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#### FLORIDA INTERNATIONAL UNIVERSITY

#### Miami, Florida

# HYBRID ELECTROCHEMICAL CAPACITORS: MATERIALS, OPTIMIZATION, AND MINIATURIZATION

A dissertation submitted in partial fulfillment of the

requirement for the degree of

#### DOCTOR OF PHILOSOPHY

in

#### MATERIALS SCIENCE AND ENGINEERING

by

Richa Agrawal

2018

To: Dean John L. Volakis College of Engineering and Computing

This dissertation entitled Hybrid Electrochemical Capacitors: Materials, Optimization, and Miniaturization, written by Richa Agrawal, having been approved in respect to style and intellectual content, is referred to you for judgment.

We have read this dissertation and recommend that it be approved.

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Date of Defense: January 11, 2018

The dissertation of Richa Agrawal is approved.

Dean John L. Volakis College of Engineering and Computing

Andrés G. Gil Vice President for Research and Economic Development and Dean of the University Graduate School

Florida International University 2018

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# DEDICATION

This work is dedicated to the greatest teacher and educator of all, life - for the plethora of crests and troughs it leads you through and for the dreams, aspirations, and the ceaseless hope that it brings.

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#### ABSTRACT OF THE DISSERTATION

# HYBRID ELECTROCHEMICAL CAPACITORS: MATERIALS, OPTIMIZATION, AND MINIATURIZATION

by

Richa Agrawal

Florida International University, 2018

Miami, Florida

Professor Chunlei Wang, Major Professor

With the ever-advancing technology, there is an incessant need for reliable electrochemical energy storage (EES) components that can provide desired energy and power. At the forefront of EES systems are electrochemical capacitors (ECs), also known as supercapacitors that typically have higher power and superior cycle longevity but lower energy densities than their battery counterparts. One of the routes to achieve higher energy density for ECs is using the hybrid EC configuration, which typically utilizes a redox electrode coupled with a counter double-layer type electrode.

In this dissertation, both scale-up (coin-cell type) as well as scale-down (on-chip miniaturized) hybrid ECs were designed, constructed and evaluated. The first part of the dissertation comprised material identification, syntheses, and electrochemical analyses. Lithium titanate-anatase titanium oxide ( $Li_4Ti_5O_{12}$ -TiO<sub>2</sub>) composites were synthesized via electrostatic spray deposition (ESD) and characterized in both half-cell and full-cell assembly against lithium and nanostructured carbon based counter electrodes, respectively. The second redox type material studied for hybrid electrochemical capacitors was ESD derived manganese oxide ( $MnO_x$ ). The  $MnO_x$  electrodes exhibited a

high gravimetric capacitance of 225F g<sup>-1</sup> in aqueous media. Further improvement in the rate handling of the  $MnO_x$  electrodes was achieved by using CNT additives. The  $MnO_x$ -CNT composites were tested in full-cell assembly against activated carbon counter electrodes and tested for different anode and cathode mass ratios in order to achieve the best energy-power tradeoff, which was the second major goal of the dissertation. The optimized hybrid capacitor was able to deliver a high specific energy density of 30.3 Wh kg<sup>-1</sup> and a maximal power density of 4kW kg<sup>-1</sup>. The last part of the dissertation focused on a scale-down miniaturized hybrid microsupercapacitor; an interdigitated electrode design was adopted in order to shorten the ion-transport pathway, and  $MnO_x$  and reduced graphene oxide (rGO) were chosen as the redox and double layer components, respectively. The hybrid microsupercapacitor was able to deliver a high stack energy density of 1.02 mWh cm<sup>-3</sup> and a maximal stack power density of 3.44 W cm<sup>-3</sup>, both of which are comparable with thin-film batteries and commercial supercapacitor in terms of volumetric energy and power densities.

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#### 1. INTRODUCTION

#### 1.1 **Overview**

With the ever-changing technology, reliable energy storage has become rather a prerequisite. Given the myriad of applications ranging from microelectronics to electric vehicles to large-scale stationary applications, the required electrochemical energy storage system becomes very device-specific. With the recent boom in the development of miniaturized electronic systems such as wireless sensors, implantable devices, smart cards etc., the demand for miniaturized power sources is at an all-time high. For such electronic devices, the power requirement typically ranges from several hundred µW to several hundred mW, while energy requirement ranges from several hundred µWh to several hundred mWh [1]. For instance, implantable devices such as pacemaker and cardiac defibrillator typically require 30-100 µW. Sensor nodes typically consume a power of 1-20 µW depending upon the complexity of the sensing requirement and speed of transmission. Micro energy systems such as microbatteries, micro fuel-cells along with micro energy harvesters are considered to be the next generation energy and power sources for such systems. However, quite akin to their larger counterparts, microbatteries and micro fuel cells suffer from low power density and limited cycle life and energy harvesters on the other hand require an energy storage component in tandem to store their excess energy [2]. Electrochemical capacitors, also known as supercapacitors or ultracapacitors can provide both transient and high powers and long cycle lives but with limited energy. One of the solutions to providing peak power and high energy at the same time is connecting the batteries and supercapacitors externally [3]. Nevertheless it is desirable for the next generation micro-power device to be a single standalone device for

a simultaneous supply of high power and high energy. In general, energy and power densities are based on larger cells. However, these values are rather diminished in microbatteries and microsupercapacitors because of the weight of the packaging, hardware, limited area, etc. All these factors demand the development of a novel on-chip micro-power, which combines both the advantages of microbatteries and microsupercapacitors. Creating such devices however, requires thorough understanding of the mechanisms of combining two disparate charge storage mechanisms harmoniously into one optimal system.

#### 1.2 **Research Problems**

The ultimate goal of this dissertation is to design, fabricate and assess high power and high energy hybrid/asymmetric electrochemical capacitors in both coin cell (scaleup) and miniaturized (scale-down) forms. However, the intrinsic disparity in the charge storage mechanisms as well as the rate handling characteristics of double layer and redox materials makes hybridization a challenging process. The *research problems* encountered in this dissertation and their possible solutions are discussed as follows:

1. What are the factors that must be addressed to obtain the optimized power and energy densities along with high cycle life in the hybrid system?

a. <u>The cell capacity (Ah) is limited by the double layer component:</u> In order to optimize the cell performance, the redox/faradaic component can be operated at a certain depth of discharge, where the capacities of the two components are similar. However, such an operation is undesirable for long cycling. Another method is choosing *an appropriate mass ratio of the redox and double layer electrode*, which

can ensure that similar charges are held by the two electrodes. However, a very massive double layer electrode can compromise with the rate capability of the system and therefore the best electrode mass ratio for optimal energy-power tradeoff should be investigated.

b. Large power disparity in the double-layer and faradaic components: Given the low RC time constant of double layer capacitors, they charge and discharge in very short periods of time. Redox materials on the other hand typically possess lower power than their double layer counterparts, which can be attributed to sluggish ion diffusion processes, as a result of which the redox/faradaic component becomes the dictating factor of the resulting cell power. However, the power mismatch can be addressed by carefully designing the redox electrode, for instance – i) nanostructuring the material can ensure shorter ion transport pathways and improve the electrode kinetics; ii) engineering the thickness of the electrode can also address the relative inferior kinetics of the redox electrode – typically thin films exhibit superior kinetics and low resistance; iii) adding optimal amounts of conducting agent additives – typically metal oxides exhibit low electronic conductivity, which can be offset by using conducting agents such as carbon black (CB) or even nanostructured graphitic carbons like carbon nanotube (CNT), which can provide for lower percolation thresholds than the conventional CB. Therefore the power mismatch between the double layer and redox electrode can be addressed by nanostructuring and optimizing the electrode thicknesses and also by optimizing nanostructured carbon additive content.

c. <u>Cycle life is typically limited by the redox component</u>: Typically the double layer electrode exhibits superior cycle character to the redox electrode. However, the cycle life of the cell also depends on the current at which the cell is cycled along with the cell voltage. Therefore, choosing optimal current and voltage can enhance the cycle-life of the hybrid/asymmetric device.

2. How ensure optimal energy-power tradeoff for the asymmetric to microsupercapacitor? Unlike the scale-up systems, miniaturized supercapacitors have much lower effective material mass loadings due to their much smaller footprints. As a result of the diminutive electrode material loading on the microsupercapacitor platforms, gravimetric performance metrics are therefore inappropriate. More reliable assessment criteria for asymmetric microsupercapacitors include geometric and volumetric normalization, which makes optimizing the active material thickness an effective route to ensure maximal energy-power tradeoff. Furthermore, from an architectural standpoint, the "in-plane interdigitated design" can offer a multitude of advantages. For instance, having alternating digits of anode and cathode materials in close proximity can shorten the ion-transport pathways and effectively improve the rate capability of the on-chip micro-system.

#### 1.3 Hypotheses

As discussed in the previous section, the inherent capacity and rate mismatch between the double layer and redox electrodes can be addressed using several different routes in order to ensure maximal energy-power tradeoff. For "scale-up" systems, the most appropriate evaluation criterion is gravimetric. In general, electrode materials that

rely on redox charge storage mechanisms such as manganese oxides  $(MnO_x)$ , lithium insertion electrodes (Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>, anatase TiO<sub>2</sub>) exhibit higher capacity than double-layer materials (activated carbons, graphene, CNT). The capacity mismatch between the two types of electrodes can be addressed by adjusting the electrode mass ratio to ensure charge equivalence in the electrodes. In order to address the intrinsic kinetics mismatch between the redox and the double layer electrode, the redox electrode can be complemented with nanostructured graphitic carbons, which have lower percolation thresholds than the conventionally used carbon black; optimal carbon content in the hybrid electrode can ensure effective dispersion of the nanostructured carbon and better rate handling of the redox material. For the "scale-down" or miniature systems, on the other hand, gravimetric metrics are inappropriate given the smaller device footprints. A more balanced system in terms of energy and power can be achieved by optimizing active material thicknesses. It is also hypothesized, that the *interdigitated asymmetric* design can enhance the rate capability of the device since it offers the feasibility of having alternating fingers of anode and cathode materials in close proximity, which can shorten the ion-transport pathways.

#### 1.4 Research Plan

The research plan adopted for this dissertation is presented in Figure 1.1; the specific goals that were worked toward are as follows:

1. *Material identification and synthesis:* In order to design and evaluate full cell hybrid systems, it is imperative to identify the electrode material. To attain this goal, the faradaic electrode materials ( $MnO_x$ ,  $Li_4Ti_5O_{12}$ -anatase  $TiO_2$ ) were synthesized via

electrostatic spray deposition (ESD) and were characterized from both materials and electrochemical aspects.

- 2. Empirical electrochemical performance optimization of the asymmetric/hybrid electrochemical capacitor: The electrodes synthesized in the previous objective served as the framework for constructing and evaluating the asymmetric full-cell system. The relatively inferior kinetics of the redox electrode was addressed using optimal nanostructured carbon additive. The full-cell asymmetric system was optimized for maximal energy-power tradeoff using different electrode mass ratios.
- 3. Microelectrode platform development and active materials integration: Microelectrodes based on carbon microelectromechanical systems (C-MEMS) and 2D interdigitated gold electrodes were developed and characterized. The active materials were integrated using ESD, electrophoretic deposition (EPD) and electrochemical deposition.
- 4. *Electrochemical performance optimization of the asymmetric/hybrid microsupercapacitor:* The hybrid microsupercapacitor was optimized using different electrode thicknesses and alternating interdigitated fingers of the anode and cathode materials.

#### 1.5 **Scope of the Dissertation**

Chapter 2 provides the background of the dissertation along with relevant literature review. Supercapacitors have been discussed from both charge-storage and configuration perspectives. Both scale-up and miniaturized supercapacitors have been discussed. Chapter 3 provides detailed methodology of the experimental techniques adopted for this dissertation, which include photolithography techniques and active

material integration methods including electrostatic spray deposition (ESD) and electrodeposition. Chapter 4 investigates a scale-up hybrid capacitor (lithium-ion capacitor) design utilizing a lithium insertion host viz. anatase TiO<sub>2</sub>-Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> (ATO-LTO) composite film in a lithium-containing electrolyte. To couple the ATO-LTO anode, an ESD based rGO-CNT cathode was used. The ESD based lithium-ion capacitor was able to demonstrate a high cell voltage of 3V in addition to superior gravimetric energy density as well as capacity. Chapter 5 discusses electrostatic spray deposition (ESD) derived manganese oxide  $(MnO_x)$  electrodes and their investigation as pseudocapacitive charge storage material as well as microelectrode-integrands. Chapter 6 provides an indepth study of ESD based manganese oxide and carbon nanotube (MnO<sub>x</sub>-CNT) composites for scale-up asymmetric supercapacitor design and evaluation. The chapter elucidates that the utilization of a pseudocapacitive component and a double layer component within the same cell significantly stretches the cell voltage of aqueous electrolytes, and results in superior energy and power characteristics. Chapter 6 also discusses the empirical conditions for optimized energy-power trade-off for the asymmetric system. Chapter 7 expands on the concept of asymmetric capacitor configuration from scale-up to scale-down miniaturized system. From the electrochemical characterization performed on the interdigital systems, the asymmetric microsupercapacitor comprising  $MnO_x$  cathode and reduced graphene oxide (rGO) anode demonstrates superior electrochemical characteristics than the symmetric rGO//rGO and  $MnO_x//MnO_x$  microsupercapacitor configurations. Chapter 8 provides with a summary and future works in the direction of this dissertation.



Figure 1.1: Flow chart of the research plan

#### 1.6 References

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#### 2. BACKGROUND AND LITERATURE REVIEW

#### 2.1 Historical Overview

The discovery of the electrochemical double layer capacitors (EDLCs) dates back to 1957 when Becker patented a "Low voltage electrolytic capacitor" with porous carbon electrodes [1]. The double layer phenomenon however was not properly understood at that time. In 1966, researchers at Standard Oil of Ohio (SOHIO) patented "electrical energy storage apparatus" while working on fuel cell designs [2]. SOHIO did not commercialize their invention and licensed their technology to Nippon Electric Company (NEC), who marketed the results as "supercapacitors" in 1978 [3]. Around the same time, Panasonic marketed its "Goldcaps" brand, which became a successful energy source for memory backup applications [3]. The earlier applications of electrochemical capacitors primarily comprised low current applications such as powering SRAM chips for data backup. In late 1970s, Brian Evans Conway conducted extensive work on ruthenium oxide based electrochemical capacitors. The charge storage mechanism in his capacitors was a combination of Helmholtz double-layer and "pseudocapacitive", which is essentially faradaic activity at the electrode-electrolyte interface. Due to the increased amounts of possible applications, the entire field of electrochemical capacitors flourished in the 1990s and a lot of research and development efforts have been invested in supercapacitors since then.

#### 2.2 Commercial Market and Research Trends in Supercapacitors

In a recent press release by Transparency Market Research [4], the global market for supercapacitors stood at US \$1.21 billion in 2014 and is anticipated to rise at a compound

annual growth rate (CAGR) of 22.3% from 2015 to 2023, as a result of which the market is projected to surge to US \$7.37 billion by 2023 [4]. The market for hybrid capacitor itself is predicted to rise at a CAGR of 23.5% during 2015-2023 and is projected to lead the market in the upcoming years [4]. The primarily impetus for the fast supercapacitor market growth is the demand for advanced energy storage systems in the electronics industry. In the automotive industry, on the other hand, the rapid charge and discharge from the supercapacitors can extend battery lifespans [4].

Some of the key players of the global supercapacitor market are *Advanced Capacitor Technologies, Axion Power International, Cap XX, EEStor Corporation, ELTON, FastCAP Systems, Maxwell Techonologies, Nesscap Energy*, and others. Apart from the thriving industry, supercapacitor research is widely popular in research laboratories and universities. Figure 2.1 elucidates the number of publications on supercapacitor research in the past decade.



Figure 2.1: Number of publications resulting from supercapacitor research in the past decade (Source: Web of Science)

#### 2.3 Fundamentals of Electrochemical Capacitors

Electrochemical capacitors (ECs), often called as "ultracapacitors" or "supercapacitors", are a class of energy storage devices that bridge the gap between conventional electrolytic capacitors and batteries. These capacitors are characterized by moderate specific energy (~5Whkg<sup>-1</sup>), high specific power (~10kWkg<sup>-1</sup>), and superior cycle lives than their battery counterparts. Figure 2.2 depicts the special positioning of electrochemical capacitors in the specific power-specific energy plot also known as "Ragone plot"; it can be seen that electrochemical capacitors bridge the gap between conventional capacitors and batteries, with intermediate time constants.



Figure 2.2: Ragone plot for different energy storage devices.

The primary electrochemical characteristics of any energy storage device are its energy density and power density, both of which can be expressed per unit mass (per kilogram), per unit area or per unit volume. The energy of an electrochemical capacitor is given as:

$$E = \frac{1}{2}CV^2 \quad (2.1)$$

where C is the capacitance and V is the cell voltage. As evident, the energy is related as power-squared and therefore, stretching the cell potential can significantly enhance the energy of the system. Power, on the other hand is the measure of the rate of energy delivery, i.e. energy per unit time. However, the maximum power delivered by a capacitor is limited by the internal resistance of the system, also known as equivalent series resistance (ESR). The maximal power of a system can be computed using equation (2.2).

$$P_{max} = \frac{V^2}{4ESR} \quad (2.2)$$

As evident from the equation, power is an inverse function of the resistance of the system - lower the resistance, higher is the power delivered by the system. The ESR can be measured as the voltage drop introduced in the discharging part of the charge-discharge curves of the system, and hence decreases the maximum voltage of a capacitor during discharge and therefore limits the maximum power of the system. However, this is the maximum power and in general, the peak power in an actual system is lower than P<sub>max</sub>.

#### 2.4 **Classification of Electrochemical Capacitors**

ECs store energy in the form of charge at the electrode/electrolyte interface of materials with high surface area. Depending on the charge storage mechanism ECs are subdivided into (i) Electrochemical Double Layer Capacitors (EDLCs) and (ii) pseudocapacitors. A third category, the so-called "hybrid electrochemical capacitors" essentially combine both EDLCs and pseudocapacitors.



Figure 2.3: Classification of Electrochemical Capacitors

#### 2.4.1 Electrochemical Double layer Capacitors (EDLCs)

EDLCs, quite analogous to electrolytic capacitors store energy in an electrostatic manner; charges are stored at the electrode/electrolyte interface and the capacitance is governed by the thickness of the Helmholtz double layer and hence the name. When an external potential is applied, charges accumulate at the electrode surface and the charge buildup leads to diffusion of opposite charges across the separator generating a "*double layer*" on each electrode. The thickness of the double layer can be computed from equation (2.3) [5, 6]:

$$\kappa^{-1} = \left(\frac{\varepsilon_r \varepsilon_0 k_B T}{F^2 \sum N_i Z_i^2}\right)^{1/2} \quad (2.3)$$

where  $\kappa^{-1}$  is the double layer thickness,  $\varepsilon_r$  is the dielectric constant of the electrolyte,  $\varepsilon_0$  is the electrical permittivity of free space,  $k_B$  is the Boltzmann constant, F is the Faraday constant,  $N_i$  is the ion concentration and  $Z_i$  is the ionic charge. Typically EDLCs have capacitances larger than one or two orders of magnitude higher than electrolytic capacitors given the fact that the electrodes used for EDLCs are porous and possess very large surface areas. Furthermore, EDLCs also exhibit high cycling abilities, usually of the order of  $10^5$ - $10^6$  cycles. EDLC materials include carbon based materials including *activated carbon (AC), carbon aerogels, carbon nanotubes (CNTs), onion like carbons (OLCs), carbon nanowires (CNWs), carbon nanorods, carbon nanofibers (CNFs), and graphene [7].* 

#### 2.4.2 Pseudocapacitors

In contrast to conventional capacitors and EDLCs, *pseudocapacitors store charge in a Faradaic manner*, or in other words, the capacitance in this kind of capacitors arises from the transfer of charge between the electrode and electrolyte. This charge transfer is highly reversible and fast and as a result of which the charging and discharging curves of these devices look like those of a typical capacitor. The latter is referred to as "pseudo" owing to the reversible Faradaic-type charging and discharging. Owing to a Faradaic mechanism of charge storage, these capacitors in general exhibit higher specific energies and capacitances than their EDLC counterparts [8, 9]. The most widely used pseudocapacitive materials include *metal oxides (mostly ruthenium oxide, manganese*  oxide, and nickel hydroxide), conducting polymers including polyaniline (PANI), polypyrrole (PPY), polythiophene (PTH) and their derivatives [7].

#### 2.4.3 Hybrid Capacitors

As their name suggests, hybrid capacitors comprise mechanisms from both double-layer and redox-based charge storage. Hybrid capacitors can be further classified based on *material design and device configuration*; the former comprises composite electrodes, whereas the latter encompasses "asymmetric" type electrochemical capacitors. Composites in general can be explained as material hybrids, containing a harmonious amalgamation of redox and double layer materials within one electrode. Asymmetric systems are essentially devices that contain one largely redox type and the other largely double layer type electrode. It should be noted that asymmetric capacitors can contain pristine redox and double layer counter electrodes and vice versa, as well as material composites as electrodes.

#### 2.4.3.1 Composite electrodes

As mentioned previously, pseudocapacitive materials exhibit rather high capacitance but since these devices depend primarily on redox processes, they have lower cycle lives than double layer capacitors. Composite hybrid electrodes can therefore benefit from higher capacitances of pseudocapacitors and long cycle lives of double layer capacitors. Among the conducting polymers, PANI, PPY, PTH and their derivatives are widely investigated. Upon oxidation, the electrolyte ions are transferred to the polymer chain, whereas upon reduction, the ions detach from the chain and get released into the electrolyte; the process is shown in Equation (2.4). The ion transfer typically takes place

through the bulk of the electrodes and as a result of which the resultant specific capacitance is high.

$$[PPY^+X^-] + e^- \leftrightarrow [PPY] + X^- (2.4)$$

However, the ion insertion/extraction is accompanied with volumetric changes in the electrodes, which results in degradation from shrinking, swelling, etc. leading to a loss in conductivity and mechanical stability. Conducting polymers can therefore benefit from the carbon based materials which are known for their mechanical strength and resilience. These dl carbons can act as buffers and alleviate mechanical stresses resulting from volumetric changes and therefore improve the electrode longevity. Furthermore, the addition of dl based materials can enhance the conductivity and rate capability of the system.

Transition metal oxides (TMOs) such as  $RuO_2$ ,  $NiO_x$ , manganese oxides ( $MnO_x$ ), on the other hand, undergo fast reversible redox reactions at their surfaces, which lend their pseudocapacitive characteristics. Typically, TMOs exhibit larger capacitances than their double layer counterparts. However, they suffer from poor electrical conductivity and low cycle lives. Optimal TMO/double layer composites can therefore benefit from the large capacitance of the metal oxides, the superior electrical conductivity and cycling performance of the carbons. Furthermore, especially for nanostructured carbons such as carbon nanotubes and graphene, TMOs can act as "*spacers*" and suppress their agglomeration, which can help fully exploit their high surface areas and capacitances. Table 2.1 lists specifications of some of the pseudocapacitive/double layer composite electrodes reported in the literature.

Composite	Morphology	Electrolyte	Performance	Capacitance retention	Ref
Graphene/PANI nanorods	Fibrous morphology with appropriate pore size distribution	1M HClO <sub>4</sub>	878.57 Fg <sup>-1</sup> at 1 Ag <sup>-1</sup>	Low capacitance fading after 1000 cycles	10
Graphene/PANI paper	Layered structure	1M H <sub>2</sub> SO <sub>4</sub>	233 Fg <sup>-1</sup>	N/A	11
Graphene/PANI	Uniform morphology with no indication of PANI and graphene agglomeration	1M H <sub>2</sub> SO <sub>4</sub>	640 Fg <sup>-1</sup>	90% after 1000 charge/discharge cycles	12
Graphene Nanosheets/PANI	Nano fibrillar morphology	1M H <sub>2</sub> SO <sub>4</sub>	1130 Fg <sup>-1</sup> at 5 mVs <sup>-1</sup>	87% after 1000 cycles	13
Graphene Oxide (GO)/PANI	Hierarchical Structure	1M H <sub>2</sub> SO <sub>4</sub>	555 Fg <sup>-1</sup> at a discharge current density of 0.2 Ag <sup>-1</sup>	92% after 2000 cycles	14
Graphene Oxide(GO)/PANI/CO <sub>2</sub>	PANI nanoparticles uniformly coated on GO sheets	1 M H <sub>2</sub> SO <sub>4</sub> solution.	$425 \text{ Fg}^{-1} \text{ at } 0.2 \text{ Ag}^{-1}$	83% after 500 cycles	15
Reduced Graphene Oxide/PANI	Fibrillar morphology	$1M \\ aqueous \\ H_2SO_4 \\ solution$	250 Fg <sup>-1</sup>	N/A	16
Graphene Nanosheets/PPy	PPy homogeneously surrounded by GNS	1M H <sub>2</sub> SO <sub>4</sub> .	$482 \text{ Fg}^{-1}$ at 0.5 Ag	95% after 1000 cycles	17
Graphene Nanosheets/PPy	Dispersed network - polypyrrole nanowire attached to basal planes of GNS	1M NaCl	165 Fg <sup>-1</sup> at 1 Ag <sup>-1</sup>	92% after 1000 cycles	18
Graphene Oxide/PPy nanowires	PPy nanowires attached to the surface of GO nanosheets	1 M KCl aqueous solution	633 Fg <sup>-1</sup> at 1 Ag <sup>-1</sup>	94% after 1000 cycles	19
Reduced Graphene Oxide/PPy	PPy located on both sides of the GO sheets	$1 \mathrm{M} \mathrm{H}_2 \mathrm{SO}_4$	376 Fg <sup>-1</sup> at a scan rate of 25mVs <sup>-1</sup>	84% after 1000 cycles	20

# Table 2.1: Summary of pseudocapacitive/double layer composites reported in the literature
Reduced Graphene Oxide (rGO)/PPy	GO/PPy composite was uniformly electropolymerized onto the surface of gold electrode	1M H <sub>2</sub> SO <sub>4</sub>	424 Fg <sup>-1</sup> at 1Ag <sup>-1</sup>	N/A	21
MnO <sub>2</sub> /Graphene/Nickel foam (NF)	Nanoneedle like MnO <sub>2</sub> uniformly grew on porous G/NF sheets	0.5 M Na <sub>2</sub> SO <sub>4</sub>	476 Fg <sup>-1</sup> at 1 Ag <sup>-1</sup> 216 Fg <sup>-1</sup> at 10 Ag <sup>-1</sup>	N/A	22
Graphene/MWNTs/MnO <sub>2</sub>	Nanowires on graphene/MWNT foam	2M Li <sub>2</sub> SO <sub>4</sub>	1108.9 Fg <sup>-1</sup> at 1.89 Ag <sup>-1</sup>	97.94% after 13000 cycles	23
Reduced Graphene Oxide/MnO <sub>2</sub>	Flower-like nanoparticles	1M Na <sub>2</sub> SO <sub>4</sub>	450 Fg <sup>-1</sup> at 2mVs <sup>-1</sup>	90% after 10000 cycles	24
N-doped graphene/MnO <sub>2</sub>	Sheet like morphology	1M Na <sub>2</sub> SO <sub>4</sub>	$257.1 \text{ Fg}^{-1}$ , 224.4 Fg <sup>-1</sup> , 205.6 Fg <sup>-1</sup> and 192.5 Fg <sup>-1</sup> at densities of 0.2, 0.5, 1 and 2 Ag <sup>-1</sup> , respectively.	94.2% after 2000 cycles	25
Graphene/Mn <sub>3</sub> O <sub>4</sub>	Nanoparticles	1M Na <sub>2</sub> SO <sub>4</sub> 6M KOH	$175 \text{ Fg}^{-1}$ and $256 \text{ Fg}^{-1}$ for $1 \text{ M}$ $\text{Na}_2 \text{SO}_4$ and $6 \text{ M}$ KOH respectively	N/A	26
RuO <sub>2</sub> /Graphene	5-10 nm RuO <sub>2</sub> NPs well anchored to the graphene backbone	1M H <sub>2</sub> SO <sub>4</sub>	570 Fg <sup>-1</sup> for 38.3 wt% of Ru at 1mVs <sup>-1</sup>	97.9% after 1000 cycles	27
Fe <sub>3</sub> O <sub>4</sub> /reduced Graphene Oxide	Nanoparticles	1M KOH	220.1 Fg <sup>-1</sup> at 0.5 Ag <sup>-1</sup>	Capacitance increases from $180.6 \text{ Fg}^{-1}$ to $220.1 \text{ Fg}^{-1}$ during first 800 cycles and remains stable until 3000 cycles	28
Reduced Graphene Oxide/Co(OH) <sub>2</sub>	Nanoparticles	2M KOH	476 Fg <sup>-1</sup> at 1 Ag <sup>-1</sup> 300 Fg <sup>-1</sup> at 10 Ag <sup>-1</sup>	90% after 1000 cycles	29
Graphene/Co <sub>3</sub> O <sub>4</sub>	Multi-layered morphology with uniform distribution of Co <sub>3</sub> O <sub>4</sub>	6М КОН	331Fg <sup>-1</sup> at 5 Ag <sup>-1</sup>	122% after 5000 cycles	30
Graphene/ZnO	Particles	1M KOH	Highest capacitance of 62.2 Fg <sup>-1</sup>	Only 5.1% drop after 200 cycles	31

Key: PPy –polypyrrole; Fe<sub>3</sub>O<sub>4</sub> – iron oxide; rGO – reduced graphene oxide, ZnO – zinc oxide, KOH – potassium hydroxide; PANI – polyaniline;  $RuO_2$  – ruthenium oxide

### 2.4.3.2 Asymmetric-type Hybrid Capacitors

In a broader sense, *asymmetric-type hybrid capacitors comprise two electrodes with different charge-storage mechanisms*. The rationale for using the asymmetric capacitor design is essentially utilizing the larger charge storage capability of the redox-based electrode and the faster kinetics and cycle longevity of the double layer electrode from one cohesive system. Figure 2.4 illustrates the schematic illustration of the construction of an asymmetric capacitor; the components are packaged and contained in an electrolyte solution. According to equation (2.1), the energy of a supercapacitor is directly proportional to the cell capacitance and has direct quadratic dependence on the cell voltage. The total capacitance of cell ( $C_{cell}$ ) containing electrodes with individual capacitances  $C_1$  and  $C_2$  can be computed using equation (2.5):

$$\frac{1}{C_{cell}} = \frac{1}{C_1} + \frac{1}{C_2} \quad (2.5)$$

Since two dissimilar electrodes are used in an asymmetric capacitor, these electrodes possess different capacitances. In general the redox electrode has a much larger capacitance than its double layer counterpart and therefore the overall capacitance exhibited by the device is  $C_{cell} \sim C_{redox}$ , which in principle, is the capacitance of the redox electrode. Hence, the capacitance of a capacitor in an asymmetric configuration is twice of that in symmetric, if the same electrode were utilized. As a result of this higher capacitance, energy density of an asymmetric cell is much higher. However, it should be noted that equation (2.4) is a theoretical approximation that only considers the electrodes

of the system, and therefore the empirical values may differ owing to other cell components including contributions from electrolyte, separator, current collectors, and so on. The optimal material choice for designing an asymmetric system stems from the following key considerations:

- i. *Matching the capacity of the active materials:* Since the redox electrode typically has a much higher specific capacitance than the double layer electrode, there is a mismatch in the charge held by the individual electrodes, if the identical masses were used for both the electrodes. To compensate for the capacity mismatch at a given current rate, the active material mass on the electrodes can be adjusted in order to ensure that the charge held by the individual electrodes is balanced.
- ii. *Maximizing the operational voltage of the cell:* Both the electrodes should be chosen such that their potentials are either at high or low end of the operating voltage. Since energy increases as potential squared, the wider the voltage window, more is the enhancement in the energy.

Furthermore the two electrodes can be engineered in terms of *porosity*, *microstructure*, *mass*, *thickness*, etc. in order to exploit the full potential of each of the component. When optimized, such a system can provide with the benefits from both the redox-based and capacitive system. Two types of asymmetric capacitor systems have been widely investigated including *pseudocapacitive/double layer systems*, and *lithium-based battery-type hybrid capacitors*. Generally, the former are based in aqueous media whereas the latter are contained in nonaqueous lithium-containing electrolytes.



Examples – Conducting Polymers, Activated Carbons, Nanostructured carbons, SnO<sub>2</sub>

Figure 2.4: Construction of an asymmetric capacitor; the assembly is contained in an electrolyte solution.

# 2.4.3.2.1 Pseudocapacitive/double layer (dl) based asymmetric capacitors

The asymmetric design blends the characteristics of both electrochemical capacitors and batteries by utilizing the high capacity of the pseudocapacitive electrodes and the fast charge-discharge response arising from the double layer mechanism from the carbon based electrodes. Typically a high surface area carbon based electrode is utilized as the negative electrode, whereas a battery-type or pseudocapacitive electrode is used as the positive electrode. Furthermore, asymmetric electrochemical capacitors with double layer and pseudocapacitive electrodes offer the advantage of stretching the voltage of full electrochemical cells even in water based media. The high overpotentials for  $H_2$  and  $O_2$  evolution at the carbon-based electrode and the pseudocapacitive electrode, respectively effectively extend the potential window of aqueous electrolytes beyond the

thermodynamic limit (~1.2V), resulting in significantly higher energy densities than the capacitors in symmetric systems. The use of aqueous electrolytes is desirable owing to their high ionic conductivity, and the feasibility to fabricate devices without the need for contained atmospheres like argon- or nitrogen-filled glove boxes [32]. Chapter 5 of the dissertation elucidates one such asymmetric capacitor constructed with manganese oxide-carbon nanotube (MnO<sub>x</sub>-CNT) composite electrodes along with activated carbon (AC) counter electrodes. Table 2.2 provides a summary of the some of the asymmetric systems based on pseudocapacitive and double layer electrodes in the literature.

Positive Electrode	Negative Electrode	Electrolyte	Current density/scan rate	Specific Capacitance /Performance	Capacitance Retention	Ref
MnO <sub>2</sub> nanowire/Graphene	Graphene	1 M Na <sub>2</sub> SO <sub>4</sub>	0.5 Ag <sup>-1</sup>	Specific capacitance of 24.5 Fg <sup>-1</sup>	79% after 1000 cycles	33
				Energy density of 7 Whkg <sup>-1</sup> at a power density of 5kWkg <sup>-1</sup>		
MnO <sub>2</sub> -coated Graphene	Graphene	1 M KCl	4 mA	Specific capacitance of 328 Fg <sup>-1</sup>	99% after 1300 cycles	34
				Energy density of 11.4 Whkg <sup>-1</sup> Power density of 25.8 kWkg <sup>-1</sup>		
MnO <sub>2</sub> nanotubes	Activated Graphene	1 M Na <sub>2</sub> SO <sub>4</sub>	0.25 Ag <sup>-1</sup>	Specific capacitance of 365 Fg <sup>-1</sup>	90.4% after 3000 cycles	35
				Energy density of 22.5 Whkg <sup>-1</sup>		
				Power density of 146.2 kWkg <sup>-1</sup>		
Reduced Graphene Oxide/MnO <sub>2</sub>	RGO	1 M Na <sub>2</sub> SO <sub>4</sub>	$10 \text{ mAg}^{-1}$	Specific capacitance of 113 mFcm <sup>-2</sup>	93% after 3600 cycles	36
				Energy density of 11.5 µWhcm <sup>-2</sup>		

 Table 2.2: Summary of some of the reported pseudocapacitive/double layer asymmetric supercapacitors

				Power density of 3.8 mWcm <sup>-2</sup>		
PANI	Graphene	1M HCl		Energy density of 4.86 Whkg <sup>-1</sup> Power density of 8.75 kWkg <sup>-1</sup>		37
Graphene/MnO <sub>2</sub> - textile	SWNTs- textiles	0.5 M Na <sub>2</sub> SO <sub>4</sub>		Energy density of 12.5 Whkg <sup>-1</sup> Power density of 110 kWkg <sup>-1</sup>	95% after 5000 cycles	38
Graphene/MnO <sub>2</sub>	Activated carbon nanofibers (ACN)	1 M Na <sub>2</sub> SO <sub>4</sub>	200 mV/s	Specific capacitance of 113.5 Fg <sup>-1</sup> Energy density of 51.1 Whkg <sup>-1</sup> Power density of 198 kWkg <sup>-1</sup>	97.3% after 1000 cycles	39
Vertically aligned MnO <sub>2</sub> nanoplates	graphene hydrogel	1 M Na <sub>2</sub> SO <sub>4</sub>	1 A	Specific capacitance of 41.7 Fg <sup>-1</sup> Energy density of 23.2 Whkg <sup>-1</sup> Power density of 1 kWkg <sup>-1</sup>	83.4% after 5000 cycles	40
Ni(OH) <sub>2</sub> /CNTs	Iron nanosheets on graphene sheets	6 M KOH		Energy density of 140 Wh/kg	78% after 2000 cycles	41
MnO <sub>2</sub> /graphene oxide composite	Graphene oxide (GO)	1 M HCl	0.5 A/g	Specific capacitance of 280 F/g Energy density of 35 Wh/kg Power density of 7.5 kW/kg	70% after 1000 cycles	42
(2D) MnO <sub>2</sub>	GNS	Ca(NO <sub>3</sub> ) <sub>2</sub> - SiO <sub>2</sub> composite gel	0.1A/g	Specific capacitance of 774 F/g Energy density of 97.2 Wh/kg	97% after 10000 cycles	43

# 2.4.3.2.2 Battery-type lithium-ion based asymmetric capacitors

Lithium-ion batteries (LIBs) are known for their outstanding energy densities (150-200 Whkg<sup>-1</sup>) and thus if an LIB electrode were coupled with an EC electrode, the resulting device can benefit from the high energy density of LIB and the high power

density of the supercapacitor. For such a hybrid capacitor, a capacitive cathode and a lithium-intercalating anode are typically used along with a lithium-ion electrolyte. For brevity, such capacitors will be referred to as "lithium-ion capacitors" from henceforth. Charge is stored by reversible adsorption/desorption of anions at the surface of the capacitive cathode while at the anode, charge is stored via a reversible insertion/extraction mechanism of the lithium ions. The combined effects provide with an opportunity to enhance both the energy and power densities, while still maintaining superior cycle lives as compared to rechargeable batteries. The concept of such a hybrid supercapacitor was pioneered by Amatucci et al. [44] based on activated carbon (AC) and Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> as the supercapacitor electrode and the Li-intercalating electrode, respectively. Although theoretically enticing, such a device poses several design challenges that must be addressed in order to fully exploit the benefits from both the battery and capacitor electrodes. For instance, lithium-ion intercalation is a Faradaic process which is far more sluggish than the non-Faradaic adsorption and desorption of ions; this mismatch in kinetics leads to a mismatch in power characteristics of the positive and negative electrodes, which must be addressed in order to realize the best of both electrodes. Several methods can be adopted in order to address the kinetics mismatch of the two electrodes - for instance adding conducting carbons in optimal ratios to metal oxides can improve their electronic conductivity and help balance the kinetics mismatch of the two electrodes. Furthermore, the "nano"-sizing the electrode materials provide the benefit of improved kinetics, given the concomitant shortening of ion and electron paths that comes with nano-structuring [45]. As noted by Cericola [46], a combination of both the double layer and redox based materials within one electrode, which they referred to as the

*"internal parallel system"* offers the advantage of realizing both the charge-storage mechanisms from each of the electrodes and offset the shortcomings that arise from having only pristine electrodes. The combination of a redox based material and a double layer material within one electrode allows for intrinsic potential matching as the materials used have to be stable for the same voltage window [46]. Furthermore, the internal parallel system mitigates the capacity mismatch arising from the disparate charge storage mechanism of the redox and double layer materials, and therefore helps in higher material utilization rate. Table 2.3 provides a summary of some of the lithium-ion capacitors reported in the literature.

Cathode	Anode	Electrolyte	Voltage window	Electrochemical Performance	Ref.
Activated graphene	Graphite	1 M LiPF <sub>6</sub> in EC/DEC 1 : 1 (volume)	2-4 V	Specific Capacitance of 266 Fg <sup>-1</sup> at a current density of 0.5 Ag <sup>-1</sup> Energy density of 147.8 Whkg <sup>-1</sup>	47
Trigol-Reduced Graphene Oxide	LTO	1 M LiPF <sub>6</sub> in EC/DEC 1 : 1 (volume)	1-3 V	Maximal energy density of 45 Whkg <sup>-1</sup>	48
Activated carbon	TiO <sub>2</sub> /rGO	1 M LiPF <sub>6</sub> in EC/DEC 1 : 1 (volume)	1-3 V	Energy density of 42 Whkg <sup>-1</sup> at a power density of 0.8 kWkg <sup>-1</sup>	49
MnO <sub>2</sub> nanorodes on rGO	V <sub>2</sub> O <sub>5</sub> nanowire on rGO	1 M LiTFSI in dry acetonitrile	0-2 V	36.9 Fg <sup>-1</sup> Energy density of 15 Whkg <sup>-1</sup> at a power density of 0.4365 kWkg <sup>-1</sup>	50
Spectracarb fiber cloth	V <sub>2</sub> O <sub>5</sub> nanowire graphene composite	1 M LiTFSI in dry acetonitrile	0-2 V	80 Fg <sup>-1</sup> Energy density of 38.8 Whkg <sup>-1</sup> at a power density of 0.455 kWkg <sup>-1</sup>	51
Functionalized graphene	Modified graphite	1 M LiPF <sub>6</sub> with 3 wt% VC in EC/DEC 1 : 1	2-4 V	Energy density of 61 Whkg <sup>-1</sup> at a power density of 1.452 kWkg <sup>-1</sup>	52

 Table 2.3: Summary of the lithium-ion capacitor based studies reported in the literature

		(volume)			
AC	Graphene sheets wrapped nano-Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1 M LiPF <sub>6</sub> /EC/ DMC (nonaqueous)	1.5–3.0 V	29.2 Wh kg <sup>-1</sup> at a power density of 58.4 W kg <sup>-1</sup> 1782.7 W kg <sup>-1</sup> , the specific energy retains 13.4 Whkg <sup>-1</sup>	53
AC	Carbon coated Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1M LiPF <sub>6</sub> in propylene carbonate (nonaqueous)	1.5- 2.5V	~30 mAhg <sup>-1</sup> at 0.17 Ag <sup>-1</sup> 16Whkg <sup>-1</sup> at 1010 Wkg <sup>-1</sup>	54
AC	Carbon modified $Li_4Ti_5O_{12}$	1-M LiPF6 in EC/DMC (1:3 in volume)	1.5- 3.0V	83 Fg <sup>-1</sup> at a current rate of 60 mAg <sup>-1</sup> 16Whkg <sup>-1</sup> at 440 Wkg <sup>-1</sup>	55
Reduced graphene oxide- carbon nanotube composite (rGO- CNT)	Anatase TiO <sub>2</sub> - Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1 M LiPF <sub>6</sub> /EC/ DMC (nonaqueous)	0.05-3V	~32 mAhg <sup>-1</sup> at 0.1Ag <sup>-1</sup> 33.35 Whkg <sup>-1</sup> at 83.55 Wkg <sup>-1</sup> 26.2 Whkg <sup>-1</sup> at 327.5 Wkg <sup>-1</sup> 15.09 Whkg <sup>-1</sup> at 1207.4 Wkg <sup>-1</sup>	56

# 2.5 Microsupercapacitors

Miniaturized supercapacitors, also known as microsupercapacitors (MSCs) have gained much attention in recent years. These devices find application in implantable biomedical devices, environmental sensors, microelectromechanical systems (MEMS) and also in some small personal electronics which require the power in microwatts [57]. Quite akin to their macro counterparts, microsupercapacitors can be connected in series or parallel in order to meet the voltage, current and capacity requirements depending upon the given application. In general, for micro-supercapacitors, the total footprint area of the device is in the millimeter or centimeter range. Microsupercapacitors consist of either thin film electrodes with a thickness of less than 10  $\mu$ m or arrays of microelectrodes with micron-scale sizes which can either be 2D or 3D. For supercapacitors in the "macro" regime, the electrochemical performance is usually reported as specific capacitance, energy and power densities, all in gravimetric terms, i.e. per unit mass. Since any physical quantity in gravimetric terms is a direct measure of mass and the mass of the electrode materials is almost negligible for a microsupercapacitor, gravimetric parameters are rendered almost inappropriate for reporting the performance of a microsupercapacitor [58]. And hence, the key to report the performance of a microsupercapacitor accurately is the footprint area and energy and power in terms of areal density [59].

The first generation of micro-supercapacitors followed the planar 2D architecture of conventional supercapacitors, consisting of two electrodes and a separator soaked in an electrolyte. And to date for cost-effective mass production, the 2D design is preferred over other designs. However, owing to the small footprint area of microsupercapacitors, the areal energy density is quite low for the 2D design. One of the approaches to increase the area of the electrodes is the construction of a platform with electrodes arranged in an "interdigited" fashion. Such a design offers several advantages over the conventional 2D design [60-63], for instance, having the electrodes in the same plane is not only is easy to fabricate, but also helps in achieving smaller distances between the electrodes, thereby improving electron transport and kinetics.

Graphene is a popular candidate for MSC applications given its high specific surface area, excellent mechanical strength and electrical conductivity. However, a critical consideration for using graphene based materials is the restacking of individual graphene sheets during the electrode processing, which hinders the facile accessibility of electrolyte ions to the electrode. In the conventional 2D design, the complete active surface of the graphene sheets is not always accessed. However, it was demonstrated by

Yoo et al [64], that having graphene electrodes side by side in an in-plane design increases the accessibility of the ions to the entire surface of graphene sheets by creating diffusion channels between the electrodes. The proposed micro-supercapacitor was based on a planar architecture of opposing graphene thin films. The structure comprised graphene flakes connecting along the flake edges, which provided sufficient porosity to maximize the coverage of the electrode surface. The effect of graphene edges resulted in specific capacitances of 80  $\mu$ Fcm<sup>-2</sup> for the few-layer graphene electrode, while much higher specific capacitances (0.394 mFcm<sup>-2</sup>) were achieved for multilayer rGO electrodes. It was concluded therefore that the planar geometry provided superior charge mobility and effective utilization of the electrochemical surface area by minimizing the diffusion barriers of electrolyte ions. To further increase the electrolyte ion accessibility to the graphene sheets and prevent restacking, CNTs can also be used as spacers. Beidaghi et al. [65], fabricated rGO/CNT composite based microsupercapacitors by combining photolithography lift-off methods with electrostatic spray deposition. The reduction of GO and the fabrication of electrodes were both achieved by deposition of a solution of GO or GO/CNT on a heated substrate. The electrochemical results indicated high accessibility of the electrolyte ions to the electrodes and faster ionic transport for a layered structure of CNT/rGO. The microsupercapacitor with the electrode composition of 90% rGO and 10% CNT exhibited a capacitance of 6.1 mFcm<sup>-2</sup> at a scan rate of 0.01 Vs<sup>-1</sup>. Even at a very high scan rate of 50 Vs<sup>-1</sup>, the rGO/CNT micro-supercapacitor showed a specific capacitance of 2.8 mFcm<sup>-2</sup>. Another example of graphene based interdigited microsupercapacitors is the carpet-based microsupercapacitors based on graphene/CNTs/Ni electrodes reported by Lin et al [66]. The microsupercapacitor showed

an impedance phase angle of -81.58 at a frequency of 120 Hz, similar to that of commercial aluminum electrolytic capacitors. The microsupercapacitor also delivered an energy density of 2.42 mWhcm<sup>-3</sup> in ionic liquid and a maximum power density of 115 Wcm<sup>-3</sup> in aqueous electrolyte at a scan rate of 400 Vs<sup>-1</sup>. The excellent performance of this micro-supercapacitor was attributed to the seamless CNT/graphene junctions at the interface of the differing carbon allotropic forms. Another important factor that affects the performance of micro-supercapacitors is the thickness of the electrode. Generally, as the thickness of the electrode increases, the increased mass loading of the electrode material increases the electrode resistance which results in decreased gravimetric capacitance. Although thin electrodes show less areal capacitance due to the small mass loading, their very high rate capability and frequency response outweigh the relatively lower specific capacitance. Liu et al [67] demonstrated a microsupercapacitor based on very thin films of graphene quantum dots (GQD). The device was fabricated by electrophoretic deposition of 365 nm thick films of GQD on patterned Au microelectrodes. The device showed capacitive behavior even at high CV scans rates and very small RC time constants of 103.6 µs in aqueous and 53.8 µs in ionic electrolytes. The remarkable performance was attributed to the small thickness of electrodes along with the device architecture and good electrical conductivity of GQDs along with the presence of abundant edge defects. However, this high rate performance came at the cost of specific capacitance and energy density, as device capacitance was 534.7  $\mu$ Fcm<sup>-2</sup> in aqueous electrolyte, which is quite low as compared to other prototypes reported in the literature.

Another consideration is for designing MSCs is the limited footprint area to construct the device. This shortcoming can be addressed by using three-dimensional architectures. The carbon microelectromechanical systems (C-MEMS) technique, also known as *carbon-MEMS* is a microfabrication procedure that essentially involves the pyrolysis of a patterned photoresist into carbon structures [68-71]. C-MEMS offers the feasibility of creating 3D micro-pillars, which offsets the limitation of the small footprint area required for miniaturized systems. The idea of using 3D C-MEMS-based microstructures as current collectors for the integration of other capacitive materials was first demonstrated by Chen et al. [72], where they grew carbon nanotubes (CNTs) on the surface of the C-MEMS structures using spray deposition. The CNT/C-MEMS structures were reported to exhibit specific capacitance as high as 20 times that of the bare C-MEMS structures. Beidaghi et al [73] reported electrochemically activated 3D C-MEMS structures for MSC applications; the electrochemically activated C-MEMS capacitors exhibited a high geometric specific capacitance of 75 mFcm<sup>-2</sup>. The superior electrochemical performance as opposed to the non-activated C-MEMS samples was ascribed to i) the introduction of oxygen-containing functional groups from the activation process, which not only enhances the wettability of the electrode surface but also adds additional pseudocapacitance; ii) the increase in the surface area by the electrochemical treatment, since the treatment oxidizes the carbon surface and opens up closed pores; finally another possible reason for the performance enhancement could be; iii) the irreversible intercalation of electrolyte ions during the polarization process; ions are intercalated into the carbon structures during the first polarization cycle and provide larger capacitance for the successive cycles [73]. Other reports documenting the use of C-MEMS based

platforms for MSC applications include manganese oxide (MnO<sub>x</sub>) integrated carbon micro-pillars [74], and polypyrrole (PPy) integrated C-MEMS structures [75]. In a symmetric two electrode setup, the MnO<sub>x</sub> integrated C-MEMS micro-electrodes exhibited a cell capacitance of 0.55 Fcm<sup>-2</sup> at 0.05 mAcm<sup>-2</sup>. Furthermore, the MnO<sub>x</sub>/C-MEMS electrodes exhibited a maximal stack power density of 28.3 mWcm<sup>-3</sup> and a maximal stack energy density of 0.51 mWhcm<sup>-3</sup>. The PPy integrated C-MEMS microsupercapacitors, on the other hand, exhibited a specific capacitance of 162.07  $\pm$  12.40 mF cm<sup>-2</sup> at 20 mV s<sup>-1</sup>, in addition to a power density of 1.62  $\pm$  0.12 mW cm<sup>-2</sup> computed for the same scan rate.

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#### **3. METHODOLOGY**

#### 3.1 Introduction

This section provides the details of the methodology adopted for this thesis – for both the scale-up capacitors as well as the miniaturized versions. For the scale-up systems designed and evaluated in this dissertation, two techniques were used to design the electrodes – i) *electrostatic spray deposition (ESD)* and ii) *slurry casting*. The former method provides the benefit of creating thin-films of different materials without the use of a binder, whereas the latter typically requires a binder and is pertinent for creating bulk electrodes with more massive active material loading. For the miniaturized systems, two designs were explored -i) three-dimensional carbon micro-pillar arrays patterned on carbon current collector; and ii) interdigitated gold micro-current collectors. The 3D carbon micro-pillar arrays were created using carbon microelectromechanical systems (C-MEMS), whereas the interdigitated gold current collectors were created using traditional photolithography and lift-off methods. In order to incorporate the active material onto the carbon micro-platforms, ESD was used, whereas *electrophoretic* and *electrochemical deposition* methods were used to selectively deposit active material films onto the interdigitated current collectors.

## 3.2 Electrostatic Spray Deposition

Electrostatic Spray Deposition, abbreviated as ESD, was first developed by Schoonman and coworkers at Delft University of Technology [1]. ESD is a low energy electrohydrodynamic spraying technique in which a precursor solution disintegrates into an aerosol spray upon the application of a high voltage between a metal nozzle and a substrate [2-5]. The desired precursor solution is fed through a syringe pump via a nozzle

connected to a high potential source, whereas the substrate is grounded [2] (Schematic shown in Figure 3.1). The aerosol formed by the charged droplets is attracted to the heated substrate leading to simultaneous solvent evaporation and chemical reactions, leaving behind a thin film [4, 5]. The advantages of ESD over other thin film production methods include the feasibility of operation in ambient atmosphere at desired temperatures without the need of vacuum, which makes it both cost-effective and facile in terms of operation [3]. Both polycrystalline phases as well as composite materials can be synthesized via ESD by adjusting parameters such as the applied potential, substrate temperature, substrate-nozzle distance, nozzle geometry, precursor solution flow rate and composition [4-6]. One of the very attractive features of ESD is the ability to tailor the morphology of the film by fine tuning the deposition parameters. A host of morphologies have been reported using ESD including dense, fractal, reticular, sponge-like, and porous [4, 5]. The feasibility of creating high-surface area porous and homogeneous synthetic films makes ESD especially suitable for energy-storage applications. Several works have documented the use of ESD based films for energy storage systems including lithium-ion batteries, electrochemical capacitors, and miniaturized electrochemical energy storage systems [4, 5, 7-9].



Figure 3.1: Schematic illustration of the ESD process (left); digital photograph of ESD lab setup.

## 3.3 Carbon Microelectromechanical Systems (C-MEMS)

Carbon microelectromechanical systems, also referred to as carbon-MEMS or C-MEMS is a term used for a set of fabrication methods used to *convert a patterned photosensitive polymers to glassy carbonaceous using pyrolysis* [9-14]. The typical C-MEMS fabrication process has been illustrated in Figure 3.2a. For the studies carried out for this dissertation, the C-MEMS-based 3D micro-pillars were prepared by a two-step photolithography process followed by a pyrolysis step. Detailed experimental procedure can be found in Chapter 5. Figures 3.2b and 3.2c illustrate typical SEM image of the C-MEMS based micro-pillar arrays and a digital image of the micro-device, respectively.



Figure 3.2: Schematic illustration of the C-MEMS process (Adapted from [14]); b) SEM micrograph of carbon micro-pillar arrays; c) Photograph of a device containing micro-pillars on carbon current collectors and contact pads.

# 3.4 Gold microelectrode fabrication

For this dissertation, in order to construct the interdigital gold micro-current collectors, traditional photolithography and lift-off methods were used. A schematic illustration has been shown in Figure 3.4. First, AZ 5214 was spun-coated on a 4" Si/SiO<sub>2</sub> (100) wafer at a speed of 5000 rpm for 30 seconds. After the spin coating process, a soft bake was carried out for 1 minute at a temperature of 110°C on a leveled hot plate. After the bake process, ultraviolet exposure was carried out using an OAI mask aligner with a UV dose of 230 mJcm<sup>-2</sup>. Following the expose step, developing was carried out using AZ 300 MIF for ~45 seconds. After the developing a descum step was carried out using an

 $O_2$  plasma at a flow rate of 60 sccm and a pressure of 400 mTorr for 30 seconds using an reactive ion etching (RIE). Following the patterning of the photoresist, metallization process with Ti/Au (20/300 nm) was carried out using e-beam evaporation using a CHA evaporator. After the metallization process, lift-off was carried out using acetone and mechanical agitation followed by isopropyl alcohol rinsing and N<sub>2</sub> drying. Finally, a 30s  $O_2$  plasma treatment at 400 mTorr was carried out in order to functionalize the gold electrodes for better active material adhesion.



Figure 3.3: Schematic illustration of the gold microelectrode fabrication.

## 3.5 Electrophoretic deposition

In order to incorporate reduced graphene oxide (rGO) onto gold microelectrodes, electrophoretic deposition (EPD) was used for this dissertation. EPD is an attractive thinfilm synthesis technique, in which essentially charged particles move under the effect of

an electric field in liquid media. The ease of tailoring the processing parameters in order to adjust the chemical and morphological conditions of the deposit is what makes EPD so versatile. EPD has been widely used in order to synthesize graphene-related materials. In its simplest form, the EPD process requires the application of an electric potential between two electrodes in a particle-suspension. The eventual collection of the particles moving under the influence of an electric field, results in the formation of a deposit. The advantages of EPD include cost effectiveness, simplicity, uniformity of the deposit, controllable deposition, predictability of deposition kinetics, and the possibility of sequential and co-deposition of different particles [15]. However, the limitations of EPD include i) the need for a stable suspension with sufficient particle surface charge; ii) the need for using electrically conducting substrates; iii) the possibility of side reactions; and iv) limited film thicknesses. Figure 3.6a illustrates a schematic description of the EPD process utilized for the purpose of this dissertation. The working electrode was the bare interdigitated gold micro-current collector whereas the counter was a platinum foil and the two electrodes were connected to dc power supply. The suspension comprised graphene oxide (GO) powder in a solution containing  $C_2H_5OH$  and deionized water (90:10 v:v). Figure 3.6b shows the microstructure of the EPD based rGO film. Further characterization details on the films are explained in Chapter 7.



Figure 3.4: a) Schematic illustration of the EPD setup used to deposit rGO films for this dissertation; b) top view of the EPD based rGO films

## 3.6 Electrochemical deposition of manganese oxide

Electrochemical deposition is a popular technique to deposit thin films of metal oxides without the use of binders. The relative simplicity, the low energy consumption, and the ability to control morphology by fine tuning the deposition parameters make electrodeposition very appealing to synthesize binder-free thin films. Different modes of electrodeposition include: i) potentiodynamic (*cyclic voltammetry* (*CV*)); ii) potentiostatic (*chronoamperometry* (*CA*)) and iii) galvanostatic (*chronopotentiometry* (*CP*)) [16]. For the purpose of this dissertation, anodic chronopotentiometry was applied. Figure 3.7a and Figure 3.7b illustrate the schematic setup used for the synthesis of the manganese oxide (MnO<sub>x</sub>) films, and the resultant microstructure, respectively. The microstructure comprised manganese oxide nanorods; detailed material investigation is presented in Chapter 7.



Figure 3.5: a) Schematic illustration of the electrochemical deposition setup used to deposit MnO<sub>x</sub> films; b) microstructure of the MnO<sub>x</sub> nanoparticles

# 3.7 Material Characterization

The techniques used for characterization of the materials used in this dissertation are described in this section:

## **3.7.1** X-Ray Diffraction (XRD)

XRD is an analytical technique that can provide information about the crystallinity and crystallographic orientations (*hkl*) of a material. Bragg's law ( $n\lambda = 2dsin\theta$ ) describes the relationship between interplanar spacing d, scattering angle  $\theta$  and wavelength  $\lambda$ . All the XRD measurements of the materials used in this dissertation were recorded using a Siemens D-5000 diffractometer with Cu Ka radiation ( $\lambda$ =0.154056 nm). The patterns were identified using the "Joint Committee on Powder Diffraction Standards - International Center for Diffraction Data (JCPDS-ICDD)" database.

### 3.7.2 Scanning Electron Microscopy (SEM)

In order to investigate the microstructure of the materials synthesized, a field emission-scanning electron microscope (JEOL 6335FE-SEM, Peabody, MA, USA) was used; the accelerating voltages for imaging were generally kept between 10-20 kV for typical working distances between 15-39 mm.

# 3.7.3 Transmission Electron Microscopy (TEM)

The TEM images were taken by using a Philips CM-200 FEG TEM operating at 200 kV. Selected area electron diffraction (SAED) analyses were performed in order to study the sample crystallinity.

# 3.7.4 Fourier Transform Infrared (FT-IR) Spectroscopy

Spectroscopic studies on the samples were carried out using a JASCO FTIR-4100 equipped with an attenuated total reflectance (ATR) accessory between wavenumbers of 4000 and 500 cm<sup>-1</sup> at room temperature.

### 3.8 Electrode Preparation and Cell Assembly

## 3.8.1 Electrodes Prepared via Casting

Casting is a general process that has been widely used in both laboratory and industrial scales. For this dissertation, first a slurry comprising the active material, binder (PVDF) and conducting additive (Super P Li<sup>®</sup>) was prepared in the ratio of 80:10:10 (in that order) in NMP solvent and thereafter casted onto stainless steel substrates. The electrodes were dried thoroughly (80°C for 24 h) before being used for final cell assembly.

### 3.8.2 Electrodes Prepared via ESD

Most of the electrodes deposited by ESD were used directly as working electrodes without the use of any additional binders or conducting agents in either half or full cell assembly (Please refer to Chapters 4, 5 and 6 for more experimental details).

### 3.8.3 Electrochemical Cell Assembly

The electrochemical test cells for this dissertation were tested in both coin-cell and beaker setups. For coin cell assembly, CR-2032 type coin cells were utilized; the ESD based or the casted electrode was used as the working electrode against the respective counter electrode (lithium, activated carbon, nanostructured carbon); Celgard 2400 microporous polypropylene film was used as the separator. Two electrolytes were used: 1 M LiPF<sub>6</sub> dissolved in carbonate solvents (nonaqueous) and 1M Na<sub>2</sub>SO<sub>4</sub> (aqueous). A nickel foam spacer was used for coin-cell assembly to ensure good electrical contact.

### 3.9 Electrochemical Characterization

### 3.9.1 Cyclic Voltammetry (CV)

Cyclic voltammetry is a type potentiodynamic electrochemical technique which is used to investigate the reversibility of different electrochemical reactions. In a typical CV experiment, the working electrode potential is ramped linearly vs. time at a certain scan rate (mV s<sup>-1</sup>). The data are plotted as current vs. voltage. For this dissertation, the CV tests were performed using a Bio-logic versatile multichannel potentiostat (VMP3, Bio logic). Detailed experimental details can be found in the respective research chapter.

## **3.9.2** Galvanostatic Charge-discharge (GCD)

GCD characterization is crucial to study the electrochemical reactions, cycling stability and rate capability of an electrochemical cell. Potential vs. time (or capacity) plot is used to review the electrochemical reactions during constant current charge/discharge by examining the plateau position (vs. potential). In order to study the rate response of a cell, GCD cycling is carried out at different currents. All the electrochemical cells were galvanostatically cycled at room temperature using BiologicVMP3 Potentiostat and NEWARE BTS-610 Battery Test System.

# **3.9.3** Electrochemical Impedance Spectroscopy (EIS)

Electrochemical impedance spectroscopy (EIS) is a perturbative characterization of the dynamics of an electrochemical reaction, which records the response of an electrochemical cell to an applied potential or current. For this dissertation, EIS studies were performed using a Bio-logic versatile multichannel potentiostat (VMP3, Bio logic). Typically an AC oscillation of 10 mV amplitude was applied over the frequencies from 100 kHz to 10 mHz; the data were fitted using Z-fit function in EC-Lab (V10.40) software using relevant Randles circuits.

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# 4. A HIGH ENERGY 3V LITHIUM-ION CAPACITOR SYNTHESIZED VIA ELECTROSTATIC SPRAY DEPOSITION

#### 4.1 Introduction

In order to keep up with the demands of the ever evolving technology and the automotive industry, developing high performing energy storage devices is extremely crucial. At the heart of electrochemical energy storage devices are electrochemical capacitors, which essentially bridge the gap between electrolytic capacitors and secondary batteries with high gravimetric power densities (~ 10kWkg<sup>-1</sup>) and moderate energy densities (< 10 Whkg<sup>-1</sup>). However, in order to expand the applicability of ECs, one of the critical factors that requires immediate attention is their relatively low energy density. In the wake of addressing this shortcoming of ECs, the concept of lithium ion battery (LIB) and EC hybridization has gained significant scientific attention in recent years. In practice, battery and capacitor hybridization can be achieved at both external and internal levels. As noted by Cericola et al [1], external hybridization involves hardwiring of the two devices in either serial or parallel arrangement, whereas internal hybridization in essence is *hybridization within the device itself*. Similar to the external setup, internal hybridization can be carried out in both serial and parallel arrangements. The internal serial configuration comprises a pristine redox battery-type electrode along with a counter double layer capacitive cathode; whereas the internal parallel arrangement consists of bi-material electrodes, in which both redox and double layer materials coexist within one electrode. One of the first reports on nonaqueous internal hybrids was documented by Amatucci et al in 2001 [2], where they used Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> as the negative lithium intercalating electrode and activated carbon as the double layer electrode; the

reported device was able to deliver a gravimetric energy density of 25Whkg<sup>-1</sup>. Since then many other systems with lithium-intercalating materials including graphite [3, 4], Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> [5, 6], LiFePO<sub>4</sub> [7], LiMn<sub>2</sub>O<sub>4</sub> [8], TiO<sub>2</sub> [9-11], and double layer materials including activated carbon [2, 5, 6], and graphene [8, 12] have been investigated.

Graphene, the one-atom thick sheet of  $sp^2$  hybridized carbon atoms is considered ideal for double layer capacitive charge storage owing to its high theoretical specific surface area ( $\sim 2600 \text{ m}^2/\text{g}$ ), exceptional electronic conductivity and superior mechanical strength [13]. However, one of the major shortcomings of graphene is sheet aggregation and restacking, which significantly reduces the effective accessible surface area for the electrolyte ions, which ultimately deteriorates the cell performance. One of the strategies to minimize the graphene sheet restacking is the addition of "nanospacers" such as CNT [14, 15]. Incorporating CNT into the graphene matrix not only allows for a larger accessible surface area but also enhances the electrical conductivity. Furthermore, the addition of CNT nanofillers has shown improvement in the mechanical robustness of different composites [16]. From our previous studies [14], microsupercapacitors fabricated with reduced graphene oxide-carbon nanotube (rGO-CNT) composites with a gravimetric composition of 90% rGO and 10% CNT exhibited exceptional power handling with a RC time constant of only 4.8 ms. The further addition of CNT enhanced the power handling but exhibited a negative impact on the specific capacitance of the device [14]. Therefore rGO-CNT composite electrodes with the same composition were chosen for the lithium hybrid electrochemical capacitor (Li-HEC) fabrication for this study. To couple the rGO-CNT electrode, an anatase TiO<sub>2</sub>-Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> (ATO-LTO) anode was chosen. TiO<sub>2</sub> (TO) with a maximum theoretical capacity of 335 mAhg<sup>-1</sup> (for x=1 for
LixTiO<sub>2</sub>) [17], is a competitive alternative to graphite-based anodes, which exhibit a theoretical capacity of 372 mAhg<sup>-1</sup>. One of the disadvantages of graphite is the low lithium intercalation potential (~0.1V vs Li/Li<sup>+</sup>). Such low operating potentials are very close to lithium plating and can promote dendritic lithium growth, which can result in catastrophic cell short-circuiting. Both TO and LTO intercalate lithium at much higher potentials ~1.4-1.8V [17] and ~1.55V vs. Li/Li<sup>+</sup> [18], respectively, which are much higher than graphite operating potential. Among the three most sought after TO polymorphs including anatase, bronze and rutile, anatase is considered an ideal host for lithium-ion storage given the highly distorted edge-sharing TiO<sub>2</sub> octahedra arrangement, which facilitates lithium insertion and extraction [19, 20]. Furthermore the very low volumetric strain (~4%) in ATO lattice during cycling is ideal for cycle longevity [20]. Furthermore, titania has superior electrical conductivity and lithium diffusivity than LTO [21, 22] and faster lithium insertion/extraction can help realize higher rate batteries than LTO alone. In other reports, TO-LTO composites have shown enhancement in lithium diffusion, improved charge-transfer kinetics along with better electronic conductivity [23].

The electrodes used for the Li-HEC construction for this study were created via electrostatic spray deposition (ESD) technique. The ESD process is a low energy electrohydrodynamic spraying technique in which a precursor solution disintegrates into an aerosol spray upon the application of a high voltage between a metal nozzle and a substrate [24-27]. The desired precursor solution is fed through a syringe pump via a nozzle connected to a high potential source, whereas the substrate is grounded [24]. The aerosol formed by the charged droplets is attracted to the heated substrate leading to

simultaneous solvent evaporation and chemical reactions, leaving behind a thin film [26, 27]. The advantages of ESD over other thin film production methods include the feasibility of operation in ambient atmosphere at desired temperatures without the need of vacuum, which makes it both cost-effective and facile in terms of operation [25]. Both polycrystalline phases as well as composite materials can be synthesized via ESD by adjusting parameters such as the applied potential, substrate temperature, substrate-nozzle distance, nozzle geometry, precursor solution flow rate and composition [26-28]. One of the very attractive features of ESD is the ability to tailor the morphology of the film by fine tuning the deposition parameters. A host of morphologies have been reported using ESD including dense, fractal, reticular, sponge-like, and porous [26, 27]. The feasibility of creating high-surface area porous and homogeneous synthetic films makes ESD especially suitable for energy-storage applications. Several works have documented the use of ESD based films for energy storage systems including both lithium-ion batteries and electrochemical capacitors [26, 27, 29-30]. The ESD based rGO-CNT and the ATO-LTO electrodes, synthesized in this work were able to deliver discharge capacities of  $\sim 63$ mAhg<sup>-1</sup> and 95 mAhg<sup>-1</sup>, respectively at a current density of 0.1Ag<sup>-1</sup> with good reversibility. The Li-HEC cells constructed with the rGO-CNT and ATO-LTO electrodes were stable for a cell potential of 0.05-3.0V and were able to deliver a high discharge capacity of  $\sim$ 32 mAhg<sup>-1</sup> at a current rate of 0.1 Ag<sup>-1</sup> with excellent rate characteristics and reversibility. Furthermore, the hybrid electrochemical cells were able to deliver a maximum gravimetric energy density of 33.35 Whkg<sup>-1</sup> and a maximum power density of 1207.4 Wkg<sup>-1</sup>, with specific energy ranging between 33.35-15.09 Whkg<sup>-1</sup> at power densities of 83.55-1207.4 Wkg<sup>-1</sup>. All the cell parameters were normalized with the total

anode and cathode active material masses. Additionally, the Li-HEC cells were able to retain a capacity of ~77% after 100 cycles. Therefore, the use of a simple and cost-effective process such as ESD was demonstrated in order to construct high energy Li-HECs with good power handling capability.

### 4.2 **Experimental Details**

# 4.2.1 Material Synthesis

## 4.2.1.1 Cathode Preparation

For the rGO-CNT cathode, the raw materials were single layer graphene oxide (GO) and carboxyl-functionalized multi-walled carbon nanotubes (MWCNT-COOH). Both the materials were procured from Cheap Tubes Inc. (USA). GO and CNT were first dissolved in 1, 2-propanediol (Sigma Aldrich) in a concentration of 1 mgml<sup>-1</sup> and were then ultrasonicated for thorough dispersion for 1h. After sonication, the suspension was used immediately for ESD on stainless steel substrates preheated at 250°C. The GO and CNT were used in a gravimetric mass ratio of 9:1, which was selected based on the optimum composition based on our previous works [14]. The flow rate was kept between 4-6 mlhr<sup>-1</sup> at a potential of 5-7 kV and the deposition was carried out for 4 hours. The electrodes were then directly used for material and electrochemical characterization without adding any binders or conducting additives.

## 4.2.1.2 Anode Preparation

The ATO-LTO anodes were prepared using lithium acetate (Sigma Aldrich) and titanium butoxide (Sigma Aldrich) in a molar ratio of 4:5, respectively in ethyl alcohol and butyl carbitol (4:1 v:v). The solution was directly used as the precursor and deposited

on a preheated nickel foam substrate using ESD. The substrate was preheated at 250°C and the precursor solution flow rate was kept between 1-2 mlhr<sup>-1</sup>. The potential was kept between 5-7 kV and the distance between the needle and the substrate was approximately 3 cm. The deposition was carried out for 2 h. Post ESD deposition, the substrates with ESD films were calcined in an argon atmosphere in a Lindberg alumina tube furnace at a temperature of 750°C for 2 h. After the calcination process, the films were allowed to cool down to room temperature and thereafter were directly used for electrochemical characterization without any further treatment or addition of binders or conducting additives.

## 4.2.2 Material Characterization

The crystallinity of the as-deposited and calcined anode powders was studied using a Siemens 5000D X-ray Diffractometer with Cu K $\alpha$  radiation. Further crystallographic studies on the anode powders calcined at 750°C were carried out using a Philips CM-200 200KeV Transmission Electron Microscope (TEM). The morphology of the as-deposited and calcined anode films and the rGO-CNT cathode films was characterized using a JEOL SEM 6330F Field Emission Scanning Electron Microscope (FE-SEM) in the secondary electron imaging (SEI) mode. To characterize GO functionalization and reduction, Fourier transform-infrared spectroscopy (FT-IR) was carried out using a JASCO FT-IR 4100 spectrometer.

## 4.2.3 Electrochemical characterization

The electrochemical characterization was carried out in CR-2032 type coin cells. In order to characterize the electrode performance versus Li/Li<sup>+</sup>, the rGO-CNT and the

ATO-LTO electrodes were first assembled in half-cells as working electrodes with a lithium foil serving both as the counter and reference electrode. 1.0M lithium hexafluorophosphate (LiPF<sub>6</sub>) in ethylene carbon (EC): diethyl carbonate (DEC) in a volume ratio of 1:1 was used as the electrolyte, and a Celgard 2400 polypropylene (Charlotte, NC, USA) film was used as the separator. The cells were assembled in an argon-filled glove box (VAC Nexus I, Hawthorne, CA, USA) with  $O_2$  level < 1ppm. Cyclic voltammetry (CV) studies on both rGO-CNT and ATO-LTO electrodes were carried out using a Bio-logic versatile multichannel potentiostat (VMP3) whereas galvanostatic charge-discharge cycling, rate performance and cycle life testing were carried out using a NEWARE BTS-610 Battery Test System (Shenzhen, China). The full hybrid cells comprising the rGO-CNT cathode and ATO-LTO anode were assembled after prelithiating the ATO-LTO anode for 5 cycles and after obtaining the activation of the rGO-CNT electrode for ~100 cycles. For the full cell systems the electrolyte was 1.0M lithium hexafluorophosphate (LiPF<sub>6</sub>) in ethylene carbon (EC): diethyl carbonate (DEC) in a volume ratio of 1:1, with a Celgard 2400 propylene film separator. Similar to the half-cell assembly, the full cell assembly was carried out in CR-2032 type coin cells.

### 4.3 **Results and Discussion**

#### 4.3.1 Material Characterization

The XRD patterns of the as-deposited and anode powders calcined at 750°C are shown in Figure 4.1a. As evident, the as-deposited powder exhibits no discernable peaks whereas the diffraction data from the calcined powder validates the presence of both LTO and anatase TiO<sub>2</sub> phase. The peaks at  $18.3^{\circ}$ ,  $35.5^{\circ}$ ,  $43.2^{\circ}$ ,  $57.2^{\circ}$  and  $62.8^{\circ}$  correspond to (111), (311), (400), (333) and (440) planes from LTO (JCPDS card number 00-049-0207)

whereas the peak at  $53.8^{\circ}$  corresponds to (105) plane from anatase TiO<sub>2</sub> (JCPDS card number 00-021-1272). The FTIR pattern of the GO powder and the ESD based rGO film is depicted in Figure 4.1b. The broad absorption peak centered around 3378 cm<sup>-1</sup> in the GO powder, which signals the presence of hydroxyl groups [14, 31] and water is substantially reduced in the rGO pattern. The other significant peaks present in the GO powder are signaled at 1727 cm<sup>-1</sup>, 1624 cm<sup>-1</sup>, 1373 cm<sup>-1</sup>, 1226 cm<sup>-1</sup>, and 1083 cm<sup>-1</sup> are attributed to C=O stretching [31], aromatic C=C stretching [32], carboxyl [33], epoxide C-O-C or phenolic C-O-H stretching vibrations [33], C-O stretching in epoxy or alkoxy groups [33], respectively. It is worth noting that the peak intensity from the groups that signal the presence of oxygen and water are substantially mitigated in the rGO spectrum. Figure 4.2a and 4.2b display the SEM images of the as deposited ESD and calcined ATO-LTO films, respectively. Prior to the thermal treatment, the film particles are mostly flaky, whereas upon the calcination, the particles become more circular with no appreciable change in size. The TEM micrograph of the ATO-LTO powder is shown in Figure 4.2c and the SAED pattern is shown as the inset. The TEM studies confirmed the presence of both anatase  $TiO_2$  and LTO. The anatase- $TiO_2$  phase with a d-spacing of 3.50 Å, 2.23 Å, 1.86 Å, 1.54 Å, and 1.19 Å had (hkl) orientations of (101), (112), (200), (213), and (008), respectively, whereas the LTO with d-spacings of 1.25 Å, 1.19 Å, and 1.09 Å and (hkl) orientation of (622), (444), and (731), respectively. The top view of the rGO-CNT electrode is shown in Figure 4.2d. As evident, the electrode morphology was porous and loose; porous morphology is ideal for double-layer charge storage mechanism and allows for high rate capability realization.



Figure 4.1: (a) The XRD pattern of the as-deposited and calcined anode powders, (b) The FTIR pattern of the GO and ESD based rGO.



Figure 4.2: Morphology of the as-deposited (a) and calcined (b) ATO-LTO films, (c) typical TEM micrograph of the calcined ATO-LTO powder, the inset shows the SAED pattern, (d) Top view of the rGO-CNT cathode



Figure 4.3: (a) Cyclic voltammograms of the rGO-CNT composite electrode for different scan rates between a potential of 2.0-4.0V (vs. Li/Li<sup>+</sup>), (b) discharge capacity of the rGO-CNT composite for the first ~90 cycles at a current density of 0.1Ag<sup>-1</sup>, (c) typical charge-discharge curves of the rGO-CNT electrode at different current densities, (d) rate capability of the rGO-CNT composites.

# 4.3.2 Electrochemical Characterization

# 4.3.2.1 rGO-CNT half-cell

The cyclic voltammograms at different scan rates of the rGO-CNT composite electrode are shown in Figure 4.3a. The shape of the curves is typical of a double layer capacitor with no discernable redox peaks. A very interesting phenomenon was observed in Figure 4.3b; the discharge capacity of the rGO-CNT cathode steadily increased until around the first 60 cycles and then stabilized. The capacity enhancement could be a result of electrochemical activation of the active material and has been reported for graphene based devices in other reports [14, 34]. Figure 4.3c shows the galvanostatic charge-discharge curves of the rGO-CNT composite after the electrochemical activation. The curves are mostly triangular in shape as expected for surface charge storage mechanism. The iR drops however were quite significant at higher current densities, which could be a result of the relatively high resistivity of the composite resulting from the remnant oxygen-containing groups present in the rGO. Figure 4.3d shows the rate capability of the rGO-CNT composite. The capacity is stable as noted for a step size of 20 cycles for each current rate and almost all of the capacity is recovered when the cell was cycled from 3.2 Ag<sup>-1</sup> to 0.1 Ag<sup>-1</sup>. Discharge capacities of ca. 63 mAhg<sup>-1</sup>, 55 mAhg<sup>-1</sup>, 50 mAhg<sup>-1</sup>, 43 mAhg<sup>-1</sup>, 32 mAhg<sup>-1</sup>, and 18 mAhg<sup>-1</sup> are noted for current rates of 0.1 Ag<sup>-1</sup>, 0.2 Ag<sup>-1</sup>, 0.4 Ag<sup>-1</sup>, 0.8 Ag<sup>-1</sup>, 1.6 Ag<sup>-1</sup>, and 3.2 Ag<sup>-1</sup> respectively. The discharge capacities are reported from the last cycle of the respective current rate.



Figure 4.4: (a) Cyclic voltammograms of the ATO-LTO composite electrode at a scan rate of 0.2mVs<sup>-1</sup> for the first five cycles, (b) cyclic voltammograms of the ATO-LTO composite at different scan rates ranging from 0.2 mVs<sup>-1</sup> to 5 mVs<sup>-1</sup>; the inset shows the dependence of the anodic peak current on the square root of the scan rate, (c) typical charge-discharge curves of the ATO-LTO composite electrode for the first two cycles at a current density of 0.1 Ag<sup>-1</sup>, (d) rate capability of the ATO-LTO composite anodes.

# 4.3.2.2 ATO-LTO half cell

The CV curves of the ATO-LTO composite electrodes for the first five cycles at a scan rate of  $0.2 \text{ mVs}^{-1}$  are shown in Figure 4.4a. In the first cycle, in the cathodic branch of the scan, two peaks were observed at 1.62V vs. Li/Li<sup>+</sup> and 0.7V vs. Li/Li<sup>+</sup>, whereas in the anodic branch one major peak at 2.21V vs. Li/Li<sup>+</sup> was observed. The peak at 0.7V disappeared in the subsequent cycles and is ascribed to the possible solid electrolyte

interphase (SEI) formation. The redox peak pair appearing at 1.62V and 2.21V is attributed to the lithium insertion and extraction in ATO. The CV of the ATO-LTO composite at different scan rates is shown in Figure 4.4b. As evident the peaks shifted upon the application of a higher scan rate. The inset depicts the relationship between the square root of the scan rate and the respective anodic peak current and a linear correlation between the two parameters is established. This indicates the predominance of redox based reactions for the anode based on the Randles-Sevcik equation [35]. It should be noted that no discernable activity of LTO is detected in the CV curves, which indicates that ATO is the primarily active electrochemical phase in the composite. The possible reason for no noticeable LTO electrochemical activity could be the competitive crystal growth during the calcination process, which could have resulted in trace LTO amounts. Similar phenomenon, where one of the phases is predominantly electrochemically active in the composite, has been reported in other works [36, 37]. Figure 4.4c shows the charge discharge curves of the first and second cycles of the ATO-LTO composite at a current density of 0.1 Ag<sup>-1</sup>. Two humps centered at 1.62V and 2.21V are observed which are consistent with the CV ATO insertion/extraction redox pair. It should be noted that the first discharge capacity of the composite is  $\sim 267 \text{ mAhg}^{-1}$  whereas the first charge capacity is  $\sim 127$  mAhg<sup>-1</sup> which results in a coulombic efficiency of  $\sim 47\%$  resulting in an irreversible capacity loss of 140 mAhg<sup>-1</sup>, which possibly is a result of the SEI formation. In the second cycle however, the discharge capacity is  $\sim 124$  mAhg<sup>-1</sup> and the charge capacity is 110.5 mAhg<sup>-1</sup> which results in a much improved coulombic efficiency of ~89%. Figure 4.4d shows the rate capability of the ATO-LTO composite anode at different rates for a cycle step of 20 cycles. Discharge capacities of ca. 88 mAhg<sup>-1</sup>, 77

mAhg<sup>-1</sup>, 68 mAhg<sup>-1</sup>, 57 mAhg<sup>-1</sup>, 44 mAhg<sup>-1</sup>, and 31 mAhg<sup>-1</sup>, were noted at the last cycle for current rates of 0.1 Ag<sup>-1</sup>, 0.2 Ag<sup>-1</sup>, 0.4 Ag<sup>-1</sup>, 0.8 Ag<sup>-1</sup>, and 1.6Ag<sup>-1</sup>, respectively. Furthermore, the composite exhibited good reversibility since all of the capacity was restored after the cell was cycled back from a high current rate of 3.2 Ag<sup>-1</sup> to a low current rate of 0.1 Ag<sup>-1</sup>.

# 4.3.2.3 Li-HEC cell

The Li-HEC cell performance is depicted in Figure 4.5. The cells were constructed after prelithiating the anode to a potential of 0.05V vs Li/Li<sup>+</sup> at a very low current rate of 0.05 Ag<sup>-1</sup>. As noted by Zheng [38], organic electrolytes have relatively lower salt concentration as opposed to aqueous electrolytes and therefore the energy of the hybrid device can be limited by the electrolyte when a lithium intercalating anode is used. As the cell charges, the lithium ions are consumed at the negative electrode whereas the anions are adsorbed at the cathode. If the electrolyte were depleted of ions, the device cannot be charged further and as a solution, they proposed the utilization of a prelithiated anode, which could compensate for the electrolyte ion depletion [39]. The rGO-CNT electrodes, on the other hand were used for Li-HEC construction after full electrochemical activation, i.e. after ~100 cycles. As was noted in Figure 4.3b, the discharge capacity of the rGO-CNT electrode increased steadily for the first ~60 cycles and then stabilized. Allowing the rGO-CNT electrode to activate before Li-HEC assembly ensured higher capacity utilization from the cathode. As noted in Figure 4.5a, the shape of the CV curves of the Li-HECs is typical of capacitive behavior with a slight deviation, which could be a result of the composite charge storage characteristics arising

from the predominantly redox-diffusion controlled lithium storage in the anode as opposed to the surface-dominated double layer charge adsorption in the cathode. The galvanostatic charge-discharge curves of the Li-HEC, displayed as Figure 4.5b, are mostly triangular for a cell potential between a cell potential of 0.01-3.0V also indicative of capacitive behavior. The rate capability of the Li-HEC cell is shown in Figure 4.5c the full cell was able to deliver discharge capacities of 32.29 mAhg<sup>-1</sup>, 27.70 mAhg<sup>-1</sup>, 22.82 mAhg<sup>-1</sup>, 17.45 mAhg<sup>-1</sup>, and 12.27 mAhg<sup>-1</sup> for current rates of 72.5 mAg<sup>-1</sup>, 145 mAg<sup>-1</sup>, 290 mAg<sup>-1</sup>, 580 mAg<sup>-1</sup>, and 1160 mAg<sup>-1</sup>, respectively. Moreover, the cell performance was very stable for a cycle step of 10 for the given current rate and all of the cell capacity is recovered after cycling from a high current rate of 1160 mAg<sup>-1</sup> to 72.5 mAg<sup>-1</sup>, which is indicative of good rate capability and reversibility of the full cell. Figure 4.5d shows the capacitive retention of the Li-HEC full after 100 cycles; the cell was able to retain ~77% of the initial capacitance. The Figure 4.6 shows the Ragone chart of the Li-HEC cell based on discharge characteristics. The hybrid capacitor was able to deliver a maximum energy density of 33.35 Whkg<sup>-1</sup> and a maximum power density of 1207.4 Wkg<sup>-1</sup>. All the cell parameters were normalized with the total anode and cathode active material masses. The range for the energy density was between 33.35-15.09 Whkg<sup>-1</sup> at power densities of 83.55-1207.4 Wkg<sup>-1</sup>. The energy-power characteristics of the Li-HEC cells are superior to aqueous hybrid systems including RuO<sub>2</sub>-TiO<sub>2</sub>//AC [40], LiTi<sub>2</sub>(PO<sub>4</sub>)<sub>3</sub>//AC [41] configurations, as well as comparable or even better than nonaqueous hybrid systems comprising modified LTO [42-44]. Table 4.1 summarizes the electrochemical performance of this work along with some of the other hybrid capacitors reported in other reports .The superior energy-power characteristics are attributed to the

utilization of an organic electrolyte, which allows for a wider stable electrochemical potential window (0.05-3V) and the porous morphology of the ESD generated rGO-CNT cathode, which is ideal for high power handling applications. It should be noted that this work combined a pristine lithium-intercalation based anode with a double layer counter cathode, categorically a "serial" system. Enhancement in energy-power characteristics is expected with the utilization of a "parallel" system. The combination of a redox based material and a double layer material within one electrode allows for intrinsic potential matching as the materials used have to be stable for the same voltage window [1]. Furthermore, the internal parallel system mitigates the capacity mismatch arising from the disparate charge storage mechanism of the redox and double layer materials, and therefore helps in higher material utilization rate. In addition, improving the ionic and electronic conductivity of the electrodes is expected to further improve the Li-HEC performance. This work is still in nascent phase and as mentioned, much enhancement is expected with the use of an ESD based parallel system, which is a subject of future works.



Figure 4.5: (a) Cyclic voltammograms of the Li-HEC at different scan rates ranging from 2-20 mVs<sup>-1</sup>, (b) typical charge-discharge curves of the Li-HEC cells at different current densities, (c) rate capability, and (d) cyclability of the Li-HEC full cells.

Positive electrode	Negative electrode	Electrolyte	Cell Voltage (V)	Capacitance (Fg <sup>-1</sup> )	Capacity (mAhg <sup>-1</sup> )	Energy-power characteristics	Ref.
RuO <sub>2</sub> /TiO <sub>2</sub>	AC	1M KOH (aqueous)	0-1.4V	46 Fg <sup>-1</sup> at 130 mAcm <sup>-2</sup>	-	12.5 Whkg <sup>-1</sup> at a power density of 150Wkg <sup>-1</sup> 5.7 Wkg <sup>-1</sup> at a power density of 1207 Wkg <sup>-1</sup>	40
AC	Carbon- coated LiTi <sub>2</sub> (PO <sub>4</sub> ) <sub>3</sub>	1M Li <sub>2</sub> SO <sub>4</sub> (aqueous)	0.3 to 1.5 V	-	$30 \text{ mAhg}^{-1} \text{ at } 2 \text{ mAcm}^{-2}$	24 Wh kg <sup>-1</sup> at a power density of about 200 W kg <sup>-1</sup>	41

 Table 4.1: Comparison of the ESD based Li-HEC with other hybrid electrochemical capacitors.

						15 Wh kg <sup>-1</sup> at a power density of 1000 W kg <sup>-1</sup>	
AC	Graphene sheets wrapped nano- Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1 M LiPF <sub>6</sub> /EC/ DMC (nonaqueous)	1.5–3.0 V			29.2 Wh kg <sup>-1</sup> at a power density of 58.4 W kg <sup>-1</sup> 1782.7 W kg <sup>-1</sup> , the specific energy retains 13.4 Wh kg <sup>-1</sup>	42
AC	Carbon coated Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1M LiPF <sub>6</sub> in propylene carbonate (nonaqueous)	1.5- 2.5V		$\sim 30$ mAhg <sup>-1</sup> at 0.17 Ag <sup>-1</sup>	16Whkg <sup>-1</sup> at 1010 Wkg <sup>-1</sup>	43
AC	Carbon modified Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1-M LiPF6 in EC/DMC (1:3 in volume)	1.5- 3.0V	83 Fg <sup>-1</sup> at a current rate of 60 mAg <sup>-1</sup>		16Whkg <sup>-1</sup> at 440 Wkg <sup>-1</sup>	44
Reduced graphene oxide- carbon nanotube composite (rGO- CNT)	Anatase TiO <sub>2</sub> - Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	1 M LiPF <sub>6</sub> /EC/ DMC (nonaqueous)	0.05-3V	-	~32 mAhg <sup>-1</sup> at 0.1Ag	33.35 Whkg <sup>-1</sup> at 83.55 Wkg <sup>-1</sup> 26.2 Whkg <sup>-1</sup> at 327.5 Wkg <sup>-1</sup> 15.09 Whkg <sup>-1</sup> at 1207.4 Wkg <sup>-1</sup>	This work



Figure 4.6: Ragone Plot of the ESD-based Li-HEC full cells based on discharge characteristics.

## 4.4 Conclusions

A novel 3V Li-HEC utilizing ESD based rGO-CNT composite cathode and an anatase TiO<sub>2</sub>-Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> anode was constructed and analyzed. The cathode and anode were first analyzed as working electrodes against a lithium counter electrode and were able to deliver discharge capacities of ca. 63 mAhg<sup>-1</sup> and 95 mAhg<sup>-1</sup> with good reversibility and cycling. The full Li-HEC cells were able to deliver a maximum energy density of 33.35 Whkg<sup>-1</sup> and a maximum power density of 1207.4 Wkg<sup>-1</sup>, with specific energy ranging between 33.35-15.09 Whkg<sup>-1</sup> at power densities of 83.55-1207.4 Wkg<sup>-1</sup>, where all the cell parameters were normalized with the total anode and cathode masses. Furthermore, the Li-HEC cells were able to retain ~77% of capacitance retention after 100 cycles. The superior energy-power cell characteristics are attributed to the porous electrode structure and the utilization of organic electrolyte which allows for a wider electrochemical potential window. The feasibility of using ESD for construction of a high performance hybrid capacitor was thus demonstrated in this report. Further enhancement in energy and power is expected with the use of ESD based internal parallel systems which can address voltage matching and mitigate double layer and redox charge storage mismatch, which are subjects of future works.

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# 5. ELECTROSTATIC SPRAY DEPOSITION BASED MANGANESE OXIDE FILMS: FROM PSEUDOCAPACITIVE CHARGE STORAGE MATERIALS TO THREE-DIMENSIONAL MICROELECTRODE INTEGRANDS

#### 5.1 Introduction

The technological advancement toward small-scale and portable devices has resulted in an increased demand for micro-power systems. For instance, the recent boom in the development of implantable medical devices, wireless sensors, smart cards, microelectromechanical systems (MEMS) and personal electronics has resulted in the need for reliable miniaturized energy storage devices. At present, the majority of the micro-devices rely on batteries to provide the required energy and power. Despite the commercial availability of thin-film or "microbatteries", their relatively poor powerhandling ability and limited lifetime hinder their applicability to systems that require high current spikes [1,2]. As an alternative to batteries, energy harvesters hold significant promise for sustainable environments; however, the currently existing energy harvester systems require an energy storage device in tandem [1]. Electrochemical capacitors or supercapacitors, on the other hand, are electrochemical energy storage systems that possess higher power densities than batteries along with superior lifetime. Conventional supercapacitors, however, are too bulky for small-scale applications and their fabrication methods are not compatible with the currently existing Integrated Circuit (IC) technology. Therefore, of immediate need is downsizing supercapacitors with compatible microelectronic fabrication techniques, so that they can be placed directly on the chip. Such devices, also referred to as micro-supercapacitors (MSCs), generally possess negligible active material masses and, therefore, their performance metrics are typically normalized by the area of the system. The typical areal energy and power densities delivered by MSCs range from  $\mu$ Wh-mWh·cm<sup>-2</sup> and  $\mu$ W-mW·cm<sup>-2</sup> [1,3–5]. Volumetric/stack normalization is also popular for reporting MSC performance, since it provides insight into intrinsic material properties, as well as device architecture.

In the past decade, carbon microelectromechanical systems (C-MEMS) technique has emerged as a potential technique to successfully fabricate carbon-based current collectors and electrodes for on-chip energy storage and bio-sensing applications [6–13]. The C-MEMS process is a microfabrication technique that essentially involves the pyrolysis of a patterned photoresist into carbon structures. C-MEMS offers the feasibility of creating 3D micro-pillars, which offsets the limitation of the small footprint area required for miniaturized systems. The idea of using 3D C-MEMS-based microstructures as current collectors for the integration of other capacitive materials was first demonstrated by Chen et al. [11], where they grew carbon nanotubes (CNTs) on the surface of the C-MEMS structures. The CNT/C-MEMS structures were reported to exhibit specific capacitance as high as 20 times that of the bare C-MEMS structures. Other reports have documented the use of C-MEMS-based MSCs including electrochemically activated C-MEMS [12], and polypyrrole (PPY) decorated C-MEMS structures [13]. Apart from CNT and PPY, manganese oxides offer great promise as active materials, owing to their high theoretical specific capacitance, environmental benignity, large abundance, and low cost [14–17]. Of all polymorphs, birnessite MnO<sub>2</sub>, in particular, is very well suited for energy storage applications, given the simultaneous utilization of the double-layer capacitance as well as the  $Mn^{3+}/Mn^{4+}$  redox couple [17]. Its layered structure exhibits edge-sharing MnO<sub>6</sub> octahedra in the sheets, and the facile in-and-out cation motion from the interlayer region allows for partial electrolyte ion intercalation into the lamellar region [17]. One of the recently proposed synthetic routes to obtaining birnessite  $MnO_2$  (layered) is the electrochemical phase transition from hausmannite  $Mn_3O_4$  (spinel) [18–20]. The synergy between the hausmannite and birnessite phases has been documented to yield superior current response as opposed to the pristine  $MnO_2$  or  $Mn_3O_4$  phases [21,22]. Furthermore, as noted by Kim et al. [23], the spontaneous transition of layered to spinel manganese oxides is one of the critical factors that compromises with their structural stability, and therefore, the opposite transition from spinel to layered phases could be advantageous for enhancing the cycle life of layered birnessite materials.

In this work, porous manganese oxide films were synthesized via electrostatic spray deposition (ESD) and evaluated as pseudocapacitive materials and as active materials for C-MEMS integration. ESD is an electrohydrodynamic spraying technique, which essentially involves the disintegration of a precursor solution into an aerosol spray upon the application of a high voltage between the feeding source and a grounded preheated substrate. The ability to tailor the film morphology by fine-tuning deposition parameters, without the need for vacuum, is what makes ESD an attractive and cost-effective thin-film synthesis method [24–29]. The ESD-derived manganese oxide films were able to deliver specific capacitances as high as  $225 \text{ F} \cdot \text{g}^{-1}$  from  $72 \text{ F} \cdot \text{g}^{-1}$  upon electrochemical cycling in neutral aqueous media. The enhancement in capacitance was ascribed to a partial phase transformation from hausmannite  $Mn_3O_4$  (spinel) to birnessite  $MnO_2$  (layered). In addition to the enhancement in charge storage capacity, a concomitant improvement in kinetics and resistivity was observed upon cycling. Given the

coexistence of the two phases, the films are referred to as  $MnO_x$  henceforth. Several reports have documented the use of ESD-based manganese oxide films but their direct applicability to microsystems has not been explored [30,31]. Given the potent advantages of thin films for microsystems, the ESD-based  $MnO_x$  were integrated onto the C-MEMS-generated 3D carbon micro-pillars and evaluated as MSC systems. In a two-electrode configuration, the  $MnO_x/C$ -MEMS microelectrodes (MEs) were able to deliver specific capacitance as high as 0.055 F·cm<sup>-2</sup>, much higher than other microsystems [32–34]; the maximal volumetric energy and power densities delivered by the  $MnO_x/MEs$  were 0.51 mWh·cm<sup>-3</sup> (1.84 J·cm<sup>-3</sup>) and 28 mW·cm<sup>-3</sup> (28.3 mJ·s<sup>-1</sup>·cm<sup>-3</sup>), respectively. The excellent areal capacitance and the relatively high stack energy density of the  $MnO_x$ -MEs are attributed to the pseudocapacitive  $MnO_x$  as well as the three-dimensional architectural framework provided by the micro-pillars.

### 5.2 **Results and Discussion**

# 5.2.1 Crystallographic, Spectroscopic and Microstructural Studies on the As-Prepared and Cycled MnO<sub>x</sub> Films

The XRD pattern of the as-deposited manganese oxide powders is depicted in Figure 5.1a. The as-deposited powder was confirmed to be hausmannite-Mn<sub>3</sub>O<sub>4</sub> (Joint Committee on Powder Diffraction Standards (JCPDS) Card Number: 00-24-0734). The peaks at 18.0°, 28.9°, 32.4°, 36.2°, 38.3°, 44.5°, 50.9°, 53.6°, 58.5°, 60.1°, 64.8° and 74.3° are attributed to the (hkl) planes (101), (112), (103), (211), (004), (220), (105), (321), (215), (400) and (413), respectively. The XRD pattern of the cycled MnO<sub>x</sub> (after 1000 cycles), depicted in Figure 5.2a, on the other hand, did not exhibit any sharp peaks indicating the phase to be mostly amorphous. The broad peak centered at 18.64° is indexed

as (002) plane of the birnessite MnO<sub>2</sub> phase, whereas the two faint peaks located at  $36.7^{\circ}$ and 65.7° are identified as (006) and (119) planes, respectively (JCPDS Card Number: 00-018-0802) [35]. The Fourier Transform Infrared (FTIR) spectrum of the as-synthesized  $MnO_x$  films between frequencies of 500–4000 cm<sup>-1</sup> is depicted in Figure 5.1b. In the highfrequency region, the broad peak centered at 3345 cm<sup>-1</sup> is assigned to -OH stretching vibrations [36], whereas the peak located at around 1624  $\text{cm}^{-1}$  is attributed to –OH bending vibrations [36]. In the lower frequency region, the absorption peaks located at  $529 \text{ cm}^{-1}$  and  $602 \text{ cm}^{-1}$  are ascribed to Mn-O stretching modes in the octahedral and tetrahedral sites, respectively [20,36–38]. The FTIR spectrum of the cycled  $MnO_x$  (after 1000 cycles) film is shown in Figure 5.2b. It should be noted that while the majority of the peaks signaling –OH bending and stretching are still visible, the peak at  $602 \text{ cm}^{-1}$  which signals the presence of the tetrahedral stretch of Mn-O disappears, indicating a loss of order in the crystal structure as compared to the as-synthesized  $MnO_x$  films. However, the peak at 525 cm<sup>-1</sup> is still present indicating that the cycled films comprise predominantly Mn-O groups from the octahedral layers, which is also indicative of birnessite phase. The microstructure of the asdeposited manganese oxide sample is shown in Figure 5.1c; the microstructure was mostly porous with reticular network-like morphology. The microstructure of the electrochemically cycled manganese oxide (after 1000 cycles) is shown in Figure 5.2c. As evident, there is a dramatic change in the morphology as compared to the as-deposited films; as opposed to the previous reticular structure, the post-cycling structure is predominantly "layered" platelet-like, which is reminiscent of birnessitic-MnO<sub>2</sub> [19,20]. Figure 5.1d shows the High Resolution Transmission Electron Microscope (HRTEM) micrograph of the sample; the particles were nano-sized with different planar orientations.

The lattice fringes with d-spacings of 4.78 Å and 2.47 Å were indexed as (hkl) orientations of (101) and (211) of hausmannite-Mn<sub>3</sub>O<sub>4</sub>. The Selected Area Electron Diffraction (SAED) pattern is shown as the inset of Figure 5.1d. The d-spacings of 2.41 Å, 2.03 Å, 1.83 Å, 1.54 Å, 1.27 Å, 1.10 Å and 1.03 Å corresponded to (hkl) orientations of (211), (220), (204), (224), (413), (512) and (327) of hausmannite-Mn<sub>3</sub>O<sub>4</sub>. The HRTEM of the cycled MnO<sub>x</sub> powders is shown in Figure 5.2d and the detailed SAED analysis is shown as the inset. The d-spacings of 2.29 Å and 1.50 Å, correspond to (hkl) planes of (006) and (119) of the birnessite phase, respectively, whereas the d-spacings of 2.01 Å, 1.82 Å and 1.13 Å correspond to (220), (204) and (512) planes of the hausmannite phase.



Figure 5.1: (a) XRD pattern of the as-deposited  $MnO_x$  powders; (b) FTIR pattern of the as-deposited  $MnO_x$  films; (c) SEM microstructure of the as-deposited  $MnO_x$  films; (d) HRTEM micrograph of the as-deposited  $MnO_x$  powders; the inset depicts the SAED pattern.



Figure 5.2: (a) XRD pattern of the cycled MnO<sub>x</sub> powders; (b) FTIR pattern of the cycled MnO<sub>x</sub> films; (c) microstructure of the cycled MnO<sub>x</sub> films showing layered platelet-like morphology; (d) HRTEM of the cycled MnO<sub>x</sub> powders; the inset shows the SAED pattern, (b) represents birnessite phases, whereas (d) represents hausmannite phase.

## 5.2.2 Electrochemical Characterization of the MnO<sub>x</sub> Films

The cyclic voltammograms (CV) of the as-synthesized manganese oxide films between potentials of -0.1 V and 0.9 V (vs. Ag/AgCl) at a sweep rate of 5 mV·s<sup>-1</sup> are shown in Figure 5.3a. As evident for the 2nd cycle, the CV has no discernible redox peaks. Upon cycling, however, there is a gradual origin and increase in the intensity of anodic and cathodic currents around 0.63 V and 0.34 V, which is attributed to the oxidation and reduction between the Mn<sup>3+</sup>/Mn<sup>4+</sup> redox couple, as per the Pourbaix

diagram [21,30,39]. It is worth noting that the area under the CV curve increases substantially upon cycling, which implies that there is enhancement in capacitance upon electrochemical cycling. The gravimetric specific capacitances ( $C_s$ ) at the 2nd, 10th, 20th, 50th, 100th, 200th and the 500th cycles were approximated as 56, 102, 129, 156, 162, 163 and 160 F·g<sup>-1</sup>, respectively, using Equation (1), where  $C_s$  is the specific capacitance, m is the mass of the electrode, s is the scan rate,  $\Delta V$  is the voltage window, I is the current, and V is the voltage.

$$C_s = \frac{1}{2ms\Delta V} \int IdV \tag{1}$$

Figure 5.3b depicts the galvanostatic charge-discharge (GCD) curves of the MnO<sub>x</sub> films at a current density of 0.5 Ag<sup>-1</sup>. As evident, there is a significant enhancement in capacitance from the 2nd cycle accompanied with a marked decrease in the voltage drop in the subsequent cycles. At the 2nd, 10th, 20th, 50th, 100th, 200th and 500th cycles, the specific capacitance was approximated as 72, 139, 172, 197, 214, 225, 223 and 215 F·g<sup>-1</sup>, respectively. In order to investigate the resistivity changes upon subsequent cycling in the sample, Electrochemical Impedance Spectroscopy (EIS) studies were carried between frequencies of 100,000 Hz and 0.01 Hz. A typical Nyquist curve comprised a depressed semicircle in the high-frequency region followed by a relatively linear slope in the lower frequencies. The diameter of the semicircular region is associated with the charge-transfer resistance of the system at the electrode-electrolyte interface, and equivalent circuit analyses were done in order to verify the effect of cycling on the resistance of the system. The equivalent circuit for the Nyquist plots has been depicted as the inset of Figure 5.3c. *R<sub>s</sub>*, *R<sub>ct</sub>*, *W*, *C<sub>dl</sub>* and *C<sub>p</sub>* stand for solution resistance, charge-transfer resistance,

Warburg impedance, double-layer capacitance, and pseudocapacitance, respectively [40]. The values of  $R_{ct}$  and  $R_s$  at different cycles have been tabulated in Table 5.1.

	Before Cycling	After 100 Cycles	After 200 Cycles	After 300 Cycles	After 400 Cycles	After 500 Cycles
$R_{s}(\Omega)$	3.56	4.51	4.51	9.54	4.44	5.11
$R_{ct}(\Omega)$	198.91	81.63	55.31	62.95	67.84	72

 Table 5.1: Solution and charge-transfer resistances computed from equivalent circuit at different cycles.

As evident, the charge-transfer resistance decreases rapidly for the first 200 cycles, which can be ascribed to the transformation of the relatively insulating  $Mn_3O_4$  to the more conducting birnessite  $MnO_2$ , and is consistent with previous reports [19]. The slight increase in the resistance after the 200th cycle can be attributed to the resistance changes in the predominantly active birnessite phase upon cycling. The long-term cycling of the  $MnO_x$  films has been shown in Figure 5.3d. The specific capacitance of the electrode steadily increases from ca. 72 F·g<sup>-1</sup> at the second cycle to a maximal capacitance of 225 F·g<sup>-1</sup> at the 200th cycle. It should be noted that even the starting capacitance of the MnO<sub>x</sub> films, which yielded a low gravimetric capacitance of 13 F·g<sup>-1</sup> [41]. At the 1000th cycle, the capacitance dropped to 199 F·g<sup>-1</sup>, resulting in a capacitive drop of approximately 11.6% when compared with the maximal capacitance reached by the system. The GCD curves at different current densities are shown in Figure 5.3e. The electrodes were able to deliver

capacitances of 233, 221, 196, 167, 131 and 88  $\text{F}\cdot\text{g}^{-1}$  at current densities of 0.1, 0.2, 0.4, 0.8, 1.6 and 3.2 Ag<sup>-1</sup>, respectively. The effect of scan rate on the capacitance of the MnO<sub>x</sub> films is shown in Figure 5.3f. The capacitances were estimated to be ca. 164, 136, 110, 77, 47 and 30  $\text{F}\cdot\text{g}^{-1}$  at scan rates of 2, 5, 10, 20, 50 and 100 mV·s<sup>-1</sup>, respectively. As evident, the capacitance of the MnO<sub>x</sub> electrodes decreases with increasing scan rate in addition to the clear deviation from the relatively rectangular capacitive shape. This is expected since the rapid electrolyte ion flux at higher scan rates limits the diffusion-controlled charge storage processes at the MnO<sub>x</sub> electrode surface, resulting in lower utilization of active charge storage sites, thereby limiting the charge storage [42].



Figure 5.3: (a) CV curves of the  $MnO_x$  films at different cycles scanned at a sweep rate of 5 mV·s<sup>-1</sup>; (b) typical GCD curves of the  $MnO_x$  films at a constant charge-discharge current rate of 0.5 Ag<sup>-1</sup> for different cycles; (c) Nyquist plots of the  $MnO_x$  films at different cycles; the inset depicts the equivalent circuit used for system analyses; (d) cycling behavior of the  $MnO_x$  films; (e) galvanostatic charge-discharge profiles of the  $MnO_x$  films at different sweep rates (2–100 mV·s<sup>-1</sup>).

## 5.2.3 MnO<sub>x</sub>/C-MEMS Characterization

Figure 5.4a shows the typical fabrication process of the  $MnO_x$ -MEs and the detailed explanation is given in Section 3.3. The typical  $MnO_x$ -ME architecture is shown in Figure 5.4b. A typical micro-pillar had an average height of ~75 µm and a width of ~35 µm (adjusted for tilt angle). Figure 5.4c shows the magnified view of the side of the manganese oxide-encrusted micro-pillars; as evident, the films were reticular with very porous and consistent network-like morphology, analogous to the ones synthesized previously. The thickness of the manganese oxide film was approximately 0.6–0.8 µm. For stack energy and power density calculations, the energy and power were normalized with the volume of the electrodes, for which the height of the posts was multiplied with the footprint of the device (1 cm<sup>2</sup>), equating to a volume of  $v = 1 cm^2 \times 0.0075 cm =$  $0.0075 \text{ cm}^3$ . In order to evaluate the electrochemical performance of the MnO<sub>x</sub>-MEs, two identical MnO<sub>x</sub>-MEs were used in a two-electrode symmetric cell setup and the cell was analyzed between a voltage window of 0 and 0.7 V in 1 M Na<sub>2</sub>SO<sub>4</sub>. For the symmetrical cell system, one of the  $MnO_x$ -MEs functioned as the working electrode, whereas the other served as the counter electrode. The typical cycling behavior of the  $MnO_x$ -MEs is shown in Figure 4d. As evident, the cell capacitance increased from  $\approx 14.7 \text{ mF} \cdot \text{cm}^{-2}$  to  $\approx 19.8$  $mF \cdot cm^{-2}$  from the 2nd to the 500th cycle, respectively. The enhancement in capacitance can be attributed to the electrochemical activation of the  $MnO_x$  films upon cycling. GCD curves at different current densities are shown as the inset; the predominantly triangular shape of the charge-discharge curves indicates the capacitive nature of the microelectrodes. Figure 4e shows rate-handling capability of the system, the system was able to deliver geometric capacitances (normalized by footprint area) as high as 55

 $mF \cdot cm^{-2}$  at a current rate of 0.05 mA·cm<sup>-2</sup>, while still maintaining a capacitance of 22.5  $mF \cdot cm^{-2}$  at a current density of 0.5  $mA \cdot cm^{-2}$ . The maximal stack capacitance (normalized by volume) achieved was 7.44  $\text{F} \cdot \text{cm}^{-3}$ , resulting in a maximal stack energy density of 0.51 mWh·cm<sup>-3</sup> (1.84 J·cm<sup>-3</sup>), whereas the maximal power density achievable was approximated as 28.3 mW·cm<sup>-3</sup> (28.3 mJ·s<sup>-1</sup>·cm<sup>-3</sup>), as shown in the Ragone chart in Figure 4f. The range of energy density achievable by the system was 0.21-0.51 mWh·cm<sup>-3</sup>, for a power density range of 28.3–1.1 mW·cm<sup>-3</sup>. It should be noted that the areal capacitance delivered by the MnOx-MEs was fairly high as compared to other microsystems reported in the literature [32-34], which is ascribed to the threedimensional carbon micro-pillar framework which provides for a much larger surface area for active material integration. Despite the excellent areal capacitance and the relatively high energy density of the  $MnO_x$ -MEs, their low power density needs to be addressed. Enhancement in the power handling is expected with the use of hybrid  $MnO_x$ structures containing a combination of pseudocapacitive MnO<sub>x</sub> and conducting doublelayer nanostructured carbons, as well as constructing on-chip inter-digitated systems. Designing inter-digitated designs with anode and cathode on the same chip reduces iontransport resistance [1], as a result of which, the kinetics of the system can be enhanced. Devising such hybrid structures/inter-digitated systems to further enhance the power of  $MnO_x$ -MEs is a subject of future works.



Figure 5.4: (a) Schematic representation of  $MnO_x$ -ME fabrication process (detailed description in Section 3.3); (b) SEM micrograph of a typical  $MnO_x$ -encrusted carbon micro-pillar; the inset shows  $MnO_x$ -encrusted micro-pillar arrays; (c) zoomed-in view of the microstructure of the electrostatic spray deposition (ESD)-generated  $MnO_x$  films, (d) cyclability of the  $MnO_x$ -ME electrodes; the inset depicts typical charge–discharge curves of the  $MnO_x$ -ME at different current rates (0.05–0.5 mA·cm<sup>-2</sup>); (e) geometric and stack capacitances of the  $MnO_x$ -MEs at different rates; (f) Ragone chart of the  $MnO_x$ -MEs.
#### 5.3 Materials and Methods

#### 5.3.1 Manganese Oxide Electrode Synthesis

Manganese (II) acetate tetrahydrate (Mn(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, Alfa Aesar, Ward Hill, MA, USA) was first dissolved in 1,2-propanediol (Sigma Aldrich, St. Louis, MO, USA) in the ratio 2.4 mg·mL<sup>-1</sup> with constant stirring for 30 min and directly used as the precursor solution in order to deposit the MnO<sub>x</sub> films. For the ESD setup, the feeding rate was kept at 3 mL·h<sup>-1</sup> and the voltage between the needle and substrate was kept between 6 and 8 kV. The distance between the needle and the substrate was approximately 4 cm and the deposition was carried out at 300 °C on stainless steel substrates. The typical gravimetric mass yield was 1 ± 0.05 mg per sample.

# 5.3.2 Structural and Material Characterization

Spectroscopic studies were carried out using FTIR spectroscopy in order to study the effect of cycling on the surface chemistry of the MnO<sub>x</sub> films using a JASCO FTIR 4100 equipped with an Attenuated Total Reflectance (ATR) accessory. For crystallinity studies, the powders were scratched off from the stainless steel substrates before and after cycling. The crystallinity of the as-deposited and cycled manganese oxide films was studied using a Siemens 5000D X-ray Diffractometer with Cu K $\alpha$  radiation (Siemens, Munich, Germany). Further crystallographic studies on the as-deposited and cycled powders were carried out using a Philips CM-200 200 KeV Transmission Electron Microscope (TEM) (FEI Philips, Hillsborough, OR, USA). The morphology of the as-deposited and cycled films, as well as the MnO<sub>x</sub>/C-MEMS microelectrodes, was studied using a scanning electron microscope (JEOL SEM 6330F, Peabody, MA, USA) in the secondary electron imaging (SEI) mode.

## 5.3.3 MnO<sub>x</sub>/C-MEMS Fabrication

The experimental setup and details of the C-MEMS process used in this work have been reported previously [3-6]. A schematic illustration of MnO<sub>x</sub>-ME fabrication is shown in Figure 5.4a. In brief, the C-MEMS-based 3D micro-pillars were prepared by a two-step photolithography process followed by a pyrolysis step. In the first photolithography step, a two-dimensional square (10 mm side) pattern was created using NANO<sup>TM</sup> SU-8 25 (Microchem, Westborough, MA, USA), as the current collector. The photoresist film was spun-coated onto a silicon oxide wafer (4", (1 0 0)-oriented, n-type) at 500 rpm for 12 s and at 3000 rpm for 30 s by using a Headway Research photoresist spinner, followed by soft baking at 65 °C for 3 min and hard baking at 95 °C for 7 min on a leveled hotplate. The baked photoresist was thereafter patterned with a UV exposure dose of 300 mJ cm<sup>-2</sup> using an OAI (800) Mask Aligner. After the exposure process, a post-expose bake was conducted at 65 °C for 1 min and 95 °C for 5 min on a hotplate. The second photolithography step comprised building the cylindrical micro-pillar arrays using NANO<sup>TM</sup> SU-8 100 (Microchem, Westborough, MA, USA) on the patterned current collector. SU-8 100 was spun-coated at 500 rpm for 12 s and at 1500 rpm for 30 s using a Headway Research photoresist spinner. The spun-coated photoresist was then soft baked at 65 °C for 10 min on a leveled hot plate and hard baked at 95 °C for 45 min in an oven. The exposure was done using a UV exposure dose of 700 mJ  $cm^{-2}$  using an OAI (800) Mask Aligner, following which a post-expose bake was performed at 65 °C for 3 min and 95 °C for 10 min in an oven. Afterward, the sample was developed by NANO<sup>TM</sup> SU-8 developer (Microchem, Westborough, MA, USA) for 15–20 min to wash away any remaining unexposed photoresist, followed by isopropanol rinsing and nitrogen drying.

Finally, the resultant SU-8 structures were pyrolyzed at 900 °C for 1 h in a Lindberg alumina-tube furnace with a continuous flow of argon at a ramp of 5 °C/min. After the carbonization process, the carbon samples were allowed to cool to room temperature naturally and directly used as substrates for  $MnO_x$  integration using ESD as described in Section 4.3.1.

#### **5.3.4** Electrochemical Characterization

The electrochemical characterization on the manganese oxide films deposited on stainless steel substrates as well as carbon micro-pillars was carried out using a Bio-logic Versatile Multichannel Potentiostat (VMP3). For half-cell studies, the MnO<sub>x</sub> films were used as the working electrode, a platinum wire served as the counter electrode, while an Ag/AgCl electrode served as the reference electrode; the MnO<sub>x</sub> films were tested between potentials of -0.1 V and 0.9 V (vs. Ag/AgCl). A neutral aqueous electrolyte of 1.0 M Na<sub>2</sub>SO<sub>4</sub> was used for the cell assembly. For the MnO<sub>x</sub>/C-MEMS characterization, two of the manganese oxide-encrusted carbon micro-pillars were used in a symmetric configuration in 1.0 M Na<sub>2</sub>SO<sub>4</sub> aqueous electrolyte for a cell potential of 0-0.7 V.

## 5.4 Conclusions

In this paper, manganese oxide films were synthesized using electrostatic spray deposition (ESD) and characterized as pseudocapacitive materials for electrochemical capacitor applications in neutral aqueous media. The initial phase synthesized was the relatively insulating hausmannite- $Mn_3O_4$ , which partially transformed into the conducting birnessite- $MnO_2$  upon electrochemical cycling, resulting in an enhanced gravimetric capacitance from 72 F·g<sup>-1</sup> to 225 F·g<sup>-1</sup>. Furthermore,  $MnO_x$ -MEs were created by

combining bottom-up ESD approach and top-down C-MEMS approach. In a twoelectrode setup, the  $MnO_x$ -MEs were able to deliver geometric specific capacitances as high as 0.055 F·cm<sup>-2</sup>, and maximal volumetric energy and power densities of 0.51 mWh·cm<sup>-3</sup> and 28.3 mW·cm<sup>-3</sup>, respectively. The excellent areal capacitance and the high stack energy density of the  $MnO_x$ -MEs are attributed to the pseudocapacitive  $MnO_x$  as well as the three-dimensional architectural framework of the micro-pillars. The feasibility of using ESD for high gravimetric thin-film manganese oxide films and high areal capacitance 3D microelectrodes was therefore established.

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# 6. EXPANDING THE POTENTIAL WINDOW OF AQUEOUS ASYMMETRIC ELECTROCHEMICAL CAPACITORS WITH ELECTROSTATICALLY SPRAYED MANGANESE OXIDE COMPOSITE FILMS

#### 6.1 Introduction

Electrochemical capacitors (ECs), also known as "supercapacitors" account for an emerging class of electrochemical energy-storage systems (EES). Typically, ECs differ from their electrostatic counterparts by storing charge at the electrode-electrolyte interface (Helmholtz double layer) as opposed to an electric field across a dielectric, and therefore demonstrate specific capacitances at least an order of magnitude higher than that of conventional capacitors [1]. The enhancement in energy however, comes with a decrease in specific power, typically by an order or two of magnitude (~10kWkg<sup>-1</sup>). Despite, the relatively high energy density (~3-5 Whkg<sup>-1</sup>) of ECs as compared to traditional capacitors, their gravimetric energy density remains much lower than secondary batteries (~200 Whkg<sup>-1</sup> for lithium-ion batteries). Much research has been invested into enhancing the energy density of ECs, since their low time constants and high cycle longevity are attractive features for harnessing and reusing the energy from repetitive motion [1]. One of the alternatives to achieving superior energy densities is the asymmetric design, which combines a positive pseudocapacitive electrode and a negative double layer (dl) electrode within one system. Such a system benefits from the large capacitance of the redox-based electrode and the high rate capability of the dl electrode. Furthermore, the synergy of using the disparate electrodes in one system allows to stretch the potential window of water based electrolytes beyond the thermodynamic limit  $(\sim 1.2V)$  by utilizing the large overpotentials for hydrogen and oxygen evolution at the negative dl electrode and the positive pseudocapacitive electrode, respectively [1, 2]. In a

symmetric setup in aqueous media, the cell voltage is typically limited to  $\sim 1V$  and therefore using the asymmetric design significantly enhances the effective working voltage of the cell. Given the benefits of aqueous electrolytes in terms of costeffectiveness, ease of packaging and safety over nonaqueous electrolytes, it is highly desirable to stretch their electrochemical potential window beyond the thermodynamic limit.

As pseudocapacitive electrode materials, manganese oxides  $(MnO_x)$  offer significant promise given their high theoretical specific capacitances in aqueous electrolytes, environmental benignity, abundance, and low cost. [3-7]. One of the shortcomings of metal oxide electrodes, however, is their low electronic conductivity. This drawback can however be offset by adding a conducting additive such as carbon nanotubes (CNTs). Given the nanostructured nature of CNTs, they can provide for lower percolation thresholds as compared to the conventionally used carbon black [8]. Furthermore, the addition of CNTs to different composites has shown to improve the mechanical robustness of different composites [9], which can be beneficial for long-term cycling. Based on previous findings, it has been established that only a thin volume of the  $MnO_x$  electrode participates in the charge-storage mechanism under electrochemical capacitor demands [1], which makes synthesizing MnO<sub>x</sub> thin-films an attractive solution for pseudocapacitive needs. Electrostatic Spray Deposition (ESD) is a thin-film synthesis technique, which essentially involves the disintegration of a precursor solution into an aerosol spray upon the application of a high voltage between the feeding source and a grounded preheated substrate [10-13]. The ability to tailor the film morphology by finetuning the deposition parameters, without the need for vacuum or addition of binders is

what makes ESD an appealing thin-film fabrication method and ESD derived thin-films have been widely reported for energy-storage applications [14-20].

Herein, pristine MnO<sub>x</sub> along with MnO<sub>x</sub>-CNT composite electrodes with 10% and 20% CNT addition were synthesized via ESD and investigated as electrochemical capacitor electrodes. The 10% CNT composition designated as MnO<sub>x</sub>-CNT 9-1 exhibited superior electrochemical characteristics as opposed to both the pristine MnO<sub>x</sub> electrode as well as the MnO<sub>x</sub>-CNT 8-2 (20% CNT) composition. The addition of CNT to the otherwise pristine MnO<sub>x</sub> films resulted in superior charge-transfer characteristics along with higher gravimetric capacitances. In a three-electrode configuration, the MnO<sub>x</sub>-CNT 9-1 electrode exhibited gravimetric capacitances as high as 281 Fg<sup>-1</sup> in addition to excellent rate capability and fairly high cycle life (~87% after 1000 cycles). Upon verifying the viability of the MnO<sub>x</sub>-CNT 9-1 electrodes as pseudocapacitive charge storage components, they were coupled with commercial activated carbon (AC) based counter electrodes in order to investigate their usage in a practical two-electrode system. Five pertinent mass ratios were evaluated in order to evaluate the optimal balanced cell characteristics. The asymmetric capacitor with MnOx-CNT 9-1//AC with the AC electrode 2.6 times massive as that of the MnOx-CNT 9-1 electrode, exhibited superior electrochemical characteristics than the other asymmetric systems as well as the symmetric MnOx-CNT 9-1 and symmetric AC systems. The optimized asymmetric capacitor exhibited a maximal energy density of 30.3 Whkg<sup>-1</sup>, which is fairly high for aqueous systems. The excellent electrochemical characteristics of the asymmetric capacitor are ascribed to the i) 2V potential window exhibited by the capacitor making full utilization of the overpotentials of H<sub>2</sub> and O<sub>2</sub> evolution at the negative and positive

electrodes, respectively; ii) high capacity utilization from the MnO<sub>x</sub>-CNT 9-1 electrode, indicating balanced hybrid system.

#### 6.2 Materials and Methods

## 6.2.1 ESD based manganese oxide electrode synthesis

Manganese (II) acetate tetrahydrate (Mn(CH<sub>3</sub>COO)<sub>2</sub>·4H<sub>2</sub>O, Alfa Aesar, Ward Hill, MA, USA) was first dissolved in 1,2-propanediol (Sigma Aldrich, St. Louis, MO, USA) in a ratio of 2.4 mgml<sup>-1</sup> with constant stirring for 30 min and directly used as the precursor solution to deposit the MnO<sub>x</sub> films. For the ESD setup, the feeding rate was kept at 3 mlh<sup>-1</sup> and the voltage between the needle and substrate was kept between 6 and 8 kV. The distance between the needle and the substrate was approximately 4 cm and the deposition was carried out at 350°C on stainless steel substrates. For the MnO<sub>x</sub>-CNT composites, carboxyl functionalized short multi-walled carbon nanotubes (CNT, Cheap tubes Inc.) were dispersed along with the manganese (II) acetate tetrahydrate in percent mass ratios of 10% and 20%; the composites are designated as MnO<sub>x</sub>-CNT 9-1 and MnO<sub>x</sub>-CNT 8-2 for the CNT mass ratio of 10% and 20%, respectively. The composite deposition was carried out on stainless steel substrates preheated at 350°C for the identical deposition conditions as that of the pristine MnO<sub>x</sub> films.

### 6.2.2 Material Characterization

In order to investigate the crystallinity of the ESD based pristine  $MnO_x$  and  $MnO_x$ -CNT films, X-ray diffraction (XRD) studies using a Siemens 5000D X-ray diffractometer with Cu K $\alpha$  radiation. The morphology of the ESD based  $MnO_x$ ,  $MnO_x$ -CNT 9-1 and  $MnO_x$ -CNT 8-2 composite electrodes as well as the slurry-casted AC electrode was studied using scanning electron microscopy using a JEOL SEM 6330 (JEOL, USA). Spectroscopic studies on the pristine  $MnO_x$  and composite  $MnO_x$ -CNT films were carried out using Fourier transform infrared spectroscopy (FTIR) using JASCO FTIR-4100 equipped with an ATR-PRO 450S (Attenuated Total Reflectance) accessory.

#### 6.2.3 Electrochemical Characterization

The electrochemical characterization on the pristine  $MnO_x$ ,  $MnO_x$ -CNT 9-1, and MnO<sub>x</sub>-CNT 8-2 electrodes as well as the full-cells was carried out using a Bio-logic Versatile Multichannel Potentiostat (VMP3). For the half-cell studies, the ESD based  $MnO_x$  and the  $MnO_x$ -CNT composite films were used as the working electrode, a platinum coil was used as the counter electrode and an Ag/AgCl electrode was used as the reference electrode. Both the pristine and composite  $MnO_x$  films were tested between potentials of -0.1 V and 0.9 V (vs. Ag/AgCl) and a neutral aqueous electrolyte of 1.0 M Na<sub>2</sub>SO<sub>4</sub> was used for the cell assembly. From comparative electrochemical studies, the MnO<sub>x</sub>-CNT 9-1 composition demonstrated superior electrochemical characteristics as opposed to both the pristine MnO<sub>x</sub> and the MnO<sub>x</sub>-CNT 8-2 composite films. For the asymmetric cell characterization, the MnO<sub>x</sub>-CNT 9-1 films were cycled for 20 chargedischarge cycles, in order to complete the electrochemical activation process and thereafter coupled with a commercial activated carbon (AC, MTI Corp.) based anode in different mass ratios of 1:2, 1:2.4, 1:2.6, 1:3, and 1:4 (m<sub>c</sub>:m<sub>a</sub>, where m<sub>c</sub> symbolizes the mass of the MnO<sub>x</sub>-CNT 9-1 cathode and m<sub>a</sub> symbolizes the mass of the AC anode). The AC electrode was prepared by combining AC, PVDF (polyvinylidene fluoride) and carbon black in a mass ratio of 8:1:1 in N-methyl-2-pyrrolidone (NMP). The resultant slurry was casted onto stainless steel substrates and dried for 24h at  $60^{\circ}$ C and was used for electrochemical characterization without any further treatment. An aqueous electrolyte of 1M Na<sub>2</sub>SO<sub>4</sub> was used for the full cell assembly.

#### 6.3 Results and Discussion

#### 6.3.1 Crystallographic, spectroscopic and microstructural studies

The X-ray diffraction (XRD) patterns of the as-prepared MnO<sub>x</sub>, MnO<sub>x</sub>-CNT 9-1, MnO<sub>x</sub>-CNT 8-2, and CNTs are shown in Figure 6.1a. The ESD derived MnO<sub>x</sub> films were of crystalline nature as confirmed by the presence of fairly sharp characteristic peaks in the XRD spectra; the MnO<sub>x</sub> phase was confirmed to be hausmannite  $Mn_3O_4$  but given the tendency of hausmannite Mn<sub>3</sub>O<sub>4</sub> to electrochemically transform to the amorphous birnessite phase, the manganese oxide based films are referred to as MnOx. For the pristine MnO<sub>x</sub> powders, the peaks located at 17.9°, 28.8°, 31.0°, 32.4°, 36.1°, 38.1°, 44.5°,  $50.9^{\circ}$ ,  $53.9^{\circ}$ ,  $56.0^{\circ}$ ,  $58.4^{\circ}$ ,  $60.1^{\circ}$ ,  $64.7^{\circ}$ , and  $74.3^{\circ}$  were attributed (hkl) orientations of (101), (112), (200), (103), (211), (004), (220), (105), (312), (303), (321), (224), (400),and (413) of the hausmannite  $Mn_3O_4$  phase (JCPDS card number: 00-024-0734), respectively. As evident, the addition of CNTs to the MnO<sub>x</sub> matrix results in diminished peak intensity, indicating relatively lower degree of crystallinity as compared to the pristine MnO<sub>x</sub> powders. A peak centered at 26.1° is observed in the MnO<sub>x</sub>-CNT 8-2 pattern, which is ascribed to the (002) plane of graphite [21, 22], as also observed in the parent CNT pattern. However, the characteristic CNT peak was not observed in the MnO<sub>x</sub>-CNT 9-1 pattern, which could be a result of the low degree of crystallinity of the parent CNTs. To further characterize the ESD derived films, spectroscopic studies using Fourier transform infrared (FTIR) spectroscopy were carried out. The FTIR spectra of the

pristine MnO<sub>x</sub>, CNTs, as well as the composites are shown in Figure 6.1b. In the CNT spectrum, the peak centered at 3339 cm<sup>-1</sup> can be attributed to -OH groups resulting from water [20] or from -OH from the graphitic framework [23]. The peaks located at 2926 cm<sup>-1</sup>, 1418 cm<sup>-1</sup>, 1020 cm<sup>-1</sup>, and 848 cm<sup>-1</sup> are ascribed to C-H groups, C-O bonds from carboxylic groups, C-O groups from –COOH or alkoxy (-O-), and C-O groups from epoxy (-C-O-C-) [23], respectively. The largely pronounced C-O based groups in the CNT spectrum could be a result of the COOH functionalization. In the pristine MnO<sub>x</sub> sample, on the other hand, the peaks at ~595 cm<sup>-1</sup> and ~510 cm<sup>-1</sup> are attributed to the tetrahedral bend and the octahedral distortion vibrations of Mn-O [15, 24-27]. It is worth noting that with the addition of CNTs to the MnO<sub>x</sub>, the absorption peaks in the low-mid frequency region (700-1700 cm<sup>-1</sup>) start becoming more pronounced, which could be ascribed to the stronger absorption signals resulting from the larger CNT content.



Figure 6.1: a) X-ray diffraction patterns of the as-prepared MnO<sub>x</sub>, MnO<sub>x</sub>-CNT 9-1, MnO<sub>x</sub>-CNT 8-2 composites and CNTs; b) FTIR spectra of the pristine MnO<sub>x</sub> films, MnO<sub>x</sub>-CNT 9-1, and MnO<sub>x</sub>-CNT 8-2 films, and the CNTs.

The morphology of the as-deposited  $MnO_x$ ,  $MnO_x$ -CNT 9-1, and  $MnO_x$ -CNT 8-2 and the AC electrodes is shown in Figure 6.2. The microstructure of the pristine  $MnO_x$ electrode (Figure 6.2a) comprised a three-dimensional continuous reticular network, which is reminiscent of the previously reported ESD based  $MnO_x$  films [15]. The microstructure of the  $MnO_x$ -CNT 9-1 film is depicted in Figure 6.2b. As evident, the fidelity of the CNTs was not comprised in the composite and the CNTs were wellanchored to the reticular  $MnO_x$  framework. The 3D porous structure is maintained in the  $MnO_x$ -CNT 9-1 sample, which is expected to be advantageous for electrolyte ion diffusion. Figure 6.2c shows the micrograph of the  $MnO_x$ -CNT 8-2 electrode; the 3D continuous network was maintained with the CNTs well anchored to the skeleton. The presence of CNTs is more conspicuous in the  $MnO_x$ -CNT 8-2 electrode as compared to the  $MnO_x$ -CNT 9-1 electrode, which is expected given the larger amount of CNTs present in the composite film. The microstructure of the AC electrode is shown in Figure 6.2d; the sample consisted of fairly large bulk sized (~10 µm) carbon particles.



Figure 6.2: Top-view of the a) pristine MnO<sub>x</sub>; b) MnO<sub>x</sub>-CNT 9-1; c) MnO<sub>x</sub>-CNT 8-2, and d) AC electrodes

# 6.3.2 Comparative electrochemical studies on the pristine MnO<sub>x</sub> and MnO<sub>x</sub>-CNT composite films

The electrochemical impedance spectroscopy (EIS) curves of the as prepared  $MnO_x$ ,

MnO<sub>x</sub>-CNT 9-1, and MnO<sub>x</sub>-CNT 8-2 electrodes are shown in Figure 6.3a. As evident, the

Nyquist curves (traced between frequencies of 100000 Hz and 0.01Hz) for all the three compositions comprised a depressed semicircle in the high frequency region followed by a linear slope in the lower frequency regions. The equivalent circuit used for impedance analyses is shown as the inset of Figure 6.3a.  $R_s$ ,  $R_{ct}$ , W,  $C_{dl}$  and  $C_p$  stand for solution resistance, charge-transfer resistance, Warburg impedance, double-layer capacitance, and pseudocapacitance, respectively [15, 28]. As noted, the slope of the linear region gets steeper with the addition of CNT to the MnO<sub>x</sub>. Typically the steeper the linear component of the curve, the better is the sample conductivity. The values of  $R_{ct}$  and  $R_s$  at different cycles have been tabulated in Table 6.1. As expected, both the serial and charge transfer resistances decreased with the addition of CNTs to the MnO<sub>x</sub> matrix. In order to examine the viability of the pristine and composite MnOx films for electrochemical cycling and capacitance values, the electrodes were cycled for 100 charge-discharge cycles at a current rate of 0.5 Ag<sup>-1</sup>. As seen in Figure 6.3b, the gravimetric capacitance of the MnO<sub>x</sub>-CNT 8-2 composite was the highest initially but started decaying after ~15 cycles. The specific capacitance of the pristine  $MnO_x$  electrode kept increasing until the ~60<sup>th</sup> cycle and then stabilized. The increase in capacitance is ascribed to the electrochemical phase transformation of the hausmannite Mn<sub>3</sub>O<sub>4</sub> to birnessite MnO<sub>2</sub> and is consistent with previous reports [15, 24, 29]. The MnO<sub>x</sub>-CNT 9-1 electrode on the other hand, demonstrated superior capacitance as compared to both the MnO<sub>x</sub>-CNT 8-2 composite electrode as well as the pristine  $MnO_x$  electrode.

Cyclic voltammetry (CV) curves of  $MnO_x$ -CNT 9-1 at different scan rates are shown in Figure 6.3c; the CV curves of the pristine  $MnO_x$  and the  $MnO_x$ -CNT 8-2 compositions can be found in the supplementary file (Figure 6S1). All the CV curves were traced after the electrochemical activation process was completed. The gravimetric specific capacitance of the electrodes were estimated using Equation (6.1), where  $C_s$  is the specific capacitance, m is the mass of the electrode, s is the scan rate,  $\Delta V$  is the voltage window, I is the current, and V is the potential.

$$C_s = \frac{1}{2ms\Delta V} \int IdV \qquad (6.1)$$

The specific capacitance values of the MnO<sub>x</sub>-CNT 9-1 were calculated as 203, 184, 154, 104, 63 Fg<sup>-1</sup> at scan rates of 5, 10, 20, 50, 100 mVs<sup>-1</sup>, respectively. The gravimetric capacitance of the MnO<sub>x</sub>-CNT 9-1 electrode decreased with increasing scan rates, with a concomitant deviation from the rectangular capacitive shape. This is expected since the rapid electrolyte ion flux at higher scan rates, limits the diffusion-controlled charge storage processes at the electrode surface, resulting in lower utilization of active charge storage sites [15, 30]. The scan rate dependence of the pristine  $MnO_x$  as well as  $MnO_x$ -CNT 9-1 and MnO<sub>x</sub>-CNT 8-2 electrodes is depicted in Figure 6.3d. As evident, both the MnO<sub>x</sub>-CNT 9-1 and MnOx-CNT 8-2 compositions exhibit superior capacitance-scan rate dependence as compared to the pristine MnO<sub>x</sub> electrode, which can be attributed to the enhancement in kinetics from the addition of CNT filler. Figure 6.3e depicts the galvanostatic charge discharge (GCD) curves of the MnO<sub>x</sub>-CNT 9-1 electrodes, whereas the GCD of the pristine MnOx and the MnOx-CNT 8-2 electrodes are depicted in the supplementary file (Figure 6S1). The GCD curves are triangular in shape, which is expected given the predominantly capacitive charge storage in the manganese oxide based electrode. The specific capacitance of the MnO<sub>x</sub>-CNT 9-1 electrode was estimated as 281, 253, 221, 186, 160, 122, and 93 Fg<sup>-1</sup> at current rate of 0.2, 0.4, 0.8, 1.6, 3.2, 6.4, and 10 Ag<sup>-1</sup>, respectively. The comparative rate capability of the pristine MnO<sub>x</sub>, MnO<sub>x</sub>-CNT 9-1, as well as the MnO<sub>x</sub>-CNT 8-2 electrodes is shown in Figure 6.3f. As evident, the rate performance of both the MnO<sub>x</sub>-CNT 9-1 and the MnO<sub>x</sub>-CNT 8-2 electrodes was much superior to that of the pristine MnO<sub>x</sub> electrode, which is attributed to the CNT additive and is validated by the more linear component in the Nyquist plots depicted in Figure 6.3a. Given the larger specific capacitance of the MnO<sub>x</sub>-CNT 9-1 electrode as compared to the MnO<sub>x</sub>-CNT 8-2 with increasing current rate, the former was identified as the optimal MnO<sub>x</sub>-CNT composition in terms of electrochemical performance and was used for further characterization and full-cell analyses.

Electrode	$R_{s}\left( \Omega ight)$	$R_{ct}\left(\Omega ight)$
MnO <sub>x</sub>	9.57	681.00
MnO <sub>x</sub> -CNT 9-1	4.76	282.00
MnO <sub>x</sub> -CNT 8-2	2.31	185.70

Table 6.1: Rs and Rct values of the pristine MnOx, MnOx-CNT 9-1 and MnOx-CNT8-2 electrodes



Figure 6.3: a) Nyquist curves of the pristine  $MnO_x$  electrodes and the  $MnO_x$ -CNT composite electrodes; b) Cycling performance of the pristine  $MnO_x$  electrodes and the  $MnO_x$ -CNT composites electrodes; c) cyclic voltammetry (CV) curves of the  $MnO_x$ -CNT electrodes at different scan rates; d) scan rate dependence of the pristine  $MnO_x$ ,  $MnO_x$ -CNT 9-1, and  $MnO_x$ -CNT 8-2 electrodes; e) galvanostatic charge-discharge (GCD) curves of the  $MnO_x$ -CNT 9-1 electrode at different current rates; and f) rate capability of the pristine  $MnO_x$ ,  $MnO_x$ -CNT 9-1, and  $MnO_x$ -CNT 9-1, and  $MnO_x$ -CNT 8-2 electrodes.

#### 6.3.3 MnO<sub>x</sub>-CNT 9-1 electrode before and after electrochemical cycling

The Nyquist plots of the freshly assembled and cycled MnO<sub>x</sub>-CNT 9-1(after chargedischarge 1000 cycles) electrode are shown in Figure 6S2a. Both the before and after EIS spectra comprised a depressed semicircular region in the high frequency region followed by a linear slope in the low frequency region, however, the diameter of the semicircular region was largely suppressed in the after curve. The equivalent circuit used for impedance analyses is depicted as the inset and is the same as the one used for previous analyses. The  $R_{ct}$  component was estimated as 22.6 $\Omega$  for the cycled MnO<sub>x</sub>-CNT 9-1 electrode; the decrease in resistance is expected given the electrochemical phase transformation from the relatively insulating hausmannite Mn<sub>3</sub>O<sub>4</sub> phase to the more conducting *birnessite*  $MnO_2$  phase [15, 29]. The post electrochemical cycling  $MnO_x$ -CNT electrode microstructure is depicted in Figure 6S2b. As opposed to the as-synthesized reticular  $MnO_x$  morphology decorated with CNT, the post cycled  $MnO_x$ -CNT 9-1 electrode was predominantly layered and highly porous, which is reminiscent of birnessite phase [15, 28, 29]. Some cracks were discernible in the cycled films and the CNTs were visible. The long term cyclability of the MnO<sub>x</sub>-CNT 9-1 electrode is shown as Figure 6S2d; 87.4% of the maximal capacitance was retained after 1000 cycles.

## 6.3.4 Electrochemical characterization of the AC anode

The Nyquist plot of the freshly assembled AC anode is depicted in Figure 6S3a; much alike the composite  $MnO_x$ -CNT electrodes, a typical Nyquist curve comprised a depressed semicircular region in the high frequency region followed by a steep linear slope in the low frequency region. The inset of Figure 6S3a depicts the equivalent circuit used for the EIS analyses; the same circuit used previously for the MnO<sub>x</sub> based electrodes

was employed.  $R_s$  and  $R_{ct}$  were estimated as 3.4 $\Omega$  and 12.6 $\Omega$ , respectively. The charge transfer resistance of the AC electrode was much smaller than the MnO<sub>x</sub> electrode, which is expected given the largely double layer capacitance and superior conductivity of carbon. Figure 6S3b shows the cycling of the AC anode at a current rate of 0.5Ag<sup>-1</sup>. The GCD curves of the AC anode at different current rates are shown in Figure 6S3c; the specific capacitance was estimated as 108, 94, 55, and 14 Fg<sup>-1</sup> at current rates of 0.1, 0.2, 0.5, and 1 Ag<sup>-1</sup>, respectively as shown in the rate capability curve (Figure 6S3d).

# 6.3.5 Electrochemical characterization of the asymmetric and symmetric MnO<sub>x</sub>-CNT 9-1 based full-cells

Given the large disparity in the specific capacitances exhibited by the MnO<sub>x</sub>-CNT 9-1 electrode and the commercial AC based anode, it is essential to balance the charges stored by the respective electrodes. As seen in Figure 6.4a, MnO<sub>x</sub>-CNT 9-1 electrode encompasses much larger area under the CV curve as compared to the AC anode. From equation (1), the specific capacitances of the AC anode and the MnO<sub>x</sub>-CNT 9-1 cathode were estimated as 50 Fg<sup>-1</sup> and 184 Fg<sup>-1</sup>. Since for the present study an excess of electrolyte was used, the charge balancing was done by  $q_+ = q_-$ , where  $q_+$  and  $q_-$  are the charges held by the positive and the negative electrode, respectively. As evident, the anode is the limiting electrode in terms of the charge stored, and it is necessary to adjust the active mass of the electrode accordingly. Depending upon the current rate, the mass of AC should be in the vicinity of 2-4 times that of the MnO<sub>x</sub>-CNT 9-1 electrode. In order to study the effect of mass ratio on the energy-power trade-off, five pertinent mass ratios (MR) were investigated 1:2, 1:2.4, 1:2.6, 1:3, and 1:4; where the latter value denotes the mass of the AC electrode. Control groups containing symmetric AC//AC and MnO<sub>x</sub>-CNT  $9-1//MnO_x$ -CNT 9-1 systems were also investigated. The GCD plots as well as the rate capability and energy-power characteristics of the different symmetric as well as asymmetric systems are depicted in the supplementary file (Figure 6S4 and 6S5).



Figure 6.4: a) CV curves of the AC electrode and the  $MnO_x$ -CNT 9-1 electrode at a scan rate of  $10mVs^{-1}$ ; b) typical Nyquist plots of the AC//AC and  $MnO_x$ -CNT 9-1//MnO<sub>x</sub>-CNT 9-1 symmetric systems as well as the asymmetric capacitor  $MnO_x$ -CNT 9-1//AC (mass

ratio of 1:2.6); c) CV and d) GCD curves of the asymmetric  $MnO_x$ -CNT 9-1//AC system (MR 1:2.6); e) cyclability of the symmetric AC//AC, symmetric  $MnO_x$ -CNT 9-1//MnO<sub>x</sub>-CNT 9-1 and  $MnO_x$ -CNT 9-1//AC system (MR 1:2.6); f) Ragone chart depicting the energy-power characteristics of the  $MnO_x$ -CNT 9-1//AC system (MR 1:2.6) with works reported in the literature.

The gravimetric energy and power densities of the system were computed using equations (6.2) and (6.3), respectively:

$$ED = \frac{1}{2}C_s V^2 \qquad (6.2)$$
$$PD = \frac{ED}{t_{discharge}} \qquad (6.3)$$

where ED and PD symbolize the energy and power densities, respectively;  $C_s$  stands for specific capacitance corresponding to a respective current rate and V is the cell voltage. From comparative studies, based on the optimal energy-power characteristics, it is evident that the asymmetric capacitors tested for mass ratios between 2-3 times AC as that of MnO<sub>x</sub>-CNT 9-1 had superior energy and power densities as compared to both the symmetric capacitors based on AC//AC and MnO<sub>x</sub>-CNT 9-1//MnO<sub>x</sub>-CNT 9-1 configurations. From the rate capability and the Ragone chart (Figure 6S5), it can be seen despite the higher capacitance of the symmetric MnO<sub>x</sub>-CNT 9-1 capacitor, the actual energy density is still lower than the symmetric AC capacitor. The lower energy density can be ascribed to the lower cell potential achievable by the MnO<sub>x</sub>-CNT 9-1 symmetric capacitor (0.8V as opposed to 1.2V of that of AC//AC). The lower cell potential of the symmetric MnOx-CNT system can be ascribed to the oxygen evolution at the positive end and the irreversible reduction of Mn<sup>4+</sup> to Mn<sup>3+</sup> and the eventual disproportionation to soluble Mn<sup>2+</sup> at the negative end [1, 31, 32]. Given the quadratic dependence of cell

potential on energy density (equation (6.2)), the enhancement from the high capacitance of the MnO<sub>x</sub>-CNT 9-1 electrode is offset in a practical two-electrode system. From capacitive as well as energy-power characteristics, the asymmetric capacitor with MR 1:2.6 exhibited superior electrochemical behavior than any other composition. The asymmetric capacitor with an MR of 1:4, on the other hand, exhibited poor energy-power trade-off in general, which could be attributed to the predominant AC component in the capacitor construction. With the massive AC component, the asymmetric capacitor starts mimicking the limiting electrode characteristics, resulting in low capacitance and relatively low rate handling. The relatively inferior characteristics of the asymmetric capacitor with MR 1:4 can be explained as an "unbalanced" system. While mass ratio is one measure to balance the charges stored by the individual electrodes, it does not necessitate that the accessibility of the actual charge storage capacities; other factors include electrode thickness, system kinetics, etc. From the comparative cell analyses at different mass ratios and cell configuration, the asymmetric capacitor with MR 1:2.6 was deemed as the optimal balanced system.

The Nyquist plots of the freshly assembled symmetric AC, symmetric  $MnO_x$ -CNT 9-1 and the optimized  $MnO_x$ -CNT 9-1//AC systems are shown in Figure 6.4b. As evident, the Nyquist curves comprised a depressed semicircular region in the high frequency region followed by a linear response in the low frequency region. Given the steep linear component of the curves and the relatively small diameters of the semicircular region, all the systems exhibited capacitive behavior. The CV curves of the optimized  $MnO_x$ -CNT 9-1//AC capacitor at different scan rates are shown in Figure 6.4c; the curves are largely rectangular with no evident electrolyte decomposition for a

potential window of 2V. The curves maintain the rectangular shape even at a high scan rate of 100mVs<sup>-1</sup>, indicating predominantly capacitive charge storage. The GCD curves of the optimized capacitor are shown in Figure 6.4d; the curves are primarily triangular with some curvature, which is expected given the coexistence of pseudocapacitive and double layer charge storage within one system. The cycling performance of the symmetric AC//AC system, the symmetric MnO<sub>x</sub>-CNT 9-1//MnO<sub>x</sub>-CNT 9-1 system, as well as the optimized MnO<sub>x</sub>-CNT 9-1//AC capacitor at a current rate of 0.5Ag<sup>-1</sup> is shown in Figure 6.4e; the symmetric AC//AC capacitor maintains ~100% of the initial cell capacitance after 500 cycles, whereas the symmetric MnO<sub>x</sub>-CNT capacitor only maintains 56.4% of the initial cell capacitance after 500 cycles. The decrease in capacitance can be attributed to the largely pseudocapacitive behavior of the MnO<sub>x</sub>-CNT 9-1 electrodes. However, it is worth noting that the MnO<sub>x</sub>-CNT 9-1 symmetric capacitor maintained larger usable cell capacitance than the symmetric AC system. The optimized  $MnO_x$ -CNT 9-1 system on the other hand maintained 76% of the cell initial capacitance after 500 cycles; the intermediate capacitance retention can be ascribed to the composite charge storage characteristics of the hybrid capacitor. Figure 6.4f illustrates the energypower characteristics of the optimized hybrid capacitor compared to different capacitive systems reported in the literature. The optimized asymmetric capacitor is able to deliver a maximal energy density of 30.3 Whkg<sup>-1</sup>, which is almost an order higher than both the symmetric capacitors. Detailed symmetric and asymmetric capacitor comparison is tabulated in Table 6S1. Furthermore, it is noteworthy that the decay in the energy density of the hybrid capacitor is not as pronounced as the power density of the system progresses; the latter is ascribed to the good rate handling of the optimized hybrid

capacitor. The excellent energy-power characteristics are attributed to the much wider potential window exhibited by the hybrid capacitor.

Figure 6.5 depicts a radar chart comparing different characteristics of the two symmetric systems as well the optimized  $MnO_x$ -CNT 9-1//AC capacitor, where all the factors have been normalized with the actual characteristic value exhibited by the hybrid capacitor. The maximal power density was calculated using equation (6.4):

$$PD_{max} = \frac{V^2}{4ESR * M} \tag{6.4}$$

where  $PD_{max}$  symbolizes the maximum power density, V is the cell voltage, ESR is the equivalent series resistance computed from the linear iR drop in the GCD curves, and M is the total mass of the active material of the anode and the cathode. The values for all the capacitors are tabulated in Table 6S1. The hybrid capacitor was superior to both the AC and MnO<sub>x</sub>-CNT 9-1 based symmetric capacitors in terms of capacitance, voltage window, and energy and power densities. However, in terms of capacitive retention, the hybrid capacitor was still inferior to the AC symmetric system (~100%), which can be ascribed to the combination of redox reactions and double layer charge storage in the asymmetric system. It should be noted that the capacitors reported in this work have been normalized with the total anode and cathode masses and for actual deliverables, a packaging factor should be considered. For a factor of 1/3, the optimal asymmetric capacitor can deliver a maximal energy density of 10 Whkg<sup>-1</sup>, which is still higher than commercial EDLCs.



Figure 6.5: A radar chart depicting the electrochemical performance of the symmetric  $MnO_x$ -CNT 9-1//  $MnO_x$ -CNT 9-1 capacitor, the symmetric AC//AC capacitor and the asymmetric  $MnO_x$ -CNT 9-1//AC capacitor evaluated for mass ratio (MR) 1:2.6; the characteristics have been normalized by the values exhibited by the asymmetric capacitor and the red numbers next to axes labels depict the true values corresponding to the asymmetric capacitor.

## 6.4 Conclusions

In this work, three different manganese oxide compositions: i) pristine  $(MnO_x)$ , ii) with 10% carbon nanotube additive  $(MnO_x-CNT 9-1)$ , and iii) 20% CNT additive  $(MnO_x-CNT 8-2)$  were synthesized using electrostatic spray deposition (ESD) and investigated as electrochemical capacitor electrodes in neutral aqueous media. The  $MnO_x-CNT 9-1$  composition exhibited superior electrochemical performance as

compared to both the pristine  $MnO_x$  and the  $MnO_x$ -CNT 8-2 composite films. The  $MnO_x$ -CNT 9-1 electrodes exhibited a high specific capacitance of 281 Fg<sup>-1</sup> for a current density of 0.2Ag<sup>-1</sup> and were able to retain 87.4% of the maximal capacitance after 1000 cycles. Upon verifying the viability of the ESD derived  $MnO_x$ -CNT 9-1 films, the latter were used in asymmetric configuration comprising activated carbon (AC) counter electrodes. For the different mass ratios investigated, the ratio with 1:2.4, with the latter corresponding to the mass of AC, exhibited the best electrochemical characteristics reaching a voltage of 2V even in aqueous media. The asymmetric capacitor exhibited superior energy-power trade-off when compared to both the control groups consisting of symmetric AC//AC capacitor as well as the  $MnO_x$ -CNT 9-1//MnO\_x-CNT 9-1 capacitor. The enhancement in the electrochemical characteristics is attributed to the combination of the wider electrochemical potential window as well as the high capacitance of the ESD based MnO\_x-CNT 9-1 electrode.

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# 7. ON-CHIP ASYMMETRIC MICROSUPERCAPACITORS COMBINING REDUCED GRAPHENE OXIDE AND MANGANESE OXIDE FOR HIGH ENERGY-POWER TRADEOFF

#### 7.1 Introduction

With the technological impetus of going "micro", it is imperative to create small-scale energy devices that can effectively power such miniaturized devices. Given the existing myriad of minuscule systems such as implantable medical devices (IMDs), wireless sensors, smart cards, personal electronics, etc. that typically require power in the range of several  $\mu W$  to several hundred mW, it is essential to shrink the sizes of the energy storage components further. Currently, the majority of the micro-devices rely on batteries to provide the required energy and power. However the relatively poor power-handling ability and limited lifetime of batteries hinder their applicability to systems that require high current spikes [1]. As an alternative to batteries, energy harvesters hold significant promise for sustainable environments; however, the currently existing energy harvester systems require an energy storage device in tandem [1]. Electrochemical capacitors, also known as supercapacitors (SCs), on the other hand, can provide high powers along with long cycle lives. Based on the charge storage mechanisms, SCs can be divided into two major categories - electrochemical double layer capacitors (EDLCs) and redox or "pseudocapacitors". The former rely on the adsorption of ions at the electrode/electrolyte interface and typically comprise different forms of carbons, whereas the latter store charges in a faradaic/redox manner with fast and reversible redox reactions and encompass different transition metal oxides (TMOs) and conducting polymers [2]. Typically, pseudocapacitive materials exhibit larger specific capacitances, whereas double

layer type materials exhibit better rate handling capability and superior cycle longevity [2].

Quite akin to their larger variants, miniaturized electrochemical energy storage (EES) systems can be connected externally for peak power and energy delivery; nevertheless, it is desirable for the next generation micro-power devices to be *single standalone* systems that can provide with simultaneous supply of high energy and high power. One of the strategies for achieving the latter is the *asymmetric or hybrid* supercapacitor design. Such systems typically combine a redox-type electrode along with a counter double layer capacitive electrode in one cohesive system and benefit from the larger capacity of the redox material and the superior kinetics and cycle life of the double layer material. Several asymmetric systems have been reported in the literature including pseudocapacitive metal oxides such as ruthenium oxide  $(RuO_2)$  [3], manganese oxide  $(MnO_x)$  [4-8], nickel oxide  $(NiO_x)$  [9, 10], as well as lithium insertion materials (lithiumion capacitors) including pre-lithiated carbons [11-13], lithium titanate ( $Li_4Ti_5O_{12}$ ) [14-17], and lithium iron phosphate (LiFePO<sub>4</sub>) [18, 19] coupled with different carbons. While the asymmetric design offers significant promise from materials perspective, the "inplane interdigital design" offers a multitude of advantages from an architectural standpoint. For instance, having alternating digits of anode and cathode materials in close proximity can shorten the ion-transport pathways and can effectively enhance the rate capability of the on-chip systems. As opposed to the conventional two-dimensional (2D) thin-film design, the interdigital architecture allows for larger accessibility of the electrodes as the sides of the microelectrodes are exposed to the electrolyte [1]. The enhanced accessibility of the electrodes is especially well-suited for layered 2D materials,
where the electrolyte ions can have facile access between the layers of the material by having the electrodes side-by-side [1].

One of the widely investigated 2D layered materials is graphene, which is essentially a one-atom thick sp<sup>2</sup> hybridized carbon sheet [2]. Owing to its high theoretical specific surface area (~2600 m<sup>2</sup>g<sup>-1</sup>), exceptional electronic conductivity, and superior mechanical strength, graphene has been extensively explored as an EDLC material [2, 20-22].Despite the phenomenal properties of graphene, it is however challenging to fully realize the theoretical values, given the high degree of graphene sheet restacking [2, 12]. Furthermore, the hydrophobic nature of graphene makes it challenging to effectively disperse it in solvents. One of the derivatives of graphene is graphene oxide (GO), which in essence is graphene decorated with oxygen-containing groups on both the basal planes and the edges [23, 24]. The oxygen functionality makes GO hydrophilic, which can assist in its effective dispersion in organic solvents as well as enhance the interaction with the electrolyte [25]. However, the oxygenated groups make GO insulating and for SC applications, effective reduction of GO is desired in order to utilize the electronic properties of graphene. Typically, GO is reduced to reduced graphene oxide (rGO) using strong reducing agents like hydrazine, which could be both cost-prohibitive and damaging to the environment [25]. As an alternative to chemical reduction, electrophoretic deposition (EPD) offers the possibility to effectively reduce GO without the need for any additional reducing agents [26]; An et al [27] noted that the rGO films synthesized via EPD exhibited much superior electrical conductivity over the parent GO papers (1.43 x  $10^4$  Sm<sup>-1</sup> as opposed to 0.53 x  $10^{-3}$  Sm<sup>-1</sup>). EPD is a thin-film synthesis method, which essentially involves the movement of charged particles in a colloidal

suspension under the influence of an electric field [26, 28]. Given the feasibility to simultaneously integrate and reduce GO using EPD, the latter method was utilized to fabricate the rGO microelectrodes for the microsupercapacitors (MSCs) for this work.

As pseudocapacitive or redox materials, manganese oxides  $(MnO_x)$ , in all polymorphs, have been widely studied owing to their high theoretical specific capacitance, environmental benignity, large abundance and low cost [29-32]. Different asymmetric configurations utilizing MnO<sub>x</sub> have been investigated for MSC applications including activated carbons (AC) [33], carbon nanotubes (CNT) [34], laser scribed graphene (LSG) [35], as well as graphene quantum dot (GQD) [36] counter electrodes. In this work, MnO<sub>x</sub> was electrochemically deposited onto gold micro-current collectors as the cathode component of the asymmetric MSCs against the electrophoretically prepared rGO counter microelectrode. The optimized asymmetric rGO//MnO<sub>x</sub> MSC was able to deliver areal capacitances as high as 1.63 mFcm<sup>-2</sup>, equivalent to a stack/volumetric capacitance of 3.6 Fcm<sup>-3</sup> as well as volumetric energy and power densities of 1.02 mWhcm<sup>-3</sup> and 3441 mWcm<sup>-3</sup>, much superior to those of both the symmetric  $MnO_x//MnO_x$  and rGO//rGO systems. The excellent energy-power tradeoff and high specific capacitance of the asymmetric capacitor is attributed to the synergy between the pseudocapacitive MnO<sub>x</sub> component and the double layer rGO component in addition to the in-plane interdigital microelectrode design.

#### 7.2 Materials and Methods

#### 7.2.1 Fabrication of the interdigital gold micro-current collectors

In order to construct the interdigital gold micro-current collectors, conventional photolithography and lift-off methods were used. A schematic illustration has been

shown in Figure 7.1 (Step I-Step IV). First, AZ 5214 was spun-coated on a 4" Si/SiO<sub>2</sub> (100) wafer at a speed of 5000 rpm for 30 seconds. After the spin coating process, a soft bake was carried out for 1 minute at a temperature of 110°C on a leveled hot plate. After the bake process, ultraviolet exposure was carried out using an OAI mask aligner with a UV dose of 230 mJcm<sup>-2</sup>. Following the expose step, a develop step was carried out using AZ 300 MIF for ~45 seconds. After the develop step, a de-scum step was carried out using an O<sub>2</sub> plasma at a flow rate of 60 sccm and a pressure of 400 mTorr for 30 seconds using reactive ion etching (RIE). Following the patterning of the photoresist, metallization process (Ti/Au (20/300 nm)) was carried out using e-beam evaporation with a CHA evaporator. After the metallization process, lift-off was carried out in order to get rid of sacrificial photoresist using acetone and mechanical agitation, followed with isopropyl alcohol rinsing and N<sub>2</sub> drying. Finally, a 30s O<sub>2</sub> plasma treatment at 400 mTorr was carried out in order to get rid of any organic residues. The typical width of the gold fingers was 100 µm with an interdigital gap of 100 µm and a length of 8800 µm. Each electrode comprised 18 fingers, resulting in a total of 36 fingers for a single device and a total finger area of  $0.3168 \text{ cm}^2$  (~0.32 cm<sup>2</sup>), whereas the effective footprint area of the device (including finger gaps) was ~0.66 cm<sup>2</sup>. Unless otherwise mentioned, the electrochemical parameters were normalized with the finger area in this work.



Figure 7.1: Schematic illustration of the asymmetric rGO//MnO<sub>x</sub> microsupercapacitor construction

# 7.2.2 Active Material Integration

After constructing the gold micro-current collectors, the active materials (rGO and  $MnO_x$ ) were integrated onto the current collectors using electrodeposition (electrochemical and electrophoretic deposition methods). For the symmetric MnOx//MnOx microsupercapacitor, a three-electrode setup was used where the interdigitated gold current collectors functioned as the working electrode, and an Ag/AgCl and a platinum coil functioned as the reference and counter electrode, respectively. An anodic current of 0.5 mAcm<sup>-2</sup> was applied for 20 minutes (equivalent to an applied charge of 0.6 Ccm<sup>-2</sup>) in an electrolyte solution containing 0.2M manganese acetate (Sigma Aldrich) and 0.2M Na<sub>2</sub>SO<sub>4</sub> (Sigma Aldrich). After the deposition process,

the electrodes were washed with DI water and dried overnight before being used for further characterization. For the rGO deposition for the symmetric rGO//rGO microsupercapacitor, a suspension containing single layer graphene oxide (SLGO, Cheap Tubes Inc., USA) and C<sub>2</sub>H<sub>5</sub>OH: DI water (90:10, v:v) in a concentration of 1 mgml<sup>-1</sup> was used for the EPD process after 1h ultrasonication. An electric field of ~40Vcm<sup>-1</sup> was applied between the gold current collectors (working electrode) and a platinum coil (counter electrode); small amounts of MgCl<sub>2</sub> (0.1 mgml<sup>-1</sup>) were added to the GO solution in order to enhance the conductivity and facilitate the EPD process. For the asymmetric microsupercapacitors (schematic illustration shown in Figure 7.1 Step V), three different depositions of manganese oxide comprising anodic charges of 0.6, 0.9 and 1.2 Ccm<sup>-2</sup> were evaluated against a 5 min deposition of rGO.

#### 7.2.3 Material Characterization

X-ray diffraction (XRD) studies on the electrochemically deposited  $MnO_x$  were carried out using a Siemens D5000 Diffractometer with Cu-K $\alpha$  radiation. For spectroscopic characterization on the electrochemically deposited  $MnO_x$  and the electrophoretically rGO films, Fourier Transform Infrared (FTIR) studies were carried out using a JASCO FTIR-4100 equipped with an attenuated total reflectance (ATR) accessory. The top and the cross sectional views of the symmetric and asymmetric microsupercapacitors were investigated using scanning electron microscopy (SEM) with a JEOL SEM 6330 in the secondary electron imaging (SEI) mode.

#### 7.2.4 Electrochemical Characterization

The electrochemical characterization on the symmetric rGO//rGO, MnO<sub>x</sub>//MnO<sub>x</sub>, as well as the asymmetric rGO//MnO<sub>x</sub> microsupercapacitors was carried out in a aqueous electrolyte containing 1M Na<sub>2</sub>SO<sub>4</sub> using a VMP3 Potentiostat (Princeton, Bio-Logic). Two-electrode studies were carried out for both the symmetric and asymmetric configurations and all the experiments were carried out room temperature. All the electrochemical parameters were normalized with the total finger/active material area (~0.32 cm<sup>2</sup>) and the systems were evaluated using cyclic voltammetry (CV), galvanostatic charging and discharging (GCD), as well as electrochemical impedance spectroscopy (EIS) measurements.

#### 7.3 **Results and Discussion**

# 7.3.1 Spectroscopic, crystallographic and microstructural characterization performed on the manganese oxide and rGO microelectrodes

The FTIR spectra of the starting GO powders and the EPD reduced GO (rGO) is shown in Figure 7.2. The broad absorption peak centered around 3378 cm<sup>-1</sup> in the GO powder is the characteristic IR band position from the OH stretching vibrations [37, 38] , whereas the peaks at 1727 cm<sup>-1</sup>, 1624 cm<sup>-1</sup>, 1377 cm<sup>-1</sup>, 1234 cm<sup>-1</sup>, and 1083 cm<sup>-1</sup> are attributed to C=O stretching [38], aromatic C=C stretching [39], carboxyl [40], epoxide C-O-C or phenolic C-O-H stretching vibrations [40], C-O stretching in epoxy or alkoxy groups [40], respectively. It is worth noting that the intensity from the hydroxyl groups is substantially mitigated in the EPD based rGO film, indicating effective reduction of GO during electrophoresis. Furthermore, the intensity of the other functional groups signaling the presence of oxygen was reduced; the peak at 1615 cm<sup>-1</sup> was however quite prevalent in the rGO spectrum, signaling the presence of aromatic C=C stretching [39], which is from the parental graphitic skeleton.



Figure 7.2: The FTIR spectra of the starting graphene oxide powders and the EPD reduced graphene oxide films

The Fourier transform infrared (FTIR) spectrum of the electrodeposited  $MnO_x$  is shown in Figure 7.3a; the peaks located around 510, 526, and 581 cm<sup>-1</sup> as ascribed to the Mn-O vibrations from the Mn-O octahedra and are consistent with previous reports [41, 42]. The XRD pattern of the electrochemically deposited manganese oxide films is shown in Figure 7.3b. The material is of low degree of crystallinity; however the faint peaks present in the diffraction pattern are ascribed to  $\alpha$ -MnO<sub>2</sub> (JCPDS Card Number: 00-044-0141). The peaks at 18.1°, 28.8°, 37.5°, 46.1°, 56.9°, and 65.2° are indexed as (hkl) plane orientations of (200), (310), (211), (321), (431), and (002), respectively of  $\alpha$ -MnO<sub>2</sub> phase. However, owing to the poor degree of crystallinity the manganese oxide is referred to as MnO<sub>x</sub>.



Figure 7.3: a) FTIR spectrum and b) the X-ray diffraction (XRD) pattern of the electrochemically deposited MnO<sub>x</sub> films.

The microstructure of the MnO<sub>x</sub>-rGO coated asymmetric capacitors is shown in Figure 7.4a; as evident the system comprised alternating fingers of MnO<sub>x</sub> and rGO electrodes. Figure 7.4b displays the cross-sectional view of the rGO electrode – the structure consisted of graphene layers as expected from the parent graphene oxide powders (SEM micrograph shown in Supplementary file Figure 7S1) and the rGO film had an average thickness of ~4.5  $\mu$ m. The top view of the rGO microelectrode is illustrated in Figure 7.4c; as evident the graphene sheets were well dispersed, thereby confirming effective sheet assembly during the EPD process. Figures 7.4d through 7.4f show the cross sectional images of the MnO<sub>x</sub> films deposited at anodic charges of 0.6, 0.9

and 1.2 Ccm<sup>-2</sup> and the corresponding morphologies of the films are exhibited as Figures 7.4g through 7.4i. As expected, the  $MnO_x$  film deposited for an anodic charge of 0.6 Ccm<sup>-2</sup> was the thinnest amongst the films deposited for different charges. The average film thicknesses for the  $MnO_x$  microelectrodes were ~0.38, ~0.81, and ~0.95 µm for deposition rates of 0.6, 0.9 and 1.2 Ccm<sup>-2</sup>, respectively. The microstructure of the different  $MnO_x$  films was similar and comprised homogeneously dispersed  $MnO_x$  nanoparticles.



Figure 7.4: a) SEM micrograph of the interdigitated rGO and  $MnO_x$  microelectrodes; b) cross sectional view and c) top view of the rGO coated microelectrodes; d-f) cross sectional view of the  $MnO_x$  microelectrodes deposited at 0.6, 0.9 and 1.2Ccm<sup>-2</sup>,

respectively; g-i) top-view of the  $MnO_x$  microelectrodes deposited at 0.6, 0.9 and  $1.2Ccm^{-2}$ , respectively.

### 7.3.2 Electrochemical Characterization of the symmetric rGO//rGO, MnO<sub>x</sub>//MnO<sub>x</sub>, and asymmetric rGO-MnO<sub>x</sub> microsupercapacitors

#### 7.3.2.1 Electrochemical evaluation of the symmetric rGO//rGO MSCs

The electrochemical characteristics of the rGO//rGO symmetric MSC are shown in Figure 7.5. The typical CV curves of the symmetric rGO//rGO MSCs at scan rates of 1, 2, 5, 10, and 20 Vs<sup>-1</sup> are shown in Figure 7.5a. As evident, even at a high scan rate of 20Vs<sup>-1</sup> <sup>1</sup>, the curves maintain predominantly rectangular shape, which is indicative of predominantly capacitive charge storage. The typical GCD curves of the rGO//rGO MSCs at different current rates are shown in Figure 7.5b; the discharge areal capacitances were estimated as ~252, 223, and 172  $\mu$ Fcm<sup>-2</sup> at current densities of 0.32, 0.64, and 1.28 mAcm<sup>-2</sup>, respectively. Figure 7.5c shows the typical Nyquist plots of the rGO//rGO MSCs scanned for a frequency range of 100000-0.01Hz; as evident the curves comprised a depressed semicircular region in the high frequency regime followed by a linear slope in the low-frequency region, indicating typical capacitive behavior; the diameter of the semicircular region was ~0.0035 k $\Omega$ cm<sup>2</sup> (~11 $\Omega$ ), indicating very low charge transfer resistance; the x-axis intercept was  $\sim 8\Omega$  mainly due to solution resistance. The typical cycling behavior of the rGO//rGO microsupercapacitor is illustrated in Figure 7.5d; the capacitor exhibited very stable cycling with a capacitive retention of ~97% after 100 cycles.



Figure 7.5: Typical CV curves (scanned at 1-20Vs<sup>-1</sup>); b) GCD curves at different current densities; c) EIS spectra (between 100000-0.01Hz) and d) cycle life of the symmetric rGO- rGO microsupercapacitor

#### 7.3.2.2 Electrochemical characterization of the $MnO_x//MnO_x$ symmetric MSCs

The electrochemical characteristics of the  $MnO_x//MnO_x$  symmetric MSCs are shown in Figure 7.6. The typical cyclic voltammograms (CV) of the symmetric  $MnO_x//_{MnOx}$  MSCs at scan rates of 1, 2, 5, 10, and 20 Vs<sup>-1</sup> are shown in Figure 7.6a. As evident, even at a high scan rate of  $20Vs^{-1}$ , the curves exhibit predominantly capacitive shape with some depressed redox peaks around 0.5-0.6V, which can be attributed to the pseudocapacitive charge storage characteristics of the manganese oxide active material. The typical GCD curves at different current densities are shown in Figure 7.6b; the GCD curves display triangular sloping-desloping behavior for a voltage range of 0-0.8V with some curvature. The discharge areal capacitances were estimated as 147, 96, 64  $\mu$ Fcm<sup>-2</sup> at current densities of 0.16, 0.32, 0.64 mAcm<sup>-2</sup>, respectively. Figure 7.6c shows the typical Nyquist plots of the freshly prepared MnO<sub>x</sub>//MnO<sub>x</sub> MSCs scanned for a frequency range of 100000-0.01Hz. As evident the curves comprised a depressed semicircular region in the high frequency regime followed by a linear slope in the low-frequency region, indicating typical redox behavior. The diameter of the semicircular region was ~0.02 k $\Omega$ cm<sup>-2</sup> (~60 $\Omega$ ) indicating low charge-transfer resistance. The typical cyclability and the capacitance retention of the MnO<sub>x</sub>//MnO<sub>x</sub> MSC are shown in Figure 7.6d; ~58% of the initial capacitance was retained after 1000 cycles. The drop in capacitance has been observed in previous reports documenting the use of MnO<sub>x</sub> for symmetric MSCs [43].



Figure 7.6: a) Typical CV curves (scanned at 1-20Vs<sup>-1</sup>); b) GCD curves at different current densities; c) EIS spectra (between 100000-0.01Hz) and d) cycle life of the symmetric MnO<sub>x</sub>//MnO<sub>x</sub> microsupercapacitor

#### 7.3.2.3 Electrochemical evaluation of the asymmetric $MnO_x//rGO$ MSCs

As seen in the previous sections, the areal capacitance of rGO//rGO MSC was higher than that of the  $MnO_x//MnO_x$  MSC (~252 µFcm<sup>-2</sup> as opposed to 96 µFcm<sup>-2</sup> at a current density of 0.32 mAcm<sup>-2</sup>), as a result of which, three different MnO<sub>x</sub> thicknesses (MnO<sub>x</sub> deposited at 0.6, 0.9, and 1.2 Ccm<sup>-2</sup>) were evaluated for asymmetric systems in order to investigate the optimal energy-power tradeoff. The asymmetric MSCs were designated as rGO//MnO<sub>x</sub>-0.6C, rGO//MnO<sub>x</sub>-0.9C and rGO//MnO<sub>x</sub>-1.2C, where the

suffix symbolizes the charge used for MnO<sub>x</sub> deposition. The detailed electrochemical characteristics of the asymmetric rGO//MnO<sub>x</sub>-0.9C MSC are shown in Figure 7.7, whereas the electrochemical characteristics of the rGO//MnO<sub>x</sub>-0.6C and rGO//MnO<sub>x</sub>-1.2C MSCs can be found in the supplementary file (Figure 7S2). The typical CV curves of asymmetric rGO//MnO<sub>x</sub>-0.9C MSC at different scan rates are shown in Figure 7.7a. As evident the current response from the asymmetric rGO//MnO<sub>x</sub>-0.9C MSC was much superior to that of both the symmetric rGO//rGO and MnO<sub>x</sub>//MnO<sub>x</sub> capacitors evaluated previously. Furthermore, composite charge storage characteristics are evident from the shape of the CV curves. GCD curves of the asymmetric rGO//MnO<sub>x</sub>-0.9C MSC at different current densities are shown in Figure 7.7b; the discharge areal capacitances were estimated as 1.63, 1.59, 1.29, and 1.2 mFcm<sup>-2</sup> at current densities of 0.32, 0.64, and 1.28, and 2.56 mAcm<sup>-2</sup>, respectively. The Nyquist plot of the asymmetric rGO//MnO<sub>x</sub>-0.9C MSC scanned for a frequency range of 100000-0.01Hz is shown in Figure 7.7c and the inset depicts the zoomed-in high-frequency response of the MSC. The diameter of semicircular region was ~0.07 k $\Omega$ cm<sup>-2</sup> (~218 $\Omega$ ), higher than both the symmetric rGO//rGO and  $MnO_x//MnO_x$  MSCs. The relatively higher charge-transfer resistivity can be attributed to the larger thickness of the manganese oxide component on the asymmetric MSC. The typical cycling performance of the asymmetric rGO//MnO<sub>x</sub>-0.9C MSC is shown in Figure 7.7d; the capacitor retained a capacitance of ~85% after 1000 cycles, which is much superior to that of the  $MnO_x//MnO_x$  MSC.



Figure 7.7: a) Typical CV curves (scanned at 5-20Vs<sup>-1</sup>); b) GCD curves at different current densities; c) EIS spectra (between 100000-0.01Hz) and d) cycle life of the asymmetric rGO//MnO<sub>x</sub>-0.9C microsupercapacitor

The comparitive rate capability of the different MSCs evaluated in this work is shown in Figures 7.8a and 7.8b. While areal normalization is essential in terms of practicality of miniaturized devices, stack calculations can provide with more insight into the intrinsic properties of the materials utilized for the MSC construction. The stack capacitances of all the asymmetric MSCs as well as the rGO//rGO MSC were normalized with the thickness of the rGO film, whereas the stack parameters for the MnO<sub>x</sub>//MnO<sub>x</sub> symmetric capacitor were normalized with the thickness of the MnO<sub>x</sub> film. Figures 7.8a and 7.8b, it is clear that the asymmetric rGO//MnO<sub>x</sub>-0.6C, rGO//MnO<sub>x</sub>-0.9C, and rGO//MnO<sub>x</sub>-1.2C MSCs as well as the symmetric rGO//rGO MSC followed the same trend for both the areal and stack capacitances with the highest values for rGO//MnO<sub>x</sub>-0.9C followed by the rGO//MnO<sub>x</sub>-1.2C, rGO//MnO<sub>x</sub>-0.6C and the rGO//rGO MSC (in that order). The only discrepancy in stack and areal capacitance was exhibited by the symmetric  $MnO_x$ //MnO<sub>x</sub> system, which can be explained by the relatively lower thickness of the  $MnO_x$  as compared to the rGO film. The stack capacitance of the  $MnO_x$ //MnO<sub>x</sub> system fades quickly with increasing current, which can be attributed to the use of pristine  $MnO_x$  as electro-active material without the addition of any conducting additives.



Figure 7.8: Rate capability of the MnO<sub>x</sub>//MnO<sub>x</sub>, rGO//rGO, rGO//MnO<sub>x</sub>-0.6C, rGO//MnO<sub>x</sub>-0.9C, and rGO//MnO<sub>x</sub>-1.2C MSCs in terms of a) areal and b) stack capacitances.

The areal energy and power densities of the MSCs were computed using equations (7.1) and (7.2):

$$ED_{areal} = \frac{1}{2*3600} C_{areal} * V^2 \tag{7.1}$$

$$PD_{areal} = \frac{ED_{areal}}{t/3600}$$
(7.2)

where  $ED_{areal}$  (Whcm<sup>-2</sup>) and  $PD_{areal}$  (Wcm<sup>-2</sup>) refer to areal energy and power density, respectively,  $C_{areal}$  refers to the areal capacitance (Fcm<sup>-2</sup>), V is the voltage window (V), and t is the discharge time (s). The stack energy and power densities were calculated by normalizing the  $ED_{areal}$  and  $PD_{areal}$  with the rGO or MnO<sub>x</sub> thickness, depending upon the higher thickness. The areal energy-power trade-off between all the MSC devices constructed in this work has been depicted in a Ragone chart (Figure 7S3); the asymmetric rGO//MnOx-0.9C MSC was able to deliver an energy density of 0.274  $\mu$ Whcm<sup>-2</sup> at a power density of 193.6  $\mu$ Wcm<sup>-2</sup> (pertaining to a capacitance of 1.63 mFcm<sup>-</sup> <sup>2</sup>) which is higher than other reports documenting on-chip  $MnO_x$  based systems [32, 35] but lower than reports on carbon onions and conducting polymers [44, 45]. A comparative Ragone chart depicting the stack energy and power densities of the asymmetric rGO//MnOx-0.9C MSC along with other commercial EES [44] as well as other MSC systems reported in the literature is shown as Figure 7.9. The asymmetric MSC was able to deliver a maximal stack energy density of 1.02 mWhcm<sup>-3</sup> at a power density of 0.22 Wcm<sup>-3</sup>, and a maximal power density of 3.44 Wcm<sup>-3</sup> at which an energy density of 0.45 mWhcm<sup>-3</sup> was maintained, resulting in a time constant of 0.47s. It can be seen that the hybrid MSC is well-placed in between the energy-power characteristics of thin film lithium-ion battery and commercial supercapacitors. It should be noted that the

device characteristics have been reported in terms of volume of the interdigitated fingers and the values will diminish taking packaging into account. While the aqueous asymmetric MSC displays high energy and power tradeoff, further enhancement in electrochemical performance is expected with the use of high voltage electrolytes, advanced hierarchical materials, as well as more balanced hybrid designs, which are subjects of future works.



Figure 7.9: Ragone plot depicting the volumetric energy and power densities exhibited by the asymmetric rGO//MnO<sub>x</sub>-0.9C MSC in comparison with thin film lithium ion battery, commercial supercapacitors and electrolytic capacitors along with carbon onion based microsupercapacitors (Reproduced with permission from reference 44) and other data points taken from the literature [32, 46, 47, 48].

#### 7.4 Conclusions

In summary, interdigitated microsupercapacitors were fabricated using photolithography, lift-off and electrodeposition methods. Symmetric MnO<sub>x</sub>//MnO<sub>x</sub>, rGO//rGO as well as asymmetric rGO//MnOx microsupercapacitors with three different  $MnO_x$  thicknesses were constructed and evaluated. The asymmetric microsupercapacitor with the  $MnO_x$  film deposited at a charge of 0.9 Ccm<sup>-2</sup> displayed the optimal energypower trade-off much superior to that of both the symmetric and well as the other asymmetric configurations. The rGO//MnO<sub>x</sub> 0.9C microsupercapacitor exhibited a high stack energy density of 1.02 mWhcm<sup>-3</sup> and a maximal power density of 3.44 Wcm<sup>-3</sup> both of which are comparable with thin film batteries and commercial supercapacitors in terms of volumetric energy and power densities, respectively. The high energy-power trade-off of the device is attributed to the synergistic effects of utilizing double layer and pseudocapacitive charge storage mechanisms along with in-plane interdigital design within one optimized micro-device.

#### 7.5 References

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#### 8. CONCLUSIONS AND OUTLOOK

#### 8.1 Summary

This dissertation presents design, construction, and evaluation of both "scale-up" and miniaturized asymmetric/hybrid supercapacitors. Utilizing redox and double-layer charge storage mechanisms within one system is an attractive solution to enhance the energy density of electrochemical capacitors. However, several research challenges are posed with the seemingly simple hybridization approach, which include relatively inferior kinetics and cycle life of the redox electrode, and lower specific capacitance of the double layer electrode. Several routes have been adopted in order to maximize the performance of the hybrid capacitors synthesized in this dissertation and the major findings are summarized as follows:

In the first part, hybrid capacitors comprising ESD based rGO-CNT composite cathode and an anatase  $TiO_2-Li_4Ti_5O_{12}$  anode was constructed and analyzed. The cathode and anode were first analyzed as working electrodes against a lithium counter electrode and were able to deliver discharge capacities of ca. 63 mAhg<sup>-1</sup> and 95 mAhg<sup>-1</sup> with good reversibility and cycling. The full Li-HEC cells were able to deliver a maximum energy density of 33.35 Whkg<sup>-1</sup> and a maximum power density of 1207.4 Wkg<sup>-1</sup>, with specific energy ranging between 33.35-15.09 Whkg<sup>-1</sup> at power densities of 83.55-1207.4 Wkg<sup>-1</sup>, where all the cell parameters were normalized with the total anode and cathode masses. Furthermore, the Li-HEC cells were able to retain ~77% of capacitance retention after 100 cycles. The superior energy-power cell characteristics were attributed to the porous electrode structure and the utilization of organic electrolyte which allows for a wider electrochemical potential window.

In the second part of the dissertation, manganese oxide films were synthesized using electrostatic spray deposition (ESD) and characterized as pseudocapacitive materials for electrochemical capacitor applications in neutral aqueous media. The initial phase synthesized was the relatively insulating hausmannite-Mn<sub>3</sub>O<sub>4</sub>, which partially transformed into the conducting birnessite-MnO<sub>2</sub> upon electrochemical cycling, resulting in an enhanced gravimetric capacitance from 72  $\text{F}\cdot\text{g}^{-1}$  to 225  $\text{F}\cdot\text{g}^{-1}$ . Furthermore, MnO<sub>x</sub>-MEs were created by combining bottom-up ESD approach and top-down C-MEMS approach. In a two-electrode setup, the MnO<sub>x</sub>-MEs were able to deliver geometric specific capacitances as high as 0.055  $\text{F}\cdot\text{cm}^{-2}$ , and maximal volumetric energy and power densities of 0.51 mWh·cm<sup>-3</sup> and 28.3 mW·cm<sup>-3</sup>, respectively. The excellent areal capacitance and the high stack energy density of the MnO<sub>x</sub>-MEs were attributed to the pseudocapacitive MnO<sub>x</sub> as well as the three-dimensional architectural framework of the micro-pillars. The feasibility of using ESD for high gravimetric thin-film manganese oxide films and high areal capacitance 3D microelectrodes was therefore established.

To further examine the utility of manganese oxide films in an asymmetric configuration, three different manganese oxide compositions: i) pristine ( $MnO_x$ ), ii) with 10% carbon nanotube additive ( $MnO_x$ -CNT 9-1), and iii) 20% CNT additive ( $MnO_x$ -CNT 8-2) were synthesized using electrostatic spray deposition (ESD) and investigated as electrochemical capacitor electrodes in neutral aqueous media. The  $MnO_x$ -CNT 9-1 composition exhibited superior electrochemical performance as compared to both the pristine  $MnO_x$  and the  $MnO_x$ -CNT 8-2 composite films. The  $MnO_x$ -CNT 9-1 electrodes exhibited a high specific capacitance of 281 Fg<sup>-1</sup> for a current density of 0.2Ag<sup>-1</sup> and were able to retain 87.4% of the maximal capacitance after 1000 cycles. Upon verifying the

viability of the ESD derived  $MnO_x$ -CNT 9-1 films, the latter were used in asymmetric configuration comprising activated carbon (AC) counter electrodes. For the different mass ratios investigated, the ratio with 1:2.6, with the latter corresponding to the mass of AC, exhibited the best electrochemical characteristics reaching a voltage of 2V even in aqueous media. The asymmetric capacitor exhibited superior energy-power trade-off when compared to both the control groups consisting of symmetric AC//AC capacitor as well as the  $MnO_x$ -CNT 9-1//MnO<sub>x</sub>-CNT 9-1 capacitor. The enhancement in the electrochemical characteristics was attributed to the combination of the wider electrochemical potential window as well as the high capacitance of the ESD based  $MnO_x$ -CNT 9-1 electrode.

To extend the applicability of asymmetric systems to on-chip miniaturized devices, asymmetric microsupercapacitors were constructed using electrodeposited manganese oxide (MnO<sub>x</sub>) as the positive electrode and electrophoretically deposited reduced graphene oxide (rGO) as the negative electrode on patterned interdigitated gold microcurrent collectors. Symmetric  $MnO_x//MnO_x$ , rGO//rGO as well as asymmetric rGO//MnO<sub>x</sub> microsupercapacitors with three different  $MnO_x$  thicknesses were constructed and evaluated. The asymmetric microsupercapacitor with the  $MnO_x$  film deposited at a charge of 0.9 Ccm<sup>-2</sup> displayed the optimal energy-power trade-off much superior to that of both the symmetric and well as the other asymmetric configurations. The rGO//MnO<sub>x</sub> 0.9C microsupercapacitor exhibited a high stack energy density of 1.02 mWhcm<sup>-3</sup> and a maximal power density of 3.44 Wcm<sup>-3</sup> both of which are comparable with thin film batteries and commercial supercapacitors in terms of volumetric energy and power densities, respectively. The high energy-power trade-off of the device is attributed to the synergistic effects of utilizing double layer and pseudocapacitive charge storage mechanisms along with in-plane interdigital design within one optimized microdevice.

#### 8.2 Future Works

Future works in the direction of this dissertation include:

- 1. *Theoretical Optimization for hybridization of redox and double layer materials:* The energy-power optimization for this dissertation is largely empirical and future works in the direction include theoretical simulations to optimize the electrochemical performance of the hybrid supercapacitors. As seen in this work, several parameters govern the final performance of the device, which *include cell voltage, electrode thickness, electrode kinetics, the anode and cathode mass ratio, the distance between the anode and the cathode*, etc. A more comprehensive and a systematic theoretical model can provide more insight into the dependence of each of the aforementioned parameters on the electrochemical performance of the final device.
- 2. Detailed investigation of performance degradation of the symmetric microsupercapacitors based on pseudocapacitive materials: As seen in Chapter 7, the symmetric microsupercapacitor based on manganese oxide degrades quickly. More detailed electron microscopy studies can be carried out to investigate the performance degradation mechanisms.
- 3. *Use of emerging advanced materials for hybrid microsupercapacitors:* This dissertation is based on popular materials (manganese oxides, nanostructured carbons, lithium insertion hosts) used for electrochemical applications. Future works along the

direction of this work include using emerging electrode materials such as MXenes [1-3], chalcogenides [4-5], etc. for microsupercapacitor applications.

4. *Packaged microsupercapacitor systems:* The electrochemical characterization for the microsupercapacitors investigated in this work was carried out in a two-electrode beaker cell setup and the energy-power values are anticipated to diminish in a fully packaged system. Future works include using *solid state electrolytes* that can facilitate packaging as opposed to liquid electrolytes or optimizing the packaging of prototype cells. Packaged systems can thereafter be used for self-powered applications along with harvesters, computing units and sensing components.

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# **APPENDIX 1: Supplemental Information for Chapter 6**

Figure 6S 1: a) cyclic voltammetry (CV) and the b) galvanostatic charge-discharge (GCD) curves of the  $MnO_x$  electrode; a) CV and the d) GCD curves of the  $MnO_x$ -CNT 8-2 electrode.



Figure 6S 2: a) Nyquist plots of the  $MnO_x$ -CNT 9-1 electrode before and after cycling; the inset depicts the equivalent circuit analyses; b)  $MnO_x$ -CNT microstructure after cycling; some cracks are visible after cycling; c) zoomed-in version of the microstructure; CNTs are conspicuous; d) long-term cycling of the  $MnO_x$ -CNT 9-1 electrode.



Figure 6S 3: a) Nyquist plot of the freshly prepared AC electrode; the inset depicts the equivalent circuit used for cell analyses; b) cycling of the AC anode; c) GCD plots of the AC anode at different current rates; d) rate capability of the AC anode.



Figure 6S 4: GCD curves of the a) symmetric AC//AC capacitor; b) symmetric  $MnO_x$ -CNT 9-1//MnO<sub>x</sub>-CNT 9-1 capacitor; c) asymmetric capacitor MR 1:2; d) asymmetric capacitor MR 1:2.4; e) asymmetric capacitor MR 1:3; f) asymmetric capacitor MR 1:4.



Figure 6S 5: a) Rate capability and b) Ragone chart of the different EC systems.

System	Capacitive retention	Cell Voltage	Cell Capacitance (Fg <sup>-1</sup> )	ED (Whkg <sup>-1</sup> )	PD (Wkg <sup>-1</sup> ) (from Ragone Chart)	PD <sub>max</sub> (Wkg <sup>-1</sup> ) (from iR calculations)
Symmetric AC//AC	~100% after 500 cycles	1.2V	28	5.6	600	888
Symmetric MnO <sub>x</sub> -CNT 9-1//MnO <sub>x</sub> - CNT 9-1	56.4% after 500 cycles	0.8V	49.9	4.4	800	1454
Asymmetric MnO <sub>x</sub> -CNT 9-1//AC (MR: 1:2.6)	76% after 500 cycles	2V	54.5	30.3	2000	4000

# Table 6S 1: Electrochemical characteristics of the symmetric AC//AC system, symmetric MnOx-CNT 9-1//MnOx-CNT 9-1 system, and the optimized asymmetric MnOx-CNT 9-1//AC system



**APPENDIX 2: Supplemental Information for Chapter 7** 

Figure 7S 1: Microstructure of the single layer graphene oxide (SLGO)


Figure 7S 2: Typical cyclic voltammograms at different scan rates of a) the asymmetric rGO//MnO<sub>x</sub>-0.6C MSC and b) the asymmetric rGO//MnO<sub>x</sub>-1.2C MSC; typical GCD curves of c) the asymmetric rGO//MnO<sub>x</sub>-0.6C MSC and d) the asymmetric rGO//MnO<sub>x</sub>-1.2C MSC; cycle life of e) the asymmetric rGO//MnO<sub>x</sub>-0.6C MSC and f) the asymmetric rGO//MnO<sub>x</sub>-1.2C MSC.



Figure 7S 3: Ragone chart of the different MSC systems.

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