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Effects of ultrasound on the fermentation profile of fermented milk products incorporated with lactic acid bacteria

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PII: S0958-6946(18)30258-9

DOI: https://doi.org/10.1016/j.idairyj.2018.10.006

Reference: INDA 4411

To appear in: International Dairy Journal

Received Date: 28 March 2018

Revised Date: 30 October 2018

Accepted Date: 30 October 2018

Please cite this article as: Abesinghe, A.M.N.L., Islam, N., Vidanarachchi, J.K., Prakash, S., Silva, K.F.S.T., Karim, M.A., Effects of ultrasound on the fermentation profile of fermented milk products incorporated with lactic acid bacteria, *International Dairy Journal*, https://doi.org/10.1016/j.idairyj.2018.10.006.

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24	ABSTRACT
25	
26	Ultrasonic processing of fermented milk products has created much interest in current research
27	on dairy products. This has been employed in cultured milk products to enhance the
28	emulsification of milk fat and to intensify the fermentation process. Benefits including
29	remarkable product stability, reduced processing time and enhanced quality are being recorded.
30	Ultrasound (US) altered the colour and flavour profile of milk; however, the effect of US-
31	induced fermentation on the synthesis of flavour compounds in milk has not been reported in the
32	literature. This review paper presents a comprehensive scenario on the impact of power US on
33	the fermentation profile and quality of ultrasonically processed dairy products. A theoretical
34	background on US and details of its effect on the metabolic performance of lactic acid bacteria
35	are presented. Finally, it describes how the quality attributes of fermented milk gels are modified
36	due to the intensification of the fermentation process with US.
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61 1. Introduction

62

63	Ultrasound (US) refers to sound waves above a frequency of 20,000 Hz, which are not
64	detectable by the human ear, and can be divided into three main categories based on frequency
65	range: (i) power US (20–100 kHz); (iii) high-frequency US (20 kHz – 2 MHz) and (iii)
66	diagnostic (1-10 MHz) (Awad, Moharram, Shaltout, Asker, & Youssef, 2012; Martini, 2013b).
67	Power US has energy intensities between 10 and 1000 W cm ⁻² . When power US travels
68	through a medium, it causes significant physical and chemical changes through a phenomenon
69	called "acoustic cavitation" that induces the formation of cavities (Martini, 2013a). This has been
70	widely employed in the food industry for technologies such as drying, deforming, microbial
71	inactivation and emulsification (Charoux, Ojha, O'Donnell, Cardoni, & Tiwari, 2017; Kumar,
72	Karim, & Joardder, 2014). The application of power US in emulsification/homogenisation and
73	microbial inactivation in milk has been extensively reviewed by Awad et al. (2012), Chemat and
74	Khan (2011) and Paniwnyk (2017) and, therefore, outside of the focus of this paper.
75	Intensification of milk fermentation using power US is another area of interest in the
76	dairy industry. Fermentation is the most time- and resource-consuming stage during the
77	manufacture of cultured milk products. Numerous research studies have revealed that power US
78	can enhance the fermentation rate of lactic acid bacteria (LAB) by modifying their metabolism
79	while improving the quality characters such as water holding capacity (WHC), texture profile
80	and syneresis of fermented milk gels (Riener, Noci, Cronin, Morgan, & Lyng, 2010; Sfakianakis,
81	Topakas, & Tzia, 2015; Shershenkov & Suchkova, 2015). However, the application of power US
82	in dairy fermentation has not yet been adequately reviewed in the literature. While a recent
83	review by Ojha, Mason, O'Donnell, Kerry, and Tiwari (2017) revealed some avenues of

applying US in milk fermentation, the objective of this review is to provide a comprehensive
analysis of recent studies on power US towards improving the overall fermentation profile of
dairy products.

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2. Ultrasound apparatus for fermentation experiments and acoustic cavitation

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90 The major components of a US generation system are an electrical power generator, 91 transducer(s), and an emitter (Bermúdez-Aguirre, Mobbs, & Barbosa-Cánovas, 2011); the 92 electrical generator supplies the required energy to run the transducer at a certain frequency. The 93 US transducer consists of a piezoelectric material that converts electrical oscillations into 94 mechanical vibrations of a similar frequency. The major function of the emitter is to discharge 95 the US wave from the transducer into the medium. Moreover, the transducer can also amplify the 96 ultrasonic vibrations.

Ultrasonication devices are classified as either direct (US probe) and indirect types (US 97 bath) as shown in Fig. 1. In the direct type, acoustic energy is directly dissipated from the 98 transducer to the sample and this is approximately 100 times higher than the energy intensity of 99 indirect sonication (Marcela, Silvana, Fabiana, Renata, & Lisiane, 2018). In this system, a horn 100 is attached to the transducer to amplify the signal and bring it to the sample. The tip of the horn, 101 102 often a separate attachable device known as a sonotrode, radiates the ultrasonic waves into the sample. The higher cavitational intensity acquired for less volume makes probe sonicators more 103 appropriate for laboratory scale operation than bath sonicators. In the case of indirect mode, US 104 105 is introduced to the sample indirectly through one or more transducers that are attached to the

106	walls or at the bottom of a vessel. US energy is indirectly dissipated from the transducer to the
107	sample through a coupling fluid, most often water (Sancheti & Gogate, 2017).
108	When US waves pass through a liquid medium it creates a series of compression (positive
109	pressure) and expansion cycles (negative pressure). During the negative pressure cycle, gaseous
110	impurities in the liquid medium such as pre-existing bubbles that are coated with contaminants,
111	solid particles with trapped gases or tiny crevices in the walls of the vessel lead to the disruption
112	of the liquid medium and nucleation to form gas bubbles (Leong, Ashokkumar, & Kentish,
113	2016). These bubbles start to grow in size due to rectified diffusion and bubble-bubble
114	coalescences.
115	Rectified diffusion is the uneven transfer of mass through the air/liquid boundary during
116	the rarefaction and compression phase of the sound wave cycle (Church, 1988). There are two
117	major causes for this uneven mass transfer, namely "area effect" and "shell effect" (Leong et al.,
118	2016). The "area effect" means that the bubbles have a larger surface area during the expansion
119	cycle, which increases the diffusion of gas and solvent vapour into the bubbles, but these are not
120	fully expelled during the subsequent compression phase where the surface area is comparatively
121	smaller. The "shell effect" refers to the increase in the thickness of liquid shell that covers the
122	bubble upon contraction, whereas the thickness reduces during the expansion phase. The
123	concentration gradient of gas is low when the bubble has a thick mass transfer boundary layer
124	and vice versa and this results in a net accumulation of mass into the bubble. Once the US energy
125	provided is not adequate enough to retain the vapour phase inside the bubble, the local pressure
126	declines to some point below the saturated vapour pressure of the liquid. As a result, a rapid
127	condensation occurs and the condensed molecules collide violently, creating shock waves and
128	generating very high temperature (Abbas, Hayat, Karangwa, Bashari, & Zhang, 2013; Huang et

129	al., 2017). The implosion of cavitation bubbles generates an excessive amount of heat and the
130	temperatures within the bubbles that could go up to 750–6000 K within a short period of time
131	(Ashokkumar, 2011).

The creation, expansion and implosive collapse of micro-bubbles in ultrasonically 132 irradiated liquids is known as acoustic cavitation (Torley & Bhandari, 2007). If cavitation occurs 133 close to a firm surface, the bubbles may break asymmetrically and create fast-moving liquid jets 134 that may create localised surface damage. There are several physical effects generated in the 135 medium during the oscillation and implosion of cavitation bubbles such as shock waves, shear 136 forces, micro-jets, turbulence, etc. (Bermúdez-Aguirre et al., 2011; Louisnard & González-137 138 García, 2011). Depending on the conditions used such as amplitude, temperature, pressure, and the composition of the medium, several mechanisms can be activated including increase of the 139 temperature, surface instability, generation of agitation and friction, increase of mass transfer, 140 141 generation of free radicals and disruption of cell materials (Ashokkumar, 2011; Martini, 2013b; Salazar, Chávez, Turó, & García-Hernández, 2009). 142

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144 3. Application of power ultrasound in lactic fermentation of milk

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Application of both low power ultrasound (LPU) and power US in fermentation has been reported in the literature. LPU has power intensities below 1 Wcm⁻² and is commonly used for non-destructive analysis in the food industry to characterise food components, often on quality assurance lines and to monitor fermentation processes (Novoa-Díaz et al., 2014) and is not a focus for this review paper. On the other hand, PU (with power intensities above 10 Wcm⁻²) alone (sonication) or in combination with external pressure (manosonication), heat

(thermosonication) or both pressure and heat (manothermosonication) has been reported to 152 influence the lactic fermentation in cows' milk, soy milk and sweet whey and is outlined in 153 Table 1. 154

155

- 4. Effect of power ultrasound on fermentation time 156
- 157

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Reducing the fermentation time in cultured dairy products by US is one of the most 158 promising approaches that has been identified previously in the literature (Barukčić, Jakopović, 159 Herceg, Karlović, & Božanić, 2015; Nguyen, Lee, & Zhou, 2009; Riener et al., 2010; 160 161 Sfakianakis et al., 2015; Shimada, Ohdaira, & Masuzawa, 2004; Wu, Hulbert, & Mount, 2001). For yoghurt, fermentation time is defined as the interval between the time of addition of cultures 162 and the time at which the pH of the yoghurt reaches pH 4.7 (Puvanenthiran, Williams, & 163 164 Augustin, 2002). Reduction of the fermentation time helps decrease production time and cost. This can also be used to improve the consistency and the texture of the milk gels. Shorter 165 fermentation time is reported to reduce the extent of rearrangements within the yoghurt gel 166 network that are caused by electrostatic repulsions and the dissolution of colloidal calcium 167 phosphate crosslinks. As a result, whey separation and formation of large pores are decreased 168 compared with longer fermentation times (Peng, 2010). 169 It was observed that the application of US (20 KHz, 180 W, 270 W and 450 W) for 8 min 170 to a mixture of Jersey and Holstein milk (sample size 150 mL) after inoculation with yoghurt 171 cultures followed by the fermentation reduced the fermentation time by 30 min in set type 172 yoghurt (Wu et al., 2001). Similarly, Dolatowski, Stadnik, and Stasiak (2007) reported a

reduction of set yoghurt production time up to 40% with the use of US. Further, the sonication of 174

reconstituted skimmed milk (15%, w/v) inoculated with Bifidobacterium sp. at 20 KHz and 100 175 W for 15 min that was followed by the fermentation at 37 °C reduced the fermentation time by 176 11–26% (Nguyen et al., 2009). More recently, the fermentation of reconstituted sweet whey (6% 177 of the dry matter) by a US treated culture of *Lactobacillus acidophilus* with 84 W for 150 s was 178 reported to reduce fermentation time by 30 min (Barukčić et al., 2015). In contrast, a few authors 179 have reported that ultrasonication led to a reduction or total elimination of the lag phase of the 180 growth curve of lactic acid bacteria (LAB) in milk without influencing the total duration of 181 182 fermentation. Sfakianakis et al. (2015) observed a complete disappearance of the lag-phase of the lactic acid bacteria during the fermentation of pre-sonicated skimmed bovine milk (fat: 0.1% 183 w/w, SNF: 14% w/w) with power US (750 W at 500 mL sample volume, 1500 kWm⁻³; 10 min) 184 without affecting the total fermentation time. Moreover, sonication of raw skim milk (fat 185 content: 0.1%) during the fermentation using an ultrasonic water bath (45 kHz, 200 W, 17 kWm⁻ 186 ³) significantly reduced the pH during the lag phase compared with the untreated sample without 187 affecting the duration of fermentation process (Nöbel et al., 2016b). 188 Apparently, the effect of US on fermentation time may rely on process parameters such 189 as acoustic intensity, frequency, treatment duration, the point of application (before inoculation 190 or after inoculation) and the composition of milk. In an initial investigation, Shimada et al. 191 (2004) found that the fermentation time of a kefir culture (time at which the pH reaches 4.5) was 192 shortened exponentially when the sonication frequency was increased from 28 kHz to 200 kHz 193 during fermentation. Consequently, authors suggested that ultrasonic waves promoted the 194 fermentation process under conditions where cavitation was not generated, and was suppressed 195 when cavitation occurred. However, the influence of factors such as different milk composition, 196

197 starter culture used and process parameters on fermentation kinetics have not been reported in198 the literature to date.

Several mechanisms are proposed to describe the role of power US in inducing the 199 fermentation process. Some authors suggested that PU can improve membrane permeability of 200 starter bacteria, so allowing the release of intracellular enzymes such as β -galactosidase (EC 201 3.2.1.23) from the cell (Ewe, Abdullah, Bhat, Karim, & Liong, 2012; Nguyen et al., 2009; Wang 202 & Sakakibara, 1997; Wu et al., 2001). Another mechanism, proposed by Shimada et al. (2004) 203 and Piyasena, Mohareb, and McKellar (2003), is that a slight local temperature rise due to the 204 heat derived from ultrasonic absorption may activate the lactic bacteria and shorten the 205 fermentation time. Moreover, Pitt and Ross (2003) suggested that US may accelerate the supply 206 207 of oxygen and nutrients for microorganisms and increase the discharge of waste products from the cells, thus enhancing microbial cell growth. A different mechanism was hypothesised by 208 Nguyen et al. (2009), who demonstrated that the stimulatory effect of fermentation was due to 209 the leakage of some cellular contents such as β -galactosidase, complex photolytic systems and 210 some growth factors from the ruptured bacterial cells under sonication. 211

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- 213 5. Effects of ultrasound on cell membrane permeability
- 214

Sonoporation describes the progressive opening of the cell membrane due to microbubble cavitation upon US exposure of cells (Lentacker, De Cock, Deckers, De Smedt, &
Moonen, 2014; Maciulevičius et al., 2016). The micro-bubbles create micro-streaming and/or
liquid jets (Maciulevičius et al., 2016), which generate a strong shear force that breaks the
chemical bonds in the cell membranes (Tabatabaie & Mortazavi, 2008), puncture cell surfaces

and create cell membrane pores (membrane permeabilisation). To date, there have been several
mechanisms proposed to understand the interaction of micro-bubbles with cell membranes that
leads to sonoporation such as: (i) push and pull effect of micro-bubble, (ii) micro-streaming
(liquid flow around micro bubbles) that tears the lipid membrane, and (iii) penetration of micro
bubbles into a cell. The recent literature reported that relatively small oscillation amplitude at
lower US intensities exhibited higher impact on the cell membrane, compared with non-adhered
micro-bubbles (Lentacker et al., 2014).

Furthermore, it has now been suggested that, apart from this mechanical stress, some 227 chemical effects induced by US are also responsible for pore formation. For example, stable 228 229 micro-bubble oscillations can induce the formation of free radicals and molecular products such as H₂O₂ (Gao, Hemar, Ashokkumar, Paturel, & Lewis, 2014a; Gao, Lewis, Ashokkumar, & 230 Hemar, 2014b), which play a vital role in lipid bilayer relocation and membrane disruption 231 232 through lipid peroxidation. Furthermore, it was also revealed that peroxidation of membrane lipids (Ewe et al., 2012; Lentacker et al., 2014) and conformational unfolding of proteins that are 233 located on the surface of the cell membrane increase membrane fluidity and membrane 234 permeabilisation upon US treatment (Ewe et al., 2012). From the available literature, it is clear 235 that a low level of sonoporation can be used to improve the permeability of cell membranes, 236 resulting in improved mass transfer of substrates across the microbial cell membrane and 237 efficient removal of by-products of cellular metabolism, which eventually improves microbial 238 growth (Ojha et al., 2017). However, to achieve the desired level of cell permeabilisation and to 239 avoid cell death, ultrasound process parameters must be precisely quantified and controlled, 240 because an excessive level of sonoporation can lead to a leakage of cellular content because of 241 the physical disruption and eventually lead to cell death (Ojha et al., 2017). 242

243	Using microscopy, the effect of power US (20 kHz, 30 min) on cell wall permeability of
244	lactic acid bacteria has been investigated by several researchers (Cameron, McMaster, & Britz,
245	2008; Shershenkov & Suchkova, 2015; Tabatabaie & Mortazavi, 2008). LAB that were exposed
246	to US treatment showed both pore formation and cellular damage (Ewe et al., 2012). Three types
247	of micro-damage, namely micro-cracks, micro-voids and ruptures, have been identified in cell
248	membranes of LAB (Tabatabaie & Mortazavi, 2008). An in-depth analysis of the effect of power
249	US (20 KHz) on the extent of structural damage of Lb. acidophilus was performed using
250	transmission electron microscopy (TEM) by Cameron et al. (2008) as shown in Fig. 2. It was
251	demonstrated that an US treatment of 5 min leads to both external and internal cell damage to Lb.
252	acidophilus where the cell terminus had been trimmed and a low number of liposome-like
253	vesicles were presented inside the cells.
254	Moreover, flow cytometric analysis revealed that US increased both membrane
255	permeability and fluidity of LAB (Ewe et al., 2012). These changes may result from
256	emulsification of cell membrane lipids (lipid peroxidation) due to intracellular cavitation or
257	associated air bubbles. Therefore, it can be suggested that the coagulation time of milk is
258	shortened by US as pore formation in bacterial cell membranes increases cell membrane
259	permeabilisation and enhances the cellular transport of metabolites. However, it was observed
260	that the changes associated with the bacterial cell membrane were more prominent with
261	increasing treatment amplitudes and treatment durations (Ewe et al., 2012). Therefore, the
262	optimum conditions for such ultrasonication parameters should be carefully determined before
263	applying sonication to the fermented dairy products.
264	

265 6. Effect of ultrasound on growth and cell viability of lactic acid bacteria during 266 fermentation

267

Depending on the intensity and the duration of sonication, US has shown both 268 acceleration and inhibition effects on proliferation and viability of microbial cells. Application 269 of US (25 kHz, 160 W for 10 min) increased the cell biomass and fibrinolytic enzyme production 270 271 in Bacillus sphaericus due to de-agglomeration of cell clusters and improvement of nutrient 272 utilisation (Avhad & Rathod, 2015). Similarly, Wang, Shi, Zhou, Yu, and Yang (2003) observed an increased proliferation ability of Saccharomyces cerevisiae upon US treatment due to 273 274 enhanced membrane permeability. Lanchun et al. (2003) found that US treatment of S. cerevisiae during the lag phase and exponential phase enhanced cell growth and proliferation by 275 overcoming the mass transfer limitations with the generation of strong convection through 276 277 micro-streaming. Moreover, Dahroud et al. (2016) showed that US treatment at 60% amplitude for 15 s increased the logarithmic phase duration and growth of Lactobacillus casei subsp. casei 278 in MRS broth (Fig. 3). 279

The inhibition effect is due to unrepairable cellular injuries such as breaking and shearing 280 of the microbial cell wall when exposed to intense US. Gao et al., (2014b) suggested that this 281 was mainly due to the mechanical forces and the pressure changes generated through the violent 282 collapse of micro-bubbles within the microbial cells (intracellular cavitation) that eventually 283 resulted in a cell death (Piyasena et al., 2003). Similarly, this can damage the cytoplasmic 284 membrane, which results in the leakage of intracellular contents and coarseness of the cell 285 286 membrane by the deposition of cell debris on the surface of other cells (Huang et al., 2017). The intensity of US and the duration of the sonication should therefore be carefully selected for 287

288 application in probiotic dairy products where the viable cell count (VCC) is a critical parameter in determining the shelf-life. The growth and viability of LAB under various ultrasonication 289 conditions, observed by different researchers are summarised in Table 2. 290 An inhibitory effect on the VCC of lactobacilli was observed by Wang and Sakakibara 291 (1997) during continuous sonication (200 kHz, 17.2 kW m⁻²) within the fermentation period. 292 Interestingly, sonicated fermentation did not affect the proliferation ability of the lactobacilli 293 294 cells that survived and the cell counts rose when fermentation continued under static conditions. However, the initial reduction of VCC may result in a slower acidification during the 295 fermentation process, leading to extended fermentation time. 296 297 Some research findings revealed that the frequency and/or power of ultrasonication that exerts a lethal effect towards microbial cells is dependent on the type of microorganism; different 298 strains have a different response to US (Huang et al., 2017). Therefore, it can be expected that 299 US may affect the viability of different lactic acid bacteria to different extents. Though the 300 effectiveness of ultrasonication on cell viability can be simply assessed through enumeration of 301 microbes before and after treatment, differences in US parameters used in previous studies make 302 comparison of results difficult. Additionally, there are several other variables that influence the 303 effect of US on growth and viability of microorganisms such as process parameters (temperature, 304 amplitude, pressure and duration of sonication) and the physical and biological properties of the 305 microorganism (growth phase, size, capsule thickness), etc. (Gao et al., 2014b; Puvanenthiran et 306 al., 2002; Vercet, Oria, Marquina, Crelier, & Lopez-Buesa, 2002). Similarly, volume of food 307 308 being processed and the properties of the food, such as composition, viscosity and size of particulates, may influence both the stimulation and inactivation effects of US on 309 microorganisms (Piyasena et al., 2003); this warrants further investigation. There is, however, 310

311	another important factor, i.e., the level of inoculation, which determines the effectiveness of
312	sonicated fermentation; inoculum rates different from those used in commercial manufacturing
313	might produce different results during sonicated fermentation, but this is not reported in the
314	literature.
315	
316	7. Effect of ultrasound on enzyme activity
317	
318	β -Galactosidase (β -gal, β -D-galactoside galactohydrolase or lactase) is the major
319	intracellular enzyme possessed by LAB to catalyse the hydrolysis of β -D-galactoside to galactose
320	(Hermanson, 2013). Several authors found that US accelerated the activity of β -galactosidase in
321	the LAB (Ewe et al., 2012; Nguyen et al., 2009; Wang, Sakakibara, Kondoh, & Suzuki, 1996).
322	This stimulation activity may be due to the collective effects of US such as: (i) enhanced
323	membrane permeabilisation of LAB causing the release of intracellular enzymes into the
324	substrate network (Ewe et al., 2012; Wang & Sakakibara, 1997), (ii) reduction of the activation
325	energy of the enzymes (Delgado-Povedano & de Castro, 2015) and (iii) alteration of the
326	characteristics of the enzyme and the substrate that may enhance the exposure of active sites of
327	membrane-bound enzymes to substrates (Ewe et al., 2012; Huang et al., 2017).
328	Alteration of the enzyme structure upon US treatment was observed by Ma et al. (2011)
329	with free cellulase where the α -helix structure was partially deformed and the random coil
330	content and the number of surface tryptophan residues were increased upon US treatment (24
331	kHz, 15 W, 10 min). It might be assumed that the changes to the unique structure of the enzyme
332	and/or the substrate should reduce the activity of the enzyme owing to failure in forming specific
333	enzyme-substrate complexes. However, some contrasting results were achieved with cellulase

334 where the enzyme activity was increased by 18.17% with US treatment compared with untreated cellulase (Wang et al., 2012). Similar findings with respect to increased enzyme activity were 335 reported by Huang et al. (2017) where the degree of hydrolysis of US treated rice proteins was 336 improved due to significant changes to the microstructure of the substrate. Although it was 337 proposed that US with suitable intensity and frequency improves efficiency of enzymolysis due 338 to sonochemistry effects such as cavitation, oscillation and magnetostrictive effects on the 339 340 molecular conformation of enzymes and substrates, further experiments are warranted to 341 elucidate the exact mechanism behind the acceleration of affinity between the enzyme and the substrate upon sonication. 342

343 It has been claimed that process parameters such as duration of sonication and amplitude have different influence towards activity of intracellular and extracellular enzymes (Nguyen et 344 al., 2009). Bacterial cells treated with increased amplitude US for shorter duration (1 min) 345 346 showed significantly higher intracellular enzyme activities, whereas higher amplitude and longer duration (3 min) were favourable with respect to activity of extracellular enzymes. This was due 347 to an increase in lipid peroxidation by higher amplitude and longer duration of US treatment 348 which eventually enhanced membrane permeability. In contrast, prolonged exposure to 349 sonication (30 min) reduced the activity of β -galactosidase in *B. longum* possibly due to 350 decreased cell viability (Nguyen et al., 2009). 351

352 Moreover, it was observed that the effect of US process parameters on enzyme activity 353 varied with the particular strain of LAB used. This strain-dependent effect upon sonicated 354 fermentation was assumed to be influenced by survival rate, the inherent ability of the LAB 355 strain to produce β -galactosidase and growth phase. The effect of US on different strains of the 356 LAB was exhibited by Nguyen et al. (2009) where *Bifidobacterium breve* and *Bifidobacterium*

357 infantis were more resistant to US and showed higher fermentation rate, even though they had lower enzyme activity. Wang and Sakakibara (1997) reported similar findings in that 358 *Lactobacillus delbrueckii* subsp. *bulgaricus* showed higher β -galactosidase activity (1.5 unit; 359 where 1 unit of β -galactosidase activity was defined as the amount of the enzyme that liberated 1 360 μ mol *o*-nitrophenol from *o*-nitrophenyl- β -D-galactopyranoside per cm³ of sample per min) 361 compared with Lb. acidophilus (0.05 unit) upon sonicated fermentation (200 kHz, 17.2 kW m⁻²). 362 Further, they revealed the release of β -galactosidase under sonicated fermentation was prominent 363 in Lb. delbrueckii subsp. bulgaricus during the exponential phase of growth where cell division 364 is active. 365

Additionally, the activity of β -galactosidase was dependent on several other process 366 conditions such as pH, temperature, ionic strength and presence of inhibitors. Stability of β-367 galactosidase was optimum at pH 6.0-7.0 for the LAB (Wang & Sakakibara, 1997; Wang et al., 368 369 1996). When the pH varied from this optimal range, there was a significant drop in enzyme activity. Wang et al. (1996) observed that the activity of extracellular β -galactosidase decreased 370 by 90% and 57% when the pH changed from 6.5 to 5.5 and from 7 to 8, respectively. However, it 371 was reported that the intracellular β -galactosidase was comparatively more resistant due to the 372 protective mechanism of the bacterial cell membrane, which isolates the internal content of the 373 microbial cell from the external environment. Further, this favourable pH range for the optimum 374 activity of β-galactosidase was influenced by some other variables such as temperature and 375 presence of ions. At 25 °C, the enzyme was relatively stable at all pH levels, whereas, at higher 376 377 temperatures (51 and 56 °C), β-galactosidase was stable only at pH 6 and 7. Presence of cations such as Na⁺ and K⁺ affect the stability and activity of β -galactosidase differently. Na⁺ acts as a 378 strong inhibitor of the β -galactosidase enzyme where lactose was the substrate. Compared with 379

Na⁺, the stability of β -galactosidase was higher with the presence of K⁺ (Kreft & Jelen, 2000). Apparently, sonication enhanced the β -galactosidase activity of LAB and the maximum activity of β -galactosidase could be achieved if sonicated fermentation was carried out under optimum conditions.

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8. Effect of ultrasound on lactose metabolism

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High-intensity US was used to accelerate lactose hydrolysis in milk through the 387 modification of metabolic performance of LAB (Dahroud et al., 2016; Kreft & Jelen, 2000; 388 389 Nguyen et al., 2009; Toba, Hayasaka, Taguchi, & Adachi, 1990; Wang et al., 1996; Wang & Sakakibara, 1997). Several authors reported that US accelerated both consumption of lactose and 390 production of glucose, galactose and oligosaccharides, and the effect was improved with 391 392 prolonged sonication. Lactose consumption by *Bifidobacterium* sp. and *Lactobacillus* sp. was enhanced 2-4 times compared with non-sonicated samples (Nguyen, Lee, & Zhou, 2012; Toba et 393 al., 1990; Wang et al., 1996). Moreover, it was observed that consumption of lactose was notable 394 when sonication was initiated at the beginning of fermentation. In contrast, lactose consumption 395 by non-sonicated cultures started at a later (exponential phase) stage of growth. However, the 396 inoculum levels of the LAB differed between experiments, ranging from 3% to 5% and hence the 397 effect of initial concentration of the LAB cells on the lactose metabolism upon sonication was 398 not adequately explained. It was assumed that sonication accelerated lactose consumption by 399 extracellular β -galactosidase released by sonoporation (Nguyen et al., 2012). US accelerates both 400 401 hydrolysis and transfer reactions of lactose metabolism, where more simple sugars such as glucose and galactose are available for the bacteria. Further, availability of partially pre-402

403	hydrolysed lactose, in return, may enhance the growth of LAB (O'Leary & Woychik, 1976).
404	There may be some other process parameters such as pH, temperature and the presence of
405	inhibitors, etc., which affect the enzyme activity and thus the rate of lactose metabolism. Even
406	though sonication resulted in the highest levels of extracellular β -galactosidase activity, lactose
407	metabolism was low at pH 4.7 (Wang & Sakakibara, 1997). However, the degree of lactose
408	hydrolysis increased by 13.2% when fermentation was carried out at controlled pH.
409	Several authors showed that enhanced lactose hydrolysis upon sonicated fermentation
410	depended on bacterial strains used. For an example, degrees of lactose hydrolysis with Lb.
411	delbrueckii subsp. bulgaricus (39.9%) and Lactobacillus helveticus (35%) were higher than Lb.
412	delbrueckii subsp. lactis (38.1%) and Lb. acidophilus (19.6%) under same conditions (Wang &
413	Sakakibara, 1997). Comparable findings were reported by Nguyen et al. (2012) who showed that
414	lactose consumption by different Bifidobacterium sp. were significantly different. This could be
415	explained by the fact that different LAB strains have different inherent abilities to hydrolyse
416	lactose since they have various degrees of trans-galactosylation activities and survival rates.
417	Moreover, US can be used to enhance production efficiency of hydrolysed lactose milk,
418	which is suited to lactose-intolerant individuals. The application of periodic sonication
419	(sonication and static incubation) under pH controlled conditions have reportedly reduced the
420	lactose content of milk inoculated with Lb. delbrueckii subsp. bulgaricus (B-6 and B-5b) and Lb.
421	helveticus (LH-17) by up to 71–76%, whereas lactose hydrolysis in non-sonicated milk was only
422	up to 39–51% (Toba et al., 1990; Wang & Sakakibara, 1997). Therefore, the development and
423	implementation of continuous sonication techniques during fermentation may help produce
424	lactose-hydrolysed fermented milk under industrial scale.

426 9. Effect of ultrasound on texture and sensory attributes of fermented dairy products
427

Fermented milk gels should have a smooth and uniform texture without defects such as weak body, wheying-off and lumpiness (Lucey & Singh, 1997). US can influence the sensory properties of fermented milk products either negatively or positively. US treatment before inoculation improved textural characteristics of fermented products whereas, sonication during fermentation caused textural defects as summarised in Table 3 and further discussed below in subsections 9.1 to 9.4.

434

435 9.1. Formation of visible particles

436

Lumpiness (the presence of large protein aggregates) adversely affects the texture of 437 438 fermented milk products. This occurs due to high incubation temperature, extreme whey protein to casein ratio and certain types of starter bacteria (Lucey & Singh, 1997). Sonication during 439 fermentation was also reported to induce the formation of lumps (d > 0.9 mm) in stirred voghurt 440 (Körzendörfer, Nöbel, & Hinrichs, 2017; Nöbel, Protte, Körzendörfer, Hitzmann, & Hinrichs, 441 2016a; Nöbel et al., 2016b). Two possible mechanisms demonstrated for this are (i) lower zeta 442 potential associated with low pH conditions (below 5.4) may enhance the formation of new 443 bonds and (ii) the disruption of casein-whey protein complexes that exposes thiol-groups in 444 whey proteins may enhance cluster formation (Körzendörfer et al., 2017; Nöbel et al., 2016b). 445 According to the observations made by Nöbel et al. (2016b), sonication of a stirred yoghurt 446 sample during fermentation (pH 5.4–5.3) using US (40 KHz, 17 kW m⁻³, 5 min) increased the 447 size of large visible particle from 1.25 mm to 1.65 mm. Additionally, the number of particles per 448

100 g was increased from 506 to 2360 over the same pH range. These colloidal particles within
the yoghurt gel structure were felt as soft grains and were broken up by subsequent low pressure.
The oscillations themselves may induce particle formation as demonstrated by Körzendörfer,
Temme, Schlücker, Hinrichs, and Nöbel (2018) who observed lumpiness in set yoghurts along
with the vibrations (25–1005 Hz) during the gelation, probably due to the increase in collision
probability of aggregating milk proteins.

Sonication-induced lumpiness in fermented milk gels was influenced by several other 455 conditions such as pH, dry matter (DM) content and the type of starter culture used 456 (Körzendörfer et al., 2017). Moreover, sonication-induced lumpiness was observed only within 457 the pH range of 5.4 to 5.1 which is known as the "critical pH range" (Nöbel et al., 2016b). Over 458 this range, the whey proteins attached to the surface of casein micelles reach their isoelectric 459 point, resulting in lump formation. However, sonication may cause reversible interaction within 460 particles above pH 5.4 and casein micelles were not affected by sonication below pH 5.1 since 461 they may already be stabilised within the gel network. Fig. 4 illustrates the macroscopic 462 transmission images of stirred yoghurt gels sonicated at 40 KHz and energy density of 17 kW m⁻ 463 ³ for 5 min under different pH values during fermentation. 464

However, stirred-milk gels with low DM content were more susceptible to sonicationinduced lump formation, whereas milk gels with DM content of more than 14.2% were not affected by sonication under any pH condition tested (Nöbel et al., 2016a). Therefore, fermented gels produced from sheep and buffalo milk, which have higher dry matter content compared with cow milk, might give different results on sonication-induced lumpiness, but this has not been reported to date. In addition, Körzendörfer et al. (2017) observed that LAB with high levels of exopolysaccharide production reduced the formation of large particles. This may be due to the

attachment of exopolysaccharides to casein particles that makes an incompatibility between the

472

473	exopolysaccharides and casein-modified gel structure, and thus behave as spacers to reduce the
474	lump formation (Körzendörfer et al. (2017).
475 476	9.2. Whey separation and syneresis
477	
478	Whey separation can be defined as the presence of whey (milk serum) on the surface of
479	acid milk gels mainly due to the shrinkage of the gel (syneresis) (Lucey, 2004). Conditions that
480	result in whey separation in cultured products are high incubation temperature, extreme whey
481	protein to casein ratio, low solids content and physical mishandling of the products. In addition,
482	fermented gels produced from milk with a high number of larger fat globules, such as buffalo
483	milk, showed porous gel network and thus excessive whey separation (Nguyen, Ong, Kentish, &
484	Gras, 2015).
485	Sonication improved WHC and reduced the syneresis of set yoghurts and fermented
486	beverages. Wu et al. (2001) observed a prominent increase in WHC when the cow milk was
487	treated with US (20 kHz, 225–450 W) for 6–8 min at 15 °C compared with the yoghurt obtained
488	through conventional homogenisation. Comparable findings were reported by Erkaya et al.
489	(2015) who showed that the thermosonication (60-80 °C, 35 KHz, 1-5 min) of a fermented
490	beverage called "Ayran" on the day following that of production reduced serum liberation by
491	31% compared with heat treatment at 90 °C for 1 min. This was further verified by Vercet et al.
492	(2002) using manothermosonication (117 μ m amplitude, 20 kHz frequency, and 2 kg cm ⁻²

493 pressure) of cow milk for the production of set yoghurts; syneresis was reduced by 14.8%

494 compared with the control that was thermised at 60 °C for 15 s and homogenised.

The effect of US over conventional homogenisation on whey separation and syneresis 495 may be due to sonochemistry effects, mainly towards the milkfat globule (MFG) and milk 496 proteins. US improves WHC through strong cavitation and results in a greater rupturing of the 497 MFG compared with conventional pressure milk homogenisation that subsequently increased the 498 surface area of MFG and the associations with the caseins. Moreover, US causes modifications 499 to the structure of both β -lactoglobulin and α -lactalbumin, which are the major whey proteins in 500 501 bovine milk. Chandrapala, Zisu, Kentish, and Ashokkumar (2012) reported that whey proteins 502 are unfolded into monomeric units due to partial cleavage of intermolecular hydrophobic interactions either reversibly or irreversibly depending on the intensity of the US treatment. 503 504 Shanmugam, Chandrapala, and Ashokkumar (2012) observed that these partially denatured whey proteins were aggregated among themselves or with other free caseins, mainly κ -caseins, to form 505 aggregates upon US treatment at 20 kHz and 20 W for up to 60 min. These soluble aggregates 506 507 further interacted with casein micelles to form micellar aggregates by thiol-disulphide exchange reactions between the denatured whey proteins and the κ -caseins of the micelles. The significant 508 increase in the surface area of MFG upon sonication enhanced the association of modified whey 509 proteins and casein micelle with the MFG membrane (Nguyen & Anema, 2017). As a result, 510 thiol groups and the hydrophobic regions of amino acids are exposed toward water molecules in 511 the surrounding environment. This enhanced the WHC of the milk proteins and serum liberation 512 was reduced. Nevertheless, pasteurisation and other intense heat treatments that were often 513 accompanied with milk before or after the US treatment may cause considerable changes to the 514 serum proteins and thus alter the WHC; this is poorly described in the literature. 515 516 However, both prolonged sonication and mechanical disturbances during gel formation

517 has been reported to have a negative impact on gel formation and WHC (Körzendörfer et al.,

2017, 2018; Zhao et al., 2014). Moreover, prolonged sonication led to dissociation of whey

519	proteins from micellar aggregates (Shanmugam, Chandrapala, & Ashokkumar, 2012). Similarly,
520	prolonged sonication (20 KHz, 20 W, for 30 min) reduced the size of MFG where the surface
521	available for aggregation was further decreased, which resulted in a weak gel network with
522	greater syneresis (Zhao et al., 2014). Moreover, it was reported that low frequency vibrations
523	(1000 Hz) during the early stages of gelation results in considerable loss of structure and a weak
524	body, leading to further occurring of syneresis (Körzendörfer et al., 2018).
525	
526	9.3. Texture
527	
528	Textural properties are typically related to the structure of the milk gel. Structure of set-
529	yoghurt is established through crosslinking of κ -casein on the surface of casein micelles with
530	denatured whey proteins, mostly β -lactoglobulin, which entraps the MFG and milk serum
531	(Lucey, 2004). Shear stress and the temperature rise during sonication resulting in a significant
532	modification in the physicochemical properties of macromolecules such as milk fat and protein
533	and thus alter the consistency and textural properties of fermented milk products. Sonication
534	reportedly has a significant reduction in the size of MFG and proteins compared with pressure
535	homogenisation; Nguyen and Anema (2017) observed a decline of the diameter of MFG from
536	375 nm to 200 nm during the first 5 min of the US treatment (22.5 kHz and 50 W) of bovine
537	milk (18 g). Moreover, Nguyen and Anema (2010) reported a reduction in the size of casein
538	micelles by about 10–20 nm during the sonication of skimmed milk at 60–70 °C for 5 min due to
539	the solubilisation of κ -casein and denaturation of whey proteins. Therefore, it is anticipated that
540	the structure of milk gels, which greatly relies on the nature of MFG and the denaturation and

541 aggregation state of proteins, and thus the textural properties of milk gels, will be affected upon US treatment (Ahmed, Ramaswamy, Kasapis, & Boye, 2009). 542

- Several researchers have found that high amplitude sonication applied either before or 543 after inoculation of starter cultures significantly increases the viscosity and firmness of set 544 yoghurt (Nguyen & Anema, 2010; Riener et al., 2010; Sfakianakis et al., 2015). This was mainly 545 due to the homogenisation of MFG and denaturation of serum proteins by US treatment (Abbas 546 547 et al., 2013; Nguyen & Anema, 2017). The substantial reduction of the size of MFG may 548 facilitate the integration of fat into the protein network, while their increased surface area by more than 50% favours the crosslinking between fat and unfolds the peptide chains of whey 549 550 proteins and subsequent formation of whey-whey and whey-casein aggregates, during gel formation (Nguyen & Anema, 2017; Shanmugam et al., 2012). It can be assumed that the 551 formation of soluble aggregate between denatured whey proteins and casein micelles leads to an 552 553 increase in viscosity. Moreover, denatured whey proteins have reduced repulsive charges and therefore, easily aggregate. These denatured whey proteins associated with casein micelles may 554 act as bridging material between casein micelles and thus firmer yoghurt gels were formed 555 easily. This effect is conventionally achieved by heating the milk before fermentation to higher 556 temperature such as 90 °C for 5–10 min. 557
- Similarly, manothermosonication was reported to increase the viscosity and firmness of 558 set-gels (Vercet et al., 2002). This might be due to some modification to the MFG membrane 559 upon manothermosonication where the interactions in between MFG and/or casein micelles were 560 enhanced. However, based on their findings, Nguyen and Anema (2010) concluded that most of 561 562 the benefit from US treatment over the modification of texture properties was due to the heat generated, and non-thermal effects of sonication resulted in minor improvements over 563

564	conventional heating. A contradictory observation was made by Riener et al. (2010) who
565	indicated that a different kind of molecular interaction may occur during gelation of
566	thermosonicated milk rather than the denaturation of whey proteins and this was responsible for
567	the viscosity modification compared with conventional heat treatment. This hypothesis was
568	further confirmed by the subsequent findings of the same author that thermosonication of 200
569	mL full-fat milk for 10 min at 400 W led to more whey protein denaturation compared with
570	heating at 90 °C for 10 min (52.2% versus 28.1%).
571	Furthermore, US homogenisation showed considerably different impact towards the
572	texture of set-gels compared with conventional pressure milk homogenisation. Sfakianakis et al.
573	(2015) observed a significant increase of the final viscosity of set yoghurts with US
574	homogenisation (20 KHz, 562 and 750 W, and 500 mL) compared with two-stage pressure milk
575	homogenisation (30 and 5 MPa). They suggested that US treatment caused whey proteins to
576	denature and both self-aggregate and aggregate with casein micelles and form insoluble high
577	molecular weight material, whereas no significant change in the soluble protein content was
578	observed with pressure homogenisation. Apparently, the US treated milk sample was exposed to
579	a strong heating as sonication itself increased the temperature up to 87 °C in addition to the
580	subsequent heating to 80 °C for 20 min compared with pressure homogenisation that had only
581	the latter heat treatment. This extensive heating of US treated milk may result in comparatively
582	higher denaturation of proteins and was not described by the authors.
583	Scanning electron microscopic analysis revealed that the set-gels produced from
584	thermosonicated milk (45 °C, 10 min, frequency 24 kHz) showed a honeycomb-like structure

untreated milk gels (Riener et al., 2010). As a result, the gel texture and viscosity were improved

585

where casein micelles were more interconnected and the pores were larger compared with the

587	in ultrasonicated milk gel sample. Untreated milk gels showed highly cross-linked network					
588	structure and few pores were interspaced throughout the gel structure. However, ultrasonication					
589	during gelation reduced the strength of stirred-milk gels and Körzendörfer et al. (2017) observed					
590	a reduction in 28% of the maximum force required to puncture the gel. Accordingly, it can be					
591	concluded that US was an alternative to homogenisation and heat treatment in yoghurt					
592	production, modifying the textural properties of yoghurts mainly through modifications to MFG					
593	and milk proteins. However, the degree of the modifications to fat and protein were significantly					
594	different as a result of US compared with the conventional method, possibly due to the					
595	sonochemistry effects associated with the US.					
596						
597	9.4. Sensory attributes					
598						
599	Effect of thermosonication on the colour of Ayran was recently investigated by Erkaya,					
600	Başlar, Şengül, and Ertugay (2015). It was found that fermentation of Ayran followed by					
601	thermosonication at 80 °C for 5 min caused a slight reduction in L* value (lightness in Lab					
602	colour space) compared with heat treatment for 1 min at 90 °C. Significant loss of L* in Ayran					
603	may be due to the acceleration of non-enzymatic browning and the structural changes in milk					
604	proteins due to heat and low pH conditions. However, the b* (colour opponents blue-yellow in					
605	Lab colour space) value was significantly increased when the duration and temperature of					
606	thermosonication increased. However, they have not reported the influence on other sensory					
607	attributes such as the flavour of the product.					
608	Similarly, several authors reported that US alters the sensory quality of fresh milk					
609	(Chouliara, Georgogianni, Kanellopoulou, & Kontominas, 2010; Marchesini et al., 2012, 2015).					

610	A recent study was conducted by Marchesini et al. (2015) on the generation of volatile					
611	compounds in US treated milk; it was found that ultrasonication of 100 mL milk under 24 kHz					
612	and 160.4 J s ⁻¹ power intensity for more than 100 s led to the production of volatile compounds,					
613	mainly, dodecanoic acid, octanoic acid, δ -dodecalactone and decanoic acid methyl ester. These					
614	compounds were responsible for the metallic, burnt, rubbery and sharp off-flavours in milk upon					
615	sonication. Hence, it was suggested that ultrasonication beyond 100 s was not appropriate for					
616	milk that is intended for direct consumption. Comparable results were reported by Riener, Noci,					
617	Cronin, Morgan, and Lyng (2009) and Chouliara et al. (2010), showing that ultrasonicated					
618	pasteurised milk resulted in a "rubbery" odour and "burnt" and "foreign" off-taste. However,					
619	Vercet et al. (2002) founded that this offensive "cooked" flavour distinguished during					
620	manothermosonication of milk, was not detectable when the milk was fermented into set-					
621	yoghurts. This might be due to the masking of "cooked" flavour by the flavour compounds					
622	generated through fermentation. As yet, the impact of ultrasound assisted fermentation on the					
623	synthesis of flavour compounds by LAB has not been reported in the literature.					
624						
625	10. Assessment of realistic conditions used for ultrasonication of fermented dairy					
626	products					
627						
628	US has numerous applications in the dairy industry, such as particle size reduction,					
629	monitoring of the fermentation process, reduction of the fermentation time, etc. Thus, the					
630	appropriate frequency, amplitude and exposure time of the US treatments should be carefully					
631	determined for each unique application. The frequency of US could be easily controlled in					
632	acoustic experiments since the US apparatus generates vibration at the set frequency. In					

comparison, the intensity of US is difficult to control during experiments because the milk 633 particles close to the emitter of the sonicator typically have greater pressure oscillations 634 compared with the particles further away as energy is dissipated as heat. Moreover, this effect is 635 enhanced by the bulk mixing of the particles during cavitation, resulting in an uneven exposure 636 of particles to US. Hence, it was suggested that the amount of particle mixing should be 637 considered together with the intensity and exposure time in US treatments (Leong, Martin, & 638 639 Ashokkumar, 2018). Similarly, the acoustic energy intensity is reported differently in the 640 experiments in the literature. Some sonicators displayed the energy intensity (total energy drawn by the ultrasonic device per unit volume of material processed in $J m L^{-1}$) whereas, in others, it 641 642 was calculated using the amplitude of US, the surface area of the emitter and the treatment time. However, a particular energy density can be attained by treating the sample for a long time with 643 a low level of amplitude or short time duration using high level of amplitude. This may bring 644 645 about different extents of physical and chemical changes in the milk and thereby variation in chemical alterations or degradation in the fermentation milieu. Moreover, the chemical and 646 physical effects of US depend on the properties of the medium. The viscosity and the density of 647 the medium greatly affect the speed and the intensity of the pressure (Leong et al., 2018). 648 Therefore, compositional variation among the milk samples used for the US experiments may 649 have a considerable impact on the results obtained. 650

651

Feasibility of using ultrasound technology in industrial-scale production processes

654 The effectiveness of US to enhance or replace different food processes such as 655 emulsification, homogenisation, extraction, crystallisation, freezing, meat tenderisation,

dewatering, low temperature pasteurisation, deforming, activation and inactivation of enzymes,
particle size reduction and viscosity alteration have been investigated by several authors (WeltiChanes, Morales-de la Peña, Jacobo-Velázquez, & Martín-Belloso, 2017). A recent approach
was to enrich plant foods with bioactive compounds by the induction of stress conditions using
US (Del Rosario Cuéllar-Villarreal et al., 2016).

Advantages of high-powered US over conventional processes are higher product yields, 661 662 shorter processing times and improved product characteristics (Patist & Bates, 2008). However, the main technological limitations that makes the scaling-up of laboratory applications of US in 663 to industrial scale is the increase of the US horn diameter without reducing the vibration 664 665 amplitude (Kiss et al., 2018). In industrial applications, a larger horn diameter is preferred to produce a larger cavitation zone. However, recent findings on "Barbell horns" shed light upon 666 the scaling-up of US devices where the diameter of the horn and the amplification of US were 667 668 simultaneously improved without any undesirable effect on the product quality (Peshkovsky, 2017). 669

In addition, overheating of transducers during continuous processing and poor uniformity are other restrictions. This limitation can be overcome by using an appropriately designed reactor chamber that guarantees the direction of the liquid to be treated through the cavitation zone without bypassing. Moreover, a suitable temperature control and/or cooling system should be installed to the reactor chamber. Peshkovsky (2017) suggested that process efficiency of scaledup US processors could be enhanced by mounting several US devices in a series or two Barbell horns on to a common reactor chamber.

677 However, there are several unsettled scale-up challenges, such as irregular cavitation field678 distribution during the installation of transducers on curved surfaces that may be essential for

distillation columns (Kiss et al., 2018). The employment of US technology to the food industry

679

680	still faces considerable challenges mainly due to the limitations in conventional US processes				
681	that have partly been resolved with the invention of the Barbell horn. Nevertheless, further				
682	improvements with precise construction procedures and methods may accelerate the adoption of				
683	US in the commercial setting.				
684					
685	12. Summary and future perspectives				
686					
687	US technology has been employed in dairy streams to intensify fermented milk product				
688	processing by reducing the processing time, minimising ingredient and additive requirements and				
689	lowering the resources required. Production of acid milk gels having good gel strength, smooth				
690	body and texture and little or no syneresis without using hydrocolloid stabilisers is a challenging				
691	task in the industry. Use of US has proved to be a good alternative for stabilisers in fermented				
692	milk gels. Further, US treatment minimised the requirement of milk solids that are usually				
693	incorporated into the raw milk to strengthen the yoghurt gel. Moreover, US treatment has been				
694	reported to shorten the fermentation time of milk through enhancing the metabolic activity of				
695	LAB. Meanwhile, it was noted that different bacterial species showed different responses to the				
696	US treatment. For example, Streptococcus sp. form longer chains than Lactobacillus sp. under				
697	US influence. Therefore, it is important to re-define optimum growth conditions such as				
698	temperature and inoculation rates for the US treated LAB starter cultures for fermented milk				
699	products; this needs further investigation. Moreover, power US may be a useful tool to overcome				
700	most of the inherent defects associated with buffalo yoghurt, which is significantly more				
701	thixotropic and exhibits greater syneresis and poorer structural stability than that made from				

702	bovine milk. However, this could be achieved if the process parameters of sonication such as
703	frequency, acoustic intensity and pressure are carefully selected. Hence, the optimisation of
704	sonication parameters to get desirable gelation and fermentation kinetics warrant further studies.
705	
706	Acknowledgements
707	
708	This work was supported by the University Grant Commission, Sri Lanka (grant number:
709	UGC/DRIC/QUT2016/UWU/01), Queensland University of Technology, Australia and
710	Queensland Government Advanced Queensland Fellowship (AQF).
711	
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Figure legends

Fig. 1. Main components of laboratary-scale ultrasound devices: (a) ultrasound probe; (b) ultrasound bath.

Fig. 2. Transmission electron micrographs of *Lactobacillus acidophilus* untreated (a) and ultrasonicated (b–d); bar = 1000 nm. Adapted from Cameron, McMaster, and Britz (2008).

Fig. 3. Growth curve of *Lactobacillus casei* subsp. *casei* ATTC 39392 in MRS broth treated with ultrasound (\blacklozenge ; amplitude 60%, 15 s, 10 g L⁻¹ peptone) and control sample without ultrasound (\blacksquare): (a) OD₆₀₀ nm; (b) bacterial counts. Adapted from Dahroud et al. (2016)

Fig. 4. Transmission images of stirred yoghurt samples sonicated at different pH values during fermentation. Average sample mass: 13 g; average layer thickness: 1.2 mm. Adapted from Nöbel et al. (2016a).

Table 1

Application of high-intensity US to lactic fermentation of milk.

Applications	Ultrasonic conditions	Type of bacteria and growth medium	Main effects observed	References
Accelerate lactic acid production	50 mL sample was sonicated at amplitudes of 20%, 40% and 60% for 15, 30 and 45 s every 2 h during fermentation using an ice bath	<i>Lb. casei</i> subsp. <i>casei</i> ATTC 39392 in permeate powder medium (Pegah Co.,Tabriz, Iran)	Increased production of lactic acid, cell reproduction and substrate consumption Increased growth indexes (specific growth rate and logarithmic phase duration) Increased the membrane permeability (3%)	Dahroud et al. (2016)
Stimulate milk fermentation of bifidobacteria	100 mL of inoculated milk was sonicated before fermentation at 100 W, 20 kHz for 7 min., 15 min. and 30 min. using an ice bath, energy density 420, 900 and 1800 J mL ⁻¹	B. breve ATCC 15700, B. infantis, B. longum (BB-46) and B. animalis ssp. lactis (BB-12) in skim milk	Reduced fermentation time for <i>B. breve</i> , <i>B. infantis</i> and BB-12 Promoted growth of bifidobacteria Lower the lactose concentration and higher the amount of oligosaccharides Increased the activity of β -galactosidase	Nguyen, Lee, and Zhou (2009)
Enhance cell production of lactic and propionic acid bacteria for industrial purposes	Sonication during fermentation using a fermenter with a flow rate of 10 mL s^{-1} at 880 kHz and 0.1–0.7 W cm ⁻³ for 100–120 s	<i>Lc. lactis</i> (VPKM B-2092), <i>Lb. plantarum</i> (VPKM B-4173), and <i>Prop. acidipropionici</i> (VPKM B-2092) under submerged cultivation	Increased the biomass of cells producing lactic and propionic acid	Durnikin, Silantyeva, and Ereshchenko (2016)
Whey fermentation with selected dairy cultures	Sonication of cultures before inoculation at 84 W and 102 W for 75 s and 150 s with a 12 mm diameter probe and frequency of 20 kHz. Sonication temperatures: 37 °C for La-5 and 43 °C for YC-380	Str. thermophilus, Lb. delbrueckii subsp. bulgaricus and Lb. acidophilus (La-5) in thermosonicated whey (480 W, 8 min, 55 °C)	Shorter time of fermentations Increased viable cell count Improved sensory properties	Barukčić, Jakopović, Herceg, Karlović, and Božanić (2015)
Kinetics of sugar and organic acid production during milk fermentation	100 mL of inoculated milk sonicated before fermentation with 20 kHz and an amplitude of \approx 100 W for 7 min, 15 min and 30 min at 30–40 °C; energy density 420, 900 and 1800 J mL ⁻¹	B. breve ATCC 15700, B. infantis, B. longum (BB-46) and B. animalis ssp. lactis (BB-12) in skimmed milk	Accelerated lactose hydrolysis and accelerate transgalactosylation Decreased acetic acid: lactic acid Decreased total acetic and propionic acids: lactic acid	Nguyen, Lee, and Zhou (2012)
Isoflavones bioconversion ability of lactobacilli in biotin- supplemented soymilk	10 mL sample sonicated at 30 kHz, 20 W, 60 W and 100 W for 60, 120 and 180 s before inoculation with a 3 mm diameter sonotrode; energy density 120–1800 J mL ⁻¹	<i>Lb. acidophilus</i> (BT 1088), <i>Lb. fermentum</i> (BT 8219), <i>Lb. acidophilus</i> (FTDC 8633) and <i>Lb. gasseri</i> (FTDC 8131) in soy milk	Induced lipid peroxidation Increased membrane fluidity and permeability Increased growth Enhanced β-glucosidase activity of lactobacilli Promoted bioconversion of glucosides to aglycones in soymilk	Ewe, Abdullah, Bhat, Karim, and Liong (2012)

Yoghurt fermentation	150 mL of inoculated milk sonicated before fermentation at 20 kHz and 450 W, 225 W and 90 W for 1, 6 and 10 min. using a 13 mm diameter probe; energy density 36–1800 JmL ⁻¹	Str. thermophilus, Lb. bulgaricus, Bifidobacterium and Lb. acidophilus in cows' milk	Faster acid development Increased water holding capacity Decreased syneresis Decreased fermentation time	Wu, Hulbert, and Mount (2001)
Lactose hydrolysis and the cell viability of lactic acid bacteria in sonicated fermentation	Sonication during fermentation using a 400 cm ³ fermenter at 200 kHz, 135 W and 17.2 kW m ^{2} for 30 min, 37 °C	Lb. delbrueckii subsp. bulgaricus B-5b, Lb. helveticus LH-17, Lb. delbrueckii subsp. lactis SBT-2080 and Lb. acidophilus SBT- 2068 in reconstituted non-fat dry milk	Lower viable cell counts Higher total β -galactosidase activity High degree of lactose hydrolysis	Wang and Sakakibara (1997)
Enhancement of lactose hydrolysis by sonication to produce hydrolysed lactose fermented milk	Sonication during fermentation using a 500 cm ³ fermenter at 200 kHz, 135 W and 17.2 kWm ² for 30 min, 37 °C	<i>Lb. delbrueckii</i> subsp. <i>bulgaricus</i> B-5b in 10% (w/v) non-fat dry milk	Released intracellular β -galactosidase Higher lactose hydrolysis activity Decreased cell viability	Wang, Sakakibara, Kondoh, and Suzuki (1996)
Compare ultrasonic homogenisation and conventional homogenisation on fermentation kinetics	500 mL milk sample sonicated before inoculation at 20 kHz and output power of 150, 262, 375, 562, and 750 W for 10 min without temperature control using a 13 mm probe; energy density180–900 J mL ⁻¹	Str. salivarius subsp. thermophilus and Lb. delbrueckii subsp. bulgaricus in skimmed bovine milk	Low pH reduction rate Low duration of pH lag phase Higher coagulum viscosity Formation of protein molecule aggregates	Sfakianakis et al. (2015)
Investigate the correlation between exopolysaccharide synthesis ability of starter cultures and the effect of sonication during fermentation of yoghurt	100 mL milk sample sonicated during fermentation using an ultrasonic bath (35 kHz, 300 W) for 5 min.	Lb. delbrueckii ssp. bulgaricus and Str. thermophilus in skimmed cows' milk	Induced syneresis in set-gels Increased particle numbers under low exopolysaccharide production	Körzendörfer, Nöbel, and Hinrichs (2017)
Effect of different ultrasonic frequencies on fermentation kinetics of Kefir	500 mL milk sample was sonicated during fermentation using an ultrasonic bath at four 28, 40, 100 and 200 kHz and 14 kPa sound pressure at 30 °C	Str. lactis, Str. cremoris, Streptococcus diacetylactis, Leu. cremoris, Lb. plantarum and Lb. casei in cows' milk	Fermentation time shortened exponentially with frequency	Shimada, Ohdaira, and Masuzawa (2004)
Effect of mild sonication intensities at different temperatures	500 mL of cultures were sonicated before inoculation at 20 kHz and 8.07, 14.68, 19.83 and 23.55 W cm ⁻² at 4, 22 and 40 °C	<i>Lb. delbrueckii</i> ssp. <i>bulgaricus</i> LB-12 in skimmed milk	14.68 W cm ⁻² improved the bile tolerance, growth and protease activity	Moncada, Aryana, and Boeneke (2012)
Effect of the presence of Na^+ and K^+ ions on the stability and enzyme activity of sonicated cultures under various temperature and pH levels	50 mL of inoculated milk sample was sonicated at 75 W for 4 min. using a 19-mm probe in an ice water bath; energy density 360 J mL ⁻¹	<i>Lb. delbrueckii</i> ssp. <i>bulgaricus</i> LB 11842 in skimmed milk	Stability of the β -galactosidase activity in sonicated cultures was higher in K+ Enzyme was relatively stable at all pH levels at 25 °C Stability of the enzyme higher at pH 6 and 7 under 51 and 56 °C	Kreft and Jelen (2000)
Impact of sonication on lactose hydrolysis	5 mL of milk was sonicated during fermentation at 20 KHz for 20 min, 0	Lb. delbrueckii subsp. bulgaricus B-6, Lb. delbrueckii subsp. bulgaricus B-5b or Lb.	Higher glucose level 71–74% of the initial lactose was hydrolysed	Toba, Hayasaka, Taguchi, and Adachi (1990)

	°C	helveticus LH-17 in milk	Increased syneresis	
Influence of sonication before fermentation on the properties of acid milk gels of skimmed milk	18 g of milk was sonicated before inoculation at 22.5 kHz and 50 W up to 30 min. with (20–70 °C) and without temperature control; energy density 5000 J g^{-1}	Str. thermophilus Lb. delbrueckii subsp. bulgaricus in skimmed milk	Increased in firmness (final G') Whey proteins denaturation Reduced casein micelle size κ-Casein dissociated from the micelles	Nguyen and Anema (2010)
Comparison of traditional heat treated and thermosonicated milk in terms of their gelation properties	Milk was sonicated before inoculation at 24 kHz and 400 W for 10 min. with a 22 mm diameter tip at 45 $^{\circ}$ C	Yogotherm yoghurt culture 77570 in skimmed milk	Higher gelation pH Firmer structure Honeycomb-like microstructure Low storage modulus (G [°])	Riener et al. (2010)
Intensify the fermentation process of cows' milk	25 mL of milk sonicated at the beginning and after 2 h fermentation using a 2.5 mm probe for 1–3 min.; 30 kHz and from 2 W to 8 W; energy density 4.8–57.6 J mL ⁻¹	Lc. lactis subsp. lactis, Lc. lactis subsp. cremoris	Accelerated fermentation process by 10% Increased shelf-life Reduced syneresis Increased viscosity Enhanced thixotropic properties and structure characteristics	Shershenkov and Suchkova (2015)
		REPAR		

Table 2

Growth and viability of LAB upon US treatment.

Treatment conditions	Types of LAB/microorganisms	Observed effects on VCC and growth	References
40 mL milk sample sonicated with a 13 mm probe at 20 kHz, 750 W for 10 min after inoculation; 24–26 $^{\circ}$ C; energy density 11.25 kJ mL ⁻¹	Lb. acidophilus	Reduced by log ₁₀ 0.82	Cameron et al. (2008)
100 mL of whey was thermosonicated with 12 mm probe; 20 kHz, 480 W and 85 Wcm ⁻² for 8 min, 55 $^{\circ}$ C; energy density 2.3 kJ mL ⁻¹	Total plate count	Reduced by log ₁₀ 2	Barukčić et al. (2015)
100 mL pasteurised whey with 0.08% (w/v) culture was treated with 12 mm probe sonicator at 20 kHz and 84 W for 150 S before inoculation under 43 °C; energy density 0.126 kJ mL ⁻¹	Streptococcus thermophilus Lb. delbrueckii subsp. bulgaricus	Increased by log ₁₀ 2	Barukčić et al. (2015)
Continuously sonication of the cell suspension at 880 kHz and 0.3-0.5 W cm $^{-3}$ for 100-120 s	Lc. lactis, Lb. plantarum, Prop. acidipropionici	Increased viability by 28.6, 9, and 16.7 times respectively	Durnikin et al. (2016)
50 mL sample sonicated at an amplitude of 60% for 15 s every 2 h during fermentation using an ice bath	Lb. casei subsp. casei	Increased biomass production and substrate consumption by $\approx 25\%$	Dahroud et al. (2016)
10 mL cell suspension sonicated with 3 mm probe at 30 kHz, 20 W, 60 W and 100 W for 60, 120 and 180 s before fermentation; energy density $0.12-1.8$ kJ mL ⁻¹	Lb. acidophilus, Lb. fermentum, Lb. gasseri	Increased viable counts by >9 $_{log}$ cfu mL ⁻¹ with higher amplitudes and longer durations whereas the low amplitude of short duration decreased in viability	Ewe et al. (2012)
100 mL inoculated milk treated at 20 kHz and 50 W for 7–30 min and 40 °C before fermentation; energy density $0.21-0.9$ kJ mL ⁻¹	B. breve, B. infantis, B. longum, B. animalis ssp. lactis	Cell counts reduced with the processing time	Nguyen et al., 2009
Sonication while fermentation using a 400 cm ³ fermenter at 200 kHz, 135 W and 17.2 kW m ⁻² for 30 min, 37 °C	Lb. delbrueckii subsp. bulgaricus Lb. helveticus, Lb. delbrueckii subsp. lactis, Lb. acidophilus	Cell viability decrease in the later period of sonicated fermentation sonication.	Wang and Sakakibara (1997)
Sonication while fermentation using a 400 cm ³ fermenter at 200 kHz, 135 W, 17.2 kW m ⁻² , 37–39 °C for 30 min followed by the incubation in static state (without sonication, agitation and pH control)	Lb. delbrueckii subsp. bulgaricus Lb. helveticus, Lb. delbrueckii subsp. lactis, Lb. acidophilus	Cell viability increased during the static incubation	Wang and Sakakibara (1997)

Table 3

Impact of US on sensory attributes of fermented dairy products.

Product	Type of starter culture	Sonication equipment	Sonication condition	Properties after sonication	Reference
Set yoghurt and stirred- yoghurt	Lb. delbrueckii ssp. bulgaricus, Str. thermophilus	Ultrasonic water bath (RK 1028/ H; Bandelin electronic GmbH& Co. KG, Berlin, Germany)	35 kHz and 300 W for 5 min at 42 °C during fermentation	Set yoghurt: Increased syneresis Reduced firmness Stirred yoghurts: Increased large particles (d > 0.9 mm) Higher viscosity	Körzendörfer et al. (2017)
Stirred yoghurt	Yo-Mix 215 YC-471 (Danisco Deutschland GmbH, Niebull, Germany)	Ultrasonic water bath (USC1200TH, VWR International GmbH, Darmstadt, Germany)	45 kHz, 200 W and 17 kW m ⁻³ for 5 min at 42 °C during fermentation	Increased large particles	Nöbel et al. (2016b)
Set yoghurt	Str. thermophilus, Lb. bulgaricus	Piezoelectric source, Hielscher, Germany	20 KHz, 30 min before fermentation	Improved the gel texture Improved viscosity Decrease in milk turbidity and lightness	Tabatabaie, Mortazavi, and Ebadi (2009)
Set yoghurt	Str. thermophilus, Lb. bulgaricus, Bifidobacterium, Lb. acidophilus	Model CP502, Cole-Parmer Instrument Company, USA	150 mL inoculated milk sonicated before fermentation at 20 kHz and 450 W for 8 min using a 13 mm diameter probe; energy density 1.44 kJmL ⁻¹	Reduce syneresis Improve viscosity	Wu et al. (2001)
Ayran (fermented milk drink)	Str. thermophilus Lb. bulgaricus	Ultrasonic bath; Model No. RK103H, Bandelin, Berlin, Germany	300 mL sample treated at 35 kHz and 60–80 °C for 1, 3 and 5 min	Increased the viscosity Decreased serum separation Whiter in colour	Erkaya, Başlar, Şengül, and Ertugay (2015)
Set yoghurt	YBCN 143	Branson 450 sonicator	Manothermosonication of 6 mL milk circulated and treated at 32 mLmin ⁻¹ , 20 kHz and 12 s under 2 kg cm ⁻² pressure, 40 °C	Firmer structure Improved texture Higher gumminess and chewiness Less structure loss upon compression	Vercet et al. (2002)
Stirred yoghurt	Yo-Mix 215 (Danisco Deutschland GmbH, Niebull, Germany)	Ultrasonic bath (RK1028H; Bandelin electronic GmbH & Co. KG, Berlin, Germany	100 mL milk sample sonicated at 35 kHz, 300 W, 15 Wm ⁻³ at 42 °C for 5 min during fermentation; energy density 0.9 kJmL ⁻¹	Induced the formation of large particles, no significant effect of the sonication to the yoghurts above 14.2% dry matter	Nöbel, Protte, Körzendörfer, Hitzmann, and Hinrichs (2016a)









Figure 4.