

### In silico analysis for the production of higher carbon alcohols using Saccharomyces cerevisiae

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# Outline

- Higher carbon alcohols
- Integrated Bioprocess Development
- Genome Scale Metabolic Models and Constraint Based Analysis
- Butanol Case Study
- Results



### **Higher Carbon Alcohols**

- Alcohols with 4 or more carbon atoms
- Higher energy content and lower hygroscopicity and vapor pressure make them a better fuel additive
- Applications in food and flavor industries
- Applications as solvent and feedstock in industries

#### **Fuel additives**



#### **Flavor compounds**



#### Feedstock / Solvent for Industry







### Production of higher carbon alcohols

- Microbial bioprocesses for the production of higher carbon alcohols
  - Advantages
    - Utilization of renewable resources
    - Environment friendly operation
    - Suitable for Large Scale production
  - Disadvantages
    - Lower yields
    - Toxicity of alcohols to microorganisms
- Bioprocess development
  - Conventional vs. Integrated processes



### **Bioprocess Development Workflow**



CFS

#### **Systems Approach for Integrated Bioprocess Development**



### Genome Scale Metabolic Models

### Genome Scale Metabolic Reconstruction (GENRE)

- Genotype  $\rightarrow$  Phenotype
- Biochemically and genetically structured, highly curated compilation of primary biological information.
- Integration of high-throughput omic and Bibliomic data with small scale detailed experiments

### Genome Scale Metabolic Model

- GENRE can be converted to a mathematical model by the application of biological and physico-chemical constraints
- Application of computational methods to assess phenotypic characteristics.





# Case Study – Butanol Production

- Selection of microorganism
- Selection of metabolic pathways
  - Fermentative Vs Non-fermentative Pathways
- In silico flux balance analysis (FBA)
  - Tradeoff between growth and product formation
  - Yield of butanol from hexose and pentose sugars
  - In silico gene manipulation studies
    - Gene Deletion
    - Gene Insertion
  - Dynamic FBA



# Criteria for the selection of microorganisms

- Micro-organism Selection
  - Yield and Productivity
  - Suitability for Industrial Conditions
  - Ease of genetic manipulation/availability of tools

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|--------------------|-----------|----------|-----------|----------|-----------|-----------|-----------|----------------|--------|-------------|-----------------------|----------|
| Organism           | Natur     | al sugar | utilizati | on pathy | ways      | Major p   | oroducts  | Tolerance      |        |             | O <sub>2</sub> needed | pH range |
|                    | Glu       | Man      | Gal       | Xyl      | Ara       | EtOH      | Others    | Alcohols       | Acids  | Hydrolysate |                       |          |
| Anaerobic bacteria | +         | +        | +         | +        | +         | +         | +         | -              | -      | -           | -                     | Neutral  |
| E. coli            | +         | +        | +         | +        | +         | -         | +         | -              | -      | -           | -                     | Neutral  |
| Z. mobilis         | +         | -        | -         | -        | -         | +         | -         | +              | -      | -           | -                     | Neutral  |
| S. cerevisiae      | +         | +        | +         |          | -         | +         | -         | ++             | **     | ++          | -                     | Acidic   |
| P. stipitis        | +         | +        | +         | +        | +         | +         | -         | -              | -      | -           | +                     | Acidic   |
| Filamentous fungi  | +         | +        | +         | +        | +         | +         | -         | ++             | ++     | ++          | -                     | Acidic   |

Pros and cons of various natural microorganisms with regard to industrial ethanol production

Hahn- Hagerdal et al.( 2007)Towards industrial pentose-fermenting yeast strains, Appl. Microb. Biotechnol. 74, 937-953



### Genome Scale Metabolic Model

#### Saccharomyces cerevisiae iND750

- 750 genes, 1149 reactions
- All the reactions are both elementally and charge balanced
- 8 Compartments
  - [c] : cytosol
  - [g] : Golgi apparatus
  - [n] : nucleus
  - [v] : vacoule

- [e] : extracellular
- [m]: mitochondrion
- [r] : endoplasmic reticulum
- [x] : peroxisome
- Current Model contains 750 genes,1266 reactions and 1061 metabolites



### **Pathways for Pentose Sugar Utilization**



Hagerdal et al., 2007, Appl Microbiol Biotechnol, 74: 937-953

### Pathways for butanol production

#### **Clostridia - Fermentative Pathway Ehrlich Pathway – Non Fermentative** GLU COSE Amino Transamination EMP Pathway acid ARO8 2-oxoglutarate PYRUVATE ARO9 BAT2/TWT2 BATI/TWT1 glutamate ACETATE +----- ACETYL-CoA ----+ ETHANOL a-keto acid ARO10 ACETYL-CoA Decarboxylation THL (thiL) CoASH PDC1 PDC5 CO. ACETOACETYL-CoA PDC6 NADH+H\* HBD (hbd) 'fusel aldehyde' NAD\* Reduction Oxidation BHYDROXYBUTYRYL-CoA ADH1, ADH2, ALD1 ADH3, ADH4, GRT (art) ALD2 NADH, H<sup>+</sup> NAD<sup>+</sup> +H,0 ADH5, ADH6, ALD3 SFAL, AAD3. CROTONYL-CoA ALD4 NAD+ 4 NADH. H\* AAD4, AAD6, ALD5 AAD10, AAD14, NADH+H\* BCD (bcd. etfA, etfB) ALD6 AADIS, AADI6. •NAD\* YCR105W. BUTYRATE +----- BUTYRYL-CoA YPL088W NADH+H\* 'fusel acid' in 'fusel alcohol' BYDH (adhe1 or adhe) NAD\* CoASH Export ATP BUTYRALDEHYDE PDR12 ADP NADH+H\* BDH (adhe1 or adhe) NAD\* 'fusel acid' out BUTANOL CFS A \* S T A R

# **Butanol Yield- Hexose and Pentose Sugars**

| Wild Type I                                   | Model iND750                  |                        |                      |   |  |  |  |  |
|---|-------------------------------|------------------------|----------------------|---|--|--|--|--|
| Substrate                                     | Growth rate (h <sup>-1)</sup> | Uptake rate<br>mmol/gh | Butanol Yield<br>g/g | Max Yield g/g<br>(Max Theo. Yield<br>0.411 g/g) |  |  |  |  |
| Glucose                                       | 0.0858                        | -5                     | 0.0168               | 0.185   |  |  |  |  |
| iND750 + F                                    | ungal Xylose                  | Utilization Pa         | thway                |   |  |  |  |  |
| Xylose  | 0.0712                        | -5                     | 0                    | 0.181   |  |  |  |  |
| iND750 + Bacterial Xylose Utilization Pathway |                               |                        |                      |   |  |  |  |  |
| Xylose  | 0.0699                        | -5                     | 0.0137               | 0.181   |  |  |  |  |
| iND750 + B                                    | acterial Arabi                | nose Utilizati         | on Pathway           |   |  |  |  |  |
| Arabinose                                     | 0.0699                        | -5                     | 0.0137               | 0.181   |  |  |  |  |
| iND750 + F                                    | ungal Arabino                 | se Utilization         | Pathway              |   |  |  |  |  |
| Arabinose                                     | 0.0802                        | -5                     | 0                    | 0.181   |  |  |  |  |
|   |                               |                        |                      |   |  |  |  |  |

### Growth vs. Product Formation



# Gene Knockout and Insertion Studies

- Manipulation of cellular metabolism is essential for enhancing the product formation
- Identification of gene targets
- Gene Deletion
  - Double and Triple Gene Knockouts were calculated based on a reduced set of initial genes (which excludes essential genes and genes associated with blocked reactions)
- Gene Insertion
  - Single gene insertion analysis was carried out based on a assembled set of candidate reactions from the KEGG database



#### Gene Deletion studies – Triple Gene Deletion



### Insertion studies - Single reaction Insertion



### Insertion studies – Single reaction Insertion



### Dynamic Flux Balance Analysis

- The mathematical model for the process is coupled to the detailed stoichiometric description of cellular metabolism (FBA model)
- The combined model can be used to identify metabolic bottlenecks and gene targets to be manipulated for enhancing the yield
- Additional constraints can be applied to this model to enable integrated strain and process development.

### Dynamic Simulation (Dynamic FBA)



# Summary

- Systems approach based on genome scale metabolic modeling and analysis has been proposed for Integrated bioprocess development.
- The utility of genome scale metabolic modeling and analysis is demonstrated using the case study for the production of butanol using *Saccharomyces cerevisiae* 
  - The metabolic bottlenecks for the production of butanol has been identified by in silico metabolic flux analysis
  - Gene targets to be manipulated for enhancing the yield of butanol has been identified based on gene knockout and gene insertion studies
  - The utility of FBA coupled with dynamic simulation for process development is demonstrated.



## Thank you for the attention...

