

Comparison of two Agricultural Wastes for Phenol Removal Via Peroxidase-Catalyzed Enzymatic Approach

Tung Chiong^{1,2}, Ee H. Khor¹, Michael K. Danquah¹ and Sie Y. Lau¹

¹Department of Chemical Engineering, Curtin University Sarawak, Malaysia

²Curtin Sarawak Research Institute, Curtin University Sarawak, Malaysia

Abstract. Agricultural wastes of jicama and luffa skin peels were used as the source for peroxidase extraction. The extracted crude enzymes showed similar activities, 1.34U/mL and 1.22U/mL for jicama and luffa peroxidase respectively. These peroxidases were used to treat phenol under varying operating conditions of buffer pH, hydrogen peroxide concentration, enzyme volume and temperature. Jicama peroxidase demonstrated a phenol removal efficiency of approximately 90% at buffer pH 7, 1mM hydrogen peroxide using 1.5mL enzyme at 25°C. Luffa peroxidase required a higher dosage of hydrogen peroxide, and exhibited a removal efficiency of 84% at 8mM with other operating conditions same as jicama peroxidase. Jicama peroxidase is sensitive to pH change and more susceptible to thermal denaturation. Luffa peroxidase showed a better stability in terms of temperature.

1 Introduction

Phenol and its derivatives are present in various industrial effluents such as petroleum refineries, coal conversion, pulp and paper, resins and textiles. Phenolic compounds are mostly toxic and have been classified as hazardous pollutants [1], because they are harmful to microorganisms even at low concentrations. Therefore, these phenol-containing industrial effluents must be properly treated before they can be discharged into the receiving water bodies.

Conventional treatment methods for phenol-containing wastewater are generally microbial degradation [2], adsorption on activated carbon [3], and chemical oxidation such as ozonation [4] and Fenton reaction [5]. Although these methods are able to show high phenol removal efficiencies, some common drawbacks have been encountered. These include lengthy start-up procedure for microbial acclimatization [6], microbial growth inhibition due to high concentrations of phenolic compounds [7], intensive cost and energy for carbon regeneration [8], and disposal concern of reagents used during reaction process [8]. Due to the shortcomings of these conventional methods, enzymatic approach has emerged as an alternative for phenol removal from wastewaters, owing to its advantages which include low energy requirements, operation over a wide range of conditions, ease of process control, and minimal environmental impact [9].

The removal of phenols and other aromatic compounds from aqueous solution via peroxidase in the presence of hydrogen peroxide was first reported by Klibanov *et al.* [10]. Since then, horseradish peroxidase

(HRP) became the most explored plant peroxidase, and its ability in removing various phenolic compounds from aqueous solutions are well documented [11]-[13]. Peroxidases from other sources such as soybean seed hulls, bitter melon, cauliflower, potato and white radish have also been evaluated for their performances in treating phenol, and the reported results were encouraging [14]-[17].

It is notwithstanding that most of the plant peroxidases being studied are extracted from the edible parts of the plants, except soybean seed hulls. This will eventually cause competition with human food intake if the peroxidase extraction process is to be scaled-up to large capacity treatment. Hence, the present work aims to evaluate the performance of peroxidases extracted from agricultural wastes for phenol removal. Peroxidases were extracted from the skin peels of two locally available plants, such as jicama and luffa, which are non-edible and generally being discarded during food preparation. The performances of both crude enzyme extracts in phenol removal process were assessed and compared under varying reaction conditions.

2 Materials and methods

2.1 Extraction of peroxidase

Jicama and luffa purchased from local vegetable market were thoroughly washed with distilled water before their respective skin was peeled off. 100g of jicama and luffa skin peels was respectively blended with 200mL of 0.1M sodium carbonate buffer pH 10 for 30s, and then

homogenized for 30min with constant stirring. The enzyme extract was then filtered through four layers of cheesecloth before being subjected to centrifugation at 4000 rpm at 4°C. The supernatant (crude extract) collected was sonicated and stored at 4°C until further use.

2.2 Batch treatment of aqueous phenol solution

The removal reaction was carried out by treating 1mM phenol solution with various dosages of enzyme volume in different buffer solutions. The enzymatic reaction was initiated by the addition of hydrogen peroxide (H₂O₂) into the reaction mixture, and the mixture was incubated for 24h with constant shaking to ensure maximum phenol removal. The efficiency of luffa and jicama peroxidases was studied in relation to the changes of pH of buffer solutions, H₂O₂ concentration, enzyme volume and temperature. The percentage of phenol removal was calculated based on equation (1).

$$\text{Phenol removal (\%)} = \frac{C_i - C_f}{C_i} \times 100\% \quad (1)$$

C_i = initial phenol concentration, C_f = final phenol concentration

2.3 Analytical procedures

Enzyme activity of peroxidase was measured using a colorimetric assay containing phenol, 4-aminoantipyrine (4-AAP) and H₂O₂. This assay is a modification of that developed by Wu *et al.* [18] in which the assay mixture consists of 250µL of 9.6mM 4-AAP, 100µL of 100mM phenol, 100µL of 2mM H₂O₂, 450-500µL of 100mM phosphate buffer (pH 6.0) and 50-100µL of enzyme solution. Prior to significant substrate depletion, activity was proportional to the rate of formation of a coloured product which absorbs light at a peak wavelength of 510nm with an extinction coefficient of 7100L/mol.cm based on the conversion of H₂O₂. One unit of activity is defined as the number of micromoles of H₂O₂ consumed per minute at pH 6.0 and 25°C.

Phenol concentrations were determined colorimetrically using 4-AAP and potassium ferricyanide in an alkaline buffer medium. Phenolic compounds react with 4-AAP under alkaline conditions to yield an intermediate species which is oxidized in the presence of the potassium ferricyanide reagent. The resulting compound is a quinone-type dye which absorbs light at 510nm. The colour intensity is linear with respect to phenol concentration, provided that this concentration does not exceed 0.1 mM in the cuvette [19]. The absorbance was measured at 510nm after 5 minutes.

3 Results and discussions

3.1 Enzyme activity of peroxidase

The extracted crude enzymes from the skin peels of jicama and luffa exhibited similar enzyme activities, being 1.34U/mL and 1.22U/mL respectively. The crude

extracts were used as produced without any further purification.

3.2 Effect of pH

The effect of pH on phenol removal was conducted by using various buffer solutions ranging from pH 4 to 9 at 25°C. The buffer solutions used were acetate buffer (pH 4 to 5), phosphate buffer (pH 6 to 7) and borate buffer (pH 8 to 9). The dependence of phenol removal efficiency on pH is as shown in Fig. 1.

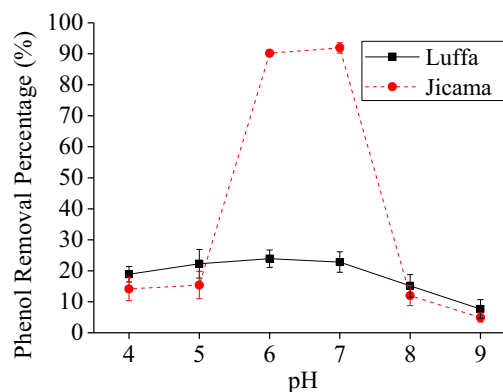


Figure 1. Effect of buffer pH on phenol removal (experiment conditions: 1.5mL enzyme, 1mM H₂O₂ at 25°C).

When 1mM phenol solution was treated with jicama peroxidase, removal efficiency of approximately 90% was observed at pH values 6 to 7, with the optimum occurring at pH 7. Removal efficiency decreased to less than 20% below pH 5 and above pH 8. This is a result of variations in enzyme protein structure in response to varying pH. The enzyme molecules undergo structural modifications as a result of protonation and hydroxylation effects which could potentially obscure the enzyme active sites before causing denaturation and permanent loss of functionality. Moreover, the decrease in removal efficiency at pH above 8 could be attributed to the formation of phenol conjugated base since the pK_a of phenol at 25°C is 10. This conjugated basic form does not permit the phenolic compounds to act as hydrogen donors, thus hindering binding onto the surface of the enzyme active sites.

Luffa peroxidase, on the other hand, showed low phenol removal efficiency of less than 24% over the pH ranges being evaluated. Though enzyme activities of both luffa and jicama were similar as mentioned earlier, this finding suggested that luffa peroxidase might require higher concentration of H₂O₂ for oxidation of its enzyme into catalytically active form which is capable of reacting with phenolic compounds [20].

Previous studies on phenol removal catalyzed by horseradish peroxidase (HRP) demonstrated optimal operating pH at pH 8 [12], which was slightly basic. Another work by Wright and Nicell [14] showed that nearly complete removal of phenol was observed over a pH range of 5 to 9, with the maximum removal at pH 6 by using high dose of soybean peroxidase (SBP). The optimum operating pH for jicama peroxidase was

narrower than SBP, implying that it is more sensitive to pH change. All subsequent enzymatic reactions were conducted using phosphate buffer pH 7.

3.3 Effect of H₂O₂ concentration

Enzymatic reaction cannot take place in the absence of H₂O₂. H₂O₂ is required in peroxidase-catalyzed reactions to oxidize the native enzyme molecules (E) into Compound I (E_i) which then accepts an aromatic compound (AH₂) into its active site and carries out its oxidation to produce a free radical ([•]AH). The free radical is released from the catalytic site leaving the enzyme as Compound II (E_{ii}). Compound II oxidizes a second aromatic molecule, resulting in the release of a second free radical into the solution and returning the enzyme to its native state. The one-electron oxidation of aromatic substrate catalyzed by peroxidase is usually depicted by the following mechanism [21]:

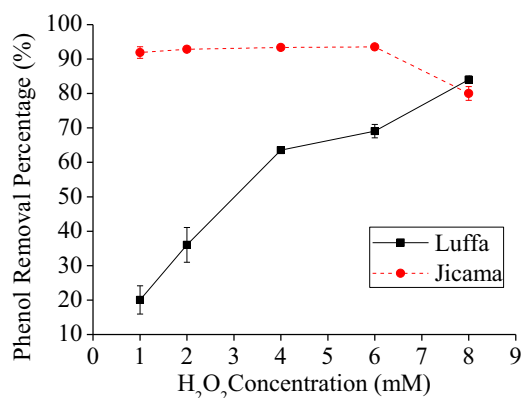
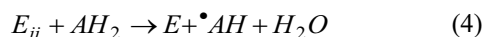
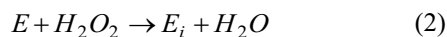


Figure 2. Effect of H₂O₂ concentration on phenol removal (experiment conditions: 1.5mL enzyme, buffer pH 7 at 25°C).

The effect of various concentrations of H₂O₂ on phenol removal by jicama and luffa peroxidases is as illustrated in Fig. 2. Phenol removal efficiency of more than 90% was recorded by jicama peroxidase over a range of H₂O₂ concentrations from 1mM to 6mM. When H₂O₂ concentration was further increased to 8mM, there was a decrease of about 10% in removal percentage. This could be attributed to enzymatic inhibition effect caused by H₂O₂. High concentrations of H₂O₂ inhibit peroxidase catalytic activity by irreversibly oxidizing the enzyme ferriheme group which is vital for peroxidase catalysis [22].

A different trend was exhibited by luffa peroxidase in regards to H₂O₂ concentration. When H₂O₂ concentration was increased, phenol removal percentage also increased. For the range of H₂O₂ concentrations being studied, the highest phenol removal efficiency of 84% was observed at 8mM. The reason that luffa peroxidase requires a much higher dosage of H₂O₂ for better performance in phenol removal could be due to the difference in the structure of its peroxidase molecules' active sites. The result obtained

also suggested that luffa peroxidase is less susceptible to H₂O₂ inhibition, a phenomenon commonly suffered by peroxidase-catalyzed enzymatic method. Subsequent experiments for luffa and jicama peroxidases were conducted using 6mM and 1mM H₂O₂ respectively.

3.4 Effect of enzyme volume

The effect of enzyme concentration on phenol removal is important as it has a significant bearing on the process economics. The effect of crude peroxidase dosage in phenol removal from aqueous solution was investigated for both jicama and luffa peroxidases under varying volumes of 1.5mL to 4.5mL, as shown in Fig. 3.

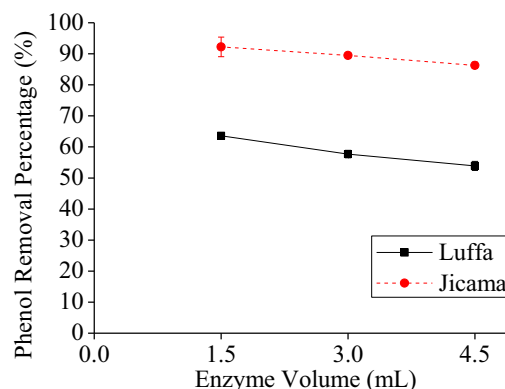


Figure 3. Effect of enzyme volume on phenol removal (experiment conditions: buffer pH 7, 6mM and 1mM H₂O₂ for luffa and jicama respectively at 25°C)

Both peroxidases exhibited similar trend, with removal efficiency decreasing when the enzyme volumes were increased. The efficiency of jicama peroxidase declined gradually from 92% at 1.5mL enzyme volume to 86% at 4.5mL enzyme volume. Luffa peroxidase showed a slightly higher drop, from 63% to 53% at 1.5mL and 4.5mL enzyme volume, respectively. Increase in enzyme volume means that there are greater amount of peroxidase molecules in the solution, and consequently increasing available active sites of enzyme for phenol binding. However, this scenario did not enhance the phenol removal efficiency as predicted. This could be a result of depletion and/or insufficient H₂O₂ under increasing concentration of enzyme. The heme prosthetic group of peroxidase reacts with H₂O₂ in the first step of the catalytic cycle, thus, under depleting levels of H₂O₂, this affects enzyme activation. A higher dosage of H₂O₂ might be required to activate both peroxidases at higher enzyme volumes.

3.5 Effect of temperature

The effect of temperature on phenol removal was examined by incubating the reaction mixtures at various temperatures, ranging from 25°C to 70°C. As depicted in Fig. 4, jicama peroxidase attained a maximum phenol removal percentage of 92% at 25°C whereas luffa peroxidase showed a constant percentage averaging at 64%. Elevated temperatures were found to demonstrate a

significant adverse effect on jicama peroxidase as compared to luffa peroxidase. When the temperatures were increased from 25°C to 40°C, jicama peroxidase suffered a drastic drop in removal efficiency from 92% to 41%, which was more than half of the value. Its removal efficiency remained constant from 40°C to 60°C. A slight decrease in removal efficiency was again observed when the temperature was further increased to 70°C. Luffa peroxidase, however, is more stable towards thermal heat. Its activity can be preserved over a wider temperature range. This is shown by its nearly constant removal efficiencies over the range of 25°C to 70°C. Higher temperatures neither enhance nor inhibit its activity in oxidizing phenol compounds.

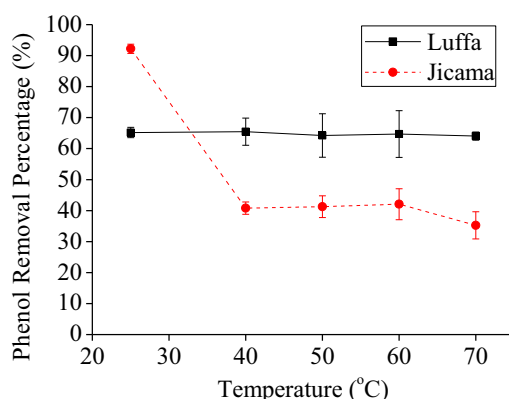


Figure 4. Effect of temperature on phenol removal (experiment conditions: 1.5mL enzyme, buffer pH 7, 6mM and 1mM H₂O₂ for luffa and jicama respectively)

The decline in efficiency by jicama peroxidase could be attributed to thermal denaturation. Under elevated temperature conditions, thermal denaturation of enzyme molecules causes loss of its active sites in catalyzing substrate molecules. The thermal stability of peroxidases is governed by the haem prosthetic group, which is released under elevated temperatures to form apoenzyme. The transient enzyme formed is less stable and more susceptible to thermal inactivation as compared to the native enzyme [23]. Higher temperature conditions distort the structure of the enzyme, causing a limited binding capacity of its active sites onto substrate molecules. The optimum operating temperature for both jicama and luffa peroxidases was selected at 25°C, in order to preserve peroxidase activities and save operating cost.

4 Conclusions

In the present study, both jicama and luffa peroxidases extracted from their respective fruit skin peels demonstrated promising performances in removing phenol from aqueous solution. Jicama peroxidase, though showing removal efficiency of about 90%, has a narrow operating pH range and is more susceptible to thermal denaturation. Luffa peroxidase requires a much higher concentration of H₂O₂ to activate its active sites before it

can carry out the oxidation of phenol. Its enzyme activity is also well preserved under the elevated temperatures being studied. The findings from this work revealed the potential of jicama and luffa peroxidases in the application of phenol removal. Nevertheless, a more comprehensive study such as optimization of the operating conditions might be necessary to better understand the factors affecting the performances of these peroxidases in phenol removal.

References

1. N. Caza, J. K. Bewtra, N. Biswas, K. E. Taylor, *Water Res.* **33**, 3012 (1999)
2. A. Krastanov, Z. Alexieva, H. Yemendzhiev, *Eng. Life Sci.* **13**, 76 (2013)
3. S. Mukherjee, S. Kumar, A. K. Misra, M. Fan, *Chem. Eng. J.* **129**, 133 (2007)
4. K. Turhan, S. Uzman, *Desalination* **229**, 257 (2008)
5. Y. Yavuz, A. Savas Koparal, Ü. Bakir Ögütveren, *Chem. Eng. Technol.* **30**, 583 (2007)
6. T. T. Firozjaee, G. D. Najafpour, A. Asgari, M. Khavarpour, *Chem. Ind. Chem. Eng. Q.* **19**, 173 (2012)
7. W. Gernjak, T. Krutzler, A. Glaser, S. Malato, J. Caceres, R. Bauer, *et al.*, *Chemosphere* **50**, 71 (2003)
8. G. Busca, S. Berardinelli, C. Resini, L. Arrighi, *J. Hazard. Mater.* **160**, 265 (2008)
9. M. Gómez, M. D. Murcia, R. Dams, N. Christofi, E. Gómez, J. L. Gómez, *Environ. Technol.* **33**, 1055 (2011)
10. A. M. Klibanov, B. N. Alberti, E. D. Morris, L. M. Felshin, *J. Appl. Biochem.* **2**, 414 (1980)
11. M. Wagner, J. A. Nicell, *Water Res.* **35**, 485 (2001)
12. J. A. Nicell, J. K. Bewtra, N. Biswas, C. C. St. Pierre, K. E. Taylor, *Can. J. Civ. Eng.* **20**, 725 (1993)
13. S. Nakamoto, N. Machida, *Water Res.* **26**, 49 (1992)
14. H. Wright, J. A. Nicell, *Bioresour. Technol.* **70**, 69 (1999)
15. H. Ashraf, Q. Husain, *Desalination* **262**, 267 (2010)
16. A. N. Deva, C. Arun, G. Arthanareeswaran, P. Sivashanmugam, *J. Environ. Chem. Eng.* **2**, 1148 (2014)
17. J. Dec, J.-M. Bollag, *Biotechnol. Bioeng.* **44**, 1132 (1994)
18. J. Wu, K. E. Taylor, J. K. Bewtra, N. Biswas, *Water Res.* **27**, 1701 (1993)
19. M. Ghiourelotis, J. A. Nicell, *Enzyme Microb. Technol.* **25**, 185 (1999)
20. M. Hamid, K. u. Rehman, *Food Chem.* **115**, 1177 (2009)
21. J. A. Nicell, J. K. Bewtra, N. Biswas, E. Taylor, *Water Res.* **27**, 1629 (1993)
22. M. A. Duarte-Vázquez, M. A. Ortega-Tovar, B. E. García-Almendarez, C. Regalado, *J. Chem. Technol. Biotechnol.* **78**, 42 (2003)
23. J. P. McEldoon, J. S. Dordick, *Biotechnol. Progr.* **12**, 555 (1996)