

Research Article

Pressure Transient Analysis of Dual Fractal Reservoir

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A dual fractal reservoir transient flow model was created by embedding a fracture system simulated by a tree-shaped fractal network into a matrix system simulated by fractal porous media. The dimensionless bottom hole pressure model was created using the Laplace transform and Stehfest numerical inversion methods. According to the model's solution, the bilogarithmic type curves of the dual fractal reservoirs are illustrated, and the influence of different fractal factors on pressure transient responses is discussed. This semianalytical model provides a practical and reliable method for empirical applications.

1. Introduction

Numerous researchers have simulated the nonuniform distribution of fractures using fractal networks and have studied fluid flow behavior in fractured reservoirs. By assuming that the fracture network is fractal, Camacho-Velázquez et al. [1] studied the production decline behavior in a naturally fractured reservoir. Zhang and Tong [2] introduced a stress-sensitive coefficient and built a transient pressure analysis model for fractal reservoirs which considers stress-sensitive effects.

Jafari and Babadagli [3] illustrated the 3D permeability distribution of a reservoir using outcrop, well log, and well test data which served as the basis for applying fractal networks to a reservoir. Zhang et al. [4] solved a nonlinear flow model for a stress-sensitive dual media fractal reservoir using a finite element method.

Previous scholars often embedded fractal structures into matrix networks by using straight or intersecting lines, but this did not correctly simulate well bottom radial flow. This type of radial flow has not been sufficiently studied in the underground seepage and oil development fields.

By referring to a plant lamina's bifurcation structure, Wechsato et al. [5] used a tree-shaped fractal structure that

connected center points to different circles. The fractal network could simulate the radial flow tending toward the well bottom. Based on their research, the construction method and optimization rules for tree-shaped fractal structures [6] were formulated.

Xu and Yu [7] presented a tree-shaped fractal flow model that considered the dynamic behavior of branching tubes in a tree-shaped fractal network. Based on this model, our model's transport properties and mass transfer capabilities [8, 9] were analyzed.

Given the capillary pressure effect, the starting pressure gradient influence, and pore fractal characteristics, Yun et al. [10] developed a fractal model that describes Bingham fluid flow in porous media. Based on Yun et al. [10], Wang et al. [11] proposed a tree-shaped fractal model that considered the influence of the starting pressure gradient on Bingham fluid seepage in a porous medium.

In this paper, fractures are simulated using a tree-shaped fractal network, as it accurately simulates radial flow tending to the well bottom, and the matrix system is simulated using fractal porous media. A transient flow model of dual fractal reservoirs is then presented by embedding the fracture network into a matrix system. Factors influencing the dynamic characteristics of transient pressure responses in dual fractal

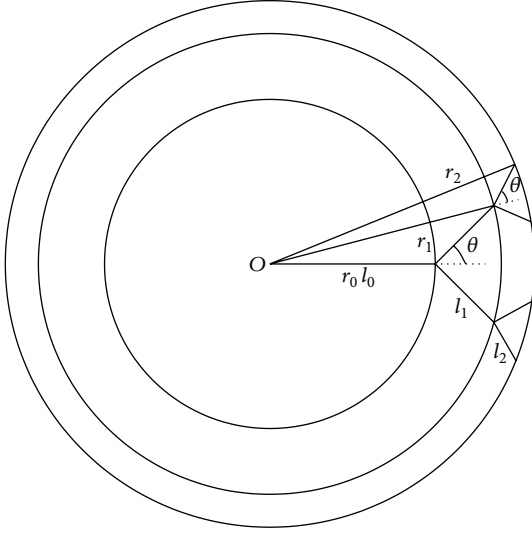


FIGURE 1: Dual fractal reservoir.

reservoirs are analyzed. This semianalytical model provides a practical and reliable method for empirical applications.

2. Physical Model

Figure 1 shows a well located in the reservoir center, O , with a thickness, h , and a well radius, r_w . The physical model assumptions are as follows.

- (1) The fractal porous media is divided into M annular sections in a tree-shaped fractal network.
- (2) Each fracture section's properties are different, but the fluid properties are identical. Matrix permeability is much lower than that of the fracture.
- (3) Rock and single-phase fluid are slightly compressible causing isothermal flow to be considered. Capillary pressure and gravity effects are neglected.
- (4) Fluid flows to the wellbore only through the fracture system. Fluid flow in the matrix and the fracture system of each section satisfies the linear flow rule.

3. Mathematical Model

3.1. Matrix System. According to fractal geometry theory, the fractal scaling law can be used to describe the cumulative size distribution of pores in matrix system [12]:

$$N_m(L \geq \lambda) = \left(\frac{\delta_{\max}}{\delta} \right)^{D_f}, \quad (1)$$

where δ is pore diameter, δ_{\max} is maximum pore diameter, and D_f is the fractal dimension of the pore space.

Tortuosity is often used to describe flow path tortuosity, as flow in porous media is tortuous. The matrix flow path tortuosity is defined as [13]:

$$T_m = \frac{L_t}{L_0}, \quad (2)$$

where L_t is the actual length of the tortuous flow path and L_0 is the straight length along the macroscopic pressure gradient.

The matrix system porosity and permeability are defined as [14]:

$$\phi_m = \frac{\pi T_m D_f}{4(2 - D_f)} \frac{\delta_{\max}^2}{A_0} \left[1 - \left(\frac{\delta_{\min}}{\delta_{\max}} \right)^{2 - D_f} \right], \quad (3)$$

$$K_m = \frac{\pi D_f}{128 T_m (4 - D_f)} \frac{\delta_{\max}^4}{A_0}, \quad (4)$$

where A_0 is the unit cell area.

3.2. Fracture System. Fracture system parameters are directly generated from a tree-shaped fractal network. Sets of branch structures form the tree-shaped fractal network. During network generation, the branches on each level must end up on the same circle with all circles having the same center of origin, O . N tubes which start at O make up the tree-shaped fractal network. The tube's initial length and diameter are l_0 and d_0 , respectively. The double branches ($n = 2$), whose angles are θ ($\theta < \pi/2$) and total network branch levels are M , are applied in this network. Furthermore, two scale factors are used in this fractal network, length ratio, α , and diameter ratio, β . The branch tube is assumed to be smooth, and tube wall thickness is ignored.

For the k th level fracture, length is given by

$$l_k = \alpha^k l_0. \quad (5)$$

For the k th level fracture, diameter is

$$d_k = \beta^k d_0. \quad (6)$$

Distance from the well to each section's boundary is defined as the radial distance, which is expressed by [8]:

$$r_k = \sum_{i=0}^k l_i \cos \theta = l_0 \left[1 + \frac{\alpha(1 - \alpha^k) \cos \theta}{1 - \alpha} \right]. \quad (7)$$

Xu et al. [8] proposed the k th level permeability expression of fracture system, which is expressed by

$$K_k = \frac{d_k^2}{32} \frac{1}{T_k}. \quad (8)$$

The k th section tortuosity of fracture systems can be obtained by the following expression:

$$T_k = \frac{l_k}{r_k - r_{k-1}} = \begin{cases} 1, & k = 0, \\ \frac{1}{\cos \theta}, & k > 0. \end{cases} \quad (9)$$

Substituting (6) and (9) into (8), the k th section permeability in the fracture system is

$$K_{fk} = N n^k \frac{d_k^2}{32} \frac{1}{T_k} = \begin{cases} \frac{N d_0^2}{32}, & k = 0, \\ \frac{N n^k \beta^{2k} d_0^2 \cos \theta}{32}, & k > 0. \end{cases} \quad (10)$$

For the k th section, total system volume can be calculated by

$$V_{tk} = \begin{cases} \pi h r_0^2, & k = 0, \\ \pi h (r_k^2 - r_{k-1}^2), & k > 0, \end{cases} \quad (11)$$

where h is the reservoir thickness.

For the k th section, pore volume of fracture systems can be calculated by

$$V_{ftk} = N n^k \frac{\pi l_k d_k^2}{4} = \frac{N \pi n^k \alpha^k \beta^{2k} l_0 d_0^2}{4}. \quad (12)$$

For the k th section, total system volume, V_{tk} , is expressed as $V_{tk} = V_{mtk} + V_{ftk}$, where V_{mtk} is total volume of the matrix system. V_{mtk} is related to the pore volume of matrix system, V_{mk} , and expressed as $V_{mtk} = \phi_m V_{mk}$, where ϕ_m is the matrix system porosity. Thus, V_{mk} can be calculated as

$$V_{mk} = \phi_m (V_{tk} - V_{ftk}). \quad (13)$$

For the k th section, porosity of a fracture system can be obtained by dividing (12) by (11):

$$\phi_{fk} = \frac{V_{ftk}}{V_{tk}} = \begin{cases} \frac{N d_0^2}{4 h l_0}, & k = 0, \\ \frac{N n^k \alpha^k \beta^{2k} l_0 d_0^2}{4 h (r_k^2 - r_{k-1}^2)}, & k > 0. \end{cases} \quad (14)$$

For the k th section, porosity of a matrix system can be obtained by the following expression:

$$\phi_{mk} = \frac{V_{mk}}{V_{tk}} = \phi_m (1 - \phi_{fk}). \quad (15)$$

The permeability of a fracture system, K_f , and the porosity of a fracture system, ϕ_f , do not change with the radial distance, r , in traditional double porosity (fracture and matrix system) reservoir transient flow models [15]. In order to compare dual fractal reservoir transient flow models with double porosity reservoir transient flow models, we have to clarify how to keep K_f and ϕ_f independent of r in dual fractal reservoir transient flow models.

Under the condition of double branches ($n = 2$), the permeability, K_{fk} , and porosity, ϕ_{fk} , of every section in a fracture system are equal; that is,

$$\begin{aligned} K_{fk} &= K_{f(k+1)}, \\ \phi_{fk} &= \phi_{f(k+1)}. \end{aligned} \quad (16)$$

Substituting (10) and (14) into (16), we can obtain: $n = 2$, $\alpha = 1$, and $\beta = 0.707$.

When β is smaller than 0.707, permeability of a fracture system increases with the radius of a dual fractal reservoir. When β is larger than 0.707, permeability of a fracture system decreases with the radius of a dual fractal reservoir.

3.3. Dual Fractal Reservoir. According to the physical model, the flow mathematical model of a dual fractal reservoir can be described as follows.

Governing differential equations in a dual fractal reservoir, we have the following.

For fracture system [15],

$$\frac{K_{fk}}{\mu} \left(\frac{\partial^2 p_{fk}}{\partial r^2} + \frac{1}{r} \frac{\partial p_{fk}}{\partial r} \right) + \frac{a K_m}{\mu} (p_{mk} - p_{fk}) = \frac{\varphi_{fk} C_{if}}{3.6} \frac{\partial p_{fk}}{\partial t} \quad r_{k-1} \leq r \leq r_k. \quad (17)$$

For matrix system [15],

$$-\frac{a K_m}{\mu} (p_{mk} - p_{fk}) = \frac{\varphi_{mk} C_{im}}{3.6} \frac{\partial p_{mk}}{\partial t} \quad r_{k-1} \leq r \leq r_k. \quad (18)$$

Initial condition:

$$p_{fk}(r, 0) = p_{mk}(r, 0) = p_i \quad (k = 0, 1, \dots, M). \quad (19)$$

Interface connecting conditions of each zone, pressure continuity [16]:

$$p_{fk} \Big|_{r=r_k} = p_{f(k+1)} \Big|_{r=r_k} \quad (k = 0, 1, \dots, M-1). \quad (20)$$

Interface connecting conditions of each zone, rate continuity [16]:

$$\frac{\partial p_{fk}}{\partial r} \Big|_{r=r_k} = \frac{k_{f(k+1)}}{k_{fk}} \frac{\partial p_{f(k+1)}}{\partial r} \Big|_{r=r_k} \quad (k = 0, 1, \dots, M-1). \quad (21)$$

Well production condition [17]:

$$q_{sf} = q + \frac{24C}{B} \frac{d p_{wf}}{dt} \quad p_{wf} = p_{f1} \Big|_{r=r_w e^{-s}}. \quad (22)$$

External boundary condition (infinite):

$$p_{fM}(r \rightarrow \infty, t) = p_i. \quad (23)$$

External boundary condition (constant pressure):

$$p_{fM}(r = r_M, t) = p_i. \quad (24)$$

External boundary condition (closed):

$$\frac{\partial p_{fM}}{\partial r} \Big|_{r=r_M} = 0. \quad (25)$$

4. Mathematical Model Solution

To simplify the mathematical model and its solution, dimensionless parameters are defined as follows [18, 19].

The dimensionless pressure of the fracture system of the k th section:

$$P_{Dfk} = \frac{K_{fk} h}{1.842 \times 10^{-3} q \mu B} (p_i - p_{fk}). \quad (26)$$

The dimensionless pressure of the matrix system of the k th section:

$$p_{Dmk} = \frac{K_{mk}h}{1.842 \times 10^{-3} q\mu B} (p_i - p_{mk}). \quad (27)$$

The dimensionless effective radius:

$$r_{De} = \frac{r}{r_w} e^S. \quad (28)$$

The dimensionless effective interface radius:

$$r_{Dek} = \frac{r_k}{r_w} e^S. \quad (29)$$

The dimensionless effective time:

$$t_{De} = \frac{3.6K_{f0}t e^{2S}}{(\varphi C_t)_{(f+m)0} \mu r_w^2}. \quad (30)$$

The dimensionless effective wellbore storage coefficient:

$$C_{De} = \frac{C_e^{2S}}{2\pi h(\varphi C_t)_{(f+m)0} r_w^2}. \quad (31)$$

The fluid capacitance coefficient of the k th section:

$$\omega_k = \frac{\phi_{fk} C_{ft}}{\phi_{mk} C_{mt} + \phi_{fk} C_{ft}}. \quad (32)$$

The interporosity flow coefficient of the k th section:

$$\lambda_k = a \frac{K_m}{K_{fk}} r_w^2. \quad (33)$$

Substituting (26)–(33) into (17)–(25), dimensionless mathematical models are obtained [20].

For a fracture system, the governing differential equation in a dual fractal reservoir is

$$\begin{aligned} \frac{\partial^2 p_{Dfk}}{\partial r_{De}^2} + \frac{1}{r_{De}} \frac{\partial p_{Dfk}}{\partial r_{De}} + \lambda_k e^{-2S} \left(\frac{K_{fk}}{K_m} p_{Dmk} - p_{Dfk} \right) \\ = \frac{\omega_k}{C_{De}} \frac{K_{f0}}{K_{fk}} \frac{\partial p_{Dfk}}{\partial (t_{De}/C_{De})} \quad r_{De(k-1)} \leq r_{De} \leq r_{Dek}; \end{aligned} \quad (34)$$

For matrix system,

$$\begin{aligned} -\lambda_k e^{-2S} \left(p_{Dmk} - \frac{K_m}{K_{fk}} p_{Dfk} \right) = \frac{1 - \omega_k}{C_{De}} \frac{K_{f0}}{K_{fk}} \frac{\partial p_{Dmk}}{\partial (t_{De}/C_{De})} \\ r_{De(k-1)} \leq r_{De} \leq r_{Dek}. \end{aligned} \quad (35)$$

Initial condition:

$$p_{Dfk}(r_{De}, 0) = p_{Dmk}(r_{De}, 0) = 0 \quad (k = 0, 1, \dots, M). \quad (36)$$

Interface connecting conditions of each zone, pressure continuity:

$$p_{Dfk} \Big|_{r_{De}=r_{Dek}} = p_{Df(k+1)} \Big|_{r_{De}=r_{Dek}} \quad (k = 0, 1, \dots, M-1). \quad (37)$$

Interface connecting conditions of each zone, rate continuity:

$$\begin{aligned} \frac{\partial p_{Dfk}}{\partial r_{De}} \Big|_{r_{De}=r_{Dek}} = \frac{K_{f(k+1)}}{K_{fk}} \frac{\partial p_{Df(k+1)}}{\partial r_{De}} \Big|_{r_{De}=r_{Dek}} \\ (k = 0, 1, \dots, M-1). \end{aligned} \quad (38)$$

Well production condition:

$$\frac{dp_{wD}}{d(t_{De}/C_{De})} - \left(r_{De} \frac{\partial p_{Df0}}{\partial r_{De}} \right) \Big|_{r_{De}=1} = 1 \quad p_{wD} = p_{Df0} \Big|_{r_{De}=1}. \quad (39)$$

External boundary condition (infinite):

$$p_{DfM}(r_{De} \rightarrow \infty, t_{De}) = 0. \quad (40)$$

External boundary condition (constant pressure):

$$p_{DfM}(r_{De} = r_{DeM}, t_{De}) = 0. \quad (41)$$

External boundary condition (closed):

$$\frac{\partial p_{DfM}}{\partial r_{De}} \Big|_{r_{De}=r_{DeM}} = 0. \quad (42)$$

The flow mathematical model in Laplace space is obtained by taking the Laplace transformation of (34)–(42) based on t_{De}/C_{De} . The flow mathematical model is as follows [20].

For fracture system,

$$\begin{aligned} \frac{d^2 \bar{p}_{Dfk}}{dr_{De}^2} + \frac{1}{r_{De}} \frac{d\bar{p}_{Dfk}}{dr_{De}} + \lambda_k e^{-2S} \left(\frac{K_{fk}}{K_m} \bar{p}_{Dmk} - \bar{p}_{Dfk} \right) \\ = \frac{\omega_k}{C_{De}} \frac{K_{f0}}{K_{fk}} z \bar{p}_{Dfk} \quad r_{De(k-1)} \leq r_{De} \leq r_{Dek}. \end{aligned} \quad (43)$$

For matrix system,

$$\begin{aligned} -\lambda_k e^{-2S} \left(\bar{p}_{Dmk} - \frac{K_m}{K_{fk}} \bar{p}_{Dfk} \right) = \frac{1 - \omega_k}{C_{De}} \frac{K_{f0}}{K_{fk}} z \bar{p}_{Dmk} \\ r_{De(k-1)} \leq r_{De} \leq r_{Dek}. \end{aligned} \quad (44)$$

Initial condition:

$$\begin{aligned} \bar{p}_{Dfk}(r_{De}, 0) = \bar{p}_{Dmk}(r_{De}, 0) = 0 \\ (k = 0, 1, \dots, M). \end{aligned} \quad (45)$$

Interface connecting conditions of each zone, pressure continuity:

$$\bar{p}_{Dfk} \Big|_{r_{De}=r_{Dek}} = \bar{p}_{Df(k+1)} \Big|_{r_{De}=r_{Dek}} \quad (k = 0, 1, \dots, M-1). \quad (46)$$

Interface connecting conditions of each zone, rate continuity:

$$\begin{aligned} \frac{d\bar{p}_{Dfk}}{dr_{De}} \Big|_{r_{De}=r_{Dek}} = \frac{K_{f(k+1)}}{K_{fk}} \frac{d\bar{p}_{Df(k+1)}}{dr_{De}} \Big|_{r_{De}=r_{Dek}} \\ (k = 0, 1, \dots, M-1). \end{aligned} \quad (47)$$

Well production condition:

$$z\bar{p}_{wD} - \left(r_{De} \frac{d\bar{p}_{Df0}}{dr_{De}} \right) \Big|_{r_{De}=1} = \frac{1}{z} \quad \bar{p}_{wD} = \bar{p}_{Df0} \Big|_{r_{De}=1}. \quad (48)$$

External boundary condition (infinite):

$$\bar{p}_{DfM}(r_{De} \rightarrow \infty, z) = 0. \quad (49)$$

External boundary condition (constant pressure),

$$\bar{p}_{DfM}(r_{De} = r_{DeM}, z) = 0. \quad (50)$$

External boundary condition (closed).

$$\frac{\partial \bar{p}_{DfM}}{\partial r_{De}} \Big|_{r_{De}=r_{DeM}} = 0. \quad (51)$$

In (43) and (44), the general solution of \bar{p}_{Dfjk} is calculated by

$$\bar{p}_{Dfjk} = A_k I_0 \left(r_{Dek} \sqrt{S_k(z)} \right) + B_k K_0 \left(r_{Dek} \sqrt{S_k(z)} \right) \quad (52)$$

($k = 0, 1, \dots, M$).

The derivative of \bar{p}_{Dfjk} in (52) is calculated by

$$\frac{d\bar{p}_{Dfjk}}{dr_{De}} = \sqrt{S_k(z)} A_k I_1 \left(r_{Dek} \sqrt{S_k(z)} \right) - \sqrt{S_k(z)} B_k K_1 \left(r_{Dek} \sqrt{S_k(z)} \right) \quad (k=0, 1, \dots, M). \quad (53)$$

Substitute (52) and (53) into well production condition equation (48);

$$z\bar{p}_{wD} - \sqrt{S_0(z)} A_0 I_1 \left(\sqrt{S_0(z)} \right) + \sqrt{S_0(z)} B_0 K_1 \left(\sqrt{S_0(z)} \right) = \frac{1}{z}, \quad (54)$$

$$\bar{p}_{wD} = A_0 I_0 \left(\sqrt{S_0(z)} \right) + B_0 K_0 \left(\sqrt{S_0(z)} \right).$$

Substitute (52) and (53) into interface connecting condition equation (46);

$$\begin{aligned} & A_k I_0 \left(r_{Dek} \sqrt{S_k(z)} \right) + B_k K_0 \left(r_{Dek} \sqrt{S_k(z)} \right) \\ &= A_{k+1} I_0 \left(r_{Dek} \sqrt{S_{k+1}(z)} \right) \\ &+ B_{k+1} K_0 \left(r_{Dek} \sqrt{S_{k+1}(z)} \right) \quad (k = 0, 1, \dots, M - 1). \end{aligned} \quad (55)$$

Substitute (52) and (53) into interface connecting condition equation (47);

$$\begin{aligned} & A_k \sqrt{S_k(z)} I_1 \left(r_{Dek} \sqrt{S_k(z)} \right) - B_k \sqrt{S_k(z)} K_1 \left(r_{Dek} \sqrt{S_k(z)} \right) \\ &= \frac{K_{f(k+1)}}{K_{fk}} A_{k+1} \sqrt{S_k(z)} I_1 \left(r_{Dek} \sqrt{S_k(z)} \right) \\ &- \frac{K_{f(k+1)}}{K_{fk}} B_{k+1} \sqrt{S_k(z)} K_1 \left(r_{Dek} \sqrt{S_k(z)} \right) \end{aligned} \quad (k = 0, 1, \dots, M - 1). \quad (56)$$

Substitute (52) and (53) into external boundary condition equations (49)–(51);

$$A_M = 0, \quad (57)$$

$$A_M I_0 \left(r_{DeM} \sqrt{S_M(z)} \right) + B_M K_0 \left(r_{DeM} \sqrt{S_M(z)} \right) = 0, \quad (58)$$

$$A_M I_1 \left(r_{DeM} \sqrt{S_M(z)} \right) - B_M K_1 \left(r_{DeM} \sqrt{S_M(z)} \right) = 0. \quad (59)$$

\bar{p}_{Dfjk} , A_k , and B_k ($k = 0, 1, \dots, M$) can be obtained by solving the simultaneous equations (54)–(59). In (54)–(59), the tree-shaped fractal network parameters can be directly used to express the parameters of the permeability ratio, $k_{f(k+1)}/k_{fk}$, the dimensionless effective interface radius, r_{Dek} , and the function, $S_k(z)$.

The dimensionless effective interface radius expression can be derived by substituting (7) into (29):

$$r_{Dek} = \frac{l_0}{r_w} \left[1 + \frac{\alpha (1 - \alpha^k) \cos \theta}{1 - \alpha} \right] e^S. \quad (60)$$

The permeability ratio can be calculated using (10):

$$\frac{K_{f(k+1)}}{K_{fk}} = \begin{cases} n\beta^2 \cos \theta, & k = 0, \\ n\beta^2, & k > 0. \end{cases} \quad (61)$$

The expression of the function $S_k(z)$ is as follows:

$$S_k(z) = \frac{(K_{f0}/K_{fk}) \lambda_k (1 - \omega_k) z}{(K_{f0}/K_{fk}) (1 - \omega_k) e^{2S} z + \lambda_k C_{De}} + \frac{K_{f0} \omega_k}{K_{fk} C_{De}} z, \quad (62)$$

where

$$\frac{K_{f0}}{K_{fk}} = (n\beta^2)^{-k}. \quad (63)$$

The interporosity flow coefficient, λ_k , can be obtained by substituting (4) and (10) into (33), and the fluid capacitance coefficient, ω_k , can be obtained by substituting (3), (14), and (15) into (32).

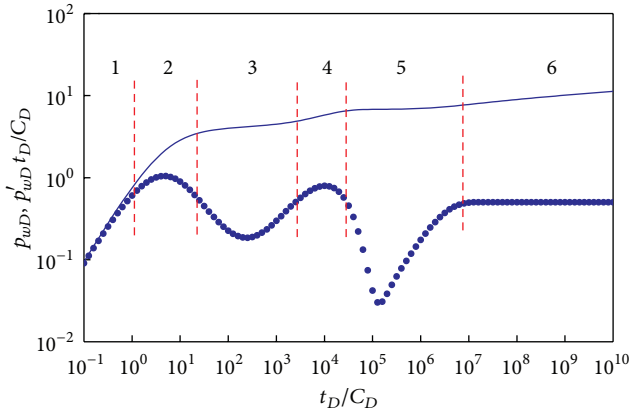


FIGURE 2: Pressure type curves of dual fractal reservoirs ($\alpha = 1$, $\beta = 0.707$, $\theta = 1$, $N = 4$, $M = 10$, $l_0 = 10$ m, $d_0 = 0.05$ m, $D_f = 1.5$, $T_m = 4$, $r_w = 0.1$ m, $S = -1$, $C_{De} = 0.0001$, $h = 10$ m, $C_{mt} = 2.2 \times 10^{-5}$ MPa $^{-1}$, and $C_{ft} = 1 \times 10^{-4}$ MPa $^{-1}$).

5. Analysis of Type Curve Characteristics

Dimensionless bottom hole pressure in Laplace space, p_{wfD} , is obtained by solving the linear equations (54)–(57) using the Stehfest numerical inversion method. The bilogarithmic type curves of the dual fractal reservoirs can then be illustrated.

In a condition of closed top and bottom boundary, the transient flow process, which has six flow regimes, can be clearly shown (Figure 2). The full and dashed lines represent pressure and pressure derivative curves, respectively. Regime 1 is the pure wellbore storage regime. Pressure and its derivative curves appear as upward straight lines with a slope of 1. Regime 2 is the transition flow regime. The shape of the derivative curve looks like an “arch,” which is influenced by the wellbore storage coefficient and skin factor. Regime 3 is the fracture system inter-porosity flow regime. The pressure derivative curve is V shaped, which depicts the response of inter-porosity flow between the fractures that are heterogeneously distributed. This inter-porosity flow regime is caused by spread of the pressure wave through the fracture system. Regime 4 is the fracture system radial flow regime. Slope of the pressure derivative curve is zero. In this scenario, the pressure wave spreads through the whole fracture system and begins to spread to the matrix system. Regime 5 is the inter-porosity flow regime of matrix system to fracture system. The pressure derivative curve is also V shaped. However, it is influenced by spread of the pressure wave through the matrix system. Regime 6 is the total system radial flow regime. The pressure derivative curve converges to a horizontal line, which depicts the response of the pressure dynamic balance state in the whole system.

Figure 3 shows the type curve characteristics affected by pore tortuosity, T_m . As T_m increases, the two V shaped curves deepen and shift to the right, which indicates a longer lasting inter-porosity flow regime and a delayed occurring time of the radial flow regime in the fracture system. It also indicates a delayed inter-porosity flow regime from matrix to fracture. An increase in the initial branch number, N , has a similar

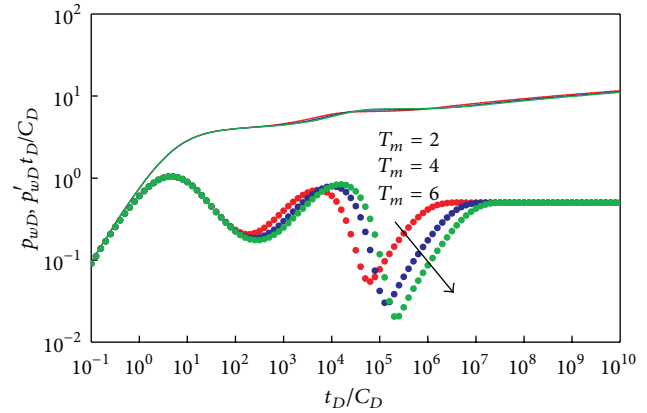


FIGURE 3: Effect of pore tortuosity (T_m) on type curves ($\alpha = 1$, $\beta = 0.707$, $\theta = 1$, $N = 4$, $M = 10$, $l_0 = 10$ m, $d_0 = 0.05$ m, $D_f = 1.5$, $r_w = 0.1$ m, $S = -1$, $C_{De} = 0.0001$, $h = 10$ m, $C_{mt} = 2.2 \times 10^{-5}$ MPa $^{-1}$, and $C_{ft} = 1 \times 10^{-4}$ MPa $^{-1}$).

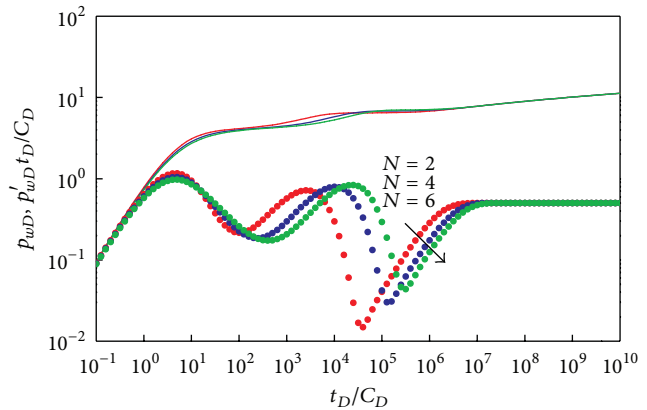


FIGURE 4: Effect of initial branch number (N) on type curves ($\alpha = 1$, $\beta = 0.707$, $\theta = 1$, $M = 10$, $l_0 = 10$ m, $d_0 = 0.05$ m, $D_f = 1.5$, $T_m = 4$, $r_w = 0.1$ m, $S = -1$, $C_{De} = 0.0001$, $h = 10$ m, $C_{mt} = 2.2 \times 10^{-5}$ MPa $^{-1}$, and $C_{ft} = 1 \times 10^{-4}$ MPa $^{-1}$).

influence on flow regimes 3, 4, and 5 as an increase in T_m , but the V shaped curves associated with the pressure derivative become shallower and shift to the right (Figure 4).

Figure 5 exhibits the type curve characteristics affected by pore fractal dimension, D_f . Permeability of matrix system, K_m , and porosity of matrix system, ϕ_m , increase with an increase in D_f . A larger K_m leads to greater flow capacity in the matrix system with an earlier transition to regime 5. A larger ϕ_m leads to a larger supplying capacity in the matrix system, and regime 5 occurs earlier and lasts longer. As D_f increases, regime 5 occurs earlier and lasts longer, which is depicted as a deeper and wider second V shaped pressure derivative curve.

Figure 6 shows the type curve characteristics affected by branch angle, θ . Permeability of fracture system, K_f , decreases with an increase in θ . A smaller K_f leads to lower flow capacity in the fracture system with an earlier transition to regime 5. Porosity of fracture system, ϕ_f , increases with an

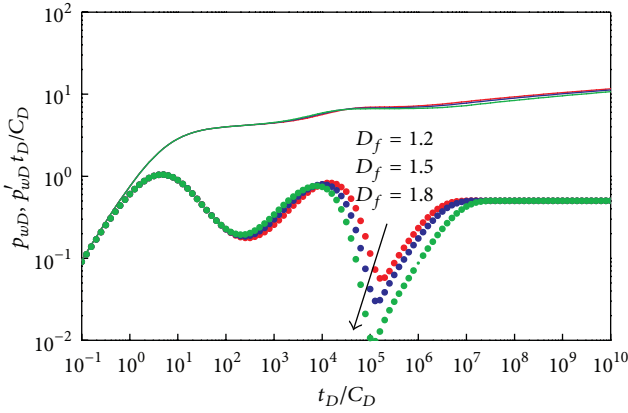


FIGURE 5: Effect of pore fractal dimension (D_f) on type curves ($\alpha = 1, \beta = 0.707, \theta = 1, N = 4, M = 10, l_0 = 10 \text{ m}, d_0 = 0.05 \text{ m}, T_m = 4, r_w = 0.1 \text{ m}, S = -1, C_{De} = 0.0001, h = 10 \text{ m}, C_{mt} = 2.2 \times 10^{-5} \text{ MPa}^{-1}$, and $C_{ft} = 1 \times 10^{-4} \text{ MPa}^{-1}$).

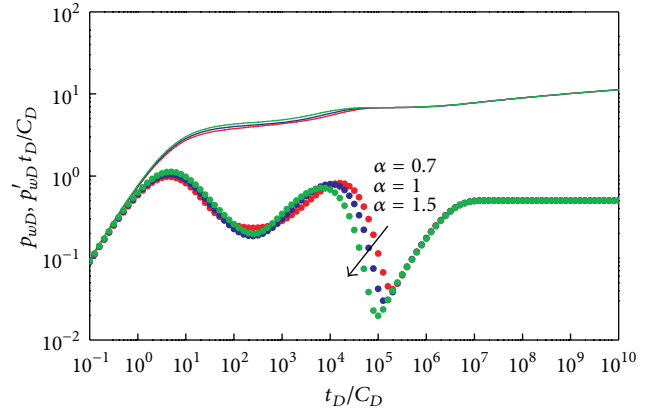


FIGURE 7: Effect of length ratio (α) on type curves ($\beta = 0.707, \theta = 1, N = 4, M = 10, l_0 = 10 \text{ m}, d_0 = 0.05 \text{ m}, D_f = 1.5, T_m = 4, r_w = 0.1 \text{ m}, S = -1, C_{De} = 0.0001, h = 10 \text{ m}, C_{mt} = 2.2 \times 10^{-5} \text{ MPa}^{-1}$, and $C_{ft} = 1 \times 10^{-4} \text{ MPa}^{-1}$).

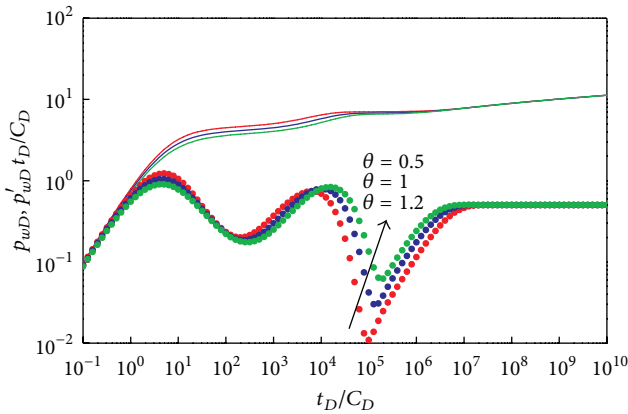


FIGURE 6: Effect of branch angle (θ) on type curves ($\alpha = 1, \beta = 0.707, N = 4, M = 10, l_0 = 10 \text{ m}, d_0 = 0.05 \text{ m}, D_f = 1.5, T_m = 4, r_w = 0.1 \text{ m}, S = -1, C_{De} = 0.0001, h = 10 \text{ m}, C_{mt} = 2.2 \times 10^{-5} \text{ MPa}^{-1}$, and $C_{ft} = 1 \times 10^{-4} \text{ MPa}^{-1}$).

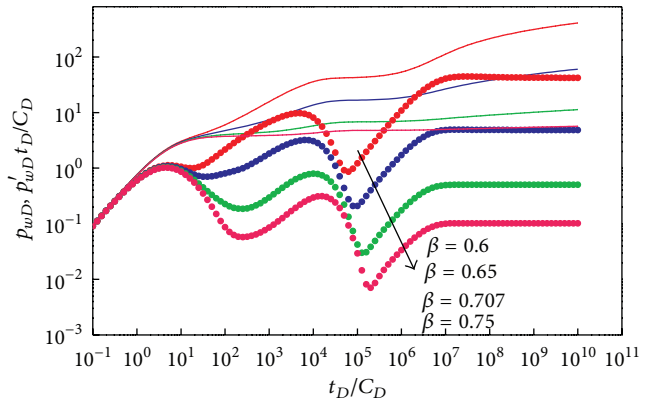


FIGURE 8: Effect of diameter ratio (β) on type curves ($\alpha = 1, \theta = 1, N = 4, M = 10, l_0 = 10 \text{ m}, d_0 = 0.05 \text{ m}, D_f = 1.5, T_m = 4, r_w = 0.1 \text{ m}, S = -1, C_{De} = 0.0001, h = 10 \text{ m}, C_{mt} = 2.2 \times 10^{-5} \text{ MPa}^{-1}$, and $C_{ft} = 1 \times 10^{-4} \text{ MPa}^{-1}$).

increase in θ . A larger ϕ_f leads to greater supplying capacity in the fracture system, and regime 5 occurs later with a shorter duration. When θ increases, it has the opposite effect on flow regime 5 as an increase in D_f .

Figure 7 exhibits the type curve characteristics affected by the length ratio, α . ϕ_f decreases with an increase in α . A smaller ϕ_f leads to a lower supplying capacity in the fracture system and an earlier transition to a longer lasting regime 5. When a large α increases, regime 5 occurs earlier, which manifests in a deeper and wider second V shaped type curve.

Figure 8 exhibits the type curve characteristics affected by diameter ratio, β . K_f and ϕ_f increase with an increase in β . A larger K_f leads to larger flow capacity in the fracture system and a later transition to regime 5. A larger ϕ_f leads to greater supplying capacity in the fracture system with a later and shorter regime 5. When β is smaller than 0.707, K_f increases with an increase in r , and when β is greater than 0.707, K_f decreases with r . β affects all regimes except for

pure wellbore storage and transition flow regime, which are not affected by K_f . A larger β leads to a lower location of the dimensionless pressure curve, and regime 5 occurs later, resulting in a shallower and narrower second V shaped type curve. When β equals the critical value of 0.707 (16), the horizontal line representing regime 6 equals 0.5.

Figures 9 and 10 exhibit the type curve characteristics affected by total branch level, M , when diameter ratio, β , is 0.65 and 0.75, respectively. Radius, r , increases with an increase in M . Additionally, r enhances the type curve characteristics affected by M . When β is less than 0.707, a large M leads to a higher dimensionless pressure curve, and vice versa, when β is greater than 0.707, a large M leads to a lower dimensionless pressure curve.

6. Conclusions

The transient flow model for pressure responses in dual fractal reservoirs is established and solved, type curves are

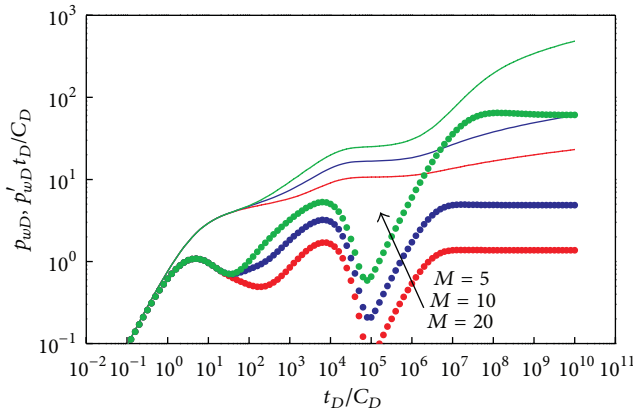


FIGURE 9: Effect of total branch level (M) on type curves ($\alpha = 1$, $\beta = 0.65$, $\theta = 1$, $N = 4$, $M = 10$, $l_0 = 10$ m, $d_0 = 0.05$ m, $D_f = 1.5$, $T_m = 4$, $r_w = 0.1$ m, $S = -1$, $C_{De} = 0.0001$, $h = 10$ m, $C_{mt} = 2.2 \times 10^{-5}$ MPa $^{-1}$, and $C_{ft} = 1 \times 10^{-4}$ MPa $^{-1}$).

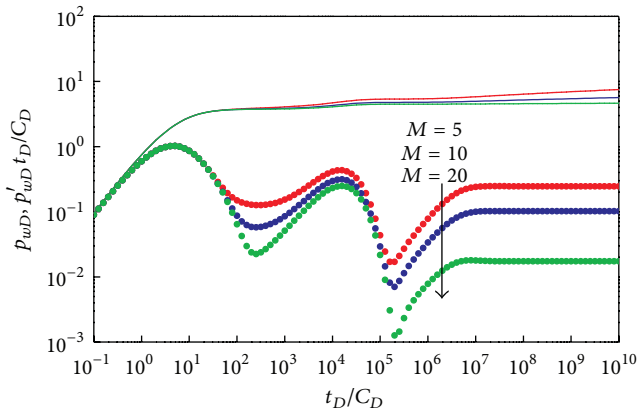


FIGURE 10: Effect of total branch level (M) on type curves ($\alpha = 1$, $\beta = 0.65$, $\theta = 1$, $N = 4$, $M = 10$, $l_0 = 10$ m, $d_0 = 0.05$ m, $D_f = 1.5$, $T_m = 4$, $r_w = 0.1$ m, $S = -1$, $C_{De} = 0.0001$, $h = 10$ m, $C_{mt} = 2.2 \times 10^{-5}$ MPa $^{-1}$, and $C_{ft} = 1 \times 10^{-4}$ MPa $^{-1}$).

illustrated, and dual fractal flow behavior characteristics are analyzed. The following conclusions were obtained.

- (1) Fracture and matrix systems can be simulated using a tree-shaped fractal network and fractal porous media, respectively.
- (2) Six flow regimes for pressure type curves can be established. Type curves are dominated by fracture and matrix fractal parameters. These various parameters affect type curves differently.
- (3) Type curves are dominated by external boundary conditions, fractal parameters the fluid capacitance coefficient and the inter-porosity flow factor.
- (4) Semianalytical dual fractal modeling is suitable for various naturally fractured oil or gas reservoirs and provides a practical method to solve empirical cases.

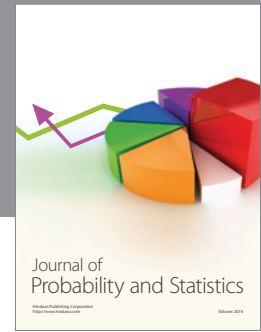
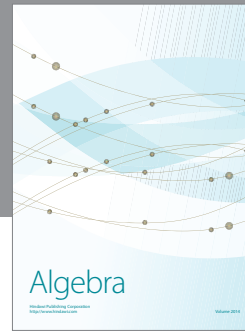
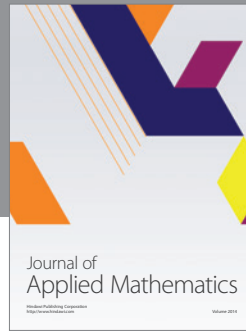
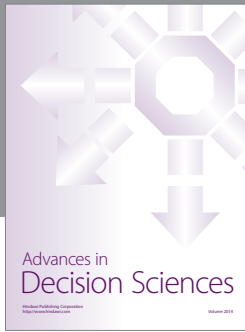
Acknowledgments

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