

Kinetic modeling of heavy metal sorption by vinyl pyridine based copolymer

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Abstract

Commercial macroporous poly(4-vinylpyridine-co-divinylbenzene) [P4VPD], known as Reillex-425, was characterized by mercury porosimetry, nitrogen physisorption, Fourier transformed infrared (FTIR) spectroscopy and elemental analysis. Sorption rates of P4VPD for Cu(II), Co(II) and Cr(VI) ions were determined in static non-competitive experiments, at room temperature (298 K). Rapid sorption was observed, especially for Co(II), with half time, $t_{1/2}$, of 1.5 min and high experimental maximal capacity, Q_{max} , of 3.08 mmol g⁻¹. Four kinetic models (pseudo-first and pseudo-second order model, intraparticle diffusion and Boyd model) were used for analyzing metal sorption by P4VPD. Metal ions sorption is well represented by the pseudo-second-order model, with definite influence of pore and film diffusion on sorption rates.

Keywords: poly(4-vinylpyridine-co-divinylbenzene) macroporous copolymer; Cu(II), Co(II) and Cr(VI) ions sorption; kinetic models.

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Kinetic modeling of metal sorption is extremely important since the effectiveness of the sorption process for pollutant removal from aqueous solutions strongly depends on the sorption dynamics. Predicting the rate at which sorption takes place in a given system is one of the crucial factors in sorption system design [1]. Modeling of sorption kinetics can be carried out by employing chemical reaction-based and particle diffusion-based models. Among the most commonly encountered expressions in pollutant sorption studies are Lagrege's pseudo-first-order and Ho's pseudo-second-order [2]. However, these and other chemical reaction-based kinetic models do not consider the importance of particle diffusion processes in metal sorption by porous materials [3]. Therefore, it is necessary to include diffusion-based kinetic modeling in order to elucidate the role of diffusion processes, such as film and intraparticle diffusion.

Heavy metal pollution is an environmental problem of worldwide concern. Adsorption is an efficient and cost-effective process for treatment of water and industrial effluents. Numerous inorganic and organic adsorbents can be applied for heavy metal removal from wastewaters; polymeric chelating and ion-exchange resins are widely utilized for these purposes.

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Cross-linked functional polymers (CFPs) based on 4-vinylpyridine (4VP) have been widely used as supports for adsorbents, metal catalysts, biomedical applications, etc. For example, quaternized poly(4-vinylpyridine-co-divinylbenzene) (P4VPD, Reillex™ HPQ) has been used for uranium sorption from acidic sulfate solution [4], hexavalent chromium removal from aqueous solutions [5] and perchlorate sorption from the acidic solutions [6]. Poly(acrylamide) grafted onto cross-linked P4VPD (Reillex 425) and quaternized with potassium chloroacetate has been used for removal of mercury from aqueous solutions [7]. Also, iodomethylated P4VPD are considered as promising polymer-supported catalysts [8].

In general, CFPs can be obtained in two ways: by treating the pre-synthesized polymer with an appropriate reagent to introduce desired moieties or by polymerization of a monomer which already carries the required functional group. The former route predominates in practice, *i.e.*, the pre-synthesized copolymers are functionalized prior to application. However, additional functionalization of porous copolymers is not always recommended. Some problems can arise, such as undesired side reactions, changes of pore structure as the consequence of chemical modification, etc. Also, the introduction of very selective, but bulky ligands can have a negative effect on selectivity and metal uptake capacity of a chelating polymer [9].

To the best of our knowledge, only few papers regarding application of porous 4VP based copolymers not additionally reacted to introduce functionalities other than pyridine nitrogen evidence their effecti-

veness. For example, REILLEX-425 (P4VPD) supported catalyst with Co(II) and Cr(VI) ions was successfully applied in aerobic liquid/phase partial oxidation of cyclohexane [10] as well as for deperoxidation of cyclohexyl hydroperoxide under mild conditions [11].

Also, macroporous crosslinked 4VP and ethylene glycol dimethacrylate copolymer, (P4VPE) synthesized in the presence of the inert component consisting of cyclohexanol and *n*-alkanes was used successfully for heavy metal ions sorption from aqueous solutions [12].

In this study, four kinetic models (chemical reaction- and diffusion-based) were used for correlating the kinetic data of Cu(II), Co(II) and Cr(VI) uptake by commercial macroporous REILLEX-425, P4VPD, from aqueous solutions.

EXPERIMENTAL

Analysis and spectroscopy

Macroporous P4VPD (REILLEX-425), produced by Reilly Tarr & Chemical Corporation was used as received in sorption experiments. All other reagents and solvents were purchased from commercial sources and used as supplied. Copper(II), cobalt(II) and chromium(VI) solutions were prepared from reagent grade copper chloride (Kemika), cobalt chloride (Carlo Erba) and potassium dichromate salt (Sigma-Aldrich), respectively, using deionized water.

The copolymer samples were analyzed for their carbon, hydrogen and nitrogen content using the Vario EL III device (GmbH Hanau Instruments, Germany). Elemental analysis was calculated from multiple determinations with $\pm 0.2\%$ agreement. The IR spectra were recorded in KBr pellets on a Perkin-Elmer FT-IR 1725X spectrophotometer ($4000\text{--}400\text{ cm}^{-1}$) with DGTS detector and IRDM software. The concentration of metal ions was measured by flame atomic absorption spectrometry (FAAS, SpektrAA Varian Instruments).

The pore size distribution of P4VPD was determined by mercury porosimetry using a Carlo Erba Model 2000 instrument, operating in the interval of 0.1–200 MPa. Sample preparation was performed at room temperature and pressure of 0.5 kPa. Nitrogen adsorption–desorption isotherms were determined on Sorptomatic 1990 Thermo Finnigan automatic system using nitrogen physisorption at 77 K. Before measurement, samples were outgassed at 403 K for 10 h.

Batch metal-uptake experiments

The sorption of Cu(II), Co(II) and Cr(VI) ions from aqueous solutions (initial metal concentrations 0.05 M) was investigated in batch experiments under non-competitive conditions, at room temperature (298 K). P4VPD (2.0 g) was soaked in 5 cm³ of buffer solution (NaOAc/HOAc, pH 5.5) for 1 h. After that, the copo-

lymer was contacted with 72.5 cm³ of metal salt solution (0.05M) and 72.5 cm³ of buffer solution. At appropriate times in each experiment, 0.5 cm³ aliquots were removed, diluted to 50 cm³ and used for metal concentration measurements. The reproducibility of the sorption experiments results was verified in triplicate. Standard statistical methods were used to determine the mean values and standard deviations for each set of data.

The amount of metal ions sorbed onto unit mass of macroporous copolymer beads (sorption capacity, mmol g⁻¹) was calculated by using the following expression:

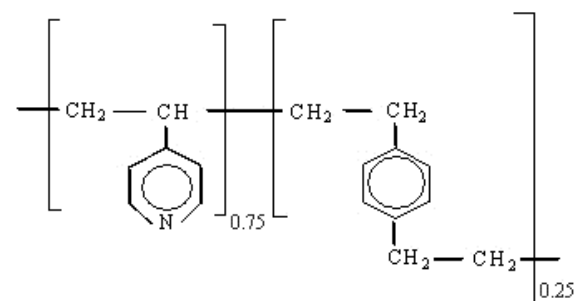
$$Q = \frac{(C_0 - C) \times V}{m} \quad (1)$$

where C_0 and C are the concentrations of the metal ions in the initial solution and in the aqueous phase after treatment for certain period of time, respectively (in mmol cm⁻³), V is the volume of the aqueous phase (cm³) and m is the amount of the copolymer beads used for the experiment (g).

RESULTS AND DISCUSSION

Characterization of P4VPD beads

The commercial macroporous poly(4-vinylpyridine-co-divinylbenzene), REILLEX-425 (P4VPD), is declared by the manufacturer as 4-vinylpyridine crosslinked with ca. 25% DVB and particle size of ca. 60 mesh (60 mesh equates to 250 μm). The assumed structural formula representation of P4VPD is given in Scheme 1.



Scheme 1. Structure of commercial macroporous P4VPD.

The elemental analysis of P4VPD yields: 78.58% C, 7.65% H, and 8.77% N. From these data, pyridine group concentration of 6.27 mmol g⁻¹ was calculated.

The structure and composition of Reillex 425 (as supplied by the manufacturer) was further verified by FTIR spectroscopy. The characteristic C=C and C=N vibrations of pyridine ring give rise to the absorption bands at 1600, 1557, 1492 and 1417 cm⁻¹ (Figure 1) [13,14]. The band at 3024 cm⁻¹ is assigned to the C-H group vibration in the aromatic ring. The absorption

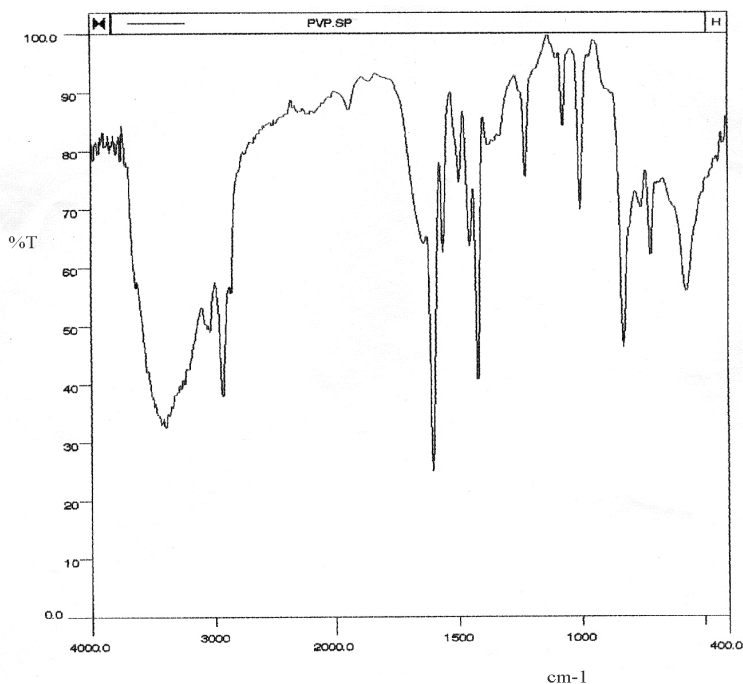


Figure 1. FTIR Spectrum of P4VPD.

bands at 1070 and 100 cm^{-1} correspond to the in-plane and out-of-plane rings C–H bending, respectively [13]. The presence of the vibration at 823 cm^{-1} in the spectrum is attributed to disubstituted aromatic rings of the copolymer. The adsorption bands at 2924 and 1450 cm^{-1} are assigned to the CH_2 of the ethyl group or aliphatic chain [14].

Two complementary methods were used for a proper evaluation of porous structure of P4VPD beads, mercury porosimetry and determination of nitrogen adsorption-desorption isotherms. The first one enables the detection of porous structure from macropores down to larger mesopores, while physisorption of nitrogen provides the most reliable results for pores in the micro- and mesopore regions [15].

Cumulative pore volume, V_{cum} , and pore diameter which corresponds to half of the pore volume, $d_{V/2}$, of P4VPD were calculated from the cumulative pore volume distribution curves while specific surface area, S_{Hg} , calculation was based on cylindrical pore model as described in literature [15,16]. Specific surface area, S_{BET} , of P4VPD was calculated by using the BET (Brunauer, Emmett and Teller) Equation [17]. The micropores, V_{micro} were analyzed using the Dubinin–Radushkevich Method [18]. Pore diameter distribution curves in mesopore region were obtained according to the Barrett, Joyner, Halenda (BJH) Method [19]. Mean pore diameter, d_{BJH} , was derived from the pore diameter distribution curve. The value of mesopore volume, V_{meso} , obtained from nitrogen adsorption-desorption isotherms

and calculated using the BJH method is lower than V_{cum} obtained from mercury porosimetry data. The relevant porosity parameters of P4VPD used in sorption tests, obtained by nitrogen physisorption and mercury porosimetry measurements are collected in Table 1.

Table 1. Relevant P4VPD porosity parameters

$S_{\text{Hg}} / \text{m}^2 \text{g}^{-1}$	60
$d_{V/2} / \text{nm}$	80
$S_{\text{BET}} / \text{m}^2 \text{g}^{-1}$	52 [11]
$V_{\text{micro}} / \text{cm}^3 \text{g}^{-1}$	0.022 [11]
$V_{\text{meso}} / \text{cm}^3 \text{g}^{-1}$	0.159 [11]
$V_{\text{cum}} / \text{cm}^3 \text{g}^{-1}$	0.748 [11]
Mean pore diameter, nm	77 [11]

Sorption kinetics

From the standpoint of potential application, one of the most important properties of the chelating polymers is the rate at which sorption reaches equilibrium. Rapid sorption of metal ions is advantageous, providing a short residence time required for the completion of the actual process.

The pH value of 5.5 was selected for the sorption experiments as close to neutral as possible, having in mind that at pH values higher than 6, significant hydrolysis of Co(II) and Cu(II) occurs at high concentrations of the order of magnitude used in this study (0.05 M) [20–22]. Thus precipitation of poorly soluble species occurs and a decline in Co(II) and Cu(II) supernatant con-

centrations cannot be ascribed to adsorptive removal by P4VPD.

The amount of Co^{2+} sorbed by P4VPD rapidly increases with time reaching high maximal capacity already after 30 min (Figure 2). The uptake of Cu(II) and Cr(VI) is considerably lower, suggesting higher affinity of P4VPD towards Co^{2+} at given pH.

The sorption of Co(II) on P4VPD was found to be very fast. After 5 min, the amount of sorbed Co(II) ions was 90%, while after 30 min 97% was sorbed. The Cu(II) and Cr(VI) maximal sorption capacities were considerably lower in comparison with Co(II). The sorption half time, $t_{1/2}$, defined as the time required to reach 50% of the total sorption capacity, for all metals was below 10 min (Table 2).

pH of the aqueous solution affects the surface charge of the adsorbent as well as metal speciation [23]. In the pH range 2.0–6.0 different forms of chromium ions such as dichromate ($\text{Cr}_2\text{O}_7^{2-}$), hydrochromate (HCrO_4^-), and polychromates ($\text{Cr}_3\text{O}_{10}^{2-}$, $\text{Cr}_4\text{O}_{13}^{2-}$) co-exist, of which HCrO_4^- predominates [24]. The dichromate ion ($\text{Cr}_2\text{O}_7^{2-}$) is the dimer of HCrO_4^- which is formed when the concentration of chromium exceeds $\sim 1 \text{ g dm}^{-3}$, applicable here.

Pyridine nitrogen is not protonated to a significant extent at the pH of the experiment ($\text{p}K_a = 5.25$ [25]) and the only possible interaction with the resin is hyd-

rogen bonding. Therein lies the explanation for such low sorption capacity of P4VPD for Cr(VI). It can be presumed that Cr(VI) sorption would be enhanced at low pH. Lončarević *et al.* [11] have shown that Cr(VI) attaches to pyridine nitrogen of P4VPD in the form of dichromate anion.

On the other hand, positively charged Co(II) and Cu(II) cations form coordination complexes with the nitrogen atom of the pyridine group as was demonstrated in some previous studies of poly(4-vinylpyridine-co-divinylbenzene) [11,13]. The evident disparity in Co(II) and Cu(II) cations behavior stems most probably from the differing nature of these cations and their affinity for pyridine nitrogen (borderline Lewis base): while Cu(II) is classified as a soft Lewis acid, Co(II) falls under the borderline category and consequently the sorption capacity of P4VPD for the latter cation is high [26,27].

The $t_{1/2}$ values obtained for P4VPD are comparable with literature data. Sugii *et al.* found the $t_{1/2}$ values for Cu(II) and Ni(II) sorption on P4VPD to be 3 and 5 min, respectively [28]. Also, they found higher Cu(II) sorption rates for P4VPE than for P4VPD in acetate buffer [29]. The $t_{1/2}$ values for Hg(II) sorption on P4VPD quaternized with 2-chloroacetamide were 4 and 14 min from diluted mercury acetate and mercury chloride solutions, respectively [30].

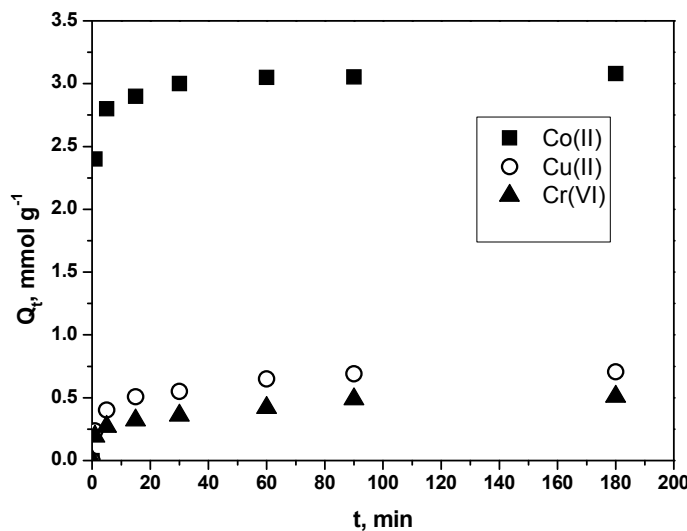


Figure 2. Sorption of Cu(II), Co(II) and Cr(VI) ions versus time, on P4VPD (metal ions initial concentration 0.05 M, pH 5.5).

Table 2. Sorption capacities after 5 min, Q_5 , and 30 min, Q_{30} , maximum sorption capacities, Q_{max} , and the sorption half time, $t_{1/2}$, for heavy metal sorption on P4VPD

Metal	Q_5		Q_{30}		Q_{max}		$t_{1/2} / \text{min}$
	mmol g^{-1}	mg g^{-1}	mmol g^{-1}	mg g^{-1}	mmol g^{-1}	mg g^{-1}	
Co(II)	2.80	165	3.00	177	3.08	181	1.5
Cu(II)	0.39	24.8	0.54	34.3	0.72	45.7	6
Cr(VI)	0.27	14.0	0.33	17.2	0.49	25.5	5

Kinetic modeling

Sorption mechanisms depend on the sorbate-sorbent interactions and the system conditions, making it impossible to classify sorption mechanisms by solute type [3]. A logical classification based on kinetic models was introduced and widely accepted. In order to examine the controlling mechanism of heavy metals sorption processes by P4VPD, such as mass transfer and chemisorption, several equations (the pseudo-first, the pseudo-second order, intraparticle diffusion and Boyd model) were tested to interpret the experimental data.

Pseudo-first and pseudo-second order equations

Probably the earliest known and one of the most widely used kinetic equations so far for the sorption of a solute from a liquid solution is Lagergren's Equation or the pseudo-first order equation [31]:

$$\log(Q_e - Q_t) = \log Q_e - \frac{(k_1 t)}{2.303} \quad (2)$$

where k_1 is the rate constant of pseudo-first-order sorption (min^{-1}), Q_e and Q_t denote the amounts of sorbed metal ions at equilibrium and at time t (mmol g^{-1}), respectively. A plot of $\log(Q_e - Q_t)$ versus t should give a straight line to confirm the applicability of the kinetic model. In a true first-order process, $\log(Q_e)$ should be equal to the intercept of a plot $\log(Q_e - Q_t)$ against t .

The pseudo-second-order rate expression is used to describe chemisorption involving valency forces through the sharing or exchange of electrons between the adsorbent and adsorbate as covalent forces, and ion exchange [32]. A pseudo-second order equation is applied in the given form [1]:

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{1}{Q_e} t \quad (3)$$

where k_2 ($\text{g}^{-1} \text{mmol}^{-1} \text{min}^{-1}$) is the rate constant of the pseudo-second order sorption. A plot of t/Q_t versus t should give a linear relationship for second-order kinetics.

Additionally, the initial adsorption rate h ($\text{mmol g}^{-1} \text{min}^{-1}$) can be determined using the Eq. [1]:

$$h = k_2 Q_e^2 \quad (4)$$

The pseudo-second-order equation has the following advantages: it does not have the problem of assigning an effective adsorption capacity, *i.e.*, the adsorption capacity, the rate constant of pseudo-second-order, and the initial adsorption rate all can be determined from the equation without knowing any parameter beforehand [1].

The rate constants k_1 , k_2 and h , equilibrium sorption capacity, Q_e , and the coefficients of determination, R^2 , calculated from the values of intercepts and slopes of

corresponding plots for the pseudo-first and the pseudo-second order equations are given in Table 3. Plots of $\log(Q_e - Q_t)$ vs. t (pseudo-first order) and t/Q_t vs. t (pseudo-second order) for heavy metals sorption by P4VPD are shown in Figure 3.

Table 3. Kinetic parameters for Co(II), Cu(II) and Cr(VI) uptake using P4VPD as sorbent

Parameter	Sorbate		
	Co	Cu	Cr
$Q_e / \text{mmol g}^{-1}$	3.08	0.71	0.51
Pseudo-first order			
k_1 / min^{-1}	0.043	0.037	0.030
$Q_e^{\text{calc}} / \text{mmol g}^{-1}$	0.62	0.47	0.36
R^2	0.7428	0.9667	0.9345
Pseudo-second order			
$k_2 / \text{g mmol}^{-1} \text{min}^{-1}$	0.462	0.251	0.230
$h / \text{mmol g}^{-1} \text{min}^{-1}$	4.409	0.1319	0.06381
$Q_e^{\text{calc}} / \text{mmol g}^{-1}$	3.09	0.726	0.526
R^2	0.9999	0.9985	0.9941
Intraparticle			
$k_{id} / \text{mmol g}^{-1} \text{min}^{-0.5}$	0.0459	0.0432	0.0271
$C_{id} / \text{mmol g}^{-1}$	2.71	0.318	0.211
R^2	0.9481	0.9793	0.9980

The theoretical Q_e values estimated from the first-order kinetic model were not in accordance with the experimental ones, and the coefficients of determination were found to be rather low. This indicates that the first-order kinetic model is not applicable to the Co(II), Cu(II) and Cr(VI) sorption on P4VPD. On the other hand, the theoretical Q_e values calculated from pseudo-second order model were found to be very close to the experimental values of equilibrium sorption, Q_e , with coefficients of determination higher than 0.99. The initial sorption rate, h , is the highest for Co(II) and the lowest for Cr(VI), which reflects the affinity of the sorbent for these sorbate species.

The superior fit of the pseudo-second-order model with experimental data implies that the adsorption process may be interaction controlled, with chemisorption involving valence force through sharing or exchange of electrons between P4VPD and heavy metal ions [33]. Plazinski *et al.*, however, showed convincing proof that the pseudo-second order equation is able to represent the kinetics of sorption in the systems for which not only the rate of surface reaction governs the overall process rate [2]. Further on, Plazinski *et al.* drew a general conclusion that the expressions of the pseudo-first order and the pseudo-second order model did not correspond to only one kinetic model, but they presented more or less flexible mathematical formulae, able to simulate adequately well the behavior characte-

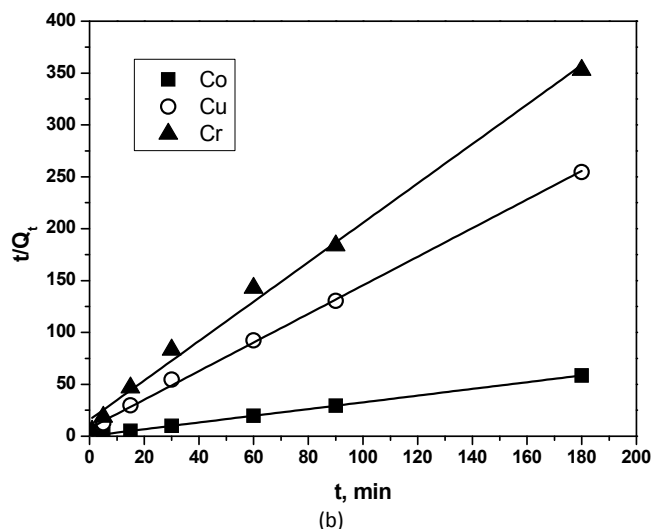
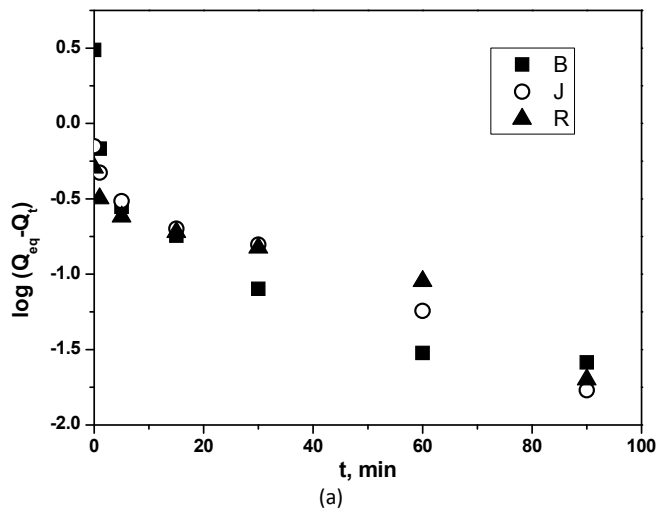


Figure 3. Pseudo-first (a) and pseudo-second order kinetics (b) of the heavy metals uptake by P4VPD at 25 °C.

ristic of physical kinetic processes of various kinds (*i.e.*, surface reaction and intraparticle diffusion) [2].

Diffusion-based kinetic modeling

Generally, if the investigated sorption process involves metal species and porous sorbent, it is a multi-step process, including [34]: *i*) bulk diffusion, *ii*) external mass transfer of sorbate molecules across the liquid film around the sorbent particles, *iii*) binding of sorbate molecules on the active sites distributed on the outer surface of the sorbent particles, *iv*) intraparticle diffusion of sorbate molecules into macro-, meso- and micropores, and *v*) sorption of sorbate molecules onto active sites distributed within the sorbent particles. The steps *iii* and *v* are usually very fast and hence they do not have a determinant role in governing sorption rates. Any of the four previous steps may be the rate controlling factor or any combination of the steps [3]. The entire sorption process is thus affected by changes

to any step, and these steps can be affected by many experimental conditions, including particle size, agitation rate and pH, among others [3]. Thus, external mass transfer and intraparticle diffusion warrant further consideration.

Since the pseudo-first and the pseudo-second order kinetic models cannot identify the influence of diffusion on sorption, the Weber and Morris equation was used for calculation of the rate constants of intraparticle diffusion [35]. The intraparticle diffusion model presumes that film diffusion or boundary layer diffusion is negligible, and that intraparticle diffusion is the only rate-controlling step.

The rate of intraparticle diffusion can be calculated according to the equation [36]:

$$Q_t = C_{id} + k_{id}t^{0.5} \quad (5)$$

where k_{id} is the intraparticle diffusion rate constant ($\text{mmol g}^{-1} \text{min}^{-0.5}$), and C_{id} is the intercept which is proportional to the boundary layer thickness (mmol g^{-1}) [37].

The rate constant of intraparticle transport, k_{id} , is estimated from the slope of the linear portion of the plot of amount sorbed against square root of time. In the case of a linear plot of Q_t versus $t^{0.5}$, and if the line passes through the origin, intraparticle diffusion is the only rate-controlling step [38]. If not, some other mechanisms are also involved.

For investigated metal ions sorption by porous P4VPD, the plots Q_t versus $t^{1/2}$ did not pass through the origin (Figure 4) suggesting that even though the adsorption process involved intraparticle diffusion, it was not the only rate-controlling step. The positive value of intercept C_{id} is indicative of some degree of boundary layer control [38].

The multilinear shape of $Q_t-t^{1/2}$ relationships indicates that more than one process affects Cr(VI) adsorption. As can be seen from Figure 5, plot Q_t versus $t^{1/2}$ for Co(II) has first sharper portion, which can be considered as an external surface adsorption or faster adsorption stage, followed by gradual adsorption where intraparticle diffusion is rate controlled. After that, in the final equilibrium stage the intraparticle diffusion starts to slow down due to the low adsorbate concentration in solution. Kumar *et al.* observed the similar for Cr(III) removal by using an amine-based polymer, aniline–formaldehyde condensate (AFC) coated on silica gel [39].

The rate of uptake is limited by the size of adsorbate molecule, the adsorbate concentration and its affinity towards the adsorbent, the diffusion coefficient of the adsorbate in the bulk, the adsorbent pore size

distribution and the degree of mixing step [38]. In this case, it is apparent from Table 3. that the size of the metal species and their affinity towards P4VPD are crucial for the observed trend in the k_{id} values. Intraparticle diffusion is facilitated by the presence of macroporosity.

The dependence of the amount adsorbed on the square-root of time has a concave character for the two polymers. A model investigation by Rudzinski *et al.* has shown that such curve shape may be due to a combined effect of the rate of surface reaction and that of the solute transport from the bulk to the surface [2], in support of deductions made in the case of this sorbate–sorbent system.

The contribution of boundary layer or film diffusion indicated by non-zero values of the intraparticle plot intercept is often confirmed using the model given by Boyd [36]:

$$F = 1 - \frac{6}{\pi^2} \sum_{n=1}^{\infty} \frac{1}{n^2} \exp\left(-\frac{n^2 \pi^2 D_i t}{r^2}\right) \quad (6)$$

$$F = 1 - \frac{6}{\pi^2} \sum_{n=1}^{\infty} \frac{1}{n^2} \exp(-n^2 B t) \quad (7)$$

where F is the fractional attainment of equilibrium at time t (min) obtained from the expression:

$$F = \frac{Q_t}{Q_e} \quad (8)$$

and

$$B = \frac{D_i \pi^2}{r^2} \quad (9)$$

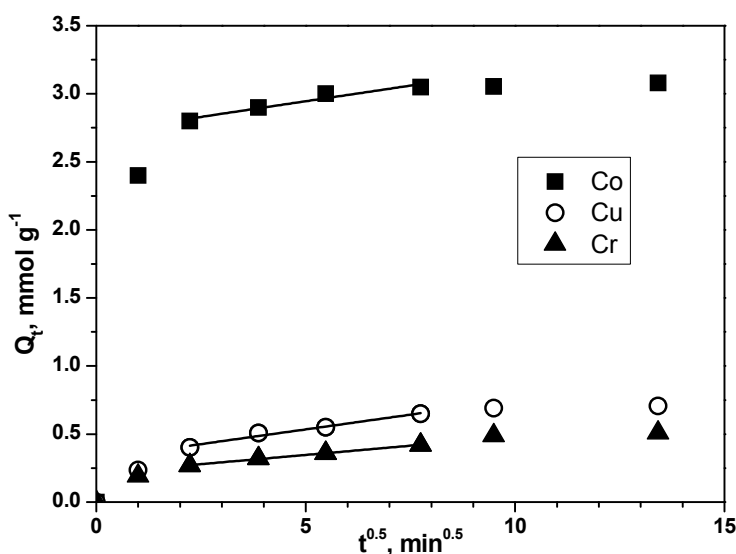


Figure 4. Intraparticle diffusion plots for Cu(II), Co(II) and Cr(VI) uptake using P4VPD as sorbent.

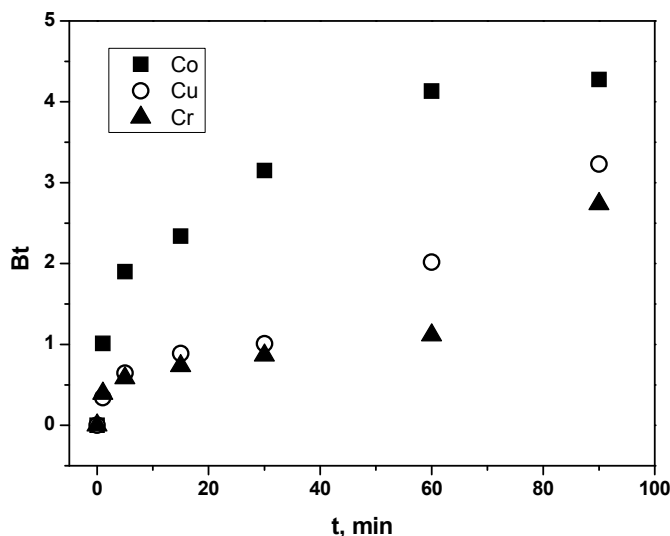


Figure 5. The Boyd plots for sorption of Cu(II), Co(II) and Cr(VI) using P4VPD as sorbent.

where B is the time constant (min^{-1}), D_i is the effective diffusion coefficient of the metal ions in the sorbent phase ($\text{cm}^2 \text{min}^{-1}$), r is the radius of the sorbent particle (cm), assumed to be spherical, n is an integer that defines the infinite series solution. The approximations for Bt proposed by Reichenberg [40] are as follows:

$$F \text{ values} < 0.85, Bt = \left(\frac{1}{\pi^2} - \left(\pi - \frac{\pi^2 F}{3} \right)^{\frac{1}{2}} \right) \quad (10)$$

$$F \text{ values} > 0.85, Bt = -0.4997 - \ln(1 - F) \quad (11)$$

Thus, the value of Bt can be computed for each value of F , and then plotted against time. The linearity of these so-called Boyd Plots (Figure 5) was employed to distinguish between sorption controlled by film diffusion and particle diffusion [20]. If the plot is in the form of straight line passing through the origin, this indicates that sorption processes are governed by particle-diffusion mechanisms; otherwise, they are controlled by film diffusion [41]. From Figure 5, it was observed that the plots were neither linear nor passed through the origin for Co(II), Cu(II) and Cr(VI) indicating the film diffusion-controlled mechanism.

The strong external resistance which hinder the external mass transfer and is rate-limiting during the initial stages of sorption (0–5 min as seen in Figure 5) may be mainly due to the the absence of mixing and high affinity of adsorbate to adsorbent [42]. The intraparticle step limits the overall transfer in the sorption period of 5–60 min since the investigated systems have high concentrations of adsorbate and relatively large particle size of adsorbent.

In order to make distinction between kinetic and diffusion control, a very general guideline can be used:

if equilibrium is achieved within 3 h, the process is usually kinetic controlled and above 24 h, it is diffusion controlled [3]. Either or both kinetic and sorption processes may be rate controlling in the 3 to 24 h period, such as in the case of Cu(II), Co(II) and Cr(VI) sorption by commercial macroporous REILLEX-425, P4VPD.

CONCLUSION

Commercial macroporous crosslinked poly(4-VP-co-DVB), P4VPD (REILLEX 425), was used as heavy metal ions sorbent from aqueous solutions without additional functionalization.

In this manner, some problems, such as the undesired side reactions and the change of pore structure as a consequence of chemical modification, are avoided, simplifying the process and reducing the costs as well. Kinetics of Co(II), Cu(II) and Cr(VI) removal from aqueous solutions was tested in batch, under non-competitive conditions at room temperature and analyzed using pseudo-first order, pseudo-second order, intraparticle diffusion and Boyd's Model. The very high maximum Co(II) capacity of 181 mg g^{-1} of P4VPD was observed. Kinetic studies showed that the adsorption adhered to the pseudo-second-order model since theoretical and experimental sorption capacities were in excellent agreement, with $R^2 \geq 0.99$. The intraparticle diffusion model revealed that pore diffusion was not the only rate-controlling step and indicated some degree of boundary layer control in the process of heavy metal sorption by the porous copolymer. Boyd plots showed that film diffusion mechanism may be involved in the process of Co(II), Cu(II) and Cr(VI) sorption by P4VPD.

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IZVOD

KINETIČKO MODELOVANJE SORPCIJE TEŠKIH METALA KOPOLIMEROM SA OSNOVOM VINIL PIRIDINA

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(Naučni rad)

Komercijalni makropozni poli(4-vinilpiridin-co-divinilbenzen) [P4VPD], Reillex-425, bez dodatne funkcionalizacije korišćen je za ispitivanje mogućnosti sorpcije teških metala iz vodenih rastvora. Na taj način su izbegnuti neki problemi do kojih može doći prilikom uvođenja funkcionalnih grupa selektivnih za određene jone metala u polimerne sorbente, kao što su nepoželjne sporedne reakcije i promena porozne strukture. P4VPD je okarakterisan živinom porozimetrijom, određivanjem adsorpciono-desorpcionih niskotemperaturnih izoterma azota, infracrvenom spektroskopijom (FTIR) i elementalnom analizom. U statičkim eksperimentima su određene brzine sorpcije Cu(II), Co(II) i Cr(VI) jona pomoću P4VPD pri nekompetitivnim uslovima i pri sobnoj temperaturi (298 K). Zapažena je brza sorpcija ispitivanih jona, naročito u slučaju Co(II), pri čemu su zapažene vrednosti poluvremena sorpcije, $t_{1/2}$, od 1,5 min i visoka vrednost maksimalnog kapaciteta sorpcije, Q_{max} , od 3,08 mmol g⁻¹ (181 mg g⁻¹). Prilikom analiziranja sorpcije ispitivanih metala pomoću P4VPD korišćena su četiri kinetička modela (model pseudo-prvog i pseudo-drugog reda, model difuzije unutar čestica i Bojdrov model). Pokazalo se da sorpciju jona metala najbolje opisuje model pseudo-drugog reda, pošto je za ovaj model dobijeno odlično slaganje eksperimentalnih i teorijskih vrednosti kapaciteta sorpcije, kao i vrednosti $R^2 \geq 0,99$. Analiza eksperimentalnih rezultata pomoću modela difuzije unutar čestica pokazala je da difuzija kroz pore nije jedini stupanj koji određuje brzinu sorpcije i ukazala na delimičan uticaj graničnog sloja na sorpciju teških metala pomoću poroznog kopolimera.

Ključne reči: Poli(4-vinilpiridin-co-divinilbenzen) • Makroporozni kopolimer • Sorpcija Cu(II), Co(II) i Cr(VI) jona • Kinetički modeli