

2015

On-line analysis of catalytic biomass products using a high pressure Tandem micro-Reactor GC/MS

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Recommended Citation

M. Soll, R.R. Freeman, Chu Watanabe, Ichi Watanabe, Y.M Kim, N. Teramae, and K. Wang, "On-line analysis of catalytic biomass products using a high pressure Tandem micro-Reactor GC/MS" in "Biorefinery I: Chemicals and Materials From Thermo-Chemical Biomass Conversion and Related Processes", Nicolas Abatzoglou, Université de Sherbrooke, Canada Sascha Kersten, University of Twente, The Netherlands Dietrich Meier, Thünen Institute of Wood Research, Germany Eds, ECI Symposium Series, (2015).
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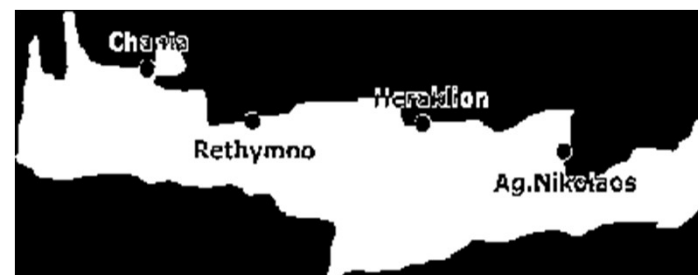
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Frontier Laboratories⁽¹⁾, Tohoku University⁽²⁾ and Iowa State University⁽³⁾



Biorefinery I: Chemicals and Materials From Thermo-Chemical Biomass Conversion and Related Processes

September 27-October 2, 2015
Atlantica Caldera Crete Paradise Hotel
Chania (Crete), Greece



“Almost everything in your daily life depends on catalysts.” – Argonne National Laboratory

- **Continuous search for new catalysts and “good” biomasses** – one that works “better” than those being used for a given process
- **Test parameters**
 - Temperature
 - Surface area (contact time)
 - Atmosphere
 - Pressure
 - Effective life time
 - Activity regeneration
- **Rapid screening of new catalysts (and biomasses) is essential if sustainable “green” products are going to exist in the future.**

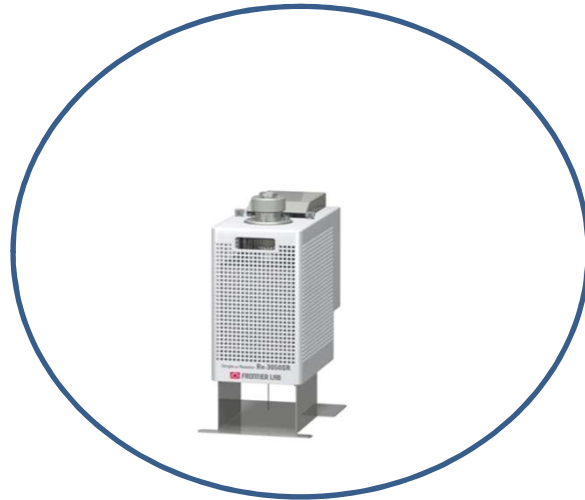
Dimensions for “Rapid screening”

~~Think~~ big !

~~Think~~ small !


Think „smart“: fast,
flexible, μ scale, online
GC/MS analysis !

Fast pyrolysis: Important features for GC/MS

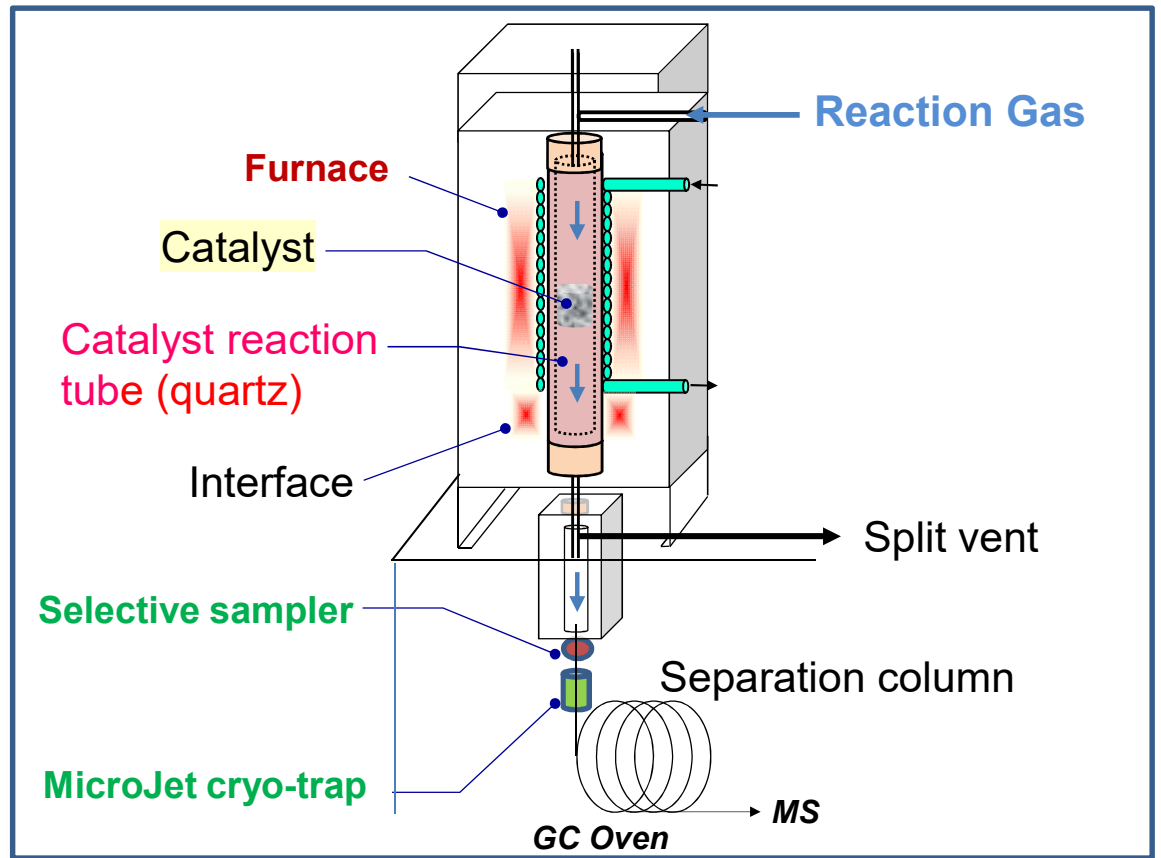
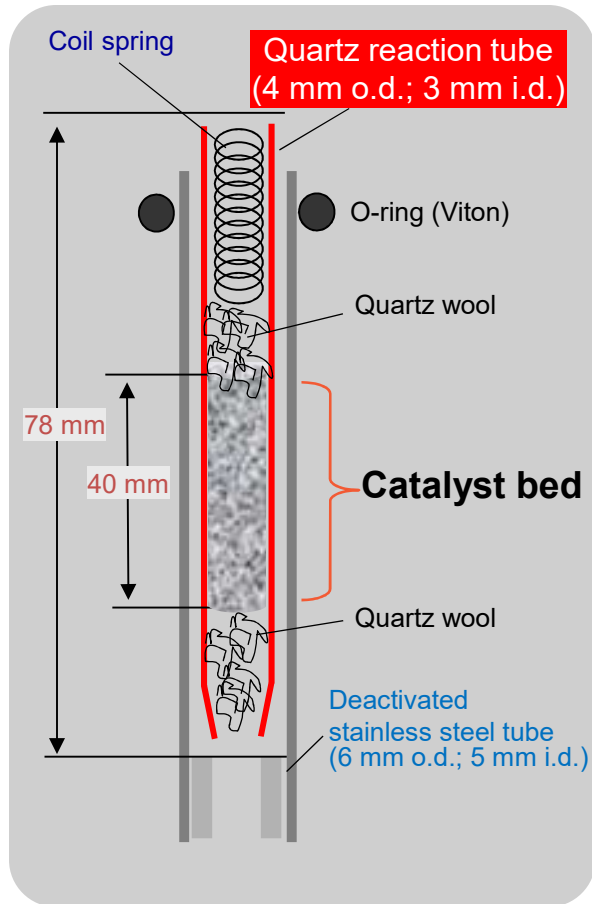


Pyrolyzers and μ -Reactors

Sample Conditioning

- Gases, liquids and solids  vapors
- Precise Temperature Control
- Low dead volume
- Inert surfaces
- No cold or hot spots

Design of Single μ -Reactor



From Single to Tandem μ -Reactor

Single μ -Reactor
Rx-3050SR



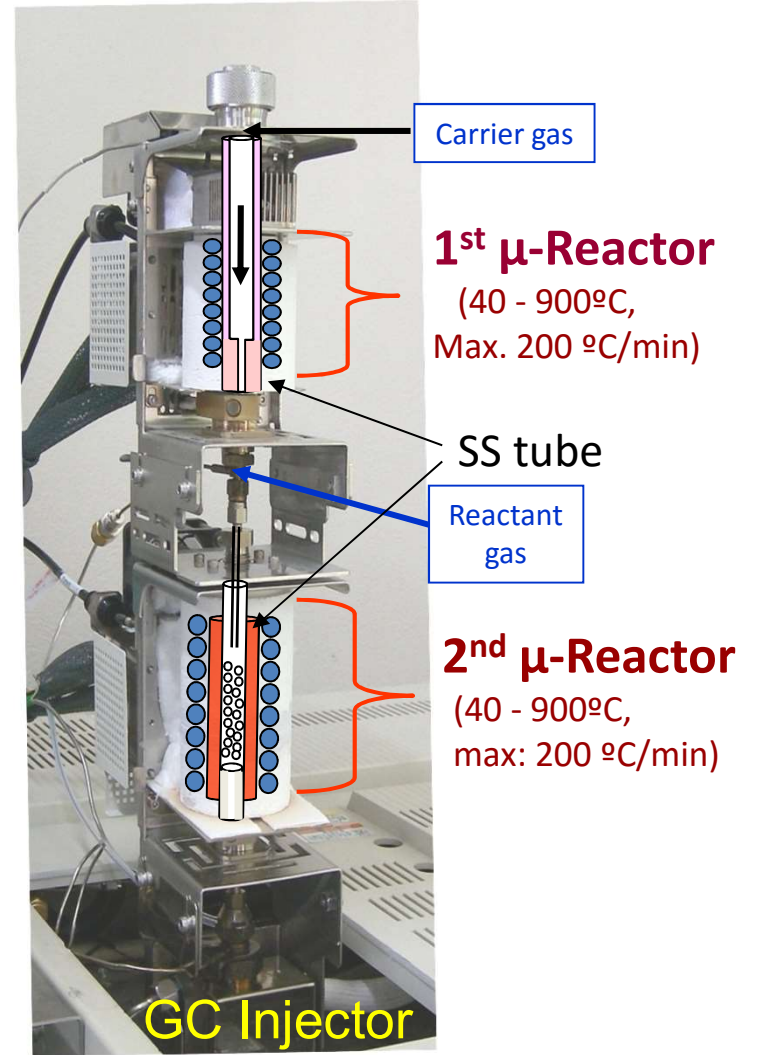
In-situ only

Tandem μ -Reactor
Rx-3050TR

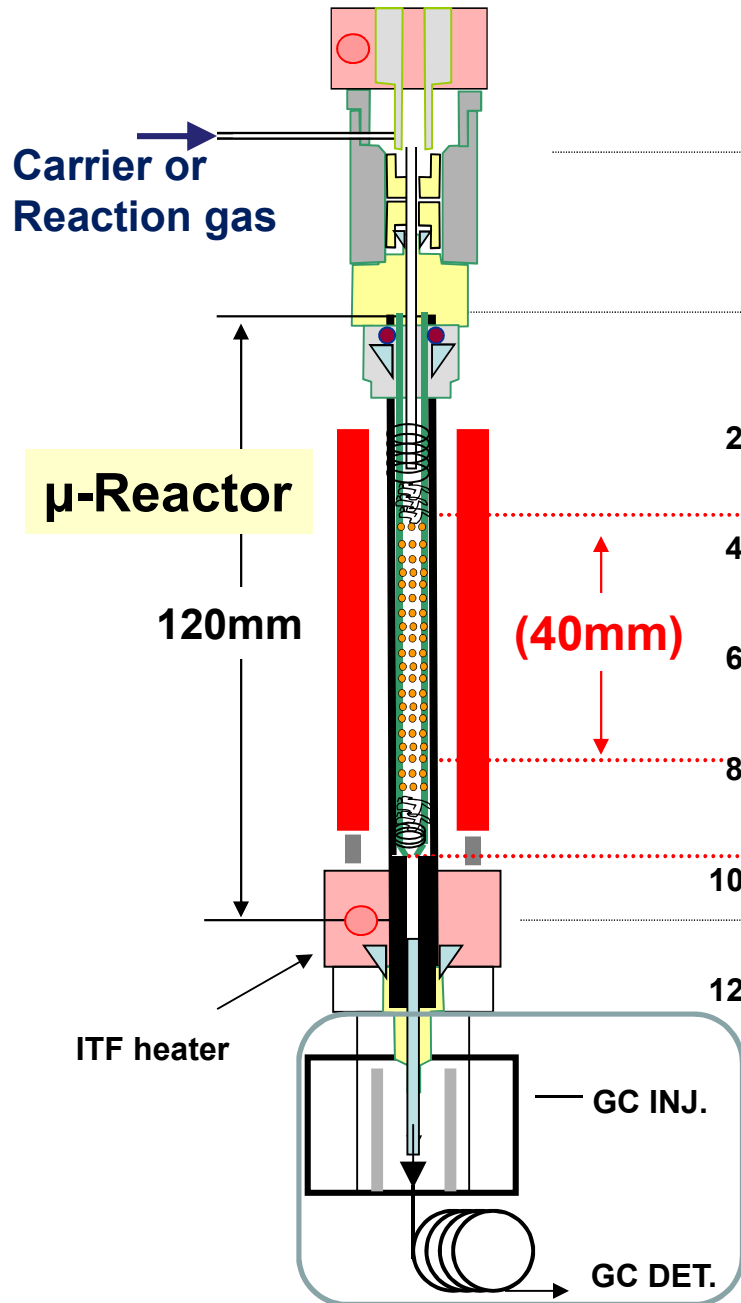


In-situ and ex-situ

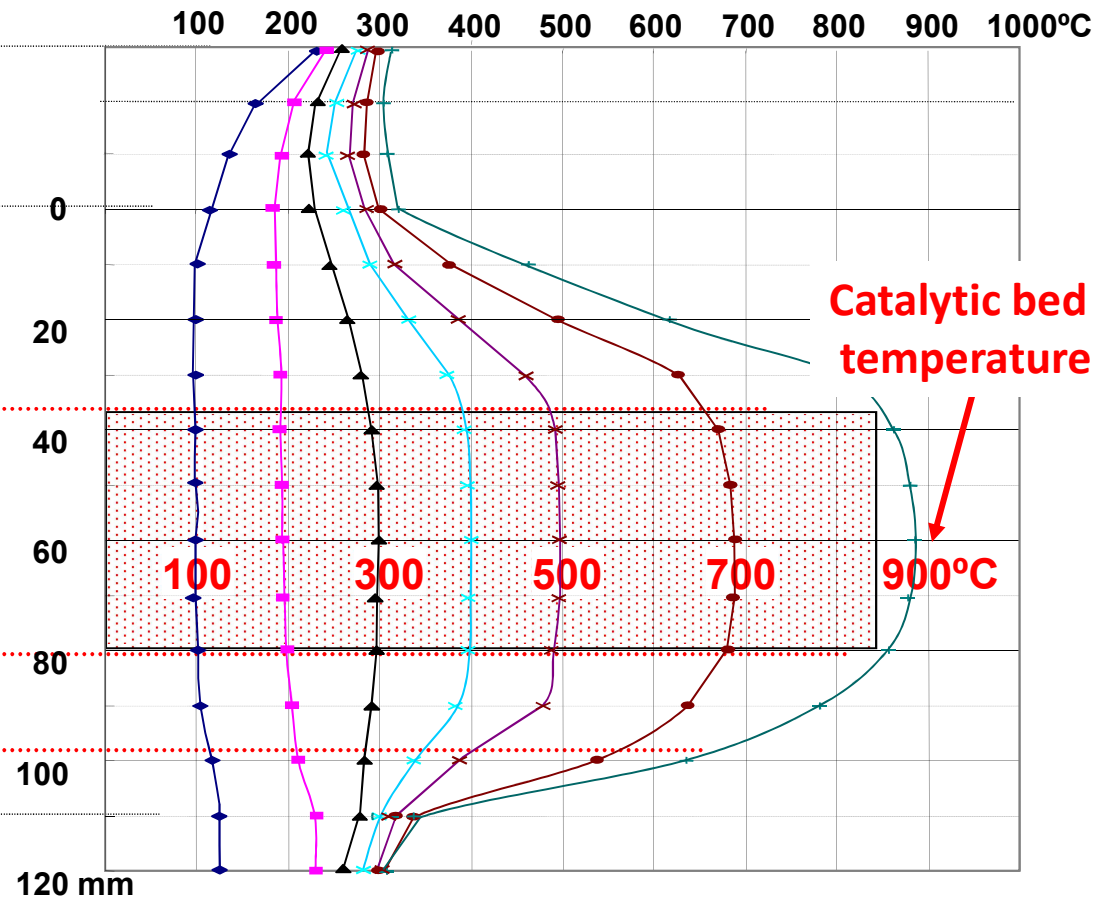
- Catalytic pyrolysis
- Catalytic cracking
- Hydropyrolysis
- High pressure pyrolysis



Catalytic bed temperature profiles [100 - 900°C]



Catalytic bed temperature at various points

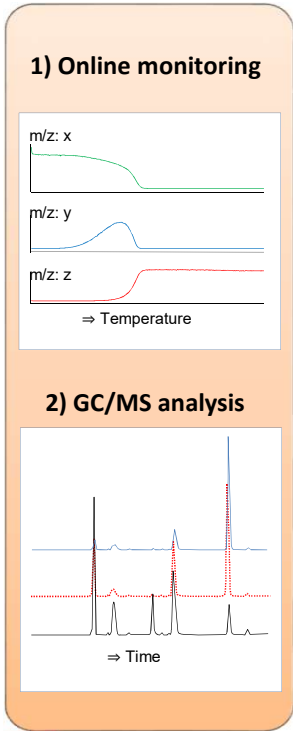
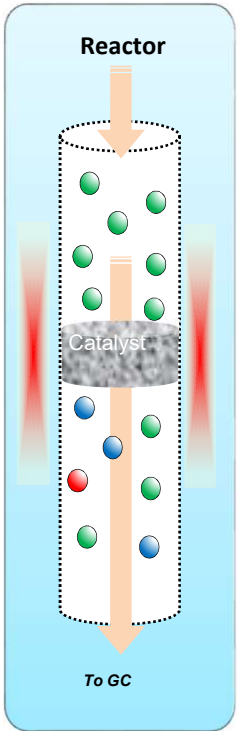
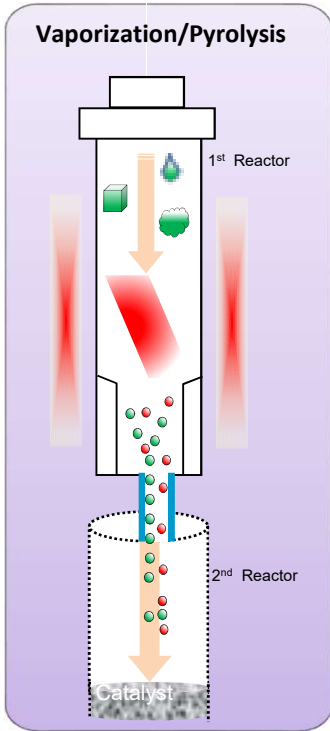
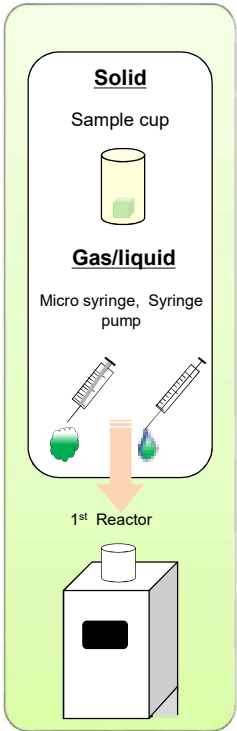
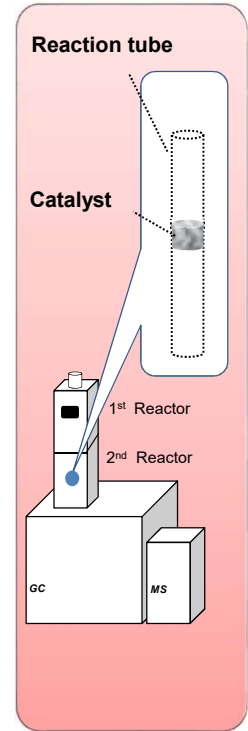
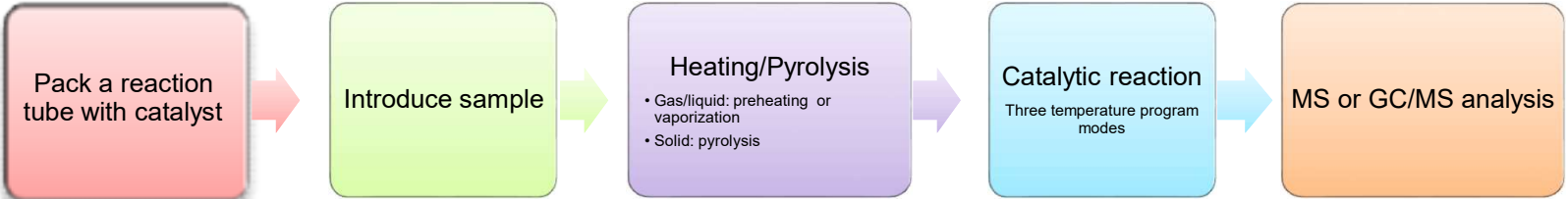


μ -Reactor: 100°C (2nd- ITF: 250°C)

μ -Reactor: 200 & 300°C (2nd- ITF: 300°C)

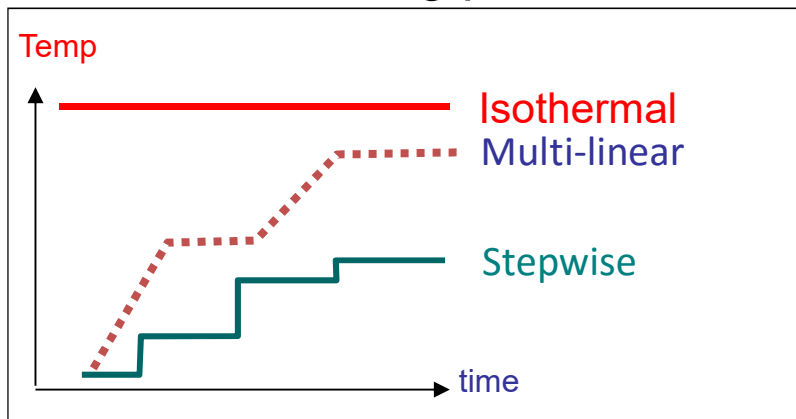
μ -Reactor: 400-900°C (2nd- ITF: 350°C)

Handling and workflow



Temperature control and two analytical modes of Tandem μ -Reactor

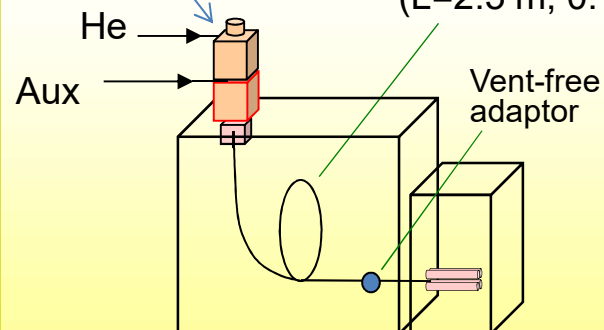
3 Reactor heating profiles



On-line EGA-MS analysis

Reactor temp progr.

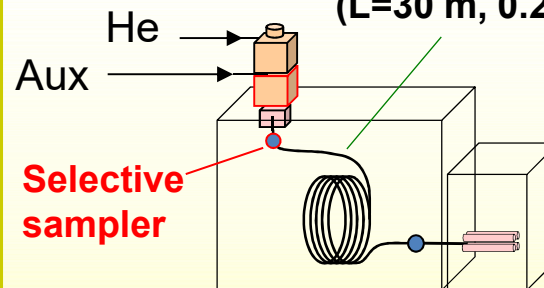
EGA tube
(L=2.5 m, 0.15 Φ)



Oven: Isothermal (300°C)

EGA-Selective zone GC/MS analysis

GC column
(L=30 m, 0.25mm)



Oven: temp program.

OTHER LAB

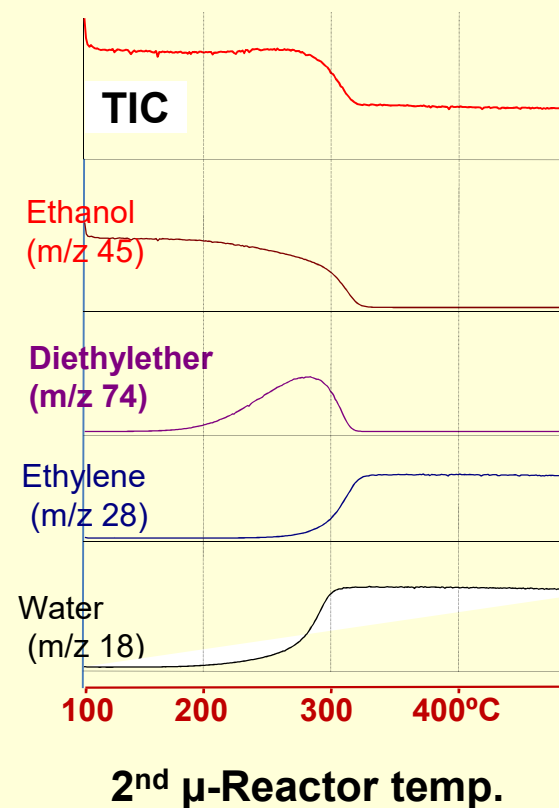
Catalytic conversion of ethanol to ethylene

(Std. config = low pressure)

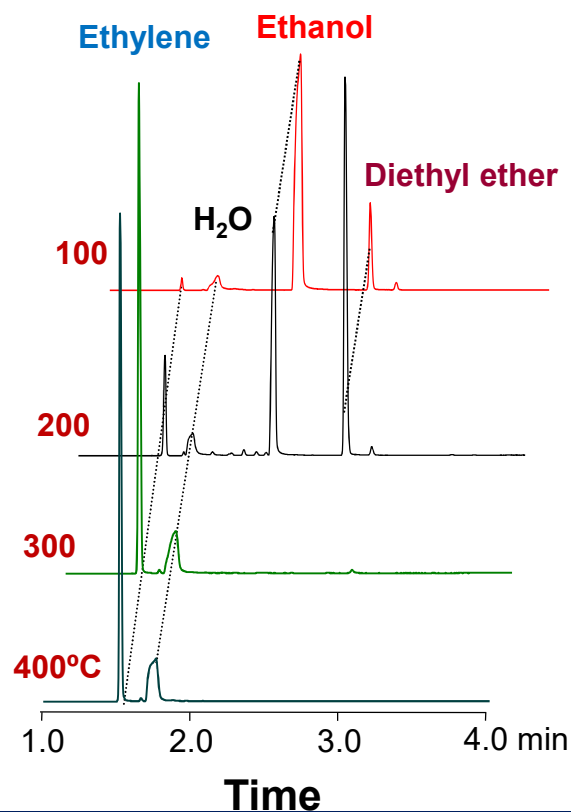
Online – MS analysis
“*Linear temp. mode*”

Separation analysis
“*Stepwise temp. mode*”

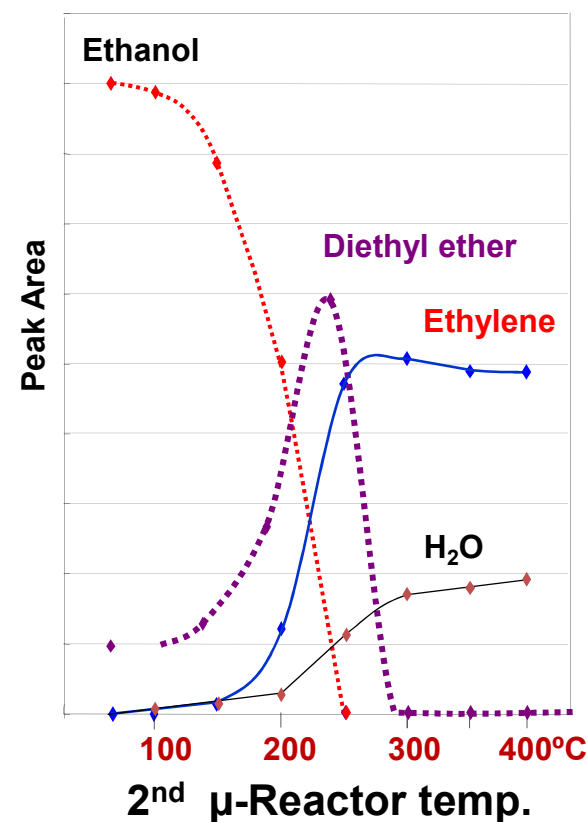
1st μ -Reactor: 100°C,
2nd μ -Reactor: 100-400°C (20 °C/min)
Catalyst: H-ZSM-5



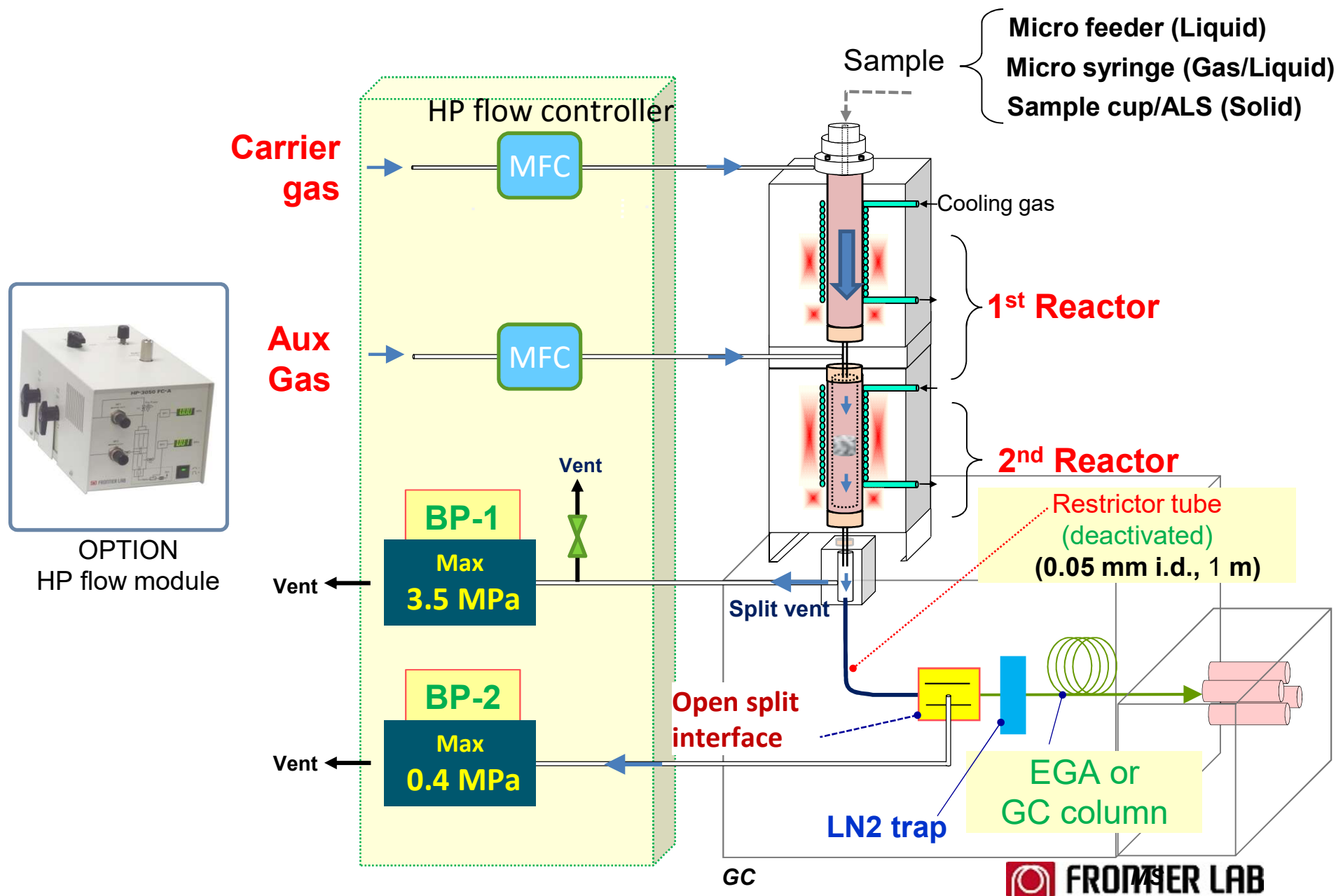
1st μ -Reactor: 100°C,
2nd μ -Reactor: 100, 200, 300, 400°C (1sec)



Reaction temp. vs. Peak area

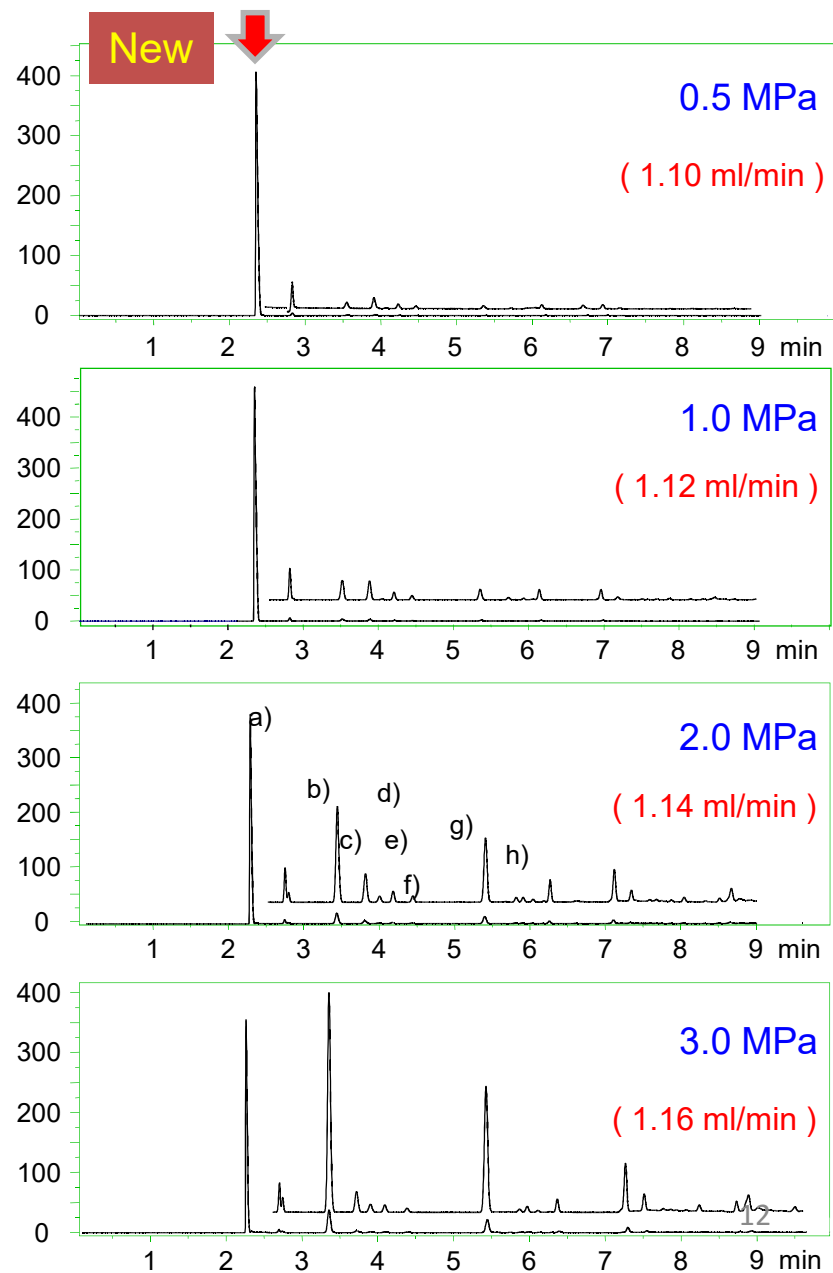
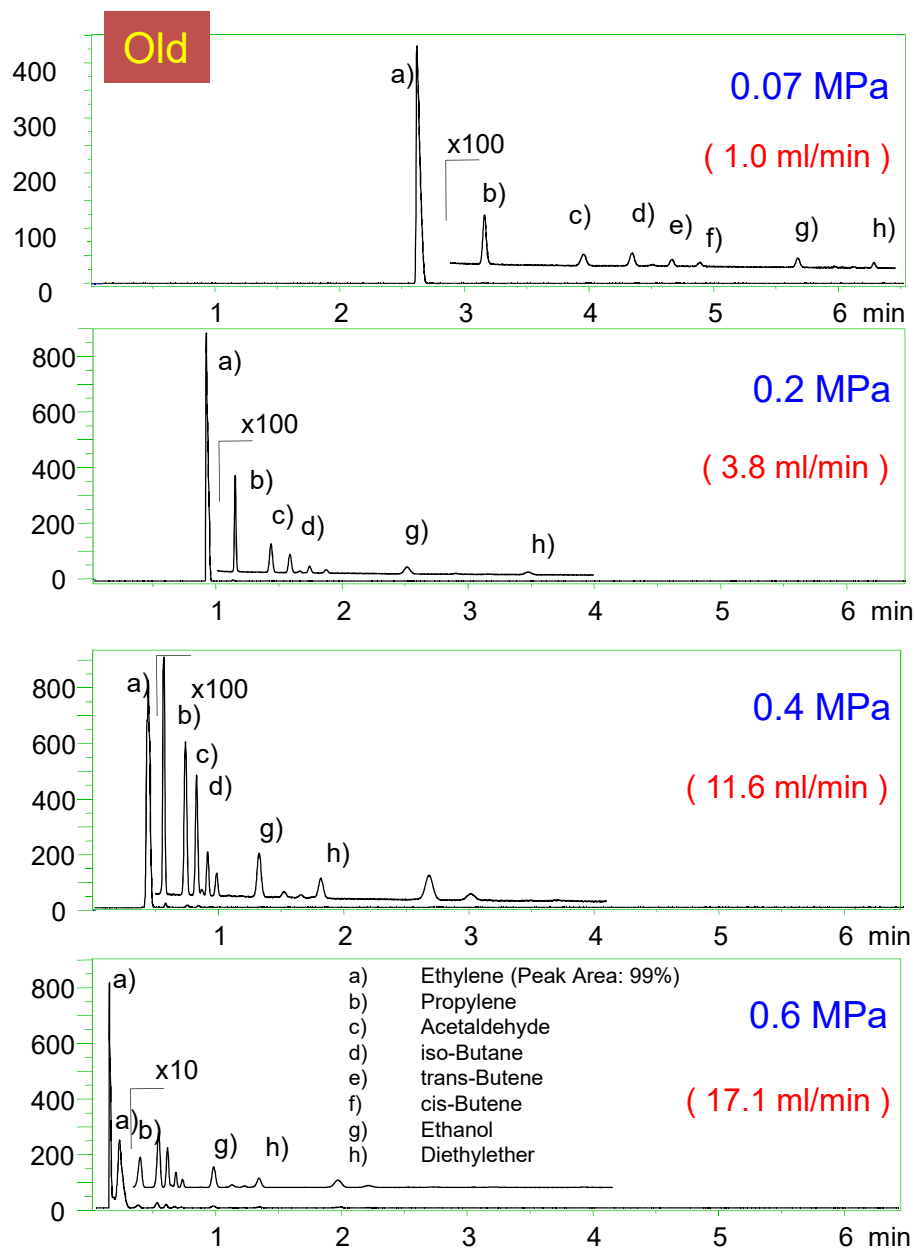


Innovative pneumatics for HP Tandem μ -Reactor



No retention time shift due to BP regulators and open split interface

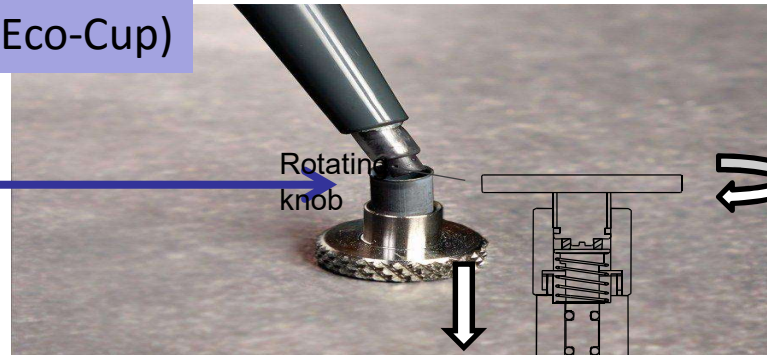
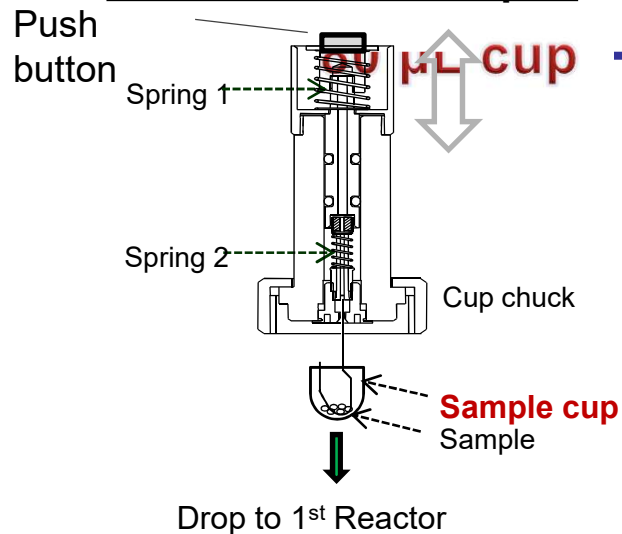
Catalyst (ZSM-5) at 230°C, : BP1: 0.5-3.0 MPa, BP2: 0.1 MPa, Restrictor: 40 cm , i.d. 50 μm, Column: UA1-30M-2.0F, Detector: FID



High pressure sample injection of solids

Sample is placed directly into the sample cup (Eco-Cup)

Standard solid sampler



Rotating knob

High pressure solid sampler

Drop to 1st Reactor



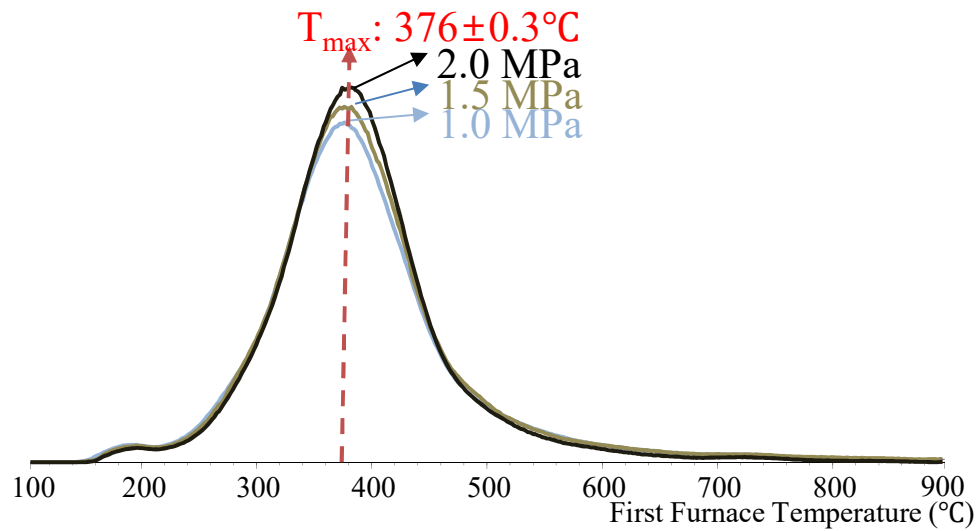
Two applications using the high pressure Tandem μ -Reactor

1. Conversion of lignin (He/H₂ and P)
2. Conversion of Ethanol (T and P)

Applying different parameters:

- ❖ Biomass (nature, amount)
- ❖ Catalysts (type, particle size, catalyst/biomass ratio)
- ❖ Temperature (1st and 2nd Reactor)
- ❖ Reaction-/Carrier-Gases (He/H₂)
- ❖ (High)-Pressure
- ❖ GC/MS settings

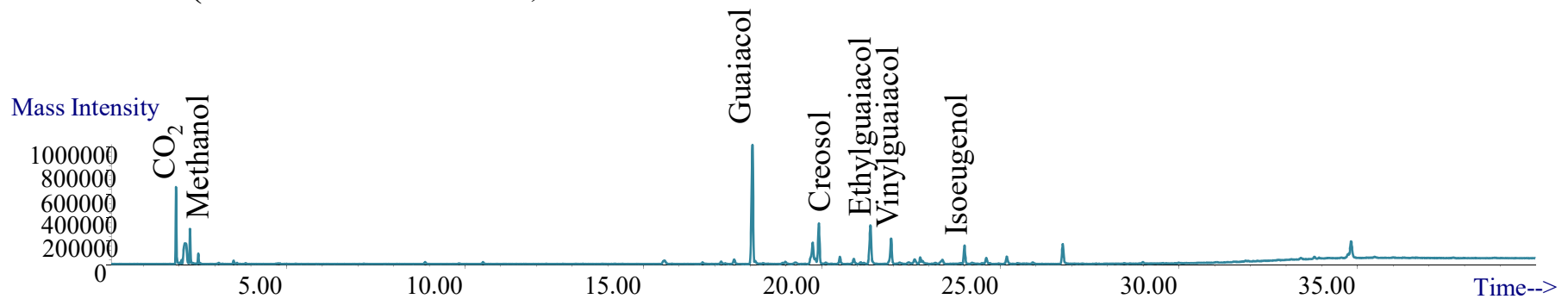
Non-catalytic pyrolysis of kraft lignin under high pressure helium (carrier gas)



EGA Thermogram of Kraft Lignin
(second Reactor = 320 °C)

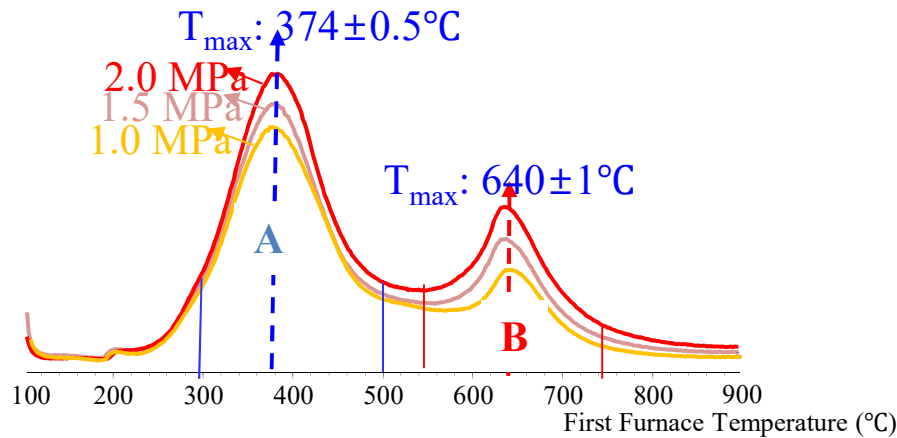
Remained char after EGA-MS analysis

Pressure (MPa)	1.0	1.5	2.0
Char (wt.%)	44.5	44.2	45.3



Pyrogram obtained heart-cut EGA-GC/MS analysis from 300 to 500°C under 2MPa of helium atmosphere

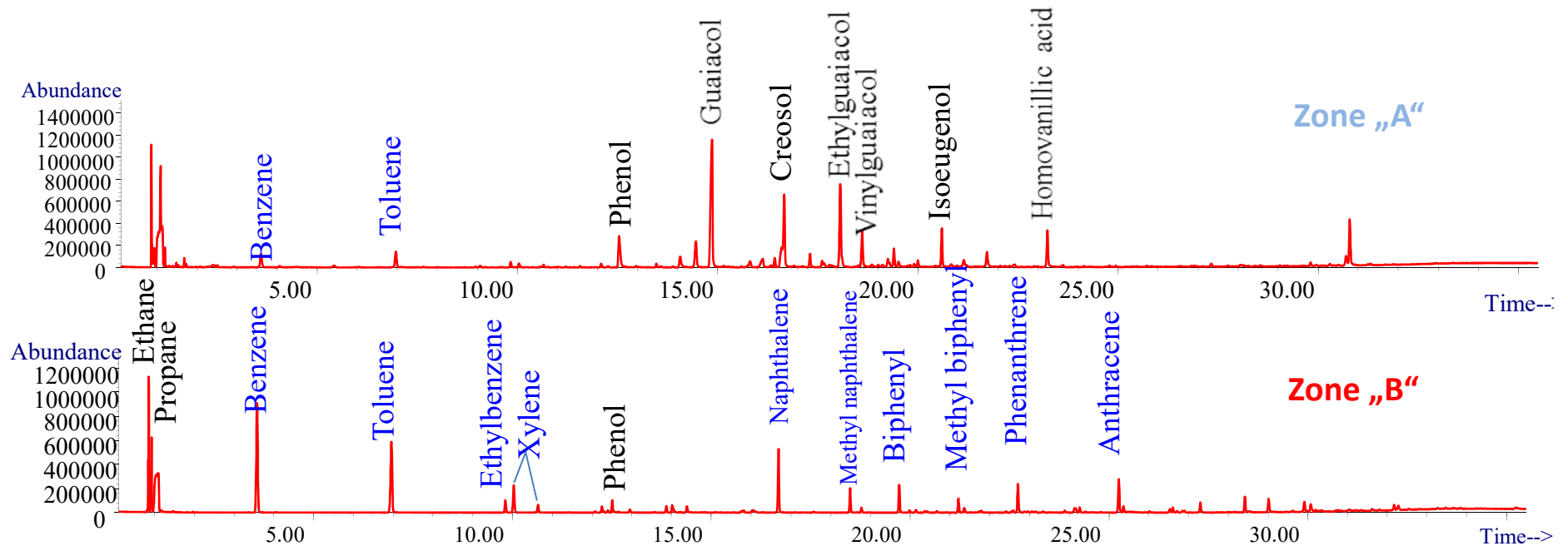
Non-catalytic „hydropyrolysis“ of kraft lignin under high pressure hydrogen



Remained char after EGA-MS analysis

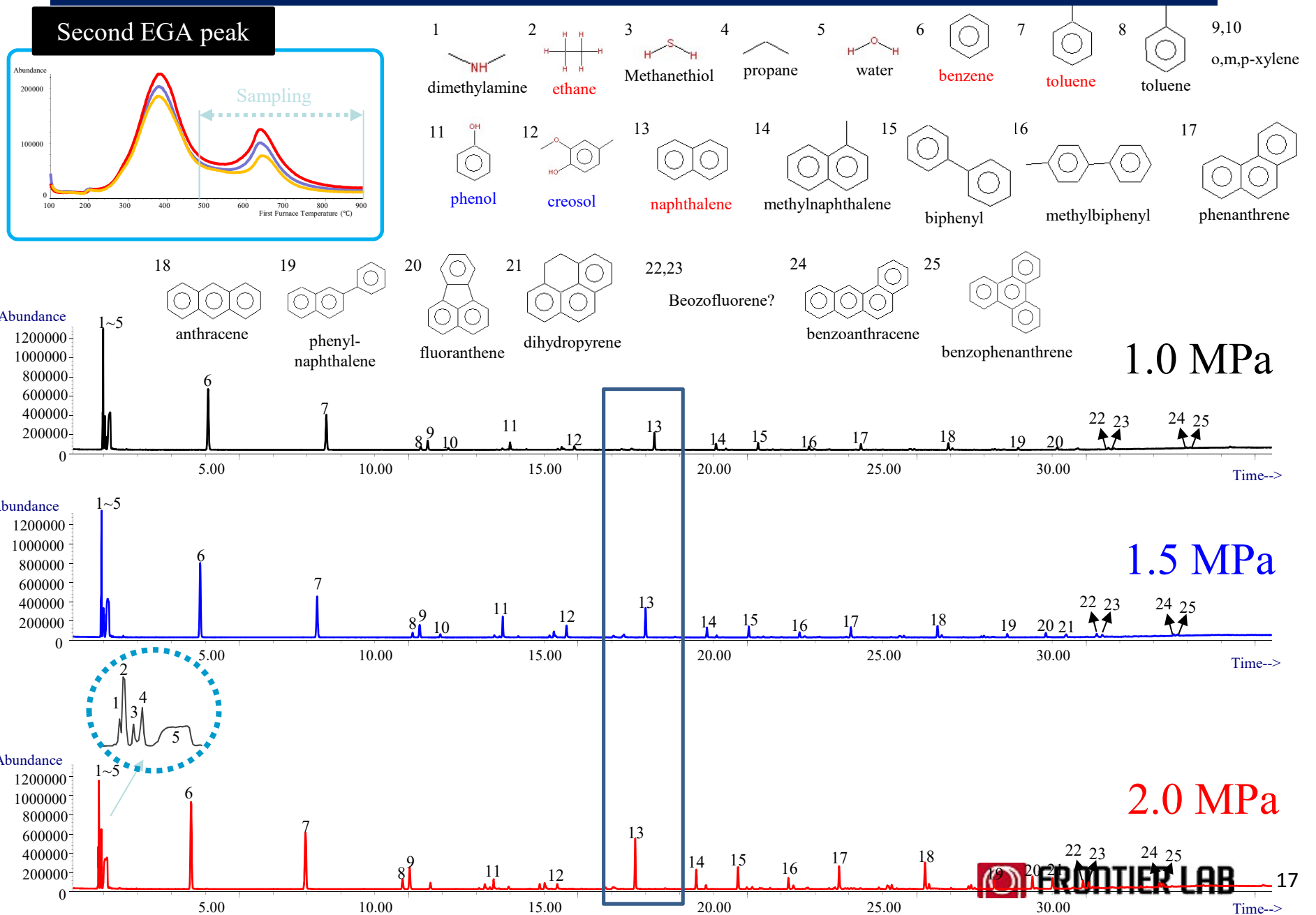
Pressure (MPa)	1.0	1.5	2.0
Char (wt.%)	35.2	26.3	21.4

EGA Thermogram of Kraft Lignin under Different Hydrogen Pressure.



Pyrogram obtained heart-cut EGA-GC/MS analysis from 100 to 800 °C under 2MPa of hydrogen atmosphere

Heart-Cut EGA-GC/MS at Different Hydrogen Pressures



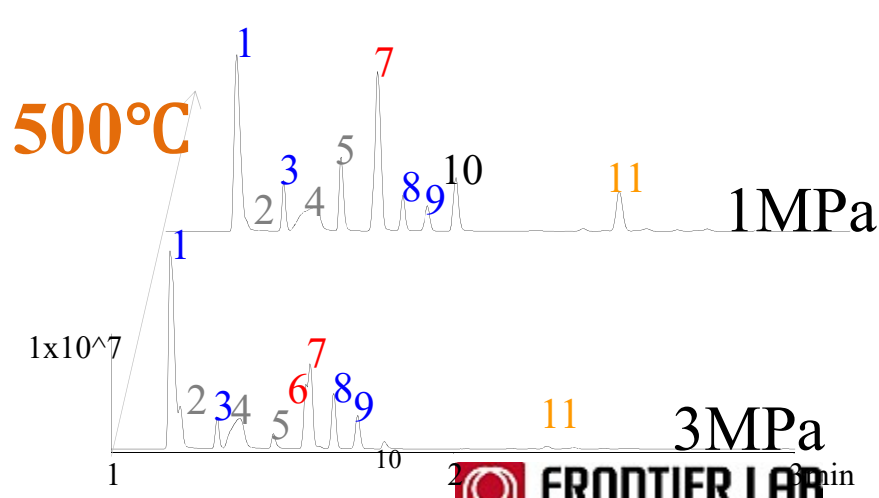
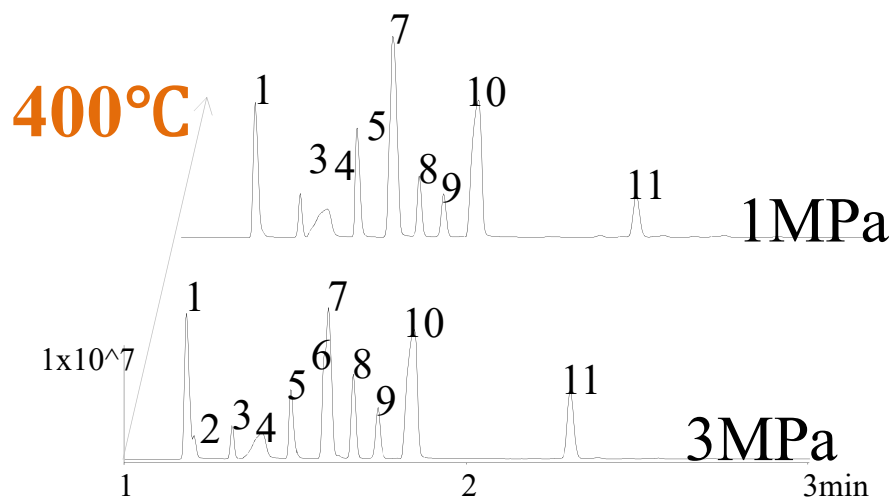
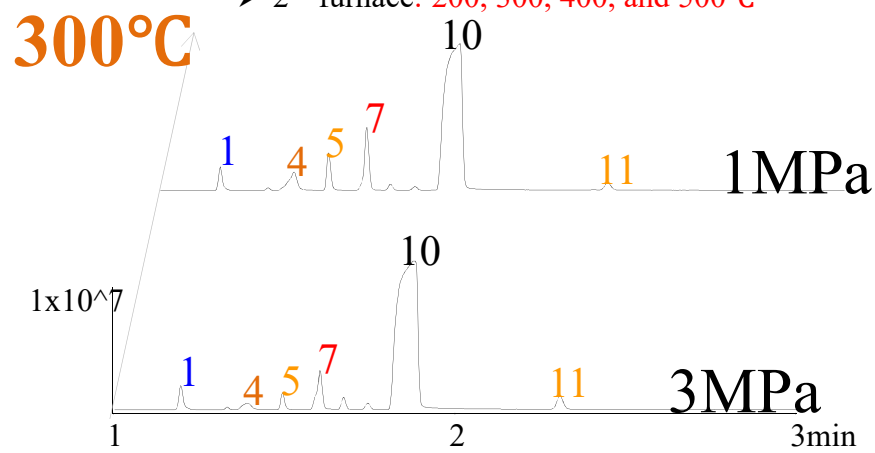
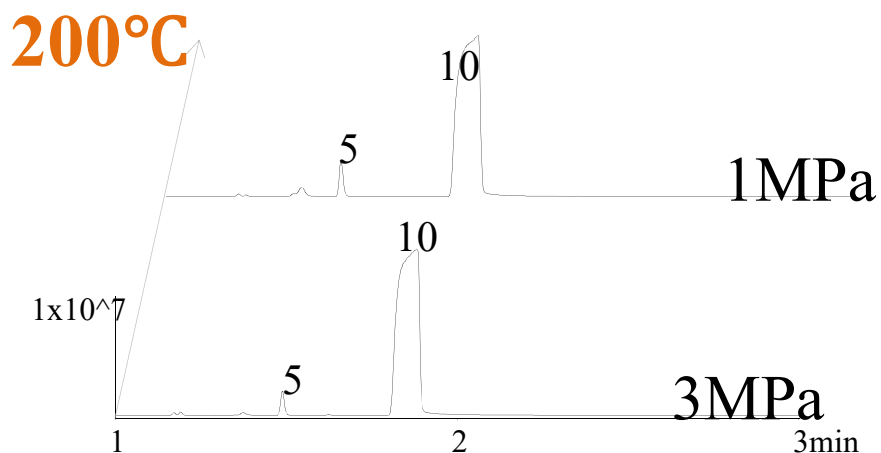
Results lignin conversion under high pressure hydrogen

- Heart-Cut EGA-GC/MS results showed that most of pyrolyzates of first EGA peak were phenolic pyrolyzates of lignin, such as guaiacols, pyrocatechol, cresol, eugenol, and homovanillic acid.
- Second EGA peak shows quite large amount of valuable aromatic compounds such as BTEXs, naphthalenes, biphenyls, phenanthrenes, and anthracenes and their peak intensities were increased under higher pressure. This can indicate that there is an important interaction between char intermediates and hydrogen gas and this interaction can produce large amount of aromatic oil under high hydrogen pressure.

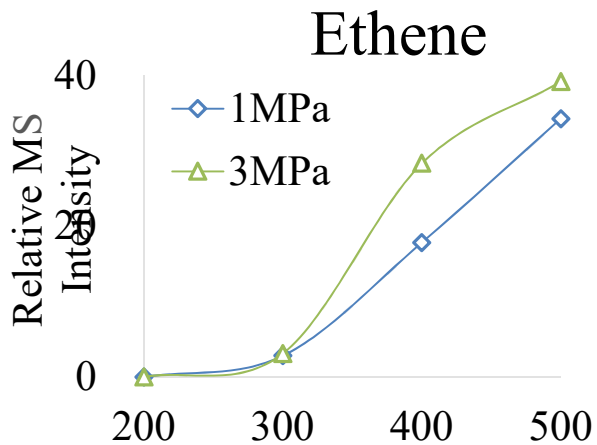
Ethanol over MgO-SiO₂ Catalyst under hydrogen and **high pressure** plus **different catalytic bed temperatures**

1: Ethylene, 2: Ethane, 3: Propene, 4: Water, 5: Acetaldehyde, 6,8,9: Butene, 7: Butadiene,
10: Ethanol, 11: Diethyl ether

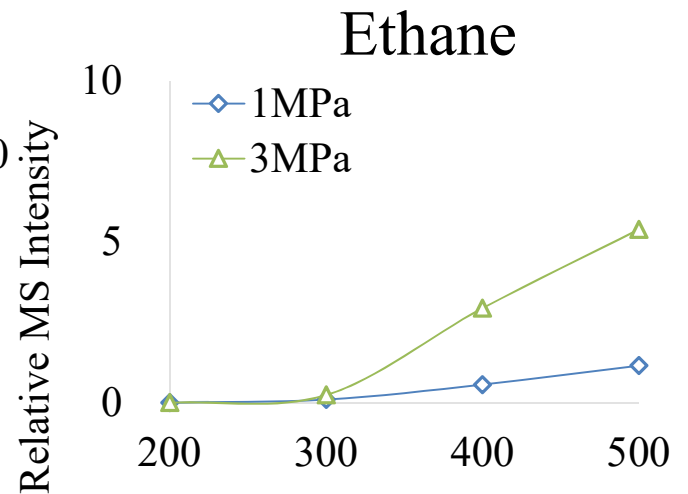
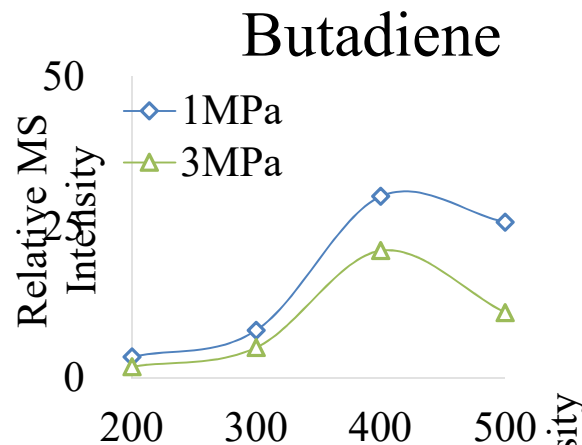
- 1st furnace: 300°C
- 2nd furnace: 200, 300, 400, and 500°C



Ethanol over MgO-SiO₂ Catalyst under hydrogen and high pressure: Different catalytic bed temperatures



- Ethanol conversion and product distribution were quite different at different catalyst bed temperature.
- Butadiene and ethene yield were maximized at 400 and 500 °C, respectively.
- By increasing reaction pressure from 1 to 3 MPa, butadiene yield was decreased, however, ethene and ethane yields were increased at all applied temperatures



Experimental Conditions

- Sample: Ethanol, 2ul
- Catalyst: MgO-SiO₂, 60mg
- 1st furnace: 300°C
- 2nd furnace: 200, 300, 400, and 500°C
- BP1: 1, 3 MPa
- BP2: 42 KPa (H₂)
- System Split ratio: He 500:1

SUMMARY

- Tandem μ -Reactor facilitates the rapid characterization of catalysts and biomasses
- Full spectrum of operating parameters can be investigated – SW controlled / online
- Easy and fast exchange of catalysts
- Real time analysis of gaseous or liquid samples
- automated analysis of solids (using “Autoshot” auto-sampler)
- species identification using MS
- High pressure option without loss of chrom. performance

The development and use of “best”/proper catalysts means new products, lower costs, and a broader range of feedstocks

Questions?

catalyst
RAPID
Process
GC/MS
Reactor
Pilot Plant
Catalyst
New
Pd
Scale-Up
Frontier Labs

SCREENING
New
catalytic
micro
ISU
biomass
FAST PYROLYSIS
Solids
engineer
Rh
Products

Tandem
Reactant gases
wood
olefinic
Carbon
ethylene
saturated
hydrogenation

Renewable
Pt
H₂O
GC/MS
Ru
New
High
RAPID
Selective

Productivity