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Photocatalytic Concrete Pavements: Laboratory Investigation of NO Oxidation Rate Under Varied Environmental Conditions

Abstract

Concrete pavements containing TiO₂ can be used for air pollution control by oxidizing NO_x under UV-bearing sunlight. This study employed a bench-scale photoreactor to estimate NO oxidation rates for varied environmental conditions. Rates correlated positively with NO inlet concentration and irradiance and negatively with relative humidity. No correlation occurred with flow rate. A decrease in slab moisture (previously unstudied) positively correlated with NO oxidation rate at 0–2% loss of saturated mass, but negatively correlated at losses greater than 2%. Although prior researchers deemed temperature insignificant, data indicated a positive correlation. Overall, rates ranged from 9.8–64 nmol·m⁻²·s⁻¹.

Keywords

photocatalytic pavement, air pollution mitigation, nitrogen oxides, titanium dioxide, photoreactor bench-scale study

Disciplines

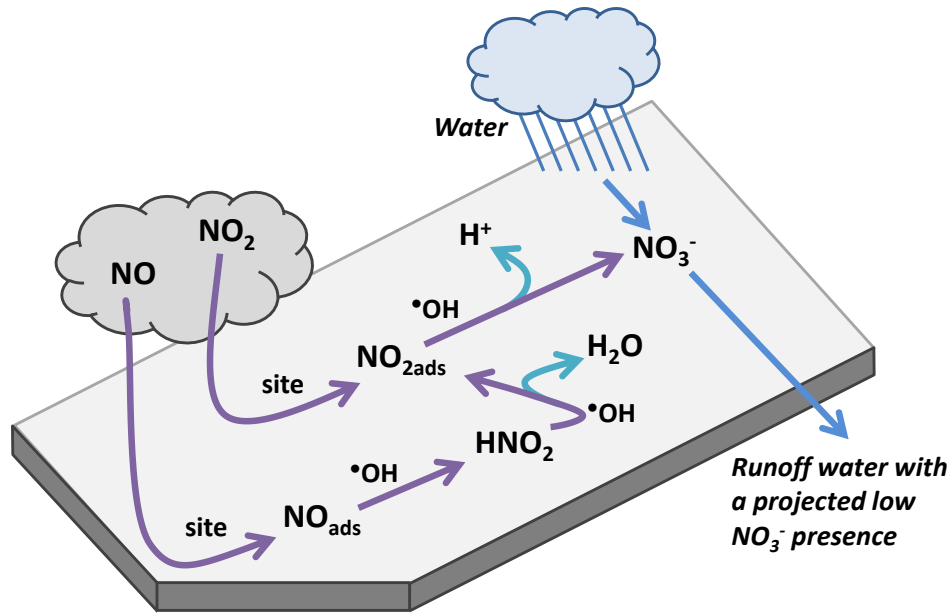
Construction Engineering and Management

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23 NO₂ falls within a group of highly reactive oxides of nitrogen commonly known as NO_x. Nitric oxide
24 (NO) accounts for 95% of NO_x emissions (USEPA, 2001). This pollutant is freely oxidized to NO₂ in the
25 atmosphere; hence, the efforts to abate NO₂ pollution target NO emissions. In fact, due to the high
26 reactivity of the various NO_x species, USEPA assumes all NO_x in emissions estimates to be in the form of
27 NO₂ (USEPA, 2001). USEPA employs various mechanisms in an effort to minimize NO_x exposure (e.g.,
28 improvements in public transportation, establishment of lanes for high occupancy vehicles, facilitating
29 non-automobile travel, and promulgation of tailpipe NO_x emissions standards) (Clean Air Act, 2008;
30 USEPA, 2007). NO_x mitigation strategies are not exempt from the law of diminishing marginal returns;
31 therefore, in addition to efficiently applying conventional mechanisms, novel technologies should be
32 considered. These technologies may yield higher levels of pollution reduction per dollar spent.
33 Photocatalytic pavements represent one of these novel approaches. When exposed to sunlight and in the
34 presence of a low concentration of water molecules, titanium dioxide (TiO₂) contained within these
35 pavements generates hydroxyl radicals (\bullet OH), a powerful oxidizing agent. These radicals promote the
36 oxidation of a variety of organic and inorganic pollutants. Notably, the photocatalytic property of these
37 pavements results in oxidation of NO_x to NO₃⁻ (Figure 1).



38

39 **Figure 1. Photocatalytic oxidation of NO and NO₂ by pavement containing TiO₂ (partially adapted from**
 40 **Ballari et al., 2011).**

41 Employment of these pavements as a mechanism to minimize the ambient concentration of NO in a
 42 targeted area will require an extensive development of what is known about NO oxidation rates under
 43 varied environmental conditions. In an effort to provide this new knowledge, various researchers have
 44 published accounts of laboratory studies that evaluated photocatalytic pavement specimens within a
 45 photoreactor, an experimental apparatus that allows for the control of various environmental conditions
 46 (Dylla et al., 2010; Hüsken et al., 2009; Murata & Tobinai, 2002). Independent environmental variables
 47 investigated have included NO concentration, irradiance, test gas flow rate, and relative humidity.
 48 Although material variables, such as TiO₂ concentration and type, will also play a role, environmental
 49 variable results presented to date have not brought about a consensus in terms of the range in NO
 50 oxidation rates that can be expected. Murata et al. (2000), Hüsken et al. (2009), and Ballari et al. (2011)
 51 each suggest that NO oxidation rates positively correlate with NO concentration in situations when the
 52 photocatalytic surface was not saturated by NO; however, for tests conducted at the same environmental

53 conditions (1.0 ppmv , $10 \text{ W}\cdot\text{m}^{-2}$, $3 \text{ L}\cdot\text{min}^{-1}$, $50\% \text{ RH}$) the range in oxidation rates was wide ($38\text{--}84 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$).
54 Similarly, publications have noted a positive correlation between irradiance and oxidation rate, but
55 at $10 \text{ W}\cdot\text{m}^{-2}$ calculated oxidation rates were $87 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$ for Murata et al. (2000) and $24 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$
56 for Hüsken et al. (2009). Both Murata et al. (2000) and Hüsken et al. (2009) observed a negative correlation
57 between relative humidity and oxidation rate; however, at 50% relative humidity oxidation rates differed
58 by $22 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}$. These prior studies have assumed that water vapor from the atmosphere serves as
59 both the source of $\bullet\text{OH}$ required for photocatalytic oxidation and the material which adsorbs on the
60 surface and blinds photocatalytically active sites. Yet, given the porous nature of cementitious mixtures,
61 water contained within a pavement could also serve as a $\bullet\text{OH}$ source and blinding material. At the time of
62 placement, these pores can become filled with water. As hydration occurs and pores become filled with
63 air, water that is available as a $\bullet\text{OH}$ source and blinding material decreases. Therefore, a decrease in
64 moisture contained in the slab could lead to either an increase or decrease in the NO oxidation rate of
65 the slab; however, no lab investigation has tested this hypothesis. Hüsken et al. (2009) observed a positive
66 correlation between percent NO removal (as opposed to NO oxidation rate) and flow rate (slope of a linear
67 fit was less than -10). This finding was also reported in Ballari et al. (2010), however in this case slope was
68 only slightly less than -1 . Finally, a review of the fundamentals of heterogeneous catalysis indicates that,
69 due to the fact that reactant adsorption is dependent on temperature, oxidation rate appears to be
70 correlated with temperature (Herrmann, 2010). However, literature pertaining to photocatalytic
71 pavements is both vague and contradictory in terms of the relationship between slab temperature and
72 NO oxidation, with one source asserting that oxidation rate increases with an increase in temperature
73 (Beeldens et al., 2011) and another reporting a decrease in oxidation rate with increased temperature
74 (Chen & Chu, 2011).

75 Consequently, this study employed TX Active mortar slabs and a photoreactor to evaluate the change
76 in NO oxidation rate that occurs with changes in NO concentration, irradiance, test gas flow rate, relative

77 humidity, decrease in slab moisture, or temperature. In instances when published photocatalytic
78 pavement data existed, the data collected in this study was compared with data published by other
79 researchers in order to draw conclusions in regards to the range of NO oxidation rates that could be
80 expected and the variation that occurs between specimens.

81 2. Materials and Methods

82 2.1. Photocatalytic Mortar Slab Preparation and Cleaning

83 Three photocatalytic mortar slabs were used to evaluate this study's objectives. These slabs measured
84 152 mm (6 in) × 152 mm (6 in) × 25 mm (1 in). For this study, the researchers used a commercially-available
85 cement that contains TiO₂ (TX Active, Essroc Italcementi Group, Nazareth, PA). Although, the TiO₂ content
86 in this cement was not provided by the manufacturer, within patents governing photocatalytic cements,
87 TiO₂ content ranges from 2–10% by mass (Paz, 2010). The proportions of the cement (TX Active or Type
88 I), water, and fine aggregate (ASTM C778 standard sand, U.S. Silica Co., Frederick, MD) were recorded as
89 624 kg·m⁻³ (1052 lb·yd⁻³), 262 kg·m⁻³ (442 lb·yd⁻³), and 1412 kg·m⁻³ (2380 lb·yd⁻³) respectively. Given the
90 cement proportion and the range in TiO₂ cement content above, estimated TiO₂ content of the mortar
91 was 12.5–62.4 kg·m⁻³. Given the small volume of the slabs constructed, the mix did not include coarse
92 aggregate. Except for the coarse aggregate, the relative proportions of materials used to manufacture the
93 laboratory mortar slabs were similar to that of a pavement section placed at a field site, which will be
94 evaluated in future research efforts (*citation removed to ensure blind review*). Particular care was taken
95 to use the same water-to-cement ratio for both lab and field mixtures. During the placement process, a
96 paste of water and photocatalytic cement coats aggregates and when hardened forms the surface that is
97 exposed to pollutants. To manufacture the slabs, a two-lift procedure was used with equal volumes of a
98 Type I cement bottom lift followed by a TX Active photocatalytic cement top lift. A possibility exists that
99 excess vibration and surface finishing could draw water to the surface, thereby reducing the TiO₂
100 concentration. To minimize this possibility the material was consolidated by tapping the sides of the form

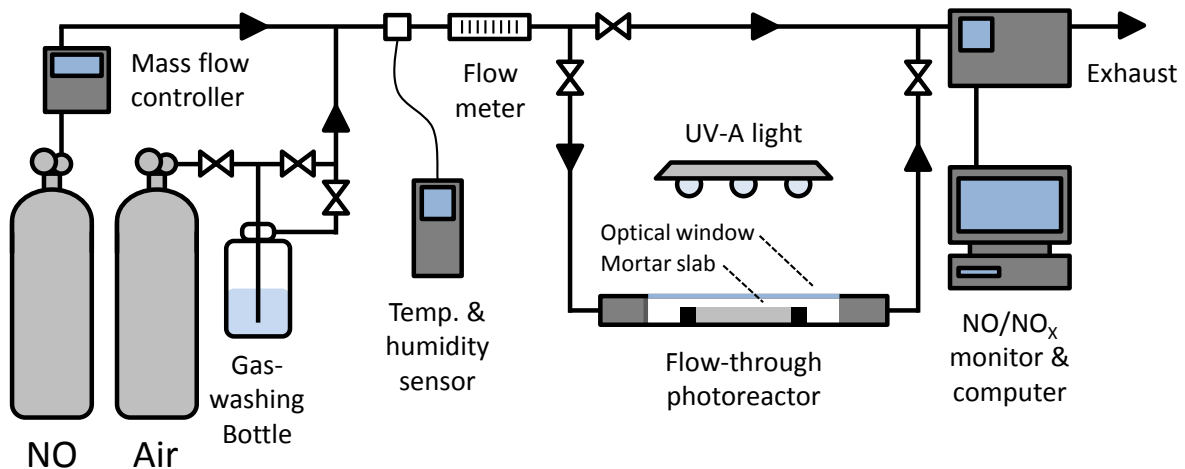
101 with a mallet and leveled with use of a screed. Following placement, a damp cloth and plastic sheet were
102 laid over the slab surface for a 24-h curing period. Following this initial curing period, the slabs were
103 removed from the forms and placed in a 100% relative humidity room for the duration of a 14-d curing
104 period.

105 Prior to evaluating NO oxidation rates (described in Section 2.3), slabs were cleaned by immersion in
106 water (Type I reagent grade) for 2 h and oven-dried at 60°C (140°F) for 20 h. This procedure was similar
107 to that specified by the International Organization for Standardization (ISO) standard 22197-1:2007(E);
108 this standard governs evaluation of NO removal by photocatalytic materials (ISO, 2007).

109 *2.2. Experimental Apparatus*

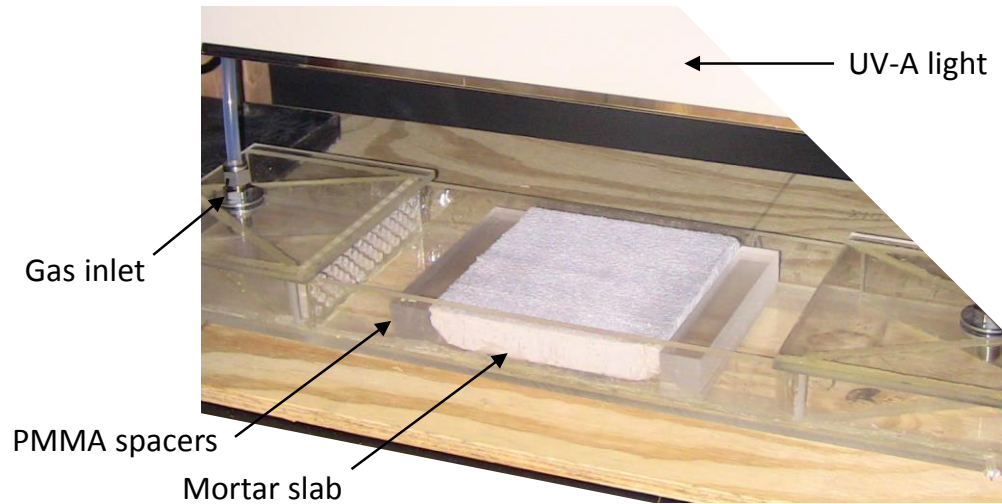
110 A flow-through poly(methyl methacrylate) (PMMA, i.e., plexiglass) photoreactor served as the primary
111 component of the experimental apparatus. Figure 2 provides a schematic of the photoreactor, along with
112 the NO test gas supply system, UV-A light source, and NO/NO_x monitor. The international standard, ISO
113 22197-1:2007(E), provided information on the construction and operation of the setup (ISO, 2007). The
114 test gas supplied to the photoreactor was a mixture of breathing air (Grade D, Airgas USA, LLC, North
115 Central Region, West Chicago, IL) and 51.6 ± 1% ppmv NO balanced in nitrogen (EPA protocol gas, Praxair,
116 Inc., Danbury, CT) adjusted to a NO concentration of 0.11–1.0 ppmv, relative humidity of 10–70%, and
117 flow rate of 1.5–5.0 L·min⁻¹. A UV-A light (XX-15BLB, Ultra-Violet Products, LLC, Upland, CA), directed at
118 the UV-A-transparent optical window located at the top of the photoreactor, activated the photocatalytic
119 properties of the mortar slab. The primary emissions spectrum peak from the light was 365 nm. At the
120 location of the slab surface, the irradiance at 365 nm was measured to be 0.22–1.5 x 10¹ W·m⁻² using 365
121 nm UV sensor and radiometer (CX-365 and VLX-3W, Vilber Lourmat, Marne-la-Vallée, France). Except for
122 instances when temperature was investigated as an independent variable, slab temperature was room
123 temperature (approximately 22°C).

124 As displayed in Figure 3, within the reactor, 25 mm (1 in) wide PMMA spacers secured the slab's
 125 position and were set at a height that was either flush with or less than 2 mm below the slab surface.
 126 Within the 300 mm long reactor, the gas flowed over the slab through a cross section with a width of 150
 127 mm (6 in) and a height (H) of approximately 6 mm (0.25 in). Turbulent airflow over the slab would
 128 introduce additional variability in the test. Using the approach detailed in Hüsken et al. (2009), Reynolds
 129 number (Re) was calculated to be 42.6 using an air kinematic viscosity of $1.54 \times 10^{-5} \text{ m}^2 \cdot \text{s}^{-1}$ ($1.66 \times 10^{-5} \text{ ft}^2 \cdot \text{s}^{-1}$)
 130 and an air flow rate of $3 \text{ L} \cdot \text{min}^{-1}$ ($0.8 \text{ gal} \cdot \text{min}^{-1}$). The length (L_d) for a parabolic velocity profile in the
 131 photoreactor was estimated to be approximately 27.1 mm (1.1 in) by the following equation: $L_d = 0.1 \cdot Re \cdot H$.
 132 The estimated length was slightly longer than the length of the PMMA spacers, which indicates that
 133 approximately 1.1% of the slab surface did not have a fully developed parabolic velocity profile. At $3 \text{ L} \cdot \text{min}^{-1}$
 134 ¹, theoretical retention time of the test gas within the photoreactor was estimated to be 38 s. Theoretical
 135 retention time of the test gas in the volume above the slab at $3 \text{ L} \cdot \text{min}^{-1}$ was estimated to be 2.7 s.



136

137 **Figure 2. Diagram of experimental apparatus (partially adapted from Ballari et al., 2011).**



138

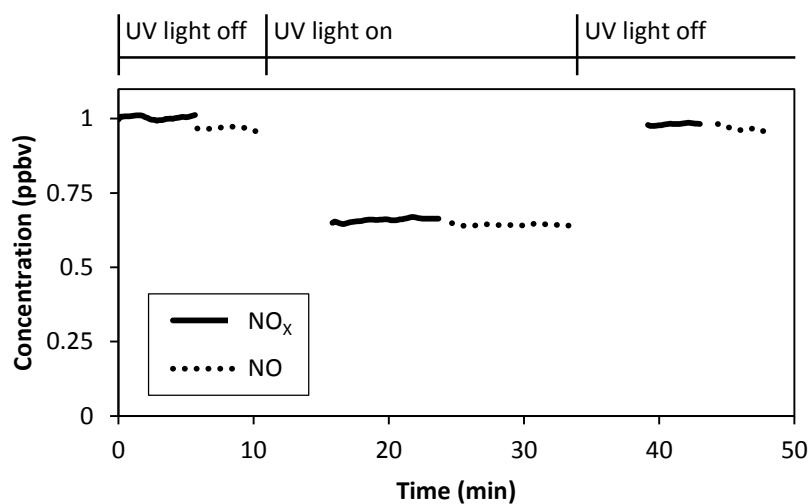
139 **Figure 3. Photograph of photoreactor and mortar slab (optical window removed to facilitate viewing).**

140 A NO/NO_x monitor, (Model 410 Nitric Oxide Monitor and Model 401 NO₂ Converter, 2B Technologies,
141 Inc., Boulder, CO), completed the experimental apparatus. The monitor recorded the gas concentrations
142 at 10 s intervals and was set to measure either NO or NO_x. Unlike chemiluminescence instruments, which
143 detect the light produced when NO reacts with ozone (O₃), the Model 410 measures the change in UV
144 absorbance at 254 nm when O₃ is consumed upon reaction with NO. UV absorbance is an absolute
145 method; therefore, the analyzer requires calibration annually to correct for non-linearity that exists in the
146 photodiode response and associated electronics.

147 *2.3. Operational Procedure*

148 Operation of the experimental apparatus was divided into two phases: parameter setting and testing.
149 While in the parameter setting phase, the test gas flowed through the photoreactor; however, the slab
150 was not irradiated by UV light. This phase was used to set airflow rate, relative humidity, and pollutant
151 concentration and lasted for approximately 10 minutes. After adjusting parameters to desired values, gas
152 flow was maintained through the photoreactor for a period sufficient to reach steady-state conditions.

153 The testing period comprised two steps during which the UV light was turned off and on and
154 concentrations of NO and NO_x were measured. Figure 4 illustrates the UV on and off measurement cycle.
155 Time to complete this cycle was limited to 60 minutes to minimize the possible influence of slab
156 degeneration (e.g., due to the adsorption of reaction products) on collected data. Of note, a gap occurred
157 between measurement of UV light on and off segments. The change in concentration that occurred when
158 the light was turned on or off was not instantaneous. The period between measurements permitted time
159 for concentration stabilization after each parameter change. In some instances, the time gap was not
160 sufficient for concentration stabilization. When analyzing the data strings, these values were identified
161 and removed. The study also did not evaluate adsorption of NO that could occur on the slab or on other
162 surfaces within the photoreactor; rather, in similarity to other studies, this research focused on NO
163 removal that occurred as result of irradiance by UV light (Ballari et al., 2011, Hüsken et al. 2009).



164

165 **Figure 4. Typical NO/NO_x monitor data from testing procedure.**

166 An alternative approach to test for photocatalytic oxidation is to measure NO concentration as the
167 test gas first flows through a bypass line and then is diverted to flow through the photoreactor. With this
168 approach a portion of the decrease in concentration that occurs as the gas flows through the photoreactor
169 could be due to adsorption on the slab and dilution by air leakage. Measuring the difference in

170 concentration between UV-off and -on periods avoided these error sources and limits the source for a
171 change concentration to photo-oxidation and photo-dissociation. To evaluate whether photo-dissociation
172 occurred within the photoreactor, the researchers also evaluated a slab that was not manufactured with
173 photocatalytic cement (see Control in Table 1). A two-tailed t -test, assuming unequal variances, did not
174 find evidence of a significant difference between average UV-off and UV-on NO concentration at 90%
175 confidence ($t=3.019$, $df = 4$, $p = 0.039$).

176 *2.4. Variable Control and Measurement for Completed Tests*

177 To evaluate the objectives listed above, the study collected data on the NO oxidation rates of
178 photocatalytic mortar slabs under varied environmental conditions. In some cases, NO_x oxidation rates
179 were also collected. The following environmental variables were considered: NO concentration ($C_{UV\ off}$),
180 irradiance ($Irrad.$), test gas flow rate (Q), relative humidity (RH), decrease in slab moisture, and slab
181 temperature ($Temp$). Table 1 presents values of these variables for the tests of NO concentration,
182 irradiance, test gas flow rate, relative humidity, and slab temperature. For these tests, at the initial
183 measurement (Test ID 0), all variables were set at the values specified by ISO 22197-1:2007(E) (i.e., $C_{UV\ off}$
184 = 1.0 ppmv, $Irrad.$ = 10 W·m⁻², Q = 3.0 L·min⁻¹, RH = 50%). In subsequent tests, each independent variable
185 was decreased or increased from the ISO-specified values in order to evaluate the change in NO and NO_x
186 oxidation. To facilitate comparison to other published work, selected values of these variables were
187 similar to values reported in said studies.

Table 1. Environmental conditions and results of tests completed.

Test #	Slab ID	Description	Environmental conditions								Results					
			C _{UV off}				Irrad.	Q	RH	Slab temp.	C _{UV on}				Oxidation rate	
			(ppmv)		(ppmv)		(W·m ⁻² × 10 ¹)	(L·min ⁻¹)	(%)	(°C)	(ppmv)		(ppmv)		(nmol·m ⁻² ·s ⁻¹)	
NO _x		NO						NO _x		NO		NO _x	NO			
		̄	s	̄	s					̄	s	̄	s			
0		Control			1.1	0.00067	1.0	3.0	50	22 ¹			1.1	0.0033	0.36	
0	1	Initial	1.0	0.0039	1.0	0.0046	1.0	3.0	50	22 ¹	0.71	0.0022	0.64	0.00054	34	42
1	1	Δ conc.	0.12	0.014	0.11	0.011	1.0	3.0	50	22 ¹	0.068	0.00062	0.043	0.0019	6.5	9.8
2	1	Δ conc.	0.31	0.013	0.30	0.010	1.0	3.0	50	22 ¹	0.19	0.00055	0.15	0.00063	15	19
3	2	Δ irradi.	1.0	0.0030	1.0	0.0036	0.22	3.0	50	22 ¹	0.93	0.00035	0.89	0.00030	7.5	10
4	2	Δ irradi.	1.0	0.0054	1.0	0.012	0.40	3.0	50	22 ¹	0.88	0.00030	0.83	0.00031	11	15
5	2	Δ irradi.	1.0	0.0015	1.0	0.0029	0.70	3.0	50	22 ¹	0.88	0.0011	0.82	0.0015	15	20
6	2	Δ irradi.	1.0	0.0060	1.0	0.0034	1.0	3.0	50	22 ¹	0.86	0.0012	0.79	0.00041	17	25
7	2	Δ irradi.	1.0	0.0049	1.0	0.0051	1.5	3.0	50	22 ¹	0.76	0.0013	0.69	0.0012	27	34
8	1	Δ Q	1.0	0.020	1.0	0.016	1.0	1.5	50	22 ¹	0.58	0.0018	0.51	0.00055	28	33
9	1	Δ Q	1.0	0.0075	1.0	0.0068	1.0	5.0	50	22 ¹	0.84	0.0036	0.79	0.00055	27	35
10	1	Δ RH	1.0	0.0054	1.0	0.011	1.0	3.0	10	22 ¹	0.55	0.0021	0.50	0.0017	59	64
11	1	Δ RH	1.0	0.0037	1.0	0.0041	1.0	3.0	20	22 ¹	0.59	0.0024	0.52	0.00083	52	61
12	1	Δ RH	1.0	0.0034	1.0	0.0044	1.0	3.0	70	22 ¹	0.80	0.0025	0.73	0.00069	23	28
13	3	Δ temp.			1.0	0.0003	1.0	3.0	20	55			0.72	0.0041	30	
14	3	Δ temp.			1.0	0.0024	1.0	3.0	20	49			0.72	0.0049	31	
15	3	Δ temp.			1.0	0.0005	1.0	3.0	20	44			0.78	0.0060	26	
16	3	Δ temp.			1.0	0.0010	1.0	3.0	20	39			0.70	0.0022	25	
17	3	Δ temp.			1.0	0.00073	1.0	3.0	20	36			0.69	0.0029	27	
18	3	Δ temp.			0.92	0.0017	1.0	3.0	20	34			0.70	0.0016	22	
19	3	Δ temp.			0.92	0.0013	1.0	3.0	20	32			0.73	0.0054	18	
20	3	Δ temp.			0.92	0.0077	1.0	3.0	20	19			0.73	0.0079	19	
21	3	Δ temp.			0.88	0.0019	1.0	3.0	20	21			0.71	0.0013	17	
22	3	Δ temp.			0.94	0.0018	1.0	3.0	20	22			0.78	0.0022	16	
23	3	Δ temp.			1.0	0.0018	1.0	3.0	20	7.1			0.85	0.0041	13	
24	3	Δ temp.			1.0	0.0013	1.0	3.0	20	13			0.81	0.0021	16	
25	3	Δ temp.			1.0	0.0011	1.0	3.0	20	15			0.81	0.0042	14	

¹slab temperature not measured during test; room temperature assumed

190 *2.4.1. NO concentration, irradiance, test gas flow rate, and relative humidity*

191 Needle valves and a mass flow controller permitted control of NO concentration, test gas flow rate,
192 and relative humidity. To control irradiance the distance between the UV light and photoreactor optical
193 window was varied until the target value was observed on the radiometer at the height of the slab surface.

194 *2.4.2. Slab temperature*

195 Prior to evaluation in the photoreactor, a pre-cleaned slab (procedure in Section 2.1) was brought to
196 an initial temperature that was either above or below room temperature. To obtain this initial
197 temperature, a slab was placed in either an oven (60°C) or a refrigerator (2-4°C) for a period of 2 h. After
198 removal from the oven or refrigerator, the slab was immediately loaded into the photoreactor. An infrared
199 thermometer (15-077-966, Thermo Fisher Scientific, Waltham, MA) recorded temperature at 5 points on
200 the slab surface (the slab center and the center of each quadrant) immediately prior to and after
201 photoreactor evaluation. If slab temperature was greater than room temperature, photocatalytic
202 evaluation began after temperature recording. When slab temperature is less than the test gas
203 temperature (22°C), the possibility of water vapor condensation—which would blind photocatalytically
204 active sites—must be considered because this condensation would falsely indicate reduced photo-
205 activity. This error can be minimized by ensuring that the lowest slab temperature is substantially above
206 the dew point temperature of the test gas. To create a substantial difference between temperatures, the
207 researchers selected a 20% relative humidity for the test gas (dew point = -2°C). As a result, even if the
208 test gas air cooled 5°C as it flowed over a cool slab, relative humidity would only increase to 60% and
209 saturation of the test gas would not occur. To further minimize this potential error, the researchers
210 attempted to evaporate condensed water by using valves to reduce the test gas relative humidity to 0%
211 for a 10 minute period. Following this period, the UV light was turned on, relative humidity was increased
212 to the target value (20%), and photocatalytic evaluation began. The possibility exists that the effort to

213 avoid error by water condensation was unsuccessful. This possibility was evaluated by comparing the
214 slope of the NO oxidation rate versus temperature line for observations below and above 22°C (Section
215 3.1.6). It must also be noted, that in this portion of the study, the researchers sought to ensure that water
216 vapor density remained constant throughout the tests, rather than relative humidity. To achieve this
217 goal, relative humidity was set in reference to the test gas temperature, which remained constant, rather
218 than the variable slab temperature.

219 Additional NO oxidation rate evaluations were completed in succession as the slab temperature
220 increased or decreased. Three sets of successive tests were recorded at the following temperature
221 classifications: hot (32–55°C, Test IDs 13–19), warm (19–22°C, Test IDs 20–22), and cool (7.1–15°C, Test
222 IDs 23–25) as shown in Table 1. Conducting successive tests could lead to a decrease in reactivity over
223 time; therefore, the testing period was reduced such that the total testing time for the hot, warm, and
224 cool classifications was 90, 40, and 40 minutes, respectively. Slab temperature was not measured at the
225 midpoint of each test; instead, this value was estimated. The temperature and time data collected during
226 the hot ($n = 40$), warm ($n = 20$), and cold ($n = 20$) sets of successive tests fit power law curves when
227 adjusted for asymptotic values ($R^2 > 0.95$ for each set). For example, temperature for the hot classification
228 was estimated using the following equation: $T = 5 \times 10^{-5} \cdot [(t + 647)/1440]^{-16.76} + 28$ ($T =$
229 *temperature in °C*, $t =$ *elapsed time in minutes*, $R^2 = 0.99$). These curves were used to estimate
230 slab temperature at the midpoint of the photoreactor test.

231 2.4.3. Decrease in slab moisture

232 To evaluate the effect of a decrease in slab moisture, NO oxidation was periodically evaluated as water
233 content decreased after starting at a saturated state. For these tests, NO concentration was set to 1.0
234 ppmv, flow rate to 3 L·min⁻¹, relative humidity to 20% and UV-A irradiance to 10 W·m⁻² at 365 nm. In
235 similarity with the approach used in Section 2.4.2, a constant vapor density was ensured by setting relative

236 humidity in reference to the test gas temperature. To achieve saturation, a slab was immersed in water
 237 for 24 h. To promote a decrease in slab moisture, the slab was placed in a 60°C oven. The slab was
 238 periodically removed from this oven in order to measure slab mass and NO oxidation rate. Testing
 239 continued for the duration of 48 h. The decrease in slab moisture was presented as a percentage using
 240 the mass at the point of saturation and the calculated moisture loss (i.e., the difference in mass at
 241 saturation and at the point of photoreactor evaluation).

242 2.5. Presentation of Results

243 Other published works present NO removal as a percentage based on the difference between UV-off
 244 and -on concentrations of NO. Percent removal data is in part a function of lab setup (e.g., slab
 245 dimensions). Presenting results in this manner can lead to misperceptions if, for example, results are not
 246 normalized by area. In this research results are presented as the average NO oxidation rate in the reactor
 247 volume using the equation given by Minero et al. (2013):

$$248 \quad NO \text{ oxidation rate} = \frac{P}{R \cdot T} \cdot \frac{Q}{A} \cdot C_{UV \text{ off}} \cdot \ln\left(\frac{C_{UV \text{ off}}}{C_{UV \text{ on}}}\right) = \left[\frac{nmol}{m^2 \cdot s}\right]$$

249 where,

$$250 \quad P = \text{atmospheric pressure} = 101.3 \text{ kPa},$$

$$251 \quad R = \text{ideal gas constant} = 8.314 \times 10^{-12} \text{ m}^3 \cdot \text{kPa} \cdot \text{nmol}^{-1} \cdot \text{K}^{-1},$$

$$252 \quad T = \text{temperature} = [K],$$

$$253 \quad Q = \text{volumetric flow rate} = [m^3/s]$$

$$254 \quad A = \text{slab surface area} = 0.023 \text{ m}^2,$$

$$255 \quad C_{UV \text{ off}} = \text{NO concentration with UV light off} = [ppmv], \text{ and}$$

$$256 \quad C_{UV \text{ on}} = \text{NO concentration with UV light on} = [ppmv].$$

257 The recorded test gas temperature was used to calculate oxidation rate for evaluations of NO
258 concentration, irradiance, flow rate, and relative humidity. Due to the low mass flow rate ($5.6 \times 10^{-5} \text{ kg}\cdot\text{s}^{-1}$) and specific heat of air ($1.007 \text{ kJ}\cdot\text{kg}^{-1}\cdot\text{°C}^{-1}$), evaluations of slab temperature and slab moisture assumed
259 that the test gas temperature was the same as the slab temperature.
260

261 3. Results and Discussion

262 3.1. NO Oxidation Rate for Tests Completed

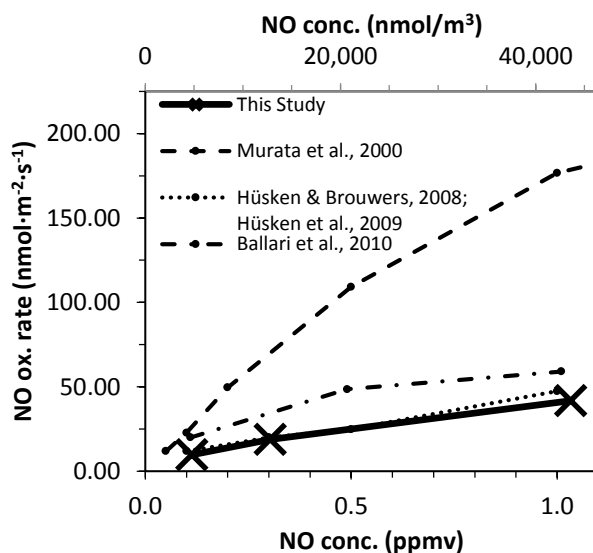
263 Table 1 documents the environmental parameters and oxidation rate results of the tests completed
264 for this study. Of note, in each instance the value of NO oxidation rate is greater than that of NO_x oxidation
265 rate. It could be expected that since the test gas supply to the reactor was nearly entirely comprised of
266 NO, then the NO and NO_x removal values would be the same value. The discrepancy arises because NO is
267 not oxidized completely to HNO₃. Rather, a portion of the gas is transformed to NO₂. NO₂ that remained
268 in the gas stream was counted as part of the outlet NO_x concentration. As a result, NO_x removal measured
269 lower than NO removal.

270 In this study, all slabs were prepared with the same procedure, materials, and proportions but in
271 different batches. Review of Table 1 finds that although Tests IDs 0 and 6 were evaluated at the same
272 environmental conditions, the observed NO oxidation rate differed by 51% from the mean. This difference
273 may be due to several non-obvious factors within the mixing, placement, and curing steps. Prior research
274 also indicated that oxidation rate differences may occur between slab replicates. For example, Hüsken et
275 al. (2009) found that the percent difference of degradation rates for various replicates of photocatalytic
276 pavement materials varied from as low as 0% to as high as 63%. Noting that differences did occur between
277 slab replicates, Figures 5 to 9 plot each independent variable versus NO oxidation rate for a selected slab.
278 To place this study's observations in context, overlaid on these plots are the data reported from previous

279 research that investigated NO oxidation rates under differing environmental conditions (Ballari et al.,
 280 2010; Ballari et al., 2011; Hüsken & Brouwers, 2008; Hüsken et al., 2009; Murata et al., 2000).

281 3.1.1. Influent NO Concentration

282 Figure 5 indicates a correlation between inlet NO concentration and NO oxidation rate ($R^2 = 0.994$)
 283 This correlation is also evident in the data from Murata et al. (2000) ($R^2 = 0.984$ for 0–1.0 ppmv, $R^2 = 0.802$
 284 for 0–5.0 ppmv), Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($R^2 = 0.991$), and Ballari et al.
 285 (2010) ($R^2 = 0.882$).



286

287 **Figure 5. Effect of influent NO concentration on NO oxidation rate.**

288 A correlation between inlet concentration and NO oxidation rate was previously reported by
 289 Herrmann (1999). This publication indicated that kinetics follow a Langmuir-Hinshelwood mechanism,
 290 under which both reactants adsorb (e.g., NO and \bullet OH) on the surface before a new molecule is formed.
 291 For these type of reactions, kinetics typically fell into low-concentration and high-concentration
 292 classifications. In the low-concentration classification, oxidation kinetics were first-order; whereas in the
 293 high-concentration classification, oxidation kinetics were zero-order. As applied to NO degradation by

294 photocatalytic pavements, this framework would indicate that, at high concentration, the rate of NO
295 oxidation would remain constant. A constant oxidation rate occurred because a finite number of active
296 sites were available for photocatalytic degradation. Once these sites were occupied, the rate of oxidation
297 did not increase. In contrast, while within the low-concentration classification, the active sites had not yet
298 been filled (Herrmann 1999).

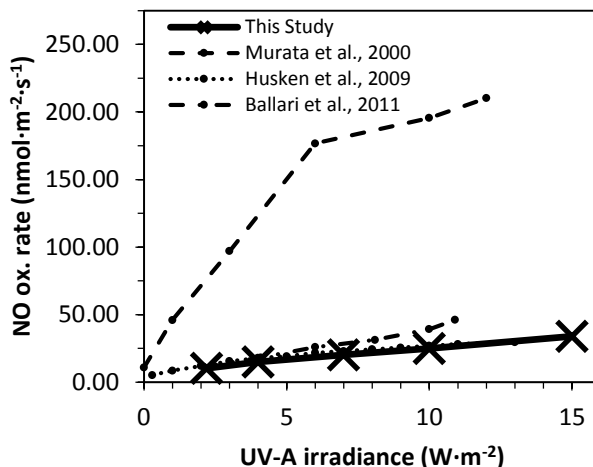
299 For reactants adsorbed from aqueous phases, Herrmann (1999) indicated that a first-order kinetics
300 apply when concentration is less than 10^{-3} M and zero-order kinetics apply at a concentration greater than
301 5×10^{-3} M. These divisions have not been established for reactants adsorbed from a gas phase. Except for
302 Ballari et al. (2010), which only had 3 observations, *t*-tests of the data presented in Figure 5 rejected a null
303 hypothesis that slope equaled $0 \text{ nmol m}^{-2}\text{-s}^{-1}\text{-ppmv}^{-1}$ ($p = <0.033$). Based on this analysis, it is evident that
304 this data falls into first-order oxidation kinetics, indicating that active sites have not been filled. For
305 applications of photocatalytic pavement, a determination of where the breakpoint between first- and
306 zero-order oxidation kinetics occurs is not necessary. Locations where these pavements may be installed
307 can be assumed to have NO_x concentrations near the National Ambient Air Quality Standards (NAAQSs)
308 for NO₂ (i.e., 53 and 100 ppbv) (Primary National Ambient Air Quality Standards for Nitrogen Dioxide: Final
309 Rule, 2010). These values are substantially below the 1.0 ppmv upper limit of the data analyzed; therefore,
310 field applications can also be assumed to be characterized by first-order oxidation kinetics.

311 In addition to finding evidence that influent NO concentration affects NO oxidation rates, a *t*-test
312 which compared the slope of linear regression lines for the presented data sets found no significant
313 difference between this study's data and the data from Hüsken and Brouwers (2008) and Hüsken et al.
314 (2009) ($t = -1.429$, $df = 3$, $p = 0.248$), and Ballari et al. (2010) ($t = -0.515$, $df = 2$, $p = 0.658$). A similar *t*-test
315 did find that the slope was significantly different than the 0–1.0 ppmv data from Murata et al. (2000) ($t =$
316 -10.834 , $df = 4$, $p = 0.000$). Review of Murata et al. (2000)'s writing found that the reactor setup was not

317 markedly different than that of the authors'; therefore, material characteristics are also likely to influence
318 the activity of photocatalytic pavements. More broadly, it can be concluded that because these slopes are
319 significantly different, a generalized assumption of the effect of NO concentration on NO oxidation rate
320 cannot be made. Instead, if a photocatalytic material is to be used in the field, it would be wise to complete
321 lab evaluations in order to project levels of oxidation that could be observed in the field.

322 3.1.2. UV-A Irradiance

323 Figure 6 indicates a positive correlation between UV-A irradiance and NO oxidation ($R^2 = 0.996$). This
324 correlation is also evident in the data from Murata et al. (2000) ($R^2 = 0.910$), Hüsken et al. (2009) ($R^2 =$
325 0.940), and Ballari et al. (2011) ($R^2 = 0.986$). This positive correlation exists because increased UV-A
326 irradiance on a photocatalytic surface increases the rate at which electron holes are created. An increase
327 in the rate of electron-hole generation results in the increased production rate of hydroxyl radicals, which
328 oxidize NO. Multiple publications report that the relationship between irradiance and pollutant oxidation
329 can be divided into two classifications. Although disagreement exists on the value of the division point
330 between classes ($10\text{--}250\text{ W}\cdot\text{m}^{-2}$), the publications note a linear relationship below the division point and
331 a non-linear relationship above this point (Herrmann et al., 2007; Jacoby et al., 1995; Kumar et al., 1995;
332 Lim et al., 2000; Obee & Brown, 1995). Jacoby et al. (1995) explains that under the linear classification,
333 electron holes are filled by reactions with species on the photocatalytic surface (e.g., OH^\cdot) faster than by
334 recombination with excited electrons; in contrast, under the non-linear classification, holes are filled by
335 recombination at a faster rate than by reaction with other species.



336

337 **Figure 6. Effect of UV-A irradiance on NO oxidation rate [Ballari et al. (2011) collected data at 0.52**
 338 **ppmv inlet NO concentration, all other studies used a 1.0 ppmv inlet NO concentration].**

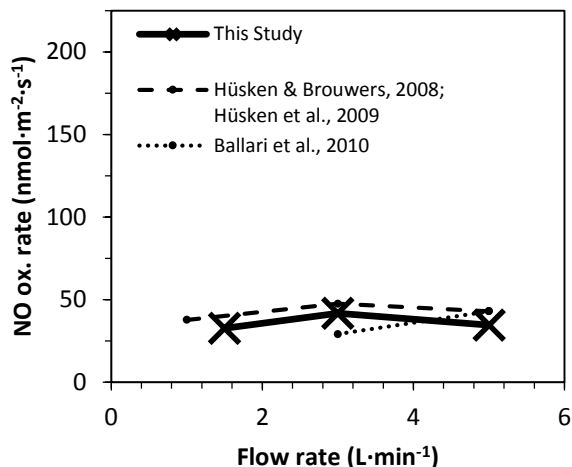
339 As noted above, a linear relationship is apparent when reviewing the data collected in this study ($R^2 =$
 340 0.996). Comparison of this data with Hüsken et al. (2009) did not find a significant difference in the slope
 341 of each data set's linear regression lines ($t = -0.403$, $df = 14$, $p = 0.693$). However, it should be noted that
 342 Hüsken et al. (2009) asserted power law relationship between percent NO removal and irradiance ($y =$
 343 $8.583x^{0.431}$, $R^2 = 0.998$) and concluded that linear behavior was limited to observations above $4 \text{ W}\cdot\text{m}^{-2}$.
 344 Linear behavior is also apparent in Ballari et al. (2011) ($R^2 = 0.986$), but comparison of slopes did find a
 345 significant difference ($t = -8.462$, $df = 7$, $p = 0.000$). In contrast, the data from Murata et al. (2000) appears
 346 non-linear ($R^2 = 0.910$ for linear regression). Furthermore, a t -test comparing the slope of linear regression
 347 lines between this data set and the authors' found a significant difference ($t = -5.672$, $df = 7$, $p = 0.001$). In
 348 similarity with the conclusion reached in Section 3.1.1, this difference indicates that lab evaluation of a
 349 specific material selected for field application is warranted in order to assess its NO oxidation potential.

350 As reported by Grant and Slusser (2005), mean daytime UV-A irradiance ranged from 10.5 to 22.3
 351 $\text{W}\cdot\text{m}^{-2}$ for the most northern and southern locations (Fairbanks, Alaska, latitude 65.1°N and Homestead,
 352 FL, latitude 25.4°N , respectively) according to the United States Department of Agriculture (USDA) climate

353 monitoring network. In addition to knowledge of the mean UV-A irradiance, application of photocatalytic
354 pavement also requires knowledge on the change in irradiance during daylight hours. This knowledge is
355 needed because in urban areas NO_x ambient concentration reportedly follows a diurnal pattern
356 associated with traffic. Urban background monitoring in London, UK, found that NO_2 peaks both in early
357 morning and late afternoon and NO , which oxidizes quickly to NO_2 during daylight hours, peaks in early
358 morning (Bigi & Harrison, 2010). At these peaks, irradiance values are substantially lower than the mean
359 daytime value. For example, at the 40th parallel north, which roughly runs through the center of the United
360 States, the difference between the typical mid-summer peak UV radiation and the radiation 4 hours earlier
361 in the day is more than 70% (Long et al., 1996). At present, oxidation rates at these low irradiance values
362 are quite low. To be effective at peak pollution hours, the ongoing efforts by other researchers to enhance
363 TiO_2 's photo-induced reactivity must be incorporated into new formulations of photocatalytic pavements.

364 3.1.3. Flow Rate

365 A model utility test on the data collected in this study (presented in Figure 7) did not reject a null
366 hypothesis that slope equaled $0 \text{ nmol} \cdot \text{m}^{-2} \cdot \text{s}^{-1} \cdot \text{C}^{-1}$ ($t = 0.118$, $df = 2$, $p = 0.925$), and therefore did not provide
367 evidence of a correlation between flow rate and NO oxidation rate. The same conclusion was found with
368 analysis of data from Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = 0.631$, $df = 2$, $p = 0.642$).
369 The independence of oxidation rate and flow rate aligns with the overall approach used by Hunger et. al
370 (2010) to model the oxidation of NO on photocatalytic concrete surfaces. Using a Langmuir-Hinshelwood
371 model and data collected with a photoreactor, Hunger et. al (2010) established that it is the conversion
372 of adsorbed species that limits the reaction rate, rather than mass transfer from the test gas to the sample
373 surface.



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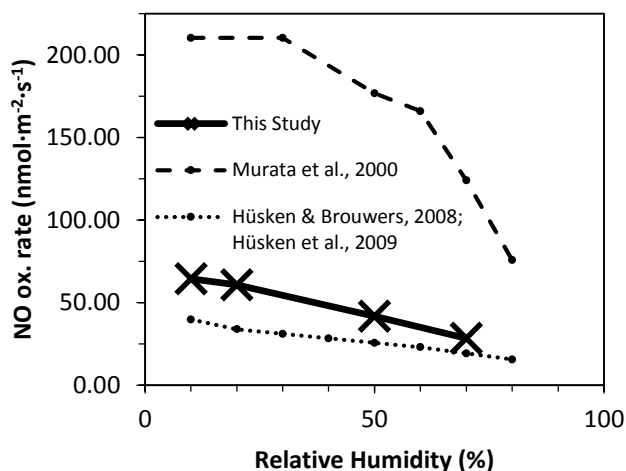
Figure 7. Effect of flow rate on NO oxidation rate.

376 Results, presented in the form of percent NO removal, were determined to be 51, 37, and 21% for
 377 flow rates of 1.5, 3, and 5 L·min⁻¹, respectively. Using these units, a negative relationship was evident
 378 between flow rate and percent removal ($t = -27.718$, $df = 2$, $p = 0.023$). This relationship was also
 379 documented by other researchers (Ballari et al., 2010; Dylla et al., 2010; Hüsken & Brouwers, 2008; Hüsken
 380 et al., 2009). These studies suggested that percent NO removal from a specific volume of test gas increases
 381 proportionally to the residence time over a photocatalytic surface because more time exists for pollutants
 382 to absorb and be oxidized at active sites. Overall, the lack of a correlation between flow rate and NO
 383 oxidation rate could simplify modeling efforts as stakeholders consider field applications. However, given
 384 the wide array of variables that need to be considered, this modeling effort will be challenging and is likely
 385 to have a high degree of uncertainty.

386 3.1.4. Relative Humidity

387 Figure 8 indicates a negative correlation between relative humidity and NO oxidation rate for the
 388 mortar slabs (created with cement that contains TiO₂) used in this study ($R^2 = 0.996$, $t = -22.257$, $df = 3$, p
 389 $= 0.002$). This correlation was also found in the study by Murata et al. (2000) ($t = -4.307$, $df = 5$, $p = 0.013$)
 390 and Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = -22.408$, $df = 7$, $p = 0.000$). Photocatalytic

391 degradation of NO by pavement containing titanium dioxide occurs when NO is oxidized by $\bullet\text{OH}$ (Figure
 392 1). These $\bullet\text{OH}$ are generated by oxidation of an OH^- by an electron hole. Current understanding proposes
 393 that water adsorbed on the slab serves as the source for OH^- . Intuition would thereby suggest that
 394 increased humidity would result in an increased rate of NO oxidation. By observation, the opposite has
 395 been found to be true. In addition to photocatalytic properties, materials containing TiO_2 also exhibit
 396 photo-induced superhydrophilicity (i.e., water on the surface has a contact angle of nearly 0°) (Fujishima
 397 et al., 2008). Adsorbed water vapor disperses over the surface, blinding photocatalytically active sites
 398 (Beeldens, 2007).



399

400 **Figure 8. Effect of relative humidity on NO oxidation rate.**

401 Although a negative correlation was found in each data set displayed in Figure 8, both data values and
 402 relationships differed. A null hypothesis that the difference in slopes of regression lines was 0 (i.e., $H_0: B_1$
 403 $- B_2 = 0$) was used to compare this study's data to the data obtained by other researchers. This evaluation
 404 found a significant difference in slope between this study and both Murata et al. (2000) ($t = 2.859$, $df = 6$,
 405 $p = 0.029$) and Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t = -9.378$, $df = 8$, $p = 0.000$).
 406 Evaluation of the y -intercept found a significant difference between this study and both Murata et al.
 407 (2000) ($t = -423.737$, $df = 6$, $p = 0.000$) and Hüsken and Brouwers (2008) and Hüsken et al. (2009) ($t =$

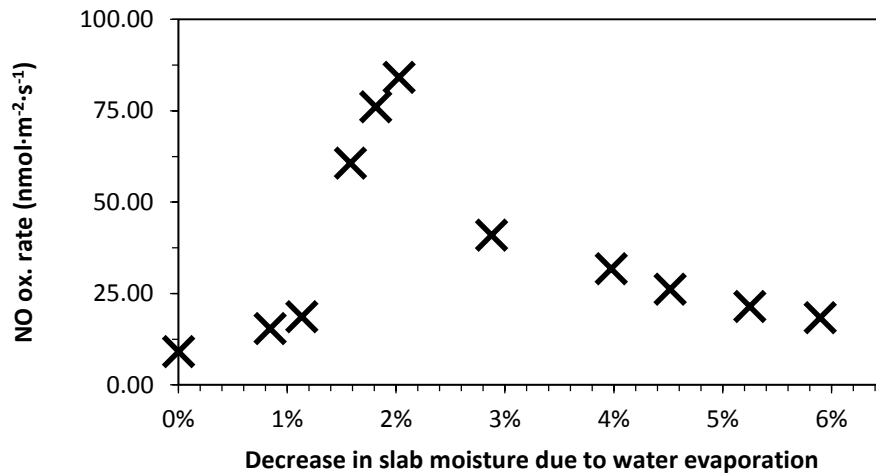
408 978.105, $df = 8$, $p = 0.000$). This evaluation provides further evidence of the complexity of photocatalytic
409 pavement materials. As concluded in previous sections, the researchers recommend that individual
410 materials undergo a thorough evaluation prior to field evaluation.

411 The observed negative correlation that occurs as a result of water's blinding effect could limit the
412 effectiveness of photocatalytic pavement in humid regions. Based on 2006–2008 data, the five counties
413 with the highest ambient NO₂ concentration in the form of the 2010-promulgated NO₂ standard for
414 counties within the United States are as follows: Cook, IL, San Diego, CA, Los Angeles, CA, Erie, NY, and
415 Denver, CO (USEPA, 2010a). With the exception of Denver County, each of the listed counties frequently
416 experiences high humidity conditions. As displayed in Figure 8, the NO oxidation rate at high humidity is
417 substantially diminished. Unless photocatalytic pavements can be modified to lessen their sensitivity to
418 changes in relative humidity, effective application in these polluted areas will be difficult.

419 3.1.5. Decrease in Slab Moisture

420 Figure 9 presents data obtained from a slab that was periodically removed from a 60°C oven and
421 evaluated in the photoreactor as internal moisture decreased from a saturated state. For a decrease in
422 moisture of 0–2% of saturated mass, a positive correlation is apparent ($R^2 = 0.822$) and a 0 slope null
423 hypothesis was rejected ($t = 4.310$, $df = 5$, $p = 0.013$). Conversely, for a decrease in slab moisture greater
424 than 2% of saturated mass, a negative correlation is apparent ($R^2 = 0.985$) and a 0 slope null hypothesis
425 was rejected ($t = -14.152$, $df = 5$, $p = 0.001$). These observations can be explained as follows: between 0
426 and 2% decrease in moisture, as water is evaporated from the slab it no longer blinds active sites and the
427 NO oxidation rate increases. This explanation is similar to the explanation for the correlation between
428 relative humidity and NO oxidation rates. For a decrease in moisture above 2% the rate of NO oxidation
429 appears to be limited because water contained within the slab is not available as a source for •OH. While
430 the primary purpose of these results is to indicate that slab moisture influences NO oxidation rate, it is

431 worth noting that these tests occurred at an average slab temperature of approximately 50°C. Data
 432 presented in Section 3.1.6 indicates that this elevated slab temperature increased reactivity by 60% in
 433 comparison to slabs at 22°C.



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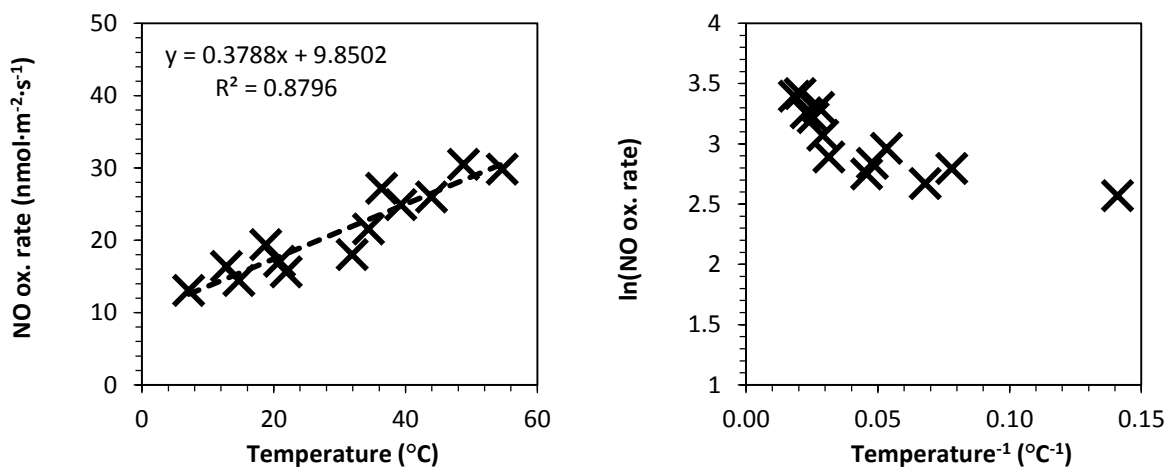
435 **Figure 9. Effect of decrease in slab moisture due to water evaporation on NO oxidation rate**
 436 **(photoreactor vapor density held constant).**

437 In this study, the peak NO oxidation rate was observed at 2% decrease in slab moisture. Under field
 438 condition a different peak would be observed. This difference would arise because water content varies
 439 throughout the depth of a concrete pavement; therefore, the decrease in moisture at the pavement
 440 surface would differ from the decrease in moisture throughout the entire slab. Overall, the findings
 441 presented in Figure 9 complicate recommendations for field application of TiO₂-containing pavements.
 442 On the basis of relative humidity, areas with sustained periods of low humidity would be recommended
 443 for application. It would be assumed that mitigation of NO pollution would continue as long as relative
 444 humidity remained low. However, sustained low humidity would also cause evaporation of water
 445 contained in the pores of the slab. Based on the data presented, a photocatalytic concrete pavement
 446 could be expected to remove NO initially; however, over time NO oxidation would decrease and the
 447 benefits would be lost. If TiO₂-containing pavement is to be applied in the field to mitigate NO pollution,

448 this complicating factor requires further investigation and methods to maintain moisture in the pavement
 449 may need to be developed.

450 3.1.6. Slab Temperature

451 Figure 10 displays the effect of temperature on NO oxidation rate on axes of NO oxidation rate versus
 452 temperature (Figure 10a) and $\ln(\text{NO oxidation rate})$ versus the inverse of temperature (Figure 10b).
 453 Linear regression of this data found a R^2 value of 0.880. A model utility test rejected a null hypothesis that
 454 slope equaled $0 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}\cdot\text{°C}^{-1}$ with confidence in excess of 99.99% ($t = 8.963$, $df = 12$). As noted in
 455 Section 2.4.2, tests which occurred at slab temperatures below 22°C presented the possibility of error due
 456 to water condensation. Linear regression of data points above 22°C found a slope of $0.459 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}\cdot\text{°C}^{-1}$
 457 ($R^2 = 0.725$, $n = 7$); for data points below 22°C the slope was $0.252 \text{ nmol}\cdot\text{m}^{-2}\cdot\text{s}^{-1}\cdot\text{°C}^{-1}$ ($R^2 = 0.417$, $n = 6$). A
 458 pooled-variance t -test of a null hypothesis that the difference between these two slopes was 0 (i.e., H_0 :
 459 $B_1 - B_2 = 0$) indicated that the slopes were not significantly different ($t = 0.967$, $df = 9$, $p = 0.359$). Although
 460 the values of the slopes differ, the data collected did not support a claim that this difference was
 461 significant.



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a.

b.

Figure 10. Effect of temperature on NO oxidation rate.

464

465 The effect of temperature on NO oxidation rates has not been studied in previous photoreactor
466 studies; therefore, comparison with other data sets was not possible. Other photocatalytic pavement
467 studies that do make statements in regard to the impact of temperature on oxidation rates are often
468 vague. In most instances these studies assert that the oxidation rate increases with an increase in
469 temperature (Beeldens et al., 2011) and that only large differences in temperature (i.e., summer vs.
470 winter) are significant (Dylla et al., 2011). In addition to being vague, the literature also is contradictory
471 and one source reported a decrease in oxidation rate with increased temperature (Chen & Chu, 2011).
472 One aqueous photocatalysis publication, Herrmann (1999), does provide useful insight for this study. It
473 stated that in the range of 20–80°C, activation energy was negligible and was not a rate limiting step.
474 Furthermore, at temperatures below 0°C, the apparent activation energy of the photocatalyst increased
475 leading to a decrease in oxidation rate.

476 The Arrhenius equation offers an empirical relationship between a reaction rate constant (k),
477 temperature (T), pre-exponential factor (A), activation energy (E_a), and the universal gas constant (R):

$$478 \quad k = A \cdot e^{\frac{-E_a}{R \cdot T}}$$

479 Using log properties, this equation can also be expressed as follows:

$$480 \quad \ln k = \frac{-E_a}{R} \left(\frac{1}{T} \right) + \ln A$$

481 When graphed on axes of $\ln(\text{NO oxidation rate})$ and the inverse of temperature ($1/T$), reactions that
482 follow the Arrhenius equation exhibit a linear relationship. Figure 10b does not display this type of
483 relationship. Overall, while the information discussed in this section partially explains the observations; it
484 would appear that given the complexity of photocatalytic pavement materials, other factors also
485 influenced the reported observations.

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4. Conclusions

Photocatalytic pavements offer a novel technological option to mitigate NO_x pollution. In order for these pavements to be adopted by potential stakeholders, information is needed that documents the NO oxidation rate under varied environmental conditions. A positive correlation was observed between NO oxidation rate and influent NO concentration. Comparison of this study with Hüsken and Brouwers (2008), Hüsken et al. (2009) and Ballari et al. (2010), who also studied cementitious photocatalytic pavements, found no significant difference in the slope of regression lines through this data. However, a significant difference in slope was observed in comparison with Murata et al. (2000). A positive correlation was also observed between NO oxidation rates and UV-A irradiance ($R^2 = 0.996$). Comparison of this study with Hüsken et al. (2009) found no significant difference in the slope of regression lines through this data. A significant difference in slope was observed in comparison with Murata et al. (2000). A correlation was not observed between NO oxidation rates and flow rate. This same conclusion was reached with analysis of data from Hüsken and Brouwers (2008) and Hüsken et al. (2009). A negative correlation was observed between NO oxidation rate and relative humidity. In contrast with evaluations for UV-A irradiance and NO concentration, no significant difference was found with comparison of this study to Murata et al. (2000). A significant difference in slope was observed between this study and Hüsken and Brouwers (2008) and Hüsken et al. (2009). Decrease in slab moisture, a variable not investigated in prior work, was found to affect NO oxidation rates. At losses of 0–2% of saturated mass, a positive correlation was observed; whereas, at losses greater than 2% a negative correlation was observed. A positive correlation was documented for slab temperature. This finding contrasts previous assertions which considered this variable insignificant.

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Overall, it can be concluded that photocatalytic mortar slabs manufactured with TX Active pavement are highly sensitive to changes in environmental variables. NO oxidation rates observed in this study ranged from 9.8–64 nmol·m⁻²·s⁻¹. Furthermore, significant differences were found by comparison to other

510 studies. Therefore, if a potential stakeholder is considering use of this technology to mitigate NO_x
 511 emissions, careful preliminary work should be undertaken to both evaluate the environmental conditions
 512 of the test site and the properties of the selected photocatalytic material.

513 5. Acknowledgments

514 The authors wish to thank the National Concrete Pavement Technology Center, the United States
 515 Department of Transportation (*grant number removed to ensure blind review*), Essroc Italcementi Group,
 516 and Lehigh Hanson, Inc. for providing funding to pursue this study. The authors also thank H. Bai and L. Y.
 517 Ong for their role in data collection and analysis.

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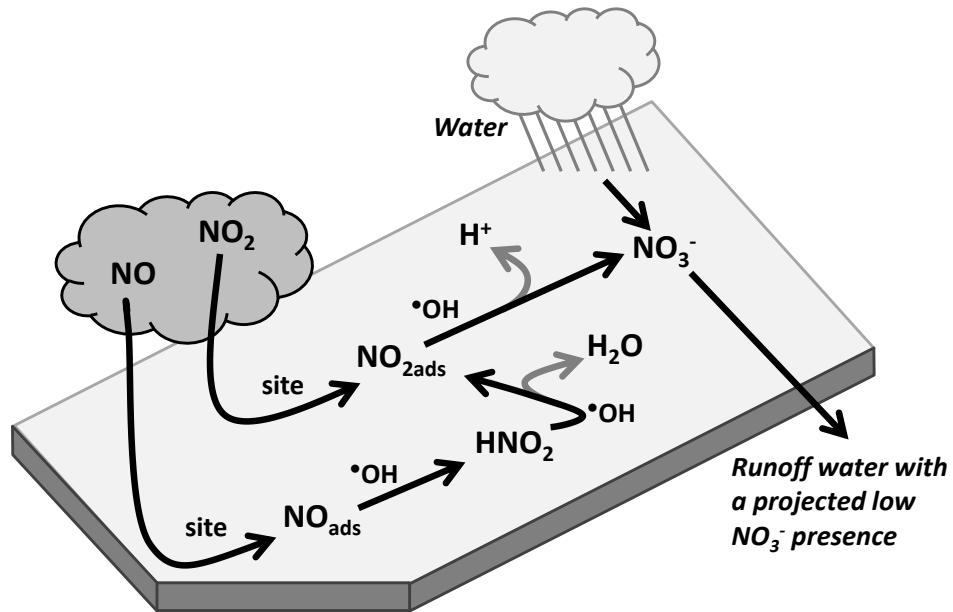
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Black and White Versions of Color Figures

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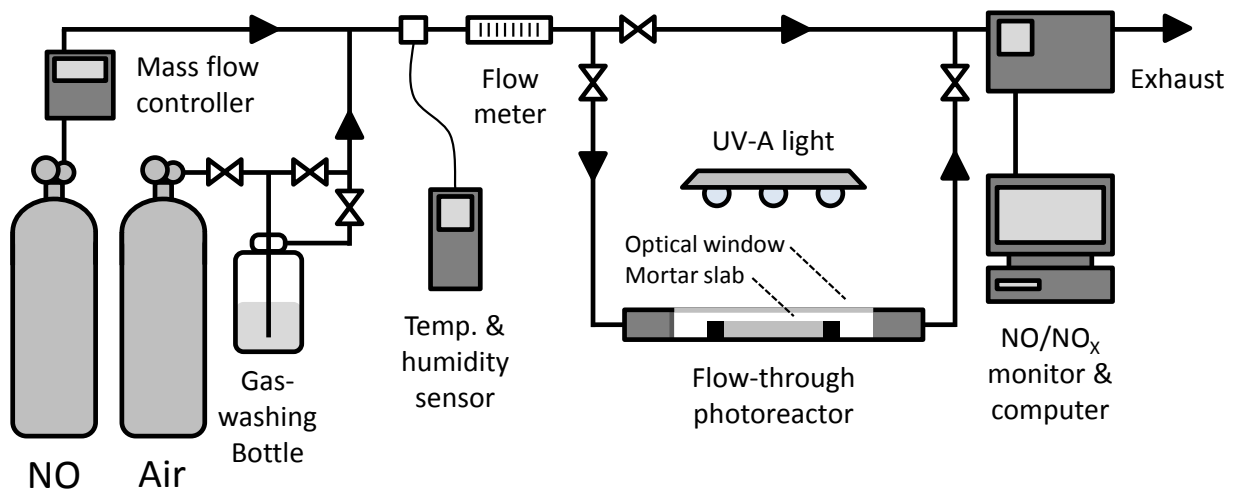
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638 **Figure1. Photocatalytic oxidation of NO and NO₂ by pavement containing TiO₂ (partially adapted from**

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Ballari et al., 2011).

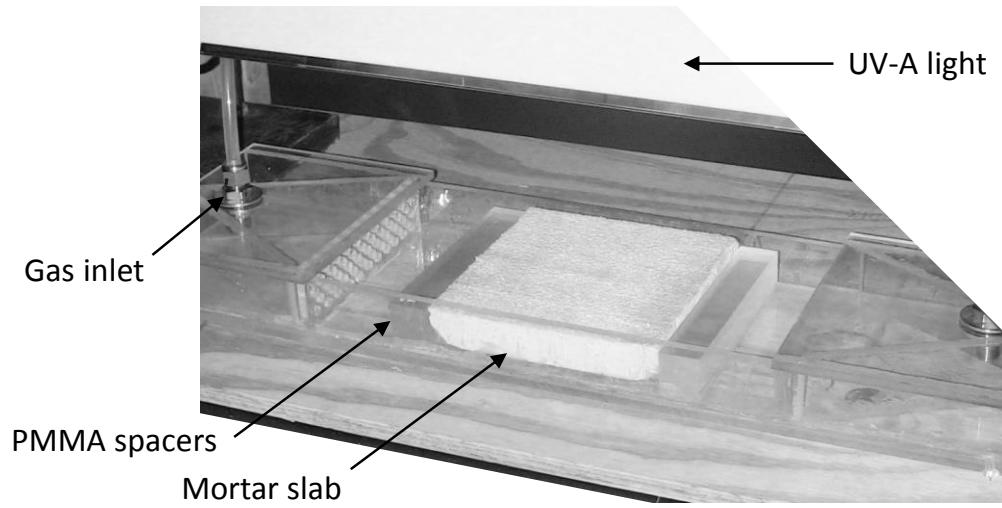
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Figure 2. Diagram of experimental apparatus (partially adapted from Ballari et al., 2011).



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644 **Figure 3. Photograph of photoreactor and mortar slab (optical window removed to facilitate viewing).**