

Ten questions concerning modeling of near-field pollutant dispersion in the built environment

Yoshihide Tominaga^a Ted Stathopoulos^b

^a *Niigata Institute of Technology, Kashiwazaki, Japan*

^b *Concordia University, Montreal, Canada*

Corresponding author. E-mail address: tominaga@abe.niit.ac.jp (Y. Tominaga).

Abstract

Outdoor air pollution is a major current environmental problem. The precise prediction of pollutant concentration distributions in the built environment is necessary for building design and urban environmental assessment. Near-field pollutant dispersion, involving the interaction of a plume and the flow field perturbed by building obstacles, is an element of outdoor air pollution that is particularly complex to predict. Modeling methodologies have been discussed in a wide range of research fields for many years. The modeling approaches are categorized into field measurements, laboratory (wind and water tunnel) experiments, (semi-) empirical models, and computational fluid dynamics (CFD) models. Each of these approaches has advantages and disadvantages. It is therefore important to use due consideration for the underlying theory and limitations when applying these modeling approaches. This paper considers some of the most common questions confronting researchers and practitioners in the modeling of near-field pollutant dispersion in the built environment.

Keywords

Built environment; Computational fluid dynamics (CFD); Modeling technique; Near-field; Pollutant dispersion; Wind tunnel Experimentation

1 Introduction

Outdoor air pollution is a major environmental problem. In the built environment, both the outdoor exposure of pedestrians and the indoor exposure of building inhabitants to airborne pollutants are of interest [1]. The dispersion regions for pollutants in these scenarios are rather small, comprising the vicinity of the emitting building within a few hundred meters of the source, as opposed to a region of impact over the entire neighborhood. Such dispersion processes are called “near-field” pollutant dispersion, which differ significantly in properties from far-field dispersion, in which horizontal motion prevails over vertical motion and the influence of individual buildings on the dispersion field is small. Near-field pollutant dispersion concerns local emission sources and the dispersion of these emissions for scales of individual nearby buildings up to neighborhoods. Because near-field pollutant dispersion involves the interaction of plumes with flow fields perturbed by building obstacles, the phenomenon has both meteorological and building aerodynamic aspects. Furthermore, surrounding variables, such as stack configurations, rooftop structures, and topography, have non-negligible effects on pollutant distribution.

The modeling methods used for near-field pollutant dispersion have been discussed in a wide range of research fields for many years, as reviewed in several studies, e.g. [2-14]. Approaches to the problem are categorized into field measurements, laboratory (wind and water tunnel) experiments, (semi-) empirical models, and computational fluid dynamics (CFD) techniques. Full and reduced-scale field measurements have provided valuable information, because they use “real fluids” with “real atmospheric conditions.” They have been conducted for many years, e.g. [15-18]; however, the boundary conditions of field measurements are neither controllable nor repeatable [19]. Therefore, the applicability of field data is limited for systematic and parametric studies. Laboratory experiments using wind and water tunnels are widely recognized as useful tools for predicting and analyzing pollutant dispersion, e.g. [20-21]. This approach also employs “real fluids”; however, the boundary conditions must be carefully modeled to resemble real atmospheric conditions. Because experimental conditions are highly controlled in laboratories, data obtained this way are far more suitable for parametric and systematic studies of various physical flow and dispersion processes. However, data can only be collected at a limited number of discrete positions, excepting non-intrusive area techniques, and the obtained results can suffer from similarity requirements. In cases where the buoyancy effect is not negligible, the law of

similitude becomes quite complex.

Micro-scale CFD has been used often recently, e.g. [22-27], because it can provide whole flow and dispersion field data and be performed at full scale. The method does not suffer from similarity requirements and this is a great advantage. However, CFD is very sensitive to the chosen parameters and conditions; best practice guidelines are necessary to select these constraints appropriately. Furthermore, reliable experimental data are also required to validate the accuracy and uncertainty of CFD results. CFD approaches used in pollutant dispersion modeling are normally classified into two main types: Reynolds-Averaged Navier-Stokes (NS) equations (RANS) modeling and Large Eddy Simulation (LES). RANS solves the ensemble-averaged NS equations by turbulence modeling, which aims to model the entire spectrum of the turbulent eddies. If the flow is assumed to be statistically steady, ensemble averaging is equivalent to time-averaging (steady-RANS), but for time-dependent flows, the ensemble-averaged NS equations can be solved transiently (unsteady-RANS; URANS). The most widely used turbulence model in RANS is the standard $k-\epsilon$ model (SKE) [28]. This model is well known for its robustness, economy, and reasonable accuracy for a wide range of turbulent flows. As the strengths and weaknesses of the SKE have become apparent for different flow geometries, modifications have been introduced to improve the performance of the model, e.g. [29, 30]. LES is based on the concept of separating turbulent motion into large and small-eddies. LES solves the large-eddy motion by the filtered NS equations governing the three-dimensional time-dependent motion. Turbulence modeling is only applied to small eddies by means of the so-called sub-grid scale (SGS) model. The Smagorinsky model is a well-known method commonly used for the SGS model [31]. The superiority of LES for flow around bluff bodies is based on the ability to capture the coherent structures derived from the large-eddy motion. The model is disadvantageous in consuming more computer time and storage than RANS.

The above modeling approaches are often time-consuming, costly, and difficult to implement within practical turn-around periods. Empirical modeling methods based on dispersion theory have been widely used as a different approach for many comprehensive evaluations, because they can be designed to enable the expeditious calculation of many different cases. Semi-empirical models include the Atmospheric Dispersion Modeling System (ADMS) [32-35] and the American Society of Heating, Refrigerating and Air Conditioning Engineers (ASHRAE) model [36-38], among others. However, these have limited applicability and decreased accuracy concerning the details of building configurations and the surrounding environment.

Given that each modeling approach has particular advantages and limitations, these approaches should be used prudently according to the modeling concepts. It is also necessary to clarify the purpose of use and the accuracy required for a scenario before choosing a model. Therefore, it is important to utilize these modeling approaches by considering the balance among accuracy, cost, and the specific features of a target to be achieved. This review paper considers some of the most common questions confronting researchers and practitioners in the modeling of near-field pollutant dispersion in the built environment.

2 Ten questions (and answers) concerning the modeling of near-field pollutant dispersion in the built environment

2.1 What is near-field pollutant dispersion in the built environment?

Answer: Near-field pollutant dispersion in the built environment is characterized by the complex interaction of plumes with flow fields perturbed by building obstacles. The dispersion field contains local emission sources and the dispersion of the emissions in nearby individual buildings and the surrounding neighborhood.

Wind flow in the built environment is described by the interactions between atmospheric flow and that around buildings. Figure 1 presents a schematic of the wind-flow pattern around an isolated building [23, 39, 40]. The flow field contains various types of flow patterns, including a boundary layer flow, horseshoe vortex, stagnation flow, separation flow, and recirculating flow. Notably, this figure shows the average wind-flow pattern; the actual flow pattern exhibits pronounced transient features, such as the build-up and collapse of the separation/recirculation bubbles and periodic vortex shedding in the wake [23]. Figure 2 depicts the flow pattern at a street intersection where a tall building is located on the upwind side of one street [6]. The additional secondary flows created by the tall building both mix external air into the canopy and draw air from it, particularly at the rear face of the building.

The pollutant concentration distributions produced by such complex flow fields can differ significantly from those predicted by conventional diffusion formulae, such as the Gaussian-based models. Such formulae contain the implicit assumptions that the flow field has straight and parallel streamlines, modest velocity gradients, and distributions of turbulent energy and length scales resulting from surface features that remain unchanged over long distances [3]. Therefore, the prediction of such concentration fields is difficult, as conventional formulae cannot be applied. Modeling requires not only the basic knowledge of air pollution meteorology and dispersion but also an understanding of wind engineering and building aerodynamics, because wind and buildings can strongly affect plume behavior. Important parameters for dispersion around buildings include environment topography, e.g. [41, 42], building geometry, e.g. [43, 44], wind speed, e.g. [45, 46, 98], wind direction, e.g. [47,

48], turbulence, e.g. [49, 50], atmospheric stability, e.g. [51, 52], temperature, e.g. [53, 54], solar radiation, e.g. [55, 56], and tree planting, e.g. [57, 58]. Furthermore, depending on the pollutant substance, the buoyancy, e.g. [59-62], chemical reactions, e.g. [63-65], particulate matters, e.g. [9, 66], and deposition of the pollutant, e.g. [67, 68], may have non-negligible effects.

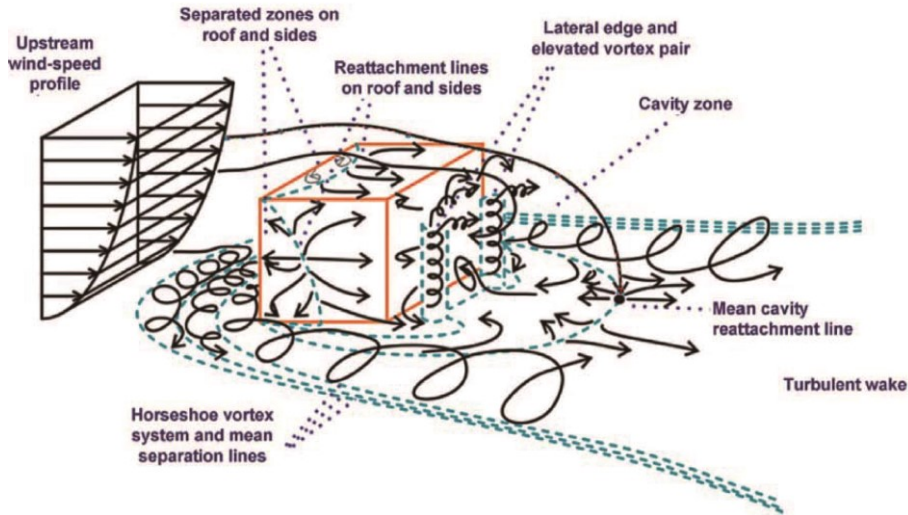


Figure 1. Schematic of the flow around an isolated low-rise building ([23]; modified from [39, 40]).

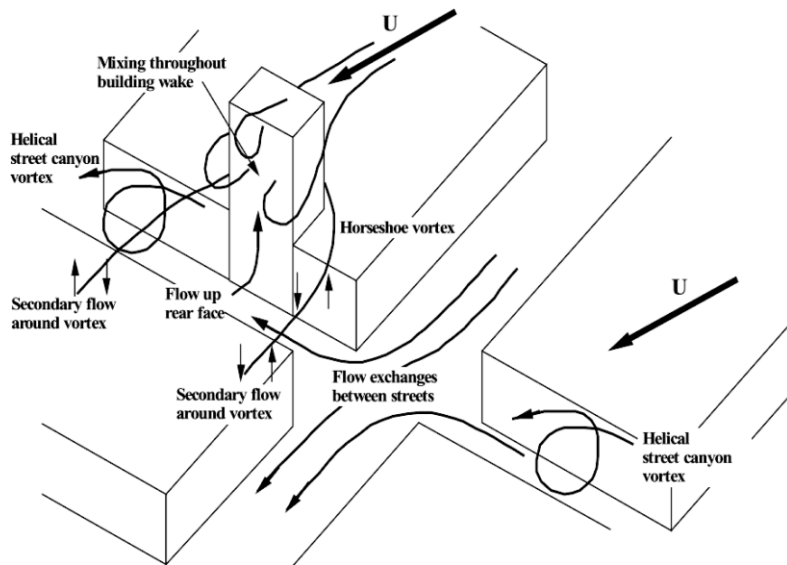


Figure 2. Flow field at a street intersection with a tall building, illustrating exchanges between the streets and the additional mixing processes due to the large building [6].

2.2 *How do the atmospheric boundary layer characteristics affect the dispersion of pollutants around buildings?*

Answer: As mentioned previously, the near-field dispersion around buildings is characterized by the interaction between atmospheric boundary layer flow and the flow around buildings. Therefore, modeling accurately the atmospheric boundary layer flow is imperative in order to obtain accurate and reliable predictions of the likely dispersion processes.

The approaching atmospheric boundary layer should be reproduced correctly in physical modeling. The common profiles representing wind speeds in atmospheric boundary layers follow logarithmic or power laws;

the parameters in these profiles are connected to the classification of the upstream terrain [69, 70]. In practice, upstream surface roughness (sometimes combined with the presence of fences and spires) is used in order to simulate an approach wind profile in a wind tunnel [71-73].

In CFD, the accurate simulation of the atmospheric boundary layer flow in the computational domain is necessary in order to obtain accurate and reliable predictions of the related atmospheric process [74]. Within the computational domain, three different regions can usually be distinguished, as illustrated in Figure 3 [74]. Although the actual geometric shapes of features such as buildings are explicitly modeled in the central (target) region of the domain, these are modeled implicitly in the upstream and downstream regions. This means that they are not included in the domain, but their effects on the flow are modeled in terms of roughness in the upstream and downstream regions. Therefore, consistent modeling of the atmospheric boundary layer flow is important to avoid unintentional changes such as streamwise gradients or horizontal inhomogeneities that can occur in the vertical profiles of the mean wind speed and turbulence quantities as they travel from the inlet of the computational domain towards the target regions [74-82]. These unintentional inhomogeneities can dramatically affect the quality of the simulation results [74]. As many commercial CFD codes employ k_S -type wall functions, using the equivalent sand-grain roughness height k_S as a parameter of roughness, Blocken et al. [74] derived specific relationships between k_S and the aerodynamic roughness length z_0 for specific CFD codes and demonstrated the importance of satisfying these relationships in CFD simulations of wind flow around buildings. These methods are utilized in RANS simulations. For LES, special treatments are introduced to generate unsteady inflow turbulence, necessary for use as the boundary conditions. Several techniques have been developed for this purpose, and can be classified into three categories. The first and simplest is to store the time history of velocity fluctuations from a preliminary LES computation. The second is to set a driver section ahead of the main computational domain to generate inflow turbulence, e.g. [83-85]. The third is to generate inflow turbulence artificially, based on the inverse Fourier transform of prescribed spectra, e.g. [86-94]. Overall reviews of recent developments in engineering fields regarding these techniques can be found in [94, 95]. The influence of the atmospheric turbulence scales on dispersion will be important to the study of LES in the future, because it is difficult to reproduce the full-scale spectra over the entire range of wavelengths in wind tunnels.

As illustrated in Figure 4, while the approaching wind profile can be significantly deformed by building obstacles, the structure of the approaching wind affects the flow structure within the building canopy. Pedestrian-level flow conditions, even in a very built-up environment, are reported to be quite sensitive to the structure of the approaching wind [96]. Saathoff et al. [97] concluded through experimental work that high turbulence associated with an urban-type atmospheric boundary layer might increase plume dilution by as much as a factor of two compared to that measured in an open-country exposure. Several numerical studies have investigated the influence of atmospheric turbulence on pollutant diffusion around buildings, e.g. [49, 50, 99] and revealed that high inflow turbulence intensities reduced the pollutant concentration around buildings. High turbulence intensities cause significant turbulent diffusion around buildings, effectively diluting the pollutants. Furthermore, stratification effects on dispersion are not negligible, even under weakly unstable conditions in urban environments [51]. The effect of atmospheric stability on plume dispersion around buildings has been investigated by experimental, e.g. [100-103] and numerical, e.g. [51, 52, 104] studies. These results suggest that mean advection is more important than turbulent diffusion in pollutant dispersion when the turbulence weakens as stratification intensifies.

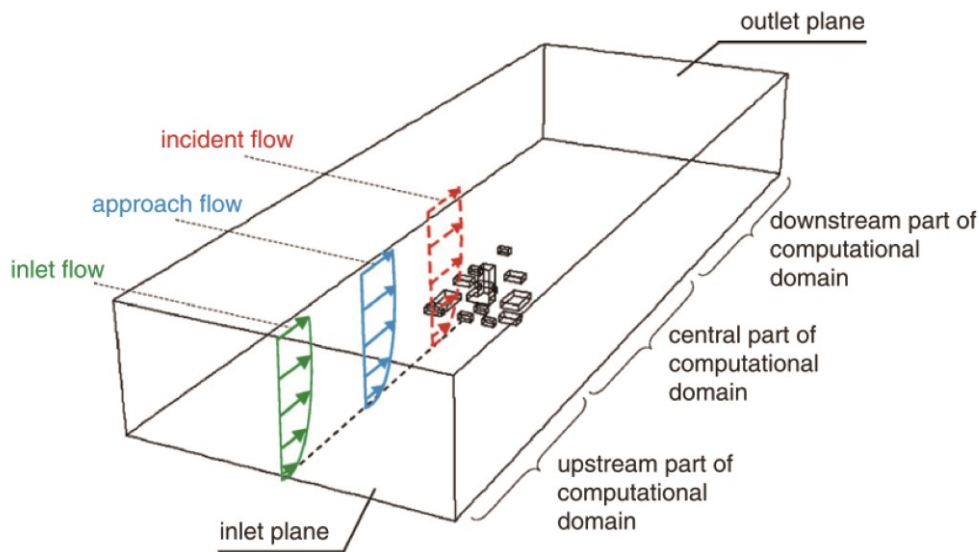


Figure 3. Computational domain with building models for CFD simulation of atmospheric boundary layer flow [74].

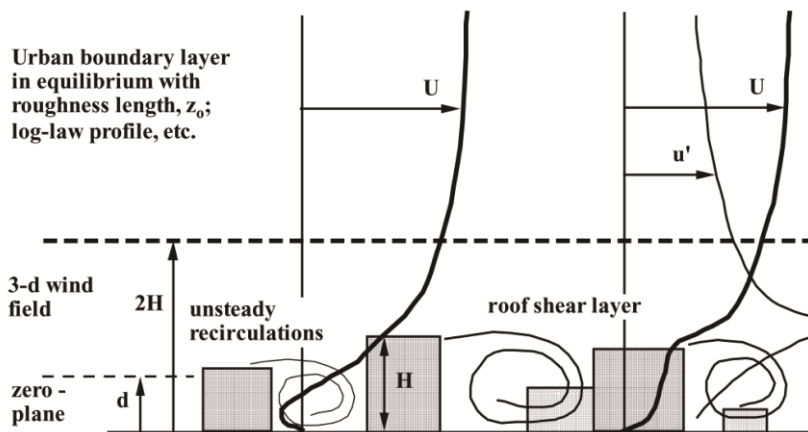


Figure 4. General features of the wind and turbulence fields over an urban area, showing regions of recirculation and ventilation [6].

2.3 How do surrounding variables like rooftop structures affect the pollutant dispersion around buildings?

Answer: The presence of stack and rooftop structures affects airflow patterns around a building, possibly contributing to exhaust re-ingestion problems. In particular, the stack installed in wake flows and the downwash effect of a rooftop structure on a plume can reduce air quality by increasing pollutant concentration near a fresh-air intake [105-107].

Based on wind tunnel experiments, guidelines for the safe placement of stacks and intakes on various building surfaces to prevent exhaust re-ingestion were proposed by Hajra et al. [108]. A schematic of the suitability of intake locations on various building surfaces is illustrated in Figure 5. The existence of surrounding or adjacent buildings significantly influences pollutant dispersion. The following parameters affecting dispersion fields have been investigated in previous studies: Building dimensions, e.g. [109-113], configuration of adjacent buildings, e.g. [114-119], and roof geometry, e.g. [120-123].

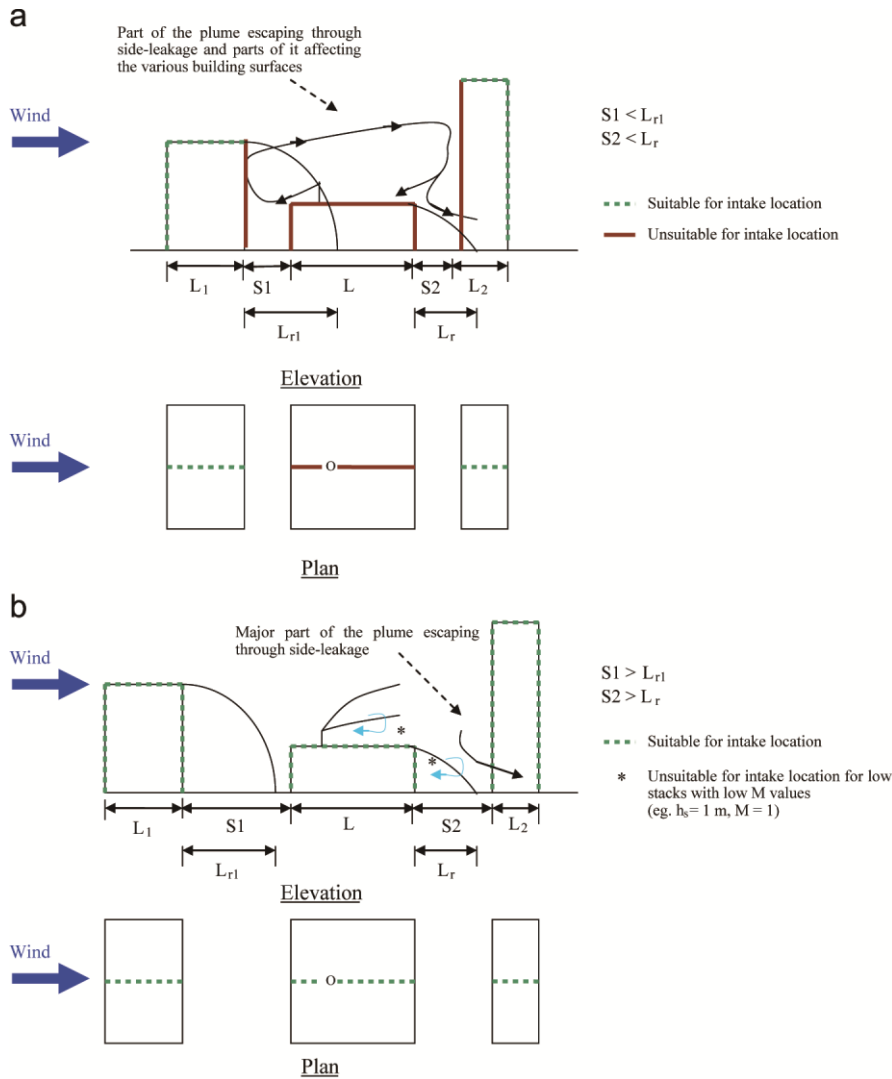


Figure 5. Schematic for suitability of intake location at various building surfaces: (a) $S1 < L_{r1}$ and $S2 < L_r$; (b) $S1 > L_{r1}$ and $S2 > L_r$ [108].

2.4 What are the important modeling parameters in physical experiments?

Answer: The specification of dimensionless parameters guaranteeing similarity has been discussed extensively [8]. For reduced-scale dispersion experiments, the dynamic and thermal characteristics of an atmospheric boundary layer and an exhaust gas should be modeled. The following similitudes are considered: 1) model geometry, 2) flow field, and 3) gas emission. Detailed and important discussion about these issues can be found in [124-126].

For the model geometry, although the agreement is satisfied by model similarity, careful attention should be paid to the relationship between the model scale and the boundary-layer scale [126, 127]. For flow field similarity, based on dimensionless forms of the equations describing flow and dispersion with buoyancy, such as momentum, advection-diffusion of pollutant, and energy equations, the following well-known dimensionless numbers that must match between the real and modeled scales are derived:

$$\text{Rossby number } Ro \equiv \frac{u_R}{L\Omega_R} \quad (1)$$

$$\text{Densimetric Froude number } Fr \equiv \frac{\Delta\rho Lg}{\rho_a u_R^2} \quad (2)$$

$$\text{Reynolds number } Re \equiv \frac{U_R L}{\nu} \quad (3)$$

$$\text{Thermal Péclet number } Pe \equiv \frac{U_R L}{\kappa} \quad (4)$$

$$\text{Mass transfer Péclet number } Pe_m \equiv \frac{U_R L}{\alpha} \quad (5)$$

$$\text{Prandtl number } Pr \equiv \frac{\nu}{\kappa} \quad (6)$$

$$\text{Schmidt number } Sc \equiv \frac{\nu}{\alpha} \quad (7)$$

Here, Ω_R is the reference angular velocity of earth rotation, U_R is the reference velocity, and L is the length. g is the gravitational acceleration, ρ_a is air density, ρ_s is the emission gas density, and $\Delta\rho = \rho_s - \rho_a$. ν is the kinematic viscosity, κ is the thermal diffusivity, and α is the mass diffusivity.

Since the simultaneous satisfaction of all similarity requirements cannot be achieved, partial or approximate similitude must be used. Several of the dimensionless parameters can be neglected because they are low in importance relative to others when simulating transport and dispersion around buildings [8]. The Rossby number (Ro) represents the inertial effects of transport in a rotating coordinate system, such as the Earth. Although it is impossible to satisfy this requirement in a usual wind tunnel, it can be neglected because the inertial force is small relative to the Coriolis force, as the target area is small in a near-field dispersion study. The densimetric Froude number (Fr) indicates the ratio of the buoyancy force from the density difference between the exhaust gas and the ambient air to the inertial force; it is equivalent to the Richardson number. Since the agreement of Fr often leads to very low wind speeds in wind tunnels, it causes difficulties in the requirements for the Reynolds number (Re). When Re is large enough, the flow structures around bluff bodies with sharp edges are similar even if Re is not identical, a phenomenon called ‘‘Reynolds Number Independence’’ [128]. The model and field values of the Prandtl (Pr) and Schmidt (Sc) numbers for wind-tunnel modeling of atmospheric flows are very similar. The thermal Péclet number (Pe) and mass transfer Péclet number (Pe_m) measure the ability of the fluid to advect heat or mass relative to the ability to disperse heat or mass by molecular transport. These parameters can also be expressed as $Re \cdot Pr$ or $Re \cdot Sc$. Therefore, Pe and Pe_m agreements are satisfied when the flow fields are turbulent enough. However, when wind speeds are very low in experiments, disagreement in these parameters may be problematic [59]. For gas emission, the following similarity parameters should be considered between the real and model fields: stack size, Fr of emission gases, density ratio of emission gases, and emission speed ratio [124, 125, 129]. When the buoyant force of the emission gas can be neglected, only the stack size and emission speed ratio are considered by using the tracer gas that has a density similar to that of air (such as ethylene or ethane). However, when the buoyant force of the emission gas cannot be neglected, the similitude becomes much more complicated. In such cases, the agreement of Fr among the emission gases is usually given priority over the other parameters, which are adjusted subserviently [124, 125]. These criteria can become more important for the study of pollutant dispersion in coupled indoor and outdoor environments, because the length and velocity scales differ significantly between these environments.

The evaluation period is also important in physical experiments. Generally, because turbulent eddies in the atmospheric flow occur with various time and spatial scales, time-averaged concentrations change significantly based on the averaging times. Appropriate evaluation time scales differ depending on the intended contaminant release being modeled. A short-term emission, representing many accidental emission releases, is usually modeled as a puff or intermittent source. For this type of emission, the impact of short concentration peaks (lasting a few seconds on the real scale) should be evaluated. A peak-to-mean ratio and intermittency can be introduced in the evaluation [130]. However, a long-term emission, representing most flue-gas stack emissions, is usually modeled as a continuous source. Pollutant dispersion studies with this type of contaminant usually employ long averaging times.

2.5 Under what conditions can the Gaussian plume models be used?

Answer: The Gaussian plume-dispersion models assume that the vertical and crosswind dispersion of the plume are Gaussian in form, and include the effect of ground reflection of the plume. Most recent models utilize the Monin-Obukhov similarity theory to derive their model parameters. These models have been used for many comprehensive formal evaluations, because they are designed to enable many different cases to be calculated expeditiously, e.g. [32-35]. Furthermore, Gaussian models may include many complex dispersion processes, such as atmospheric stratification, buoyancy, chemistry, deposition, and concentration fluctuations.

One of the most widely used models is the ADMS, developed in England but also endorsed by the United States Environmental Protection Agency [32, 33]. This advanced dispersion model can calculate effluent

concentrations emitted either continuously from point, line, volume, and area sources, or discretely from point sources. The model assumes concentration distributions to be Gaussian in neutral and stable conditions, but the vertical distributions are assumed non-Gaussian in convective conditions, to account for the skewed structure of the vertical component of turbulence [131]. In a study assessing the quality and applicability of various dispersion models for near-field dispersion, ADMS was the only model producing good comparisons with wind tunnel results. Other models, such as CALPUFF, SCREEN, and AFTOX, did not provide promising results for near-field dispersion in the built environment [132].

However, Hajra et al. [133] found that ADMS could not model the effects of rooftop structures, causing higher dilutions near the stack in comparison with wind tunnel results. The Gaussian-based empirical models could not explicitly treat detailed plume behaviors affected by building obstacles because of the modeling derivation. Therefore, in applying these models to near-field dispersion in urban environments, it is necessary to understand the fundamental concepts used in them [134, 135]. The complex geometry, unsteady process, and short-time exposure, which cannot be specified when applying Gaussian-based plume models, may cause considerable errors in target areas where these effects are dominant.

2.6 How accurate are the results produced by the ASHRAE empirical models in assessment cases?

Answer: The ASHRAE provides practical guidelines for the proper design of exhaust stacks and the placement of air intakes to avoid negatively affecting air quality in their Handbook. The ASHRAE model [36-38] consists of the two methods of geometric design and the Gaussian plume equations. The geometric design method is a qualitative approach, derived from the results of wind tunnel experiments, e.g. [114, 120] and it is typically used to assess the minimum stack height that can avoid plume re-ingestion through the roof or leeward wall of the emitting building. The geometric design method assumes that the plume, when released from a stack, follows a triangular path with a slope of 5:1 away from the centerline (Figure 6). The dimensions of the flow recirculation zones formed on the building are expressed in terms of L_r , the recirculation length formed in the wake of the building, which can be estimated using the dimensions of the building face perpendicular to the wind direction [120]. The boundary of the high-turbulence region is defined by a line with a slope of 10:1, extending from the top of the leading-edge separation bubble. The geometric design method has remained unchanged in the ASHRAE 2007, 2011 and 2015 versions. Meanwhile, the Gaussian plume equation is a quantitative technique used to estimate rooftop dilutions. Plume dilutions are estimated by calculating certain parameters, including the effective height of the plume above the roof, the exhaust velocity, the wind speed at building height, and plume spread standard deviations.

Notably, the Gaussian plume models have changed somewhat between the ASHRAE 2007 and 2011 versions, particularly in estimating plume dilutions. ASHRAE 2011 was recently introduced because discrepancies were observed between ASHRAE 2007 and experimental data from previous studies for cases of isolated buildings [132, 133]. New formulations for estimating plume rise, plume spread parameters, and dilution for shorter time periods have been suggested. Hajra et al. [108] presented results from a wind tunnel study of near-field pollutant dispersion from the rooftop emissions of two multiple-building configurations. The dilutions obtained by the wind tunnel experiments were also compared to the ASHRAE 2007 and 2011 predictions. They found that ASHRAE 2007 predictions were overly conservative for the isolated building, while the ASHRAE 2011 estimates compared better with experimental data in some cases. However, as suggested by [117, 118], neither ASHRAE model is capable of modeling the effect of adjacent buildings; further investigation of the formulations underlying these models is required. There is no change in the Gaussian plume models between 2011 and 2015 versions.

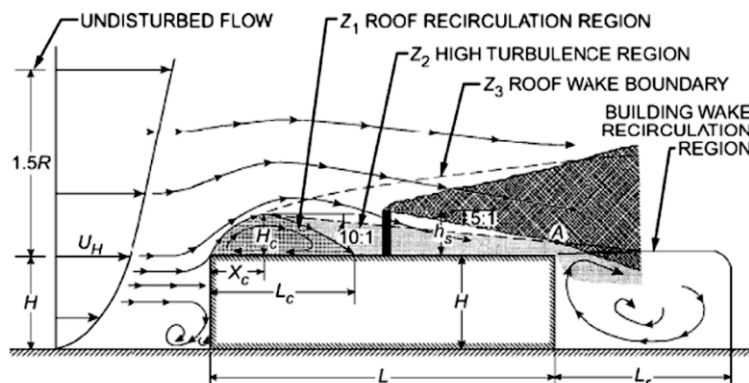


Figure 6. Design procedure for required stack height to avoid contamination [120].

2.7 *What are the advantages and limitations of CFD for near-field pollutant dispersion?*

Answer: CFD can overcome the disadvantages of full- and reduced-scale measurements in real atmospheric flow; in real conditions, variations in the wind and weather conditions cannot be controlled, so repeating an experiment under identical conditions is not possible. With CFD, these conditions can be set as boundary parameters. CFD can also overcome the disadvantages of wind tunnel testing, which generally only provides data for a limited number of discrete positions and can suffer from similarity requirements. CFD simulation is especially advantageous for stable atmospheric conditions and highly buoyant flows, as described in Section 2.4. Moreover, CFD is generally less expensive and time-consuming in setup, compared to the above approaches. However, CFD is disadvantageous in that it depends strongly on the computational parameters and conditions set during the simulation. Therefore, the accuracy and uncertainty of CFD are crucial. Both sensitivity analyses of the parameters and conditions as well as experimental validation studies are necessary for the utility of CFD results. The quality of results and computational time in CFD also depend crucially on the grid used to discretize the computational domain. The grid resolution should be fine enough to capture the important flow structures related to the pollutant dispersion, such as shear layers, vortices, and jets.

Researchers generally agree that both physical and numerical approaches are useful and should be complementary [14], by considering the advantages and limitations of multiple methods, e.g. [22-27, 136-138]. Given that the prediction accuracy of CFD in pollutant dispersion with highly buoyant flow fields has not been clarified yet, further studies are necessary in this area.

2.8 *How different are the simulation results obtained by steady-RANS and LES?*

Answer: According to previous studies comparing steady-RANS and LES for near-field dispersion modeling around buildings [139, 146], LES provides more accurate results than steady-RANS when calculating the mean distribution of concentration, although the difference between LES and RANS results for the mean velocities is not large. This is because the horizontal and vertical diffusion of concentrations are reproduced well by LES, because of the larger mixing effect of the large-scale velocity fluctuations behind the building [147]. Figure 7 illustrates the predicted results of pollutant dispersion by steady-RANS with RNG $k-\epsilon$ and LES from a stack located immediately downstream of an isolated rectangular building [145]. The average and instantaneous shapes of the plume are symbolized by the iso-surface $K = 1$, where K is the non-dimensional pollutant concentration. Because of large-scale fluctuations behind the building, as seen in the instantaneous plume shape (Fig. 7c), LES predicts that the average plume shape is shifted downwards and spread laterally (Fig. 7b), whereas RANS (RNG $k-\epsilon$) predicts it to extend farther downstream without significant disturbances by the presence of the building (Fig. 7a). For cases in which advection effects are more prominent than those of diffusion, results obtained by steady-RANS are typically acceptable, assuming an appropriate turbulence model is selected. Figure 8 illustrates the results of concentration distributions by CFD (SKE and RNG $k-\epsilon$) and experimental measurements [148] on the roof and wall surfaces with a downwind vent location [149]. Because most of the contaminant is advected by the strong separated flow in the streamwise direction in this case, the RNG, which successfully reproduces the reverse flow on the roof, provides good predictive concentrations in comparison with the SKE, which fails to reproduce the reverse flow. However, in cases where diffusion effects by large-scale coherent fluctuations around buildings, such as vortex shedding, are dominant, the steady-RANS significantly underestimates the pollutant diffusion.

In order to compensate for the underestimation of the mixing effect in steady-RANS, smaller values of the turbulent Schmidt number (Sc_t) are occasionally introduced, as discussed by Tominaga and Stathopoulos [150]. Because Sc_t is defined as the ratio of the eddy viscosity to the eddy mass diffusivity, increasing Sc_t leads to increases in eddy mass diffusivity. As demonstrated in many previous studies, e.g. [119, 144, 145, 151, 152], smaller Sc_t values often provide better results compared with experimental values. However, this cancellation of errors cannot be generalized and, therefore, is not recommended. The deficiency of steady-RANS is partly attributed to the shortcoming of the standard gradient diffusion hypothesis, e.g. [153, 154], and is partially improved by introducing higher-order closures for the turbulent scalar fluxes, e.g. [155-160]. However, the reproduction of unsteady large-scale fluctuations, captured only by unsteady computations, is more important in predicting near-field pollutant dispersion.

In addition, when an exhaust gas contains toxic, flammable, or odorous components, both the instantaneous and time-averaged concentrations are of interest. LES is advantageous in yielding important information on unsteady behavior of the concentration; this cannot be directly obtained by RANS computations neither by empirical models.

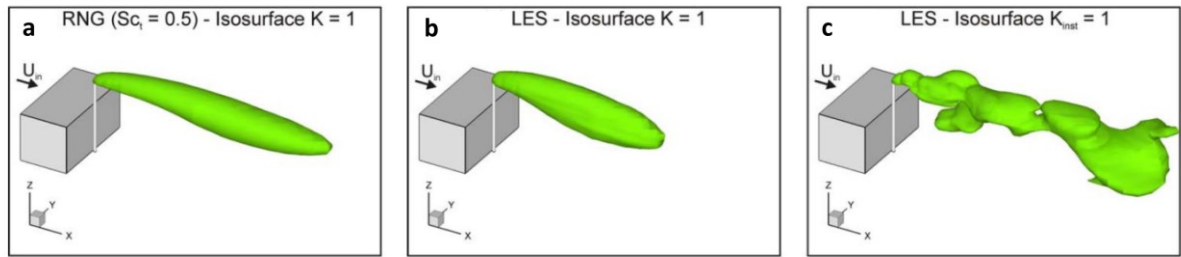


Figure 7. Average plume shapes obtained with (a) steady-RANS (RNG $k-\epsilon$) (b) LES and (c) instantaneous plume shape obtained with LES ([145]; partly modified by the present authors).

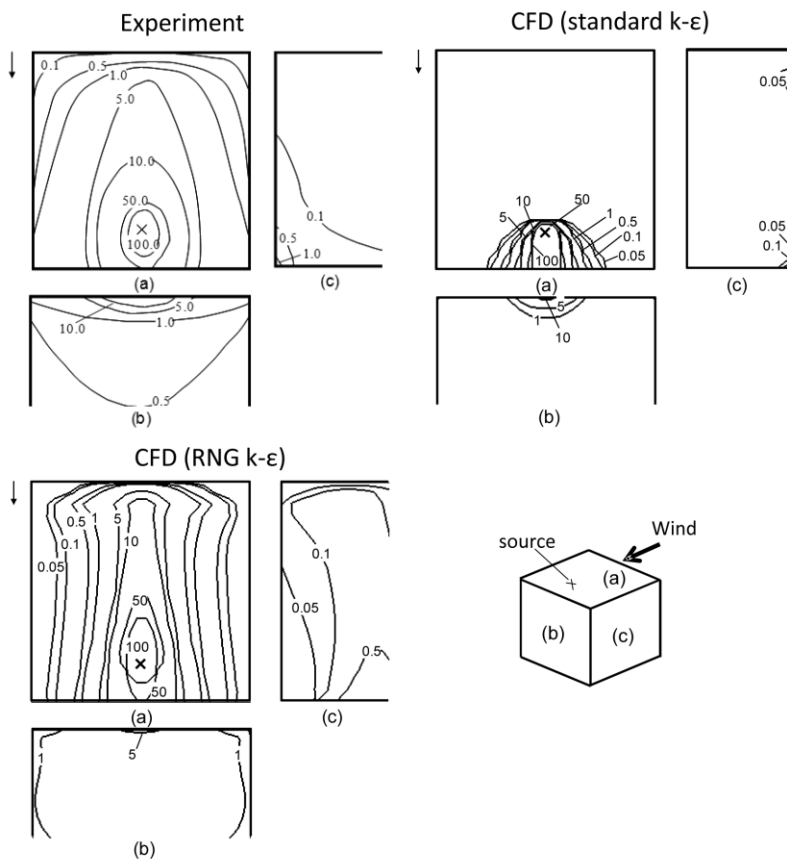


Figure 8. Contours of dimensionless concentration K on roof surface, obtained by experiments [148] and CFD (downwind roof vent release) [149].

2.9 Are there any validation databases for CFD simulation?

Answer: In order to perform high-quality validations and uncertainty evaluations of CFD simulations, reliable experimental data are indispensable. It is particularly important that the required boundary conditions, such as inflow conditions, be provided for the computations. Several experimental datasets for near-field dispersion based on field and boundary layer wind tunnel experiments are available, as listed in Table 1.

Validation is the process of determining the degree to which a model accurately represents the real world regarding the intended uses of the model [164]. The fundamental strategy of validation relies on the identification and quantification of the error and uncertainty in both conceptual and computational models, quantification of the numerical error in computational solutions, estimation of experimental uncertainty, and comparison of computational results to the experimental data [165]. As suggested by Schatzmann and Leitzl [19], the major source of uncertainty in field data relates to the question of measurement representativeness. The lack

thereof is caused by the difference in the time scales of atmospheric turbulence and the duration of individual measurements with common averaging intervals of 10 or 30 min. Therefore, in order to achieve data of known quality and uncertainty, as necessary for model validation, it is advisable to combine field measurements with corresponding laboratory measurements [19].

Moreover, as addressed by Harms [166], the validation of LES results is not as straightforward as that for models based on RANS. For LES, validation procedures are complicated because comparisons must be based not only on mean quantities but also on the frequency distributions of statistically representative ensembles of results.

Table 1. Validation database for near-field dispersion studies available online.

Database	Measurement data	Refs.	URL
COST 732 Model Evaluation Case Studies	Flow and concentrations for MUST and Oklahoma City cases (Wind tunnel)	[161, 162]	http://www.mi.zmaw.de/index.php?id=484 (Valid April, 2016)
CODASC	Concentrations around street canyons with avenue-like tree planting (Wind tunnel)	[57, 58]	http://www.windforschung.de/CODASC.htm (Valid April, 2016)
CEDVAL	Flow and concentrations around isolated obstacles, regular arrays of obstacles, and building complex (Wind tunnel)	[163]	http://www.mi.uni-hamburg.de/cedval/ (Valid April, 2016)
DAPPLE Datasets	Flow and concentrations in the complex urban environment in central London (Field measurements and Wind tunnel)	[16]	http://www.dapple.org.uk/ (Valid April, 2016)
TPU Database	Flow and concentrations around an isolated building (Wind tunnel)	[53]	http://www.wind.arch.t-kougei.ac.jp/info_center/pollution/pollution.html (Valid April, 2016)

2.10 *Are there any best practice guidelines to follow in the CFD simulation?*

Answer: Several best practice guidelines exist to assist in achieving high-quality CFD simulations; these provide relevant information on the most important credibility issues, especially regarding the most common sources of errors and uncertainties in CFD, e.g. [164, 165, 167]. For urban wind environment applications, best practice guidelines have been proposed as verification and validation processes for CFD, intended for the prediction of wind field around buildings [77, 168-171]. General best practice advice was provided by Blocken and Gualtieri [172] for environmental fluid mechanics. Although these guidelines are effective in the near-field pollutant dispersion problem, additional recommendations are specific to the dispersion problem. These include the requirements of modeling for contaminant transport equations and sensitivities to computational parameters, e.g. [145, 150, 152, 173, 174]. While the above-mentioned guidelines focus on steady-RANS simulations, the establishment of appropriate practical guidelines for LES is underway. Gousseau et al. [175] have performed quality studies on external wind-flow around an isolated building, based on several influencing factors. Such studies could be extended to the dispersion problem and to more influencing factors. Recently, Ai and Mak [176] investigated the factors influencing the LES modeling of flow and dispersion around an isolated building. Hertwig et al. [177, 178] suggest and apply a novel validation strategy for LES, consisting of a multilevel hierarchy of comparative analysis methods, in which not only low-order statistical moments but also higher-order eddy statistics and structural turbulence information are compared.

3 Summary and conclusions

The modeling methods for the near-field pollutant dispersion have been discussed in wide-ranging research fields for many years. In this review paper, some common questions confronting researchers and practitioners in modeling near-field pollutant dispersion in the built environment were discussed. Modeling approaches were categorized into field measurements, laboratory (wind and water tunnels) measurements, (semi-) empirical models, and CFD models. The important points in the application of these methods are as follows:

- Both full- and reduced-scale field measurements have provided valuable information, because they use real fluids with real atmospheric conditions. However, the boundary conditions in such experiments are uncontrollable and not reproducible. Therefore, the applicability of the datasets obtained from field measurements is limited for systematic and parametric studies.

- Laboratory experiments also employ real fluids; however, boundary conditions must be carefully modeled to resemble real atmospheric conditions. Because experimental conditions are easily controlled in the laboratory, results obtained from laboratory experiments are suitable for parametric and systematic studies of various physical flow and dispersion processes. However, the experiments can suffer from similarity requirements. In cases where thermal and buoyancy effects are non-negligible, the law of similitude becomes very complicated.
- Empirical modeling methods based on dispersion theory have been designed to enable the expeditious calculation of many different cases. The methods are relatively simple and easy to use but they have limited applicability and lower accuracy when building configuration details and the surroundings are considered.
- CFD can provide data for the entire flow and dispersion fields, performed at full scale and thus avoiding restrictions by similarity requirements. However, because CFD is very sensitive to the parameters and conditions, best practice guidelines are necessary to choose these aspects appropriately. Reliable experimental data are also required to validate the accuracy and uncertainty of CFD models.
- The existing modeling methods are best suited for steady pollutant distributions and relatively poor in modeling unsteady effects. However, CFD based on LES, which can overcome the limitations of the existing methods, may become a powerful tool in predicting and analyzing unsteady pollutant behavior. The establishment of appropriate practical guidelines and validation databases dedicated to LES are necessary but further research is required for their development.

Given that each modeling approach has distinct features and advantages, each method should be used in a manner appropriate to the modeling purpose. It is therefore important to use these modeling approaches while considering the underlying theory and limitations of the models. Current consensus is that both physical and numerical approaches are useful; they should be complementary in their advantages and limitations, thereby reducing the inaccuracy in the results of a single-approach method.

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Biography

Yoshihide Tominaga is a professor of the Department of Architecture and Building Engineering at the Niigata Institute of Technology. His area of expertise is the numerical modeling of micro-scale wind flow and related processes in urban environments, including urban microclimates, air pollutant dispersion, pedestrian wind comfort, and snowdrift. Ted Stathopoulos is a professor of the Department of Building, Civil & Environmental Engineering at Concordia University. His research has focused on wind engineering and building aerodynamics, including wind load, air pollutant dispersion, natural ventilation, and wind comfort using both experimental and numerical approaches. The authors have collaborated jointly on this topic for nearly 10 years and the outcomes of this collaboration have been published as several peer-reviewed journal papers.

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