

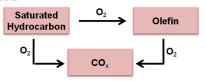
ODH of Ethane to Ethylene on a MoO_x Sphere Bed Investigated by Spatial **Reactor Profiles and Raman Spectroscopy**

Michael Geske, Oliver Korup, Robert Schlögl, and Raimund Horn* Fritz Haber Institute of the Max Planck Society, Department of Inorganic Chemistry, Faradayweg 4-6, 14195 Berlin, Germany



Motivation

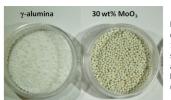
Oxidative dehydrogenations (ODH) of saturated hydrocarbons to olefins are characterized by a network of consecutive and parallel reactions



To study the interrelation between catalytic performance and catalyst structure we present spatial reactor profiles for ethane ODH on γ alumina supported MoOx as model catalyst and correlate them to the catalyst structure studied by Raman spectroscopy of the quenched catalyst bed.

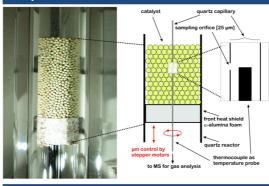
Catalyst preparation

Catalysts are prepared by incipient wetness from an aqueous solution of Ammonium heptamolybdate tetrahydrate. For the 30 wt% catalyst nine impregnation steps were necessary with 2 h drying at 120 °C between each step followed by calcination at 540 °C in air for 12 h.



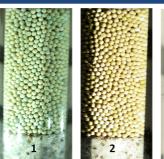
BET surface area decreased from 157 m²/g for the pure support to 107 after calcination but remains stable under reaction.

Setup² and reaction conditions



- 66 ml/min : 4 ml/min C₂H₆, 4 ml/min O₂, 58 ml/min Ar → GHSV: 520 h-1
- 132 ml/min : 8 ml/min C2H6, 8 ml/min O2, 116 ml/min Ar → GHSV: 1040 h-1
- oven temperature set to 485 °C to keep the maximum reaction temperature around 500 $^{\circ}\text{C}$ to minimize MoO₃ sublimation
- 30 mm bed length with spheres of about 1 mm diameter
- 300 um spatial resolution per mass spectrum
- 1 h activation in pure oxygen at 500 °C before each

Catalyst reaction stages and characterization by XRD



- after preparation (1) the spheres were activated for 1h pure O₂ at 500 °C prior reaction resulting in the dehydrated state (2)
- depending on flow conditions during the reaction color and oxidation state of the MoO_x species changed (3) as function of position inside the catalyst bed
- XRD diffractograms of the "as prepared" 30 wt% MoO₃ catalyst (1) shows the presence of only γ -alumina and $Al_2(MoO_4)_3$ but no crystalline MoO₃ phase
- \bullet XRD analysis of the used catalyst (3) shows Al₂(MoO₄)₃ species only in the reaction zone containing gas phase oxygen (3 - grey spheres), the dark spheres in (3) show MoO2 as major species

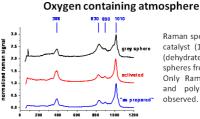
Results

Catalytic results

Total flow - 66 ml/min catalytic bed temperature [°C] 455 420 0.2 B flo∾ 0.1 CO

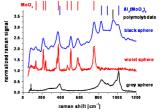
- the high loading of 30 wt% ensures a nearly complete coverage of the acidic centers of the γ-alumina support
- oxygen is fully converted in both experiments
- the main oxidation products are CO and H2O
- C2H4 is formed only in presence of gas phase oxygen and levels off at about 90 to 95 % oxygen conversion
- CO₂ is identified a secondary product by its initial zero slope
- after total conversion of gas phase oxygen ethylene is totally oxidized by lattice oxygen from the molybdate species reducing the catalyst to MoO2 (violet spheres in area B of the catalyst) as evidenced by Raman and XRD
- the MoO₂ containing spheres show a high electrical conductivity typical for MoO₂

Raman analysis



Raman spectra of the "as prepared" catalyst (1), under ${\rm O_2}$ atmosphere (dehydrated sample, 2) and the grey spheres from the oxidation zone (A). Only Raman bands of Al₂(MoO₄)₃ and poly-molybdate species are observed.

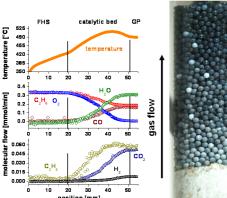
Area A, B and C of the 66 ml/min experiment



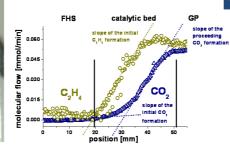
Violet spheres from area B consist purely of MoO₂. Spheres from area C are a mixture of molybdenum in the +IV and +VI state. With further time on stream also zone C will transforminto MoO2.

Reference wavenumbers taken from:

Total flow - 132 ml/min



C₂H₄ and CO₂ profiles in the 132 ml/min experiment



Conclusion

- in the oxidation zone where C2H4 is formed Mo is present as polymolybdate species
- after total oxygen consumption lattice oxygen becomes co-reactant, totally oxidizing C2H4 to CO2 reducing the catalyst to MoO₂, as shown by Raman
- C2H6 oxidation by lattice oxygen is less pronounced



Measurement of spatially resolved kinetic and spectroscopic data allows insight into the mechanism of ODH reactions.

References

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