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Novel Ni-based catalysts for the hydrotreatment of fast pyrolysis oil

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Novel Ni-based catalysts for the hydrotreatment of fast pyrolysis oil

Agnes Ardiyanti, Arjan Kloekhorst, Y. Wang , Erik Heeres (University of Groningen)

S.A. Khromova, Vadim Yakovlev (BIC)

Robbie Venderbosch (BTG)



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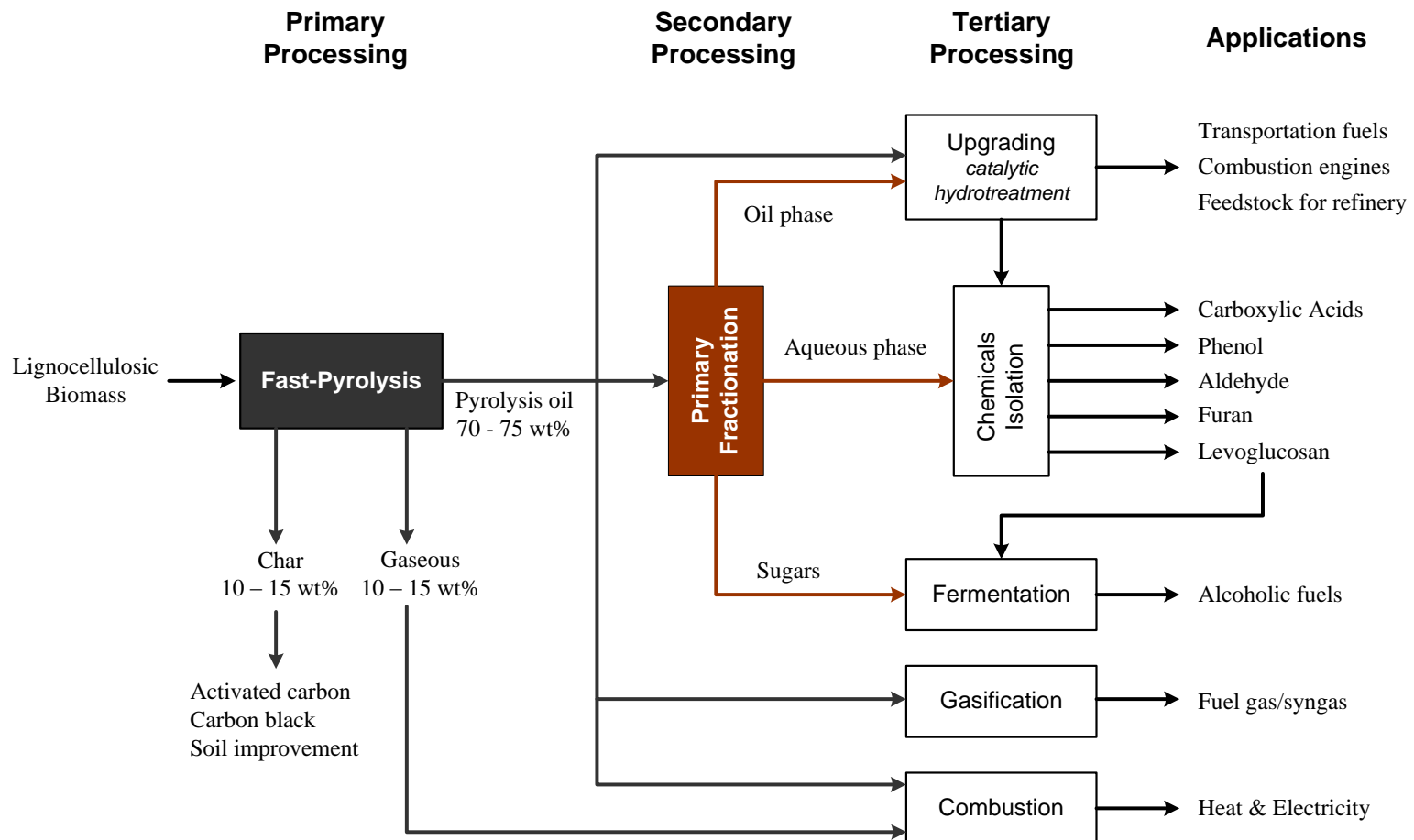
- > Results and discussion
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 - Process studies

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- > Acknowledgment

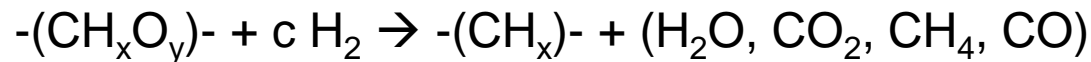
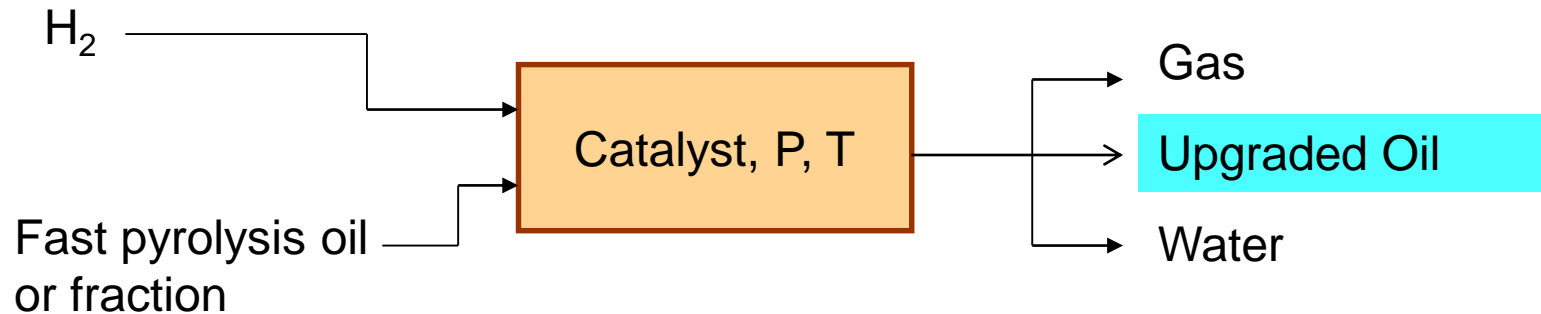


Pyrolysis 2.0: a biorefinery





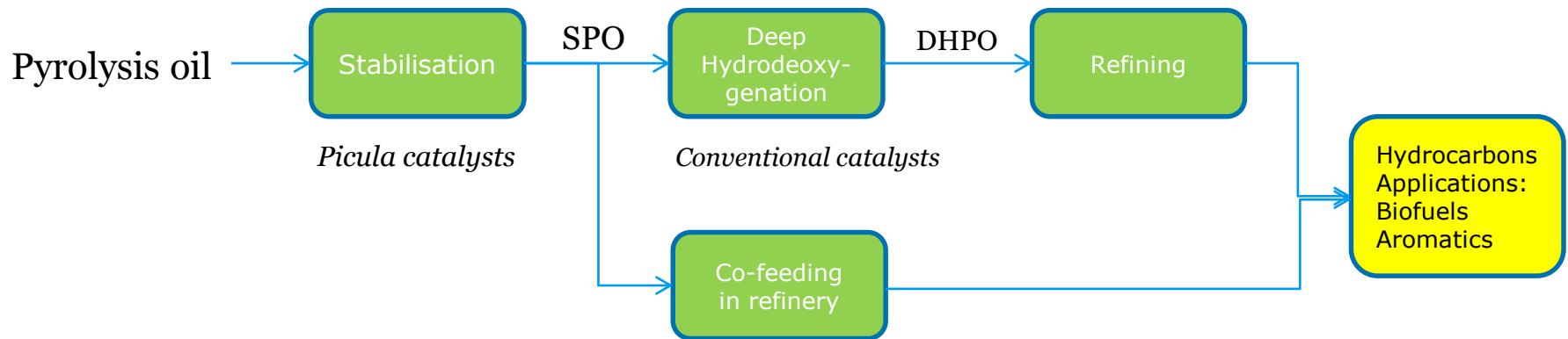
Catalytic hydrotreatment



Typical conditions: 125-400 C, 20-200 bar pressure



Two stage hydrotreatment





Objectives catalytic hydrotreatment

- > Process considerations:
 - Low hydrogen consumption
 - Active, stable and cheap catalysts

- > Product considerations
 - Reduced oxygen content, exact amount depending on product application
 - Low viscosity
 - Low water content
 - Low coking tendency (improved thermal stability)
 - Preferably miscible with hydrocarbons



Stabilisation: catalyst developments

- > Benchmark: Ru/C
- > Bimetallic noble metal catalysts^a
- > Ni-Cu catalyst on supports^{b,c}
- > Improved Ni-Cu catalysts (Picula)^d

- A.R. Ardiyanti, A. Gutierrez, M Honkela. O. Krause, H.J. Heeres, *Applied Catalysis A* 407(1-2) (2011) 56-66.
- A.R. Ardiyanti, S.A. Khromova, R.H. Venderbosch, V.A. Yakovlev, I.V. Melián-Cabrera, H.J. Heeres, *Applied Catalysis A* 449 (2012) 121-130.
- A.R. Ardiyanti, S.A. Khromova, R.H. Venderbosch, V.A. Yakovlev, H.J. Heeres, *Applied Catalysis B: Environmental* 117– 118 (2012) 105– 117.
- Venderbosch and Heeres; Chapter 17: Pyrolysis Oil Stabilisation by Catalytic Hydrotreatment, *Biofuel's Engineering Process Technology*, **Free download:** <http://www.intechopen.com>, Patent application pending

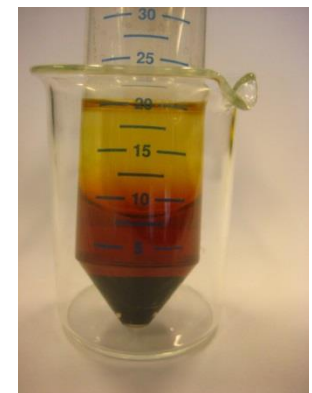
Picula catalysts

Table 2 Catalyst composition

Code	Active metal loading (wt%)	Support (wt%)
Picula Cat B	Ni 58.3 Pd 0.7	SiO ₂ 41
Picula Cat C	Ni 28.8 Cu 3.7	SiO ₂ 33.8 Kaolin 33.8
Picula Cat D	Ni 57.9 Cu 7	SiO ₂ 35.1
Picula Cat E	Ni 36.5 Cu 2.3	SiO ₂ 12.6 ZrO ₂ 37.2 La ₂ O ₃ 0.9

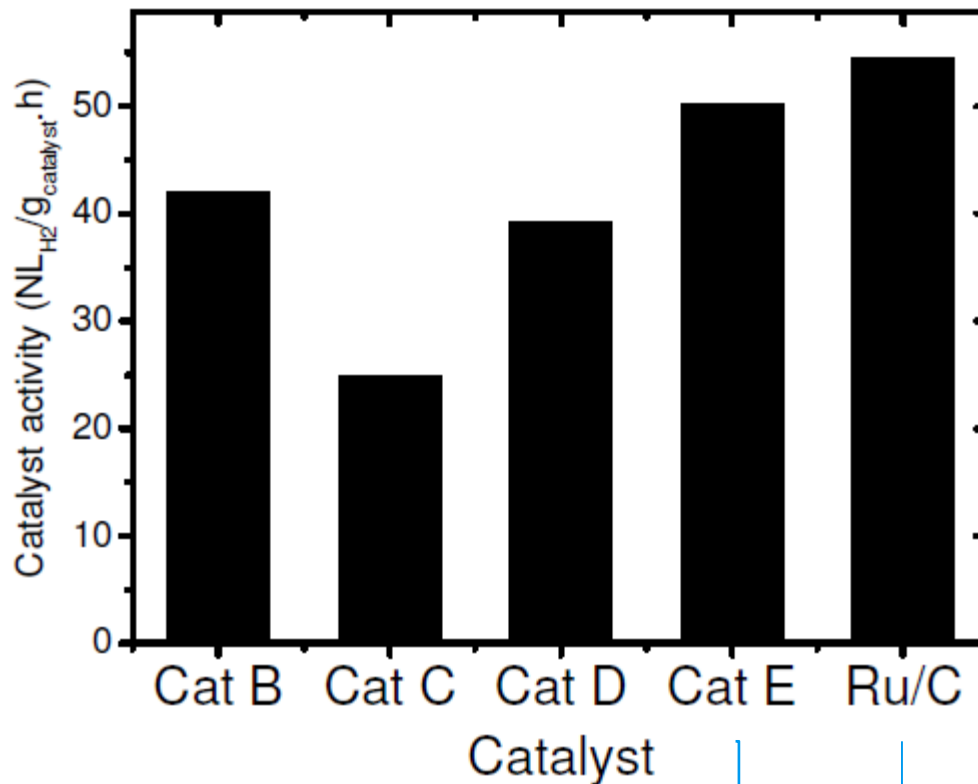
- High Ni content (29-58 wt%)
- Promoted with Cu, Pd
- Various supports

- Prepared by BIC





Batch studies

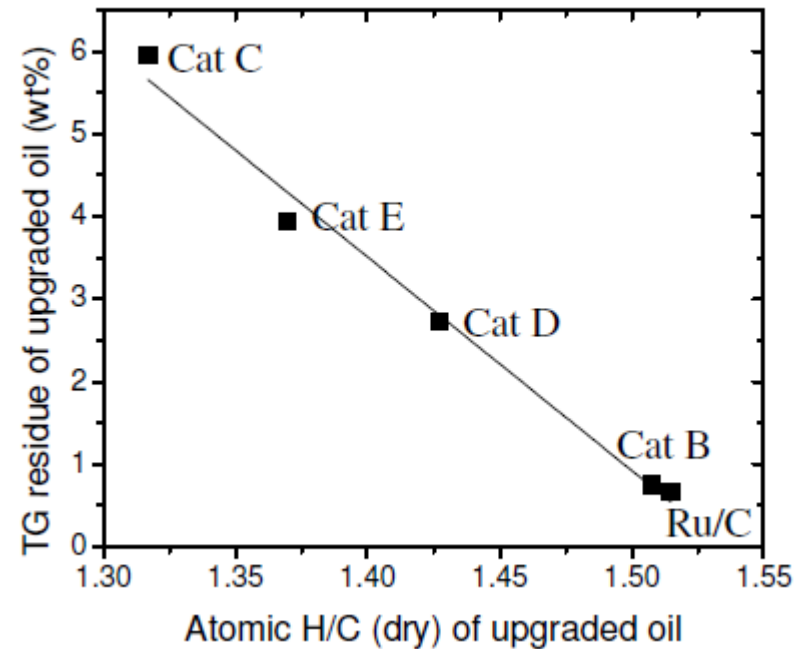
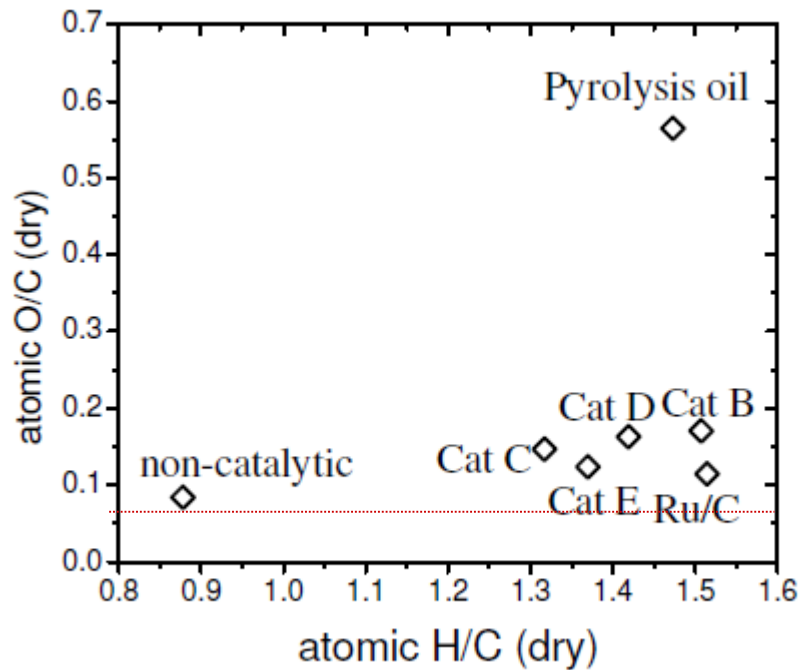


- 150 C, 1 h
- 350 C, 3 h
- 200 bar

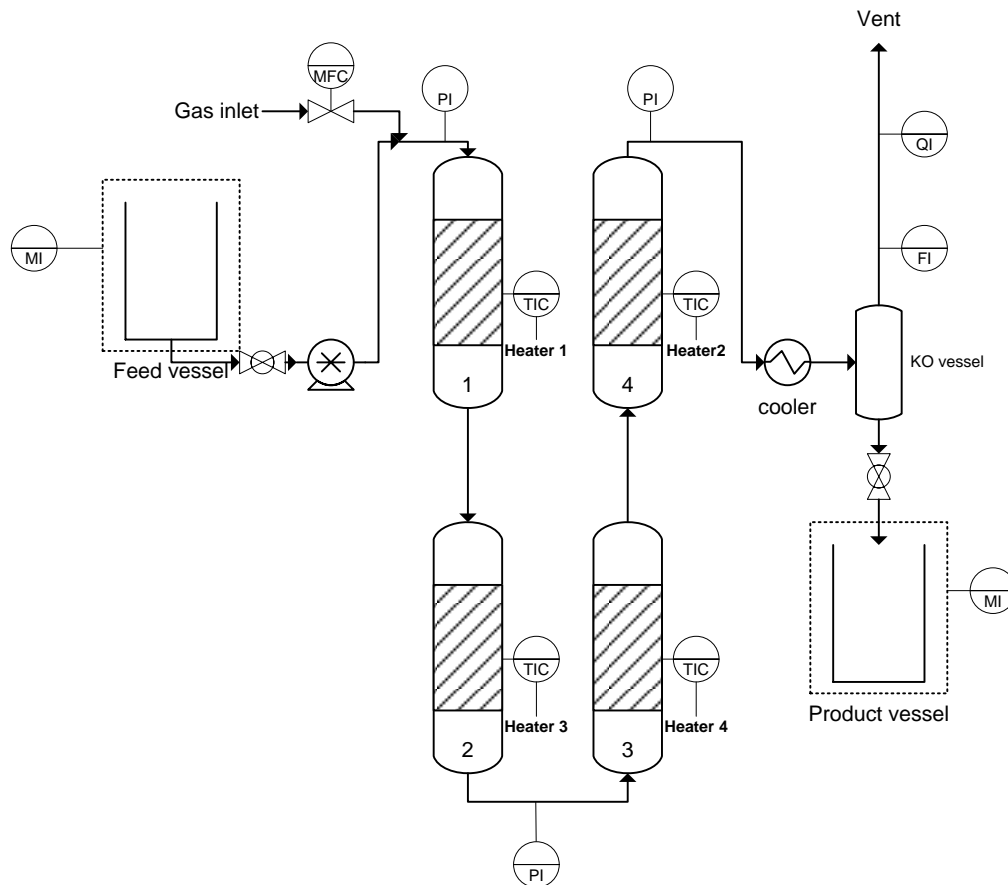
Methanation!



Batch studies



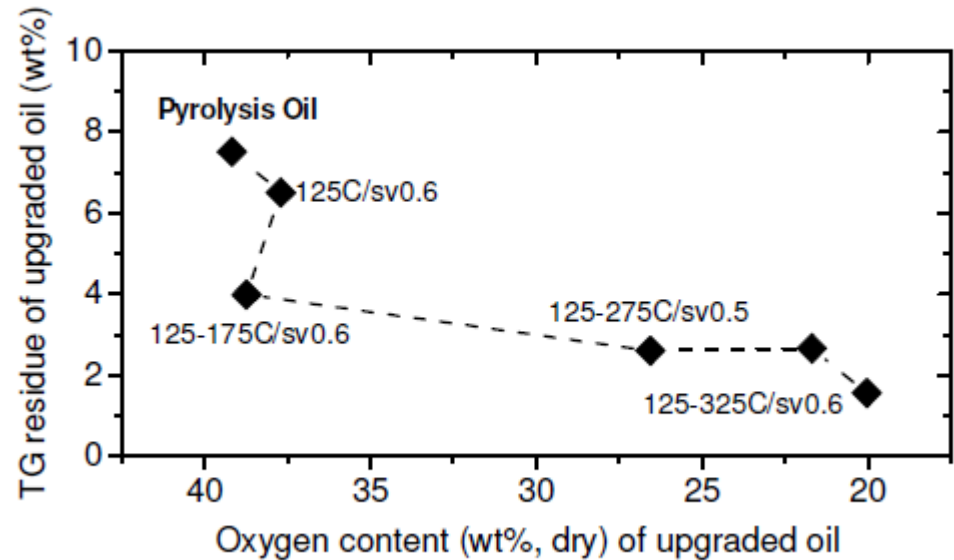
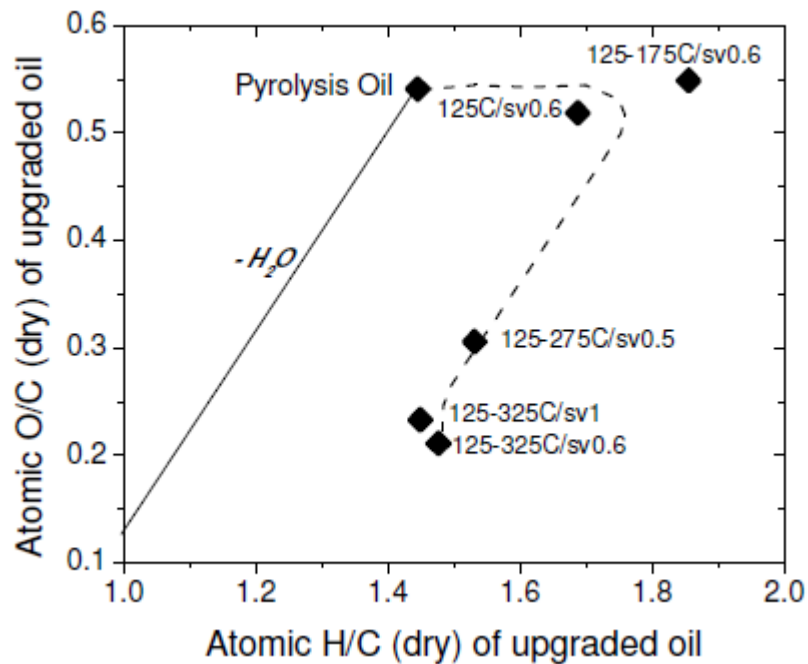
Continuous experiments



- > 4 fixed-bed reactors in-series
- > Catalyst: Picula catalyst D
- > H₂ pressure: 200 bar
- > WHSV = 0.6 – 1 h⁻¹
- > Variable: T
- > Analysis:
 - Elemental composition, TGA, GPC, TAN, CAN, 2D-GC



Continuous experiments





Visual appearance



Pyrolysis oil

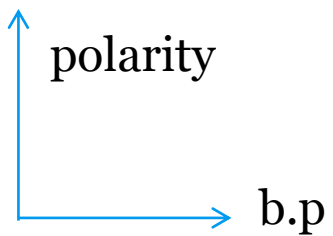
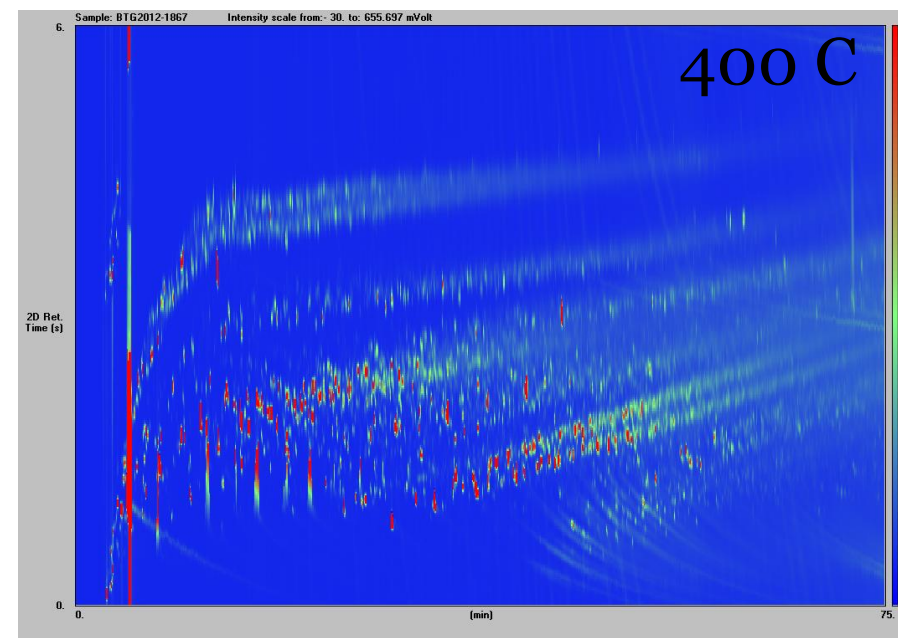
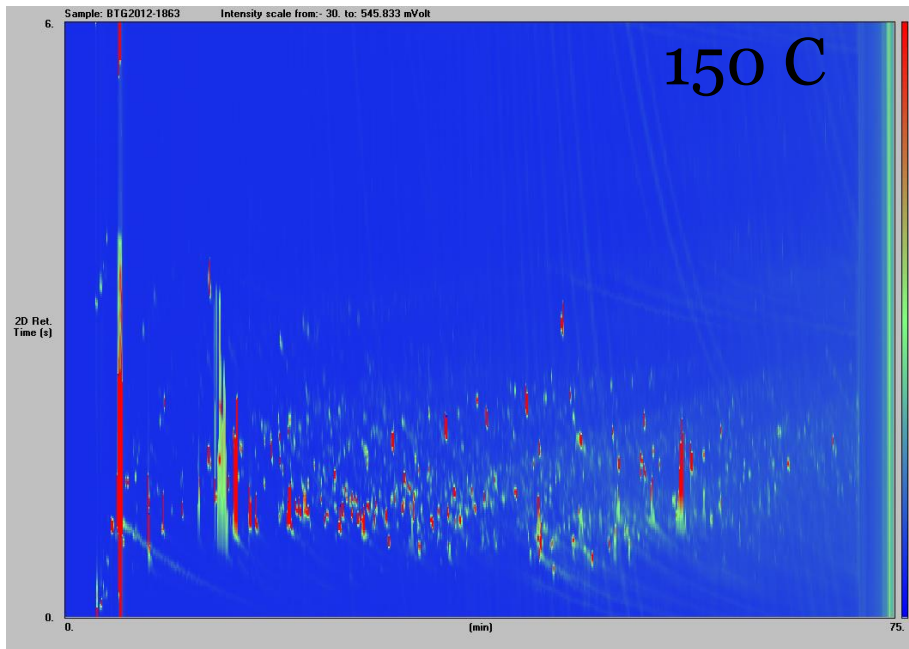
150°C

400 °C

distillates

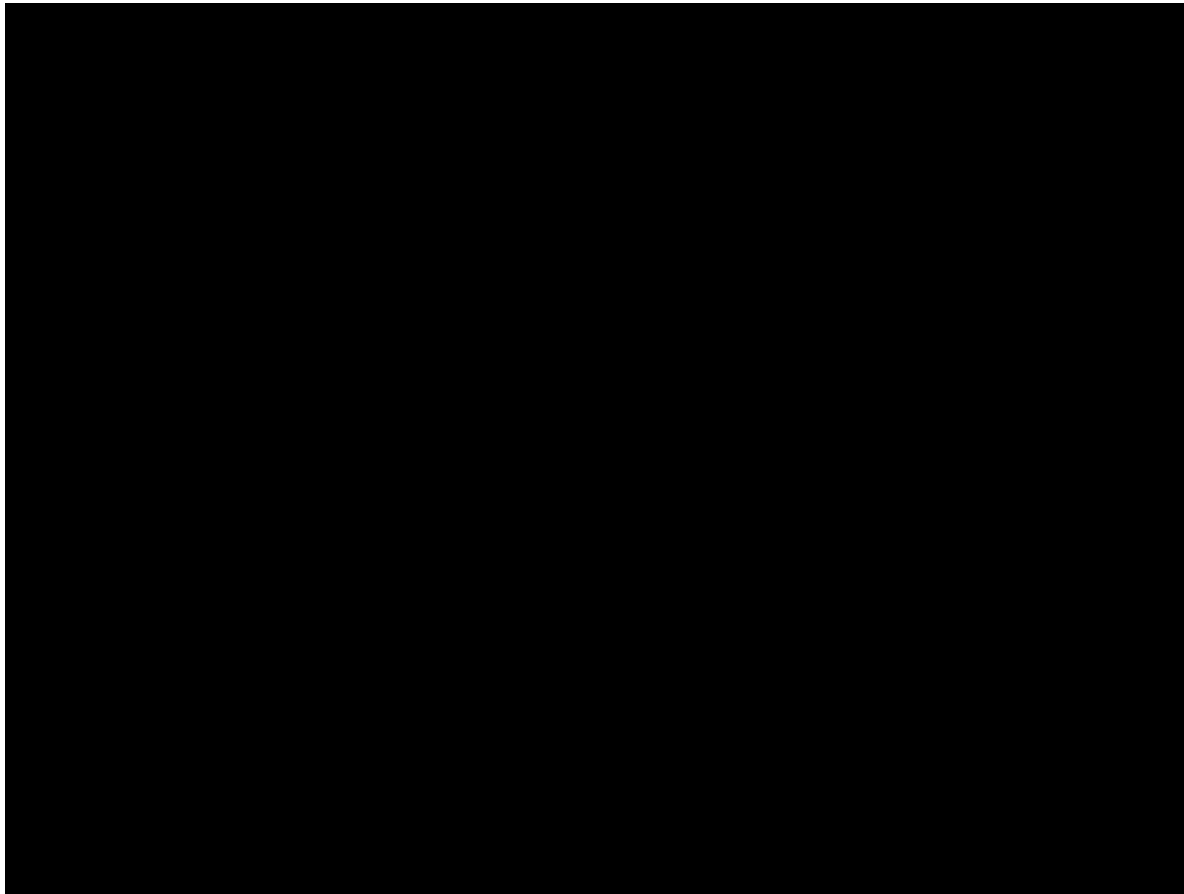


2D-GC



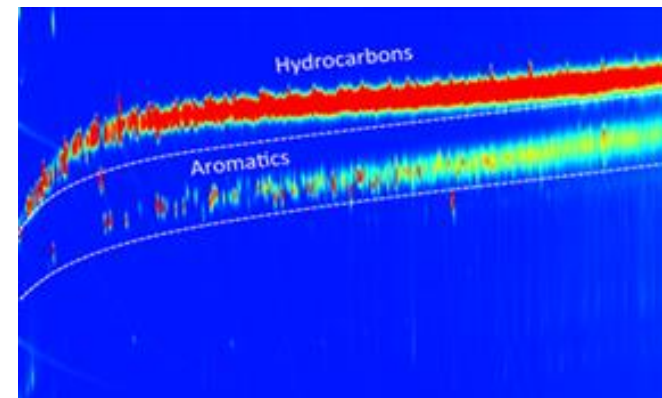
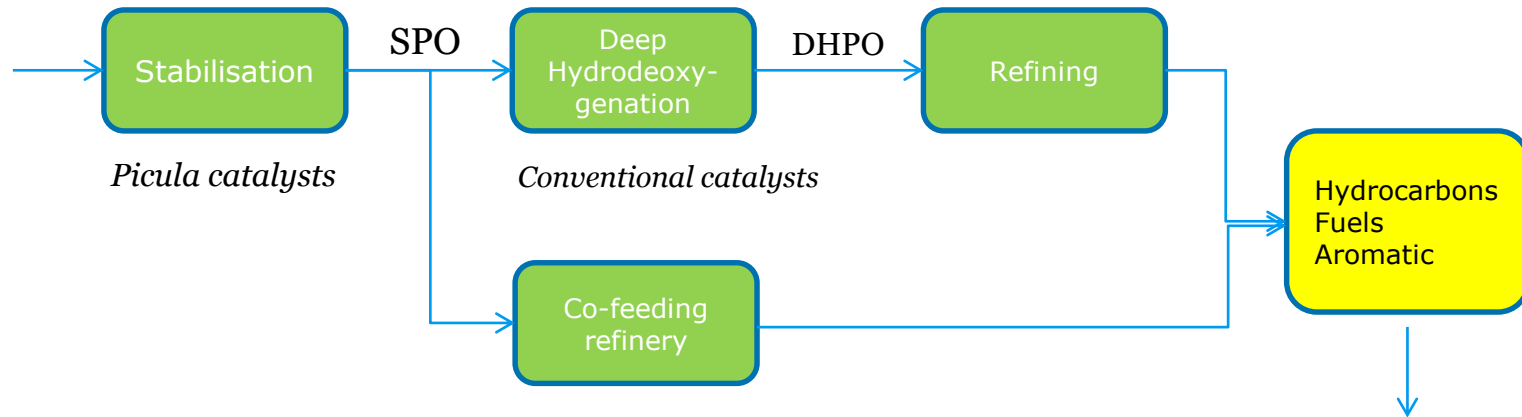


Product is distillable





Two stage hydrotreatment





Conclusions

- > Novel catalysts for pyrolysis oil stabilisation by catalytic hydrotreatment have been identified
- > Products are distillable, indicative for improved thermal stability
- > Picula catalysts show unique performance
 - Improved product properties at low processing temperature
 - Low hydrogen consumptions due to limited methane formation
 - Good hydrothermal stability (run times up to 400 h have been demonstrated)
- > Two stage hydrotreatment leads to deep deoxygenation and formation of hydrocarbons



Acknowledgement



Agentschap NL
 Ministerie van Economische Zaken





Vacancy

Tenure Track Assistant Professor Green Chemistry
and Technology (1,0 fte)

Deadline for applications: June 28, 2013

Contact: h.j.heeres@rug.nl

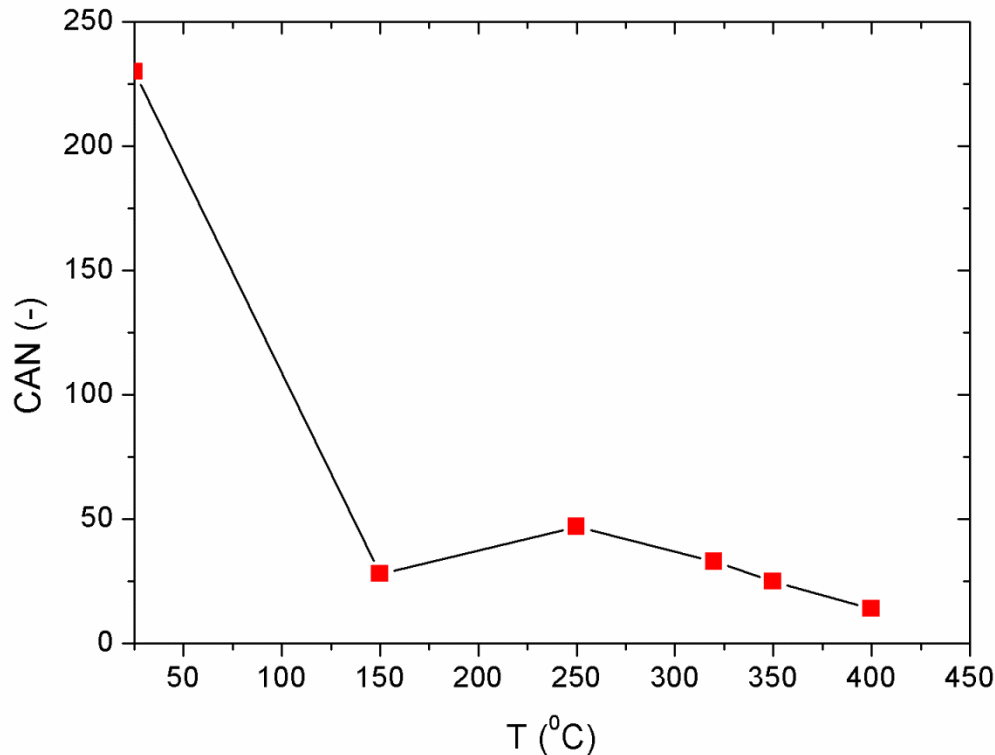


university of
 groningen

Date 25.06.2010 |



Carbonyl number

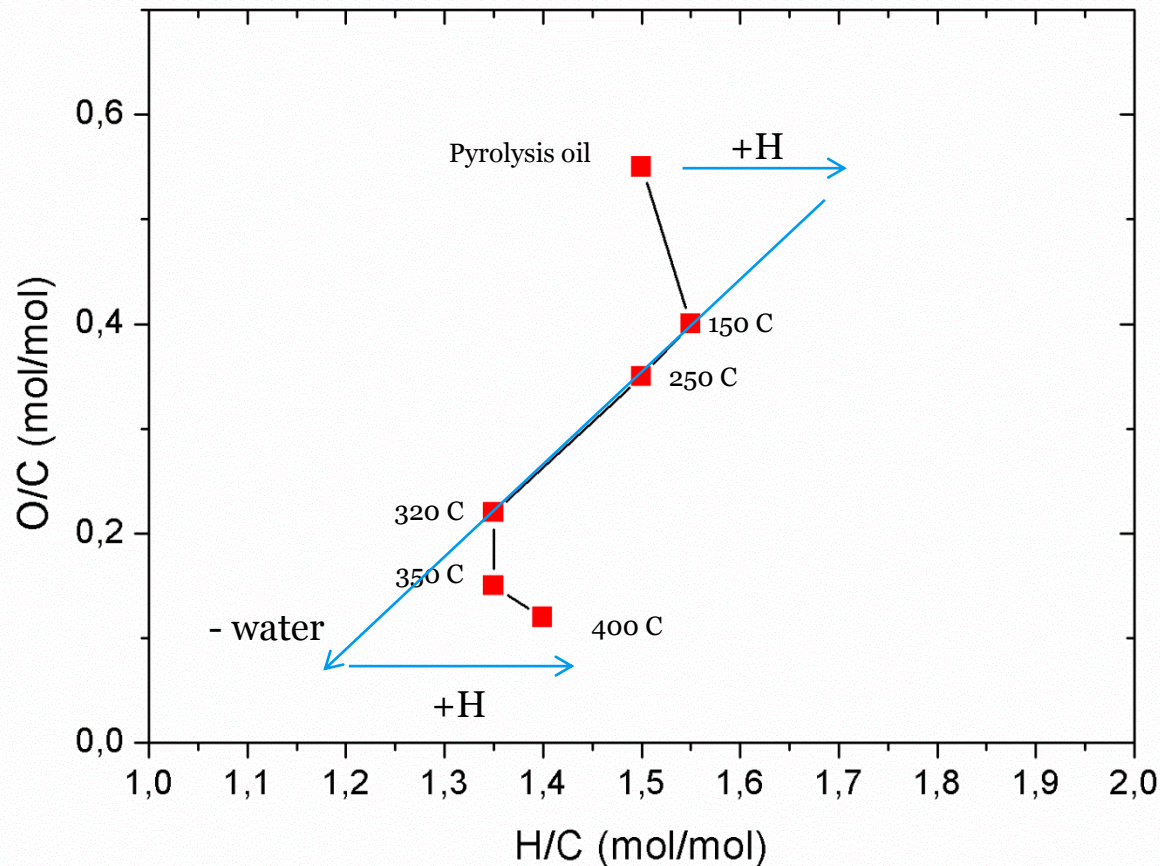


Aldehydes and ketones
 are very reactive at low
 temperature

Formation of new
 compounds at about
 250 °C



Elemental composition

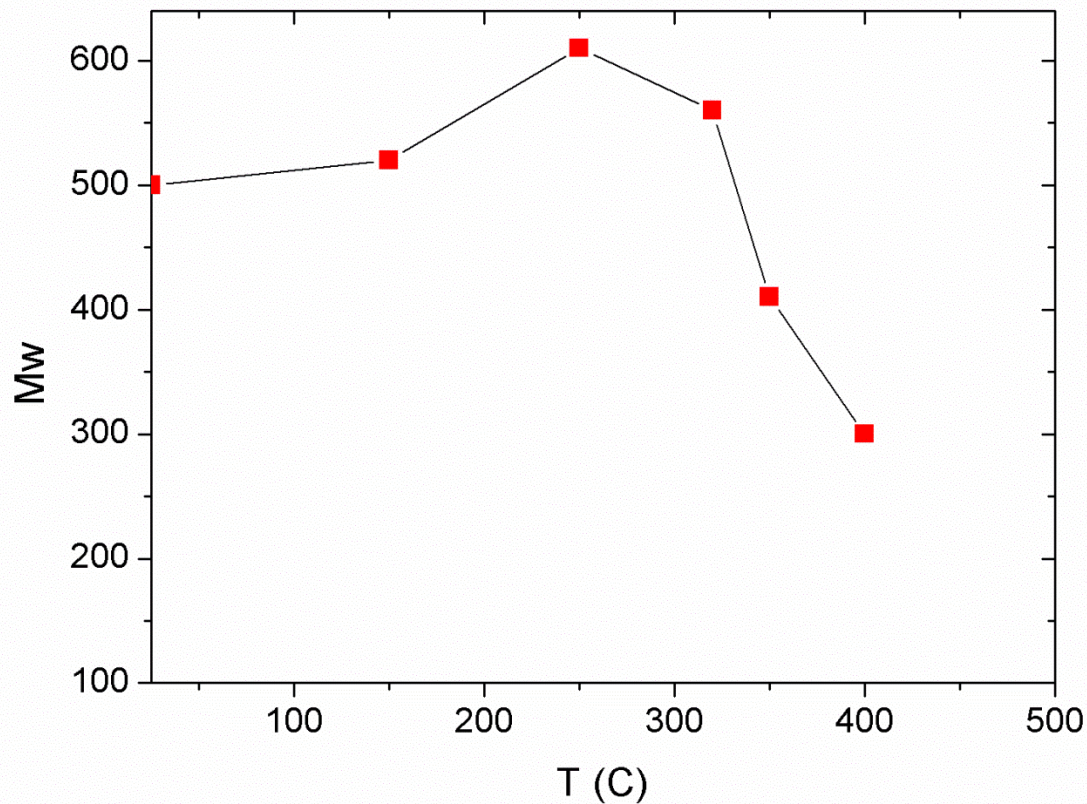


Sequence:

- Hydrogenation
- Dehydration
- Hydrogenation



Molecular weight (GPC)

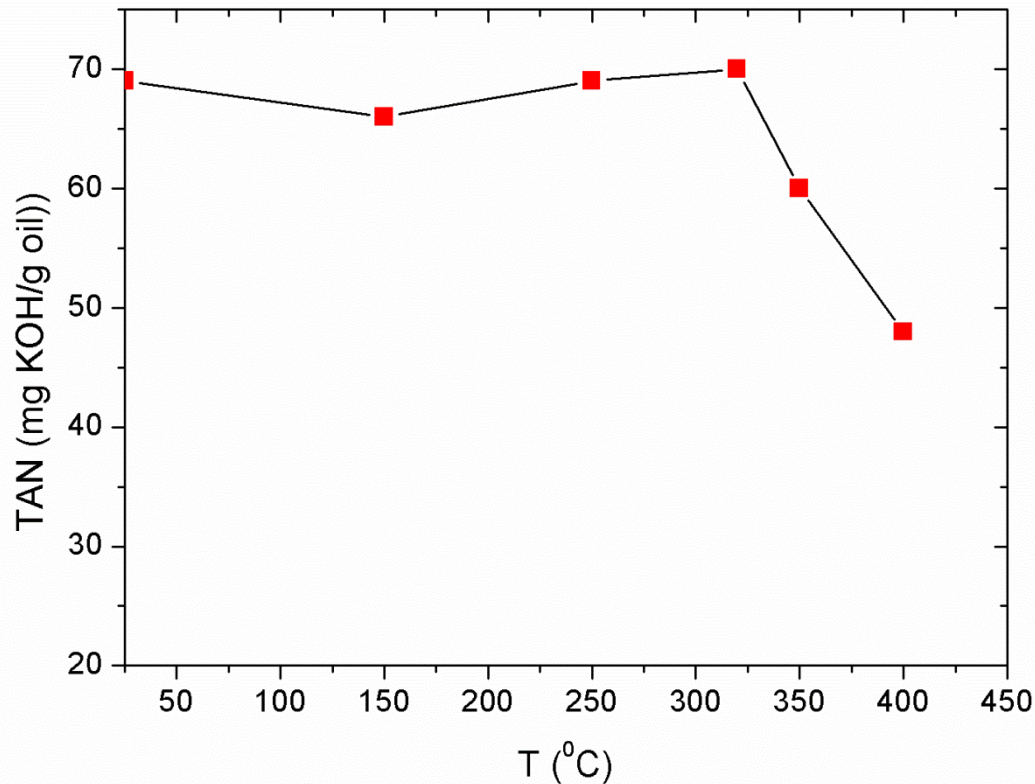


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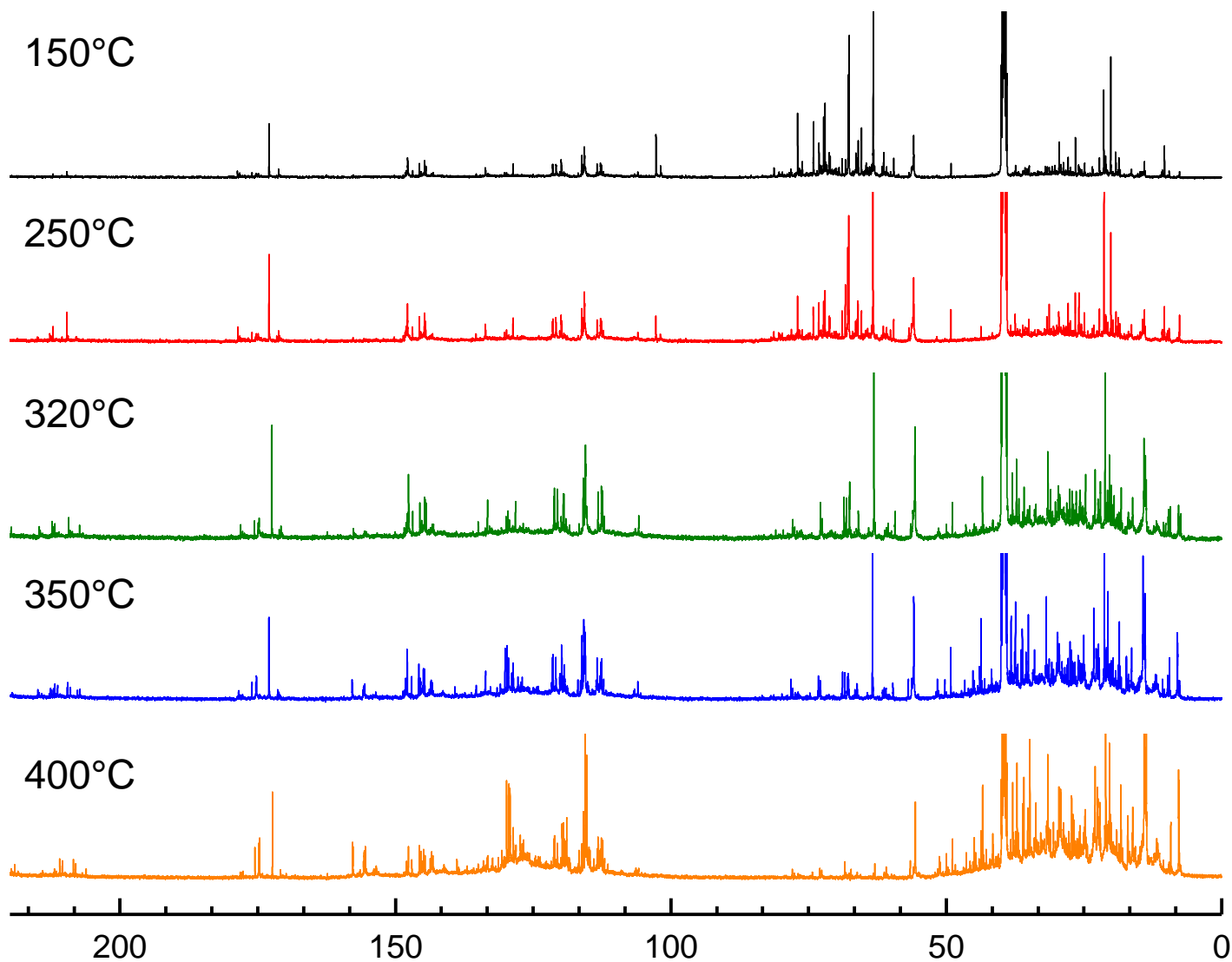
- Limited polymerisation till 250 °C
- Hydrocracking above 300 °C



Total acid number



Acids are very persistent,
 reactive only above 300 °C





Overview

Stabilisation ($< 250\text{ }^{\circ}\text{C}$)

Competition between
hydrogenation and
polymerisation

Water formation by
condensation reactions

Slight increase in Mw

Hydrogenation of
aldehyde/ketones

Sugar chemistry
dominates

Mild hydrotreatment ($250\text{-}350\text{ }^{\circ}\text{C}$)

hydrogenation-
dehydration

Reduction in Mw

Water formation by
alcohol dehydration

Breakdown of higher
Mw fractions

Sugar-sugar alcohol
chemistry dominates

Deep hydrotreatment ($> 350\text{ }^{\circ}\text{C}$)

Hydrocracking

Further reductions in Mw

Formation of aromatics
and aliphatic
hydrocarbons

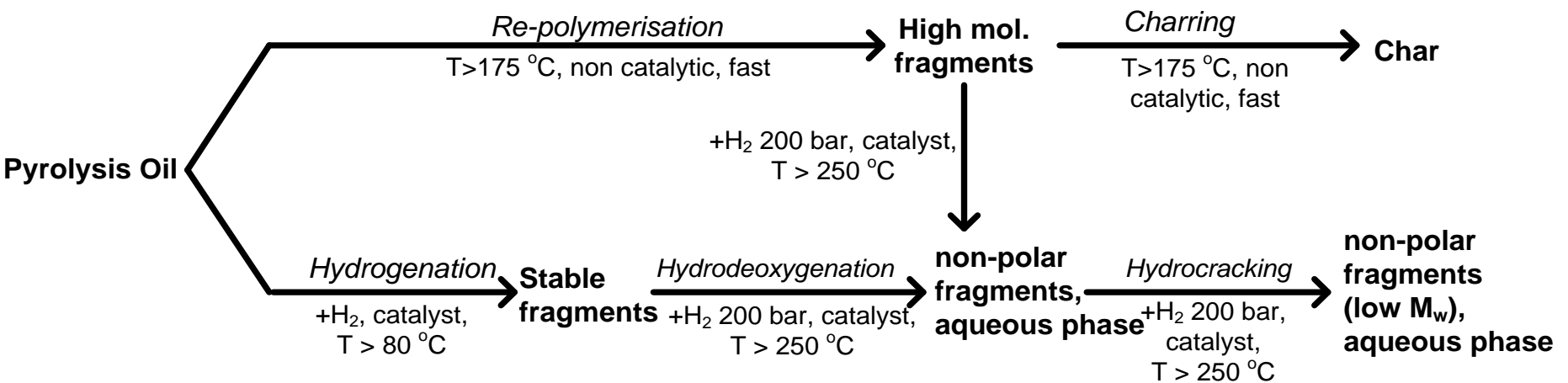
Acid conversion

Lignin chemistry
dominates

Temperature



Reaction pathway





Catalytic biomass conversions RUG/CRE

Biofuels

- Catalytic pyrolysis oil upgrading
- Biodiesel from *Jatropha Curcas*
- Green gas by supercritical gasification in water

Bio-based performance materials

- Starch modifications in non-conventional solvents
 - alcohols
 - supercritical CO₂

Biobased chemicals

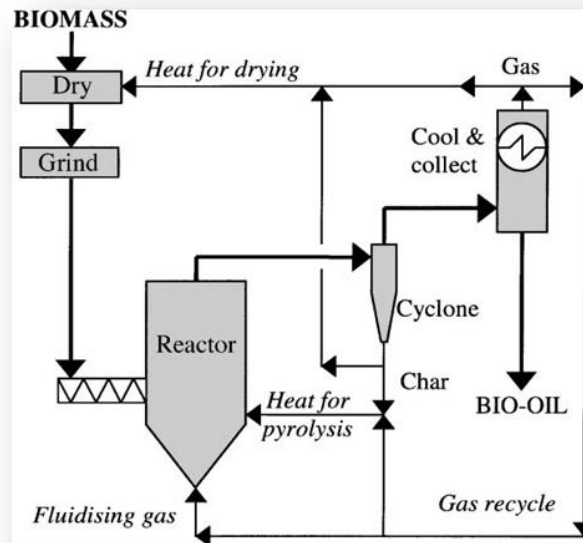
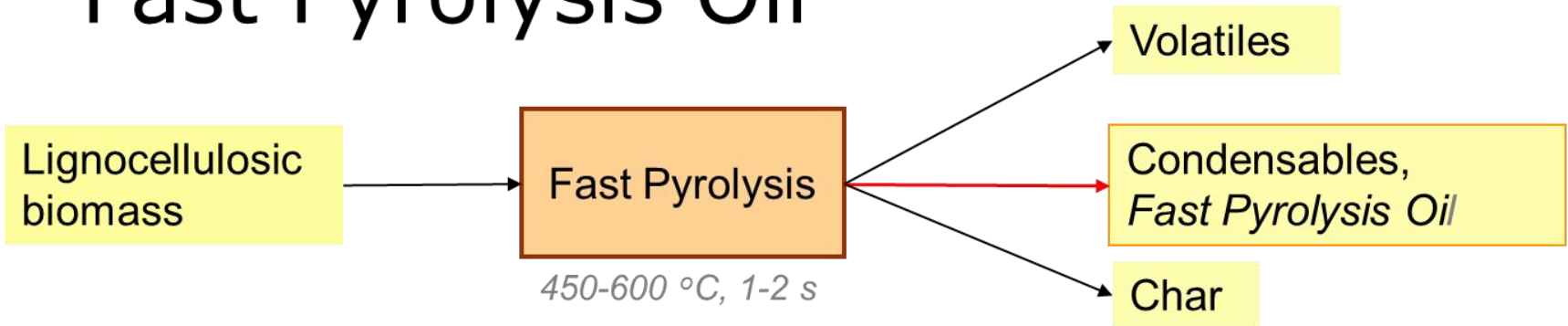
- Platform chemicals
- hydroxymethylfurfural
 - levulinic acid/lactic acid
 - methanol
 - furanics based diols
 - phenolics

Enabling science and technology

- Catalyst development
- Process intensification using centrifugal contactor separators



Fast Pyrolysis Oil

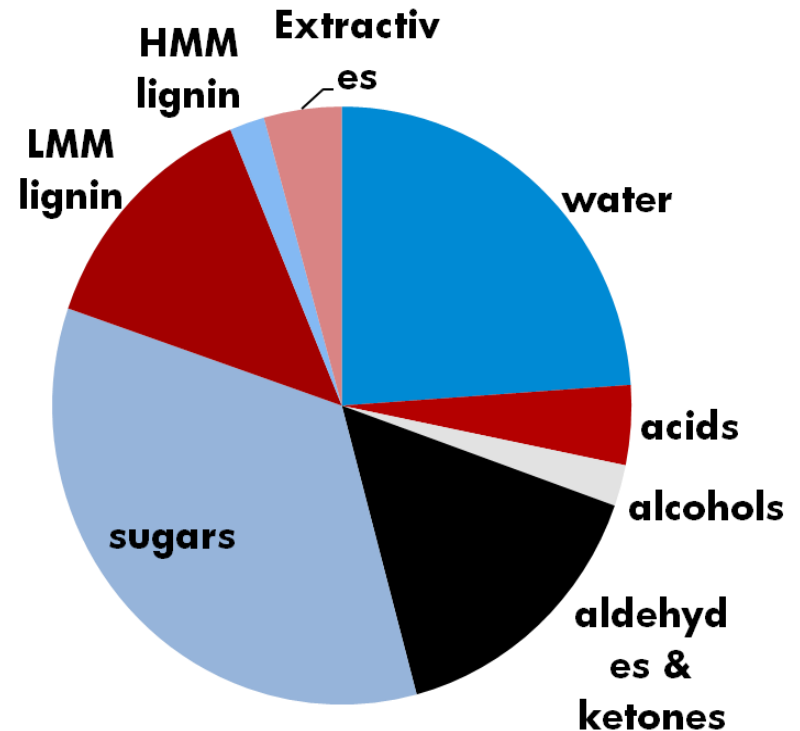


BTG, Enschede

Fast pyrolysis oil characteristics

- > High oxygen content (up to 50%)
- > Immiscible with petroleum products
- > Limited stability upon heating and storage (coke formation, repolymerization)

Pyrolysis oil composition	
C (wt%)	40.1
H (wt%)	7.6
O (wt%)	52.1
Moisture (wt%)	23.9





Biomass application platforms

