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Microbial fermentation: New tools to speed-up vaccine antigen development and increase process knowledge

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Microbial fermentation: New tools to speed-up vaccine antigen development and increase process knowledge

Catherine Jourdat

Sanofi Pasteur

**Bioprocess R&D Upstream platform
Vaccine technology IV May 23rd 2012,
Albufeira, Portugal**

SANOFI PASTEUR :

The vaccines division of SANOFI group

- **World leader in vaccines**

- 20 diseases
- More than 1 billion doses/year
- More than 500 million people vaccinated/year
- 13 vaccines in development(1)



- **Nearly 13,000 employees(2)**

- **12 production/R&D sites in the world**

- France (Marcy l'Etoile and Val de Reuil)
- US (Swiftwater, Cambridge, Canton, Orlando and Rockville)
- Canada (Toronto)
- Argentina (Pilar)
- China (Shenzhen)
- India (Hyderabad)
- Thailand (Chachoengsao)

And 3 new facilities under construction: Mexico (Ocoyoacac), France (Neuville) and China (Shenzhen)

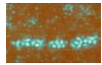
1. As of July 28, 2011, from phase I to "submitted"
2. FTEs as of December 2010 – Vaccines activities



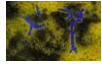
MARCY L'ETOILE, OUR VACCINES

- The site manufactures vaccines against 11 of the 20 diseases that Sanofi Pasteur's vaccines protect against throughout the world

Viral diseases



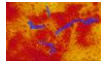
Yellow fever



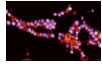
Mumps



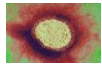
Poliomyelitis



Measles



Rubella



Influenza



Hepatitis A



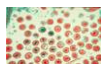
Hepatitis B



Rabies



Japanese Encephalitis



Chickenpox

Bacterial diseases



Pertussis



Diphtheria



Haemophilus influenzae type b Infections



Meningococcal meningitis



Pneumococcal infections



Tetanus



Tuberculosis



Typhoid Fever



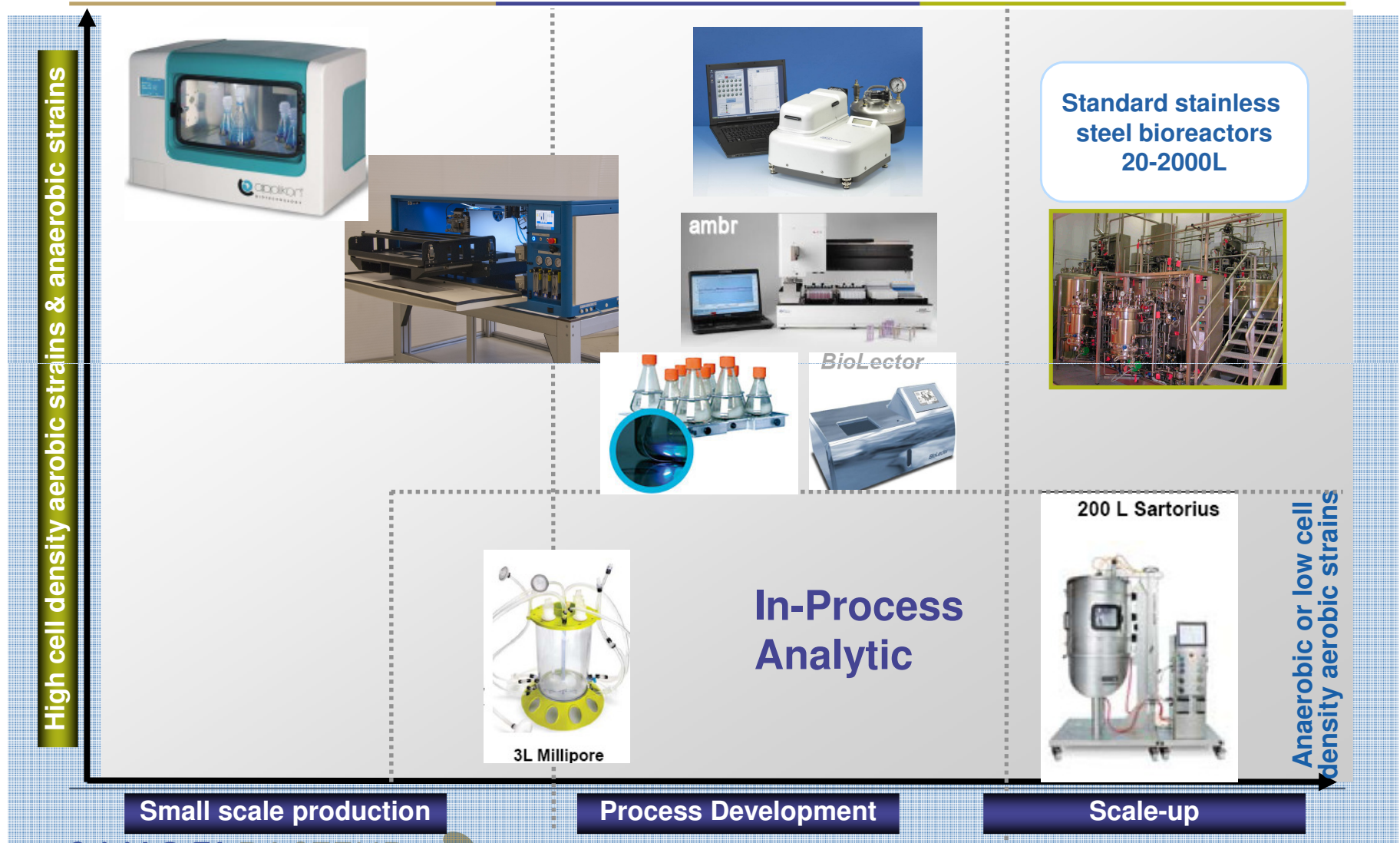
Cholera



Marcy l'Etoile also purifies immunoglobulins

Microbial fermentation

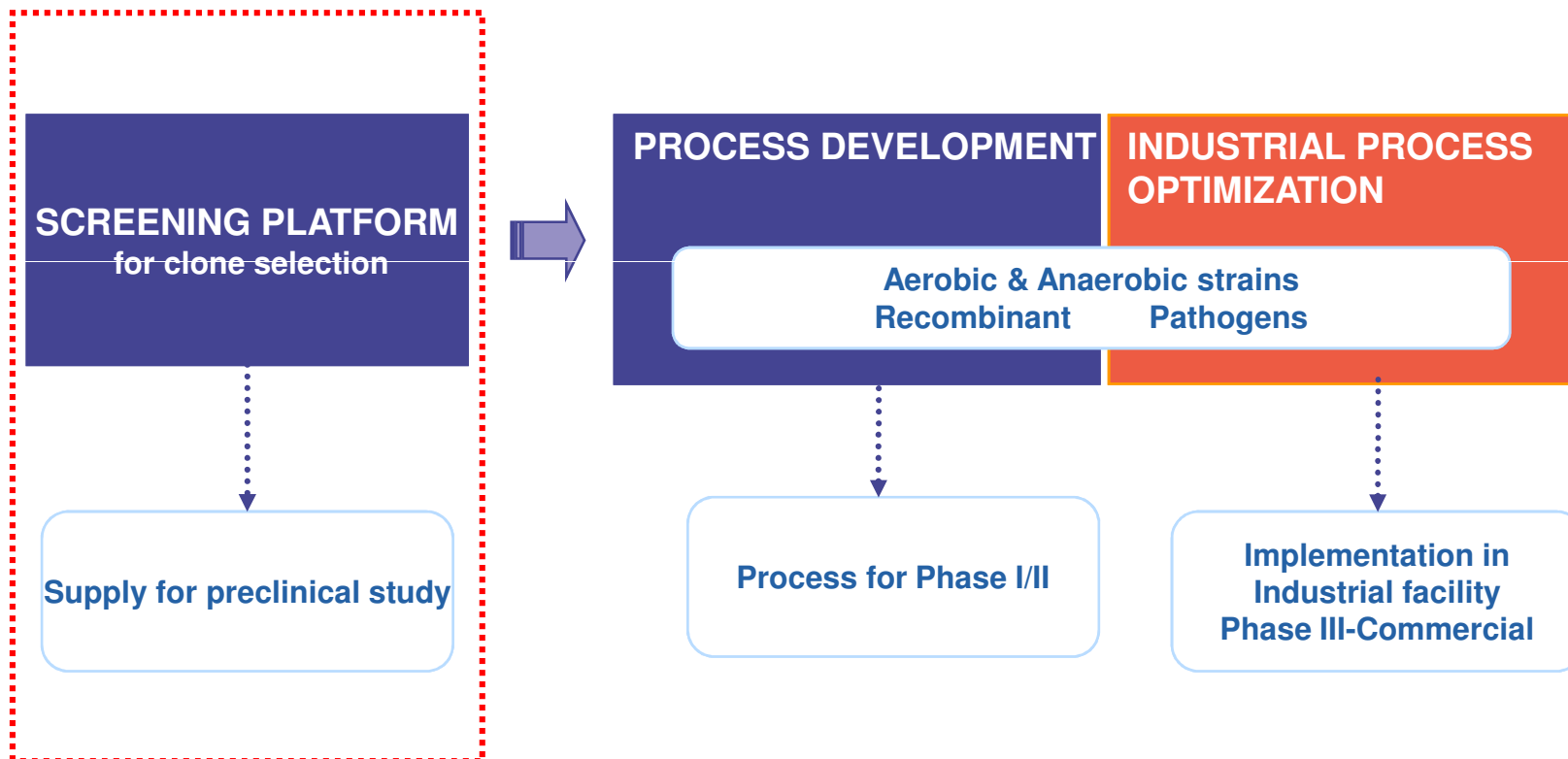
Innovative tools for high density aerobic and pathogenic strains



Microbial fermentation

Different sequential process screening/development platforms

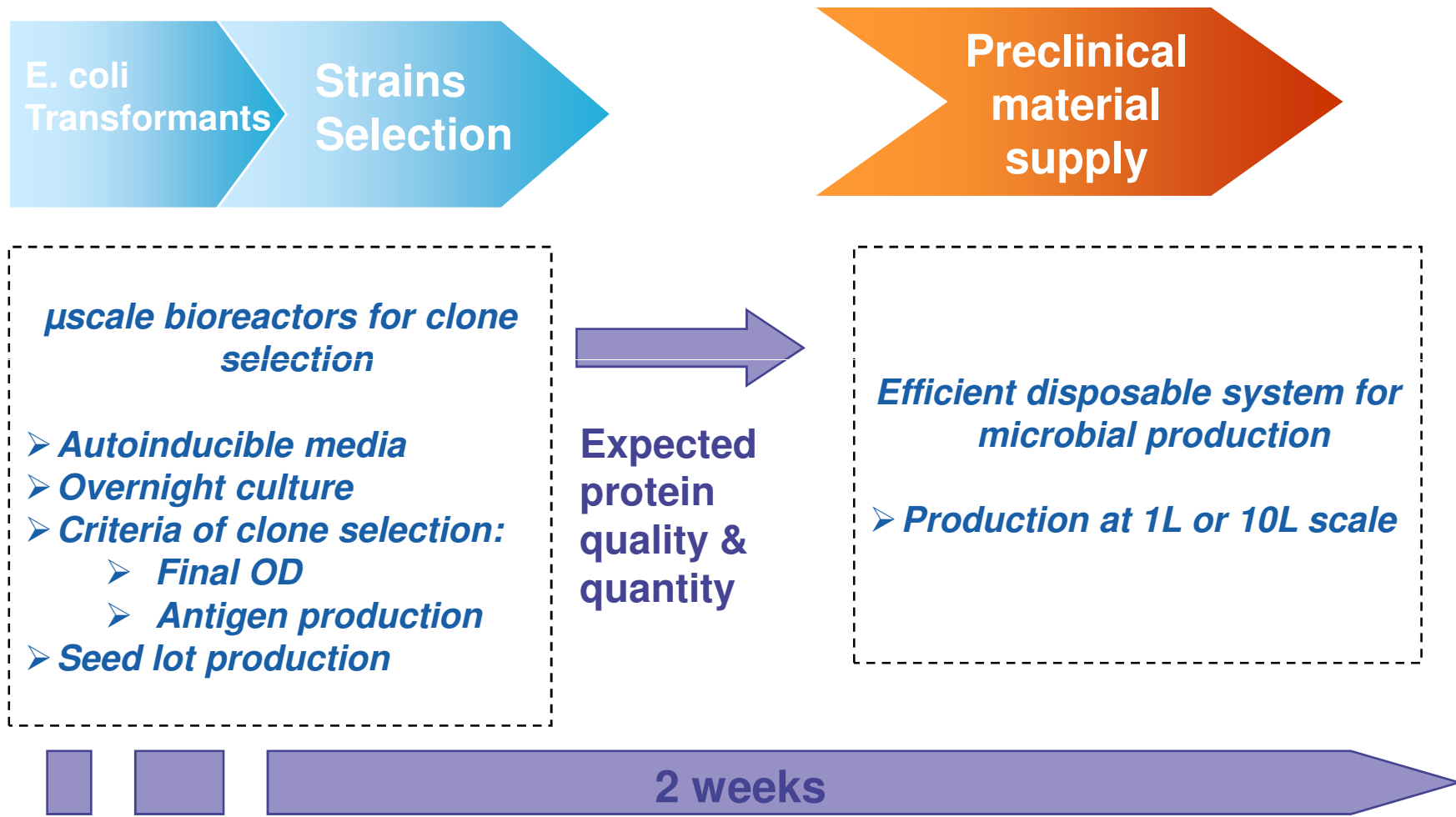
- Tools architecture organized in each platform to speed-up strain selection, process development and optimization of industrial processes



Screening platform

1/8

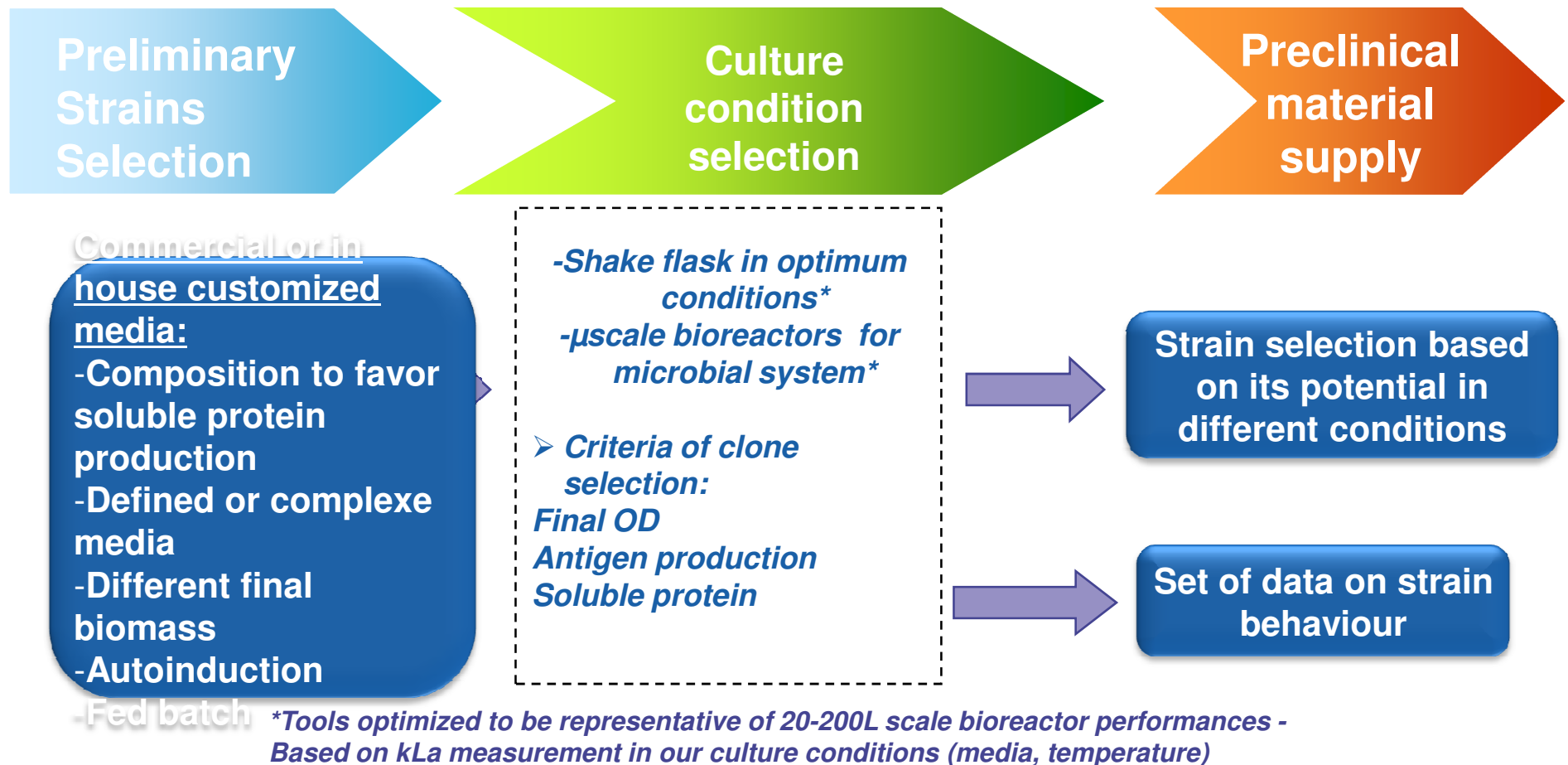
μscale and disposable bioreactors for fast material supply



Screening platform

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Set-up of predictive μ scale tools for difficult to express protein

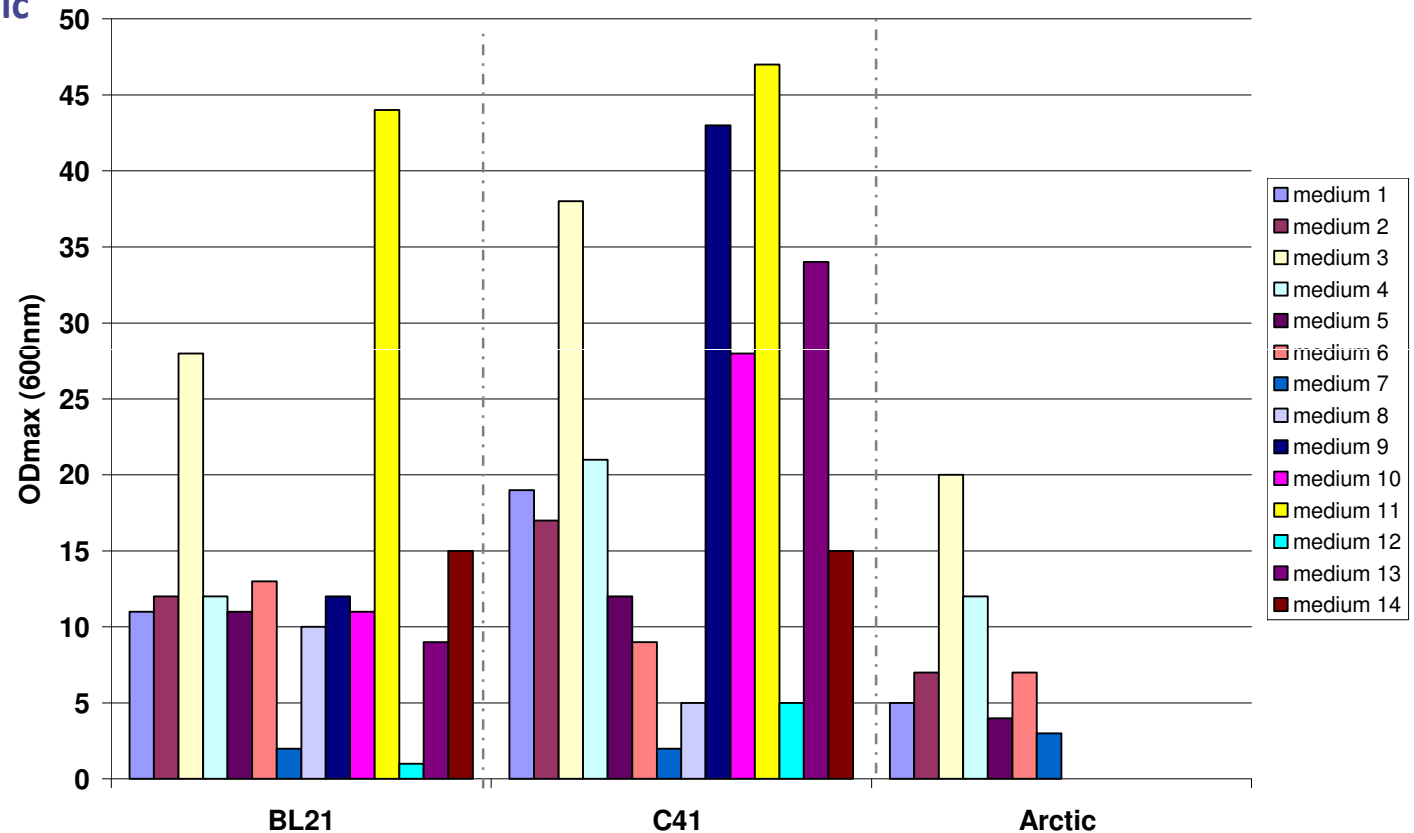


Screening platform



Case study: screening of different hosts/media in μ 24 bioreactors

- Difficult to solubilize protein for vaccine antigen subunit
- Evaluation of different culture conditions, under induction, for pre-selected functional clones: *E. coli* BL21, C41 and Arctic



- Differential behaviour among strains, and culture conditions

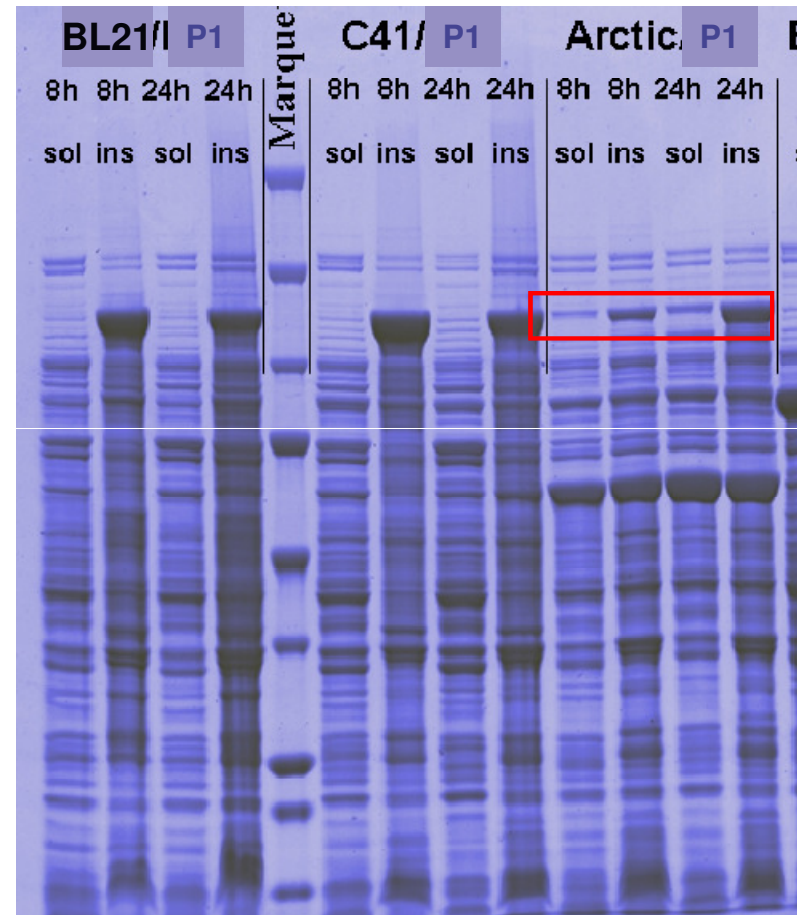
Screening platform

Case study: screening of different hosts/media



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- Evaluation of production in the soluble and insoluble fractions for each condition
- Main results
 - Soluble fraction for the protein P1 expressed in *E. coli* Arctic host in a specific medium
 - No soluble fraction with *E. coli* BL21 whatever the culture conditions
- Next step: optimize best clone culture conditions to increase the protein production in the soluble fraction



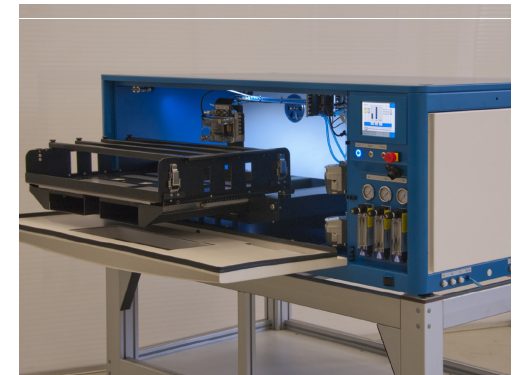
Screening platform

Preclinical
material
supply

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Case study: Cell tainer system® evaluation

- **Initial process in stainless steel fermentor (30L scale)**
 - *E.coli* strain, protein production induced with IPTG
 - Regulations:
 - pH: 7.00, 37 °C, DO: 30% (cascade: stirrer , air flow then oxygen enrichment)
- **Evaluated system for fast preclinical production turn around: Cell tainer system**
 - Flexibility (1 to 15L, batch or fed batch mode, optional on line glucose measurement (TRACE system))
 - Atypical agitation system allowing to reach high K_{La} values
- **Preliminary run performed with working volume at 11 liters :**
 - Foam in out air filter, Oxygen limitation
- **Optimal settings identified via k_{La} measurement :**
 - Working volume (7L), stirrer (45 rpm)
 - Addition of anti-foam before inoculation
 - Angle of agitation fixed at the maximum



➡ **Max k_{La} value: 300h⁻¹**

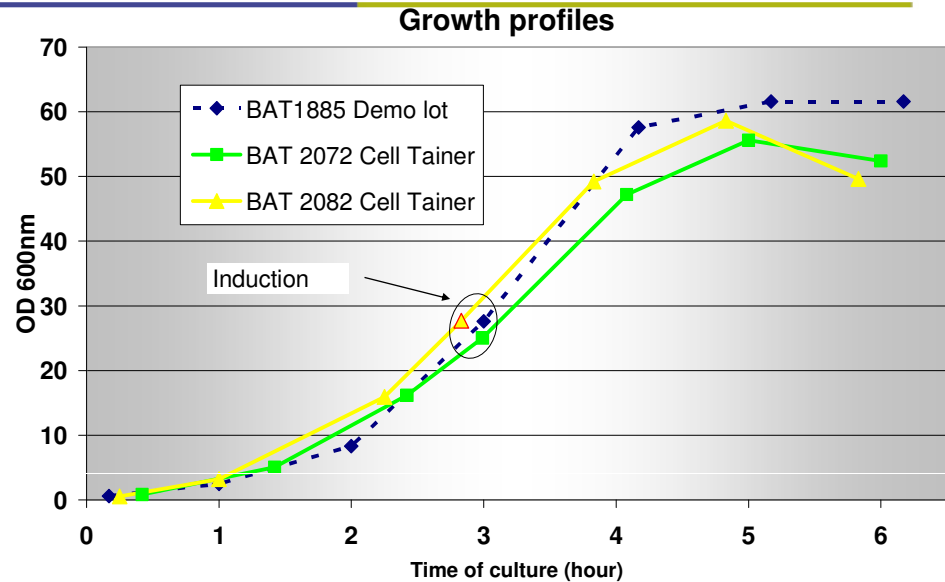
Batch mode process performance



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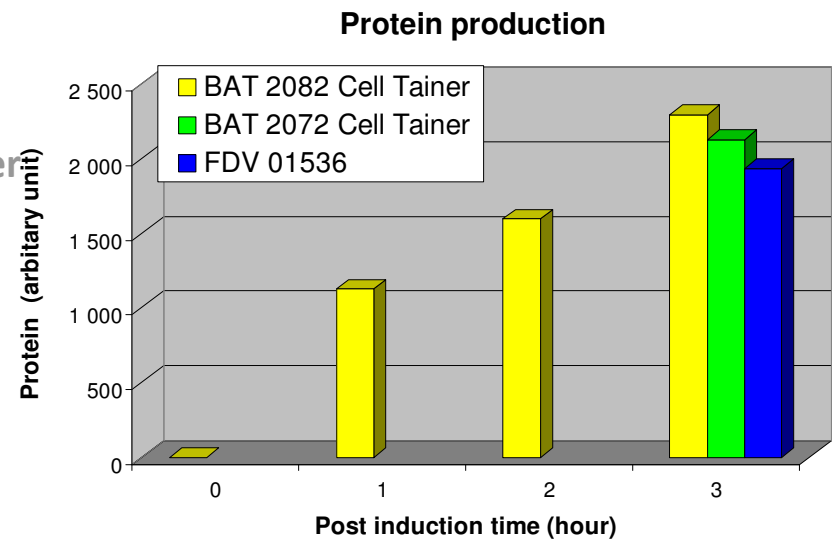
- **Growth kinetics with optimum settings**

- similar growth and biomass between stainless steel reactor and cell tainer system



- **Protein production analysis by SDS – PAGE / Scan**

- Comparable protein expression between Cell Tainer and stainless steel reference



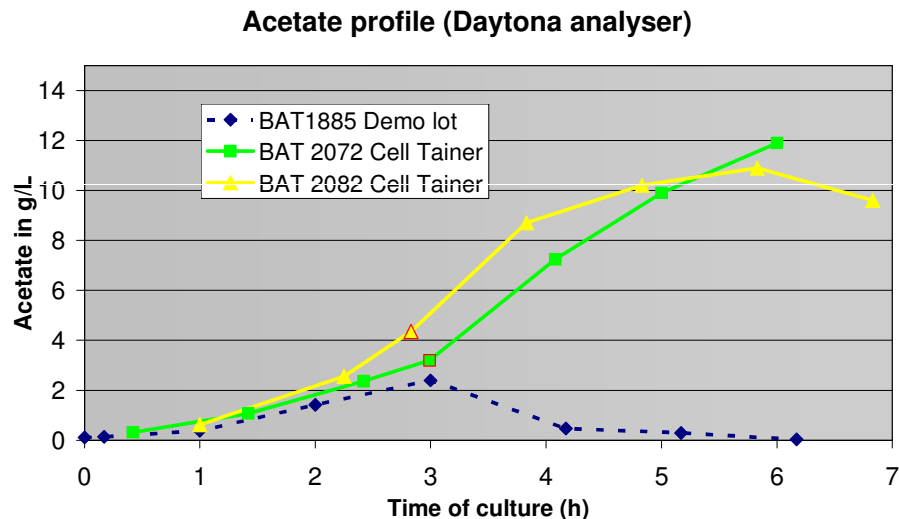
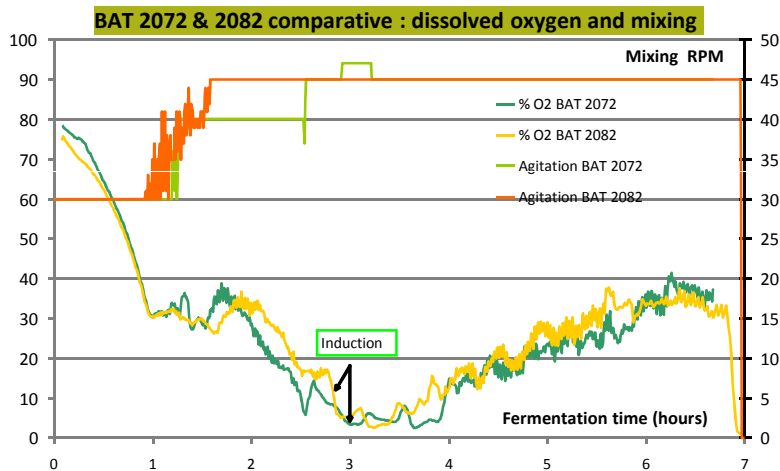
Batch mode process performance



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● Process parameters and metabolites follow-up:

- Kinetic of glucose consumption identical to our standard process
- No oxygen limitation but set point not maintained during the culture
- High level of acetate production at the end of the culture



● Fed batch process:

- Preliminary work shows that we can maintain DO above 20%
- Acetate level is low (below 2.5 g/L)

Advantages / Perspectives



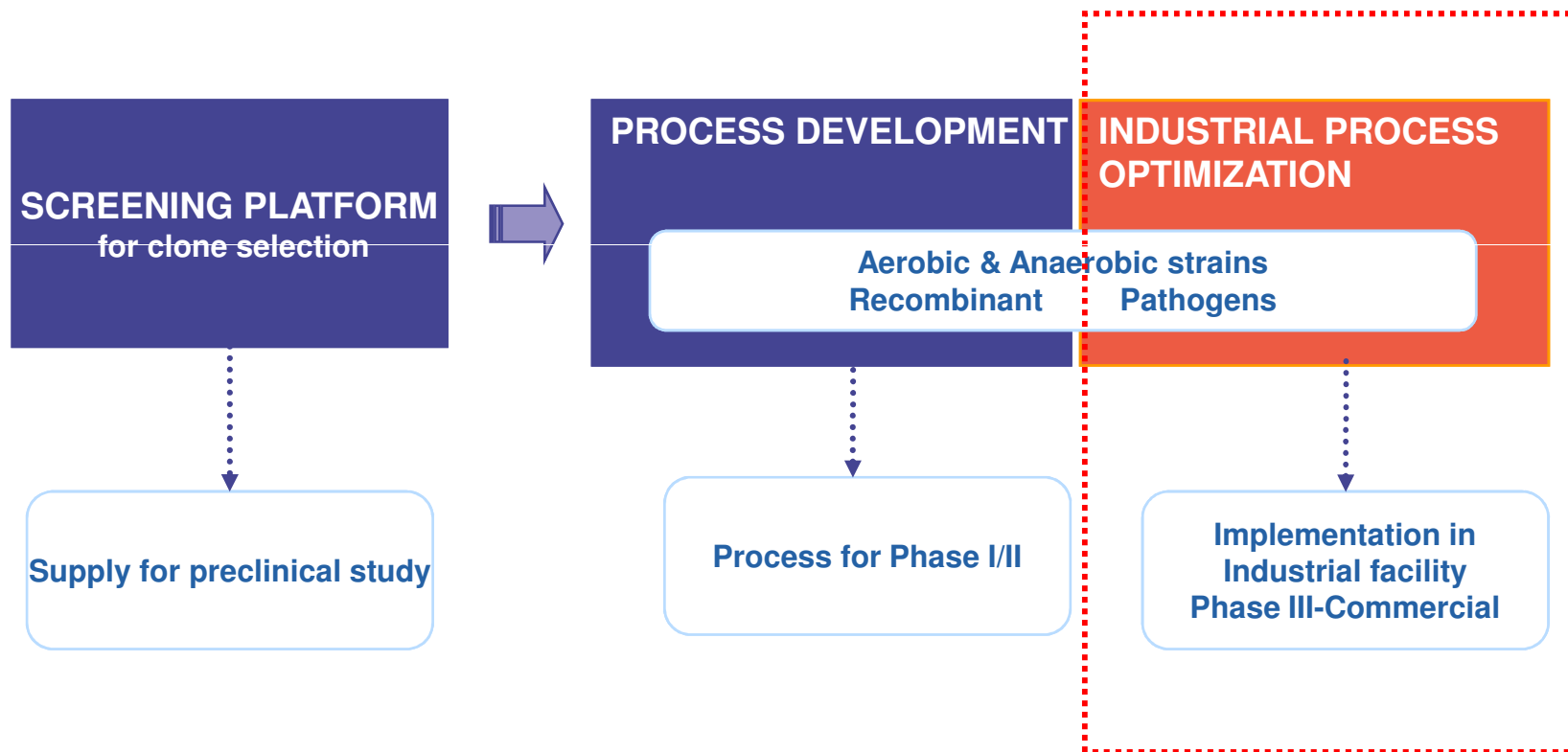
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- **First efficient *E.coli* batch process in a single use bioreactor**
 - Similar biomass (around 20g/L cdw) and protein production versus standard fermentor
 - Batch and fed batch processes capabilities
 - Good reproducibility
- **Advantages thanks to the high turn-around for process development and small scale batches**
- **However, system scalability limited for purposes beyond preclinical supplies, seed train, phase I GMP production**

Microbial fermentation

Different sequential process screening/development platforms

- Tools architecture organized in each platform to speed-up strain selection, process development and optimization of industrial processes



Industrial process optimization

Case study: μ scale to industrial scale

- Aerobic pathogenic strain – Industrial process
- Aim of the study:
 - To model the impact of 3 process parameters (pH, DO, T) on biomass and antigen production and impurity level
 - To identify optimal process productivity conditions

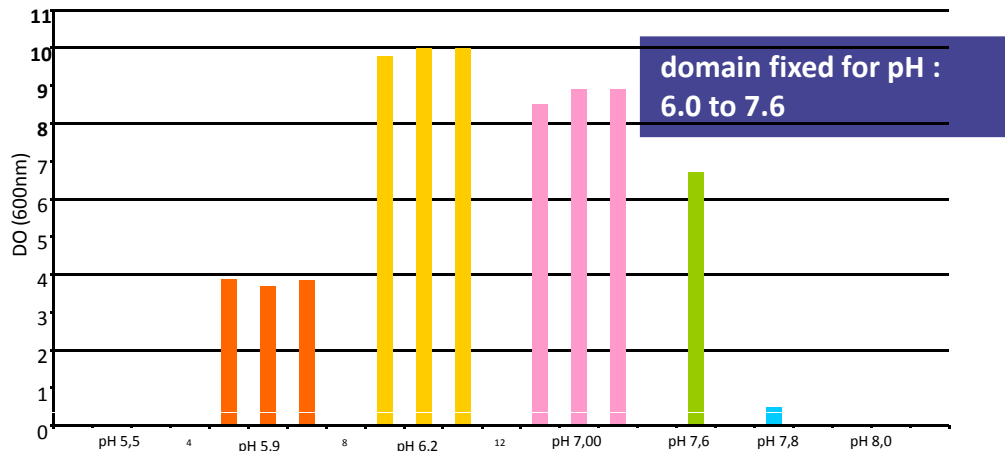
Implementation of micro scale-down and DOE combination for process modelization and improvement of culture parameters for an industrial process

Scale down model tested	flask	Micro - fermentor	Fermentor 1L	Fermentor 30L	Reference Industrial
Working volume	150 ml	3 ml	0.5L	30L	1000L
Capacity of fermentors available in the lab	No limit	24	4	2	/
Results	Biomass (OD _{600nm})	7.9	9 - 10	9 - 10	8 - 9
	Product yield (g/L)	0.4	0.75	0.8	0.62

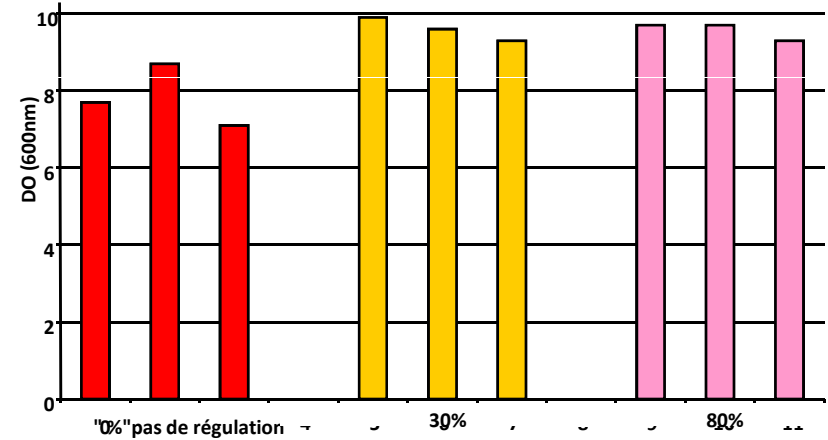
Experimental domain definition :

identification of limit values for each parameter investigated

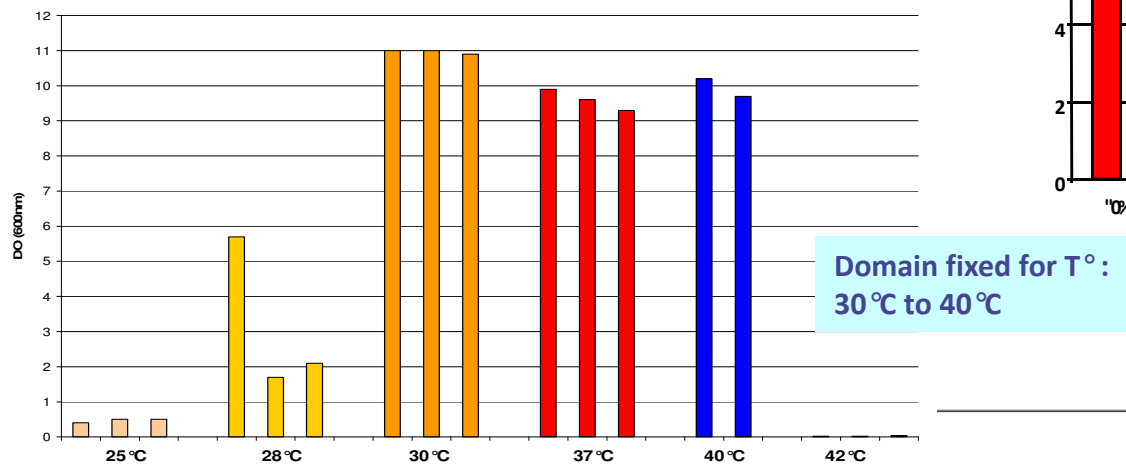
- Effect of pH on biomass (T at 37°C, DO₂ at 30%)



- Effect of DO₂ on biomass (no pH regulation and T at 37°C)



- Effect of Temperature on biomass (no pH regulation, DO₂ at 30%)

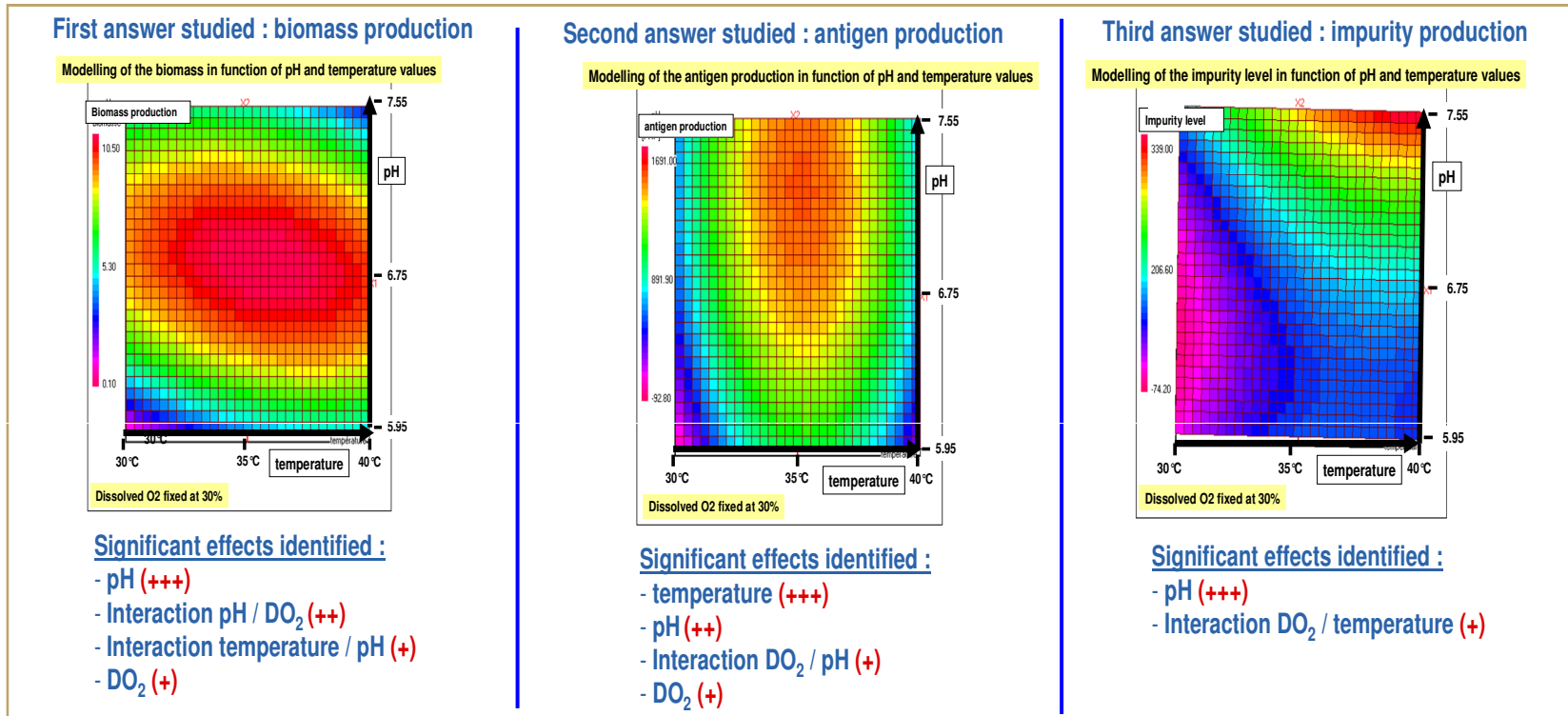


N°Exp	température °C	pH Unité	pO2 %
1	30.0	5.90	6.0
2	40.0	5.90	6.0
3	30.0	7.60	6.0
4	40.0	7.60	6.0
5	30.0	5.90	70.0
6	40.0	5.90	70.0
7	30.0	7.60	70.0
8	40.0	7.60	70.0
9	30.0	6.75	38.0
10	40.0	6.75	38.0
11	35.0	5.90	38.0
12	35.0	7.60	38.0
13	35.0	6.75	6.0
14	35.0	6.75	70.0
15	35.0	6.75	38.0
16	35.0	6.75	38.0
17	35.0	6.75	38.0
18	33.0	6.55	32.7
19	37.0	6.55	32.7
20	35.0	7.15	32.7
21	35.0	6.75	54.0

Response surface model (central composite matrix)

	Facteur	Unité	Centre	Pas de variation
U1	température	°C	35.0	5.0
U2	pH	Unité	6.75	0.85
U3	pO2	%	38.0	32.0

- Use of the software Nemrodw®
- Response surface model (central composite matrix)
- 21 cultures
 - 15 conditions for the DOE
 - 3 repetitions of central point
 - 4 test points to validate the model



- Effect of the 3 parameters investigated on the 3 responses (single effect or interaction)
- But no condition allowing at the same time to maximize antigen production and minimize the impurity quantity

- **Modelisation of the phenomena investigated in the experimental domain**

- **Compromise :**

Identification of conditions allowing at the same time the increase of the antigen production and the maintain/control impurity level

Implementation of results obtained through the DOE

- Testing of new settings at intermediary scales (fermentors 1liter and 100 liters) then at industrial scale (fermentor 1000 liters)

Confirmation of results obtained with DOE at micro scale :

increase of antigen production confirmed up to industrial scale

Settings	Initial	DOE predictions with new settings
Fermentor Scale	Fermentor 1L	
OD max (600nm)	11	12
Product yield (g/L)	0.8	1.23
Impurity Level (UI/ml)	900 000	800 000



Conclusion

- **Technological evolution in the single use domain**
 - For microbial fermentation new single-use and μ scale bioreactors have been recently developed than can deal with the high oxygen demand
- **Benefits of the single use and μ scale bioreactors implementation**
 - Conduce fast expression system screening to select best host, clone, media, vector for antigen production at the expected quality and quantity
 - Generate predictable results at industrial scale thanks to parameters regulation
 - Increase process knowledge and robustness through DoE with limited workload
 - Reduced time of process development trough downscale, multiple parallel bioreactors
 - Ressource allocated to core expertise instead of non value tasks (cleaning, bioreactor decontamination)
 - Lead significant increase of the antigen production for two industrial processes
- **Next steps**
 - Implementation of highthrough-put sample treatment,
 - Automation of the different steps (culture, sampling, sample treatment, analytics),
 - Data management

Acknowledgement

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Thank you!
Questions ?