



**Transient Unbalance of a Turbo-Compressor Rotor
due to
Thermal-Gradient Induced Bow
from a
Seal Gas Heater**



Thom Eldridge: Shell Global Solutions (US) Inc.

Markus Hampel: QatarShellGTL

20 March, 2013, Doha, State of Qatar



DEFINITIONS AND CAUTIONARY NOTE

Resources: Our use of the term "resources" in this announcement includes quantities of oil and gas not yet classified as Securities and Exchange Commission of the United States ("SEC") proved oil and gas reserves or SEC proven mining reserves. Resources are consistent with the Society of Petroleum Engineers 2P and 2C definitions.

The companies in which Royal Dutch Shell plc directly and indirectly owns investments are separate entities. In this announcement "Shell", "Shell Group" and "Royal Dutch Shell" are sometimes used for convenience where references are made to Royal Dutch Shell plc and its subsidiaries in general. Likewise, the words "we", "us" and "our" are also used to refer to subsidiaries in general or to those who work for them. These expressions are also used where no useful purpose is served by identifying the particular company or companies. "Subsidiaries", "Shell subsidiaries" and "Shell companies" as used in this announcement refer to companies in which Shell either directly or indirectly has control, by having either a majority of the voting rights or the right to exercise a controlling influence. The companies in which Shell has significant influence but not control are referred to as "associated companies" or "associates" and companies in which Shell has joint control are referred to as "jointly controlled entities". In this announcement, associates and jointly controlled entities are also referred to as "equity-accounted investments". The term "Shell interest" is used for convenience to indicate the direct and/or indirect (for example, through our 23 per cent. shareholding in Woodside Petroleum Ltd.) ownership interest held by Shell in a venture, partnership or company, after exclusion of all third-party interest.

This announcement contains forward looking statements concerning the financial condition, results of operations and businesses of Shell and the Shell Group. All statements other than statements of historical fact are, or may be deemed to be, forward-looking statements. Forward-looking statements are statements of future expectations that are based on management's current expectations and assumptions and involve known and unknown risks and uncertainties that could cause actual results, performance or events to differ materially from those expressed or implied in these statements. Forward-looking statements include, among other things, statements concerning the potential exposure of Shell and the Shell Group to market risks and statements expressing management's expectations, beliefs, estimates, forecasts, projections and assumptions. These forward looking statements are identified by their use of terms and phrases such as "anticipate", "believe", "could", "estimate", "expect", "goals", "intend", "may", "objectives", "outlook", "plan", "probably", "project", "risks", "seek", "should", "target", "will" and similar terms and phrases. There are a number of factors that could affect the future operations of Shell and the Shell Group and could cause those results to differ materially from those expressed in the forward looking statements included in this announcement, including (without limitation): (a) price fluctuations in crude oil and natural gas; (b) changes in demand for Shell's products; (c) currency fluctuations; (d) drilling and production results; (e) reserves estimates; (f) loss of market share and industry competition; (g) environmental and physical risks; (h) risks associated with the identification of suitable potential acquisition properties and targets, and successful negotiation and completion of such transactions; (i) the risk of doing business in developing countries and countries subject to international sanctions; (j) legislative, fiscal and regulatory developments including regulatory measures addressing climate change; (k) economic and financial market conditions in various countries and regions; (l) political risks, including the risks of expropriation and renegotiation of the terms of contracts with governmental entities, delays or advancements in the approval of projects and delays in the reimbursement for shared costs; and (m) changes in trading conditions. All forward looking statements contained in this announcement are expressly qualified in their entirety by the cautionary statements contained or referred to in this section. Readers should not place undue reliance on forward looking statements. Additional factors that may affect future results are contained in Shell's 20-F for the year ended 31 December 2011 (available at www.shell.com/investor and www.sec.gov). These factors also should be considered by the reader. Each forward looking statement speaks only as of the date of this announcement, 20 March 2013. Neither Shell nor any of its subsidiaries nor the Shell Group undertake any obligation to publicly update or revise any forward looking statement as a result of new information, future events or other information. In light of these risks, results could differ materially from those stated, implied or inferred from the forward looking statements contained in this announcement.

Shell may have used certain terms, such as resources, in this announcement that the SEC strictly prohibits Shell from including in its filings with the SEC. U.S. investors are urged to consider closely the disclosure in Shell's Form 20-F, File No 1-32575, available on the SEC website www.sec.gov. You can also obtain these forms from the SEC by calling 1-800-SEC-0330.

OUTLINE

Introduction - Pearl GTL

GTL unit, Hydrocracker and Hydrogen Recycle Compressor

High Vibration during Process Gas Start-Up

It always happens at night or on the weekend – troubled starts
Initial reaction and assessment

Comparison to Inert Gas Start-Up

”It didn’t do this before” – What’s the same, What’s different
What could it be?

Root Cause Assessment – Process Correlation

Behavior summary and Problem statement

Conclusion

Acknowledgements

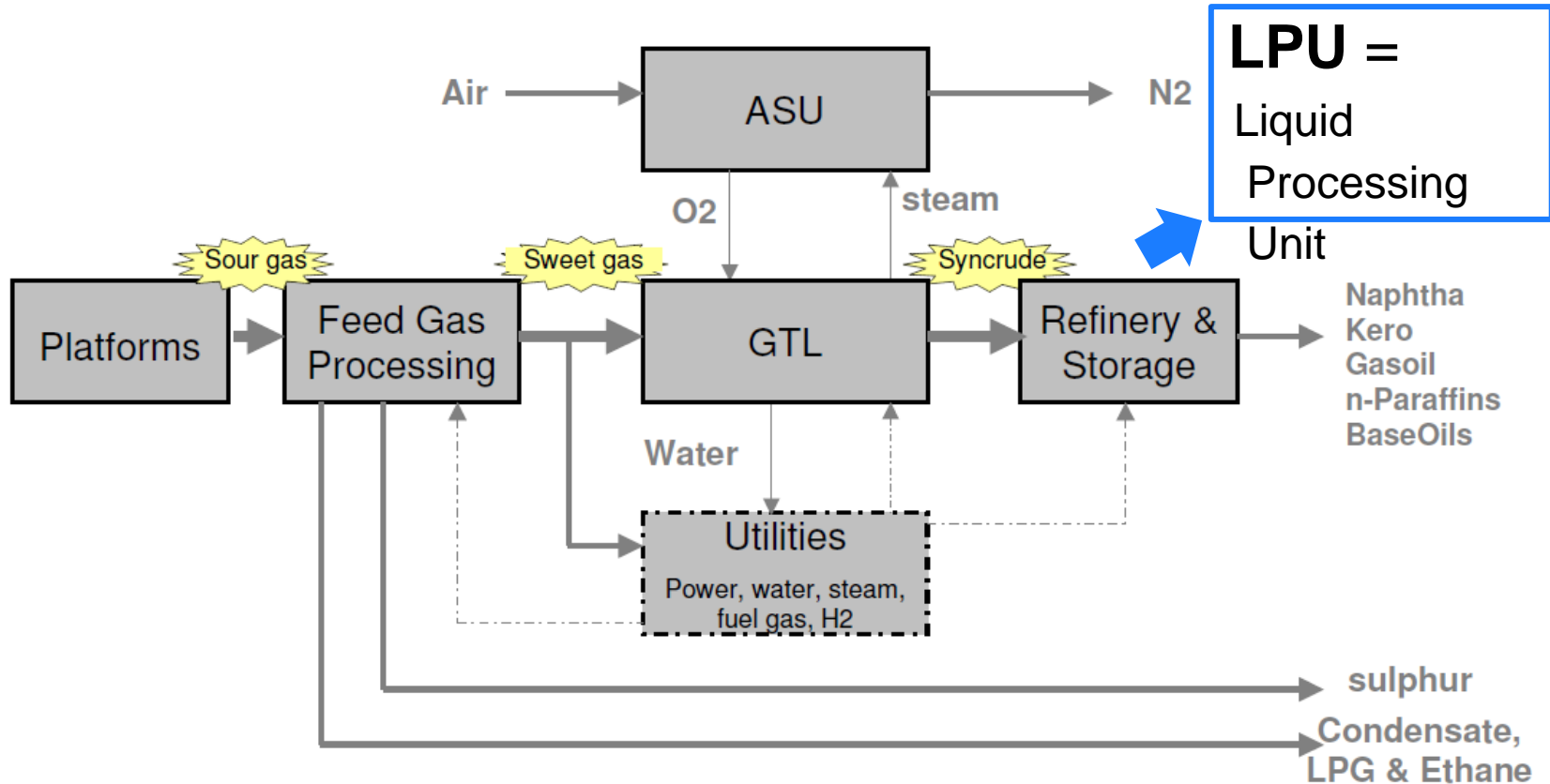
PEARL GTL – RAS LAFFAN, STATE OF QATAR



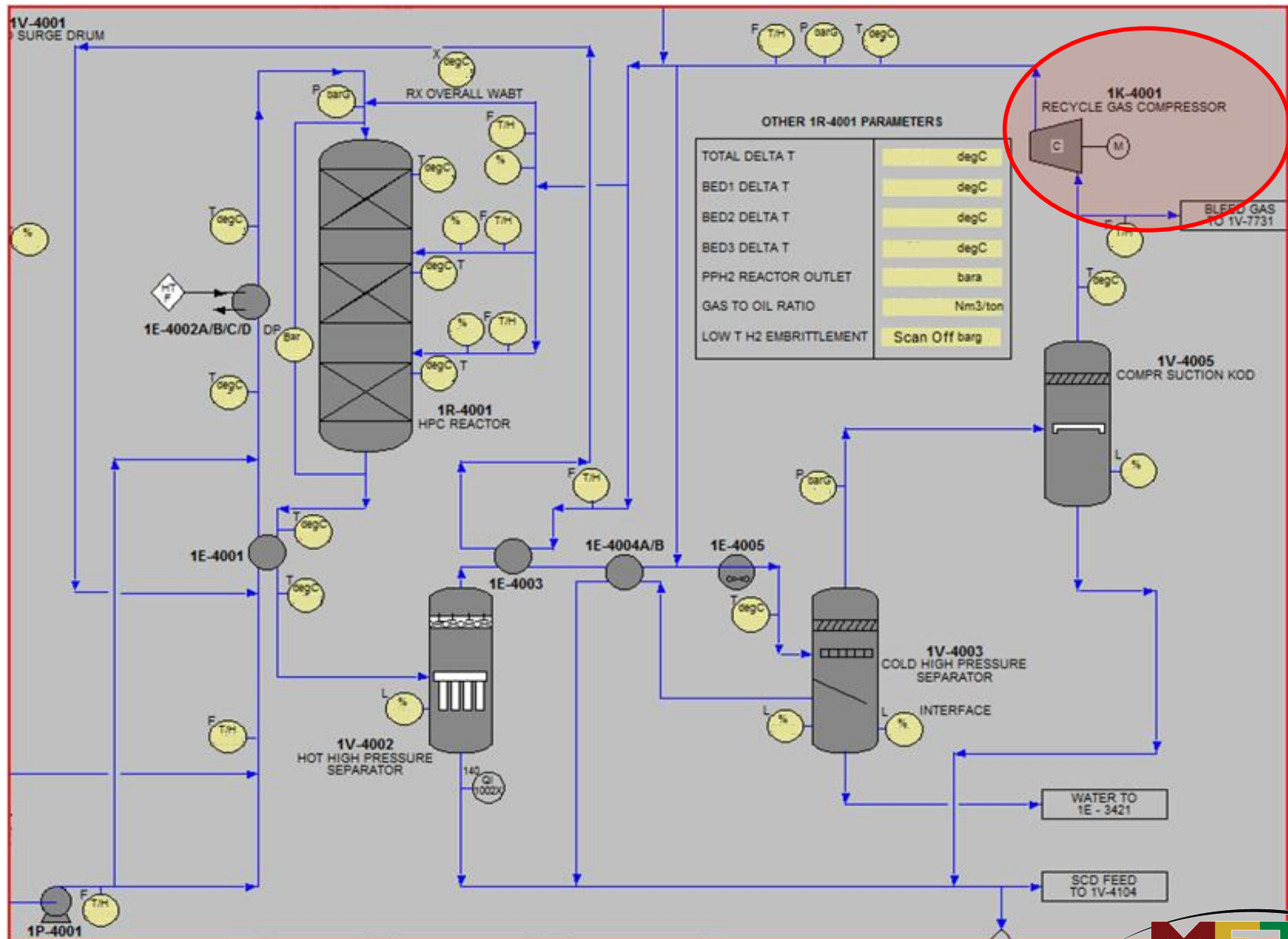
Aerial View of Pearl GTL plant at Ras Laffan, Qatar

PEARL GTL – HIGH LEVEL PROCESS FLOW

Simplified Process Integration Scheme



PEARL GTL – LPU – HYDROCRACKER



HYDROCRACKER - RECYCLE GAS COMPRESSOR- K4001

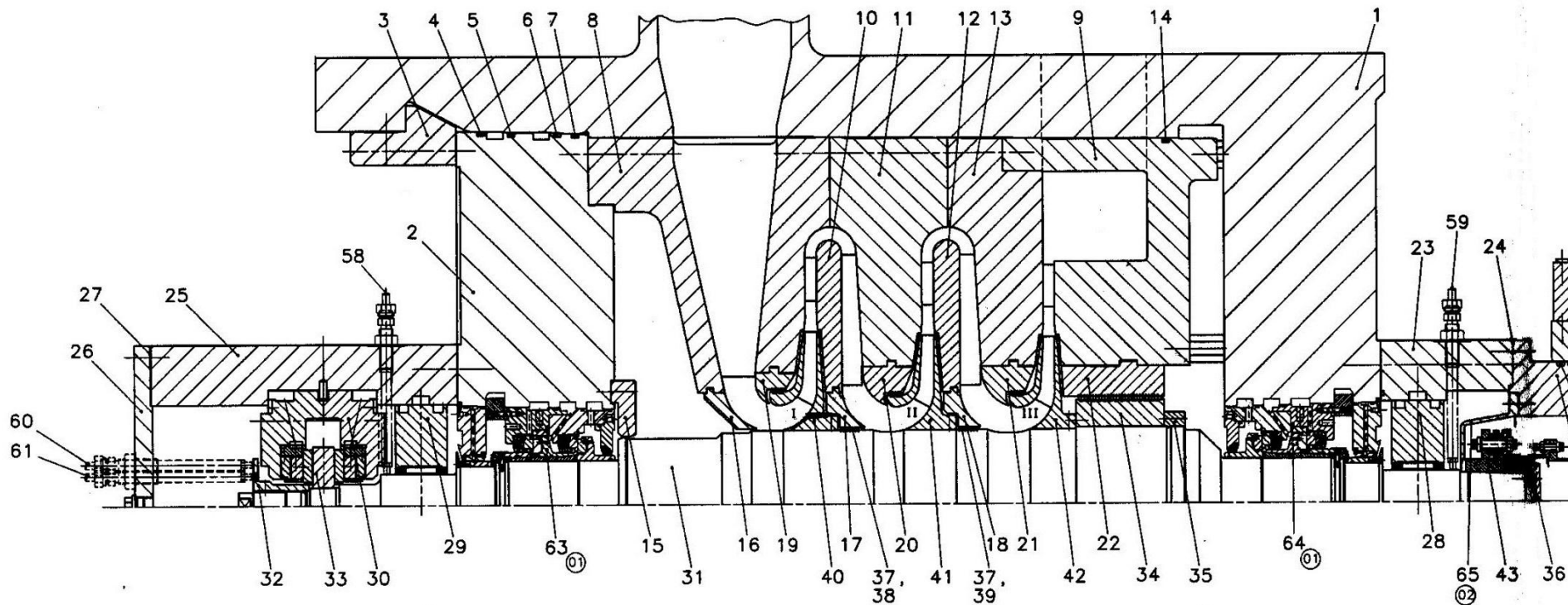
3 Stage Centrifugal Compressor – “Recycle Gas Compressor”

92 Bar (~1500 psi)

3.6 MW

Tilt Pad Journal Bearings and Tandem Dry Gas Seal with intermediate Laby

NC1 = 6 800 RPM MCOS = 11 718 RPM TRIP = 12 887 RPM



1K-4001 – HIGH VIBRATION DURING START-UP

Flawless Start-Up

Compressor had been run on N₂ (March) and completed H₂ loop dry out (early Apr)

Initial Start on Process Gas (H₂)

Compressor could not pass NC1 (6800 rpm) - Trip on High High Bearing Vibration

Start-Up Engineer and Operations implemented a “soft start” including a hold near 3500 rpm (*What would have happened if this was not a VSIDS?*)

Vibration level steadily dropped during hold, compressor was able to pass NC1

On subsequent days, effectiveness of soft start was repeated, and with minor tweaking, became the “normal” start-up procedure

Engineering Team Assembled to Understand Why

Same OEM had a similar compressor in H₂ service that does not have VSIDS

1K-4001 – HIGH VIBRATION DIAGNOSIS

Pearl GTL has fully configured Bently Nevada System1®

Pearl GTL staff spent many hours setting up and verifying plot sessions

Primary Characteristics of Vibration

Compressor had been run on N₂ (March)

Completed H₂ loop dry out (early April)

Low vibration levels and consistent behavior

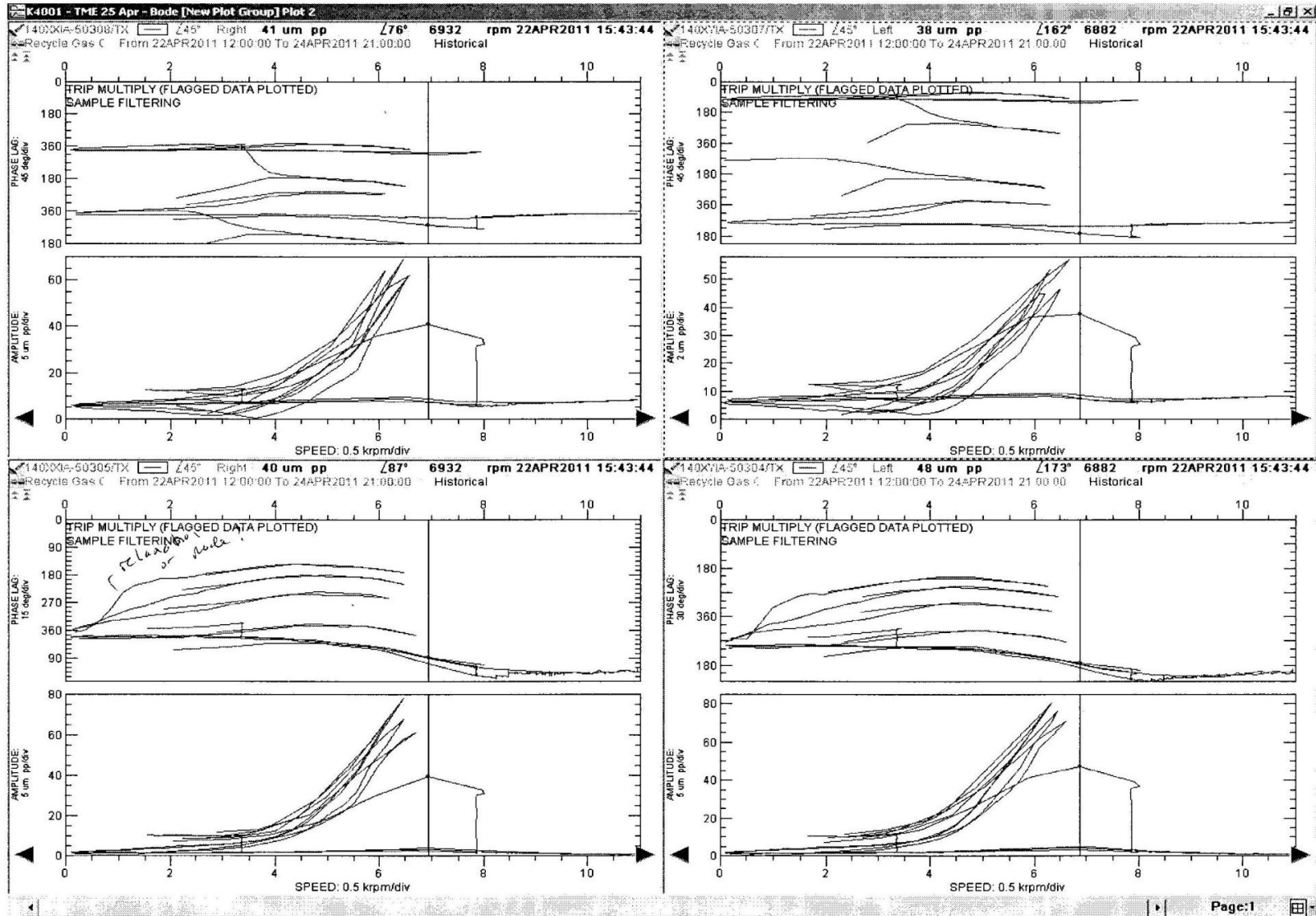
First run on process gas showed high level through NC1 (6 800 rpm)

Primarily 1x vibration (GREEN)

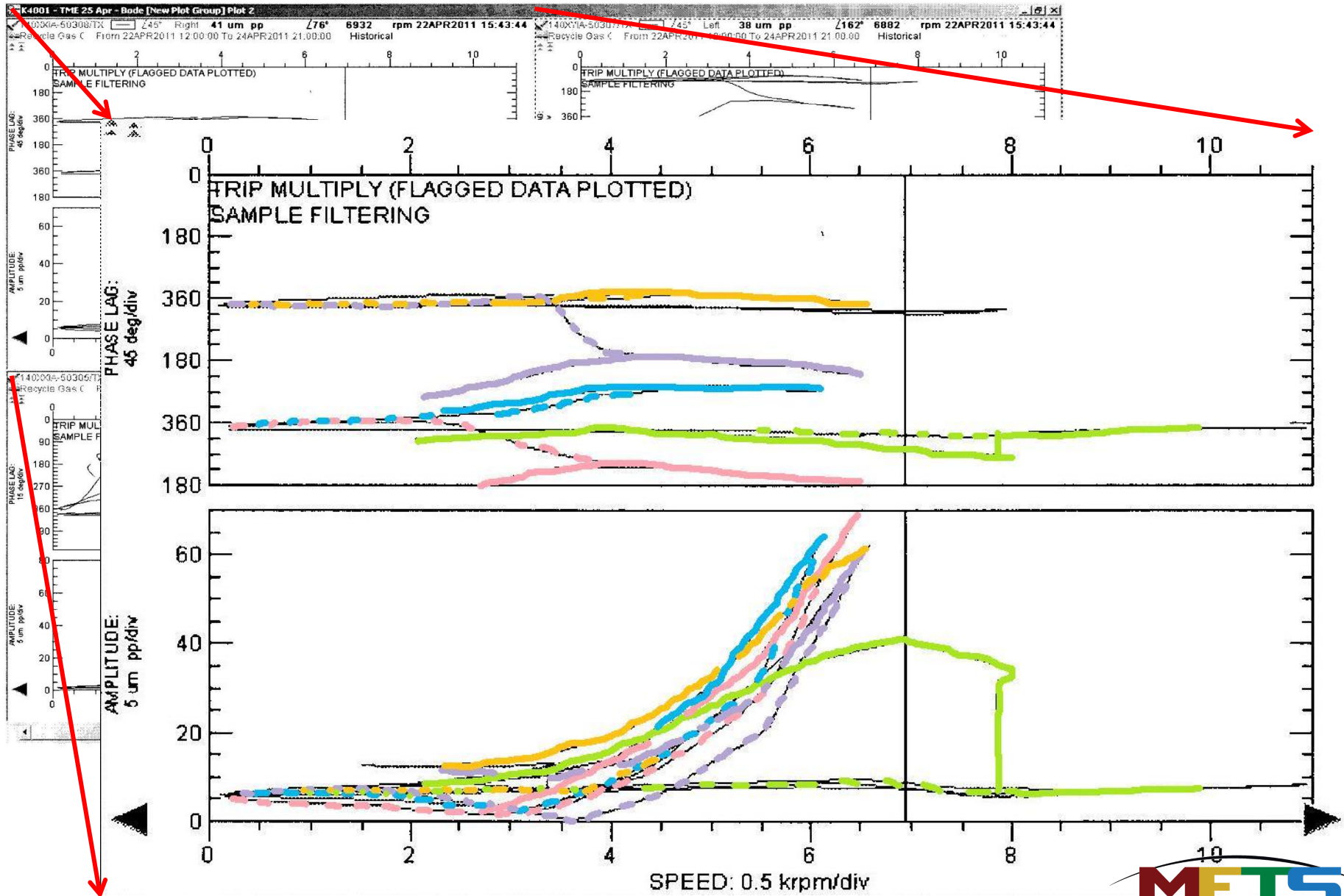
Subsequent attempts to start also primarily 1x vibration

(In plots that follow, Solid Line is Start-Up, Dashed Line is Shut-Down)

1K-4001 – HIGH VIBRATION DIAGNOSIS



1K-4001 – HIGH VIBRATION DIAGNOSIS



1K-4001 – HIGH VIBRATION DIAGNOSIS

Primary Characteristics of Vibration

Attempts to start could not pass NC1, primarily 1x vibration

High Vibration through NC1 suggests

Excess unbalance or high Amplification Factor (AF)

Possibly a rub (think how to break in seals on a steam turbine)

– typically not only 1x

Previous runs and Factory Test do not show high AF (lack of damping)

Bode plot, amplitude is consistent, phase is highly irregular

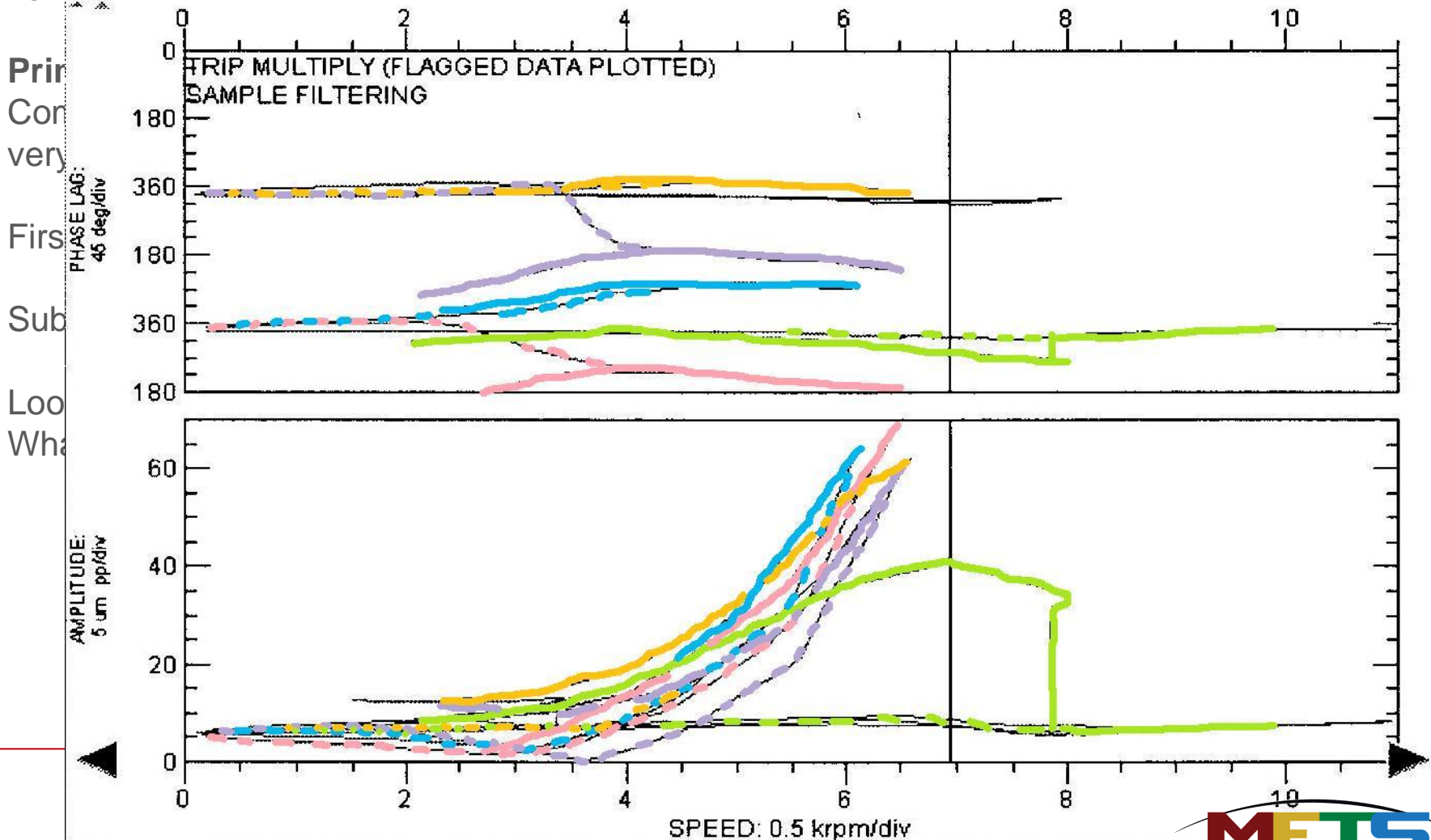
Phase: What are PURPLE and PINK doing?

Behavior at Start-up (Solid Line) and Shut-down (Dashed Line) appears different

1K-4001 – HIGH VIBRATION DIAGNOSIS

Pearl GTL has fully configured Bently Nevada System1

Tony Sobhy spent many hours setting up and verifying plot sessions on all equipment



1K-4001 – HIGH VIBRATION DIAGNOSIS

Primary Characteristics of Vibration

Looking at Bode plot – amplitude appears consistent, phase is highly irregular

Phase: What are PURPLE and PINK doing?

Behavior at Start-up (Solid Line) and Shut-down (Dashed Line) appears different

Our Goal is to tie Vibration Response to a Physical State or Behavior:

High Vibration through NC1 suggests excess unbalance or high AF

Previous runs do not show high AF => Excess Unbalance

What is causing the unbalance?

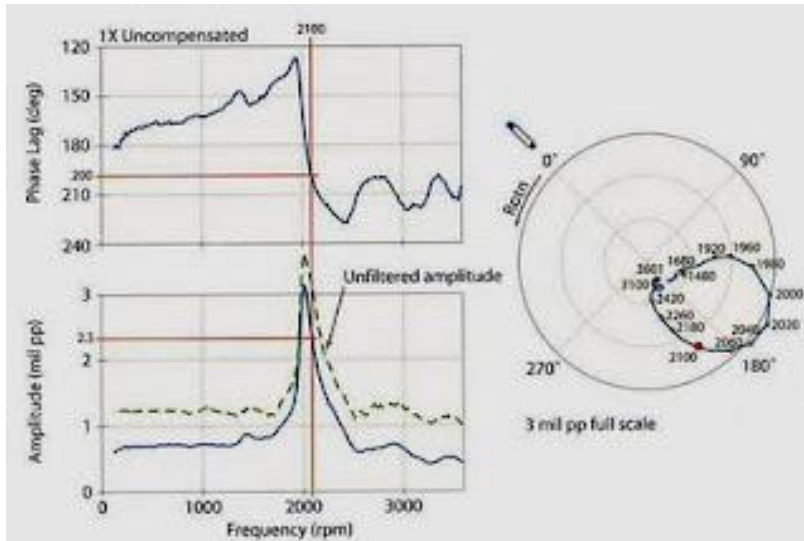
Where did it come from? (Why did it not appear in N₂ runs?)

Is there another way of looking at the data? **Yes: Polar Plot**

Shows same data (rpm, amplitude and phase), different graphical format

Polar Plot makes it clear the rotor starts and returns to same slow roll

POLAR AND BODE PLOTS



Polar and Bode plots show similar data

Natural Frequency or Resonance = peaking of amplitude and 180 phase shift

Bode – “Slide and Mountain”
Offers clear amplitude and AF comparison

Polar – “Loop”

Offers intuitive slow roll compensation

Polar and Bode plots show similar data

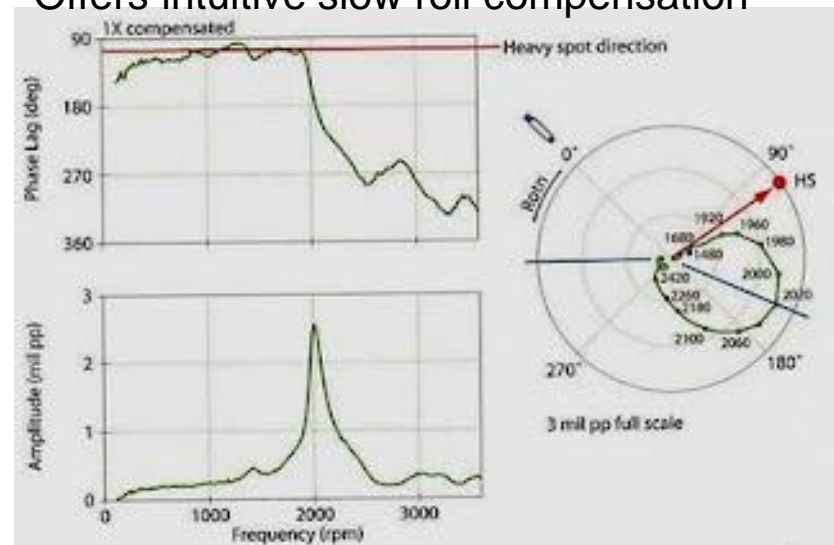
Unbalance Location

Initial direction of phase (compensated)

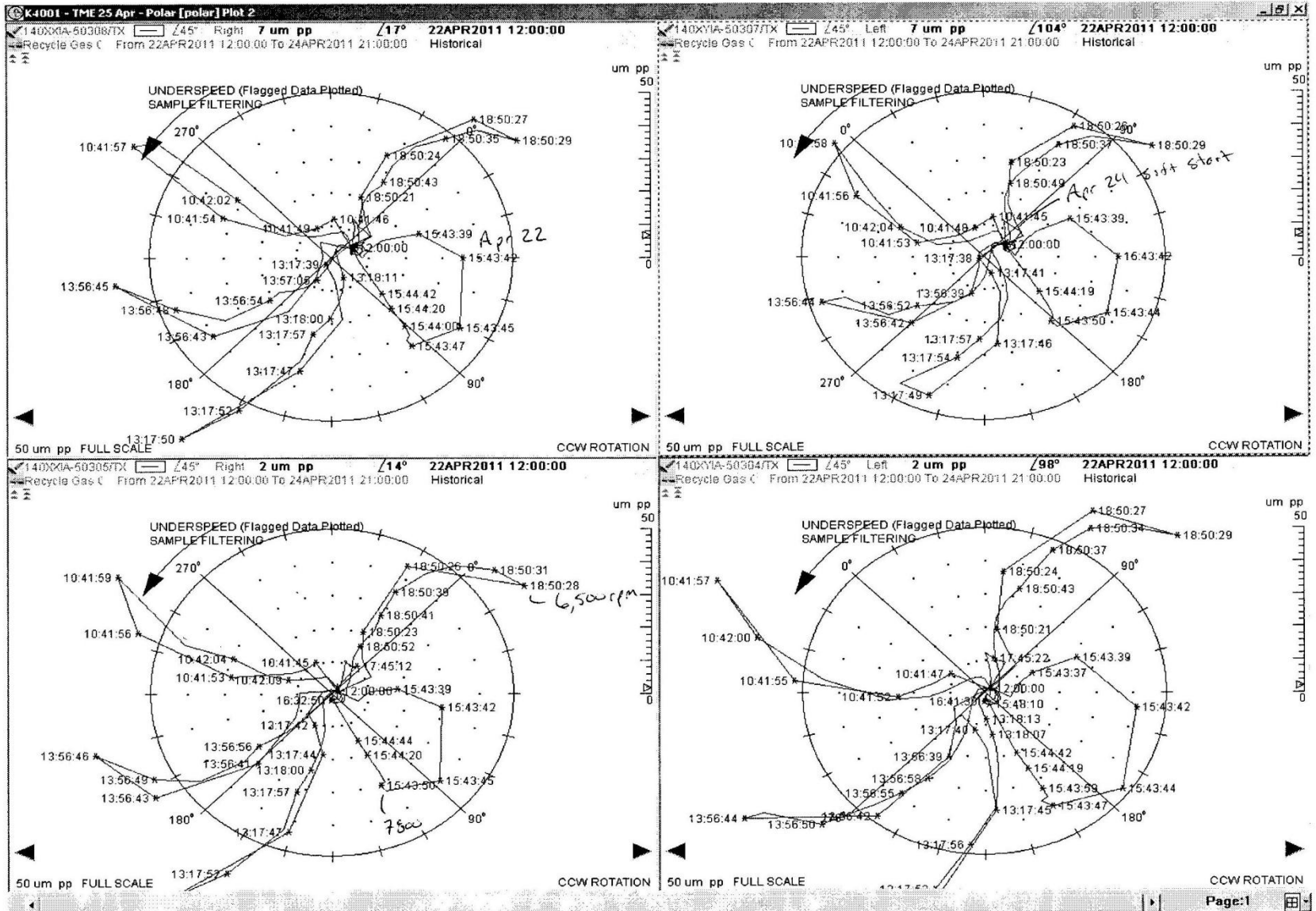
“High Spot follow Heavy Spot”

Bode – Need to properly 1x compensate for slow roll

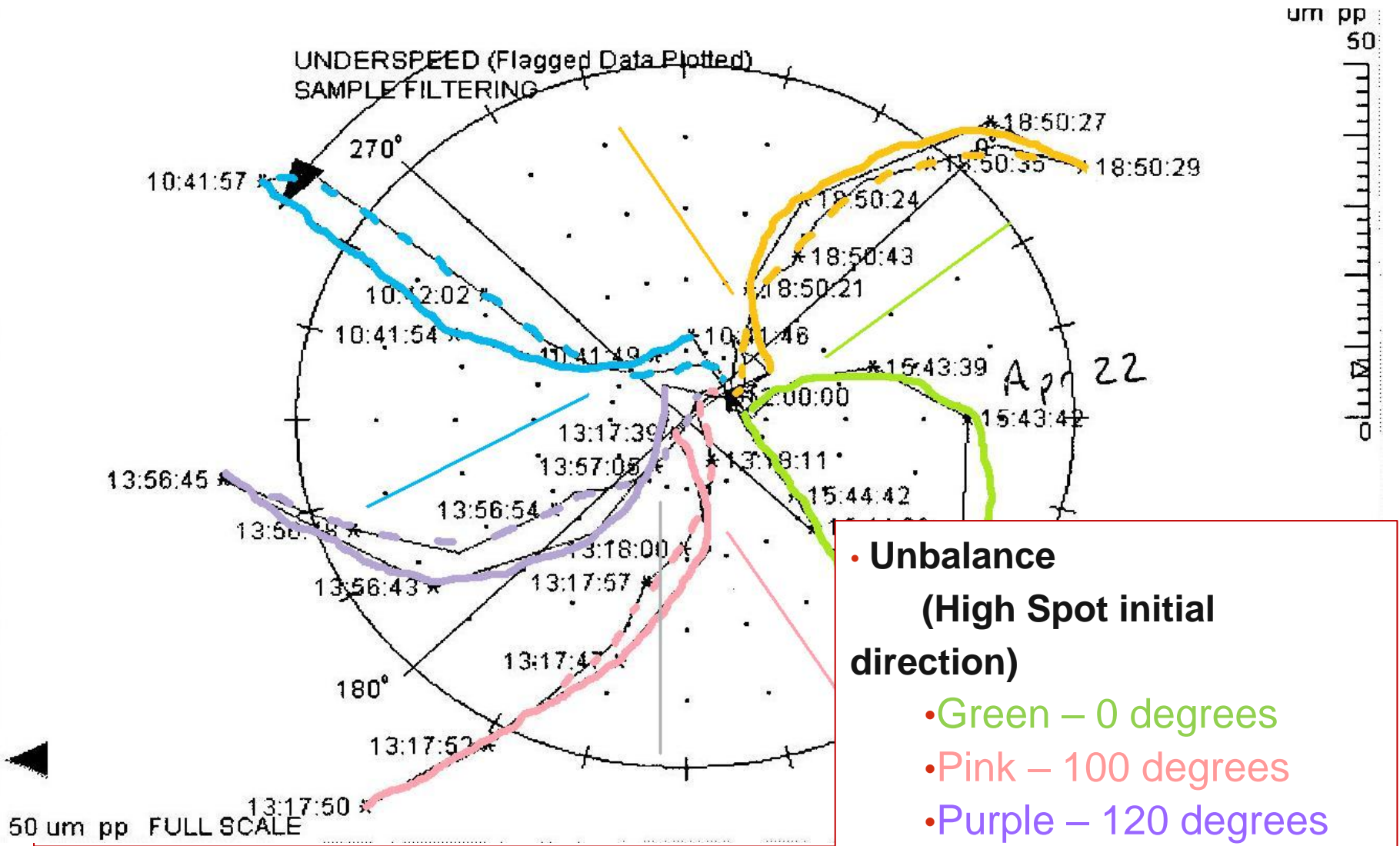
Polar – Unbalance Location and 1x compensation can be done intuitively



1K-4001 – HIGH VIBRATION DIAGNOSIS



1K-4001 – HIGH VIBRATION DIAGNOSIS



1K-4001 – HIGH VIBRATION DIAGNOSIS

Polar Plot

Behavior during start-up and shut-down is consistent, except
Phase Angle of initial Unbalance seems to Change with each start

Unbalance – Center of Mass offset from Centerline of Bearings

Mechanical or Residual Unbalance (fixed over speed, temp, starts)

Bow - deformation of the rotor shaft that causes centerline of rotor to shift off centerline of bearings (CoM assumed to be at center of rotor)

Mechanical Bow – “permanently” bowed due to initial processing, plastic deformation during handling (fixed over speed, temp, starts)

Thermal Bow – bowing of rotor due to heat-> temperature (fixed or random)

Gravity Sag Bow – rotor takes a “set” when not rotating (random orientation)

1K-4001 – HIGH VIBRATION DIAGNOSIS

Thermal Bow of rotor due to heat-> temperature (mixed)

Variety of sources:

Differential growth on opposite sides due to temperature difference

e.g. rub on high spot

Axial binding – lack of thermal axial gap between added components

e.g. seal rings and impellers

Internal, residual stresses or abnormality that result in non-isotropic growth

All repeatable: same circumferential location, phase angle, unbalance location

Gravity Sag Bow, rotor takes a “set” when stationary (random orientation!)

This is temporary – rotor will straighten as it rotates

Typically associated with heavy, long bearing span rotors

Worse with hot rotors, which is why Gas and Steam Turbines have turning gear

However - *This rotor is too short, too light, too cold...*

Similar Behavior was Described in:

Modeling of Rotor Bow During Hot Restart in Centrifugal Compressors

Baldassarre and Fontana, 39th Turbosymposium

1K-4001 – HIGH VIBRATION DIAGNOSIS

After multiple runs and attempts to start, team was able to establish:

If rotor sits for a moderate time, it establishes a bow – *not sure why*

With 5 minutes of roll-out, bow is relaxed and unbalance eliminated

This is effective method of dealing with the symptom

Strong motivation to identify root cause:

There is a narrow window between NC1 and TNF – delicate balance

Project has two other Hydrogen Compressors from same OEM, without VSIDS

Will not be able to hold and allow rotor to relax if same issue occurs

Look for Process Correlation:

Inlet Pressure

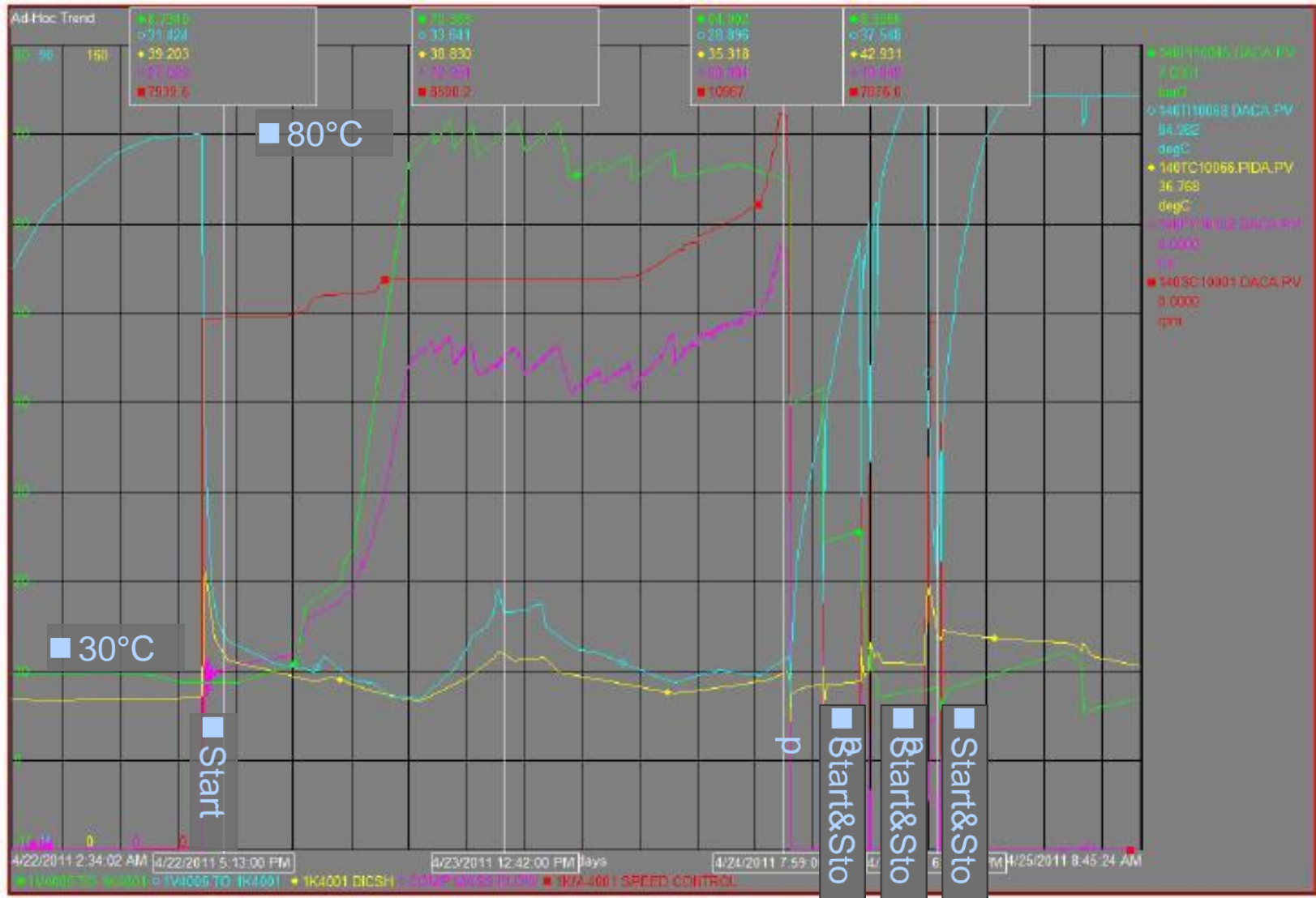
Discharge Pressure

Inlet Temperature (T_{in})

Discharge Temperature (T_{out})

T_{in} (Blue Line) Rises when unit stops, normal running is 30°C, stop is 80°C

1K-4001 – PROCESS CORRELATIONS



1K-4001 – PROCESS CORRELATIONS

Process Correlation =

Tin (Blue Line) Rises when unit stops

normal running is 30°C, stop is 80°C

Temperature falls rapidly when RPM rises

appears to be locally trapped heat

Build Spread Sheet with various inputs and parameters

Engineering Team found correlation with Seal Gas Heater

Had not been used during N₂ runs

Was only needed when drawing Seal Gas from Process (dew point)

During start-up, Seal Gas supplied by Plant N₂, no risk of liquids

Perform Test Run: Confirm when seal gas heater Off

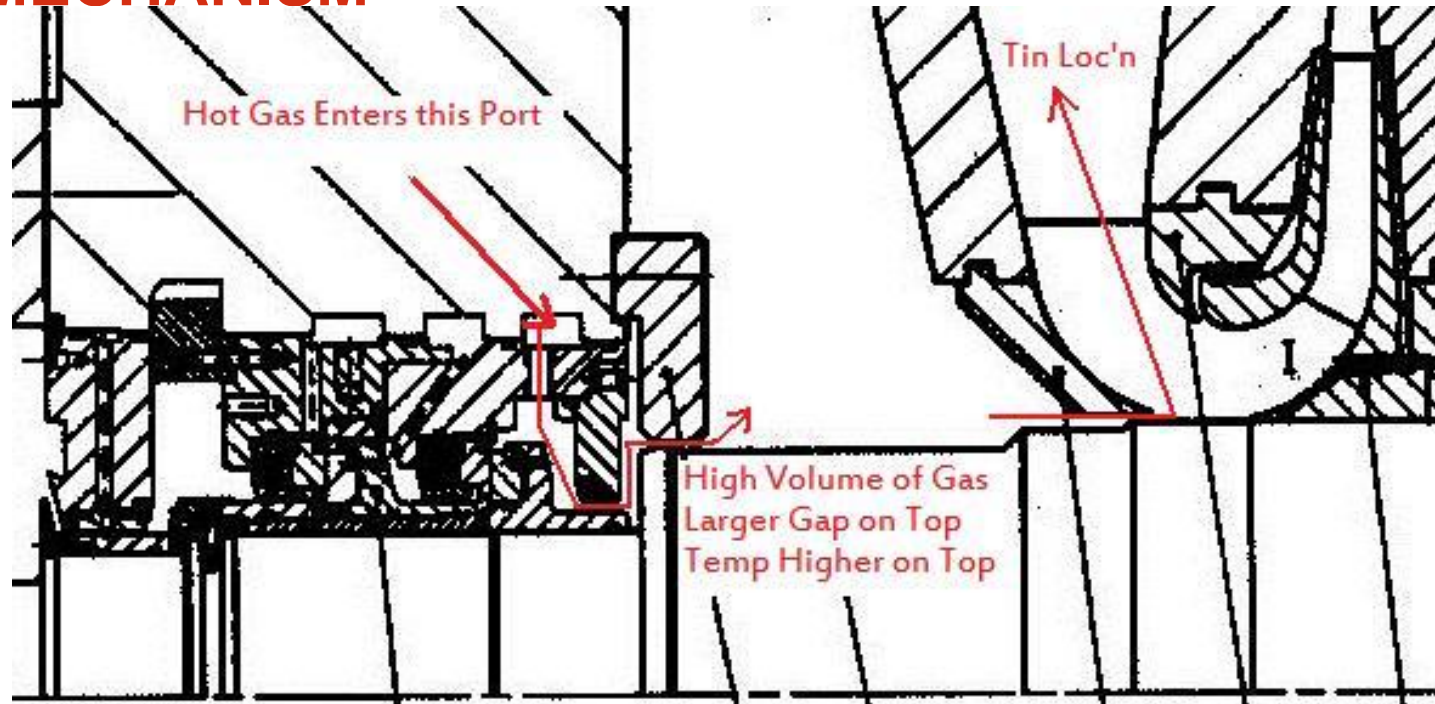
- Hold is not necessary (no bow present)

1K-4001 – PROCESS CORRELATIONS

1K-4001 LPU Start-up Problem Timeline

	DATE							
	3/17/2011	4/11/2011	4/22/2011	4/24/2011 - 1	4/24/2011 - 2	4/24/2011 - 3	4/24/2011 - 4	5/11/2011
Purpose	Mech Run ³	Dry Out	Process Run	Process Run	Process Run	Process Run	Process Run	Process Run
Run time	5hrs	5 days	2 days	HH trip on Start	HH trip on Start	1 hour	HH trip on Start	Running
Process Gas	N2	N2	Process Gas	Process Gas	Process Gas	Process Gas	Process Gas	Process Gas
Line up	Long Loop	Long Loop	Long Loop	Long Loop	Long Loop	Long Loop	Long Loop	Long Loop
Previous start (before)	First	13 days	5 days	2 hours	2 hours	4 hours	30 min.	3.5days running
Compressor:								
Ts, degC	20	24,31,24	85 initial, 24 normal	85	85	85 initial, 24 normal	45	85
Td, degC	66-103	110 ¹ ,73,63	55 initial, 31 normal	39	43	55 initial, 31 normal	41	46
rpm		8022-8067	7934- 8900			8534		11700 ⁹
Start Type:								
Fast	Yes ⁴	Yes	Yes	Yes	Yes		Yes ⁶	
Slow						Yes		Yes to 4000rpm
SU Vibration:								
Initial "Bump"	yes, 28um	Yes, 20um	Yes, 23um	Yes, 22um	Yes, 24um	Yes, 25um	Yes, 26um	yes,23um
Nc (6500rpm)	Very Low	Low but chng ²	Yes 48um	yes, 80um	Yes, 79um	Uneventful ⁵	Yes, 70um	Uneventful
H or HH alarms"	No	No	H alarm	HH trip on Start	HH trip on Start	No	HH trip on Start	No
Vib "Relax"	Yes	Yes, very low	Yes	Trip no data	Trip no data	yes "slow roll"	Trip no data	yes "at slow roll"
"Relax rpm"	7876	7876	7876			3471		4000
Primary Seal Gas:								
Type Gas	N2	N2	H2	H2	H2	H2	H2	H2
T, deg C	19	28	105	105	105	?	105	55
P, barg	3barg>Ps	3barg>Ps	3barg>Ps	3barg>Ps	3barg>Ps	3barg>Ps	3barg>Ps	3barg>Ps
Heater	off	off	On	On	On	off	on	off
Lube Oil:								
P, barg	1.6	1.6	1.6	1.6	1.6	1.6	1.6	1.6
T, deg C	42	42	42	42	42	42	42	39

1K-4001 – DIFFERENTIAL HEATING – BOW MECHANISM



Seal Gas Heater – Injects a Large Volume of Hot Gas =>

Larger gap at Top of Inner Seal => more heat and Temperature Rise on Top
Top vs Bottom Differential Temperature causes a *Temporary Thermal Bow*
As shaft rotates, heat becomes distributed, temperature equalizes, bow
straightens, eventually Unbalance is Eliminated and Vibration Decreases

CONCLUSION

- Significant Value in Categorizing Vibration
- Use a variety of plots
- Establish Slow Roll vector and Repeatability
- Determine if vibration change on sequential runs
- Find correlation to Process or other Environmental Variables

- Get Help!
 - Others at Facility or within Company
 - Industry Experts (like those you meet at METS!)

ACKNOWLEDGEMENTS

The Authors would like to thank Royal Dutch Shell and QatarShellGTL for their support in this endeavor.

We appreciate the State of Qatar and Texas A&M for sponsoring METS and the opportunity to share knowledge and learning with our colleagues.