

Pyrolysis of Agricultural and Forestry Residues into Bio-oil



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Outline

- **Motivation**
- **Approach**
- **Experimental Set Up**
- **Experimental Results**
- **Conclusions**



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Motivation -1

- Global Warming.
 - Depleting Conventional Fossil Fuel Reserves.
- Demand for renewable energy.



Demand for proper disposal of agricultural and forestry residues.



Utilization of Agricultural and Forestry Residues as Energy Resources

Motivation -2



Wine Grape



Wine



Grape Skins and Seeds

12.2 million tonnes worldwide



Corn



Bio ethanol



Dried Distiller's Grains

3.5 million tonnes in North America



Sugarcane



Sugarcane Juice



Sugarcane Bagasse

500 million tonnes worldwide



Forest Resources



Pulp and Paper

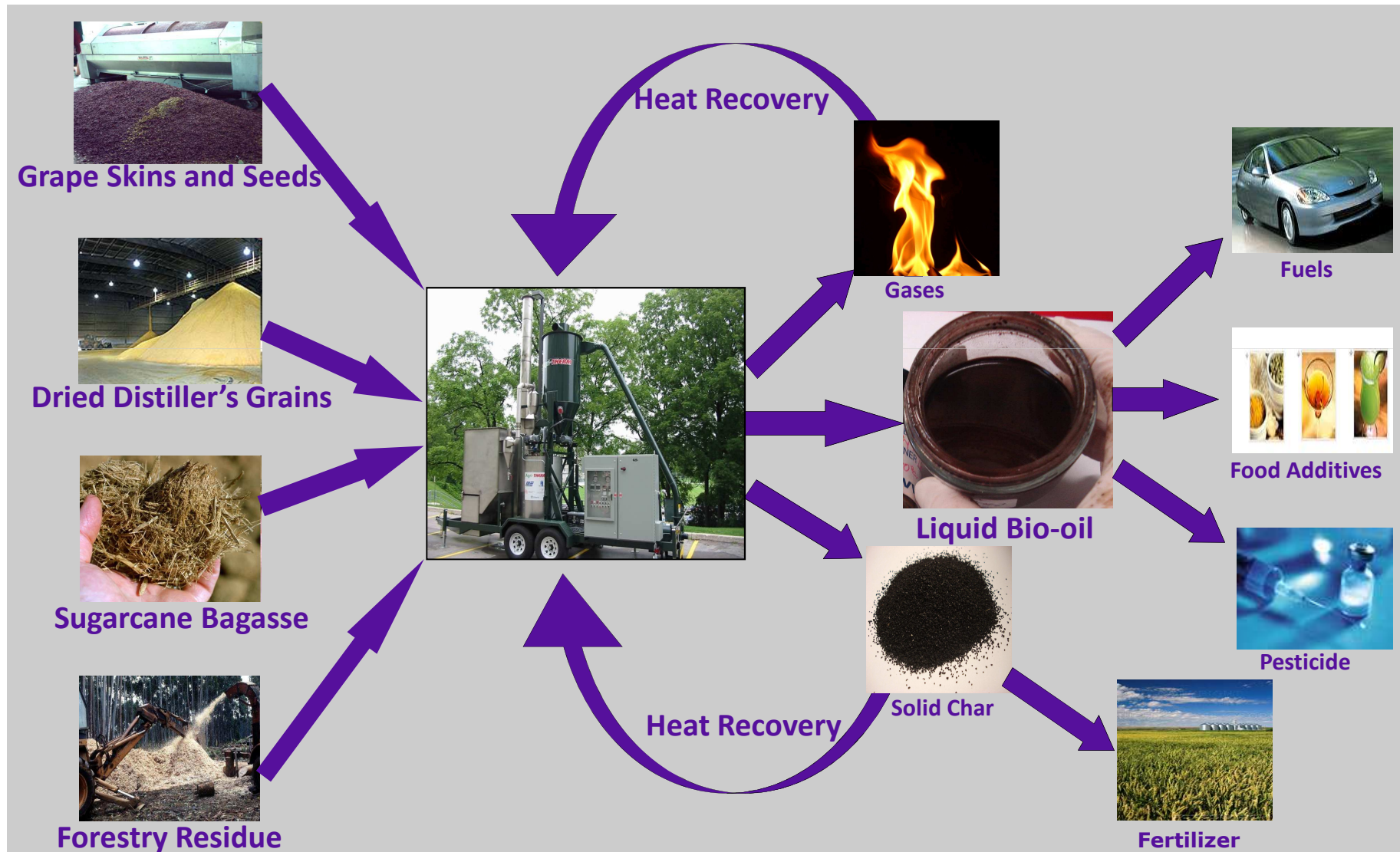


Forestry Residue

280 million tonnes worldwide

One Possible Solution

- Conversion of Agricultural and Forestry Residues into Bio-Oil via **Fast Pyrolysis**.



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Experimental Set Up

Pilot Plant Reactor

Fluidized bed:

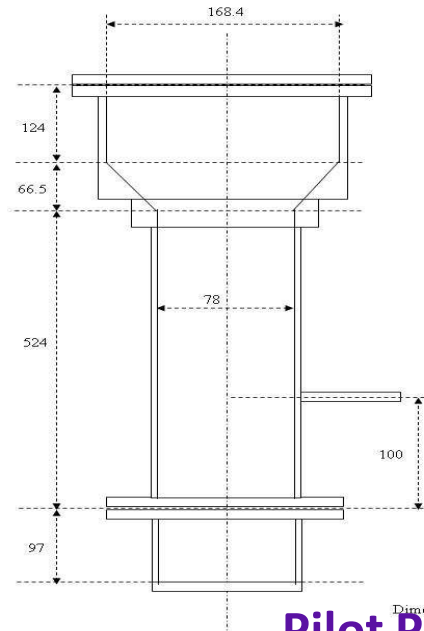
- 7.8 cm diameter
- 0.5 m high.

Equipped with removable freeboard sections.

- Residence Time Range:
1 to 30 seconds.

Intense heat transfer & mixing

Operating Temperature Range:
Up to 700 ° C.



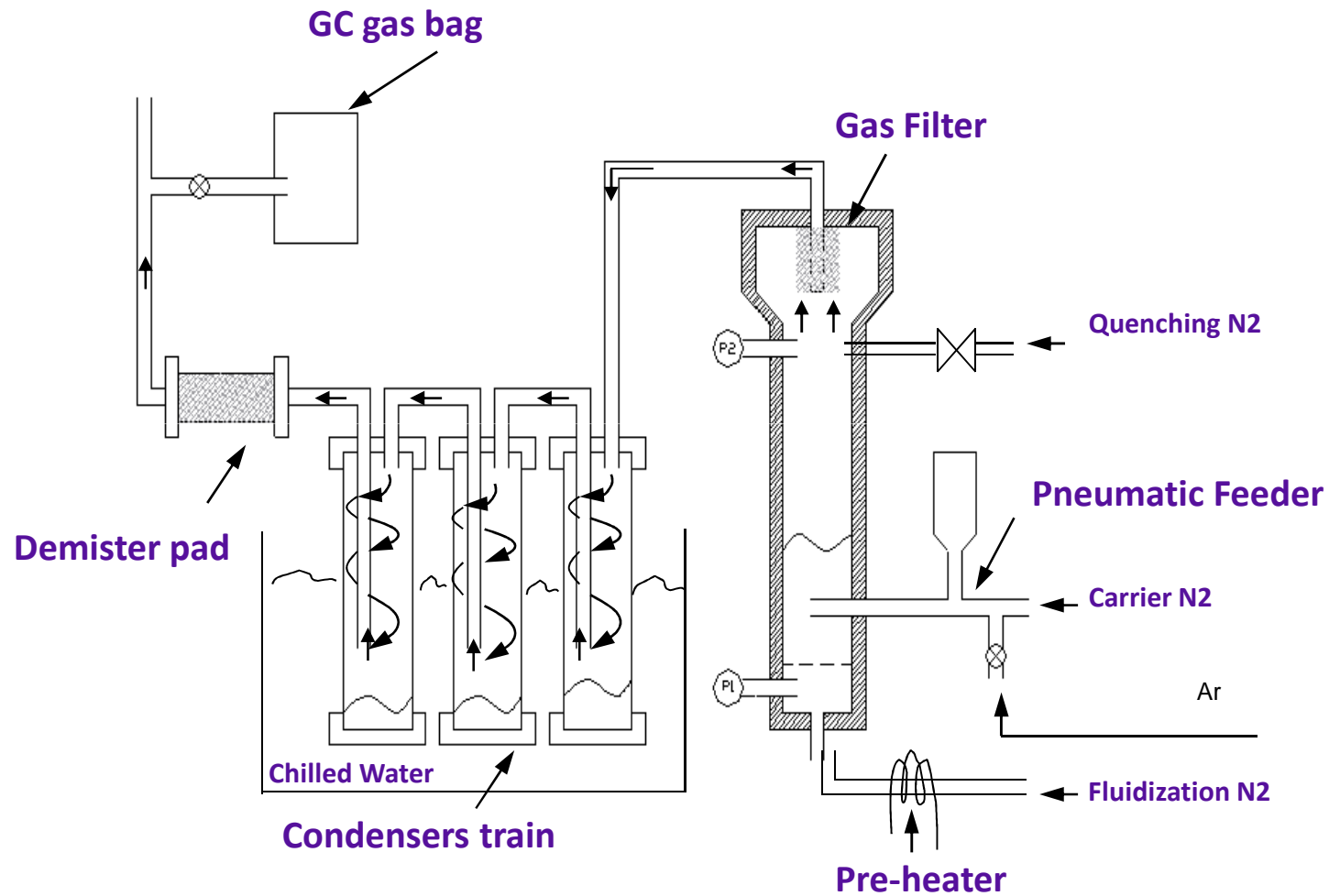
Pilot Plant Reactor



Pilot Plant Reactor Top

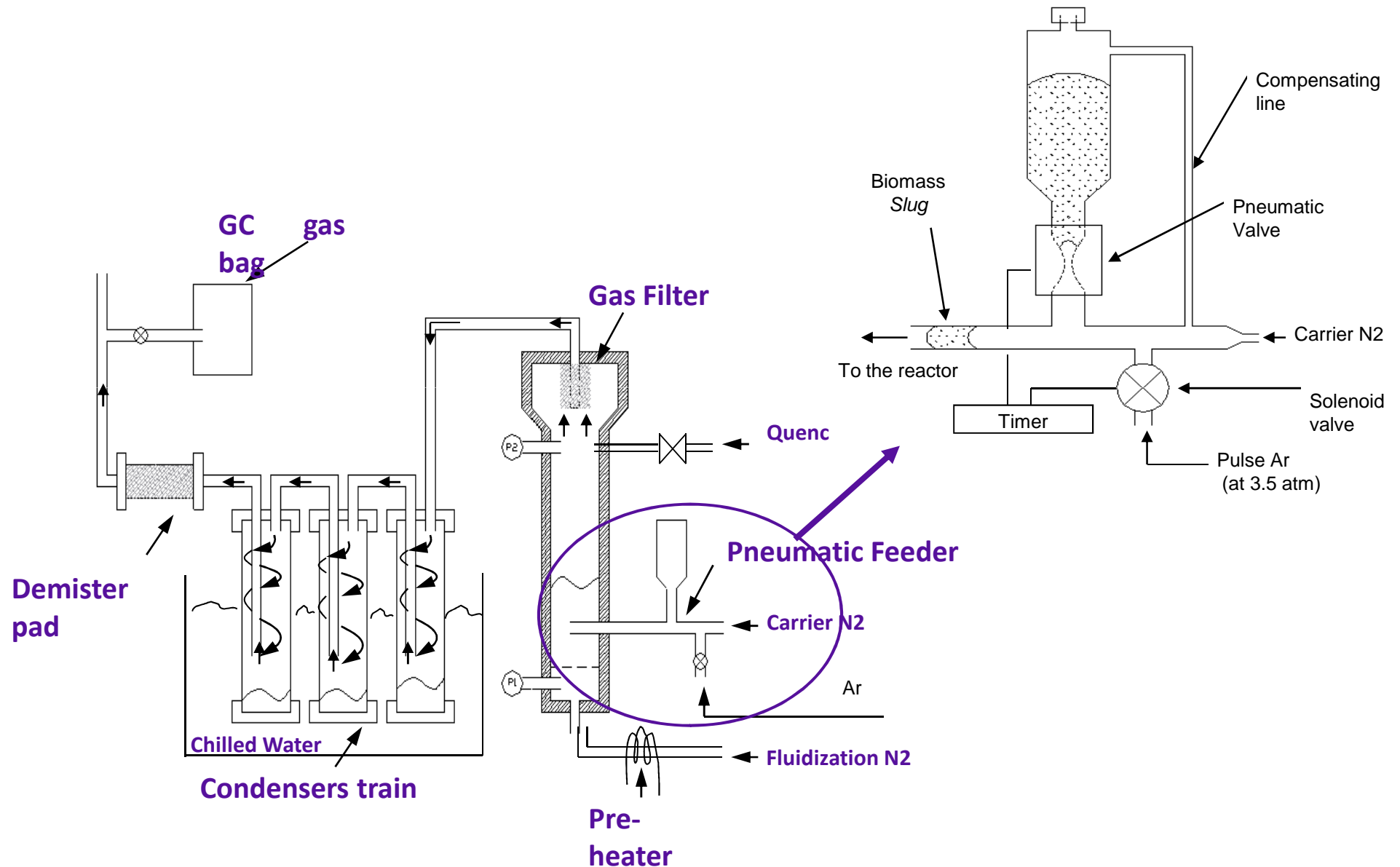
Experimental Set Up

ICFAR Pilot Plant



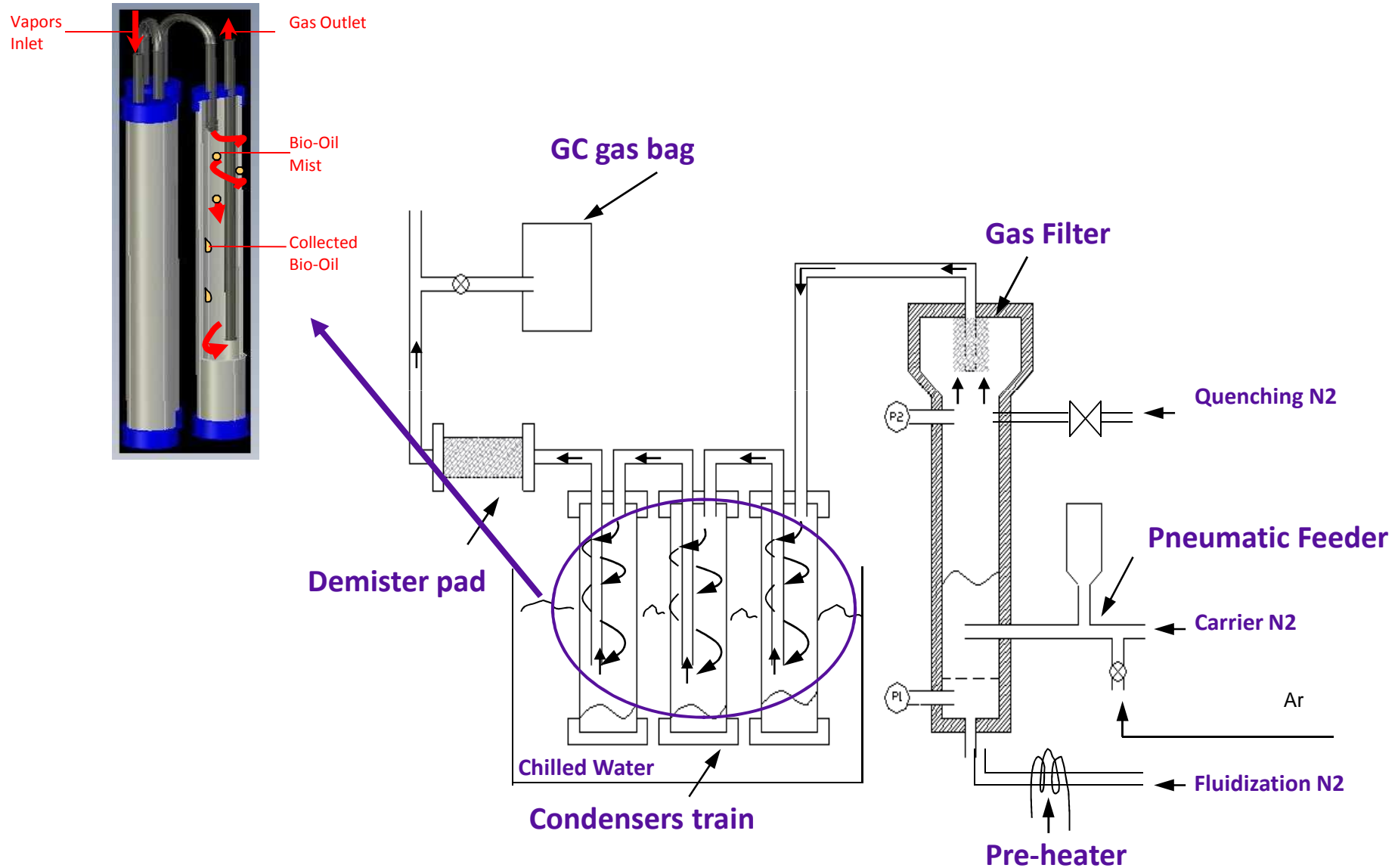
Experimental Set Up

ICFAR Pilot Plant



Experimental Set Up

ICFAR Pilot Plant



Outline

- Motivation
- Approach
- Experimental Set Up
- **Experimental Results**
 - Product Yields (Mass Balance)
 - Thermal Sustainability (Heat Balance)
 - Liquid Bio-Oil Product
- Conclusion

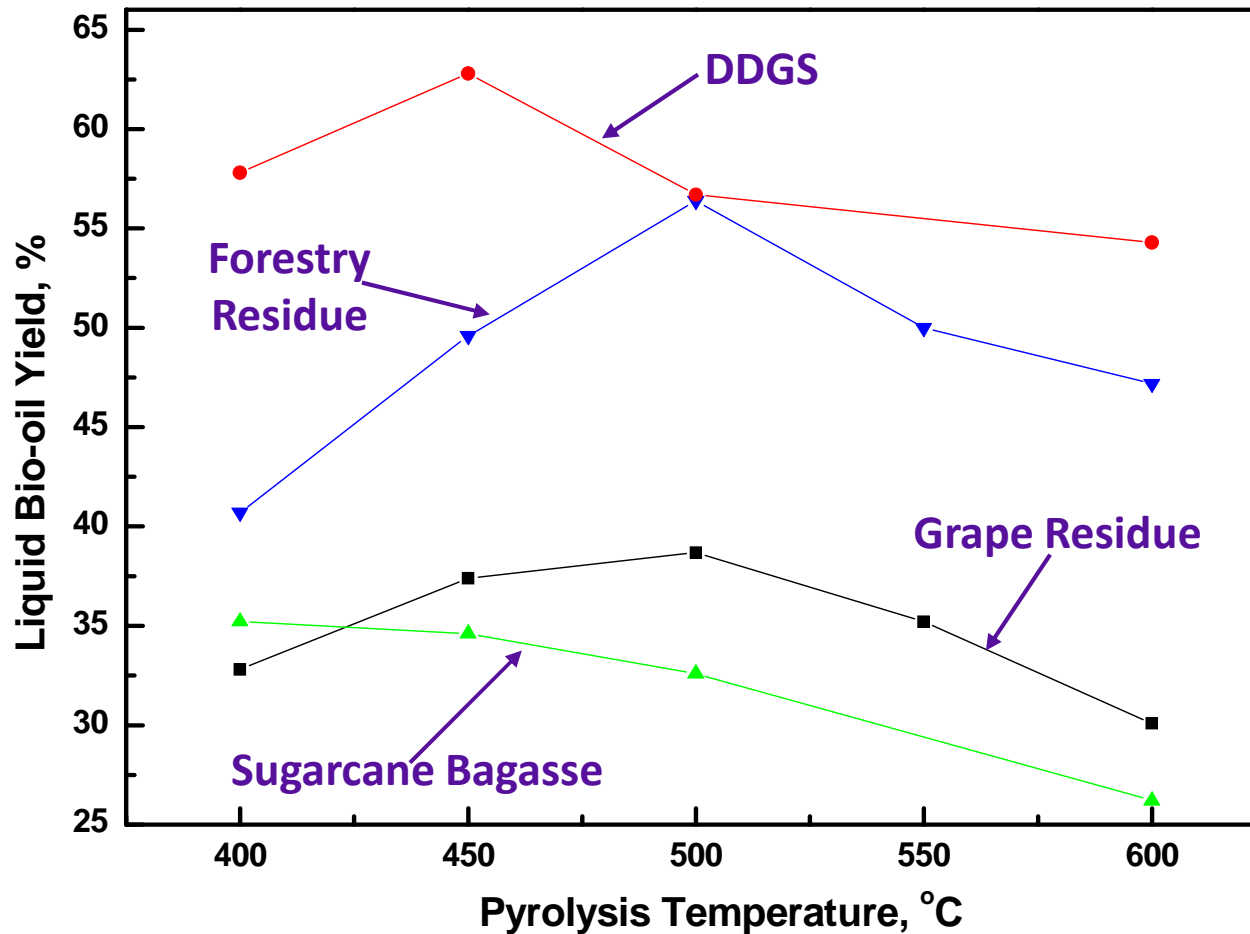


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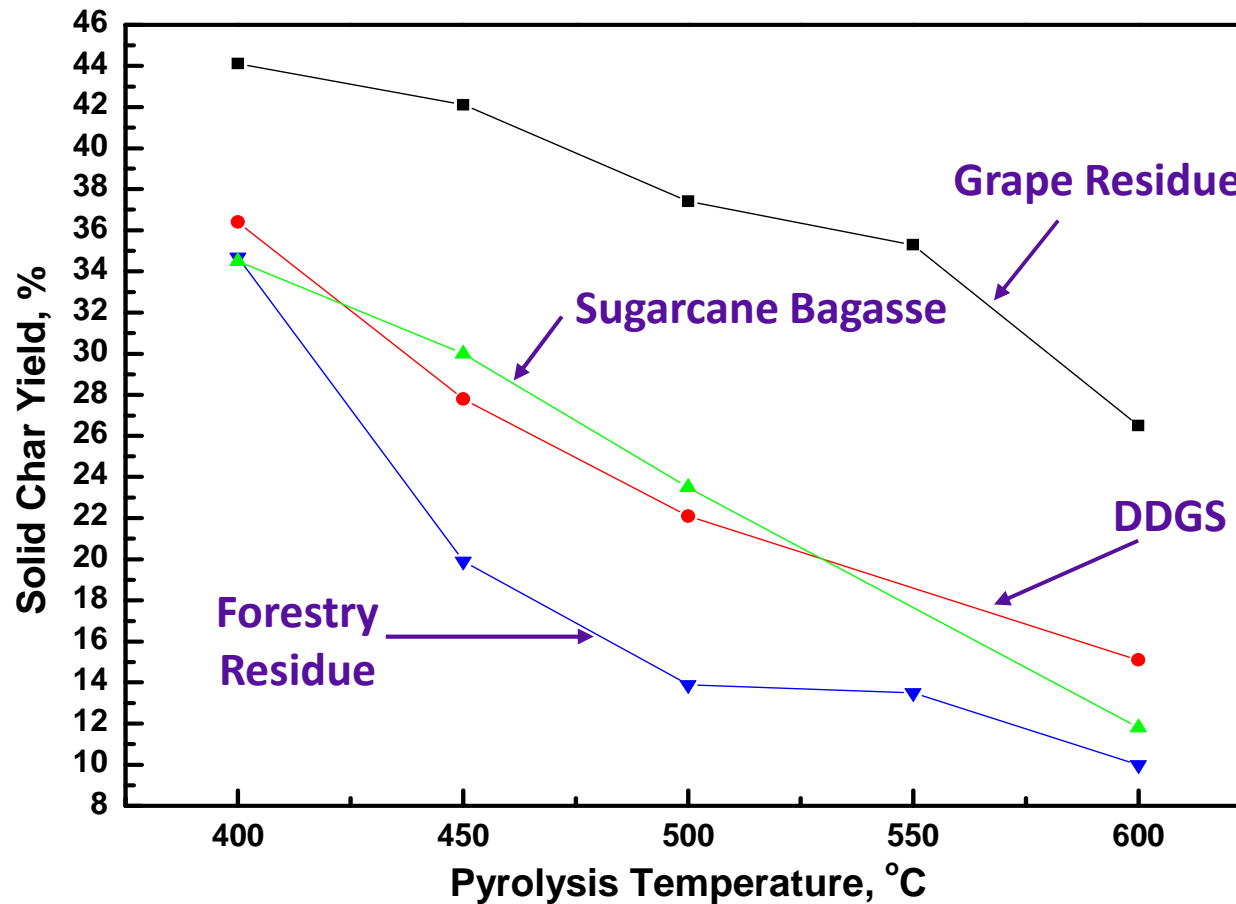


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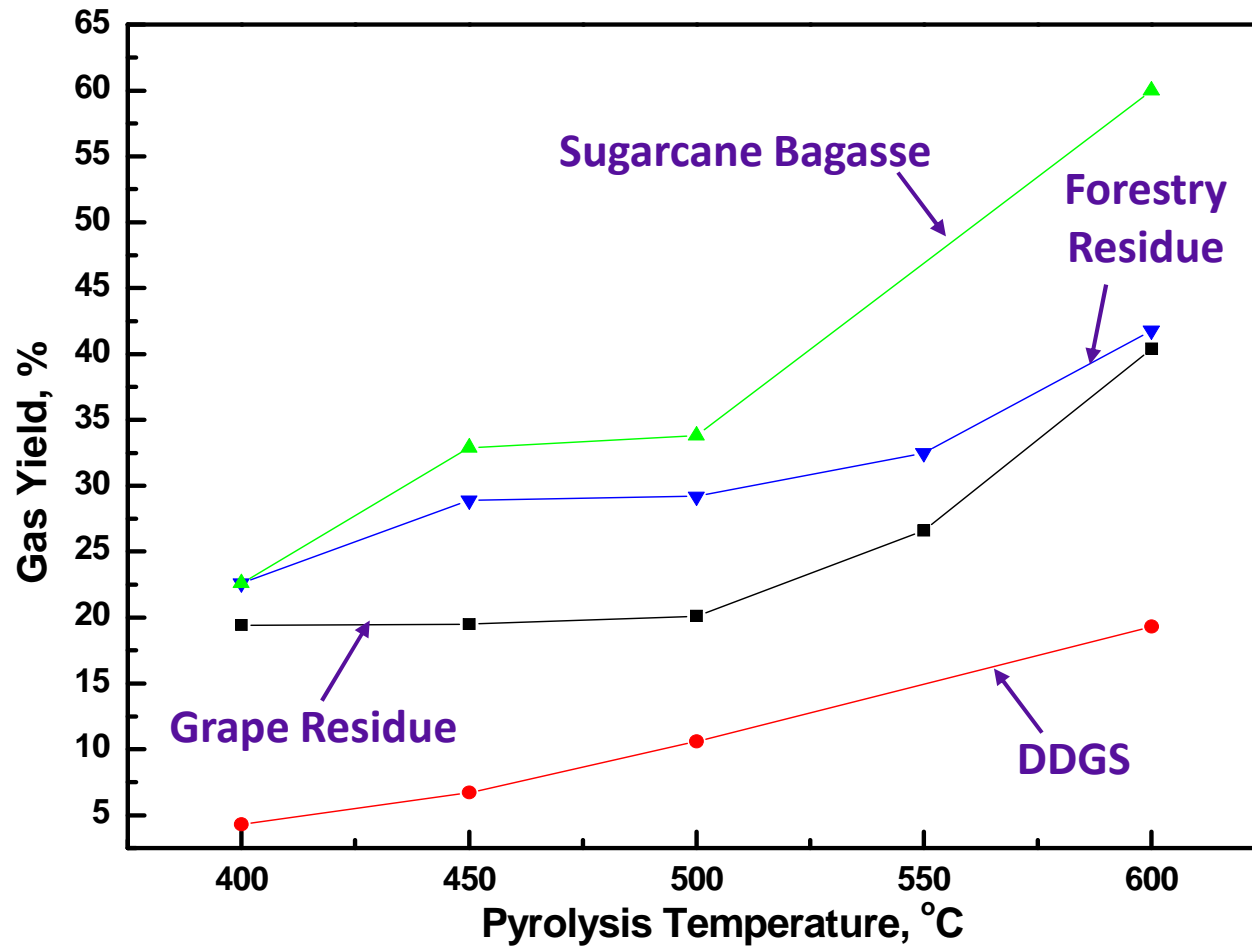
Liquid Bio-oil Yields of Different Biomass Resources
Residence Time: 5 seconds



Solid Biochar Yields of Different Biomass Resources Residence Time: 5 seconds



Gas Yields of Different Biomass Resources
Residence Time: 5 seconds



Heat Measurements

- Heat of Pyrolysis = Heaters Power consumption during the pyrolysis test - Power consumption before the start of the feed
- Lower Heating Value (LHV) of the Feedstocks and Liquids Products = Higher Heating Value (HHV) - Water vapor in the combustion gases
- Lower Heating Value (LHV) of the product gases estimated from the product gases composition and the lower calorific value of each gas.

Thermal Sustainability

Heat of Pyrolysis

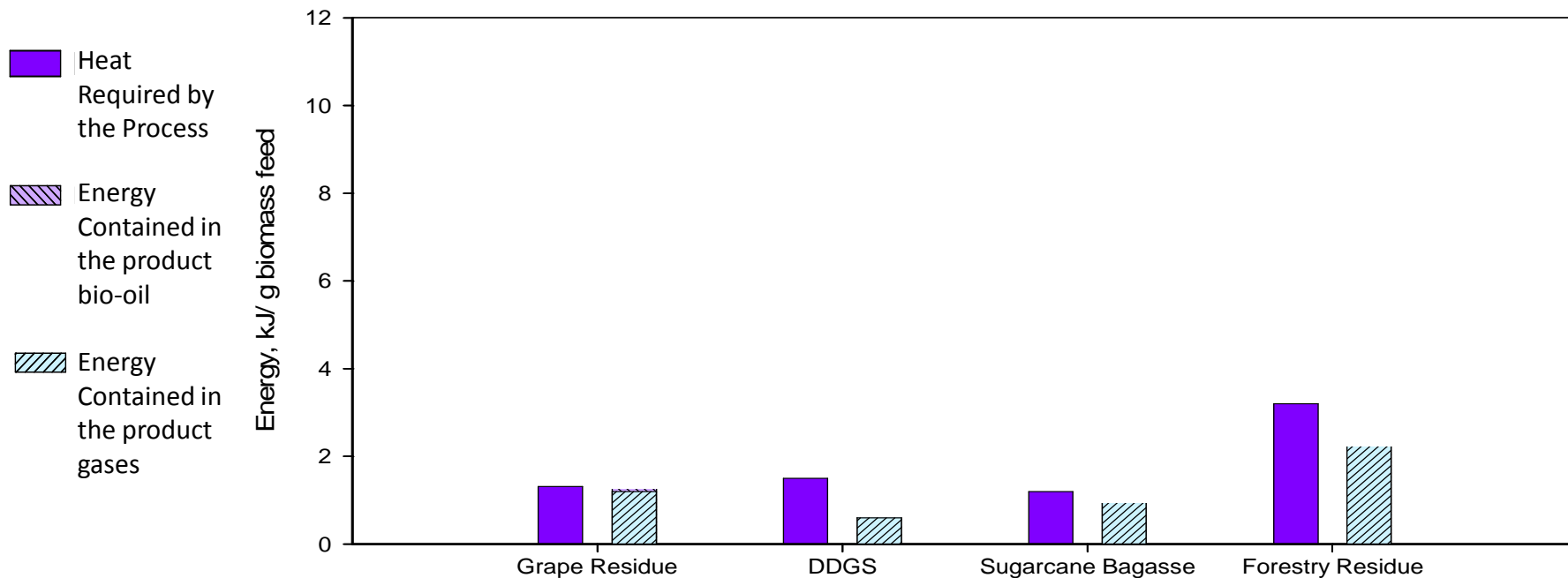
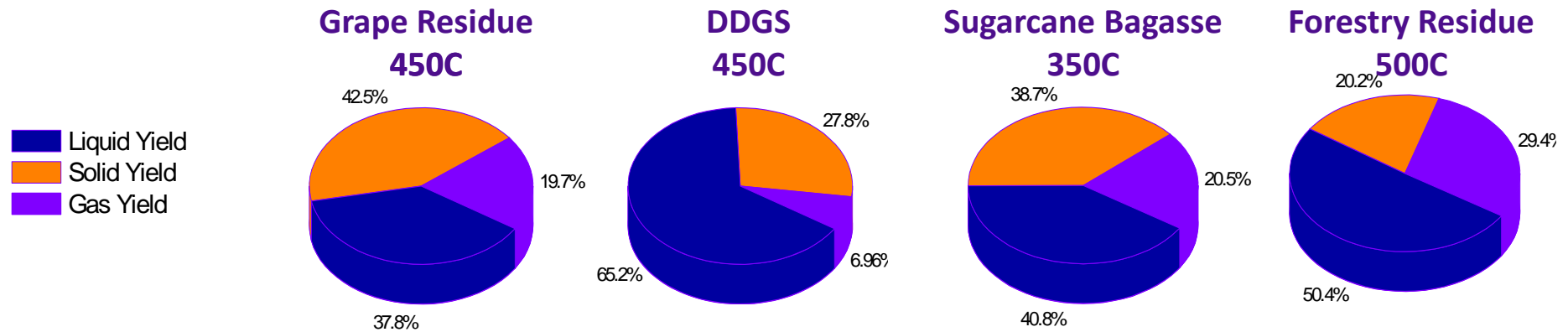
vs.

Product Gases LHV
Product Bio-oil LHV

Experimental Results

Thermal Sustainability (Heat Balance)

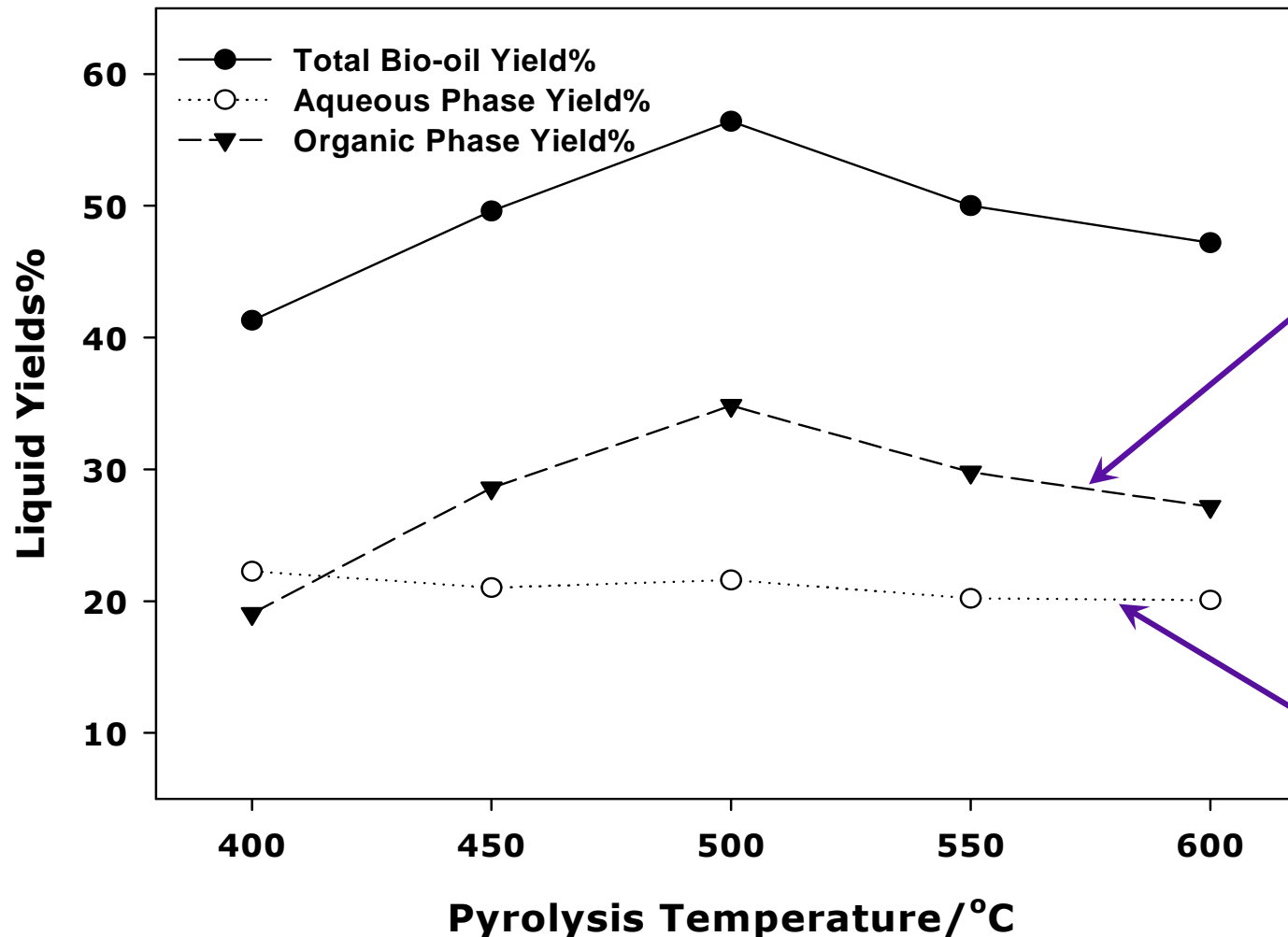
Pyrolysis at the Temperature for Maximum Liquid Yield, 5s Residence Time



Forestry Residue Bio-oil

Bio-oil Phase Separation

Forestry Residue Pyrolysis Liquid Biooil Aqueous Phase & Organic Phase Yields



Organic Phase



Aqueous Phase

Grape Residue Bio-oil

Aqueous Phase Environmental Analysis

- Environmental analysis has been conducted for the distilled aqueous phase (85 C to 115 C):

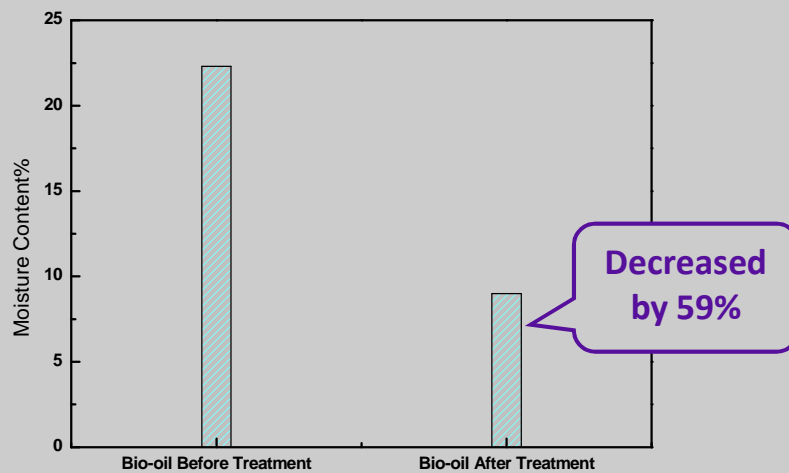
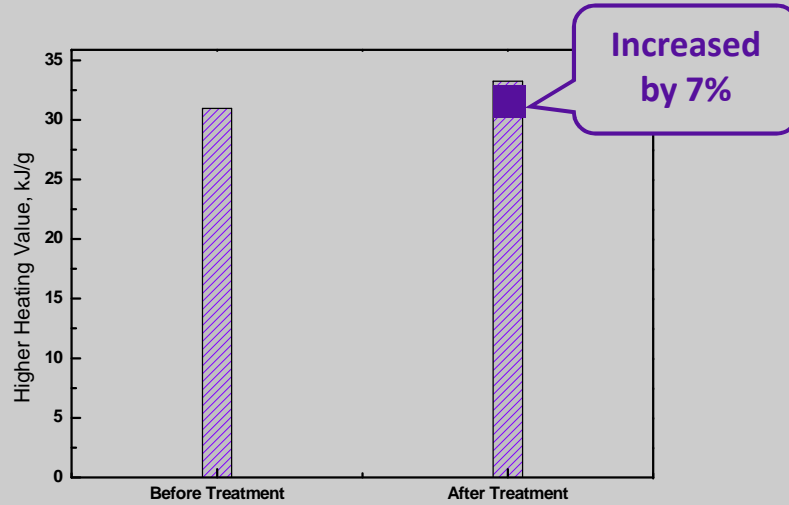
Total Ammonia-N, Total BOD, COD, TKN, TOC, Phenols-4AAP, etc.

- Comparison with "Sanitary and Combined Sewer Discharge by Law, Toronto, Canada" shows that the distilled aqueous phase needs to be treated before disposal to sewer.

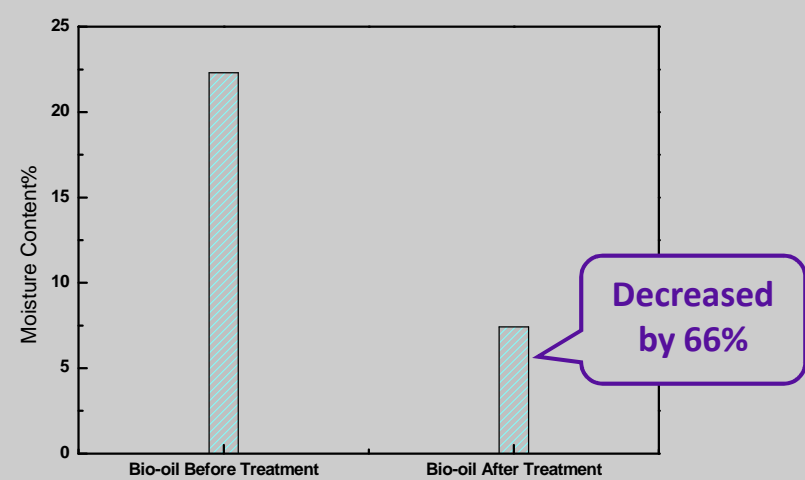
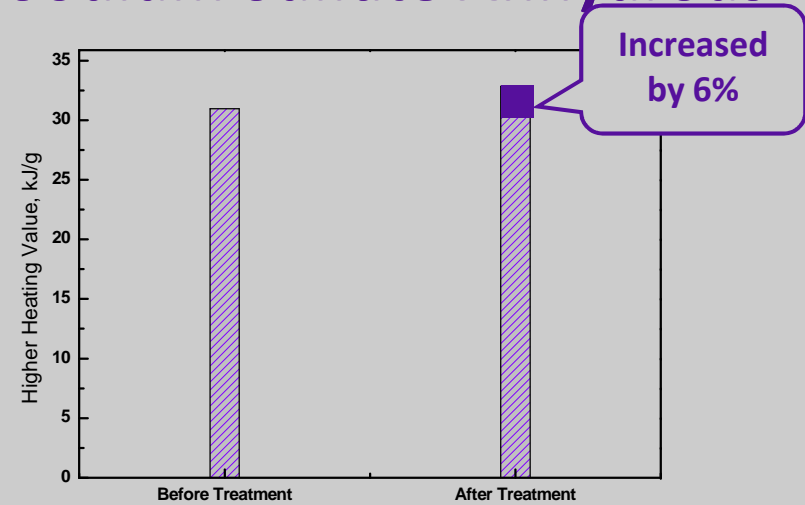
Dried Distiller's Grains Bio-oil

Organic Phase Drying Agents

Molecular Sieve 4A



Sodium Sulfate Anhydrous



Conclusions

For the product yields at 5 s residence time:

Maximum liquid yield at:

- 450 °C for grape residue and DDGS.
- 350 °C for sugarcane bagasse.
- 500 °C for forestry residue.

Thermal Sustainability : It can be achieved by burning all the gas products and part of the bio-oil

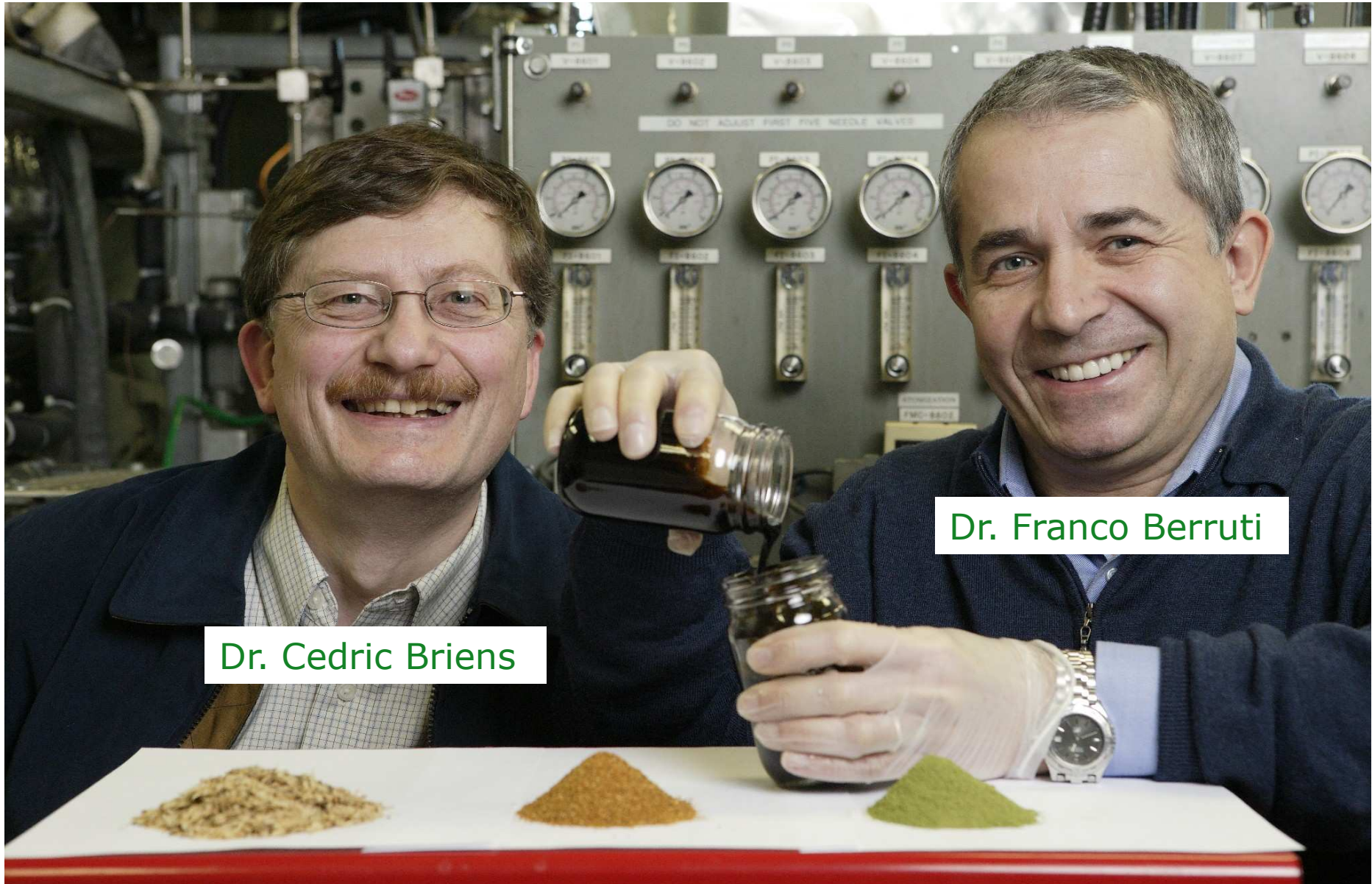
Phase separation of Bio-oil :

- The aqueous phase of grape bio-oil needs to be treated before disposal to sewer.
- The heating value of the organic phase of DDGS bio-oil can be enhanced through the use of drying agents.

Acknowledgements

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Our Team: Supervisors



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Our Team: Lab Pilot Plant Team



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WE ARE ICFAR!



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Questions?

Thank You!



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Grape Residue Bio-oil

Aqueous Phase Environmental Analysis

| | Units | Distilled Aqueous Phase Grape Bio-oil | Sanitary and combined sewer discharge by Law, Toronto, Ontario ^[1] | RDL |
|--|--------------------|---------------------------------------|---|-----|
| Calculated Parameters | | | | |
| Hardness (CaCO ₃) | mg L ₋₁ | 11 | | 1 |
| Inorganic | | | | |
| Total Ammonia-N | mg L ₋₁ | 10000 # | <50 | 300 |
| Total BOD | mg L ₋₁ | 3400 | <300 | 2 |
| Total Chemical Oxygen Demand (COD) | mg L ₋₁ | 21000 | <500 | 800 |
| Conductivity | Umho/cm | 29100 | | 2 |
| Total Kjeldahl Nitrogen (TKN) | mg L ₋₁ | 10000 # | <100 | 400 |
| Total Organic Carbon (TOC) | mg L ₋₁ | 7010 | <500 | 5 |
| pH | pH | 9.5 | 6~10.5 | |
| Phenols-4AAP | mg L ₋₁ | 1080 | <1.0 | 250 |
| Total Phosphorus | mg L ₋₁ | ND * | <10 | 1 |
| Total Suspended Solids | mg L ₋₁ | 36 | <350 | 10 |
| Volatile Suspended Solids | mg L ₋₁ | 36 | <350 | 10 |
| Alkalinity (Total as CaCO ₃) | mg L ₋₁ | 32700 | <250 | 10 |
| Nitrite (N) | mg L ₋₁ | ND | | 1 |
| Nitrate (N) | mg L ₋₁ | ND | | 10 |
| Nitrate + Nitrite | mg L ₋₁ | ND | | 10 |
| Petroleum Hydrocarbons | | | | |
| Total Oil & Grease | mg L ₋₁ | 1 | <150 | 1 |