- 1 A novel split cycle internal combustion engine with integral waste heat recovery
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- 6 Keywords
- 7 Split cycle
- 8 Isothermal compression
- 9 Isobaric combustion
- 10 Heat recuperation
- 11 Waste heat recovery
- 12 Abstract

13 To achieve a step improvement in engine efficiency, a novel split cycle engine concept is proposed. 14 The engine has separate compression and combustion cylinders and waste heat is recovered 15 between the two. Quasi-isothermal compression of the charge air is realized in the compression 16 cylinder while isobaric combustion of the air/fuel mixture is achieved in the combustion cylinder. 17 Exhaust heat recovery between the compression and combustion chamber enables highly efficient 18 recovery of waste heat within the cycle. Based on cycle analysis and a one-dimensional engine 19 model, the fundamentals and the performance of the split thermodynamic cycle is estimated. 20 Compared to conventional engines, the compression work can be significantly reduced through the 21 injection of a controlled quantity of water in the compression cylinder, lowering the gas temperature 22 during compression. Thermal energy can then be effectively recovered from the engine exhaust in a 23 recuperator between the cooled compressor cylinder discharge air and the exhaust gas. The resulting 24 hot high pressure air is then injected into a combustor cylinder and mixed with fuel, where near 25 isobaric combustion leads to a low combustion temperature and reduced heat transferred from the 26 cylinder wall. Detailed cycle simulation indicates a 32% efficiency improvement can be expected 27 compared to the conventional diesel engines.

#### 28 1. Introduction

29 The internal combustion engine (ICE) has been the incumbent power source for road transport 30 applications for over 100 years. The high power density, good transient response and low cost make 31 the ICE an excellent fit with the needs of road vehicles in an environment with an abundant supply of 32 low cost liquid fossil fuels [1-3]. However, climate change and diminishing stocks of petroleum have 33 led to a drive for higher efficiency solutions [4, 5]. Alternative power converters such as fuel cells and 34 batteries and increased electrification of the transmission between the prime mover and the wheels 35 and downsizing of the ICE have also been proposed to improve the vehicle system performance [6]. 36 Fuel cells and electrification are attractive for the passenger cars, but the high load factor of 37 commercial vehicles is particularly challenging to such alternative powertrains [7, 8]. Recent research 38 [9] has shown improvements to the thermal efficiency of the ICE offers the most effective means of 39 reducing energy consumption when compared to other solutions on the basis of both cost and overall 40 efficiency (including fuel processing and logistics chain efficiencies).

41 Incremental improvements in the ICE efficiency through friction reduction and improvements in the 42 combustion system will continue but savings will become increasingly difficult and costly [10]. Waste 43 heat recovery such as organic Rankine cycles [9] and open gas and steam cycles [11] have been 44 proposed and could deliver improvements of the order of 2-5%. Alternative combustion systems, 45 such as Low temperature combustion to reduce heat losses [12] could also improve efficiency. 46 However, these approaches, even when combined with waste heat recovery are likely to yield a 47 maximum system efficiency of 45-50% [13]. Further improvements to efficiencies beyond 50% require 48 a fundamental change to the ICE cycle.

The splitting of the compression and expansion strokes into separate cylinders has the potential togreatly improve the overall cycle efficiencies through:

51 1) Reduction of the compression work by induction into a cool cylinder or direct cooling of the charge52 air during compression

53 2) Decoupling of the compression and expansion strokes effectively enabling a Miller cycle

54 3) High pressure waste heat recovery between the compression and combustion cylinders

55 The concept of splitting the ICE cycle into separate cylinders is not new, and was first described by 56 Ricardo in 1908 [14]. Coney [15] evolved the cycle to add isothermal compression and high pressure 57 recuperation for stationary power applications. Water injection into the compression cylinder was 58 proposed to achieve isothermal compression. A break efficiency of 60% was predicted using cycle 59 simulation, but the contribution of the various features of the cycle was not described. Scuderi [16] 60 proposed an alternative concept for road transport applications, that utilised a cool compressor 61 cylinder and separate combustion cylinder with a close coupled transfer port. Both concepts were 62 taken to lab demonstration, but were not commercialised. More recently, Atkins [17] has suggested a 63 variant of the Coney engine that uses liquid nitrogen to cool the compressor, exploiting both the latent 64 and sensible heat of the cryogenic fluid. It is claimed this overcomes the difficulties of carrying a 65 water handling system on a road vehicle.

In this paper, we analyse the split cycle engine in detail to understand the contribution of various features of the cycle to the overall efficiency. Classical analysis is first used to investigate the global trade offs of compression ratio and waste heat recovery on a reciprocating split cycle engine. Full cycle analysis is then used to investigate in detail key features of the cycle and the impact on the engine architecture. The paper concludes with a discussion on the potential of a split cycle engine in road transport and stationary applications.

а	droplet surface area (m <sup>2</sup> /kg)	ER	expansion ratio	Q <sub>LH</sub>	Fuel heat release amount (kJ)	V	volume
atdc	after top dead centre	EVC	exhaust valve close timing	Q <sub>RE</sub>	recuperated heat (kJ)	Greeks	
AFR	air fuel ratio	EVO	exhaust valve open timing	S	entropy	ε	specific heat ratio
С	Isothermal index	h	enthalpy (kJ/kg))	Т	temperature (K)	σ	recuperator effectiveness
CA	crank angle	IVC	Intake valve close timing	T <sub>in</sub>	Intake air temperature (K)	η	thermal efficiency
C <sub>v</sub>	specific heat under constant volume	IVO	Intake valve open timing	T <sub>out</sub>	Outlet air temperature (K)	Subscri	pts
$C_{\rho}$	specific heat under constant pressure	k	isentropic exponent	Δ	difference	LH	fuel lower heating value
CR	compression ratio	p	pressure	u	heat transfer coefficient	RE	heat recuperation

## 72 Nomenclature

73

## 74 2. Engine structure and theatrical thermodynamic cycle analysis

75 2.1 Description of the split engine cycle

76 A schematic of the 'isoengine' type of split cycle engine is shown in Fig. 1. Ambient air at stage point 77 1 is pre-compressed in the turbocharger, and then sent to the reciprocating compression cylinder (2). 78 A certain amount of water is injected into the cylinder to cool down the air during compression, 79 resulting in a quasi-isothermal compression process. After the compression stage (3), a high-pressure 80 two-phase water/air mixture leaves the isothermal compressor, and the water is recovered in a 81 separator. The liquid water is cooled and sent back to a water tank (5). A recuperator is installed 82 downstream the separator to heat the high-pressure air (4). Within the recuperator, the air is heated 83 by the exhaust flow (7), and then an intra-cylinder heat recovery process is achieved.

After the recuperation process (6), the fully preheated compressed air is fed to the combustion cylinders. As the combustion chamber intake valve opening time (IVO) is near to top dead centre (TDC), the diffusion of the combustion flame occurs in the expansion stroke of the cylinder. As a result, the combustion peak pressure is not increased significantly and a quasi-isobaric combustion process can be assumed. At the end of the expansion stage, the cylinder pressure is very close to the pressure in the exhaust pipe (7), so the exhaust stroke can be assumed as nearly isobaric as well. Based on the above processes, a complete split cycle is achieved.

91 2.2 Thermodynamic cycle analysis of the split cycle engine

92 The introduction of the split cycle engine indicates that both the combustion and exhaust stroke are 93 nearly isobaric, and the expansion stroke can be treated as nearly adiabatic. The thermodynamic 94 characteristics of the split cycle engine are therefore very similar to the Brayton cycle [18, 19]. A 95 comparison between a simple Brayton cycle, recuperated Brayton cycle, ideal iso-thermal split cycle 96 and quasi-isothermal split cycle is shown in Table 1.

97 For the Brayton cycle, the efficiency of the cycle is decided by the compression ratio (CR) only. The 98 ideal efficiency of the cycle is greater than 60% when the CR is greater than 15. However, this 99 efficiency can be improved, especially under a lower CR conditions by recovering waste heat through 100 a recuperator to pre-heat the charge air post compression. The efficiency of this cycle is decided not 101 only by the compression ratio, but also the regenerator effectiveness and the amount of heat released 102 from the combustion process. In this thermodynamic cycle, the compressed air will be pre-heated by 103 the exhaust gas. The recuperation process only works when the exhaust temperature  $T_4$  is higher than the compressed air temperature T<sub>2</sub>. According to Table 1, the following relationship should besatisfied:

106 
$$(\underline{T_1 \cdot CR^{k-1} + \frac{Q_{LH}}{C_p}}) / CR^{k-1} > \underbrace{T_1 \cdot CR^{k-1}}_{T_2}$$
(1)

107 Clearly, with the increase of  $T_2$  and the decreases of  $T_4$ , the efficiency of this cycle cannot be 108 improved when a higher CR is applied. To find the available compression ratio range, the variables *x* 109 and *l* are defined as:

110 
$$x = CR^{k-1}, l = \frac{Q_{LH}}{C_p T_1}$$
 (2)

111 So the relationship 1 can be rearranged as:

112 
$$(x-1/2)^2 - (l-1/4) < 0$$
 (3)

Assuming a 2,200 K maximum combustion temperature which represents the normal heat release case in diesel engines [20], and a recuperator effectiveness of 0.8, the available compression ratio range is shown in Fig. 2. Under such conditions, recuperation only can be achieved when the CR value is lower than 15.6, lower than the normal CR value is 17 or higher for a diesel engine.

The split thermodynamic cycle, enables a much wider recuperation range than can be achieved with a
recuperated Brayton cycle. In an ideal Split cycle, an isothermal compression process is applied.
Thus the compression air temperature T<sub>2</sub> is the same as the initial intake air temperature T<sub>1</sub>. Then the
temperature T4 can be expressed as:

121 
$$T_4 = (T_1 + (Q_{LH} + Q_{RE}) / C_p) / CR^{(K-1)}$$
 (4)

122 The expansion temperature  $T_4$  is therefore always higher than  $T_2$  regardless of the compression ratio. 123 As a result, the recuperation process can be achieved throughout the compression ratio range.

For the real split cycle engine, the compression process is assumed to be quasi-isothermal. As a result, the  $T_4$  is not always higher than the compression temperature  $T_2$  and a limited recuperation range exists for this cycle. 127 The temperature  $T_{2'}$  is strongly affected by the heat transfer process between the injected water and 128 the intake air. The effect of heat transfer from the air to water droplets can be represented by a 129 modified form of the well-known relationship for an ideal gas undergoing isentropic compression or 130 expansion [21]. The modified equation is derived from the First Law of Thermodynamics in a similar 131 way to the original equation, yielding:

132 
$$\frac{T_{2'}}{T_1} = CR^{\left(K-1\right) \cdot \exp\left[-\frac{ua}{c_p}\left(1 - \frac{T_w}{T_1}\right)\Delta t\right]}$$
(5)

133 Equation (5) relates the change of air temperature and pressure during a time interval  $\Delta t$ , with the 134 exponential function representing the effect of heat transfer to the droplets.  $T_w$  is the mean spray 135 water temperature, C<sub>p</sub> is the specific heat of the air in the cylinder, K is the isentropic index, u is the 136 heat transfer coefficient between the air and the water droplets and a is the droplet surface area per 137 kg of air. If  $u_a \Delta t$  is near zero then the exponential function tends to unity and the temperature ratio 138 tends to the unmodified isentropic relationship. On the other hand if  $u_a \bullet \Delta t$  is large then T<sub>2</sub> rapidly 139 converges on Tw. Since the parameters of the exponential function depend on time and may undergo 140 rapid changes during compression, the above expression should only be applied to small time 141 intervals and small pressure ratios. Here, we define the isothermal index C as:

142 
$$\mathbf{C} = \exp\left[-\frac{ua}{c_p}\left(1 - \frac{T_w}{T_1}\right)\Delta t\right]$$
(6)

Then the value of C is directly affected by the water injection amount. When the water injection rate is high, the value of C is close to 0 and the compression process can be treated as nearly isothermal. On the contrary, the value is close to 1 and an isentropic compression process can be assumed. Accordingly, the temperature of  $T_2$  and  $T_4$  can be expressed as:

147 
$$T_{2'} = T_1 \cdot CR^{(K-1) \cdot C}$$
 (7)

148 
$$T_4 = \frac{T_1 \cdot CR^{(K-1)C} + (Q_{RE} + Q_{LH}) / C_p}{CR^{(K-1)}}$$
(8)

According to the above two equations, we can conclude that  $T_4$  is not necessarily higher than  $T_2$ . However, comparing to the case of the recuperated Brayton cycle, the compression temperature  $T_{2'}$  is much lower. Given the same compression ratio, the recuperation available range in the split cycleengine is wider than the recuperated Brayton cycle.

153 Fig. 3 shows the efficiency comparison between the above 4 cycles. Here a recuperator effectiveness 154 is defined as  $\sigma = (T_{2'} - T_2) / (T_4 - T_2)$  to calculate the recuperated heat  $Q_{RE}$ . The  $\sigma$  is assumed to be 0.8 155 which represent the performance typical of a commercial recuperator. The variable C is assumed to 156 be 0.45 which represents moderate cooling of the air by the injected water. From the Fig. 3 it can be 157 seen that, compared to the simple Brayton cycle, the efficiency of the recuperated Brayton cycle can 158 be improved when the compression ratio is less than 15.6. However a further improvement can be 159 achieved on the split cycle engine until the compression ratio is 23.7. Within this range, the ideal split 160 cycle efficiency can exceed 60%. This analysis demonstrates the split cycle engine is expected to 161 significantly improve the efficiency when it is applied to conventional reciprocating engines. To 162 analyse the engine performance in detail, a one dimensional model is constructed and discussed in 163 the following sections.

#### 164 3. Engine modelling and experimental validation

A numerical model of the system was realised using the LMS Imagine.Lab AMESim [22], a software for the simulation and analysis of one-dimensional systems. The IFP engine system module is in particular devoted to the development of internal combustion engine models, allowing the simulation of the considered engine system in both stationary and transient conditions [23]. Fig. 4 shows the layout of the proposed split cycle engine model. To simulate the effect of the water injection, the spray heat transfer model in the IFP engine package was applied, and validated by the experimental data achieved on a prototype engine [24].

172 Concerning the separator, there is no available model template available in the AMEsim environment. 173 However, considering that the efficiencies of commercial water separators are very close to 100%, we 174 assumed that the water was completely removed from the air-water mixtures without changing the 175 status of the flow transfer from the compression chamber to the recuperator. Accordingly, the 176 compression chamber is connected to a dummy combustion chamber in the model, and then the 177 mixture flow status such as temperature and pressure can be collected in real time and used to define 178 the status of the pure air flow sent to the real combustion chamber. Also, the flow rate of the pure air 179 can be calculated by a water percentage sensor which is coded with C in the AMEset environment 180 [25]. To predict the recuperator behaviour, a heat exchanger model is applied. Then the heat transfer 181 between the intake air and exhaust gas can be evaluated. Finally, the combustion behaviour is 182 predicted by the combustion chamber which is based on the IFP engine package in AMEsim. The 183 heat release process and the heat transfer behaviours in the combustion chamber are validated and 184 calibrated by the experimental data collected on a conventional diesel single cylinder engine. The 185 specifications of the split cycle engine modelled are shown in Table 2.

186 Fig. 5 shows a comparison between the split cycle engine and the conventional diesel engine. As 187 shown in fig.5 (a), the pressure in the combustion chamber of the split cycle engine increased 188 dramatically when the intake valve opened, but the rate of pressure rise at the start of combustion is 189 much lower compared to a conventional diesel engine, leading to a quasi-isobaric combustion 190 process. The fuel injection timing on the split cycle is retarded to avoid the start of combustion 191 coinciding with an open intake valve [15], leading to backflow into the intake manifold. Subsequently 192 the combustion phase is delayed to the expansion stroke as shown in Fig. 5 (b). Due to the retarded 193 combustion, the peak heat transfer rate is much lower than in a conventional diesel engine, whereas 194 the rate falls more slowly during the expansion stage due to late combustion, as can be seen in fig. 5 195 (c). The T-S diagrams of both engines can be seen in Fig. 5 (d). Due to the quasi-isothermal 196 compression and recuperation process, the work, represented by the area bound by the TS diagram 197 is higher for the same heat addition from combustion resulting in a 13% total efficiency improvement. 198 Details of cycle will be discussed in the following sections.

199 4. Results and discussions

200 4.1. Evaluation of the isothermal compression process

201 Isothermal compression can yield significant savings in compression work compared to the adiabatic 202 (isentropic) compression, where more work is needed to compress the hotter gas. The effect of the 203 injection of water into the compressor chamber, for a 350K intake air temperature and 2 bar initial 204 pressure is shown in Fig. 6. The adiabatic case results in a 92 bar final pressure at the position of 205 EVO for a CR of 18. When a 20g/s water injection applied, the compression pressure is significantly 206 decreased for the same compression ratio. When the CR value increased to 31.5, the same final 207 pressure is achieved as the adiabatic case, to provide equivalent combustor inlet pressure. Since the 208 compression stroke length is fixed, the compression work is decided by the in-cylinder pressure

209 during the compression. Compared to the pressure curve of adiabatic compression, the pressure is 210 decreased when the water injection is applied. The water injection therefore reduces both the 211 compression temperature and the consumed work on the split cycle engine.

212 Under different compression ratios (CR), the effect of the water injection rate on the work 213 consumption is shown in Fig. 7 (a). When the water injection rate increases, the work saving also 214 increases. Similarly, the consumed work is greatest under high compression ratio conditions. For an 215 80g/s water injection rate, 15.7% of the compression work can be saved with a CR value of 22. 216 However, the percentage does not increase significantly when the injection rate is higher than 40g/s. 217 The effect of the water injection rate on the in-cylinder temperature can be seen in Fig.7 (b), a 218 significant decrease is observed even when the water injection is as low as 5g/s. With a CR value of 219 18, the compressed air temperature is as low as 380K for a 37g/s of water injection, only slightly 220 higher than the 350K intake temperature. The water injection rate should therefore be calibrated 221 carefully to achieve quasi-isothermal compression to avoid excessive water injection and associated 222 parasitic losses.

223 4.2. Heat recovery system evaluation

In section 2.2, we assumed a constant recuperation effectiveness  $\sigma$  in the theoretical model. However, the effectiveness will vary depending on the operating conditions. The specifications of the recuperator can be seen in table 3. A one-dimensional recuperation system model was developed via AMEsim, and validated by the recuperator data modelled by Oliverira [26].

228 According to the definition of the recuperator effectiveness  $\sigma$  in section 2.2, the  $\sigma$  is mainly affected by 229 the fresh air inlet temperature  $T_{2'}$  (which is the inlet air temperature of the recuperator, slave side), 230 and exhaust outlet temperature  $T_4$ . As discussed in section 2,  $T_{2'}$  is the temperature at the end of 231 quasi-isothermal compression process, and the  $T_4$  is the temperature at the end of the expansion 232 process (which is the inlet exhaust temperature of the recuperator master side). Given a fixed 233 temperature  $T_2$ , the compression ratio is the key factors which affect the effectiveness. Figs. 8 (a) and 234 (b) show the one dimensional temperature distribution within the recuperator for compression ratios 235 (CR) 20 and 25 respectively. From the inlet to the outlet of the recuperator, 10 nodes are applied with 236 a fixed interval of 60mm (1/10 of the total length), and then the one dimension temperature 237 distribution is calculated. The air-fuel ratio was fixed at 18 and a 10g/s water injection is applied. As the water injection rate is the same, the air inlet temperatures  $T_{2'}$  is nearly the same under these two cases. In Fig.8 (a), it can be seen that the temperature difference between  $T_4$  and  $T_2$ , is 69K when the CR is 20. But this difference increases to 198K when the CR increases to 25 as seen in Fig. 8 (b). Due to the effect of the heat transferred form the combustion cylinder, the recuperator temperature is pinched at 0.6-0.7 normalised distance from the cold end. The above results indicate that the recuperator effectiveness decreases when the CR is increased.

To investigate this issue, the recuperator wall temperature was analysed. As seen in both cases (Fig. 8), the wall temperature is very close to the expansion temperature  $T_4$ . So it can be deduced that a higher expansion temperature leads to a higher wall transfer heat losses. Accordingly, the rate of temperature rise at the outlet side of the recuperator is lower when the expansion temperature is higher. As a result, it can be deduced that the recuperator effectiveness decreases under the higher compression ratio condition.

250 4.3 Combustion process

For the split thermodynamic cycle, the cycle efficiency is decided by 3 independent parameters; the isothermal index C, the recuperator effectiveness  $\sigma$ , and the combustion heat release  $Q_{LH}$ . For the real engine, the value C is mainly determined by the water injection rate, the recuperator effectiveness  $\sigma$  is determined by the recuperator specifications and its operation conditions.  $Q_{LH}$ directly affects the peak combustion temperature T<sub>3</sub>. Setting the compression ratio at 16 and keeping the water injection rate at 25g/s, the effect of air-fuel ratio  $\lambda$  is discussed in this section.

257 Fig. 9 (a) shows the pressure curves with different air-fuel ratios. In contrast to the conventional 258 engine, a moderate rate of pressure rise is observed on the split cycle engine. This phenomenon is 259 mainly due to the intake valve open timing being close to the TDC, and the combustion occurring 260 during the expansion process. The combustion process for the split cycle engine can be treated as 261 near isobaric. Given a certain thermal load constraint, such a combustion process enables a higher 262 compression ratio, and high cycle thermal efficiency. Fig. 9 (b) shows the peak temperatures for 263 different  $\lambda$  values. When the air-fuel ratio is 16, the peak combustion temperature is still less than 264 1,600K, which is lower than conventional diesel engines. Referring to the diesel engine and split 265 cycle engine model mentioned in section 3, a comparison between the two cycles is discussed below.

266 Given a fix air-fuel ratio of 17, and maintaining the compression ratios of 16, the in-cylinder energy 267 balance is compared. Fig. 10 (a) and (b) are the energy balances within the combustion cylinders of 268 the conventional and the split engine. In a split cycle engine, the cumulative energy in the combustor 269 is higher than the total energy abstracted from the fuel. This phenomenon is due to the fact that part 270 of the heat in the exhaust flow is recovered and delivered into the combustion chamber. Within the 271 chamber, the total wall heat transfer of the split cycle engine is lower due to the lower average 272 combustion temperature. This results in a 4% total thermal efficiency improvement in the split cycle 273 engine case. Consequently, the network output in the split cycle engine is significantly increased.

#### 274 4.4 System efficiency analysis

275 The theoretical analysis indicates the split cycle engine efficiency is improved by three parameters: 276 the isothermal index C, the regenerator effectiveness  $\sigma$ , and the combustion release heat Q<sub>LH</sub>. On a 277 real split cycle engine, the cycle efficiency is also affected by losses in the quasi-isothermal 278 compression, the recuperation and the combustion process. These processes were discussed in the 279 previous section based on a one-dimensional engine model. Since the compression process is 280 independent of the recuperation and combustion process, it can be discussed separately. After the 281 separator, the pure air is pre-heated by the recuperator and delivered into the combustion chamber. 282 The property and mass flow rate of the working fluid can then be considered as constant, and the 283 recuperation and combustion process can be analysed together. The overall cycle efficiency 284 improvement on the split cycle engine is the combination of three factors and can be expressed as:

$$285 \qquad E_{impro} = E_{comp} + \underbrace{E_{recup} + E_{comb}}_{Recuperated - combustion}$$
(9)

286 Where  $E_{impro}$  is the efficiency improvement of the split cycle engine compared to the conventional 287 diesel engine, expressed as the increase in work for a given fuel input normalised by the fuel input. 288 Ecomp is the incremental efficiency improvement through the reduction of compression work through 289 the quasi-isothermal process, *E<sub>recup</sub>* is the efficiency improvement through the recovery of waste heat 290 through the recuperation process, and the  $E_{comb}$  represents the efficiency improvement due to the 291 nearly isobaric combustion. Keeping the compression ratio and air-fuel ratio the same, and 292 maintaining the engine speed at 1200 rpm, the engine energy balance of a split cycle engine and 293 conventional diesel engine are shown in Fig. 11 (a) and (b) respectively. In the split cycle engine, a

294 5% indicated thermal efficiency improvement can be directly achieved by the guasi-isothermal 295 compression; comparing to diesel engine, a 1% thermal loss can be avoided because of the lower 296 compression temperature. Also, 8% energy can be re-utilized through the recuperation process. Due 297 to the energy re-utilization and heat losses reduction, 53% of the energy from the fuel can be 298 converted to work in the combustion cylinder. Compared to the conventional engine with a break 299 thermal efficiency of 40%, a 32% efficiency improvement (increase in work) can be expected by the 300 split cycle engine. At this stage, a comprehensive optimisation and calibration of the recuperation and 301 combustion parameters has not been done. Comparing the 60% efficiency predicted by pure 302 theoretical analysis reported by Coney [15], the result from this one dimensional model are lower. 303 Further performance improvements can be expected through further system optimization.

304 5. Conclusions

305 Based on the theoretical analysis and a one-dimensional engine model, the fundamentals and the 306 performance of the split thermodynamic cycle is evaluated. The major findings of the study are as 307 follows:

308 1) Isothermal compression in a split cycle engine design, significantly improves the recuperation
 309 efficiency of a reciprocating engine, and expands the compression ratio range available for
 310 recuperation.

311 2) A quasi-isothermal compression process can be achieved by injecting a certain amount of water in312 the compression cylinder and increasing the geometric compression ratio.

313 3) Recuperation efficiency is improved at higher compression ratios.

4) Isobaric combustion enables a low peak combustion temperature. Given a fixed thermal load
constraint, such a low temperature leads to a cycle efficiency improvement and a reduction of wall
heat transfer losses.

5) Concerning the whole cycle efficiency, a 53% break thermal efficiency can be expected for splitcycle engines, compared to a baseline efficiency of 40% efficiency for a conventional diesel engine.

319 Acknowledgement

- 320 The authors would like to thank the UK's Technology Strategy Board for their co-funding of the
- 321 Cryopower Project under the IDP8 programme.
- 322
- 323 References

<ol> <li>Heywood, J.B., Internal combustion engine fundamentals. McGraw-Hill series in mechanical engineering. 1988, New York: McGraw-Hill. xxix, 930 p., 2 p. of plates.</li> <li>Caresana, F., et al., Energy and economic analysis of an ICE-based variable speed- operated micro-cogenerator. Applied Energy, 2011. 88(3): p. 659-671.</li> <li>Venkanna, B.K. and C.V. Reddy, Effect of injector opening pressure on performance, emission and combustion characteristics of DI diesel engine fueled with diesel and honne oil methyl ester. Environmental Progress &amp; Sustainable Energy, 2013. 32(1): p. 148-155.</li> <li>Millo, F., et al., Real CO2 emissions benefits and end user's operating costs of a plug-in Hybrid Electric Vehicle. Applied Energy, 2014. 114: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, Performance comparison of autothermal reforming for liquid hydrocarbons, gasoline and diesel for fuel cell applications. Journal of Power Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles. Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to Market Future Commercial Methyle fucient and Clean Engines to</li> </ol>
<ol> <li>Mechanical engineering. 1988, New York Work analysis of an ICE-based variable speed- operated micro-cogenerator. Applied Energy, 2011. 88(3): p. 659-671.</li> <li>Venkanna, B.K. and C.V. Reddy, Effect of injector opening pressure on performance, emission and combustion characteristics of DI diesel engine fueled with diesel and honne oil methyl ester. Environmental Progress &amp; Sustainable Energy, 2013. 32(1): p. 148-155.</li> <li>Millo, F., et al., Real CO2 emissions benefits and end user's operating costs of a plug-in Hybrid Electric Vehicle. Applied Energy, 2014. 114: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, Performance comparison of autothermal reforming for liquid hydrocarbons, gasoline and diesel for fuel cell applications. Journal of Power Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles. Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> </ol>
<ol> <li>Series and Provide the analysis of a second marked and the second marked and the second and the se</li></ol>
<ol> <li>Venkanna, B.K. and C.V. Reddy, Effect of injector opening pressure on performance, emission and combustion characteristics of DI diesel engine fueled with diesel and honne oil methyl ester. Environmental Progress &amp; Sustainable Energy, 2013. 32(1):</li> <li>p. 148-155.</li> <li>Millo, F., et al., Real CO2 emissions benefits and end user's operating costs of a plug-in Hybrid Electric Vehicle. Applied Energy, 2014. 114: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, Performance comparison of autothermal reforming for liquid hydrocarbons, gasoline and diesel for fuel cell applications. Journal of Power Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles. Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> </ol>
<ul> <li>emission and combustion characteristics of DI diesel engine fueled with diesel and honne oil methyl ester. Environmental Progress &amp; Sustainable Energy, 2013. 32(1):</li> <li>p. 148-155.</li> <li>Millo, F., et al., Real CO2 emissions benefits and end user's operating costs of a plug-in Hybrid Electric Vehicle. Applied Energy, 2014. 114: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, Performance comparison of autothermal reforming for liquid hydrocarbons, gasoline and diesel for fuel cell applications. Journal of Power Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles. Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to Most Further Commercial Vehicle Commerciant of Highly Efficient and Clean Engines to</li> </ul>
<ul> <li>honne oil methyl ester. Environmental Progress &amp; Sustainable Energy, 2013. 32(1):</li> <li>p. 148-155.</li> <li>Millo, F., et al., <i>Real CO2 emissions benefits and end user's operating costs of a</i></li> <li><i>plug-in Hybrid Electric Vehicle</i>. Applied Energy, 2014. 114: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, <i>Performance comparison of autothermal reforming for</i></li> <li><i>liquid hydrocarbons, gasoline and diesel for fuel cell applications</i>. Journal of Power</li> <li>Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., <i>From the internal combustion engine to the fuel cell: Moving towards</i></li> <li><i>the hydrogen economy</i>. Science and Technology in Catalysis 2002, 2003. 145: p. 21-</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, <i>Cost-effectiveness of alternative</i></li> <li><i>powertrains for reduced energy use and CO2 emissions in passenger vehicles</i>.</li> <li>Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, <i>Advances and challenges in ORC systems</i></li> <li><i>modeling for low grade thermal energy recovery</i>. Applied Energy, 2014. 121: p. 79-</li> <li>95.</li> <li>Stanton, D.W., <i>Systematic Development of Highly Efficient and Clean Engines to</i></li> </ul>
<ul> <li>p. 148-155.</li> <li>Millo, F., et al., <i>Real CO2 emissions benefits and end user's operating costs of a plug-in Hybrid Electric Vehicle</i>. Applied Energy, 2014. <b>114</b>: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, <i>Performance comparison of autothermal reforming for liquid hydrocarbons, gasoline and diesel for fuel cell applications</i>. Journal of Power Sources, 2006. <b>163</b>(1): p. 538-546.</li> <li>Farrauto, R.J., <i>From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy</i>. Science and Technology in Catalysis 2002, 2003. <b>145</b>: p. 21-29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, <i>Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles</i>. Applied Energy, 2014. <b>124</b>: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, <i>Advances and challenges in ORC systems modeling for low grade thermal energy recovery</i>. Applied Energy, 2014. <b>121</b>: p. 79-95.</li> <li>Stanton, D.W., <i>Systematic Development of Highly Efficient and Clean Engines to Mart Future Commercial Vehicle</i>. <i>Commercial Vehicle</i>.</li> </ul>
<ol> <li>Millo, F., et al., <i>Real CO2 emissions benefits and end user's operating costs of a</i> <i>plug-in Hybrid Electric Vehicle.</i> Applied Energy, 2014. <b>114</b>: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, <i>Performance comparison of autothermal reforming for</i> <i>liquid hydrocarbons, gasoline and diesel for fuel cell applications.</i> Journal of Power Sources, 2006. <b>163</b>(1): p. 538-546.</li> <li>Farrauto, R.J., <i>From the internal combustion engine to the fuel cell: Moving towards</i> <i>the hydrogen economy.</i> Science and Technology in Catalysis 2002, 2003. <b>145</b>: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, <i>Cost-effectiveness of alternative</i> <i>powertrains for reduced energy use and CO2 emissions in passenger vehicles.</i> Applied Energy, 2014. <b>124</b>: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, <i>Advances and challenges in ORC systems</i> <i>modeling for low grade thermal energy recovery.</i> Applied Energy, 2014. <b>121</b>: p. 79- 95.</li> <li>Stanton, D.W., <i>Systematic Development of Highly Efficient and Clean Engines to</i> <i>Mact Future Commercial Vehicle Creationes Constantione</i> <i>Commercial Vehicle Creationes Constantiones</i></li> </ol>
<ul> <li><i>plug-in Hybrid Electric Vehicle.</i> Applied Energy, 2014. <b>114</b>: p. 563-571.</li> <li>Kang, I., J. Bae, and G. Bae, <i>Performance comparison of autothermal reforming for</i> <i>liquid hydrocarbons, gasoline and diesel for fuel cell applications.</i> Journal of Power Sources, 2006. <b>163</b>(1): p. 538-546.</li> <li>Farrauto, R.J., <i>From the internal combustion engine to the fuel cell: Moving towards</i> <i>the hydrogen economy.</i> Science and Technology in Catalysis 2002, 2003. <b>145</b>: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, <i>Cost-effectiveness of alternative</i> <i>powertrains for reduced energy use and CO2 emissions in passenger vehicles.</i> Applied Energy, 2014. <b>124</b>: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, <i>Advances and challenges in ORC systems</i> <i>modeling for low grade thermal energy recovery.</i> Applied Energy, 2014. <b>121</b>: p. 79- 95.</li> <li>Stanton, D.W., <i>Systematic Development of Highly Efficient and Clean Engines to</i></li> </ul>
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<ul> <li>liquid hydrocarbons, gasoline and diesel for fuel cell applications. Journal of Power</li> <li>Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards</li> <li>the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21-</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative</li> <li>powertrains for reduced energy use and CO2 emissions in passenger vehicles.</li> <li>Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems</li> <li>modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79-</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> </ul>
<ul> <li>Sources, 2006. 163(1): p. 538-546.</li> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles. Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to Maet Future Commercial Value of Constructions.</li> </ul>
<ol> <li>Farrauto, R.J., From the internal combustion engine to the fuel cell: Moving towards the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21- 29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles.</li> <li>Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> </ol>
<ul> <li>the hydrogen economy. Science and Technology in Catalysis 2002, 2003. 145: p. 21-</li> <li>29.</li> <li>8. Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles.</li> <li>Applied Energy, 2014. 124: p. 44-61.</li> <li>9. Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79-</li> <li>95.</li> <li>10. Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> </ul>
<ol> <li>29.</li> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, <i>Cost-effectiveness of alternative powertrains for reduced energy use and CO2 emissions in passenger vehicles.</i></li> <li>Applied Energy, 2014. <b>124</b>: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, <i>Advances and challenges in ORC systems modeling for low grade thermal energy recovery.</i> Applied Energy, 2014. <b>121</b>: p. 79-95.</li> <li>Stanton, D.W., <i>Systematic Development of Highly Efficient and Clean Engines to Mart Future Commercial Vehicle Crean Engines to Stanton.</i></li> </ol>
<ol> <li>Bishop, J.D.K., N.P.D. Martin, and A.M. Boies, <i>Cost-effectiveness of alternative</i> <i>powertrains for reduced energy use and CO2 emissions in passenger vehicles.</i> Applied Energy, 2014. <b>124</b>: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, <i>Advances and challenges in ORC systems</i> <i>modeling for low grade thermal energy recovery.</i> Applied Energy, 2014. <b>121</b>: p. 79- 95.</li> <li>Stanton, D.W., <i>Systematic Development of Highly Efficient and Clean Engines to</i> Maat Future Commercial Vehicle Crean Future Commercial Vehicles.</li> </ol>
<ul> <li>powertrains for reduced energy use and CO2 emissions in passenger vehicles.</li> <li>Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> <li>Mast Future Commercial Value of Crean Insurance Constraints of List of Energy.</li> </ul>
<ul> <li>Applied Energy, 2014. 124: p. 44-61.</li> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to Mart Future Commercial Values Case Development of Energy and Clean Engines to</li> </ul>
<ol> <li>Ziviani, D., A. Beyene, and M. Venturini, Advances and challenges in ORC systems modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79- 95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to Mast Future Commercial Values.</li> </ol>
<ul> <li>modeling for low grade thermal energy recovery. Applied Energy, 2014. 121: p. 79-</li> <li>95.</li> <li>Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> <li>Most Future Commercial Value Crean bases Constraints and Clean Engines to</li> </ul>
<ul> <li>347 95.</li> <li>348 10. Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to</li> <li>349 Most Future Commercial Vahiele Crean bases Case Desculations 2015 International Commercial Vahiele Crean bases Case Desculations 2015 International Commercial Vahiele Crean bases Case Desculations 2015 International Case Case Desculations 2015 International Case Case Desculations 2015 International Case Case Case Case Case Case Case Case</li></ul>
348 10. Stanton, D.W., Systematic Development of Highly Efficient and Clean Engines to
349 Intert Future Commercial Venicle Greenhouse Gas Regulations. SAE Int. J. Engines,
350 2013. <b>6</b> (3): p. 1395-1480.
351 11. Fu, J.Q., et al., A comparative study on various turbocharging approaches based on
352 IC engine exhaust gas energy recovery. Applied Energy, 2014. 113: p. 248-257.
555 12. Calon, J.A., Thermodynamic Advantages of Low Temperature Compusition (LTC)
255 12 Sprouse C and C Dencik, <i>Paview of organic Panking cycles for internal combustion</i>
356 and the set of the
350 engine exhaust waste neat recovery. Applied methal Engineering, 2013. <b>31</b> (1-2), p. $357$ 711-722
358 14 Arcoumanis C. Internal combustion engines 1988 London: Academic x 397 n
359 15 Coney MW C Linneman and HS Abdallah A thermodynamic analysis of a
360 novel high efficiency reciprocating internal combustion engine - the isoengine
361 Energy 2004 <b>29</b> (12-15): p. 2585-2600
362 16 Sud K S Cetinkunt and S B Fiveland Modeling and Validation of a Split Cycle
363 <i>Clean Combustion Diesel Engine Concept.</i> Journal of Engineering for Gas Turbines
364 and Power-Transactions of the Asme, 2013. <b>135</b> (8).
365 17. Jackson, N.S. and A.F. Atkins, Split Cycle Reciprocating Piston Engine, 2012.
366 Google Patents.

- 367 18. Yan, X.L. and L.M. Lidsky, *Dual brayton cycle gas turbine pressurized fluidized bed*368 *combustion power plant concept.* Journal of Engineering for Gas Turbines and
  369 Power-Transactions of the Asme, 1998. **120**(3): p. 566-572.
- Khaliq, A. and S.C. Kaushik, Second-law based thermodynamic analysis of
  Brayton/Rankine combined power cycle with reheat. Applied Energy, 2004. 78(2): p.
  179-197.
- 20. Cong, S., C.P. Garner, and G.P. McTaggart-Cowan, *The effects of exhaust back pressure on conventional and low-temperature diesel combustion.* Proceedings of
  the Institution of Mechanical Engineers Part D-Journal of Automobile Engineering,
  2011. 225(D2): p. 222-235.
- 377 21. Incropera, F.P. and D.P. DeWitt, *Fundamentals of heat and mass transfer*. 5th ed.
  378 2002, New York: J. Wiley. xix, 981 p.
- Chen, D.G., et al., A Research on Compressed Natural Gas Engine Fuel Supply
  System for Rapid Prototyping Based on AMEsim. Applied Energy Technology, Pts 1
  and 2, 2013. **724-725**: p. 1317-1323.
- Wu, Z.W., et al., *Numerical Simulations of TWC Light off Characteristics Based on AMESim.* Industrial Instrumentation and Control Systems, Pts 1-4, 2013. 241-244: p.
   785-788.
- 385 24. Najafi, M. and Z. Benjelloun-Dabaghi, A New Modelica Model and Scicos Simulation
  386 for 0D/1D NonlinearComplex Systems. Oil & Gas Science and Technology-Revue D
  387 Ifp Energies Nouvelles, 2008. 63(6): p. 723-736.
- Li, M., et al., Simulation on Static and Dynamic Characteristics of Servovalve. History
   of Mechanical Technology and Mechanical Design 2012, 2012. 163: p. 281-285.
- Oliveira, S.G., et al., *The importance of control considerations for heat exchanger network synthesis: A case study.* Brazilian Journal of Chemical Engineering, 2001.
- 392 **18**(2): p. 195-210.

Figure.1 Schematic of the 'isoengine' type Split cycle engine

Figure 2. The recuperation available range regarding to the value of CR (Compression ratio)

Figure 3. Efficiency comparison of the 4 thermodynamic cycles

Figure 4. Layout of the Split cycle engine model

Figure 5. A comparison between the Split cycle engine and the conventional diesel engine

Figure 6. Effect of water injection on the compression process

Figure 7. Effect of the water injection rate on (a) the work consumption and (b) in-cylinder temperature

Figure 8. Temperature distributions within the recuperator under the condition of (a) CR=20 and (b) CR=25

Figure 9. Varying curves of (a) pressure and (b) temperature-entropy with different air-fuel ratios

Figure 10. Inner-cylinder energy balances of (a) conventional diesel engine and (b) split cycle engine

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Figure 11. Energy consumption comparison of (a) split cycle engine and (b) conventional diesel engine

	Brayton cycle	Recuperated Brayton	Split cycle with ideal	Split cycle with quasi
		cycle	iso-thermal	iso-thermal compression
			compression	
	3 4 1	2 2 1	2 2 2	2 2 1
Temperature	$T_{1} = T_{amb}$ $T_{2} = T_{1} \cdot CR^{K-1}$ $T_{3} = T_{2} + Q_{LH} / Cp$ $T_{4} = T_{3} / CR^{K-1}$	$T_{1} = T_{amb}$ $T_{2} = T_{1} \cdot CR^{K-1}$ $T_{2'} = T_{4}$ $T_{3} = T_{2} + Q_{LH} / C_{p}$ $T_{4} = T_{3} / CR^{K-1}$ $T_{4'} = T_{2}$	$T_{1} = T_{amb}$ $T_{2'} = T_{1}$ $T_{2} = T_{2'} + Q_{RE} / C_{p}$ $T_{3} = T_{2} + Q_{LH} / C_{p}$ $T_{4} = T_{3} / CR^{(K-1)}$	$T_{1} = T_{amb}$ $T_{2'} = T_{1} \cdot CR^{(K-1) \cdot C}$ $T_{2} = T_{2'} + Q_{RE} / C_{p}$ $T_{3} = T_{2} + Q_{LH} / C_{p}$ $T_{4} = T_{3} / CR^{(K-1)}$ $C = \exp\left[-\frac{ua}{C_{p}}\left(1 - \frac{T_{w}}{T_{1}}\right)\Delta t\right] (0 < C < 1)$
Efficiency	$\eta_t = 1 - \frac{1}{CR^{k-1}}$	$\eta_{t} = 1 - \frac{CR^{k-1}}{CR^{k-1} + Q_{LH} / C_{p}T_{1}}$	$\eta_{t} = B(1 - \frac{1}{CR^{k-1}}) - D \cdot \ln(CR^{k-1})$ $B = \frac{\left(1 + (Q_{RE} + Q_{LH}) / (C_{p} \cdot T_{1})\right)}{(Q_{LH}) / (C_{p} \cdot T_{1})}$ $D = \frac{R_{g}}{C_{p}(k-1)}$	$\begin{split} \eta_{r} &= 1 - \begin{bmatrix} CR^{(k-1)C-1} - F(1 - \frac{1}{CR^{(k-1)}}) + \\ \frac{C_{v}}{C \cdot C_{p}} (CR^{(k-1)C} - 1) \end{bmatrix} / E \\ E &= (Q_{LH}) / (C_{p} \cdot T_{1}) \\ F &= (Q_{RE} + Q_{LH}) / (C_{p} \cdot T_{1}) \end{split}$
Recuperation available range	_	$T_4 > T_2$	$T_4 > T_1$	$T_4 > T_2$

Table 1 Comparison of the 4 typical thermo dynamical cycles

# Table 2 Split cycle engine specifications

Stroke	2 stroke	IVO	17° BTDC
Туре			(compression
			5° BTDC
			(combustion
			cylinder)
Number of	2	IVC	174° BTDC
cylinders	(1		(compression
	compressor		cylinder)
	+		10° ATDC
	1 combustor)		(combustion
			cylinder)
CR	23	EVO	5° BTDC
			(compression
			cylinder)
			152° ATDC
			(combustion
			cylinder)
Bore [mm]	128	EVC	10° ATDC
			(compression
			cylinder)
			2° ATDC
			(combustion
			cylinder )
Stroke	148	Speed	1200 rpm
[mm]			

# Table 3 Recuperator specifications

Parameter	Units	Value
Total length	mm	600
Inlet connection diameter (master fluid)	mm	40
Outlet connection diameter (master fluid)	mm	40
Number of tubes		35
Inlet tank volume	liter	0.3
Outlet tank volume	liter	0.3
Dry mass of heat exchanger material	kg	0.23
Tube inner diameter	mm	4
Channel inner cross-sectional flow area	mm^2	12.5
Number of channels (in one tube)		1
Shell diameter	mm	35
Inlet connection diameter (slave fluid)	mm	30
Outlet connection diameter (slave fluid)	mm	30
Slave inlet location relative to master		Opposit Sid