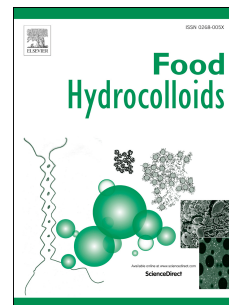


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Superabsorbent food packaging bioactive cellulose-based aerogels from *Arundo donax* waste biomass

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1 **SUPERABSORBENT FOOD PACKAGING BIOACTIVE CELLULOSE-**  
2 **BASED AEROGELS FROM *Arundo donax* WASTE BIOMASS**

3

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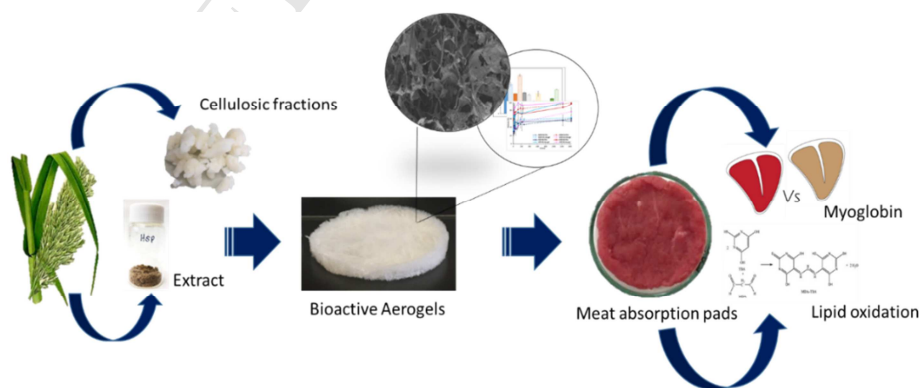
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20

21 **Abstract**

22 *A. donax* waste biomass has been valorized for the extraction of cellulosic fractions  
23 with different purification degrees, as well as aqueous bioactive extracts, which were  
24 then combined to develop superabsorbent bioactive aerogels. All the developed  
25 aerogels presented excellent water and oil sorption capacities; however, the presence  
26 of hemicelluloses yielded more porous and hydrophilic aerogels, capable of  
27 absorbing more water. With regards to the aqueous extracts, the hot water treatment  
28 (HW) of *A. donax* stems promoted the extraction of polysaccharides and  
29 polyphenols, producing the extract (S-HW) with the highest antioxidant capacity.  
30 This extract was then incorporated into the aerogels produced from the less purified  
31 stem fractions (F2A and F3A), which were chosen due to their good water sorption  
32 capacity, higher antioxidant potential and lower production costs and environmental  
33 impact. The hybrid aerogels showed a great potential to be used as bioactive pads for  
34 food packaging. In particular, the F2A+S-HW aerogel would be the most optimum  
35 choice since it provides a complete release of the extract in hydrophilic media, as  
36 demonstrated by *in-vitro* release and  $\beta$ -carotene bleaching inhibition studies, and it is  
37 able to reduce the colour loss and lipid oxidation in red meat upon refrigerated  
38 storage to a greater extent.

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44 **Keywords:** Aquatic biomass; porous materials; valorization; release; food  
45 preservation, active packaging.

## 46 **1. Introduction**

47 In the context of the extremely demanding market within the food industry,  
48 packaging plays a crucial role, not only protecting the product from the external  
49 environment and maintaining food quality to extend products' shelf life, but also  
50 being able to provide added functionalities, such as the incorporation of health-  
51 beneficial compounds (e.g. antioxidants) which can improve the nutritional value of  
52 the packaged product. Accordingly, strategies based on the controlled release of  
53 bioactive compounds from the package towards the food product, are being  
54 extensively investigated. For instance, some studies have reported on the  
55 incorporation of bioactive extracts into packaging films to preserve meat quality and  
56 organoleptic properties (Barbosa-Pereira, Aurrekoetxea, Angulo, Paseiro-Losada, &  
57 Cruz, 2014; Bolumar, Andersen, & Orlie, 2011; Camo, Lorés, Djenane, Beltrán, &  
58 Roncalés, 2011; Jofré, Aymerich, & Garriga, 2008; Lorenzo, Batlle, & Gómez,  
59 2014), demonstrating that the processes of lipid oxidation and colour loss upon  
60 storage could be reduced through the antioxidant activity of the incorporated  
61 extracts.

62 In the particular case of meat packaging, absorption pads are commonly used as  
63 moisture control elements, which absorb the excess liquids released by meat upon  
64 storage. These pads are typically made of a non-permeable/non-stick synthetic  
65 polymer, such as polyethylene and a hydrophilic non-woven bottom layer filled with  
66 active substances which prevent bacterial growth, such as citric acid and sodium  
67 bicarbonate (McMillin, 2017). Given the severe environmental issues associated to

68 the production and use of synthetic plastics, current trends in the food packaging  
69 sector are clearly moving towards the utilization of more sustainable bio-based and  
70 renewable materials, i.e. biopolymers. Polysaccharides and, in particular,  
71 lignocellulosic materials, have already demonstrated their great potential to develop  
72 high performance bio-based packaging structures (Benito-González, López-Rubio, &  
73 Martínez-Sanz, 2018; Martínez-Sanz, Erboz, Fontes, & López-Rubio, 2018;  
74 Rampazzo et al., 2017; Satyanarayana, Arizaga, & Wypych, 2009). Lignocellulosic  
75 materials can be extracted from multiple sources such as terrestrial and aquatic  
76 plants, algae and agriculture and forestry-derived waste by-products (Trache, Hussin,  
77 Haafiz, & Thakur, 2017). However, the extraction from waste or underutilized  
78 resources that do not compete with the food chain is particularly interesting and in  
79 line with the principles of circular economy. For instance, lignocellulosic fractions  
80 have been extracted from waste biomass derived from the aquatic plant *Posidonia*  
81 *oceanica* (Benito-González et al., 2018) and the aquatic invasive species *Arundo*  
82 *donax* (Martínez-Sanz et al., 2018).

83

84 In addition to other polysaccharides, cellulosic materials have been used to produce  
85 aerogel structures, which are extremely light, highly porous materials, with low  
86 density, large surface area and high water sorption capacity (Henschen, Illergård,  
87 Larsson, Ek, & Wågberg, 2016; Lin et al., 2014; Wang et al., 2016). Due to their  
88 large inner surface areas and high surface-to-volume ratios, these aerogels may be  
89 suitable for the development of controlled release systems. In fact, cellulose aerogels  
90 from different vegetal and bacterial sources have already demonstrated their potential  
91 as templates for the incorporation and sustained release of drugs (Haimer et al., 2010;

92 Valo et al., 2013), although their application in the food area has not been evaluated  
93 yet. One of the issues associated to the production of cellulose aerogels is that they  
94 are typically obtained by means of a complex synthesis method involving multiple  
95 steps: (i) dissolution of cellulose through the disruption of its crystalline structure,  
96 (ii) gelation, (iii) cellulose regeneration, (iv) solvent exchange and (v) a final drying  
97 step such as freeze-drying or supercritical drying (Gavillon & Budtova, 2007;  
98 Innerlohinger, Weber, & Kraft, 2006). Such process presents two main drawbacks:  
99 the high production costs and the unsuitability of the produced aerogels for food-  
100 grade applications due to the use of organic solvents.

101

102 In this work, the possibility of producing cellulose-based aerogels using a simple  
103 freeze-drying method from aqueous suspensions of cellulosic fractions from *A.*  
104 *donax* waste biomass with different purification degrees has been explored. To  
105 further valorize this waste biomass, aqueous extracts were produced by simple  
106 heating and ultrasound protocols and their composition and antioxidant capacity was  
107 evaluated. Finally, the most active extract was incorporated into selected aerogels to  
108 investigate the extract release and the antioxidant capacity of the hybrid structures, as  
109 well as to evaluate them as bioactive superabsorbent pads to preserve the quality of  
110 packaged red meat by reducing colour loss and lipid oxidation processes.

111

## 112 **2. Materials and Methods**

### 113 **2.1 Materials**

114 *Arundo donax* (*A. donax*) was collected from a freshwater environment in Buñol,  
115 Valencia (Spain) in September 2017. The leaves were separated from the stems and

116 the material was washed vigorously with water, ground with an electric blender and  
117 stored at 4 °C until use.

118 Gallic acid (97.5-102.5%), hydrochloric acid (37%), sulphuric acid ( $\geq 97.5\%$ ),  
119 potassium sulphate, potassium persulphate ( $\geq 99\%$ ), potassium chloride (99%),  
120 phosphate buffered saline tablets, ABTS ( $\geq 98\%$ ) and 6-hydroxy-2,5,7,8- tetramethyl  
121 chroman-2-carboxylic acid (97%),  $\beta$ - carotene ( $\geq 97\%$ ), linoleic acid ( $\geq 99\%$ ),  
122 Tween<sup>®</sup> 40, 2-Thiobarbituric acid (98%), ethylenediaminetetraacetic acid disodium  
123 salt dehydrate (98.5-101.5%), propyl gallate, were obtained from Sigma-Aldrich  
124 (Spain). Sodium chlorite 80% was obtained from Acros organics (Spain). The Folin-  
125 Ciocalteu reagent, modified Lowry reagent and bovine serum albumin were  
126 obtained from the “modified Lowry protein assay kit” purchased from Thermo Fisher  
127 scientific (Spain).

128

## 129 **2.2 Preparation of holocellulosic fractions**

130 A purification procedure previously reported (Martínez-Sanz et al., 2018) for the  
131 extraction of holocellulosic fractions from *A. donax* leaves and stems was applied,  
132 generating six different fractions labelled as F2, F3, F2A, F3A, F2L and F3L.

133 Briefly, the stem biomass was subjected to a Soxhlet treatment, followed by a de-  
134 lignification step with NaClO<sub>2</sub>, obtaining F2. After that, the hemicelluloses were  
135 removed by means of alkali treatment with KOH, yielding F3. The same process, but  
136 omitting the initial Soxhlet treatment, was carried out to produce the fractions  
137 labelled as F2A and F3A (obtained from the stem biomass) and F2L and F3L  
138 (obtained from the leaf biomass). The obtained fractions were stored in the fridge as  
139 partially hydrated materials until use.

140

141 **2.3 Production of water-soluble extracts from *Arundo donax***

142 Water-soluble extracts were generated from *A. donax* leaves and stems, using two  
143 different methods: (i) Hot water extraction (HW) and (ii) ultrasound-assisted  
144 extraction (US).

145 For the hot water extraction, 10 g of leaf or stem biomass (dry weight basis) were  
146 added to 200 mL of distilled water and mixed in a blender until a paste was obtained.  
147 The material was then heated up to 90 °C and kept at a constant temperature and  
148 under stirring for 1 h. After that, the material was centrifuged at 12500 rpm and 15°C  
149 for 20 min. The supernatant was separated, placed in an ice bath and the required  
150 volume of ethanol (75% with regards to the volume of aqueous supernatant v/v) was  
151 slowly added. The material was kept stirring in the ice bath overnight and after that,  
152 centrifuged again (12500 rpm, 15°C, 20 min). The precipitate was collected, re-  
153 suspended in distilled water and freeze-dried. The obtained powder extracts were  
154 labelled as S-HW (stem biomass) and L-HW (leaf biomass).

155 For the ultrasound-assisted extraction, 10 g of leaf or stem biomass (dry weight  
156 basis) were added to 200 mL of distilled water, mixed in a blender and subjected to  
157 an ultrasound treatment with a probe UP-400S (Hielcher GmbH, Germany) operating  
158 at a maximum power of 400W and a constant frequency of 24 kHz for 30min. After  
159 that, the material was centrifuged (12500 rpm, 15°C, 20 min) and processed  
160 following the same procedure described for the hot water extraction. The obtained  
161 powder extracts were labelled as S-US (stem biomass) and L-US (leaf biomass).

162 All the extracts were stored at 0% RH until further use.

163



## 164 **2.4 Preparation of aerogels**

165 Pure cellulosic aerogels were prepared by adding 0.075 g of the different fractions  
166 (dry weight) to 15 mL of distilled water and dispersing them by ultra-turrax  
167 homogenization until obtaining homogeneous suspensions. These were then poured  
168 into Petri dishes (diameter of 6 cm), frozen at -80 °C and subsequently, freeze-dried  
169 using a Genesis 35-EL freeze-dryer (Virtis). For the production of bioactive aerogels,  
170 0.015 g of water-soluble extract (ca. 17 wt.-% with regards to the total solids content)  
171 were dispersed together with the corresponding lignocellulosic fraction. In order to  
172 assess the effect of the material porosity the same formulations used to produce the  
173 bioactive aerogels were utilized to generate films by a vacuum filtration method, as  
174 previously described (Martínez-Sanz et al., 2018). The produced aerogels and films  
175 were stored at 0% RH.

## 176 177 **2.5 Density of aerogels**

178 Aerogel densities were determined by measuring the weight and volume of each  
179 individual aerogel. The weight of each aerogel was measured by an analytical  
180 balance (Precisa Gravimetrics AG SERIES 320XB, Dietikon, Switzerland) and the  
181 dimensions were measured by a digital caliper at three different positions.

## 182 183 **2.6 Scanning electron microscopy (SEM)**

184 Aerogel samples were coated with a gold-palladium mixture under vacuum and their  
185 morphology was studied using a Hitachi microscope (Hitachi S-4800) at an  
186 accelerating voltage of 10kV and a working distance of 8-16 mm.

187

## 188 **2.7 Water vapour sorption**

189 The water vapour sorption capacity of the aerogels was evaluated by registering the  
190 weight gain, using an analytical balance, when placing the samples in a cabinet  
191 equilibrated at 25 °C and 100 % RH. Square samples with a total surface area of 6.25  
192 cm<sup>2</sup> were cut from the aerogels and their initial weight was registered. The assays  
193 were carried out at least in triplicate.

194

## 195 **2.8 Water and oil sorption and desorption**

196 Square specimens with a total surface area of 1 cm<sup>2</sup> were cut, weighed and immersed  
197 in sealed containers containing 15 mL of distilled water or soybean oil. The samples  
198 were periodically taken out of the liquid and weighed after removing the liquid  
199 excess. Measurements were taken until the samples were equilibrated and the total  
200 weight gain was calculated. After equilibration, the samples were removed from the  
201 liquid, placed on top of absorbent paper and left drying at ambient conditions. The  
202 weight was registered periodically, until it was constant. The water and oil retention  
203 was calculated from the difference between the weight after drying and the initial  
204 weight of the samples, before soaking them in the liquids.

205

## 206 **2.9 Determination of extract composition**

207 The total phenolic compounds in the water-soluble extracts from *A. donax* were  
208 estimated by the Folin-Ciocalteu colorimetric assay (Singleton, Orthofer, &  
209 Lamuela-Raventós, 1999) and the results were expressed as mg gallic acid (GA)/g  
210 extract. The total protein content was measured following the Lowry method (Lowry,  
211 Rosebrough, Farr, & Randall, 1951) and the results were expressed as mg bovine

212 serum albumin (BSA)/g extract. The total carbohydrate content was determined after  
213 sulphuric acid hydrolysis, following the method described in (Martínez-Abad,  
214 Giummarella, Lawoko, & Vilaplana, 2018) A detailed description of these protocols  
215 can be found elsewhere (Martínez-Sanz et al., 2019). All the determinations were  
216 carried out in triplicate.

217

### 218 **2.10 ABTS Assay**

219 The radical cation scavenging activity of the different lignocellulosic fractions and  
220 the water-soluble extracts was determined according to (Re et al., 1999). Briefly,  
221 0.192 g of ABTS were dissolved in 50 mL of PBS at pH = 7.4 and mixed with 0.033  
222 g of potassium persulfate overnight in the dark to yield the ABTS<sup>•+</sup> radical cation.  
223 Prior to use in the assay, the ABTS<sup>•+</sup> was diluted with PBS for an initial absorbance  
224 of  $\sim 0.700 \pm 0.02$  (1:50 ratio) at 734 nm, at room temperature. Free radical  
225 scavenging activity was assessed by mixing 1.0 mL diluted ABTS<sup>•+</sup> with 10  $\mu$ L of  
226 aqueous suspensions of the samples (5 mg/mL) and monitoring the change in  
227 absorbance at 0, 1, 5, 10 min and 24 h. A calibration curve was developed by using  
228 6-Hydroxy-2,5,7,8-tetramethylchromane-2-carboxylic acid (Trolox). The antioxidant  
229 capacity of test extracts was expressed as mg Trolox equivalents (TE)/g extract. All  
230 determinations were carried in triplicate.

231

### 232 **2.11 $\beta$ -Carotene-linoleic acid assay**

233 The antioxidant capacity of the extracts and the generated aerogels was evaluated by  
234 the  $\beta$ -carotene-linoleic acid assay, according to (Martins et al., 2013), with minor  
235 modifications. In brief, 2 mg of  $\beta$ -carotene was dissolved in 10 mL of chloroform. 2

236 mL of this solution were placed on a rotary evaporator and the chloroform was  
237 evaporated. Then, 50  $\mu$ L of linoleic acid and 400 mg of Tween 40 were added and  
238 the content of the flask was mixed with stirring. After that, 100 mL of aerated  
239 distilled water was transferred to the flask and stirred vigorously. 0.5 mL of ethanolic  
240 solutions of the extracts (0.5- 5 mg/mL), BHT (0.5 mg/mL), or 0.5 mL of ethanol as  
241 a control were transferred to test tubes and then 5 mL of the  $\beta$ -carotene emulsion  
242 were added. For testing the bioactive aerogels, 25 mg of sample was transferred to  
243 the tubes and 5 mL of the  $\beta$ -carotene emulsion were added. The samples were  
244 incubated in a water bath at 50 °C for 120 min. The absorbance of each sample at  
245 470 nm was measured every 15 minutes using a spectrophotometer. The  
246 determinations were carried out in duplicate.

247

#### 248 **2.12 *In-vitro* release assays**

249 *In-vitro* release assays were carried out for the bioactive aerogels and films using  
250 water and ethanol as the release media. 10 mg of the films and aerogels were soaked  
251 in 2 mL of ethanol or water at room temperature. At appropriate time intervals, the  
252 concentration of the extract in the release media was estimated by measuring the  
253 absorbance of the supernatant at a wavelength of 271 nm using a NanoDrop ND1000  
254 spectrophotometer (Thermo Fisher Scientific, USA), until equilibrium was reached.

255 A calibration curve was previously built by recording the whole spectra of the extract  
256 diluted in water and ethanol at concentrations ranging from 0.1 mg/mL to 0.5  
257 mg/mL. The obtained data were used to determine the total amount of the extract  
258 released from the samples at each time point, taking into account that the maximum  
259 concentration of extract, if 100% release occurred, was 0.85 mg/mL

260  $(\frac{10 \text{ mg aerogel/film}}{2 \text{ mL H}_2\text{O/etOH}} \cdot \frac{17 \text{ mg extract}}{100 \text{ mg aerogel/film}})$ . Three independent replicates of each sample

261 were analyzed.

262

### 263 **2.13 Evaluation of the antioxidant effect of bioactive aerogels on red meat**

264 Bioactive aerogels containing the S-HW extract (F2A + S-HW and F3A + S-HW)

265 and the respective control samples (F2A and F3A) were tested as absorption pads for

266 the preservation of red meat. The aerogels were placed covering the bottom surface

267 of glass Petri dishes (diameter=6 cm) and portions of ca. 12 g of minced beef meat

268 were placed on top of the aerogels. The samples were then sealed with plastic wrap

269 film and stored in the fridge at 4 °C for 10 days. Control samples were prepared by

270 using commercial meat pads and blank samples were prepared by adding the same

271 amount of meat to Petri dishes with no pads.

272

#### 273 **2.13.1 Determination of oxymyoglobin and metmyoglobin**

274 The ability of the aerogels to prevent the colour loss in the red meat after storage was

275 evaluated through the determination of the oxymyoglobin and metmyoglobin content

276 proportions in the raw red meat and in the samples after refrigerated storage for 10

277 days by following the procedure described by Carlez et al. (Carlez, Veciana-Nogues,

278 & Cheftel, 1995). Briefly, two grams of minced meat samples were homogenized

279 with 20 mL of 0.04 mol/L potassium phosphate buffer (pH=6.8). The homogenized

280 samples were kept in an ice bath for 1 h and after that, they were centrifuged at 4200

281 rpm and 10 °C for 30 minutes. The supernatant was then filtered using 0.45 µm pore

282 size filters (Nylon, OlimPeak) and the volume of the filtrate was adjusted to 25 mL

283 with the same phosphate buffer. The absorbance of the supernatant was measured at

284 525, 545, 565 and 572 nm in a spectrophotometer. The concentrations of  
285 oxymyoglobin and metmyoglobin were calculated using the following equations:

286

$$287 \quad \% MbO_2 = (0.882 R_1 - 1.267 R_2 - 0.809 R_3 + 0.361) \times 100 \quad (1)$$

$$288 \quad \% MetMb = (-2.541 R_1 + 0.777 R_2 + 0.800 R_3 + 1.098) \times 100 \quad (2)$$

289

290 Where  $R_1$ ,  $R_2$ ,  $R_3$  are the absorbance ratios  $A^{572}/A^{525}$ ,  $A^{565}/A^{525}$ ,  $A^{545}/A^{525}$ ,  
291 respectively.

292 All the determinations were done in triplicate.

293

#### 294 **2.13.2 Measurement of lipid oxidation**

295 The degree of lipid oxidation in the red meat samples after 10 days of storage was  
296 also measured by following the 2-thiobarbituric acid (TBA) distillation method  
297 (Tang, Sheehan, Buckley, Morrissey, & Kerry, 2001). 10.0 g of meat were  
298 homogenised with 30 mL of water. The sample was then transferred to a distillation  
299 flask with 65 mL of water and the pH was adjusted to 1.5 with HCl 4N. Ethanolic  
300 propyl gallate (10%, 1mL), 10% EDTA (disodium salt, 1 mL), and a drop of  
301 antifoaming agent were added. The flask was connected to a Soxhlet apparatus and  
302 the mixture was boiled until 50 mL of distillate was collected. In a screw capped test  
303 tube, 5 mL of the distillate was reacted with 5 mL of TBA reagent (0.02 M TBA in  
304 90% acetic acid) in a boiling water bath for 35 min. A control made up of 5 mL  
305 distilled water and 5 mL of TBA reagent was also boiled for 35 min. The tubes were  
306 cooled to room temperature and the absorbance was measured at 535 nm in a  
307 spectrophotometer. The TBA reactive substances (TBARS) were calculated by

308 multiplying the absorbance readings by a factor of 7.8 and expressed as mg  
309 malondialdehyde (MDA)/Kg meat. The inhibition of lipid oxidation was calculated  
310 as follows:

$$312 \text{ Inhibition (\%)} = \frac{(TBARS_{Blank} - TBARS_{Day 0}) - (TBARS_{Pad} - TBARS_{Day 0})}{(TBARS_{Blank} - TBARS_{Day 0})} \times 100 \quad (3)$$

313

314 Where  $TBARS_{Day 0}$  refers to the TBARS in the raw minced meat and  $TBARS_{Blank}$   
315 and  $TBARS_{Pad}$  correspond to the TBARS in the meat samples after 10 days of  
316 refrigerated storage (blank sample and samples with the commercial or the cellulosic  
317 aerogel pads, respectively). These determinations were carried out in triplicate.

318

## 319 **2.14 Statistics**

320 All data have been represented as the average  $\pm$  standard deviation. Different letters  
321 show significant differences both in tables and graphs ( $p \leq 0.05$ ). Analysis of variance  
322 (ANOVA) followed by a Tukey-test were used when comparing more than two data  
323 sets.

324

## 325 **3. Results**

### 326 **3.1 Characterization of cellulosic aerogels**

327 Aquatic biomass from the invasive species *A. donax* was valorized for the extraction  
328 of different holocellulosic fractions, as described in a previous work (Martínez-Sanz  
329 et al., 2018). These fractions were previously used to produce films by a simple  
330 vacuum filtration method and their properties were seen to be significantly different

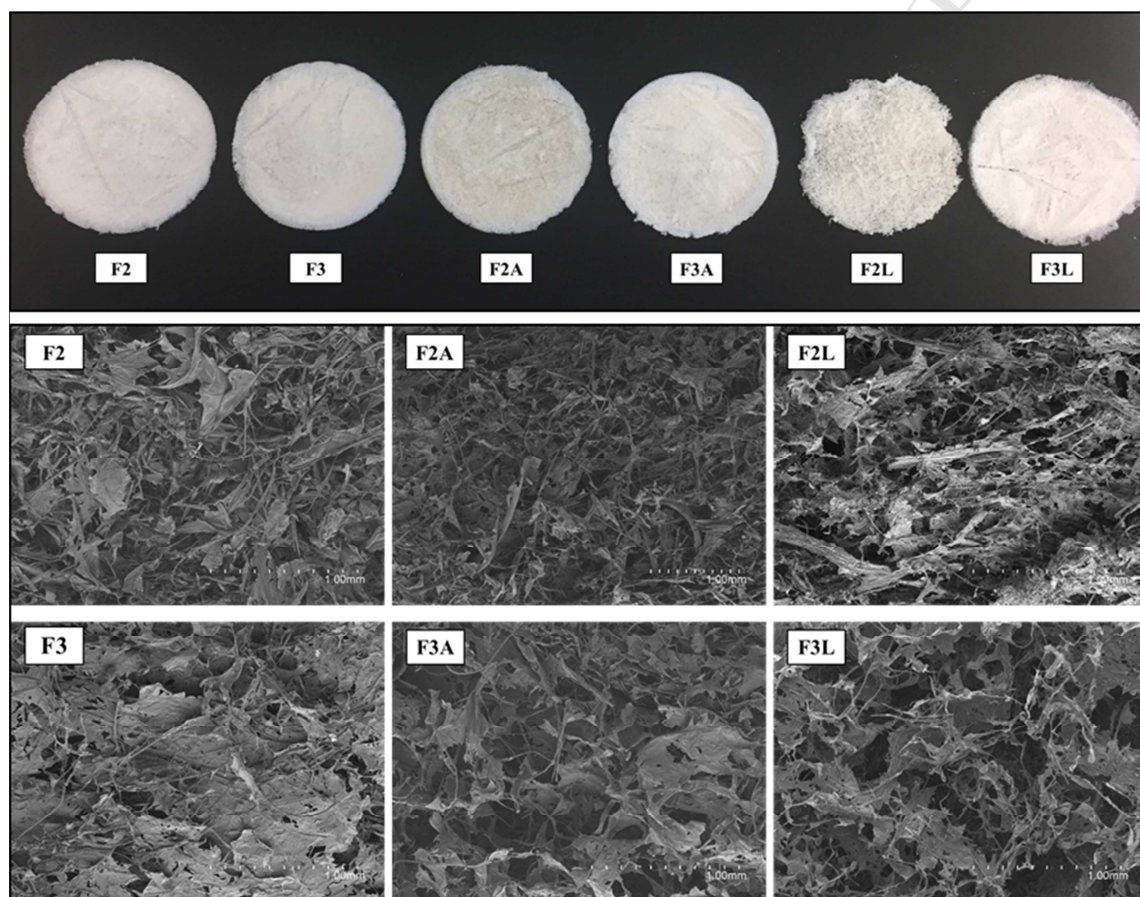
331 depending on the source (stems vs. leaves) and the extraction protocol (Martínez-  
332 Sanz et al., 2018). In this work, the extracted fractions were dispersed in water and  
333 subsequently freeze-dried to generate aerogel structures. As shown in Figure 1A, the  
334 obtained aerogels consisted of whitish sponge-like materials, with a soft consistency  
335 but good mechanical integrity (see also Figure S1). The aerogels obtained from the  
336 leaf fractions (F2L and F3L) were more heterogeneous than the homologous aerogels  
337 obtained from the stem fractions (F2A and F3A). In particular, the F2L aerogel  
338 presented a very soft consistency and poor integrity. It was also observed that the  
339 more purified cellulose aerogels presented a whiter coloration than the less purified  
340 ones. Specifically, the presence of hemicelluloses and lipids in the F2A and F2L  
341 aerogels conferred them a brownish hue.

342

343 The morphology of the aerogels was characterized by SEM and representative  
344 images are shown in Figure 1B. As observed, in general the aerogels presented an  
345 open porous network structure. It appears that those aerogels composed of fractions  
346 where the hemicelluloses had been removed (i.e. F3, F3A and F3L) presented a more  
347 compacted structure with less pores than their analogous aerogels containing  
348 hemicelluloses. Comparing the aerogels obtained from fractions extracted with (F2  
349 and F3) and without (F2A and F3A) the Soxhlet treatment, it seems that the presence  
350 of lipidic impurities also promoted the formation of slightly more porous structures.  
351 Moreover, it should be noted that the aerogels obtained from leaf biomass fractions  
352 (F2L and F3L) presented a more heterogeneous structure, especially F2L, where  
353 large fibrillar aggregates were also detected. This can be attributed to the presence of  
354 higher amounts of impurities such as minerals and proteins in the leaf biomass



355 (Martínez-Sanz et al., 2018), suggesting that stem fractions are more suitable for the  
356 production of aerogels. Thus, it seems that a higher degree of cellulose purity led to  
357 the formation of more homogenous and continuous structures, while the presence of  
358 other components resulted in the formation of more porous structures.  
359



360  
361 **Figure 1.** (A) Visual appearance and (B) SEM micrographs of the surface from the  
362 *A. donax* cellulosic aerogels.

363  
364 The density of the aerogels was estimated and the results are summarized in Table 1.  
365 Although the differences were not statistically significant, the more purified cellulose  
366 aerogels seemed to present greater density values than the aerogels containing  
367 hemicelluloses, supporting the porosity differences observed by SEM. The F2L

368 aerogel presented an anomalously high density, which may be the result of its more  
 369 heterogeneous structure. On the other hand, the F2A aerogel was the most  
 370 lightweight material, corresponding with its more open porous structure (cf. Figure  
 371 1A). The densities of most aerogels were significantly lower than those previously  
 372 reported for aerogels prepared by solvent exchange and supercritical CO<sub>2</sub> drying of  
 373 cellulose solutions in NMMO (ca. 50 mg/cm<sup>3</sup>) (Innerlohinger et al., 2006) and  
 374 cellulose nanowhiskers aqueous suspensions (78 mg/cm<sup>3</sup>) (Heath & Thielemans,  
 375 2010), having the same cellulose concentration used in this work (i.e. 0.5 wt.-%) and  
 376 similar to aerogels produced by supercritical CO<sub>2</sub> drying of regenerated tunicate  
 377 cellulose (10 mg/cm<sup>3</sup>) (Cai, Kimura, Wada, Kuga, & Zhang, 2008). In contrast,  
 378 lower density values (down to 6-8 mg/cm<sup>3</sup>) have been reported for optimized  
 379 aerogels produced by means of freeze-drying of aqueous suspensions of rice straw  
 380 cellulose nanofibrils produced by coupled TEMPO-oxidation and mechanical  
 381 blending (Jiang & Hsieh, 2014a, 2014b).

382

383 **Table 1.** Density and water vapour sorption of the cellulosic aerogels.

	Density (mg/cm <sup>3</sup> )	Water vapour sorption (g/g aerogel)
F2	12.84 ± 0.0029 <sup>ab</sup>	0.91 ± 0.02 <sup>b</sup>
F3	13.77 ± 0.0053 <sup>ab</sup>	0.39 ± 0.04 <sup>c</sup>
F2A	10.21 ± 0.0010 <sup>b</sup>	0.83 ± 0.02 <sup>b</sup>
F3A	14.39 ± 0.0004 <sup>ab</sup>	0.41 ± 0.02 <sup>c</sup>
F2L	25.55 ± 0.0057 <sup>a</sup>	1.09 ± 0.01 <sup>a</sup>
F3L	12.55 ± 0.0008 <sup>ab</sup>	0.52 ± 0.05 <sup>c</sup>

384 Values with different letters are significantly different ( $p \leq 0.05$ ).

385

386 The highly porous structure of cellulose aerogels offers a great advantage for the  
387 development of superabsorbent materials and/or matrices for the selective release of  
388 bioactive components in different media. The differences in composition and  
389 structure of the developed aerogels are expected to affect their behaviour when  
390 exposed to different media, which will ultimately determine their suitability to be  
391 used as template for the sorption and/or release of bioactive extracts. The water  
392 vapour sorption capacity of the aerogels was evaluated gravimetrically by exposing  
393 the samples to 100% RH conditions and the results are summarized in Table 1. As  
394 observed, the presence of hemicelluloses in the aerogels clearly had a significant  
395 impact, leading to increased water sorption capacity. This might be attributed to (i)  
396 the more hydrophilic character of hemicelluloses, provided by the greater amount of  
397 free hydroxyl groups in their structure and to their amorphous structure, as opposed  
398 to cellulose, which presents a more crystalline structure, with greater degree of self-  
399 association (Benito-González et al., 2018) and (ii) the more porous aerogel structure  
400 induced by the presence of hemicelluloses. The same trend has been previously  
401 reported for films produced from the cellulosic fractions extracted from *A. donax*,  
402 although the absolute water uptake values obtained for the films (0.06-0.1 g/g film  
403 for the films containing hemicelluloses and 0.02-0.05 g/g film for the purified  
404 cellulose films) (Martínez-Sanz et al., 2018) were significantly lower than those  
405 estimated for the aerogels, hence evidencing the great impact of the porosity on the  
406 sorption capacity. It is also worth noting that the presence of minor amounts of  
407 lipidic impurities in the aerogels obtained from fractions without the Soxhlet  
408 treatment did not have an impact on the water vapour sorption.  
409

410 Further to the behaviour of the aerogels when exposed to high relative humidity,  
411 which could take place, for instance, upon storage of foodstuffs at ambient  
412 conditions, their capacity to absorb and retain hydrophilic and hydrophobic media  
413 was also evaluated through immersion in water and soybean oil and subsequent  
414 drying at ambient conditions. All the aerogels were able to maintain their integrity,  
415 even after soaking them for 24h in both media. Figure S2 shows the  
416 sorption/desorption kinetics and Figure 2 displays the sorption equilibrium values  
417 (after immersion in the liquid media and after subsequent drying). As observed, both  
418 water and oil were quickly absorbed into the aerogels, reaching equilibrium values  
419 approximately after 24h. When drying the samples at ambient conditions, water was  
420 quickly released from the aerogels, producing a steep weight decrease within the first  
421 30 min and reaching the equilibrium after ca. 2 h. In contrast, the drying process took  
422 place more slowly in the case of oil, which was expected due to its higher viscosity  
423 (ca. 0.041 Pa·s at 20°C (Diamante & Lan, 2014) versus 0.001 Pa·s for water) and  
424 evaporation temperature. A sharper weight loss occurred during the first 3 h,  
425 reaching the equilibrium after ca. 7-8 h. A significant amount of both water and oil  
426 was released from the aerogels upon drying and, thus, the retention values were  
427 much lower than the sorption capacities, indicating that a significant amount of the  
428 absorbed liquids was not strongly interacting with the aerogel matrix materials. It  
429 should be noted that the lowest water and oil sorption capacity values corresponded  
430 to the F2L aerogel, which can be related to its heterogeneous structure.

431

432 For the water sorption/desorption process, the aerogels containing hemicelluloses  
433 showed a faster sorption/desorption kinetics than their more purified counterparts,

434 which can be attributed to their more porous structure. Furthermore, the water  
435 sorption equilibrium values were greater for the hemicellulose-containing aerogels.  
436 This can be ascribed to the greater compatibility of the more hydrophilic  
437 hemicelluloses with water, as compared with the cellulose hydrogels, where less  
438 amount of free hydroxyl groups may be available on the surface of the pore walls due  
439 to strong self-association. In fact, Chen et al. (2011) reported that aerogels with  
440 higher cellulose contents lead to the formation of stronger hydrogen bonding  
441 networks, resulting in a decreased water uptake. It should also be noted that the  
442 aerogels obtained from fractions without the Soxhlet treatment, containing  
443 hydrophobic lipidic impurities, showed lower water and oil sorption capacities than  
444 their purified counterparts. These results suggest that although the water  
445 sorption/desorption process was mostly a physical phenomenon, the affinity and  
446 interactions established between the components in the aerogels and the water played  
447 also an important role. This can be explained by the existence of two different  
448 adsorbed water domains, as previously reported for silica aerogels: (i) one fraction of  
449 bound water interacting with the aerogel components through hydrogen bonding and  
450 (ii) one fraction of bulk water which is physically adsorbed within the aerogel pores  
451 (Da Silva, Donoso, & Aegerter, 1992).

452

453 In the case of the soybean oil, the opposite trend was observed for the sorption  
454 process, i.e. the more purified cellulose-based aerogels presented faster kinetics and  
455 reached greater oil sorption equilibrium values. In particular, the purest cellulose  
456 aerogel, i.e. F3, presented the greatest oil sorption capacity. This seems to confirm  
457 the more hydrophobic behaviour of the cellulose-based aerogels due to the strong

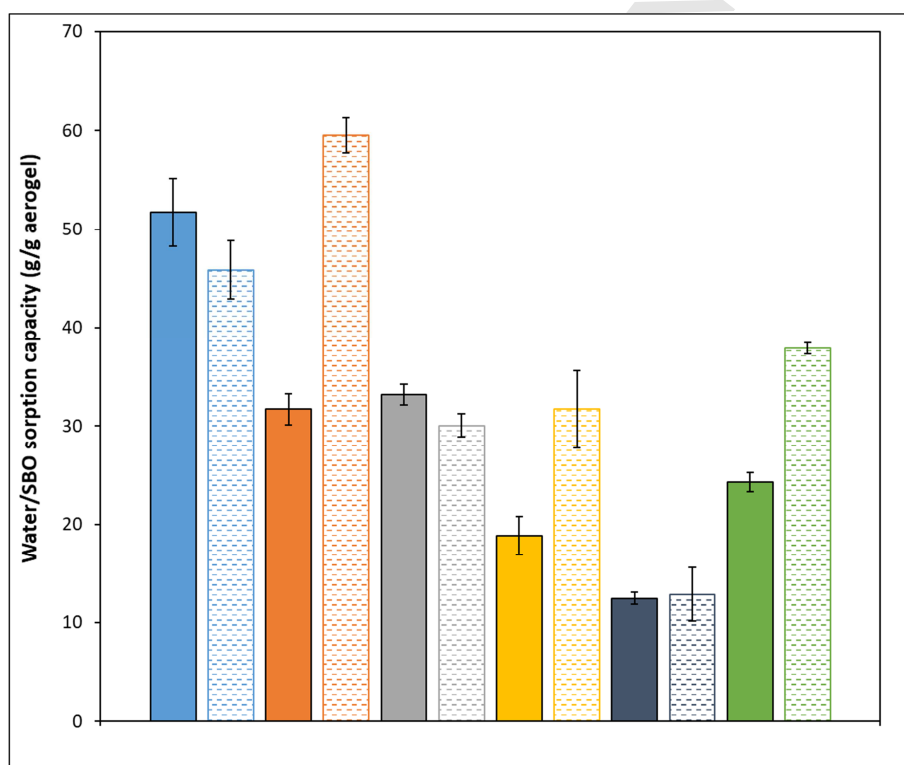
458 cellulose self-association, facilitating the oil sorption process. However, although the  
459 more purified aerogels seemed to show a faster oil desorption process, no significant  
460 differences were encountered between the oil retention values for all the samples.  
461 The soybean oil retention values were greater than those for water for all the  
462 samples, which is explained by the stronger effect of capillary forces in the case of  
463 the more viscous oil, a fraction of which remained adhered to the pore walls and  
464 trapped within the macropores (Hu, Zhao, Gogotsi, & Qiu, 2014). The same effect  
465 has been previously observed for oils with different viscosities (Feng, Nguyen, Fan,  
466 & Duong, 2015; Nguyen, et al., 2013).

467

468 The values previously reported in the literature for the sorption of liquids of  
469 cellulose-based aerogels evidence the excellent capacity of the *A. donax* aerogels to  
470 absorb liquid media, without the need of any physical or chemical modification. A  
471 lower water sorption capacity of 19.8 g water/g aerogel has been previously reported  
472 for aerogels from native recycled cellulose (Nguyen et al., 2014). Only modified  
473 cellulose aerogels have been shown to present greater water sorption capacities. For  
474 instance, water sorption values of 104-210 g water/g aerogel have been reported for  
475 aerogels from TEMPO-oxidated and defibrillated cellulose nanofibers (Jiang &  
476 Hsieh, 2014a, 2014b). It should be noted that these aerogels possessed a less dense  
477 structure than the ones developed in this work, confirming the relevance of the  
478 porosity for the liquid sorption capacity of the aerogels. Salam et al. (2011) obtained  
479 hemicellulose aerogels incorporating carboxylic groups from a reaction with citric  
480 acid followed by cross-linking with chitosan, increasing the water sorption capacity  
481 up to 100 g water/g sample. With regards to the oil sorption capacity, lower values of

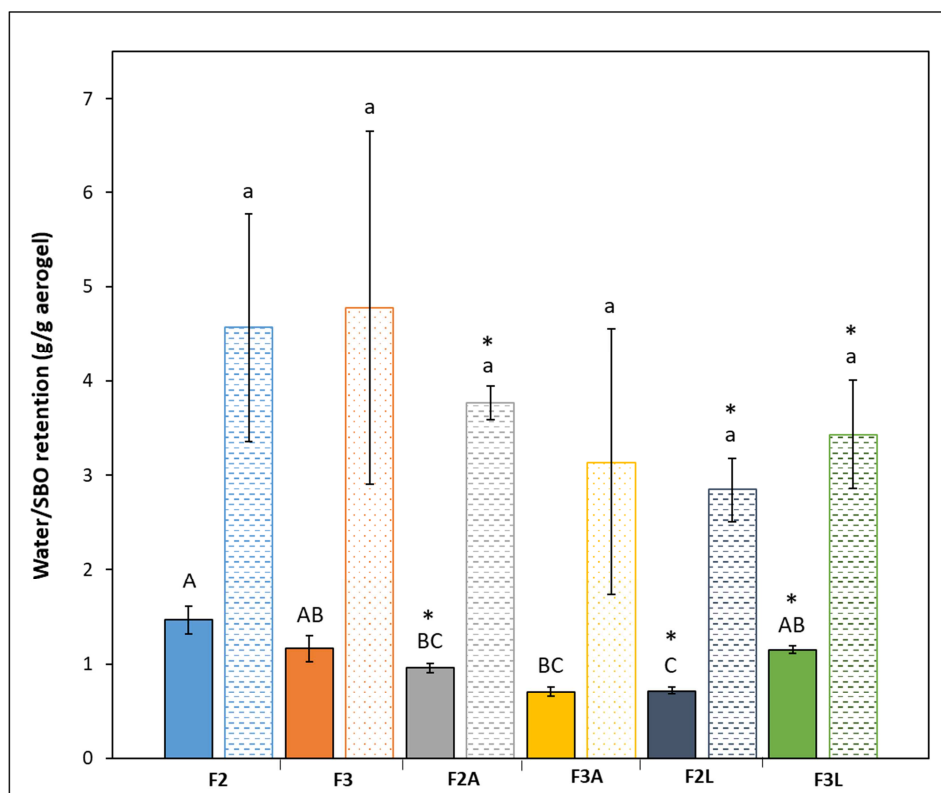
482 18-20 g crude oil/g aerogel were reported for methyltrimethoxysilane-coated  
483 cellulose aerogels (Nguyen et al., 2013) and a similar value of 62.6 g motor oil/g  
484 aerogel was obtained for cross-linked and hydrophobized 0.5 wt.-% cellulose  
485 aerogels (measured at 25 °C) (Feng, et al., 2015). The authors reported a maximum  
486 sorption capacity of 95 g motor oil/g aerogel, which could be achieved by lowering  
487 the cellulose concentration down to 0.25 wt.-% and producing less dense and more  
488 porous structures. Lower sorption capacities for different oils and organic solvents  
489 have also been reported for nanocellulose aerogels chemically modified to increase  
490 their hydrophobicity (Mulyadi, Zhang, & Deng, 2016; Phanthong et al., 2018).

491



492

493



494

495 **Figure 2.** (A) Water and soybean oil sorption capacity and (B) water/oil retention  
 496 capacity of the *A. donax* cellulosic aerogels after drying at ambient conditions. Solid  
 497 bars represent the water sorption/retention values and patterned bars represent the  
 498 soybean oil sorption/retention values. Bars with different letters are significantly  
 499 different ( $p \leq 0.05$ ). \* indicates significant differences ( $p \leq 0.05$ ) for the same sample  
 500 when soaked in water and oil.

501

502 The overall objective of this work was to generate bioactive aerogel structures by  
 503 utilizing the waste biomass from *A. donax*. Since some of the components remaining  
 504 in the less purified extracts, such as polyphenols, proteins and lipids may present  
 505 antioxidant properties, the different cellulosic fractions, prior to the preparation of  
 506 the aerogels, were characterized by means of the ABTS assay. From the results  
 507 compiled in Table S1, it is clear that (i) the stem fractions presented higher



508 antioxidant capacity than the leaf fractions and (ii) the components remaining in the  
509 less purified fractions conferred them greater antioxidant capacity. These results  
510 show the potential of the less purified aerogels to be used as bioactive food  
511 packaging structures.

512

### 513 **3.2 Production and characterization of water-soluble extracts from *A. donax***

514 Aquatic plants and algae are known to contain bioactive components such as  
515 polyphenols and sulphated polysaccharides that possess bioactive functionalities.  
516 Thus, the biomass from *A. donax* (stems and leaves) was also utilized to produce  
517 water-soluble extracts and their composition and antioxidant capacity were  
518 evaluated. To generate the extracts, two different protocols based on hot-water and  
519 ultrasound treatments were explored. The composition of the four different extracts  
520 was determined and the results are compiled in Table 2. As observed from this table,  
521 while polysaccharides were the main component in the stem extracts, similar  
522 amounts of proteins and polysaccharides were detected in the leaf extracts. It should  
523 be noted that, in general, the hot water treatment promoted the extraction of  
524 polysaccharides and polyphenols.

525

526 The antioxidant capacity the extracts was measured by using the ABTS and  $\beta$ -  
527 carotene bleaching assays. The first method is based on the scavenging capacity of  
528 the tested extract against the ABTS radical, converting it into a colourless product.  
529 On the other hand, the second protocol quantifies the ability of the extract to prevent  
530 the  $\beta$ -carotene degradation when subjected to high temperatures. The results listed in  
531 Table 2 evidence that the S-HW extract presented the highest antioxidant capacity

532 according to the ABTS assay, which can be related to the higher content of  
533 polysaccharides and polyphenols in this extract. To the best of our knowledge, no  
534 previous data on the antioxidant capacity of aqueous *A. donax* extracts are available.  
535 In general, organic solvents are preferred to produce plant extracts with antioxidant  
536 capacity, since bioactive compounds such as non-glycosilated flavonoids,  
537 phospholipids, carotenoids and chlorophyll analogues, are known to be more soluble  
538 in these solvents. However, other bioactive compounds such as sulphated  
539 polysaccharides and glycosylated polyphenols present a more hydrophilic character.  
540 In fact, lower antioxidant capacity values of ca. 70  $\mu\text{mol TE/g}$  extract have been  
541 reported for the acetone extracts from *A. donax* leaves (Piluzza & Bullitta, 2011),  
542 which can be directly related to their lower polyphenol content (ca. 21 mg GA/g  
543 extract) (Piluzza & Bullitta, 2011). The aqueous *A. donax* extracts presented greater  
544 phenolic contents than those previously reported in the literature for the methanolic  
545 extracts from a range of aquatic plants (1.6-21.6 mg GA/g extract) (Dellai, Laajili,  
546 Morvan, Robert, & Bouraoui, 2013; Kannan, Arumugam, Thangaradjou, &  
547 Anantharaman, 2013). Thus, the results seem to point out that *A. donax*, in particular  
548 the stem fraction, is rich in polysaccharides and polyphenols which confer the  
549 aqueous extracts a relatively high antioxidant capacity.

550

551 With regards to the capacity of the extracts to inhibit the  $\beta$ -carotene bleaching,  
552 Figure S2 shows the effect of the extracts when tested at three different  
553 concentrations, while the values compiled in Table 2 correspond to the highest  
554 concentration of 5 mg/mL. From Figure S3, increasing the extract concentration  
555 seemed to slightly improve the inhibition capacity, although the effect was not

556 significant due to the large standard deviation values. It should be highlighted that  
 557 the extracts presented similar antioxidant activities to that of a commercial synthetic  
 558 antioxidant such as BHT. No significant differences amongst the extracts were found  
 559 at a concentration of 5 mg/mL, although the S-HW extract showed the highest  
 560 percentage of inhibition. To the best of our knowledge, the capacity of *A. donax*  
 561 extracts to inhibit the  $\beta$ -carotene bleaching has not been reported in the literature,  
 562 although data for other plant extracts can be found in the literature. For instance, the  
 563 aqueous extract from *Tossa jute* leaves has been reported to present ca. 70.8%  
 564 inhibition when tested at 0.5 mg/mL (Ben Yakoub et al., 2018) and the ethanolic  
 565 extracts from *Osmundaria obtusiloba* and *Pteroclatiella capillacea* have shown 90%  
 566 and 45% inhibition, respectively, when tested at a concentration of 1 mg/mL (De  
 567 Alencar et al., 2016). Thus, although no reference values could be found in the  
 568 literature for a fair comparison, the  $\beta$ -carotene bleaching results, together with the  
 569 ABTS assay, seem to evidence the high antioxidant capacity of the aqueous *A. donax*  
 570 extracts.

571

572 **Table 2.** Composition and antioxidant activity of *A. donax* water-soluble extracts.

	Polysaccharides (mg/g sample)	Proteins (mg BSA/g extract)	Polyphenols (mg GA/g sample)	TEAC ( $\mu$ mol TE/g sample) (*)	$\beta$ -Carotene bleaching inhibition (%) <sup>(†)</sup>
S-HW	432.3 $\pm$ 84.6 <sup>a</sup>	150.0 $\pm$ 2.1 <sup>a</sup>	52.3 $\pm$ 0.9 <sup>a</sup>	143.7 $\pm$ 17.2 <sup>a</sup>	93.3 $\pm$ 0.7 <sup>a</sup>
L-HW	170.1 $\pm$ 51.2 <sup>b</sup>	143.7 $\pm$ 0.7 <sup>a</sup>	43.7 $\pm$ 3.4 <sup>ab</sup>	86. $\pm$ 7.2 <sup>b</sup>	86.9 $\pm$ 14.9 <sup>a</sup>
S-US	224.4 $\pm$ 16.4 <sup>b</sup>	149.3 $\pm$ 11.0 <sup>a</sup>	35.4 $\pm$ 5.4 <sup>b</sup>	97.1 $\pm$ 11.9 <sup>b</sup>	84.76 $\pm$ 12.32 <sup>a</sup>
L-US	117.1 $\pm$ 28.8 <sup>b</sup>	148.5 $\pm$ 8.5 <sup>a</sup>	35.2 $\pm$ 1.0 <sup>b</sup>	79.6 $\pm$ 5.3 <sup>b</sup>	60.80 $\pm$ 16.05 <sup>a</sup>

573 Values with different letters are significantly different ( $p \leq 0.05$ ).

574 (\*) TEAC values were calculated after 10 minutes.

575 (†) Calculated for the extracts at a concentration of 5 mg/mL.

576

577 **3.3 Production of bioactive aerogels**

578 Highly porous, superabsorbent aerogels and bioactive extracts from *A. donax*  
579 biomass were generated by green processes. Subsequently, these two components  
580 were combined to develop bioactive aerogels for food packaging applications. The  
581 F2A and F3A aerogels were selected as the matrices for several reasons: (i) these  
582 fractions were produced by a more cost-effective and greener process in which the  
583 use of organic solvents was avoided, (ii) they showed greater inherent antioxidant  
584 capacity and (iii) the produced aerogels showed excellent water and oil sorption  
585 capacities (although lower than the more purified F2 and F3 aerogels) and, thus, they  
586 were good candidates for the incorporation and release of bioactive extracts. The S-  
587 HW extract was selected due to its higher antioxidant capacity and it was  
588 incorporated into the F2A and F3A aerogels at a concentration of 17 wt.-%, which  
589 was the maximum concentration allowing to preserve the integrity of the aerogels.

590

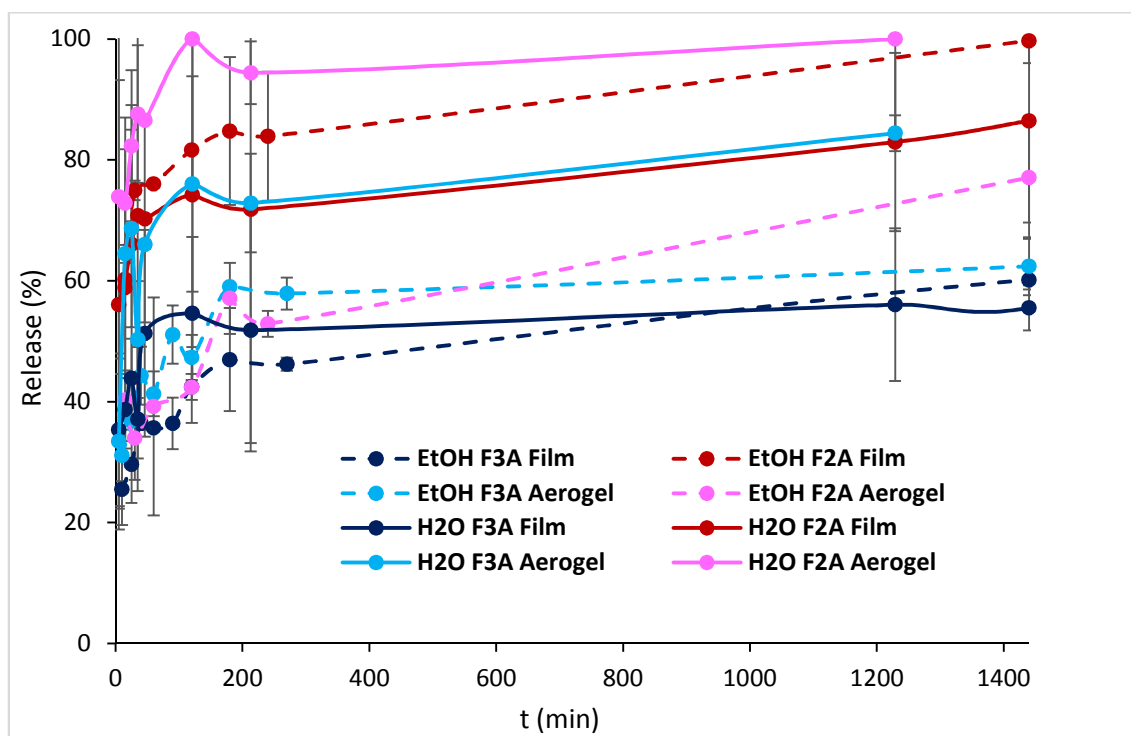
591 In order to evaluate the release of the bioactive extract from the F2A and F3A  
592 aerogels when exposed to different liquid media, *in-vitro* release studies were carried  
593 out in ethanol and water. Additionally, to assess the impact of the material porosity  
594 in the release behaviour, F2A and F3A films, presenting a much more compact  
595 structure (Martínez-Sanz et al., 2018), were also prepared by incorporating the same  
596 amount of extract. The results from the release studies, shown in Figure 3, indicate  
597 that, in general, the less purified F2A fraction provided greater extract release than  
598 the F3A fraction, both in films and aerogels. When water was selected as the release  
599 medium, a steeper release took place in the aerogels during the first 25 minutes, but

600 after that both aerogels and films showed a much slower release, reaching the  
601 equilibrium after ca. 3-4 h (ca. 100% release for the F2A aerogel, 84% for the F3A  
602 aerogel, 86% for the F2A film and 56% for the F3A film). The greater release values  
603 in the aerogels may be directly linked to their morphology, i.e. their porous structure  
604 facilitated the diffusion of water inwards and outwards the aerogel structure and as a  
605 consequence, promoted the quick release of the hydrophilic extract. In contrast, the  
606 compact structure of the films hindered the accessibility of water, releasing mostly  
607 the extract present on the surface of the films during the beginning of the experiment.  
608 Furthermore, stronger matrix-extract interactions seem to have been developed in the  
609 case of the films, hence leading to lower amounts of extract released after reaching  
610 the equilibrium. Moreover, in agreement with the water swelling experiments (cf.  
611 Figures 2A and 2B), the F2A aerogel seemed to promote water diffusion to a greater  
612 extent, thus increasing the amount of hydrophilic extract released to the liquid  
613 medium. Bacterial cellulose aerogels loaded with L-ascorbic acid and dexpanthenol,  
614 prepared by antisolvent precipitation with supercritical CO<sub>2</sub>, showed similar release  
615 profiles, achieving 100% release of the bioactives after ca. 2-3 h and the authors  
616 claimed that the release process was purely diffusion driven (Haimer et al., 2010).  
617 On the other hand, Valo et al., 2013 observed that the release of a drug incorporated  
618 into nanocellulose aerogels obtained from different sources was not only dependent  
619 on the structure but was also strongly affected by the interactions between the drug  
620 nanoparticles and the cellulose matrix, reaching equilibrium release values of ca. 40-  
621 60% for those cellulose aerogels where stronger interactions with the drug were  
622 established.

623

624 The use of a less polar solvent such as ethanol reduced the amount of released extract  
625 in the case of the aerogels. Interestingly, in that case very similar or even lower  
626 release values were obtained for the aerogels (ca. 62% for the F3A aerogel and 77%  
627 for the F2A aerogel) as compared with the films (ca. 60% for the F3A film and 99%  
628 for the F2A film). This might be due to a reduced diffusion of ethanol through the  
629 aerogel pores due to the lower affinity of this solvent with the cellulosic components.  
630 These results seem to indicate that while the release of the extract took place mostly  
631 at the surface level in the case of the films, a liquid medium diffusion-induced  
632 release mechanism took place in the case of the aerogels. Thus, the aerogels offer a  
633 clear advantage for their application as bioactive food packaging structures, since  
634 they are expected to release large amounts of extract when placed in contact with  
635 high moisture content foodstuffs.

636



637

638 **Figure 3.** Release profiles of S-HW extract from *A. donax* aerogels and films in  
 639 ethanol and water.

640

641 The high release of the bioactive S-HW extract when the aerogels were subjected to  
 642 high moisture conditions, together with the inherent antioxidant effect of the F2A  
 643 and F3A fractions, were expected to confer the hybrid aerogels antioxidant capacity.  
 644 To confirm this and to compare the performance of aerogels and films, the  $\beta$ -  
 645 carotene bleaching assay was carried out by soaking film and aerogel samples in the  
 646  $\beta$ -carotene emulsion. Since the cellulosic fractions were previously observed to  
 647 present antioxidant potential, the pure films and aerogels with no added extract were  
 648 firstly tested. As observed in Table 3, the aerogels, in particular the F2A aerogel,  
 649 were able to reduce the degradation of  $\beta$ -carotene, while the films did not show a  
 650 significant effect. This confirms that (i) the F2A fraction presented greater

651 antioxidant capacity due to the presence of impurities like phenolic compounds and  
 652 (ii) the release of bioactive components into aqueous media is favoured in the porous  
 653 aerogels as compared to the compact-structured films. The  $\beta$ -carotene bleaching  
 654 inhibition of the hybrid aerogels and films, containing the S-HW extract was then  
 655 evaluated and the difference between the obtained inhibition values and those  
 656 corresponding to the pure aerogels and films was calculated to evaluate the effect of  
 657 the incorporated extract. On the other hand, the inhibition of the pure extract at the  
 658 same concentration present in the films and aerogels (i.e. 0.84 mg/mL) was estimated  
 659 as  $58.8 \pm 0.9$  %. The results, gathered in Table 3, show that the hybrid F2A aerogel  
 660 provided the greatest inhibition capacity. Interestingly, no significant differences  
 661 were found between the analogous aerogels and films when removing the  
 662 contribution from the matrices (see third column in Table 2), suggesting that the  
 663 extract was released to the same extent in both types of structures when heating up to  
 664 50°C for 120 min. Furthermore, and in agreement with the *in-vitro* release  
 665 experiments, the results indicate that stronger matrix-extract interactions must have  
 666 been established in the case of the F3A aerogel/film, limiting the release. Overall, the  
 667 hybrid F2A aerogel presented the highest inhibition percentage, thus being the most  
 668 promising material for the development of antioxidant food packaging structures.

669  
 670 **Table 3.** Antioxidant capacity of *A. donax* aerogels and films, measured from the  $\beta$ -  
 671 carotene bleaching assay.

	$\beta$ -Carotene bleaching inhibition (%)		
	Pure Aerogel/Film	Aerogel/Film + S-HW	(Aerogel/Film + S-HW) – Aerogel/Film
Aerogel F2A	$32.8 \pm 8.8^a$	$90.1 \pm 2.8^a$	$57.3 \pm 2.9^a$
Aerogel F3A	$19.3 \pm 0.7^{ab}$	$57.7 \pm 0.06^b$	$38.4 \pm 0.1^b$



Film F2A	$5.6 \pm 3.2^b$	$58.9 \pm 4.4^b$	$53.3 \pm 4.4^{ab}$
Film F3A	$5.7 \pm 1.5^b$	$42.5 \pm 6.1^b$	$36.8 \pm 6.1^b$

672 Values with different letters are significantly different ( $p \leq 0.05$ ).

673

674

### 675 **3.4 Evaluation of the antioxidant effect of bioactive aerogels on red meat**

676

677 As a final proof of concept, the hybrid and the pure cellulosic aerogels were tested as

678 absorption pads to inhibit lipid oxidation and colour loss during storage of minced

679 red meat. Meat discoloration is attributed to the process of oxymyoglobin oxidation,

680 giving rise to the formation of metmyoglobin. The proportion of these two

681 myoglobin forms was determined in the raw minced meat and in the samples after

682 storage for 10 days. The visual appearance of representative meat samples after

683 storage is shown in Figure 4A and the estimated myoglobin contents are shown in

684 Figure 4B. It is observed that at day 0 (i.e. fresh meat) the oxymyoglobin content was

685 higher than metmyoglobin, as expected. After storage, a colour loss, indicated by the

686 lower oxymyoglobin content and the higher metmyoglobin content, took place in all

687 the samples. Interestingly, and as supported by Figure 1A, the samples stored with

688 aerogel pads presented higher oxymyoglobin and lower metmyoglobin content than

689 the control sample prepared using commercial pads, highlighting the potential of

690 these materials to limit the oxidation processes giving rise to meat discoloration upon

691 storage. In particular, the F2A+S-HW aerogel showed the strongest effect, which

692 may be attributed to the antioxidant capacity of its components (both the extract and

693 the F2A fraction). To the best of our knowledge, no previous works have reported on

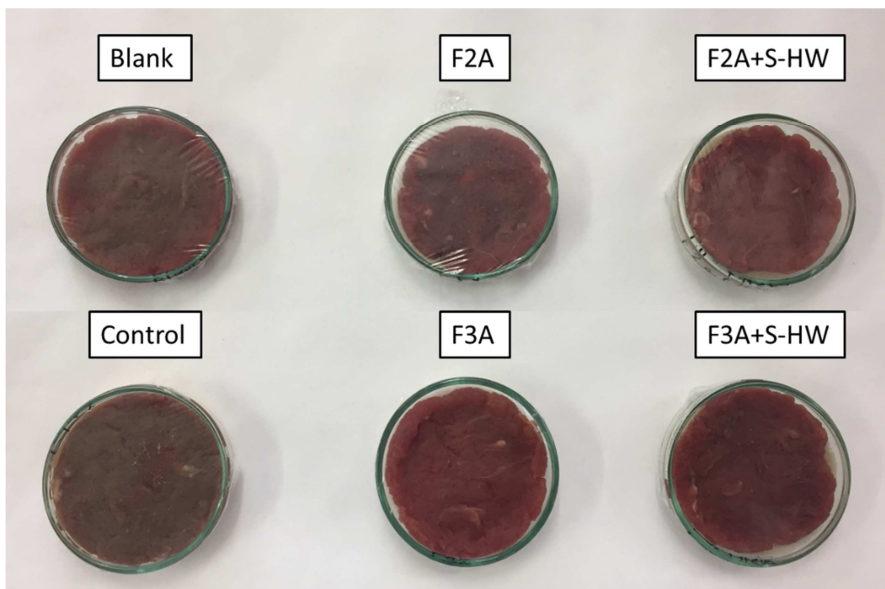
694 the utilization of aerogel structures or cellulose-based materials as antioxidant food

695 packaging structures. As a reference, 60% of metmyoglobin was detected in foal

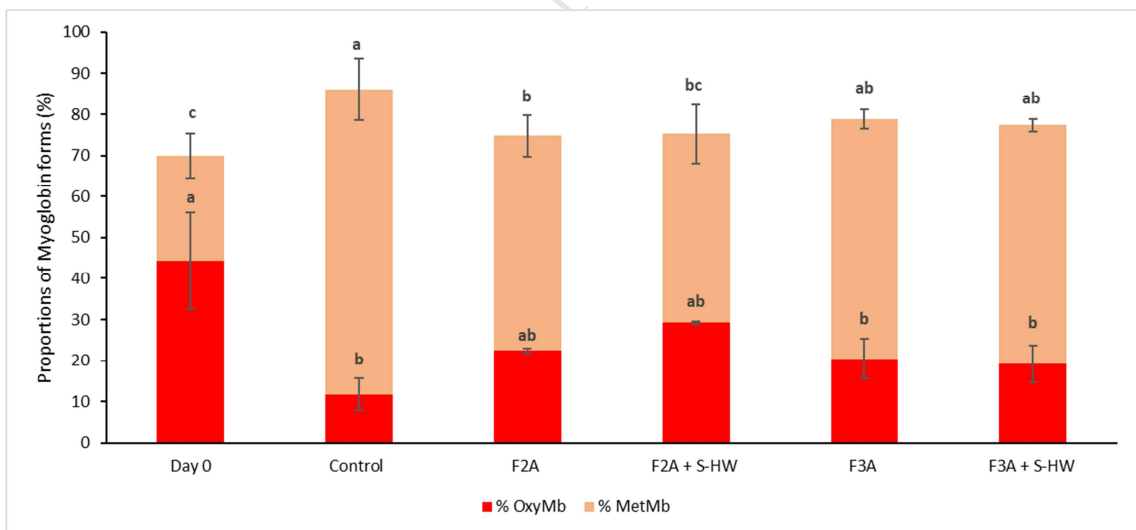
696 meat after storage for 10 days in modified atmosphere using bioactive films

697 containing oregano extract (Lorenzo et al., 2014), which is higher than the value  
 698 estimated for the meat stored in contact with the F2A+S-HW aerogel (ca. 46%  
 699 metmyoglobin).

700



701



702

703 **Figure 4.** (A) Visual appearance of the meat samples after storage for 10 days. (B)

704 Proportions of oxymyoglobin (%OxyMb) and metmyoglobin (%MetMb) in the raw

705 minced red meat (day 0) and in the meat after 10 days of storage. Bars with different

706 letters are significantly different ( $p \leq 0.05$ ).

707

708 The ability of the developed aerogels to prevent lipid oxidation in red meat was also  
709 evaluated by calculating the TBARS content in the raw minced meat and in the  
710 samples after storage and estimating the percentage of lipid oxidation inhibition with  
711 regards to a blank sample (i.e. meat stored without any pad). Although, as seen from  
712 the results summarized in Table 4, due to the large standard deviation values arising  
713 from the large inherent variability of the meat samples, no significant differences  
714 were found between samples, the meat stored in contact with the F2A+S-HW aerogel  
715 showed the lowest TBARS content and the highest lipid oxidation inhibition. To the  
716 best of our knowledge no previous works have reported on the potential of highly  
717 porous cellulose-based aerogels as bioactive food packaging structures. The most  
718 typical approach reported in the literature to prevent lipid oxidation in meat consists  
719 on the utilization of natural extracts. For instance, active packaging films containing  
720 2% of oregano essential oil or 1% of green tea extract were utilized to store foal  
721 steaks, although no significant effect in the TBARS content was detected after 10  
722 days of storage (Lorenzo et al., 2014). In another work, meat steaks were packaged  
723 in polystyrene trays and sprayed with oregano extract. The addition of 0.5% of  
724 oregano extract showed a high inhibitory effect on lipid oxidation, reaching a  
725 maximum value of 2 mg malonaldehyde/Kg meat after 28 days of storage (Camo et  
726 al., 2011). These results, together with the results from the meat colour evaluation  
727 and the antioxidant capacity of the aerogels, evidence the antioxidant potential of the  
728 F2A+S-HW aerogel, which could be used as bioactive pads in high moisture fresh  
729 packaged foods such as red meat.

730

731 **Table 4.** 2-thiobarbituric acid reactive substances (TBARS) and estimated lipid  
 732 oxidation inhibition in the raw minced red meat (day 0) and in the meat after 10 days  
 733 of storage.

	TBARS (mg malonaldehyde/ Kg meat)	Lipid oxidation Inhibition (%)
Day 0	$0.53 \pm 0.15^b$	---
Control	$6.37 \pm 1.68^a$	2.2
F2A	$4.36 \pm 1.25^{ab}$	35.9
F2A+S-HW	$4.04 \pm 2.34^{ab}$	41.3
F3A	$4.84 \pm 0.89^{ab}$	27.9
F3A+S-HW	$4.57. \pm 1.50^{ab}$	32.3

734 Values with different letters are significantly different ( $p \leq 0.05$ ).

735

#### 736 **4. Conclusions**

737 Highly porous bio-based bioactive aerogels have been produced by valorizing the  
 738 lignocellulosic waste biomass from *A. donax* biomass. Cellulosic aerogels were  
 739 produced by a simple freeze-drying method from aqueous suspensions of the  
 740 fractions extracted from *A. donax* stems and leaves. All the developed aerogels  
 741 presented an excellent water and oil sorption capacity, comparable to those  
 742 previously reported for chemically modified nanocellulose aerogels. The presence of  
 743 hemicelluloses in the F2 and F2A aerogels conferred them a less dense, more porous  
 744 structure, as well as a more hydrophilic character, promoting water sorption through  
 745 diffusion and water-hemicelluloses interactions.

746

747 Additionally, aqueous extracts with high antioxidant capacities were generated by  
 748 subjecting the *A. donax* biomass to simple heating and ultrasound methods. The  
 749 higher polysaccharide and polyphenol content in the stems extract generated by

750 heating (S-HW) conferred it the highest antioxidant capacity. This extract was  
751 incorporated into the F2A and F3A aerogels, which were selected due to their good  
752 water sorption capacity, their inherent antioxidant potential and their greater  
753 suitability from an economical and environmental perspective.

754

755 The release of the extract from the hybrid aerogels towards liquid media was mostly  
756 a diffusion-driven process, which was strongly promoted by the highly porous  
757 structure of the aerogels. In particular, the more porous structure and the greater  
758 water affinity of the F2A aerogel led to a complete release of the extract in water  
759 after 2-4 h. This, together with the inherent antioxidant capacity of the F2A fraction,  
760 resulted in a high inhibitory effect on the  $\beta$ -carotene bleaching upon heating.  
761 Furthermore, all the tested aerogels showed promising results to be used as bioactive  
762 food packaging pads, as they were able to reduce the colour loss and lipid oxidation  
763 in red meat upon refrigerated storage, being the hybrid F2A+ S-HW aerogel the most  
764 active.

765

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- 901



**Highlights**

- Cellulosic fractions extracted from *A. donax* biomass produced superabsorbent aerogels.
- Fractions containing hemicelluloses produced more hydrophilic and porous aerogels.
- Extracts with the highest antioxidant capacity were obtained by a heating treatment.
- Selected aerogels provided a complete release of the extract in hydrophilic media.
- Hybrid aerogels reduced oxidation processes in red meat upon storage.