

1 **Selective catalytic reduction of NO_x with NH₃ over short-range ordered W-O-Fe structures**
2 **with high thermal stability**

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4 Ying Xin¹, Nana Zhang¹, Qian Li¹, Zhaoliang Zhang^{1,*}, Xiaoming Cao², Lirong Zheng³, Yuewu
5 Zeng⁴, James A. Anderson^{5,*}

6
7 ¹ School of Chemistry and Chemical Engineering, Shandong Provincial Key Laboratory of
8 Fluorine Chemistry and Chemical Materials, University of Jinan, Jinan 250022, China

9 ² Center for Computational Chemistry, School of Chemistry and Molecular Engineering, East
10 China University of Science and Technology, Shanghai 200237, China

11 ³ Institute of High Energy Physics, Chinese Academy of Sciences, Beijing 100049, China

12 ⁴ Center of Electron Microscopy and State Key Laboratory of Silicon Materials, Zhejiang
13 University, Hangzhou 310027, China

14 ⁵ Surface Chemistry and Catalysis Group, Materials and Chemical Engineering, University of
15 Aberdeen, AB24 3UE, United Kingdom

16
17
18 *Corresponding authors:

19 Zhaoliang Zhang: chm_zhangzl@ujn.edu.cn

20 James A. Anderson: j.anderson@abdn.ac.uk

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22

23 **Abstract**

24 The selective catalytic reduction (SCR) of NO_x with NH_3 was studied over poorly-
25 crystalline W-Fe composite oxides (W_aFeO_x). The short-range order present within the W-O-
26 Fe structure was found to be responsible for the excellent SCR activity, in which the strong
27 atomic-level interaction between Fe and W atoms promoted the formation of both Lewis and
28 Brønsted acidity. The W-O-Fe structure existed as amorphous overlayers, approximately 2 nm
29 thick over the surface of crystalline particles after high-temperature aging as shown by high-
30 angle annular dark field scanning transmission electron microscopy (HAADF-STEM). After
31 treatment at 800°C for 5 h, the W_aFeO_x catalysts still showed almost 100% NO conversion in
32 the range $300\text{-}450^\circ\text{C}$ with 100% N_2 selectivity, despite the loss in surface area. This resistance
33 to the impacts of high temperature ageing guarantees high activity of SCR catalysts which
34 often suffer during high-temperature excursions as in the case of diesel exhaust due to diesel
35 particulate filter (DPF) regeneration.

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37 **Keywords:** Nitrogen oxides; Selective catalytic reduction; Ammonia; Short-range order; High
38 thermal stability

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46 **1. Introduction**

47 Nitrogen oxides (NO_x , referring to NO and NO_2) are major air pollutants, which contribute to
48 environmental issues such as acid rain, photochemical smog, atmospheric oxidant ozone increase
49 and haze and harm human health [1, 2]. To reduce these effects, the removal of NO_x from
50 anthropogenic sources including stationary (coal-fired power plants, etc.) and mobile sources
51 (motor vehicles) is crucial. Selective catalytic reduction (SCR) of NO_x with NH_3 has proved to
52 be an efficient means of reducing NO_x emission (deNO_x) [3-5]. $\text{V}_2\text{O}_5\text{-WO}_3/\text{TiO}_2$ is the most
53 widely used NH_3 -SCR catalyst, which has been commercialized for deNO_x . However, the
54 disadvantages including the toxicity of vanadium, the narrow operational temperature window,
55 and the deterioration of the structure and constituents after high-temperature aging, restricts its
56 wider application [6, 7]. Development of new catalysts with improved NH_3 -SCR performance
57 and research on active site identification continues. Amorphous active catalysts/active species
58 have attracted considerable attention due to their high activity.

59 As early as 1990s, the amorphous Cr_2O_3 catalyst was reported to exhibit superior SCR activity
60 and N_2 selectivity compared to its crystalline counterpart [8, 9]. In 2007, Tang *et al.* found that
61 the amorphous phase of MnO_x was much more active than its crystalline counterpart at low
62 temperatures [10]. Similar phenomena were also found for composite oxides, for example,
63 amorphous Mn and Ce species were thought to be responsible for SCR activity in Mn-supported
64 TiO_2 [11, 12], and Ce-Ti mixed oxides [13-15], respectively. Significantly, the consensus for
65 composite oxides is that short-range ordered structure is the location of active sites, as in Fe-
66 O-Ti [16-18], Ce-O-Ti [19], and Ce-O-W [20] systems, thereby highlighting the pivotal role of
67 atomic-scale interaction.

68 It is well known that the amorphous structure is characterized by the absence of long-range
69 order [21], which is metastable and readily transformed into the crystalline phase or is
70 to phase separation after high-temperature treatment [22]. Both transformations generally lead
71 to decreased SCR activity [10, 14]. For instance, during the diesel particulate filter (DPF)
72 regeneration, the diesel exhaust gas temperature occasionally rises above 600°C, which may
73 causes severe deactivation of V₂O₅-WO₃/TiO₂ catalysts [23]. Hence, the thermal stability of an
74 SCR catalyst is crucial if it is to withstand such harsh environment. In this study, short-range
75 ordered W-O-Fe active species in poorly-crystalline W-Fe composite oxides (W_aFeO_x) have
76 been developed which exhibit excellent NH₃-SCR activity. Most importantly, the W-O-Fe
77 structure was retained on the surface of a crystalline phase even after aging at 800°C for 5 h.
78 Despite a significant loss in surface area, NO conversion in the range 300-450°C was close to
79 100% with 100% N₂ selectivity. These findings demonstrate the importance of fabrication of
80 materials with short-range ordered W-O-Fe structure, which are highly dispersed at the
81 outermost surface layer of crystallites after high-temperature and long-term operation.

82

83 **2. Experimental**

84 **2.1 Sample preparation**

85 The W_aFeO_x catalysts (with a W/Fe atomic ratio of *a*, ICP data) was prepared by a co-
86 precipitation method using an aqueous solution of sodium tungstate (Na₂WO₄·2H₂O, 200 mL)
87 and ferrous sulfate (FeSO₄·7H₂O, 100 mL) with ammonium hydroxide (NH₃·H₂O, 25-28
88 wt.%) at 35°C, with the pH of the precipitation process maintained above 6.0 and that of the
89 resulting solution maintained at 9.0. The total amount of the metallic salt precursor was 0.03
90 mol. Ascorbic acid (C₆H₈O₆, 100 mg) was added to the initial iron precursor solution to mol.

91 ascorbic acid ($C_6H_8O_6$, 100 mg) was added to the initial iron precursor solution to enhance the
92 reducibility of the Fe^{2+} . The obtained slurry was aged at $35^\circ C$ with stirring for 3 h and
93 subsequently filtrated and washed. The resulting solid was dried overnight at $70^\circ C$ and calcined
94 at $500^\circ C$ (or $800^\circ C$) for 5 h. For comparison purposes, Fe_2WO_6 was prepared by calcination of a
95 stoichiometric mixture of iron oxide and tungsten oxide [24]. The mechanically mixed catalyst
96 (Fe_2O_3 -800+ Fe_2WO_6) is thought to simulate the ideal $W_{0.13}FeO_x$ catalyst with complete
97 crystallization.

98 **2.2 Sample characterization**

99 X-ray diffraction (XRD) patterns were recorded on a Rigaku D/max-2500/PC diffractometer
100 employing Cu $K\alpha$ radiation ($\lambda = 1.5418 \text{ \AA}$) operating at 50 kV and 200 mA. The Brunauer-
101 Emmett-Teller (BET) surface area and pore structure were measured by N_2
102 adsorption/desorption using a Micromeritics 2020 M instrument. Before N_2 physisorption, the
103 sample was outgassed at $300^\circ C$ for 5 h. Inductively coupled plasma-atomic emission
104 spectrometer (ICP-AES) experiments were carried out on the IRIS Intrepid IIXSP instrument
105 from Thermo elemental. Field emission scanning electron microscope (FESEM) was performed
106 on a Hitachi SU-70 microscope. High-resolution transmission electron microscopy (HRTEM)
107 equipped with selected area electron diffraction (SAED) and energy dispersive X-ray analysis
108 (EDX) was conducted on a JEOL JEM-2010 microscope at an accelerating voltage of 200 kV.
109 High-angle annular dark field scanning transmission electron microscopy (HAADF-STEM)
110 images were recorded in a Tecnai F20. X-ray photoelectron spectroscopy (XPS) data were
111 obtained on an AXIS-Ultra instrument from Kratos Analytical using monochromatic Al $K\alpha$
112 radiation (225 W, 15 mA, 15 kV) and low-energy electron flooding for charge compensation. To
113 compensate for surface charge effects, the binding energies were calibrated using the C 1s

114 hydrocarbon peak at 284.80 eV. X-ray absorption fine structure (XAFS) measurements at the
115 W L_{III}-edge and Fe K-edge were performed in the transmission mode and fluorescence mode
116 at room temperature on the XAFS station of the 1W1B beamline of Beijing synchrotron
117 radiation facility (BSRF, Beijing, China), respectively. XAFS data were analyzed using
118 IFEFFIT software package [25]. In the least-squares-fitting procedure, the possible scattering
119 paths were also calculated using this software package.

120 Temperature-programmed reduction in H₂ (H₂-TPR) was performed in a quartz reactor with
121 a thermal conductivity detector (TCD) to monitor the H₂ consumed. A 50 mg sample was
122 pretreated *in situ* at 500°C for 1 h in a flow of O₂ and cooled to room temperature in the same
123 gas. TPR was conducted at 10°C/min to 900°C in a 30 mL/min flow of 5 vol.% H₂ in N₂. CuO
124 was used as a calibration reference.

125 The temperature-programmed desorption of NH₃ (NH₃-TPD) experiments were performed
126 in a quartz reactor using 50 mg catalyst. NH₃ was monitored using a quadrupole mass
127 spectrometer (MS; OmniStar 200, Balzers) with m/z=16. Prior to the experiments, the samples
128 were pretreated at 500°C for 30 min in 10 vol% O₂/He (50 mL/min) and cooled to 100°C.
129 Sample was exposed to 0.4 % NH₃ (50 mL/min) until the outlet NH₃ concentration was stable.
130 The samples were then purged with He to remove any weakly absorbed NH₃ and then the
131 heated to 800°C at 10°C/min.

132 The *in situ* FTIR spectra of reaction were recorded using a Bruker Tensor 27 spectrometer
133 over the range 4000-400 cm⁻¹, with 16 scans, at a resolution of 4 cm⁻¹. Self-supporting wafers
134 were pretreated in the IR cell at 500°C in a flow of He for 30 min to remove adsorbed species.
135 After cooling to room temperature (RT) or 100°C, the background spectrum was recorded.
136 The IR spectra were recorded at RT or 100°C in a flow of 500 ppm NH₃ + He (150 mL/min)

137 or 500 ppm NO + 500 ppm NH₃ + 5.3 % O₂ + He (300 mL/min). Samples were then heated to
138 450°C at 10°C/min.

139 **2.3 Catalytic testing**

140 The steady state SCR and NO oxidation activity over W_aFeO_x catalysts was tested in a fixed-
141 bed quartz tube reactor (6.0 mm i.d.) with a thermocouple placed inside catalysts in the
142 temperature range of 150-500°C. In the SCR reaction, the model flue gas consisting of 500 ppm
143 NO, 500 ppm NH₃, 5.3 vol.% O₂, 10 vol.%, and balanced with He. The total flow rate
144 maintained at 300 mL/min, corresponding to a gas hourly space velocity (GHSV) of 50000 h⁻¹.
145 In the case of NO oxidation, the feed consisted of 500 ppm NO, and 5 vol.% O₂ with He as
146 balance. The total flow rate kept at 100 mL/min and the same GHSV (50000 h⁻¹) was used.
147 Concentrations of NO and NO₂ were monitored by chemiluminescence analyzer (42i-HL,
148 Thermo). N₂O and NH₃ were detected by a quadrupole mass spectrometer (MS, OmniStar 200,
149 Balzers) using the m/z signals of 44 for N₂O, and 17 for NH₃. The data for steady-state activities
150 of catalysts were collected after ca. 1 h on stream. **The durability tests of the catalysts were**
151 **performed in the SCR reaction feed at 300°C for 12 h.**

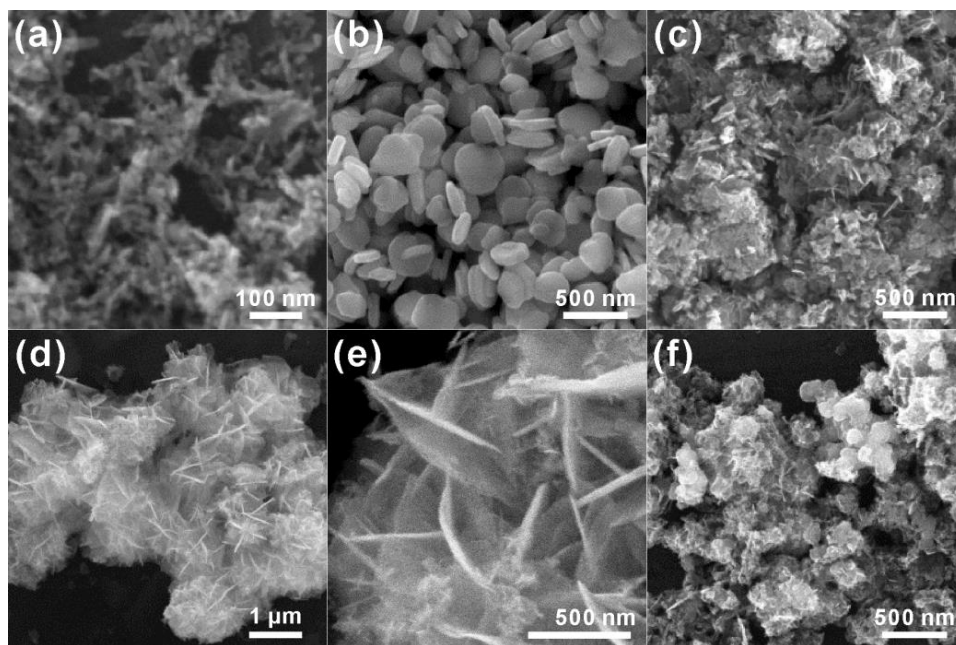
152 The reaction rate was measured using the same conditions as for steady-state reaction.
153 However, in this case, the powder samples were pressed, crushed and sieved (100-200 mesh)
154 prior to use. The GHSV was estimated as 200,000 h⁻¹. Isothermal reactions at 180°C were
155 conducted at a stable and low NO_x conversion (≤15%) ensuring operation within the kinetic
156 regime.

157

158 **3. Results and discussion**

159 XRD patterns of W_aFeO_x show the presence of few Fe_2O_3 microcrystals in the large-scale
160 amorphous phase [26]. Strong interaction between W and Fe in the W_aFeO_x inhibits
161 crystallization of the individual components during the precipitation process, and results in
162 much higher surface areas [19, 26, 27] and gives rise to the geometry and morphology changes
163 observed (Figure 1). The 3D flower-type structure of W_aFeO_x is composed of numerous
164 irregular nanosheets which randomly stack together. The HAADF-STEM image and
165 corresponding elemental mapping confirmed that the W atoms are incorporated into the
166 rhombohedral matrix of Fe_2O_3 [26].

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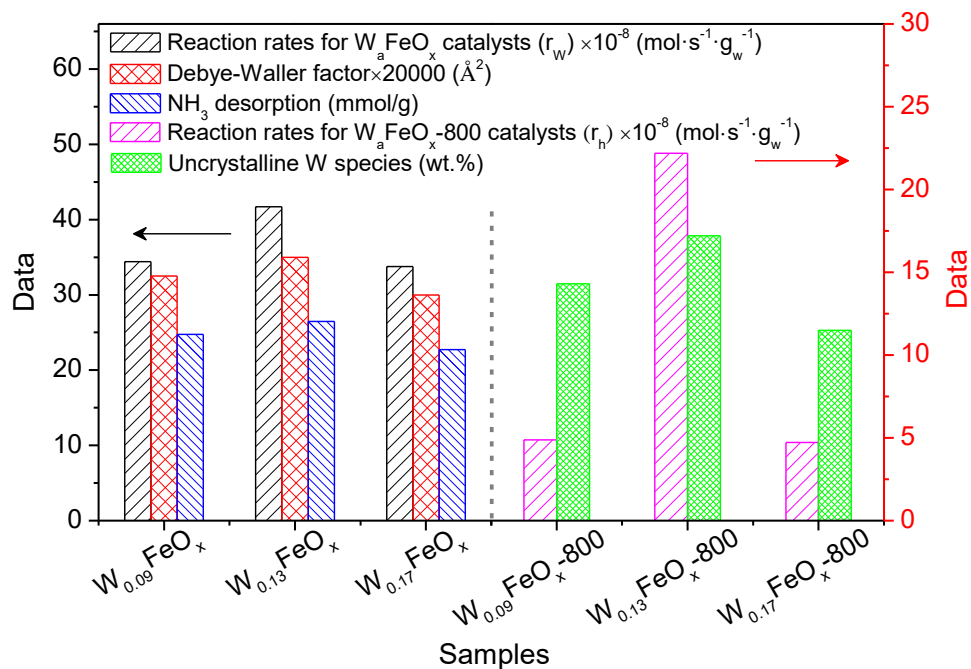
169 **Figure 1.** SEM images of W_aFeO_x catalysts: (a) Fe_2O_3 , (b) WO_3 , (c) $W_{0.09}FeO_x$, (d, e) $W_{0.13}FeO_x$,
170 and (f) $W_{0.17}FeO_x$.

171

172 XAFS spectra were measured in order to obtain information about the local environment
173 around the specific atoms in poorly-crystalline W_aFeO_x [19, 28]. The Fe K-edge XANES

174 spectra and RSF curves for Fe_2O_3 and W_aFeO_x are similar, indicating that the Fe atoms in
 175 W_aFeO_x are trivalent and exhibit octahedral (O_h) coordination, similar to Fe_2O_3 (Figure S1a)
 176 [26]. In the case of the W L_{III} -edge, the peak position and shape of the normalized XANES and
 177 RSF curves for W_aFeO_x correspond with those of Fe_2WO_6 , which implies that most of the
 178 hexavalent W atoms in W_aFeO_x exist in the same O_h coordination environment as that of
 179 Fe_2WO_6 anions (Figure S1b and c), namely forming W-O-Fe short-range ordered structure [29].
 180 The lower intensity of the RSF curves can be attributed to the higher local disorder level for
 181 W_aFeO_x [30]. Notably, the disordered structure is strongly reflected in the Debye-Waller factor
 182 (DWF, σ^2), a term appearing in the EXAFS equation that accounts for the level of disorder of a
 183 given sample [31, 32]. DWFs for W_aFeO_x were obtained by quantitative curve fitting in R-space
 184 of the W L_{III} -edge EXAFS spectra (Figure 2, Figure S1c and Table S1).

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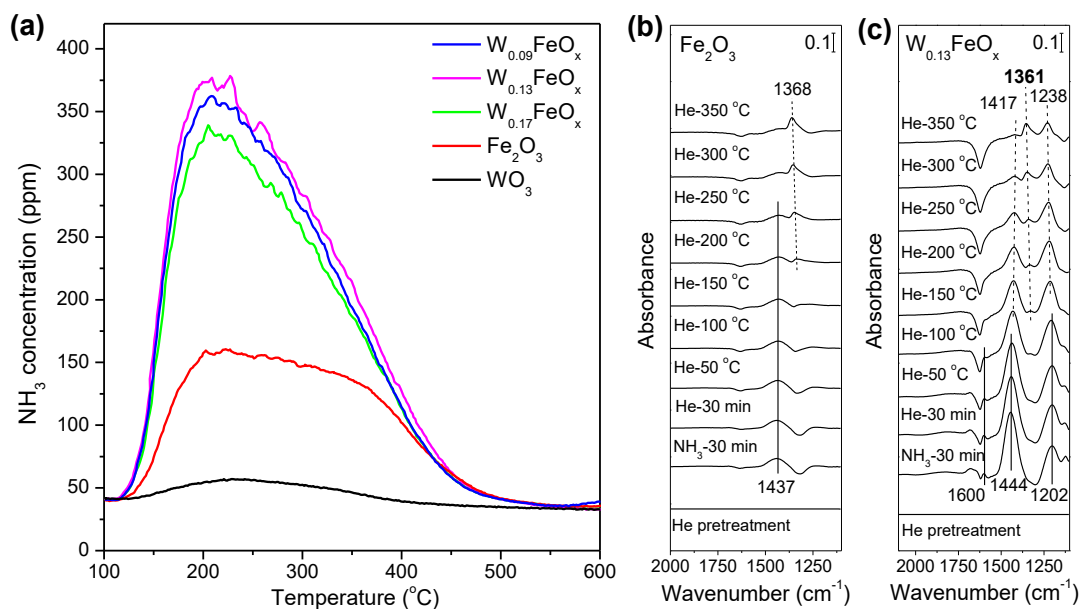


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187 **Figure 2.** Reaction rates normalized by W contents (r_w), Debye-Waller factor (DWF), NH_3
 188 adsorption amount for W_aFeO_x catalysts; reaction rates (r_h) and amount of non-crystalline W
 189 species for W_aFeO_x -800 catalysts.

190
 191 In our previous studies [26], W_aFeO_x promoted NO conversion at low temperature
 192 compared with Fe_2O_3 and WO_3 due to the higher surface area and surface W/Fe atomic ratios
 193 (Table S2). In the present work, the reaction rates of W_aFeO_x normalized by W content (r_w)
 194 were measured to provide a reliable correlation between the intrinsic activity and the amount
 195 of W-containing species. As shown in Figure 2, the r_w at 180°C shows a clear positive
 196 correlation with the DWF for W_aFeO_x , suggesting that the W-O-Fe structure acts as the active
 197 sites for W_aFeO_x catalysts, as all W atoms participate in the formation of the W-O-Fe
 198 structure.

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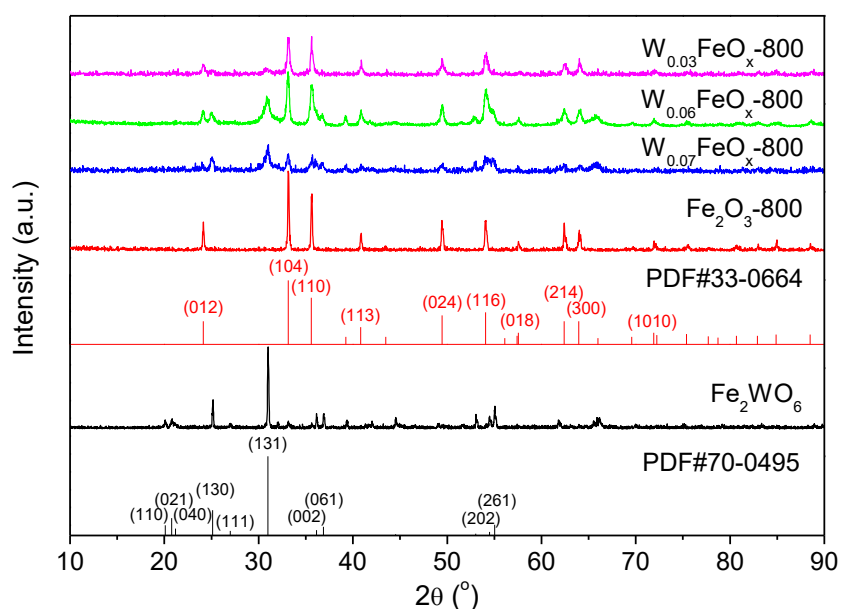
201 **Figure 3.** (a) NH₃-TPD profiles for Fe₂O₃, WO₃, and W_aFeO_x catalysts; *in situ* FTIR spectra of
202 NH₃ exposed to (b) Fe₂O₃ and (c) W_{0.13}FeO_x at room temperature and subsequently heated to
203 350°C in a flow of He.

204
205 To further clarify how the chemical properties of W_aFeO_x were improved by the presence of
206 short-range ordered W-O-Fe structures, the redox properties and acidity were assessed, as these
207 are key characteristics associated with the SCR activity [7, 33-35]. As shown in the H₂-TPR
208 (Figure S2), the reduction of the Fe species was delayed for W_aFeO_x in comparison with Fe₂O₃,
209 suggestive of interactions between W and Fe [36]. On the other hand, NH₃-TPD spectra show a
210 greater amount of ammonia desorption in the range 100-500°C (NH₃ adsorption on WO₃ is
211 negligible) (Figure 3a), indicating numbers of acid sites in W_aFeO_x. By using the integrated NH₃-
212 TPD peak areas, the relative amounts of adsorbed NH₃ show a clear correlation with the reaction
213 rates of W_aFeO_x (Figure 2), suggesting that the enhanced activity is primarily related to the
214 enhanced acidity derived from the strong interactions in the W-O-Fe structure.

215 To study the nature of species adsorbed on sites within the short-range ordered W-O-Fe
216 structure during NH₃ exposure, *in situ* FTIR spectra were collected (Figure 3b and c). Fe₂O₃ does
217 not show evidence for Lewis acidity although Brønsted acid sites are detected (~1437 cm⁻¹,
218 Figure 3b). The coordinated NH₃ (~1202 and 1600 cm⁻¹) suggests the presence of Lewis acidity
219 on W_{0.13}FeO_x (Figure 3c) [12]. As for Brønsted acidity, a greater intensity peak ~1440 cm⁻¹ was
220 observed for W_{0.13}FeO_x than Fe₂O₃. The increase in amounts of both the Lewis and Brønsted
221 acidity promotes catalytic activity [37-42]. With increasing temperature, both the peak intensities
222 due to adsorption at Lewis and Brønsted acid sites decreased, with the later exhibiting lower
223 thermal stability compared with ammonia on Lewis acid sites. The band at ~1417 cm⁻¹ nearly

224 disappeared at 350°C, whereas the band at 1238 cm⁻¹ is still clearly observed. An additional
 225 band at ~1361 cm⁻¹ was observed which could be ascribed to an oxidised product of adsorbed
 226 ammonia [38, 43, 44]. These results provide persuasive evidence that the atomic-scale
 227 interaction in the short-range ordered W-O-Fe structure enhances both Lewis and Brønsted
 228 acidity of the catalysts and these are favorable for catalytic activity.

229



230

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Figure 4. XRD patterns of Fe₂O₃-800, Fe₂WO₆, and W_aFeO_x-800 catalysts.

232

233

Table 1. Textural properties, XRD and ICP data of Fe₂O₃-800 and W_aFeO_x-800 catalysts.

Sample	Surface area (m ² /g)	Pore volume (cm ³ /g)	Pore size (nm)	Fe ₂ WO ₆ concentration from XRD (wt.%)	W mass concentration from ICP[26] (wt.%)	W contents in Fe ₂ WO ₆ phase (wt.%)	Non-crystallized W contents (wt.%)
W _{0.09} FeO _x -800	23.7	0.0843	16.4	4.42	16.4	2.1	14.3
W _{0.13} FeO _x -800	20.0	0.0573	14.1	12.82	23.2	6.0	17.2

W _{0.17} FeO _x -800	18.3	0.0657	14.4	33.91	27.4	15.9	11.5
Fe ₂ O ₃ -800	2.5	0.0078	67.3	--	--	--	--

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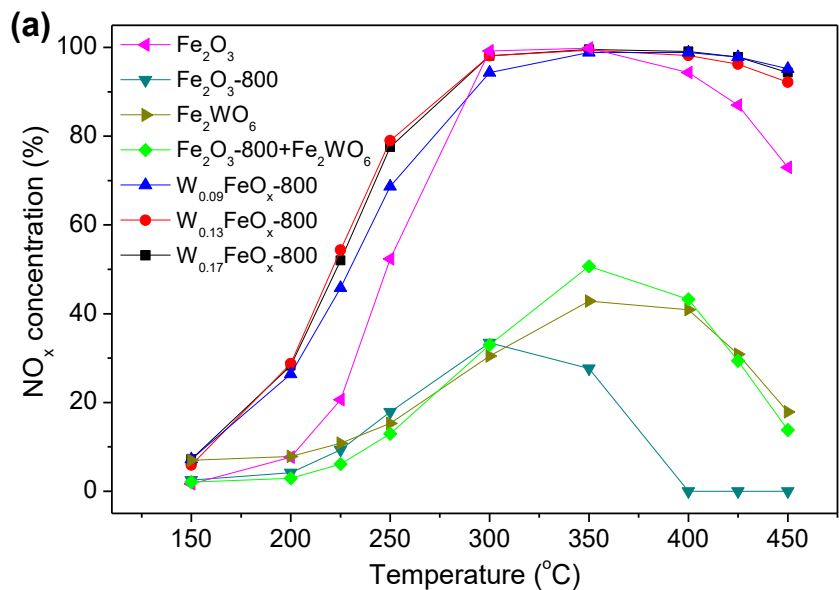
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236 To determine the stability of the short-range ordered W-O-Fe structure at higher temperature,
 237 the W_aFeO_x samples were calcined at high temperature (800°C, 5 h) (denoted as W_aFeO_x-800).
 238 An increase in calcination temperature (Figure 4), results in the emergence of a new phase,
 239 Fe₂WO₆ (JCPDS 70-0495) in addition to Fe₂O₃, indicating a transformation from amorphous to
 240 crystalline. This confirmed the XAFS results that W in W_aFeO_x exists in the O_h coordination
 241 environment as in Fe₂WO₆. From quantitative analysis of W concentrations (wt.%) in Fe₂WO₆
 242 phase over different samples on the basis of XRD data, it is interesting to note that the
 243 concentrations are lower than those obtained by ICP, suggesting that only a part of the
 244 amorphous W-containing species in W_aFeO_x are transformed into Fe₂WO₆ crystallites, while the
 245 other remains in an amorphous state (Table 1). As shown in Table 1, W_{0.13}FeO_x-800 possesses
 246 the highest non-crystallized W content. As expected, the BET surface area was significantly
 247 decreased on increasing the calcination temperature.

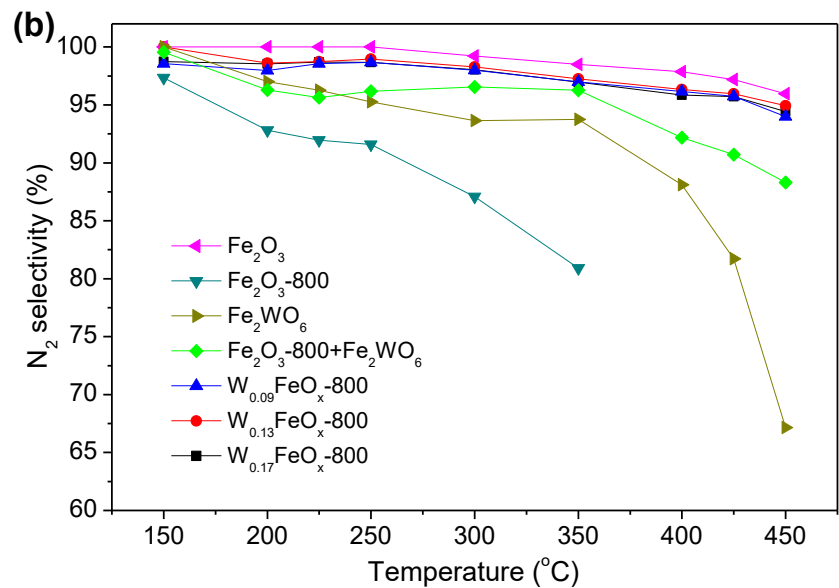
248 SCR performances of W_aFeO_x-800 catalysts show that the increasing calcination temperature
 249 resulted only in the decrease of low-temperature activity due to the decreased BET surface area,
 250 but had no clear influence on the high-temperature activity (Figure 5). Furthermore, NO_x
 251 conversion for W_{0.13}FeO_x-800, as an example, was stable over a 12 h test period (Figure S3). The
 252 high activity at 300-450°C compared with the low activity of Fe₂O₃-800 might be ascribed to
 253 Fe₂WO₆ microcrystals or the synergistic effect of Fe₂O₃ and Fe₂WO₆ microcrystals. However,
 254 this proposal is rejected based on the poor SCR activity of pure Fe₂WO₆ and Fe₂O₃-800+Fe₂WO₆
 255 samples (Figure 5). The latter is thought to simulate the ideal W_{0.13}FeO_x catalyst with complete

256 crystallization. It remains unanswered as to whether the retained activity is related with the
257 residual amorphous phase and where these are located.

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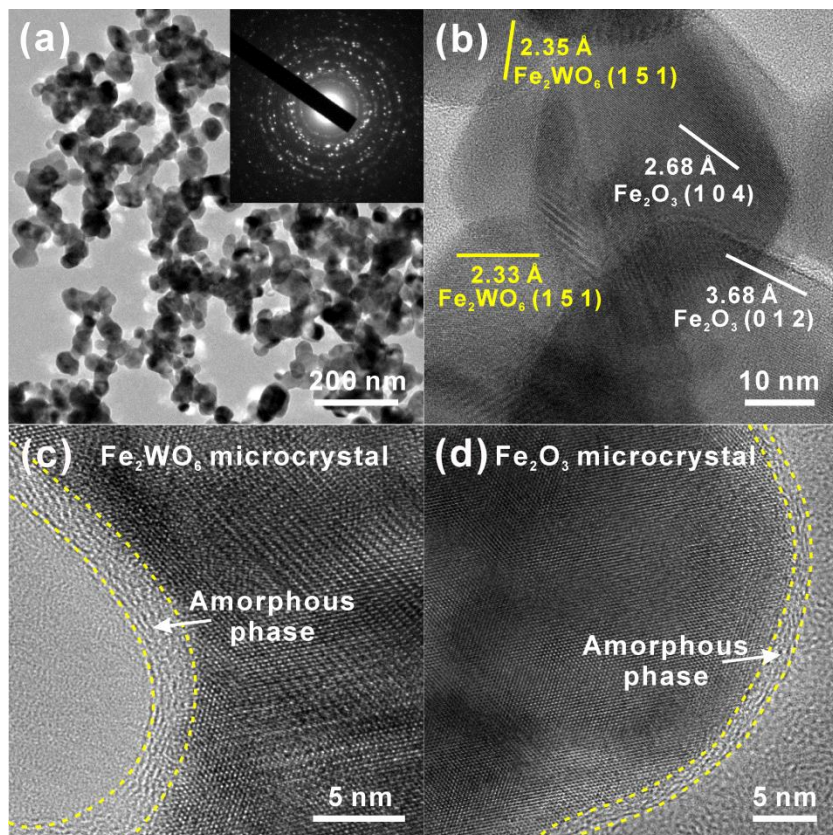
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261 **Figure 5.** (a) NO_x conversion and (b) N₂ selectivity of W_aFeO_x-800 catalysts and reference
262 samples.

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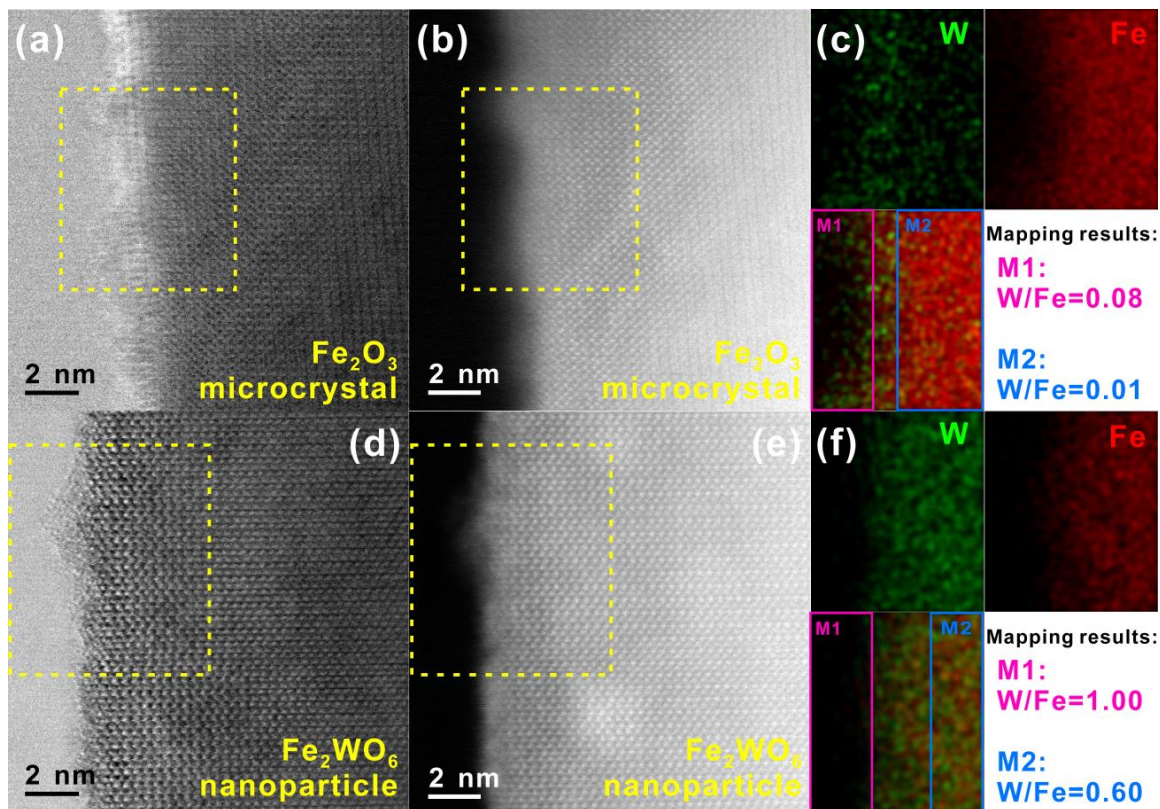
264 Figure 6 shows TEM images for $W_{0.13}FeO_x-800$. The well-crystallized Fe_2O_3 and Fe_2WO_6
265 microcrystals are randomly aggregated for $W_{0.13}FeO_x-800$ (Figure 6a). Based on the extensive
266 characterization, the Fe_2WO_6 phase consists of long-range ordered W-O-Fe structures, which are
267 derived from the sintering of the coordinated W, O, and Fe atoms in amorphous phase (Figure
268 S4). HRTEM was used to provide directly interpretable images of W_aFeO_x-800 to search for the
269 remaining amorphous phases (Figure 6b-d). Surprisingly, an amorphous phase layer of ~ 2 nm
270 thickness was detected on the surfaces of Fe_2WO_6 and Fe_2O_3 microcrystals for $W_{0.13}FeO_x-800$.
271 According to the semi-quantitative analysis of surface atomic concentrations (% as molar ratio)
272 over $W_{0.13}FeO_x-800$ from XPS data, the surface W/Fe atomic ratio was 0.48, which is much
273 higher than the surface and bulk ratios for $W_{0.13}FeO_x$ (XPS and ICP data [26], respectively, Table
274 S2), suggesting an enrichment of amorphous W-containing species on the surface.

275



276

277 **Figure 6.** (a) TEM images with SAED patterns (insets), (b-d) HRTEM images for $W_{0.13}FeO_x$ -
 278 800.
 279



280
 281 **Figure 7.** HRTEM images and EDX analysis of Fe_2O_3 and Fe_2WO_6 nanoparticles in $W_{0.13}FeO_x$ -
 282 800 catalyst: (a) HRTEM bright-field image, (b) HAADF image, and (c) EDX mapping results
 283 of the region in the yellow dashed box for a Fe_2O_3 nanoparticle; (d) HRTEM bright-field image
 284 (e) HAADF image, and (f) EDX mapping results of the region in the yellow dashed box for a
 285 Fe_2WO_6 nanoparticle.

286
 287 The chemical composition of the amorphous overlayer was determined by HAADF-STEM
 288 in conjunction with the corresponding EDX mappings (Figure 7). The latter was acquired from
 289 both the overlayer and the inside of Fe_2O_3 and Fe_2WO_6 nanoparticles. HAADF-STEM clearly

290 shows that the Fe atoms are homogeneously distributed over the Fe₂O₃ nanoparticle, while the W
291 atoms are detected primarily on the surface of the amorphous overlayers of the Fe₂O₃
292 nanoparticles (Figure 7a-c). EDX gives a W/Fe molar ratio of about 0.08 for the amorphous
293 overlayer on the Fe₂O₃ nanoparticle, which is much higher than that in the Fe₂O₃ nanoparticle
294 (0.01), suggesting that W atoms are primarily doped in the amorphous Fe-O overlayer of the
295 Fe₂O₃ nanoparticle (Figure 7a-c), with similar short-range ordered W-O-Fe structure as in
296 W_aFeO_x. Comparatively, HAADF-STEM images of the Fe₂WO₆ nanoparticle show Fe and W
297 atoms throughout the whole section (Figure 7d-f). EDX indicates that the W/Fe molar ratio of the
298 overlayer on the Fe₂WO₆ nanoparticle is 1.00, consistent with that of the short-range ordered W-
299 O-Fe structure. On extending to the inside of the Fe₂WO₆ nanoparticle, the W/Fe molar ratio
300 decreases to 0.60, which is very close to that of the bulk Fe₂WO₆. The above analysis confirms
301 that the non-crystallized W species as derived from XRD are mainly located in the amorphous
302 overlayers of the Fe₂O₃ and Fe₂WO₆ nanoparticles, which agrees well with the XPS.
303 Consequently, the retained high-temperature activity of W_aFeO_x-800 is a consequence of the
304 amorphous phase on the surface of microcrystals.

305 Following the same strategy as applied to W_aFeO_x, the reaction rates (r_h) of W_aFeO_x-800 were
306 also measured (Figure 2). Apparently, the variation of r_h correlates well with the amount of
307 amorphous W-containing species (Figure 2 and Table 1), providing proof that the intrinsic
308 activity was derived from the W-O-Fe structure on the surface amorphous overlayer. In other
309 words, the short-range ordered W-O-Fe active sites in W_aFeO_x were retained in the W_aFeO_x-800
310 in the form of the surface amorphous overlayer, which ensures retained the high-temperature
311 activity at 300-450°C after aging at 800°C for 5 h.

312

313 **4. Conclusions**

314 Poorly-crystalline W-Fe composite oxides (W_aFeO_x), consisting of short-range ordered W-
315 O-Fe structures were prepared. A direct correlation between the level of disorder and the
316 intrinsic activity indicated that the short-range ordered W-O-Fe structure hosts the active
317 catalytic sites. Strong atomic-level interactions between Fe and W atoms within the disordered
318 W-O-Fe structure was shown and this enhanced the amounts of Lewis and Brønsted acidity,
319 leading to improved deNO_x activity. Of significance, the short-range ordered W-O-Fe
320 structure was retained as amorphous overlayers over the surface of crystalline particles after
321 aging at 800°C for 5 h, leading to the retention of activity. This finding may open up new
322 pathways in the fabrication of the active deNO_x catalysts with high thermal stability by
323 rationally enhancing atomic-scale interactions between heteroatoms in composite oxides.

324

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