

Summer 6-4-2012

Development of Microbial Cell factories for Production of Biofuels and Bio-based Chemicals through Consolidated Bioprocessing

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Akihiko Kondo, "Development of Microbial Cell factories for Production of Biofuels and Bio-based Chemicals through Consolidated Bioprocessing" in "Metabolic Engineering IX", E. Heinzle, Saarland Univ.; P. Soucaille, INSA; G. Whited, Danisco Eds, ECI Symposium Series, (2013). http://dc.engconfintl.org/metabolic_ix/4

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Metabolic engineering IX

June 3-7, 2012

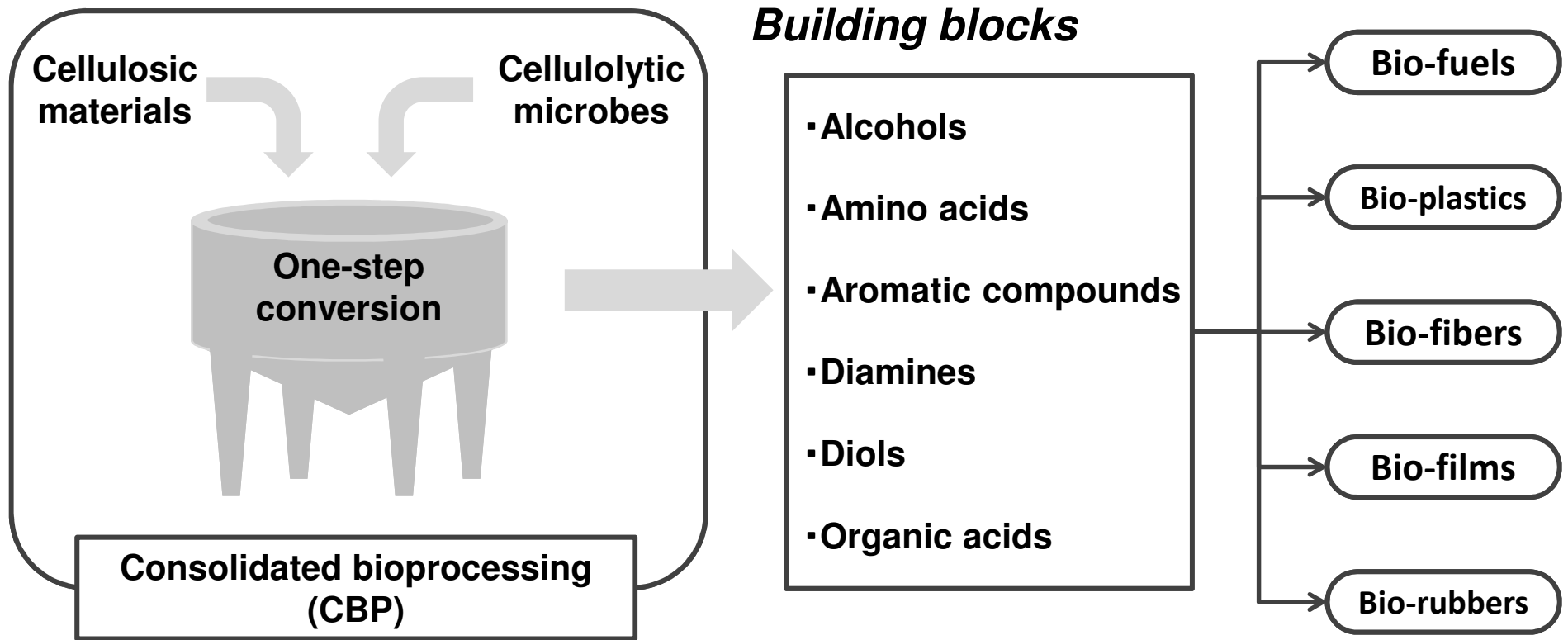


Development of microbial cell factories for production of biofuels and bio-based chemicals through consolidated bioprocessing



Kobe University
Professor, Department of Chemical Science and Engineering
Director, Biorefinery Center
RIKEN Institute, Team Leader, BMEP,
Akihiko Kondo

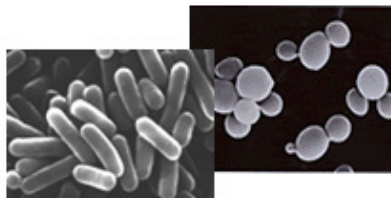
Bio-refinery through CBP



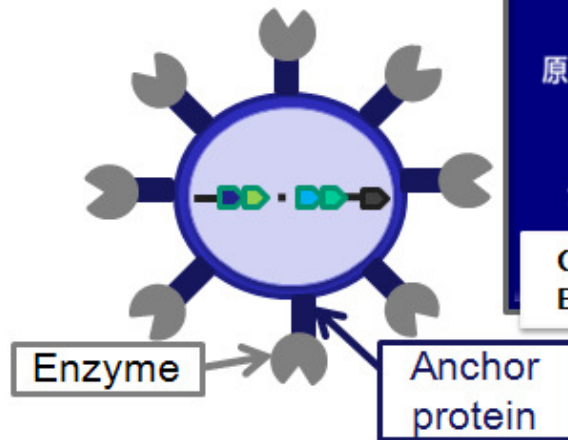
Ishii J, Poster 37 : Isobutanol production

Cell-surface Engineering

Biomass degradation potential



Arming yeast



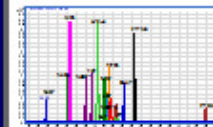
Synthetic Bio-engineering

Development of metabolic pathway



In silico metabolic simulation

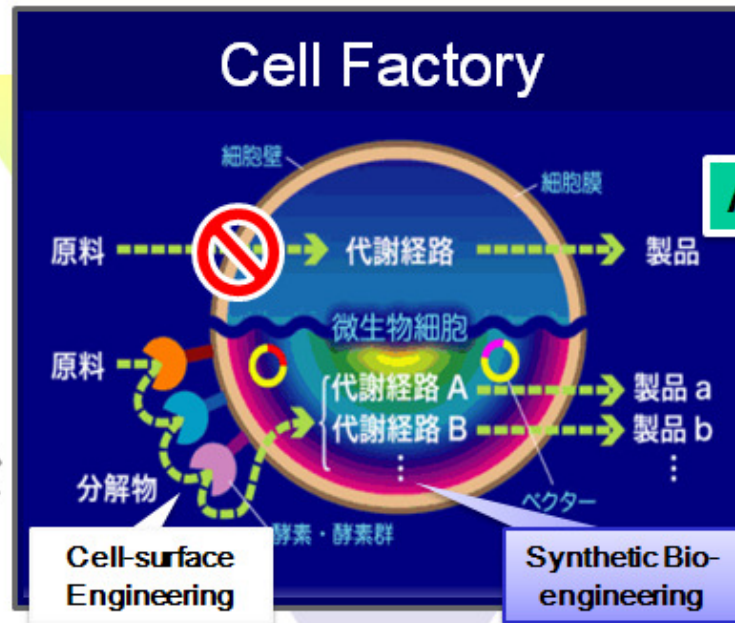
*Design of metabolic pathway
Proposing of mutation strategy*



DNA array GC-MS CE-MS

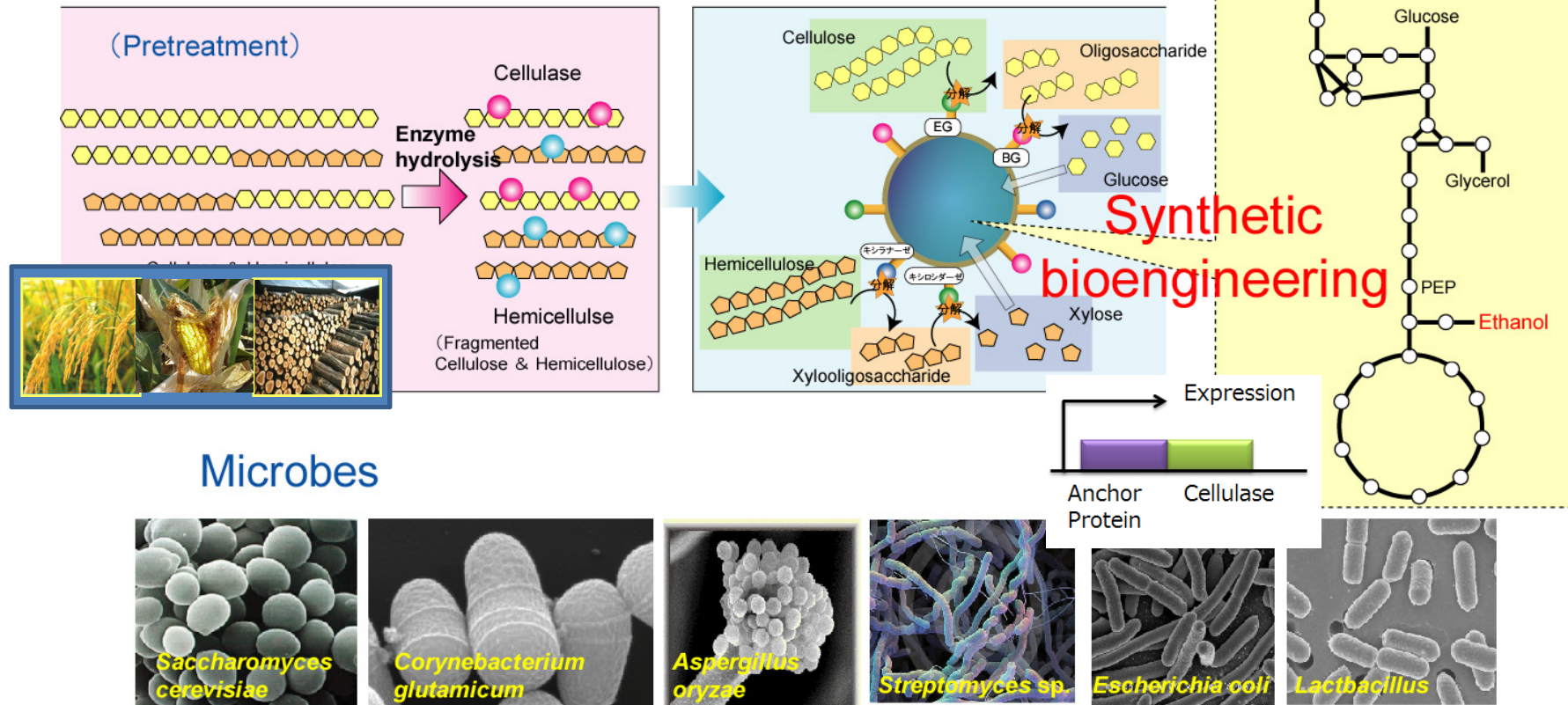
Multi-omics analysis

Simultaneous analysis of cell component



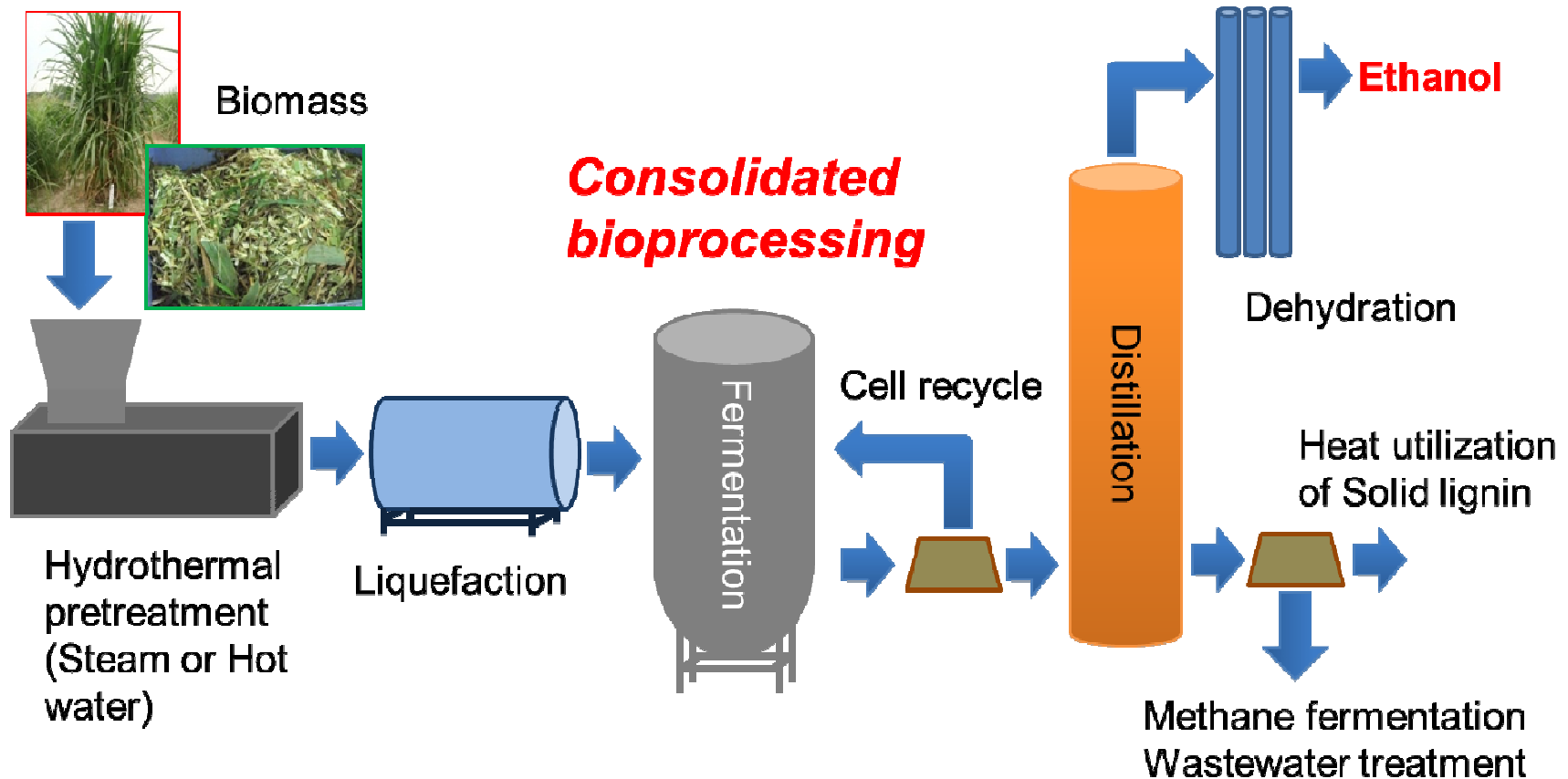
Breeding of **super microbial cells (cell factory)** for direct production of fuels and chemicals from biomass

Cell surface engineering (Consolidated bioprocessing)



A combination of cell surface engineering and synthetic bioengineering will be a very effective approach to develop cells with novel metabolic ability for industrial applications.

Environmentally benign and consolidated process



Bench-scale plant in Kobe University



50 kg/h presser



100 kg/batch steamer



100 L
liquefaction reactor



50 L fermentation reactor

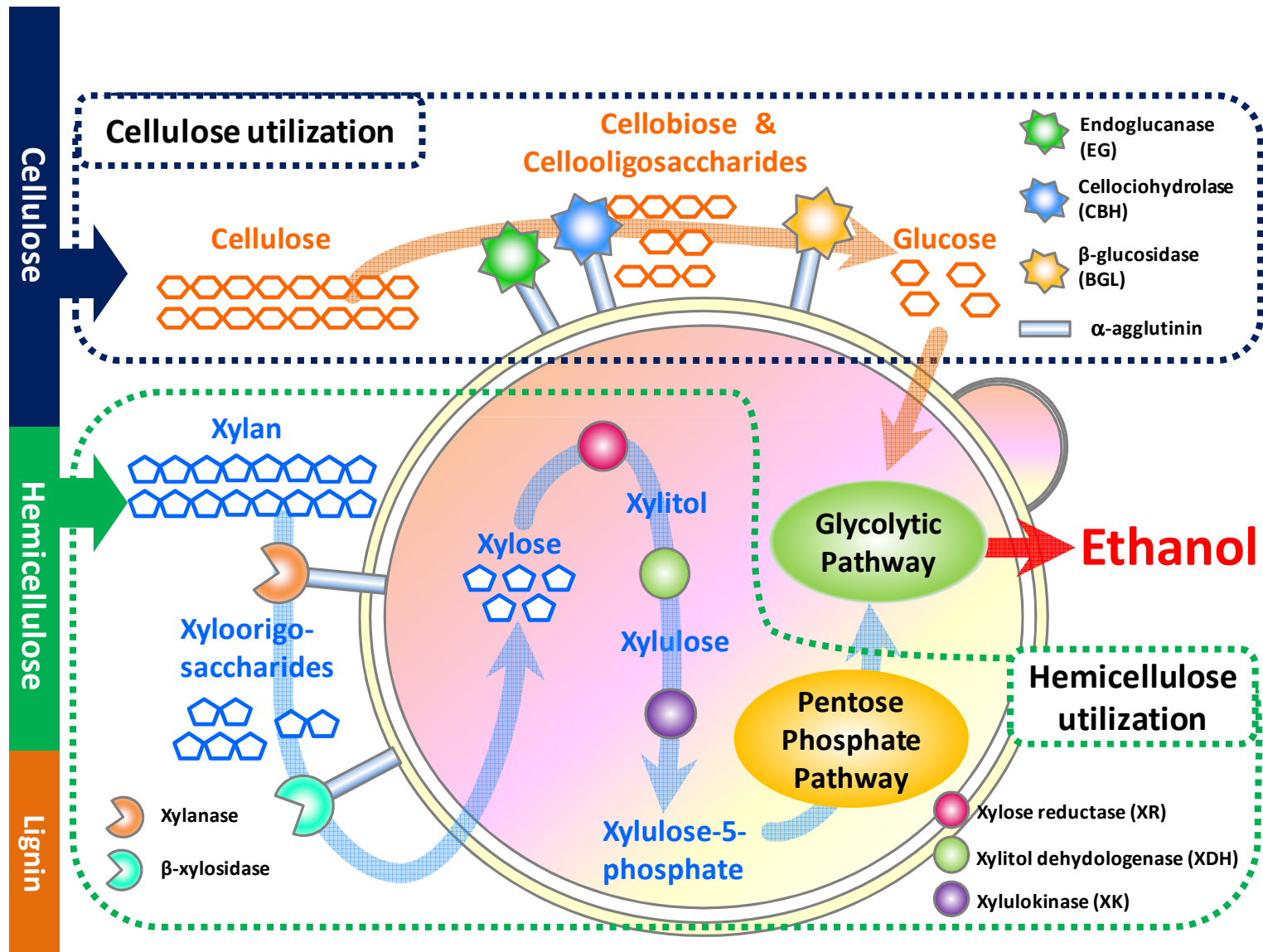


30 L fermentation reactor (x3)



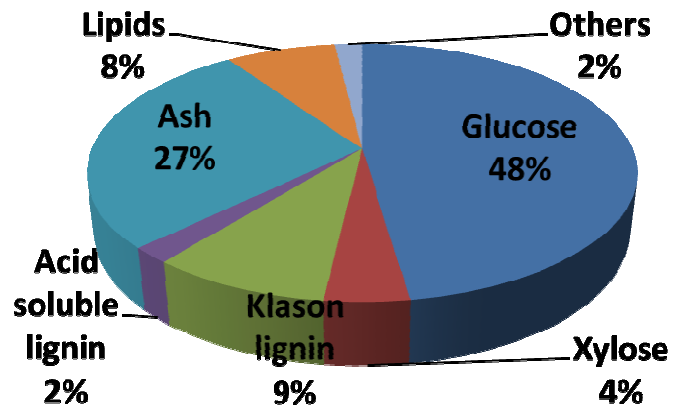
Cell recycling system

Arming Yeast for CBP



Ethanol production from lignocellulosic biomass

Composition of C6 fraction



Rice straw

Liquid hot water treatment

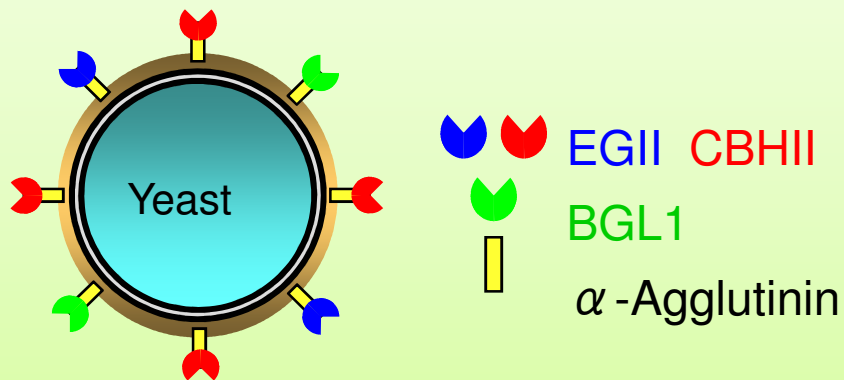


C6 fraction
(Water insoluble)



C5 fraction
(Water soluble)

Yeast cells co-displaying BGL1, EGII and CBHII



Ethanol production from high-solid biomass

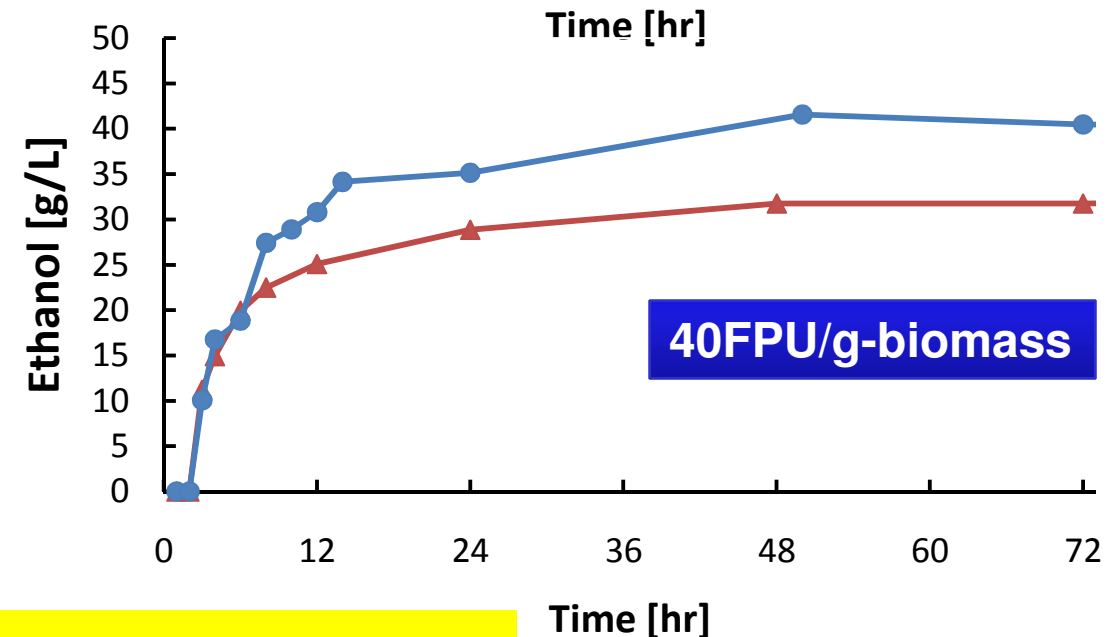
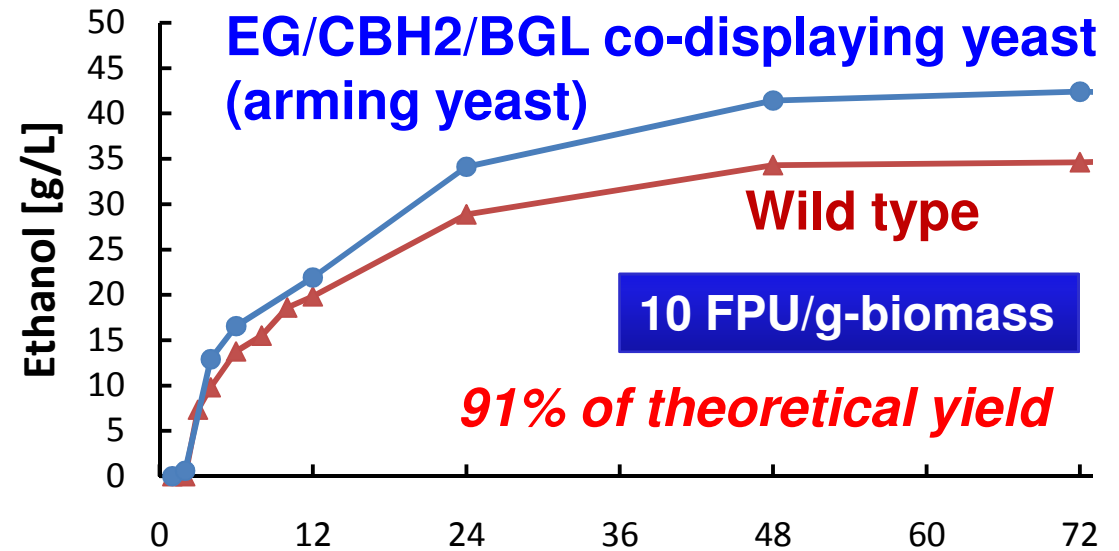
Liquefaction of pretreated rice straw at **50 °C for 2h**



Initial biomass; **200 g/L**
Cellulase; **10 -40 FPU/g-biomass**

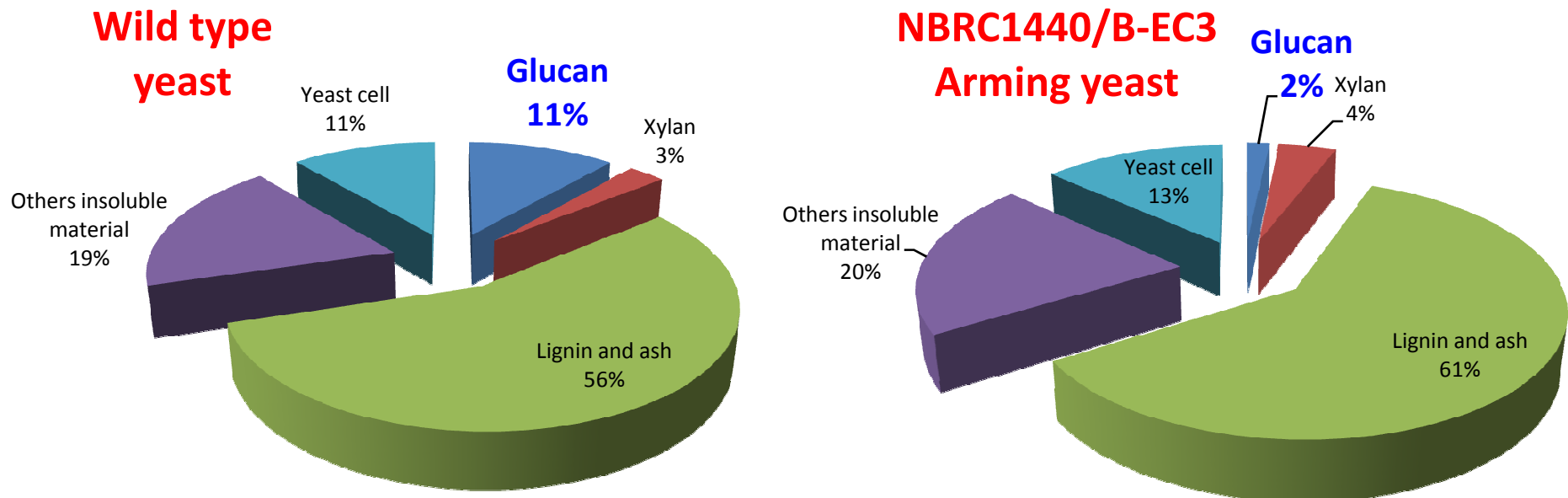


Fermentation at **35 °C**



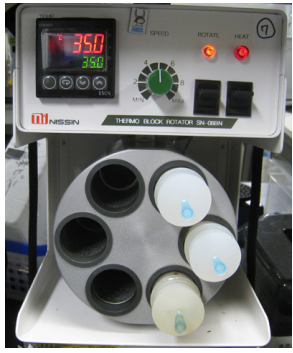
Ethanol production from high-solid biomass

Residue after high-solid fermentation



Cellulases displayed on the yeast cell surface hydrolyzed cellulose that was not hydrolyzed by commercial cellulases, leading to increased ethanol production.

Cell recycle fermentation of high-solid biomass



Initial biomass ; 200 g/L
Liquefaction; 2 h, 50°C
Cellulase added; 10 FPU/g-biomass



Fermentation mixture

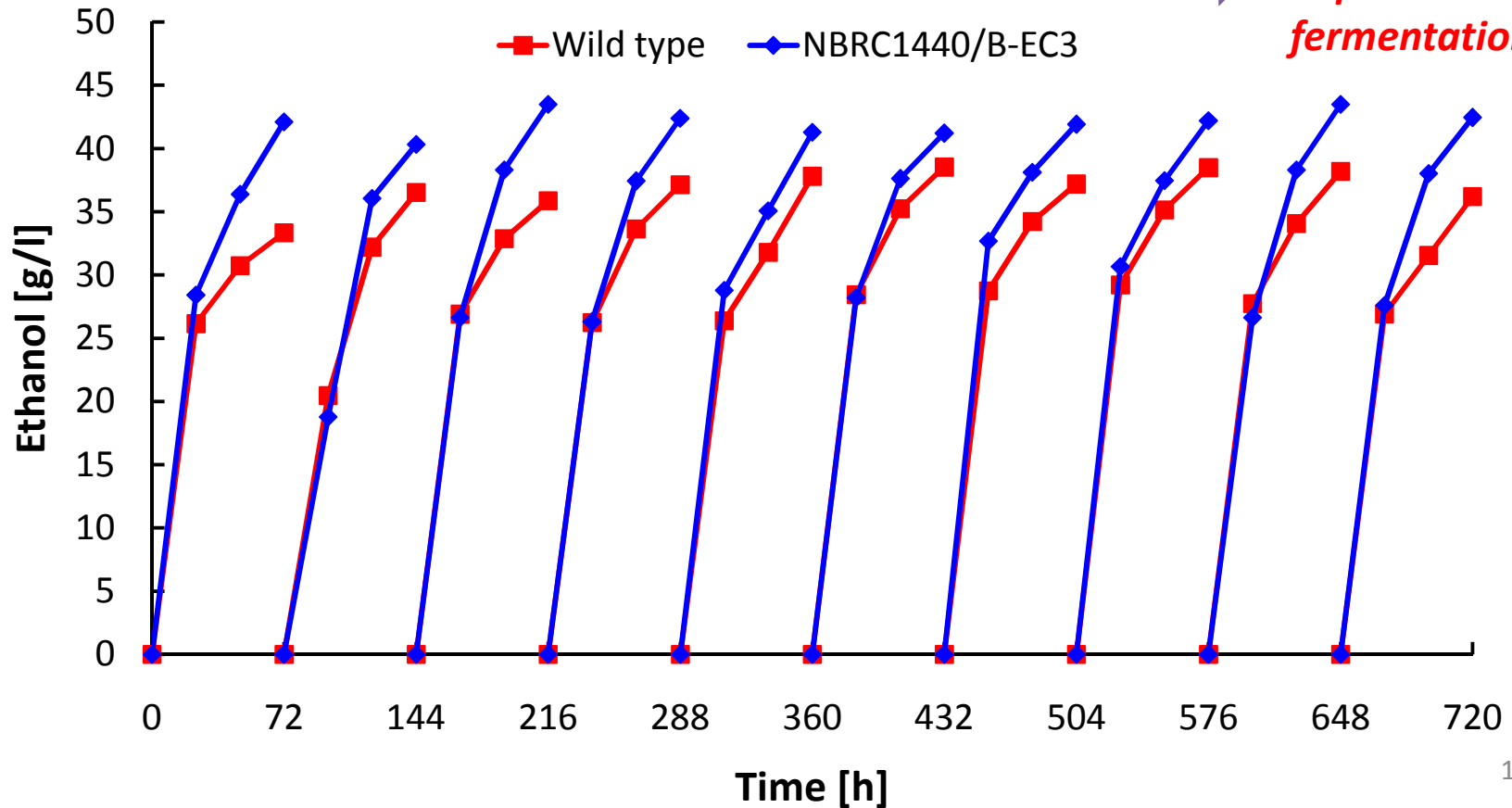
↻ Centrifugation at 20 x g

Supernatant

↻ Centrifugation at 6,000 x g

pellet

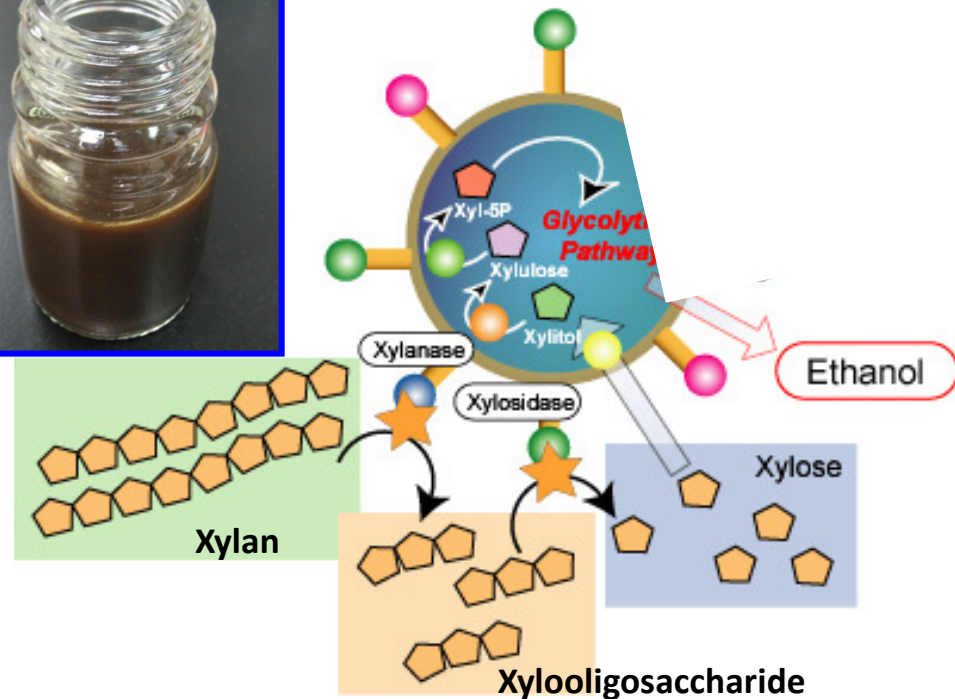
➔ *Repeated
fermentation*



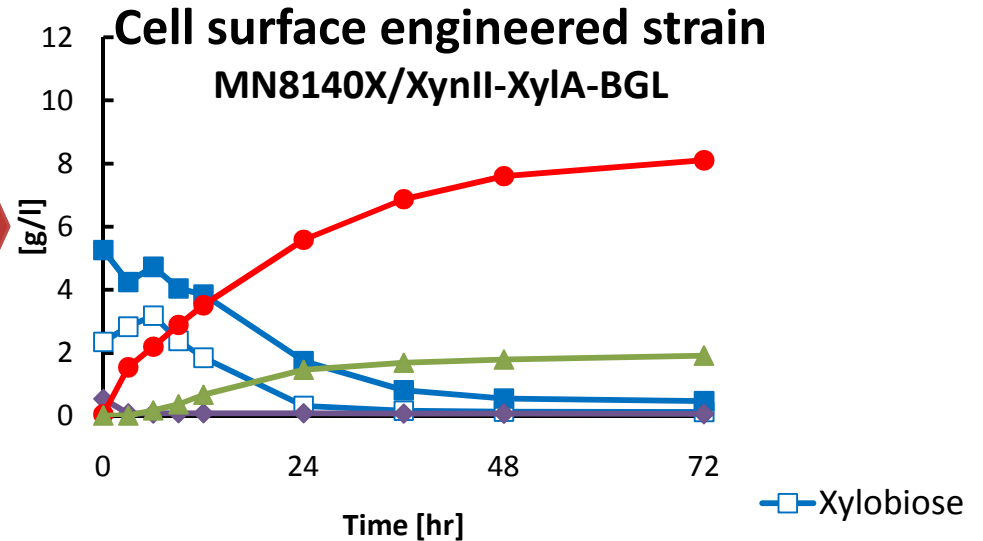
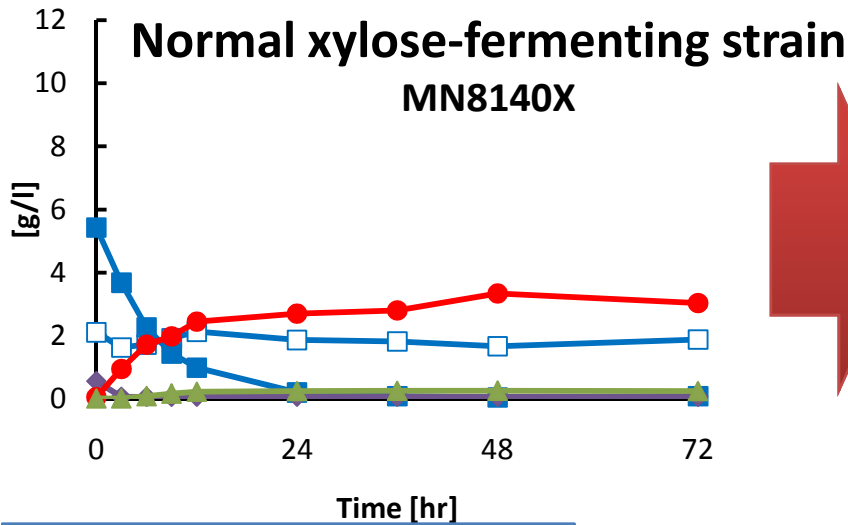
Fermentation of **C5 fraction** of rice straw obtained by hydrothermal pretreatment

Oligosacchrides	
Xylose [g/L]	4.19
Xylobiose [g/L]	1.69
Xylotriose [g/L]	15.77
Xylotetraose [g/L]	1.10
Xylopentaose [g/L]	0.013
Xylohexaose [g/L]	0.111
Glucose [g/L]	0.036
Cellobiose [g/L]	0.002
Cellotriose [g/L]	0.019
Cellotetraose [g/L]	0
Total oligosaccharide [g/L]	9.62
Total sugar [g/L]*	38.12

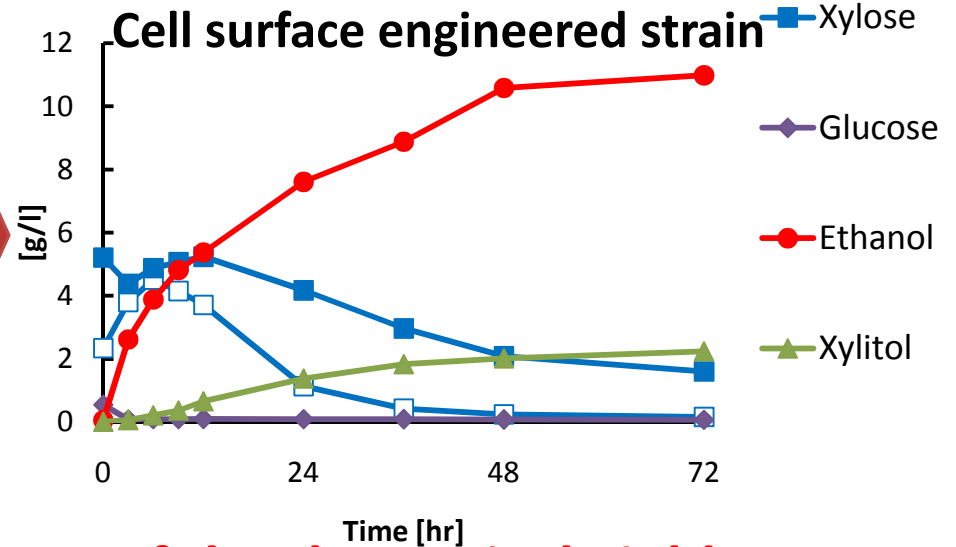
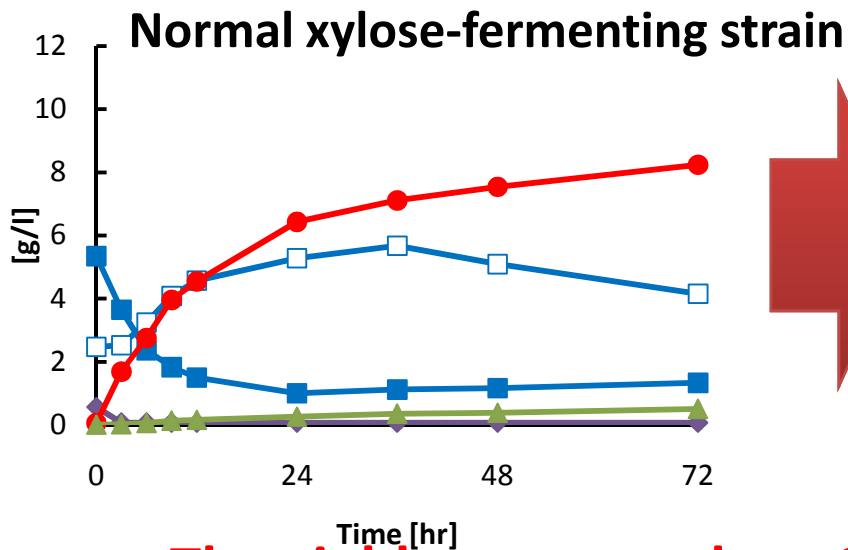
Inhibitors	
Acetate [mM]	46.2
Formate [mM]	28.1
Furfural [mM]	15.77
5-HMF [mM]	1.10



Fermentation of hemicellulosic hydrolysate



0.02 % (w/v) Hemicellulase

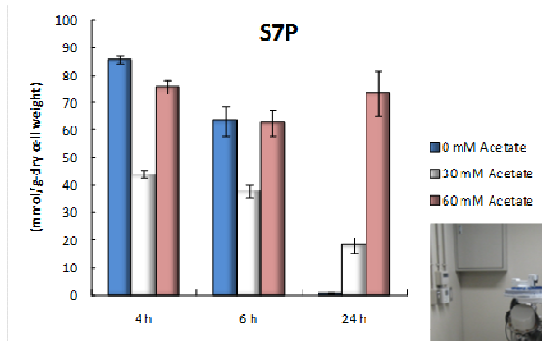


The yield corresponds to 82.1% of the theoretical yield.

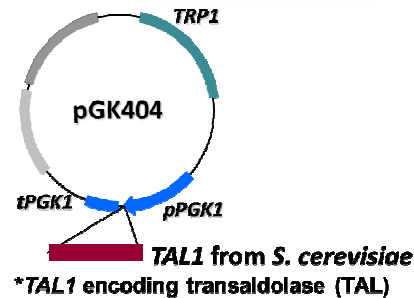
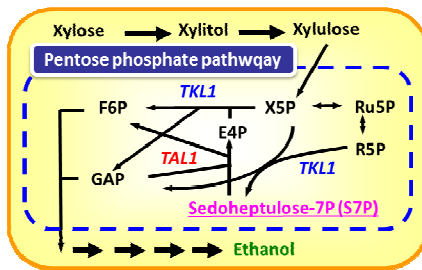
Sakamoto et al. (2011) *J Biotechnol*

Several approaches to improve tolerance

Overexpression of TAL1 and FDH



Metabolomic approach

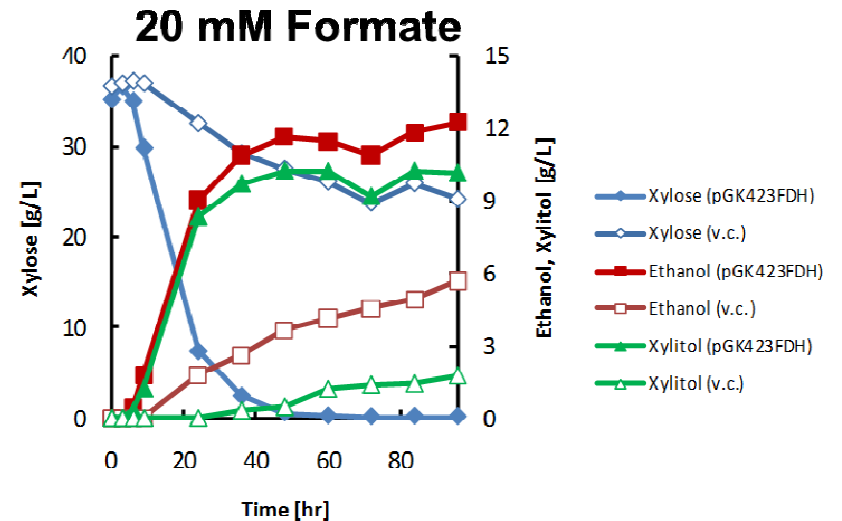
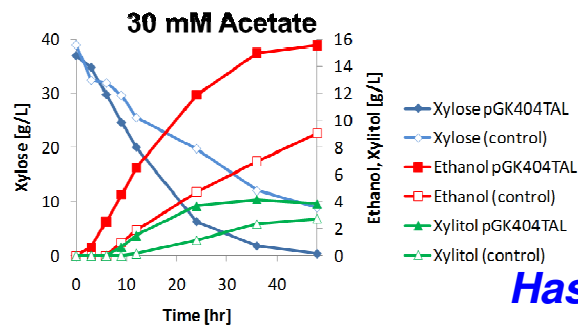
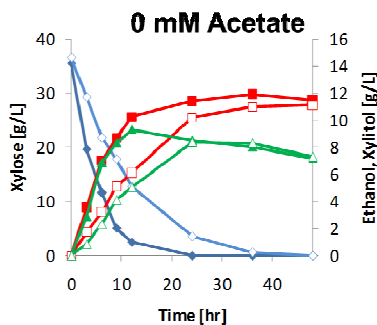


Transcriptomic approach



Formate-responsive genes

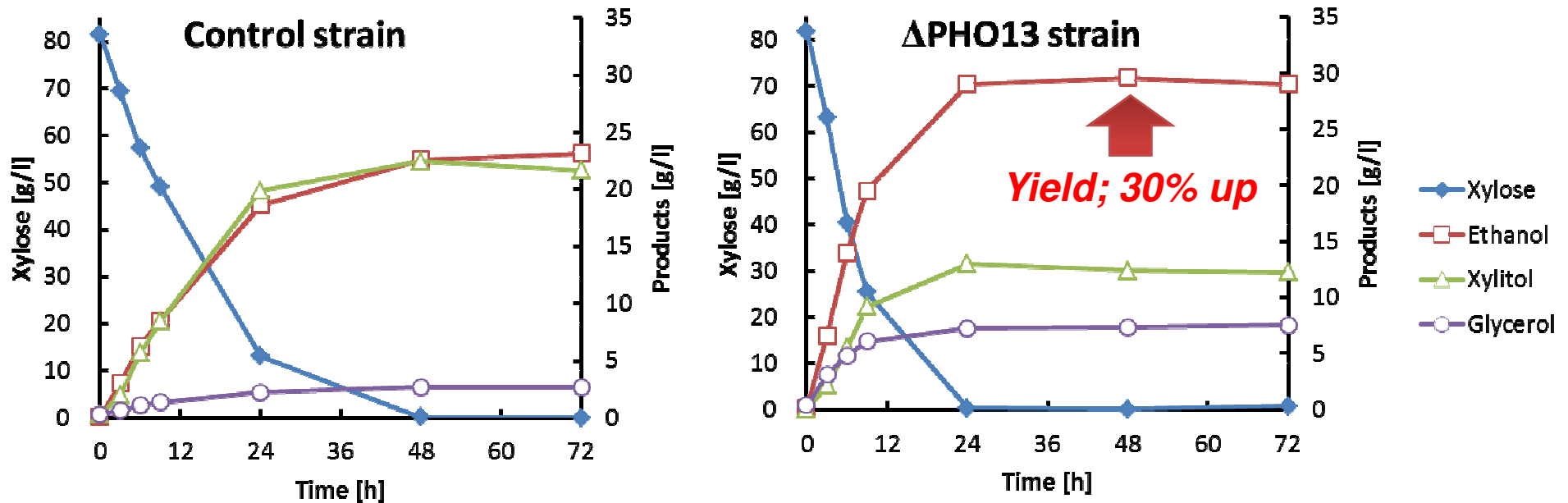
Gene	Relative mRNA expression				Description
	0 mM	5 mM	10 mM	15 mM	
<i>FDH1</i>	1	2.05	8.62	23.09	formate dehydrogenase (FDH)
<i>BAT1</i>	1	1.53	2.81	7.22	BCAA aminotransferase
<i>ALD5</i>	1	1.66	2.45	5.07	aldehyde dehydrogenase
<i>HXK2</i>	1	1.37	1.94	2.79	hexokinase
<i>VCX1</i>	1	1.54	2.08	2.78	Ca ²⁺ ion transporter
<i>GPD2</i>	1	1.33	1.70	2.45	glycerol-3P dehydrogenase
<i>HXT4</i>	1	1.29	1.70	2.27	glucose transporter
<i>PFK2</i>	1	1.34	1.58	1.85	6-phosphofluctokinase



Hasunuma et al (2011) *Microb Cell Fact*
(2011) *Appl Microbiol Biotechnol*

Improvement of xylose fermentation

Effect of *PHO13* deletion on xylose fermentation



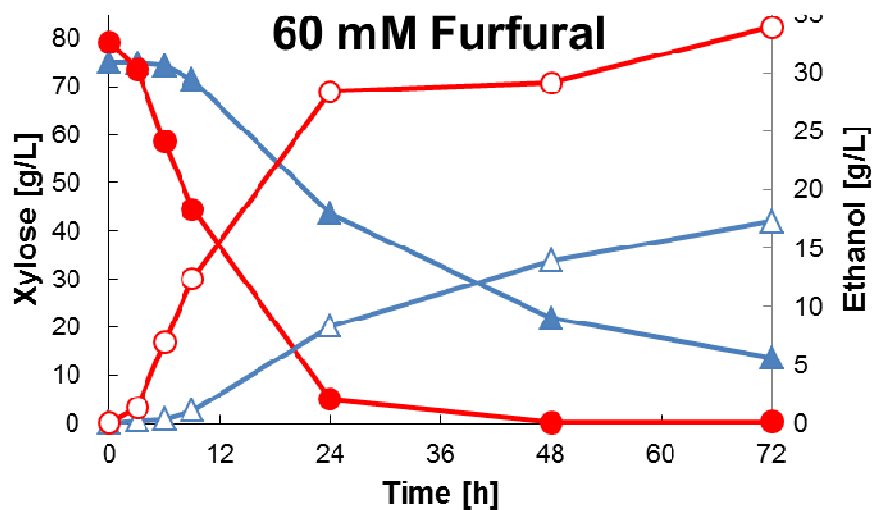
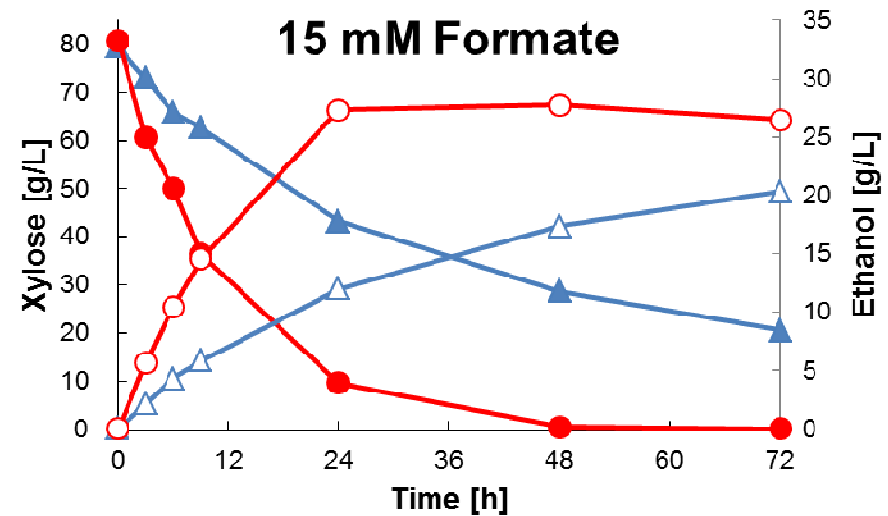
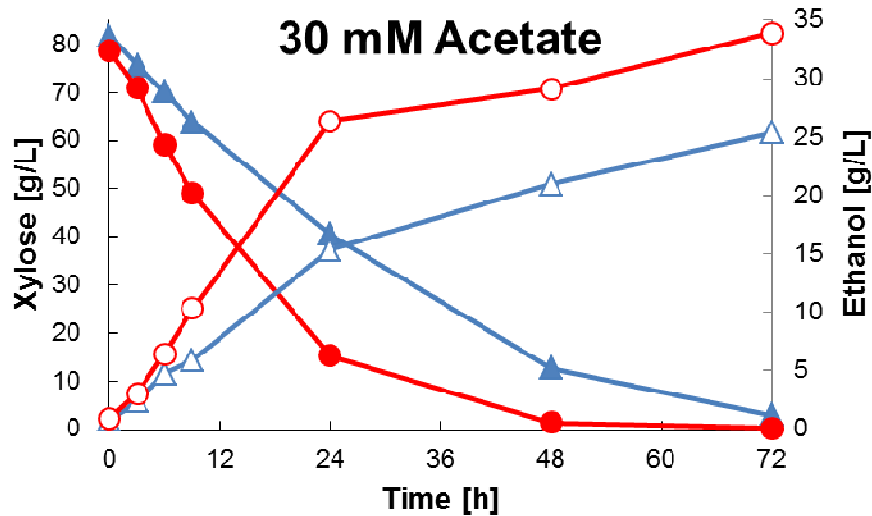
Hasunuma T, Poster12

Medium; YP, 80 g/l xylose
Condition; Oxygen limited
Temp; 30°C

Deletion of *p*-nitrophenyl phosphatase gene, *PHO13* in xylose-fermenting strain improved ethanol production from xylose

Effects of *PHO13* deletion on xylose fermentation

Improvement of xylose fermentation **in the presence of inhibitors** by *PHO13* deletion



—●— *PHO13*-deleted strain
—▲— Wild type

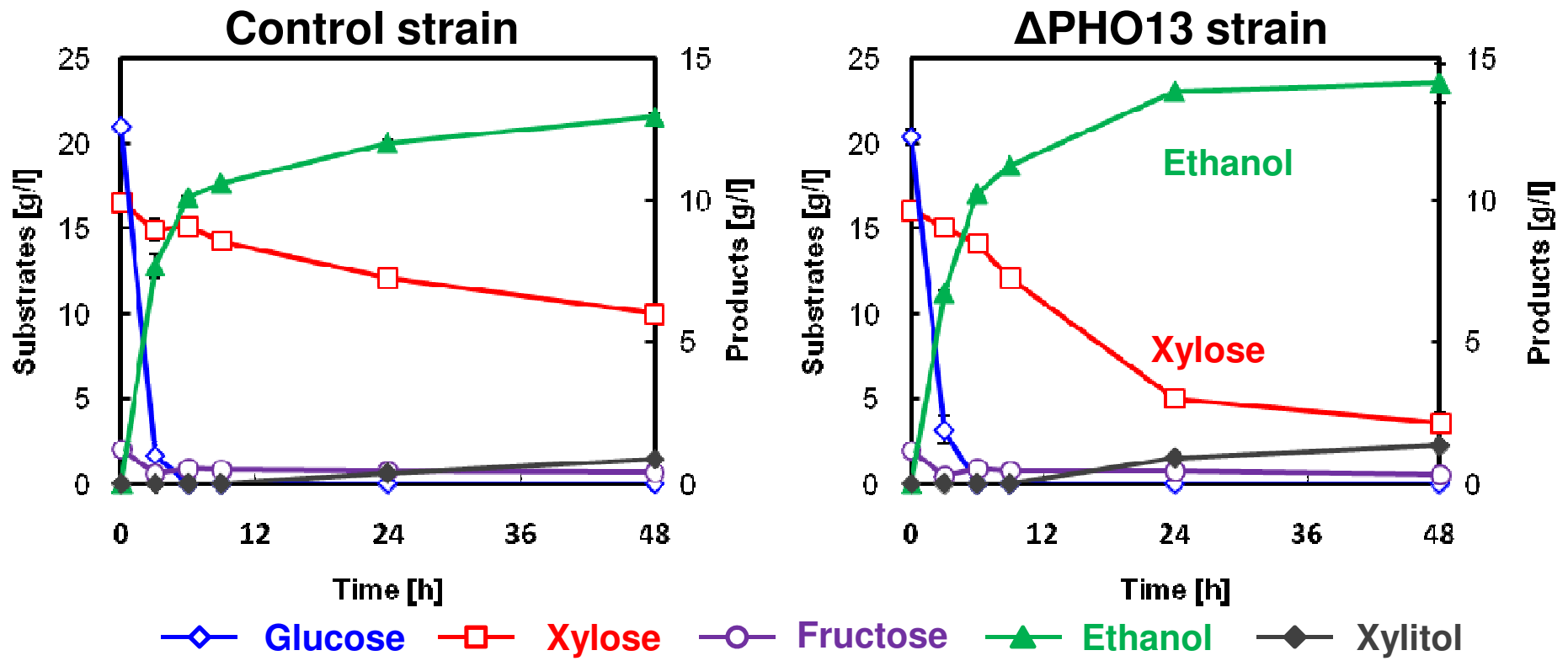
Medium; YP, 80 g/l xylose
Condition; Oxygen limited
Temp; 30°C

Effects of *PHO13* deletion on xylose fermentation



Fermentation Inhibitors

Acetate	3.23 g/L (53.9 mM)
Formate	1.08 g/L (23.4 mM)
Furfural	1.22 g/L (12.7 mM)



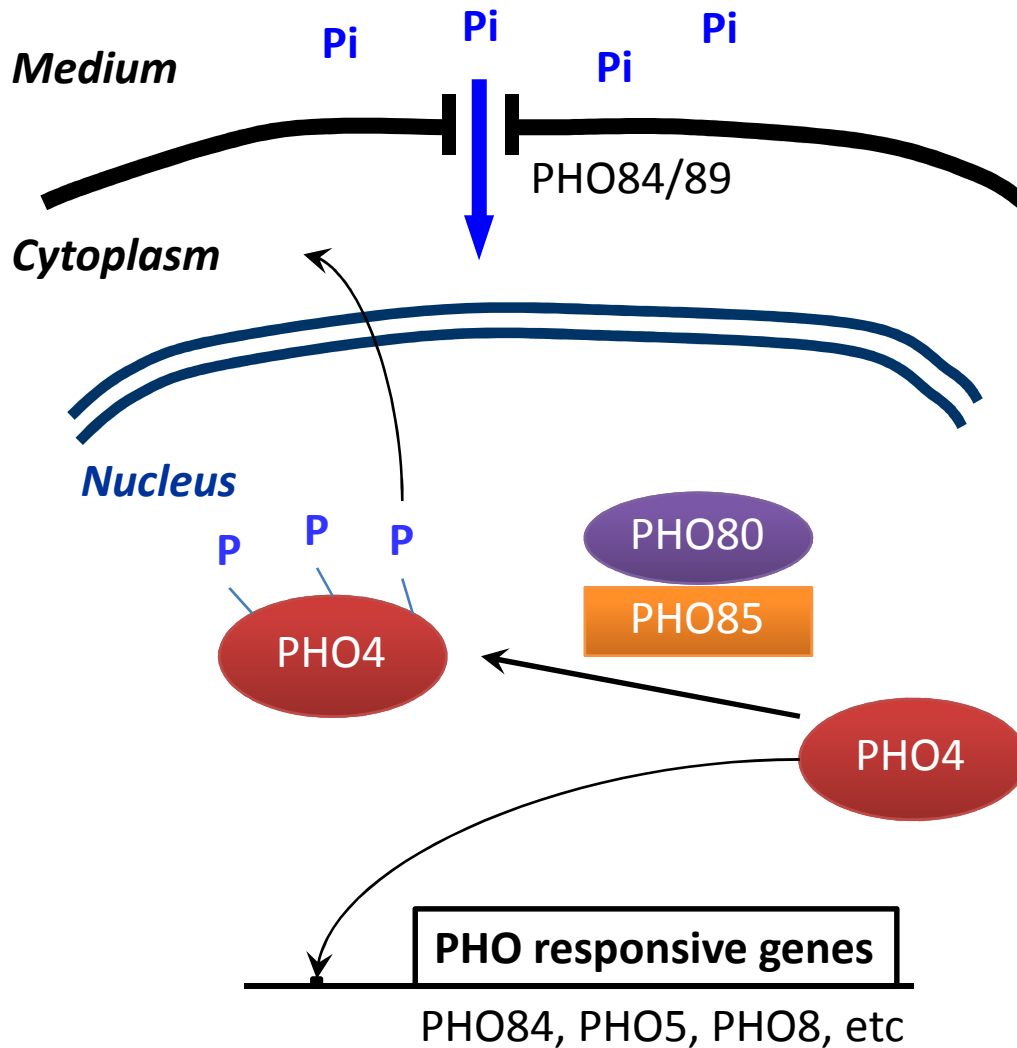
Global gene expression analysis of $\Delta PHO13$ mutant

Genes highly up- or down-regulated by deleting the *PHO13* gene from a xylose-fermenting recombinant *S. cerevisiae* strain

Gene	Category	Annotated function	Fold change
<i>ZWF1</i>	Metabolic pathway (Glycolysis, PPP, Alcohol biosynthesis)	Glucose-6-phosphate dehydrogenase	4.00
<i>SOL3</i>		6-phosphogluconolactonase	3.67
<i>GND1</i>		6-phosphogluconate dehydrogenase	1.64
<i>TKL1</i>		Transketolase	1.57
<i>PFK1</i>		Alpha subunit of heterooctameric phosphofructokinase involved in glycolysis	1.55
<i>TDH1</i>		Glyceraldehyde-3-phosphate dehydrogenase	1.48
<i>PDC1</i>		Major of three pyruvate decarboxylase isozymes	2.04
<i>ADH1</i>		Alcohol dehydrogenase	1.94
<i>GPD1</i>		NAD-dependent glycerol-3-phosphate dehydrogenase	1.64
<i>COX2</i>		Respiratory chain	Subunit II of cytochrome c oxidase
<i>COX3</i>	Subunit III of cytochrome c oxidase		0.30
<i>CYC1</i>	Cytochrome c		0.59
<i>QCR6</i>	Subunit 6 of the ubiquinol cytochrome-c reductase complex		0.57
<i>ATP1</i>	ATP synthase	Alpha subunit of the F1 sector of mitochondrial F1F0 ATP synthase	2.24
<i>ATP19</i>		Subunit k of the mitochondrial F1F0 ATP synthase	2.60
<i>ATP5</i>		Subunit 5 of the stator stalk of mitochondrial F1F0 ATP synthase	1.64

Phosphate responsive signaling pathway

The PHO system

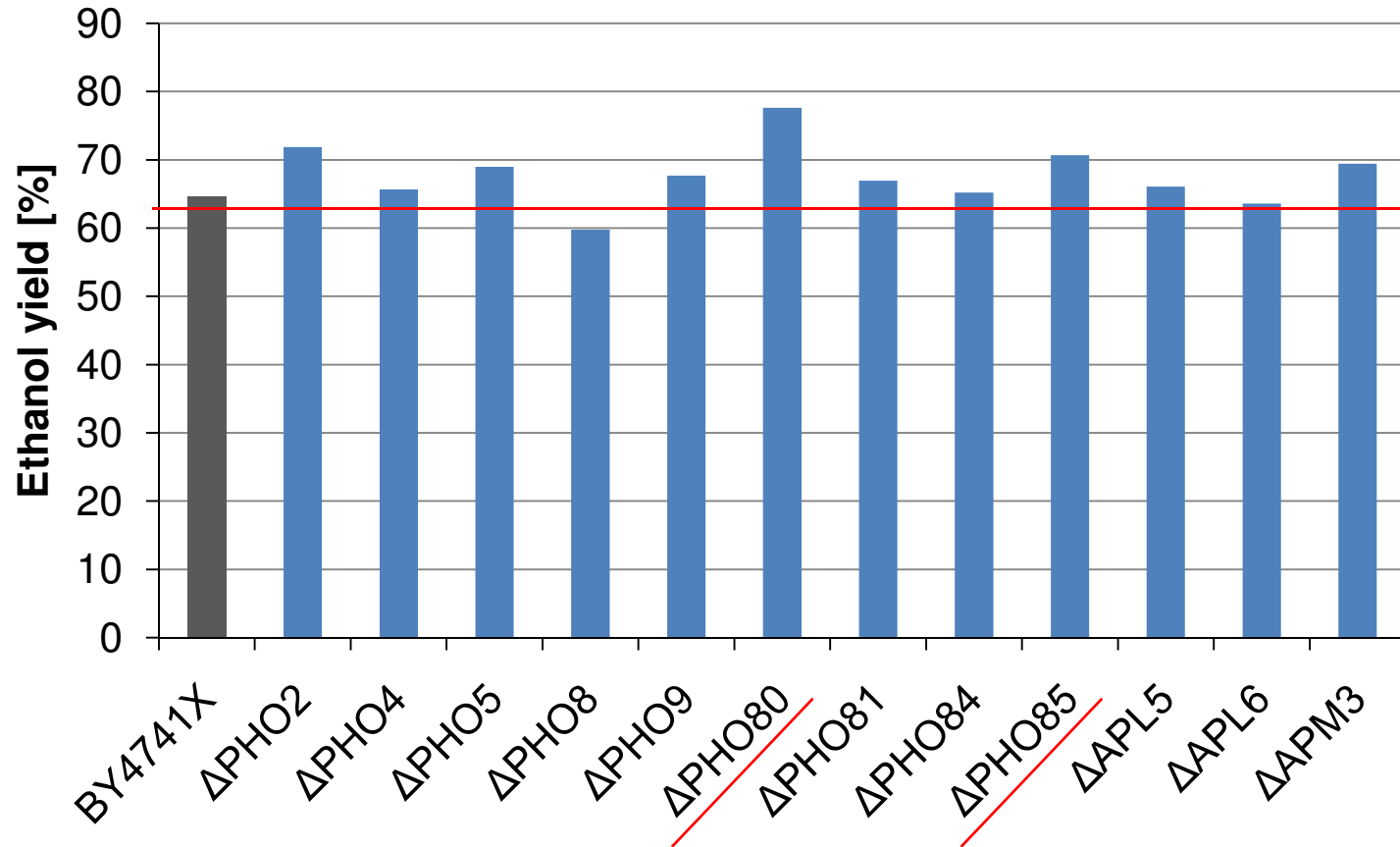


Gene	Function of gene product
<i>Pho84</i>	Pi-transporter
<i>Pho89</i>	Pi-transporter
<i>Pho4</i>	DNA-binding transcriptional activator
<i>Pho80</i>	Cyclin; inhibitor of Pho4p
<i>Pho85</i>	Cyclin-dependent kinase; inhibitor of Pho4p
<i>Pho5</i>	Repressible vacuolar alkaline phosphatase
<i>Pho8</i>	Repressible vacuolar alkaline phosphatase

(Ohshima et al., 1997; Lu et al., 2007)

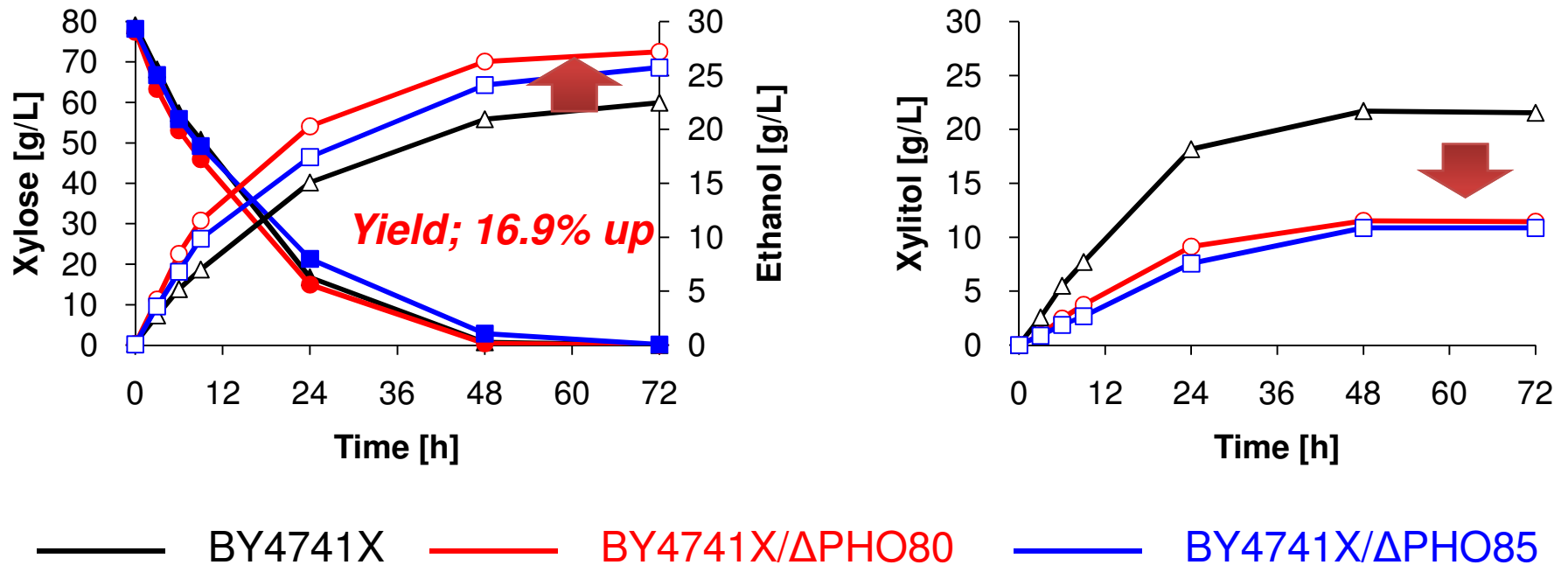
Xylose fermentation

Effect of deletion of *PHO*-related genes on ethanol production



Medium; YP, 80 g/l xylose
Condition; Oxygen limited
Temp; 30°C

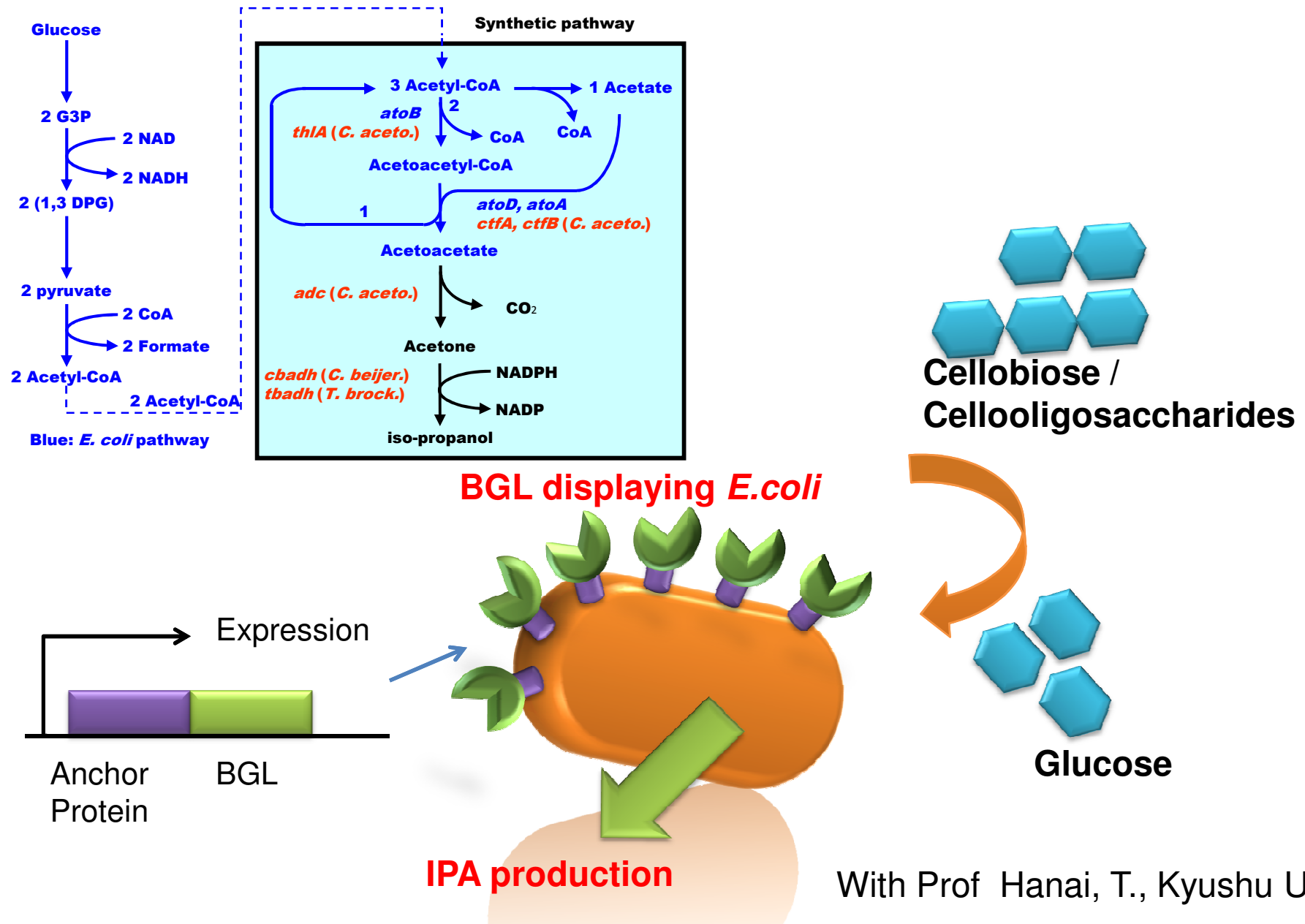
Effect of *Pho80/Pho85* deletion on xylose fermentation



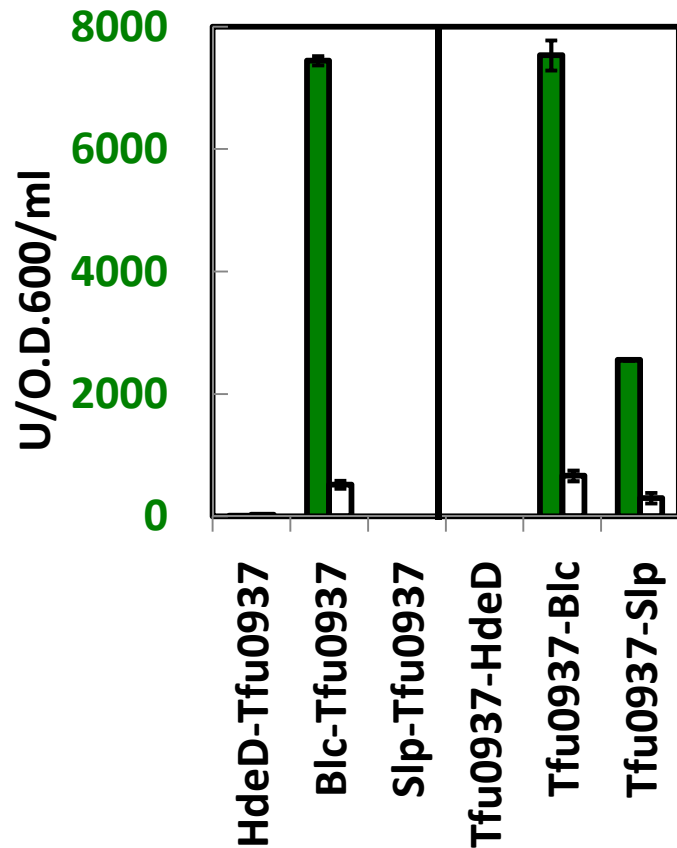
Strain	Volumetric productivity (g/L/h)	Ethanol yield (g/g)	Xylitol yield (g/g)
BY4741X	0.730	0.28	0.27
BY4741X/ΔPHO80	0.844	0.35	0.15
BY4741X/ΔPHO85	0.920	0.33	0.14

Xylose fermentation is affected by the PHO metabolism.

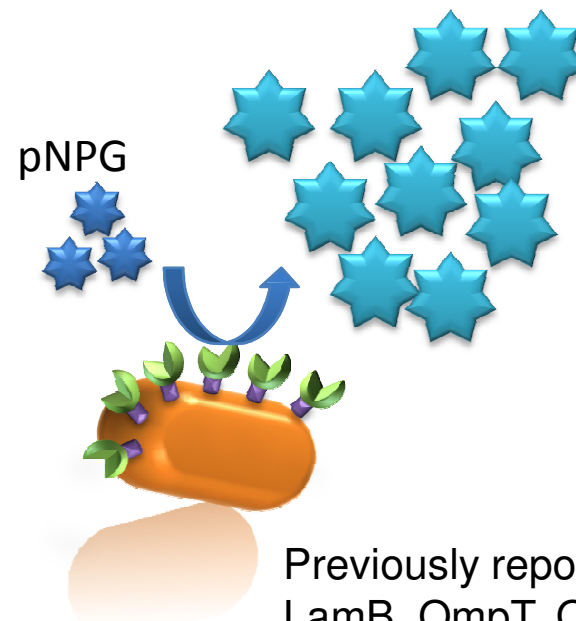
IPA production from cellobiose



Optimization of BGL and anchor



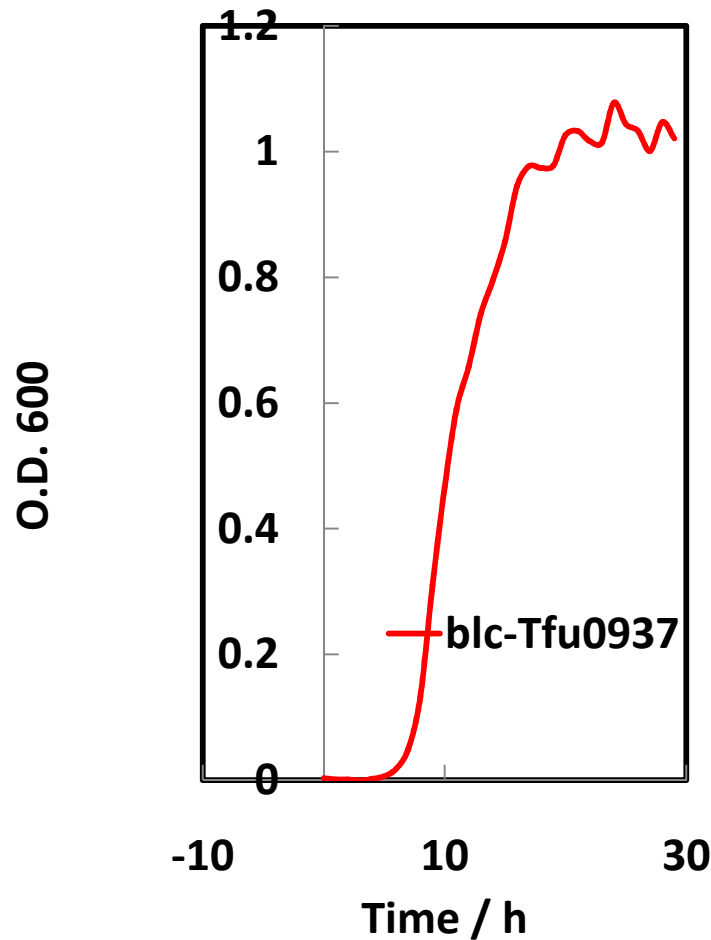
Tfu0937 was fused to an anchor, HdeD, Blc and Slp.



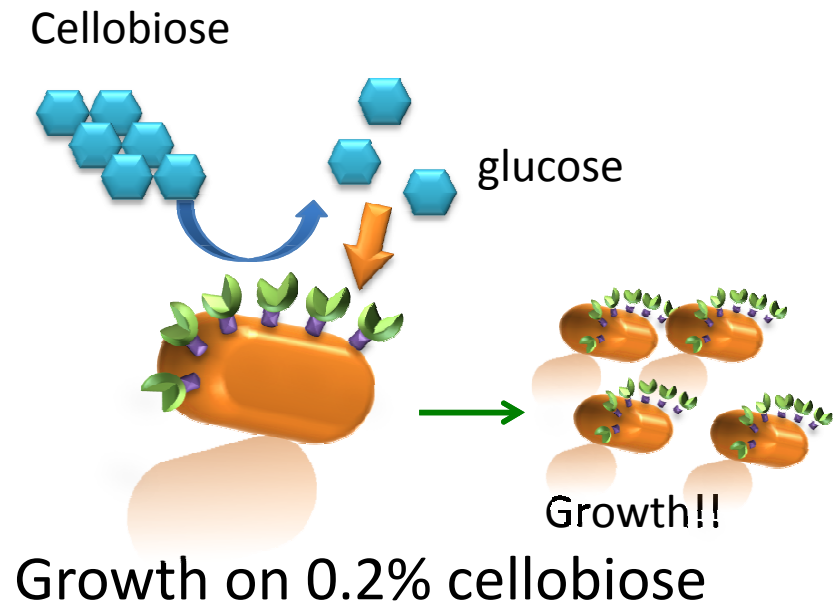
Previously reported anchor such as LamB, OmpT, OmpL did not work for activ BGL display

BGL activity of Blc-Tfu0937 were improved up to 70-fold higher compared to PgsA-BglA.

Growth on 0.2% cellobiose using BGL-displaying *E.coli*

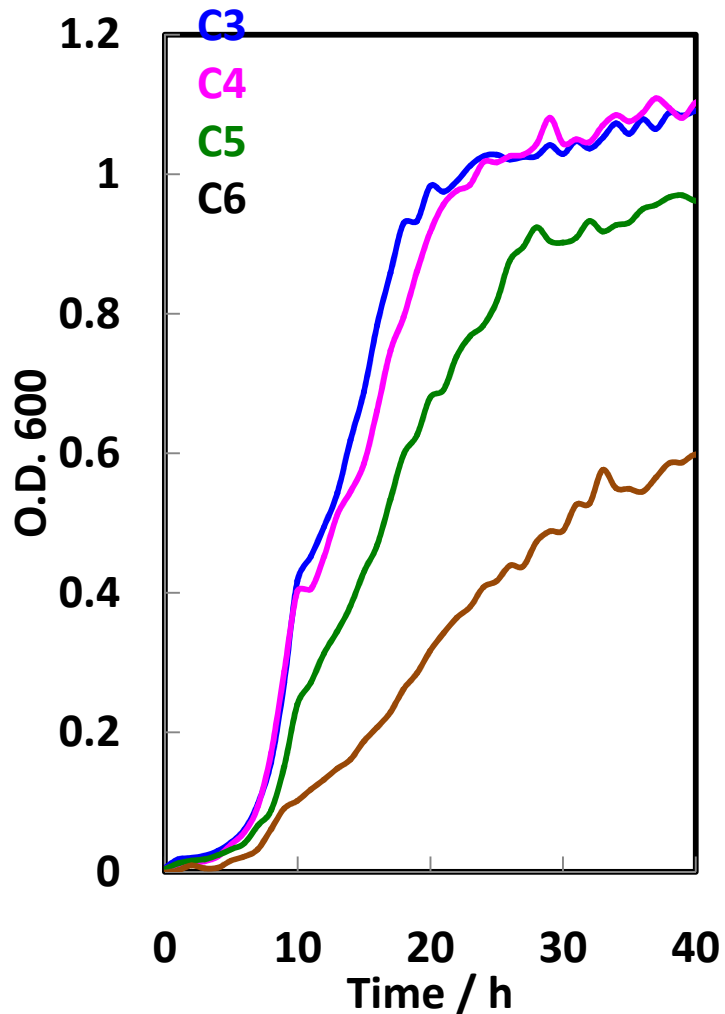


0.2% cellobiose as the sole carbon source
M9 minimum medium, Initial O.D.600 = 0.01

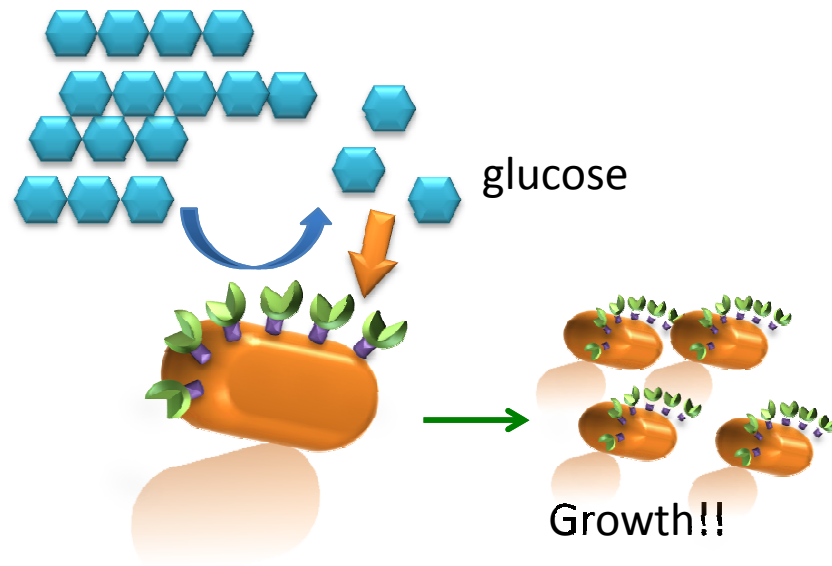


Blc-Tfu0937 was growth on 0.2% cellobiose
O.D.600=1.05 after 20h cultivation, almost same levels of glucose

Growth on 0.2% cellooligosaccharide



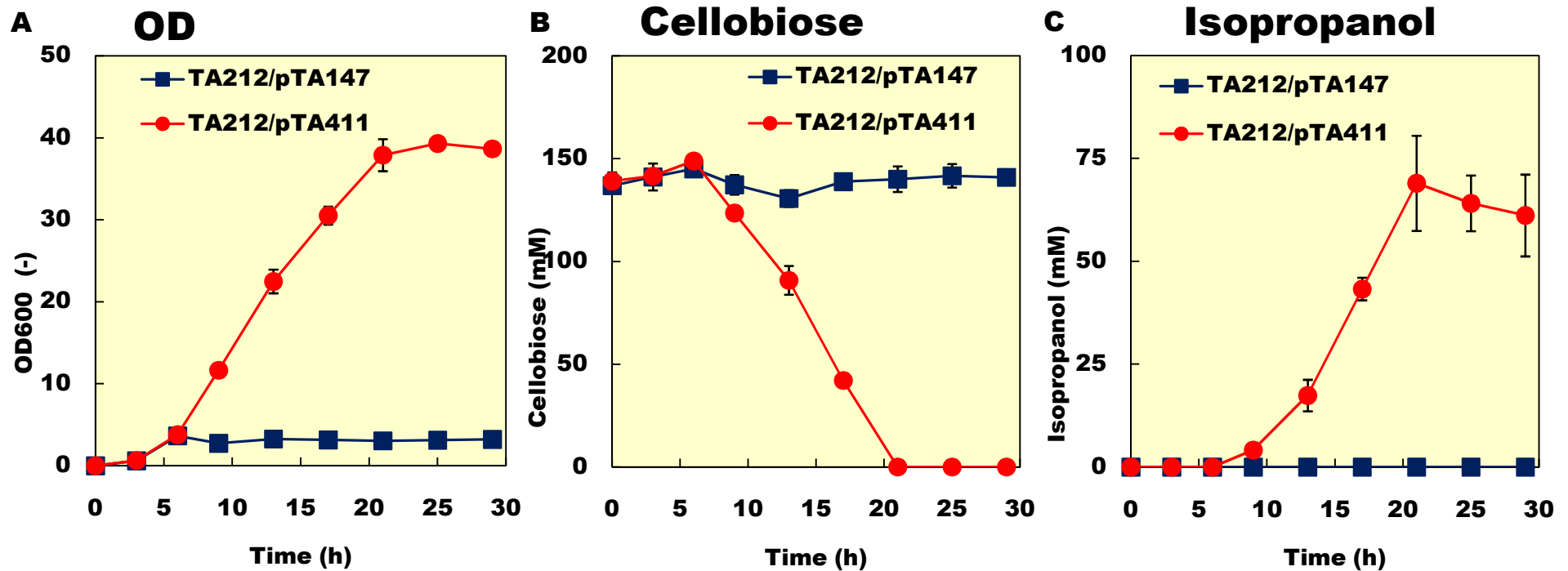
- Cellotriose (C3), Cellotetraose (C4), Cellopentaose (C5), Cellohexaose (C6) were used as carbon source, respectively Cellooligosaccharides



Successful growth on cellooligosaccharides

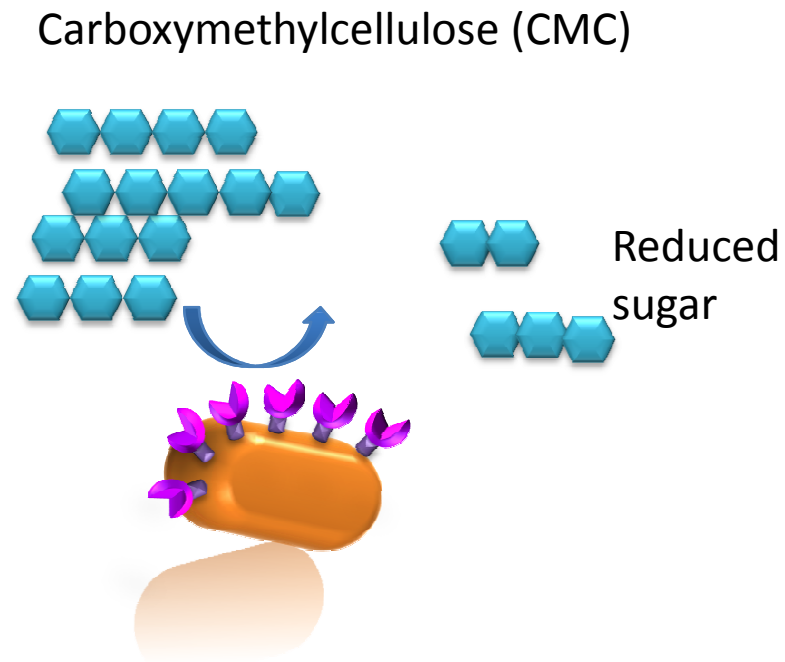
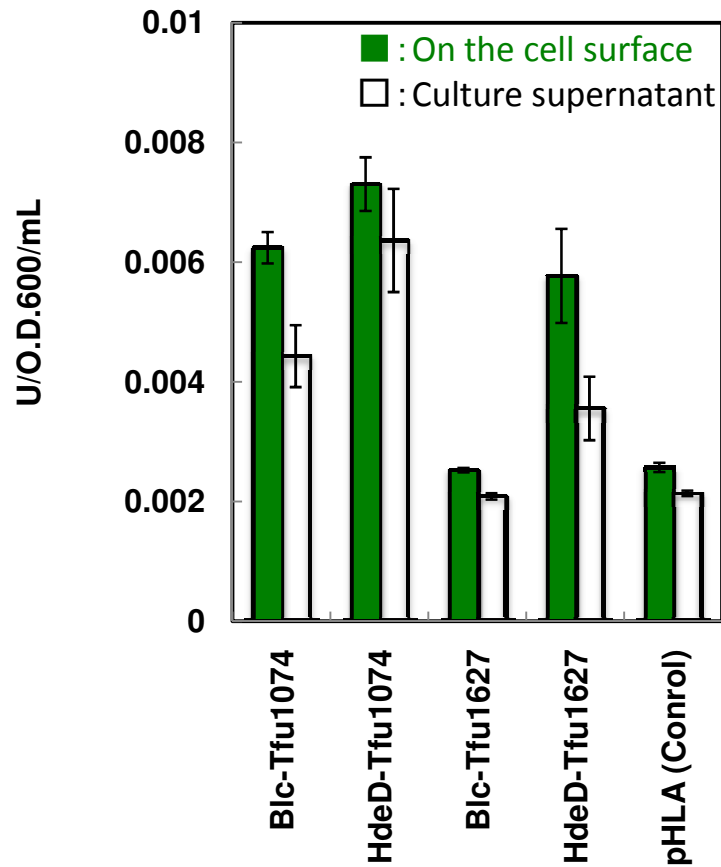
Direct IPA production from cellobiose Using BGL-displaying engineered *E.coli*

5wt% vol cellobiose in SD8 medium



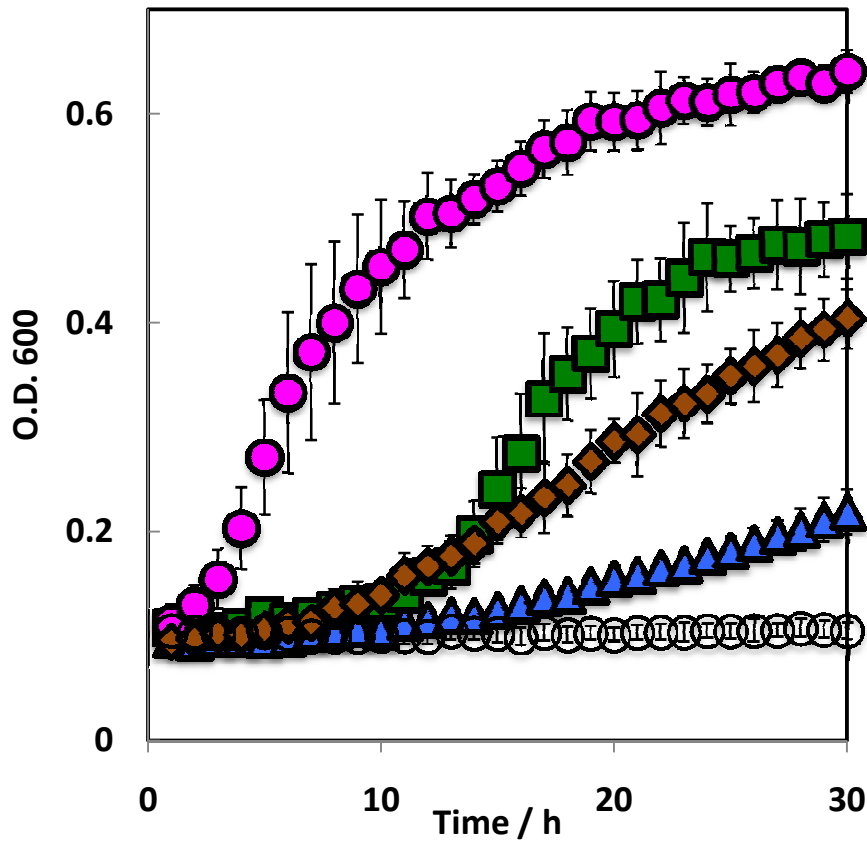
Successful IPA production from cellobiose (69 mM = 4.1 g/L)

EG activity displayed on the *E.coli*



EG displayed on the cell surface has CMC degradation activity

Direct growth on CMC both BGL and EG displaying *E. coli* in the minimum medium



Blc-Tfu1627

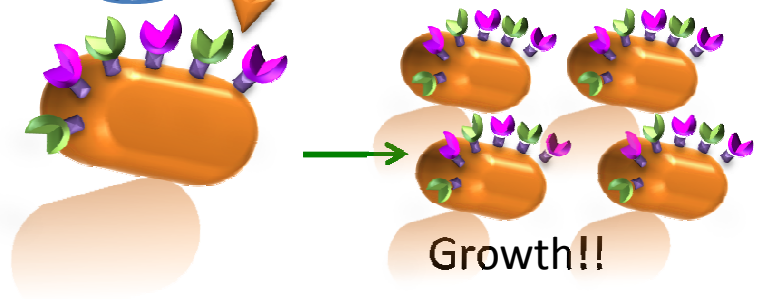
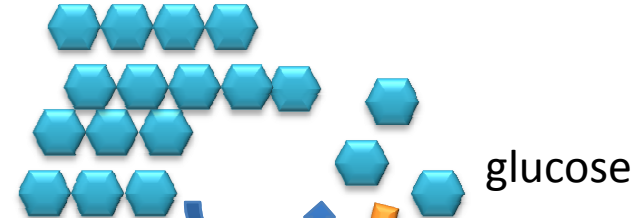
HdeD-Tfu1074

HdeD-Tfu1627

Blc-Tfu1074

pHLA

CMC



EG displayed on the cell surface has CMC degradation activity

Thank you very much for your attention



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MINISTRY OF EDUCATION,
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独立行政法人
科学技術振興機構
Japan Science and Technology Agency

Matsuda F, Poster28 Effect of metabolic inhibitors



Strategy for construction of super microbial cells

Metabolome analysis

UPLC/Q-TOF MS



GC/TOF MS



CE/TOF MS



Transcriptome analysis

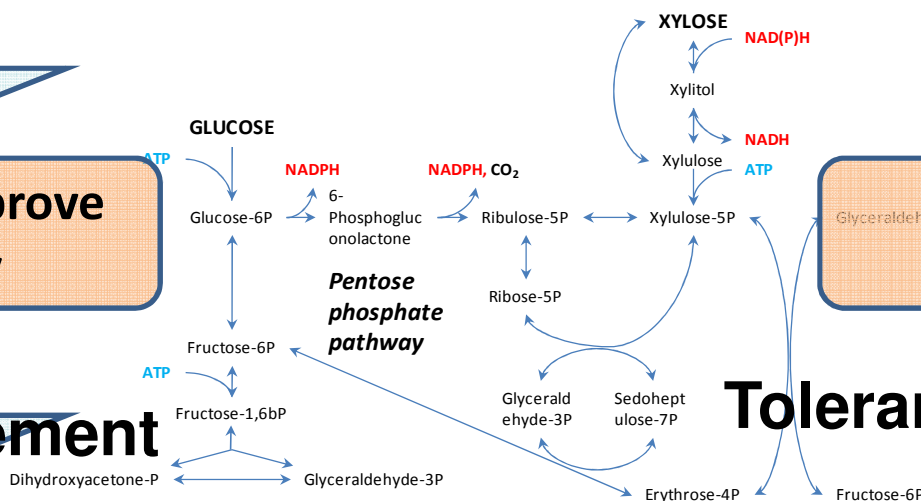


Key genes to improve productivity

Mechanisms of pH, temperature tolerance

Flux improvement

Tolerance improvement



Super microbial cells for cell factories