

Advanced biofuels and added value products from residual quasi-homogeneous biomass: from ethanol to *drop-in* fuels

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Biorefinery

- Comes from « bio » et « refinery »
 - Refine biological material
- Despite what we might think:
 - Biomass HAS a market
- It is diversified and complex
- Despite these facts – it stills represents an opportunity:
 - Carbon content, locally available and still as important : IT IS RENEWABLE





A lesson from the master



- Oil industry:
 - Use petroleum and refines it
- The first steps of a refinery



- COMMODITIES (fuels)
- For which there will always be a market
- Commodities covers for the OPEX

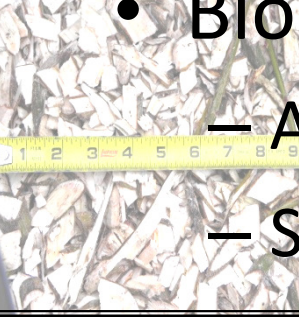


- Where is the margin of profit?
 - Added value chemicals



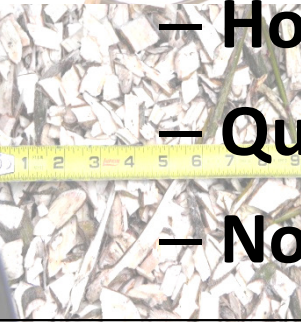
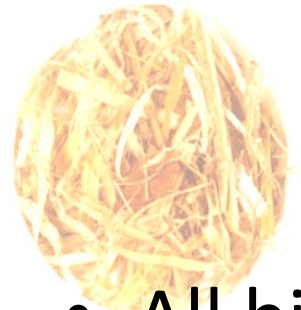
Convert this reality

- Implementing something as a biorefinery:
 - First objective should be commodities
 - It will ensure economical viability
 - Will also cover for the OPEX of the biorefinery
- Where should be the profit?
 - Added value molécules (and it's not easy!)
- Biomass:
 - As oil: an opportunity
 - Source of renewable and « green » compounds



Biomass

- All biomasses are rich in C [45 - 50 wt%]
- Few biomasses have an homogeneous composition
- Homogeneity will influence «conversion strategies»
- Biomass can be divided in three category:
 - Homogeneous
 - Quasi-homogeneous
 - Non-homogeneous



Abundance

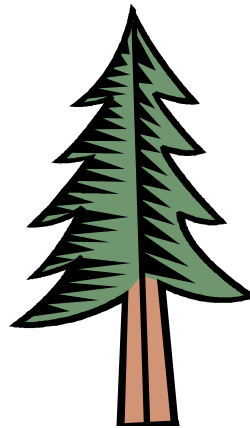


>200 k AMT/year



- Dedicated area
- Large forest/agricul activities
- Contracts should go by:
Governments
Large corporations

25-200 k AMT/year



- Residual Biomass
- Available in more locations
- Contracts should go by:
Region and/or municipalities
Private

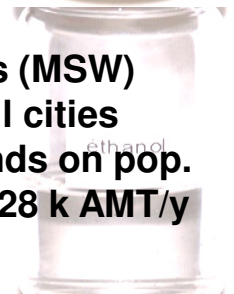
< 25-200 k TMA/year



- Urban biomass (MSW)
- Available in all cities
- Abundance depends on pop.
100k population ≈ 28 k AMT/y



triticale fermenté.
10,3% d'éthanol



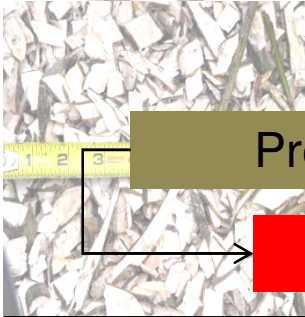
éthanol



Composition VS conversion

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- Cellulose
- Hemicelluloses
- Lignin
- Extracts
- Proteins

Predictable composition

Fractionation

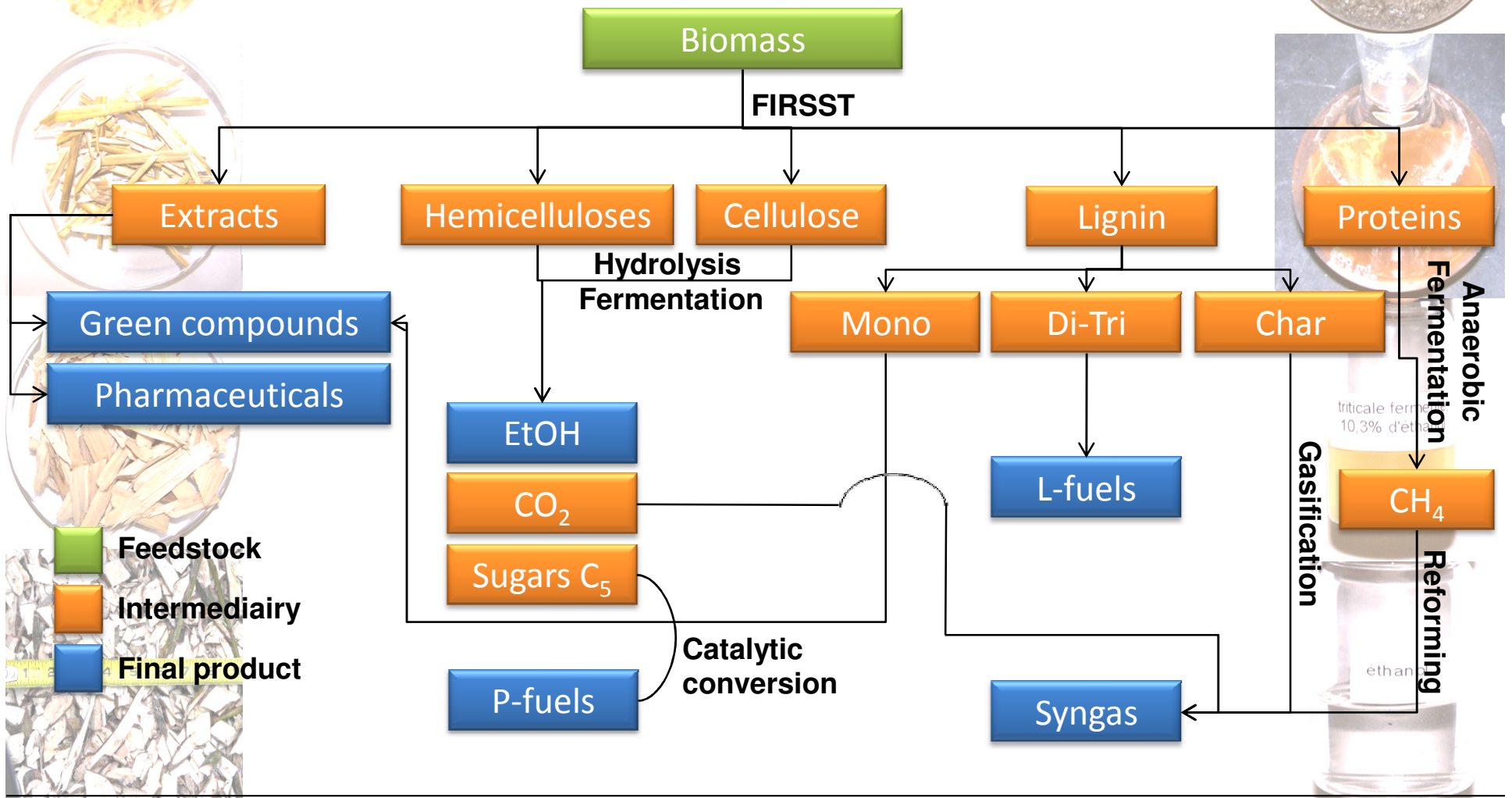


- Plastics (non-recyclable)
- Wood
- Paper (non-recyclable)
- Fabrics
- Etc

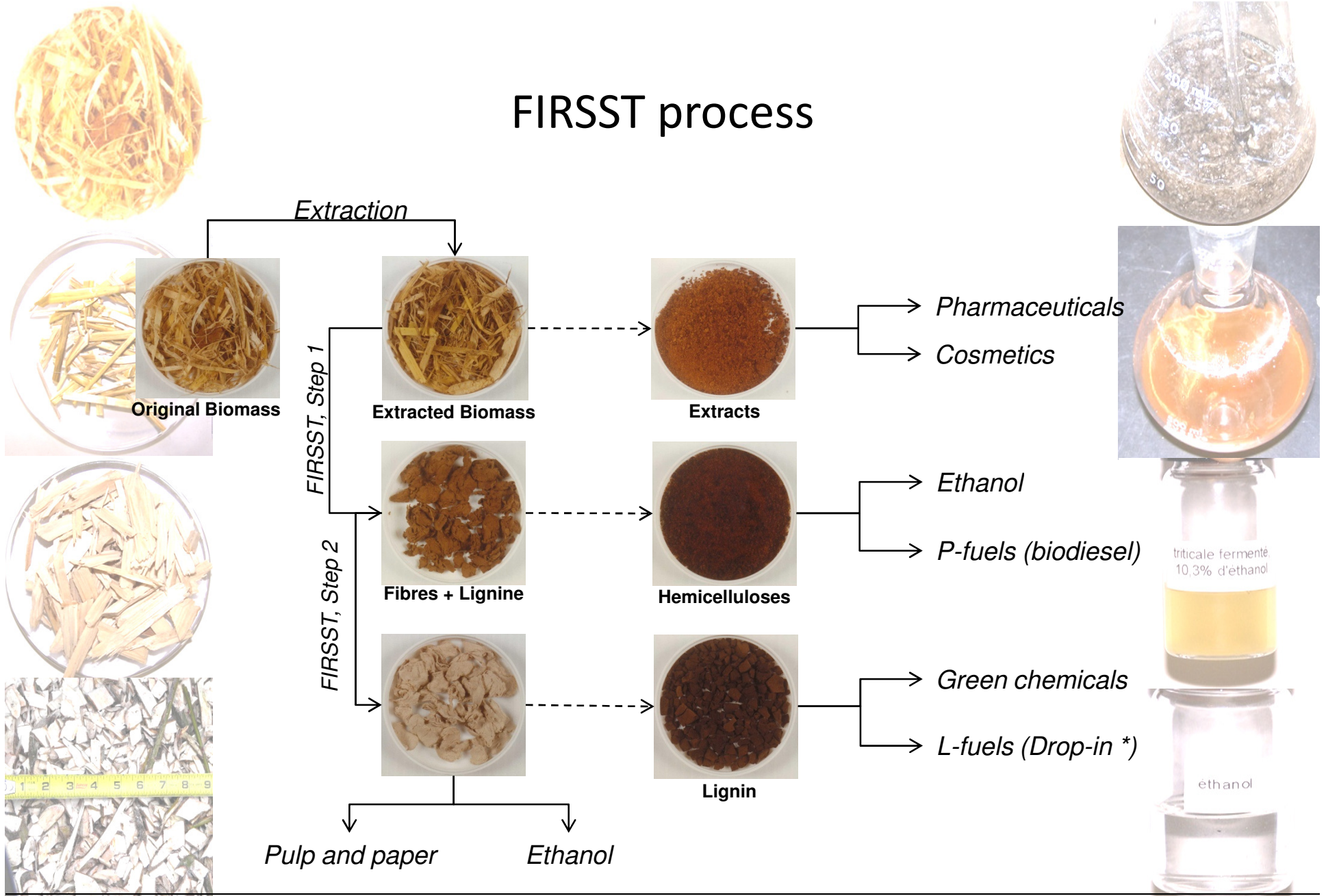
Unpredictable composition

Gasification

UdS – CRB Biorefining Process



FIRSST process



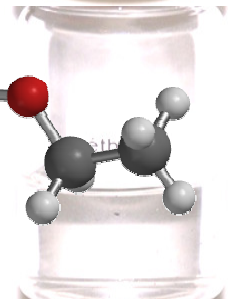
Extractives

- Extraction is performed before the FIRSST process
- Important:
 - Added value products
 - Limit the inhibitors in the aqueous mixture
- Process – Emulsification-assisted extraction
- Application:
Pharma/Cosmetics/Food/Gasification

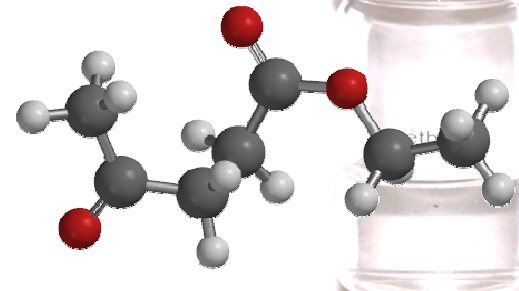
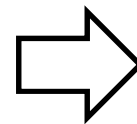
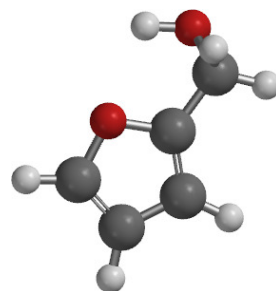
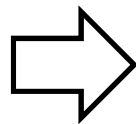
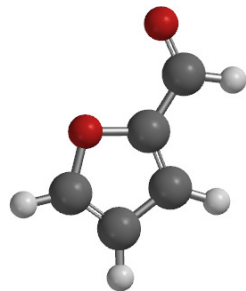
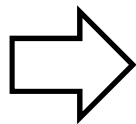
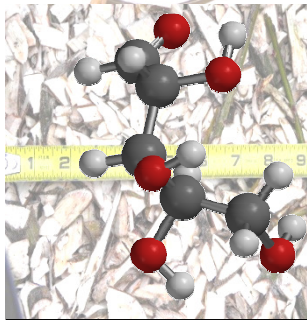




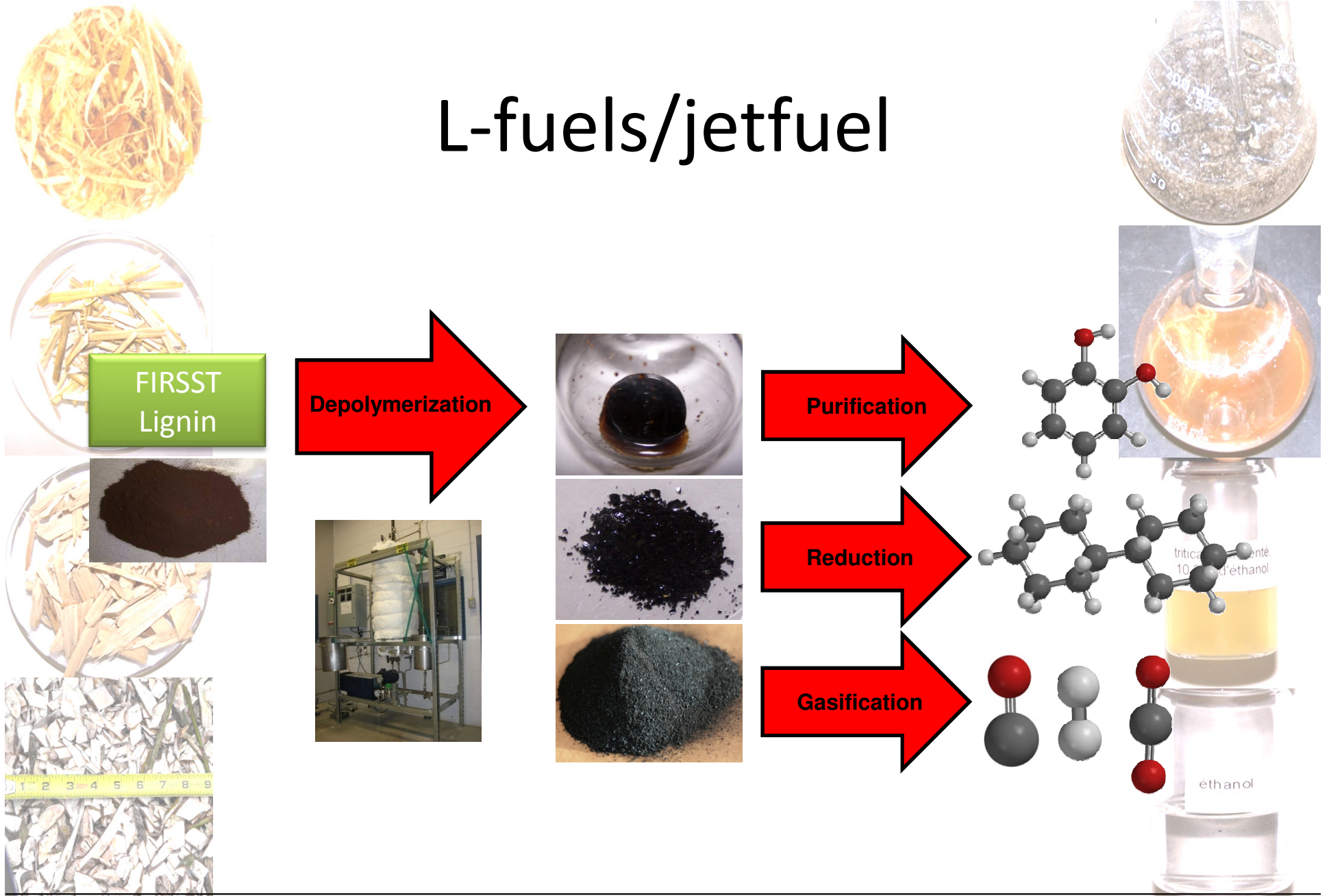
P-fuels/biodiesel



- C₅ sugars are hard to ferment
- Under acid catalyst – furfural
- Highly efficient 3 step process
 - Furfural
 - Furfurylic alcohol
 - Ethyl levulinate



L-fuels/jetfuel





Non-enzymatic hydrolysis

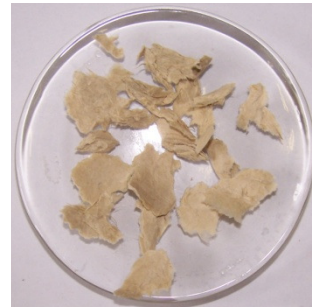


Biomass (100 MU)

Triticale



FIRSST



Cellulose (43MU)

- 12 MU - Extractives
- 20 MU - Hemicelluloses
- 20 MU - Lignin
- 05 MU - Proteins



Decrystallisation

Hydrogel



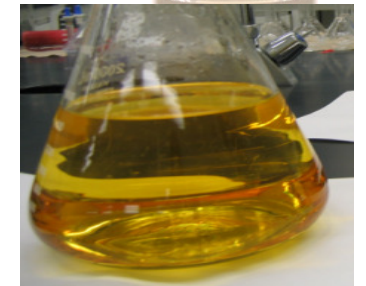
Hydrolysis

Ion rich solution

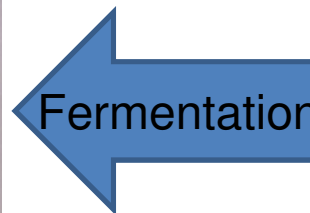
Reactives



Purification



Glucose solution (4-12%wt)
35-40MU



Fermentation



triticale fermenté,
10,3% d'éthanol



Distillation



éthanol

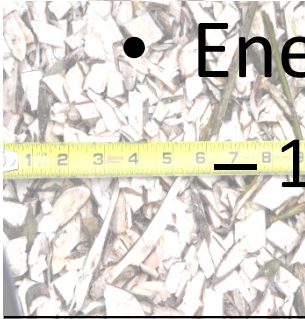


US Patent Appl. 2010/0163019; Prov. Appl. 61/195,886 filed Oct 10, 2008



A biorefinery scenario

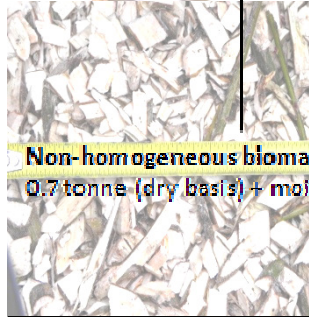
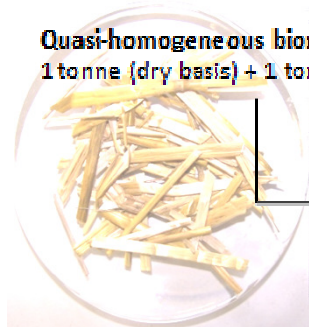
- Exemple : 1 tonne of agricultural residues
(In this case triticale)
 - 221 l of EtOH (+46 l invested in p-fuels)
 - 110 l of p-fuels (biodiesel)
 - 110 l of l-fuels (bio jetfuel)
 - 25 kg of green molecules
- Energetic demand
 - 13 GJ/tonne



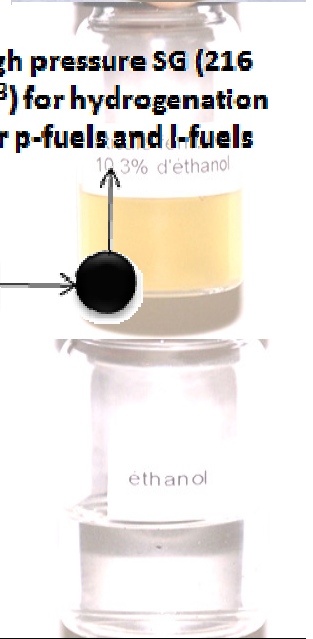
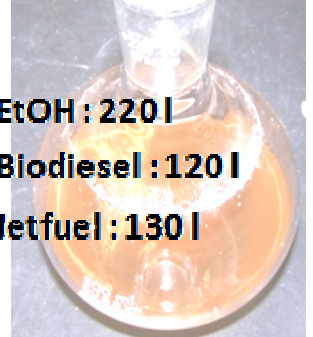
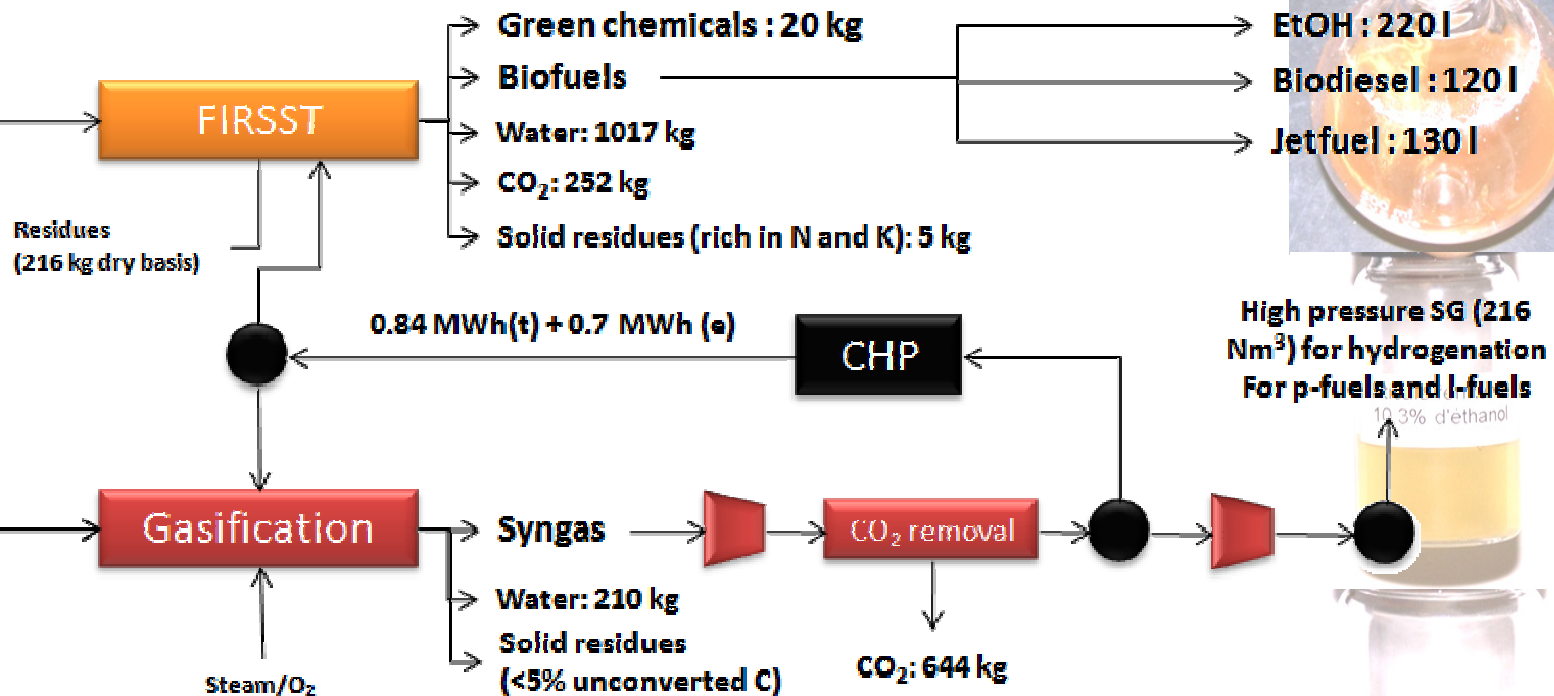
Synergetic approach



Quasi-homogeneous biomass
1 tonne (dry basis) + 1 tonne moisture



Non-homogeneous biomass
0.7 tonne (dry basis) + moisture





Energy balance



| Biomass | GJ | MWh |
|---|-----------|------------|
| 1 AMT residual lignocellulosic biomass | 18 | 5.0 |
| 0.7 AMT non-homogeneous biomass | 14 | 3.9 |
| Total : 1.7 AMT | 32 | 8.9 |

| Products (agricultural residues as an example) | GJ | MWh |
|--|-----|-------------|
| Ethanol (216 l – 167 kg) | 5.1 | 1.41 |
| P-fuels : Ethyl Levulinate (124 l – 126 kg) | 3.3 | 0.92 |
| L-fuels : Propylcyclohexane (100l – 88 kg) | 3.5 | 0.97 |
| Residual syngas | | 0.3 |
| Lignin derived chemicals (31 kg) | | 0.2 |
| Total Output | | 3.80 |

TOTAL EFFICIENCY 42% and up to 45%

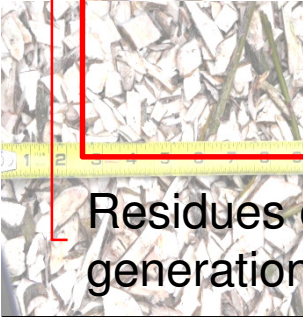
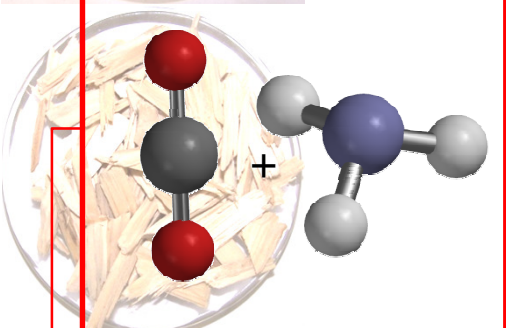
« Negative » Carbon footprint

- The Chair's approach
 - Complete utilisation of carbon
 - Including CO₂
- From this the biorefineries:
 - Will only produce biofuels and green molecules
- Three approaches are considered:
 - Thermochemical
 - Chemical
 - Biological

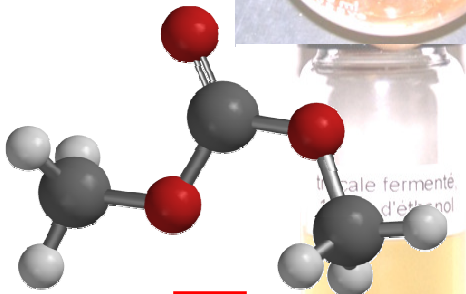
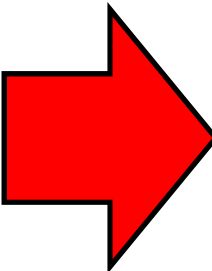
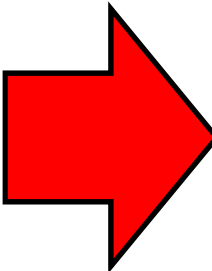


Chemical approach

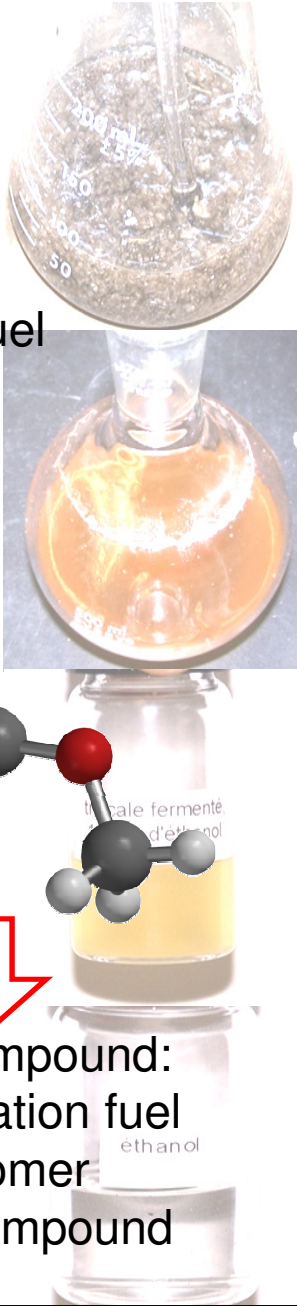
Products from the second generation biofuel industries



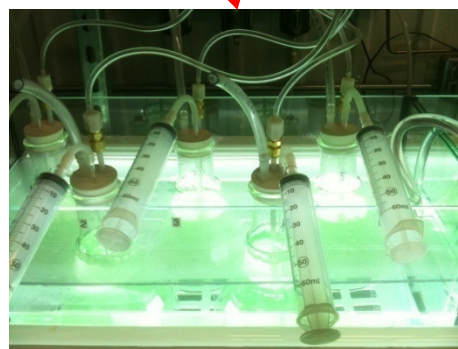
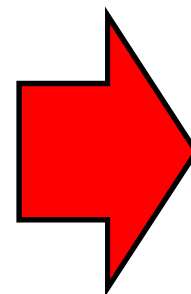
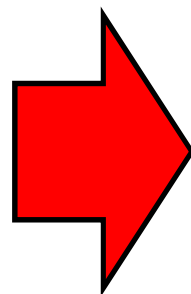
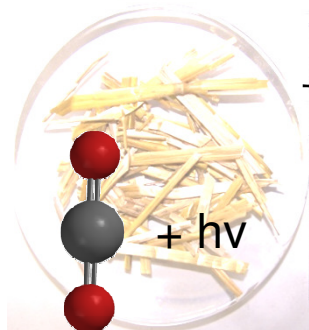
Residues or co-product from 1st and 2nd generation biofuels industries



Green compound:
-3rd generation fuel
-Monomer
-Green compound



Biological approach



Acknowledgments



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MERCI