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# Modeling Reactions Between Activated Sludge Fractions and Ozone to Optimize Biosolids Reduction Processes

Dominic Frigon  
*McGill University*

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**McGill**

# Modeling Reactions Between Activated Sludge Fractions and Ozone to Optimize Biosolids Reduction Processes

**Dominic Frigon**

Microbial Community Engineering Laboratory  
Department of Civil Engineering  
McGill University

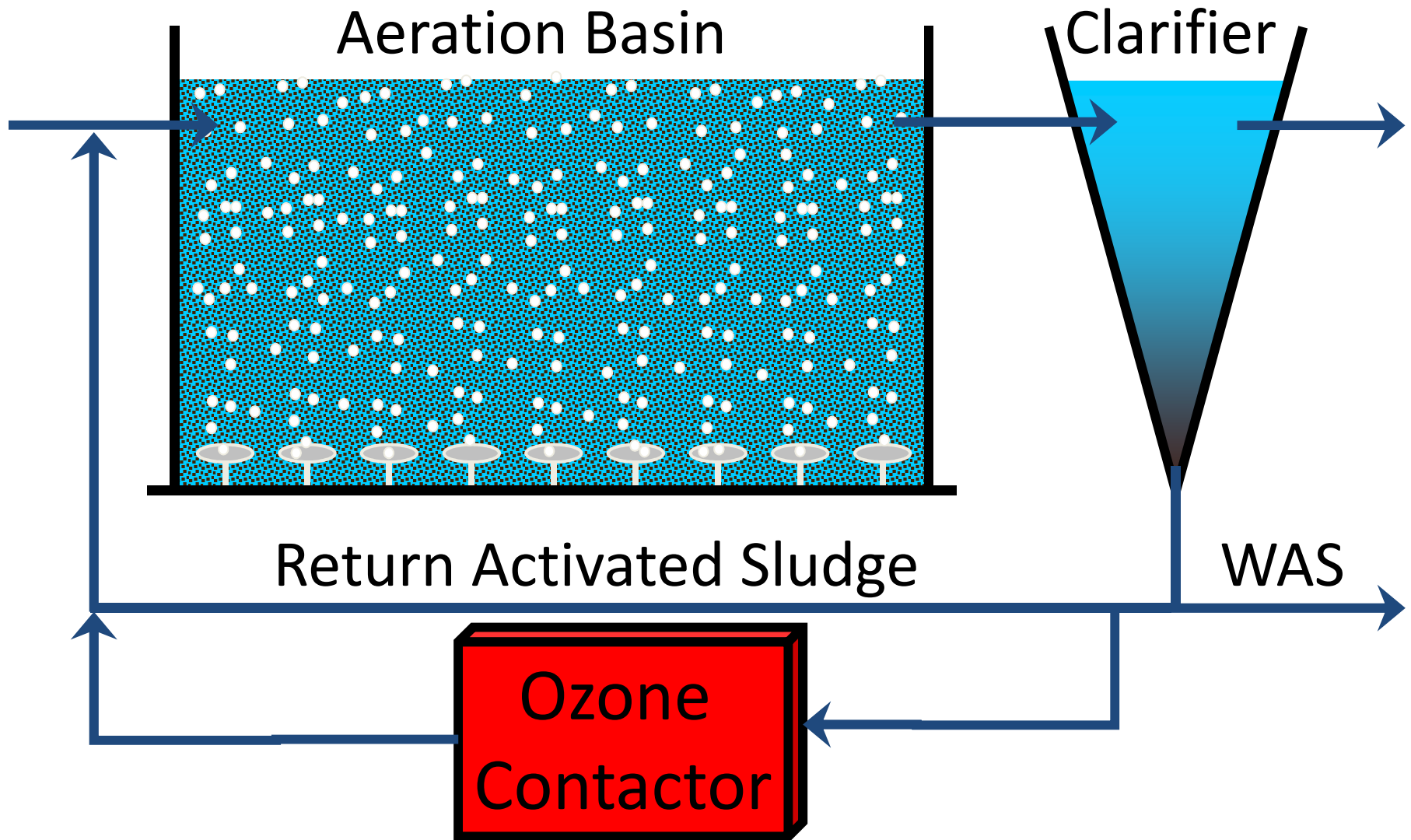
June 12, 2014



# Introduction

- Cost of biosolids disposal is rising in North America due to disposal options and environmental taxes.
  - For our partner wastewater treatment facility, disposal cost more than doubled over the last 7 years.
- In some Canadian jurisdictions (e.g., Province of Quebec), landfilling of biosolids will be banned by 2020.
- Thus, facilities want to reduce biosolids production.
- Air Liquide tries to open the North American market, but imprecision in performance predictions remain an obstacle.
- New Canadian laws require proper nitrification even during winter (water temperature  $\ll 10^{\circ}\text{C}$ )
  - Is nitrification affected by RAS-ozonation?

# Schematics of RAS Ozonation Unit

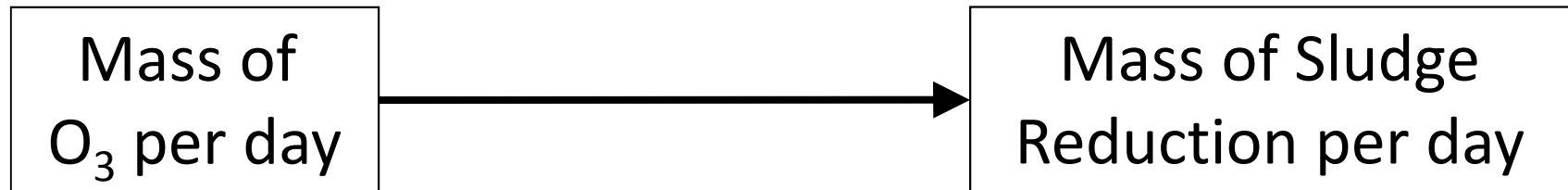


# Objectives

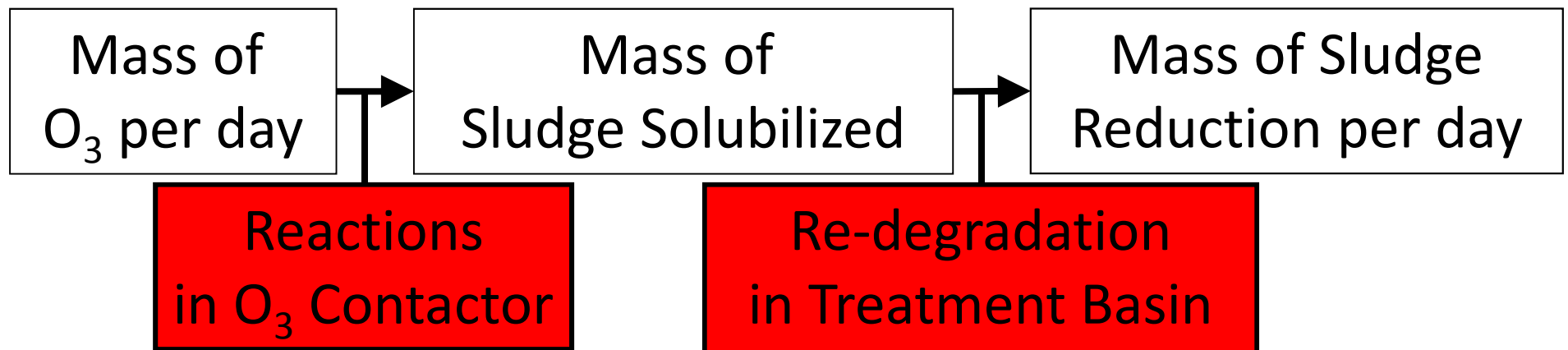
- Develop and validate a mathematical model to improve performance predictions.
- Perform a global sensitivity analysis to understand the impact of biological processes on biosolids reduction.
- Perform a scenario analysis on nitrification stability to identify threatening operation conditions.

# Concept of Ozone Unit Performance

- Technical/economic performance

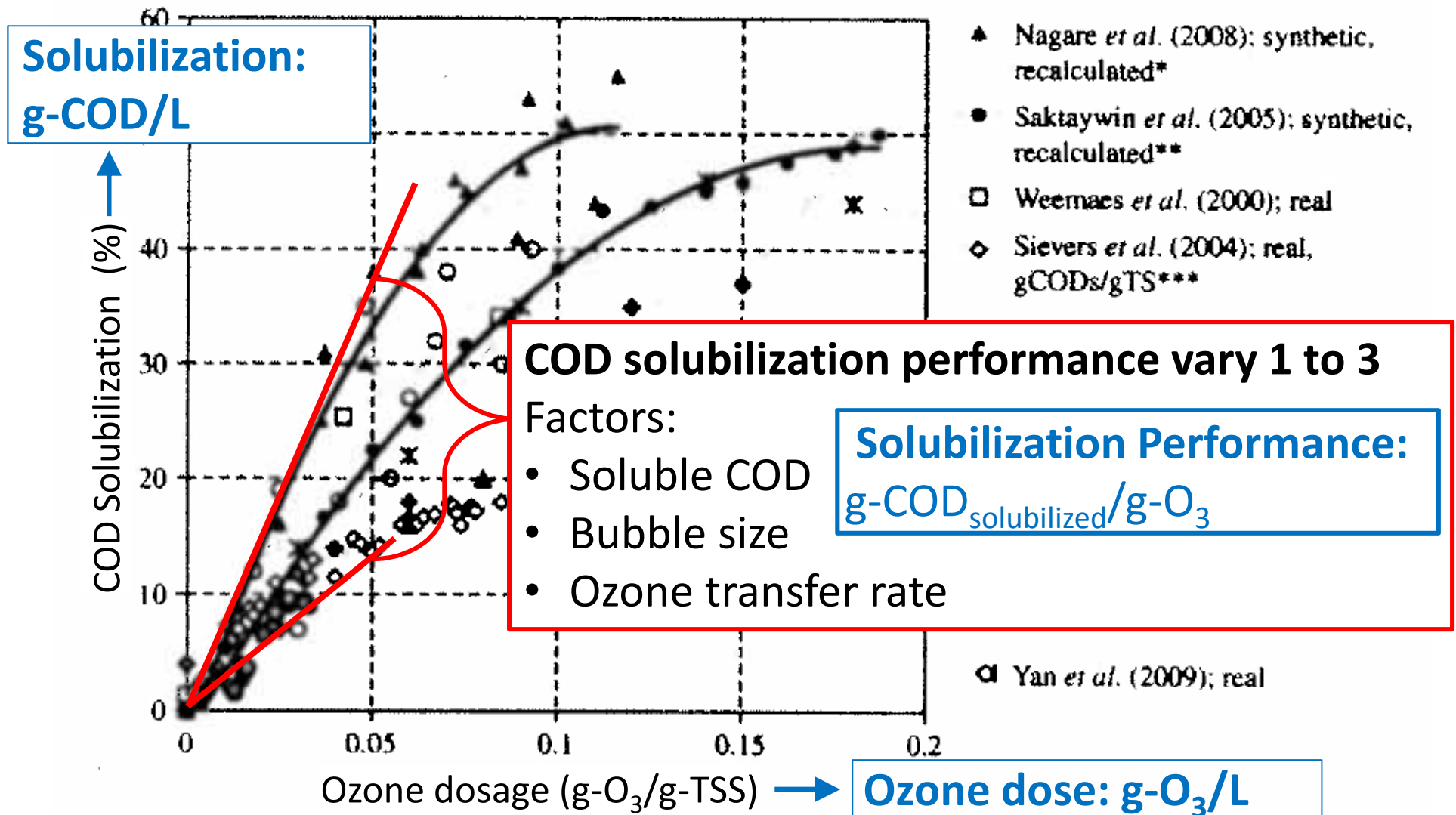


- True performance evaluation steps

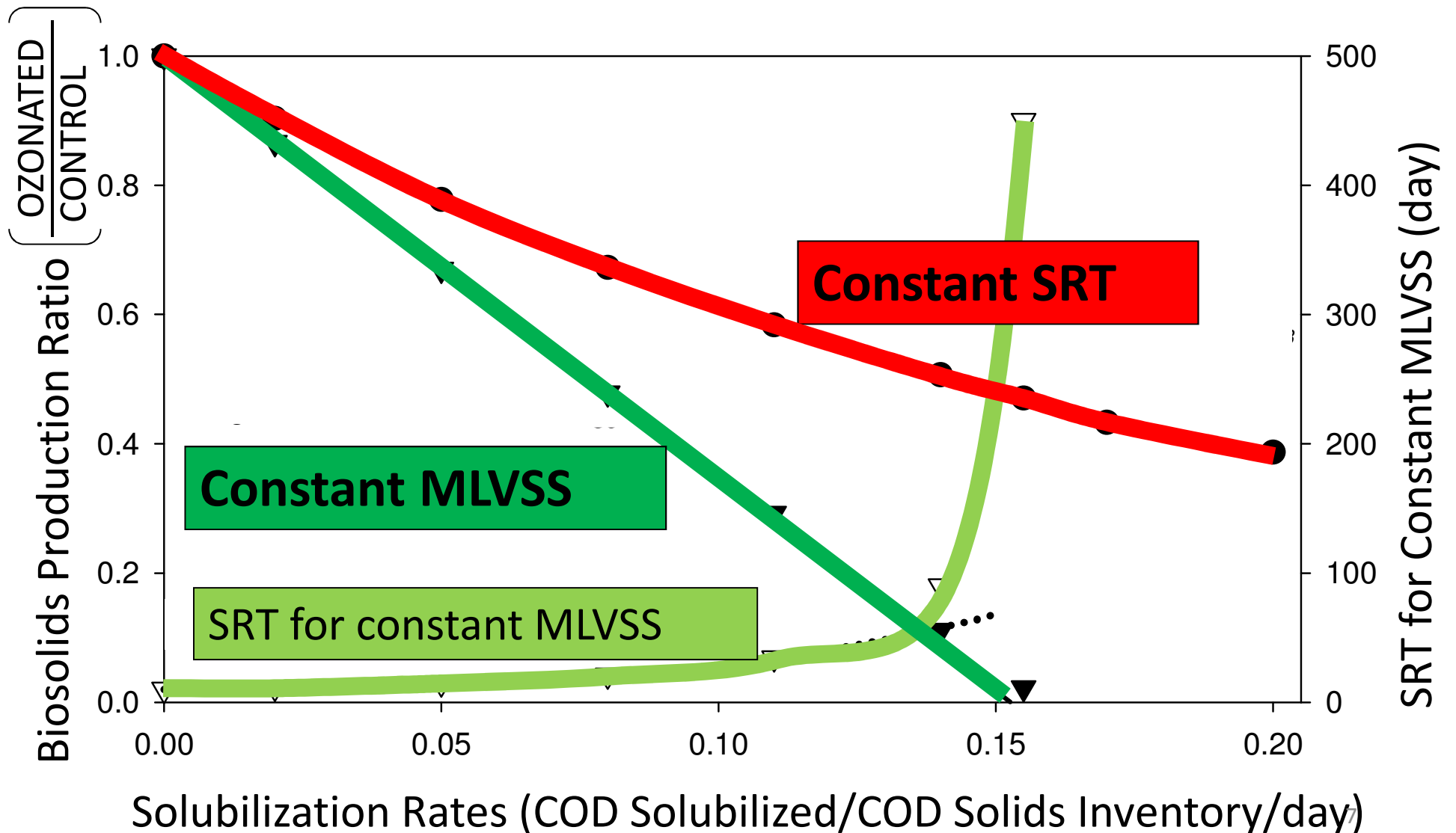


# O<sub>3</sub> Contactor Performance by COD Solubilization

Note: total COD and total suspended solids (TSS) are related



# Biosolids Reduction with Increasing Solubilization Rate (COD Solubilized/Solids Inventory/day)





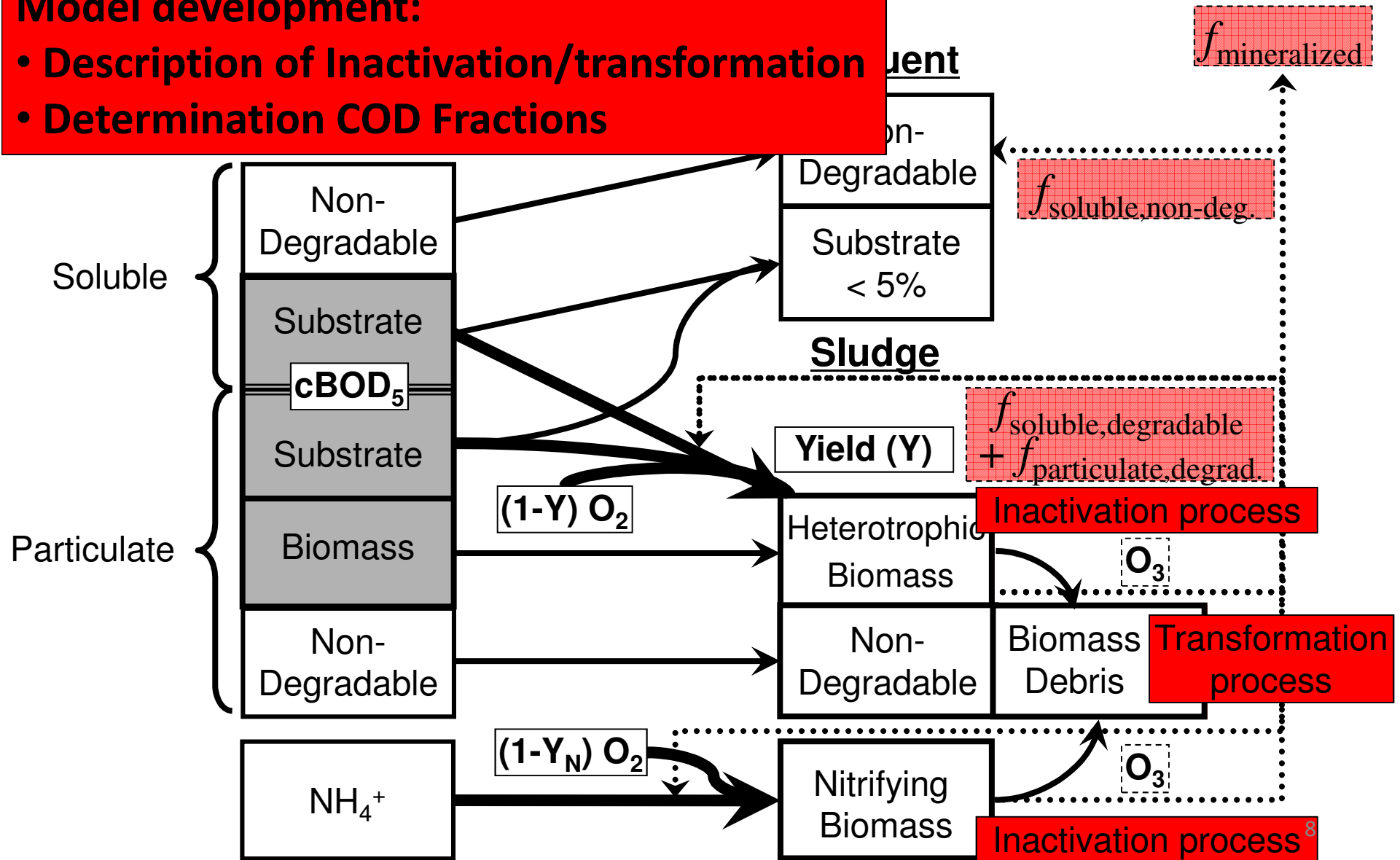
# Model of Activated Sludge + RAS-Ozonation

Influent COD

Outlet COD (Effluent+Sludge)

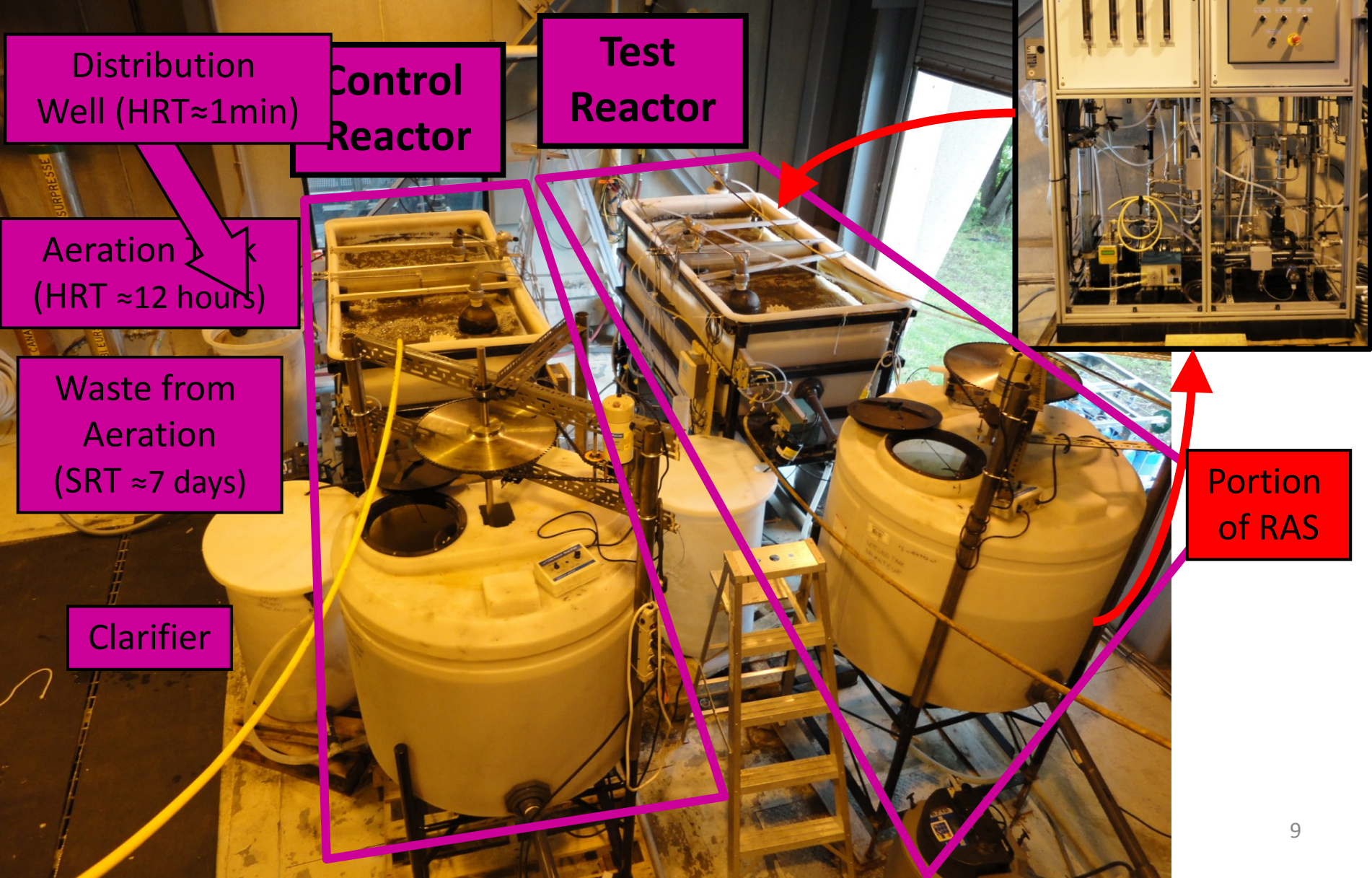
## Model development:

- Description of Inactivation/transformation process
- Determination COD Fractions



# Pilot-Scale Parallel Reactors

(1 m<sup>3</sup> Aeration Tank)



# Modeling Development and Validation

- Description of inactivation
  - kinetics and stoichiometry
- Model prediction of pilot-scale experiments' data
  - Same installation studied in 3 different years



# Modeling Effects of Ozone on RAS Biomass

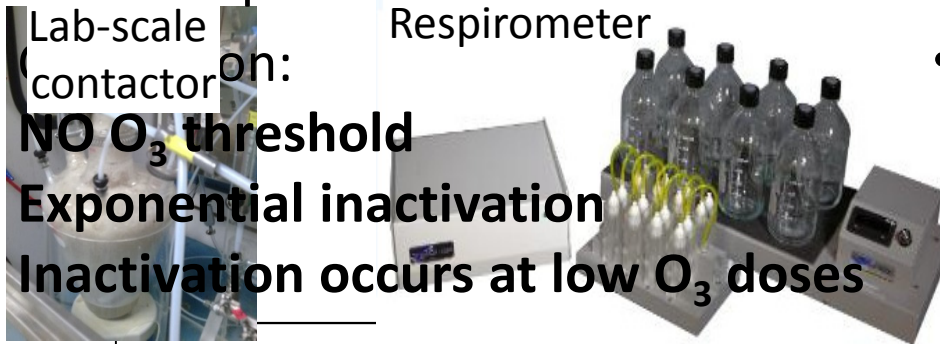
Is biomass inactivated at low O<sub>3</sub> dose?

- Others reported dose threshold
- Others reported linear inactivation

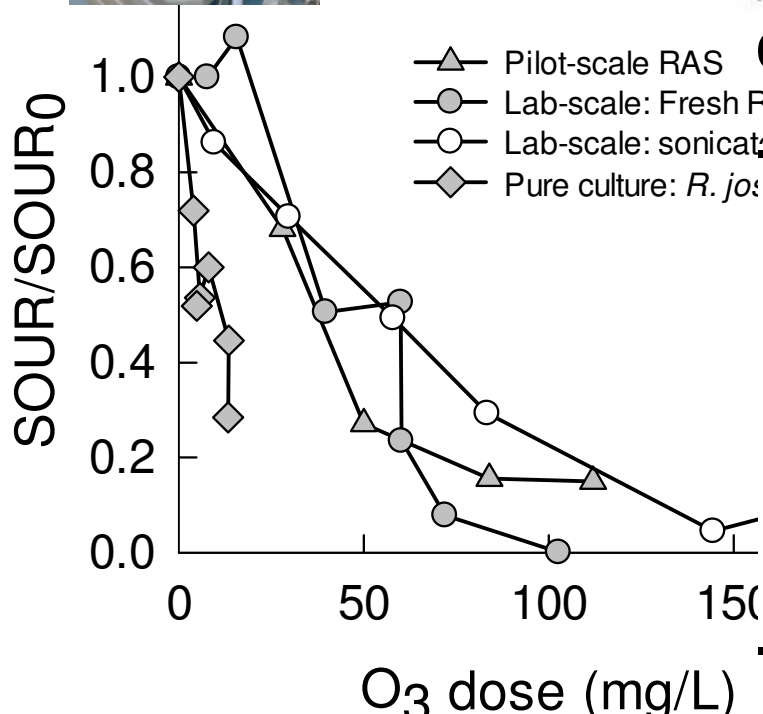
Does inactivation solubilize biomass?

- From literature: ozone solubilizes cellular content...

- Lab-scale contactor on: **NO O<sub>3</sub> threshold**
- **Exponential inactivation**
- **Inactivation occurs at low O<sub>3</sub> doses**



- Conclusion: **Little COD solubilization upon inactivation**



Ozonator Scale/Solids source COD solubilization (mg-COD/mg-O<sub>3</sub>)

Pilot-scale on RAS

Control reactor 2.29 ± 0.27

Ozonated reactor 2.04 ± 0.25

Laboratory-scale on RAS

Fresh RAS 2.47 ± 0.03

Sonicated RAS 3.34 ± 0.40

Laboratory-scale on Pure culture

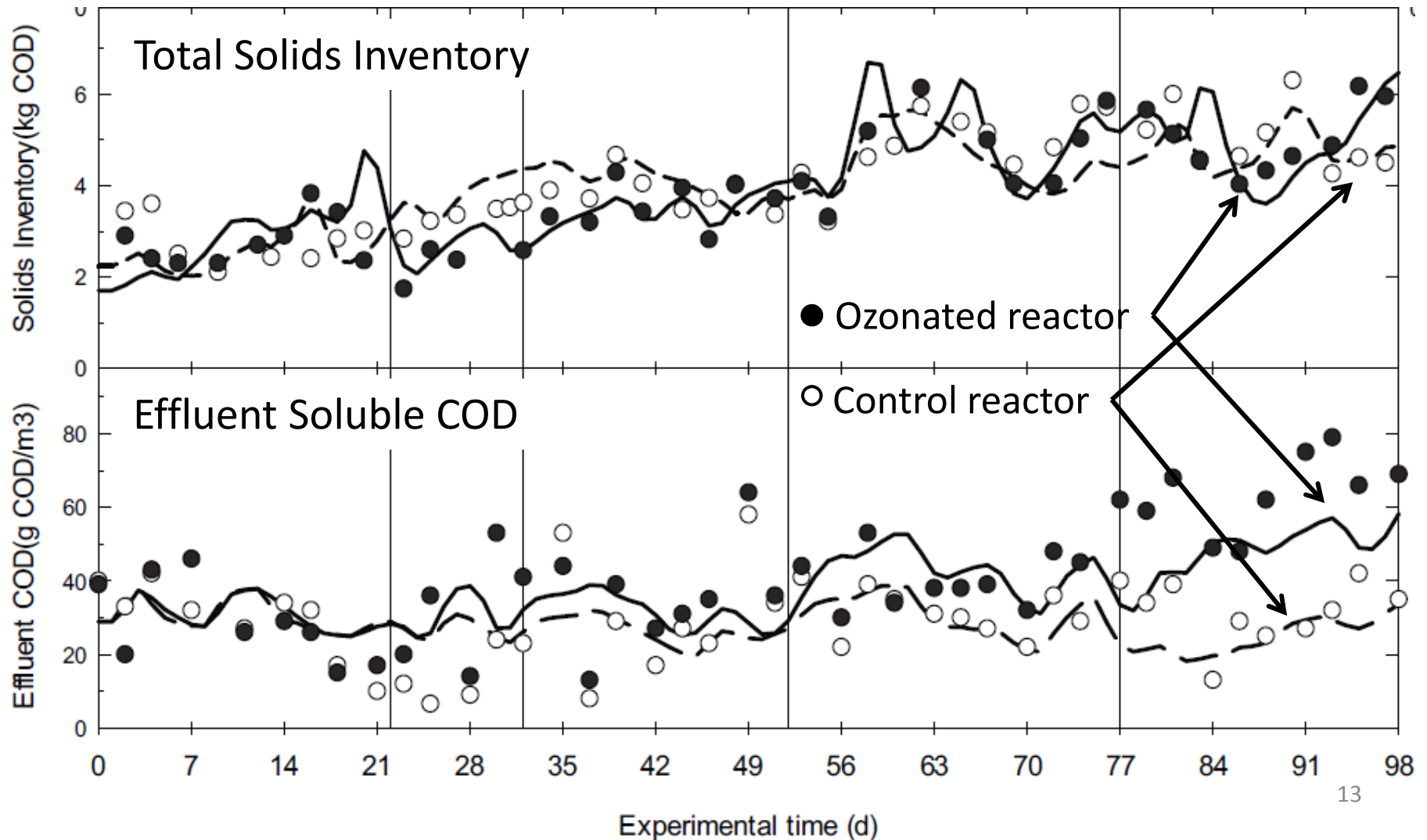
Average of four pure cultures<sup>a</sup> 1.48 ± 0.37

# 3 Pilot-Scale Experiments (3-5 months each)

	Aeration +Ozonated Reactor Control Rule	SRT (day)	Ozone Dose $\left( \frac{\text{g-O}_3}{\text{kg-VSS Inventory}\cdot\text{day}} \right)$	Biosolids Reduction
Year 1	Aerobic +Constant MLVSS	6	0 to 6.5	0 to 46%
Year 2	Aerobic +Constant SRT	6	10.3	53%
Year 3				
Phase 1	• Anoxic/Aerobic	• 12	• 7.3	• 22%
Phase 2	• Aerobic	• 12	• 8.9	• 19%
Phase 3	• Aerobic +Constant MLVSS	• 6	• 11.4 (lower COD solubilization)	• 18%

# Year 1 – Calibration of Model

- Independent calibration of inactivation parameters
- Fitting of inventory with transformation parameters.
- Good fit of the observed state variable.



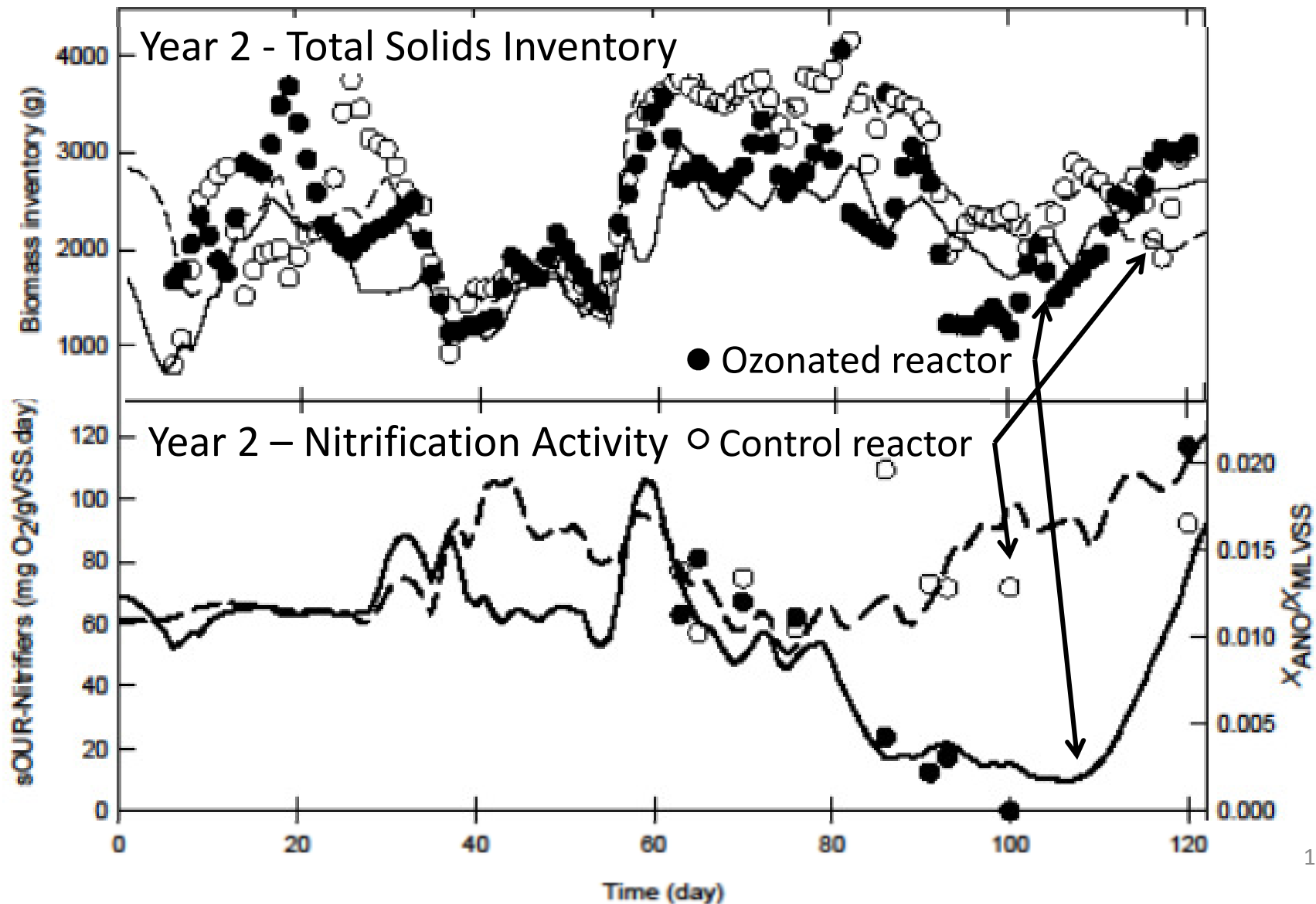
# Improvements in State-Variables' Predictions for Different Descriptions of Inactivation

Inactivation	Linear	Exponential	Exponential
<b>Fractions: Inactivation vs. Transformation</b>	Same	Same	Independent
<b>Predicted State-Variables Relative Squared Errors</b>			
Biosolids inventory <sup>a</sup> [%]	23.3	22.0	21.8
Soluble undegradable ( $S_U$ ) <sup>b</sup> [%]	19.5	14.0	12.0
Soluble biodegradable ( $S_B$ ) <sup>b</sup> [%]	27.9	25.9	20.5
Nitrate ( $S_{NO_3}$ ) [%]	23.8	21.8	20.1

## Conclusions

- Exponential inactivation works better
- Inactivation solubilizes <10% of cellular COD

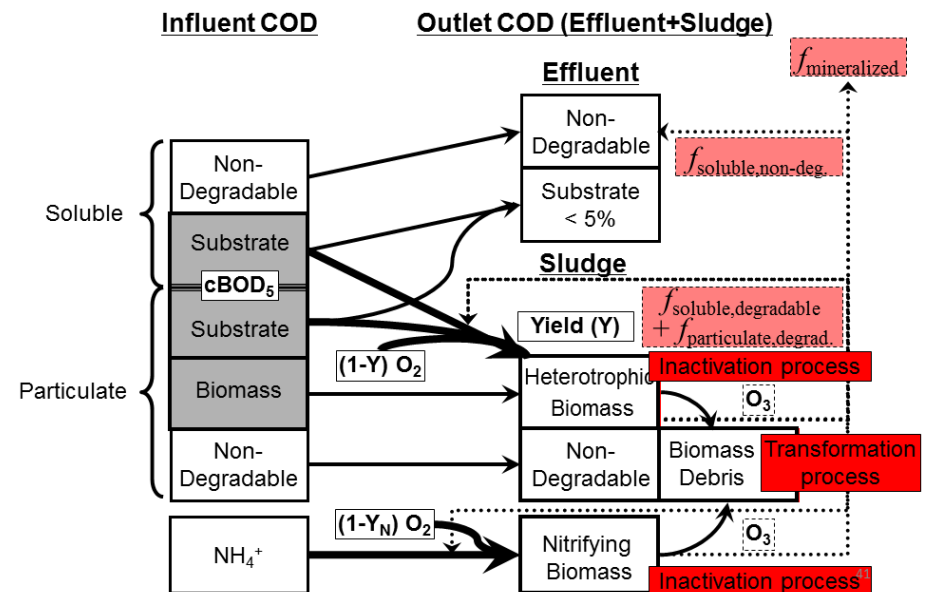
# Calibrated Parameters of Year 1 Satisfactorily Predicted Year 2 and Year 3 Observations



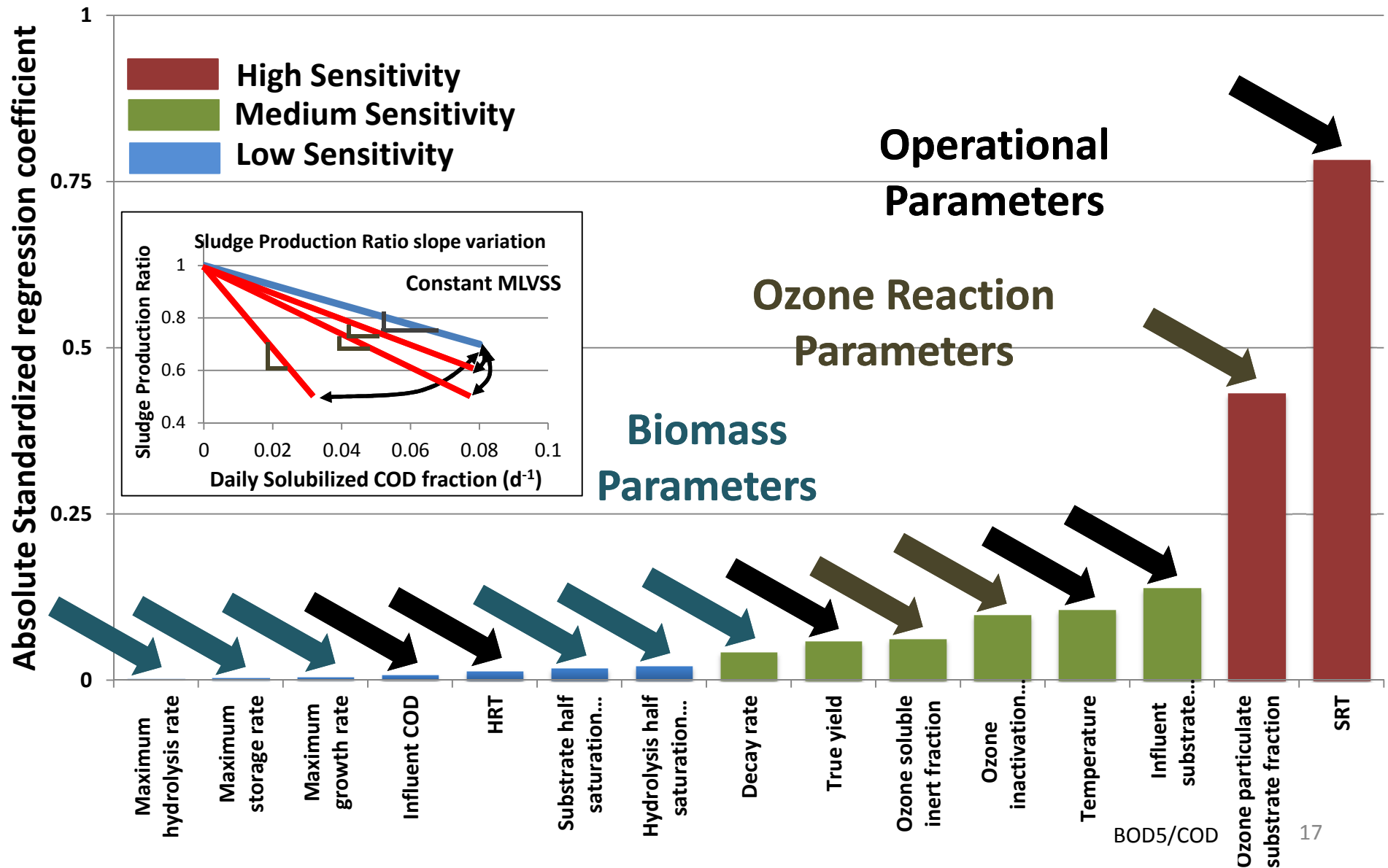


# Model Global Sensitivity Analysis

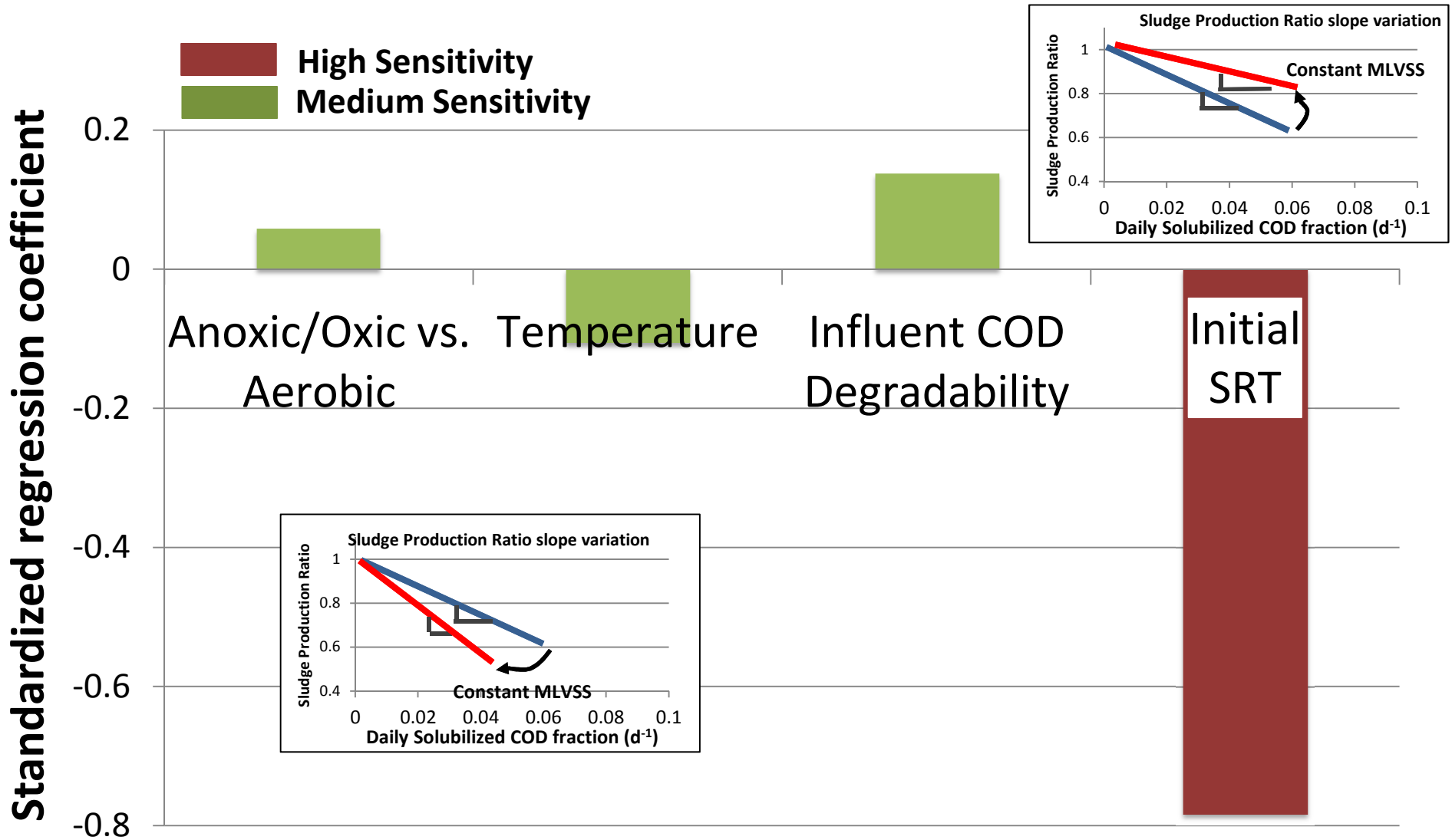
- Trends in biosolids reduction performance
- Generate implementation guideline



# Sensitivity of Biosolids Reduction to Model and Operation Parameters



# Operation Parameters Most Influential of Biosolids Reduction

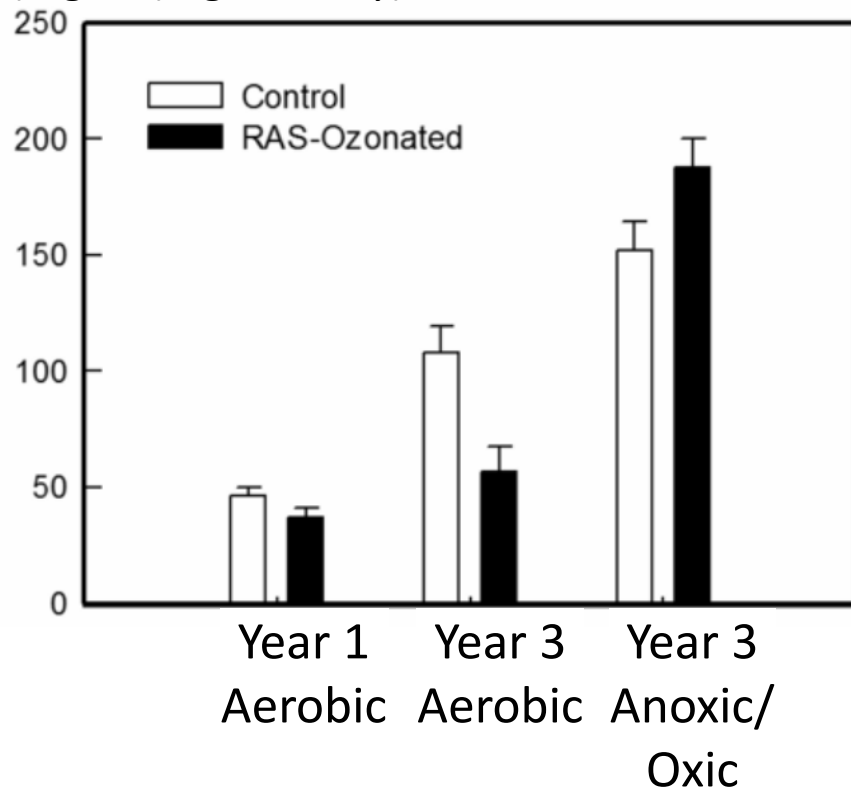




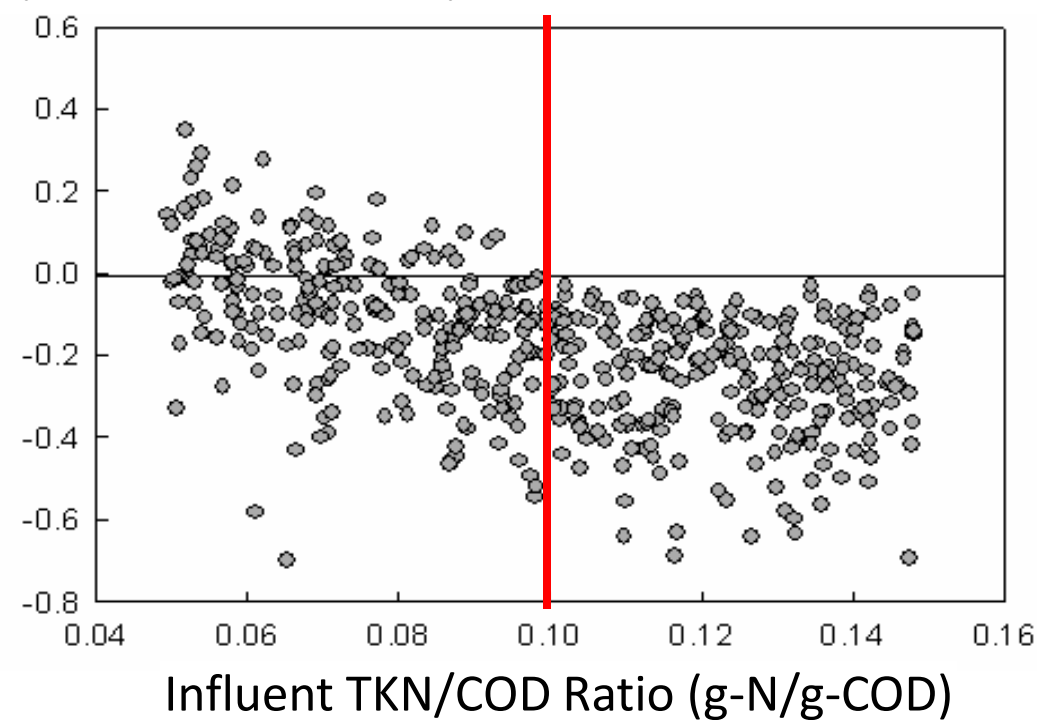
# Change in Specific Nitrification Rates

- Anoxic/Oxic conditions less detrimental than fully aerobic
- Specific nitrification rates can increase in some cases:  
influent TKN/COD < 0.1 g-N/g-COD

Specific Nitrification Rate  
(mg-N/(mg-VSS·day))

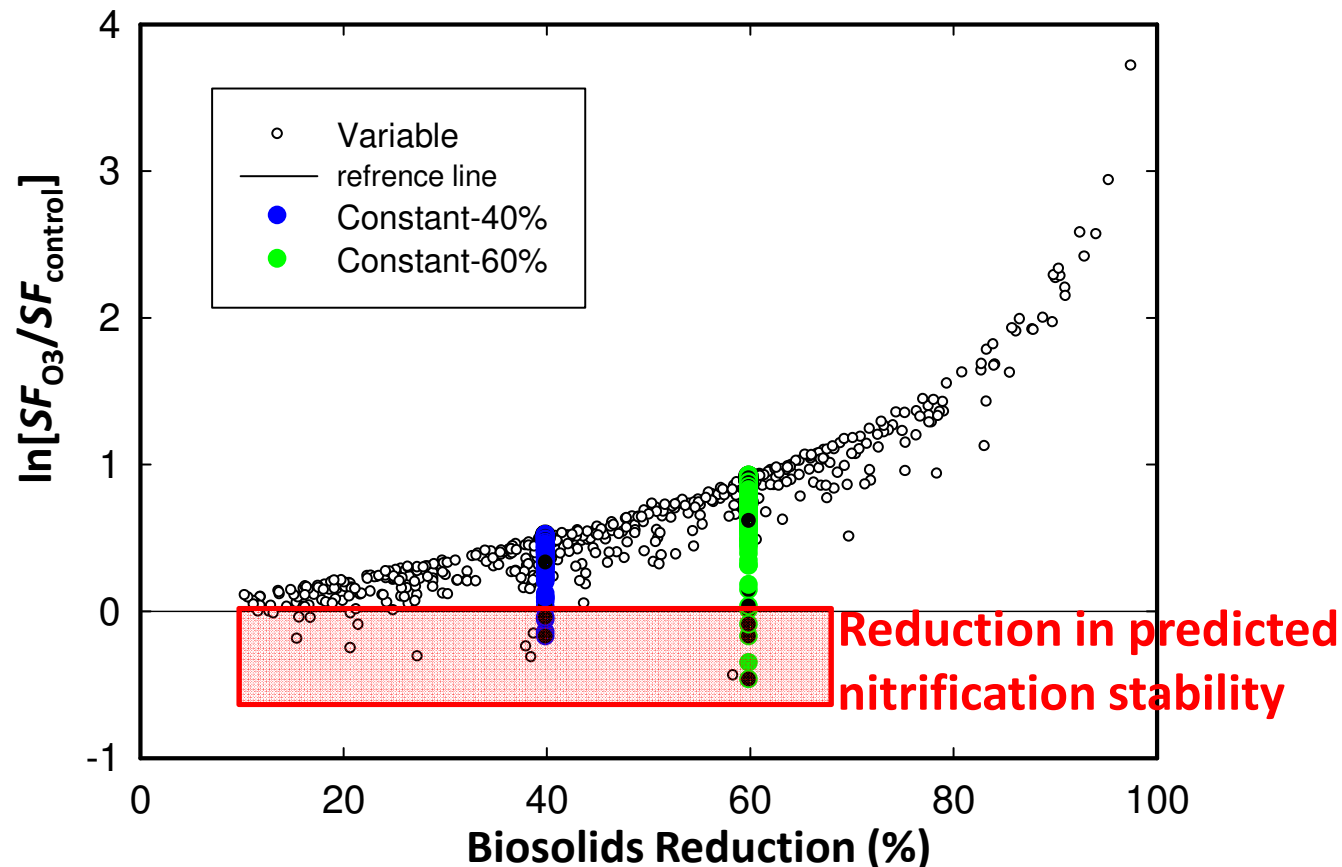


Change in Specific Nitrification Rates  
(ln[Ozonated/Control])

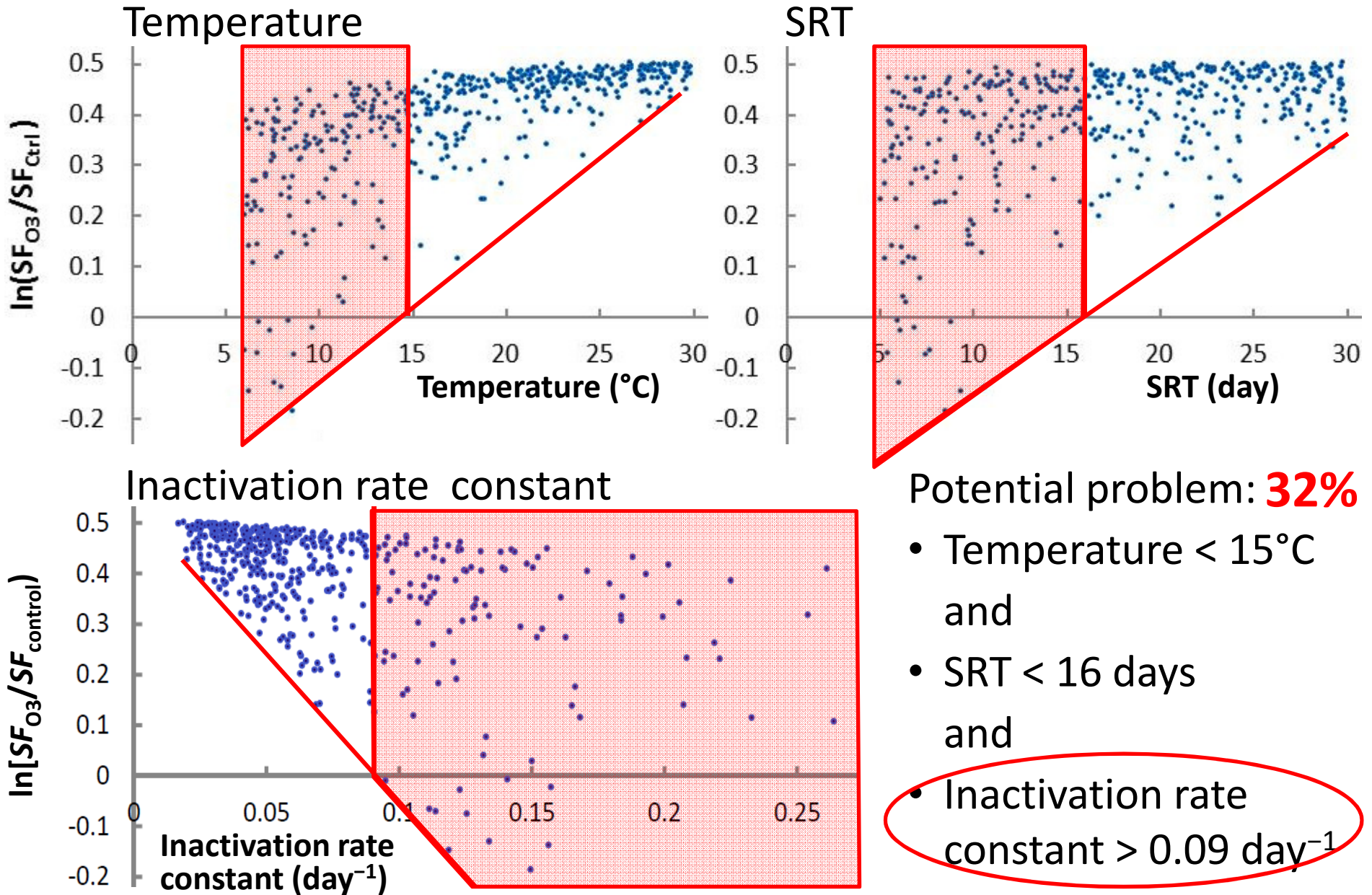


# Operation Conditions Threatening Nitrification

- Safety Factor ( $SF$ ) =  $SRT_{\text{operation}}/SRT_{\text{min}}$   
 $SRT_{\text{min of nitrifiers}} = (\mu_{\text{ANO,max}} - b_{\text{ANO}} - b_{\text{ANO,O3}})^{-1}$
- 3 simulation studies of 1,500 simulations:  
variable reductions, 40% and 60% reduction
- Lower sludge reduction shows higher risk



# Operation Conditions Threatening Nitrification (Constant 40% Biosolids Reduction)



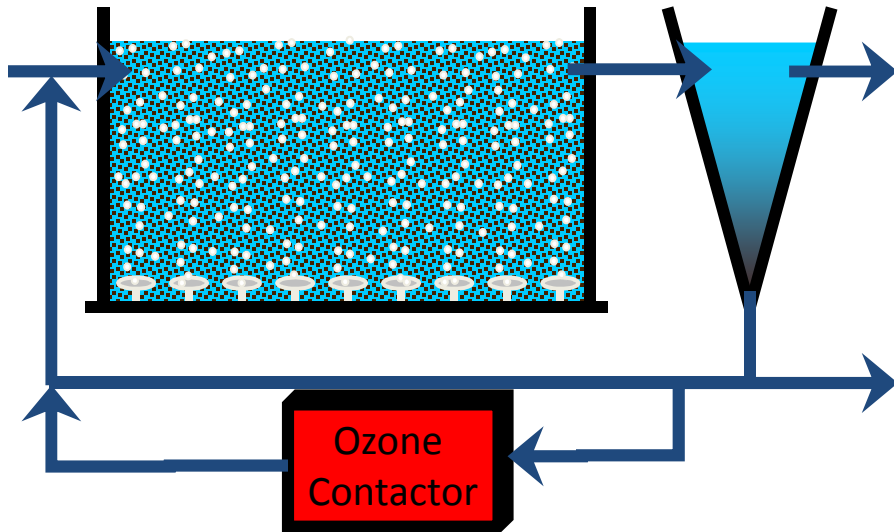
Potential problem: **32%**

- Temperature  $< 15^{\circ}C$   
and

- SRT  $< 16$  days  
and

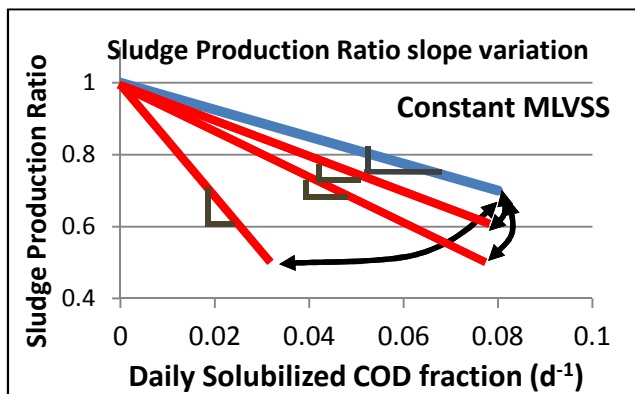
- Inactivation rate constant  $> 0.09\ day^{-1}$

# How to minimize inactivation rate?

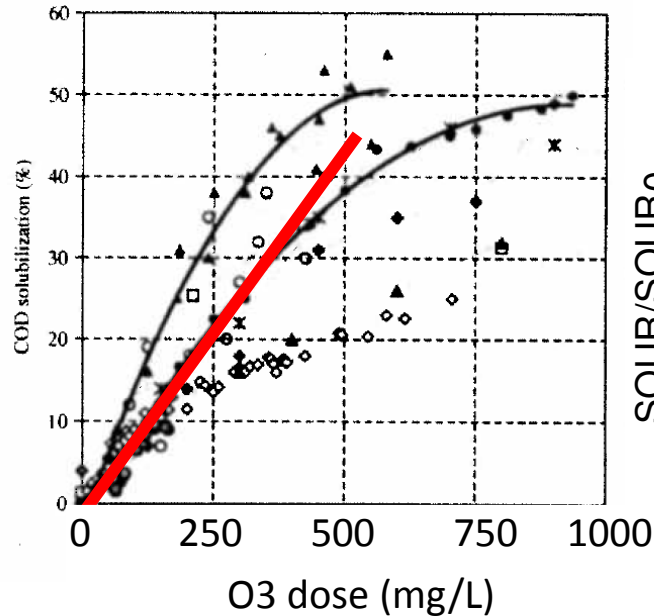


- Biosolids production is function of overall daily solubilization
- Overall daily solubilization:
  - Solubilization in contactation
  - Proportion of inventory treated
- Same factors for overall inactivation
  - Minimize proportion of inventory

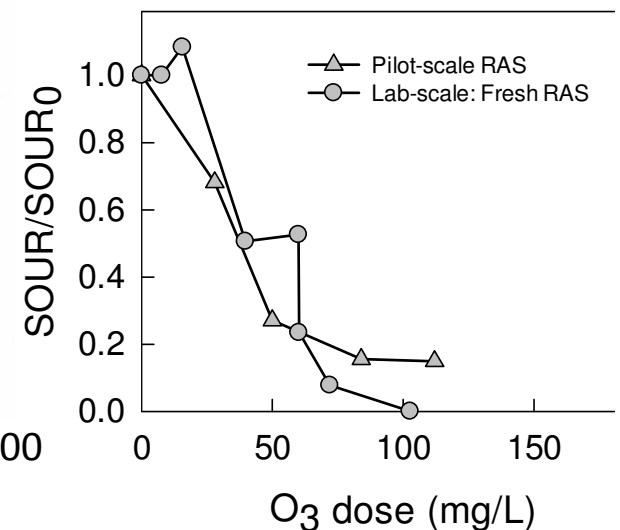
Biosolids Production vs. Overall Solubilization



Solubilization in Contactor



Inactivation in Contactor





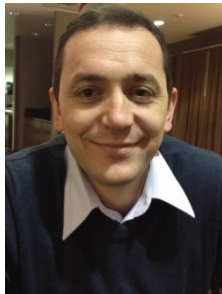
# Conclusion

- Bioprocess conditions influence greatly performance of RAS-ozonation units for biosolids reduction.
- Developed a model capable of predicting performance based on inactivation and COD solubilization.
- Nitrification stability is generally enhanced.
- Nitrification can be negatively impacted at lower temperature, SRT and higher overall inactivation.
  - Contactor operation can be adjusted to alleviate problems.

# Acknowledgements

- Students

Overall Operation



Siavash  
Isazadeh  
PhD



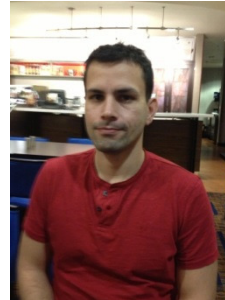
Pinar  
Ozcer  
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Inactivation



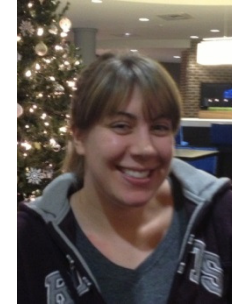
Min  
Feng  
MEng

Sensitivity



Luis  
Urbina Rivas  
MEng

Lab-scale reactors



Theresa  
Luby  
MEng



Shameem  
Jaffur  
MEng

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