

## KG<sup>2</sup>B, a collaborative benchmarking exercise for estimating the permeability of the Grimsel granodiorite – Part 1: measurements, pressure dependence and pore-fluid effects

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### SUMMARY

Measuring the permeability of tight rocks remains a challenging task. In addition to the traditional sources of errors that affect more permeable formations (e.g. sample selection, non-representative specimens, disturbance introduced during sample acquisition and preparation), tight rocks can be particularly prone to solid–fluid interactions and thus more sensitive to the methods, procedures and techniques used to measure permeability. To address this problem, it is desirable to collect, for a single material, measurements obtained by different methods and pore-fluids. For that purpose a collaborative benchmarking exercise involving 24 laboratories was organized for measuring the permeability of a single low permeability material, the Grimsel granodiorite, at a common effective confining pressure (5 MPa). The objectives of the benchmark were: (i) to compare the results for a given method, (ii) to compare the results between different methods, (iii) to analyze the accuracy of each method, (iv) to

study the influence of experimental conditions (especially the nature of pore fluid), (v) to discuss the relevance of indirect methods and models and finally (vi) to suggest good practice for low permeability measurements. In total 39 measurements were collected that allowed us to discuss the influence of (i) pore-fluid, (ii) measurement method, (iii) sample size and (iv) pressure sensitivity. Discarding some outliers from the bulk data set (4 out of 39) an average permeability of  $1.11 \times 10^{-18} \text{ m}^2$  with a standard deviation of  $0.57 \times 10^{-18} \text{ m}^2$  was obtained. The most striking result was the large difference in permeability for gas measurements compared to liquid measurements. Regardless of the method used, gas permeability was higher than liquid permeability by a factor approximately 2 ( $k_{\text{gas}} = 1.28 \times 10^{-18} \text{ m}^2$  compared to  $k_{\text{liquid}} = 0.65 \times 10^{-18} \text{ m}^2$ ). Possible explanations are that (i) liquid permeability was underestimated due to fluid-rock interactions (ii) gas permeability was overestimated due to insufficient correction for gas slippage and/or (iii) gases and liquids do not probe exactly the same porous networks. The analysis of Knudsen numbers shows that the gas permeability measurements were performed in conditions for which the Klinkenberg correction is sufficient. Smaller samples had a larger scatter of permeability values, suggesting that their volume were below the Representative Elementary Volume. The pressure dependence of permeability was studied by some of the participating teams in the range 1–30 MPa and could be fitted to an exponential law  $k = k_0 \cdot \exp(-\gamma P_{\text{eff}})$  with  $\gamma = 0.093 \text{ MPa}^{-1}$ . Good practice rules for measuring permeability in tight materials are also provided.

**Key words:** Permeability and porosity; Microstructure; Hydrogeophysics.

## 1 INTRODUCTION

Permeability is a property of a given porous medium which quantifies its ability to allow fluid flow. Since the introduction of Darcy's phenomenological law (Darcy 1856), permeability characterization usually involves pressure gradient and flow measurements of a single fluid phase. In the field, such measurements may only provide apparent permeability estimates for rock masses including pore, crack and fracture networks which are usually saturated or partially saturated with several fluids (Zinszner 2007). Estimates of the single phase (or intrinsic, or absolute) permeability (hereafter simply referred to as permeability) are typically made by laboratory testing of core samples, following a saturation or a drying procedure for, respectively, liquid or gas phase testing. In the case of liquids, fluid saturation can be assessed from the evolution of poroelastic parameters such as the isotropic Skempton coefficient (Makhnenko & Labuz 2013) which is very sensitive to residual air, during a step by step back fluid pressure increase to dissolve trapped air bubbles (Wild *et al.* 2015a). For tight rocks, the sample preparation and saturation procedures can be particularly long and may disturb the original pore network. For example saturation can change the equilibrium between solid and fluid phases naturally present in clay rocks (Pearson *et al.* 2011; Wild *et al.* 2015b). The drying procedure can also have dramatic effects in the presence of clay minerals, causing desiccation cracks (Wild *et al.* 2015b). Many observations have been made regarding perturbations and modifications of rock properties due to sampling processes and stress release effects during coring (Schild *et al.* 2001; Blümling *et al.* 2007).

Measuring the permeability of tight formations, which can potentially serve as seals for nuclear waste repositories and/or strata for geological sequestration of  $\text{CO}_2$ , for instance, poses a number of challenges. In addition to the traditional sources of errors that affect more permeable formations (e.g. sample selection, non-representative specimens, disturbance introduced during sample acquisition and preparation), rocks that are particularly tight and prone to solid–fluid interactions can be more sensitive to the methods, procedures and techniques used to acquire permeability data. In low

permeability rocks, classical steady-state flow measurements may be very difficult to perform because of slow variations of the measured quantities (pore pressure, flow rate) and the long time needed for flow stabilization. Due to the long duration of flow experiments, variations in external conditions (typically ambient temperature) may occur, compromising the accuracy of permeability estimates. For this reason two other methods have been developed: the transient pore pressure (or pulse) method and the pore pressure oscillation method which is similar to a steady-state oscillatory method. The pulse decay method pioneered by Brace *et al.* (1968) involves applying a pressure step increase in an upstream reservoir and measuring the pressure variations with time in both upstream and downstream reservoirs connected to the sample. As pressure diffusion occurs through the rock sample, permeability can be estimated from decay of the differential pore pressure which follows a decreasing exponential law. Further knowledge on transient pulse tests was gained from parametric analysis of pore pressure diffusion processes in rocks by Hsieh *et al.* (1981) and Neuzil *et al.* (1981). The pulse method has been widely and successfully used both in crystalline and shaly rock samples during triaxial mechanical tests in the laboratory (Bourbie & Walls 1982; Brace *et al.* 1968; Selvadurai *et al.* 2005; Carles *et al.* 2007). Other transient methods, like the draw-down method or the pressure build-up method (Martin 1959) are particularly well adapted to use in the field in boreholes (Jakubick & Franz 1993; Bossart *et al.* 2002; Wassermann *et al.* 2011). Transient methods can be applied step by step after re-equilibration periods during loading tests, providing discrete measurements of permeability. Continuous measurements have been developed in order to investigate loading effects on low permeability rocks and are more representative of the evolution of in situ conditions during reservoir activities. Such methods are based on continuous oscillatory flow and analysis of sinusoidal signals of pore pressure at both ends of a sample through phase lag and amplitude ratio (Fischer 1992; Kranz *et al.* 1990; Song & Renner 2007).

All the above methods assume Darcy flow and more or less steady state conditions during the measurements. The measured quantities in the pulse decay and steady-state flow experiments are more

sensitive to ambient temperature variations than the phase shift or amplitude ratio continuously measured in the oscillatory method (Kranz *et al.* 1990). The pulse decay method has the advantage of being relatively easy to perform but requires appropriate selection of the reservoir volume compared to the pore volume of the tested sample (Hsieh *et al.* 1981). Derivative techniques have been developed to face such issues linked to the experimental apparatus (Trimmer *et al.* 1980; Lin 1982). The oscillation technique also requires some experimental adjustments concerning mainly: (i) the frequency of the forcing pore pressure signal—as pointed out by Song & Renner (2007), the frequency dependence of hydraulic properties could be a way to define scaling parameters of the pore structure and (ii) the peak-amplitude of the forcing waveform which has to be small enough to avoid local poroelastic and fluid compressibility effects. Sometimes it is also a technical challenge to maintain a sinusoidal forcing signal. In addition to permeability, the oscillatory method allows estimation of other key parameters such as diffusivity and specific storage capacity (Song & Renner 2007). Theoretically, permeability depends only on the pore structure of the material, and should be independent of the nature of the pore fluid used for the measurement (Muskat & Wyckoff 1937). However, differences have been reported in the literature between water and gas permeability measurements. Gas permeability estimations must take into account the gas compressibility, and the measured permeability is an apparent value that needs to be corrected for the so-called gas slippage effect: the ‘liquid equivalent’ permeability can be obtained by applying the Klinkenberg correction (Klinkenberg 1941) to gas permeability measurements made at different mean pore pressures. When the pore size is of the same order as the gas molecule mean free path, additional corrections have to be done to account for Knudsen diffusion (Ziarani & Aguilera 2012; Anez *et al.* 2014). This effect is minimized when using high pore pressures (typically larger than several MPa). Whatever the fluid used, permeability measurements require also a sufficiently low flow rate to avoid inertial effects, otherwise the Forchheimer correction has to be applied (e.g. Rust & Cashman 2004).

In order to bring a know-how about accurate transport property characterization in low permeability material, we proposed a benchmarking exercise involving 24 laboratories around the world using both direct (steady-state, transient, oscillatory) and indirect methods (pore and crack network imagery, modeling) to study fluid flow. Such an extensive benchmarking effort in rock physics has not been done before to our knowledge: the FEBEX benchmark study numerically modeled the results of a fluid injection test in the Grimsel Test Site (Alonso *et al.* 2005) and, within the framework of the SAFOD project, an inter-laboratory benchmark of physical rock properties measurements involving 20 research organizations was organized several years ago. In the SAFOD effort, measured rock properties were permeability, ultrasonic wave speed, electrical resistivity, friction and strength; however very few of the participating laboratories provided results, so that the outcome of this benchmark was never published (Lockner *et al.* 2009).

The selected material for the present benchmarking exercise came from a single metre scale rock volume in a well-known underground rock laboratory, the Grimsel Test Site (GTS) in Switzerland. The GTS consists of several meter long galleries of 3.5 m diameter excavated at 450 m depth in 1983 in granite and granodiorite of the Central Aar massif in the Swiss Alps in order to perform *in situ* experiments in the context of nuclear waste storage research in Switzerland (Lieb 1989). Here the objectives and organization of the benchmark will be presented, and then the permeability measurements data set will be analyzed and discussed.

## 2 THE KG<sup>2</sup>B PROJECT

Following a workshop on «The challenge of studying low permeability materials» that was held at Cergy-Pontoise University in December 2014, a benchmark in which several laboratories would estimate the permeability of a single material was proposed to the attendees. The material to be selected for this benchmark had to fulfill different criteria such as availability, homogeneity and scientific interest. Several options were examined until finally we selected the Grimsel granodiorite (Switzerland). The benchmark was named the ‘KG<sup>2</sup>B’ project, which derived from ‘K for Grimsel Granodiorite Benchmark’ where K stands for the symbol of permeability. Fresh cores from the Swiss Grimsel test site, an underground research laboratory in hard rock, were drilled during the coring campaign of a scientific project funded through the Swiss Competence Center of Energy Research—Supply of Electricity (SCCER-SoE), that was aimed at performing a series of demonstration experiments at various scales (up to 1 km) to support implementation of deep geothermal energy in Switzerland. From published work on the Grimsel Granodiorite (Ota *et al.* 2003), we expected a porosity of about 0.7 per cent, and an order of magnitude in permeability of  $10^{-19}$  to  $10^{-18}$  m<sup>2</sup>.

### 2.1 The objectives and organization of the benchmarking exercise

Multiple objectives were defined for the benchmark: (i) to compare the results for a given method, (ii) to compare the results between different methods, (iii) to analyze the accuracy of each method, (iv) to study the influence of experimental conditions (especially the nature of pore fluid), (v) to discuss the relevance of indirect methods and models and finally (vi) to suggest good practice for low permeability measurements. Guidelines were given to the participants, in which they were requested to follow a number of mandatory instructions: (i) permeability should be measured along the same direction, (ii) permeability should be measured at 5 MPa effective pressure (a pressure high enough to prevent leakage, small enough to minimize crack closure) and (iii) rock samples should not experience any effective pressure higher than 5 MPa before the permeability measurement was done. Effective pressure was assumed to be the difference between confining and pore pressure: indeed experimental evidence was found to support this statement (see section on pressure dependence). No recommendations or requirements were made concerning the pore fluid, confining and pore pressures, sample size and method to be used for estimating permeability. However we requested that all of this information be reported on a results spreadsheet (David *et al.* 2017). The benchmark was designed as a ‘blind-test’: other results were not shared with the participants until after they had submitted their own results. The participants were also encouraged, once the permeability at 5 MPa effective pressure was obtained, to study the pressure dependence of permeability, in particular by reproducing the *in situ* stress conditions (estimated effective pressure 30 MPa). Any additional data reported was also welcome, such as porosity values. This complementary data set is discussed in the companion paper (part 2).

### 2.2 The participants

When the benchmark was announced, 30 laboratories from eight different countries volunteered to participate. Three groups were forced to withdraw participation for different reasons (experimental setup not available, technical problems, work overload), one group

was not able to provide the results in due time, and two others did not respond to our further solicitations. Ultimately, we received results from 24 laboratories that form the ‘KG<sup>2</sup>B Team’. The complete list of participants who sent their results is given in alphabetic order in Appendix A. A dedicated website <https://labo.u-cergy.fr/~kggb/> was created, including in particular a web page where the progress of the project could be followed on the so-called ‘KG<sup>2</sup>B-wheel’ (David *et al.* 2017) which was updated as soon as results were received from any of the participants. It took one year to collect all the results. Participants were regularly sent updates on the benchmark progress, to encourage those who had not yet sent their results.

### 2.3 The selected material

Two cores of Grimsel granodiorite, each about 1 m long and 85 mm in diameter, were provided by our Swiss colleagues in September 2015. These cores were retrieved at a distance of 4–6 m from the tunnel where the borehole has been drilled; the sampling region was expected to be sufficiently distant from the fracture network of the excavation damage zone (EDZ) and the cores were therefore assumed to be free of tunnel induced damage. It was decided to send to the participants a different piece of the cores, rather than to ask them to work on a single sample that would ‘travel’ from one lab to the other. Indeed working on a single rock sample hinges on a number of problems: (i) all the labs are not using the same sample size in their setup, (ii) successive permeability measurements induce a complex history of loading and unloading that could generate irreversible changes in the porous space (iii) multiple handling and sending of the sample would increase the risk of damage or loss and (iv) the time necessary to complete the benchmarking exercise would be much longer. The cores were cut into small blocks at lengths requested by each participant (2–10 cm). Foliations are visible on the cores, at an angle of about 20–30° with respect to the core axis. The foliation is related to compositional banding of alternating dark biotite layers and quartz-rich layers (Schild *et al.* 2001). A thorough microstructural study is presented in the companion paper: the minerals identified are quartz, feldspars (albite, plagioclase), micas (muscovite, biotite) and apatite. Before blocks were sent to the participants, a quality check was performed on each block by the organizers at Cergy-Pontoise University. After drying the samples at 60° C for 24 hr, their P-wave velocity was measured at room conditions in three orthogonal directions, using ultrasonic transducers connected to a Panametrics 5058PR pulser and a digital oscilloscope. We observed that the P-wave velocity in the core axis direction increased with the distance from the tunnel, and decreased slightly with distance in the radial direction perpendicular to the foliation (David *et al.* 2017). This trend may result from mineralogical changes along the borehole or from the persistent influence of the excavation damage effects. A significant P-wave velocity anisotropy was found, due to the foliation inclination with respect to the core axis. It was necessary to require that all participants make permeability measurements in a common direction. This common direction was chosen for convenience as the core axis direction. Some laboratories performed additional permeability measurements in other directions, thus providing insight into the permeability anisotropy in the Grimsel granodiorite (see the discussion in the companion paper). The main result of this quality check was that reproducibility is acceptable.

## 3 PERMEABILITY MEASUREMENTS AT CONSTANT EFFECTIVE STRESS

We will use the following convention for presenting the data set. Each lab was assigned a number in increasing order based upon the distance between their sample and the borehole mouth. Lab#01 worked on the sample closest to the borehole mouth (i.e. closest to the tunnel wall), and Lab#24 on the farthest sample (i.e. the deepest from the tunnel wall).

In the following analysis, the number of results is larger than the number of laboratories in the KG<sup>2</sup>B team for several reasons: (i) some laboratories tested several small samples subcored from the original core, (ii) some laboratories made different kinds of measurements on a single sample. Before permeability measurements were made, the samples were systematically dried before being saturated with the working fluid. Our benchmarking exercise specifically excludes two-phase flow and relative permeability estimation which, although important, imply higher order of complexity.

### 3.1 General characteristics of the data set

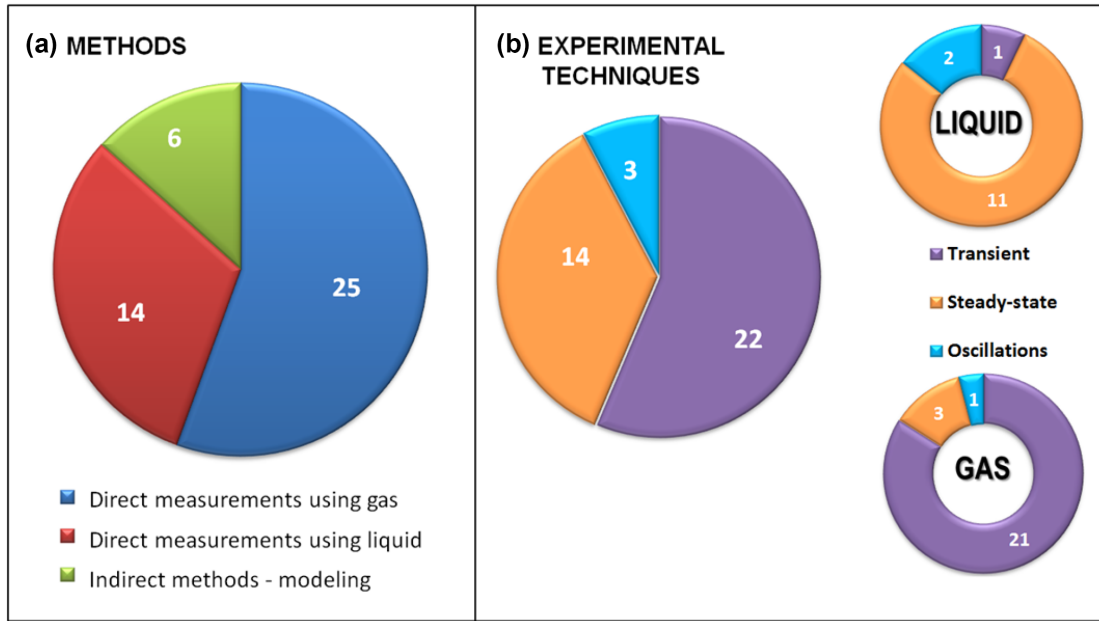
In Table B1 of Appendix B we report the location of each sample (distance from the tunnel), the size of the subcored samples on which permeability was measured, the method applied and the fluid used to conduct the measurements. In total we collected 45 permeability values from measurements (39) and modeling (6). Most of the results (56 per cent) come from direct measurements using gas as the pore fluid (Fig. 1a), about 31 per cent of the results come from direct measurements using liquids (mostly water) as the pore fluid, and only six results (about 13 per cent) were collected from models using microstructural data to predict the permeability. Here we will only consider the experimental data set, while the modeling data set will be presented in the companion paper. Fig. 1(b) summarizes the techniques which were used.

Regardless of the nature of the pore fluid, the transient technique was the most used (56 per cent) followed by the standard steady-state method (36 per cent), a direct application of Darcy’s law. A few laboratories used the pore pressure oscillation technique (8 per cent). The distribution is, however, very different if one takes into account the fluid used to measure the permeability. In experiments with liquid as the working fluid, 78 per cent of the results were obtained with the steady-state technique. In contrast, with gas as the working fluid, only 12 per cent of the results were obtained with the steady-state technique and 84 per cent of the results come from the pulse transient technique. Various gases were used: mostly nitrogen, but also argon, helium and air.

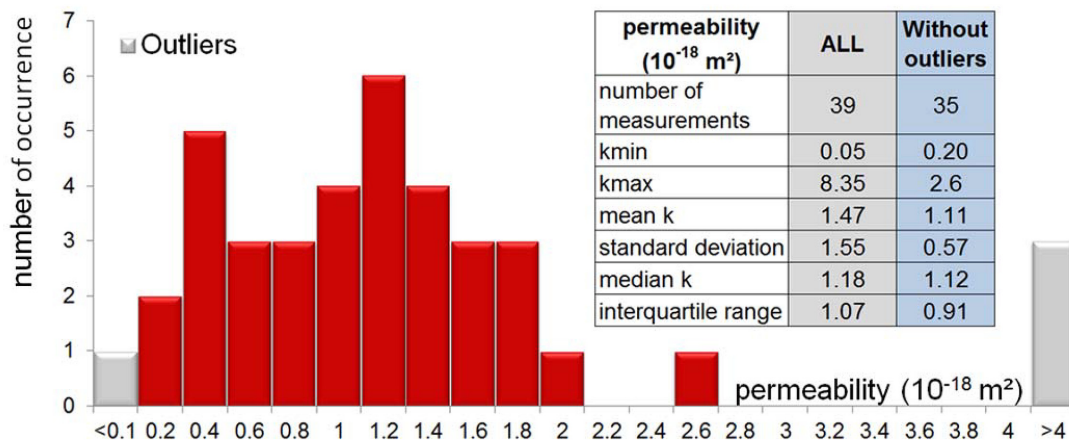
### 3.2 Statistical analysis of the raw data set

The complete data set is reported in Table B2 of Appendix B. Here we present the statistical analysis for all measured permeability values at 5 MPa effective pressure in the core axis direction only (no anisotropy effect included), regardless of the method, pore fluid or sample size (Fig. 2). For the complete data set, permeability ranges between 0.05 and  $8.35 \times 10^{-18} \text{ m}^2$ , with an average value of  $1.47 \times 10^{-18} \text{ m}^2$  and a high standard deviation of  $1.55 \times 10^{-18} \text{ m}^2$ . We identified four outliers (three in the last bin, one in the first bin in Fig. 2) with permeability higher or lower by a factor three than the average permeability. It is, consequently, preferable to use the median ( $1.18 \times 10^{-18} \text{ m}^2$ ) and interquartile range ( $1.07 \times 10^{-18} \text{ m}^2$ ) as estimators of the permeability statistics. If we remove the four outliers, we find a range of permeability spanning one order of





**Figure 1.** (a) Methods used in the benchmark and (b) techniques used for the experiments, global distribution (left) and distribution by working fluid type (right).



**Figure 2.** Statistical distribution of the raw data set for all methods, fluids and sample size. Each label gives the central value of each bin (e.g. bin 0.2 corresponds to the range [0.1, 0.3]).

magnitude (between  $0.20$  and  $2.6 \times 10^{-18} \text{ m}^2$ ) with a mean value of  $1.11 \times 10^{-18} \text{ m}^2$  close to the median ( $1.12 \times 10^{-18} \text{ m}^2$ ), and a standard deviation significantly reduced ( $0.57 \times 10^{-18} \text{ m}^2$ ). These values are in good agreement with the Grimsel granodiorite values reported by Schild *et al.* (2001)—between  $0.35$  and  $2.5 \times 10^{-18} \text{ m}^2$  at 5 MPa effective pressure, depending on the sample orientation with respect to foliation.

### 3.3 Influence of the pore fluid

Considering only the measurements in the core axis direction ('axial' flow), the 39 permeability values at 5 MPa effective pressure (Fig. 2) can be divided into two subsets based on the nature of the pore fluid (gas or liquid) used to measure the permeability. The statistical distribution of these two subsets exhibits two

overlapped distributions (Fig. 3) and defines possible new outliers for the gas group:  $2.6 \times 10^{-18} \text{ m}^2$  (extrapolated value and poorly defined stresses) and  $0.2 \times 10^{-18} \text{ m}^2$ . The influence of these possible gas outliers is low.

A first analysis shows that the statistical parameters of the gas subset are about twice those of the liquid sub-set without outliers. Whereas the lowest outlier value seems to reflect to a bad measurement (according to the operator who did the measurement), the higher ones probably owe to anomalous samples.

Permeability measurements using gas and liquid on a single sample were carried out by two labs with the following results:  $1.3$  and  $0.94 \times 10^{-18} \text{ m}^2$  @5 MPa (Lab#09) and  $0.034$  &  $0.028 \times 10^{-18} \text{ m}^2$  @27 MPa (Lab#23), respectively, giving a 1.3 ratio between gas and liquid permeability values. In both cases, the gas pressure was higher than 1.7 MPa and the Klinkenberg correction should be small.

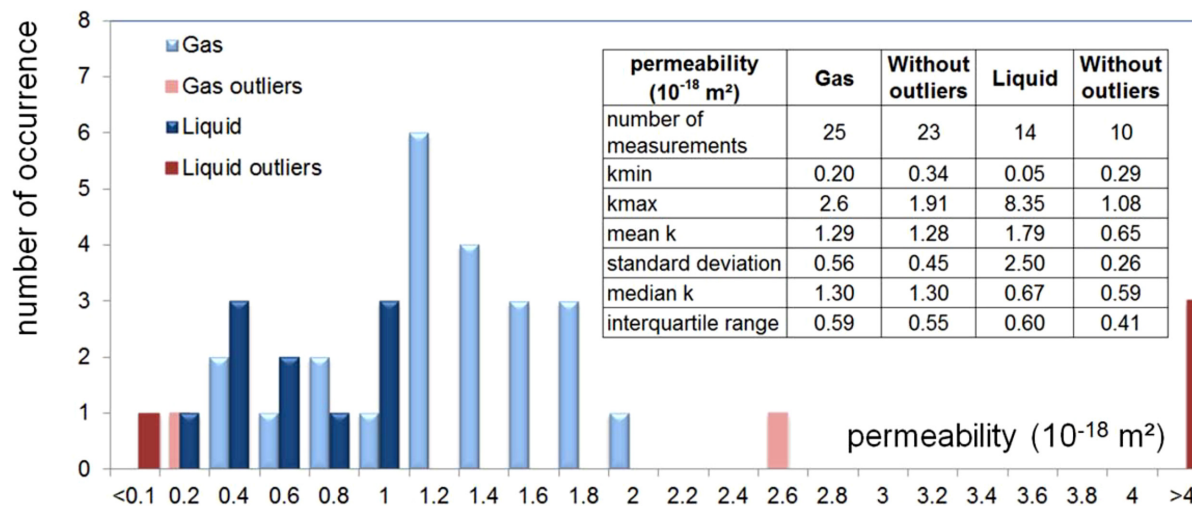


Figure 3. Statistical distribution of measured permeability values as a function of the working fluid.

Each team described the protocol used to saturate the porous space of the tested samples. There is no basis for associating low permeability values with incomplete saturation or to low pore pressures. Each lab which used a low gas pressure, attempted accurate evaluation of the Klinkenberg slip factor  $b$ .

Some labs provided several values of permeability by using the same sample with different gases, pore pressures and confinement pressures at constant effective pressure. Some labs used several sub samples from their initial piece of core. To remove the large weight of repetitive measurements, a single value for each lab was obtained by replacing multiple values by their average. The reduced data set contains 20 permeability values. Removing two outliers in the gas subset (light blue diamonds), the set of data was further reduced to 18 values: 11 for the gas subset and 7 for the liquid subset (Fig. 4).

The overlapping of gas and liquid sub-sets is now reduced and this new representation of the data clearly confirms that measured gas permeability values tend to be larger than liquid permeability values by a factor of about two. This significant difference leads us to separate both subsets in the following discussion.

### 3.4 Influence of the distance to the tunnel

The permeability as a function of distance to the tunnel (Fig. 5) shows no clear trend. David *et al.* (2017) reported P-wave velocity measurements at room temperature and unconfined conditions on the original core samples: they observed that P-wave velocity in the core axis direction increases with distance from the tunnel. The P-wave velocity increases linearly from  $\sim 4200$  m s<sup>-1</sup> at a distance of 4.2 m to approximately 4600 m s<sup>-1</sup> at 5.7 m, and then jumps to a value close to 4800 m s<sup>-1</sup> from 5.7 to 6 m. Between 4.2 and 5.7 m, the average gas permeability seems to be relatively constant, whereas the average liquid permeability seems to increase slightly. The observed trend in P-wave velocity may result from changes in mineralogy or foliation orientation along the borehole. This trend could also be linked to a varying Borehole Damage Zone which induced different stress release patterns from the tunnel to the deepest part of the borehole. Between 5.7 and 6 m, the average gas permeability seems to decrease, which could be correlated with the observed 200 m s<sup>-1</sup> jump in P-wave velocity. Both observations could reflect a preexisting crack density (Fortin *et al.* 2011), which is lower for the samples located between 5.7 and 6 m. However,

only three samples are located in this interval, so that we cannot draw any firm conclusion on the effect of sample location (distance to tunnel) or porosity (see companion paper).

### 3.5 Influence of the sample size

No recommendations were made with respect to sample size for permeability estimation. Most of the laboratories chose to subcore the provided material (Table B1) and prepared small samples (volume approximately 20 cm<sup>3</sup>, length 2–5 cm) in order to reduce the time required for completing the permeability measurements (David *et al.* 2017). Two laboratories decided to work directly on the original cores without subcoreing, whereas one group used a special device designed to work on tiny samples or chips (Lenormand *et al.* 2010). Permeability measurements with gas (open symbols) or liquid (solid symbols) are plotted in Fig. 6(a) as a function of sample length in the direction of flow. As mentioned previously there is a wide range of permeability values (about two orders of magnitude), and the scatter appears larger for smaller samples, while little variation is found for the few long samples that were studied. This size dependence can be linked to the magnitude of the representative elementary volume (REV), which may be large in the case of the Grimsel granodiorite because the grain size can be up to 2 cm (Schild *et al.* 2001). In Fig. 6(b) a density map obtained from micro-CT scanning reveals the size of mineralogical heterogeneities. Although the density map is not necessarily correlated with pore network heterogeneity, one may expect an REV size larger than a few centimetres.

The sample length  $L$  has also a significant influence on the time required to establish steady-state flow conditions. Assuming no gas slippage effect, the duration of the transient scales as  $(\mu C_f \phi / k) L^2$  with  $\phi$  the porosity,  $k$  the permeability,  $C_f$  the fluid compressibility and  $\mu$  the fluid viscosity. In addition there is a non-linear effect of mean pore pressure that can be quantified using numerical simulation. Taking  $k = 1.0 \times 10^{-18}$  m<sup>2</sup> and  $\phi = 1$  per cent for the Grimsel granodiorite, the transient time at low fluid pressure ( $< 1$  MPa) is about 15 s for a one centimeter long sample, but increases to about 30 min for a 10 cm long sample. At higher fluid pressure (approximately 10 MPa) the transient time is shorter, about 2 min for a 10 cm long sample. As stability is generally obtained after a few minutes, due to the relatively high permeability and low porosity,

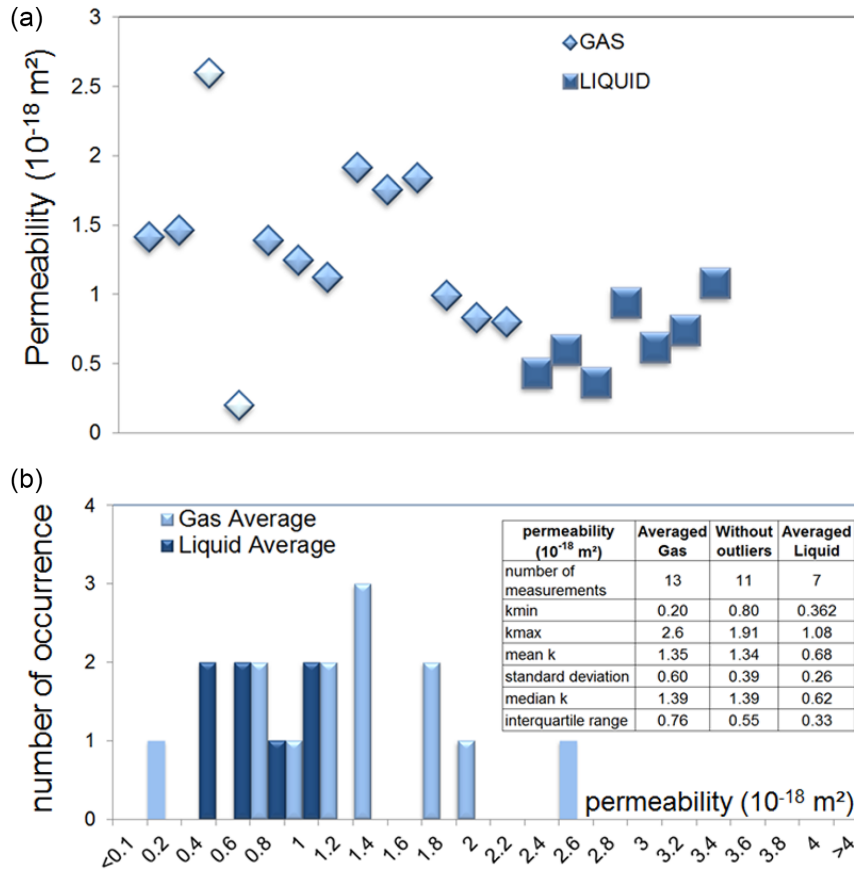


Figure 4. (a) Average permeability values at a 5 MPa effective pressure for each lab (data are ordered by lab number) and (b) statistical parameters for these average values.

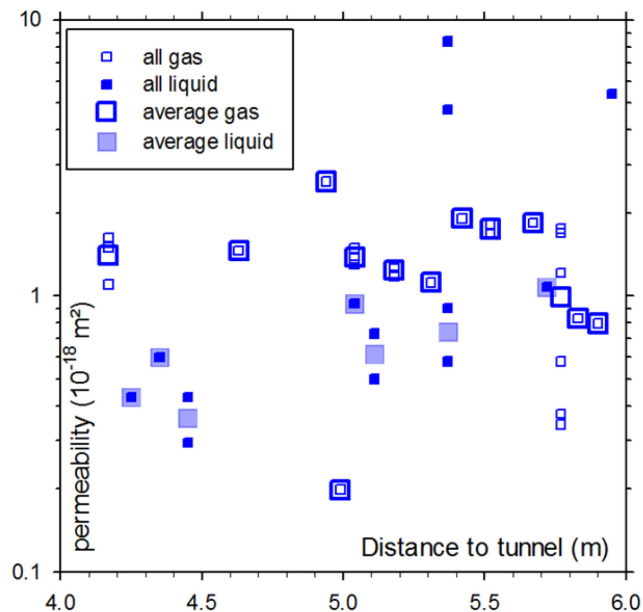


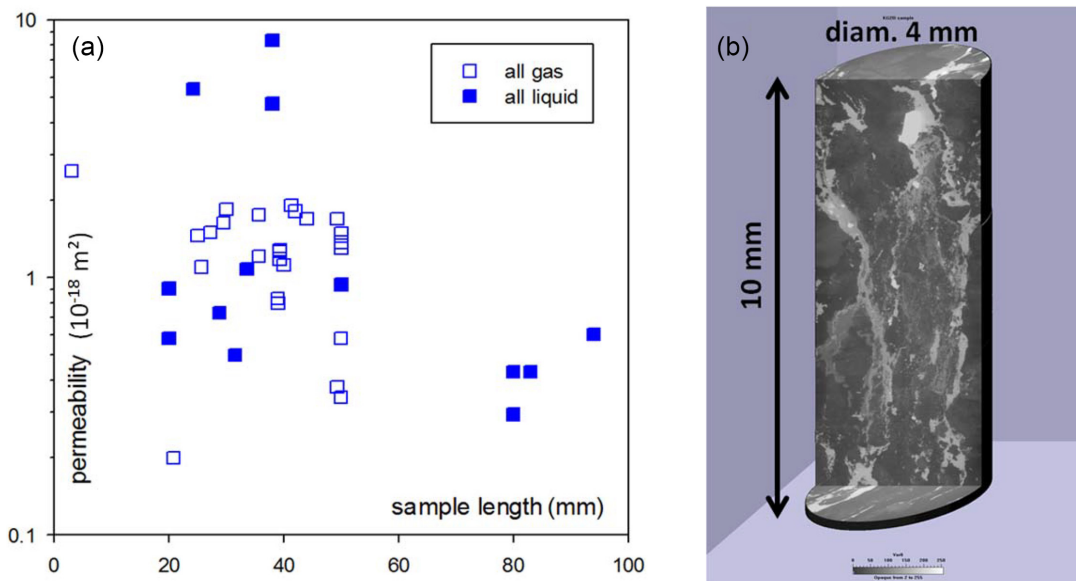
Figure 5. Measured axial permeability versus distance to the tunnel from which the long cores were drilled.

the transient is not likely to be a source of error for the KG<sup>2</sup>B measurements. However for a sample with a permeability in the range of 10<sup>-21</sup> m<sup>2</sup>, the stabilization time for a similar measurement at low pressure on a 10 cm plug would be multiplied by 1000 (20 d).

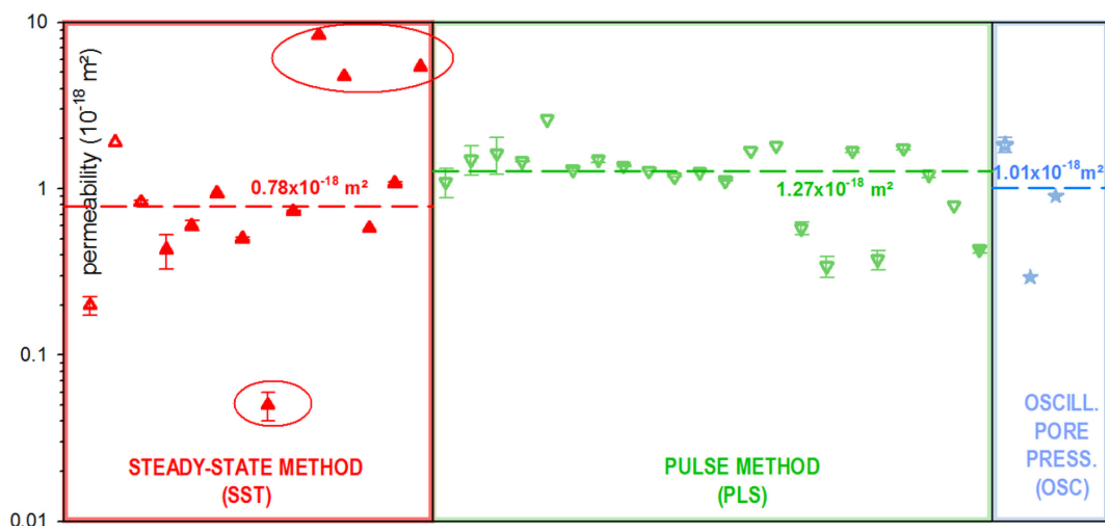
### 3.6 Influence of the experimental method

Steady-state measurements with gas were systematically corrected for the Klinkenberg effect. Not all transient measurements with gas were corrected for the Klinkenberg effect when the pore pressure was higher than 3 MPa. Several transient techniques were used to extract permeability from the recorded pressure decay data, including the standard transient pulse approximation (Brace *et al.* 1968), a complex transient inversion scheme that additionally provides specific storage (based on Kranz *et al.* 1990) and the more recent step decay method that provides the intrinsic permeability, porosity and Klinkenberg coefficient for gas measurements in tight rocks (Lasseux *et al.* 2012). In Fig. 7 the data set is divided into three groups according to the method used for measurements (SST for steady-state, PLS for transient pulse, and OSC for pore pressure oscillation). For each sub-group we also separate gas (open symbols) and liquid (solid symbols) measurements. For each subgroup, we estimated an average permeability value, omitting outliers. The average value for the transient pulse method (1.27 × 10<sup>-18</sup> m<sup>2</sup>) is the highest, and that for the steady state method is the smallest (0.78 × 10<sup>-18</sup> m<sup>2</sup>). For the pore pressure oscillation method, there are only three values available, so it is difficult to draw any statistically meaningful conclusion. Notice however that there is a great overlap between the division in terms of testing and the division in terms of working fluid (SST mostly liquids and PLS mostly gases).

To address this problem, we analyzed results provided by four teams who measured permeability on the same sample using different methods but the same pore fluid, sometimes at different pressure conditions (Lab#18). Fig. 8 is a cross-plot of permeability using one



**Figure 6.** (a) Measured axial permeability values versus sample length in the flow direction. (b) 3-D reconstruction from micro-CT images obtained on a small volume of Grimsel granodiorite (voxel size  $5 \mu\text{m}$ ).



**Figure 7.** Measured axial permeability for the different techniques used with error bars when known (data points are ordered by lab number in each group). Open symbols correspond to measurements using gas. Dashed lines correspond to the average permeability value per method (without the outliers highlighted by ellipses).

particular method versus permeability using another one. For this limited set of measurements, the permeability values are such that  $k_{\text{SST}} < k_{\text{OSC}} < k_{\text{PLS}}$  which is the same order derived from statistical analysis on the three subgroups (Fig. 7).

### 3.6.1 Example of Steady-state flow method for permeability determination

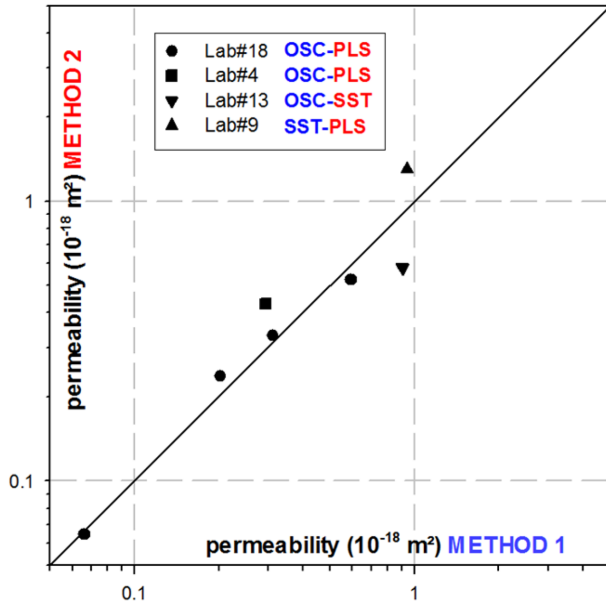
[Contribution of Lab#19] Permeability was measured on a section of whole core using the steady-state flow technique at a series of effective pressures and pore pressure gradients. Normally, subcores would be prepared from the original samples for testing. However, since the starting material had relatively large grain size, we decided that the best determination of average permeability would be obtained if the entire sample were tested. In this case, the core

circumference, which was smooth and even, was used without modification and faces were ground flat and parallel using a diamond wheel on a surface grinder. The resulting sample, shown in Fig. 9(a), had physical dimensions of diameter =  $8.3348 \pm 0.0008 \text{ cm}$  and height =  $3.3617 \pm 0.0005 \text{ cm}$ .

Stainless steel end caps with 1.5-mm-diameter centre holes and groove patterns on faces were placed on either end of the sample. Fine mesh stainless steel screen was placed between end caps and the sample to provide uniform pore pressure on sample faces. Shrink tubing covered the sample + end cap assembly which was then cast in 2-part polyurethane (approximately 5 mm thickness) to isolate the sample from the silicone oil confining fluid (Fig. 9b). A coiled stainless return tubing provided pore fluid access to the bottom end cap.

This assembly was placed in a pressure vessel and an initial confining pressure,  $P_c = 2 \text{ MPa}$  was applied. The pore pressure system





**Figure 8.** Comparison of permeability values for the same sample under the same pressure condition but using two different techniques. OSC, oscillating pore pressure method; SST, steady-state flow method; PLS, transient pulse method.

was evacuated and then pressurized to  $P_p = 1$  MPa with deionized water.  $P_c$  and  $P_p$  were then increased together to assure that effective pressure ( $P_{\text{eff}} = P_c - P_p$ ) never exceeded 2 MPa. The low-aspect-ratio cracks that provide flow paths in this crystalline rock are sensitive to effective pressure and have memory of past pressure history. Therefore, it is important that the target test pressure is not exceeded during sample pressurization.

Evacuation of the combined sample + pore pressure system, prior to saturation, is important in a low porosity sample to prevent air bubbles that would alter the fluid flow paths being trapped in the pore space. Conducting permeability tests at elevated pore pressure further reduces the risk of spurious measurements by compressing and dissolving remnant air bubbles that might remain trapped in pore space. The sample assembly in the pressure vessel, as well as the pore pressure pump and flow rate sensor were enclosed in a

temperature-controlled chamber that maintained  $23.5 \pm 0.1$  °C. For steady flow tests in low permeability samples, variations in ambient temperature can become the primary source of uncertainty in determining permeability, since room temperature changes produce fluid volume fluctuations that appear as transients in flow rate (Morrow *et al.* 2014, Fig. A1)

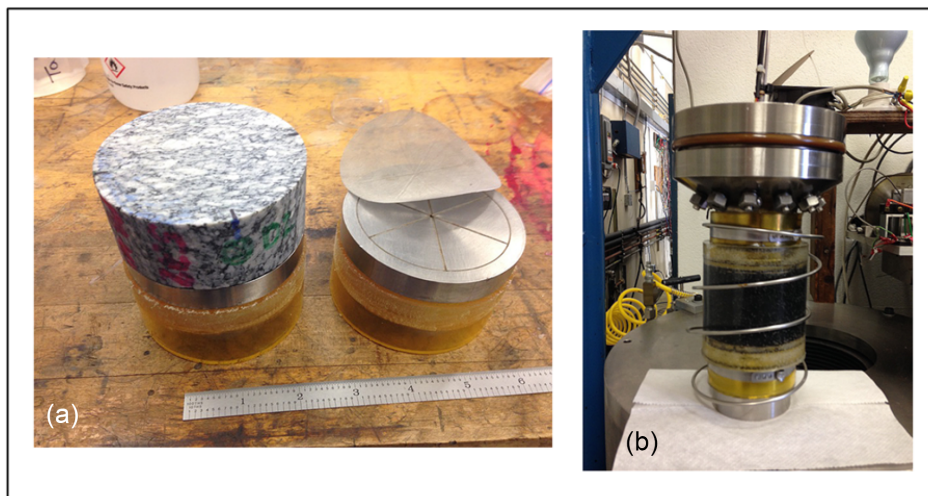
Confining pressure, up-stream ( $P_{\text{UP}}$ ) and down-stream ( $P_{\text{DOWN}}$ ) pore pressure were independently computer controlled. Reported effective pressure is defined as  $P_{\text{eff}} = P_c - P_p = P_c - P_{\text{MEAN}}$ , where  $P_{\text{MEAN}} = (P_{\text{UP}} + P_{\text{DOWN}})/2$  is the mean pore pressure. Pressure drop across the sample is just  $P = P_{\text{UP}} - P_{\text{DOWN}}$ . The pore pressure generator on the up-stream side of the sample recorded the change in pore volume ( $V_p$ ) needed to maintain constant pressure with a precision of  $10^{-5}$  cm<sup>3</sup>. This volume change was used to determine the volumetric flow rate,  $Q = dV_p/dt$ . Once the pressure drop across the sample is established and a steady state flow condition is attained, permeability  $k$  can be calculated from Darcy's law

$$k = \left( \frac{\mu L}{A} \right) Q / \Delta P, \quad (1)$$

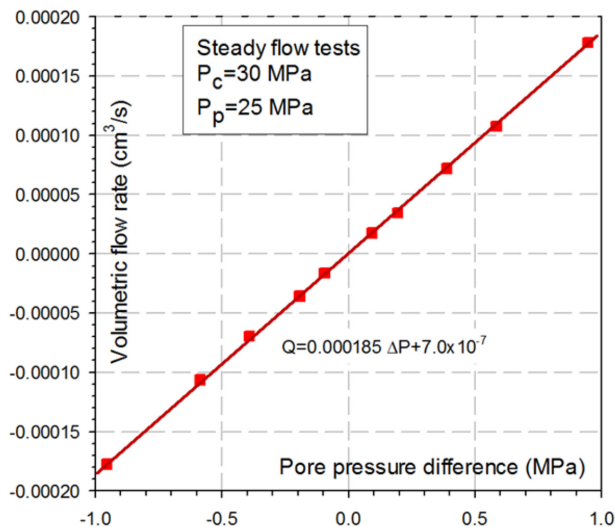
where  $A$  is the cross-sectional area of the sample. Dynamic viscosity of water at 23.5 °C is  $0.921 \times 10^{-3}$  Pa.s and  $L A^{-1}$  for this sample is  $0.06161$  cm<sup>-1</sup>. As an example, a flow measurement at  $P_c = 30$  MPa,  $P_{\text{eff}} = 5$  MPa and  $P = 0.946$  MPa resulted in  $k = 1.068 \times 10^{-18}$  m<sup>2</sup>.

This reported permeability is of limited use without estimating errors. We next consider different methods for determining confidence intervals for the permeability measurements. The first method is to take multiple measurements of  $k$  and compute a mean value and standard error. We performed a series of 10 flow tests at  $P_{\text{eff}} = 5.0$  MPa and at varying pore pressure gradients that produced both forward and reverse flow (Fig. 10). If we assume that the individual determinations of  $k$  are random samples from the same distribution, and the 'true' permeability is represented by the mean of the distribution, then uncertainty can be expressed as standard error of the measurements. In this case, permeability, based on ten measurements, is  $k = (1.04 \pm 0.01) \times 10^{-18}$  m<sup>2</sup>.

An equivalent method is to compute a least squares fit to the data in Fig. 10 to provide the ratio  $Q/P$ . The result, including a calculation of the formal error is  $\partial q/\partial P = 0.00185 \pm 0.00001$  cm<sup>3</sup>/MPa, and applying eq. (1) leads to a similar estimate of permeability.



**Figure 9.** (a) Whole core KG<sup>2</sup>B test sample with stainless steel end caps and stainless screen that assures uniform pore water access to sample faces. (b) Sample assembly, including coiled return pore fluid line, is jacketed and ready to place in the pressure vessel.



**Figure 10.** Permeability tests at  $P_{eff} = 5.0$  MPa. Flow rate is a linear function of pressure gradient,  $P$ , and using eq. (1) gives  $k = (1.04 \pm 0.01) \times 10^{-18}$  m<sup>2</sup>.

A more complete measure of uncertainty includes consideration of errors in all of the variables on the right-hand side of eq. (1). In this case, an uncertainty of  $\pm 0.1$  °C for the environmental chamber implies an uncertainty of  $\pm 0.002 \times 10^{-3}$  Pa.s in viscosity (i.e.  $\pm 0.2$  per cent). Uncertainties in physical sample dimensions ( $L A^{-1}$ ) are estimated to be only  $\pm 0.03$  per cent and errors in  $P$  are 0.001 MPa. Taken together, these contribute uncertainty of approximately  $\pm 0.5$  per cent in computing  $k$ . The final quantity to consider is the flow rate  $Q$ . The displacement transducer that measures  $V_p$  has a linearity of about 0.05 per cent which limits the accuracy of determining  $Q$ . During a permeability test,  $V_p$  is sampled ten times per second and averaged at 1 s intervals. If we assume that the errors in measuring  $V_p$  are uncorrelated, we can divide the total measurement time into  $N$  intervals of equal length and estimate a  $Q_i$  for each interval. Then, the mean of the  $Q_i$ 's provides an estimate of  $Q$  and the standard error provides an estimate of the uncertainty in  $Q$ . Using this approach, with the standard recording interval used in this study of approximately 2500 s, accuracy in determining  $Q$  was typically  $\pm 0.5$  per cent. Taken together with the uncertainties in the other variables, we estimate a total uncertainty in determining  $k$  of approximately 1 per cent. This is in close agreement with the confidence interval quoted above and probably represents the best accuracy that we can expect to achieve with the current test system. Notice that the two largest contributions to uncertainties in determining permeability are variations in ambient temperature and uncertainties in determining  $Q$ . Some improvement in accuracy can be gained by sampling flow rate over longer intervals. However, accuracy in  $Q$  will improve, at best, as  $(\text{time})^{1/2}$  and fluctuations in ambient temperature will ultimately limit accuracy. The importance of controlling ambient temperature cannot be overstated. The viscosity of water decreases by about  $0.02 \times 10^{-3}$  Pa.s °C<sup>-1</sup>, so an error of 1 °C in measurement temperature will result in a 2 per cent error in calculated permeability.

### 3.6.2 Example of transient method for permeability determination

[Contributions of Lab#11 and Lab#12] The transient (or pulse) method (Bruce *et al.* 1953) consists of instantaneously applying a pulse of differential pore fluid pressure across the sample that will re-equilibrate with time by fluid flow through the sample. An

interpretative model was reported later by (Brace *et al.* 1968). The permeability is derived from the time-dependent decrease of the upstream pore fluid pressure  $P_{UP}(t)$ , which can be approximated by an exponential law:

$$P_{UP}(t) - P_{\infty} \propto e^{-\alpha t} \text{ with } \alpha = \frac{kA}{\mu C_f L} \left( \frac{1}{V_{UP}} + \frac{1}{V_{DOWN}} \right), \quad (2)$$

where  $P_{\infty}$  is the final upstream pressure,  $k$  the permeability, and  $V_{UP}$  and  $V_{DOWN}$  the volume of the tanks connected to the upstream and downstream end of the sample, respectively. The permeability of a Grimsel granodiorite subcore (length = 40.10 mm; diameter = 19.74 mm) was measured in a high pressure vessel (maximum confining pressure 50 MPa) at room temperature using water as the confining medium and argon as pore fluid (Fig. 11a). Prior to experiments, the sample was vacuum dried at 40 °C for 48 hr, a period beyond which no additional mass decrease was recorded. To apply the confining pressure to the sample and avoid any leak, the sample was inserted in a rubber sleeve clamped onto end-pieces.

The decay through time of the upstream gas pressure  $P_{UP}$  is monitored whereas the downstream gas pressure  $P_{DOWN}$  is kept constant at atmospheric pressure  $P_{ATM}$ , that is  $P_{\infty} = P_{DOWN} = P_{ATM}$  and the term  $1/V_{DOWN}$  of eq. (2) can be neglected. This configuration was shown to be the optimal one for a pulse-decay experiment (Jannot *et al.* 2007). Since the experiments are run at constant temperature ( $T = 20$  °C) and low gas pressure ( $\leq 0.5$  MPa), one may also assume that the gas compressibility  $C_f$  can be approximated by  $C_f = 1/P_{MEAN}$ . Then, by calculating the time derivative of eq. (2), one obtains the following equation relating the gas permeability  $k_{gas}$  to the evolution of the upstream gas pressure:

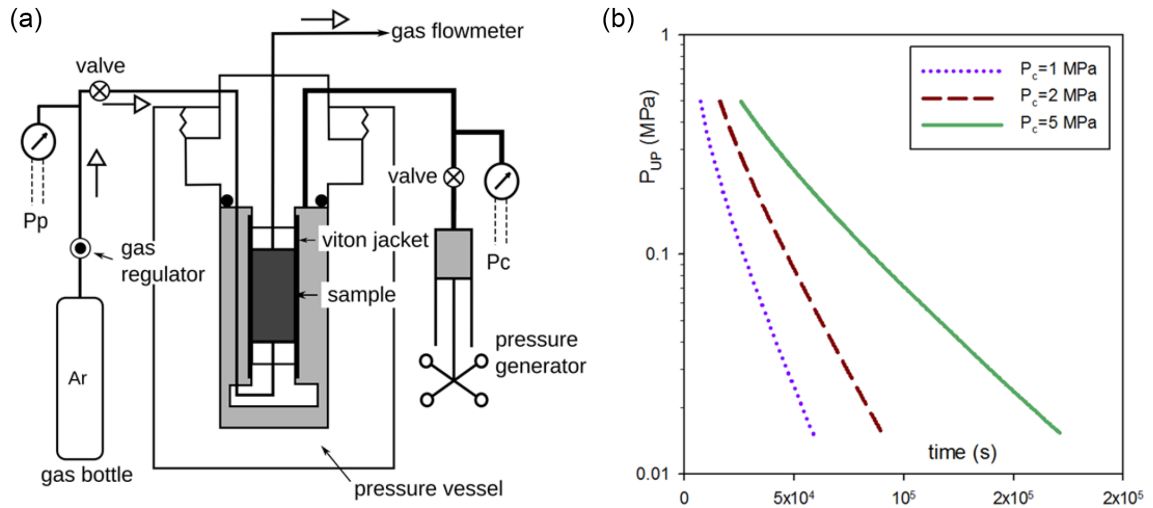
$$k_{gas} = \frac{\mu L}{A} \frac{V_{UP}}{P_{MEAN} \Delta P} \left| \frac{dP_{UP}}{dt} \right|, \quad (3)$$

where the viscosity of Argon is  $\mu = 2.21 \times 10^{-5}$  Pa.s at 20 °C. Due to the narrow flow path in such a low permeability rock, the Klinkenberg correction must be carried out (see the section devoted to slip flow). Three confining pressure levels were tested: 1, 2 and 5 MPa. For each pressure level, the sample was allowed to rest in the cell for one night. The upstream inlet gas pressure is then increased to 0.5 MPa, the outlet downstream gas pressure is maintained constant at atmospheric pressure and the outlet gas volume flow rate  $Q_{DOWN}^V$  is measured. Once the latter has stabilized, the inlet valve is closed and the upstream gas pressure is allowed to decrease. In Fig. 11(b), we show the pressure decay curves obtained at the various confining pressure levels. Note that in contrast to experiments using liquids (with constant compressibility), the pressure decay is not linear on the semi-log plot as expected from eq. (2): this is so because the gas compressibility depends on the mean pressure which decreases with time.

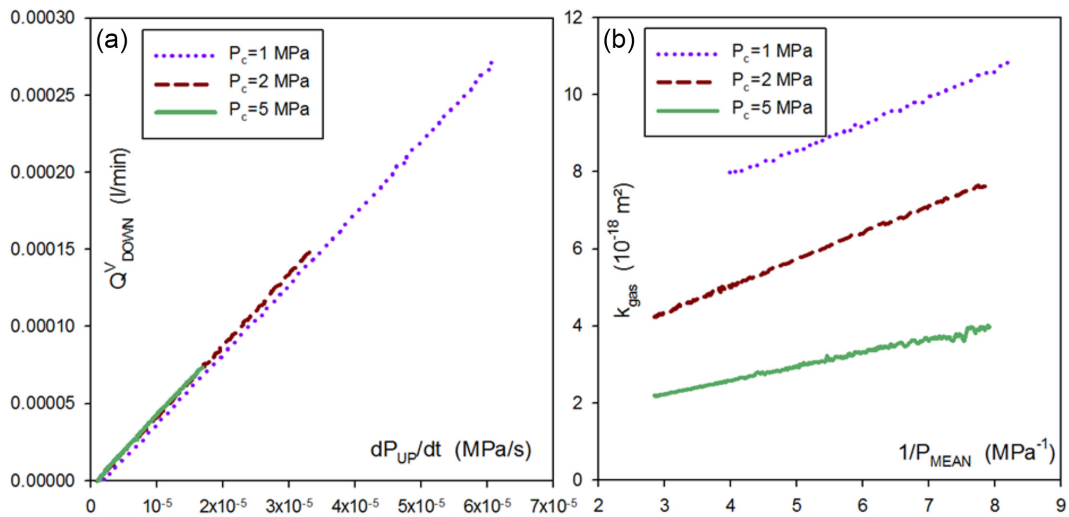
The time derivative of the pressure decay curve  $dP_{UP}/dt$  is calculated by applying a moving linear regression to the pressure decay curve over a constant number of points. The volume  $V_{UP}$  of the upstream gas circuit is either calibrated independently or by using the equation relating the outlet gas volume flow rate and the upstream pressure decay rate. At the upstream side of the sample, the inlet gas mass flow rate  $Q_{UP}^M$  is equal to:

$$Q_{UP}^M = \frac{M}{RT} V_{UP} \left| \frac{dP_{UP}}{dt} \right|, \quad (4)$$

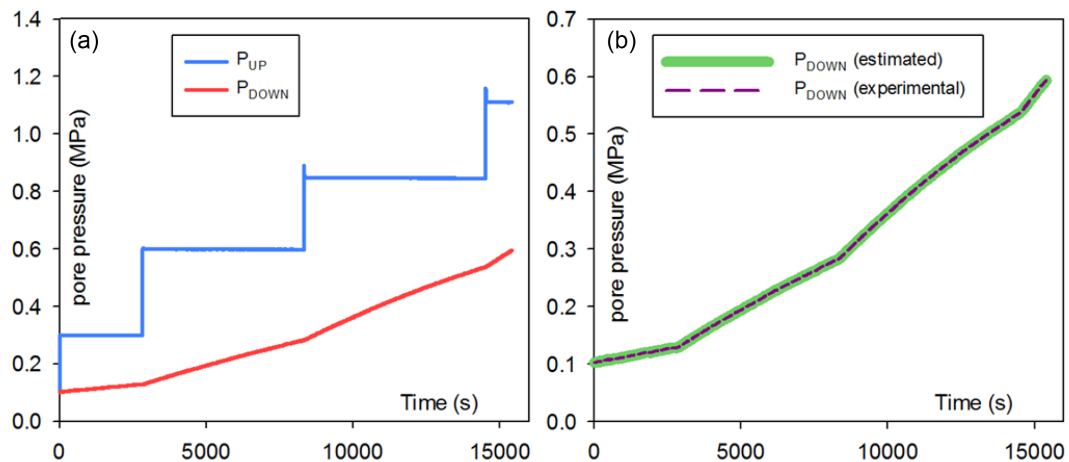
where  $M$  is the molar mass of the gas,  $R$  is the universal gas constant, and  $T$  is the temperature. Assuming that the gas mass stored in the sample can be neglected, we have  $Q_{UP}^M = Q_{DOWN}^M$ , where  $Q_{DOWN}^M$  is the outlet gas mass flow rate. The latter quantity can be expressed



**Figure 11.** (a) Experimental setup for measuring gas permeability in rock samples stressed up to 50 MPa hydrostatic confining pressure. (b) Pressure decay curves on a semi-log plot obtained at confining pressures  $P_c$  of 1, 2 and 5 MPa, respectively.



**Figure 12.** (a) Linear relationship between outlet flow rate and inlet pressure decrease obtained at a confining pressure  $P_c$  of 1, 2 and 5 MPa, respectively. (b) Evolution of gas permeability  $k_{gas}$  with mean gas pressure for the three tested confining pressure levels.



**Figure 13.** (a) Upstream ( $P_{UP}(t)$ ) and downstream ( $P_{DOWN}(t)$ ) pressure evolutions recorded during Test1. (b) Downstream pressure signal measured during Test1 and obtained from the model with the fitted parameters  $k$ ,  $b$  and  $\phi$  at the end of the inverse procedure.

as a function of the measured outlet gas volume flow rate  $Q_{\text{DOWN}}^{\text{V}}$ :

$$Q_{\text{DOWN}}^{\text{M}} = \frac{M}{RT} P_{\text{DOWN}} Q_{\text{DOWN}}^{\text{V}}. \quad (5)$$

Combining eqs (4) and (5) yields a relationship between the outlet gas volume flow rate and the upstream gas pressure decrease rate that allows calculation of the upstream volume  $V_{\text{UP}}$ :

$$Q_{\text{DOWN}}^{\text{V}} = \frac{V_{\text{UP}}}{P_{\text{DOWN}}} \left| \frac{dP_{\text{UP}}}{dt} \right|. \quad (6)$$

In Fig. 12(a), the linear relationship between outlet flow rate and inlet pressure time-derivative is shown for all three confining pressure levels. Assuming a constant atmospheric pressure  $P_{\text{DOWN}}$ , the volume of the upstream gas circuit is derived from the slope of this linear relationship following eq. (6). Then the apparent gas permeability  $k_{\text{gas}}$  is estimated from eq. (3) as a function of time and finally Klinkenberg's correction is applied to the data set in order to derive the true permeability  $k$  (see Section 4.2). In Fig. 12(b), the gas permeability  $k_{\text{gas}}$  is plotted versus inverse mean gas pressure  $1/P_{\text{MEAN}}$  for the three tested confining pressures. As one can see, the linear trend is rather good, confirming that Klinkenberg's correction has to be applied. The intercept of the best linear fit at  $1/P_{\text{MEAN}} = 0$  is the Klinkenberg corrected permeability which approximates the permeability measured using a liquid, and the Klinkenberg slip  $b$  factor is inferred from the slope. From the plot in Fig. 12(b) the following results are obtained: at 5 MPa confining pressure (effective confining pressure between 4.5 and 5 MPa, close to the  $\text{KG}^2\text{B}$  pressure target)  $k = 1.12 \times 10^{-18} \text{ m}^2$  and  $b = 0.33 \text{ MPa}$ ; at 2 MPa confining pressure  $k = 2.26 \times 10^{-18} \text{ m}^2$  and  $b = 0.30 \text{ MPa}$ ; at 1 MPa confining pressure  $k = 4.99 \times 10^{-18} \text{ m}^2$  and  $b = 0.15 \text{ MPa}$ . The last point is to check the reproducibility, and hence the accuracy, of the measurements. This has been done by doubling each measurement at each confining pressure level. After the first measurement, the sample was allowed to rest at the prescribed confining pressure for one night, before repeating the above mentioned procedure. Repeatability is very good, with permeability variations lower than 2 per cent.

The well-known and widely employed transient method based on the pulse decay technique described above has been extended recently (Lasseux *et al.* 2012; Patent WO/2011/08 9367, Lasseux & Jannot 2011). The main purpose for the development of this new method is to avoid repeating several experiments at different values of  $P_{\text{MEAN}}$  to determine permeability  $k$  and slippage factor  $b$ . One could consider using an inverse technique applied to the complete unsteady flow model for the pulse-decay instead of the approximated analytical model of eq. (1) so that these two parameters (along with porosity  $\phi$ ) could be identified on a single upstream pressure decay  $P_{\text{UP}}(t)$  in the least square sense (Jannot *et al.* 2008). However, the sensitivity of the signal to these parameters were shown to be insufficient in the general case for a reliable identification (Lasseux *et al.* 2012). With the step-decay method, a downstream tank is introduced and both  $P_{\text{UP}}(t)$  and  $P_{\text{DOWN}}(t)$  are recorded, the former being taken as the input for the history matching that is carried out on the latter considered as the response. While  $P_{\text{UP}}(t)$  can be modulated in any convenient way to improve sensitivity (a simple choice is a succession of steps, giving the name to the method of 'step-decay'), it was shown that, for the interpretation: (i) the volume of the upstream tank does not need to be known; (ii) the presence of a dead volume between the upstream tank and the entrance of the porous sample, which represents a critical issue in the pulse decay method, is of no consequence on the measurement and can be ignored and (iii) any irregularity on  $P_{\text{UP}}(t)$ , due to thermal effects

or resulting from a leak at the upstream, will not introduce any bias in the interpretation as it is part of the input signal. Moreover, it was shown that, with this method, the three parameters,  $k$ ,  $b$  and  $\phi$ , can be simultaneously identified from a single experiment (Lasseux *et al.* 2012).

The step decay experiment was run with nitrogen at 30 °C on a Grimsel granodiorite sub-core (length = 39.32 mm, diameter = 25.48 mm) that was first dried at 30 °C for 3 weeks. The sample was placed in a Hassler sleeve and a confining pressure of 5.5 MPa was applied. The volume of  $V_{\text{DOWN}}$  was determined from 100 nitrogen pycnometry tests yielding  $V_{\text{DOWN}} = 8.38 \text{ cm}^3$  with a standard deviation of  $0.018 \text{ cm}^3$ . Three different tests were carried out for which the applied average pore pressure difference over the different upstream pressure steps were 0.376 MPa (Test1, 4 steps), 0.275 MPa (Test2, 7 steps) and 0.327 MPa (Test3, 4 steps). The experimental recording times of  $P_{\text{UP}}(t)$  and  $P_{\text{DOWN}}(t)$  were 4h16min (Test1), 3h27min (Test2) and 1h10min (Test3).

The interpretation, using an inverse technique, is performed with a complete model with no assumption, except that the flow is isothermal and 1-D in the  $x$ -direction within the sample which upstream and downstream faces are at  $x = 0$  and  $x = L$ , respectively, while the gas is supposed to obey ideal gas law:

$$\frac{\partial^2 \Pi}{\partial x^2} = \frac{\phi \mu}{k} \frac{1}{\sqrt{\Pi}} \frac{\partial \Pi}{\partial t}, \quad \Pi = \Pi(x, t) = (P(x, t) + b)^2 \quad (7)$$

$$\Pi(x, 0) = (P(x, 0) + b)^2, \quad 0 \leq x \leq L \quad (8)$$

$$\Pi(0, t) = (P_{\text{UP}}(t) + b)^2, \quad t \geq 0 \quad (9)$$

$$\frac{\partial \Pi}{\partial t} \Big|_{x=L} = \frac{kA}{\mu V_{\text{DOWN}}} \left( \sqrt{\Pi} \frac{\partial \Pi}{\partial x} \right)_{x=L}, \quad t \geq 0. \quad (10)$$

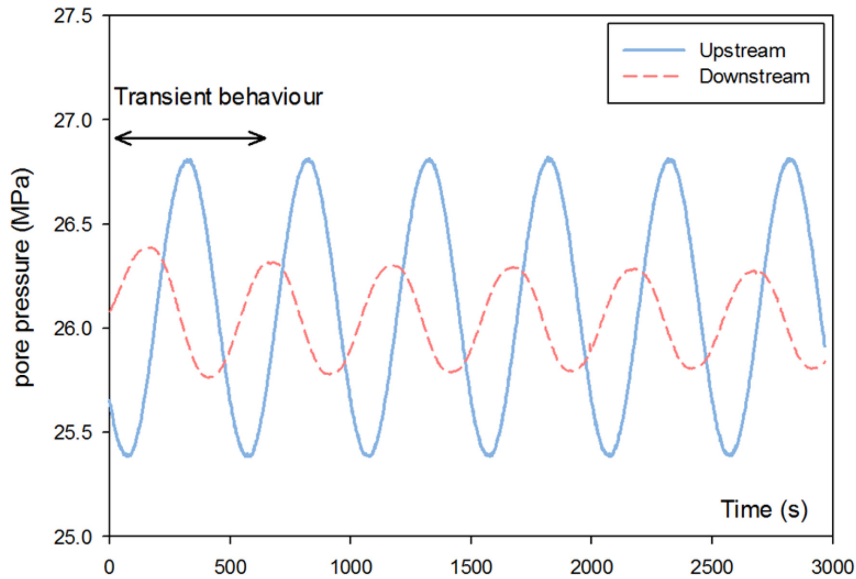
The recorded evolution of  $P_{\text{UP}}(t)$  and  $P_{\text{DOWN}}(t)$  for Test1 are reported in Fig. 13(a). For the same experiment, the comparison between the measured signal  $P_{\text{DOWN}}(t)$  and the signal obtained at the end of the inverse procedure with the identified parameters  $k$ ,  $b$  and  $\phi$  in the least square sense is represented in Fig. 13(b), showing the excellent fit obtained with this procedure.

The fitted values of the parameters are, respectively,  $k = 1.28 \times 10^{-18} \text{ m}^2$ ,  $b = 0.257 \text{ MPa}$  and  $\phi = 0.012$  for Test1;  $k = 1.18 \times 10^{-18} \text{ m}^2$ ,  $b = 0.304 \text{ MPa}$  and  $\phi = 0.008$  for Test2;  $k = 1.26 \times 10^{-18} \text{ m}^2$ ,  $b = 0.279 \text{ MPa}$  and  $\phi = 0.012$  for Test3. These values are consistent, in their trend, with the expected variations due to the difference between the confining pressure and the actual average pore pressure in the three different tests. Moreover, repeatability tests showed few per cent of error on the above values.

### 3.6.3 Example of oscillating pore pressure method for permeability determination

[Contribution of Lab#18] Initially proposed by Turner (1958), the oscillation method was first applied to rocks by Kranz *et al.* (1990) and Fischer (1992). It uses a fixed-frequency, sinusoidally oscillating pore pressure signal applied at one end of the sample. The resultant (downstream) signal maintains the same period as the upstream signal, but is amplitude-attenuated and phase-shifted (Fig. 14).





**Figure 14.** Example of oscillating pore pressure behaviour, showing amplitude attenuation of the forcing waveform and the phase shift of the downstream wave.

Bernabé *et al.* (2006) re-analyzed the oscillating pore pressure method and defined two independent dimensionless material parameters;  $\eta$  (dimensionless permeability) and  $\xi$  (dimensionless storativity ratio) which are functions of permeability and specimen storativity ( $\beta$ , Pa<sup>-1</sup>), respectively and are defined:

$$\eta = \frac{A\tau k}{\pi L\mu\beta_D} \quad (11)$$

$$\xi = \frac{AL\beta}{\beta_D}, \quad (12)$$

where  $\tau$  is the oscillation period (s), and  $\beta_D$  the downstream reservoir storage (m<sup>3</sup> Pa<sup>-1</sup>). Bernabé *et al.* (2006) improved upon the solutions presented by Kranz *et al.* (1990) and Fischer (1992) by defining  $\xi$  and  $\eta$  such that each would be dependent on only one material parameter of the rock, thus allowing them to be assessed as independent material properties. In terms of  $\xi$  and  $\eta$  the solution to the diffusion equation is:

$$Ge^{-i\theta} = \left( \frac{1+i}{\sqrt{\xi}\eta} \sinh \left[ (1+i) \sqrt{\frac{\xi}{\eta}} \right] + \cosh \left[ (1+i) \sqrt{\frac{\xi}{\eta}} \right] \right)^{-1} \quad (13)$$

$G$  is the ratio of downstream to upstream wave amplitude (Gain) and  $\theta$  is the phase shift between the upstream and downstream waveforms. Solving eq. (13) to find  $G$  and  $\theta$  using a range of valid values of  $\eta$  and  $\xi$  defines the region in which physically meaningful values of  $G$  and  $\theta$  can be found. The region is limited by the lines  $\xi = 0$  and  $\xi \rightarrow \infty$  (Bernabé *et al.* 2006). Sample storativity ( $\beta$ ) is directly proportional to porosity ( $\phi$ ) and is given by:

$$\beta = \phi (C_f + C_p), \quad (14)$$

where  $C_p$  is the compressibility of the porosity in response to changes in pore pressure at constant confining pressure. As  $C_f \gg C_p$  the  $C_f \phi$  term will dominate. Thus iso- $\xi$  paths are nominally lines of constant porosity for a given value of downstream storage volume provided the compressibility of the pore fluid and the pores remain constant, there are no adsorption-desorption effects, and the sample behaves isotropically.

When the permeating fluid is a liquid its compressibility is small and varies only slowly with pressure, but for an ideal gas the compressibility is  $1/P_p$ . At low temperatures and high pressures gases become non ideal, expressed by the gas deviation factor  $Z$  in the gas law for a single mole:

$$P_p V = ZRT, \quad (15)$$

where  $V$  is the gas volume. The gas compressibility is modified thus

$$c_f = \frac{1}{P_p} - \frac{1}{Z} \left( \frac{dZ}{dP_p} \right)_T. \quad (16)$$

For argon gas, for example, Stewart & Jacobsen (1989) show how  $Z$  varies with pressure, from which  $C_f(P_p)$  can be calculated. Viscosity of the pore fluid must also be known as a function of pressure and temperature. For liquids the viscosity varies only slowly with pressure and temperature, but larger variations apply for gases. Data for argon are provided in Michels *et al.* (1954) and Younglove & Hanley (1986).

Applying this method, it is usual to work with short core plugs, for example 25 mm in length and of similar diameter. Samples are jacketed in rubber tubing sealed to end pistons bearing a narrow (1 mm diameter) hole to carry the pore fluid. Sintered metal discs are placed at each end of the specimen to diffuse the pore fluid across the whole diameter of the specimen. It is important that the jacket be pressed uniformly against the outer surface of the specimen to prevent short-circuit fluid paths. A steel blank can be used in lieu of a specimen to ensure that the experimental arrangements do not permit any unwanted fluid flow and for calibration of the downstream volume. It is important to avoid any contamination of the specimen with liquid when gas is being used as a permeant. Liquid contamination will generally reduce apparent permeability.

The downstream volume (including pipework, downstream sintered plate and pressure transducer) must be determined as accurately as possible, and for very low permeability materials this volume will usually be as small as is feasible. Filler rods can be inserted into the pipes to minimize the volume further. For good resolution of low permeabilities a downstream volume of less than 500 mm<sup>3</sup> is desirable. The downstream pressure transducer must have high sensitivity (typically 0.02 MPa) and good stability. A servo-controlled

piston-cylinder pressure generator/volumometer can be used to determine the downstream volume by first establishing an upstream pore pressure, then opening access to the downstream volume and measuring the volume of fluid that must be accepted to bring the downstream volume to the same pressure. In order to investigate the sensitivity of permeability to effective pressure, experiments are carried out over a sequence of confining pressures at a fixed pore pressure. Initially the confining and pore pressures must be raised together such that the minimum desired effective pressure is not exceeded, to avoid permanent changes to permeability before permeability measurement at low effective pressure. The desired mean pore pressure and confining pressures are allowed to stabilize, with the open bypass valve linking upstream and downstream reservoirs. The bypass valve is closed slowly, to prevent buildup of unequal pore pressures and the upstream oscillation is started. The amplitude of the oscillation will typically be 1 MPa or less, to avoid violation of Darcy's law and pressure transients due to adiabatic heating and cooling. After any initial transient effects a downstream waveform at a constant mean pressure will develop, after which data from approximately 10 cycles will be collected (Fig. 14). The period of the forcing waveform can be varied between about 60 s and several thousand seconds, in order to keep the gain ratio smaller than about 0.7, above which the resolution of permeability rapidly deteriorates (Fig. 15a).

From these data the gain (ratio of downstream to upstream wave amplitudes) and phase shift must be determined. This can be done in several ways (i) from the Fourier transforms of the two waveforms (e.g. Faulkner & Rutter 2000; Bernabé *et al.* 2006; Song & Renner 2007), (ii) from the parameters (orientation and axial ratio) of the Lissajou ellipses linking the two waveforms (e.g. Song & Renner 2007) or (iii) by applying inverse amplitude ratio and phase shifts to match the two waveforms. The permeability is found by solving eq. (13) iteratively for both  $\eta$  and  $\xi$ , from which permeability and storativity can be calculated. This can be done using a numerical equation solver. Initial values of  $\xi$  and  $\eta$  are obtained from a look-up table containing the values plotted in Fig. 15(a). The algorithm then seeks the values of  $\xi$  and  $\eta$  that simultaneously solve the modulus and argument of eq. (13) that correspond to the measured amplitude ratio  $G$  and phase shift  $\theta$ , respectively.

Core plugs with three different orientations were taken from the main core section; the gneiss foliation plane is oriented  $16^\circ$  to the axis of the main core. Core A is parallel to the large core axis, Core B is normal to the main core axis and parallel to the foliation, and core C is perpendicular to the first two, nearly normal to the foliation. Helium pycnometry for four short core plugs yielded porosity  $1.028 \pm 0.011$  per cent. Permeability for each core orientation was measured at a constant effective pressure ( $P_{\text{eff}}$ ) of 4.5 MPa, at each of three different pore pressures, 5.5, 10.5 and 15.5 MPa (Fig. 15b). Anisotropy is low, with the foliation-normal orientation displaying the lowest permeability (see section on anisotropy in the companion paper).

The experimental data in Fig. 15(a) plot well to the left of the expected trend for a porosity of 1.0 per cent, and imply that flow does not access all pore space with equal facility. The sample storativity calculated using  $\xi$  from the oscillation technique is commonly found to be lower than the total storativity of the sample, calculated from porosity ( $\phi$ ), the known compressibility of the pore fluid using eq. (12) (Fischer 1992) and the downstream storage of the experimental setup. This is evident from the plot of  $\log G$  versus phase shift  $\theta$  for the Grimsel granodiorite (Fig. 15a). The data lie along a track expected for a porosity of 0.3 per cent or smaller, compared with the track expected for the measured porosity. There is a weak

indication that the deviation is greater for foliation-parallel flow than foliation-normal flow. Stronger deviation is seen for anisotropically textured rocks (e.g. Mckernan *et al.* 2017), and suggests that for 1-D fluid flow a reduced fraction of the pore space is readily accessible. In contrast, porosity measurement when all faces of the specimen are equally accessible to permeating gas allows the full connected porosity to be measured.

#### 4 PRESSURE DEPENDENCE OF PERMEABILITY

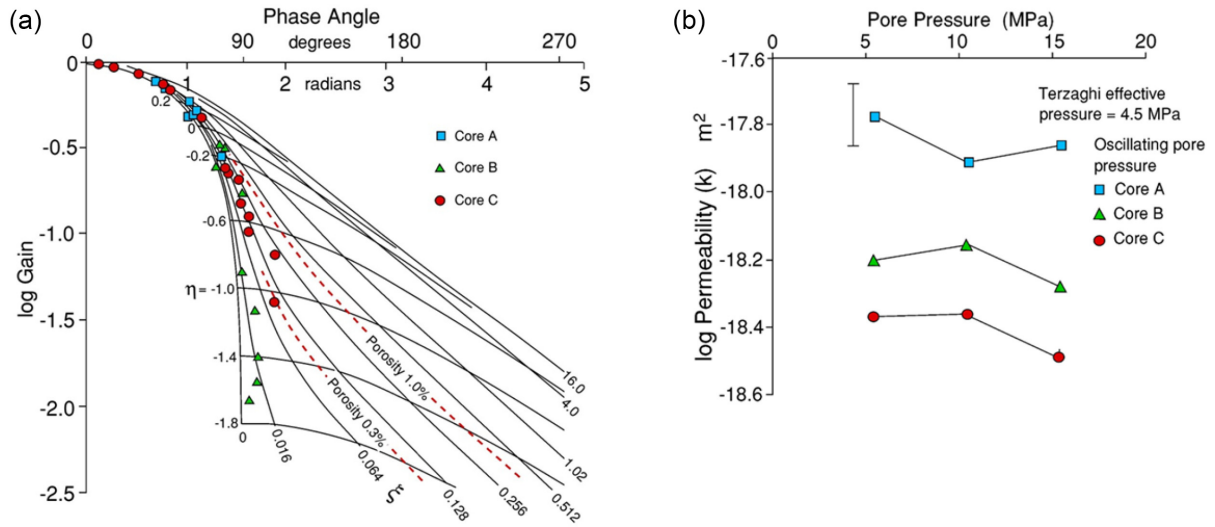
The main target of the benchmarking exercise was permeability of the Grimsel granodiorite samples at 5 MPa effective pressure; in addition, on a voluntary basis, measurement at *in situ* effective pressure (30 MPa) was also encouraged. Several teams provided measurements at several pressures. Therefore we have: (i) single permeability values at 5 and 30 MPa (2-point analysis, 4 teams), (ii) multiple permeability values over an extended pressure range of 1–30 MPa (multipoint analysis, 9 teams). The complete data set is given in Table 1 and the results for the second data set are shown in Fig. 16(b). Note that the effective pressure is defined here as the difference between confining and pore pressure, corresponding to an effective pressure coefficient  $\alpha$  equal to 1, in good agreement with the effective pressure law found by one participating lab (Fig. 16a) showing that permeability measurements are nearly constant at fixed confining pressure minus pore pressure (2 MPa). Note that the weak increasing trend in Fig. 16(a) suggesting that  $\alpha$  could be larger than one is not considered as meaningful, and probably results from errors in the measurements. It should also be noted that these data do not allow separation of pressure sensitivity in response to variations of effective pressure by varying total confining pressure at constant pore pressure, compared with varying pore pressure at a constant total confining pressure. Differences in behavior in this respect have been discussed for various rock types by several authors, (e.g. Kwon *et al.* 2001; Heller *et al.* 2014; Mckernan *et al.* 2017).

A striking result is that the permeability evolution with effective pressure is generally linear on the semi-log plot: therefore the pressure-dependence of permeability can be accounted for using an exponential law:

$$k = k_0 \exp(-\gamma P_{\text{eff}}) \quad (17)$$

Such an exponential decrease is in agreement with the data compiled by David *et al.* (1994) for sedimentary and hard rocks. The stress-sensitivity parameter  $\gamma$  and zero-pressure permeability parameter  $k_0$  are given in Table 1.

In the pressure range above 5 MPa, four experiments (Lab#4, 5, 9 and 21) found quite consistent results, with an average stress-sensitivity parameter  $\gamma = 0.093 \pm 0.015 \text{ MPa}^{-1}$  while two other experiments found both lower permeability and stronger pressure dependence ( $\gamma > 0.18 \text{ MPa}^{-1}$ ), possibly because these samples might have lower crack density and with higher compliance and/or because of the different sample orientation (Lab#18). In their compilation for crystalline, metamorphic and volcanic rocks, David *et al.* (1994) found that the stress-sensitivity parameter  $\gamma$  ranged between 0.023 and  $0.11 \text{ MPa}^{-1}$ ; the Grimsel granodiorite is toward the higher end of this range. In the pressure range below 5 MPa, the pressure dependence seems also to be larger (except for Lab#07 who applied only axial stress). In this pressure range, one might both be impacted by crack closure and possibly leakage flow at the sample surface. From the 2-point analysis, we estimated the ratio



**Figure 15.** (a) Solution space of eq. (13) bounded by curves for  $\xi = 0$  and 16, showing how gain and phase angle relate to  $\eta$  and  $\xi$ , with experimental results for KG<sup>2</sup>B cores A, B and C. (b) Permeability versus pore pressure at constant effective pressure (4.5 MPa) for the three cores.

**Table 1.** Permeability measured at different effective pressures.

	PERM ( $10^{-18}$ m <sup>2</sup> )	2-Point analysis	Ratio			
	@5MPa	PERM ( $10^{-18}$ m <sup>2</sup> ) @30MPa		$k_o$ ( $10^{-18}$ m <sup>2</sup> )	Multipoint analysis $\gamma$ (MPa <sup>-1</sup> )	Comment
Lab#02 (L)	<b>0.43</b>	<b>0.030</b>	14.3			
Lab#13 (L)	<b>0.91</b>	<b>0.277</b>	3.27			
Lab#14 (G)	<b>1.91</b>	<b>0.189</b>	10.1			
Lab#16 (G)	<b>1.81</b>	<b>0.155</b>	11.7			
Lab#04 (L)	<b>0.43</b>	<i>0.043</i>	10.0	0.609	0.0885	fit on 5 points
Lab#19 (L)	<b>1.08</b>	<i>0.0118</i>	91.4	2.65	0.180	fit on 4 points, low pressure range
Lab#23 (L)	<i>Not relevant</i>	<i>0.00101</i>	–	30.0	0.343	fit on 5 points, high pressure range
Lab#05 (G)	<b>1.46</b>	<i>0.068</i>	21.5	2.26	0.117	fit on 7 points
Lab#07 (G)	2.78	<i>0.474</i>	5.86	3.96	0.0707	fit on 5 points, low pressure range, axial stress only
Lab#12 (G)	<b>1.12</b>			not exponential		low pressure range
Lab#09 (G)	<b>0.92</b>	<i>0.115</i>	8.03	1.43	0.0842	fit on 6 points
Lab#18 (G)	<b>0.25</b>	<i>0.00257</i>	98.7	0.666	0.185	fit on 4 points, radial normal to foliation permeability
Lab#21 (G)	<b>0.83</b>	<i>0.0758</i>	10.9	0.975	0.0851	fit on 10 points

For the multipoint analyses, exponential laws with parameters  $k_o$  and  $\gamma$  have been determined. Bold numbers are measurements; italic numbers are extrapolated values from the exponential law. All data were obtained for the axial core orientation unless otherwise stated.

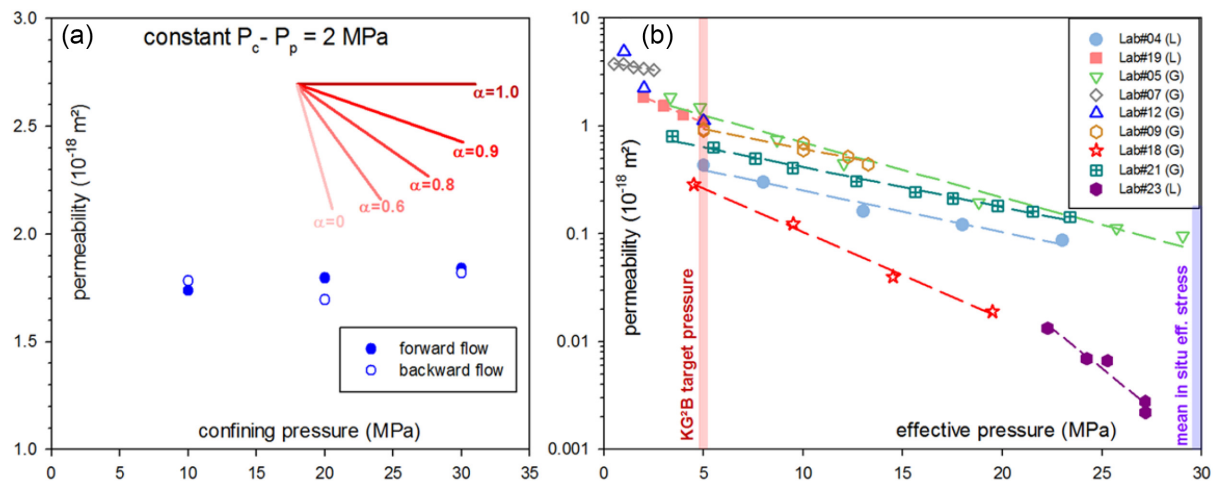
$k(P_{eff} = 5 \text{ MPa})/k(P_{eff} = 30 \text{ MPa})$  for both measured and extrapolated values (Table 1). Except two large values close to 100, most of the ratios range between 3.3 and 21 with an average value of 10.6. The Grimsel granodiorite exhibits a strong pressure dependence of permeability which can be well described by an exponential law.

## 5 DISCUSSION

### 5.1 Outcome of the Benchmarking exercise

Three main techniques were used to test sample permeability: steady-state flow that satisfies Darcy’s law, pulse-decay (Brace *et al.* 1968) and oscillating flow (Fischer & Paterson 1992; Kranz *et al.* 1990). The steady-state flow technique is often the simplest and

easiest to interpret. Some rocks such as shales, clay-rich sandstones and fault gouge undergo time-dependent relaxation in response to pressure changes or the introduction of pore fluid (Gehne & Benson 2017). The steady-state method, which requires establishment of a constant flow rate, can be used to identify when transient changes in pore geometry have ended and a reliable measurement of permeability can be made. In some cases, the time needed for a sample to adjust to a new stress state can be in excess of a day (Morrow *et al.* 2014). If the sample has low permeability, then the flow rate due to an applied pressure gradient will be low, and water expelled as the sample compacts can result in erroneous flow rate determinations. Reversing the flow direction can help identify when time-dependent pore volume changes are important. Otherwise, it is best to confirm independently that changes in porosity have ceased before starting



**Figure 16.** (a) Test on effective pressure law by Lab#19 showing permeability measurements are consistent with  $\alpha = 1$ ; (b) Permeability versus effective pressure. Solid symbols: measurements with liquid; open symbols: measurements with gas. All the measurements were made in the core axis direction.

the flow test. For low permeability samples with small flow rates, both a high-accuracy flow sensor and a stable test chamber (especially controlled temperature) are needed for accurate determination of permeability (see Section 3.6.1). In describing flow in porous media, effects are separated between fluid properties (viscosity,  $\mu$ ) and pore geometry (permeability,  $k$ ) with flow rate  $Q$  proportional to  $k/\mu$ . Thus, for low permeability samples, increased flow rate can be accomplished by using a low-viscosity fluid, typically argon or nitrogen.

When testing low permeability crystalline rocks, accurate measurement of steady-state flow rate can be technically challenging. Brace *et al.* (1968) presented a transient pulse-decay technique that avoided this difficulty by measuring transient pressure changes rather than flow rate. This can be a fast and reliable method for measuring low permeability. It requires that the volume in closed chambers connected to the sample be optimized for the flow rate such that fluid flow through the sample produces a measurable pressure change over a convenient time interval. Similar to the steady-state technique, relaxation of pore volume in response to changes in stress state can produce pressure transients that mimic pressure transients from the pulse-decay test. Therefore, care must be taken to minimize these potential sources of error. On account of the small pressurized volumes used, the technique is very sensitive to any slow pressure leaks. Changes in ambient temperature can also lead to erroneous signals and need to be identified when making pulse-decay measurements.

The oscillating flow technique introduced for rocks in the early 1990's (Kranz *et al.* 1990; Fischer 1992; Fischer & Paterson 1992) represents a significant advance in the measurement of flow properties of geologic materials. A time-independent oscillating pore pressure (generally a sine wave) is applied on one side of the sample and the amplitude and phase of the pressure in a chamber attached to the other side of the sample is recorded. The signal is time-stationary and can be stacked over multiple cycles to improve accuracy. In this case, both permeability and storativity ( $\beta$ ) of the sample can be determined. There is a limited range in the frequency of the pressure oscillation and the volume of the downstream chamber over which accurate measurements can be made. In general, the downstream volume has to be larger than the pore volume in the test sample if storativity needs to be measured, but not so large as to affect adversely the sensitivity of the downstream pressure measurements. Then, the period of the input signal that will produce a

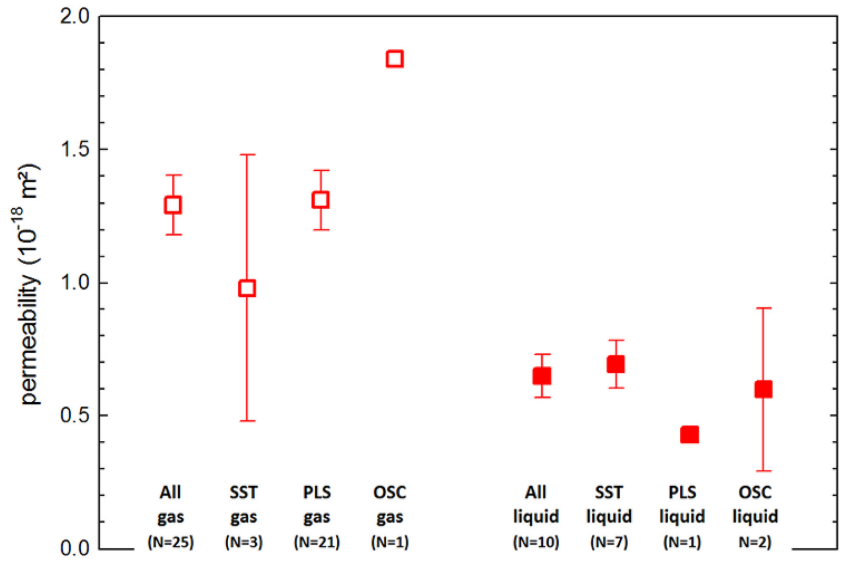
usable response will fall within a limited range that depends on the sample permeability. Measurement of lower permeability generally requires increased period of the sinusoid. If there is time-dependent relaxation of the sample, pressure on the downstream side will show a steady drift that often can be separated from the oscillating signal of known period. In the non-linear inversion procedure for analyzing the amplitude/phase data,  $k$  is not determined uniquely. Rather, the ratio  $k/\beta$  is determined and errors in  $k$  and  $\beta$  are correlated. Increasing the downstream reservoir solves this problem: permeability can then be estimated accurately but not storativity.

All reported determinations of permeability for the KG<sup>2</sup>B core, measured at  $P_{eff} = 5$  MPa in the axial direction, are plotted in Fig. 18 along with standard deviation. Many uncertainties for individual measurements are smaller than the symbol size in the figure. Fig. 5 shows that there is no indication that  $k$  varies systematically with distance from the tunnel (the same holds for porosity  $\phi$  also, see companion paper). Pulse decay measurements are most abundant and tend to be higher than steady-state measurements. The two values that deviate the most from the mean value (both higher and lower) were steady-state measurements. Since measurements were carried out in different laboratories, using different samples and different techniques, the outlier values are probably due to sample variability or test procedures. In the samples there is obvious foliation, anisotropy and sample variability on a scale comparable to the individual sample dimensions. A number of laboratories reported porosities of test samples spanning more than one order of magnitude (see companion paper) implying that much of the variability in permeability is the result of heterogeneity in the test samples.

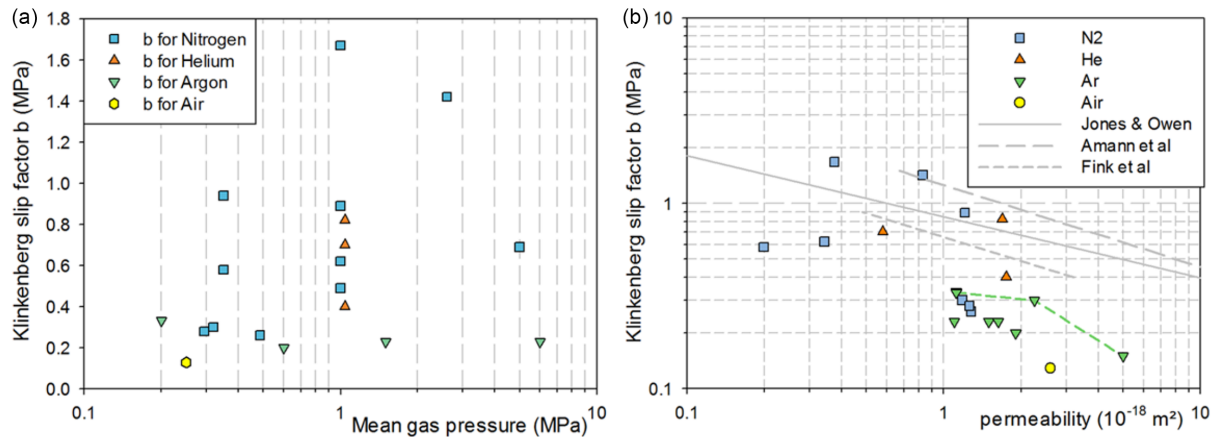
Figs 3 and 4 show separate analyses of permeability determinations based on gas and liquid (primarily water) pore fluids. Average permeability determined using gas is about twice the average permeability based on water measurements. This is consistent with Fig. 17, where mean values and standard errors are plotted for different types of tests and different fluids. Permeability determinations are grouped by technique and working fluid. Some results plotted in Fig. 17 are not statistically significant since three of the subcategories only contain one or two measurements.

Still, interesting trends can be seen. The left-most data point is the average permeability of all of the reported gas measurements ( $k = 1.29 \times 10^{-18} \text{ m}^2$ ). Average values for the three techniques using gas are adjacent. On the right-hand side of the plot, the average permeability for all liquid measurements is plotted ( $k = 0.649 \times 10^{-18}$





**Figure 17.** Summary of all the permeability results in the axial direction at 5 MPa effective pressure per fluid and method. The averaged measurements with gas are systematically larger than those with liquids.



**Figure 18.** (a) Klinkenberg slip factor  $b$  versus mean pore pressure for gas permeability measurements with Klinkenberg correction. (b) Klinkenberg slip factor  $b$  versus permeability, grey lines are published data on gas sands (Jones & Owens 1980), tight gas sandstones (Amann-Hildenbrand *et al.* 2016) and shale (Fink *et al.* 2017).

m<sup>2</sup>). Here the steady-state outlier values that were identified previously have been omitted. The correlation between permeability outliers and porosity values suggests that these samples were anomalous. When the permeability values are separated into six subgroups, there is no clear difference based on technique (steady-state, pulse decay or oscillating flow). However, a significant difference does exist in which gas permeability is about twice the permeability measured with liquid.

The choice of liquid or gas pore fluid can be problematic. For low permeability rocks and fault gouge, measurements can be completed much faster using gas, which has a relatively low viscosity. For some exceedingly tight samples, it may not be possible to obtain a usable flow rate with water as a pore fluid. At the same time, many samples have grain contacts and pore-filling minerals that are chemically reactive with water or brine. In this case, the choice of pore fluid becomes critical. Porosity filled with an inert gas may not have the same structure or pressure sensitivity as porosity filled with naturally occurring brine, or with water with which it is in chemical dis-equilibrium. This can cause water permeability to be up to 1–2 orders of magnitude lower than gas permeability. The reason for this

phenomenon is not clear and various hypotheses are discussed in the literature, including core damage by clay plugging, clay swelling, structured water films on the mineral surfaces resulting in reduction of the effective transport volume, and electro-osmotic counter pressures (Gray & Rex 1966; Faulkner & Rutter 2000; Weber & Stanjek 2012; Heap *et al.* 2018). These issues may not be so important in crystalline rocks, but can be of major concern when measuring shales or clay-rich fault gouge.

Many of the permeability measurements had reported uncertainties of 1–2 per cent. This appears to be a practical lower limit to the accuracy that can be obtained by any of the three techniques used. When all reported measurements are included and estimates are based on  $\log(k)$ , the standard error in estimating permeability is about 20 per cent. The largest potential gain in reducing uncertainty appears to be related to the systematic difference between liquid and gas measurements. If this two-fold difference can be explained, the standard error might drop below 8 per cent.

Two other important issues have been highlighted by the benchmarking exercise: the effect of sample size and the pressure sensitivity of permeability. Results were obtained on a large range of

volumes, from 1 to 500 cm<sup>3</sup>. Whereas the results for the largest samples were consistent, the permeability values for the smallest ones were scattered (Fig. 6a) which may indicate that the volume of the smaller samples is below the REV. In this regard the choice of the Grimsel granodiorite, selected for its availability, convenience and relevance to geothermal energy studies, probably was not optimal. Foliation and mineralogical heterogeneity (Fig. 6b) require to work on samples larger than the largest heterogeneity. Unfortunately this was not systematically the case. Despite the size effect, consistent results were found regarding pressure dependence, and showed that the Grimsel granodiorite is strongly pressure sensitive. The choice of a common effective confining pressure was a key for the success of the benchmarking exercise.

## 5.2 Offset between average gas and liquid permeability

Most of the permeability measurements were done using gas as the pore fluid (Fig. 1), so it is important to assess the corrections for gas slippage. Intrinsic (or absolute) permeability is expected to be: (i) determined only by the porous media structure and (ii) independent of the (homogeneous) working fluid passing through it. Nevertheless differences between water and gas permeability have been reported in literature for decades, and for several lithotypes (Muskat & Wyckoff 1937) including shales/mudrocks, tight sandstones and carbonates (e.g. Busch & Amann-Hildenbrand 2013; Ghanizadeh et al. 2013; Amann-Hildenbrand et al. 2016). Klinkenberg (1941) introduced a theory regarding slip flow and its microscale effect: the slippage of gas molecules along capillary walls resulting in a non-zero wall velocity. He introduced a gas slippage parameter (or Klinkenberg slip factor)  $b$  relating the apparent gas permeability  $k_{app}$  to the mean (absolute) gas pressure  $P_{MEAN}$ :

$$k_{app} = k_{\infty} \left( 1 + \frac{b}{P_{MEAN}} \right) \quad (18)$$

where  $k_{\infty}$  is the permeability at infinite gas pressure (equivalent to the permeability  $k$  measured using a liquid). The slip of gas near a solid wall was first studied by Maxwell (1866) and Klinkenberg's concept of slippage was developed for gas flow within a bundle of constant radius capillaries. Hence, this theory may only be applicable within certain boundary conditions. Its validity for flow in tortuous pore systems including bulges and bottlenecks or in crack-like porosity remains questionable.

Our study clearly shows differences depending on the fluid used. Gas permeability values appear to be about twice the permeability values obtained using liquids (Fig. 4). This discrepancy is observed even after the Klinkenberg correction for gas slippage effects. Moreover the type of gas used is expected to have an effect as well. Gas permeability (both apparent and Klinkenberg corrected) has been observed to decrease in the order He > N<sub>2</sub> > CH<sub>4</sub> > CO<sub>2</sub>, (e.g. Han et al. 2010). In organic rich material (coals, shales) this phenomenon is linked to sorption and swelling effects—in such cases a clear dependence upon total organic carbon can be identified. In the absence of sorption the fluid dynamic characteristics of the different gases have to be accounted for. Differences in molecule size and mean free path length result in different slip flow characteristics and, for larger gas molecules, in size exclusion.

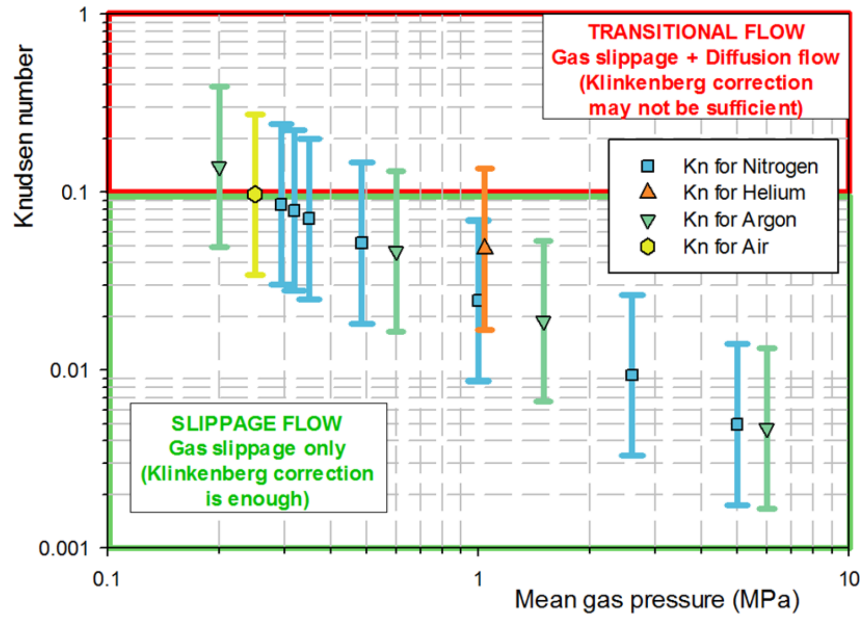
The Klinkenberg slip factor values for each of the gas permeability experiments are plotted versus the mean gas pressure in Fig. 18(a). Significant differences are observed between Helium, Argon, Nitrogen and air. The lowest slip factors  $b$  are found for air and Argon, followed by Helium. For Nitrogen, slip factor values

span one order of magnitude, from 0.12 to 1.7 MPa, without noticeable dependence on mean pressure. Although several parameters can disturb the determination of slip factor  $b$  (accuracy of mean pressure value, lack of back pressure, inertia effects, effective pressure effects), it is surprising that such a large range of values was found for Nitrogen. Slip factor estimation is very sensitive to experimental procedures and several measurements along large mean pressure values are needed to ensure a robust regression in order to limit hazardous extrapolation for infinite mean pore pressure (McPhee & Arthur 1991). In Fig. 18(b) the  $b$  values are plotted versus permeability. A weak linear trend is observed, in agreement with published results from tight sands, sandstones and shales (Jones & Owens 1980; Amann-Hildenbrand et al. 2016; Fink et al. 2017). The three Argon data points are linked with a dashed line: these are measurements on a single sample at different confining pressures, showing a decreasing trend for  $b$  versus permeability similar to published data on sedimentary rocks.

Flow in porous media is generally modeled under the assumption that the fluid is slow, continuous and viscous, with negligible flow of molecules adjacent to the pore wall (Darcy flow conditions). As mentioned above, the use of the Klinkenberg slip factor  $b$  is related to the hypothesis of a slippage flow regime at the microscale along capillary walls. The presence of high-surface-area minerals in the Grimsel granodiorite, such as biotite and chlorite, and their micropore structures, enhances diffusion, adsorption, and reactivity to gases and liquids. Specifically, if the gas or liquid exhibits chemical affinity with the biotite/chlorite minerals, then adsorption onto clay platelets, swelling and particle mobilization may occur. When gas pressure is low, the mean free path  $\lambda$  of the gas molecules (i.e. the average distance travelled without molecular collisions, depending on the temperature, the reciprocal mean pore pressure and the nature of the gas (McPhee & Arthur 1991) will exceed the size of pores/cracks. In such conditions, molecule/molecule collisions become so rare that the concept of viscosity becomes irrelevant, rendering the concept of continuum and bulk flow inapplicable. Knudsen number is classically used to quantify the validity or failure of the Navier-Stokes flow regime, defined as  $K_n = \lambda/H$  where  $\lambda$  is the mean free path and  $H$  a characteristic hydrodynamic length scale (Hadjiconstantinou 2006). For sake of simplicity, we take for  $H$  the crack aperture. When  $K_n$  is high, wall friction is reduced which can be interpreted as a decrease in viscosity leading to an apparent increase of permeability (Carrigy et al. 2012; Allan & Mavko 2013). Depending on the magnitude of  $K_n$ , several flow regimes can be identified (Schaaf & Chambre 1961; Wang et al. 2016). For example, when  $0.01 < K_n < 0.1$  the flow is in the slippage flow regime and the Klinkenberg correction is applicable, but for  $0.1 < K_n < 10$  the flow is in the transitional regime and the Klinkenberg correction may not be sufficient. In the latter case additional corrections need to be done to account for Knudsen diffusion flow. Following (Wang et al. 2016), the mean free path  $\lambda$  can be derived from a hard-sphere gas model and the Knudsen numbers are estimated using the following relation:

$$K_n = \frac{RT}{\pi \sqrt{2} (D_m)^2 r N_A P_{MEAN}} \quad (19)$$

where  $N_A$  is Avogadro's number, and  $D_m$  the gas molecule diameter. For the length scale  $H$  we take the average crack aperture obtained from microstructural analyses on the Grimsel granodiorite ( $H = 283$  nm, see companion paper) and we allow this parameter to vary in the range 100–800 nm (see Fig. 4A in the companion paper). Knudsen numbers are plotted versus the mean pore pressure in Fig. 19 for all the gas permeability measurements.



**Figure 19.** Knudsen numbers  $K_n$  versus mean gas pressure for all the gas permeability experiments. The ‘error bars’ correspond to a range of crack aperture from 100 to 800 nm, the symbols correspond to the average crack aperture (283 nm).

All the data points are located in the slippage flow region or close to the  $K_n = 0.1$  boundary. This suggests that the slippage flow has been correctly accounted for by the Klinkenberg correction. However complexity can arise from the pore size heterogeneity: in some pores the local Knudsen number may be very low while in others it may be high. Another assumption is that gases follow the ideal gas law, which might not always be true (e.g. in the event of water vapor contamination).

When gas transport in microporous rocks is dominated by gas diffusion through pores/cracks, the amount of gas adsorbed changes dynamically as pore pressure changes and is closely related to the properties of the adsorbate (viscosity and density) and solid adsorbent as well as the pore-space geometry (Cui *et al.* 2009; Silin & Kneafsey 2012). In particular, since molecular collisions are controlled by the molecular kinetic energy, diffusion is controlled by pressure and temperature. Allan & Mavko (2013) show that a tortuous pore network with a static adsorbed layer experiences variable Knudsen diffusion as a function of pore pressure. Below a critical pore pressure, the effective permeability is significantly greater than the continuum prediction due to rarefaction of the gas and the onset of Knudsen diffusion. Above the critical pressure, the effect of Knudsen diffusion relative to adsorption is significantly reduced, resulting in effective permeability values up to 40 per cent lower than the continuum prediction. It must also be noted that errors arise not only from measured values but also from computed ones.

Previous studies suggested that permeability tests should be performed using distilled water, because such water is expected to be inert. In fact, distilled water may cause sample leaching leading to the expansion of adsorbed cations around clay particles and reducing hydraulic conductivity. Leaching can also mobilize particles due to either the expansion of diffuse double layers or the removal of cement (Wilkinson 1969). This movement of particles results in ‘dynamic permeability reduction’ (Todd *et al.* 1978) caused by particle trapping at sub-critical pore throats. This dynamic permeability reduction can be regarded as non-reversible in the absence

of dynamic stresses. Alternatives to distilled water include non-polar solvents, direct use of field-collected water and duplication of the original pore water as permeant. Another common source of measurement error in very tight formations is entrapped gas, or air dissolved in the permeant while injecting it into the sample at high pressure. As pressure in the flowing water decreases, air can exsolve, causing pore clogging and erroneous measurements. Loosveldt *et al.* (2002) showed that water permeability was systematically lower than gas permeability, whereas ethanol permeability was intermediate. However, when gas permeability was corrected for the Klinkenberg effect, ethanol and gas permeabilities were found to be of the same order. In presence of chemical activity induced by polar fluids, Loosveldt *et al.* (2002) suggest that the Klinkenberg effect is only a small contributor to observed differences between gas and water permeability: other processes such as rehydration, dissolution/precipitation, migration of fine elements, and water adsorption in the smallest pores of the matrix may be more important.

Finally, it may also be possible that liquids and gases do not probe the porous media in the same way: in such a situation, a common value of permeability is not expected at all between permeability measured with gases and liquids. Heap *et al.* (2018) showed that in volcanic rocks the gas permeability can be a factor two to five higher than water permeability; they speculate that water adsorption on the surfaces of thin microcracks reduces their effective thickness and prevent water flow, leading to water permeability reduction. Our data set suggests that in this case gases probe a more efficient pore network in terms of fluid transport than do liquids. Further studies are needed to support this viewpoint.

### 5.3 Handling of outliers and source of errors in low permeability measurements

Consistent results and convincing trends were obtained in our collaborative benchmarking exercise. Nevertheless few outliers had to be discarded from the analysis. These outliers in permeability values were assumed to result from the rock heterogeneity. Indeed the

Grimsel granodiorite cannot be considered as a homogeneous material; the choice of this material was dictated by the opportunity to work on a rock retrieved from an underground research laboratory, on meter long cores freshly drilled at a single spot *in situ*. The scientific value of the benchmarking exercise was therefore assessed by our Swiss colleagues. A lot of thinking was done before the decision was made to work on that rock, considering especially criteria of homogeneity and reproducibility. Other options had all strong and weak points. So at the end the benchmark had to deal with a rock with visible heterogeneity. We believe that the measurements off the trend that we call outliers are mostly due to heterogeneity, not to wrong measurements. However, it should also be mentioned that the number of outliers is rather small, and the conclusions derived from our data set, although not as decisive as expected, are considered to be sound.

We discuss here the most common experimental problems and mechanisms for sources of error in permeability measurements from tight formations. The first source of error is methodological and procedural diversity that, to a large extent, controls the degree of variability in the results. The pressure pulse decay method is often the standard technique for low permeability material, as the conventional steady state method may not work if flow rate and/or differential pressure are too low to measure accurately. McPhee & Arthur (1991) showed that the effect of pressure transducer error ( $\pm 0.69$  kPa) on the derived slip factor becomes more pronounced (approximately 73 per cent) when measurements are performed under constant flow rate mode (rather than constant differential pressure). When utilizing the pressure pulse decay method, extreme care must be taken to ensure constant temperature over the experiment so that the measured pressure changes are associated only with flow through the pore space. In addition, it may be difficult to reconcile gas or liquid permeabilities measured by laboratories that use different sleeve specifications and/or confining pressure. The extent to which the radial pressure on the sleeve is effectively transferred to the specimen is a function of sleeve hardness and thickness. If measurements refer to ambient conditions, sleeve confining pressure should be sufficiently high (1.5–5.5 MPa) for the sleeve to laterally seal the sample by filling its surface irregularities, thus avoiding fluid bypass, and sufficiently low to avoid permeability reduction due to pore volume compaction. This issue may become particularly relevant in the presence of schistose microstructure and large amounts of soft (compressible) minerals. When comparing data from different laboratories, it is important to decide *a priori* whether to emphasize the data from ‘virgin’ (unseasoned) samples during their first loading or limit the investigation to elastic regimes by pre-stressing the specimen.

The second source of error is associated with tight rock microstructure and solid–fluid interactions. The samples under investigation show visible foliation that relates to compositional banding (segregation of mineral phases). This mineralogical differentiation forms alternating layers of biotite and quartz (Schild *et al.* 2001), white mica and chlorite (Goncalves *et al.* 2012), and small amounts of chlorite/smectite (vermiculite), the latter resulting from alteration of biotite layers (Kralik *et al.* 1992). The analyses conducted in this study show that a significant part of the pore space resides within the biotite phase as a network of submicron cracks exhibiting an average fracture aperture of 283 nm (see companion paper). Both mineralogical and microstructural features lead to processes that change the macroscale permeability measured in the laboratory and its sensitivity to pressure.

#### 5.4 Good practice for low permeability measurements

Experimental studies aim to determine of the ‘true’ or ‘*in situ*’ permeability value and increase understanding of contributing processes. However, the measured permeability depends on various parameters and their interdependencies. In the context of this study, reported permeability coefficients varied by approximately 1–2 orders of magnitude. Systematic and random errors are considered irrelevant here, as the experiments were performed at controlled temperature and pressure conditions, and any erratic fluctuations were accounted for in data analysis. The most important factors influencing the experimental results for single-phase flow were (a) effective stress history and loading time, including stress-release effects due to coring, (b) the pore fluid (gas, water) used in the experiments and (c) sample heterogeneity. The latter category includes intrinsic lithological/textural features but also those induced by plug preparation, transportation and the drying/saturation procedure. The impact of each factor will differ among rock types, especially where swelling processes in clays can modify the pore space, in which case the choice of measuring fluid becomes a critical issue. In order to account for these different effects, the design and protocol of the experimental procedure, and data management must be discussed beforehand. In this benchmark study, laboratories were asked to submit their results in a standard form (see fig. 3 in David *et al.* 2017), that contained all information required for thorough knowledge of the permeability estimation process (method, fluid, pressure and temperature conditions). However, in many cases it was extremely important to receive additional information including:

- (1) Time information (absolute, relative) to identify whether the system had reached equilibrium with the applied pressure and temperature conditions and to investigate the effect of pressure cycling. The time required for pressure equilibration in low permeability material can be up to a month.
- (2) In the case of gas permeability tests, additional data at all pressure steps should be provided: (i) apparent permeability and slip factor, (ii) mean pore pressure, (iii) pressure difference, (iv) absolute pressure and (v) temperature and equation of state for the gas. We recommend against averaging values obtained with different gases.
- (3) Pressure history: the target effective pressure for a benchmarking exercise must never be exceeded during the loading stage prior to permeability measurement.

Based on this additional information, detailed study of transport processes becomes possible and any deviation from the expected behavior can be analyzed.

## 6 CONCLUSION

A benchmarking measurement exercise for low permeability material involving 24 laboratories allows us to discuss the influence of (i) pore-fluid, (ii) measurement method, (iii) sample size, (iv) pressure sensitivity and (v) gas slippage effects on the permeability of the selected rock, the Grimsel granodiorite. A complementary data set on (vi) microstructures and pore size distributions, (vii) porosity and (viii) permeability modeling is presented in a companion paper. In measurements at 5 MPa effective confining pressure, an average permeability of  $1.47 \times 10^{-18}$  m<sup>2</sup> was found, with a high standard deviation of  $1.55 \times 10^{-18}$  m<sup>2</sup> which can be explained by the presence of few outliers (4 of 39 values). Discarding those outliers yields an average permeability of  $1.11 \times 10^{-18}$  m<sup>2</sup> with a smaller



standard deviation ( $0.57 \times 10^{-18} \text{ m}^2$ ). The most striking result was the large difference in average permeability between gas and liquid measurements: independently of the method used, gas permeability is higher than liquid permeability by approximately a factor 2 ( $k_{\text{gas}} = 1.28 \times 10^{-18} \text{ m}^2$  compared to  $k_{\text{liquid}} = 0.65 \times 10^{-18} \text{ m}^2$ ). Possible explanations include (i) liquid permeability underestimated due to fluid-rock interactions (ii) gas permeability overestimated due to insufficient correction for gas slippage effects and/or (iii) gases and liquids do not probe exactly the same pore networks, and so there is no reason to expect a single permeability value. No decisive clue was found to favor one or the other explanation. However, the estimation of Knudsen numbers shows that all measurements using gas fell in the gas slippage regime and that no additional corrections are required to account for other gas flow. The larger scatter of permeability values for smaller samples seems to indicate that those samples have a volume below the REV, due to centimeter-sized mineralogical heterogeneities in the Grimsel granodiorite. Nevertheless our results are mostly self-consistent (except for few outliers) and in good agreement with other studies (Schild *et al.* 2001), especially the pressure dependence of permeability in the range 1–30 MPa. The permeability decrease with effective pressure can be described reasonably well with an exponential law,  $k = k_o \cdot \exp(-\gamma P_{\text{eff}})$  with  $\gamma = 0.093 \text{ MPa}^{-1}$ . Three examples of measurements are described in detail, using (i) the steady-state flow method, (ii) the transient pulse method and (iii) the pore pressure oscillation method: these experiments clearly show that many parameters need to be carefully controlled for successful permeability measurements in low permeability rocks. Another outcome of the benchmarking exercise was a set of good practice rules for measuring permeability in tight materials. A second round of benchmarking is currently under way with another tight material, the Cobourg Limestone. Additional challenges are expected in this benchmark (called KCL), as this rock has a permeability in the  $10^{-21} \text{ m}^2$  range. With the experience gained with KG<sup>2</sup>B, the team is keen to take up this new challenge.

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## APPENDIX A: THE COMPLETE LIST OF CO-AUTHORS

<sup>(3)</sup>**The KG<sup>2</sup>B Team:** the benchmark involved 24 rock physics laboratories around the world. In Fig. [A1](#) the logo of each participating institution is shown on a world map, with the benchmark logo and

the collection of core samples sent to the participants. The name, e-mail addresses and institution of each participant and co-author are given in Table [A1](#).

## APPENDIX B: SAMPLES, METHODS AND DATA SET

Each participating laboratory was assigned a number following the core sample order, from #01 for the sample closest to the tunnel (at 4.17 m) to #24 for the deepest sample in the borehole (at 5.95 m). Table [B1](#) provides sample location in the tunnel, the length and diameter of the sub-core drilled from the original core, and the method and pore fluid used for permeability measurements. Table [B2](#) provides the permeability values measured at 5 MPa and (when available) at in situ stress 30 MPa. Note that porosity and radial permeability values have also been included in the table, although they are discussed in the companion paper.



**Figure A1.** World map with the participants' logos, the benchmark logo and the core sample collection sent to the participants.

**Table A1.** The KG<sup>2</sup>B Team: list of participants and co-authors.

Participants (alphabetic order)	E-mail	Institution
Alexandra AMANN HILDENBRAND/Bernhard KROOSS/Reinhard FINK	alexandra.amann@emr.rwth-aachen.de	EMR group, Aachen University, Germany
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**Table B1.** List of samples with distance to the borehole mouth, length and diameter, and methods used for permeability estimation with corresponding fluids.

	Distance from tunnel (m)	Subcored sample length (mm)	Subcored sample diameter (mm)	Method for permeability estimation	Fluid used for permeability measurement
Lab#01	4.17	25.6	25	Transient pulse & Step-decay (transient)	GAS (Argon)
	4.17	27.2	25		
	4.17	29.5	25		
Lab#02	4.25	83	40	Steady-state flow	LIQUID (water)
Lab#03	4.35	94	83 (no subcoring)	Steady-state flow	LIQUID (non degassed water)
Lab#04	4.45	80	40	Transient pulse, Pore pressure oscillation & Modeling	LIQUID (brine)
Lab#05	4.63	25	38	Transient pulse & Modeling	GAS (Nitrogen)
Lab#06	4.78	86	hollow cylinder 83/60	Steady-state flow (radial flow)	LIQUID (distilled water)
Lab#07	4.94	1 to 5	chips	Transient pulse	GAS (Air)
Lab#08	4.99	21.4	19.5	Steady-state flow	GAS (Nitrogen)
		20.8	19.5		
Lab#09	5.04	50	40	Transient pulse	GAS (Nitrogen)
				Steady-state flow	LIQUID (deaerated tap water)
				Transient pulse	GAS (Argon)
Lab#10	5.11	31.5	29.9	Steady-state flow	LIQUID (water)
	5.11	28.3	30		
	5.11	28.8	30		
Lab#11	5.18	39.3	25.5	Step-decay (transient)	GAS (Nitrogen)
Lab#12	5.31	40	20	Transient pulse	GAS (Argon)
Lab#13	5.37	38	38	Steady-state flow	LIQUID (deionised water)
	5.37	20	20	Steady-state flow	
	5.37			Pore pressure oscillation	
Lab#14	5.42	41.3	64.6	Steady-state flow	GAS (Argon)
Lab#15	5.47	15	15 (cube)	Microstructure analysis (MICP) & Modeling	NA
Lab#16	5.52	44	38		
	5.52	42	38		
Lab#17	5.57	21.5	25.4	Transient pulse	GAS (Argon)
Lab#18	5.67	30	26	Pore pressure oscillation & Transient pulse	GAS (Argon)
	5.67	30	26		
	5.67	30	26		
Lab#19	5.72	33.6	83.3 (no subcoring)	Steady-state flow	LIQUID (deionized water)
Lab#20	5.77	49.9	25.4	Transient pulse	GAS (Helium and Nitrogen)
	5.77	49.3	25.3		
	5.77	35.6	25.4		
Lab#21	5.83	38.9	39	Steady-state flow	GAS (Nitrogen)
Lab#22	5.9	39	25.4	Transient pulse	GAS (Argon)
		38	25.4		
		38.9	25.4		
Lab#23	5.95	24.2	38.3	Steady-state flow	LIQUID (degassed tap water)
				Steady-state flow & Transient pulse	GAS (Helium and Nitrogen)
Lab#24	5.95	Thin section	thin section	Microstructure analysis (BIB-SEM) & Modeling	NA

**Table B2.** Permeability and porosity values.

LAB#	Fluid	Method	Porosity (%)	Axial PERM@5_MPa (10 <sup>-18</sup> m <sup>2</sup> )	Axial PERM@30_MPa (10 <sup>-18</sup> m <sup>2</sup> )	Radial PERM@5_MPa (10 <sup>-18</sup> m <sup>2</sup> )
#01	Gas	PLS		1.1		
	Gas	PLS		1.5		
	Gas	PLS		1.63		
#02	Liquid	SST		0.43	0.03	
#03	Liquid	SST	0.6	0.6	0.04	
#04	Liquid	PLS	0.62	0.43	0.055 (*)	
#04	Liquid	OSC	0.62	0.294		
#05	Gas	PLS	0.6	1.46	0.064 (*)	
#06		SST				0.84 @1.75MPa
#07	Gas	PLS	0.7	2.6 (*)		
#08	Gas	SST				0.243
	Gas	SST		0.199		
	Gas	PLS	0.8	1.3		
#09	Liquid	SST	0.8	0.94		
	Gas	PLS	0.8	1.49		
	Gas	PLS	0.8	1.37		
	Gas	PLS	0.8	1.3		
#10	Liquid	SST	0.46	0.5		
	Liquid	SST	0.17	0.05 (**)		
	Liquid	SST	0.51	0.73		
#11	Gas	PLS	1.16	1.28		
	Gas	PLS	0.78	1.18		
	Gas	PLS	1.18	1.26		
#12	Gas	PLS	0.52	1.12		
#13	Liquid	SST		8.35 (**)	2.06 (**)	
	Liquid	SST		4.73 (**)		
	Liquid	SST		0.579		
	Liquid	OSC		0.906	0.277	
#14	Gas	SST	0.73	1.91	0.189	
#16	Gas	PLS	0.23	1.69		
	Gas	PLS	0.43	1.81	0.155	
#17		PLS	1.8			0.66
#18	Gas	OSC	1.03	1.84		
	Gas	OSC	1.03			0.843
	Gas	OSC	1.03			0.501
#19	Liquid	SST		1.08		
#20	Gas	PLS	0.51	0.579		
	Gas	PLS	0.51	0.342		
	Gas	PLS	0.88	1.69		
	Gas	PLS	0.88	0.375		
	Gas	PLS	1.29	1.75		
	Gas	PLS	1.29	1.21		
#21	Gas	SST	1.5	0.83	0.07 (*)	
#22	Gas	PLS	0.7	0.795		
	Gas	PLS	0.5			0.825
#23	Liquid	SST	0.26	5.4 (**)		

(\*) Extrapolated values; (\*\*) outliers discarded from the global analysis (SST, steady-state flow method; PLS, transient pulse method; OSC, oscillating pore pressure method).