16,17,15
0066          16 IF(IX(I))5,5,8
0067          17 IF(IX(I))5,5,9
0068          15 RETURN
0069          END

```

FORTRAN IV G LEVEL 20.7 VS

FMAX

DATE = 6/07/77

14:32

```
0001      FUNCTION PMAX(PT,NP,NS,KE)
0002      DIMENSION PT(NP,NS),KE(30)
0003      PMAX=PT(1,1)
0004      DO 1 I=1,NP
0005      K=KE(I)
0006      DO 1 J=1,K
0007      IF(PT(I,J) .GT. PMAX) PMAX=PT(I,J)
0008      1 CONTINUE
0009      RETURN
0010      END
```

```

FORTRAN IV G LEVEL 20.7 VS          GRD2          DATE = 6/07/77 14:32:
0001          SUBROUTINE GRD2(A,DX,DZ,PX,PZ,PB,PG,PCOS,PSIN,NP,NS,KE,XD,ZD,JD,
          1JD)
0002          COMMON /STORE1/IND(30),INDT(30),NOVIK(30),IS(30)
0003          DIMENSION A(ID,JD),RM(5),C(5),IC(4),PX(NP,NS),PZ(NP,NS),PG(NP,NS),
          1PB(NP,NS),PCOS(NP,NS),PSIN(NP,NS),KE(30)
0004          DO 210 I=1,JD
0005          DO 210 J=1,JD
0006          210 A(I,J)=0.
0007          DO 1 N=1,NP
0008          DO 1 I=1,NS
0009          PX(N,I)=PX(N,I)+XD
0010          1 PZ(N,I)=PZ(N,I)+ZD
0011          KX=1
0012          DO 2 N=1,NP
0013          KY=KE(N)-1
0014          IF(KX .GE. KY) GO TO 2
0015          RM(1)=0.
0016          C(1)=PZ(N,KX)
0017          IC(1)=(PX(N,KX)-PB(N,KX))/DX+1.0005
0018          IC1=PX(N,KX)/DX+1.0005
0019          IC(2)=(PX(N,KX)+PB(N,KX))/DX+1.0005
0020          DO 2 K=KX,KY
0021          PB2S=PB(N,K+1)*PSIN(N,K+1)
0022          IC(3)=(PX(N,K+1)-PB2S)/DX+1.0005
0023          IC2=PX(N,K+1)/DX+1.0005
0024          IC(4)=(PX(N,K+1)+PB2S)/DX+1.0005
0025          PB2C=PB(N,K+1)*PCOS(N,K+1)
0026          PB1C=PB(N,K)*PCOS(N,K)
0027          PB1S=PB(N,K)*PSIN(N,K)
0028          DZZ=PZ(N,K+1)-PZ(N,K)
0029          DXX=PX(N,K+1)-PX(N,K)
0030          DPBC=PB2C-PB1C
0031          DPBS=PB2S-PB1S
0032          DS=SQRT(DZZ*DZZ+DXX*DXX)
0033          CB=PB(N,K+1)-PB(N,K)
0034          DG=PG(N,K)-PG(N,K+1)
0035          IF(PSIN(N,K+1) .LT. 0.) GO TO 101
0036          IF(IC(1)-IC(3)) 103,104,105
0037          105 IL=IC(3)+1
0038          GO TO 112
0039          104 IL=IC(3)+1
0040          GO TO 113
0041          103 IL=IC(1)+1
0042          112 RM(3)=(DZZ+DPBC)/(DXX-DPBS)
0043          C(3)=PZ(N,K+1)+PB2C-(PX(N,K+1)-PB2S)*RM(3)
0044          113 DXPB=DXX+DPBS
0045          IF(DXPB .EQ. 0.) GO TO 20
0046          RM(4)=(DZZ-DPBC)/DXPB
0047          C(4)=PZ(N,K+1)-PB2C-(PX(N,K+1)+PB2S)*RM(4)
0048          20 IF(PSIN(N,K+1) .EQ. 0.) GO TO 109
0049          RM(2)=-PCOS(N,K+1)/PSIN(N,K+1)
0050          C(2)=PZ(N,K+1)-PX(N,K+1)*RM(2)
0051          109 IR=IC(4)
0052          IF(IL .GT. IR) GO TO 99
0053          DO 12 I=IL,IR
0054          IF(I .GT. ID) GO TO 12

```


FORTRAN IV G LEVEL 20.7 VS

GRD2

DATE = 6/07/77

14:32:

```

0055          IF(I .LT. 1) GO TO 12
0056          X=DX*FICAT(I-1)
0057          IF(I .GT. IC(3)) GO TO 7
0058          ZU=RM(3)*X+C(3)
0059          GO TO 8
0060          7 ZU=RM(2)*X+C(2)
0061          8 JU=ZU/DZ+1.0001
0062          IF(I .GT. IC(2)) GO TO 10
0063          IF(I .GT. IC(1)) GO TO 115
0064          ZL=RM(3)*X+C(3)
0065          GO TO 11
0066          115 ZL=RM(1)*X+C(1)
0067          GO TO 11
0068          10 ZL=RM(4)*X+C(4)
0069          11 IF((ZL-DZ*FLOAT(JU-1)) .GT. 0.) GO TO 12
0070          JL=ZL/DZ+1.9999
0071          IF(JU .LT. JL) GO TO 12
0072          CALL PD2(A,PX,PZ,PB,PG,PCOS,PSIN,RM,C,NP,NS,N,JL,JU,DB,DG,DZ,X,
          1DXX,DZZ,I,K,ID,JD)
0073          12 CCNTINUE
0074          GO TO 99
0075          101 IF(IC(2)-IC(4)) 121,122,123
0076          122 IL=IC(2)+1
0077          GO TO 124
0078          123 IL=IC(4)+1
0079          GO TO 125
0080          121 IL=IC(2)+1
0081          125 RM(4)=(DZZ-DPBC)/(DXX+DPBS)
0082          C(4)=PZ(N,K+1)-PB2C-(PX(N,K+1)+PB2S)*RM(4)
0083          124 DXDP=DXX-DPBS
0084          IF(DXDP .EQ. 0.) GO TO 21
0085          RM(3)=(DZZ+DPBC)/DXDP
0086          C(3)=PZ(N,K+1)+PB2C-(PX(N,K+1)-PB2S)*RM(3)
0087          21 RM(2)=-PCOS(N,K+1)/PSIN(N,K+1)
0088          C(2)=PZ(N,K+1)-PX(N,K+1)*RM(2)
0089          IR=IC(3)
0090          IF(IL .GT. IR) GO TO 99
0091          DO 128 I=IL,IR
0092          IF(I .GT. ID) GO TO 128
0093          IF(I .LT. 1) GO TO 128
0094          X=DX*FLOAT(I-1)
0095          IF(I .GT. IC(1)) GO TO 130
0096          IF(I .GT. IC(2)) GO TO 132
0097          ZU=RM(4)*X+C(4)
0098          GO TO 133
0099          132 ZU=RM(1)*X+C(1)
0100          GO TO 133
0101          130 ZU=RM(3)*X+C(3)
0102          133 JU=ZU/DZ+1.0001
0103          IF(I .GT. IC(4)) GO TO 135
0104          ZL=RM(4)*X+C(4)
0105          GO TO 136
0106          135 ZL=RM(2)*X+C(2)
0107          136 IF((ZL-DZ*FLOAT(JU-1)) .GT. 0.) GO TO 128
0108          JL=ZL/DZ+1.9999
0109          IF(JU .LT. JL) GO TO 128

```

FORTRAN IV G LEVEL 20.7 VS

GRD2

DATE = 6/07/77

14:32:

```
0110      CALL PD2(A,PX,PZ,PB,PG,PCOS,PSIN,RM,C,NP,NS,N,JL,JU,DB,DG,DZ,X,  
          1DXX,DZZ,I,K,LD,JD)  
0111      128 CONTINUE  
0112      99 RM(1)=RM(2)  
0113      C(1)=C(2)  
0114      IC(1)=IC(3)  
0115      IC(2)=IC(4)  
0116      IC1=IC2  
0117      2 CONTINUE  
0118      CH=1.  
0119      IP=1  
0120      IW=20  
0121      171 IF(ID .GT. IW) GO TO 172  
0122      IW=ID  
0123      CH=0.  
0124      172 WRITE(6,178)  
0125      178 FORMAT(1H1)  
0126      DO 662 J=1,JD  
0127      L=JD+1-J  
0128      662 WRITE(6,3) (A(I,I),I=IP,IW)  
0129      3 FORMAT(1X,20(F5.2,1X))  
0130      IF(CH .EQ. 0.) GO TO 173  
0131      IP=IP+20  
0132      IW=IW+20  
0133      GO TO 171  
0134      173 DO 310 N=1,NP  
0135      CO 310 I=1,NS  
0136      PX(N,I)=PX(N,I)-X0  
0137      310 PZ(N,I)=PZ(N,I)-Z0  
0138      RETURN  
0139      END
```

```

FORTRAN IV G LEVEL 20.7 VS          FD2          DATE = 6/07/77 14:32.
0001      SUBROUTINE PD2(A,PX,PZ,PB,PG,PCOS,PSIN,RM,C,NP,NS,N,JL,JU,DB,DG,
          1CZ,X,DX,DZ,I,K,ID,JD)
0002      DIMENSION A(ID,JD),PX(NP,NS),PZ(NP,NS),PB(NP,NS),PG(NP,NS),
          1PCOS(NP,NS),PSIN(NP,NS),RM(5),C(5)
0003      DO 1 J=JL,JU
0004      IF(J.GT. JD) GO TO 1
0005      IF(J.LT. 1) GO TO 1
0006      Z=DZ*ELCAT(J-1)
0007      PDX=PX(N,K)-PX(N,K+1)
0008      IF(PDX.NE. 0.) GO TO 5
0009      XK1=X
0010      XK=X
0011      ZK1=RM(2)*XK1+C(2)
0012      ZK=RM(1)*XK+C(1)
0013      GO TO 7
0014      5 RM(5)=DZ/DXX
0015      C(5)=PZ(N,K+1)-PX(N,K+1)*RM(5)
0016      CP=Z-X*RM(5)
0017      IF(PSIN(N,K+1).EQ. 0.) GO TO 3
0018      XK1=(C(2)-CP)/(RM(5)-RM(2))
0019      GO TO 4
0020      3 XK1=PX(N,K+1)
0021      4 ZK1=RM(5)*XK1+CP
0022      7 DXK1=XK1-X
0023      DZK1=ZK1-Z
0024      DSB=SQRT(DXK1*DXK1+DZK1*DZK1)
0025      IF(PSIN(N,K).EQ. 0.) GO TO 9
0026      IF(PDX.EQ. 0.) GO TO 10
0027      XK=(C(1)-CP)/(RM(5)-RM(1))
0028      GO TO 11
0029      9 XK=PX(N,K)
0030      11 ZK=RM(5)*XK+CP
0031      10 DXK=XK-XK1
0032      DZK=ZK-ZK1
0033      DSP=SQRT(DXK*DXK+DZK*DZK)
0034      RDSBP=DSB/DSP
0035      XPC=PX(N,K+1)-RDSBP*DXX
0036      ZPC=PZ(N,K+1)-RDSBP*DZZ
0037      DXPC=X-XPC
0038      DZPC=Z-ZPC
0039      DSC=SQRT(DXPC*DXPC+DZPC*DZPC)
0040      B=PB(N,K+1)-RDSBP*DB
0041      AN=(1.-DSC/B)*(PG(N,K+1)+RDSBP*DG)
0042      IF(AN.GT. A(I,J)) A(I,J)=AN
0043      1 CONTINUE
0044      RETURN
0045      END

```

```

0001      SUBROUTINE CONTU(A,B,C,ISET,LIM,NN,IPNT)
0002      DIMENSION A(ISET,1),B(1),C(1)
0003      COMMON/CONTUU/WIT,HITE,KEY(4),HEDN(20),
* XNIN,XNAX,YNIN,YNAX,XOFF,YOFF,XSIZ ,YSIZ ,NCONT ,IFLAG
0004      COMMON/LBLCOM/ITEST,SLBL,STTL,SSCL,STICKL
0005      IF(IPNT.LT.0) GOTO 999
0006      IF(IPNT.GT.0) GOTO 888
0007      IF(NN.EQ.0) NN=-10
0008      NCONT=IABS(NN)
0009      MAX=MAXO(LIM,ISET)
0010      DO 2 I=1,LIM
0011      2 CALL MAXMIN(A(I,I),ISET,C(I),C(LIM+I))
0012      CALL MAXMIN(C,LIM*2,YMAX1,YMIN1)
0013      CALL SCALE(YMAX1,YMIN1,TCP,BCT,NCONT,IERR)
0014      IF(IERR.NE.0) GOTO 1000
0015      CALL MAXMIN(B,NCONT,BMAX,BMIN)
0016      IF(BMAX.LT.YMIN1.OR.BMIN.GT.YMAX1) GOTO 4
0017      IF(NN.GT.0) GOTO 1
0018      4 DELTA=(TOP-BOT)/NCONT
0019      B(1)=BOT
0020      DO 3 I=2,NCONT
0021      3 B(I)=B(I-1)+DELTA
0022      1 IF(IFLAG.NE.0) GOTO 6
0023      ISET1=ISET-1
0024      LIM1=LIM-1
0025      YSIZE=HITE
0026      XSIZE=WIT
0027      XMIN=1.
0028      YMIN=1.
0029      XMAX=ISET
0030      YMAX=LIM
0031      YNAX=YMAX
0032      YNIN=YMIN
0033      XNAX=XMAX
0034      XNIN=XMIN
0035      IF(KEY(2).EQ.1) GOTO 10
0036      DX=XMAX-XMIN
0037      DY=YMAX-YMIN
0038      IF(DX.GT.DY) GOTO 11
0039      DUM=XSIZE
0040      XSIZE=YSIZE
0041      YSIZE=DUM
0042      11 YSIZE=AMIN1(YSIZE,26.)
0043      DX=AMIN1(XSIZE/DX,YSIZE/DY)
0044      XSIZE=DX*(XMAX-XMIN)
0045      YSIZE=DX*(YMAX-YMIN)
0046      10 XBIG=1.3*XSIZE
0047      IF(XBIG.LT.15.) XBIG=15.
0048      IF(XBIG.GT.50.) CALL SYSXMX(XBIG)
0049      YBIG=10.
0050      IF(YSIZE.LE.10.) GOTO 12
0051      YBIG=29.
0052      CALL SYSPSZ(1)
0053      12 YOFF=0.5*IFIX(YBIG-YSIZE)
0054      XOFF=0.5*IFIX(XBIG-XSIZE)+0.5
0055      XD=XSIZE/(XMAX-XMIN)

```

FORTRAN IV G LEVEL 20.7 VS

CGNTU

DATE = 8/03/77

10:14

```

0056      YD=YSIZE/(YMAX-YMIN)
0057      XTOFF=0.1
0058      IF(YSIZE.GT.10.) XTOFF=YSIZE*.01
0059      IF(YSIZE.LT.5..AND.XSIZE.LT.7.5) XTOFF=YSIZE*.02
0060      XTOFF=AMAX1(XTOFF,.05)
0061      ITES=1
0062      SLBL=1.1*XTOFF
0063      STTL=1.2*XTOFF
0064      SSCL=XTOFF
0065      STICKL=STTL
0066      IF(KEY(4).NE.0) STICKL=0
0067      SYMS=0.8*XTOFF
0068      YT =YOFF+YSIZE*XTOFF
0069      IF(YT+STTL.GT.YBIG) YT=YOFF+YSIZE-XTOFF-XTOFF-STTL
0070      XSIZ=XSIZE
0071      YSIZ=YSIZE
0072      IF(LIM.GT.ISET) XSIZ=XSIZ*LIM1/ISET1
0073      IF(ISET.GT.LIM) YSIZ=YSIZ*ISET1/LIM1
0074      CALL LABEL(XOFF,YSIZE+YOFF,XMIN,XMAX,XSIZE,-ISET1,' ',-1,0)
0075      CALL LABEL(XSIZE+XOFF,YOFF,YMIN,YMAX,YSIZE,-LIM1,' ',-1,1)
0076      CALL FINDMT(HEDN(16),MT16,20)
0077      CALL FINDMT(HEDN(11),MT ,20)
0078      CALL LABEL(XOFF,YOFF,XMAX,XMIN,XSIZE,-ISET1,HEDN(16),MT16,0)
0079      CALL LABEL(XOFF,YOFF,YMAX,YMIN,YSIZE,-LIM1,HEDN(11),MT,1)
0080      CALL FINDMT(HEDN,MT,40)
0081      IF(MT.EQ.0) GOTO 6
0082      XBEGIN=XOFF+XTOFF
0083      IF(KEY(3).EQ.0) XBEGIN=XOFF+.5*XSIZE+(.1-.4286*MT)*STTL
0084      CALL SYSSYM(XBEGIN ,YT,STTL,HEDN,MT,0.)
0085      6 IDUM1=1
0086      IDUM2=IDUM1+MAX
0087      IDUM3=IDUM2+MAX
0088      IDUM4=IDUM3+MAX
0089      CALL TOPO(A,B,C(IDUM1),C(IDUM2),C(IDUM3),C(IDUM4),LIM,ISET)
0090      WRITE(6,100) (B(I),I=1,NCONT)
0091      100 FORMAT(' ++ CONTU LEVELS ',8G13.5/(1X)PIOG13.5)
0092      IFLAG=1
0093      IF(KEY(1).NE.0) RETURN
0094      50 CALL SYSPLT(0.,0.,999)
0095      IFLAG=0
0096      RETURN
0097      1000 WRITE(6,1001) YMIN1,YMAX1,NCONT
0098      1001 FORMAT(' ** TROUBLES ** MIN,MAX,NCONTOUR = ',2G13.5,I5)
0099      RETURN
0100      888 IDUM1=IPNT
0101      DO 88 I=1,ISET
0102      XBIG=XOFF+(B(I)-XMIN)*XD
0103      YBIG=YOFF+(A(I,1)-YMIN)*YD
0104      88 CALL SYSSYM(XBIG,YBIG,SYMS,IDUM1,-1,0)
0105      RETURN
0106      999 XBIG=XOFF+(B(1)-XMIN)*XD
0107      YBIG=YOFF+(A(1,1)-YMIN)*YD
0108      CALL SYSPLT(XBIG,YBIG,3)
0109      IDUM1=MAXO(LIM,1)
0110      DO 99 I=1,ISET,IDUM1
0111      XBIG=XOFF+(B(I)-XMIN)*XD

```

FORTRAN IV G LEVEL 20.7 VS

CONTU

DATE = 8/03/77

10:14:

```
0112          YBIG=YOFF+(A(I,1)-YMIN)*YD
0113          99 CALL SYSPLT(XBIG,YBIG,2)
0114          RETURN
0115          END
```

FORTRAN IV G LEVEL 20.7 VS

BLK DATA

DATE = 8/03/77

10:1

```
0001      BLOCK DATA
0002      COMMON/CONTUU/WIT,HITE,KEY(4),HEDN(20),STUFF(9),IFLAG
0003      DATA WIT,HITE,KEY,HEDN/8.,8.      ,4*0,20*1H /
0004      DATA IFLAG/0/
0005      END
```

FORTRAN IV G LEVEL 20.7 VS

TOPO

DATE = 8/03/77

10:14

```

0001      SUBROUTINE TOPO(      V,CNTR,RA,RB,X,Y,M,N)
0002      DIMENSION V(  N ,1),CNTR(1),RA(1),RB(1),X(1),Y(1)
0003      COMMON/CONTUU/SKUPD(26),
*          XMIN,XMAX,YMIN,YMAX,XOFF,YOFF,XSIZ ,YSIZ ,NCONT
0004          SX=XMAX-XMIN
0005          SY=YMAX-YMIN
0006          SMAX=AMAX1(SX,SY)
0007          SMAX1=1./SMAX
0008          SS=SX*SMAX1
0009          SYS=SY*SMAX1
0010          SSS=0.5*SYS
0011          Y1 = SY*SMAX1- .001
0012          X2 = SX*SMAX1- .001
0013          YCCNV=SMAX1
0014          DELTAX=N-1
0015          DELTAX=(XMAX-XMIN)/DELTAX
0016          X(1) = 0.
0017          RB(1) = V(1,1)
0018          DO 27 J=2,N
0019              RB(J)=V(J,1)
0020      27  X(J)=X(J-1)+DELTAX
0021          DELTAY=M-1
0022          DELTAY=(YMAX-YMIN)/DELTAY
0023          Y(1) = 0.
0024          DO 28 J=2,M
0025      28  Y(J)=Y(J-1)+DELTAY
0026          DO 118 K=2,M
0027              DO 30 J=1,N
0028                  RA(J)=RB(J)
0029      30  RB (J)=V(J,K)
0030          DO 118 J=2,N
0031      35  ASSIGN 112 TO L
0032          RR=RA(J)
0033          XX=X(J)
0034          YY=Y(K-1)
0035      37  RL=RR
0036          XL=XX
0037          YL=YY
0038      39  IF(RL.LT.RA(J-1)) GOTO 41
0039      40  IF(RL-RB(J))42,50 ,50
0040      41  RL=RA(J-1)
0041          XL=X (J-1)
0042          YL= Y(K-1)
0043          GO TO 40
0044      42  RL=RB(J)
0045          XL=X (J)
0046          YL=Y(K)
0047      50  RS=RR
0048          XS=XX
0049          YS=YY
0050          IF(RS.GT.RA(J-1)) GOTO 53
0051      52  IF(RS-RB(J)) 60,60,54
0052      53  RS=RA(J-1)
0053          XS=X (J-1)
0054          YS =Y(K-1)
0055          GO TO 52

```


FORTRAN IV G LEVEL 20.7 VS

TOPD

DATE = 8/03/77

10:14:

```

0056      54 RS=RB(J)
0057      XS=X (J)
0058      YS=Y (K)
0059      60 RM=RR
0060      XM=XX
0061      YM=YY
0062      IF (RM-RS) 62,2062,61
0063      2062 IF (XM.EQ.XS .AND. YM.EQ.YS) GO TO 62
0064      61 IF (RM-RL) 70,2065,62
0065      2065 IF(XM.EQ.XL .AND. YM.EQ.YL) GO TO 62
0066      GO TO 70
0067      62 RM=RA(J-1)
0068      XM=X (J-1)
0069      YM=Y (K-1)
0070      IF (RM-RS) 64,2063,63
0071      2063 IF (XM.EQ.XS .AND. YM.EQ.YS) GO TO 64
0072      63 IF (RM-RL) 70,2064,64
0073      2064 IF (XM.EQ.XL .AND. YM.EQ.YL) GO TO 64
0074      GO TO 70
0075      64 RM = RB(J)
0076      XM=X (J)
0077      YM=Y (K)
0078      70 YCS=YS*YCONV
0079      YCM=YM*YCCNV
0080      YCL=YL*YCONV
0081      71 YS=YS-YMAX+YMIN
0082      YM=YM-YMAX+YMIN
0083      YL=YL-YMAX+YMIN
0084      72 XCS=XS*SMAX1
0085      XCM=XM*SMAX1
0086      XCL=XL*SMAX1
0087      NC=1
0088      RC=CNTR(1)
0089      80 IF(NC.GT.NCONT) GOTO110
0090      IF ( RC .NE. RM ) GO TO 91
0091      81 IF ( RM .NE. RS ) GO TO 91
0092      82 IF ( RL .EQ. RM ) GO TO 100
0093      91 IF(RC.LT.RS) GOTO 100
0094      IF(RC-RM)96,93,94
0095      93 XPA=XCM
0096      YPA=YCM
0097      GO TO 99
0098      94 IF(RC-RL)106,103,110
0099      96 Q = (RC-RS)/(RM-RS)
0100      97 XPA = XCS-Q*(XCS-XCM)
0101      YPA = YCS-Q*(YCS-YCM)
0102      99 Q = (RC-RS)/(RL-RS)
0103      XPB = XCS-Q*(XCS-XCL)
0104      YPB = YCS-Q*(YCS-YCL)
0105      IF(RC)10115,10116,10116
0106      10115 XPB1=0.5*(XPA+XPB)
0107      YPB1=0.5*(YPA+YPB)
0108      IF(ABS (XPA-XPB1)-.001)5001,5002,5002
0109      5001 IF(ABS (YPA-YPB1)-.001)100,5002,5002
0110      5002 CALL PLOTZ(XPA,YPA,XPB1,YPB1)
0111      GO TO 100

```

FORTRAN IV G LEVEL 20.7 VS

TOPD

DATE = 8/03/77

10:14

```
0112      10116 IF(ABS (XPA-XPB)-.001)5003,5004,5004
0113      5003 IF(ABS (YPA-YPB)-.001)100,5004,5004
0114      5004 CALL PLOTZ(XPA,YPA,XPB,YPB)
0115      100 RC=CNTR(NC+1)
0116      NC=NC+1
0117      GO TO 80
0118      103 XPA = XCL
0119      YPA = YCL
0120      GO TO 99
0121      106 Q=(RC-RM)/(RL-RM)
0122      XPA=XCM-Q*(XCM-XCL)
0123      YPA=YCM-Q*(YCM-YCL)
0124      GO TO 99
0125      110 GO TO L,(112,118)
0126      112 ASSIGN 118 TO L
0127      RR =RB(J-1)
0128      XX =X (J-1)
0129      YY =Y (K)
0130      GO TO 37
0131      118 CONTINUE
0132      RETURN
0133      END
```

FORTRAN IV G LEVEL 20.7 VS

PLOTZ

DATE = 8/03/77

10:14:

```
0001      SUBROUTINE PLOTZ(X1,Y1,X2,Y2)
0002      INTEGER EC
0003      LOGICAL*1 LXS
0004      DIMENSION X(2),Y(2),LXS(1)
0005      COMMON/CONTUL/SKIUP(26),
*          XMIN,XMAX,YMIN,YMAX,XOFF,YOFF,XSIZE,YSIZE,NCONT
0006      X(1)=XSIZE *X1+XOFF
0007      X(2)=XSIZE *X2+XOFF
0008      Y(1)=YSIZE *Y1+YOFF
0009      Y(2)=YSIZE *Y2+YOFF
0010      CALL SYSPLT(X(1),Y(1),3)
0011      CALL SYSPLT(X(2),Y(2),2)
0012      RETURN
0013      ENTRY FINDMT(LXS,MT,NBT)
0014      MT=NBT
0015      DO 44 J=1,NBT
0016      IF(EC(LXS(MT),' ').EQ.0) RETURN
0017 44  MT=MT-1
0018      RETURN
0019      END
```

LOC	OBJECT CODE	ADDR1	ADDR2	STMT	SOURCE STATEMENT	ASM 0200 10.13 08/03/77
			0000F	2	X15 EQU 15	11
			00000	3	X0 EQU 0	12
			00001	4	X1 EQU 1	13
			00002	5	X2 EQU 2	14
			00003	6	X3 EQU 3	15
			00004	7	X4 EQU 4	16
				8	ENTRY FREEUP	16
				9	GETVEC CSECT	23
0C0000				10	SAVE (14,4),,*	SAVE REGISTERS.
0C0000	47F0 F00C	0000C		11+	B 12(0,15)	BRANCH AROUND ID
000004	06			12+	DC AL1(6)	00860000
000005	C7C5E3E5C5C3			13+	DC CL6*GETVEC*	00880000
0C0008	00					IDENTIFIER
0C000C	90E4 D00C	0000C		14+	STM 14,4,12(13)	SAVE REGISTERS
000010	184F			15	LR X4,X15	01180000
		00000		16	USING GETVEC,X4	SET UP A BASE REGISTER.
000012	1821			17	LR X2,X1	#X4 55
000014	5830 2000	00000		18	L X3,0(,X2)	(X2)= A(PARAMETER LIST).
		00000		19	USING ANCHOR,X3	(X3)= A(ARRAY ANCHOR).
000018	5800 3004	00004		20	L X0,DIMEN	#X3 59
00001C	8800 0002	00002		21	SLA X0,2	(X0)= DIMENSION OF ARRAY.
000020	5000 3000	00000		22	ST X0,LENGTH	(X0)= LENGTH OF ARRAY IN BYTES.
				23	GETMAIN R,LV=(0)	(X1)= A(ARRAY).
0C0024	4510 4028	00028		24+	BAL 1,*,+4	INDICATE GETMAIN
000028	0A0A			25+	SVC 10	ISSUE GETMAIN SVC
0C002A	5010 3004	00004		26	ST X1,LENGTH+4	
00002E	4130 3000	00000		27	LA X3,0(,X3)	(X3)= A(ANCHOR(1)).
000032	1B13			28	SR X1,X3	(X1)= A(ARRAY(1)) - A(ANCHOR(1)).
000034	8A10 0002	00002		29	SRA X1,2	CONVERT TO ARRAY INDEX WITH
000038	4110 1001	00001		30	LA X1,1(,X1)	RESPECT TO THE ANCHOR: *
						ARRAY(1) = ANCHOR(1).
0C003C	5010 3008	00008		31	ST X1,INDEX	PLANT INDEX IN ARRAY ANCHOR.
				32	DROP X3	#X3 70
				33	RETURN (14,4),T,RC=0	71
000040	98E4 D00C	0000C		34+	LM 14,4,12(13)	RETURN TO CALLER.
000044	92FF D00C	0000C		35+	MVI 12(13),X'FF'	RESTORE THE REGISTERS
000048	41F0 0000	00000		36+	LA 15,0(0,0)	SET RETURN INDICATION
00004C	07FE			37+	BR 14	LOAD RETURN CODE
				38	FREEUP SAVE (14,4),,*	RETURN
00004E	47F0 F00C	0000C		39+	FREEUP B 12(0,15)	00800000
000052	06			40+	DC AL1(6)	SAVE REGISTERS.
0C0053	C6D9C5C5E4D7			41+	CC CL6*FREEUP*	124
000059	00					BRANCH AROUND ID
00005A	90E4 D00C	0000C		42+	STM 14,4,12(13)	00860000
0C005E	184F			43	LR X4,X15	00880000
		0004E		44	USING FREEUP,X4	00900000
000060	1821			45	LR X2,X1	SAVE REGISTERS
000062	5830 2000	00000		46	L X3,0(,X2)	01180000
		00000		47	USING ANCHOR,X3	SET UP A BASE REGISTER.
0C0066	9801 3000	00000		48	LM X0,X1,LENGTH	(X2)= A(PARAMETER LIST).
				49	DROP X3	(X3)= A(ARRAY ANCHOR).
				50	FREEMAIN R,LV=(0),A=(1)	#X3 129
0C006A	4111 0000	00000		51+	LA 1,0(1)	(X0,X1)= FREEMAIN PARAMETERS.
00006E	0A0A			52+	SVC 10	130
				53	RETURN (14,4),T,RC=0	131
						RELEASE THE CORE.
						CLEAR THE HIGH ORDER BYTE
						ISSUE FREEMAIN SVC
						RETURN TO CALLER.

C-49

LOC	OBJECT CODE	ADDR1	ADDR2	STMT	SOURCE STATEMENT	ASM 0200 10.13 08/03/77
000070	98E4 D00C	0000C		54+	LM 14,4,12(13)	RESTORE THE REGISTERS 00260000
000074	92FF D00C	0000C		55+	MVI 12(13),X'FF'	SET RETURN INDICATION 00640000
000078	41F0 0000	00000		56+	LA 15,0(0,0)	LOAD RETURN CODE 00700000
00007C	07FE			57+	ER 14	RETURN 00800000
000000				58	ANCHOR DSECT	465
000000				59	DS F	UNUSED WORD. 469
000004				60	DIMEN DS F	BITS/ROW OR # OF FULLWORDS. 470
000008		00000		61	ORG ANCHOR	475
000000				62	LENGTH DS 2F	LENGTH OF THE ARRAY, BYTES. 476
000008				63	INCR DS F	BYTES BETWEEN ROWS IN A BIT * 480
						ARRAY. 481
		00008		64	INDEX EQU INCR	INDEX FROM START OF ANCHOR TO * 482
						START OF ARRAY FOR FULLWORD * 483
						ARRAYS. 484
				65	END	486