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Experimental and simulation study on heat transfer in fluidized beds with heat production: An integrated DIA/PIV/IR technique and CFD-DEM

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[DPI Project # 751 Predictive Modeling of Polyolefin Reactors]

Experimental and simulation study on heat transfer in fluidized beds with heat production

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Content

- Project background
- Characterization of the heat source
 - CO₂/zeolites 13X adsorption: the adsorption kinetics and adsorption enthalpy
- Image processing
 - Visual and IR camera and images overlapping
- Modeling of the particle temperature in fluidized bed
 - Ideal CSTR model and Discrete Particle Model (DPM)
- Conclusion





Project background Polymerization process



Several characteristic length scales in a fluid bed reactor for catalytic olefin polymerization.







Project background Polymerization process



Several characteristic length scales in a fluid bed reactor for catalytic olefin polymerization.







Project background Polymerization process



Several characteristic length scales in a fluid bed reactor for catalytic olefin polymerization.







Characterization of zeolites 13X CO₂ adsorption



Rate of

Figure 1. pseudo-nth-order fitting of the adsorption rate from TGA measurements.









Experimental set-up and digital image analysis







Experimental set-up and digital image analysis







High speed visual camera (540x1024 pixels)







Image processing







Image processing







Fluidization experiments







Particle temperature evolution

Control the heat source by changing the concentration of CO₂ in the gas mixture



















Models



CSTR Model

Both solid and gas phases are wellmixed

$$\varepsilon_{g}\rho_{g}C_{p,g}V_{B}\frac{dT_{g}}{dt} = V_{B}h_{pg}a_{s}(T_{p}-T_{g}) + u_{g}A_{B}C_{p,g}\rho_{g}(T_{g}^{in}-T_{g}^{out}) + Q_{loss}$$

$$(1-\varepsilon_{g})\rho_{p}C_{p,p}\frac{dT_{p}}{dt} = a_{s}h_{gp}(T_{g}-T_{p}) + \frac{dq}{dt}m_{p}\Delta H_{ads}$$

$$\frac{\partial}{\partial t} \varepsilon \rho_g \mathbf{u} + \nabla \cdot \varepsilon \rho_g \mathbf{u} \mathbf{u} = -\varepsilon \nabla p - \nabla \cdot \varepsilon \mathbf{\tau}_g - S_p + \varepsilon \rho_g \mathbf{g}$$
$$m_a \frac{d \mathbf{v}_a}{dt} = \mathbf{F}_d + \mathbf{F}_p + \mathbf{F}_g + \mathbf{F}_c$$

$$C_{p,g}\left[\frac{\partial(\varepsilon_{g}\rho_{g}T_{g})}{\partial t} + (\nabla \cdot \varepsilon_{g}\rho_{g}\mathbf{u}_{g}T_{g})\right] = -(\nabla \cdot \varepsilon_{g}\mathbf{q}) + Q_{p} + Q_{loss}$$

$$\rho_{p}V_{p}C_{p,p}\frac{dT_{p}}{dt} = -hA_{p}\left(T_{p,a} - T_{g}\right) + \frac{dq}{dt}m_{p}\Delta H_{ads}$$





Model fitting results: CSTR $\mathcal{E}_{g}\rho_{g}C_{p,g}V_{B}\frac{dT_{g}}{dt} = V_{B}h_{pg}a_{s}(T_{p}-T_{g}) + u_{g}A_{B}C_{p,g}\rho_{g}(T_{g}^{in}-T_{g}^{out}) + Q_{loss}$ $(1 - \varepsilon_g)\rho_p C_{p,p} \frac{dT_p}{dt} = a_s h_{gp} (T_g - T_p) + \frac{dq}{dt} m_p \Delta H_{ads}$ $\frac{dq}{dt} = k_{ads} (q - q_e)^{nads}$ $Q_{loss} = h_{bw}(T_g - T_w)$ 330 330 330 Tp Expe1 Tp Expe20-1 -T_p Expe60-1 CO₂/N₂ (40% CO₂) CO₂/N₂ (60% CO₂) CO₂/N₂ (20% CO₂) Tp Expe2 325 Tp Expe20-2 325 325 T_Expe60-2 Tp Expe20-3 Tp Expe3 q_e=0.13 [g/g] q_e=0.1 [g/g] q_e=0.15 [g/g] - T_ CSTR(60%) Tp CSTR(40%) Tp CSTR(20%) Barticle temperature [K] 315 315 305 300 300 Barticle temperature [K] 320 315 305 305 300 300 295 295 295 290 ^L 0 290 290 20 100 40 60 80 40 60 60 80 100 0 20 80 100 20 40 0 Time [s] Time [s] Time [s]

11





One to one comparison with DPM









One to one comparison with DPM









Conclusions

- A non-intrusive visual technique combined with high speed IR camera and visual camera has been utilized to visualize the particle temperature distribution in a fluidized bed with a heat source from adsorption.
- The spatial-averaged particle temperature evolution obtained from processing of experimental results using visual image mask technique, was used to verify a CSTR model and further more to validate CFD-DEM.
- Compare to the experiment, CFD-DEM can well capture the spatial particle temperature distribution and particle temperature evolution.





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Thanks for your attention!