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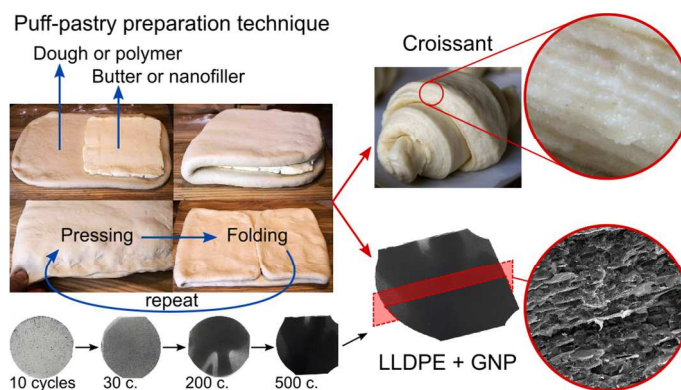
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Abstract



The intrinsic properties of nanomaterials promise technological revolutions in many fields including transportation, soft robotics, and energy. Unfortunately, the exploitation of such properties in polymer nanocomposites is extremely challenging due to the lack of viable dispersion routes when the filler content is high. We usually face a dichotomy between degree of nanofiller loading and degree of dispersion (and thus performance), as dispersion quality decreases with loading. Here, we demonstrate

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3 a potentially scalable pressing-and-folding method (P&F), inspired by the art of croissant-making, to
4 efficiently disperse ultra-high loadings of nanofillers in polymer matrices. A desired nanofiller dispersion
5 can be achieved simply by selecting a sufficient number of P&F cycles. Because of the fine
6 microstructural control enabled by P&F, mechanical reinforcements close to the theoretical maximum
7 and independent of nanofiller loading (up to 74 vol. %) were obtained. We propose a universal model
8 for the P&F dispersion process, parameterised on an experimentally-quantifiable “D factor”. The model
9 represents a general guideline for the optimisation of nanocomposites with enhanced functionalities
10 including sensing, heat management, and energy storage.
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25 **KEYWORDS:** polymer nanocomposites; nanoparticle dispersion; graphene; nanoclay; predictive model;
26 multifunctional materials.
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33 Facing technological challenges in fields like transportation, soft robotics, biomedical, and wearable
34 electronics will require the availability of materials able to simultaneously bear loads and integrate
35 multi-functionalities like sensing, adaptation, responsiveness, energy harvesting and communication.¹
36 Polymer nanocomposites are promising candidates to meet these requests, as they employ
37 nanoparticles having exceptional intrinsic properties. Graphene,² for instance, has been proven to
38 possess exceptional mechanical properties,³ excellent gas barrier properties,⁴ high charge carrier
39 mobility and high thermal conductivity,^{5,6} and visual transparency.⁷ Yet, it has proven difficult to exploit
40 the intrinsic properties of the embedded nanoparticles: the performance of nanocomposites are often
41 disappointing and well below theoretical predictions. For example, according to classical composite
42 theories,⁸ we would expect graphene nanocomposites to exhibit extraordinary mechanical performance.
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55 However, only a very limited number of papers have reported nanocomposites standing up to these
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3 expectations.⁹⁻¹² Good performance and agreement with the theory is usually observed for very low
4 nanofiller contents only (below 1 vol.%).⁸ But this is the range in which the absolute performance is low,
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6 questioning the use of nanoparticles in place of more conventional alternatives. The issue lies in the
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8 following dilemma: the smaller the material's size, the more appealing its intrinsic properties, but also
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10 the more difficult the control over the nanoparticle dispersion quality during processing.^{13,14}
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15 On the other hand, nanocomposites are readily found in Nature and their intrinsic performance can
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17 surpass that of the best man-made composites. For instance nacre, often taken as the golden standard
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19 in structured composites, combines CaCO₃ "bricks" and protein "mortar" in a layered microstructured
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21 composite ~3000 times tougher than each of nacre's components.¹⁵ The hierarchical structure of nacre
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23 is believed to be the key to its properties. Hence, researchers have attempted to exploit nanoparticle
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25 properties by developing methods to obtain better microstructural control. The best resulting
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27 nanocomposites have demonstrated high mechanical performances,⁹⁻¹² unusual interaction with
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29 light,^{16,17} resistance to flammability,¹⁸⁻²² self-regulating heating,^{23,24} energy management,²⁵⁻²⁷ high
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31 electrical and thermal conductivity,²⁸ sensing and structural health monitoring.²⁹⁻³²
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36 However, the control over nanoparticle dispersion is usually compromised for high filler loading,^{11,12,33-37}
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38 making it impossible to exploit the desired large nanofiller-polymer interfacial area.³⁸ As a consequence,
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40 nanocomposites often contain nanoparticle agglomerates that dramatically reduce performance,^{11,12,33,39}
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42 unless they were prepared by bottom-up, but hardly-scalable, approaches.⁴⁰⁻⁴²
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46 To overcome the dichotomy between nanofiller loading and dispersion (and hence properties), herein
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48 we present an iterative materials processing technique (P&F) that draws inspiration from the process of
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50 preparation of puff pastry to make croissants (Figure 1a). This technique can create nanocomposites
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52 with well-defined nanofiller dispersion levels, without loss of dispersion efficiency even at ultra-high
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54 nanofiller loadings. This is not achievable by traditional solution-mixing or melt-blending techniques.
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3 Moreover, we propose an analytical model that quantitatively correlates nanocomposite properties with
4 nanofiller dispersion level. To prove the potential of the P&F technique, we produce nanocomposites
5 with exceptional combination of functionalities, including energy management, self-heating, and strain
6 sensing.
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11 12 13 Results and Discussion

14 15 16 Micromechanical considerations and modelling of the P&F 17 dispersion process

18 The (P&F) technique is based on the addition of nanoparticles (*i.e.* graphite nanoplatelets, GNP) in
19 between two polymer films (*i.e.* linear-low density polyethylene, LLDPE) (Figure 1b, left), followed by the
20 application of P&F cycles (Figure 1b, right) an arbitrary number of times. Each P&F cycle is composed of
21 a folding step, in which an approximately circular GNP-containing layer is folded twice to produce a
22 quadrant slice, and a pressing step executed at a temperature slightly above the polymer melting point
23 ($\cong 120^{\circ}\text{C}$ for LLDPE). The pressing step produces a strong flow that simultaneously breaks the
24 agglomerates, aligns the dispersed particles and substantially increases the GNP-LLDPE contact area,
25 yielding a well-mixed dispersion after a number of cycles. The P&F process implements Baker's
26 transformation⁴³ (Figure 1a, right) at very high applied viscous stresses.
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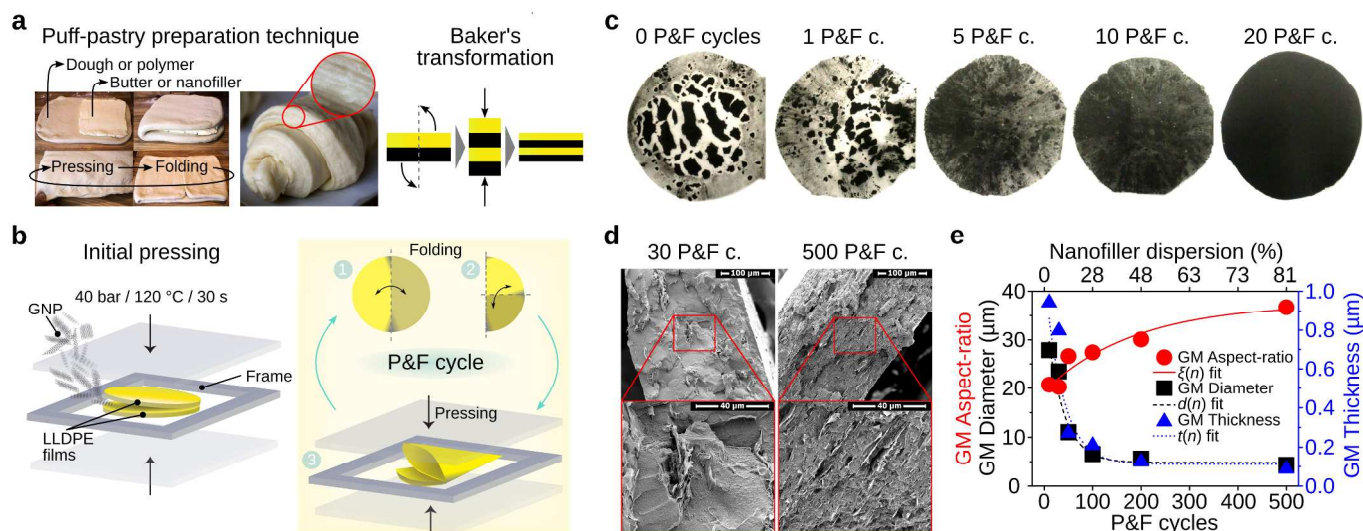


Figure 1. Nanofiller dispersion process. (a) The P&F technique draws inspiration from the puff-pastry preparation technique (left), and its stretching & folding effect can be idealized as a Baker's transformation (right). (b) Schematic of the P&F technique. (c) Top view images of samples of LLDPE + 4.8 vol.% GNP after different P&F cycles (sample diameter ~ 8 cm; sample thickness ~ 300 μm). (d) Cross-sectional SEM images of LLDPE + 4.8 vol.% GNP samples for very different filler dispersion levels: the left image shows thick and well separated GNP agglomerates; the right image shows well dispersed GNPs. (e) Geometric mean (GM) values of diameter, thickness, and aspect-ratio (ratio between diameter and thickness) of GNP agglomerates. The GM values were obtained from analysis of cross-sections of LLDPE + 4.8 vol.% GNP samples for different P&F cycles. The lines are best fits using Equation (4).

As shown in Figure 1c, after a few P&F cycles the colour of the nanocomposites becomes homogeneous to the naked eye (see also Figure S5 in the Supporting Information). At small cycle numbers, the nanocomposites present large GNP agglomerates (Figure 1d, left). The size of the agglomerates decreases with increasing cycles (Figure 1e), and many well-dispersed individual particles appear throughout the samples, forming a layered structure (see further microstructural observations in Supporting Section S.7.1). After 500 P&F cycles, the initial agglomerates have mostly disappeared (Figure 1d, right), and the thickness of the dispersed particles approaches that of individual GNP (~ 30 nm, see Section S.3 for GNP characterizations).

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3 The combined effect of dispersion and orientation obtained by P&F cannot be reached by conventional
4 melt processing like twin-screw melt-compounding, or multilayer co-extrusion⁴⁴ (which is also based on
5 the Baker's transformation). The flow has a dominant extensional component that orients the particles
6 with their flat faces perpendicular to the pressing direction. The squeeze flow in the thin gap between
7 the plates produces large shear rates. Such high shear rates may not be achievable by conventional
8 multilayer co-extrusion because the materials are processed at temperatures much higher than the
9 polymer melting point, otherwise they will hardly flow through the extrusion line. By solving for the
10 velocity profile for a power-law fluid using the lubrication approximation, we estimate the volume-
11 averaged shear rate magnitude during each P&F cycle to be between $\dot{\gamma} = 12 \text{ s}^{-1}$ and $\dot{\gamma} = 1150 \text{ s}^{-1}$ in
12 the final stages of compression, depending on whether the polymer is assumed to slip completely from
13 the wall or to adhere perfectly to it. Given the high viscosity of the polymer (we are working just above
14 the melting temperature), the corresponding viscous stresses are large, between 3 KPa and 90 KPa
15 (assuming 4.8 vol.%, see Section S.11.1 of Supporting Information), and sufficient to break the initial
16 aggregates (from the surface energy of graphene $\Gamma \cong 70 \text{ mN/m}$ and the diameter of the platelets
17 D_p we estimate the yield strength $\sigma_y \propto \frac{\Gamma}{D_p}$ of the initial aggregates to be smaller than 0.74 KPa, see
18 Section S.11.1). The controlled flow in P&F has a further crucial benefit. With conventional processing
19 methods, characterised by complex flow streamlines, the flow can promote re-agglomeration rather
20 than dispersion if converging streamlines are present that force the particles to come into contact with
21 each other. In contrast, in the P&F approach the dominant extensional flow increases the particle
22 separation at each cycle by "stretching" the fluid containing the suspended platelets.

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50 A key aspect of the method is that after the pressing step has ended, the shear rate goes practically to
51 zero. As a consequence the sample viscosity increases dramatically, "freezing" the microstructure (for
52 samples at 120 °C containing 4.8 vol.% GNP the viscosity increases from $\eta \cong 10 \text{ Pa} \cdot \text{s}$ for $\dot{\gamma} \cong 10 \text{ s}^{-1}$ to
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3 $\eta \cong 10^5 \text{ Pa} \cdot \text{s}$ for $\dot{\gamma} \cong 10^{-3} \text{ s}^{-1}$). Moreover, the sample is cooled down and folded at room
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5 temperature. Hence, once dispersed, the platelets remain dispersed until the next pressing step. To
6
7 quantify the dispersion during the P&F process, we can define a dispersion factor D as

$$D \equiv \frac{A(n)}{A_p} \quad \text{Equation (1)}$$

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15 where $A(n)$ and A_p are the nanofiller-matrix contact area at cycle n and the total nanofiller surface area,
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17 respectively. The D -factor ranges from 0 for completely agglomerated GNPs to 1 for perfectly dispersed
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19 GNPs. This parameter can either be measured indirectly (*e.g.* by analysing SEM and TEM images³⁹) or
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21 analytically derived *a priori* from the preparation technique used (see Sections S.11.3 for melt-blending,
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23 and S.11.4 for solution-mixing/casting).

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27 By assuming that the variation of D within a Δn interval depends on a distribution-rate I (a constant that
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29 describes how fast the polymer melt erodes the agglomerates and distributes the nanoparticles) and on
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31 a saturation term $A_p - A(n)$ (once all the GNPs are in contact with LLDPE, D becomes 1 and cannot further
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33 increase, see Section S.11.2), we can estimate that D changes with n according to

$$D(n) = 1 - \frac{(A_p - A_0)}{A_p} e^{-I \cdot n} \quad \text{Equation (2)}$$

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37 where A_0 is the initial contact area. We calculate a pre-exponential factor $(A_p - A_0)/A_p$ of 0.999 by
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39 analysing the optical pictures of the samples at the first few cycles, and a distribution rate $I \approx 3.3 \cdot 10^{-3}$
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41 using two different methods (Sections S.11.5 and S.11.6): one based on the analysis of the optical
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43 pictures of films prepared at low P&F cycles, and the other one by fitting the mechanical and electrical
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45 properties of the nanocomposites presented later. We used Equation (2) to convert the number of P&F
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47 cycles into a nanofiller dispersion level on the top axis of Figure 1e and Figure 2b,c. The knowledge of
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49 the dispersion state allows predicting nanocomposites physical properties.
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Prediction of nanocomposite properties for different dispersion levels

Nanocomposite physical properties can be parameterized on D assuming that the effective nanofiller loading V_p^{eff} scales with the nominal nanofiller loading V_p in the same way as the area does:

$$V_p^{eff}(D) \equiv D \cdot V_p \quad \text{Equation (3)}$$

The effective volume fraction can be used to replace V_p inside theoretical models for composites (such as the Halpin-Tsai model^{45,46} for the elastic modulus or the Pukanszky model⁴⁷ for the yield stress) provided the nanofiller dispersion level is known, or to back-calculate an unknown D factor. Any physical properties P that follows the rule-of-mixture,^{48,49} such as the Young's Modulus or the thermal conductivity, can be expressed (see Section S.11.2) as

$$P(D) \approx P_0 + (P_{th} - P_0) \cdot D$$

Equation (4)

where P_0 is the value of P for $D = 0$, and P_{th} is the value of P when the nanofiller is perfectly dispersed. In contrast, properties that are very sensitive to percolation, such as the electrical conductivity σ , are expected to follow an exponential relation (Section S.11.2):

$$\sigma(D) = \sigma_{th} + (\sigma_M - \sigma_{th}) \cdot e^{-a(D-D_c)^2} \quad \text{Equation (5)}$$

where σ_{th} is the theoretical conductivity at high dispersion levels, σ_M is the maximum conductivity reached at a critical nanofiller dispersion level D_c , and a is a parameter that describes how fast the conductivity changes with inter-particle distance (and thus with the dispersion level). In the next section we will explain this correlation between nanofiller dispersion and electrical conductivity in more detail.

Despite their simplicity, Equations 4, 5, 6 are very useful to both interpret nanocomposites physical properties and to do predictions and materials design.

Effect of GNP dispersion level on nanocomposite properties

Figure 2a shows representative stress-strain curves corresponding to different P&F cycles for samples containing 4.8 vol.% GNP. The mechanical reinforcement E_c/E_m (ratio between elastic modulus E_c of the composite and elastic modulus of the matrix, with $E_m = 140 \pm 5$ MPa), the stress at yield Y , and the stress at break B are improved by nanofiller dispersion (Figure 2b), as expected from previous studies.^{39,50} Since the yield stress depends also on the nanofiller specific surface area,³⁸ its increase compared with neat LLDPE (7.85 ± 0.27 MPa) is likely explained by an increasing nanofiller-matrix interfacial area with P&F cycles. However, nanofiller dispersion may change also the crystallinity and the spherulitic and lamellar features of the polymer, which in turn can further affect the nanocomposite mechanical properties. In Sections S.4 and S.5 we show that these changes are negligible for our samples, so any mechanical improvement must be mainly caused by an increased nanofiller-polymer interface. The stress at break overtakes the value of neat LLDPE (9.5 ± 0.7 MPa) only after 150 P&F cycles; for this number of cycles failure initiation due to stress concentrations generated by GNP agglomerates is overcome (see fracture surfaces in Section S.7.2). For comparison, a reference sample containing 4.8 vol.% GNP prepared by melt-blending followed by compression-moulding presents mechanical properties as low as those of samples prepared between 100 and 150 P&F cycles (Figure 2b and Section S.8). This is believed to be mainly due to the reduced in-plane alignment of the GNP nanoparticles.

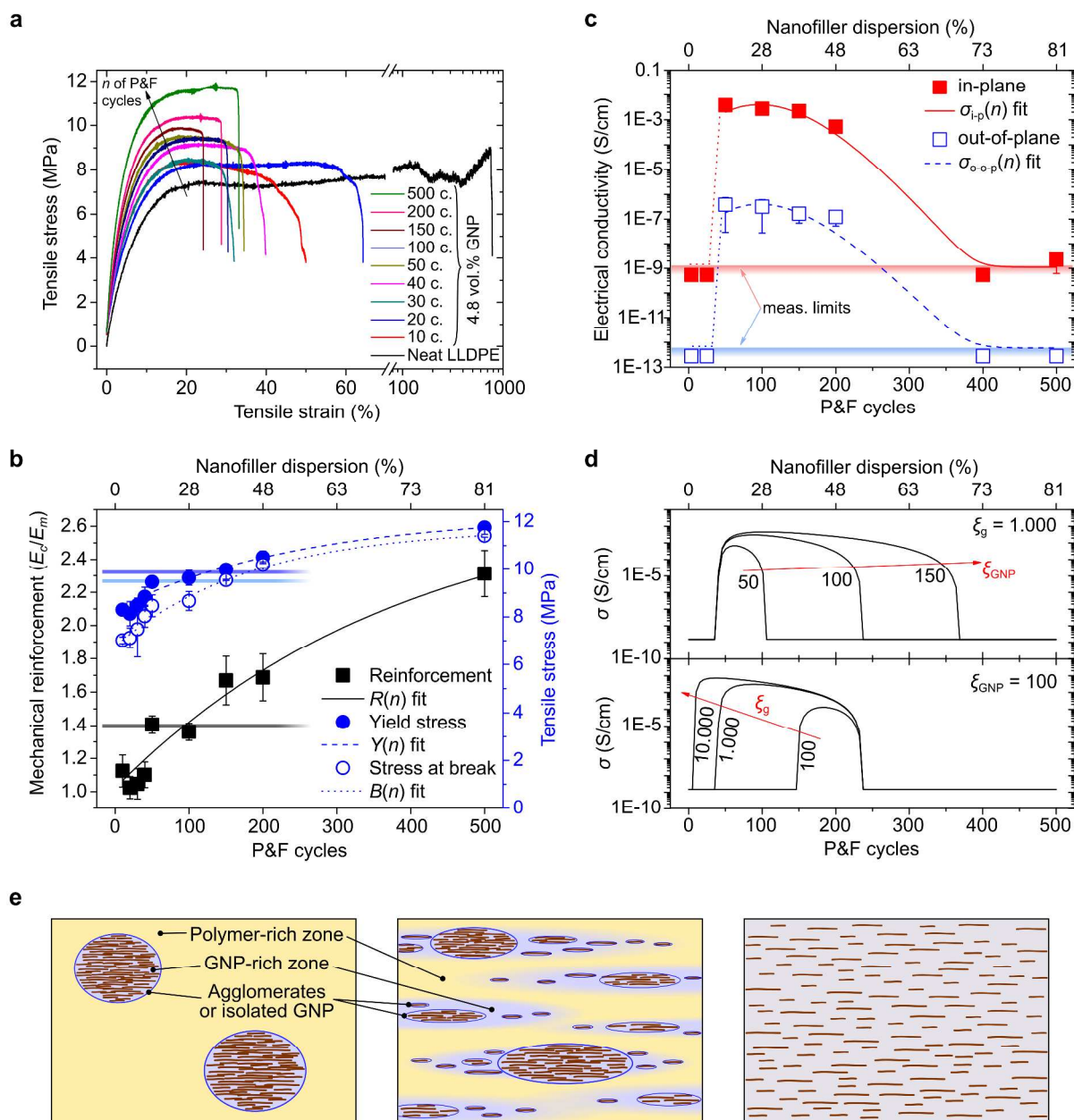


Figure 2. Effect of nanofiller dispersion on mechanical and electrical properties of LLDPE + 4.8 vol.% GNP nanocomposites.

(a) Representative stress-strain curves. (b) Measured mechanical reinforcement R , stress at yield Y , and stress at break B , with best fits using Equation (4). The three horizontal lines represent the yield stress (top line), stress at break and reinforcement (bottom line) of the reference sample prepared by traditional melt blending. (c) Electrical conductivity as a function of P&F cycles n (horizontal shaded areas indicates the lower measurement limits for in-plane and out-of-plane electrical conductivities; dotted lines are guides for the eye) fitted with Equation (5). The measurement limits are due to the apparatus employed that could measure a minimum conductance of $2 \cdot 10^{-11}$ S, multiplied by the geometries of the samples used: $1.5/(0.8 \times 0.03)$ cm^{-1} for in-plane measurements, and $0.03/(1 \times 1)$ cm^{-1} for out-of-plane). (d) Theoretical predictions of nanocomposite electrical conductivities

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3 based on the model of Wang *et al.*⁵¹ for different GNP aspect-ratios (top graph, assuming that ζ_g reaches the value of 1000 after
4 500 cycles) and for GNP-rich zones that reach different aspect-ratios after 500 P&F cycles (bottom graph). (e) Representation of
5 the nanocomposite microstructures with the polymer-rich and GNP-rich zones.
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13 The anisotropic microstructure observed by SEM is reflected in the electrical properties (Figure 2c): the
14 in-plane conductivity is approximately 4 orders of magnitude higher than the out-of-plane conductivity.
15 The in-plane and out-of-plane conductivities of samples prepared with less than 50 P&F cycles are not
16 measurable, suggesting well-isolated GNP agglomerates inside the matrix. Between 50 and 150 P&F
17 cycles the dispersion of the particles leads to an optimally conductive network and the conductivities
18 reach a maximum (this rise in conductivity with the nanofiller dispersion agrees with several literature
19 observations^{39,52,53}). The conductivities then decrease at higher P&F cycles, suggesting a breakup of the
20 percolating network. This other behaviour agrees with the results of Tkalya *et al.*, who reported
21 increased percolation thresholds in nanocomposites with improved graphene dispersions.⁵⁴ The
22 reduction in electrical conductivity can also be explained by a partial fragmentation of GNP. This effect,
23 however, should be less dominant than the nanofiller dispersion/distribution effect, as there is no
24 evidence of a reduction of mechanical properties with P&F cycles. Notably, a reference sample prepared
25 by melt-blending/compression-moulding (also containing 4.8 vol.% GNP) is not electrically conductive.
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43 To better understand the reasons behind the trend of the electrical conductivities with the P&F cycles,
44 we refer to the study of Wang *et al.*, who developed a conductivity model based on the continuum
45 theory that takes into account the effects of nanofiller agglomeration, imperfect nanofiller/matrix
46 interface, and electron tunnelling.⁵¹ Because of the GNP agglomerates, the volume of nanocomposites
47 must be divided into two different zones: a GNP-rich zone and a polymer-rich zone (Figure 2e). The size
48 of the GNP-rich zones may not be the same of those reported in Figure 1e for the GNP agglomerates:
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3 the GNP-rich zones – represented by violet areas in Figure 2e as opposed to the blue contours used to
4 denote the agglomerates and individual GNP that can be measured by SEM – can consists also of well
5 dispersed GNP that are just well close to each other so that their local concentration is higher than V_p .
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7 Assuming that the polymer-rich zone does not contain any GNP, the GNP concentration inside the GNP-
8 rich zones is $V_{GNP} = V_p/V_g$,⁵¹ where V_g is the volume fraction of the GNP-rich zones inside the
9 nanocomposites. The value of V_g must increase from V_p at the first few P&F cycles to 1 at very high
10 cycles, where there is no more distinction between GNP-rich and polymer-rich zones (Figure 2e).
11
12 Unfortunately, there is no a direct way to measure the size of the GNP-rich zones. However, considering
13 that the P&F dispersion mechanism involves repetitive extensional flows, it is reasonable to expect that
14 the GNP-rich zones increase their aspect-ratio ξ_g with the number of P&F cycles. Based on the model of
15 Wang *et al.*,⁵¹ when ξ_g is higher than the aspect-ratio ξ_{GNP} of the individual GNP, the overall electrical
16 percolation decreases and the conductivity of the nanocomposites increases. Indeed, approximating
17 their model, the nanocomposite conductivity σ is controlled by the electrical percolation between the
18 GNP-rich zones:
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$$\sigma \cong \sigma_g (V_g - V_g^c)^2$$

Equation (6)

42 where V_g^c is the critical volume fraction of the GNP-rich zones, and σ_g is their conductivity, which is
43 based in turn on the percolation of the GNP within the GNP-rich zones:
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$$\sigma_g \cong \sigma_{GNP} (V_{GNP} - V_{GNP}^c)^2$$

Equation (7)

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3 where V_{GNP}^c is the critical volume fraction of the GNP inside the GNP-rich zones. Some literature
4 studies^{55,56} suggest that the critical volume fractions are inversely correlated to the filler aspect-ratio:
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6 $V_g^c \propto 1/\xi_g$ and $V_{GNP}^c \propto 1/\xi_{GNP}$, hence the reason why ξ_g must be higher than ξ_{GNP} to enhance the
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8 conductivity of nanocomposites. Using Equation (7) inside Equation (6), we can simulate the trend of
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10 nanocomposite conductivity with P&F cycles (Figure 2d, where we assumed a linear increment of V_g and
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12 ξ_g with P&F cycles). This trend is quite similar to that of data in Figure 2c and to the model of Equation
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14 (5). Therefore, the parameter D_c of Equation (5) represents the situation where there is the best
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16 compromise between ξ_g and V_{GNP} during the P&F process that gives the maximum possible conductivity,
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18 $\sigma_M: D_c \propto V_{GNP}/\xi_g$ and $\sigma_M \propto \xi_{GNP}/D_c$.
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24 In summary, our nanocomposites can be divided in three categories according to the nanofiller
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26 dispersion state: 1) nanocomposites with $D < 15\%$ containing inhomogeneous GNP distribution and
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28 isolated GNP agglomerates that do not form an electrically conductive network and for which the
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30 mechanical properties are comparable to or worse than those of the neat LLDPE; 2) nanocomposites
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32 with $15\% < D < 50\%$ containing well dispersed and aligned GNPs, showing high and anisotropic
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34 conductivities and good mechanical reinforcement; 3) nanocomposites with $D > 50\%$ presenting highly
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36 dispersed and aligned GNP, having enhanced mechanical properties but poor electrical conductivity. The
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38 combination of electrical and mechanical properties is thus a strong function of the parameter D .
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47 Towards ultra-high nanofiller loadings

48 Figure 3a compares values found in literature^{52,57–61} for the reinforcement of layered nanocomposites of
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50 LLDPE and GNP/graphene with theoretical predictions using the Halpin-Tsai model, which assumes
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52 “optimally dispersed” systems. None of the literature datasets follow the linear trend expected from the
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54 theory: the datasets show the typical reduction in reinforcing efficiency with nanofiller loading,
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commonly attributed to decreasing nanofiller dispersion quality as the concentration of nanoparticle increases. Here we examine the properties of nanocomposites prepared at 200 P&F cycles (LLDPE and GNP are not affected by such high cycles as demonstrated in S.9) as a function of GNP loading.

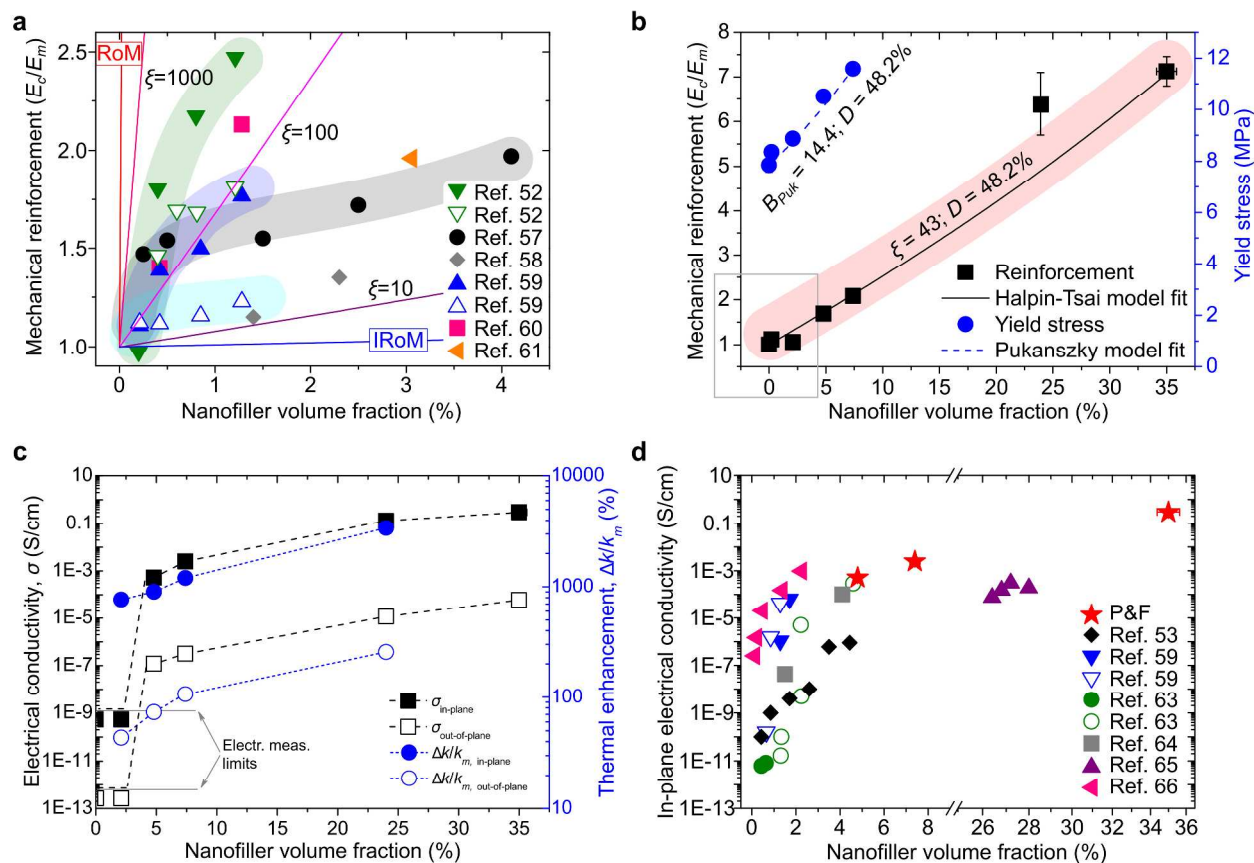


Figure 3. Properties of LLDPE nanocomposites for different GNP loadings but similar dispersion level (48.2%). (a) Mechanical reinforcement of GNP-LLDPE nanocomposites from literature, together with prediction lines of the Halpin-Tsai model at different aspect-ratios ξ of mono-layer graphene. The shadowed areas are a guide for the eye to highlight the decrease of reinforcing efficiency with nanofiller loading. For some cases there are two data-sets per reference corresponding to nanocomposites prepared by different techniques or with different matrix/nanofiller functionalisation. (b) Mechanical reinforcement and yield stress of GNP-LLDPE nanocomposites for $n=200$ P&F cycles. The frame corresponding to low volume fractions indicates the region where literature data typically fall (see Figure 3a). Because of the high GNP loading that increases nanocomposite brittleness, the sample containing 35 vol.% GNP does not show any yield before fracture. The modified Halpin-Tsai and Pukanszky models modified by Equation (3) fit the reinforcement and yield data. In both fits, the D -factor was kept constant at 48.2% (value found for previous nanocomposites containing 4.8 vol.% GNP prepared at $n=200$). (c) Electrical conductivity of GNP-LLDPE nanocomposites prepared with $n=200$ (lines are guides for the eye), and thermal conductivity

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3 *enhancement with respect to the value obtained for LLDPE, k_m . (d) In-plane electrical conductivity of LLDPE-GNP*
4 *nanocomposites. Note the high in-plane conductivity of 0.3 S/cm for the sample at 35 vol.% obtained via P&F.*
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11 We find that the mechanical reinforcement vs. volume fraction data for P&F (representative stress-
12 strain curves can be found in Figure S10) can be well fitted by the Halpin-Tsai and Pukanszky models
13 using V_p^{eff} with a fixed $D = 48.2\%$ (Figure 3). The model parameters correspond to a nanofiller aspect-
14 ratio of 43 (in agreement with the theoretical one, $\xi_{th} = 38$, from the fit in Figure 1e), and nanofiller-
15 matrix interaction parameter B_{Puk} of 14.4, similar to values reported for clay nanocomposites.⁶²
16 Considering that no compatibiliser was used, the high value of the parameter B_{Puk} suggests a fairly good
17 GNP-LLDPE interaction. These results demonstrate that the dispersion efficiency of the P&F technique –
18 and hence the resulting reinforcement – does not decrease at high nanofiller amounts (*i.e.* D factor
19 remains constant), contrary to what is usually reported (Figure 3a).
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32 The in-plane conductivity of our samples is four orders of magnitude higher than the out-of-plane
33 conductivity (Figure 3c). This reflects the anisotropic layered microstructure of the nanocomposite.
34 Considering the aspect ratio of our GNP (~40) we should expect a percolation threshold around 15 vol.%
35 if GNP were perfectly dispersed.⁵⁵ The measured percolation threshold lies between 2.1 and 4.8 vol.%
36 (Figure 3c). This range is theoretically expected for perfectly dispersed nanoplatelets with aspect-ratios
37 of 150 – 250. Therefore, the non-homogeneous, imperfect GNP dispersion ($D \approx 50\%$) in our
38 nanocomposites increases the electrical conductivity (as depicted in Figure 2c), hence lowering the
39 percolation threshold to values theoretically expected for higher aspect-ratio fillers. This result
40 corroborates our conductivity model of Equation (5).
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53 The high electrical conductivities come with massive in-plane thermal conductivity enhancements: >10
54 W/m·K, more than 3000% higher than LLDPE thermal conductivity. The out-of-plane conductivity
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3 increases up to ~ 1 W/m·K. To the best of our knowledge, this is the highest combination of thermal
4 conductivity enhancement and thermal anisotropy ever reported. A comparison of the in-plane
5 electrical conductivity data with the values found in literature^{53,59,63–66} for layered nanocomposites of
6 LLDPE with GNP/graphene (Figure 3d) shows how our samples are the most conductive nanocomposites
7 reported. It is noted that the conductivity is predicted to be even higher for a D -factor close to $D_c \approx 25\%$.
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15 Materials multifunctional design and general applicability of the 16 approach 17

18 The P&F approach addresses the optimization of nanocomposite microstructures to fulfil particular
19 technological applications. For example, a layered microstructure with perfectly dispersed nanoparticles
20 is needed for materials with enhanced mechanical, gas-barrier or thermal properties, *e.g.* films for food
21 packaging and flexible electronics^{67,68} and heat dissipating devices.²⁸ We measured the thermal
22 conductivity of polymer nanocomposites with 4.8 vol.% GNP after 400 P&F cycles. Unexpectedly,
23 thermal conductivities were ~ 3 W/m·K in-plane ($\sim 900\%$ higher than neat LLDPE thermal conductivity)
24 and ~ 0.3 W/ m·K out-of-plane, while being electrically insulating in all directions (average inter-particle
25 distance longer than electron mean-free path⁶⁹). The combination of high thermal conductivity and low
26 electrical conductivity makes these nanocomposites promising for anisotropic thermal interface
27 management of modern electronic, optoelectronic and photonic devices.⁶⁹
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42 High dispersion levels can be useful for energy-storage devices^{25,26} (Figure 4a), provided that the
43 electrical conductivity (σ_{th}) is small enough to allow huge polarization effects inside the layered
44 microstructure without dielectric loss. A much lower nanofiller dispersion (corresponding to the critical
45 level D_c) is sufficient if high electrical conductivity is required, for example in Joule-heating materials
46 (Figure 4b) for de-icing⁷⁰ or safety self-limiting power devices.^{23,24} An intermediate level of electrical
47 conductivity, close to that corresponding to the percolation threshold, is normally required for resistive
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3 sensors (Figure 4c, for instance, shows strain sensitivity) which could find applications in smart textile
4 and structural health monitoring applications.^{29,30}
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8 If a combination of properties is simultaneously desired, a compromise in nanofiller dispersion needs to
9 be found. We found a good balance between mechanical and electrical properties when our GNP is
10 ~50% dispersed. At high nanofiller loadings, the theoretical conductivity at high dispersion states (σ_{th})
11 should not be very different from that at the critical dispersion level (σ_M). Therefore, one should find
12 good electrical properties even if the nanofiller dispersion is greater than D_c . This is the case for our
13 nanocomposites prepared with more than 20 vol.% GNP, which appear to be simultaneously promising
14 for self-heating devices triggered by low voltages (Figure 4b), health-monitoring (Figure 4c), and
15 mechanical applications.
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27 To prove the general applicability of our technique to different filler-matrix combinations, a number of
28 different nanocomposites were prepared by dispersing by P&F four types of nanoparticles of different
29 shapes and sizes (GNP with low specific surface area, GNP with high specific surface area,
30 montmorillonite MMT, and magnetite nanoparticles) into five different polymeric matrices.
31 Independently from the specific filler/matrix system selected, nanofillers could always be efficiently
32 dispersed into a given polymer matrix after a sufficient number of P&F cycles (Section S.11.6). The
33 performance of the resulting material is extremely promising. Let's take a LLDPE + MMT nanocomposite
34 for example. As we found a distribution rate of $\sim 7 \cdot 10^{-2}$ for MMT in LLDPE (much higher than $\sim 3 \cdot 10^{-3}$ for
35 GNP), we expected to reach a dispersion of $\sim 99\%$ after only ~ 50 P&F cycles. Therefore, we prepared a
36 sample containing an ultrahigh MMT loading of ~ 74 wt.%, and it appeared to be transparent indeed
37 (Figure 4d) because of the good MMT dispersion and alignment. The nanocomposite had a Young's
38 modulus of ~ 1.8 GPa, approximately 13 times higher than that of the pure polymer. This is a surprisingly
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high value for a nanocomposite based on a commodity or engineering plastic prepared by a top-down technique (Figure 4d, and Section S.12.4).

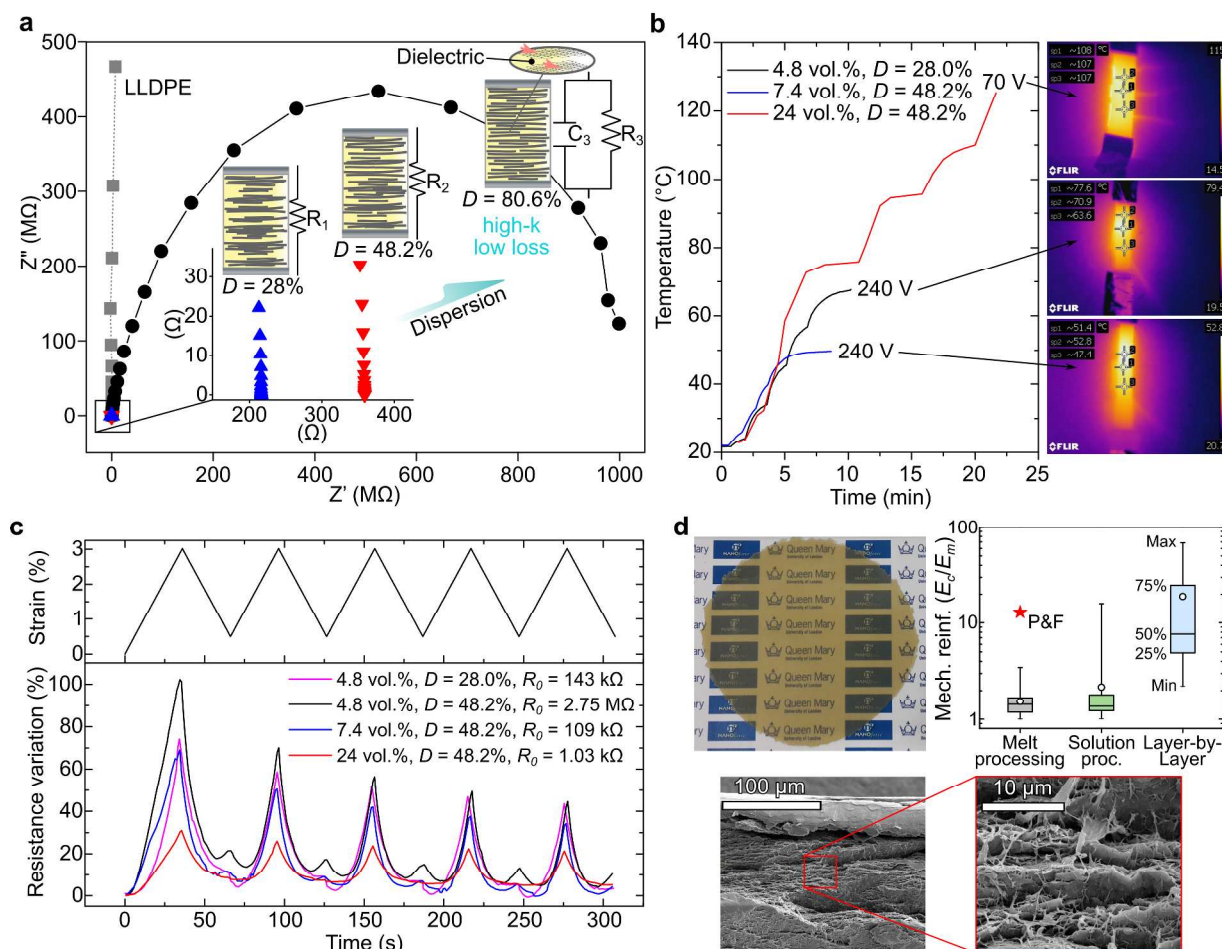


Figure 4. Examples of nanocomposites with optimized microstructures (nanofiller dispersion) for a variety of applications. (a) Imaginary (Z'') vs. real impedance (Z') obtained from electrochemical impedance spectroscopy of LLDPE containing 4.8 vol.% GNP for different dispersion levels. In accordance with value of σ_{th} expected from Equation (5) the sample with $D = 80.6\%$ is the only one showing a capacitive effect, demonstrated by the Nyquist semicircle. (b) Self-heating originating from Joule effect for LLDPE composites at different GNP loadings and dispersion levels. The sample with 4.8 vol.% GNP shows a better self-heating effect than the sample containing 7.4 vol.% GNP because its nanofiller dispersion level ($D = 28$), is closer to the critical value $D_c = 25\%$ predicted by Equation (5). (c) Strain sensing of LLDPE composites with for different GNP loadings and dispersion levels. High values of D give high resistance variations (gauge factor of ~ 30) because the nanocomposite conductivity approaches the theoretical value σ_{th} more quickly with the strain (see sample containing 4.8 vol.% GNP with $D = 48.2\%$).

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3 *Dispersions closer to D_c provide better electrical signals. The resistance variation becomes less evident for increasing amounts*
4 *of GNP because the difference between σ_M and σ_{th} is smaller (for details, see Section S.12.2). (d) Optical picture (top-left) of*
5 *LLDPE + 70 wt.% MMT (~10 cm wide, and ~400 μm thick), SEM cross-sections (bottom), and comparison (top-right) of*
6 *mechanical reinforcement with literature values for MMT nanocomposites grouped by the processing method. We achieved the*
7 *highest mechanical reinforcement ever reported for melt processing. QMUL logo is used with permission.*
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16 Conclusions

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18 The lack of control over nanofiller dispersion, exacerbated at high nanofiller loadings, has often
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20 prevented nanocomposites from fulfilling multi-functional requirements. In this study we have
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22 demonstrated a top-down scalable polymer processing method, the Pressing & Folding method, that
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24 can enable the dispersion of ultra-high concentrations of nanofiller (at least up to 74 vol.%) by selecting
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26 a sufficient number of P&F cycles. With this method we have been able to achieve mechanical
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28 reinforcements close to the maximum theoretical prediction levels, independently of nanofiller loading.
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30 Key aspects of the method are the controlled mixing, the use of a strong flow with a dominant
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32 elongational component, and the processing at temperatures just above the glass transition
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34 temperature. As an example of the potential of the method to optimize microstructures to achieve
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36 multifunctional properties, we have produced nanocomposites by P&F simultaneously presenting
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38 enhanced mechanical reinforcement, strain sensing, self-heating, and energy management properties.
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50 Methods

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52 Linear low-density polyethylene (LLDPE, density 0.921 g/cm³, melting point 116 °C) Flexirene MS20A
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54 (Versalis S.p.A., Italy), and expanded graphite (EG, bulk density 0.04 g/cm³, BET specific surface area 25
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3 m²/g) Timrex C-Therm 002 (Timcal Ltd, Switzerland) were used as polymer matrix and nanofiller,
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9 The pressing-and-folding (P&F) technique used to prepare the nanocomposites can be divided in three
10 steps. First, two LLDPE films (~100 μm thick) were prepared by hot-pressing polymer pellets inside a hot-
11 press (Collin P 300 E). Subsequently, EG powder was deposited with a spatula in the middle of the
12 surface of one LLDPE film so that the other film could be placed on top preventing the powder from
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The 'sandwich' was then hot-pressed inside of an aluminium frame (~300 μm thick) at 40
bar and 120 °C for 30 s to join the two materials. In the final processing step, LLDPE and EG were
gradually dispersed by repetitive folding and hot-pressing these films. In particular, at each P&F cycle
the sample was manually folded twice in a symmetric manner and pressed at 40 bar and 120 °C for 30 s
inside the aluminium frame in order to maintain the resulting thickness at ~300 μm after the pressing.
The weight concentration of GNP inside each sample was calculated by measuring the weight of the
initial LLDPE films, before and after adding EG (after the second step).

In order to study the properties of the nanocomposites as a function of P&F cycles – corresponding to
GNP dispersion and distribution throughout the matrix – samples of LLDPE containing 10.7 wt.% (4.8
vol.%) of GNP were prepared at different P&F cycles. To study the effect of possible degradation of the
polymer matrix with the P&F cycles, samples of neat LLDPE at 1, 50, 100, and 150 P&F cycles were also
prepared.

A reference sample of LLDPE + 10.7 wt.% of GNP was prepared by traditional melt-blending followed by
a compression moulding technique. Here LLDPE pellets and EG were used without drying. The composite
was prepared by melt-blending at 120 °C under nitrogen atmosphere using a DSM X'plore 15cc micro
compounder. Compounding was performed for 9 min at a screw speed of 180 rpm. The resulting
compound was hot-pressed at 40 bar and 120 °C for 30 s inside an aluminium frame ~300 μm thick.

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3 Finally, samples of 0.5, 5, 10.7, 16, 43.6 and 56 wt.% (corresponding to 0.21, 2.1, 4.8, 7.4, 24 and 35
4 vol.%) of GNP were prepared at 200 P&F cycles to validate the effectiveness of this technique in
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6 dispersing different concentrations of nanofiller. It was chosen to prepare all samples at 200 P&F cycles
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8 because we found that this number of cycles gave optimal mechanical properties, which were even
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10 higher than those of the reference sample prepared by melt-blending, whereas electrical conductivity
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12 values were among the highest reported in literature.
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17 The methods used to characterize the nanofiller, matrix, and nanocomposites are described in the
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19 Supporting Information. Methods used to test the self-heating effect, strain-sensing, and
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21 impedance/energy-storage are also reported in the Supporting Information.
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28 Author Contributions

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30 E. Bilotti designed the experiments. G.S., L.R., and Y.L. developed the P&F technique. G.S. and L.R.
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32 prepared the P&F samples. O.T.P. prepared the melt blended reference sample. G.S. and H.Z. tested the
33
34 strain-sensing behaviour of samples. H.P. performed the self-heating tests and analysed the related
35
36 data. M.C. performed the EIS tests and analysed the related data. S.C. and A.F. performed thermal
37
38 conductivity tests and A.B.S., G.B. and J.P.P. transmission electron microscopy. G.S., O.T.P. and L.R.
39
40 carried out all other samples characterizations. G.S., O.T.P., N.M.P., T.P., E. Barbieri, L.B. and E. Bilotti
41
42 interpreted and discussed the results. G.S. analysed the data, derived the dispersion model and wrote
43
44 the paper under the supervision of N.M.P., T.P. and E. Bilotti. L.B. derived the micromechanical model of
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46 the P&F technique.
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Competing Financial Interests

The authors declare no competing financial interests.

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Supporting Information Available:

Characterization techniques; XRD observations; nanofiller characterization; influence of P&F cycles on the properties of neat LLDPE; influence of P&F cycles on the properties of LLDPE and GNP inside nanocomposites; nanocomposites of LLDPE + 0.21 vol.% GNP at different P&F cycles; filler agglomerates inside nanocomposites of LLDPE + 4.8 vol.% GNP at different P&F cycles; tensile failure of nanocomposites of LLDPE + 4.8 vol.% GNP; nanocomposites of LLDPE + 4.8 vol.% GNP prepared by melt blending; influence of GNP loading on the properties of GNP and LLDPE inside nanocomposites; rheology study; models derivation; details of potential applications; overview of classical composite theories. This material is available free of charge *via* the Internet at <http://pubs.acs.org>.

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