MACROSEGREGATION IN ELECTROSLAG REMELTED INGOTS

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ABSTRACT

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Submitted to the Department of Materials Science and Engineering on January 13, 1978 in partial fulfillment of the requirements for the degree of Doctor of Philosophy.

Laboratory-scale ESR and simulated ESR apparatus were designed and used to study the formation of macrosegregation in ESR ingots. The laboratory-scale ESR apparatus was used to make a series of Al-4% Cu ingots with a solidification rate of about 4 x 10^{-2} cm/sec. Macrosegregation in these ingots varied from no macrosegregation in an ingot with a flat mushy zone to 4.25% Cu at the center and 4.6% Cu at the edge for an ingot with a deep mushy zone (Co = 4.4% Cu).

In order to induce more severe macrosegregation, the apparatus for simulating the ESR process was used to make a series of Sn-15% Pb ingots with a solidification rate of about 5 x 10^{-3} cm/sec. Compositions as rich as 38% Pb (freckling) at the center and as poor as 7% Pb at the edge were found, depending on solidification conditions. In order to study the effect of centrifugal force on macrosegregation across the ESR ingots, the same apparatus was modified to allow rotation of the ingot. A series of rotated Sn-Pb ingots ($12\sim14\%$ Pb) was made in this way. Solidification rates were varied from 5.3 x 10^{-3} cm/sec to 1.36 x 10^{-2} cm/sec and rotation speeds were varied from 54 rpm to 119 rpm. The centerline composition varied from 9% Pb higher than the edge composition to 20% Pb lower than it (freckling at the edge).

Equations for predicting flow of interdendritic liquid and macrosegregation in ESR ingots are derived and a computer model based on these equations is used to numerically calculate the macrosegregation. Agreement between calculations and experimental results is good.

The influence of the important solidification parameters such as the shape and depth of the mushy zone and the local solidification time on the macrosegregation across the ingot is demonstrated quantitatively. The solidification shrinkage effect and the gravity effect on convection in the mushy zone lead to different types of macrosegregation. The conditions under which either effect dominates and the resultant macrosegregation are discussed. In addition, the effect of the important dimensionless group, $\vec{v} \cdot \nabla T/\epsilon$, on the different macrosegregation results is discussed. The most important innovation of this work is to introduce and demonstrate the idea of effectively reducing macrosegregation and eliminating "freckles" by rotating the ingot at a suitable speed during solidification. The experimental and calculated results of the rotated ingots show significant reduction in macrosegregation across the ingot and "freckles", which would otherwise be present, are eliminated.

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I". INTRODUCTION

The ESR process is one of the most important new processes developed for special purpose alloys. The main advantages are that refining can be obtained by melting through a slag of controlled composition, and special control over solidification. Such a control can lead to reduction of dendrite arm spacing, microsegregation, and macrosegregation, giving a sound ingot (1).

However, the recent production of ESR ingots for large, heavy forgings for nuclear-reactor pressure vessels and generator rotors has faced very serious macrosegregation problems including centerline segregation and channel-type segregation (freckles) (2). The non-uniformity of properties and structure can affect deleteriously the mechanical properties of ingots during forging or rolling. Also, in the production of electroslag remelted U-7.5Nb-2.5Zr ingots, it has been found that niobium tends to concentrate at the center of the ingots and results in center-line segregation (3).

Furthermore, due to the strong effect of ingot size on the economics of ESR processing, the production of ingots for forged round billets of stainless steel and tool steels has been found to be profitable only when the ingot size exceeds about 20 inches in diameter (4), and the greater the ingot diameter, the more profitable the ESR process. However, like other casting processes, the macrosegregation problem is expected to become increasingly severe when the ingot size becomes very large. So far, much experimental and theoretical work has been conducted on the heat transfer in ESR ingots leading to many theoretical heat transfer models which relate the operating parameters in the ESR process to the solidification parameters such as the shape and depth of the mushy zone and the solidification rate (5-7). However, quantitative studies have not been done on how these solidification parameters in turn affect macrosegregation. This work is focused on the experimental and theoretical study of the effects of solidification parameters on macrosegregation in ESR ingots. Also, more importantly, an effective means of reducing macrosegregation and eliminating "freckles" in ESR ingots is demonstrated. Therefore, as a result of this study, one is able to predict solidification conditions required to produce ESR ingots of optimum homogeneity.

It should be emphasized that although macrosegregation in the ESR processes is analyzed in this study, the basic equations can be equally applied to other casting processes such as continuous casting and the VAR process.

II. LITERATURE SURVEY

1. General Background on Macrosegregation

There has been much research on macrosegregation in ingots and castings in the past decade. The direct observation of fluid flow in the mushy zone of solidifying $NH_{L}CI-H_{2}O$ system (8, 9, 10, 11) and analytical and experimental results on macrosegregation in ingots and castings (12, 13, 14, 15, 16) have lead to the conclusion that interdendritic fluid flow in the mushy zone is the most important mechanism of macrosegregation. Since the interdendritic liquid is rich in solute, its physical displacement can lead to considerable solute redistribution and result in macrosegregation. This flow of solute-rich interdendritic fluid is caused primarily by two driving forces (17). The first is the solidification shrinkage, which causes the interdendritic liquid to flow toward the solidus isotherm in order to satisfy continuity. The second driving force is gravity which causes convection since the density varies within the interdendritic liquid. Another but less important force driving the interdendritic flow is the bulk liquid convection which can sometimes penetrate into the mushy zone and sweep away the solute from behind the dendrite tips.

The calculation of the interdendritic fluid flow caused by solidification shrinkage and gravity and the resulting macrosegregation was first performed by Mehrabian et al. (15). They applied D'Arcy's law to calculate the interdendritic fluid flow in horizontally solidified Al-Cu ingots. No bulk motion in the liquid pool was assumed and the metallostatic pressure was used as the boundary condition at the liquidus isotherm. For simplicity, fluid flow and solute redistribution equations were uncoupled in their numerical calculation. The agreement between the experiment and calculation was reasonably good (16). Szekely and Chen (18) calculated heat transfer and fluid flow in the mushy zone of an Al-Cu ingot solidifying in the horizontal direction. However, variations in the volume fraction and density of the interdendritic liquid within the mushy zone were neglected in their equation of continuity. The volume fraction of liquid was calculated from the heat balance only since no mass balance was considered. Later, Jassal and Szekely (11, 19, 20) carried out an experimental and analytical study of the fluid flow in the mushy zone of a solidifying NH_LC1-H_2O ingot. The calculation was basically the same as that of Szekely and Chen (18). However, this time they calculated the fluid flow in the bulk liquid pool assuming zero velocity of liquid at the liquidus isotherm. Then, by choosing the velocities at some point away from the liquidus isotherm as the velocity boundary condition at the liquidus isotherm, they calculated the fluid flow in the mushy zone. Although agreement between experiment and calculation was claimed, the choice of velocity boundary condition at the liquidus is arbitrary. More recently, Asai and Muchi (10) calculated simultaneously heat, mass and momentum transfer in the mushy zone of a solidifying $NH_{L}C1-H_{2}O$ ingot. Although a mass balance was considered, variations in the density and fraction of interdendritic liquid were neglected in their equation of continuity. While fraction of liquid was calculated; macrosegregation was not measured nor calculated. Also, no quantitative

comparison between experiment and calculation was made.

2. Effects of Solidification Parameters on Macrosegregation in ESR Ingots

Like other solidification processes, the shape and depth of the mushy zone plays an important role in macrosegregation formation in ESR ingots. It has been found that operating conditions that favor a deep shape of mushy zone will cause more macrosegregation (21, 22). For example, Fredriksson and Jarleborg (21) observed positive segregation of Ni at the centerline of a 18/8 ingot when the electrode melt rate was high and the liquid pool was deep. However, no segregation was observed at a slower melt rate. Ward and Hambleton (22) pointed out that when the slag skin is reduced (in order to get better surface quality) by increasing the power input subsequent deepening of the liquid pool occurs and causes segregation problems. Moreover, since pool depth increases with the size of ESR ingots (23, 24), macrosegregation problems become particularly serious in very large ESR ingots (2).

The reason why a deep mushy zone causes more macrosegregation in ESR ingots, according to the macrosegregation theory (8, 15), is that the solute-rich interdendritic fluid flow can be strongly affected by solidification shrinkage and gravity in a deep mushy zone. In short, if the solidification conditions favor the solute-rich interdendritic liquid to flow from the center of the ingot to the edge, the solute is depleted at the center and hence negative segregation at the center occurs. Conversely, if flow is from the edge to the center, solute is accumulated at the center, and positive segregation at the center occurs.

Experimental (25) and computer (5) studies have shown that the melting rate of the electrode is the most important parameter in determining the liquid metal pool depth. A higher melting rate results in a deeper metal pool and hence a deeper mushy zone. Other operating parameters such as composition and amount of slag, thermal conductivity of metal, current and voltage, electrode polarity also affect the depth of liquid pool and mushy zone.

3. Prediction and Control of Magrosegregation in ESR Ingots

Although a number of heat flow models (5, 6, 7) have been developed to relate the solidification parameters, such as the shape of the mushy zone and solidification rate to the ESR operating parameters, very little work has been done on the quantitative prediction of macrosegregation in ESR ingots. Mitchell (26) calculated macrosegregation in the axial direction of ESR ingots due to the composition change in the bulk liquid (caused by electrode change or inadequate slag control during solidification). However, this type of segregation, if it exists, is far less severe than that caused by interdendritic liquid flow in the mushy zone. Serious macrosegregation, such as "freckles", cannot be predicted using this approach.

Although no quantitative prediction of macrosegregation in ESR ingots exists at this time, some techniques of improving ingot homogeneity have been reported recently. For example, Cooper (2) developed a so-called "central zone remelting" (C Z R) technique by punching out and remelting the badly segregated central region of big ingots. Success was achieved

in improving homogeneity at the ingot centers. However, punching out and remelting the central part consumes extra time and energy. Moreover, any discontinuities (e.g., change in ingot structure or entrapped slag) between the old part and the newly remelted part could cause problems during the subsequent mechanical processing. Thomas et al. (27) also reported success in improving the ingot homogeneity by shielding the solidifying ESR ingot and slag from the disturbance of any stray magnetic field outside the mold. However, it is obvious that this technique cannot reduce the macrosegregation caused by interdendritic fluid flow induced by gravity and/or solidification shrinkage.

Contrary to the work of Thomas et al. (27), Zabaluer et al. (28) claimed success in improving ingot homogeneity by applying a magnetic field to enhance the movement of liquid slag, which, according to the authors, changed the character of dropwise transfer of metal from the electrode and therefore decreased the depth of the conical part of the metal pool.

4. Effect of Centrifugal Force on Macrosegregation

Stewart et al. (29) studied macrosegregation in rotated and oscillated Al-3% Ag conventional-type ingots. In the stationary ingot, the composition ranged from about 2.9% Ag at the center to about 3.1% Ag at the wall. The rotated ingot (126 rpm) showed no significant difference from the stationary one. This might be attributed to the fact that the test castings employed solidified too rapidly to observe any effect of centrifugal force; the ingots were cast in water-cooled stainless steel molds which were only 8 cm in diameter. The oscillated ingot (126 rpm with

the direction of rotation being reversed every 5 sec.), however, showed significant macrosegregation. Early in the freezing of the oscillating casting (i.e., near the wall), the high shear force near the solid-liquid interface caused extensive interdendritic flow and swept the solute-rich liquid out of the mushy zone. Therefore, final solute concentration increased from the casting surface toward the interior. Near the midradius, however, the temperature gradient decreased and the dendrite fragments, broken off by the shear force, were able to survive and grow. Because of the lower concentration of these fragments, the overall concentration in the center was reduced and, therefore, final solute concentration decreased toward the center.

Recently, Keane (30) studied the effect of centrifugal force on the macrosegregation in Al-4.5% Cu ingots. His work was unidirectional solidification in the radial direction and simulated a slice out of a non-unidirectionally solidified ingot. However, only theoretical calculation was done; no experimental work was performed.

III. THE OUTLINE AND PLAN OF WORK

The plan of work may be summarized as follows:

1. Design and build a laboratory-scale ESR unit suitable for macrosegregation study.

2. Reproduce severe macrosegregation (including freckles) often found in industrial ESR ingots.

3. Study the effects of important solidification parameters such as solidification time and shape and depth of mushy zone on the macrosegregation in ESR ingots.

4. Develop a computer model to predict macrosegregation in ESR ingots. Verify the validity of this model by comparing the calculated results with the experimental macrosegregation results.

5. Study the effect of centrifugal force on the macrosegregation in ESR ingots. Demonstrate experimentally and theoretically the idea of effectively reducing macrosegregation and eliminating freckles by rotating the ingot at a suitable speed during solidification.

IV. THEORETICAL ANALYSIS OF MACROSEGREGATION IN ESR INGOTS

In order to predict quantitatively macrosegregation in ESR ingots, theoretical equations are derived based on fluid flow and mass transfer in solid-liquid system. The basic concept employed is that macrosegregation in ESR ingots is caused by interdendritic fluid flow, as described earlier for other types of ingots by Flemings and Nereo (12), and by Mehrabian, Keane and Flemings (15). In the latter work, equations were derived for the pressure distribution, and hence interdendritic flow, inside the planar mushy zone of a unidirectionally solidifying ingot, using D'Arcy's Law for the interdendritic fluid flow, and taking both gravity and solidification shrinkage as driving forces for the flow. However, in order to simplify the numerical calculation, the governing equations for fluid flow and solute redistribution were uncoupled. In this work, (1) the relevant equations are solved simultaneously and (2) the pressure distribution, flow behavior, and macrosegregation in cylindrical coordinates for the conditions of solidifying ESR ingots are described.

A schematic summary of the analytic work to be described herein is given in Figure 1. Figure 1a shows an ESR ingot during solidification. Liquidus and solidus isotherms are presumed to be known by calculation or by thermal measurement. Properties of the semisolid alloy are known (dendity, solidification shrinkage, etc.) so interdendritic flow behavior can be calculated, as shown in Figure 1b. Solidification theory is then employed to calculate macrosegregation, as shown in Figure 1c. More precisely, as noted in the previous paragraph, the equations for flow behavior and segregation must be solved simultaneously.

A. Analysis of Macrosegregation

The derivation of our pressure distribution equation is briefly given below. First, the "equation of continuity" in the mushy zone is given below (12):

$$\frac{\partial}{\partial t} (\rho_{S} g_{S} + \rho_{L} g_{L}) = - \nabla \cdot \rho_{L} g_{L} \vec{v}$$
(1)

where \vec{v} is the interdendritic fluid velocity, ρ_{S} and ρ_{L} are the densities and g_{S} and g_{L} are the volume fractions of the solid and liquid, respectively. According to D'Arcy's Law

$$\vec{v} = \frac{K}{\mu g_L} (-\nabla P + \vec{F}_{gravity} + \vec{F}_{centrifugal})$$
 (2)

where K is specific permeability, P is pressure, μ is viscosity of the interdendritic liquid, $\vec{F}_{gravity}$ is the gravity force and $\vec{F}_{centrifugal}$ is the centrifugal force applied. Substituting Equations (2) into Equation (1), we get

$$\nabla \cdot \left(\frac{K\rho_{L}}{\mu} \quad \nabla P - \frac{K\rho_{L}}{\mu} \quad \vec{F}_{gravity} - \frac{K\rho_{L}}{\mu} \quad \vec{F}_{centrifugal}\right)$$
$$= \left(\rho_{L} - \rho_{S}\right) \left(\frac{\partial g_{L}}{\partial t}\right) + g_{L}\left(\frac{\partial \rho_{L}}{\partial t}\right)$$
(3)

Then, the "local solute redistribution equation" is used to account for the partitioning of solute which takes place in dendritic freezing. That equation is (12)

$$\frac{\partial g_{L}}{\partial t} = -\left(\frac{1-\beta}{1-k}\right) \left(1+\frac{\overrightarrow{v}\cdot\nabla T}{\varepsilon}\right) \frac{g_{L}}{C_{L}} \left(\frac{\partial C_{L}}{\partial t}\right)$$
(4)

where β is the solidification shrinkage, k is the equilibrium partition ratio, ε is the cooling rate, C_L is the liquid composition and T is the temperature. Equation (4) was first derived by Flemings and Nereo (12). It should be pointed out that in the derivation of the "local solute redistribution equation," ρ_S has been assumed constant. Therefore, in our derivation of Equation (3), ρ_S has also been assumed constant. From Figures 2(b) and 3(b), we see that this assumption is quite reasonable for alloys considered herein.

Now with the chain rule Equation (4) can be written as (see Appendix A):

$$\frac{\partial g_{\rm L}}{\partial t} = -\left(\frac{1-\beta}{1-k}\right) \left(1+\frac{\vec{v}\cdot\nabla T}{\epsilon}\right) \frac{g_{\rm L}}{C_{\rm L}}\frac{\epsilon}{m}$$
(5)

Similarly,

$$\frac{\partial \rho_{\rm L}}{\partial t} = \left(\frac{d\rho_{\rm L}}{dC_{\rm L}}\right) \frac{\varepsilon}{m}$$
(6)

where m is the slope of the liquidus line of the phase diagram, and $d\rho_L/dC_L$ is the slope of ρ_L versus C_L curve for the interdendritic liquid during solidification. Finally, assuming the dendritic structure is similar to a bundle of capillary tubes, Mehrabian et al. (15) proposed the following equation for K, the specific permeability:

$$K = \gamma g_{\rm L}^2$$
(7)

where γ is a proportional constant. Substituting Equations (5) - (7), and (2) into (3), and then expanding it into cylindrical coordinate form (note that $\vec{F}_{gravity} = -\rho_L g \vec{z}$ and $\vec{F}_{centrifugal} = \rho_L \omega^2 r \vec{r}$ where g is acceleration due to gravity, ω is rotation speed, \vec{z} and \vec{r} are the axial and the radial unit vectors and r is the radial position), we get the following equation for pressure distribution:

$$\frac{\partial^2 P}{\partial r^2} + \frac{\partial^2 P}{\partial z^2} + A \frac{\partial P}{\partial r} + B \frac{\partial P}{\partial z} + C = 0$$
(8)

where A, B, and C are defined as follows:

$$A = \frac{1}{r} + \frac{2}{g_{L}} \quad \frac{\partial g_{L}}{\partial r} + \frac{1}{\rho_{L}} \quad \frac{\partial \rho_{L}}{\partial r} + \alpha \quad (\frac{\partial C_{L}}{\partial r})$$

$$B = \frac{2}{g_{L}} \quad \frac{\partial g_{L}}{\partial z} + \frac{1}{\rho_{L}} \quad \frac{\partial \rho_{L}}{\partial z} + \alpha \quad (\frac{\partial C_{L}}{\partial z})$$

$$C = g \quad \rho_{L} \quad [\frac{2}{g_{L}} \quad \frac{\partial g_{L}}{\partial z} + \frac{2}{\rho_{L}} \quad \frac{\partial \rho_{L}}{\partial z} + \alpha \quad (\frac{\partial C_{L}}{\partial z}) - \alpha \quad (\frac{\partial C_{L}}{\partial r}) \quad \frac{\omega^{2} r}{g}]$$

$$- \frac{\varepsilon \mu}{m \gamma g_{L}} \quad [\frac{1}{\rho_{L}} \quad \frac{d \rho_{L}}{d C_{L}} + \alpha] - 2 \omega^{2} [\rho_{L} + r \quad \frac{\partial \rho_{L}}{\partial r} + \frac{\rho_{L} r}{g_{L}} \quad \frac{\partial g_{L}}{\partial r}]$$

$$\alpha = \frac{\beta}{(1 - k) C_{L}}$$

The boundary conditions are shown in Figure 4. Since the mold wall is impermeable, $v_r = 0$ at the wall. At the center-line, $v_r = 0$ because of symmetry. At the solidus isotherm, continuity requires that

$$\vec{v}_{E} = -\left(\frac{\rho_{SE} - \rho_{LE}}{\rho_{LE}}\right) \vec{U}_{E}$$
(9)

where \vec{v}_E is the interdendritic fluid velocity at the solidus isotherm, \vec{U}_E is the velocity of the solidus isotherm (eutectic temperature), and ρ_{SE} and ρ_{LE} are the densities of eutectic solid and liquid respectively. Within the bulk liquid pool, we assume no convection so that at the liquidus isotherm the pressure is given approximately by

$$P(\text{liquidus}) = P_0 + \rho_{\text{L0}}g h + \rho_{\text{L0}} \omega^2 r^2 / 2$$
 (10)

where P_0 is the pressure at the top of the liquid pool, ρ_{L0} is the density of the bulk liquid, and h is the height of the liquid pool.

B. Calculation of Macrosegregation

From the measured shape of mushy zone, temperature distribution in the mushy zone, solidification rate and cooling rate, all the unknown variables (except g_{L}) involved in coefficients A, B, and C are determined with the help of the phase diagram and the density-liquid composition diagram (i.e., Figures 2 and 3). To initiate calculations ${\rm g}_{\rm L}$ is approximated using the Sheil Equation (i.e., Equation (4) with eta and $\stackrel{\scriptstyle
ega}{v}$ equal to zero). Now, with the boundary conditions given in Figure 4, Equation (8) is solved for the pressure distribution in the mushy zone. Once the pressure distribution is known, the velocity of interdendritic liquid in the mushy zone is calculated using D'Arcy's Law, Equation (2). With the obtained velocity distribution, the "Local Solute Redistribution Equation", Eqn. (4), is integrated to obtain new values of ${\rm g}_{\rm L}$ which are substituted into A, B and C so that a new pressure and velocity distribution can be recalculated. This procedure is repeated until g_I stops changing. This final g₁ distribution is the correct one. Finally, with this correct $g_{T_{i}}$ distribution in the mushy zone, the local average composition, \bar{C}_{S} , is (12)

$$\bar{c}_{S} = \frac{\rho_{S} \int_{0}^{1-g_{E}} c_{S} dg_{S} + \rho_{SE} g_{E} c_{E}}{\rho_{S} (1 - g_{E}) + \rho_{SE} g_{E}}$$
(11)

where C_E and g_E are the composition and fraction of eutectic, respectively, $g_S = 1 - g_L$, and $C_S = kC_L$.

A simplified version of the flow chart of the computer program is given in Appendix B. The numerical technique used to solve for pressure is based upon finite difference approximations for all derivatives. The finite difference forms of equations needed for the calculations are shown in Appendix C. The computer program is given in Appendix D. A list of computer notations used is given in Table 4 of the appendix.

V. APPARATUS AND EXPERIMENTAL PROCEDURE

Two different types of experimental apparatus were employed and these are each described below. The first (employed for Al-4% Cu alloy) was a small scale ESR unit comprised of a DC power source, a water cooled mold, a consumable electrode, and slag layer as in conventional ESR, Figure 5.

The second type of apparatus employed was one which simulates the solidification behavior of the ESR process, but did not utilize slag. This unit, used for Sn-15% Pb alloy, consisted of a source of molten alloy drops, a cooled mold, and a heat source to simulate the heat input of the ESR process, Figure 6.

Small Scale ESR Unit

A sketch of the apparatus is shown in Figure 5 and, with the exception of the mold, is the same previously used by Basaran et al. (31). The power supply is a D.C. arc-welder capable of providing up to 1600 amp and 40 volts for a total power of 55 KW. The electrode mount is connected to a feed screw about 6 ft long which is driven by one of two gear reduction boxes in series with an electric motor. The driving speed of the electrode can be controlled and operated with a speed in the range of 0.2 - 14 cm/min. The electrodes used were 2024 rods (A1-4% Cu) 1 inch in diameter by 6 feet long.

The dimensions of the copper mold where 3 in. diameter by 9 in. high. A thin wash of graphite powder or alumina powder was applied to the mold wall in order to avoid the attack of the mold by the slag (45% LiCl-55% KC1). Two mold designs were used; the first is shown in Figure 7. The second, shown in Figure 8, was designed for the convenience of replacing the mold wall whenever the mold failed due to the slag attack. This design also made it easy to insert up to 5 thermocouples into the ingot during a run. With both molds, an aluminum bottom hearth was used to insure good bottom welding at the start-up and to prevent the start-up arc from damaging the copper bottom chill.

About 250 cc. of liquid slag of eutectic composition (45wt% LiCl and 55wt% KCl) was poured into the mold at start-up. Immediately after pouring the slag, melting was initiated with a power of 10 KW. The cooling water was turned on and then the power lowered to the working value between 2 and 4 KW. The amperage was kept constant by adjusting the driving speed of the electrode. The electrode position was recorded on a chart recorder during each run. When thermal data were obtained, five chromel-alumel thermocouples were inserted into the mold and pushed to predetermined positions (shown as "X's" in Figure 5) immediately after the electrode passed these positions, and their output recorded. Cooling curves were used to determine the shape of mushy zone, temperature distribution, cooling rates and solidification rates. Thermal data for two ingots (Nos. 1 and 2) were obtained with the second mold design (Figure 8).

Ingot No. 3, made in the first mold design (Figure 7) was doped with about five grams of Al-50% Cu to reveal the liquid pool shape. The ingots were cut into sections in order to obtain analysis by X-ray

fluorescence, which was used to detect macrosegregation across the ingots, and in order to obtain samples for microstructures.

Simulated ESR Apparatus

A sketch of the apparatus is shown in Figure 6. The stainless steel mold is 3-1/4 in. in diameter and 13 in. long. The metal pool inside the mold is heated with six 3 in. long resistance heaters connected in parallel. These heaters are positioned inside holes drilled into a 3 in. long by 1-1/4 in. diameter stainless steel bar. Power input is controlled with a Variac transformer.

Cooling water or air runs through a movable cooling jacket surrounding the mold. Both the resistance heaters and the cooler are fixed to the same system used for driving the electrodes in making the Al-4% Cu ingots. Thermal measurements are made with three chromel-alumel thermocouples located inside three vertical stainless steel tubes. The tubes are fixed but the position of the thermocouples is varied during a run by sliding them up and down inside the tubes.

Flow of liquid Sn-15% Pb alloy from the top stainless steel container is controlled by an adjustable valve. Heating of the melt in the top container is done with two 1.5 in. wide band heaters which are controlled by a thermocouple hooked up with a temperature controller. A stirrer was used to insure uniform temperature and composition in the liquid supply.

Tin (99.9%) and lead (99.9%) were melted and stirred well in a crucible furnace. About one-fourth of the charge was poured into the

stainless steel mold until the liquid level rose to almost the top of the resistance heaters (about 3.5 in. from the bottom of the mold). The remaining alloy was then poured into the top container. The band heaters, the resistance heaters and cooling water were then turned on.

With the resistance heaters and the cooling jacket fixed, the initial position and the shape of the mushy zone were determined by moving the three thermocouples up and down and locating the position of the liquidus and solidus temperatures of the alloy. Power input to the heaters and cooling jacket position were adjusted until the desired position and shape of mushy zone were obtained.

The resistance heaters and the cooler were then moved upwards at a predetermined speed, and the valve for supply of liquid metal adjusted so that the liquid level inside the mold rose at the same speed. As solidification progressed the three thermocouples were moved up and down in order to determine the temperature distribution in the mushy zone. In the case of rotating ingots, the mold was seated on a turn-table (Fig. 9). One thermocouple was located inside the central stainless steel tube. As in the case of no mold rotation, this thermocouple was allowed to slide up and down in order to trace the positions of solidus and liquidus isotherms. Due to the rotation of the mold, thermocouples inside the other two stainless steel tubes could not be slid up and down. Therefore, inside each of these tubes three thermocouples were located and fixed at different heights. All six of these thermocouples were connected to a slip ring for the purpose of thermal measurement.

The heaters for the liquid pool inside the mold also rotated with the mold in this case.

After casting, the ingots were cut into sections for microstructural study and analysis by X-ray fluorescence to determine macrosegregation.

Chemical Analysis

Chemical analysis of macrosegregation in the ingots was by X-ray fluorescence. A General Electric X-ray diffraction unit (model XRD3, Type 1) was used with a Mo tube. The primary white radiation from the tube fluoresced the samples on an area of 0.32 cm. diameter. This area covered many dendrite arms (secondary dendrite arm spacing is about $40^{0.65\mu}$) and therefore the compositions measured were local average compositions.

The secondary radiation from the sample was received by a Si (Li) X-ray detector and the intensity of the characteristic line (K_{α} for Cu and L_{α} for Pb) was compared with a standard intensity versus composition curve to determine the composition.

The standards were prepared from rapidly cooled thin sections of known compositions. The Al-Cu standards used were those prepared by Nereo (14). The Pb-Sn standards were prepared by melting lead and tin together in a graphite crucible to form the liquid alloy of desired composition. About 5 grams of the liquid alloy was quickly removed from the crucible and dropped 1.5 feet onto a copper chill (1.5 inches x 6 inches x 10 inches). The descending drop hit the copper and solidified very rapidly as a splat. A significant portion of the splat formed an area which was similar to a thin disk (about 0.8 mm thick and 2 inches in diameter) with a very smooth and flat bottom surface. A rectangular plate (0.8 inch x 1.2 inches) was cut from the disk and polished with 600 grit metallographic paper for X-ray fluorescence. The remainder of the disk was analyzed by wet chemical analysis to serve as a standard.

VI. RESULTS

A. Experimental Results

Aluminum-4% Copper ESR Ingots

Results of three ingots are summarized in Table 1. The isotherms for Ingots 1 and 2 were obtained from thermal measurements; for Ingot 3, the shape of the isotherm was determined by doping.

Ingot 1 (A1-4.4% Cu)

The cooling curves obtained from the thermocouples as positioned in Figure 8 are given in Figure 10. Figure 11 shows plots of the position of the liquidus isotherm (Z_L) and eutectic isotherm (Z_E) at the center of the ingot. After steady state is achieved, the isotherms move with a vertical speed of 0.053 cm/s. Figure 12 shows the isotherm positions across the ingot.

Figures 11 and 12 can be used to construct the shape of the mushy zone as given in Figure 13a after 7 minutes of ingot solidification has elapsed. As a consequence of cooling rate not varying with radius, the isotherms are parallel. Figure 14 shows the measured temperature distribution along the centerline.

Figure 13c shows the macrosegregation in Ingot 1. The overall analysis of the ingot is 4.4% Cu; as a result of solidification, there is positive segregation at the surface (4.6% Cu) and negative segregation at the center (4.25% Cu). Macroetching showed no evidence of localized segregates, such as "freckles" or "V"-segregates. Dendrite cell size, \overline{d} , in this ingot was also measured (Fig. 15). No variation in d across the ingot was observed which, of course, is predictable by the fact that cooling rate during solidification is also constant across the ingot.

Ingot 2 (A1-4.4% Cu)

This ingot was cast in the same manner as Ingot 1 with the exception that an unusually thick (about 3 mm.) coating of mold wash (graphite and powdered zirconia) was applied to the inside mold wall. As a result, solidification was unidirectional.

Figures 16 and 17 show cooling curves and isotherm positions, respectively. From Figure 16, we see that temperature is independent of radius, so isotherms must be flat. Cooling rate during solidification is about equal to that observed in Ingot 1, and consequently dendrite cell size is also equal (61µ) (Fig. 15). Figure 18 shows the mushy zone after 7 minutes have elapsed. Since solidification is unidirectional, no macrosegregation is detected in this ingot; nor is there any evidence of localized segregates found in an etched macrosection.

Ingot 3 (A1-4.2% Cu)

Thermal data for Ingot 3 were not measured, but with isotherm shape obtained by doping, the thermal history can be constructed with a knowledge of the electrode melting rate and cooling rate (32) (calculated from dendrite cell sizes). Figure 19 shows the etched macrostructure of Ingot 3. The isotherm is not exactly symmetrical because the electrode was not centered exactly. Dendrite cell size is also uniform across
this ingot (61 μ , Fig. 15); therefore the isotherms are considered to be parallel to each other.

The degree of macrosegregation for Ingot 3 is shown in Figure 20b. The extent of segregation is considerably less than that of Ingot 1.

Tin-Lead Simulated ESR Ingots

Results of macrosegregation in the series of the Al-4% Cu experimental ingots show that severely localized segregates, as sometimes found in large commercial ESR ingots, cannot be produced using this alloy cast by ESR in small laboratory scale (3 inches in diameter) molds. Although surface-to-center compositional variations were produced, these variations are rather modest and no severe-localized segregates were detected. It was decided, therefore, to design laboratory experiments which could be used to study a wider range of segregation problems encountered in ESR ingots. Accordingly, experimental efforts were directed towards solidifying Sn-Pb alloy in the simulated ESR apparatus (Figure 6). Results from three ingots are summarized in Table 2.

Ingot 4 (Sn-15% Pb)

The positions of the solidus and the liquidus at three radii are given in Figure 21. After 9 minutes steady state was achieved and the isotherms moved with a vertical speed of 4.0×10^{-3} cm/sec, about one order of magnitude less than that obtained in the Al-4% Cu ingots. From Figure 21 the shape of mushy zone after 25 min. is plotted in Figure 22a and the secondary dendrite arm spacing shown in Figure 23. The measured temperature distribution along the centerline is shown in Fig. 24.

In this ingot the resulting macrosegregation across the ingot is pronounced (Figure 22c). The composition ranges from 11.7% Pb at the edge of the ingot to 28.2% Pb at the center. Microstructures show no evidence of "freckles" in this ingot.

Ingot 5 (Sn-15% Pb)

The positions of the solidus and the liquidus during solidification were recorded for this ingot in the same manner as for Ingot 4 isotherms. At steady state, the isotherms moved with a vertical speed of 7.0 x 10^{-3} cm/sec, Figure 25. Figure 26a shows the shape of mushy zone at 14 min., and the measured secondary dendrite arm spacing is shown in Figure 23.

The macrosegregation is shown in Figure 26c which shows that the composition ranges from 7% Pb at the mid-radius of the ingot to 28% Pb at the center. This segregation pattern is more severe than in Ingot 4 (Figure 22c), and the microstructures show clear evidence of "freckling" in this ingot (Figure 27).

Ingot 6 (Sn-15% Pb)

In this ingot, steady state solidification was not achieved until after 20 min. when the isotherms moved with a vertical speed of 5.1×10^{-3} cm/sec (Figure 28). The shape of mushy zone after 23 min. is plotted in Figure 29a and the greater secondary dendrite arm spacings shown in Figure 23 reflect a lower cooling rate than in Ingots 4 and 5.

As seen in Figure 29c, macrosegregation across this ingot is even more severe than in Ingot 5; composition varies from 11.5% Pb at the edge of the ingot to 38% Pb (eutectic composition) at the center of the ingot. The microstructures (Fig. 30) show that along the centerline there is a large channel or "freckle"; other areas show no evidence of "freckling."

Tin-Lead Simulated ESR Ingots with Mold Rotation

Results of macrosegregation in the series of Sn-Pb ingots (Ingots 5 and 6) show not only very severe surface-to-center compositional variations, but also "freckles". It was decided to rotate the mold during casting in order to study the effect of centrifugal force on macrosegregation.

Ingot 7 (Sn-12% Pb)

This ingot was cast with three different rotation speeds: 0 rpm, 45 rpm and 76 rpm. The measured shapes and positions of the mushy zone 25 minutes, 50 minutes and 75 minutes after the start are shown in Fig. 31. The solidification rate was 3.0×10^{-3} cm/sec. The macrosegregation results are shown in Fig. 32. It can be seen in Fig. 32 that the degree of macrosegregation was slightly reduced in the case of 45 rpm rotation, but was reduced significantly in the case of 76 rpm rotation. Microstructures showed "freckling" at the center of the ingot for zero and 45 rpm. rotations (Fig. 33), but no "freckling" was observed in the case of 76 rpm rotation.

Ingots 8^{12} were cast with detailed thermal measurement. Each ingot was cast under one single rotation speed and in each ingot solidification reached state at about 10^{25} minutes after the start. Results from these five ingots are summarized in Table 3.

Ingot 8 (Sn-12.4% Pb)

Results of thermal measurements are shown in Figs. 34, 35 and 36. At steady state, the isotherms moved with a vertical speed of 5.6×10^{-3} cm/sec. The shape of the mushy zone 30 minutes after the start is shown in Fig. 37a. The rotation speed was 83 rpm (8.7 rad./sec). The measured dendrite arm spacings are given in Fig. 38.

The macrosegregation is shown in Fig. 37c. The composition ranges from 11% Pb at the edge of the ingot to 19% Pb at the center. Microstructures show no evidence of freckles.

Ingot 9 (Sn-14.0% Pb)

Results of thermal measurement are given in Figs. 39, 40 and 41. At steady state, the isotherms moved with a vertical speed of 6.6 x 10^{-3} cm/sec. The shape of the mushy zone 28 minutes aftet the start is given in Fig. 42a. The rotation speed was 97 rpm (10.1 rad/sec). Dendrite arm spacings are shown in Fig. 38. The resulting macrosegregation is shown in Fig. 42c. The W-shape composition profile is the result of rotation. Microstructures show no evidence of freckles.

Ingot 10 (Sn-12.8% Pb)

Results of thermal measurement are given in Fig. 43, 44 and 45. At steady state, the isotherms moved with a vertical speed of 5.3×10^{-3} cm/sec. The shape of the mushy zone 30 minutes after the start is given

in Fig. 46a. The rotation speed was 119 rpm (12.5 rad/sec). Dendrite arm spacings are shown in Fig. 38. The resulting macrosegregation is shown in Fig. 46c. The composition is relatively uniform across the ingot except near the edge where it jumps to nearly the eutectic composition. This can be seen from the microstructures at the wall, Fig. 47 and 48. The evidence of "freckling" at the wall is very clear.

Ingot 11 (Sn-12.4% Pb)

Results of thermal measurement are given in Figs. 49, 50 and 51. At steady state, the isotherms moved with a vertical speed of 8.3×10^{-3} cm/sec. The shape of mushy zone 35 minutes after the start is given in Fig. 52a. The rotation speed was 66 rpm. The dendrite arms spacings are shown in Fig. 38.

The macrosegregation is given in Fig. 52c. The composition jumps to approximately 25% Pb at about 0.8 cm from the wall, where the slopes of the isotherms go up drastically. The microstructures show clear evidence of "freckling" at this position, Fig. 53.

Ingot 12 (Sn-12% Pb)

Results of thermal measurement are given in Figs. 54, 55 and 56. At steady state, the isotherms moved with a vertical speed of 1.36×10^{-2} cm/sec. The shape of mushy zone at 12 minutes after the start is given in Fig. 57a. The rotation speed was 54 rpm. The dendrite arm spacings are shown in Fig. 38.

The macrosegregation is shown in Fig. 57c. As expected, the macrosegregation is slight because the solidification rate was high. Micro-

structual show no evidence of "freckles".

B. Comparison Between Experimental and Calculated Results

Aluminum-Copper ESR Ingots

Calculation of flow lines and macrosegregation were done using the phase diagram and density data for Al-Cu system as shown in Figures 2b and c, respectively. The value of viscosity used was 1.3 centipoises (33, 34). The value of γ used is on the order of 10^{-7} cm² which agrees with the value used by Mehrabian et al. (16) to obtain the best fit between their theoretical and experimental results of macrosegregation in Al-4.5% Cu ingots.

Ingot 1 (A1-4.4% Cu)

With γ equal to 5 x 10⁻⁷ cm² the agreement between theory and the experiment is quite good for most part of the ingot (Figure 13c). Flow lines based on the calculated velocity distribution of the interdendritic liquid are shown in Figure 13b. The spacing of the flow lines is approximately proportional to the inverse of velocity magnitude.

Flow is predominantly downward and outward, Figure 13b, and so segregation, calculated and observed, is negative at the center, Figure 13c.

Ingot 2 (A1-4.4% Cu)

The value of γ was again 5 x 10⁻⁷ cm². Calculations show no macrosegregation, which is in agreement with the experiment. Flow lines are downward and vertical as expected and consistent with the absence of macrosegregation.

Ingot 3 (A1-4.2% Cu)

The mushy zone was not symmetrical because as previously mentioned the electrode was not centered exactly; however for calculations we assume a symmetrical mushy zone (Figure 20a). The width of the mushy zone (vertical distance between the solidus and liquidus) is constant since cooling rate was also independent of radius as indicated by a constant dendrite cell size (61 microns) across the ingot.

The degree of macrosegregation for ingot 3 is shown in Figure 20b. The extent of segregation is less than that of Ingot 1. Calculations with $\gamma = 3 \times 10^{-7}$ cm² agree remarkably well with experiment except that the minimum point in the experimental curve is off-center.

Tin-Lead Simulated ESR Ingots

Calculation of flow lines and macrosegregation were done using the phase diagram and density data for the Sn-Pb system as shown in Fig. 3a and b, respectively. The value of viscosity used was 2.2 centipoises (35).

In Ingots 4, 5, and 6, the width of the mushy zone and the cooling rate vary from center to surface. This is seen in Figure 23 which shows a decrease in the secondary dendrite arm spacing in going from the center to the surface. The calculations take into account this variation by making permeability (and, hence, γ) a function of the secondary dendrite arm spacing. Data of Streat and Weinberg (36) show that permeability varies with square of secondary dendrite arm spacing, d, for 25<d<60 microns. Accordingly, we select a value of γ at the centerline (γ_{α}) and vary γ according to

$$\gamma/\gamma_{o} = (d/d_{o})^{2}$$
⁽⁷⁾

Ingot 4 (Sn-15% Pb)

Calculations of flow lines and macrosegregation are shown in Figures 22b and 22c respectively. With $\gamma_0 = 3.7 \times 10^{-6} \text{ cm}^2$, the calculated result of macrosegregation agrees reasonably well with experiment. Since permeability in lead-rich Pb-Sn alloys (36) is reported to be $10^1 - 10^2$ greater than the value of permeability for aluminum alloys (37, 38), it is reasonable that γ is on the order of 10^{-6} cm^2 assuming similar behavior of tin-rich and lead-rich Sn-Pb alloys.

The calculated flow pattern, shown in Figure 22b shows that gravity has a very strong effect on the flow, causing the interdendritic liquid to flow from the surface towards the ingot center and up near the center resulting in positive segregation in the center of the ingot. It will be seen that such flow (from "cold" to "hot" regions in the mushy zone), when sufficiently strong, leads to localized channels of increased flow and the formation of freckles.

Ingot 5 (Sn-15% Pb)

A value of γ_o was selected by using the best value determined for Ingot 4 ($\gamma_o = 3.7 \times 10^{-6} \text{ cm}^2$) and adjusting for the decrease in secondary arm spacing at the centerline (Figure 23). This gives $\gamma_o = 2.4 \times 10^{-6} \text{ cm}^2$. Flow calculations show that $(\vec{v} \cdot \nabla T/\epsilon) < -1$ in Equation (4), and hence $\partial g_T / \partial t > 0$ in these regions of the ingot. This phenomenon is discussed in more detail below. Essential points are that, when $\vec{v} \cdot \nabla T/\epsilon < -1$, (a) "freckles" can form, and (b) the method of quantitatively calculating macrosegregation is no longer valid.

Figure 26b shows calculated flow lines with permeability decreased to the point that their directions are observed just at the onset of developing a flow instability. With $\gamma_o = 2.0 \times 10^{-7} \text{ cm}^2$, $(\vec{v} \cdot \nabla T/\epsilon) > -1$ throughout the entire mushy zone. With permeability decreased by almost one order of magnitude, the flow is still towards the centerline and upwards at the center. Flow is strongly enhanced in Ingot 5 over that in Ingot 4, because the isotherms in the mushy zone are significantly deeper; this difference is apparent in Figures 22a and 26a. With $\gamma_o > 2.0 \times 10^{-7} \text{ cm}^2$, the flow is stronger than indicated in Figure 26b, and the formation of freckles is predicted as observed in Figure 27.

Ingot 6 (Sn-15% Pb)

As with Ingot 5, when permeability is selected to correspond to the dendrite arm spacing in Figure 23 ($\gamma_0 = 4.4 \times 10^{-6} \text{ cm}^2$), calculations indicate ($\vec{v} \cdot \nabla T/\epsilon$)<-1 in the central regions of the ingot predicting the formation of a freckle. The flow lines shown in Figure 29b are calculated using $\gamma_0 = 8 \times 10^{-7} \text{ cm}^2$; with greater values, the instability develops. Figure 29b however does indicate that the overall interdendritic flow is similar to that observed in Ingots 4 and 5. Macrosegregation in Ingot 6 is more severe than in Ingot 5 because the local solidification time is significantly greater (Figure 23).

Tin-Lead Simulated ESR Ingots with Mold Rotation

Ingot 8 (Sn-12.2% Pb)

The calculated flow pattern and macrosegregation are shown in Fig. 37b and c, respectively. The value of γ_0 used was $1.2 \times 10^{-6} \text{ cm}^2$, which was obtained from the best fit between the theoretical and experimental results. This value is close to the value estimated from Equation (7) and the dendrite arm spacings (Figs. 23 and 38), $\gamma_0 = 2.0 \times 10^{-6} \text{ cm}^2$ (see Fig. 58). Therefore, as with no mold rotation, the agreement between theory and experiment is reasonably good.

Ingot 9 (Sn-14.0% Pb)

The calculated flow pattern and macrosegregation are shown in Fig. 42b and c,respectively. A value of $\gamma_o = 0.98 \times 10^{-6} \text{ cm}^2$ was obtained from the best fit between measured and calculated results. The corresponding value estimated from the dendrite arm spacing measurements is 1.0 x 10^{-6} cm² (see Fig. 58). The agreement is, therefore, excellent.

Ingot 10 (Sn-12.8% Pb)

The calculated flow pattern and macrosegregation are shown in Fig. 46b and c respectively. A value of $\gamma_0 = 1.3 \times 10^{-6} \text{ cm}^2$ was obtained from the best fit between theoretical and experimental results. The corresponding value estimated from the dendrite arm spacing measurement is $1.1 \times 10^{-6} \text{ cm}^2$ (see Fig. 58). Again, the agreement is very good.

The calculated flow pattern shown upward interdendritic fluid flow near the wall. Calculations also indicate $(\stackrel{\rightarrow}{v} \cdot \nabla T/\epsilon) < -1$ here predicting

the formation of freckles.

Ingot 11 (Sn-12.4% Pb)

The calculated flow pattern and macrosegregation are shown in Fig. 52b and c, respectively. The value of γ_0 estimated from the dendrite arm spacing measurements, 3.3×10^{-6} cm², was used in the calculation. The agreement between calculated and experimental macrosegregation results are not as good as Ingots 8-10. However, the calculations do show the peaks in the concentration profile, though the positions of these peaks are not exactly the same as the observed ones.

The calculated flow pattern shows upward interdendritic fluid flow in the region between the mid-radius and the wall. The calculations also indicate $\vec{v} \cdot \nabla T/\epsilon < -1.0$ in this region predicting the formation of "freckles."

Ingot 12 (Sn-12.0% Pb)

The calculated flow pattern and macrosegregation are shown in Fig. 57b and c, respectively. A γ_0 value of 1.0 x 10^{-6} cm² was obtained from the best fit between the calculated and experimental macrosegregation results. The corresponding value estimated from the dendrite arm spacing measurement is 1.43 x 10^{-6} cm² (see Fig. 58). Therefore, the agreement is reasonably good.

VII. DISCUSSION

1. Effect of Solidification Time and Permeability

Both the Al-4% Cu ingots (1 and 3) and Sn-15% Pb ingots (4, 5 and 6) have concave shapes of mushy zone, and in both alloys, (1) the equilibrium partition ratio k is less than one and (2) the density of the interdendritic liquid increases progressively during solidification. However, the Al-4% Cu ingots have negative center-line macrosegregation while the Sn-15% Pb ingots have positive center-line macrosegregation. The reason for this can be explained as follows.

In a concave mushy zone, solidification shrinkage tends to suck the solute-rich interdendritic liquid toward the solidus isotherm and, therefore, the solute-rich interdendritic liquid in the mushy zone tends to flow downwards and outwards (see, for example, Fig. 13b). But, at the same time, the gravity effect also tends to cause flow of the dense, solute-rich interdendritic liquid from the upper, outer region of the mushy zone to the lower, central region of the mushy zone (see, for example, Fig. 26b). Therefore, the convection effects of solidification shrinkage and gravity compete during solidification. If the shrinkage effect dominates, solute is diverted away from the center-line of the ingot and, therefore, negative center-line macrosegregation will occur. On the other hand, if the gravity effect dominates, solute will be accumulated along the center-line of the ingot and, therefore, positive centerline macrosegregation will occur. Both solidification time and permeability are very important in determining whether solidification shrinkage or gravity will dominate. According to the continuity requirement, the interdendritic liquid always feeds solidification shrinkage (1) no matter whether the solidification time is long or short and (2) no matter whether the permeability is high or low. But, if the solidification time is too short and the permeability is too low, the interdendritic liquid is already sucked toward the solidus isotherm by the solidification shrinkage before gravity has sufficient time to affect significantly the flow pattern of the interdendritic liquid. Therefore, solidification shrinkage is more likely to dominate when the solidification time is short and the permeability is low. Conversely, the gravity effect is more likely to dominate if the solidification time is long and the permeability is high.

In short, since the Al-4% Cu ingots were produced with a much greater (10 times faster) vertical solidification rate and a narrower mushy zone than were the Sn-15% Pb ingots, the solidification time of Al-4% Cu ingots was much shorter than that of Sn-15% Pb ingots. Also, as mentioned before, the permeability of Al-4% Cu alloy is 10^{1} - 10^{2} less than that of Sn-15% Pb alloy. Therefore, solidification shrinkage dominated in the Al-4% Cu ingots during solidification and resulted in negative center-line macrosegregation. The gravity effect dominated in the Sn-15% Pb ingots during solidification and resulted in the Sn-15% Pb ingots during solidification and resulted in the Sn-15% Pb ingots during solidification and resulted in the Sn-15% Pb ingots during solidification and resulted in the Sn-15% Pb ingots during solidification and resulted in freckling as well as positive center-line macrosegregation.

2. Effect of Mushy Zone Shape

The three A1-4% Cu ingots were cast with the same local solidification time since secondary dendrite arm spacings are equal. However, the results show that the deeper the shape of mushy zone, the greater the degree of negative center-line macrosegregation. This is because, in a deep mushy zone, the solute-rich interdendritic liquid is sucked toward the steep solidus isotherm and the solute is diverted away from the center-line of the ingot. Therefore, a greater degree of negative center-line macrosegregation results. Of course, if there is vertical unidirectional solidification, no macrosegregation results.

As another example of this effect, let us now consider Ingot 4 and Ingot 5 of Sn-15% Pb alloy. The upward solidification rate of Ingot 5 is about twice the value of Ingot 4 while the width (i.e., vertical distance from solidus to liquidus) of the mushy zone of Ingot 5 is slightly smaller than that of Ingot 4. Therefore, the solidification time of Ingot 5 is less than that of Ingot 4. This can also be seen from secondary dendrite arm spacings shown in Figure 23 (smaller secondary dendrite arm spacing means shorter solidification time.) However, the shape of the mush zone of Ingot 5 is much deeper than that of Ingot 4. Therefore, the resultant macrosegregation of Ingot 5 is still more severe than that of Ingot 4.

The effects of solidification time and shape of mushy zone on macrosegregation are further illustrated in Figure 59. Here, macrosegregation has been calculated in Al-4.4% Cu ESR ingots of geometry studied in this work, for different solidification conditions. Calculated flow lines and macrosegregation are shown for two different solidification times (solidification time = $(Z_L-Z_S)/R$, where Z_L-Z_S is the width of mushy zone and R is the upward solidification rate) and for mushy zones of three different degrees of concavity (i.e., three different "depths" where depth refers to distance from the highest to the lowest point in the mushy zone). Note that for both short and long solidification time, the degree of macrosegregation increases with increasing depth of mushy zone. In the case of short solidification time (a, b and c), we have negative centerline macrosegregation, while in the case of long solidification time (d, e and f), we have positive centerline macrosegregation.

3. The Dimensionless Group, $\vec{v} \cdot \nabla T/\epsilon$

According to macrosegregation theory (4, 5), the important dimensionless parameter affecting macrosegregation is $\vec{v} \cdot \nabla T/\epsilon$. When this is equal to $\beta/1-\beta$ no macrosegregation results; when it is greater, segregation is negative and when it is less, segregation is positive. Figure 60a shows a plot, for Ingot 1, of $\vec{v} \cdot \nabla T/\epsilon$ at the centerline during solidification (i.e., as C_L increases from C_0 to C_E). $\vec{v} \cdot \nabla T/\epsilon$ is greater than $\beta/1-\beta$ throughout solidification, resulting in a lower composition of solid forming at any time during solidification and a lower fraction eutectic than would form in the absence of segregation (Figure 60b). Hence segregation is negative here.

Figure 61 is a plot similar to that of Figure 60 in all respects except that here $\overrightarrow{v} \cdot \nabla T/\varepsilon$ is less than $\beta/1-\beta$ and so segregation is positive. This plot applies to the centerline of Ingot 4. Note in Ingot 4 that $\vec{v} \cdot \nabla T/\epsilon$ is never less than -1. At the critical point where this occurs, flow velocity in the direction of isotherm movement is greater than velocity of isotherms and "remelting" occurs. This is the criterion for formation of freckles (15). $\vec{v} \cdot \nabla T/\epsilon$ was calculated to be less than -1 in Ingots 5, 6, 10 and 11, and here, as expected, "freckles" (channel type segregates) were observed.

4. Effect of Centrifugal Force

The experimental results from Ingot 7 demonstrate clearly the effect of centrifugal force on reducing the macrosegregation across the ESR ingots and eliminating "freckles". The quantitative effect of the centrifugal force can be better demonstrated with the help of the computer model. Figure 62 shows the calculated macrosegregation for different rotation speeds. The mushy zone of Ingot 8 was used in all of these calculations. The γ value of Ingot 8 was used, as well.

As can be seen in Fig. 62, without mold rotation, there is very severe positive centerline macrosegregation and pronounced "freckling" at the center of the ingot. With increasing rotation speed the high solute concentration at the centerline decreases and the low solute concentration at the wall increases. Freckling at the centerline also disappears. At higher rotation speeds (e.g. $\omega = 13.0 \text{ rad./sec}$), the concentration profile resembles the shape of a "W". At even higher rotation speeds (e.g., $\omega = 15 \text{ rad./sec}$), the solute-rich interdendritic liquid is pushed to the wall and is forced to flow upwards. Therefore, "freckling" as well as positive macrosegregation develops near the wall. As can be seen from Figs. 62 and 63 (similar to Fig. 62 except the solidification rate is **hig**her), the optimum concentration profile can be obtained if a suitable rotation speed is applied in this ingot (e.g., $\omega = 12 \text{ rad/sec}$).

The effect of centrifugal force on macrosegregation across ESR ingots is affected by the solidification rate. Examination of Figs. 62 and 63 shows that the effect of centrifugal force is more pronounced at lower solidification rates. This can be seen more clearly in Fig. 64, where $\Delta C/C_o$ is plotted vs. ω^2 . ΔC is the concentration at the ingot center minus the concentration at the edge, and C_o is the original concentration. As can be seen in this figure, at high solidification rates (e.g., 0.056 cm/sec), the macrosegregation is very slight and the centrifugal force has hardly any effect on the macrosegregation. However, when the macrosegregation is severe due to a very slow solidification rate (e.g., 0.0035 cm/sec), sufficient mold rotation not only reverses the concentration profile from positive centerline segregation to negative centerline segregation, but also changes the location of freckling from the center of the ingot to the edge.

Finally, it is to be noted that although Fig. 64 shows the strong influence of the solidification rate on the effectiveness of the centrifugal force, it also shows that the optimum rotation speed for minimizing the macrosegregation is independent of solidification rates (e.g., $\omega = 12$ rad/sec for this ingot).

VIII. CONCLUSION

1. Laboratory-scale ESR apparatus was used to make a series of Al-4% Cu ingots with a solidification rate of about 4 x 10^{-2} cm/sec. Macro-segregation in these ingots varied from no macrosegregation in an ingot with a flat mushy zone to 4.25% Cu at the center and 4.6% Cu at the edge for an ingot with a deep mushy zone (C₀ = 4.4% Cu).

2. Apparatus for simulating the ESR process was used to make a series of Sn-15% Pb ingots with a solidification rate of about 5 x 10^{-3} cm/sec. Compositions as rich as 38% Pb (freckling) at the center and as poor as 7% Pb at the edge were found, depending on solidification conditions.

3. The apparatus for simulating the ESR process was modified to allow rotation of the ingot. A series of rotated Sn-Pb ingots $(12 \lor 14\% \text{ Pb})$ was made in this way. Solidification rates were varied from 5.3×10^{-3} cm/sec to 1.36×10^{-2} cm/sec and rotation speeds were varied from 54 rpm to 119 rpm. The centerline composition varied from 9% Pb higher than the edge composition to 20% Pb lower than it (freckling at the edge).

4. Calculations which predict macrosegregation in ESR ingots compare very well with experimental results. The calculated interdendritic fluid flow patterns clearly demonstrate the influence of solidification shrinkage and gravity on the observed macrosegregation across experimental ESR ingots. 5. The effects of the important solidification parameters such as the upward solidification rate and the depth of the mushy zone on macrosegregation in ESR ingots can be evaluated quantitatively.

6. The computer model developed predicts correctly the conditions which cause the formation of "freckles".

7. Severe positive centerline macrosegregation can be reduced significantly and freckling at the center of the ESR ingots can be eliminated if a suitable speed of mold rotation is applied during solidification. The computer model can be applied to predit the optimum rotation speed for minimizing macrosegregation and eliminating freckles.

8. The effect of centrifugal force on macrosegregation across ESR ingots is influenced by the solidification rate. At high solidification rates (e.g., 10^{-2} cm/sec) the macrosegregation is slight and the centrifugal force has little effect on the macrosegregation. However, when macrosegregation is severe due to a very slow solidification rate (e.g., 10^{-3} cm/sec), a very fast rotation speed (e.g., 150 rpm) not only reverses the concentration profile from positive centerline segregation to negative centerline segregation, but also changes the location of freckling from the center of the ingot to the edge.

9. The optimum rotation speed for minimizing the macrosegregation is independent of solidification rates.

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(a)









(a)



Figure 2: Phase diagram and density used for calculations of macrosegregation in A1-4% Cu ESR ingots.(a) Phase diagram, Ref. 39; (b) density of solid and liquid during solidification, Ref. 15.



(a)



⁽b)

Figure 3: Tin-lead system. (a) Phase diagram (from ref. 40);
 (b) densities of solid and liquid phases during
 solidification computed with data from refs. 41-44.



Figure 4: Boundary conditions used in solving for flow of interdendritic liquid



Figure 5: The experimental set-up used to study macrosegregation in A1-4% Cu ESR ingots



Figure 6: Apparatus used as an analog ESR process to produce Sn-15% Pb ingots.



Figure 7: ESR mold design with brazed cooling-water jacket.



Figure 8: Design with replaceable mold wall. Numbers indicate thermocouples.



Figure 9: Apparatus used as an analog ESR process to produce Sn-Pb ingots with mold rotation.

Table I. Results of AI-Cu Ingots

Ingot #	I	3	2
Solid'n Rate	5.3 x 10 ⁻² cm/sec	4.0 x 10 ⁻² cm/sec	3.2 x 10 ⁻² cm/sec
Shape of Mushy Zone	12 - 6.8 cm -	12 8	12 - 6.8cm - 8
Macrosegre- gation	5 ⁰ 4	4.4	4.6 4.4 0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-0-
Freckle	Νο	No	No
Solid'n Time	68 sec	68 [°] sec	70 sec
Comment	Increasing Depth of Mushy Zone		



Figure 10: Cooling curves for Ingot 1 (A1-4.4% Cu). Numbers refer to thermocouples shown in Figure 8.







Figure 12: Liquidus and solidus isotherms with respect to radius at 7.6 cm from the bottom in Ingot 1 (A1-4.4% Cu).


Figure 13: Results obtained for Ingot 1 (A1-4.4%CU).

- (a) Liquidus and solidus isotherms after 7 min.;
 - (b) flow lines of interdendritic liquid;
 - (c) macrosegregation as measured (solid curve) and calculated with $\gamma = 5 \times 10^{-7} \text{ cm}^2$ (broken curve).



Figure 14: The temperature gradient in Ingot 1 (A1-4.4%Cu).



Figure 15: Dendrite cell sizes in the Al-4% Cu ingots.



Figure 16: Cooling curves for Ingot 2 (A1-4.4% Cu).



Figure 17: The liquidus and solidus isotherms in Ingot 2 (A1-4.4% Cu).



Figure 18: The shape of the mushy zone at 7 minutes in Ingot 2 (A1-4.4% Cu).



Figure 19: Isotherm detected by doping Ingot 3 (A1-4.2% Cu).



Figure 20: Ingot 3 (A1-4.2% Cu). (a) Position of isotherms used for calculations; (b) macrosegregation by experiment (solid curve) and by calculation with $\gamma = 3 \times 10^{-7} \text{ cm}^2$ (broken curve).

Ingot #	4	5	6		
Solid'n Rate	4.0 x 10 ⁻³ cm/sec	7.0x10 ⁻³ cm/sec	5.1 x 10 ⁻³ cm/sec		
Shape of Mushy Zone	15 10	10	15 8 cm		
Macrosegre- gation					
Freckle (Transverse Cross Section)	N o				
Solid'n Time	900 sec at 🗲	457 sec at €	980 sec at €		
Comment	Flat Mushy Zone	Steep Mushy Zone Shorter Solid'n Time	Steep Mushy Zone Longer Solid'n Time		
	Increasing "+" & Macrosegregation				

Table 2. Results of Sn-Pb Ingots without Rotation



Figure 21: Positions of the liquidus and solidus isotherms in Ingot 4.



Figure 22: Results obtained for Ingot 4 (Sn-15% Pb).
 (a) Liquidus and solidus isotherms after 25 minutes;
 (b) flow lines of interdendritic liquid;

(b) flow lines of interdendritic liquid; (c) macrosegregation as measured (solid curve) and calculated with $\gamma_0 = 3.7 \times 10^{-6} \text{ cm}^2$ (broken curve)



Figure 23: Secondary dendrite arm spacings in Ingots 4, 5 and 6.



Figure 24: The temperature gradient in Ingot 4.



Figure 25: Position of the liquidus and solidus isotherms in Ingot 5.





(a) Liquidus and solidus isotherms after 14 minutes;

(b) calculated flow lines of interdendritic liquid with $\gamma_0 = 2 \times 10^{-7} \text{ cm}^2$; (c) macrosegregation as measured.



Figure 27: Longitudinal microsections of Ingot 5 (Sn-15% Pb). (a) center; (b) 1.5 cm radius; (c) near surface. Mag. 25.6X.



Figure 28: Position of the liquidus and solidus isotherms in Ingot 6.



Results obtained for Ingot 6 (Sn-15% Pb). Figure 29:

- (a) Liquidus and solidus isotherms after 21 minutes;
- (b) flow lines of interdendritic liquid calculated with γ = 8 x 10⁻⁷ cm²;
 (c) macrosegregation as measured.



Figure 30: Longitudinal microsections of Ingot 6 (Sn-15% Pb). (a) center; (b) mid-radius; (c) near surface. Mag. 25.6X.



Figure 31: The shapes of the mushy zone in Ingot 7 (Sn-12% Pb).



Figure 32: Macrosegregation in Ingot 7 (Sn-12% Pb).



Figure 33: Longitudinal microsections at the center of Ingot 7 (Sn-12%Pb) (a) 0 rpm; (b) 45 rpm; (c) 76 rpm. Mag. 25.6X.

Ingot #	8	9	10	11	12
Solid'n Rate	5.6 x 10 ⁻³ cm/sec	6.6 x 10 cm/sec	5.3 x 10 ⁻³ cm/sec	8.3x10 ⁻³ m/sec	1.36x10cm/sec
Rotation Speed	83 r pm	97 rpm	ll9 rpm	66 rpm	54 rpm
Shape of Mushy Zone	E 15 10 8 cm -	E 15 10 € 8 cm →	E 15 10 10 10 10	20 E 15 Bcm	E 15 10 8 cm
Macrosegre- gation	% 20 10	%d 20 10	30 10	⁸ d 25 5	20 10
Freckle (Transverse Cross Section)	No	No		\bigcirc	No
Comment	Increasing (Decreasing (Spinning Effe Gravity Effec C <mark>Ccenter ⁻ Cec</mark> Corigional	Abrupt change in Isotherm Slopes Near Edge	Fast Solid'n Rate and Little Segre- gation	

Table 3. Results of Sn-Pb Ingots with Rotation

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Figure 34: Position of the liquidus and solidus isotherms along the centerline of Ingot 8.



Figure 35: Cooling curves for Ingot 8.



Figure 36: Position of the liquidus and solidus isotherms in Ingot 8.





(c) macrosegregation as measured (solid curve) and calculated with $\gamma_0 = 1.2 \times 10^{-6} \text{ cm}^2$ (broken curve).



Figure 38: Secondary dendrite arm spacings in Ingots 8-12.



Figure 39: Position of the liquidus and solidus isotherms along the centerline of Ingot 9.



Figure 40: Cooling curves for Ingot 9.



Figure 41: Position of the liquidus and solidus isotherms in Ingot 9.





- (b) flow lines of interdendritic liquid;
- (c) macrosegregation as measured (solid curve) and calculated with $\gamma_0 = 0.98 \times 10^{-6} \text{ cm}^2$ (broken curve)



Figure 43: Position of the liquidus and solidus isotherms along the centerline of Ingot 10.



Figure 44: Cooling curves for Ingot 10.



Figure 45: Position of the liquidus and solidus in Ingot 10.






Figure 47: Longitudinal microsections of Ingot 10 (Sn-12.8% Pb). (a) center; (b) mid-radius; (c) near surface. Mag. 25.6X.



Figure 48: Longitudinal microsection at the edge of Ingot 10 (Sn-12.8% Pb). Mag. 128X.



Figure 49: Position of the liquidus and solidus along the centerline of Ingot 11.



Figure 50: Cooling curves for Ingot 11.



Figure 51: Position of the liquidus and solidus isotherms in Ingot 11.



Results obtained for Ingot 11 (Sn-12.4% Pb). Figure 52: (a) Liquidus and solidus isotherms after 35 minutes;

- (b) flow lines of interdendritic liquid; (c) macrosegregation as measured (solid curve) and calculated with $\gamma_0 = 3.3 \times 10^{-6} \text{ cm}^2$ (broken curve)



Figure 53: Transverse microsections of Ingot 11 (Sn-12.4% Pb). (a) center; (b) mid-radius; (c) near surface. Mag. 25.6X.



Figure 54: Position of the liquidus and solidus isotherms along the centerline of Ingot 12.







Figure 56: Position of the liquidus and solidus in Ingot 12.





- (a) Liquidus and solidus isotherms after 12 minutes;
- (b) flow lines of interdendritic liquid; (c) macrosegregation as measured (solid curve) and calculated with $\gamma_0 = 1.0 \times 10^{-6} \text{ cm}^2$ (broken curve)



Figure 58: Permeabilities used in Calculation



Figure 59: Effects of mushy zone shape and solidification rate on macrosegregation in Al-4.4%Cu. $\gamma_0 = 5 \times 10^{-7} \text{ cm}^2$







Figure 61: Parameters leading to positive segregation at the center of Ingot 4 (Sn-15% Pb). (a) Values of the dimensionless group in the local solute redistribution equation; (b) solute accumulation with interdendritic liquid flow and neglecting flow (Scheil equation).



Figure 62: Effect of centrifugal force on macrosegregation across Ingot 8 when solidification rate is 0.0035 cm/sec.



Figure 63: Effect of centrifugal force on macrosegregation across Ingot 8 when solidification rate is 0.0056 cm/sec.



Figure 64: Influence of solidification rates on the spinning effect in Ingot 8.

TABLE 4

LIST OF COMPUTER NOTATIONS

Computer Notation	Algebraic Notation	Explanation of Symbols
A1,A2,A3		Components of AX
A1L(I)		Dimensionized slope of liquids isotherm
A1S(I)		Dimensionized slope of solidus isotherm
ALFA	C.	$\beta / [(1-k)/C_L]$
AX	A	A1+A2+A3
В	В	B1+B2
B1,B2		Components of B
С	С	C3-C4-C5-C6
C1,, C6		Components of C
CE	С _Е	Eutectic composition
CL(I,J)	С _L	Composition of liquid at (I,J)
СО	C	Composition of bulk liquid
CONTR		$\rho_{SE}^{\prime}/\rho_{LE}^{-1}$
CONTRL		$\rho_{\rm S}/\rho_{\rm LO}^{-1}$
CRAT		C _o -C _E
CSE	C _{SE}	Composition of solid in equilibrium
		with liquid at eutectic temperature
CSINGT		Average ingot composition
CS(J)	°s	Composition of solid
DECLR	9C ^L /9r	Radial gradient of C_L

Computer Notation	Algebraic Notation	Explanation of Symbols
DECLZ	9C ^L \9z	Vertical gradient of C_L
DEGLR	∂g _L ∕∂r	Radial gradient of g_L
DEGLZ	∂g ^L ∖9z	Vertical gradient of g_L
DELRAD	HC or HC/2	Horizontal spacing
DEPMZ		Depth of mushy zone
DERHOR	96 ^{. L} \ 9r	Radial gradient of ${}^{ m ho}{}_{ m L}$
DERHOZ	96 [°] / 95	Vertical gradient of $ ho_L$
DIFTEM		T(I,J)-TE
DRODCL	$d\rho_L^{}/dC_L^{}$	Variation of ρ_L with C_L
EM	m	(TE-TM)/CE
EPPS(I,J)		ε at (I,J)
FOR(I,J)		Coefficient of finite difference equation
GADS	Υ _ο	Permeability at the centerline of mushy zone
GAMMA	Υ	Permeability
GE		Scheil's fraction eutectic
GEE	g _E	Real fraction eutectic
GLE		Fraction eutectic
GLEUT(I)		Dimensionized GEE
GL(I,J)	gL	Fraction liquid
GRAV	g	Gravitational acceleration
GR(I,J)	ƏT/ Ər	Radial temperature gradient at (I,J)
GS(I,J)	gs	Fraction solid
GZ(I,J)	JT/ Jz	Vertical temperature gradient at (I,J)

Computer Notation	Algebraic Notation	Explanation of Symbols
HA	ha	Right horizontal grid spacing
HB	h _b	Left horizontal grid spacing
HC	Δr	Radial spacing increment
HEIT(I)		Maximum depth of metal pool at column I
HORAT		ρ _ο -ρ _{LE}
HTE		Depth of mushy zone at the center
HTMZ		HTT(I) - DEPMZ
HTFRAC		HTMZ/HTT(I)
HTT(I)		ZL(I) - ZS(I)
I		Column designation
IMAX		Column at wall
IMAXN		IMAX-1
ITER		Iteration step
J		Row designation
JJ1(I),, J	J5(1)	Column selection for output
JMIN(I)		Minimum value of J at column I
JMN(I)		JMIN(I+1)
JWALL		JMIN(I) at I=IMAX
КАҮ	k	Partition ratio
KA	k _a	Upper vertical grid spacing
КВ	k _b	Lower vertical grid spacing
КС	k _c	Vertical spacing increment
KONST(I,J)		Coefficient of finite difference equation
LOCCOM(I)	Ē,	Local average composition at column I

Computer Notation	Algebraic Notation	Explanation of Symbols
MAXITI		Maximum number of iterations
MLIQ		Slope of liquids isotherm
MO(I,J)		Slope of isotherm at (I,J)
MSOL		Slope of solidus isotherm
MU	μ	Viscosity
NLGL(J)	lngL	Natural log of fraction liquid
NMT		NT(I)-1
NNT		NT(I)
NSI(I)		JMIN(I)+1
NT(I)		Top row of column I
NTOP		Maximum number of rows
ONE(I,J)		Coefficient of finite difference equation
РА	Po	Atmospheric pressure
PERMI(I,J)	K	γg _L ²
P(I,J)		Pressure at (I,J)
PDR	∂P/∂r	Radial pressure gradient
PDZ	9 P/ 9z	Vertical pressure gradient
PPP	,	JMIN(I)
Q1, Q8		Coefficients of finite difference equation
RADIUS		Radius of Ingot
RARA		Ϋ.∇Τ/ε
RATER		$\overrightarrow{\mathbf{v}} \cdot \nabla \mathbf{T}$
RHO(I,J)	ρ _L	Liquid density at (I,J)
R(I,J)	r	Radius at (I,J)

Computer Notation	Algebraic Notation	Explanation of Symbols
RE	ρ _s	Solid density
RFRACS		(RS(J) - R(I,J))/HC
RL(J)		Radius of liquidus isotherm at row J
RLE	ρ _{LE}	Density of liquid eutectic
RO	ρ _L Ο	Density of bulk liquid
ROR(I)		Radius at column I
RR		
RS(J)		Radius of solidus isotherm at row J
RSE	^ρ se	Density of eutectic solid
SOLHZ		<pre>∂p/dr at boundary point 1</pre>
SOLVE		∂p/∂z at boundary point 2
T(I,J)	Т	Temperature at (I,J)
TABOT(I,J)		Coefficient of finite difference equation
TAKONS(I,J)		Coefficient of finite difference equation
TALEFT(I,J)		Coefficient of finite difference equation
TART(I,J)		Coefficient of finite difference equation
TATOP(I,J)		Coefficient of finite difference equation
TE	T_{E}	Eutectic temperature
TL	$^{\mathrm{T}}$ L	Liquidus temperature
TM		Melting point of pure solvent
TRAT		TL-TE
TRE(I,J)		Coefficient of finite difference equation
TTHETA	θ	Angle
TWO(I,J)		Coefficient of finite difference equation

Computer Notation	Algebraic Notation	Explanation of Symbols
<u>Motation</u>		
TYPE		Different types of pressure calculation
UR	^U r	r-component of $\dot{\vec{U}}$
UZ(I,J)	U _z	z-component of \vec{U}
UZCL		Casting speed
VR	vr	r-component of \vec{v}
VTOT	v	Magnitude of \vec{v}
VZ	vz	z-component of \overrightarrow{v}
W	ω	Angular velocity
Z(I,J)	z	Height of node (I,J)
ZAT(I)		Ratio of 2nd D.A.S. to 2nd D.A.S. at
		centerline
ZF R ACS		(Z(I,J)-ZS(I))/KC
ZILIQ		Height of liquidus at centerline
ZISOL		Height of solidus at centerline
ZL(I)		Height of liquidus isotherm at column I
ZLHIGH		ZL(I) at wall
ZS(I)		Height of solidus isotherm at column I

APPENDIX A - Composition and Density of Interdendritic Liquid

In the "local solute redistribution equation", it is assumed that equilibrium exists at the interface between the interdendritic liquid and the solid phase (5). Therefore, the temperature of a solidifying alloy is dictated by the liquidus line on the corresponding phase diagram, and the composition of interdendritic liquid is a function of temperature only, i.e., $C_L = C_L(T)$. The temperature, T, is a function of position and time, i.e., T = T(r,z,t). Therefore, from chain rule,

$$\frac{\partial C_{L}}{\partial t} = \frac{\partial C_{L}}{\partial t} = \frac{\partial C_{L}}{\partial t} = \frac{\varepsilon}{m}$$
(13)

where m is the slope of the liquidus line of the phase diagram (Figures 2(a), 3(a), and ε is the cooling rate. By substituting Equation (13) into Equation (4), we get Equation (5).

The density of a liquid is a function of both composition and temperature. But, since $C_L = C_L(T)$ we can write for the interdendritic liquid that $\rho_L = \rho_L(C_L)$. Since $C_L = C_L(r,z,t)$, from chain rule, we get

$$\frac{\partial \rho_{L}}{\partial t} \Big|_{r,z} = \left(\frac{d \rho_{L}}{d C_{L}} \right) \left(\frac{\partial C_{L}}{\partial t} \right)_{r,z} = \left(\frac{d \rho_{L}}{d C_{L}} \right) \frac{\varepsilon}{m}$$
(6)

where $d\rho_L/dC_L$ is the slope of the ρ_L versus C_L plot for the interdendritic liquid (Figures 2b and 3b).









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APPENDIX C

FINITE DIFFERENCE FORMS OF PRESSURE DISTRIBUTION EQUATION

1. Interior Grid Points

$$\frac{\partial P}{\partial r}\Big|_{I,J} = (P(I+1,J) - P(I-1,J))/(2h_b)$$

$$\frac{\partial P}{\partial z}\Big|_{I,J} = (P(I,J+1) - P(I,J-1))/(2k_a)$$

$$\frac{\partial^2 P}{\partial r^2}\Big|_{I,J} = (P(I+1,J) + P(I-1,J) - 2P(I,J))/(h_b^2)$$

$$\frac{\partial^2 P}{\partial z^2}\Big|_{I,J} = (P(I,J+1) + P(I,J-1) - 2P(I,J)/(k_a^2))$$

Substituting these equations into the pressure distribution equation, Eqn (8), we get

where

ONE(I,J) =
$$(h_b^{-2} + A(I,J) (2h_b)^{-1})$$

. $(2h_b^{-2} + 2k_a^{-2})^{-1}$



regular interior grid point

$$TWO(I,J) = (k_a^{-2} + B(I,J)(2k_a)^{-1})$$
$$\cdot (2h_b^{-2} + 2k_a^{-2})$$
$$TRE(I,J) = (h_b^{-2} - A(I,J)(2h_b)^{-1})$$
$$\cdot (2h_b^{-2} + 2k_a^{-2})$$
$$FOR(I,J) = (k_a^{-2} - B(I,J)(2k_a)^{-1})$$
$$\cdot (2h_b^{-2} + 2k_a^{-2})$$
$$KONST(I,J) = C \cdot (2h_b^{-2} + 2k_a^{-2})$$

2. Solidus Interior Grid Points

Solidus interior grid points are those grid points inside the mushy zone and just next to the solidus isotherm. They can be classified into three types. Each type has its own finite difference form of the pressure distribution equation.

Type A:ZFRACS \leq 1.0 and RFRACS \leq 1.0Type B:ZFRACS \leq 1.0 and RFRACS > 1.0Type C:ZFRACS > 1.0 and RFRACS \leq 1.0

where

ZFRACS = (Z(I,J) - ZS(I))/KC

and

RFRACS = (RS(I) - R(I,J))/HC

Type A:

From Darcy's law and the solidus boundary condition, we get the following relation for point 1:

SOLHZ =
$$\frac{\partial P}{\partial r}\Big|_{1} = \frac{\mu}{\gamma g_{LE}} \left(\frac{\rho_{SE}}{\rho_{LE}} - 1\right) U_{rE} + \rho_{LE} \omega^{2} r$$

Similarly, at point 2, we have:

SOLVE =
$$\frac{\partial P}{\partial z}\Big|_{2} = \frac{\mu}{\gamma g_{LE}} (\frac{\rho_{SE}}{\rho_{LE}} - 1) U_{zE} - \rho_{LE} g$$

Using the "Level Rule" for unequal grid spacings around (I,J), we have:

$$\frac{\partial P}{\partial r}\Big|_{I,J} = SOLHZ \cdot h_b / (h_a + h_b) + (P(I,J) - P(I-2,J)) \cdot (h_a / 2h_b) / (h_a + h_b)$$

$$\frac{\partial P}{\partial z}\Big|_{I,J} = SOLVE \cdot k_a / (k_a + k_b) + (P(I,J+2) - P(I,J)) \cdot (k_b / 2k_a) / (k_a + k_b)$$

$$\frac{\partial^2 P}{\partial r^2}\Big|_{I,J} = (SOLHZ - (P(I,J) - P(I-2,J)) / (2h_b)) / (h_a + h_b)$$

$$\frac{\partial^2 P}{\partial z^2}\Big|_{I,J} = ((P(I,J+2) - P(I,J)) / (2k_a) - SOLVE) / (k_a + k_b)$$

Substituting these equations into the pressure distribution equation, Eqn (8), we get

$$P(I,J) = TATOP(I,J) P(I,J+2) + TALEFT(I,J) P(I-2,J) + TAKONS(I,J)$$



where

TATOP(I,J) =
$$(Q2+Q4)/Q6$$

TALEFT(I,J) = $(Q1-Q3)/Q6$
TAKONS(I,J) = $Q5/Q6$
 $Q1 = (2h_b(h_a+h_b))^{-1}$
 $Q2 = (2k_a(k_a+k_b))^{-1}$
 $Q3 = h_aA(I,J)Q1$
 $Q4 = k_bB(I,J)Q2$
 $Q5 = SOLHZ \cdot (h_a+h_b)^{-1} (1 + h_bA(I,J))$
 $- SOLVE \cdot (k_a+k_b)^{-1} (1-k_aB(I,J)) + C(I,J)$
 $Q6 = Q1 + Q2 - Q3 + Q4$

Type B:

 $\frac{\partial P}{\partial r} \bigg|_{I,J} \text{ and } \frac{\partial^2 P}{\partial r^2} \bigg|_{I,J} \text{ are the same as in the case of interior grid}$ points. While $\frac{\partial P}{\partial z} \bigg|_{I,J}, \frac{\partial^2 P}{\partial z^2} \bigg|_{I,J} \text{ and SOLVE are the same as in Type A.}$ Substituting these into the pressure distribution equation, Eqn. (8), we get:

$$P(I,J) = TART(I,J) P(I+1,J) + TATOP(I,J) P(I,J+2)$$

+ TALEFT(I,J) P(I-1,J) + TAKONS(I,J)

where

TART(I,J) =
$$(h_b^{-2} + A(I,J)(2h_b)^{-1})/(Q2+Q4+2h_b^{-2})$$

TALEFT(I,J) = $(h_b^{-2} - A(I,J)(2h_b)^{-1})/(Q2+Q4+2h_b^{-2})$
TATOP(I,J) = $(Q2+Q4)/(Q2+Q4+2h_b^{-2})$


regular interior grid pointOsolidus interior grid point

TAKONS(I,J) =
$$Q7/(Q2+Q4+2h_b^{-2})$$

Q7 = -SOLVE· $(k_a+k_b^{-1})^{-1}(1-k_a^{-2}B(I,J)) + C(I,J)$

Q2 and Q4 are the same as in Type A.

Type C:

 $\frac{\partial P}{\partial z} \bigg|_{I,J} \text{ and } \frac{\partial^2 P}{\partial z^2} \bigg|_{I,J} \text{ are the same as in the case of interior grid}$ points. While $\frac{\partial P}{\partial r} \bigg|_{I,J}$, $\frac{\partial^2 P}{\partial r^2} \bigg|_{I,J}$ and SOLHZ are the same as Type A. Substituting these into the pressure distribution equation, Eqn. (8), we get

$$P(I,J) = TATOP(I,J) P(I,J+1) + TALEFT(I,J) P(I-2,J)$$
$$+ TABOT(I,J) P(I,J-1) + TAKONS(I,J)$$

where

TATOP(I,J) =
$$(k_a^{-2} + B(I,J)(2k_a)^{-1})/(Q1-Q3+2k_a^{-2})$$

TALEFT(I,J) = $(Q1-Q3)/(Q1-Q3+2k_a^{-2})$
TABOT(I,J) = $(k_a^{-2} - B(I,J)(2k_a)^{-1})/(Q1-Q3+2k_a^{-2})$
TAKONS(I,J) = $Q8/(Q1-Q3+2k_a^{-2})$
Q8 = SOLHZ· $(h_a+h_b)^{-1}$ (1+ $h_bA(I,J)$) + C(I,J)
Q1 and Q3 are the same as in Type A.



regular interior pointOsolidus interior point

3. Centerline Grid Points

$$\frac{\partial P}{\partial r}\Big|_{I,J}, \frac{\partial^2 P}{\partial r^2}\Big|_{I,J}, \frac{\partial P}{\partial z}\Big|_{I,J} \text{ and } \frac{\partial^2 P}{\partial z^2}\Big|_{I,J} \text{ are the same as in the}$$

case of interior grid point. But since all properties are symmetrical with respect to the centerline, P(I-I,J) equals to P(I+1,J) and A $\frac{\partial P}{\partial r}$ of the pressure distribution equation now equals to $\frac{\partial^2 P}{\partial r^2}$. Substituting these into the pressure distribution equation, Eq. (8), we get

where

ONE(I,J) =
$$(4 h_b^{-2}) \cdot (4 h_b^{-2} + 2 k_a^{-2})^{-1}$$

TWO(I,J) = $(k_a^{-2} + B(I,J)(2k_a)^{-1}) \cdot (4 h_b^{-2} + 2 k_a^{-2})^{-1}$
FOR(I,J) = $(k_a^{-2} - B(I,J)(2k_a)^{-1}) \cdot (4 h_b^{-2} + 2 k_a^{-2})^{-1}$
KONST(I,J) = $C(I,J) \cdot (4 h_b^{-2} + 2 k_a^{-2})^{-1}$

4. Wall Grid Points

$$\frac{\partial P}{\partial r}\Big|_{I,J}, \frac{\partial^2 P}{\partial r^2}\Big|_{I,J}, \frac{\partial P}{\partial z}\Big|_{I,J} \text{ and } \frac{\partial^2 P}{\partial z^2}\Big|_{I,J}$$

are the same as in the case of interior grid points. But now because of the wall boundary condition, $P(I+1,J) = P(I-1,J) + (2h_b) \rho_L(I,J) \omega^{2R}$, where R is the radius of the mold. Substituting these into the pressure distribution equation, we get

where

$$TWO(I,J) = (k_a^{-2} + B(I,J)(2k_a)^{-1}) \cdot (2h_b^{-2} + 2k_a^{-2})^{-1}$$
$$TRE(I,J) = (2h_b^{-2}) \cdot (2h_b^{-2} + 2k_a^{-2})^{-1}$$
$$FOR(I,J) = (k_a^{-2} - B(I,J)(2k_a)^{-1}) \cdot (2h_b^{-2} + 2k_a^{-2})^{-1}$$
$$KONST(I,J) = (\rho_L \omega^2 R(2h_b^{-1} + A(I,J)) + C(I,J))^{-1}$$
$$\cdot (2h_b^{-2} + 2k_a^{-2})^{-1}$$

	0001
APPENDIX D	0002
C	0003
C	0004
C THIS IS INGOT 1	0005
C ************************************	0006
C	0007
C	0008
C	0009
C	0010
C* ***********************************	0011
C DIMENSION AND PRECISION STATEMENTS****BEGIN	0012
C* *** *** *** *** *** *** *** *** ***	0013
C	0014
INTEGER PT1	0015
INTEGER NPARAM	0016
INTEGER*4 N	0017
INTEGER PPPMAX	0018
INTEGER PPP	0019
INTEGER NSI(25), NSIMAX(25), JMIN(25), NT(25), JMN(25)	0020
REAL*8 THEDA7, THEDA8, THEDA9	0021
REAL*4 ROO(25), COO(25)	0022
INTEGER JJ1(25), JJ2(25), JJ3(25), JJ4(25)	0023
INTEGER JJ5 (25), JJ6 (25), JJ7 (25), JJ8 (25)	0024
REAL*8 D(22,82), E(22,82), F(22,82)	0025
PEAL*8 KAB, KAC, KBB	0026
REAL#4 NLGE	0027
REAL*8 ANG	0028
REALTO GADS	0029
$REAL^{FO} = LL^{FO} = LL^{F$	0030
N GALMO VR (22,02), VG (22,02) DENI+(NICI (02) EN (02)	0031
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REAL*8	THEDA1, THEDA2, THEDA3, THEDA4, THEDA5, THEDA6	0037
REAL*8	EPPSE	0038
REAL*8	01,02,03,04,05,06,07,08	0039
REAL*8	LEFT, KC, KAY, KA	0040
PEAL*8	KON1, KON2, KON3, KON4	0041
REAL*8	GAMO1, GAMO2, CONSTT	0042
PEAL*4	SLOLIQ, SLOSOL	0043
REAL*4	LTSEG	0044
REAL*8	RSS (82), BL (82)	0045
REAL*8	ZOZ (82)	0046
REAL*8	VZE (25) , VRE (25)	0047
REAL*8	RS (82)	0048
REAL*4	ROR (25)	0049
REAL*8	HTT (25), HEIT (25), GRAV, EM, DTT	0050
REAL*8	HTE, TL, TE, HORAT, CRAT, TRAT, RADIUS	0051
REAL*8	RO, RLE, RSE, RE, GE, MU, CO, CE	0052
REAL*8	H, HA, HB, HC, HM, HT	0053
REAL*8	DABS	0054
REAL*8	UR, UZ (22, 82), ZL (25), ZS (25)	0055
PEAL*8	PA	0056
REAL*8	SOLVE, SOLHZ	0057
REAL*4	A1S (25), A1L (25), DELA1 (25)	0058
REAL*8	TABOT (22,82), TAKONS (22,82)	0059
REAL*8	TART (22,82), TATOP (22,82), TALEFT (22,82)	0060
REAL*8	GOPS	0061
REAL*8	T(22,82), RHO(22,82), MO(22,82)	0062
REAL*8	CL (22,82), GL (22,82), Z (22,82), R (22,82)	0063
REAL*8	UZURRO, UZURCL, DERHOR, DERHOZ, DECLR, DECLZ, DEGLR, DEGLZ	0064
REAL*8	DENOM1, DENOM2, THETA	0065
REAL*8	ONE (22,82), TWO (22,82), TRE (22,82), FOR (22,82)	0066
REAL*8	PERMI (22, 82), GAMMA (22, 82)	0067
REAL*8	GR (22,82), GZ (22,82), EPPS (22,82)	0068
REAL*8	A1, A2, A3, B1, B2, C1, C2, C3, C4	0069
REAL*8	AX, B, C	0070
PEAL*8	P (22,82), KONST (22,82)	0071
REAL*8	ZAT (22)	0072
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REAL*8 PDR,PDZ 0074 PEAL*8 GLEUT (25) 0076 C DIMENSION AND PRECISION STATEMENTS***END 0076 C 0078 C 0078 C 0080 C 0080 C GENERAL DATA INPUTS************************************
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MU=.013 0091 PA=1.0D6 0092 TRIG=1 0093 HC=0.25 0094 KC=0.14 0095 RADIUS=3.4 0096 ZISOL=0.0 0097
PA=1.0D6 0092 TRIG=1 0093 HC=0.25 0094 KC=0.14 0095 RADIUS=3.4 0096 ZISOL=0.0 0097
TRIG=1 0093 HC=0.25 0094 KC=0.14 0095 RADIUS=3.4 0096 ZISOL=0.0 0097
HC=0.25 KC=0.14 RADIUS=3.4 2ISOL=0.0 0094 0095 0095 0097
KC=0.14 RADIUS=3.4 ZISOL=0.0 0095 0095
RADIUS=3.4 2ISOL=0.0 0097
ZISOL=0.0
DTT=0.
GRAV=980.
RO=2.45 0100
PI=3.14156 0101
RSE=3.38 0102
PLE=3.2 0103
BE=2.62 0104
TE=548.
TM=660.
CSE=5.65
CE=33.
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С		0109
С	INPUT OF (2'NDARY D.A.S./2'NDARY D.A.S. AT CENTER LINE)	0110
С		0111
	ZAT(1) = 1.0	0112
	$Z \operatorname{AT}(2) = 1.0$	0113
	ZAT(3) = 1.0	0114
	Z AT (4) = 1.0	0115
	7 AT(5) = 1.0	0116
	ZAT(6) = 1.0	0117
	ZAT(7) = 1.0	0118
	2AT(8) = 1.0	0119
	ZAT(9) = 1.0	0120
	Z AT(10) = 1.0	0121
	ZAT(11) = 1.0	0122
	7 AT(12) = 1.0	0123
	ZAT(13) = 1.0	0124
	ZAT(14) = 1.0	0125
	Z AT (15) = 1.0	0 1 2 6
	ZAT(16) = 1.0	0127
	ZAT(17) = 1.0	0128
С		0129
С	GENERAL DATA INPUTS**********END	0130
С		0131
	IMAX=RADIUS/HC+.0001	0132
	IMAX = IMAX + 1	0133
	J1MAX=ZILIQ/KC+0.0001	0134
	J1MAX=J1MAX+1	0135
	DRODCL = (RO - RLE) / (CO - CE)	0136
	KAY=CSE/CE	0137
	KON1 = (1, 0D0/CO) ** (1, /(KAY - 1,))	0138
	KON 2 = 1.0DO / (KAY - 1.0DO)	0139
	KON3 = KON2 - 1.0D0	0140
	KON4 = -KON2	0141
	KAY=CSE/CE	0142
	GE = (CE/CO) ** (1./(KAY-1.))	0143
	EM = (TE - TM) / CE	0144
		ω ω

	TL = EM * (CO - CE) + TE	0145
	CONTR = RSE/BLE - 1.	0146
	CONTRL = (RE/RO-1.)	0147
	HOBAT = RO - RLE	0148
	TRATETIOTE	0149
	CRATECO-CE	0150
	TMAXN = TMAX - 1	0151
	I MAXP = I MAX + 1	0152
	WRITE (6,5650) IMAX.J1MAX	0153
5650	FORMAT (1X, 2116)	0154
	DO 8 I=1.IMAX	0155
	GLEUT(I) = GE	0156
8	CONTINUE	0157
	WRITE (6,6925)	0158
6925	FORMAT(12X, ************************************	0159
	WRITE (6,9000)	0160
9000	FORMAT(12X, 'Z-SOLIDUS', 10X, 'Z-LIQUIDUS', 9X, 'I')	0 16 1
	WRITE (6,6926)	0162
6926	FORMAT (12X, ************************************	0163
С		0164
C****	********	0165
c c	ALCULATION OF HFIGHTS OF LIQUIDUS POINTS, AND HEIGHTS & RADIUS OF	0166
C S	OLIDUS POINT****BEGIN	0167
C****	**************	0168
С		0169
	DO 10 $I=1,IMAX$	0170
	H=HC	0171
С		0172
C I	NPUT OF SLOPES OF SOLIDUS AND LIQUIDUS ISOTHERMS****BEGIN	0173
С		0174
	IF $(I.EQ.1)$ MSOL=0.0	0175
	IF $(I \cdot EQ \cdot 1)$ MLIQ=0.0	0176
	IF(I.GT.1) MLIQ=0.80	0 177
	IF(I.GT.1) $MSOL=0.80$	0178
	IF(I.EQ.1) A 1S(I) = 0.0	0179
	IF(I.EQ.1) A 1L(I) = 0.0	0180
		2
		+-

INPUT OF SLOPES OF SOLIDUS AND LIQUIDUS ISOTHERMS****END A1S (I) = MSOL A1L (I) = MLIQ IF (I.EQ.1) GO TO 22 GO TO 23 22 CONTINUE ROP (1) = 0.0 ZS (I) = ZISOL ZL (I) = ZILIQ GO TO 19 23 CONTINUE ROP (I) = ROP (I-1) + HC ZL (I) = ZL (I-1) + A1L (I) * HC ZS (I) = ZS (I-1) + A1S (I) * HC 19 CONTINUE	0182 0183 0184 0185 0186 0187 0188 0189 0190 0190 0191 0192 0193 0194 0195 0196
A 1S (I) = MSOL A 1L (I) = MLIQ IF (I.EQ.1) GO TO 22 GO TO 23 22 CONTINUE ROR (1) = 0.0 ZS (I) = ZISOL ZL (I) = ZILIQ GO TO 19 23 CONTINUE ROR (I) = ROR (I-1) + HC ZL (I) = ZL (I-1) + A1L (I) * HC ZS (I) = ZS (I-1) + A1S (I) * HC 19 CONTINUE	0183 0184 0185 0186 0187 0188 0189 0190 0191 0192 0193 0194 0195 0196
A 1S (1) = MSOL A 1L (I) = MLIQ IF (I.EQ.1) GO TO 22 GO TO 23 22 CONTINUE ROR (1) = 0.0 ZS (I) = ZISOL ZL (I) = ZILIQ GO TO 19 23 CONTINUE ROR (I) = ROR (I-1) + HC ZL (I) = ZL (I-1) + A1L (I) * HC ZS (I) = ZS (I-1) + A1S (I) * HC 19 CONTINUE	0184 0185 0186 0187 0188 0189 0190 0191 0192 0193 0194 0195 0196
<pre>X1L(I) = MLIQ IF (I.EQ.1) GO TO 22 GO TO 23 22 CONTINUE ROR(1) = 0.0 ZS(I) = ZISOL ZL(I) = ZILIQ GO TO 19 23 CONTINUE ROR(I) = ROR(I-1) + HC ZL(I) = ZL(I-1) + A1L(I) * HC ZS(I) = ZS(I-1) + A1S(I) * HC</pre>	0185 0186 0187 0188 0190 0190 0191 0192 0193 0194 0195 0196
IF (I.EQ.1) GO TO 22 GO TO 23 22 CONTINUE ROP (1) =0.0 ZS (I) = ZI SOL ZL (I) = ZI LIQ GO TO 19 23 CONTINUE ROP (I) = ROP (I-1) + HC ZL (I) = ZL (I-1) + A1L (I) * HC ZS (I) = ZS (I-1) + A1S (I) * HC 19 CONTINUE	0188 0187 0188 0189 0190 0191 0192 0193 0194 0195 0196
GO TO 23 22 CONTINUE ROP (1) =0.0 ZS(I) = ZISOL ZL(I) = ZILIQ GO TO 19 23 CONTINUE ROP (I) = ROP (I-1) + HC ZL(I) = ZL(I-1) + A1L(I) * HC ZS(I) = ZS(I-1) + A1S(I) * HC 19 CONTINUE	0187 0188 0189 0190 0191 0192 0193 0194 0195 0196
22 CONTINUE ROR (1) =0.0 ZS (I) = ZISOL ZL (I) = ZILIQ GO TO 19 23 CONTINUE ROR (I) = ROR (I-1) + HC ZL (I) = ZL (I-1) + A1L (I) * HC ZS (I) = ZS (I-1) + A1S (I) * HC 19 CONTINUE	0185 0189 0190 0191 0192 0193 0194 0195 0196
<pre>ROF(1) = 0.0 ZS(I) = ZISOL ZL(I) = ZILIQ GO TO 19 23 CONTINUE ROR(I) = ROR(I-1) + HC ZL(I) = ZL(I-1) + A1L(I) * HC ZS(I) = ZS(I-1) + A1S(I) * HC 19 CONTINUE</pre>	0190 0191 0192 0193 0194 0195 0196
ZS(I) = ZISOL ZL(I) = ZILIQ GO TO 19 23 CONTINUE ROR(I) = ROR(I-1) + HC ZL(I) = ZL(I-1) + A1L(I) + HC ZS(I) = ZS(I-1) + A1S(I) + HC 19 CONTINUE	0190 0191 0192 0193 0194 0195 0196
$ \begin{array}{c} 21 (1) = 21 (10) \\ \text{GO TO } 19 \\ \hline 23 \text{ CONTINUE} \\ \text{ROR (I) = ROR (I-1) + HC} \\ 21 (1) = 21 (I-1) + A1L (I) + HC \\ 2S (I) = 2S (I-1) + A1S (I) + HC \\ \hline 19 \text{ CONTINUE} \\ \hline \end{array} $	0192 0193 0194 0195 0196
23 CONTINUE ROR (I) = ROR (I-1) + HC ZL (I) = ZL (I-1) + A1L (I) * HC ZS (I) = ZS (I-1) + A1S (I) * HC 19 CONTINUE	0192 0193 0194 0195 0196
$\begin{array}{l} \text{ROR}(I) = \text{ROR}(I-1) + \text{HC} \\ \text{ZL}(I) = \text{ZL}(I-1) + \text{A1L}(I) + \text{HC} \\ \text{ZS}(I) = \text{ZS}(I-1) + \text{A1S}(I) + \text{HC} \\ 19 \text{CONTINUE} \end{array}$	0 19 4 0 19 5 0 19 6
ZL (I) = ZL (I-1) + A1L (I) + HC ZS (I) = ZS (I-1) + A1S (I) + HC I9 CONTINUE	0195 0196
ZS(I) = ZS(I-1) + A1S(I) + HC $19 CONTINUE$	0 196
19 CONTINUE	• • • •
	0197
WRITE $(6, 6000)$ ZS (1) ZL (1) T	0198
00 FORMAT(1X - 2E20, 4 - T 10/)	0 199
10 CONTINUE	0200
ZLHIGH=ZL(IMAX)	0201
DO 11 $J=1.NTOP$	0202
IF (J.EO.1) GO TO 4	0203
GO TO 5	0204
4 CONTINUE	0205
202(1) = 0.0	0206
GO TO 6	0207
5 CONTINUE	0208
ZOZ(J) = ZOZ(J-1) + KC	0209
6 CONTINUE	0210
11 CONTINUE	0211
WRITE (6,6927)	0212
27 FORMAT (12X, ************************************	0213
WRITE (6,6917)	0214
17 FORMAT (14X, 'RS (J) ', 15X, 'J')	0215
WRITE (6,6928)	0216
	1 5 5
1 2 1	<pre>6 CONTINUE 1 CONTINUE WRITE(6,6927) 7 FORMAT(12X,'************************************</pre>

6928 FORMAT (12X . ***********************************	0217
DO 7991 I=2.IMAX	0218
SUM=KC	0219
DO 7992 $J=2$, NTOP	0220
IF ((ZS (I), GE, SUM), AND, (ZS (I-1), LT, SUM)) GO TO 7993	0221
GO TO 7994	0222
7993 $RS(J) = (I-1) * HC - HC * ((ZS(I) - SUM) / (ZS(I) - ZS(I-1)))$	0223
WRITE(6,7995) RS(J),J	0224
7995 FORMAT (5X, 1E15.4, 1115/)	0225
7994 SUM=SUM+KC	0226
IF(ZS(I).LT.SUM) GO TO 7991	0227
7992 CONTINUE	0228
7991 CONTINUE	0229
	0230
C CALCULATION OF HEIGHTS OF LIQUIDUS POINTS, AND HEIGHTS & RADIU	S OF 0231
C SOLIDUS POINT****END	0232
2	0233
	0234
~~××××××××××××××××××××××××××××××××××××	0235
CONSTRUCTION OF THE GRID MESH****BEGIN	0236
, , , , , , , , , , , , , , , , , , ,	0237
	0238
THIS PARTICULAR SECTION DEALS WITH THE SETTING UP OF TH	E GRID 0239
C MESH FOR THE MUSHY ZONE	0240
	0241
DO 50 I=1, IMAX	0242
HTT (I) = ZL (I) - ZS (I)	0243
Z(I, 1) = ZISCL	0244
B(I, 1) = ROB(I)	0245
DO 40 $J=2$, NTOP	0246
7 (I, J) = ZOZ (J)	0247
R(I,J) = ROR(I)	0248
40 CONTINUE	0249
50 CONTINUE	0250
DO 51 I=1, IMAX	0251
HEIT(I) = ZLHIGH - ZL(I)	0252
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	<u>о</u>

51	CONTINUE	0253
	DO 53 I=1, INAX	0254
	DO 41 $J=1$, NTOP	0255
	IF(Z(I,J),GT,ZS(I)) GO TO 33	0256
	IF(Z(I,J), EO, ZS(I)) GO TO 35	0257
	GO TO 41	0258
33	ZFRACS = (Z(I,J) - ZS(I)) / KC	0259
	TF (ZFRACS. LT. 1.0) GO TO 34	0260
	GO TO 41	0261
34	JMIN(I) = J	0262
	GO TO 41	0263
35	JMIN(I) = J + 1	0264
	GO TO 41	0265
41	CONTINUE	0266
53	CONTINUE	0267
	I=IMAX	0268
	JWALL=JMIN(I)	0269
	JWAL=JWALL-1	0270
	DO 5583 I=1,IMAX	0271
	DO 5584 $J=J1MAX, NTOP$	0 27 2
	722=2(I,J)-2L(I)	0273
	ZZ7Z = DABS(ZZZ)	0274
	IF (ZZZZ.LE.0.001) GO TO 5586	0275
	IF (ZZZ.GT.0.001) GO TO 5585	0276
	GO TO 5584	0277
5585	ZFRACL = (Z(I,J) - ZL(I)) / KC	0278
	IF (ZFRACL.LT.1.0) GO TO 5588	0279
	GO TO 5583	0280
5588	NT(I) = J - 1	0281
	GO TO 5583	0282
5586	NT(I) = J - 1	0283
	GO TO 5583	0284
5584	CONTINUE	0285
5583	CONTINUE	0286
с		0287
c co	ONSTANTS NEEDED FOR SUBSEQUENT HEIGHT SELECTION IN THE PRINTOUTS	0288
-		
		7

c		0289
U	DO 52 T-1 THAY	0290
	$\frac{1}{10000} = \frac{1}{10000} = \frac{1}{10000000000000000000000000000000000$	0291
		0292
		0293
	$JJI(\mathbf{I}) = JHIN(\mathbf{I}) + O I H$	0294
	JJZ(1) = JMIN(1) + 2. *NOTH	0295
	$JJJ(1) = JMIN(1) + 3 \cdot *N8TH$	0296
	$JJ4(I) = JMIN(I) + 4 \cdot *N8TH$	0297
	$JJ5(I) = JMIN(I) + 5 \cdot *N8TH$	0298
52	CONTINUE	0299
	WRITE (6,6929)	0300
6929	FORMAT (10X, ************************************	0301
	WRITE (6,9010)	0302
9010	FORMAT(10X, VALUE OF JMIN, 4X, VALUE OF NT, 8X, 1)	0302
	WRITE (6,6930)	030/
6930	FORMAT (10X, ************************************	0305
	DO 88 I=1,IMAXN	0305
	NSI(I) = JMIN(I) + 1	0300
	JMN(I) = JMIN(I+1)	0307
	$IF(JMIN(I) \cdot EQ \cdot JMIN(I+1)) JMN(I) = NSI(I)$	0308
	WRITE(6,8010) JMIN(I), NT(I), I	0.309
8010	FORMAT (1X, 21 16, 11 14/)	0310
88	CONTINUE	0311
С		0312
C C	ONSTRUCTION OF THE GRID MESH****END	0313
С		0314
С		0315
C****	*******	0316
с т	EMP AND TEMP RELATED ITEMS FOR EACH NODE****BEGIN	0317
Ċ		0318
c		0319
c s	CHEIL 'GL' AND HYDROSTATIC 'P' ARE ASSIGNED!	0320
C****	*****	0321
Ċ		0322
<u> </u>	I = IMAX	0323
	PPP=JMIN(I)	032,4
		ž.
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NMT = NT(I) - 1	0325
DO 70 $I=1, IMAX$	0326
MNT = JMIN(I)	0327
NNT = NT(I)	0328
DO $60 J = MNT \cdot NNT$	0329
D EPMZ = Z L (I) - Z (I, J)	0330
HTMZ = HTT(I) - DEPMZ	0331
HTFRAC=HTM7/HTT(I)	0332
T(I,J) = TRAT * HTFRAC + TE	0333
DIFTEM=T(I,J)-TE	0334
RHO(I,J) = (HORAT/TRAT) * DIFTEM + RLE	0335
CL(I,J) = (CRAT/TRAT) * DIFTEM + CE	0336
GL(I, J) = KON1*(CL(I, J) * KON2)	0337
GAMMA(I,J) = GADS*(ZAT(I)) **2	0338
P(I,J) = .5D0*(RHO(I,J)+RO)*GRAV*DEPMZ+GRAV*RO*HEIT(I)	0339
P(I, J) = P(I, J) + 0.5 * RO * (W * 2) * (R(I, J) * 2)	0340
P(I,J) = P(I,J) + PA	0341
60 CONTINUE	0342
70 CONTINUE	0343
GL(1,1)=KON1*(CE**KON2)	0.344
GL (IMAX, JWAL) = KON1* (CE**KON2)	0345
DO 5590 I=1, IMAX	0346
NNT=NT(I)	0347
J = NNT + 1	0348
T(I,J) = TL	0349
B HO (I, J) = BO	0350
CL(I,J) = CO	0351
GL(I,J) = 1.0	0352
GAMMA(I,J) = GADS*(ZAT(I)) **2	0353
P(I,J) = RO*GRAV*HEIT(I) + PA+0.5*RO*(W**2)*(R(I,J)**2)	0354
5590 CONTINUE	0355
с	0356
C	0.357
C TEMP AND TEMP RELATED ITEMS FOR EACH NODE****END	0358
C	0359
С	0360
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C * * * * * * * * * * * * * * * * * * *	0361
C CALCULATION OF VARIABLES AT BOUNDARIES (NEEDED FOR SUBSEQUENT	0362
C MACROSEGREGATION CALCULATION) ****BEGIN	0363
C************************************	0364
	0365
r · · · ·	0366
C VARTARIES AT WAIT	0367
	0368
T=TMAX	0369
PPP=.TMTN(T)	0370
NMT = NT(T)	0371
DO 250 J=PPP NMT	0372
$IF(J_GT_NT(T-1))$ GO TO 200	0373
GO TO 201	0374
$200 \text{ GR}(\mathbf{I}_{-J}) = (\mathbf{T}_{-T}(\mathbf{I}_{-J})) / (((\mathbf{Z}_{-L}(\mathbf{I}) - \mathbf{Z}(\mathbf{I}_{-J}))) / (\mathbf{Z}_{-L}(\mathbf{I}) - \mathbf{Z}_{-L}(\mathbf{I} - 1))) * \text{HC})$	0375
GO = TO = 202	0376
201 GR (T_{-J}) = (T_{-J}) - T_{-J} (T_{-1} , J) / HC	0377
$202 \ G7 (I J) = (T J - T F) / (7 J (I) - 7 S (I))$	0378
EPPS $(I,J) = -GZ (I,J) * UZCL$	0379
250 CONTINUE	0380
T=TMAX	0381
J = NT(T) + 1	0382
GZ (T - J) = (T L - T F) / (Z L (T) - Z S (T))	0383
GP(T,J) = -A II (T) * GZ (T,J)	0384
$EPPS(I_{1},I) = -GZ(I_{1},I) * UZCL$	0385
	0386
C VARIABLES AT LIGHTDUS	0387
	0388
DO 300 T=2.TMAXN	0389
NNT = NT(T)	0390
J = NNT + 1	0391
$GZ (T_{-}J) = (TL - TE) / (ZL (T) - ZS (T))$	0392
GR(T,J) = -GZ(T,J) * A II. (T)	0393
$EPPS(I_{-J}) = -GZ(I_{-J}) * UZCI.$	0394
300 CONTINUE	0395
	0.396
	É.
	60

c	VADIADIES AT CENTER LINE	0397
C C	VARIADES AL CURILE DIND	0398
Ľ	T - 1	0399
	1 - 1 NNT-NT (T) 11	0400
	DO 200 I-2 NHT	0401
	$\frac{1}{2} \frac{1}{2} \frac{1}$	0402
		0403
	$G_{2}(1, J) = 1 \text{ MAI} / \Pi_{11}(1)$ RDDC (I = 1) = -C7 (I = 1) #U7CI	0404
	$\frac{1}{1} \frac{1}{1} \frac{1}{1} = \frac{1}{1} $	0405
	Tr(J = EQ + RNT) = GO = TO = 55.5	0406
		0407
		0408
	$\frac{350 \text{ CONTINUE}}{\text{VP}(T \text{ I}) = 0.0}$	0409
		0410
	$r_{3}(1,3) = 0.201,0000000000000000000000000000000000$	0411
	339 CONTINIE	0412
		0413
	T=1	0414
	I=1	0415
	$G = \{1,, 1\} = 0, 0$	0416
	$G_{2}(T,J) = (TL - TE) / (ZL(T) - ZS(T))$	0417
	$PPPS(T_{1},T) = -G7(T_{1},T) * 117CL$	0418
		0419
C		0420
č	CALCULATION OF VARIABLES AT BOUNDARIES (NEEDED FOR SUBSEQUENT	0421
č	MACROSEGREGATION CALCULATION) ****END	0422
ř		0423
ĉ		0424
c*	* * * * * * * * * * * * * * * * * * * *	0425
c*	* * * * * * * * * * * * * * * * * * * *	0426
č	ITERATION SEQUENCE FOR 'P', VELOCITY, 'GL' AND COPM****BEGIN	0427
Č*	****	0428
Č	* * * * * * * * * * * * * * * * * * * *	0429
c		0430
-	DO 1000 ITER=1,MAXIT1	0431
С		0432
		16
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C * * * * * * * * * * * * * * * * * * *	0433
C CALCULATION OF COEFFICIENTS****BEGIN	0434
C * * * * * * * * * * * * * * * * * * *	0435
С	0436
C THIS SECTION DEALS WITH THE DETERMINATION OF THE PARAMETERS	0437
C DEALING WITH THE COEFFICIENTS OF THE SECOND ORDER PARTIAL	0438
C DIFFERENTIAL EQUATION USED TO FIND THE VALUES OF PRESSURE	0439
C AT ANY GIVEN NODE WITHIN THE MUSHY ZONE.	0440
C	0441
DO 150 $I=2.IMAXN$	0442
PPP=JMIN(I)	0443
NMT = NT (I)	0444
DO 145 $J=PPP$, NMT	0445
IF (J. GE. JWALL) GO TO 8004	0446
7 FRAC S = (Z(I,J) - ZS(I)) / KC	0447
RFRACS = (RS(J) - R(I, J)) / HC	0448
IF ((ZFRACS.LE. 1.0) . AND. (RFRACS.LE. 1.0)) GO TO 17	0449
IF ((ZFRACS.LE.1.0) .AND. (RFRACS.GT.1.0)) GO TO 71	0450
IF ((ZFRACS.GT. 1.0). AND. (RFRACS.LE. 1.0)) GO TO 171	0451
8004 CONTINUE	0452
IF((J.LE.NMT).AND.(J.GT.NT(I-1))) GO TO 111	0453
GO TO 737	0454
17 $GL(I, J-1) = GLEUT(I)$	0455
GL(I+1, J) = (GLEUT(I+1) - GLEUT(I)) * RFRACS + GLEUT(I)	0456
CL(I, J-1) = CE	0457
CL(I+1,J) = CE	0458
RHO(I,J-1) = RLE	0459
RHO(I+1,J) = RLE	0460
T(I,J-1)=TE	0461
T(I+1,J) = TE	0462
KB=2(I,J)-2S(I)	0463
KA = KC	0464
H B=HC	0465
HA=RS(J)-R(I,J)	0466
TYPE=1.0	0467
GO TO 7997	0468
	16
	Ň

71 GL $(I, J-1) = GLEUT(I)$	0469
CL(I,J-1) = CE	0470
R HO (I, J-1) = R L F	0471
T(I, J-1) = TE	0472
KB=7(1,J)-7S(1)	0473
KA = KC	0474
HB=HC	0475
HA = HC	0476
TY PE=2.0	0477
GO TO 7997	0478
171 GL(I+1.J) = (GLEUT(I+1) - GLEUT(I)) * RFRACS+GLEUT(I)	0479
CL(I+1,J) = CE	0480
R HO (I+1,J) = P L E	0481
T(I+1,J) = TE	0482
K P=KC	0483
K A=KC	0484
H B= HC	0485
HA=RS(J)-R(I,J)	0486
TYPE=3.0	0487
GO TO 7997	0488
111 HB= $((2L(I) - 2(I,J)) / (2L(I) - 2L(I-1))) * HC$	0489
GL(I-1,J)=1.0	0490
CL(I-1,J) = CO	0491
$R \operatorname{HO} (\mathbf{I} - 1, \mathbf{J}) = RO$	0492
T(I-1,J) = TL	0493
H A=HC	0494
K A = KC	0495
22K=2L(I)-2(I,J)	0496
IF (J. EQ. NMT) KA=ZZK	0497
KB=KC	0498
TYPE=4.0	0499
GO TO 7997	0500
737 CONTINUE	0501
H A = H C	0502
H B=HC	0503
K A= K C	0504
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	ZZK=ZL(I)-Z(I,J)	0505
	IF (J. EO.NMT) KA=ZZK	0506
	KB=KC	0507
	TYPE=5.0	0508
	GO TO 7997	0509
7997	CONTINUE	0510
	FACT1=1.0	0511
	FACT 2=GI (I I) **2	0512
	$PERMT (T_J) = GAMMA (T_J) * (GL (T_J) * *2)$	0513
	GZ(T,J) = (T(T,J+1) - T(T,J-1)) / (KA+KB)	0514
	GR(I,J) = (T(T+1,J) - T(T-1,J)) / (HA+HB)	0515
	EPPS $(I, J) = -GZ (I, J) * UZCL$	0516
	DERHOR = (RHO(I+1, J) - RHO(I-1, J)) / (HA+HB)	0517
	DERHOZ = $(RHO(I, J+1) - RHO(I, J-1)) / (KA+KB)$	0518
	DECLR = (CL(I+1,J) - CL(I-1,J)) / (HA+HB)	0519
	DECLZ = (CL(I, J+1) - CL(I, J-1)) / (KA + KB)	0520
	DEGLR = (GL(I+1,J) - GL(I-1,J)) / (HA+HB)	0521
	DEGLZ = (GL(I, J+1) - GL(I, J-1)) / (KA+KB)	0522
	A LPA = (RHO(I,J)/RE-1) * KON2/CL(I,J)	0523
	A = 1.0D0/R(I,J)	0524
	A = 2 + DEGLE/GL(I + J) + DERHOR/RHO(I + J)	0525
	A = A L F A + D E C L R	0526
	$B_{1=2} * DEGLZ/GL(I, J) + DERHOZ/RHO(I, J)$	0527
	B2=ALFA*DECLZ	0528
	C1=2.*DEGLZ/GL(I,J)+2.*DERHOZ/RHO(I,J)	0529
	C2=ALFA*(DECLZ-(W**2)*DECLR*R(I,J)/GFAV)	0530
	C3 = GRAV * RHO(I, J) * (C1 + C2)	0531
	C4 = DRODCL / RHO (I, J) + ALFA	0532
	C5 = EPPS(T,J) * MI/(EN*GAMMA(T,J)*GL(T,J))	0533
	C6 = (W * * 2) * (2 * RHO (I J) + 2 * RHO (I J) * R (I J) * DEGLR/GL (I J) + 2 * R (I J) *	0534
	1DRHOR)	0535
	A X = A 1 + A 2 + A 3	0536
	B=B1+B2	0537
	$C = C_{3} - C_{4} + C_{5} - C_{6}$	0538
	JF (TYPE, EO. 1.0) GO TO 7998	0539
	TF(TYPE, E0.2.0) GO TO 7999	0540
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IF (TYPE.E0.3.0) GC TO 8000	0541
IF(TYPE.E0.4.0) GO TO 8001	0542
IF (TYPE.E0.5.0) GO TO 8001	0543
7998 CONTINUE	0.544
GLE=RFRACS*(GLEUT(I+1)-GLEUT(I))+GLEUT(I)	0545
MO(I,J) = A 1S(I+1)	0546
SOLVE=MU*CONTR*UZCL/(GAMMA(I,J)*GLEUT(I)*(1.+A1S(I)**2))-RLE*GRAV	0547
SOLHZ =- MU*CONTR*UZCL*MC(I,J)/(GAMMA(I,J)*GLE*(1.+MO(I,J)**2))	0548
\$+RLE*PS(J)*(W**2)	0549
01=1./(2.*HB*(HA+HB))	0550
02=1./(2.*KA*(KA+KB))	0551
0.3 = (HA*AX) / (2.*HB*(HA+HB))	0552
O4 = KB * B / (2 * KA * (KA + KB))	0553
05 = SOLHZ/(HA + HB) - SOLVE/(KA + KB) + SOLHZ * AX * HB/(HA + HB)	0554
\$+ SOLVE*B*KA/(KA+KB) +C	0555
IF(I.EQ.2) GO TO 6711	0556
GO TO 6712	0557
6711 01=0.0	0558
Q3=0.0	0559
6712 CONTINUE	0560
06=Q1+Q2-Q3+Q4	0561
TATOP $(I, J) = (Q2+Q4)/Q6$	0562
TALEFT $(I, J) = (Q1 - Q3) / Q6$	0563
TAKONS $(I, J) = 0.5/0.6$	0564
TART(I,J) = 0.0	0565
TABOT $(I,J) = 0.0$	0566
GO TO 113	0567
7999 CONTINUE	0568
GLE=RFRACS* (GLEUT (I+1) -GLEUT (I)) + GLEUT (I)	0569
MO(I, J) = A1S(I+1)	0570
SOLVE=MU*CONTR*UZCL/(GAMMA(I,J)*GLEUT(I)*(1.+A1S(I)**2))-RLE*GRAV	0571
Q2=1./(2.*KA*(KA+KB))	0572
04 = KB * B / (2 * KA * (KA + KB))	0573
Q7 = -SOLVE/(KA+KB) + KA*SOLVE*E/(KA+KB) + C	0574
TART $(I, J) = (1./HA**2+AX*1.0/(2.*HB))/(02+04+2./(HB**2))$	0575
TATOP $(I, J) = (Q2+Q4) / (Q2+Q4+2. / (HB**2))$	0576
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	TALEFT $(I,J) = (1,/HB**2-AX*1,0/(2,*HB))/(02+04+2,/HB**2)$	0577
	TAKONS $(I,J) = 07/(02+04+2, /HB**2)$	0578
	TABOT $(\mathbf{I}, \mathbf{J}) = 0.0$	0579
	GO TO 113	0580
8000	CONTINUE	0581
9900	GLE=RPRACS*(GLFUT(T+1)-GLEUT(T))+GLEUT(T)	0582
	$MO(T_{-}J) = A 1 S (J + 1)$	0583
	SOLVE=MU*CONTR*UZCL/(GAMMA (T_J)*GLEUT(T)*(1.+A1S(T)**2))-RLE*GRAV	0584
	$SOLH7 = -MU*CONTB*U7CL*MO(I_J) / (GAMMA(I_J)*GLE*(1.+MO(I_J)**2))$	0585
:	\$+RLE*RS (J) * (W**2)	0586
	01=1./(2.*HB*(HA+HB))	0587
	03 = (HA*AX*1.0) / (2.*HB*(HA+HB))	0588
	Q8 = SOLHZ/(HA+HB) + AX * 1.0 * HB * SOLHZ/(HA+HB) + C	0589
	TATOP $(I, J) = (1./(KA**2) + B*1.00/(2.*KA))/(0.1-0.3+2./(KA**2))$	0590
	TABOT $(I, J) = (1. / (KA**2) - B*1.00 / (2. *KA)) / (01-03+2. / (KA**2))$	0591
	TALEFT $(I, J) = (Q1-Q3) / (Q1-Q3+2. / (KA**2))$	0592
	TAKONS $(I, J) = \frac{08}{(01-03+2)} (KA**2)$	0593
	TART(I,J) = 0.0	0594
	GO TO 113	0595
8001	CONTINUE	0596
	IF (J.EQ.NT(I)) GO TO 5625	0597
	GO TO 5626	0598
5625	CONTINUE	0599
	X X = K A / K C	0600
	YY=HB/HC	0601
	IF((XX.LE.0.10).AND.(YY.LE.0.10)) GO TO 5620	0602
	THEDA 1=KA*KB* (2. + AX*HB-AX*HA) + HA*HB* (2. + B*KB-B*KA)	0603
	THEDA2= $(2. + HB + AX) + HB + KA + KB / (HA + HB)$	0604
	THEDA3 = (2. + KB + B) + HA + HB + KB / (KA + KB)	0605
	THEDA4 = (2 HA * AX) * HA * KA * KB / (HA + HB)	0606
	THEDA5 = (2KA * B) * HA * HB * KA / (KA + KB)	0607
	THEDA6=KA*KB*HA*HB*C	0608
	ONE (I, J) =THEDA 2/THEDA 1	0609
	TWO $(I, J) = THEDA3/THEDA1$	0610
	TRE (I, J) = THEDA 4/THEDA 1	0611
	FOR (I, J) = THEDA5/THEDA1	0612
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	KONST(I.J) = THEDA6/THEDA1	0613
	GO TO 5628	0614
5620	CONTINUE	0615
	ONE(I,J)=0.	0616
	TWO(I,J) = 1.	0617
	TRE(I,J)=0.	0618
	FOR(I,J)=0.	0619
	$KONST(\mathbf{I}, \mathbf{J}) = 0.$	0620
5628	CONTINUE	0621
	GO TO 5627	0622
5626	CONTINUE	0623
	THEDA $1=4.*(HB/HA+1.0)*(KA**2)$	0624
	THEDA2=4.*(HA/HB+1.0)*(KA**2)	0625
	THEDA 3=2. *AX * 1.0 *HB* (KA ** 2) * (1.0+HB/HA)	0626
	THEDA4=2.*AX*1.0*HA* (KA**2)*(1.+HA/HB)	0627
	THEDA5 = ((HA + HB) * * 2)	0628
	THEDA6=4.*THEDA5+THEDA1+THEDA2+THEDA3-THEDA4	0629
	ONE $(I, J) = (THEDA1 + THEDA3) / THEDA6$	0630
	TWO $(I, J) = (2. + KA + B + 1.00) + (THEDA5/THEDA6)$	0631
	TRE(I,J) = (THEDA2 - THEDA4) / (THEDA6)	0632
	FOR(I, J) = (2KA*B*1.00) * (THEDA5/THEDA6)	0633
	KONST (I, J) =2.* (KA**2) * (THEDA5/THEDA6) *C	0634
	GO TO 5627	0635
5627	CONTINUE	0636
113	CONTINUE	0637
145	CONTINUE	0638
150	CONTINUE	0639
С		0640
C CI	ALCULATION OF COEFFICIENTS*****END	0641
C		0642
С		0643
C****	**************	0644
C C	ALCULATION OF PRESSURES****BEGIN	0645
C****	*** *** *****************	0646
С		0647
С		0648
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С	CALCULATION OF PRESSURES ALONG CENTER-LINE	0649
с		0650
	NNT = NT(1)	0651
	NMT=NNT	0652
	I=1	0653
	DO 5563 $J=2.NMT$	0654
	DEGLZ = (GL(I, J+1) - GL(I, J-1)) / (2.*KC)	0655
	PERMI(I,J) = GAMMA(I,J) * (GL(I,J) * * 2)	0656
	ALFA = (RHO(I,J)/RE-1.) * KON2/CL(I,J)	0657
	GZ(I,J) = (TL-TE)/ZILIQ	0658
	EPPS(I,J) = -G7(I,J) * UZCL	0659
	DERHOZ = (RO-RLE) / ZILIO	0660
	DECLZ = (CO-CE) / ZILIQ	0661
	$GR(\mathbf{I},\mathbf{J})=0.$	0662
	DERHOR=0.0	0663
	DECLR=0.	0664
	DEGLR=0.	0665
	B1=2.*DEGLZ/GL(I,J)+DERHOZ/RHO(I,J)	0666
	B2=ALFA*DECLZ	0667
	C1=2.*DEGLZ/GL(I,J)+2.*DERHOZ/BHO(I,J)	0668
	C2=ALFA*(DECLZ-(W**2)*DECLR*R(I,J)/GRAV)	0669
	C3=GRAV*RHO(I,J)*(C1+C2)	0670
	C4 = DRODCL/RHO(I, J) + ALFA	0671
	C5=EPPS(I,J)*MU/(EM*GAMMA(I,J)*GL(I,J))	0672
	C6= (W**2) * (2.*RHO(I,J) +2.*RHO(I,J) *R(I,J) *DEGLR/GL(I,J) +2.*R(I,J) *	0673
	1DERHOR)	0674
	B=B1+B2	0675
	c=c3-c4*c5-c6	0676
	D(I,J) = AX	0677
	B(I,J) = B	0678
	F(I,J) = C	0679
55	563 CONTINUE	0680
	NNT = NT(1)	0681
	NMT = NNT - 1	0682
	I=1	0683
	DO $430 J=2.NMT$	0684
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	IF (J. EO. 2) GO TO 5555	0685
	050=4.7(HC**2)+2.7(KC**2)	0686
	051=1./(KC * * 2) + E(I.J)/(2.*KC)	0687
	052=4./(HC**2)	0688
	0.53 = 1.7 (KC**2) -E(T.J) /(2.*KC)	0689
	$P(T_{-},T) = 051 \times P(T_{-},T+1) / 050 + 052 \times P(T+1_{-},T) / 050 + 053 \times P(T_{-},J-1) / 050 + P(T_{-},J) / 050 + P(T_{-},J-1) / 050 +$	0690
	\$050	0691
	2000 GO TO 5556	0692
5555	CONTINUE	0693
	$0.54 = 4 \cdot 1(10 \times 2) + 1 \cdot 1(4 \cdot 2) + E(1 \cdot 1) / (4 \cdot 2)$	0694
	055=4,/(HC**2)	0695
	0.56 = 1.7(4 = *KC * *2) + E(T = J) / (4 = *KC)	0696
	SOLVE=MI*CONTR*IZCL/(GAMMA(T.J)*GLEUT(T)*(1.+A1S(T)**2))-RLE*GRAV	0697
	$057 = F(T_{-J}) + SOLVE/2 + F(T_{-J}) - SOLVE/(2 + KC)$	0698
	$P(T_{1}) = 055 * P(T_{1}) / 054 + 056 * P(T_{1}) + 2) / 054 + 057 / 054$	0699
5556	CONTINUE	0700
430	CONTINUE	0701
C		0702
č c	ALCULATION OF PRESSURES ALONG SOLIDUS-INTERIOR	0703
C		0704
C.	DO 410 $T=2.TMAXN$	0705
	PPP=JMIN(T)	0706
	NMT = NT(T)	0707
	DO 408 $J=PPP$.NMT	0708
	TEGLGEJWALL) GO TO 8005	0709
	RFRACS = (RS(J) - R(J,J)) / HC	0710
	Z FRACS = (7 (1 - 1) - 7S (1)) / KC	0711
	$TF((ZFRACS_LF_1))$ AND (RFRACS_LE_1)) GO TO 888	0712
	TF((ZFRACS, LE, 1,), AND, (RFRACS, GT, 1,)) GO TO 889	0713
	$TF((2FBACS, GT, 1_), AND, (RFRACS, LE, 1_))$ GO TO 891	0714
8005	CONTINUE	0715
	TF((J, LE, NMT), AND, (J, GT, NT(T-1))) GO TO 405	0716
	GO TO 406	0717
888	CONTINUE	0718
~~~	IF (I. EO. 2) GO TO 6713	0719
	P(I,J) = TATOP(I,J) * P(I,J+2) + TALEFT(I,J) * P(I-2,J) + TAKONS(I,J)	0720
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	0721
GU = TU = 0/14	0722
6/13 P(1,J) = TATOP(1,J) + P(1,J+2) + TARONS(1,J)	0723
6714 CONTINUE	0724
GO TO 408	0725
889 CONTINUE	0726
P(I,J) = TART(I,J) * P(I+I,J) + TATOP(I,J) * P(I,J+Z) + IALEPI(I,J)	0727
P(I-1,J) + TAKONS(1,J)	0728
GO TO 408	0729
891 CONTINUE	0730
P(I,J) = TATOP(I,J) * P(I,J+1) + TALEFT(I,J) * P(I-2,J) + IABOT(I,J) + P(I-2,J) + P(I-2,J	0731
P(I, J-1) + TAKONS(I, J)	0732
GO TO 408	0733
	0734
C CALCULATION OF PRESSURES FOR INTERIOR GRID POINTS	0735
C	0736
405 CONTINUE	0737
$\frac{RR=R}{(I,J)} - HC^{*} (2L(1) - 2(1,J)) / (2L(1) - 2L(1-1))$	0738
$pp = (XLHIGH-X(I,J)) + RO + GRAV+PA+U \cdot D+ RO + (R + +2) + (R + +2)$	* 0739
P(I,J) = ONE(I,J) * P(I+1,J) + TWO(I,J) * P(I,J+1) + IKE(I,J) + P+P OR(I,J)	0740
P(I, J-1) + KCNST(I, J)	0741
GO TO 408	0742
406 CONTINUE	0742
PIGHT=ONE(I,J)*P(I+1,J)	0740
TOP=TWO(I,J)*P(I,J+1)	0745
LEFT=TRE(I,J)*P(I-1,J)	0745
BOTTOM=FOR(I,J)*P(I,J-1)	0748
P (I, J) = RIGHT + TOP + LEFT + BOTTOM + KONST (I, J)	0747
408 CONTINUE	0740
410 CONTINUE	0750
C	0750
C CALCULATION OF PRESSURES ALONG THE WALL	0751
c	0752
I=IMAX	U/00 0754
NMT = NT (I)	0704
MNT = JMIN(I)	
DO 5567 $J=MNT, NMT$	0720
	70

	IF ( (J. LE. NMT) . AND. ( J. GT. NT ( I-1 ) ) GO TO 5569	0757
	GO TO 5570	0758
5569	CONTINUE	0759
	HB = HC * (7LHIGH - 7(I, J)) / (7LHIGH - 7L(I - 1))	0760
	T(I-1,J) = TL	0761
	CL(I-1,J) = CO	0762
	RHO(I-1,J) = RO	0763
	GL(I-1,J) = 1,0	0764
	GO TO 5571	0765
5570	CONTINUE	0766
	HB=HC	0767
	GO TO 5571	0768
5571	CONTINUE	0769
	GP(I, J) = (T(I, J) - T(I - 1, J)) / HB	0770
	DERHOR = (RHO(I, J) - RHO(I-1, J)) / HB	0771
	DECLR = (CL(I,J) - CL(I-1,J)) / HB	0772
	DEGLR = (GL(I,J) - GL(I-1,J)) / HB	0773
	GZ(I,J) = (TL-TE) / (ZLHIGH-ZS(I))	0774
	DERHOZ= (RO-RLE) / (ZLHIGH-ZS (I))	0775
	DECLZ = (CO-CE) / (ZLHIGH-ZS(I))	0776
	K B=K C	0777
	K A= KC	0778
	KBB=Z (I, J) - ZS (I)	0779
	IF (J. EQ. MNT) KB=KBB	0780
	7.2K = 2L(I) - 7.(I, J)	0781
	IF(J.EQ.NMT) $KA=ZZK$	0782
	DEGLZ = (GL(I, J+1) - GL(I, J-1)) / (KA+KB)	0783
	PERMI $(I,J) = GAMMA(I,J) * (GL(I,J) * *2)$	0784
	ALFA = (RHO(I, J)/RE-1.) * KON2/CL(I, J)	0785
	FPPS(I, J) = -GZ(I, J) * UZCL	0786
	A = 1.0D0/R(I, J)	0787
	$A = 2 \cdot DEGLR/GL(I, J) + DERHOR/RHO(I, J)$	0788
	A 3= ALF A* DECLP	0789
	B 1=2. *DEGLZ/GL (I, J) + DERHOZ/RHO (I, J)	0790
	B2=ALFA*DECLZ	0791
	C1=2.*DEGLZ/GL(I,J)+2.*DERHOZ/RHO(I,J)	0792
		17
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	C2=ALFA*(DECLZ-(W**2)*DECLE*E(I,J)/GEAV)	0793
	C3 = GRAV * RHO(I, J) * (C1 + C2)	0794
	C4 = DRODCL / RHO(I, J) + ALFA	0795
	C5=EPPS(I,J) * MU/(EN*GAMMA(I,J)*GL(I,J))	0796
	$C6 = (W * * 2) * (2 * RHO (I \cdot J) + 2 * RHO (I \cdot J) * R (I \cdot J) * DEGLR/GL (I \cdot J) + 2 * R (I \cdot J) *$	0797
	1DERHOR)	0798
	AX = A1 + A2 + A3	0799
	B=B1+B2	0800
	C = C3 - C4 + C5 - C6	0801
	D(I,J) = AX	0802
	$E(\mathbf{I},\mathbf{J}) = B$	0803
	P(I,J) = C	0804
5567	CONTINUE	0805
	I =I MAX	0806
	NMT=NT(I)	0807
	MNT = JMIN(I)	0808
	DO 450 J=MNT, NMT	0809
	IF (J.EQ.MNT) GO TO 5560	0810
	IF((J.LE.NMT).AND.(J.GT.NT(I-1))) GO TO 1021	0811
	GO TO 1022	0812
5560	CONTINUE	0813
	K A=KC	0814
	KB=Z (I,J) - ZS (I)	0815
	070=2./(HC**2)+1./ (2.*KA*(KA+KB))+KB*E(I,J)/(2.*KA*(KA+KB))	0816
	071=2./(HC**2)	0817
	$Q72 = (1. + KB \times E(I,J)) / (2. \times KA \times (KA + KB))$	0818
	SOLV E=MU*CONTR*UZCL/(GAMMA(I, J)*GLEUT(I)*(1.+A1S(I)**2))-RLE*GRAV	0819
	Q73 = RHO(I, J) * (W**2) * R(I, J) * (2./HC+D(I, J)) + SOLVE* (KA*E(I, J) - 1.)/	0820
	\$ (KA+KB) +F (I, J)	0821
	P(I, J) = Q71 * P(I-1, J) / Q70 + Q72 * P(I, J+2) / Q70 + Q73 / Q70	0822
	GO TO 5561	0823
1021	RR=RADIUS-HC*(ZLHIGH-Z(I,J))/(ZLHIGH-ZL(I-1))	0824
	HB=HC* (ZLHIGH-Z(I,J)) / (ZIHIGH-ZL(I-1))	0825
	PP = PA + RO * G BAV * (ZLHIGH-Z(I, J)) + 0.5 * RO * (W * * 2) * (RR * * 2)	0826
	KB=KC	0827
	H A =HC	0823
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	K A = K C	0829
	72K = 7L(I) - 7(I,J)	0830
	IF(J.EO.NMT) KA=ZZK	0831
5559	CONTINUE	0832
	X X = K A / K C	0833
	YY=HB/HC	0834
	IF ((XX.LE.0.10), AND. (YY.LE.0.10)) GO TO 5623	0835
	060=2. *KA*KB+HB**2*(2.+KB*E(I.J)-KA*E(I.J))	0836
	0.61 = KE* (HB**2) * (2.+KB*E(I.J)) / (KA+KB)	0837
	062=2.*KA*KB	0838
	063 = KA * (HB * *2) * (2 - KA * E(I, J)) / (KA + KB)	0839
	064=RHO(I,J)*(W**2)*RADIUS*(2.*HB*KA*KB+D(I,J)*(HB**2)*KA*KB)	0840
ç	5+F(I,J)*(HB**2)*KA*KB	0841
	GO TO 5624	0842
5623	CONTINUE	0843
	Q60=1.	0844
	Q61=1.	0845
	062=.0	0846
	Q63=.0	0847
	064=.0	0848
5624	CONTINUE	0849
	P(I,J) = Q61 * P(I,J+1) / Q60 + Q62 * PP / Q60 + Q63 * P(I,J-1) / Q60 + Q64 / Q60	0850
	GO TO 5561	0851
1022	CONTINUE	0852
	H`B=HC	0853
	H A= HC	0854
	KB=KC	0855
	K A = K C	0856
	ZZK=ZL(I)-Z(I,J)	0857
	IF(J.EQ.NMT) KA=ZZK	0858
	060=2.*KA*KB+HB**2*(2.+KB*E(I,J)-KA*E(I,J))	0859
	Q61 = KB * (HB * 2) * (2 + KB * E (I, J)) / (KA + KB)	0860
	Q62=2.*KA*KB	0861
	Q63=KA* (HB**2) * (2KA*E(I,J))/(KA+KB)	0862
	Q64=BHO (I, J) * (W**2) *RADIUS* (2. *HB*KA*KB+D (I, J) * (HB**2) *KA*KB)	0863
;	<b>\$+F(I,J) *(HB**2) *KA*KB</b>	086,4
		17
		ω

P(I,J)=Q61*P(I,J+1)/Q60+Q62*P(I-1,J)/Q60+Q63*P(I,J-1)/Q60+Q64/Q60	0865
5561 CONTINUE	0866
450 CONTINUE	0867
C	0868
C CALCULATION OF PRESSURES****END	0869
C	0870
С	0871
C * * * * * * * * * * * * * * * * * * *	0872
C CALCULATION OF INTERDENDRITIC FLUID VELOCITY****BEGIN	0873
C * * * * * * * * * * * * * * * * * * *	0874
C	0875
IF (ITER. EQ. 50) GO TO 6920	0876
IF(ITER.EQ.70) GO TO 6920	0877
IF (ITER. EQ. 90) GC TO 6920	0878
IF(ITER.EQ.110) GO TO 6920	0879
GO TO 6921	0880
6920 WRITE (6,6931)	0881
6931 FORMAT(7X,'****',10X,'***',10X,'****',8X,'****',7X,'*****',	0882
\$5X, <b>!*******</b> ,4X, <b>!*****!</b> ,5X, <b>!***!</b> ,2X, <b>!***!</b> ,2X, <b>!***</b> *)	0883
WRITE (6,6922)	0884
6922 FORMAT (8X, 'GL', 12X, 'P', 12X, 'VZ', 10X, 'VR', 9X, 'VTOT', 7X, 'TTHETA',	0885
\$6X, 'RARA', 7X, 'I', 4X, 'J', 4X, 'ITER')	0886
WRITE (6,6932)	0887
6932 FORMAT(7X, *****, 10X, ****, 10X, *****, 8X, *****, 7X, ******,	0888
\$5X <b>,*******</b> ,4X, <b>******</b> ,5X <b>,****</b> ,2X <b>,***</b> ,2X <b>,***</b> */,2X <b>,**</b> ***//)	0889
6921 CONTINUE	0890
DO 790 I =1, IMAX	0891
PPP=JMIN(I)	0892
NNT = NT(I) + 1	0893
DO 776 $J=PPP$ , NNT	0894
IF (J.GE.JWALL) GO TO 8006	0895
PFRACS = (RS(J) - R(I, J)) / HC	0896
ZFRACS = (Z(I, J) - ZS(I)) / KC	0897
IF((ZFRACS.LE.1.).AND.(RFRACS.LE.1.)) GO TO 710	0898
IF ((ZFRACS.LE.1.).AND. (RFRACS.GT.1.)) GO TO 709	0899
IF((ZFRACS.GT.1.).AND.(RFRACS.LE.1.)) GO TO 722	090,0
	17

0.000		0901
8000	CONTINUS	0902
	$\frac{11}{1000} (1000) = 0.0000000000000000000000000000000$	0903
	1F((1.EQ.1MAX) AND. (J.EQ. JH1A(1))) GO 10 709	0904
		0905
/10	CONTINUE	0906
	k = 2(1, 0) - 35(1)	0907
	KA = KC	0908
	HB=HC	0909
	HA=RS(J)-R(1,J)	0910
	SOLV E=MU*CONTR*UZCL/(GAMMA(1, J)*GLEUI(1)*(I•*AIS(1)*Z)/(Z*KA)))	0911
	PDZ = (KA/(KA+KB)) * SOLVE + ((KB/(KA+KB)) * ((P(1,0+2) - P(1,0))) / (2 - KA/))	0912
	PERMI(I,J) = GAMMA(I,J) * (GL(I,J) * * 2)	0913
	VZ(I, J) = -PERMI(I, J) / (MU*GL(I, J)) + (PDZ+GRAV+RHO(I, J))	0914
	IF((I.EQ.1).OR.(I.EQ.IMAX)) GO TO OUT	0915
	GLE=RFRACS * (GLEUT (1+1) - GLEUT (1)) + GLEUT (1)	0916
	MO(I,J) = A IS(I+I)	0917
	SOLHZ = -MU * CONTR*UZCL*MU(1,J) / (GAMMA(1,J) * GLE*(1.10(1,J) * 2))	0918
	\$+RLE*RS (J) * (W ** 2)	0919
	$IF(I \cdot EQ \cdot 2) = GO = 10 = 67.15$	0920
	PDR=SOLHZ*HB/(HA+HB) + (HA/(HA+HB)) + ((P(1,0) - P(1-2,0))) / (2.1HD))	0921
	GO TO 6715	0922
6715	PDR = SOLHZ * HB/(HA + HB)	0923
6716	CONTINUE	0924
	VR(I, J) = -P ERMI(I, J) / (MU*GL(I, J)) * (PDR-RHO(I, J) * (W**2) * R(I, J))	0925
	GO TO 602	0926
601	VR(I, J) = 0.0	0927
	GO TO 602	0927
602	CONTINUE	0920
	GO TO 740	0220
709	CONTINUE	0930
	H A=HC	0.22
	HB=HC	0932
	K A = KC	0933
	KB=Z (I, J) -ZS (I)	0734 0035
	SOLVE=MU*CONTR*UZCL/(GAMMA(I, J)*GLEUT(I)*(1.+A1S(I)**2))-RLE*GRAV	0930
	PDZ = (KA/(KA+KB)) *SOLVE+((KB/(KA+KB)) * ((P(I,J+2)-P(I,J))/(2.*KA)))	9260
		75

DEDMT /T T) -CAMMA /T T) */CT /T T) **2)	0937
$\frac{1}{2} = \frac{1}{2} = \frac{1}$	0938
$\frac{1}{1} = \frac{1}{2} E_{\text{RH}} (1,0) / (1000 E_{1},0) / (2000 E_{1},0) / (2$	0939
$\frac{1}{1} \left( \frac{1}{1} + \frac{1}{2} + \frac{1}{1} + \frac{1}{2} + \frac{1}{1} + \frac{1}{2} + \frac{1}{1} + \frac{1}{2} + 1$	0940
$PDR = \left\{ P \left\{ I + P \right\} \right\} = P \left\{ I - P \left\{ I - P \right\} \right\} / \left\{ Z + P D \right\}$ $PDR = \left\{ P \left\{ I + P \right\} \right\} = P \left\{ I - P \right\} + \left\{ I - P \right\} + \left\{ I - P \right\} \right\} + \left\{ I - P \right\} + \left\{ I - $	.1)) 0941
$\sqrt{\pi} (1,0) = 2 \ln \pi 1 (1,0) / (\pi 0 - 0 - (1,0)) + (2 - \pi \pi 0 - (1,0)) + (\pi - 2) + \pi (1,0)$	0941
60  10  004	0942
	0945
GO 10 004 60# CONTINUE	0945
	0945
90 10 740 700 CONTINUE	0947
$\frac{1}{22} = \frac{1}{2} = 1$	0948
n H - n S(0) = n(1,0)	0948
	0950
	0951
$PD7 = (P(T_1, I+1) - P(T_1, I-1)) / (2 + KA)$	0952
PRRMI (T, J) = GAMMA (T, J) * (GL (T, J) * 2)	0953
$V_{2}(T_{1}J) = -PFRMT(T_{1}J) / (MI*GL(T_{1}J)) * (PD2+GRAV*RHO(T_{1}J))$	0954
TE((T, FO, 1), OR, (T, FO, TMAX)) GO TO 605	0955
GLR = R FR A C S * (GL FUT (T+1) - GL RUT (T)) + GL RUT (T)	0956
$MO(T_{-1}) = 15(T+1)$	0957
SOLHZ= $-MU \times CONTR \times UZCL \times MO(T_J) / (GAMMA(T_J) \times GLE \times (1_+MO(T_J) \times A$	(2)) 0958
\$+RIE*RS(.1) */W**2)	0959
$PDR = SOLHZ * HB / (HA + HB) + (HA / (HA + HB)) * ((P (T_J) - P (T - 2_J)) / (2_* * HB))$	(B)) 0960
$VR(T_{J}) = -PRMT(T_{J}) / (MI*GL(T_{J})) * (PDP-RHO(T_{J})) * (W**2) * R(T_{J})$	
	0962
605  VB(T,J) = 0.0	0963
GO TO 606	0964
606 CONTINUE	0965
$\begin{array}{c} \text{GO}  \text{TO}  \textbf{740} \end{array}$	0966
8002 CONTINUE	0967
7.7 K = 7.1 (1) - 7.(1 - 1)	0968
IF(J, EO, NT(I)) KA = 7.7K	0969
IF(J.LT.NT(I)) KA=KC	0970
PDZ = (P(I, J+1) - P(I, J-1)) / (KA+KC)	0971
PERMI(I,J) = GAMMA(I,J) * (GL(I,J) * * 2)	0972
	6

IF ((I.EQ.1).OB. (I.EQ.IMAX)) GO TO 727 NMT=NT (I) IF ((J.LE.NMT).AND. (J.GT.NT (I-1))) GO TO 7777 GO TO 7778 7777 CONTINUE HB=HC* (ZL (I)-Z (I,J)) / (ZL (I)-ZL (I-1))	0974 0975 0976 0977 0978 0979 0980 0981 0981 0982 0983 0983
NMT=NT(I) IF((J.LE.NMT).AND.(J.GT.NT(I-1))) GO TO 7777 GO TO 7778 7777 CONTINUE HB=HC*(ZL(I)-Z(I,J))/(ZL(I)-ZL(I-1))	0975 0976 0977 0978 0979 0980 0981 0981 0982 0983 0983
IF ((J.LE.NMT) AND. (J.GT.NT(I-1))) GO TO 7777 GO TO 7778 7777 CONTINUE HB=HC* (ZL(I)-Z(I,J)) / (ZL(I)-ZL(I-1))	0976 0977 0978 0979 0980 0981 0981 0982 0983 0983
GO TO 7778 7777 CONTINUE HB=HC*(ZL(I)-Z(I,J))/(ZL(I)-ZL(I-1))	0977 0978 0979 0980 0981 0982 0983 0984
7777 CONTINUE HB=HC*(ZL(I)-Z(I,J))/(ZL(I)-ZL(I-1))	0978 0979 0980 0981 0982 0983 0983
HB = HC * (ZL(I) - Z(I, J)) / (ZL(I) - ZL(I-1))	0979 0980 0981 0982 0983 0983
	0980 0981 0982 0983 0984
RB=R(I,J)-HB	0981 0982 0983 0984 0984
PP = PA + RO * GRAV * (ZLHIGH - Z(I, J)) + 0.5 * RO * (W * * 2) * (RR * * 2)	0982 0983 0984
PDR = (P(I+1,J) - PP) / (HC + HB)	0983 0984
VR(I, J) = -PERMI(I, J) / (MU*GL(I, J)) * (PDR-RHO(I, J) * (W**2) * R(I, J))	0984
GO TO 728	1005
7778 CONTINUE	1100
HB=HC	0986
GO TO 5604	0987
5604 CONTINUE	J988
PDR = (P(I+1,J) - P(I-1,J)) / (HC+HB)	0989
VR(I,J) = -PERMI(I,J) / (MU*GL(I,J)) * (PDR-RHO(I,J) * (W**2) * R(I,J))	0990
GO TO 728	0991
727 VP $(I, J) = 0.0$	0992
GO TO 728	0993
728 CONTINUE	0994
GO TO 740	0995
724 PDZ= $(P(I,J)-P(I,J-2)) / (ZL(I)-Z(I,J-2))$	0996
PERMI (I,J) = GAMMA (I,J) * (GL (I,J) * * 2)	0997
VZ (I,J) = -P ERMI (I,J) / (MU*GL (I,J)) * (PDZ+GRAV*RHO (I,J))	0998
IF((I.EQ.1).OR.(I.EQ.IMAX)) GO TO 730	)999
IF(ZL(I-1).EQ.ZL(I)) GO TO 5598	1000
IF (ZL (I+1).GE.Z (I+1,J)) GO TO 5596	1001
IF(ZL(I+1).LT.Z(I+1,J)) GO TO 5597	1002
GO TO 5600	1003
5596 PDR=((P(I+1,J-1)+(P(I+1,J)-P(I+1,J-1))*(ZL(I)-Z(I,J-1))/KC)	1004
\$-P(I,J))/HC	1005
GO TO 5600	1006
5597 PDR=((P(I+1,J-1)+(P(I+1,J)-P(I+1,J-1))*(ZL(I)-Z(I,J-1))/(ZL(I+1)-	1007
\$Z (I+1,J-1)))-P(I,J))/HC	100 <u>ള</u>
	77

	GO TO 5600	1009
5598	PDR = (P(T+1,J) - P(T-1,J)) / (2,*HC)	1010
5600	CONTINUE	1011
	VP(I,J) = -PERMI(I,J) / (MU*GL(I,J)) * (PDR-RHO(I,J) * (W**2) * R(I,J))	1012
	GO TO 731	1013
730	$V = (T_{-}, J) = 0, 0$	1014
100	GO TO 731	1015
731	CONTINUE	1016
740	CONTINUE	1017
	VTOT = (VR(I,J) **2 + VZ(I,J) **2) **0.5	1018
	IF(VR(I,J),EO,0.0) VR(I,J)=1.0D-6	1019
	A NG = VZ (I, J) / VR (I, J)	1020
	TTHETA = (180.0/PI) * DATAN (ANG)	1021
	BARA = (VR(I,J) * GR(I,J) + VZ(I,J) * GZ(I,J)) / EPPS(I,J)	1022
	IF(ITER.E0.50) GO TO 6911	1023
	IF (ITER. EQ. 70) GO TO 6911	1024
	IF (ITER. EQ. 90) GO TO 6911	1025
	IF (ITER. EQ. 110) GO TO 6911	1026
	GO TO 776	1027
6911	CONTINUE	1028
	WRITE (6,7500) GL (I, J), $P(I, J)$ , $VZ(I, J)$ , $VR(I, J)$ , $VTOT$ , TTH ETA, RARA,	1029
	\$I, J, ITER	1030
7500	FORMAT(1X, 1E13.4, 1E15.6, 5E12.3, 2I5, 1I7/)	1031
776	CONTINUE	1032
790	CONTINUE	1033
805	CONTINUE	1034
С		1035
СС	ALCULATION OF INTERDENDRITIC FLUID VELOCITY****END	1036
С		1037
С		1038
C****	** *** ********************************	1039
с с	ALCULATION OF MACROSEGREGATION****BEGIN	1040
C****	** ** * * * * * * * * * * * * * * * * *	1041
С		1042
С	INTEGRATION OF THE LOCAL SOLUTE DISTRIBUTION EQUATION IS	1043
С	FOLLOWED-THROUGH COLUMN-WISE STARTING FROM THE LIQUIDUS.	1044
	~	4 7
		â

С

	1045
IF(ITER.E0.50) GO TO 6918	1046
IF (ITER.E0.70) GO TO 6918	1047
IF (ITER. EQ. 90) GO TO 6918	1048
IF (ITER. EO. 110) GO TO 6918	1049
GO TO 6919	1050
6918 CONTINUE	1051
WRITE (6,6933)	1052
6933 FORMAT (5X, ************************************	1053
\$ ! ************* <b>!</b> 5X <b>! ******</b> ** <b>!</b> 5X <b>! ***</b> ***!)	1054
WRITE (6,9900)	1055
9900 FORMAT (5X, 'LOCAL SOLUTE COMP', 4X, 'FRACT LIQUID EUTECTIC', 4X,	1056
\$'RADIUS OF INGOT', 5X, 'COLUMN NO', 5X, 'ITERAT')	1057
WRITE (6,6934)	1058
6934 FORMAT (5X, ************************************	1059
\$1************************************	1060
6919 CONTINUE	1061
SUUM1=0.0	1062
SUUM2=0.0	1063
DO 1020 I=1, IMAX	1064
NMT = NT(I)	1065
SUM=0.	1066
MNT = JMIN(I)	1067
DO 810 IT=MNT, NMT	1068
NN=NMT-IT	1069
J=NN+MNT	1070
IF $(J.EQ.NMT)$ NLGL $(J+1) = 0.0$	1071
COEFT 1 = -KON4 * RHO (I, J) / (CL (I, J) * RE)	1072
COEPT2 = -KON4 * RHO(I, J+1) / (CL(I, J+1) * RE)	1073
RATER1=VR(I,J) *GR(I,J) + $VZ(I,J)$ * GZ(I,J)	1074
RATER2=VB(I, J+1) *GR(I, J+1) +VZ(I, J+1) *GZ(I, J+1)	1075
VZE(I) = -CONTR*UZCL/(1.+A1S(I)**2)	1076
VRE(I) = -A1S(I) * VZE(I)	1077
RATERE=VZE(I) * (TL-TE) / (ZL(I) -ZS(I)) - VBE(I) * (TL-TE) *A1S(I) /	1078
\$ (ZL (I) - ZS (I) )	1079
FN(J) = COEFT1*(1.+RATER1/EPPS(I,J))	1080
	1 7
	9

	$FN(J+1) = COEFT2*(1_{+}+RATER2/EPPS(1_{+}J+1))$	1081
	NLGL(J) = .5 * (CL(T, J) - CL(T, J+1)) * (FN(J) + FN(J+1)) + SUM	1082
	TF(NLGL(J), GT, 0, 0) $NLGL(J) = 0, 0$	1083
	SIIM = N LGL (J)	1084
	GL(T,J) = EXP(NLGL(J))	1085
	GS(J) = 1, 0 - GI(J, J)	1086
	CS(J) = KAY * CL(T, J)	1087
	GO TO 810	1088
	810 CONTINUE	1089
	J=MNT	1090
	EPPSE = -(TL - TE) * UZCL / (ZL(I) - ZS(I))	1091
	NLGE=NLGL(J)+0.5*(CE-CL(I,J))*((-KON4*RLE/(CE*RSE))*(1.+RATERE/	1092
	EPPSE) + FN(J)	1093
	GEE=EXP(NLGE)	1094
С		1095
С	LOCAL SOLUTE COMPOSITION FOR DESIGNATED RADII WITHIN	1096
С	THE INGOT IS INITIATEE.	1097
С		1098
	J=JMIN(I)	1099
	SUMMS = 0.5*(CSE + CS(J))*((1GEE) - GS(J))	1100
	NNT = NT(I) + 1	1101
	J=NNT	1102
	GS(J) = 0.0	1103
	CS(J) = KAY * CO	1104
	PPP=JMIN(I)+1	1105
	DO 850 J=PPP,NNT	1106
	SUMMS = .5*(CS(J)+CS(J-1))*(GS(J-1)-GS(J))+SUMMS	1107
	850 CONTINUE	1108
	GLEUT (I) =GEE	1109
	TNT=RE*SUMMS+RSE*CE*GEE	1110
	DDD=RE*(1GEE)+RSE*GEE	1111
	LOCCOM(I) = TNT/DDD	1112
С		1113
С	AVERAGE INGOT COMPOSITION ACROSS THE INGOT IS CALCULATED	1114
С		1115
	$1 F (1 \cdot EQ \cdot T) = GO = TO = 880$	1116
		80
	TE(T. RO. TMAX) GO TO 885	1117
----------	---------------------------------------------------	----------
	DELEAD=HC	1118
		1119
880	DELBAD=HC/2.	1120
67 CF AF	BOR(T) = HC/4	1121
	$\frac{1}{2} = \frac{1}{2} + \frac{1}{2}$	1122
885	$DFLB \Delta D = HC/2$	1123
890		1124
095	SHIM $1 = ROR(T) * TNT * DELRAD + SHIM 1$	1125
	SUUM 2 = ROR(I) * DDD * DEL RAD + SUUM 2	1126
	CSINGT=SHUM1/SHUM2	1127
	ROR(1) = 0.0	1128
	IF(ITER.E0.50) GO TO 6913	1129
	IF (ITER. E0.70) GO TO 6913	1130
	IF(ITER.E0.90) GO TO 6913	1131
	IF (ITER. EO. 110) GC TO 6913	1132
	GO TO 1020	1133
6913	CONTINUE	1134
	WRITE (6,7900) LOCCOM(I), GEE, ROR(I), I, ITER	1135
7900	FORMAT(1X, 1E18.4, 1E23.4, E20.3, 1I13, 1I13/)	1136
	IF (I. EQ. I MAX) GO TO 6914	1137
	GO TO 1020	1138
6914	WRITE(6,6935)	1139
6935	PORMAT (5X, ************************************	1140
	WRITE (6,6915)	1141
6915	FORMAT (5X, 'AVFRAGE INGOT COMPOSITION')	1142
	WRITE (6,6936)	1143
6936	FORMAT (5X, ************************************	1144
	WRITE (6,6916) CSINGT	1145
6916	FORMAT (1X, 1E20.4///)	1146
С		1147
C C	ALCULATION OF MACROSEGREGATION****END	1148
С		1149
	WRITE (6,6937)	1150
6937	FOR MAT (2X, ************************************	× 1151
	\$* * * * * * * * * * * * * * * * * * *	1152
		18
		<u>с</u>

1020 CONTINUE	1153
C	1154
C CALCULATION OF MACROSEGREGATION****END	1155
C	1156
GL(1,1) = GLEUT(1)	1157
GL (IMAX, JWAL) =GLEUT (IMAX)	1158
1000 CONTINUE	1159
C	1160
C ITERATION SEQUENCE FOR 'P', VELOCITY, 'GL' AND COPM****END	1161
С	1162
STOP	1163
END	1164

## BIOGRAPHICAL NOTE

The author was born on September 5, 1949 in Taiwan, the Republic of China. He completed his Bachelor's degree in Chemical Engineering at National Taiwan University in 1971 and Master's degree in Materials Engineering at the University of Wisconsin, Milwaukee in 1974. He entered MIT Graduate School in 1974.

He has the following publications:

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