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An Ion-Neutral Model to Investigate Chemical Ionization Mass Spectrometry Analysis of Atmospheric Molecules – Application to a Mixed Reagent Ion System for Hydroperoxides and Organic Acids

Brian G. Heikes University of Rhode Island, bheikes@uri.edu

Victoria Treadaway University of Rhode Island

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Authors

Brian G. Heikes, Victoria Treadaway, Ashley S. McNeill, Indira K. C. Silwal, and Daniel W. O'Sullivan



An ion-neutral model to investigate chemical ionization mass spectrometry analysis of atmospheric molecules – application to a mixed reagent ion system for hydroperoxides and organic acids

Brian G. Heikes¹, Victoria Treadaway¹, Ashley S. McNeill^{1,2}, Indira K. C. Silwal^{3,4}, and Daniel W. O'Sullivan³

¹Graduate School of Oceanography, University of Rhode Island, Narragansett, RI 02882, USA

²Department of Chemistry, The University of Alabama, Tuscaloosa, AL 35401, USA

³Chemistry Department, United States Naval Academy, Annapolis, MD 21402, USA

⁴Forest Bioproducts Research Institute, University of Maine, Orono 04469, USA

Correspondence: Brian G. Heikes (bheikes@uri.edu)

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Abstract. An ion-neutral chemical kinetic model is described and used to simulate the negative ion chemistry occurring within a mixed-reagent ion chemical ionization mass spectrometer (CIMS). The model objective was the establishment of a theoretical basis to understand ambient pressure (variable sample flow and reagent ion carrier gas flow rates), water vapor, ozone and oxides of nitrogen effects on ion cluster sensitivities for hydrogen peroxide (H₂O₂), methyl peroxide (CH₃OOH), formic acid (HFo) and acetic acid (HAc). The model development started with established atmospheric ion chemistry mechanisms, thermodynamic data and reaction rate coefficients. The chemical mechanism was augmented with additional reactions and their reaction rate coefficients specific to the analytes. Some existing reaction rate coefficients were modified to enable the model to match laboratory and field campaign determinations of ion cluster sensitivities as functions of CIMS sample flow rate and ambient humidity. Relative trends in predicted and observed sensitivities are compared as instrument specific factors preclude a direct calculation of instrument sensitivity as a function of sample pressure and humidity. Predicted sensitivity trends and experimental sensitivity trends suggested the model captured the reagent ion and cluster chemistry and reproduced trends in ion cluster sensitivity with sample flow and humidity observed with a CIMS instrument developed for atmospheric peroxide measurements (PCIMSs). The model was further used to investigate the potential for isobaric compounds as interferences in the measurement of the above species. For ambient O_3 mixing ratios more than 50 times those of H_2O_2 , $O_3^-(H_2O)$ was predicted to be a significant isobaric interference to the measurement of H_2O_2 using $O_2^-(H_2O_2)$ at m/z 66. O_3 and NO give rise to species and cluster ions, $CO_3^-(H_2O)$ and $NO_3^-(H_2O)$, respectively, which interfere in the measurement of CH₃OOH using $O_2^-(CH_3OOH)$ at m/z 80. The $CO_3^-(H_2O)$ interference assumed one of its *O* atoms was ¹⁸O and present in the cluster in proportion to its natural abundance. The model results indicated monitoring water vapor mixing ratio, m/z 78 for $CO_3^-(H_2O)$ and m/z 98 for isotopic $CO_3^-(H_2O)_2$ can be used to determine when $CO_3^-(H_2O)$ interference is significant. Similarly, monitoring water vapor mixing ratio, m/z 62 for NO_3^- and m/z 98 for $NO_3^-(H_2O)_2$ can be used to determine when $NO_3^-(H_2O)$ interference is significant.

1 Introduction

Atmospheric measurements of hydrogen peroxide (H₂O₂), methyl peroxide (CH₃OOH), formic acid (hereafter referred to as HFo) and acetic acid (hereafter referred to as HAc) have evolved over the past half century. Current state-of-theart measurements use chemical ionization mass spectrometry (e.g., Crounse et al., 2006; de Gouw and Warneke, 2007; Veres et al., 2008; St. Clair et al., 2010; Le Breton et al., 2012; Lee et al., 2014; Baasandorj et al., 2015; O'Sullivan et al., 2018; Treadaway et al., 2018) with a variety of reagent ions (e.g., H₃O⁺, O⁻₂, CF₃O⁻, I⁻, CH₃C(O)O⁻, O⁻₂(CO₂)). O'Sullivan et al. (2018) and Treadaway et al. (2018) have presented a hybrid reagent ion instrument for the simultaneous measurement of the peroxides and organic acids. Here an ion-neutral chemical kinetic model is described and used to simulate the negative ion chemistry occurring within their mixed-reagent gas chemical ionization mass spectrometer (PCIMS). The "P" is derived from the instrument's original configuration to measure H_2O_2 and CH_3OOH (O'Sullivan et al., 2018), and which was later modified to quantify HFo and HAc (Treadaway, 2015; Treadaway et al., 2018).

The PCIMS instrument and basic ion cluster schemes are described in O'Sullivan et al. (2018), Treadaway (2015) and Treadaway et al. (2018). Serendipity led to the use of a mixed reagent gas stream composed of nitrogen (N₂), oxygen (O₂), carbon dioxide (CO₂) and iodomethane (CH₃I). O₂ and CO_2 reagent gases provided O_2^- , $O_2^-(O_2)$ and $O_2^-(CO_2)$ as reagent ions. CH_3I reagent gas yielded iodide ions (I⁻). The PCIMS instrument was specifically designed to be mounted and utilized from an aircraft and was flown on the NCAR HIAPER (UCAR/NCAR-EOL, 2005) aircraft in the Deep Convective Clouds and Chemistry experiment (DC3; Barth et al., 2015) and on the NCAR C-130 (UCAR/NCAR-EOL, 1994) aircraft in the Front Range Air Pollution and Photochemistry Experiment (FRAPPE; https://www2.acom.ucar. edu/frappe). In these programs, a fixed area critical orifice was used on the sample inlet to the PCIMS. Consequently, the air sample flow rate into the instrument varied with ambient sample pressure and analyte sensitivity (defined as the cluster ion counts per second per analyte reaction cell mixing ratio, e.g., $cps ppb^{-1}$), varied with ambient pressure. As documented for many atmospheric CIMS instruments (e.g., Slusher et al., 2004; Crounse et al., 2006; St. Clair et al., 2010; Le Breton et al., 2012; Lee et al., 2014; Baasandorj et al., 2015), analyte sensitivity was dependent upon the reaction cell water vapor mixing ratio. The humidity and pressure sensitivity dependencies were complex and explored in the laboratory to improve calibration. As will be shown below within the discussion section, depending upon the reagent ion-analyte pair, the effect of water vapor can lead to:

- a relative constant sensitivity as water vapor mixing ratios increase until near maximum water vapor mixing ratios are encountered after which the sensitivity decreases with increasing water vapor;
- sensitivity increases as water vapor mixing ratio increases;
- sensitivity decreases as water vapor mixing ratio increases; and
- 4. "parabolic" response in which the sensitivity to an ionanalyte cluster is low at low water vapor mixing ratio, passes through a maximum sensitivity at an intermediate water vapor mixing ratio, and is low again at high water vapor mixing ratio.

Ambient pressure changes can also lead to decreasing or increasing sensitivity with an increase in sample pressure (flow). The objective of this paper is to present a model chemical mechanism which provides a theoretical basis to investigate the influences of ambient pressure (variable sample flow and reagent ion carrier gas flow rates), water vapor and other trace gases: ozone (O₃), nitric oxide (NO), nitrogen dioxide (NO₂) and nitric acid (HNO₃) on ion cluster sensitivities for H₂O₂, CH₃OOH, HFo and HAc. The model is extensible to simulating the negative ion chemistry of other reagent gas, ion source and reaction cell or drift-tube systems.

2 Methods

2.1 PCIMS instrument

The physical PCIMS instrument is described in O'Sullivan et al. (2018), Treadaway (2015) and Treadaway et al. (2018). A physical description of the instrument and calibration schemes are presented in the Appendix. The instrument flow and electronic configuration described in the Appendix was used throughout the field and laboratory work reported here. The PCIMS m/z range was 1–500 m/z and the mass resolution was 1.0 m/z. The main component effecting ion cluster transmission through the system was the collision dissociation chamber (CDC) consisting of an entrance plate and octopole ion guide. The CDC plate DC voltage and the octopole DC and RF voltages were adjusted to maximize the transmission of the hydroperoxide analyte cluster ions O_2^- (CO₂) (H₂O₂) and O_2^- (CH₃OOH) and to reduce the signal from other ions near their respective masses. To estimate the "declustering" energy employed, an analysis of the thermodynamics of the following hydration reactions:

$$\begin{aligned} & O_2^-(H_2O)_{n-1} + H_2OO_2^-(H_2O)_n; \quad n = 1 - 5, \\ & CO_3^-(H_2O)_{n-1} + H_2OCO_3^-(H_2O)_n; \quad n = 1 - 3, \\ & NO_3^-(H_2O)_{n-1} + H_2ONO_3^-(H_2O)_n; \quad n = 1 - 2, \end{aligned}$$

and

 $I^{-}(H_2O)_{n-1} + H_2OI^{-}(H_2O)_n; \quad n = 1 - 4,$

and the PCIMS signals of the respective hydrates was carried out. There was an absence of signals for $O_2^-(H_2O)_{n>3}$, $CO_3^-(H_2O)_{n>2}$ and $I^-(H_2O)_{n>1}$ clusters. The absence of these clusters suggested a CDC "declustering" enthalpy cut off at -50 kJ mol^{-1} or a CDC "declustering" Gibbs energy of -20 kJ mol^{-1} . The thermodynamic data used in this analysis were from NIST Chemistry WebBook SRD69 (Bartmess, 2016).

PCIMS uses a mixed reagent ion chemistry: O_2^- , O_2^- (CO₂) and I⁻ to produce cluster ions with H₂O₂ [O_2^- (H₂O₂), O_2^- (CO₂) (H₂O₂), I⁻ (H₂O₂) at masses 66, 110 and 161, respectively], with CH₃OOH [O_2^- (CH₃OOH),

mass 80], with HFo [I⁻ (HFo), mass 173] and HAc [I⁻ (HAc), mass 187]. There is a weaker signal for I⁻ (CH₃OOH) at mass 175 but it is not considered in the model.

In flight, ambient air was sampled through a heated probe held at 30 °C in DC3 and 70 °C in FRAPPE. The higher temperature in FRAPPE was used to partially alleviate an inlet contamination issue. Sample air is passed from the inlet to the instrument using heated PFA® Teflon tubing. All "wetted" surfaces from the probe to the physical instrument are PFA[®] Teflon. The inlet system is pumped by the instrument's vacuum system and by a second scroll pump (Varian model IDP-3) to increase sample airflow though the inlet tubing, therefore improving response time and ameliorating potential wall artifacts in H₂O₂, CH₃OOH, HFo and HAc. Standard additions of hydroperoxides were performed in DC3 and hydroperoxide and organic acid standard additions were performed in FRAPPE. The gas standards were added before a selectable entrance to two traps in series (Carulite- 200°), Carus Corp., Peru, IL; NaOH on fiberglass wool). There was a constant flow of standard gas to within 0.3 m of the inlet and a "draw-back" line was used to divert the standard and an equal amount of sample air to waste under normal conditions (Fig. A2b). A 2-way valve on the "draw-back" line of the syringe addition system and a 3-way valve near the instrument inlet (Fig. A2b) were used to select between one of four modes: (1) the sample air, (2) sample air with gas standard addition, (3) sample air passed through the traps as a field blank or (4) sample air with gas standards added and passed through the traps to evaluate trap efficiency. In this way instrument calibration and trap efficiency were monitored.

H₂O₂, CH₃OOH and CD₃OOH (trideuterated methyl peroxide) gas standard additions are available for research flights 6-22 in DC3. H₂O₂ and HFo standard additions are reported for all 15 research flights in FRAPPE. However, in FRAPPE, the instrument experienced severe vibration in flight, which caused "chatter" in the MFCs (mass flow controllers), and there was a significant contaminant in the hanger. Consequently, CH₃OOH calibrations were reported for the last 11 flights after the MFC mounts were reconfigured and "chatter" was greatly reduced. HAc standard additions were only available for a portion of these FRAPPE flights as the contamination problem was only minimized on longer flights or after high altitude runs. The standard additions used here were further screened to ensure each standard addition cycle, (ambient air, ambient air with gas standards added, ambient air), was completed at constant pressure (altitude).

The laboratory calibration set up is described fully in Treadaway (2015) and only briefly here (block schematic shown in Fig. A2a). A pure-air generator (Model 737-10A, Aadco Instruments Inc., Cleves, OH) supplied the carrier air stream at 10 slpm (standard liters per minute, $T_{\text{ref}} = 0$ °C, $P_{\text{ref}} = 1013.25$ hPa). This air stream was split between dry

(5-10 slpm) and humidified lines (0-5 slpm) and the total flow was maintained at 10 slpm. The water concentration in the humidified line is controlled with two gas washing bottles and a gas-water equilibration coil immersed in a water bath held at either 15 or 25 °C. At the latter bath temperature, it was necessary to reset the room temperature from 22 to 30 °C to prevent condensation in the line. For some experiments, gas standard additions were performed with an external Henry's Law type equilibration coil with concurrent aqueous flow at 0.4 mL min^{-1} , air flow at 0.4 slpm, gas and aqueous flows are separated at the end of the coil using a cyclone separator, and the coil/cyclone is immersed in a water bath held at 15 °C. The Henry's Law system was plumbed to the carrier air stream after the humidification line. A needle valve was used to simulate lower ambient pressures (Fig. A2a) as in flight. The aircraft standard addition system was also used and this remained plumbed downstream of the laboratory air pressure control system. Air pressures between 120 and 1013 hPa were sampled (nominally set at 120, 180, 300, 600 and 1013 hPa). By changing the proportion of air flow through the dry (10, 9, 8, 7, 6 and 5 slpm) and humidified lines (0, 1, 2, 3, 4, and 5 slpm) and the inlet pressure, it was possible to alter the reaction cell water vapor mixing ratio from 30 to 20 000 ppm.

2.2 Ion-neutral chemical mechanism

The chemical mechanism is guided by the ion-neutral reaction suites and kinetic summaries of Albritton (1978), Huertas et al. (1978), Ikezoe et al. (1987), Turunen et al. (1996), Kazil (2002), Popov (2010) and Kovács et al. (2016) developed to simulate ion-neutral chemistry of the atmosphere. Necessary modifications and extensions of the chemical mechanisms to fit the PCIMS sensitivities are described here and in more detail within the Supplement.

Some trace components of ambient air can compete for the reagent ions and ion-neutral clusters effecting the yield (sensitivity) of the analyte ion clusters of interest as well as forming isobaric interfering ion or ion clusters. Analyte ion clusters and identified potential interfering ion species at specific m/z ratios are listed in Table 1. Also listed are primary ion cluster m/z ratios used to assess potential isobaric interferences. For example, m/z 78 is used to monitor $CO_3^-(H_2O)$, which in turn is used to estimate the potential interference at m/z 80 from $CO_3^-(H_2O)$ should one of its four O atoms be a mass 18 stable isotope of oxygen, ¹⁸O, and present at its natural abundance of 0.204 %.

Time-dependent concentrations of 73 species (neutrals, ions and ion clusters), listed in Appendix Table A1, are predicted in time according to the 209 bi- and ter-molecular reactions presented in Appendix Table A2. For clarity, analyte cluster ion formation reactions are re-listed in Table A3. Potential isobaric interference ion cluster formation reaction sequences are additionally listed in Table A4 for clarity. A set of 72 ordinary differential equations was solved using

Table 1. PCIMS m/z for species clusters of interest and potential isobaric interfering ions or ion clusters at the mass resolution of the quadrupole mass selector. Bold font indicates a primary PCIMS analyte ion cluster mass; "¹⁸O of" indicates one of the ion cluster's oxygen atoms is a mass 18 isotope of oxygen; in CD₃OOH the D represents deuterium atoms; EtOH refers to ethanol; PrOH refers to 1-propanol; 2-PrOH refers to 2-propanol; CH₂(OH)₂ refers to methane-diol; MeFo refers to methyl formate; and GA refers to hydroxy acetaldehyde (a.k.a. glycolaldehyde).

m/z	Ion or ion-neutral cluster
50	$O_{2}^{-}(H_{2}O), {}^{18}O \text{ of } O_{3}^{-}$
60	$\tilde{CO_3}$
62	NO_{3}^{-} , ¹⁸ O of CO_{3}^{-}
66	$O_{2^{-}}(H_2O_2)$, ¹⁸ O of NO ₂ ⁻ (H ₂ O), O ₃ ⁻ (H ₂ O), ¹⁸ O of O ₂ ⁻ (O ₂)
76	$O_2^-(CO_2)$
78	$\tilde{CO}_{3}^{-}(H_{2}O), {}^{18}O \text{ of } O_{2}^{-}(CO_{2})$
80	$O_{2^{-}}(CH_{3}OOH), NO_{3}^{-}(H_{2}O), {}^{18}O \text{ of } CO_{3}^{-}(H_{2}O),$
	$NO_{2}^{-}(H_{2}O_{2}), {}^{18}O \text{ of } O_{2}^{-}(HFo), O_{2}^{-}(CH_{2}(OH)_{2})$
83	$O_2^{-}(CD_3OOH)$
110	$\tilde{O_{2^-}(CO_2)}(H_2O_2)$
147	$I^{-}(H_{2}^{18}O)$
161	$\bar{\mathbf{I}^{-}(\mathbf{H}_{2}\mathbf{O}_{2})}, \bar{\mathbf{I}^{-}(^{18}\mathbf{O}^{16}\mathbf{O})}$
173	$I^{-}(HFo), I^{-}(EtOH), I^{-}(C^{18}O^{16}O)$
175	$I^{-}(CH_{3}OOH), I^{-}(CH_{2}(OH)_{2}), I^{-}(O_{3})$
187	$I^{-}(HAc)$, $I^{-}(MeFo)$, $I^{-}(PrOH)$, $I^{-}(2-PrOH)$, $I^{-}(GA)$

the *ode23t* solver (MatLab version R2016b, The MathWorks, Inc.) with relative tolerance equal to 3×10^{-9} and the absolute tolerance equal to 3×10^{-12} .

2.3 Reaction rate coefficients

Reaction rate coefficients are taken from Popov (2010), Kazil (2002), Ikezoe et al. (1987), Kawamoto and Ogawa (1986), Fahey et al. (1982), Albritton (1978), Huertas et al. (1978), Fehsenfeld and Fergusson (1974), Adams et al. (1970), Fehsenfeld et al. (1969, 1967) and references therein. Reaction rate coefficient units are s^{-1} , $cm^3 molec^{-1} s^{-1}$, and $cm^6 molec^{-2} s^{-1}$ for uni-, bi- and ter-molecular reactions, respectively. Equilibrium constants determined using reaction Gibbs energy, have been converted appropriately assuming (ideal gas behavior, $T_{ref} = 298.15$ K, $P_{\rm ref} = 1013.25 \,\mathrm{hPa}$ and $N_{\rm ref} = 2.46 \times 10^{25} \,\mathrm{molec} \,\mathrm{m}^{-3}$). Most of the reaction rate coefficients were experimentally determined and a few were theoretically estimated (e.g., Kazil, 2002; Iyer et al., 2016). However, some of the rate constants listed in the above compilations were simply presumed (e.g., Mohnen, 1972; Huertas et al., 1978) and these presumptions have carried forward into later works. Several rate coefficients were estimated from the Gibb's reaction energy, G_{rxn}^o , or equilibrium constant, K_{eq} , with either a measured forward or reverse reaction rate coefficient following Albritton (1978), i.e., $K_{eq} = \frac{k_{for}}{k_{rev}}$ and $K_{\text{eq}} = e^{\{G_{\text{rxn}}^o/(\text{RT}_o)\}}$. The majority of Gibbs reaction energies are taken directly from the NIST Chemistry WebBook (Bartmess, 2016). Generally available neutral, ion and ion cluster formation enthalpy, entropy and Gibb's formation energy for the $O_2^- - O_2 - CO_2 - H_2O_-$ hydroperoxide system are listed in Table A5 in the Appendix. Reaction enthalpy, reaction entropy and Gibb's reaction energies for this system are listed in Table A6 in the Appendix. Notes on the development of the thermodynamic Tables A5 and A6 are given in the Supplement Sect. S1.1. As called out below and in the Supplement, care is required in applying $K_{eq} = \frac{k_{forward}}{k_{reverse}}$ as the implied reaction system may not represent a simple concerted reaction pair in equilibrium but involve a reaction sequence in steady-state. For several of the ion-hydrate cluster reactions:

$$X^{-}(\mathrm{H}_{2}\mathrm{O})_{n-1} + \mathrm{H}_{2}\mathrm{O} + M \Leftrightarrow X^{-}(\mathrm{H}_{2}\mathrm{O})_{n} + M$$
$$K_{\mathrm{eq}} = \frac{k_{\mathrm{hydration}}}{k_{\mathrm{dehydration}}} = e^{\left\{G_{\mathrm{rxn}}^{o}/R/T_{o}\right\}},$$

neither the forward termolecular hydration rate constant $(k_{hydration})$ nor the bimolecular dehydration rate constant $(k_{dehydration})$ is known. In this case, rate coefficients are estimated from the observation that a strong correlation exists between the log of $k_{dehydration}$ and the Gibbs energy of the hydration reaction (G_{rxn}^{o}) . The correlation is shown in Fig. 1a. Known dehydration rate coefficients include those that are experimentally determined by direct measurement of $k_{dehydration}$ and those that are estimated from the hydration equilibrium constant and a measured $k_{hydration}$. For the cases in which neither $k_{hydration}$ or $k_{dehydration}$ is known, $k_{dehydration}$ is first estimated using ΔG_{rxn}^o as its predictor (i.e., the linear regression model "fit" in Fig. 1a) and k_{hydration} is subsequently estimated from the predicted $k_{dehydration}$ value and K_{eq} . Figure 1b shows known $k_{hydration}$ and estimated $k_{hydration}$ plotted as a function of G_{rxn}^o . Note further that, with only a few exceptions, individual $k_{hydration}$ rates fall within a factor of two of the mean value (dashed green line) and are near the collision limit. A factor of two falls within the accepted uncertainty estimated for the reaction rate coefficients. The uncertainties in ion-molecule reaction rate coefficients as reported by their original authors are included in the summary by Ikezoe et al. (1987). Typically, reaction rate coefficient uncertainty is reported to be a factor of two (e.g., Albritton, 1978; Fahey et al., 1982; Ikezoe et al., 1987). Although for a few reactions, "best" reaction rate coefficient uncertainties of ± 20 % can be found (e.g., Ikezoe et al., 1987). Here a factor of two is taken as the uncertainty in the reaction rate coefficients. Additional notes on the development of reaction rate coefficients are given in Sect. 1.2–1.4 of the Supplement.

The following generic equilibrium reaction sequences, after, e.g., Crounse et al. (2006) and Le Breton et al. (2012), are used to describe negative ion, X^- , cluster formation with an analyte, A, representing H₂O₂, CH₃OOH, HFo, and HAc:

 $X^{-} + H_2O + M \leftrightarrow X^{-} (H_2O) + M$ (R1)

 $X^- + A + M \leftrightarrow X^-(A) + M \tag{R2}$



Figure 1. Ion cluster dehydration (**a**) and hydration (**b**) reaction rate coefficients plotted as a function of the Gibbs reaction energy (G_{rxn}^o) for I⁻, O₂⁻, O₃⁻, CO₃⁻, HO⁻, NO⁻, NO₂⁻ and NO₃⁻ ions for n = 1-3 water molecules. Solid circles are reported rate coefficients from the literature (see text) and open circles are estimates based upon linear regression of $\ln(k_{dehydration})$ versus G_{rxn}^o or $k_{hydration} = k_{dehydration} \times K_{eq}$.

$$X^{-}(\mathrm{H}_{2}\mathrm{O}) + A \leftrightarrow X^{-}(A) + \mathrm{H}_{2}\mathrm{O}$$
(R3)

Reactions (R1)–(R3) correspond to our Reactions (22)–(45). As discussed below, we added poly-hydrate "switching" type reactions:

$$X^{-}(\mathrm{H}_{2}\mathrm{O})_{n} + A \leftrightarrow X^{-}(A)(\mathrm{H}_{2}\mathrm{O})_{n-1} + \mathrm{H}_{2}\mathrm{O}$$
(R4)

to account for observed higher order humidity effects on O_2^- , O_2^- (CO₂⁻) and I⁻ hydroperoxide and organic acid sensitivity. This simple system with a variety of reaction rate coefficients can yield a suite of sensitivity responses to water vapor.

- Case 1: sensitivity independent of water.

Assumptions, water vapor does not deplete the reagent ion concentration and the product $k_{R2f}[M][X^-]$ is much larger than $k_{R3f}K_{R1}[H_2O]$ over the range of $[H_2O]$ encountered.

 Case 2: sensitivity increases with water vapor mixing ratio.

Assumptions, water vapor does not deplete the reagent ion concentration and the product $k_{R2f}[M][X^-]$ is smaller than $k_{R3f}K_{R1}[X^-][H_2O]$ over the range of [H₂O] encountered.

- Case 3: sensitivity decreases with water vapor mixing ratio.

Assumption set A: water vapor depletes the reagent ion concentration via Reaction (R1) and successive hydration reactions represented by:

$$X^{-}(\mathrm{H}_{2}\mathrm{O})_{m-1} + \mathrm{H}_{2}\mathrm{O} + M \leftrightarrow X^{-}(\mathrm{H}_{2}\mathrm{O})_{m} + M \quad (\mathrm{R1'})$$

and reactions like Reaction (R3f) are slow.

Assumption set B: product $k_{R3r}[X - (A)][H_2O]$ becomes progressively larger than the sum of $k_{R2f}[M][X-]$ and $k_{R3f}K_{R1}[X^-][H_2O]$ as $[H_2O]$ increases.

For the most part, our ion-analyte cluster reaction kinetics are unstudied. The ion hydration kinetics of Reaction (R1) are discussed above. Measured reaction rate coefficients were available for H_2O_2 clustering with NO_2^- , NO_3^- , Cl^- and HSO_4^- (Böhringer et al., 1984). Iyer et al. (2016) using ab initio methods estimated reaction rate coefficients and binding energies for I⁻ with HFo and HAc. They also calculated binding energies for I⁻ reactions with H₂O₂ and CH₃OOH (Siddharth Iyer, personal communication, 2017). The calculated binding energies for I⁻ (HFo), I⁻ (HAc), I⁻ (H₂O₂) and I⁻ (CH₃OOH) were 100, 73, 70 and 60 kJ mol^{-1} , respectively. Iver et al. predicted sensitivities for the Lee et al. (2014) instrument using the calculated binding energies and measured sensitivities. We have normalized these to I^{-} (HFo) and the predicted relative sensitivities were 1.000, 0.034, 0.007 and 0.001 for I⁻ (HFo), I⁻ (HAc), I⁻ (H₂O₂) and I⁻ (CH₃OOH), respectively. These were consistent with the observations of O'Sullivan et al. (2018) in which they noted observing I⁻ (H₂O₂) and sometimes I⁻ (CH₃OOH) clusters with the PCIMS instrument. They were furthermore, consistent with Treadaway et al. (2018) in which they observed a weak standard addition calibration signal for I⁻ (CH₃OOH) during FRAPPE and in the laboratory in preparation for FRAPPE.

At the constant reaction cell instrument pressure of 22 hPa, the forward rate coefficient for Reaction (R2) was taken to be



Figure 2. Relationship between the negative ion-protonation reaction Gibbs energy, $-\Delta G_{R4}^o$, and (a) negative ion-hydration reaction Gibbs energy, $-\Delta G_{R1}^o$, and ion-H₂O₂ cluster reaction Gibbs energy, $-\Delta G_{R2}^o$, or (b) negative H₂O and H₂O₂ switching reaction Gibbs energy, $-\Delta G_{R3}^o$. Reactions (R1)–(R4) refer to reactions introduced in the text with $A = H_2O_2$. Filled symbols denote measured values and open symbols indicate estimated values. The lines indicate least square linear regression fits with the regression constants and coefficient of determination given in the respective boxes. The use of negative values of the Gibbs energy of reaction follows NIST (Bartmess, 2016) nomenclature.

constant and the reaction and its rate coefficient were given as a pseudo-bimolecular reaction with an initial reaction rate coefficient of 3×10^{-9} , which is near the bi-molecular collision limits calculated by Kazil (2002) and Iyer et al. (2016). This reaction rate coefficient was presumed for Reaction (R3), as well, although in the literature switching reaction rate coefficients on the order of 10^{-10} are also used as estimates.

The reverse reaction coefficient of Reaction (R2) is estimated using the assumed forward rate constant and the equilibrium constant for Reaction (R2). As noted above, reaction Gibbs energies and equilibrium constants are available for Reaction (R1) (Bartmess, 2016). A more limited set of Gibbs energies and equilibrium constants are available for Reaction (R2) with H₂O₂ as the analyte (Böhringer et al., 1984; Cappa and Elrod, 2001; Messer et al., 2000; O'Sullivan et al., 2018). Following Böhringer, we used known reaction enthalpies, ΔH_{R5}^o , or reaction Gibbs energies, ΔG_{R5}^o , of the ion protonation reaction (Reaction R5),

$$X^- + \mathrm{H}^+ \leftrightarrow X\mathrm{H} \tag{R5}$$

as linear predictors of the reaction Gibbs energy for Reactions (R1) and (R2), ΔG_{R1}^o and ΔG_{R2}^o , (and therefore the equilibrium constant) with $A = H_2O_2$ and $X^- = O_2^-$, O_2^- (CO₂) or I⁻. Figure 2a illustrates the linear relationships between ΔG_{R5}^o with ΔG_{R1}^o for H₂O, and with ΔG_{R2}^o for H₂O₂. Figure 2b shows the linear relationship between ΔG_{R5}^o and ΔG_{R3}^o , where $\Delta G_{R3}^o = \Delta G_{R2}^o - \Delta G_{R1}^o$. Figure 2 is plotted with $A = H_2O_2$ as introduced in Reactions (R2)– (R4). The predicted equilibrium constants, K_{R2} , for O_2^- , O_2^- (CO₂) and I⁻ are 3.2×10^{16} , 3.5×10^7 and 1.4×10^7 (atm⁻¹), respectively. The coefficients of determination were the same regardless of whether ΔH_{R5}^o or ΔG_{R5}^o was used to predict ΔG_{R1}^o or ΔG_{R2}^o and subsequently ΔG_{R3}^o . As noted in the Supplement, there is some question as to whether O_2^- (CO₂) (H₂O) follows a simple reaction pair or involves a more complex set of reactions at steady state and a linear prediction of ΔG_{R3}^o could be an oversimplification and a source of error for reaction rate constants involving this species.

The kinetics and equilibrium constants for CH₃OOH ion cluster formation are more speculative. Cappa et al. (2001) using ab initio methods have estimated ΔH_{R2}^o and ΔG_{R2}^o for cluster formation with CO_3^- , -69 and -34 kJ mol^{-1} , respectively, and ΔH_{R3}^o and ΔG_{R3}^o for Reaction (R3), -17 and -9 kJ mol^{-1} , respectively. Siddharth Iyer (personal communication, 2016) estimated the CH₃OOH binding energy with I^- is -60 kJ mol^{-1} . Messer et al. (2000) also using ab initio methods examined the kinetics and energetics of H₂O₂ and CH₃OOH cluster ion formation with F⁻. They reported theoretical collision-limit rate coefficients of 1.42×10^{-9} and 1.47×10^{-9} , respectively, for reactions with $F^{-}(H_2O)_3$. Their theoretical rate coefficients were bracketed by their experimental determined rates of $0.96-1.92 \times 10^{-9}$. The $F^{-}(H_2O)_3$ ion was the predominant reagent ion under their experimental humidity conditions that gave rise to an ion-peroxide signal. Messer et al. further stated the rate of reaction was relatively unchanged for F⁻ hydration numbers less than six. Payzant and Kebarle (1972), Fehsenfeld and Ferguson (1974) and Fahey et al. (1982) discussed reaction rates of O_2^- with variable numbers of water molecules attached and indicated they varied only slightly with different extents of hydration. We have therefore assumed the reaction rate coefficients for hydrated O_2^- ions with H_2O_2 and

CH₃OOH do not vary significantly with hydration. The forward rate constants for Reactions (R2), (R3) and (R4) are set at near the collision rate for H₂O₂ and CH₃OOH. As a caveat, we note some switching reaction rate coefficients for less tightly bound neutral species, e.g., O₂, CO₂, H₂O, are reported to be on the order of 10^{-10} .

Water vapor is commonly added to the CH₃I reagent gas stream in I⁻ based CIMS instruments because it enhances sensitivity for some analytes (e.g., Slusher et al., 2004; Le Breton et al., 2012). Whether this is because H_2O is a better third body energy carrier, such as in Reaction (R2), or adds a switching reaction (Reaction R3) to the instrument's development of an $I^{-}(A)$ cluster ion is not clear, although discussions point to the latter. Per Iyer et al. (2016), the Reaction (R2) forward reaction rate coefficient is initially set at the collision limit for HFo and HAc. The forward reaction rate coefficients for these two compounds in Reaction (R3) were initially set at the collision limit. The hydration equilibrium constants for I⁻ are such that under our laboratory and field experimental conditions, I⁻ and I⁻ (H₂O) dominate over $I^{-}(H_2O)_{n>1}$ ions. Even so at the highest humidities studied it was necessary to include Reaction (R4) for n = 2, but inclusion of Reaction (R4) with n > 2 was unnecessary even when the Reaction (R4) reaction rate coefficient was set at the collision limit.

Last, Iyer et al. (2016) examined the probability of collisional stabilization of HFo (atom number 5) compared to maximum sensitivity molecules (atom number >8) and found the former gave sensitivities dependent on reaction cell pressure, whereas, the latter were independent of pressure. Our analytes have between four and six atoms and our use of collision limit reaction rate coefficients could have resulted in an over prediction of the rates of I^- cluster formation.

2.4 Model assumptions

Individual model runs are performed in two stages. The first simulated the chemistry of the ion source region (alpha emitter, and reagent ion gas mixture). The product ion outflow of the source was then instantaneously mixed with the sample air stream and the ion-neutral chemistry of the reaction cell was simulated second. The following assumptions were made:

- 1. Alpha particle emission was uniform along the ion source tube length.
- 2. The ions directly generated by the alpha particles passing through >99 % N₂ gas consisted solely of e^- and N₂⁺ ions; the mechanism included several negative ions and N₂⁺ is the only positive ion considered.
- 3. The energy of a ²¹⁰Po alpha particle is 5.3 MeV; the formation enthalpy of a N₂⁺ and e⁻ ion pair from N₂ gas is 34 eV; thus, as a zeroth-order estimate, a 20 mCi ²¹⁰Po alpha source (the stated activity of the NRD P-

2130 Electrostatic Eliminator[®]) generated on the order of 10^{14} ion pairs per second.

- 4. Ion and neutral molecule concentrations varied along the flow direction and were radially uniform in the ion source tube and reaction cell.
- 5. Gas fluid flow in the ion source tube and in the reaction cell followed plug-flow.
- 6. The reagent gas stream and ambient air stream were mixed instantaneously and uniformly at the point of contact.
- 7. Ion clusters containing N_2 , O_2 , and CO_2 as neutrals were not considered with the exceptions of O_2^- (CO₂) and O_2^- (O₂).
- 8. Wall effects on negative ions, neutral species and heterogeneous chemistry were ignored. The first assumption is supported by the fact the ion source tube and reaction cell walls have a -2 V bias applied.
- 9. The negative ion positive ion recombination was parameterized using a single pseudo positive ion, " N_2^+ ", that reacts with each negative ion and whose rate constant followed Kazil (2002) and was tracked through:

$$N_2^+ + X_i^{-k=6x10^{-8}(300/T)+1.25\times10^{-25}[M](300/T)} \xrightarrow{\text{neutral products,}} (157i)$$

where, 157i indicated the reaction was included for each of the negative ion species.

2.5 Initial concentrations

The initial reagent gas mixture was composed of N₂, O₂, CO₂ and CH₃I in proportions that vary with sample air pressure and sample-air flow rate. The total flow rate through the reaction cell was constant at 4.68 slpm (standard liters per minute; $T_{ref} = 0$ °C, $P_{ref} = 1013.25$ hPa). The ambient air sample flow rate varied (range 0.3 to 3 slpm) with ambient pressure (range 120 to 1013.25 hPa) as did the N₂ flow rate through the ion-source tube (range 2.1 to 4.3 slpm). Reagent gas concentrations in the ion-source tube varied accordingly and their initial concentrations for different sample pressures and flow conditions are listed in Table 2. Six representative pressures are shown, which span the range of pressures encountered in the DC3 and FRAPPE airborne field campaigns and in the laboratory work. The ion source tube and reaction cell temperature and pressure were taken to be 25 °C and 22 hPa, respectively. The model chemical system was then integrated in time for the length of the gas transit time through the ion source tube.

Ambient air was then mixed with the reagent ion stream. Ambient air, for the purpose of defining reaction cell ion

Sample pressure, hPa ^a	120	180	306	600	800	1013
N ₂ flow rate, slpm ^b	4.27	4.23	3.98	2.99	2.58	2.05
CO_2 in air flow rate, slpm	0.08	0.08	0.08	0.08	0.08	0.08
CH ₃ I in N ₂ flow rate, slpm	0.0005	0.0005	0.0005	0.0005	0.0005	0.0005
CH ₃ I, ppb ^c	0.575	0.580	0.616	0.814	0.939	1.174
CO_2 , ppm ^d	7.36	7.42	7.88	10.42	12.02	15.02
O ₂ , ppm	3678	3712	3941	5212	6015	7512
N ₂ , ppm	996 322	996 288	996 059	994 788	993 866	992 488

Table 2. Initial reagent gas flow rates and reagent gas mixing ratios at six sample air pressures.

^a Pressure in hPa (hectopascal, equivalent to milli-bars). ^b slpm, standard liters per minute ($T_{ref} = 0$ °C; $P_{ref} = 1013.25$ hPa). ^c ppb, parts per billion (molecular mixing ratio times 10⁹). ^d ppm, parts per million (molecular mixing ratio times 10⁶).

concentration and analyte ion-molecule cluster concentration, included N₂ (\sim 79 %), O₂ (\sim 21 %), CO₂ (\sim 400 ppm), CH₄ (~2 ppm), H₂ (~0.5 ppm), N₂O (~0.32 ppm), O_3 (~0.05 ppm), NO (~1 ppb), NO₂ (~1 ppb), HNO₃ $(\sim 1 \text{ ppb}), \text{ H}_2\text{O}_2$ $(\sim 1 \text{ ppb}), \text{ CH}_3\text{OOH}$ $(\sim 1 \text{ ppb}), \text{ HFo}$ $(\sim 1 \text{ ppb})$ and HAc $(\sim 1 \text{ ppb})$. The noble gases, carbon monoxide, and other oxygenated volatile organic compounds were not considered here. The air-sample water vapor mixing ratio was varied from 10 to 31 700 ppm to span the range found in the troposphere. Simulation results are presented as a function of reaction cell water vapor mixing ratio and ambient sample pressure.

3 Model results

The development of ions along the length of the ionsource tube for representative ambient pressures of 1013 and 307 hPa is illustrated in Fig. 3 for the fully developed model. The total ion density was at or near steady-state approximately 2/3 s of the way through the ion source tube, although $O_2^-(CO_2)$ increased throughout the length of the source tube at the expense of O_2^- and $O_2^-(O_2)$ (blue traces). Distance along the length of the source tube is displayed on the x axis instead of time because the time of transit through the tube varied with air-sample pressure.

In the ion-source tube, electrons (e^{-}) were captured by O₂. and dissociatively captured by CH₃I:

$$e^- + O_2 \xrightarrow{M} O_2^-$$
 (1,2)
 $e^- + CH_3 I \rightarrow I^- + CH_3$ (3)

$$e^{-} + \mathrm{CH}_{3}I \to \mathrm{I}^{-} + \mathrm{CH}_{3} \tag{3}$$

The *M* indicates that a third molecule participates in the reaction. A portion of the initial O_2^- reacted with O_2 , CO_2 and CH₃I in the source tube and in the reaction cell yielding secondary I⁻ and O⁻₂ (CO₂) and O⁻₂ (O₂) cluster ions:

$$O_2^- + CH_3I \rightarrow \to I^- + O_2 + CH_3 \tag{4}$$

$$O_2^- + CO_2 \xrightarrow{M} O_2^- (CO_2) \tag{5}$$

$$O_2^- + O_2 \xrightarrow{M} O_2^- (O_2)$$
(55)



Figure 3. Ion densities – arbitrary units – along the 210 Po source tube for flow conditions of 306 hPa ambient pressure (dashed lines) and 1013 hPa (solid lines). The predominant ion after e^- is $O_2^-(CO_2)$ and I^- is the smallest.

Note reaction numbers follow their order within the model code. Reaction (4) was inferred based on O_2^- reactivity with CH₃F, CH₃Cl, CH₃Br, CF₄, CF₃Cl, CF₃Br and CF₃I (Fehsenfeld et al., 1975; Streit, 1982; McDonald and Chowdhury, 1985; Grimsrud, 1992; Morris, 1992; Kazil, 2002). At high CH₃I mixing ratios such as those used in Slusher et al. (2004) and Le Breton (2012) without O2 or CO2, CH3I initially captured the electrons and I⁻ was the primary neg-

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ative reagent ion generated within the ion source tube. For our reagent mixture, the model indicated approximately 20% of the initial electrons lead to I⁻ formation and 80% to $O_2^$ and its clusters. The secondary formation of I⁻ from O_2^- was small. At the end of the ion source tube, the concentrations of the primary reagent ions: O_2^- , O_2^- (CO₂) and I⁻, were predicted at comparable concentrations.

In the termolecular reactions above, others below, and in Appendix Table A2, M represented the concentration of all other gases, mostly N₂ followed by O₂, H₂O, Ar and CO₂, whereas in the experiments used to determine reaction rate constants, M usually represented a single predominant gas like O₂, CO₂, Ar or He. N₂ or H₂O were seldom included as the third body. In the case of electron attachment, Pack and Phelps (1966) noted faster rates of e^- attachment with H₂O as the third body compared to O₂ or CO₂ and that rates with these two gases were faster than those when N₂ was the third body. Under humid conditions in the reaction cell section, this was a potential source of error, larger than the factor of two given above. Electron concentrations at the end of the source tube were predicted, under our assumptions, to be a factor three larger than any of the other reagent ions.

Figure 4 shows the predicted concentrations of I^- , O_2^- , $O_2^-(CO_2)O_3^-$ and CO_3^- ions, ion-hydrates and analyte-ion clusters along the length of the reaction cell after the ion source stream was mixed with the sample air stream for the fully developed model. In Fig. 4, distance along the reaction cell was used for the x axis for consistency with Fig. 3, although the transit time through this section was constant and time or distance were equivalent. The reaction cell transit time was 17.8 ms. Two representative simulations are shown, one with an atmospheric pressure and subsequent sample flow rate commensurate with 1013 hPa and air sample water vapor mixing ratio of 17 800 ppm (16 °C dew point temperature) and the other with a sample pressure of 307 hPa, a commensurate sample flow rate and water vapor mixing ratio of 1000 ppm ($-32 \degree C$ frost point temperature). The corresponding reaction cell water vapor mixing ratios were \sim 9700 and \sim 130 ppm, respectively. The ions and ion-hydrates were at or near steady-state approximately 1/3 of the way down the reaction cell length. The ion-analyte clusters increased steadily down the length of the cell (Fig. 4e), with the exception of $I^-(H_2O_2)$ and $I^-(HAc)$ and possibly $O_2^-(H_2O_2)$, which peaked at 1 to 3 cm and then decline with distance down the remainder of the reaction cell. This was attributed to the time needed to form the clusters of interest and their titration after formation by ion–ion recombination with N_2^+ . This suggested a longer flow tube could improve sensitivity for those ions which have not reached their maximum value by the end of the reaction cell but at the expense of those clusters which have already peaked.

The ambient ozone mixing ratio was set to 50 ppb in all cases show here. No appreciable difference in O_2^- (H₂O₂), O_2^- (CH₃OOH), O_2^- (CO₂) (H₂O₂), O_2^- (H₂O₂), I^- (HFo) and I^- (HAc) sensitivity was observed when the assumed

sample O₃ mixing ratio was halved, doubled or set to 500 ppb. The latter was apropos to the UTLS (upper troposphere lower stratosphere). Simulated hydroperoxide and organic acid sensitivities were relatively unchanged even with a 10-fold increase in O₃. However, as will be discussed later, O₃ influenced potential isobaric interferences at m/z 66, O₃⁻ (H₂O), and 80, ¹⁸O of CO₃⁻ (H₂O) and the changes in O₃ resulted in a nearly proportionate increase in these ions. As an aside to O₃⁻ and CO₃⁻ chemistries, O'Sullivan et al. (2018) proposed to use CO₃⁻ as a hydroperoxide reagent ion following the work of Cappa and Elrod (2001) but were unsuccessful in its implementation. Our simulations indicated O'Sullivan's O₃ reagent concentrations were likely too low.

Figures 5a-10a show experimentally determined sensitivities as a function of reaction cell water vapor mixing ratio for $O_{2}^{-}(H_{2}O_{2}), O_{2}^{-}(CH_{3}OOH), O_{2}^{-}(CO_{2})(H_{2}O_{2}), I^{-}(H_{2}O_{2}),$ I⁻ (HFo) and I⁻ (HAc), respectively. The field and laboratory calibration data were primarily dependent upon humidity and secondarily on sample ambient pressure. The experimental data were first binned by humidity irrespective of ambient or sample pressure. The horizontal bar of the plus symbol denotes the limits of a reaction cell water vapor mixing ratio bin and is plotted at the mean sensitivity for that bin. The length of the vertical bar of the plus symbol indicates one standard deviation of the bin and the variability was due to variations arising from pressure, ambient concentrations during the standard addition, systematic variations due to water vapor across a bin, calibration gas precision and instrument precision. The yellow shaded portions outlined the experimentally determined sensitivity from laboratory experiments and field calibrations from DC3 and FRAPPE.

Figures 5b-10b show the model simulated ion-analyte cluster sensitivities at the end of the reaction cell as a function of reaction cell water vapor mixing ratio and ambient sample pressure for the fully developed model. The simulated ion-analyte cluster sensitivities are expressed in arbitrary units as Lee et al. (2014) and Iyer et al. (2016) have argued instrumental factors make it nearly impossible to map simulated instrument sensitivity to that determined experimentally. However, assuming instrumental process effects were proportional for each individual ion-neutral cluster, instrument sensitivity trends with pressure and water vapor for each ion-neutral should be captured by the simulations and scalable on an individual basis. "Sensitivity", as shown, is the ion cluster concentration divided by the analyte's ambient mixing ratio, 1 ppb, and was expected to be proportional to counts per ppb. These were further scaled to a maximum of 1 by dividing the predicted sensitivities by the maximum sensitivity calculated for that cluster regardless of sample pressure or humidity.



Figure 4. Simulated ion cluster densities along the reaction cell path for ambient pressure of $P_a = 307$ hPa and reaction cell H₂O = 133 ppm (dashed line) or $P_a = 1013$ hPa and reaction cell H₂O = 9706 ppm (solid line). Ambient O₃ was set equal to 50 ppb for both pressures. Reaction cell time of transit is $t_x = 17.8$ ms. (a) Unhydrated reagent ion density. (b) First-hydrate reagent ion density. (c) Second-hydrate reagent ion densities. (d) Third-hydrate reagent ion densities. (e) Ion–analyte cluster ion density–arbitrary units.

4 Discussion

The initial model mechanism including O_2^- , O_2^- (H₂O), O_2^- (CO₂), I⁻ and I⁻ (H₂O) alone was unable to simulate the sample pressure and water dependent trends in sensitivity for O_2^- (H₂O₂), O_2^- (CH₃OOH), O_2^- (CO₂) (H₂O₂), I⁻ (H₂O₂),

I⁻ (HFo) and I⁻ (HAc), not shown. The simulated O_2^- hydroperoxide cluster sensitivity showed too steep of an increase to the maximum value and then too steep of a decrease after the maximum as the water vapor mixing ratio varied from 10 to 20000 ppm. The maximum sensitivity was at water vapor mixing ratios near a few 100 ppm.



Figure 5. (a) Experimental sensitivity (counts per second per ppb, $\operatorname{cps} \operatorname{ppb}^{-1}$) trend in $O_2^- (H_2O_2)$ as a function of reaction cell water vapor mixing ratio (χ_{H_2O} , ppm), from DC3 (red), FRAPPE (blue), and the laboratory [$F_{CH_3I} = 0.0005$ (cyan) and 0.001 (green) slpm]. All calibrations were binned by χ_{H_2O} and bin widths are shown by the horizontal lines. Vertical bars indicate one standard deviation of a bin and include sample pressure variation effects, water variation within a bin, precision of the standard addition calibration gas concentration, instrument precision and ambient mixing ratio variation across the standard addition period. There were fewer than four observations per bin in FRAPPE for water vapor mixing rations less than 10^3 ppm. Magenta crosses in panel (a) correspond to DC3 post mission calibrations without the addition of CH₃I and after there had been multiple refills of the reagent CO₂ in air bottle. (b) Normalized simulated sensitivity as a function of χ_{H_2O} for six different sample pressures as shown in the legend. The yellow shading maps the trends in experimental sensitivity (a) to the calculated trends in sensitivity (b) using the same normalization process.



Figure 6. Same as Fig. 5 except for O_2^- (CH₃OOH).

The addition of reactions leading to higher order ion hydrates, $(H_2O)_{n>1}$, carbonates, $(CO_2)_{n>1}$ and mixed hydratecarbonates, $(H_2O)_m(CO_2)_n$, were included to reduce the steepness on each side of the maximum (see Supplement for details).

The mechanism so modified remained insufficient to reproduce the O_2^- and O_2^- (CO₂) peroxide sensitivities as a function of reaction cell H₂O mixing ratio and ambient sample pressure (not shown) observed in the field and laboratory measurements. Multiple avenues were explored including (see Supplement):

modification of reaction rate coefficients for Reactions (12), (13), (14), (21), (24), (147), and (148), which describe the O₂⁻ - (H₂O) - (CO₂) switching system;



- 2. the inclusion of Reactions (149)–(152) allowing for higher order hydrates to form the analyte cluster ions for peroxides;
- the inclusion of O₃ reactions with O₂⁻ to yield O₃⁻ and subsequent CO₃⁻ ions;
- 4. invoking a new carbonation Reaction (199),

$$O_2^-(H_2O_2) + (CO_2) + M \to O_2^-(CO_2) (H_2O_2) + H_2O + M;$$
 (199)

5. the addition of Reactions (204)–(209) allowing for higher order hydrates of I⁻ to form the analyte cluster ions for hydrogen peroxide and the organic acids.



Figure 7. Same as Fig. 5 except for $O_2^-(CO_2)(H_2O_2)$.



Figure 8. Same as Fig. 5 except for $I^-(H_2O_2)$. Magenta crosses in panel (a) correspond to DC3 post mission calibrations without the addition of CH₃I; there had been multiple refillings of the reagent CO₂ in the air bottle and the CH₃I reagent gas concentration is presumed to be very small.

The addition of O3 chemistry had little effect on sensitivity, whereas the first two changes improved the pressure dependent sensitivity and water vapor trends for the O_2^- hydroperoxide clusters but did not significantly improve the pressure and water vapor sensitivity trends in $O_2^-(CO_2)(H_2O_2)$, necessitating a process like Reaction (199).

Under low water vapor conditions the model under predicted O_2^- (H₂O₂) and O_2^- (CH₃OOH) at higher sample pressures relative to low sample pressures. This was primarily due to the conversion of most of the O_2^- reagent ion to $O_2^-(CO_2)$ in the absence of water vapor (e.g., Kebarle et al., 1972). The conversion of O_2^- to O_3^- was of minor influence. Significantly, at higher water vapor mixing ratios, the O_2^- hydroperoxide clusters and the O_2^- (CO₂) (H₂O₂) cluster were under predicted because of O_2^- hydrate formation, $O_2^{-}(H_2O)_{n=1.5}$ and the switching reactions included in the initial mechanism:

$$O_2^-(H_2O) + H_2O_2 \to O_2^-(H_2O_2) + H_2O$$
 (28)

$$O_{2}^{-}(H_{2}O) + CH_{3}OOH \rightarrow O_{2}^{-}(CH_{3}OOH) + H_{2}O$$
 (36)

with rate coefficients set at approximately the collision limit (3×10^{-9}) were unable to simulate enough hydroperoxide cluster formation.

A solution to the low humidity problem was suggested by the work of Fehsenfeld and Ferguson (1974), Fahey et al. (1982) and Böhringer et al. (1984). Böhringer et al. (1984) suggested there is a hierarchical shift in cluster ion ligands, $X^- \cdot L$, according to ion-ligand bond energy (E_{bond}), for a specific ion. Their ordering followed: $E_{\text{bond}} (X^- \cdot H_2 O) <$ $E_{\text{bond}}(X^- \cdot \mathrm{SO}_2) < E_{\text{bond}}(X^- \cdot \mathrm{H}_2\mathrm{O}_2) <$ $E_{\text{bond}}(X^- \cdot \text{HCl}) < E_{\text{bond}}(X^- \cdot \text{HNO}_3).$ Adams et al. (1970), Fehsenfeld and Ferguson (1974) and Fahey et al. (1982) presented and discussed the thermodynamics and kinetics of O_2^- , $O_2^-(O_2)$, $O_2^-(CO_2)$, $O_2^-(H_2O)_{n=1,3}$ and $O_2^-(CO_2)(H_2O)_{n=1,3}$. Their bond energies suggested the series given by Böhringer et al. (1984) could be extended to include O_2 and CO_2 as ligands with O_2 more weakly bound than H₂O and with CO₂ and H₂O being comparably bound, such that: $E_{\text{bond}}(X^-N_2) < E_{\text{bond}}(X^-O_2) <$ $E_{\text{bond}}(X^-\text{H}_2\text{O}) \approx E_{\text{bond}}(X^-\text{CO}_2) < E_{\text{bond}}(X^-\text{SO}_2) <$



Figure 9. Same as Fig. 5 except for I^- (HFo). Field calibrations for HFo were not performed in DC3.



Figure 10. Same as Fig. 9 except for $I^-(HAc)$. Field calibrations for HAc were not performed in DC3.

 $E_{\text{bond}}(X^-\text{H}_2\text{O}_2) \approx E_{\text{bond}}(X^-\text{CH}_3\text{OOH}) < E_{\text{bond}}(X^-\text{HCl}) < E_{\text{bond}}(X^- + \text{HNO}_3)$. Last, ab initio calculations suggested the ligand bond energy of CH₃OOH lies above H₂O and near or just below H₂O₂ (Cappa and Elrod, 2001) or well above that of both H₂O and H₂O₂ (O'Sullivan et al., 2018). Consequently, we have speculated that both peroxides may readily switch with the CO₂ in O₂⁻(CO₂) and have included the following two CO₂ – peroxide "switching" reactions in the model mechanism:

$$O_2^-(CO_2) + H_2O_2 \to O_2^-(H_2O_2) + CO_2$$
 (160)

$$O_2^{-}(CO_2) + CH_3OOH \rightarrow O_2^{-}(CH_3OOH) + CO_2$$
(161)

From sensitivity studies varying forward rate constants, k_{160} and k_{161} , rate coefficient values of 2×10^{-12} and 1×10^{-12} cm⁻³ molec⁻¹ s⁻¹, respectively, or greater were sufficient to remove the pressure dependent discrepancy in O_2^- peroxide sensitivity noted at low water vapor mixing ratios. The magnitude of these rate coefficients was reasonable given the bonding energy progression and the rate coefficients reported by Adams et al. (1970) for CO₂–H₂O switch-

ing reactions:

$$O_{2}^{-}(H_{2}O) + CO_{2} \rightarrow O_{2}^{-}(CO_{2}) + H_{2}O$$

$$k_{12} = \sim 6 \times 10^{-10}$$

$$O_{2}^{-}(CO_{2}) + H_{2}O \rightarrow O_{2}^{-}(H_{2}O) + CO_{2}$$

$$k_{13} = \sim 2 \times 10^{-10}$$
(13)

where, $k_{13} = k_{12}/K_{eq}$ (2.3), and those estimated by Fahey et al. (1982) for:

$$O_2^-(H_2O)_2 + CO_2 \rightarrow O_2^-(CO_2) (H_2O) + H_2O$$

 $k_{147} = 7 \times 10^{-11}$ (147)

and

$$O_2^-(CO_2)(H_2O) + H_2O \rightarrow O_2^-(H_2O)_2 + CO_2$$

 $k_{148} \sim 1 \times 10^{-9}$ (148)

Finally, a new hybrid clustering reaction was invoked:

$$O_2^-(H_2O_2) + (CO_2) + M \rightarrow O_2^-(CO_2)(H_2O_2) + M$$

$$k_{199} = 5.0 \times 10^{-29},\tag{199}$$

which finally enabled the modified chemical mechanism to resolve the pressure and water vapor trends in O_2^- and O_2^- (CO₂) peroxide sensitivities as shown in Figs. 5b–7b. This reaction has a calculated Gibb's reaction energy of 7kJ mol⁻¹ (see Supplement) and is therefore not spontaneous. However, as discussed within the Supplement, the reaction is expected to be exothermic, many of the formation and reaction enthalpy and Gibb's energy terms used to derive this value were from experimental data having factor of two uncertainties in rates, and 5 to 10 kJ mol⁻¹ uncertainties. A Gibb's reaction energy of 7 kJ mol⁻¹ is at the 6th significant figure of the ab initio calculations and may be near the limit of the theoretical calculations of O'Sullivan et al. (2018) from which it was derived.

The pressure and humidity trends exhibited in the laboratory CH_3I experiments and in the field calibrations for H_2O_2 (Fig. 8; DC3 and FRAPPE); HFo (Fig. 9; FRAPPE) and HAc (Fig. 10; FRAPPE) could not be reconciled using only monohydrate switching reactions (Reactions 30–33, 38–41, and 42–45). The decrease in sensitivity with increasing humidity was too steep (not shown), and hypothesized reactions (Reactions 204–209) were added. These reactions likely summarize multistep sequences such as:

$$I^{-}(H_2O)_n + A \rightarrow I^{-}A(H_2O)_{n-1} + H_2O$$

...
 $I^{-}A(H_2O) \xrightarrow{M} I^{-}A + H_2O.$

where A represents H_2O_2 , HFo or HAc. It should be noted that Reactions (205), (207) and (209) involving $I^-(H_2O)_3$ were inconsequential in reconciling the observed pressure and humidity trends in sensitivity even when reaction rate coefficients were set equal to those of Reactions (204), (206) and (208). Consequently, the reaction rate coefficients for the $I^-(H_2O)_3 + A$ reactions were unconstrained by our analyses.

The families of O_2^- and I^- concentrations from the fullmodel chemical mechanism are shown in Fig. 11 as a function of reaction cell water vapor mixing ratio for several sample pressures. Sample flow rate (sample pressure) had virtually no effect on I^- and $I^-(H_2O)_n$ concentrations, whereas, the reaction cell water vapor mixing ratio has a very strong effect on $I^-(H_2O)_n$ at all levels and on I^- when the mixing ratio is above 10^3 ppm. Sample flow rate and reaction cell water vapor mixing ratio have a profound effect on $O_2^-(H_2O)_n$ and $O_2^-(CO_2)_n$ speciation and their concentrations. It was the steep drop in $O_2^-(CO_2)$ at water vapor mixing ratios greater than 10^2 ppm, which necessitated the invocation of a reaction like Reaction (199) to predict the experimental sensitivity trends observed at m/z 110 for $O_2^-(CO_2)(H_2O_2)$.

The I^- (H₂O₂) sensitivity was a critical test point in adjusting the laboratory and FRAPPE CH₃I concentrations to best match the sensitivity observed in DC3 (Treadaway, 2015; Treadaway et al., 2018). The measurement objective in DC3 was the quantification of H_2O_2 and CH_3OOH and it was conducted without organic acid field standards. During DC3 it was recognized there were quantifiable but uncalibrated signals at spectral locations attributed to I⁻ (HFo) and I⁻ (HAc) (Treadaway, 2015; Treadaway et al., 2018). Post mission calibrations and calibrations during the FRAPPE field campaign with hydroperoxides provided an estimate of the CH₃I reagent concentration as evidence by I⁻ (H₂O₂) and its trends with pressure and humidity (Fig. 8). The modeled trends in I⁻ (H₂O₂) reinforce this and provide collaborative data supporting the extrapolation of the laboratory and FRAPPE HFo and HAc sensitivities to DC3 (Treadaway, 2015; Treadaway et al., 2018).

Many of the reaction rate coefficients used to model analyte cluster ion sensitivity trends with water vapor and pressure have been estimated by ourselves and others. This introduces uncertainties to the results but within the constraints of the calibration data. The reaction rate coefficient for Reaction (38) is used as an example of the constraints placed on the rate of Reaction (38) in the context of Reactions (38)-(41), the I⁻ hydrate Reactions (17), (18), (78)–(81) and the inferred higher hydrate switching Reactions (206) and (207). The estimated rate was $1.5 \times 10^{-10} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1}$. Doubling the rate constant for Reaction (38) led to a flattening of the linear trend in I⁻ (HFo) sensitivity with water vapor at low water vapor mixing ratios and too sharp a peak at the maximum sensitivity. Halving the reaction rate coefficient for Reaction (38) excessively steepened the trend in I⁻ (HFo) sensitivity with water vapor. The reaction rate coefficient for Reaction (40) would have to exceed the bimolecular rate limit in order to increase the reaction rate coefficient for Reaction (39) and maintain the observed sensitivity trend. The same would also apply to Reaction (206) needed to broaden the maximum in sensitivity in I⁻ (HFo) at 10 000 ppm water vapor. The reaction rate coefficient for Reaction (38) could be reduced but would require proportionate reductions in the reaction rate coefficients for the linked reactions to maintain the modeled sensitivity trend. A halving or doubling was used for the purpose of illustration as this was within the range of uncertainty quoted for many of the measured reaction rate coefficients in the literature.

The model was further used to examine the potential for isobaric interference at m/z 80, where CH₃OOH is observed, and at m/z 66, a potential m/z for H₂O₂ (Table 1). Figure 12a shows the predicted concentrations of O₂⁻ (H₂O₂), ¹⁸O of NO₂⁻ (H₂O), O₃⁻ (H₂O) and ¹⁸O of O₂⁻ (O₂) all of which would appear at m/z 66. The interference ion production pathways involving NO₂⁻, NO₃⁻, CO₃⁻, O₃⁻ and O₂⁻ (O₂) are outlined in the Appendix, Table A4. Figure 12b shows the predicted concentrations of O₂⁻ (CH₃OOH), ¹⁸O of CO₃⁻ (H₂O) and NO₃⁻ (H₂O), which would all be observed at m/z 80. The simulations assumed the ambient air contained NO, NO₂, HNO₃, H₂O₂, CH₃OOH, HFo and HAc at mixing ratios of 1 ppb for each. O₃ and CO₂ were assumed



Figure 11. (a) Oxygen anion speciation: O_2^- , $O_2^-(H_2O)_{n=1,3}$, $O_2^-(CO_2)_{n=1,2}$, $O_2^-(CO_2)(H_2O)$ and $O_2^-(O_2)$, as a function of water vapor at sample pressures of 120 (dotted), 300 (dashed) and 1013 (solid) hPa. (b) As in panel (a) except for iodide speciation: I^- , $I^-(H_2O)$, $I^-(H_2O)_2$ and $I^-(H_2O)_3$.

to be 50 ppb and 400 ppm, respectively. The ambient water vapor mixing ratio and sample pressure were varied from 10 to 3×10^5 ppm and from 120 to 1013 hPa, respectively. Note that while reaction cell water vapor pressures from 1 to 10^5 ppm can be prescribed, the higher mixing ratios at the lower sample pressures simulated were unrealistic owing to the decrease in air temperature, maximum dew point temperature and consequent decrease in maximum air saturation vapor pressure with decreasing air pressure (increasing altitude). The dotted lines (left panel) indicate the contribution to m/z 66 from O₃⁻ (H₂O) which was proportional to the O₃ mixing ratio but which passed through a maximum with respect to water vapor, increasing at lower humidities due to Reaction (19) and then decreasing at higher humidities due to Reaction (72). At the highest sample pressure, $O_3 = 200 \text{ ppb}$ yields a maximum predicated interference of $\sim 1.6 \times 10^6$ A.U. at 2×10^3 ppm of water and was comparable to the predicted signal from 1 ppb H₂O₂. Increasing NO₂ to 100 ppb lead to a 18O of NO₂ (H₂O) predicted interference comparable to the signal for 1 ppb H₂O₂. Note reductions in H₂O₂ mixing ratios increase the potential for interference by these other gases. ¹⁸O of $O_2^-(O_2)$ is not predicted to be a significant interference at any of the pressures or humidities examined. The above discussion assumes PCIMS does not inherently discriminate between clusters due to instrumental factors.

The measurement of CH₃OOH at m/z 80 is predicted to suffer from interference by both ¹⁸O of CO_3^- (H₂O), and NO_3^- (H₂O). O₃ through reaction sequence (8), (9) and (15) leads to the formation of CO_3^- (H₂O) and a predicted inference was proportional to the O₃. The predicted interference as a function of the H₂O mixing ratio passed through a maximum, increasing at first due to Reaction (15) and then decreasing due to Reaction (53). NO primarily through reactions with O_3^- or $O_2^-(H_2O)_{n\geq 1}$ produced NO₃⁻, which went on to form a hydrate. The predicted NO₃ (H₂O) interference also passed through a maximum as a function of water vapor due to Reactions (115) and (116). At reaction-cell water-vapor mixing ratios greater than a few hundred ppm, $O_3 = 50$ ppb and NO = 1 ppb gave predicted interference signals comparable to the signal from 1 ppb of CH₃OOH. In the DC3 project after research flight 12 and throughout FRAPPE, m/z 78 was monitored for CO₃⁻ (H₂O) to ensure an ¹⁸O isotope of this compound did not appreciably interfere in the measurement of CH₃OOH. Similarly, m/z 62, 78 and 98, corresponding to NO_3^- , CO_3^- (H₂O) and NO_3^- (H₂O)₂ or ¹⁸O of $CO_3^-(H_2O)_2$ were monitored to ensure $NO_3^-(H_2O)$ did not appreciably interfere in the CH₃OOH measurement.



Figure 12. (a) Predicted ion cluster concentrations for species having m/z equal to 66: $O_2^-(H_2O_2)$ solid lines, ${}^{18}O$ of $NO_2^-(H_2O)$ dashed lines, $O_3^-(H_2O)$ dotted lines and ${}^{18}O$ of $O_2^-(O_2)$ dash-dot lines, for six sample pressures (hPa) indicated by color as given in the legend. (b) Predicted ion cluster concentrations for species having m/z equal to 80: $O_2^-(CH_3OOH)$ solid lines, ${}^{18}O$ of $CO_3^-(H_2O)$ dashed lines and $NO_3^-(H_2O)$ dash-dot lines, for six sample pressures (hPa) indicated by color as given in the legend. See text for sample air flow rate and composition and reagent gas composition used in the simulation.

As above this assumes PCIMS does not inherently discriminate between clusters due to instrumental factors nor does it discriminate between the oxygen isotopic clusters of CO_3^- (H₂O).

Currently, experimental kinetic data to examine the isobaric interferences for I⁻ (HFo) and I⁻ (HAc) by ethanol and propanol, methyl formate or glycolaldehyde, respectively are unavailable. Treadaway (2015) and Treadaway et al. (2018) tested ethanol and 1-propanol and 2-propanol at very low and high water vapor conditions and found the sensitivity for I⁻ (HFo) was 100 times that for I⁻ (ethanol) and the sensitivity for I⁻ (HAc) was 100 times that for I⁻ clustering with either 1- or 2-propanol. These relative sensitivities agreed with those predicted by Siddharth Iyer (personal communication, 2017) for HFo, HAc, ethanol and 2-propanol based upon their calculated binding energies with I⁻.

In review, it was pointed out the model did not include the ion-neutral chemistry of organic compounds, specifically the potential for oxygen superoxide ion to abstract a proton from acetic acid, and subsequently acetate ion to abstract a proton from weaker acids. Currently, the paucity of reaction rate coefficients for O_2^- + organic reactions precludes their inclusion in our model. We must note, the potential exists for such chemistry to impact the simulations and we are unable to quantitatively assess their importance.

5 Conclusions

An ion-neutral chemical kinetic model is described and used to simulate the negative ion chemistry occurring within a mixed-reagent ion chemical ionization mass spectrometer (CIMS). The model established a theoretical basis for investigation of ambient pressure (variable sample flow and reagent ion carrier gas flow rates), water vapor, ozone and oxides of nitrogen effects on ion cluster sensitivities for hydrogen peroxide (H₂O₂), methyl peroxide (CH₃OOH), formic acid (HCOOH) and acetic acid (CH₃COOH). The model was built with established mechanisms, thermodynamic data and reaction rate coefficients and these were augmented with additional reactions with estimated reaction rate coefficients. Some existing reaction rate coefficients were modified to enable the model to match laboratory and field campaign determinations of ion cluster sensitivities as functions of CIMS sample flow rate and ambient humidity. Relative trends in sensitivity were compared as instrument specific factors preclude a direct calculation of instrument sensitivity. Predicted sensitivity trends and experimental sensitivity trends suggest the model captured the PCIMS reagent ion and cluster chemistry and reproduced observed trends in ion cluster sensitivity with sample flow and humidity. The model was further used to investigate the potential for isobaric compounds as interferences in the measurement of the above species. For ambient O₃ mixing ratios more than 50 times those of H_2O_2 , O_3^- (H_2O) is predicted to be a significant isobaric interference to the measurement of H_2O_2 using $O_2^-(H_2O_2)$ at m/z 66. O₃ and NO give rise to the species and cluster ions, CO_3^- (H₂O) and NO₃⁻ (H₂O), respectively, which interfere in the measurement of CH_3OOH using $O_2^-(CH_3OOH)$ at m/z 80. The CO₃⁻ (H₂O) interference requires one of the O atoms to be the stable isotope ^{18}O . The model results indicate monitoring water vapor mixing ratio, m/z 78 for CO_3^- (H₂O) and m/z 98 for isotopic CO_3^- (H₂O)₂ can be used to determine when ¹⁸O of CO_3^- (H₂O) interference is significant. Similarly, monitoring water vapor mixing ratio, m/z 62 for NO₃⁻ and m/z 98 for NO₃⁻(H₂O)₂ can be used to determine when $NO_3^-(H_2O)$ interference is significant.

Data availability. The field measurements for the DC3 experiments are archived at https://www-air.larc.nasa.gov/cgi-bin/ ArcView/dc3?GV=1 and the field measurements for FRAPPE are archived at https://www-air.larc.nasa.gov/cgi-bin/ArcView/ discover-aq.co-2014?C130=1. These archives are updated as new and revised datasets are placed in the archive. The data sets follow the ICARTT format, which is described at https://www-air. larc.nasa.gov/missions/etc/IcarttDataFormat.htm. The ion-neutral chemical kinetics model and the calibration data are available from the authors. Field and laboratory sensitivity results are not typically archived. The model as written uses proprietary software, MATLAB (The MathWorks, Inc., 1 Apple Hill Drive, Natick, MA 01760-2098, USA). However, the model can be written in any language using the data contained within the method description found within the body of the text and paper's appendix.

Appendix A: Instrument details

The PCIMS instrument is shown schematically in Fig. A1 from the sample inlet to the exhaust. It was manufactured by THS Instruments, LLC (Atlanta, Georgia). The instrument consists of five separate chambers: a sample entrance chamber (labeled Split), a reaction drift tube (RXN cell), a collision dissociation chamber (CDC), a main chamber (Main), and the quadrupole and detector chamber (Quad). The entrance section allows for excess sample flow through the transfer plumbing from a sample's origin to minimize wall surface artifacts. In an aircraft, the sample probe and transfer line were heated to 35 and 70 °C during DC3 and FRAPPE, respectively. The higher temperature in FRAPPE was used because of a ground contamination problem. The sample stream is split with the fraction entering the PCIMS reaction cell (RXN Cell) determined by a 0.51 mm critical orifice; the highpressure side was set by the sample inlet pressure and the low-pressure side fixed at 22.4 hPa. The excess flow rate is regulated by an MKS Instruments (Andover, MA) 0-30 slpm mass flow controller (not shown). The reagent gas stream dynamically blends three gas streams: ultra-high purity N₂ (Scott-Marrin, Riverside, CA), 400 ppm CO₂ in ultra-high purity air (Scott-Marrin, Riverside, CA) and 5 ppm CH₃I in ultrahigh purity N2. These flows are regulated using MKS mass flow controllers (not shown). Representative reagent gas flow rates and mixing ratios for different sample air pressures are listed in Table 2. The total flow through the RXN cell is 4.68 slpm and the sample flow rate can be determined by subtraction of the reagent gas flow rates from the total flow; for example, at a sample pressure of 600 hPa, the sample flow rate was 1.61 slpm. Ions are generated by passing the reagent gas stream through a commercially available Nuclecel Ionizer (Model P2031-1000, NRD LLC., Grand Island, NY), containing an α -emitter, ²¹⁰Po, with an initial activity of 20 milli-curie. The reagent ion stream is mixed at a right angle to the sample air stream, approximately 12 mm downstream from the sample entrance orifice and 82 mm before the RXN cell to CDC chamber (collision dissociation chamber) and a pumped second port for dumping the bulk of the RXN cell reagent-sample gas stream. The RXN-to-CDC critical orifice diameter is 0.81 mm and with a high-pressure side at 22.4 hPa and a low-pressure side at 0.61 hPa, has a nominal flow rate of 0.11 slpm (http://www.tlv.com/global/ TI/calculator/air-flow-rate-through-orifice.html) assuming a discharge coefficient of 1.0. The voltage on the CDC plate is -2.0 V. The PCIMS has two THS Instruments, LLC. octopole ion lenses; one set is in the CDC (DC bias voltage = 20 V, RF voltage = 2 V) and the other is in the main chamber after the CDC (DC bias voltage = 2.49 V, RF voltage = 0.04 V). The CDC plate and first octopole voltages regulated collision energy between molecules and the cluster ions and were used to fragment weakly bound clusters. These voltages were manually adjusted to improve the signal-tonoise ratio at the m/zs of interest. The second octopole acts to focus the ions onto the entrance of the quadrupole mass selector (Extrel 19 mm rod quadrupole, controlled by an Extrel QC-150 oscillator at 2.1 MHz and a THS Instruments control board), and the ions at a selected m/z are counted by a Channeltron detector (rear plate at 3.43 kV and front plate at 1.51 kV). The pressures in the CDC, the main chamber and the octopole and quadrupole chamber were 0.61, 0.0065 and 0.00011 hPa, respectively. There are two more critical orifices which separate the CDC and the main chambers, 2.08 mm, and the main and quadrupole chambers, 2.57 mm. The nominal flow rates through these orifices are 19 and 1.3 sccm (standard cubic centimeters per second), respectively. From a mechanical perspective, 0.03 % of the total flow through the RXN cell enters the quad chamber. The above instrument settings were used throughout the DC3, laboratory, FRAPPE and post FRAPPE laboratory and field work.

The m/z range of the quadrupole filter is 1–500 m/z. The PCIMS controller software provides two modes of mass selection: "hop" and "scan". In scan mode, lower and upper m/z limits, a m/z step size and the dwell time at a m/zstep are defined. The smallest step size is 0.3 m/z. A typical dwell time for a scan is 50 ms. In hop mode, a variable number of fixed m/z values can be selected at an increment of 0.05 m/z. The dwell time at each fixed m/z can also be specified. In practice with the Channeltron detector rear plate at 3.43 kV and front plate at 1.51 k, the softwarehardware range limits are nominally 0 to 2×10^6 cps (counts per second) or for a 50 ms dwell time, 0 to 10⁵ counts. Random "dark" count noise in 50 ms was $\ll 1$ count or $\ll 20$ cps. The practical mass resolution of the quadrupole and detector was 1.0 m/z. This was defined as the average of the fullwidth at half-height of the calibration peaks for O_2^- (H₂O₂), O_{2}^{-} (CH₃OOH), O_{2}^{-} (HFo), O_{2}^{-} (HAc), O_{2}^{-} (CO₂) (H₂O₂), $I^{-}(H_2O)$, $I^{-}(H_2O_2)$, $I^{-}(HFo)$ and $I^{-}(HAc)$ at 66, 78, 80, 92, 110, 145, 161, 173 and 187 m/z, respectively, and determined using a scan step size of 0.3 m/z (mode = 0.9; range 0.9–1.2; n = 9) during a HP, MHP, HFo and HAc calibration. Treadaway et al. (2018) showed the full scan from 40 to 190 m/z.

Three schemes were employed to develop calibration mixing ratios. In the laboratory and in flight, a syringe based systems inject $< 10^{-9}$ m³ per min. of an aqueous solution containing the species of choice in to a N₂ carrier stream. This flow is constantly on. Just prior to the CIMS inlet the flow is normally diverted to waste by a "drawback" flow. This flow is turned off when calibration gas is added in to the sample stream – "standard addition". In the laboratory, two Henry's Law equilibration coils with concurrent flows of an aqueous solution containing the species of choice and an ultrahigh purity air stream as carrier. The coils are immersed in a temperature controlled water bath. These systems are show as block diagrams in Fig. A2.



Figure A1. Block schematic of the PCIMS instrument as used on the aircraft and in the laboratory, mass flow controllers are not shown. As per Slusher et al. (2004), Le Breton et al. (2012), O'Sullivan et al. (2018) and Treadaway et al. (2018).



Figure A2. Block schematic of laboratory (**a**) and in-flight calibration systems (**b**), mass flow controllers are not shown. After Treadaway et al. (2018).

Index	Species	Index	Species	Index	Species
Neutral	species				
4	CH ₃ I	20	CH ₃ OOH	3	CO ₂
21	HFo (formic acid)	22	HAc (acetic acid)	55	HNO ₃
16	H ₂ O	19	H_2O_2	1	N ₂
41	NO	42	NO ₂	2	O ₂
10	O ₃				
Positive	e species				
5	N ₂ ⁺				
Negativ	ve species				
12	CO_3^-	15	$CO_3^-(H_2O$	31	$CO_{3}^{-}(H_{2}O)_{2}$
38	$CO_{3}^{-}(H_{2}O)_{3}$	65	$CO_3^{-}(H_2O_2)$	67	CO ₃ (CH ₃ OOH
6	e^{-3}	34	HO ⁻	59	$HO^{-}(H_2O)$
60	$HO^{-}(H_2O)_2$	61	$HO^{-}(H_2O)_3$	7	I
17	$I^{-}(H_2O)$	39	$I^{-}(H_{2}O)_{2}$	40	$I^{-}(H_2O)_3$
25	$I^{-}(H_2O_2)$	27	I ⁻ (HFo)	28	I ⁻ (HAc)
64	$I^{-}(O_{3})$	43	NO ⁻	44	$NO^{-}(H_2O)$
45	$NO^{-}(H_2O)_2$	46	$NO^{-}(H_2O)_3$	47	NO_2^-
48	$NO_2^-(H_2O)$	49	$NO_2^-(H_2O)_2$	50	$NO_2^{-}(H_2O)_3$
56	$NO_2^{-}(H_2O_2)$	51	NO_3^2	62	ONÕO-
58	$NO_2^{-}(HFo)$	52	$NO_{2}^{-}(H_{2}O)$	53	$NO_{2}^{-}(H_{2}O)_{2}$
54	$NO_{2}^{-}(H_{2}O)_{3}$	72	$NO_{2}^{-}(H_{2}O)_{4}$	57	$NO_{2}^{-}(H_{2}O_{2})$
32	0-3 2 75	33	$O^{-}(H_2O)$	8	0_{2}^{-3}
26	$O_{2}^{-}(CH_{3}OOH)$	9	$O_2^{-}(CO_2)$	14	$O_{2}^{2}(CO_{2})(H_{2}O)$
69	$O_{2}^{-}(CO_{2})(H_{2}O)_{2}$	73	$O_{2}^{-}(CO_{2})(H_{2}O)_{3}$	23	$O_{2}^{-}(CO_{2})(H_{2}O_{2})$
13	$O_{2}^{2}(H_{2}O)$	30	$O_{2}^{2}(H_{2}O)_{2}$	35	$O_{2}^{2}(H_{2}O)_{3}$
70	$O_{2}^{-}(H_{2}O)_{4}$	71	$O_{2}^{-}(H_{2}O)_{5}$	24	$O_{2}^{-}(H_{2}O)(H_{2}O)$
63	$O_{2}^{-}(H_{2}O_{2})$	29	$O_{2}^{-}(O_{2})$	11	0_{2}^{-}
20 20	$O^{-}(CH_{2}OOH)$	18	$O_{2}^{-}(U_{2})$	36	$O^{-}(H_{2}O)_{2}$
0.0					

alphabetically d b al cie Table A1. Ion and

Reaction	Reaction rate coefficient ^a (reference) ^b	Index
$CO_3^- + CH_3OOH + M \rightarrow CO_3^-(CH_3OOH) + M$	1.0×10^{-28}	170
$\operatorname{CO}_3^- + \operatorname{H}_2\operatorname{O} + M \to \operatorname{CO}_3^-(\operatorname{H}_2\operatorname{O}) + M$	1.0×10^{-28} (FF, NIST)	15
$CO_3^- + HNO_3 \rightarrow NO_3^- + CO_2 + HO$	3.5×10^{-10} (Kaz)	144
$\operatorname{CO}_{3}^{-} + \operatorname{H}_{2}\operatorname{O}_{2}^{-} + M \rightarrow \operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}_{2}) + M$	1.0×10^{-28} (est)	162
$CO_3^- + NO \rightarrow NO_2^- + CO_2$	1.1×10^{-11}	83
$CO_3^- + NO_2 \rightarrow NO_3^- + CO_2$	2.0×10^{-10}	84
$\mathrm{CO}_3^- + \mathrm{N}_2\mathrm{O} \rightarrow \mathrm{O}_2^-(\mathrm{CO}_2) + \mathrm{N}_2$	5.0×10^{-13} (Kov)	69
$\overline{\mathrm{CO}_{3}^{-}(\mathrm{H}_{2}\mathrm{O}) + M \rightarrow \mathrm{CO}_{3}^{-} + \mathrm{H}_{2}\mathrm{O} + M}$	$3.5 \times 10^{-14} (FF)$	16
	3.9×10^{-14} (<i>Kaz</i>)	
$\operatorname{CO}_3^-(\operatorname{H}_2\operatorname{O}) + \operatorname{CH}_3\operatorname{OOH} \to \operatorname{CO}_3^-(\operatorname{CH}_3\operatorname{OOH}) + \operatorname{H}_2\operatorname{O}$	1.0×10^{-9}	171
$\operatorname{CO}_3^-(\operatorname{H}_2\operatorname{O}) + \operatorname{H}_2\operatorname{O} + M \to \operatorname{CO}_3^-(\operatorname{H}_2\operatorname{O})_2 + M$	2.1×10^{-28}	53
$CO_3^-(H_2O) + H_2O_2 \rightarrow CO_3^-(H_2O_2) + H_2O$	1.0×10^{-9}	163
$\mathrm{CO}_3^-(\mathrm{H}_2\mathrm{O}) + \mathrm{NO} \rightarrow \mathrm{NO}_2^- + \mathrm{CO}_2 + \mathrm{H}_2\mathrm{O}$	3.5×10^{-12}	85
$\mathrm{CO}_{3}^{-}(\mathrm{H}_{2}\mathrm{O}) + \mathrm{NO} \rightarrow \mathrm{NO}_{2}^{-}(\mathrm{H}_{2}\mathrm{O}) + \mathrm{CO}_{2}$	3.5×10^{-12}	86
$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}) + \operatorname{NO}_{2} \rightarrow \operatorname{NO}_{3}^{-} + \operatorname{CO}_{2} + \operatorname{H}_{2}\operatorname{O}$	4.0×10^{-11} (Kaz)	87
$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}) + \operatorname{NO}_{2} \rightarrow \operatorname{NO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}) + \operatorname{CO}_{2}$	4.0×10^{-11} (Kaz)	88
$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O})_{2} + M \to \operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}) + \operatorname{H}_{2}\operatorname{O} + M$	3.7×10^{-12} (<i>NIST</i>)	54
$CO_3^-(H_2O)_2 + CH_3OOH \rightarrow CO_3^-(CH_3OOH) + 2H_2O$	1.0×10^{-10}	172
$CO_{3}^{-}(H_{2}O)_{2} + H_{2}O + M \rightarrow CO_{3}^{-}(H_{2}O)_{3} + M$	1.7×10^{-28}	76
$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O})_{2} + \operatorname{H}_{2}\operatorname{O}_{2} \rightarrow \rightarrow \operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}_{2}) + 2\operatorname{H}_{2}\operatorname{O}_{2}$	1.0×10^{-10}	164
$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O})_{3} + M \rightarrow \operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O})_{2} + \operatorname{H}_{2}\operatorname{O} + M$	1.3×10^{-11} (<i>NIST</i>)	77
$CO_3^-(H_2O)_3 + CH_3OOH \rightarrow CO_3^-(CH_3OOH) + 3H_2O$	1.0×10^{-11}	173
$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O})_{3} + \operatorname{H}_{2}\operatorname{O}_{2} \rightarrow \rightarrow \operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}_{2}) + 3\operatorname{H}_{2}\operatorname{O}$	1.0×10^{-11}	165
e^- + CH ₂ I \rightarrow I ⁻ + CH ₂	1.0×10^{-7} (est)	3
$e^+ + O_2 + N_2 \rightarrow O_2^- + N_2$	1.0×10^{-31} (H)	2
$e^{-} + \Omega_2 + \Omega_2 \rightarrow \Omega_2^{-} + \Omega_2$	1.9×10^{-30} (H)	-
$e^+ + O_2 + CO_2 \rightarrow O_2^- + + CO_2$	$7/5 \times 1.9 \times 10^{-30}$ (PP1966)	not used
$e^{-} + O_2 + H_2O \rightarrow O_2^{-} + H_2O$	$7 \times 1.9 \times 10^{-30}$ (<i>PP1966</i>)	not used
$e^+ + O_3 \rightarrow O^- + O_2$	9×10^{-12} (Kaz)	58
$e^- + N_2^+ \rightarrow N_2$	$3.6 \times 10^{-8} (Kaz)$	7
$\frac{1}{100} HO^{-1} + CH_2 I \rightarrow I^{-1} + HO + CH_2$	3.0×10^{-9} (Ike)	135
$HO^- + CO_2 + M \rightarrow HCO_2^- + M$	7.6×10^{-28}	66
$HO^- + H_2O + M \rightarrow HO^-(H_2O) + M$	2.5×10^{-28}	136
$HO^- + NO_2 \rightarrow NO_2^- + HO$	1.1×10^{-9}	90
$HO^- + O_2 \rightarrow O_2^- + HO$	9.0×10^{-10}	67
$HO^{-}(H_2O) + M \rightarrow HO^{-} + H_2O + M$	$2.5 \times 10^{-28}/4.2 \times 10^{-6}$ (NIST)	137
$HO^{-}(H_{2}O) + H_{2}O + M \rightarrow HO^{-}(H_{2}O)_{2} + M$	3.5×10^{-28}	138
$HO^{-}(H_{2}O) + M_{2}O + M^{-}(H_{2}O) + H_{2}O + M$	$3.5 \times 10^{-28}/6.7 \times 10^{-12}$ (NIST)	139
$HO^{-}(H_2O)_2 + H_2O + M \rightarrow HO^{-}(H_2O)_2 + M$	3.0×10^{-28}	140
$HO^{-}(H_{2}O)_{2} + M_{2}O + M_{2}O + H_{2}O + M_{2}O $	1.85×10^{-13} (NIST)	141
	7 10-10 (7)	
$1 + HAc \longrightarrow I^{-}(HAc)$	1×10^{-10} (lyer)	42
$I^- + HFo \xrightarrow{in} I^-(HFo)$	$1.5 \times 10^{-10} (\text{est})$	38
$\mathrm{I}^- + \mathrm{H}_2\mathrm{O} + M \to \mathrm{I}^-(\mathrm{H}_2\mathrm{O}) + M$	1.86×10^{-28} (<i>Iyer</i> , <i>NIST</i>)	17
$I^- + H_2O_2 \xrightarrow{M} I^-(H_2O_2)$	1×10^{-9} (Iyer)	30
$I^- + HNO_3 \rightarrow NO_3^- + HI$	5.0×10^{-11}	91
$I^- + O_3 + M \rightarrow I^-(O_3) + M$	1.0×10^{-29} (Wil)	158
$I^-(HAc) + M \rightarrow I^- + HAc + M$	2×10^{-9} (Iyer)/4.9 × 10 ⁷ (<i>NIST</i>)	43
$I^{-}(HAc) + H_2O \rightarrow I^{-}(H_2O) + HAc$	$2 \times 10^{-9} \text{ (est)}/1.6 \times 10^4 \text{ (NIST)}$	45
$I^-(HFo) + M \rightarrow I^- + HFo + M$	$1.5 \times 10^{-10} \text{ (est)}/2.01 \times 10^9 \text{ (NIST)}$	39

Table A2.	Continued.
140101120	continueu.

Reaction	Reaction rate coefficient ^a (reference) ^b	Inde
$I^{-}(HFo) + H_2O \rightarrow I^{-}(H_2O) + HFo$	$2 \times 10^{-9} \text{ (est)}/2.21 \times 10^5 \text{ (NIST)}$	41
$I^{-}(H_2O) + M \rightarrow I^{-} + H_2O + M$	$1.86 \times 10^{-28}/2.9 \times 10^{-16}$ (Iyer, NIST)	18
$I^{-}(H_2O) + HAc \rightarrow I^{-}(HAc) + H_2O$	$2 \times 10^{-9} (est)$	44
$I^-(H_2O) + HFo \rightarrow I^-(HFo) + H_2O$	2×10^{-9} (est)	40
$I^{-}(H_{2}O) + H_{2}O + M \rightarrow I^{-}(H_{2}O)_{2} + M$	1.74×10^{-28}	78
$I^{-}(H_2O) + H_2O_2 \rightarrow I^{-}(H_2O_2) + H_2O$	2×10^{-9} (est)	32
$I^{-}(H_2O)_2 + M \rightarrow I^{-}(H_2O) + H_2O + M$	3.57×10^{-12} (<i>NIST</i>)	79
$I^{-}(H_2O)_2 + HAc \rightarrow I^{-}(HAc) + 2H_2O$	3×10^{-9} (est)	208
$I^{-}(H_{2}O)_{2} + HFo \rightarrow I^{-}(HFo) + 2H_{2}O$	2×10^{-9} (est)	206
$I^{-}(H_2O)_2 + H_2O + M \to I^{-}(H_2O)_3 + M$	$2.14 \times 10^{-11} * 1.28 \times 10^{-17}$ (NIST)	80
$I^{-}(H_2O)_2 + H_2O_2 \rightarrow I^{-}(H_2O_2) + 2H_2O$	2×10^{-9} (est)	204
$I^{-}(H_2O)_3 + M \to I^{-}(H_2O)_2 + H_2O + M$	2.14×10^{-11}	81
$I^{-}(H_2O)_3 + HAc \rightarrow I^{-}(HAc) + 3H_2O$	$< 3 \times 10^{-9}$ (not used)	209
$I^{-}(H_{2}O)_{3} + HFo \rightarrow I^{-}(HFo) + 3H_{2}O$	$< 3 \times 10^{-9}$ (not used)	207
$I^{-}(H_2O)_3 + H_2O_2 \rightarrow I^{-}(H_2O_2) + 3H_2O$	$<3 \times 10^{-9}$ (not used)	205
$I^{-}(H_2O_2) + M \to I^{-} + H_2O_2 + M$	$1 \times 10^{-9}/6.33 \times 10^5$ (est)	31
$I^{-}(H_2O_2) + H_2O \rightarrow I^{-}(H_2O) + H_2O_2$	$2 \times 10^{-9} / 4.26 \times 10^3$ (est)	33
$\mathbf{I}^{-}(\mathbf{O}_{3}) + M \to \mathbf{I}^{-} + \mathbf{O}_{3} + M$	1.0×10^{-13} (Wil)	159
$NO^- + CO_2 \rightarrow e^- + NO + CO_2$	8.3×10^{-12}	117
$NO^- + H_2O + M \rightarrow NO^-(H_2O) + M$	2.63×10^{-28}	121
$NO^- + NO_2 \rightarrow NO_2^- + NO$	7.4×10^{-10}	118
$NO^- + O_2 \rightarrow O_2^- + NO$	5.0×10^{-10}	119
$NO^{-}(H_2O) + M \rightarrow NO^{-} + H_2O + M$	3.05×10^{-18} (NIST)	122
$NO^{-}(H_2O) + H_2O + M \rightarrow NO^{-}(H_2O)_2 + M$	2.12×10^{-28}	123
$NO^{-}(H_2O)_2 + M \rightarrow NO^{-}(H_2O) + H_2O + M$	4.62×10^{-15} (NIST)	124
$NO^{-}(H_2O)_2 + H_2O + M \rightarrow NO^{-}(H_2O)_3 + M$	1.90×10^{-28}	125
$NO^{-}(H_2O)_3 + M \to NO^{-}(H_2O)_2 + H_2O + M$	1.95×10^{-13} (NIST)	126
$NO_2^- + H_2O + M \rightarrow NO_2^-(H_2O) + M$	1.6×10^{-28}	112
$NO_2^- + H_2O_2 + M \rightarrow NO_2^-(H_2O_2) + M$	1.0×10^{-28} (est)	129
$NO_2^2 + NO_2 \rightarrow NO_3^2 + NO_2$	2.0×10^{-13}	92
$NO_2^2 + N_2O \rightarrow NO_3^2 + N_2$	1.0×10^{-12}	120
$NO_2^2 + O_3 \rightarrow NO_2^2 + O_2$	1.2×10^{-10}	98
$NO_2^2(H_2O) + M \rightarrow NO_2^2 + H_2O + M$	3.53×10^{-15} (NIST)	93
$NO_2^2(H_2O) + H_2O + M \rightarrow NO_2^2(H_2O)_2 + M$	8.0×10^{-29}	113
$NO_2^-(H_2O)_2 + M \rightarrow NO_2^-(H_2O) + H_2O + M$	8.3×10^{-14} (NIST)	94
$NO_{2}^{-}(H_{2}O)_{2} + H_{2}O + M \rightarrow NO_{2}^{-}(H_{2}O)_{3} + M$	8.0×10^{-29}	114
$NO_2^-(H_2O)_2 + M \rightarrow NO_2^-(H_2O)_2 + H_2O + M$	1.4×10^{-12} (NIST)	95
$NO_{2}^{-}(H_{2}O_{2}) + M \rightarrow NO_{2}^{-}(H_{2}O_{2}) + M_{2}O_{2} + M_{2}O_{2} + M_{2}O_{2}$	$1.0 \times 10^{-28} \text{ (est)}/1.7 \times 10^{-12} \text{ (NIST)}$	130
$\frac{2}{NO_{-}^{-} + HF_{0} + M} \rightarrow NO_{-}^{-}(HF_{0}) + M$	1.0×10^{-28} (est)	133
$NO_{3}^{-} + H_{2}O + M \rightarrow NO_{3}^{-}(H_{2}O) + M$	1.6×10^{-28}	115
$NO^{-} + H_2O_2 + M \rightarrow NO^{-}(H_2O_2) + M$	1.0×10^{-28} (est)	131
$NO_3 + NO \rightarrow NO^- + NO_2$	3.0×10^{-15}	06
$NO_3 + NO \rightarrow NO_2 + NO_2$	3.0×10^{-13}	90
$NO_3 + O_3 \rightarrow NO_2 + 2O_2$ $NO_2(IE_2) + M \rightarrow NO_2 + IE_2 + M$	1.0×10^{-28} (ast)/0.25 × 10 ¹² (NIST)	97
$NO_3(HFO) + M \rightarrow NO_3 + HFO + M$	1.0×10^{-12} (est)/9.23 × 10 ⁻² (NIST)	134
$NO_3(\Pi_2O) + M \rightarrow NO_3 + \Pi_2O + M$	1.6×10^{-28}	99 117
$NO_{3}(H_{2}O) + H_{2}O + M \rightarrow NO_{3}(H_{2}O)_{2} + M$	1.0×10^{-20}	116
$\operatorname{NO}_3(\operatorname{H}_2\operatorname{O})_2 + M \to \operatorname{NO}_3(\operatorname{H}_2\operatorname{O}) + M$	6.81×10^{-13} (Kaz, NIST)	100
$NO_3 (H_2O)_2 + H_2O + M \to NO_3 (H_2O)_3 + M$	1.0×10^{-20}	127
$NO_3 (H_2O)_3 + M \to NO_3^- (H_2O)_2 + H_2O + M$	5.56×10^{-12} (NIST)	128
$NO_3 (H_2O)_3 + H_2O + M \to NO_3^- (H_2O)_4 + M$	2.0×10^{-25} (est)	196
$NO_3 (H_2O)_4 + M \to NO_3^- (H_2O)_3 + H_2O + M$	1.0×10^{-11} (est, NIST)	197
$NO_{2}^{-}(H_{2}O_{2}) + M \rightarrow NO_{2}^{-} + H_{2}O_{2} + M$	1.0×10^{-28} (est)/ 1.0×10^{10} (NIST)	132

Reaction	Reaction rate coefficient ^a (reference) ^b	Index
$NO_2^{-*} + CO_2 \rightarrow CO_2^{-} + NO_2$	3.0×10^{-9} (FF)	142
$NO_2^{-*} + NO \rightarrow NO_2^{-} + NO_2$	3.0×10^{-9} (FF)	143
<u> </u>		
$N_2^+ + \sum X^{-k=6x10^{-\circ}(300/T)+1.25\times10^{-23}[M](300/T)} \text{ products}$	1.2×10^{-8} (Kaz)	157
$\rm O^-\!+CH_4 \rightarrow HO^-\!+CH_3$	1.0×10^{-10}	59
$O^- + CO_2 + M \rightarrow CO_3^- + M$	3.0×10^{-28}	60
$O^- + H_2 \rightarrow HO^- + H$	6.0×10^{-10}	62
$O^- + H_2O + M \to O^-(H_2O) + M$	1.3×10^{-28}	61
$O^- + NO_2 \rightarrow NO_2^- + O$	1.25×10^{-9}	101
$O^- + N_2 O \rightarrow NO^- + NO$	2.0×10^{-10}	102
$O^- + O_2 + M \rightarrow O_3^- + M$	1.5×10^{-31}	63
$O^- + O_3 \rightarrow O_3^- + O$	8.0×10^{-10}	64
$O^{-}(H_2O) + H_2O \rightarrow HO^{-}(H_2O) + HO$	6.0×10^{-11} (Kaz)	145
	$>1 \times 10^{-11}$ (Alb)	
$O^{-}(H_2O) + O_2 \rightarrow O_3^{-} + H_2O$	6×10^{-11} (<i>Kaz</i>)	65
$O_2^- + CH_3I \rightarrow I^- + O_2 + CH_3$	$2.0 \times 10^{-9} \ (est)$	4
$O_{2}^{-} + CH_{2}OOH \xrightarrow{M} O_{2}^{-}(CH_{2}OOH)$	3×10^{-9} (est)	34
$O_2^- + CO_2 + M \rightarrow O_2^-(CO_2) + M$	$4.7 \times 10^{-29} (FF)$	5
$O_2^- + H_2O + M \rightarrow O_2^-(H_2O) + M$	2.2×10^{-28} (FF)	10
$a_2 + m_2 a_2 + m_1 + a_2 (m_2 a_2) + m_1$	2.2×10^{-9} (11)	20
$O_2 + H_2O_2 \longrightarrow O_2(H_2O_2)$	3×10^{-5} (est)	26
$O_2 + NO_2 \rightarrow NO_2 + O_2$	8.0×10^{-10} (P)	103
$O_2 + O_2 + M \rightarrow O_2 (O_2) + M$	3.8×10^{-50} (Kaz)	55
$O_2 + O_3 \rightarrow O_3 + O_2$	7.8×10^{-10} (Fah)	8
	$3.0 \times 10^{-10} (FF)$	
	7.8×10^{-10} (Fah)	
	$6.0 \times 10^{-10} (Do)$	
	$7.8 \times 10^{-10} (Kaz)$	
	$4.0 \times 10^{-10} (Pop)$	
O_2 (CH ₃ OOH) + $M \rightarrow O_2$ + CH ₃ OOH + M	$3 \times 10^{-9}/1.1 \times 10^{42}$ (O'Su)	35
$O_2^-(CH_3OOH) + H_2O \rightarrow O_2^-(H_2O) + CH_3OOH$	$2 \times 10^{-9} / 7.7 \times 10^{6}$ (est)	37
$O_2^-(CO_2) + M \to O_2^- + CO_2 + M$	$4.7 \times 10^{-29}/2.34 \times 10^{-11}$ (FF, NIST)	6
$O_2^-(CO_2) + CH_3OOH \rightarrow O_2^-(CH_3OOH) + CO_2$	2.0×10^{-10}	161
$O_2^-(CO_2) + CO_2 + M \to O_2^-(CO_2)_2 + CO_2 + M$	1.0×10^{-28} (est)	200
$O_2^-(CO_2) + H_2O \rightarrow O_2^-(H_2O) + CO_2$	$5.8 \times 10^{-10}/2.3$ (Alb, FF)	13
	$k(T = 298) = 2.5 \times 10^{-9} (Kaz)$	
$O_2^-(CO_2) + H_2O + M \to O_2^-(CO_2)(H_2O) + M$	1×10^{-28} (est H, P)	21
$O_2^-(CO_2) + H_2O_2 \xrightarrow{M} O_2^-(CO_2)(H_2O_2)$	2×10^{-11} (est)	22
$O_{2}^{2}(CO_{2}) + H_{2}O_{2} \rightarrow O_{2}^{2}(H_{2}O_{2}) + CO_{2}$	1.8×10^{-10}	160
$O_2^{-}(CO_2) + NO \rightarrow NO_3^{-*} + CO_2 + H_2O$	4.8×10^{-11}	89
$O_{2}^{-}(CO_{2}) + O_{3} \rightarrow O_{3}^{-} + CO_{2} + O_{2}$	$7.0 \times 10^{-11} (Alb)$	46
$O_{2}^{-}(CO_{2})_{2} + M \rightarrow O_{2}^{-}(CO_{2}) + CO_{2} + M$	3.8×10^{-10} (est, NIST)	201
$O_2^{-}(CO_2)_2 + H_2O \rightarrow O_2^{-}(CO_2)(H_2O) + CO_2$	1.0×10^{-9} (est)	202
$O_2^{-}(CO_2)_2 + H_2O_2 \rightarrow O_2^{-}(CO_2)(H_2O_2) + CO_2$	1.0×10^{-9} (est)	203
$O_{2}^{-}(CO_{2})(H_{2}O) + M \rightarrow O_{2}^{-}(CO_{2}) + H_{2}O + M$	$1.0 \times 10^{28}/1.9 \times 10^{-13}$ (est H, NIST)	14
$O_{2}^{-}(CO_{2})(H_{2}O) + M \rightarrow O_{2}^{-}(H_{2}O) + CO_{2} + M$	2.7×10^{-15} (est, NIST)	198
$O_{2}^{-}(CO_{2})(H_{2}O) + H_{2}O \rightarrow O_{2}^{-}(H_{2}O)_{2} + CO_{2}$	1.0×10^{-9} (Fah, est)	148
$O_{2}^{-}(CO_{2})(H_{2}O) + H_{2}O + M \rightarrow O_{2}^{-}(CO_{2})(H_{2}O)_{2} + M$	1.0×10^{-28}	180
$O_2^{-}(CO_2)(H_2O)_2 + M \rightarrow O_2^{-}(CO_2)(H_2O) + H_2O + M$	1.0×10^{-13}	181
$O_{2}^{-}(CO_{2})(H_{2}O)_{2} + H_{2}O \rightarrow O_{2}^{-}(H_{2}O)_{2} + CO_{2}$	1.0×10^{-10}	182
$O_{2}^{-}(CO_{2})(H_{2}O)_{2} + O_{3} \rightarrow O_{2}^{-}(H_{2}O)_{3} + CO_{2}$	1.0×10^{-10}	183
$O_2^{-}(CO_2)(H_2O_2) + M \rightarrow O_2^{-}(CO_2) + H_2O_2 + M$	$2 \times 10^{-11}/2.0 \times 10^{12}(est)$	23

Reaction	Reaction rate coefficient ^a (reference) ^b	Index
$O_2^-(CO_2)(H_2O_2) + H_2O \rightarrow O_2^-(CO_2)(H_2O) + H_2O_2$	$3 \times 10^{-9} / 7 \times 10^{9}$ (est)	25
$O^{-}(CO_{1})(U,O_{1}) + U_{1}O_{2} \rightarrow O^{-}(CO_{1})(U,O_{2}) + U_{1}O_{2}$	1.0×10^{-9} (est H, M)	24
$O_2^-(CO_2)(H_2O) + H_2O_2 \rightarrow O_2^-(CO_2)(H_2O_2) + H_2O$	$2.2 \times 10^{-28/3} 0.4 \times 10^{-11} (FE NIST)$	24 11
$O_2(\Pi_2 O) + M \rightarrow O_2 + \Pi_2 O + M$	$k(T = 298) = 4.33 \times 10^{-18} (Kaz)$	11
$O_2^-(H_2O) + CH_3OOH \rightarrow O_2^-(CH_3OOH) + H_2O$	$2 \times 10^{-9} \text{ (est)}$	36
$O_2^-(H_2O) + CO_2 \rightarrow O_2^-(CO_2) + H_2O$	$5.8 \times 10^{-10} (Alb)$	12
	$k(T = 298) = 2.5 \times 10^{-9} (Kaz)$	
$O_2^-(H_2O) + CO_2 + M \rightarrow O_2^-(CO_2)(H_2O) + M$	1.0×10^{-30}	178
$O_2^-(H_2O) + H_2O + M \to O_2^-(H_2O)_2 + M$	$5.4 \times 10^{-28} (PK)$	50
$O_2^-(H_2O) + H_2O_2 \rightarrow O_2^-(H_2O_2) + H_2O$	3×10^{-9} (est)	28
$O_2^-(H_2O) + H_2O_2 + M \to O_2^-(H_2O_2)(H_2O) + M$	1.0×10^{-29} (est)	153
$O_2^-(H_2O) + NO \rightarrow NO_3^- + H_2O$	3.1×10^{-10}	104
$O_2^-(H_2O) + NO_2 \rightarrow NO_2^- + H_2O + O_2$	9.0×10^{-10}	105
$O_2^-(H_2O) + O_2 \rightarrow O_2^-(O_2) + H_2O$	2.5×10^{-15}	82
$O_2^-(H_2O) + O_3 \rightarrow O_3^- + H_2O + O_2$	$8.0 \times 10^{-10} (Fah)$	47
$O_2^-(H_2O)_2 + M \to O_2^-(H_2O) + H_2O + M$	$1.1 \times 10^{-14} \ (PK)$	51
$O_2^-(H_2O)_2 + CH_3OOH \rightarrow O_2^-(CH_3OOH) + 2H_2O$	3.0×10^{-11} (est)	151
$O_2^{-}(H_2O)_2 + CO_2 \rightarrow O_2^{-}(CO_2)(H_2O) + H_2O$	7.0×10^{-11} (Fah)	147
$\tilde{O_2^{-}}(H_2O)_2 + H_2O + M \to O_2^{-}(H_2O)_3 + M$	5.0×10^{-28}	70
$\tilde{O_2}(H_2O_2 + H_2O_2 \rightarrow O_2(H_2O_2) + 2H_2O_2)$	7.5×10^{-10} (est)	149
$\tilde{O_2}(H_2O)_2 + NO \rightarrow NO_3 + 2H_2O$	3.0×10^{-10}	106
$\tilde{O_2}(H_2O)_2 + NO_2 \rightarrow NO_2 + 2H_2O + O_2$	9.0×10^{-10}	107
$\tilde{O_2}(H_2O)_2 + O_3 \rightarrow O_3(H_2O) + H_2O + O_2$	$7.8 \times 10^{-10} (Fah)$	52
$O_{2}^{2}(H_{2}O)_{3} + M \rightarrow O_{2}^{2}(H_{2}O)_{2} + H_{2}O + M$	$5.0 \times 10^{-28}/3.33 \times 10^{-16}$ (NIST)	71
$O_2^{-}(H_2O)_3 + CH_3OOH \rightarrow O_2^{-}(CH_3OOH) + 3H_2O$	5.0×10^{-14} (est)	152
$O_{2}^{2}(H_{2}O)_{3}+CO_{2} \rightarrow O_{2}^{-}(CO_{2})(H_{2}O)_{2}+H_{2}O$	1.0×10^{-14}	179
$O_{2}^{2}(H_{2}O)_{3} + H_{2}O + M \rightarrow O_{2}^{2}(H_{2}O)_{4} + M$	1.0×10^{-28} (H)	192
$O_2^{-}(H_2O)_3 + H_2O_2 \rightarrow O_2^{-}(H_2O_2) + 3H_2O_2$	1.25×10^{-10} (est)	150
$O_{2}^{2}(H_{2}O)_{3} + O_{3} \rightarrow O_{2}^{-}(H_{2}O)_{2} + H_{2}O + O_{2}$	6.4×10^{-10} (Fah)	146
$O_2^{-}(H_2O)_3 + NO \rightarrow NO_2^{-}(H_2O)_2 + H_2O$	1.5×10^{-10} (P)	187
$O_{2}^{2}(H_{2}O)_{4} + M \rightarrow O_{2}^{2}(H_{2}O)_{3} + H_{2}O + M$	1.2×10^{-12} (H. NIST)	193
$O_2^-(H_2O)_4 + H_2O + M \rightarrow O_2^-(H_2O)_5 + M$	5.0×10^{-29} (H)	194
$O_2^-(H_2O)_4 + NO \rightarrow NO_2^-(H_2O)_3 + H_2O$	1.2×10^{-10} (P)	188
$O_2^-(H_2O)_5 + M \rightarrow O_2^-(H_2O)_4 + H_2O + M$	4.5×10^{-12} (H. NIST)	195
$O_2^-(H_2O)_5 + NO \rightarrow NO_2^-(H_2O)_4 + H_2O$	1.2×10^{-10} (P)	189
$O_2^-(H_2O_2) + M \to O_2^- + H_2O_2 + M$	$3.0 \times 10^{-9}/2.96 \times 10^{16}$ (est)	27
$O_2^-(H_2O_2) + CO_2 + M \rightarrow O_2^-(CO_2)(H_2O_2) + M$	3.5×10^{-30} (est)	199
$O_2^-(H_2O_2) + H_2O \rightarrow O_2^-(H_2O) + H_2O_2$	$3.0 \times 10^{-9}/3.9 \times 10^{8}$ (est)	29
$O_2^-(H_2O_2)(H_2O) + M \rightarrow O_2^-(H_2O_2) + H_2O + M$	2.0×10^{-21} (est)	154
$O_2^-(H_2O_2)(H_2O) + M \to O_2^-(H_2O_2) + H_2O_2 + M$	1.0×10^{-22} (est)	155
$O_2^-(H_2O_2)(H_2O) + GO_2 \rightarrow O_2^-(GO_2)(H_2O_2) + H_2O_2$	7.0×10^{-11} (est)	155
$O_2^-(O_2) + M \rightarrow O_2^- + O_2 + M$	$1 \times 10^{-14} (Kaz)$	68
$O_2^-(O_2) + O_2^- + O_2^- + O_2^- + O_2^-$	$4.3 \times 10^{-10} (FF)$	56
$O_2^-(O_2) + UO_2^- + O_2^-(UO_2) + O_2^-$	$1.5 \times 10^{-9} (lk_{\theta})$	57
$O_2^-(O_2) + N_2 \rightarrow N_2^{-*} + O_2$	2.5×10^{-10}	108
$O_2^- (O_2) + HO^- (O_3^- + O_2^-)$	1.0 10-28	174
$O_3 + CH_3OOH + M \rightarrow O_3 (CH_3OOH) + M$	1.0×10^{-2}	1/4
$O_3 + O_2 \rightarrow O_3 + O_2$	(F0/)	די 10
$O_3 + \Pi_2 O + M \rightarrow O_3 (\Pi_2 O) + M$	$1.92 \times 10^{-20} (FF)$	19
$O_3 + H_2O_2 + M \rightarrow O_3 (H_2O_2) + M$	1.0×10^{-22}	100
$O_3 + NO \rightarrow NO_2 + O_2$	$1.1 \times 10^{-12} (50.50)$	109
$O_3 + NO \rightarrow NO_3 + O$	$1.1 \times 10^{-12} (50.50)$	110

Reaction	Reaction rate coefficient ^a (reference) ^b	Index
$O_3^- + NO_2 \rightarrow NO_2^- + O_3$	$7.0 \times 10^{-10} \text{ (P)}$	191
$O_3^- + NO_2 \rightarrow NO_3^- + O_2$	2.8×10^{-10}	111
5 5	> 1×10^{-11} (Alb)	
$O_{3}^{-}(H_{2}O) + M \rightarrow O_{3}^{-} + H_{2}O + M$	$1.92 \times 10^{-28}/1.46 \times 10^{-15}$ (FF, NIST)	20
$O_3^-(H_2O) + CH_3OOH \rightarrow O_3^-(CH_3OOH) + H_2O$	1.0×10^{-9}	175
$O_3^-(H_2O) + CO_2 \rightarrow CO_3^-(H_2O) + O_2$	1.75×10^{10} (Do, Wil)	48
$O_3^{-}(H_2O) + CO_2 \rightarrow CO_3^{-} + H_2O + O_2$	1.75×10^{10} (Do, Wil)	49
$O_3^-(H_2O) + H_2O + M \rightarrow O_3^-(H_2O)_2 + M$	1.92×10^{-28}	72
$O_{3}^{-}(H_{2}O) + H_{2}O_{2} \rightarrow O_{3}^{-}(H_{2}O_{2}) + H_{2}O$	1.0×10^{-9}	167
$O_3^{-}(H_2O)_2 + M \rightarrow O_3^{-}(H_2O) + H_2O + M$	1.28×10^{-13} (<i>NIST</i>)	73
$O_3^-(H_2O)_2 + CH_3OOH \rightarrow O_3^-(CH_3OOH) + 2H_2O$	1.0×10^{-10}	176
$O_3^-(H_2O)_2 + CO_2 \rightarrow CO_3^-(H_2O) + H_2O + O_2$	$1.0 \times 10^{-10} (P)$	185
$O_3^-(H_2O)_2 + H_2O + M \rightarrow O_3^-(H_2O)_3 + M$	1.68×10^{-28}	74
$O_3^-(H_2O)_2 + H_2O_2 \rightarrow O_3^-(H_2O_2) + 2H_2O$	1.0×10^{-10}	168
$O_3^-(H_2O)_3 + M \to O_3^-(H_2O)_2 + H_2O + M$	2.17×10^{-12} (<i>NIST</i>)	75
$O_3^-(H_2O_3 + H_2O_2 \rightarrow O_3^-(H_2O_2) + 3H_2O_3)$	1.0×10^{-11}	169
$O_3^-(H_2O)_3 + CH_3OOH \rightarrow O_3^-(CH_3OOH) + 3H_2O$	1.0×10^{-11}	177
$O_3^-(H_2O)_3 + CO_2 \rightarrow CO_3^-(H_2O)_2 + H_2O + O_2$	5.0×10^{-11} (P)	186

^a Reaction rate coefficient units: unimolecular, s⁻¹; bimolecular, cm³ molec⁻¹ s⁻¹; termolecular, cm⁶ molec² s⁻¹. First listed reaction rate coefficient for a reaction is used in the model mechanism, others are included to show published range of values. ^b AK1970 (Arshadi and Kebarle, 1970); Alb (Albritton, 1978); Do1977 (Dotan et al., 1977); F67 (Fehsenfeld et al., 1967); FF1974 (Fehsenfeld and Ferguson, 1974); H (Huertas et al., 1978); HY1992 (Hiraoka and Yamabe, 1992); Ike (Ikezoe et al., 1987) Iyer (Iyer et al., 2016); Kaz (Kazil, 2002); KFP1972 (Kebarle et al., 1972); Kov (Kovács et al., 2016); M (Mohnen, 1974); NIST (Bartmess, 2016); O'Su (O'Sullivan et al., 2018); P (Popov, 2010); PP1966 (Pack and Phelps, 1966); Wil (Williams et al., 202).

Cluster ion	Cluster ion source reaction	Rate	Index
$\mathrm{O}_2^-(\mathrm{H}_2\mathrm{O}_2)$			
	$O_2^- + H_2O_2 \xrightarrow{M} O_2^-(H_2O_2)$	3.0×10^{-9}	26
	$O_{2}^{2}(H_{2}O) + H_{2}O_{2} \rightarrow O_{2}^{-}(H_{2}O_{2}) + H_{2}O_{2}$	3.0×10^{-9}	28
	$O_2^2(H_2O)_2 + H_2O_2 \rightarrow O_2^2(H_2O_2) + 2H_2O$	7.5×10^{-10}	149
	$O_{2}^{2}(H_{2}O_{3}+H_{2}O_{2} \rightarrow O_{2}^{2}(H_{2}O_{2})+3H_{2}O_{2}$	1.25×10^{-10}	150
	$O_2^-(H_2O) + H_2O_2 + M \rightarrow O_2^-(H_2O_2)(H_2O) + M$	1.0×10^{-29}	153
	$O_2^-(H_2O_2)(H_2O) + M \rightarrow O_2^-(H_2O_2)(H_2O) + M$	2.0×10^{-21}	154
	$O_2^-(CO_2) + H_2O_2 \rightarrow O_2^-(H_2O_2) + CO_2$	1.8×10^{-10}	160
O_2^- (CH ₃ OC	DH)		
2		2.0 10 0	
	$O_2^- + CH_3OOH \longrightarrow O_2^-(CH_3OOH)$	3.0×10^{-9}	34
	$O_2^-(H_2O) + CH_3OOH \rightarrow O_2^-(CH_3OOH) + H_2O$	2.0×10^{-9}	36
	$O_2^-(H_2O)_2 + CH_3OOH \rightarrow O_2^-(CH_3OOH) + 2H_2O$	3.0×10^{-11}	151
	$O_2^-(H_2O)_3 + CH_3OOH \rightarrow O_2^-(CH_3OOH) + 3H_2O$	5.0×10^{-14}	152
	$\tilde{O_2^-}(CO_2) + CH_3OOH \rightarrow O_2^-(\tilde{CH}_3OOH) + CO_2$	2.0×10^{-10}	161
$O_2^-(CO_2)(H)$	H ₂ O ₂)		
	$\Omega_{-}^{-}(C\Omega_{2}) + H_{2}\Omega_{2} \xrightarrow{M} \Omega_{-}^{-}(C\Omega_{2})(H_{2}\Omega_{2})$	2.0×10^{-11}	22
	$O_2^{-}(CO_2)(H_2O_2) + H_2O_2 \rightarrow O_2^{-}(CO_2)(H_2O_2) + H_2O_2$	2.0×10^{-9}	24
	$O_2^-(U,O_2)(H_2O) + H_2O_2 \rightarrow O_2^-(CO_2)(H_2O_2) + H_2O_2$	3.0×10^{-11}	24 156
	$O_2(H_2O_2)(H_2O) + CO_2 \rightarrow O_2(CO_2)(H_2O_2) + H_2O$	7.0×10^{-30}	100
	$O_2(H_2O_2) + CO_2 + M \rightarrow O_2(CO_2)(H_2O_2) + M$	3.5×10^{-50}	199
	$O_2 (CO_2)_2 + H_2O_2 \rightarrow O_2 (CO_2)(H_2O_2) + CO_2$	1.0×10^{-9}	203
CO_3^- (H ₂ O ₂)		
	$\operatorname{CO}_3^- + \operatorname{H}_2\operatorname{O}_2 + M \to \operatorname{CO}_3^-(\operatorname{H}_2\operatorname{O}_2) + M$	1.0×10^{-28}	162
	$CO_{3}^{-}(H_{2}O) + H_{2}O_{2} \rightarrow CO_{3}^{-}(H_{2}O_{2}) + H_{2}O$	1.0×10^{-9}	163
	$CO_3^-(H_2O_2) + H_2O_2 \rightarrow O_3^-(H_2O_2) + 2H_2O_3^-(H_2O_2) + 2H$	1.0×10^{-10}	164
	$\operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O})_{3} + \operatorname{H}_{2}\operatorname{O}_{2} \rightarrow \rightarrow \operatorname{CO}_{3}^{-}(\operatorname{H}_{2}\operatorname{O}_{2}) + 3\operatorname{H}_{2}\operatorname{O}$	1.0×10^{-11}	165
CO ₃ ⁻ (CH ₃ C	DOH)		
	$CO_{2}^{-} + CH_{2}OOH + M \rightarrow CO_{2}^{-}(CH_{2}OOH) + M$	1.0×10^{-28}	170
	$CO_{-}^{-}(H_{2}O) + CH_{2}OOH \rightarrow CO_{-}^{-}(CH_{2}OOH) + H_{2}O$	1.0×10^{-9}	171
	$CO_{-}^{-}(H_{2}O)_{2} + CH_{2}OOH \rightarrow CO_{-}^{-}(CH_{2}OOH) + H_{2}O$	1.0×10^{-10}	172
	$CO_{3}^{-}(H_{2}O)_{2} + CH_{3}OOH \rightarrow CO_{3}^{-}(CH_{3}OOH) + 2H_{2}O$ $CO_{2}^{-}(H_{2}O)_{3} + CH_{3}OOH \rightarrow CO_{2}^{-}(CH_{3}OOH) + 3H_{2}O$	1.0×10^{-11} 1.0×10^{-11}	173
I ⁻ (H ₂ O ₂),	[⁻ (HFo) and I ⁻ (HAc)		
	$I^- + H_2 O_2 \stackrel{M}{\longrightarrow} I^- (H_2 O_2)$	1.0×10^{-9}	30
	$I \rightarrow \Pi_2 \cup 2 \longrightarrow I (\Pi_2 \cup 2)$	1.0×10^{-9}	30
	$I (H_2O) + H_2O_2 \rightarrow I (H_2O_2) + H_2O$	2.0×10^{-9}	32 201
	$I (H_2 U)_2 + H_2 U_2 \to I (H_2 U_2) + 2H_2 U_2$	2×10^{-5}	204
	$I^{-}(H_2O)_3 + H_2O_2 \rightarrow I^{-}(H_2O_2) + 3H_2O$	$<3 \times 10^{-9}$	205
	$I^- + HFo \xrightarrow{M} I^- (HFo)$	1.5×10^{-10}	38
	$I^{-}(H_{2}O) + HFO \rightarrow I^{-}(HFO) + H_{2}O$	2.0×10^{-9}	40
	$I^-(H_2O)_2 + HF_0 \rightarrow I^-(HF_0) + 2H_2O$	2×10^{-9}	206
	$I^{-}(H_2O)_3 + HFo \rightarrow I^{-}(HFo) + 3H_2O$	$< 3 \times 10^{-9}$	207
	$I = I H \Lambda_0 = M I = (H \Lambda_0)$	7.0×10^{-10}	40
	$I + \Pi AC \longrightarrow I (\Pi AC)$	7.0×10^{-9}	42
	$I (H_2 U) + HAC \rightarrow I (HAC) + H_2 U$	2.0×10^{-9}	44
	$I (H_2 U)_2 + HAc \rightarrow I (HAc) + 2H_2 U$	3×10^{-5}	208
	$I^{-}(H_2O)_2 + HAc \rightarrow I^{-}(HAc) + 3H_2O$	$<3 \times 10^{-9}$	209

 $\textbf{Table A3.} \ \text{Reactions that yield } O_2^- \ (H_2O_2), \ O_2^- \ (CH_3OOH), \ O_2^- \ (CO_2) \ (H_2O_2), \ I^- \ (H_2O_2), \ I^- \ (HFo) \ \text{and} \ I^- \ (HAc).$

Table A4. Reaction sequences leading to potential interferences at m/z 66 [¹⁸O of NO₂⁻ (H₂O), O₃⁻ (H₂O), and ¹⁸O of O₂⁻ (O₂)] for O₂⁻ (H₂O₂) and at m/z 80 [¹⁸O of CO₃⁻ (H₂O) and NO₃⁻ (H₂O)] for O₂⁻ (CH₃OOH).

Interference cluster	Source description	Cluster formation reaction sequence	Index
18 O of NO ₂ ⁻ (H ₂ O)	from N_2O to NO^- to NO_2^-	$O^- + N_2 O \rightarrow NO^- + NO$	102
-	-	$NO^- + NO_2 \rightarrow NO_2^- + NO$	118
	from NO to NO_2^-	$CO_3^- + NO \rightarrow NO_2^- + CO_2$	83
		$\mathrm{CO}_3^-(\mathrm{H}_2\mathrm{O}) + \mathrm{NO} \rightarrow \mathrm{NO}_2^- + \mathrm{CO}_2 + \mathrm{H}_2\mathrm{O}$	85
		$\mathrm{CO}_3^-(\mathrm{H}_2\mathrm{O}) + \mathrm{NO} \rightarrow \mathrm{NO}_2^-(\mathrm{H}_2\mathrm{O}) + \mathrm{CO}_2$	86
	from NO ₂ to NO ₂ ⁻	$\rm HO^- + NO_2 \rightarrow NO_2^- + HO$	90
		$O_2^- + NO_2 \rightarrow NO_2^- + O_2$	190
		$O_3^- + NO_2 \rightarrow NO_2^- + O_3$	191
		$O^- + NO_2 \rightarrow NO_2^- + O$	101
		$O_2^- + NO_2 \rightarrow NO_2^- + O_2$	103
		$O_2^-(H_2O) + NO_2 \rightarrow NO_2^- + H_2O + O_2$	105
		$O_2^-(H_2O)_2 + NO_2 \rightarrow NO_2^- + 2H_2O + O_2$	107
		$O_3^- + NO \rightarrow NO_2^- + O_2$	109
	then the NO_2^- hydrate	$NO_2^- + H_2O \xrightarrow{M} NO_2^-(H_2O)$	112
$O_3^-(H_2O)$		$O_2^- + O_3 \rightarrow O_3^- + O_2$	8
		$O_3^- + H_2O \xrightarrow{M} O_3^-(H_2O)$	19
18 O of $O_2^-(O_2)$		$O_2^- + O_2 \xrightarrow{M} O_2^-(O_2)$	55
18 O of CO ₃ ⁻ (H ₂ O)		$O_2^- + O_3 \rightarrow O_3^- + O_2$	8
5		$O_3^2 + CO_2 \rightarrow CO_3^2 + O_2$	9
		$\operatorname{CO}_3^- + \operatorname{H}_2\operatorname{O} \xrightarrow{M} \operatorname{CO}_3^-(\operatorname{H}_2\operatorname{O})$	15
NO ₃ ⁻ (H ₂ O)	from NO to NO_3^-	$O_2^-(H_2O) + NO \rightarrow NO_3^- + H_2O$	104
		$O_2^-(H_2O)_2 + NO \rightarrow NO_3^- + 2H_2O$	106
		$O_3^- + NO \rightarrow NO_3^- + O$	110
		$O_2^-(H_2O)_3 + NO \rightarrow NO_3^-(H_2O)_2 + H_2O$	187
		$O_2^-(H_2O)_4 + NO \rightarrow NO_3^-(H_2O)_3 + H_2O$	188
		$O_2^-(H_2O)_5 + NO \rightarrow NO_3^-(H_2O)_4 + H_2O$	189
	from NO ₂ to NO ₃ ⁻	$\text{CO}_3^- + \text{NO}_2 \rightarrow \text{NO}_3^- + \text{CO}_2$	84
		$\mathrm{CO}_3^-(\mathrm{H}_2\mathrm{O}) + \mathrm{NO}_2 \rightarrow \mathrm{NO}_3^- + \mathrm{CO}_2 + \mathrm{H}_2\mathrm{O}$	87
		$\mathrm{CO}_3^-(\mathrm{H}_2\mathrm{O}) + \mathrm{NO}_2 \rightarrow \mathrm{NO}_3^-(\mathrm{H}_2\mathrm{O}) + \mathrm{CO}_2$	88
		$\mathrm{O}_3^- + \mathrm{NO}_2 \rightarrow \mathrm{NO}_3^- + \mathrm{O}_2$	111
	from NO_2^- to NO_3^-	$NO_2^- + NO_2 \rightarrow NO_3^- + NO$	92
		$\mathrm{NO}_2^- + \mathrm{O}_3 \rightarrow \mathrm{NO}_3^- + \mathrm{O}_2$	98
		$NO_2^- + N_2O \rightarrow NO_3^- + N_2$	120
	from HNO ₃ to NO_3^-	$I^- + HNO_3 \rightarrow NO_3^- + HI$	91
	then the NO_3^- hydrate	$NO_3^- + H_2O_2 \xrightarrow{M} NO_3^-(H_2O_2)$	131

Table A5. Enthalpy of formation, entropy and Gibb's formation energy for neutral, ion and ion clusters in the $O_2^- - O_2 - CO_2 - H_2O_-$ hydroperoxide system. Note: bold font indicates value derived in this work using published formation and reaction enthalpy, entropy and Gibb's energy.

Species or cluster	$\Delta H_{\rm f}^o$ kJ mol ⁻¹	S^o J ° K ⁻¹ mol ⁻¹	$\Delta G_{\mathrm{f}}^{o}$ kJ mol ⁻¹	Reference*
Neutral				
Cgraphite	0	6	0	NIST2016
СН3ООН	-128	281	-71	Gold2012
CO_2	-394	214	-394	NIST2016; Gold2012
H ₂	0	131	0	NIST2016; Gold2012
H ₂ O	-242	189	-229	NIST2016; Gold2012
H_2O_2	-136	233	-105	NIST2016; Gold2012
O ₂	0	205	0	NIST2016; Gold2012
Ion or ion cluster				
e ⁻	0	23	0	Bartmess (1994)
0_{2}^{-}	-43	210	-38	NIST2016; Bartmess (1994)
O_2^{-} (CH ₃ OOH)			-340	OSull2017; this work
$O_{2}^{2}(CO_{2})$	-516	322	-481	this work
$O_{2}^{2}(CO_{2})_{2}$	-937	460	-880	this work
$O_{2}^{-}(CO_{2})(H_{2}O)$	-819	430	-747	this work
$O_{2}^{2}(CO_{2})(H_{2}O)_{2}$	-1105	555	-1000	this work
$O_{2}^{2}(CO_{2})(H_{2}O_{2})$			-630	OSull2017; this work
$O_{2}^{2}(H_{2}O)$	-362	314	-318	this work
$O_{2}^{2}(H_{2}O)_{2}$	-676	398	-588	this work
$O_{2}^{\frac{1}{2}}(H_{2}O)_{3}$	-982	469	-846	this work
$O_{2}^{-}(H_{2}O)_{4}$			-1092	this work
$O_{2}^{2}(H_{2}O)_{5}$			-1335	this work
$O_{2}^{-}(H_{2}O_{2})$			-237	OSull2017; this work
$O_2^{\frac{2}{2}}(O_2)$	-115	310	-79	NIST2016; AK1970; this work

* AK1970 (Arshadi and Kebarle, 1970); Gold2012 (Goldsmith et al., 2012); NIST2016 (Bartmess, 2016); OSull2017 (O'Sullivan et al., 2018).

Table A6. Reaction enthalpy, entropy and Gibb's energy for neutral, ion and ion cluster reactions in the $O_2^- - O_2 - CO_2 - H_2O$ hydroperoxide system. Note: bold font indicates value derived in this work using published formation and reaction enthalpy, entropy and Gibb's energy.

Reaction	ΔH_r^0	ΔS_r^o	ΔG_r^o	Reference*
	$kJ mol^{-1}$	$J \circ K^{-1} \operatorname{mol}^{-1}$	$kJ mol^{-1}$	
$O_2^- + CO_2 \rightleftharpoons O_2^- (CO_2)$	-80	-101	-49	NIST2016, HY1992
$O_2^2(CO_2) + CO_2 \rightleftharpoons O_2^2(CO_2)_2$	-28	-76	-5	NIST2016, HY1992
$O_2^{-1}(CO_2) + H_2O \rightleftharpoons O_2^{-1}(H_2O) + CO_2$	2	17	-3	NIST2016, FF1974 ($\Delta G_r^o = -2.1$),
				this work
$O_{2}^{-}(CO_{2}) + H_{2}O \rightleftharpoons O_{2}^{-}(CO_{2})(H_{2}O)$	-61	-81	-37	KFP1972, this work
$\tilde{O_2^{-}}(CO_2)(H_2O) + H_2O \approx O_2^{-}(H_2O)_2 + CO_2$	-9	-7	-7	NIST2016, FF1974, KFP1972,
2 2 -				this work
$O_{2}^{-}(CO_{2})(H_{2}O) + H_{2}O \rightleftharpoons O_{2}^{-}(CO_{2})(H_{2}O)_{2}$	-44	-65	-25	Mohnen (1972), HFG1978, this work
$O_2^- + H_2O \rightleftharpoons O_2^- (H_2O)$	-77	-84	-52	NIST2016, AK1970
$O_2^-(H_2O) + H_2O \rightleftharpoons O_2^-(H_2O)_2$	-72	-105	-41	NIST2016, AK1970
$O_2^{-}(H_2O) + CO_2 \rightleftharpoons O_2^{-}(CO_2)(H_2O)$	-63	-98	-34	NIST2016, FF1974, this work
$O_{2}^{-}(H_{2}O)_{2} + CO_{2} \rightleftharpoons O_{2}^{-}(CO_{2})(H_{2}O) + H_{2}O$	9	7	7	this work
$O_2^-(H_2O)_2 + H_2O \rightleftharpoons O_2^-(H_2O)_3$	-64	-118	-29	NIST2016, AK1970
$O_2^{-}(H_2O)_3 + H_2O \rightleftharpoons O_2^{-}(H_2O)_4$			-18	NIST2016, AK1970
$O_2^{-}(H_2O)_4 + H_2O \rightleftharpoons O_2^{-}(H_2O)_5$			-14	NIST2016, AK1970
$O_2^{-} + O_2 \rightleftharpoons O_2^{-}(O_2)$	-44	-102	-13	NIST2016
$O_2^{-} + CH_3OOH \rightleftharpoons O_2^{-} (CH_3OOH)$			-231	OSull2017, this work
$\tilde{O_2} + H_2O_2 \rightleftharpoons \tilde{O_2} (\tilde{H_2O_2})$			-99	OSull2017, this work (-94)
$O_2^{-}(CO_2) + H_2O_2^{-} \rightleftharpoons O_2^{-}(CO_2)(H_2O_2)$			-43	OSull2017
O_2^{-} (H ₂ O) + CH ₃ OOH \rightleftharpoons O_2^{-} (CH ₃ OOH) + H ₂ O			-181	OSull2017, this work
$\tilde{O_2}(H_2O) + H_2O_2 \rightleftharpoons \tilde{O_2}(\tilde{H_2O_2}) + H_2O$			-42	this work
$\tilde{O_{2}^{-}}(H_{2}O_{2}) + H_{2}O_{2} \Rightarrow \tilde{O_{2}^{-}}(H_{2}O_{2}) + 2H_{2}O_{2}$			-1	this work
$\tilde{O_2}(H_2O_3 + H_2O_2 \rightleftharpoons \tilde{O_2}(H_2O_2) + 3H_2O_2)$			28	this work
$O_2^{-}(H_2O_2) + CO_2 \rightleftharpoons O_2^{-}(CO_2)(H_2O_2)$			7	this work

* AK1970 (Arshadi and Kebarle, 1970); FF1974 (Fehsenfeld and Ferguson, 1974); HFG1978 (Huertas et al., 1978); HY1992 (Hiraoka and Yamabe, 1992); KFP1972 (Kebarle et al., 1972); NIST2016 (Bartmess, 2016); OSull (O'Sullivan et al., 2018).

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Competing interests. The authors declare that they have no conflict of interest.

Disclaimer. The manuscript has not been reviewed by the Colorado Department of Public Health and Environment. The scientific results and conclusions, as well as any views or opinions expressed herein, are those of the author(s) and do not necessarily reflect the views of the department or the State of Colorado.

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