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PIM-1/graphene pervaporation membranes for bioalcohol recovery

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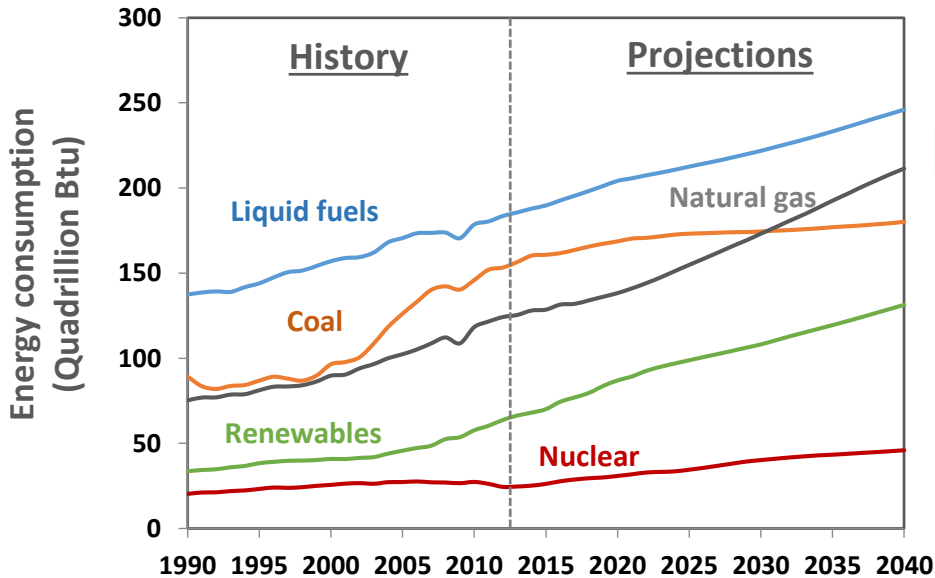
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PIM-1/graphene pervaporation membranes for bioalcohol recovery

Monica Alberto, Jose Miguel Luque-Alled, Lei Gao, Maria Iliut, Aravind Vijayaraghavan,
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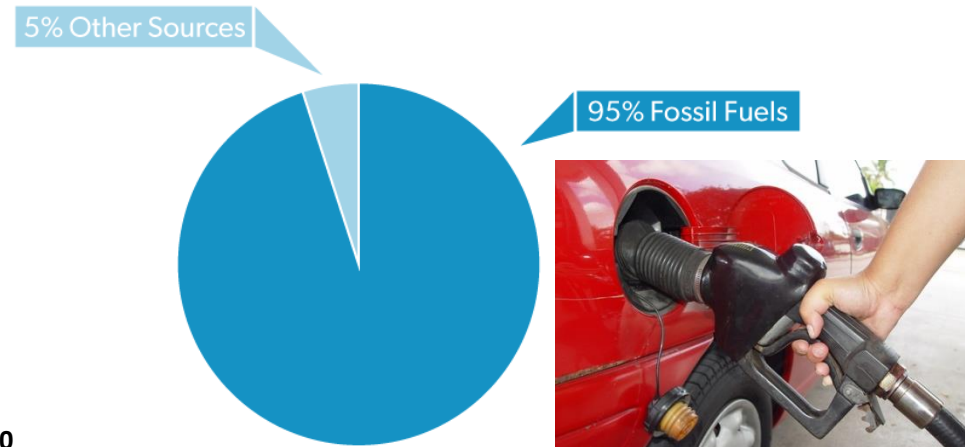
School of Chemical Engineering and Analytical Science
National Graphene Institute
The University of Manchester



Source: EIA, International Energy Outlook, May 2016

Fossil Fuels

Percent of U.S. Transportation Sector Consumption



Source: EIA, MER, March 2016

IER INSTITUTE FOR ENERGY RESEARCH

- The demand for energy requirement is increasingly growing.
- It is difficult to reach the world energy demand only by using fossil fuel



Alternative: BIOFUELS

A [biofuel](#) is any fuel source that is made from biological materials. The two most common kinds of biofuels are both gasoline alternatives: ethanol and biodiesel.



A Volkswagen Golf model that uses E10 blended bioethanol



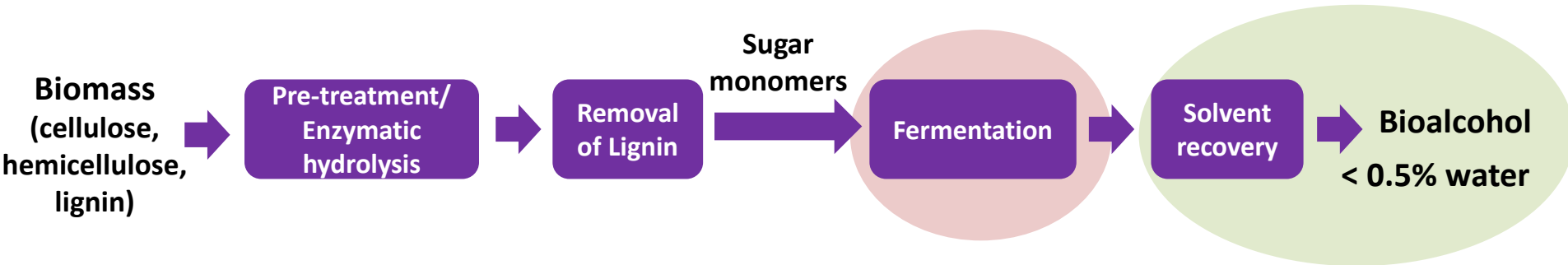
The Ferrari F430 Spider Bio Fuel Concept car runs on E85 biofuel



The Saab BioPower runs on E85 which has higher octane rating than petrol

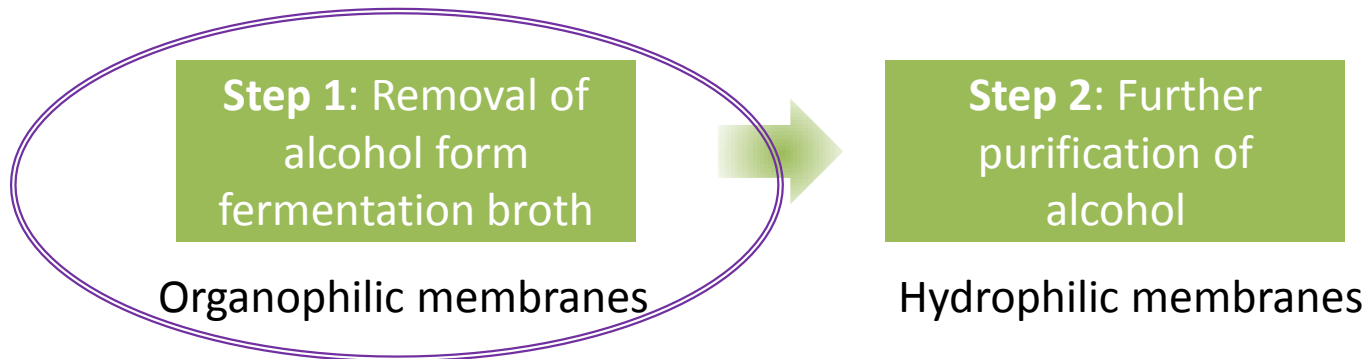
- ✓ Reduces greenhouse gas emissions as the release of CO₂ from burning the biofuels is matched by the CO₂ absorbed by the plants growing the biomass used to produce it
- ✓ Using so-called second-generation technologies to convert material such as crop residues into bioenergy can avoid competition for land

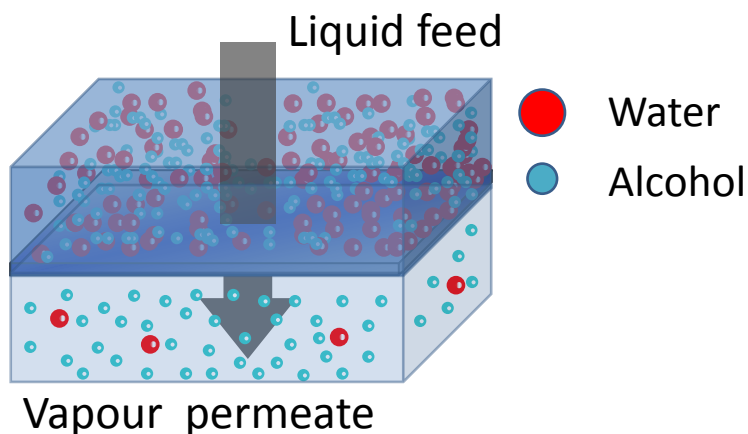
Bioethanol and biobutanol are produced via fermentation of biomass.



End-product inhibition is caused by the toxicity of the alcohol produced on the bacteria. A concentration of less than 2% of bioalcohol (ABE fermentation process for biobutanol production) is typically achieved.

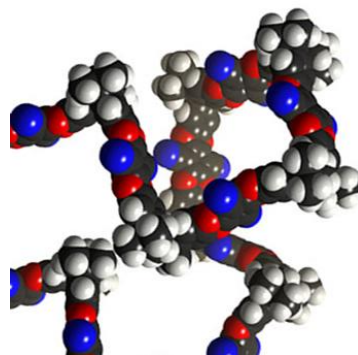
The bioalcohol needs to be purified from the fermentation broth (contains mainly water) by a series of distillation columns → 60-80% of the total production costs.





- **Inorganic membranes**, zeolites: silicalite-1, ZSM-5
- **Polymeric membranes**, polydimethylsiloxane (PDMS), poly[1-(trimethylsilyl)-1-propyne] (PTMSP), PEBA, PTFE
- **Hybrid membranes**, polymer matrices containing selective fillers e.g. silicalite-silicon rubber

Polymers of intrinsic microporosity (PIMs)

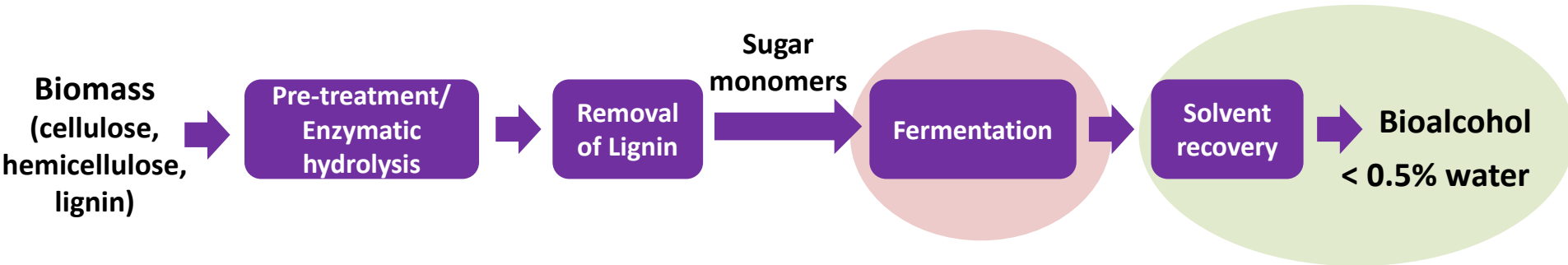


A continuous network of interconnected intermolecular voids, which forms as a direct consequence of the shape and rigidity of the component macromolecules.

N.B. McKeown & P.M. Budd,
Macromolecules, 2010, **43**, 5163.

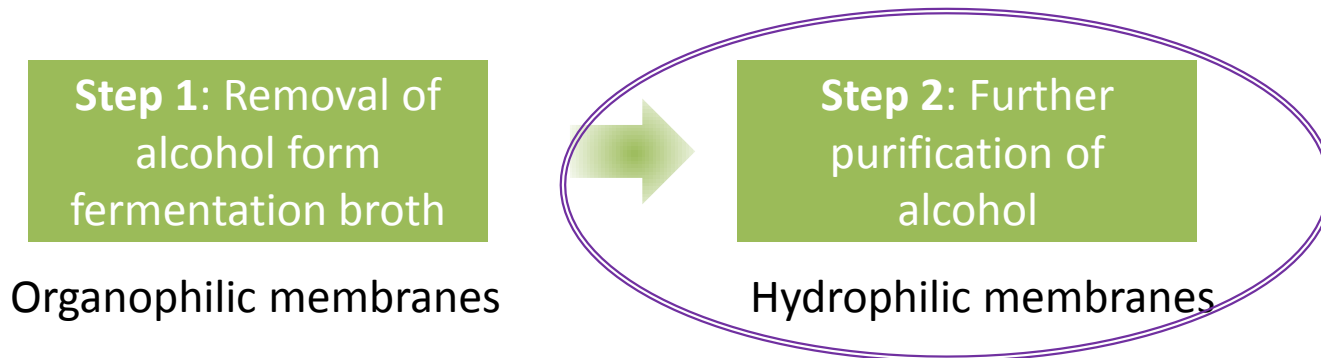
- ❑ Swelling in the presence of organic solvents → Reduction of the selectivity
- ❑ Ages over time → Increase in selectivity and reduction of flux

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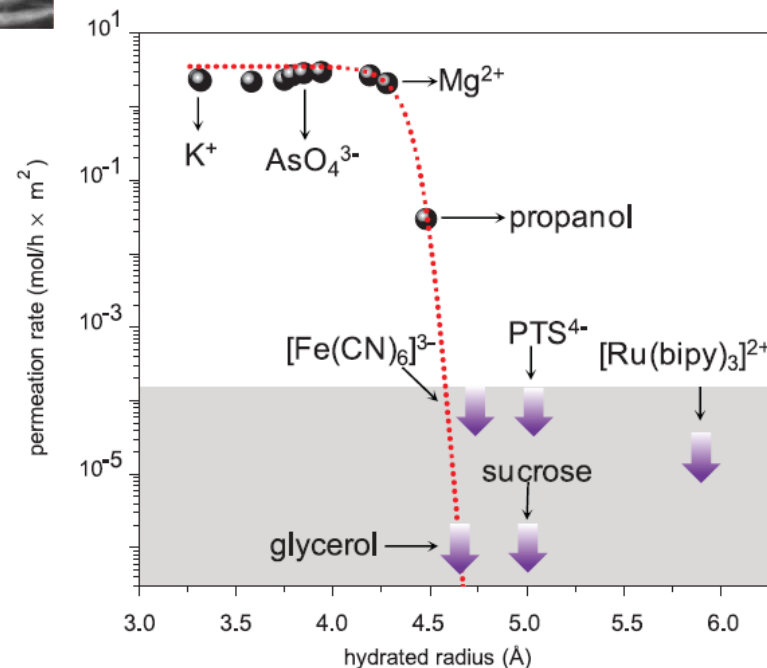
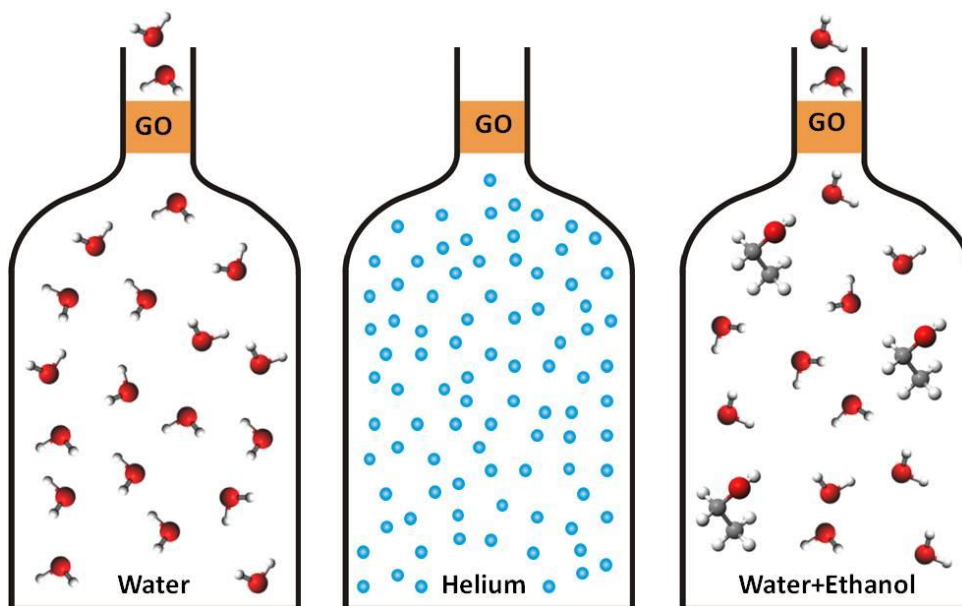
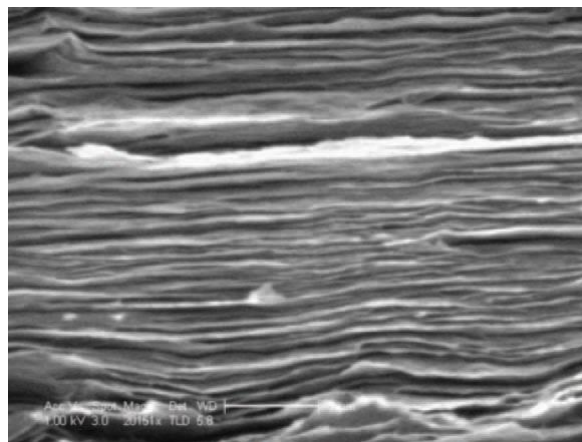
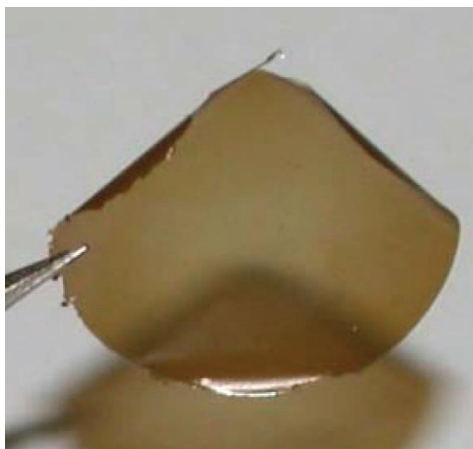


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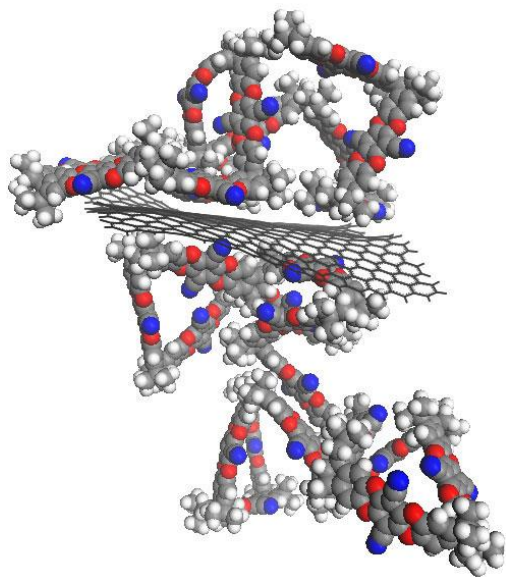
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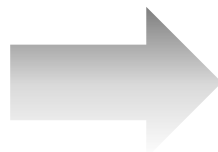
Hydrophilic graphene oxide (GO) membranes



Simulations



A. Gonciaruk et al., *Micropor. Mesopor. Mater.*, 209 (2015) 126-134



Experimental work

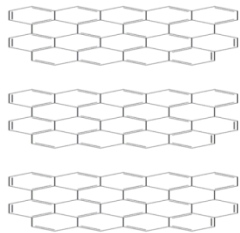


- PIM-1 is soluble just in few organic solvents, (CHCl_3 , THF, DMAc)
- Direct mechanical exfoliation of graphite in these solvents is not good
- GO and rGO flakes prepared via oxidation of graphite cannot be dispersed



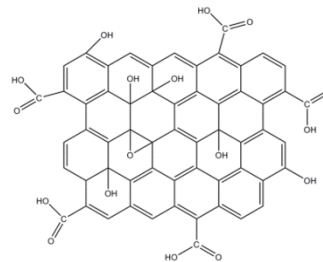
Functionalization of GO with alkylamines can lead to monolayer and few-layered graphene flakes that are easily dispersed in CHCl_3

Preparation of graphene-like flakes



Graphite

Oxidation
→
Hummers
modified
method



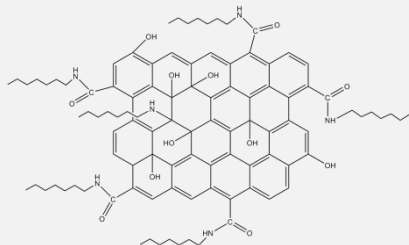
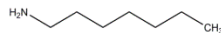
Graphene Oxide (GO)



GO

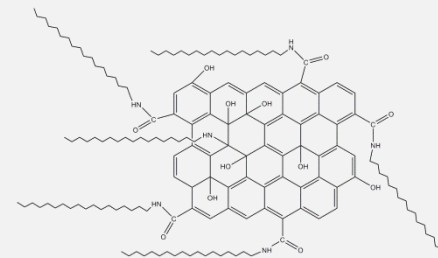
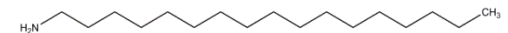
Functionalization

Octylamine (OA)



GO-OA

Octadecylamine (ODA)



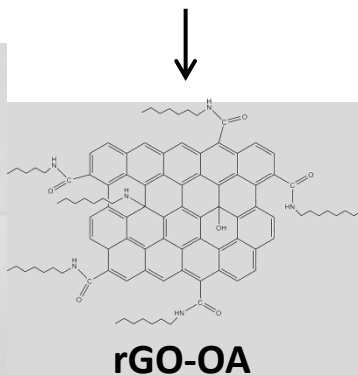
GO-ODA



GO-ODA

Chemical reduction
(hydrazine)

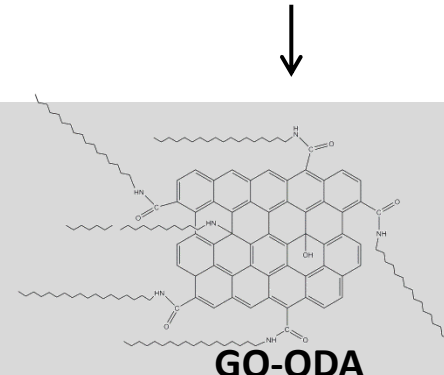
rGO-OA



rGO-OA

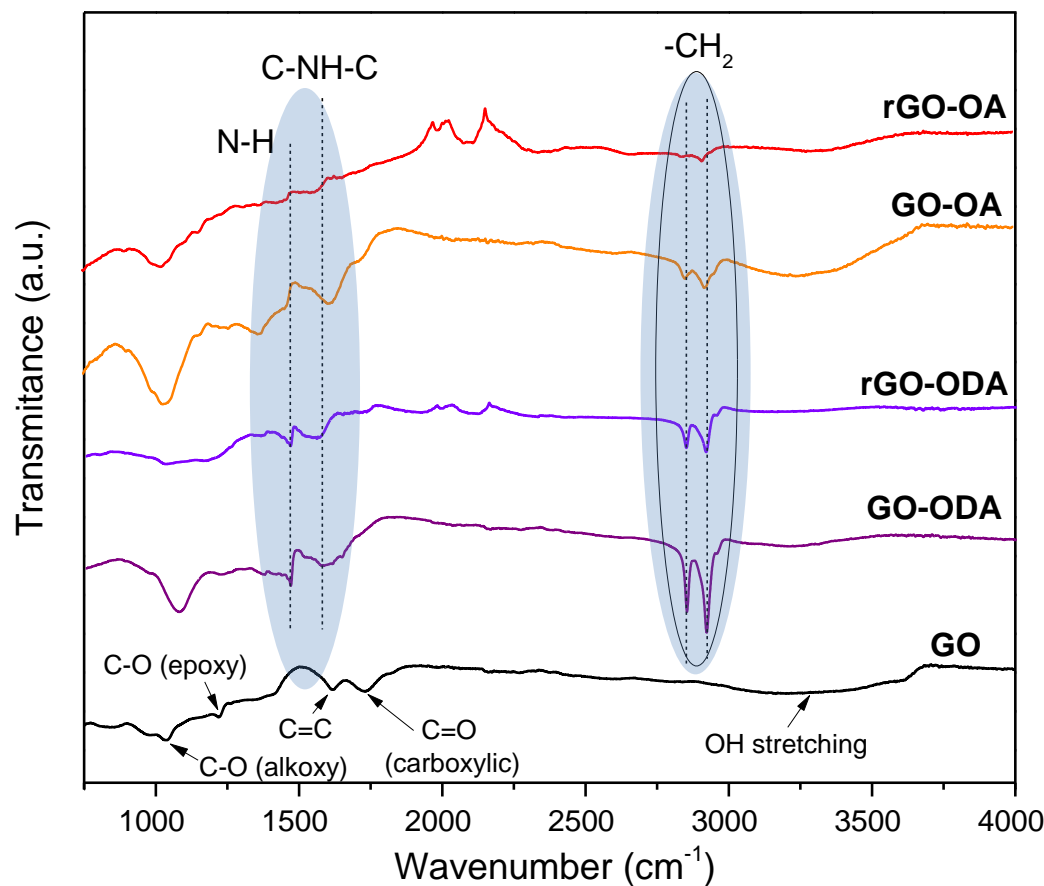
D. Li, et al., *Nature Nanotechnology*,
2008, 3(2), 101-105

GO-ODA



rGO-ODA

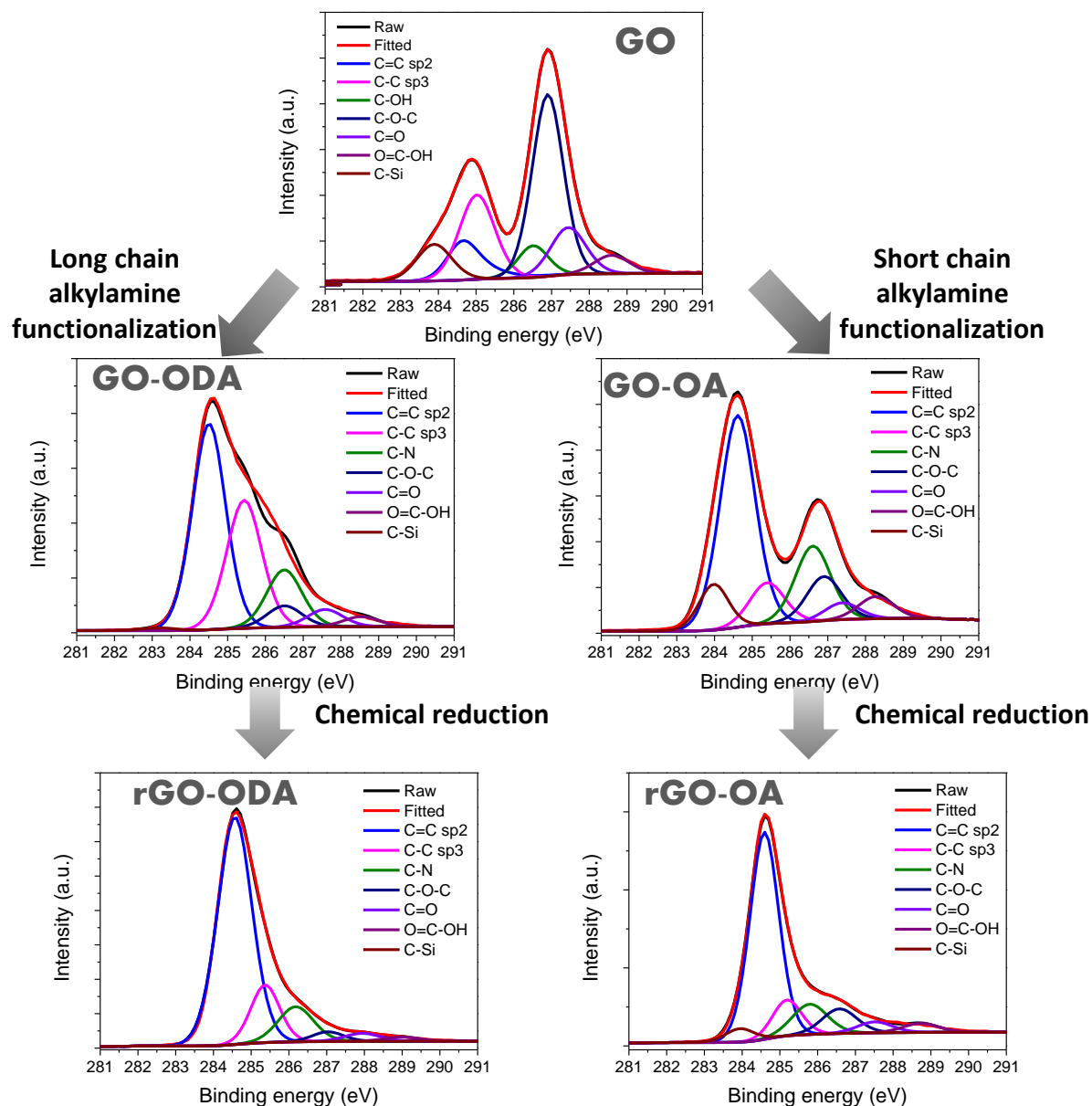




Peaks at $2850/2920\text{ cm}^{-1} \rightarrow -\text{CH}_2$
of alkylamines

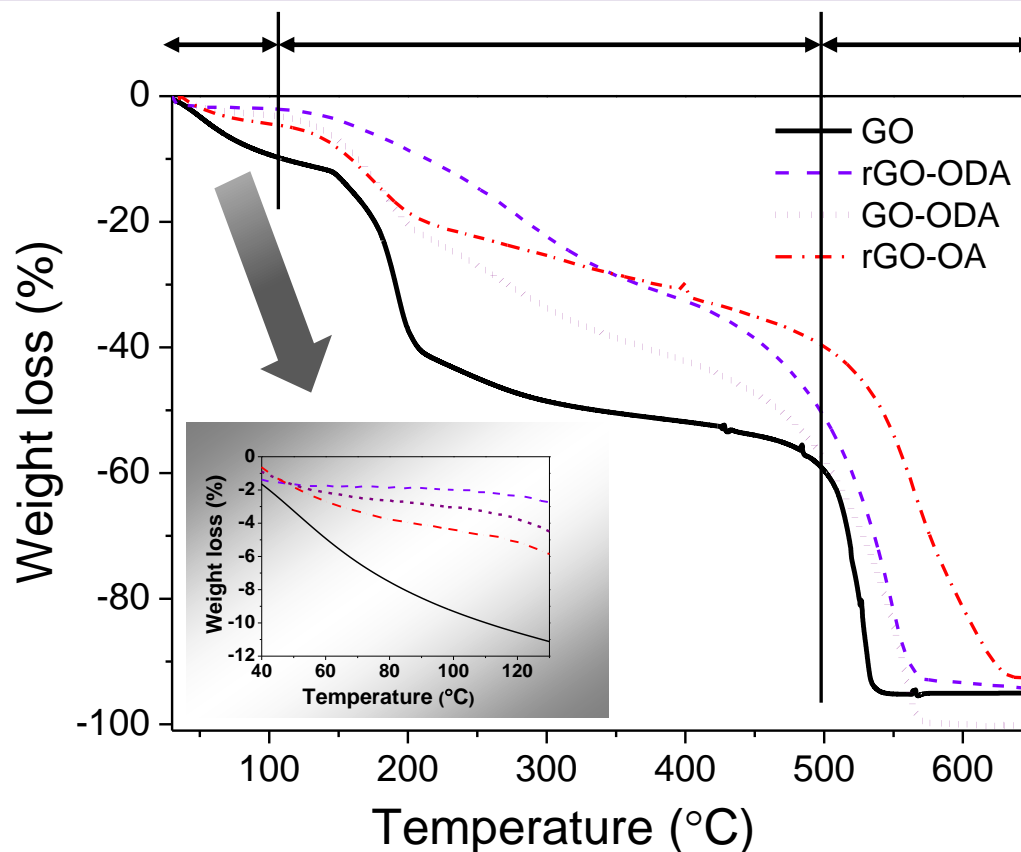
Decrease in intensity for reduced
samples \rightarrow loss of some alkylamine
upon treatment with hydrazine

Peaks at 1470 cm^{-1} and $1580\text{ cm}^{-1} \rightarrow$ covalent bonds (C-N-C)
between alkylamines and GO

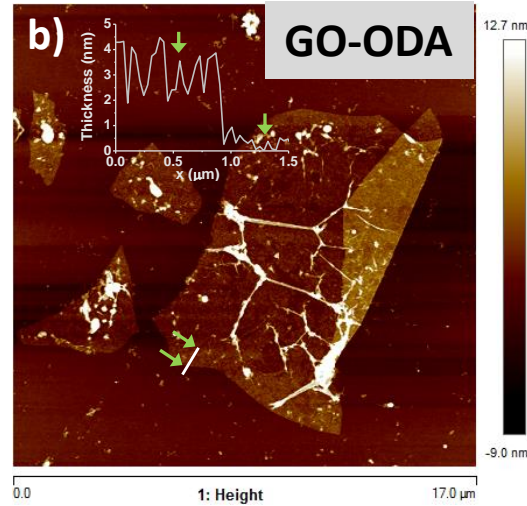
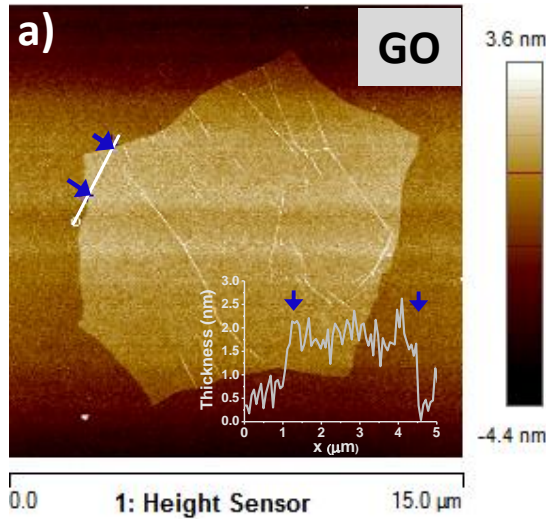


Filler	C:O ratio
GO	1.74
GO-ODA	13.8
rGO-ODA	12.9
GO-OA	4.80
rGO-OA	3.80

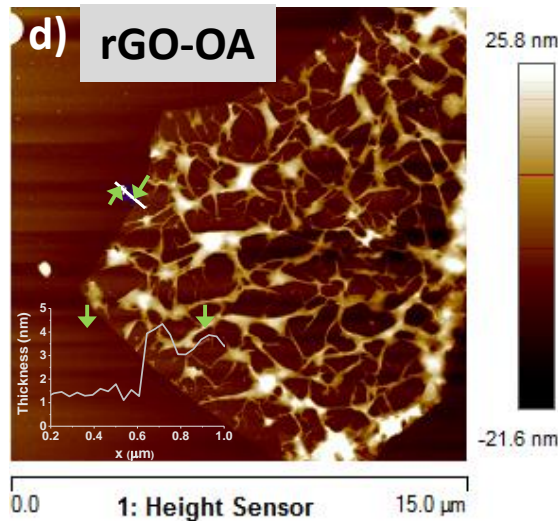
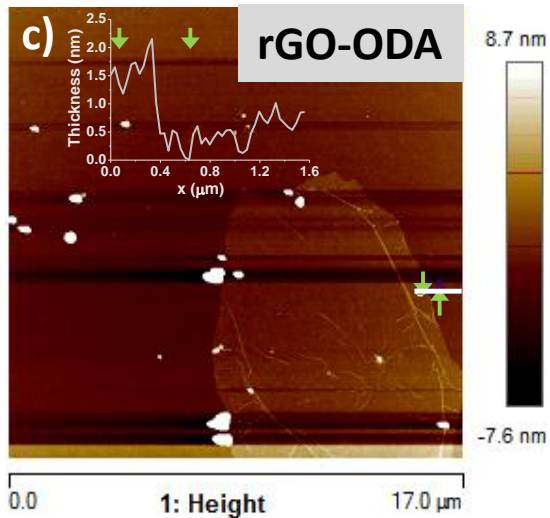
- ✓ The higher C:O ratio corresponds to the sample functionalised with the alkylamine that has the longer chain
- ✓ C:O ratio decreases upon chemical reduction as a result of a small portion of the grafted alkyl chains being removed.



- Enhancement in the hydrophobicity degree of starting material GO in this order: rGO-ODA > GO-ODA > rGO-OA
- Presence of both physically adsorbed and chemically bonded ODA to the GO flakes
- Weight loss for rGO-ODA > rGO-OA as ODA chains having larger mass



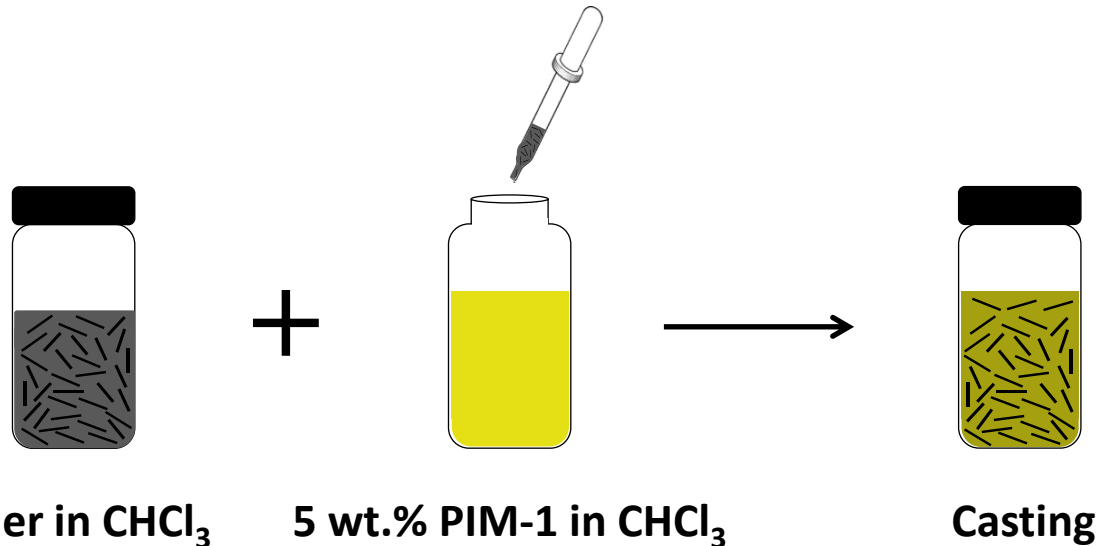
lateral dimensions of GO sheets are in the expected range with flakes of sizes ranging from few tens of nanometers to few micrometers



monolayer and few-layered structures are observed

1. Preparation of casting solutions

wt.%	Filler
0.01	rGO-ODA
0.05	GO-ODA
0.1	rGO-OA
1	

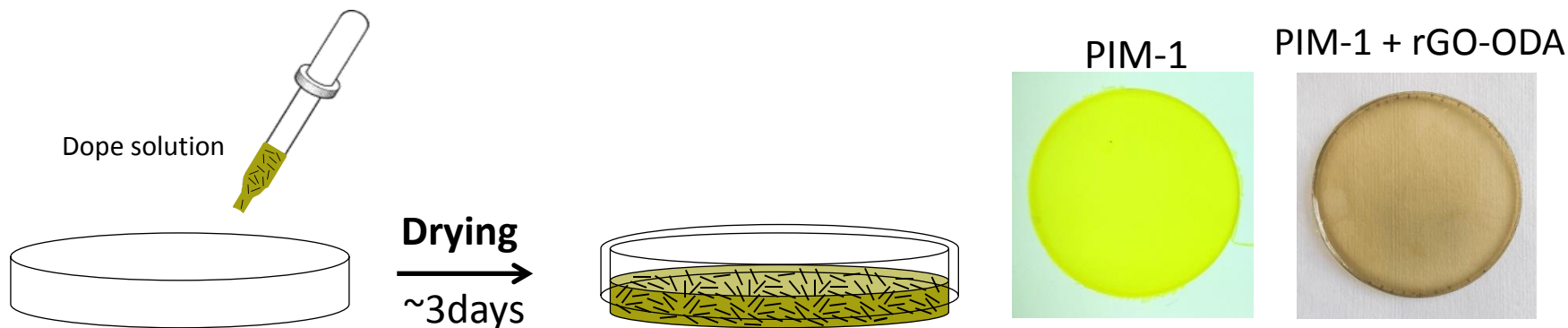


Filler in CHCl_3

5 wt.% PIM-1 in CHCl_3

Casting solution

2. Casting-evaporation on flat petri dishes



Dope solution

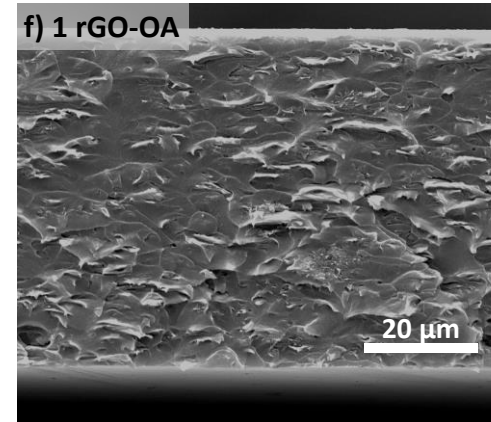
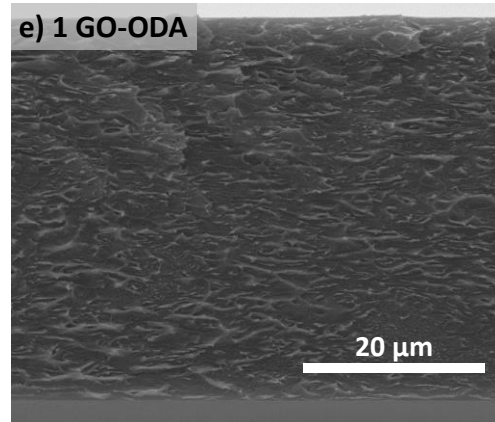
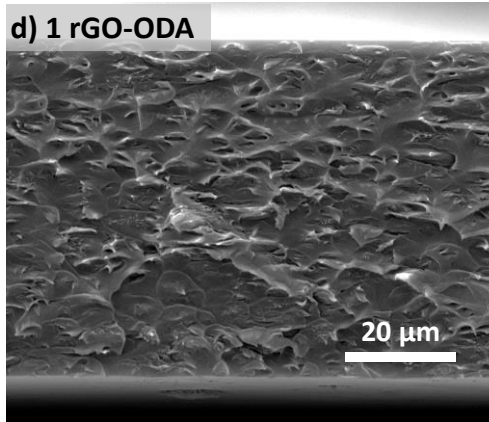
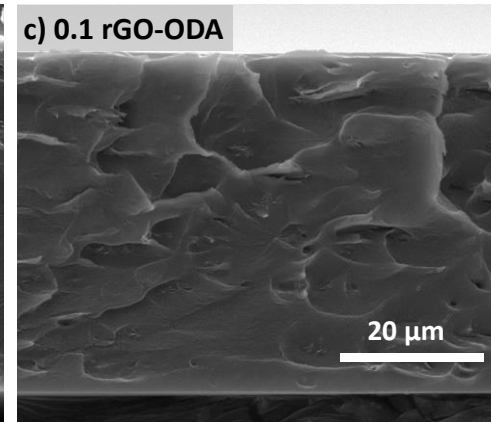
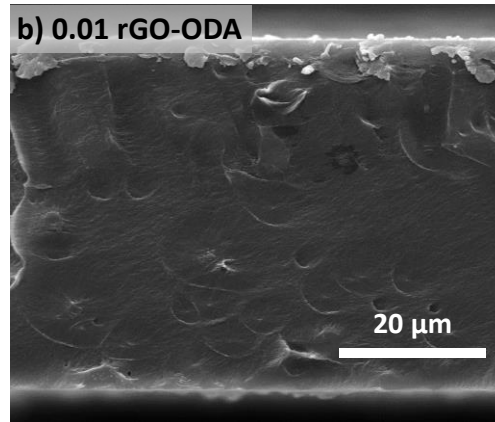
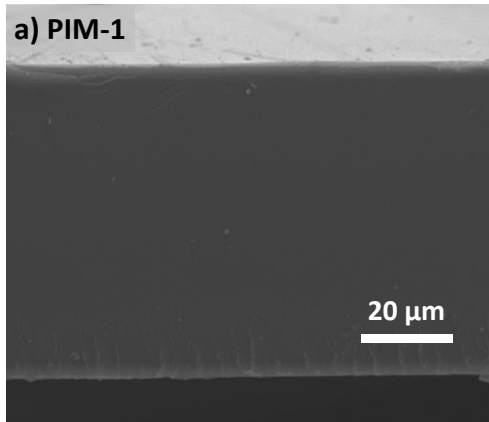
Drying
→
~3days

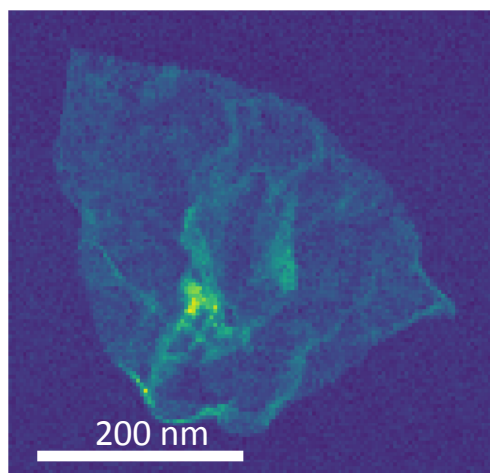
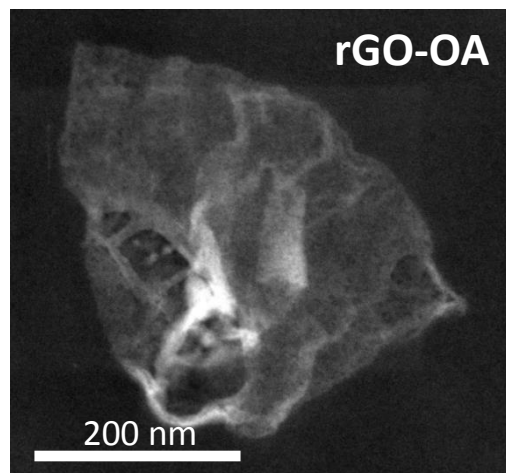
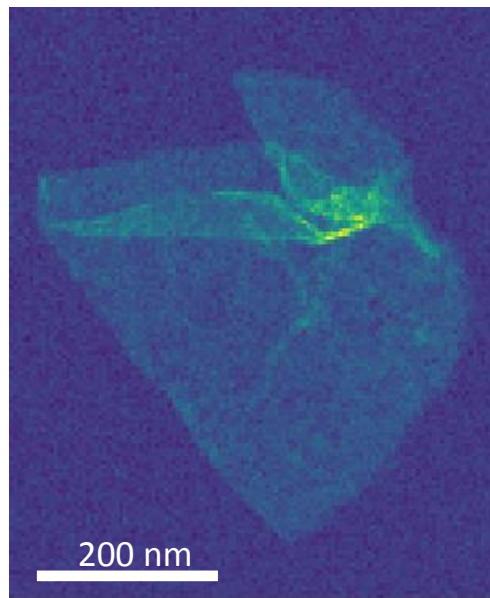
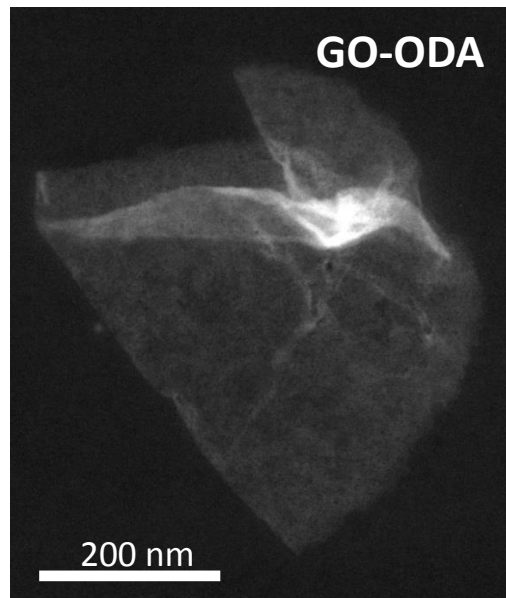
PIM-1

PIM-1 + rGO-ODA

Membrane code	Filler	wt% of filler Values from the preparation of casting solutions	wt% of filler Values from UV of re-dissolved membranes *	Membrane Thickness (μm)*
PIM-1	-	-	-	60 ± 9.1
0.01GO-ODA	GO-ODA	0.01	0.040 ± 0.008	54 ± 6.5
0.1GO-ODA		0.1	0.197 ± 0.024	65 ± 4.2
0.5GO-ODA		0.5	0.601 ± 0.045	57 ± 2.2
1GO-ODA		1	1.340 ± 0.316	51 ± 8.8
0.01rGO-ODA	rGO-ODA	0.01	0.018 ± 0.003	59 ± 6.2
0.1 rGO-ODA		0.1	0.065 ± 0.012	56 ± 2.4
0.5rGO-ODA		0.5	0.316 ± 0.078	68 ± 7.6
1rGO-ODA		1	0.704 ± 0.207	52 ± 6.9
0.01rGO-OA	rGO-OA	0.01	0.031 ± 0.006	48 ± 3.9
0.1rGO-OA		0.1	0.125 ± 0.094	51 ± 2.1
0.5rGO-OA		0.5	0.487 ± 0.085	54 ± 6.3
1rGO-OA		1	0.972 ± 0.097	59 ± 6.1

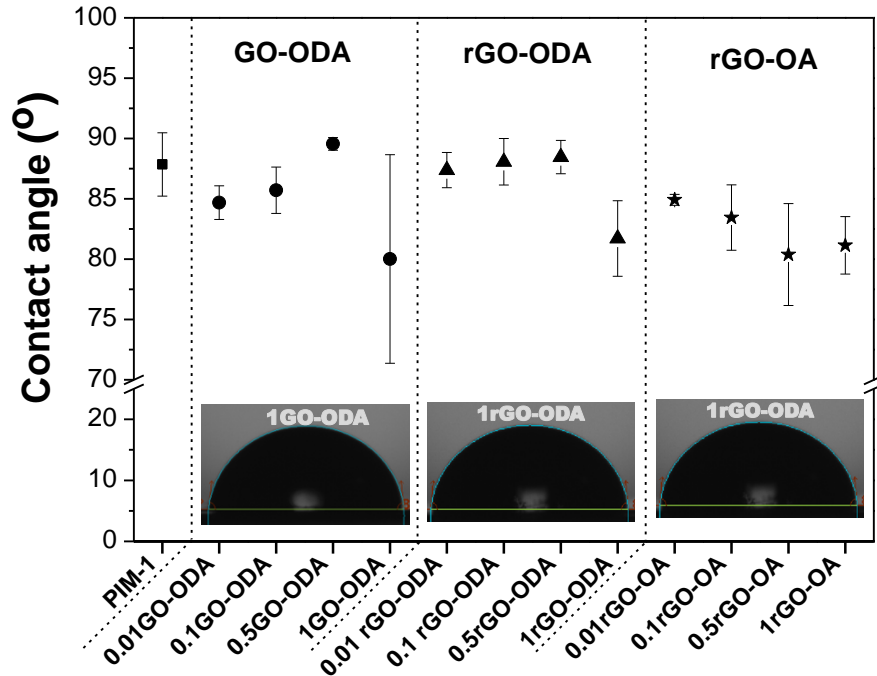
(*) Average of 10 measurements with a screw gauge in different areas of the membrane.





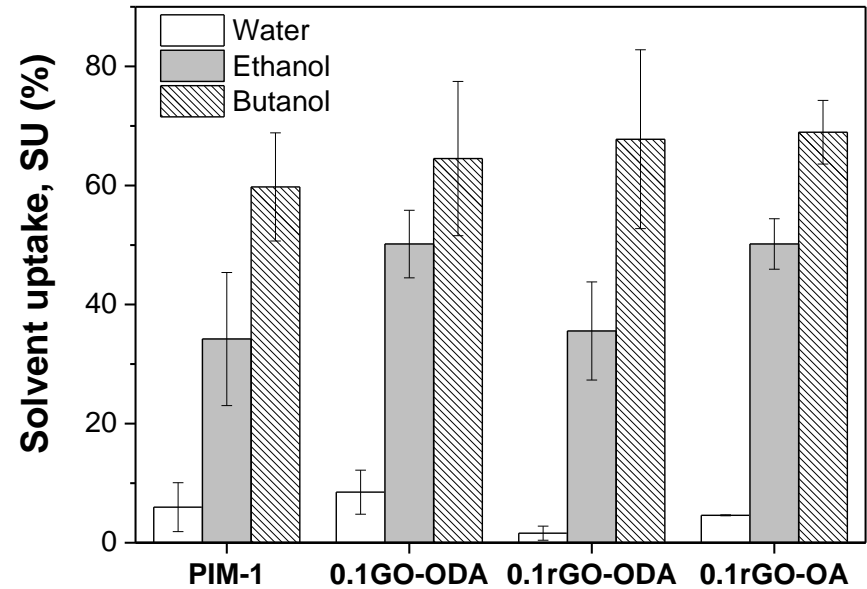
- Presence of single-layer flakes of GO-ODA and rGO-OA in the polymeric matrices
- O:C ratio mapping → features correspond to alkylamine - functionalized GO flakes

Contact angle



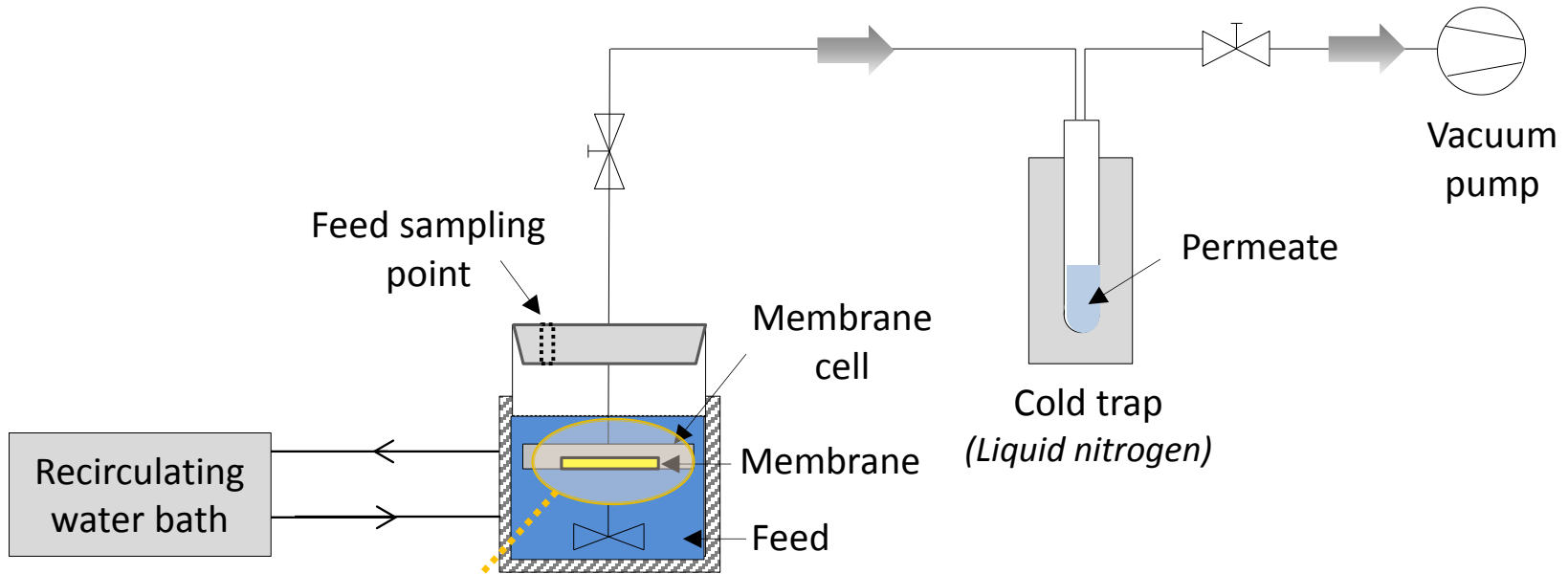
- All values for water ranged from 80 to 90° → addition of graphene-like fillers do not change significantly the surface properties
- ethanol contact angles 9.8° - 15.4° (13° for PIM-1)
- butanol contact angles 7.6° - 9.8° (9° for PIM-1)

Solvent uptake

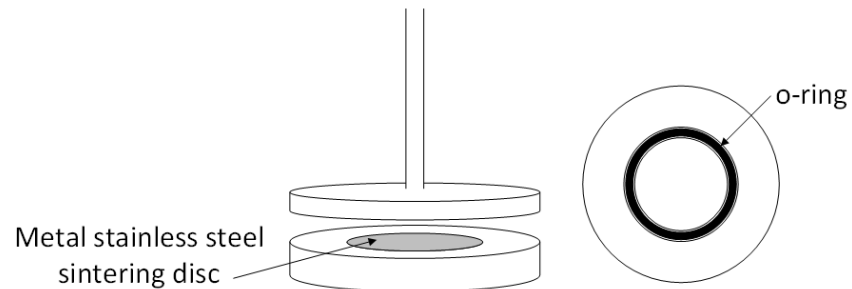
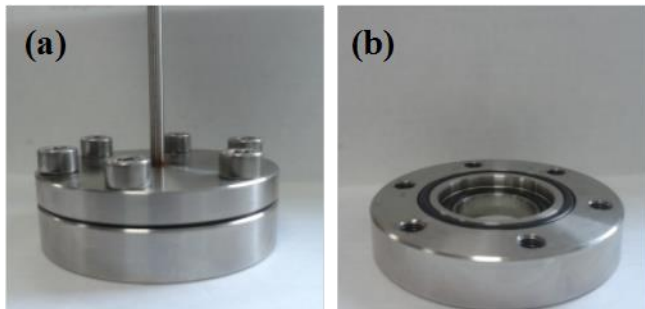


$$SU = \frac{m_f - m_i}{m_i} \times 100\% \quad \text{3 days}$$

- All the membranes show preferential sorption butanol > ethanol > water,
- Graphene-based fillers improve in all cases the sorption towards alcohols
- Chemically reduced samples hinder the sorption of water



Liquid samples are analysed with a GC equipped with FID



Experiment conditions

Feed composition: ~5wt% EtOH/BtOH in H₂O

Feed temperature: 65 °C

Downstream pressure: 10 mbar

Effective membrane area: 2.5 x 10⁻⁴ m²

Flux, J

$$J = \frac{m}{A t}$$

m : weight of the permeate (kg)

A : effective area of the membrane (m²)

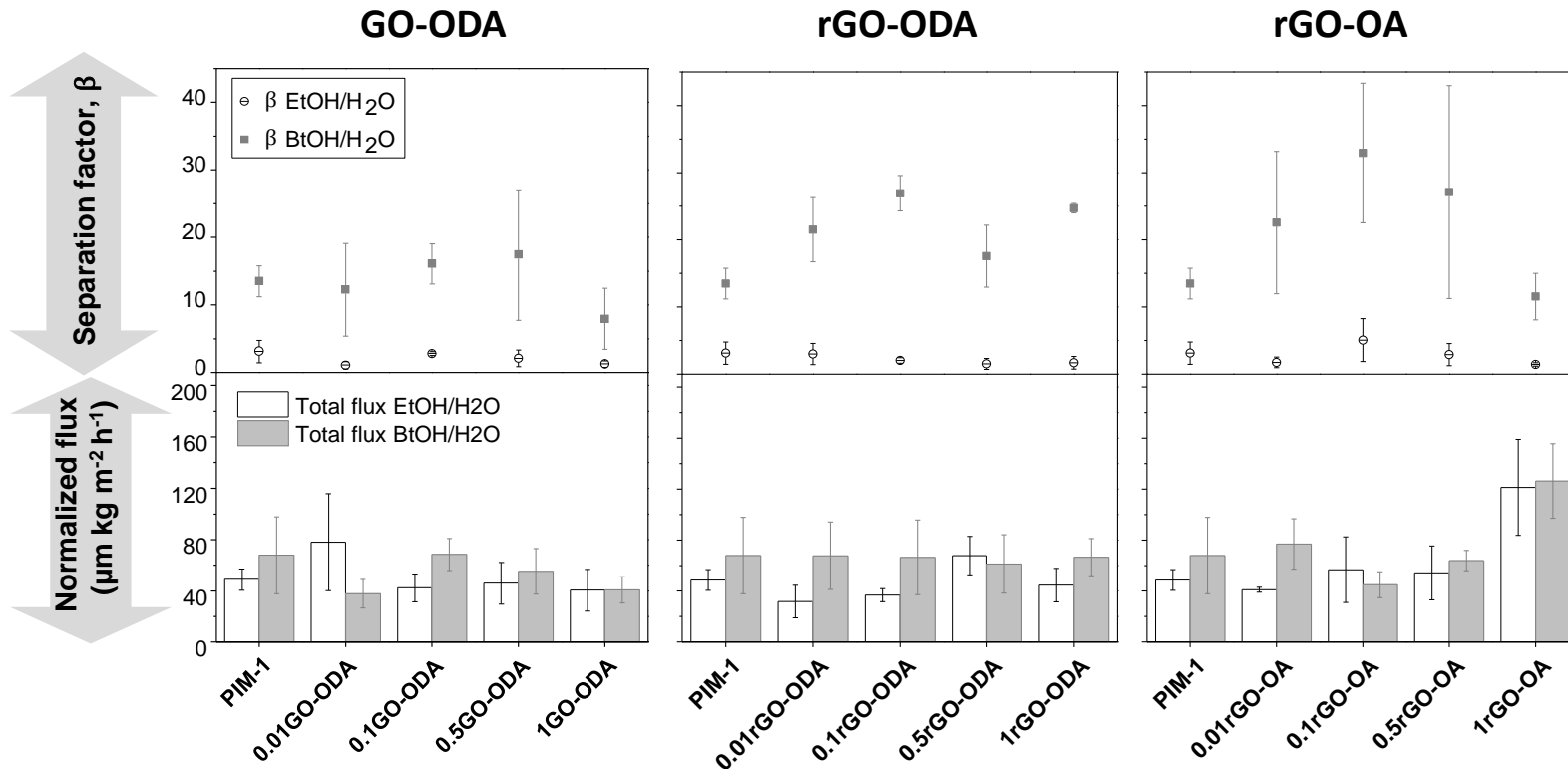
t : permeate collection time (h)

Separation factor, β

$$\beta = \frac{Y/(1 - Y)}{X/(1 - X)}$$

Y : mole fraction of the alcohol in the permeate

X : mole fraction of the alcohol in the feed side



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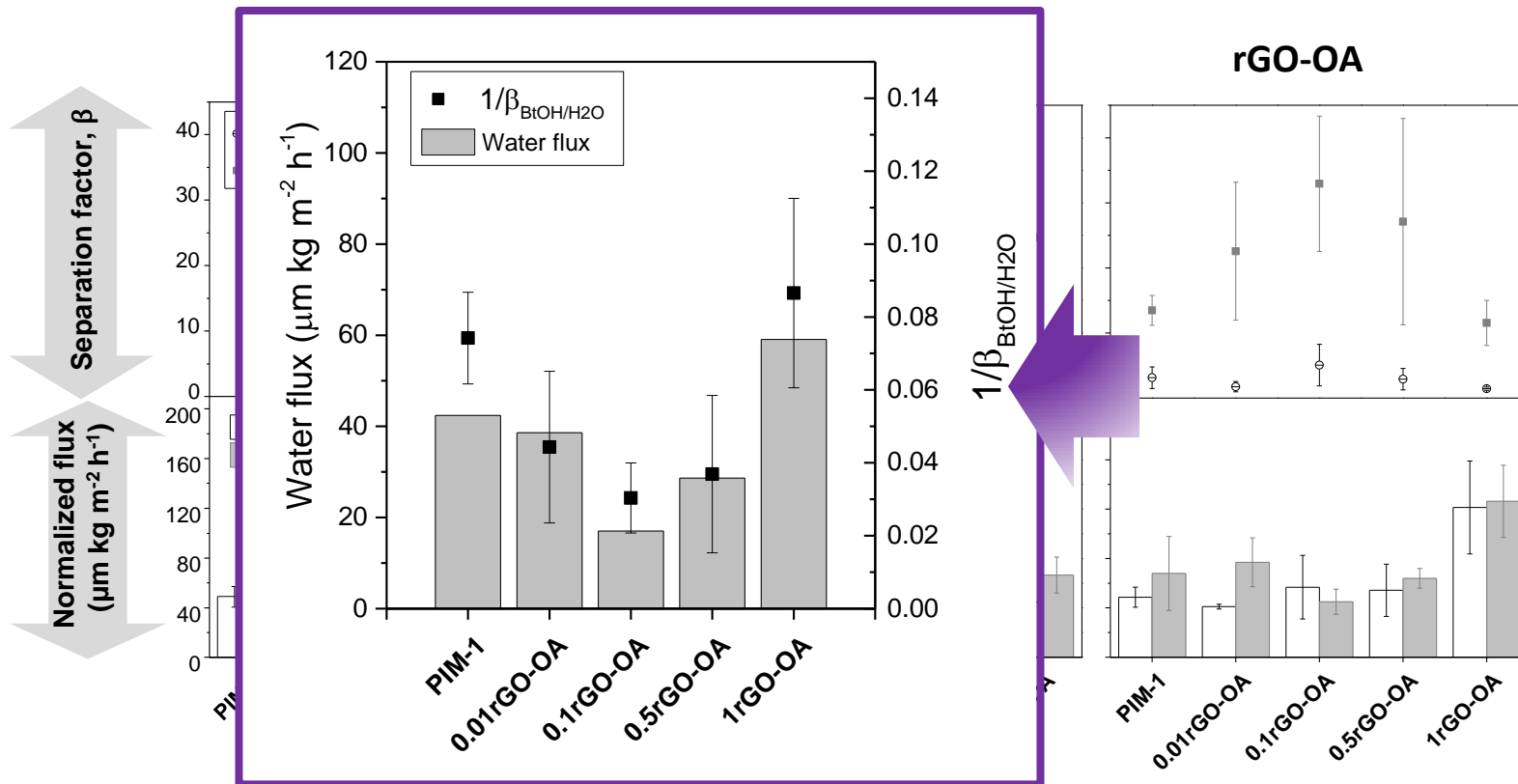
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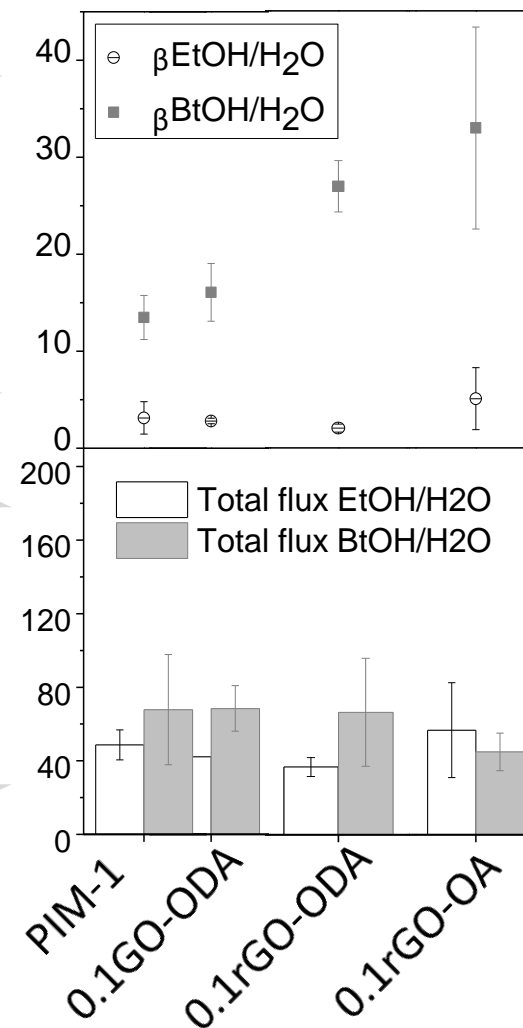
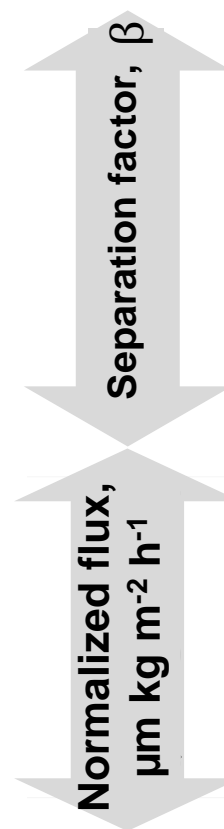
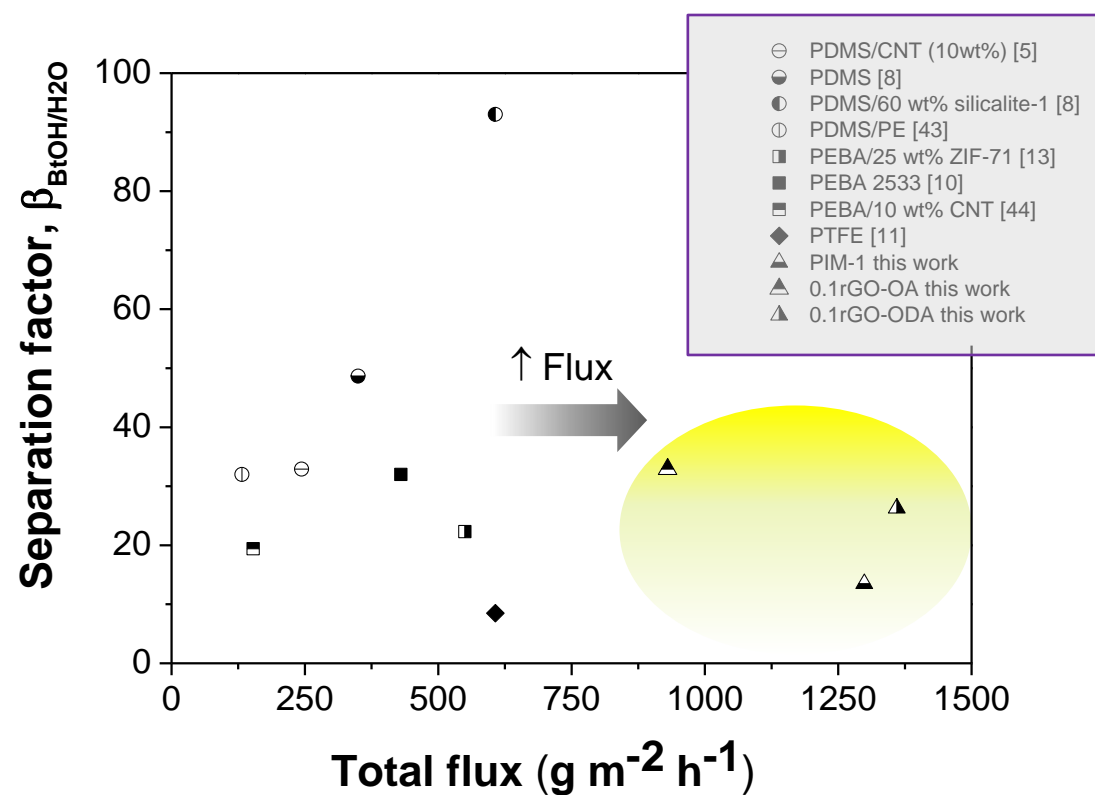
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Y : mole fraction of the alcohol in the permeate

X : mole fraction of the alcohol in the feed side



Comparison with reported values



- i. Alkylamine-functionalized GO and rGO (GO-ODA, rGO-ODA, rGO-OA that could be dispersed in chloroform was prepared.
- ii. Free-standing MMMs were prepared with PIM-1 and these graphene-like materials.
- iii. The MMMs were tested for ethanol and butanol recovery from water via pervaporation
- iv. 0.1 wt% of filler showed the highest improvement in selectivity towards butanol



**Molecular separations
(School of Chem. Eng.)
&
Nano-functional materials
(School of Materials)**



**Prof Budd's group
School of Chemistry**

**Dr Haigh and Dr Prestat
TEM experts**

