

INTENSIFICATION OF MVA AND INFLUENZA VIRUS PRODUCTION THROUGH HIGH-CELL-DENSITY CULTIVATION APPROACHES

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Background. Unlike production of recombinant proteins, continuous production of viral vaccines at high cell densities (HCD) is often constrained by a decrease in cell-specific virus yields, early host cell lysis during virus propagation and limited virus recovery from culture broth. Nevertheless, advanced fed-batch [1] and perfusion strategies can be applied to achieve high-yield virus production processes. In this study, the development of a semi-continuous process for the production of the modified vaccinia Ankara virus isolate MVA-CR19 and influenza virus A/PR/8/34 (H1N1) in HCD cultivations of the suspension cell line AGE1.CR.pIX (ProBioGen AG, Berlin) is presented.

Methods. Depending on the required scale, high cell concentrations ($\sim 50 \times 10^6$ cells/mL) were achieved either through medium renewal by periodic centrifugation (semi-perfusion) in 50 mL cultivations or using an alternating tangential flow (ATF) perfusion system for 1 L bioreactors. Process development and optimization comprised three phases: 1) assessment of different fed-batch and medium exchange strategies for the propagation of MVA-CR19 or influenza A/PR/8/34 viruses in 50 mL cultivations; 2) scale-up and process optimization of the selected high-yield process strategy to a 1 L bioreactor with the ATF system, and 3) integration of a one-step purification process using magnetic sulfated cellulose particles (MSCP). For both viruses, conventional batch cultivation (no addition/medium exchange after infection) was compared with processes applying fed-batch, periodic medium exchange and the combination of both during virus propagation.

Results. Perfusion and semi-perfusion at a feeding rate of 0.05 nL/cell \times d was suitable to propagate AGE1.CR.pIX cells above 60×10^6 cells/mL with neither limitation nor overload of nutrients. For infections at 50 mL scale, the application of a combined strategy comprising an initial fed-batch phase followed by a periodic virus harvest phase resulted in the highest product yield with a more than 10-fold increase in virus particles concentration compared to the conventional batch processes operated at 4 to 8×10^6 cells/mL [2]. Additionally, a 3-fold increase in both cell-specific yield (virus particles/cell) and volumetric productivity (virus particles/L \times d) could be obtained. Comparable yields were observed when up-scaling to a 1 L bioreactor using an ATF-system, even when virus particles were retained within the bioreactor. Further selection of the optimal pore size of the ATF membrane allowed semi-continuous harvesting of the produced viruses and its purification with MSCPs with a recovery from 30 to 50%. In all cases, cell-specific yields and volumetric productivities reached their maxima at 72 h post-infection, indicating that the process should be stopped at that time point.

Conclusion. Compared to conventional batch processes, the developed HCD process offers significantly higher productivities including the option to integrate a one-step purification process in a semi-continuous mode. Overall, the results show that there is a great potential for semi-continuous HCD processes for the production of viral vaccines in larger scales, which could support efforts towards the establishment of continuous vaccine manufacturing.

References.

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