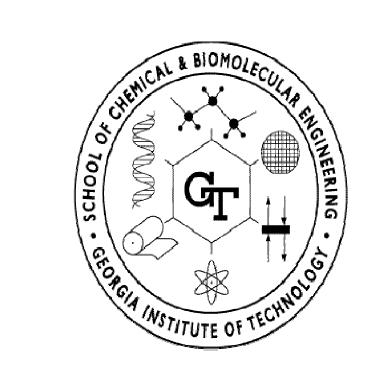
Engineering *E. co*li biocatalysts for consolidated biofuel production from hemicellulose

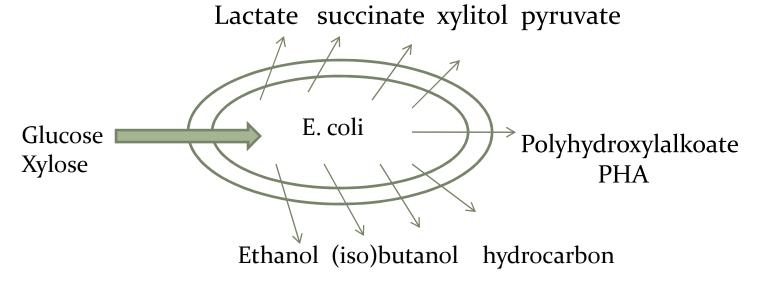


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> Bioenergy III, Canary Island, May 2011

E. coli as biocatalyst for bioenergy and biorefinery

• Metabolic engineering has been successful in making E. coli to churn out anything desirable

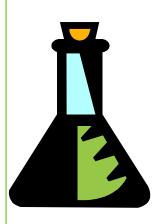


 Need to take on polymeric substrates (cellulose/hemicellulose) to reduce cost

Consolidated Production for cost reduction

Consolidated

- Single step accomplished in a reactor as single unit operation
- Requires biocatalyst to multitask



Traditional

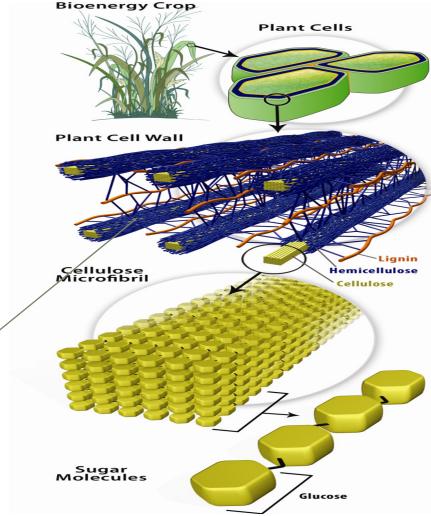
- Multi-step accomplished as separate unit operations
 - Enzyme production
 - Enzymatic hydrolysis
 - Fermentation (product formation)

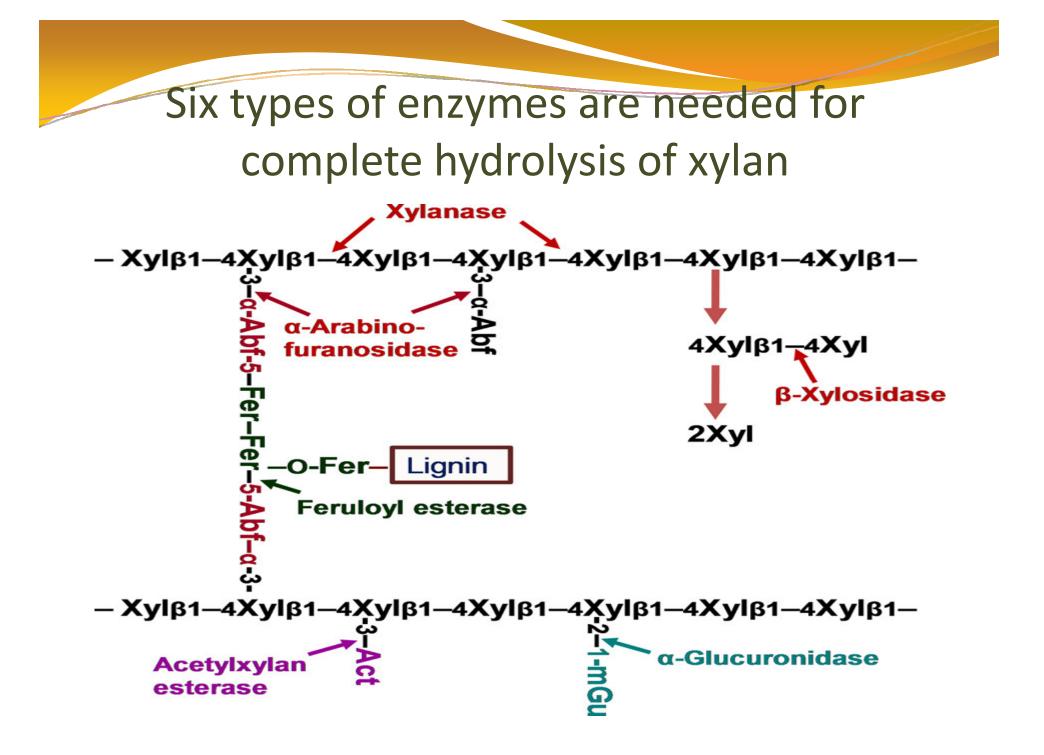
Could this be done?

Objectives:

Demonstrate a binary strategy to achieve direct fermentation of xylan to ethanol

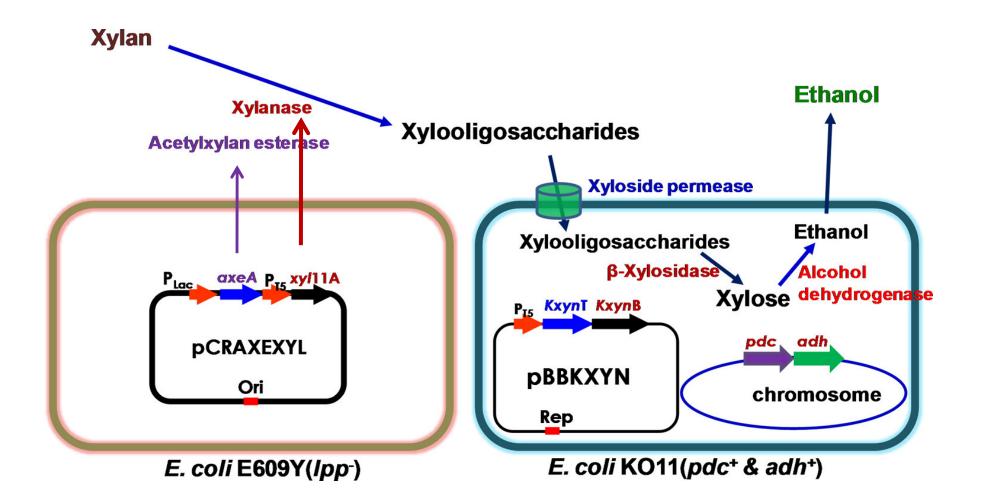
Hemicellulose: 20-40% of lignocellulose





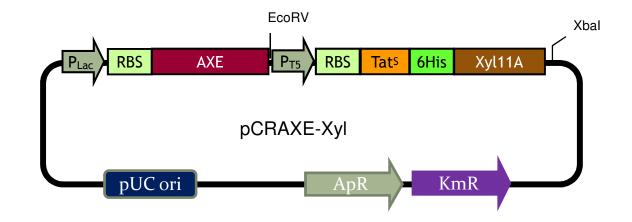


First design of the binary system

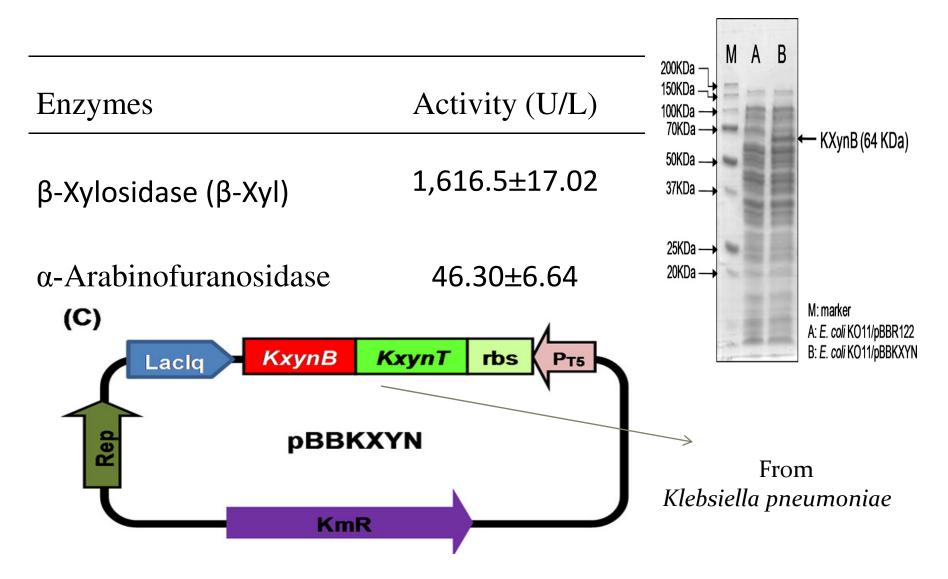


1st strain as hemicellulase producer/secretor

Enzyme activity (U/ml)	pCRAXE-T5Xyl			
	Total	Extracellular	Secretion percentage (%)	
Xylanase	0.28	0.26	93	
Acetylxylan esterase (AXE)	2.76	2.62	95	



2nd strain to convert oligosaccharides to ethanol



converting xylooligosaccharide to ethanol

2nd strain:

	0 h		48 h	
-	VO11	KO11/	KO11	KO11/
_	KO11	pBBKXYN		pBBKXYN
Cell growth(A ₆₀₀)	1 ± 0.08	1 ± 0.11	3.02 ± 13	4.74±0.35
Reducing Sugar (g/L)	1.74±0.13	1.74±0.15	4.39±0.25	1.49±0.17
Ethanol (g/L)	N.D.	N.D.	1.30±0.12	2.91±0.18

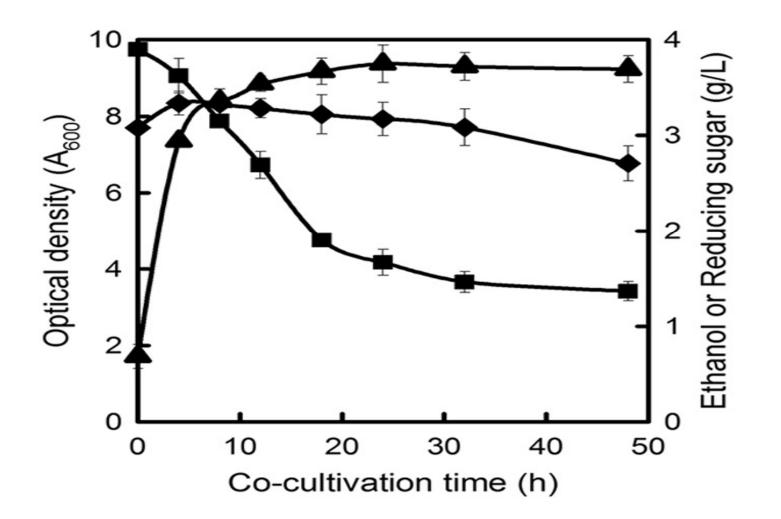
Binary vs. Single strain vs. acid hydrolysis

24 h fermentation			
Residual Ethanol (g/l		Ethanol yield	
reducing sugar(g/L)	Lunanoi (g/L)	(%)	
1.71±0.06	2.84±0.13	54.5	
0.84 ± 0.07	1.95±0.14	37.6	
1.16±0.06	4.38±0.11	84.1	
	Residual reducing sugar(g/L) 1.71±0.06 0.84±0.07	Residual Ethanol (g/L) reducing sugar(g/L) 2.84±0.13 0.84±0.07 1.95±0.14	

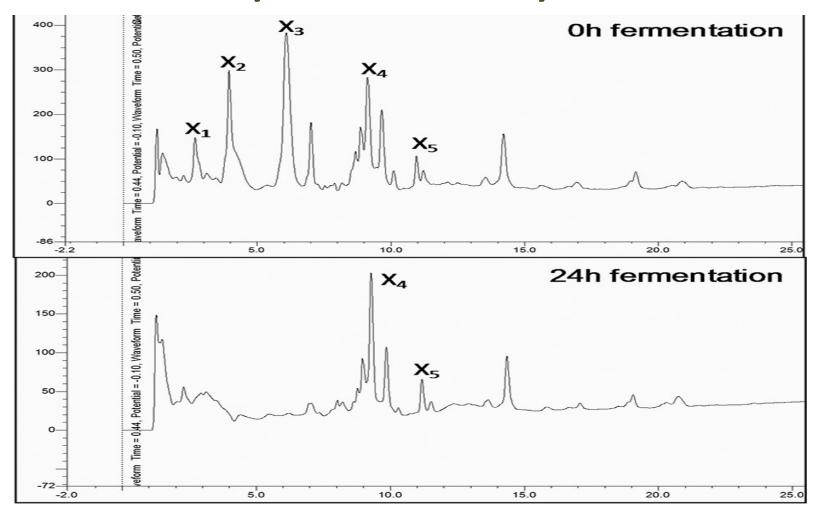
Improvement on ethanol yield

	After 36h induction		After 24h fermentation	
Case	Reducing sugar	Hydrolysis	Ethanol	Ethanol
	(g/L)	yield (%)	(g/L)	yield (%)
A(3 enzymes)	3.35 ± 0.11	32.7	2.84 ± 0.13	54.5
В	3.35 ± 0.13	32.7	3.29 ± 0.12	63.1
С	3.87 ± 0.12	37.8	3.11 ± 0.14	59.6
D	3.92 ± 0.06	38.3	3.22 ± 0.13	61.7
E (6 enzymes)	3.95 ± 0.25	38.6	3.71 ± 0.27	71.1

Xylan to ethanol



Why not 100% yield?

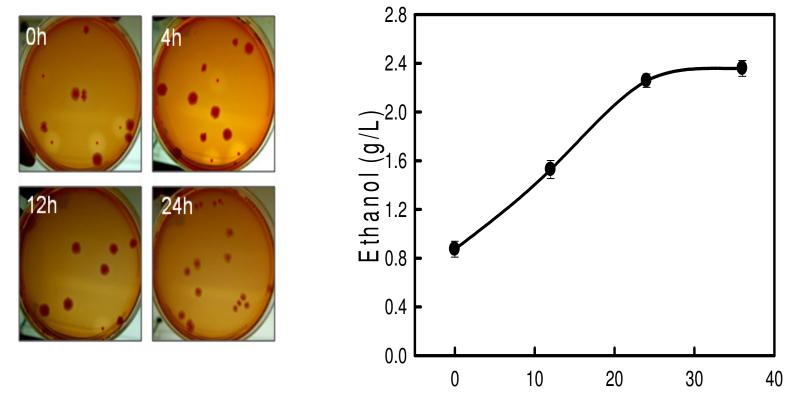


Xylooligosaccharides with 4 or more xylose units were not utilized

Conclusions

- Binary strategy is a viable option for consolidated bioprocessing of lignocellulose.
- Modular design allows easy extension to other biofuel and biorefinery products.
- Inclusion of all enzymes necessary to de-polymerize lignocellulose and judicious division of labor are important to achieve high yield.
- Hydrolysis of xylan to smaller units outside the cells or identifying a transporter for uptake larger xylooligosaccharides is important for further improvement.

Co-cultivation of two strains



Induction time (h)

Acknowledgements

