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PHD'S PROGRAM IN SCIENCE AND TECHNOLOGIES OF  
CHEMISTRY AND MATERIALS

**PRODUCTION OF GRAPHENE AND TWO  
DIMENSIONAL CRYSTALS BASED  
FUNCTIONAL ELECTRODE FOR LITHIUM  
ION BATTERIES**

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# LIST OF PUBLICATIONS AND CONTRIBUTIONS

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# LIST OF ABBREVIATIONS

0D	zero dimensional
1D	one dimensional
2D	two dimensional
3D	three dimensional
$\gamma$	surface tension
AFM	atomic force microscopy
BET	Brunauer – Emmett – Teller measurement
BM	ball-milling
b.p.	boiling point
CB	carbon black super-P
CMGs	chemically modified graphene
CNTs	carbon nanotubes
CPE	constant phase element
CV	cyclic voltammetry
CVD	chemical vapor deposition
CHP	N-cyclohexyl-2-pyrrolidone
DMC	dimethyl carbonate
DMF	dimethylformamide
DOD	depth of discharge
EC	ethylene carbonate
EFTEM	energy filtered elemental mapping
(HAADF)-STEM	high angular annular dark field - scanning TEM
EDS	energy dispersive X-ray spectroscopy
EIS	electrochemical impedance spectroscopy
EELS	electron energy loss spectroscopy
ESSs	energy storage systems
EtOH	ethanol
EVs	electric vehicles
FCs	fuel cells
FL-BP	few-layer black phosphorous
FLG	few layer graphene
FWHM	full width at half maximum
GNPs	graphene nanoplatelets
GO	graphene oxide
HAADF-STEM	high angular annular dark field-Scanning TEM
HEVs	hybrid electric vehicles
HMWPs	high molecular-weight polymers
HRTEM	high resolution-TEM
IPA	2-propanol
LCO	LiCoO <sub>2</sub>
LFP	LiFePO <sub>4</sub>
LIBs	lithium ion batteries
LNMO	LiNi <sub>0.5</sub> Mn <sub>1.5</sub> O <sub>4</sub>
LO	longitudinal
LPE	liquid phase exfoliation
MC	micromechanical cleavage

MLG	multi-layer graphene
MoO <sub>3</sub> /SWNTs	hybrid structure of SWNT-bridged MoO <sub>3</sub>
MoS <sub>2</sub> /C	MoS <sub>2</sub> /amorphous carbon composites
m-SWNTs	metallic SWNTs
OES	optical extinction spectroscopy
OAS	optical absorption spectroscopy
PAA	poly(acrylic acid)
PVdF	polyvinylidene fluoride
RBM <sub>s</sub>	radial breathing modes
R <sub>CT</sub>	charge transfer resistance
R <sub>E</sub>	electrolyte resistance
RGO	reduced graphene oxide
SA	surface area
SBS	separation based sedimentation
SC <sub>s</sub>	supercapacitors
SEI	solid electrolyte interface
SEM	scanning electron microscopy
HRSEM	high resolution-SEM
SLG	single-layer graphene
SOC	state of charge
s-SWNTs	semiconducting SWNTs
SWNT <sub>s</sub>	single wall carbon nanotubes
TEM	transmission electron microscopy
TGA	thermogravimetric analysis
TMO <sub>s</sub>	transition metal oxides
TMS <sub>s</sub>	transition metal sulfides
TO	tangential
XPS	X-ray Photoelectron Spectroscopy
XRD	powder X-ray diffraction

# CONTENTS

<b>Abstract</b> .....	1
<b>Chapter 1: Introduction</b>	
1.1. Global overview of lithium ion batteries.....	5
1.2. Fundamental of lithium ion batteries.....	6
1.2.1. History of lithium ion batteries .....	6
1.2.2. Working principles of lithium ions batteries.....	8
1.2.3. Anode of lithium ion batteries.....	11
1.2.4. Cathode of lithium ion batteries .....	15
1.2.5. Electrolyte, separator and current collectors .....	16
1.3. Current challenges and opportunities of anodes in lithium ion batteries .....	19
1.4. Graphene and other 2 dimensional materials: the promising anode materials for lithium ion batteries .....	22
1.4.1. Graphene .....	24
1.4.2. Molybdenum trioxide.....	24
1.4.3. Molybdenum disulfide .....	25
1.4.4. Black Phosphorus .....	25
<b>Chapter 2: Experimental procedure</b>	
2.1. Production and processing of graphene and other two dimensional materials .....	28
2.1.1. Liquid phase exfoliation.....	28
2.1.2. Solvent exchange processes .....	30
2.1.3. Experimental .....	30
2.2. Preparation of single wall carbon nanotube-bridged molybdenum hybrid and molybdenum disulfide/amorphous carbon composite.....	32
2.2.1. Preparation of single wall carbon nanotubes-bridged molybdenum hybrid .....	32
2.2.2. Preparation of molybdenum disulfide/amorphous carbon hybrid.....	33
2.3. Material characterization techniques .....	33
2.3.1. Optical absorption spectroscopy .....	33

2.3.2. Thermogravimetric analysis .....	34
2.3.3. Powder X-ray diffraction .....	34
2.3.4. Raman spectroscopy.....	34
2.3.5. Transmission electron microscopy .....	34
2.3.6. Scanning electron microscopy .....	35
2.3.7. Atomic Force Microscopy.....	35
2.3.8. X-ray Photoelectron Spectroscopy.....	35
2.3.9. Specific surface-area measurements .....	35
2.3.10. Optical extinction spectroscopy .....	36
2.4. Electrode fabrication and battery assembling .....	36
2.4.1. Electrode fabrication.....	36
2.4.2. Assembling of half- and full-cells .....	37
2.5. Electrochemical characterizations .....	38
2.5.1. Cyclic voltammetry.....	38
2.5.2. Galvanostatic charge/discharge cycling measurement .....	39
2.5.3. Electrochemical impedance spectroscopy .....	40

### **Chapter 3: Characterizations of graphene and other two dimensional materials**

3.1. Graphene flakes.....	43
3.1.1. Characterizations of graphene flakes in N-Methyl-2-pyrrolidone and ethanol.....	43
3.1.2. Characterizations of graphene flakes having different lateral size and thickness.....	48
3.2. Single wall carbon nanotubes.....	53
3.3. Molybdenum trioxide nanosheets and single wall carbon nanotube-bridged molybdenum oxide hybrid.....	55
3.4. Molybdenum disulfide flakes and molybdenum disulfide/amorphous carbon hybrid.....	57
3.4.1. Molybdenum disulfide flakes .....	57
3.4.2. Molybdenum disulfide/amorphous carbon hybrids .....	60
3.5. Black phosphorus .....	63
3.5.1. Solvent analysis.....	63



3.5.2. Morphological characterization of BP flakes in CHP and acetone .....	68
<b>Chapter 4: Application of graphene for lithium ion batteries</b>	
4.1. Introduction .....	76
4.2. Graphene based binder-free anode for lithium ion batteries .....	79
4.3. The influence of graphene flake morphology on electrochemical properties of graphene based anode in lithium ion batteries .....	84
4.4. Conclusion.....	91
<b>Chapter 5: Application of molybdenum trioxide and molybdenum disulfide for lithium ion batteries</b>	
5.1. Introduction .....	93
5.2. Carbon nanotubes-bridged MoO <sub>3</sub> hybrid structure as high performance anode for lithium ion batteries .....	95
5.3. Molybdenum disulfide flakes/amorphous carbon hybrid as anode for lithium ion batteries .....	104
5.4. Conclusion.....	115
<b>Chapter 6: Application of black phosphorous for lithium ion batteries</b>	
6.1. Introduction .....	117
6.2. Few-layer black phosphorus as anode for lithium ion batteries .....	118
6.3. Conclusion.....	122
<b>Chapter 7: Conclusion and outlook</b>	
7.1. Graphene-based anode for lithium ion batteries.....	123
7.2. Molybdenum oxide- and molybdenum trioxide-based anode for lithium ion batteries .....	125
7.3. Black phosphorous-based anode for lithium ion batteries .....	127
7.4. Future development.....	128
<b>References</b> .....	131

# Abstract

The rapid development of electronic portable devices, electric cars, etc. has boosted the requirement of portable and efficient energy storage systems. In this context, lithium ion batteries (LIBs) technology has emerged as one of the most promising for the aforementioned applications. In the last years, strong efforts have focused on LIBs research and technology. As a result, substantial achievements in LIB technology have been harvested, such as the introduction of new electrode materials with high capacity, and the invention of new electrolytes with high electrochemical stability in different environmental conditions. Although the present LIBs exhibit more than twice the energy density with respect to the first commercial one introduced by Sony in 1991, several challenges still need to be solved in order to further apply LIBs for high energy and power applications, *e.g.*, electrical vehicles. These challenges include safety, cost, improvement in life-time, and increase in energy and power densities of LIBs. It should be noted that most of these concerns are related to the use of electrode active materials; therefore, the development of high-performance anode and cathode is one of the critical requirements in current LIBs technology. The on-going research exhibits that the current cathode with particular specific capacity values leaves small room for further improvement in energy density, but the anode can be tuned to obtain higher specific capacity and energy efficiency, as well as longer cycle life. Thus, tremendous efforts have been devoted to the development of high-performance LIB anodes, which can provide high energy, power density for the LIBs and can adapt to the environmental constraints and ultimately suit the needs of industrial-scale production at low-cost. Up to date, conventional LIB anodes commonly use graphite as active material due to its high coulombic efficiency ( $\sim 99\%$ ), low potential profile versus lithium ( $\sim 0.2$  V) and structural stability during charge/discharge cycling. However, the main limiting factor of graphite relies on its theoretical maximum specific capacity that is limited to  $372 \text{ mA h g}^{-1}$  since every six carbon atom can host only one  $\text{Li}^+$  determined by the  $\text{LiC}_6$  stoichiometry, which is not suitable for the development of high energy density LIBs. For this reason, there is a significant scientific interest in replacing graphite with higher specific capacity anode materials. For example, metal and metal oxides, such as Sn ( $933 \text{ mAh g}^{-1}$ ), Si ( $3579 \text{ mAh g}^{-1}$ ), Ge ( $1623 \text{ mAh g}^{-1}$ ),  $\text{SnO}_2$  ( $782 \text{ mAh g}^{-1}$ ), and  $\text{Co}_3\text{O}_4$  ( $890 \text{ mAh g}^{-1}$ ), have higher lithium storage capacities than graphite via the formation of alloys with lithium or through the reversible reactions with  $\text{Li}^+$ . However, these electrodes are still facing with the severe issue associated with the large volume change during the charging/discharging cycles, resulting in the pulverization of the electrode, and consequently poor electrochemical reversibility. The exploitation of anode materials with long lasting life cycles and high specific capacity for LIBs is still a challenge for the scientific community.

Thus, seeking new anode materials for the next-generation of LIBs is a mandatory task for both academia and industry. The aim of my PhD work was to investigate nanomaterials, *e.g.*, carbon nanotubes (CNTs), graphene and other two-dimensional (2D) crystals as potential materials for future LIB electrodes. In particular, I studied the electrochemical properties of four promising materials for LIB anodes, *e.g.*, graphene, molybdenum trioxide ( $\text{MoO}_3$ ), molybdenum disulfide ( $\text{MoS}_2$ ) and black phosphorous (BP). For what concerns graphene, I focused on the production and processing to optimize the fabrication of binder-free graphene anode. Furthermore, I carried out the study of the effect of graphene flakes dimension (lateral size and thickness) on the  $\text{Li}^+$  storage capability. In particular, I sorted graphene flakes by layer numbers and lateral size, investigating the influence of the flakes morphology on the electrochemical performance upon lithiation/de-lithiation. This strategy provides useful guidelines for the practical exploitation of few- (FLG) and multi- (MLG) layer graphene as stand-alone anode materials in LIBs. To achieve this target, I have produced graphene flakes by liquid phase exfoliation (LPE) of graphite and then tuned the morphology of graphene flakes by means of *sedimentation-based separation* (SBS).

After the study on graphene, I shifted my interest to other layered materials such as  $\text{MoO}_3$  and  $\text{MoS}_2$ . Similar to the production of graphene, I started carrying out the production of few-layer  $\text{MoO}_3$  and  $\text{MoS}_2$  flakes via LPE of their bulk counterparts, then studied the electrochemical behaviors of  $\text{MoO}_3$  and  $\text{MoS}_2$  flakes based anodes in order to find the strategies to improve  $\text{Li}^+$  storage ability of these anodes. This approach utilizes the LPE to produce nano-sized flakes, which are able to resist the mechanical degradation caused by volume changes of these materials upon cycling of LIB. Although the nano-sized  $\text{MoO}_3$  and  $\text{MoS}_2$  flakes can exhibit the advantage in structural preservation of anodes, they are still facing with the issues of low intrinsic electrical conductivity which cause poor rate performance. Thus, it is necessary to integrate the high electrical conductive materials, *e.g.*, carbon based materials, with  $\text{MoO}_3$  and  $\text{MoS}_2$  to improve their electrical conductivity when integrated in LIB anodes.

To realize this strategy, I firstly synthesized the hybrid structure of single wall carbon nanotubes-bridged  $\text{MoO}_3$  ( $\text{MoO}_3/\text{SWNTs}$ ) via a low-cost, non-toxic and simple solution mixing method. Afterward, the binder-free  $\text{MoO}_3/\text{SWNT}$  anodes were fabricated to study the effects of SWNTs content (wt%) on the electrochemical behaviors of  $\text{MoO}_3$ . The SWNTs network in this electrode is demonstrated to play the role of conducting channels for electronic transport, and a buffered network for volume change of  $\text{MoO}_3$ . This study sets the basis for the exploitation of exfoliated  $\text{MoO}_3$  flakes as anode materials in high performance

LIB. Moreover, the binder-free MoO<sub>3</sub>/SWNTs hybrid anode prepared by the simple aforementioned method can boost the development of high performance anodes for LIBs.

As for MoS<sub>2</sub>, I designed a fabrication method of MoS<sub>2</sub> flakes/amorphous carbon hybrid (MoS<sub>2</sub>/C) anodes based on a thermal composition of a carbon source, *e.g.*, poly(acrylic acid) (PAA) in the mixtures of MoS<sub>2</sub>/PAA. The MoS<sub>2</sub>/C based anodes are built to investigate the effects of different carbon contents on electrochemical performance of the hybrid and optimize the proper carbon content. This work clarified that a proper content of carbon not only improves the electrical conductivity of electrode by facilitating the electron transport, but also acting as a buffer layer for active materials to avoid its pulverization upon cycling. Hence, the study of MoS<sub>2</sub>/C electrodes gives the research community a protocol for large-scale production of MoS<sub>2</sub>/carbon hybrid and also can be easily extended to the construction of other 2D nano-crystals, such as transition metal sulfide (TMSs), transition metal oxides (TMOs), dispersed in amorphous carbon networks for Li<sup>+</sup> storage application.

The last activity in this thesis focuses on the study of production and LIB application of few-layer BP (FL-BP) flakes. Similar to the production of graphene, MoO<sub>3</sub> and MoS<sub>2</sub>, LPE was used as strategic route for the large-scale production of FL-BP. The exploitation of FL-BP flakes in cutting-edge technologies, *e.g.*, in flexible electronics and energy storage, is however limited by the fact that the LPE of BP is usually carried out at a high boiling point (b.p.) and in toxic solvents. In fact, the solvent residual is detrimental to device performance in real applications, thus complete solvent removal is critical. To overcome these issues, I carried out the LPE of BP in different low-b.p. solvents. Among these solvents, the LPE of BP in acetone exhibited a high concentration of FL-BP (FL-BP<sub>acetone</sub>) flakes. Taking the advantage of low-b.p. solvent, *e.g.*, acetone, I further fabricated the FL-BP based anode to study the electrochemical properties of this material for LIB anode. The electrochemical study of FL-BP<sub>acetone</sub>-based anode indicates a promising design of fast charge/discharge devices.

In summary, the Thesis is organized as follow.

**Chapter 1** shows the global view and the fundamental understanding of current LIB technology, a brief review of challenges and opportunities for future LIB, together with the introduction of several promising candidates for LIB anodes such as graphene and other 2D materials (MoO<sub>3</sub>, MoS<sub>2</sub> and BP).

**Chapter 2** reviews LPE for layered materials. The production and processing of graphene, MoO<sub>3</sub>, MoS<sub>2</sub> and BP by LPE as well as the synthesis of MoO<sub>3</sub>/SWNTs and MoS<sub>2</sub>/C hybrids

for LIB are reported. The electrode fabrication, cell-assembling are introduced, together with full material and electrochemical characterization techniques.

**Chapter 3** dedicates to the characterizations of each type of materials, e.g., graphene, MoO<sub>3</sub>, MoS<sub>2</sub>, MoO<sub>3</sub>/SWNTs, MoS<sub>2</sub>/C hybrids and BP. This chapter lays a solid foundation for the understanding of electrochemical performances of each material which will be discussed in Chapter 4, 5 and 6.

**Chapter 4** concerns the study of graphene for LIB application. The first part of this chapter focuses on the processing of LPE graphene via a solvent exchange process and electrochemical performance of binder-free graphene anode in both half-cell and full-cell configurations. The second part provides a fundamental understanding of the role of graphene flakes dimension (lateral size and thickness) on the Li<sup>+</sup> storage ability of graphene anodes.

**Chapter 5** covers the activities of MoO<sub>3</sub> and MoS<sub>2</sub> based LIB anodes. The study on electrochemical properties of MoO<sub>3</sub> and MoO<sub>3</sub>/SWNTs hybrid demonstrates the role of SWNTs in Li<sup>+</sup> storage ability of MoO<sub>3</sub>. While the study on electrochemical properties of MoS<sub>2</sub> and MoS<sub>2</sub>/C hybrid provides the understanding of the effects of carbon content on Li<sup>+</sup> storage ability of MoS<sub>2</sub> based anodes.

**Chapter 6** describes the study on electrochemical properties of FL-BP-based anodes for LIBs. The study on electrochemical properties of FL-BP exfoliated in acetone indicates that it is promising with regards to the fast charge/discharge LIBs. Overall, the presented process is a step towards the fabrication of phosphorene-based devices.

**Chapter 7** summarizes the most important insights achieved in the research topics of graphene, MoO<sub>3</sub> and MoS<sub>2</sub>, from material to electrochemical characterizations. Moreover, the future plans for exploring these materials for LIBs are discussed.

# Chapter 1:

## Introduction

### 1.1. Global overview of lithium ion batteries

The changing global landscape, such as industrial development and growing human population, has led to a range of problems, such as environmental pollution, fossil fuel exhaustion and climate change. In this context, energy has been recognized as a primary factor to resolve the aforementioned problems. [1] Therefore, the exploitation of various sustainable and renewable energy resources, such as solar and wind energy, have been continually progressed. [2] However, those energy resources are highly intermittent being dependent on time, climate, or region. Hence, there is urgent need for the development of efficient energy storage systems (ESSs) in order to make use of those energy resources globally and in full. Moreover, the extreme progress of portable electronic devices (cell phones, laptops, cameras, etc.) and electric- (EVs) or hybrid- electric vehicles (HEVs) have created an ever-increasing demand for ESSs. In this regard, one of the greatest challenges is to construct highly efficient, convenient, low-cost, and environmentally friendly ESS devices. Many effective and practical technologies for portable ESSs, such as rechargeable batteries, [3-5] fuel cells (FCs), [6-8] and supercapacitors (SCs), [9-11] have been developed in the past decade. The recent researches have shown that FCs and SCs can provide high energy density which can meet the requirement of EVs/HEVs. [12-14] However, on the one hand, the operation problems related to electro-catalysis in FCs and hydrogen storage will need more research & development effort. [14, 15] On the other hand, the absences of chemical reactions in SCs enable them to deliver energy quickly, with charging time in the order of minutes or even seconds. [16] Therefore, SCs are primarily used to provide peak power and store regenerative braking energy. [17, 18] Owing to the issues of FCs and SCs, rechargeable batteries have been recognized to be the most practically viable power source for both portable electronic and EV/HEV applications for the near future. [2, 19] In particular, in order to meet the requirement of ever-growing portable electronic market, battery technology need to be improved in term of high power, large capacity and light weight. [20] For this reason, many investigations have been dedicated to different battery types such as lead-acid (Pb-acid) batteries, [21] Nickel-Cadmium (Ni-Cd) batteries, [22] Nickel-metal-hydride batteries [23] and LIBs. [2] Among these, LIBs have been recognized as promising candidate for portable electronic and EV/ HEV applications because of its remarkable advantages: (i) the low reduction potential of Li (-3.04 V vs. standard hydrogen electrode) allows LIBs to have higher

working voltage than the Pb-acid, Ni-Cd, Ni-metal-hydride batteries; [24] (ii) the light weight of Li element ( $6.94 \text{ g mol}^{-1}$ ) [2] allows LIBs to have high energy and power densities (Figure 1.1a). [20, 25] As a result, LIBs became the most advanced mobile power sources [15] and currently dominates the market for portable electronic devices (Figure 1.1b). [25] However, despite LIBs are currently the first choice for portable energy storage, the improvement of their performances can greatly expand their applications and enable new technologies. [24] In this perspective, researchers worldwide continue to work on many different aspects of this technology such as enhancing the energy and power densities, improving the cycling life and stability, as well as reducing the cost. [26] For instance, the ever-growing markets of EVs and larger stationary storage systems require the significant improvement of current LIB technology, such as the increase in energy density, the reduction in cost and the enhancement of safety. [15, 24, 27]

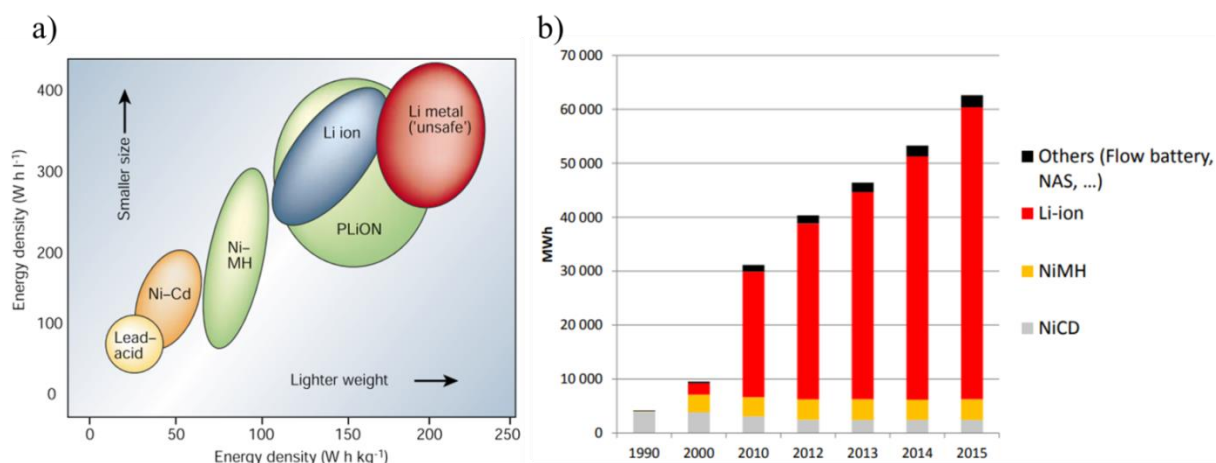


Figure 1.1. (a) Comparison of the different battery technologies in terms of volumetric and gravimetric energy density [2] and (b) Worldwide battery market. [28]

## 1.2. Fundamental of lithium ion batteries

### 1.2.1. History of lithium ion batteries

The first rechargeable LIB with metallic Li based anode and  $\text{TiS}_2$  based cathode was proposed by Whittingham (Exxon Mobil Corporation) in 1976. [29] However, Exxon unsuccessfully commercialized these LIBs due to the problems of Li dendrite formation and short circuit upon extensive cycling and safety concern. [30] In 1981, Goodenough firstly proposed to use layered  $\text{LiCoO}_2$  (LCO) as high energy ( $1.11 \text{ kWh kg}^{-1}$ ) and high voltage ( $\sim 4.0 \text{ V vs. Li/Li}^+$ ) cathode materials. [31] Nevertheless, the lack of safety in anode materials, *e.g.*, Li metal, limited the application of layered LCO cathode in LIBs. In late 1970s and early 1980s, graphite, having a layered structure was recognized as a good candidate to reversibly store Li

by intercalation/de-intercalation by Besenhard, [32] Yazami, [33] and Basu. [34] In 1987, Yohsino *et al.* had filed a patent and built a prototype cell using carbonaceous anode and LCO as cathode. [35] The high stability of carbon and LCO in air is highly beneficial from the engineering and manufacturing point of view. In 1991, Sony Corporation successfully commercialized LIBs for the first time. Since then, LIBs have been attracting increasing attention and Japan became the leader of global LIB market with 57% market share in 2010. [24] The global production of LIBs continuously increases in the past two decades, especially with the growing popularity of portable electronics devices. Besides, to satisfy the ever-increasing demand of energy market, the research activity in LIBs has also been progressively increased year after year. In fact, the number of scientific publications also keep increasing each year (see Figure 1.2), [36] achieving impressive progresses in term of electrode materials, safety and cell-design, etc.

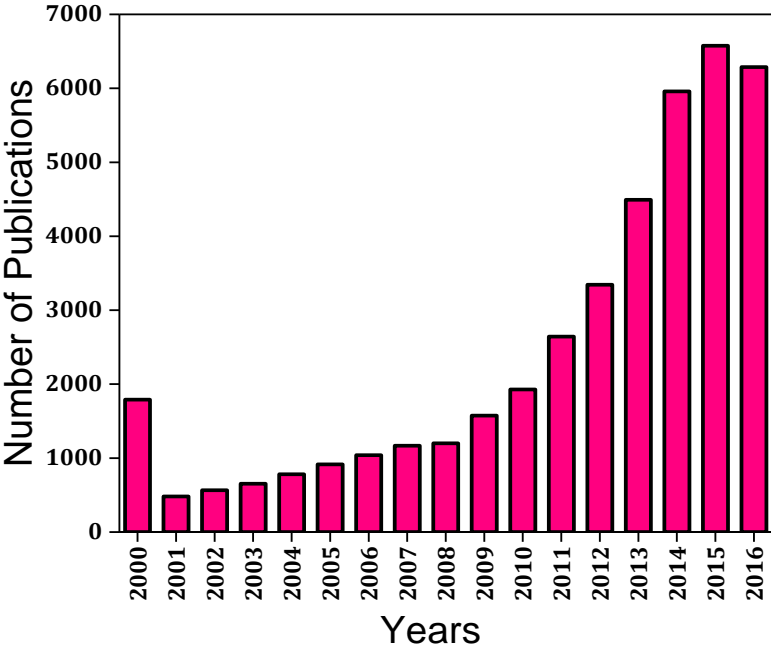


Figure 1.2. *The increase in number of publications related to lithium ion batteries since 2000 to 2016. [37]*

To date, there are four well-known different types of LIB geometries according to the current manufacturing market, namely the prismatic, cylindrical, coin, and the pouch cell configurations (Figure 1.3a). [2] Both the cylindrical and prismatic cells are commonly made of “laser-welded” aluminum can with cylindrical or rectangular shape, which contains a jelly-rolled cathode, anode and separator immersed in a liquid electrolyte. [38, 39] Typical applications for the cylindrical and prismatic cells are medium-scale electronic devices, such as power tools, laptops, electrical bikes, mobile phones, and tablets. [40] The pouch cell with aluminized plastic bag contains a flexible cathode, anode and polymer/gel electrolyte. The



pouch cell offers a flexible and light-weight solution to battery design with respect to cylindrical and prismatic cells, resulting in its wide range of applications in consumer, military, as well as automotive industries. [2] The coin cell exhibits a compact design, consisting of a round cathode, anode, separator, spacer and spring (O-ring) immersed in a liquid electrolyte (Figure 1.3b). [41] Thanks to the simplest design, coupling with the advantage of lightness and versatile assembling with respect to other LIB geometries, coin cells have been popularly used for small-scale electronic devices, *e.g.*, watches, hearing aids, car keys and memory backup, [40] as well as research samples in laboratories.

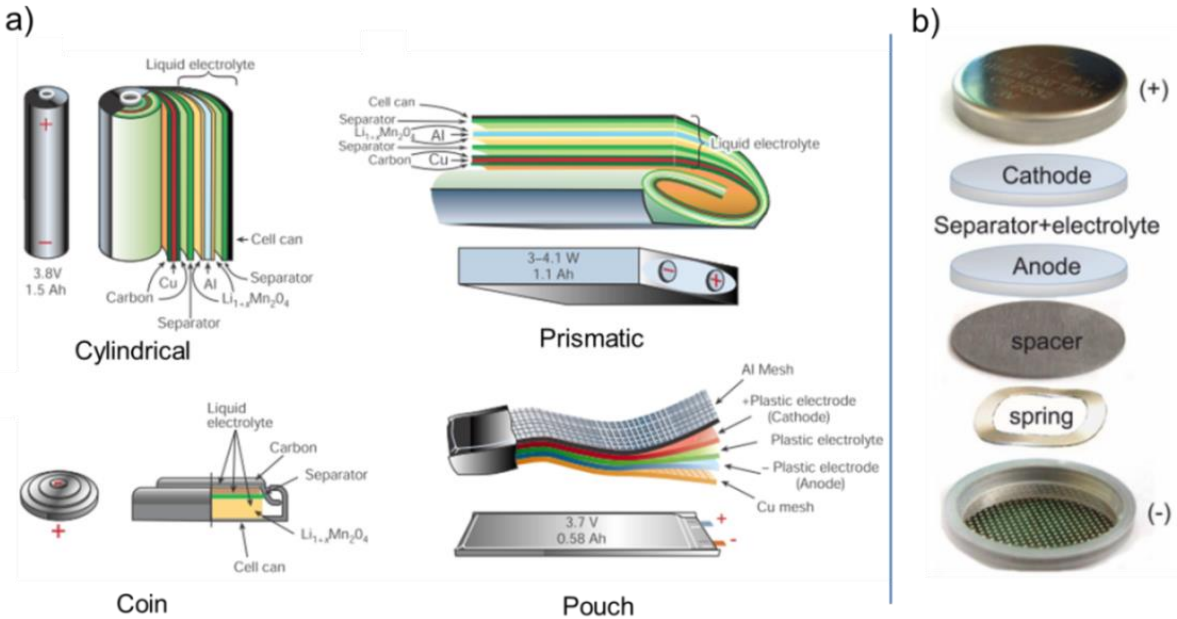


Figure 1.3. (a) Schematic drawing showing the shape and components of various Li-ion battery geometries, [2] and (b) Detailed configuration of coin cell. [41]

**1.2.2. Working principles of lithium ion batteries**

In general, LIB is a simple electrochemical system that is able to convert chemical energy into electrical energy during discharging process and then re-convert the electrical energy to chemical energy during charging process. [42] As shown in Figure 1.4, a conventional LIB consists of two major components: anode (negative electrode) and cathode (positive electrode), immersed in an electrolyte which acts as an environment for  $\text{Li}^+$  transfer between two electrodes. [25] The anode and cathode are separated by a porous permeable membrane, namely separator, which not only allows  $\text{Li}^+$  to pass through but also prevents a short circuit due to direct contact of electrodes. [36] Both anode and cathode are deposited onto copper (Cu) and aluminum (Al) current collectors, respectively which are connected by an external electrical circuit. The working mechanism of LIBs, taking LCO and graphite as typical cathode and anode materials, respectively, can be described as following. During charging

process,  $\text{Li}^+$  de-intercalates from cathode, travels through the electrolyte and intercalates to the anode. Meanwhile, the electrons travel through the external electrical circuit in order to couple with the intercalated  $\text{Li}^+$  in anode. The reverse mechanism occurs in the discharging process. The electrode reactions can be expressed by the following equations: [42]

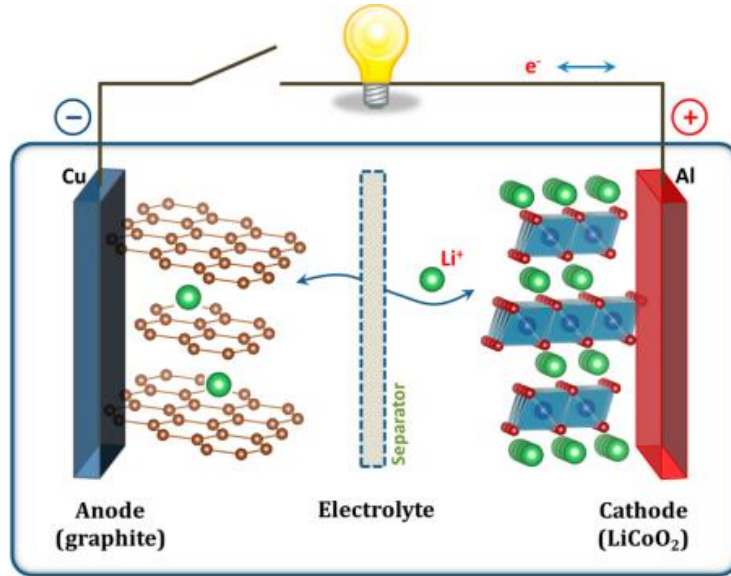
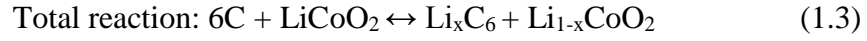
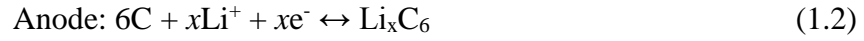
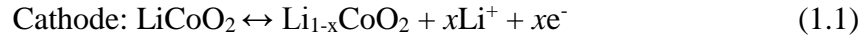


Figure 1.4. Schematic illustration of the first lithium-ion battery ( $\text{LiCoO}_2/\text{Li}^+$  electrolyte/graphite). [25]

The performance of LIBs can be evaluated by several parameters, such as open circuit voltage, operating voltage, theoretical specific capacity, specific capacity, coulombic efficiency, energy density, power density, and the charge/discharge rate. [43]

The *open circuit voltage* ( $V_{ocv}$ ) is the voltage between anode and cathode when there is no current load on the battery (equation 1.4). [43] The *operating voltage* ( $V_{ov}$ ) is determined by the potential difference between anode and cathode when there is a current load (equation 1.5). [43]

$$V_{ocv} = (\mu_A - \mu_C) \quad (1.4)$$

$$V_{ov} = \frac{I}{nF(\mu_A - \mu_C)} \quad (1.5)$$

in which  $\mu_A$  and  $\mu_C$  is the chemical potential of anode and cathode, respectively;  $n$  is the number of electrons involved in the chemical reaction of the cell and  $F$  is the Faraday constant (96485 C mol<sup>-1</sup>).

The *theoretical specific capacity* ( $Q_{th}$ ) of active electrode material is the maximum charges that can be stored per unit mass of active electrode material. The value of  $Q_{th}$  can be obtained by Faraday law, see equation 1.6. [43]

$$Q_{th} = \frac{nF}{3.6 \times M_w} \quad (1.6)$$

in which  $n$  is the number of electrons involved in the chemical reactions of the electrode and  $M_w$  (g mol<sup>-1</sup>) is the molecular mass of the active electrode material.

The *specific capacity* ( $Q$ ) (mAh g<sup>-1</sup>) of active electrode material measures the amount of charge that can be reversibly stored per unit mass of active electrode material at a certain current load during the charging/discharging process, see equation 1.7 [41]

$$Q = \frac{It}{m} \quad (1.7)$$

in which  $I$  (mA) is the current load during charging/discharging process,  $t$  (h) is the total charging/discharging time and  $m$  (g) is the weight of electrode active material.

In case of the full-battery, *e.g.*, graphite as anode and LCO as cathode, the specific capacity of the full battery ( $Q_{cell}$ ) is determined by both specific capacity of anode  $Q_A$  and cathode  $Q_C$ , see equation 1.8 [43]

$$Q_{cell} = \frac{Q_A \times Q_C}{Q_A + Q_C} \quad (1.8)$$

The *coulombic efficiency* ( $CE$ ), is the ratio between *discharge specific capacity* ( $Q_{discharge}$ ) and the *charge specific capacity* ( $Q_{charge}$ ) for each cycle: [36]

$$CE = \frac{Q_{discharge}}{Q_{charge}} \times 100\% \quad (1.9)$$

The *energy density* ( $E$ ) (Wh g<sup>-1</sup>) [43] defines the amount of energy that can be stored and released per unit mass of the electrode. It can be obtained by multiplying the  $Q$  with  $V_{ov}$ , see equation 1.10. The *energy density* is an important parameter for practical application as it determines the ultimate useful work from a battery. [24]

$$E = V_{ov} \times Q \quad (1.10)$$

The *power density* ( $P$ ) ( $\text{W g}^{-1}$ ) is the output energy per unit mass of the electrode, see equation 1.11. The  $P$  is a characteristic of the battery chemistry and packaging. It determines the battery size required to achieve a given performance target.

$$P = \frac{I \times V_{ov}}{m} \quad (1.11)$$

The *charge/discharge rate* ( $C$ -rate) is the current (mA) used to charge/discharge the battery relative to its maximum capacity. A charge at  $x\text{C}$  rate means a full charge in a time of  $1/x$  hours. For instance, a  $2\text{C}$  rate means that the current will charge/discharge the entire battery in  $1/2$  h. [43]

### 1.2.3. Anodes of lithium ion batteries

Various anode materials have been extensively investigated for the development of LIBs. Depending on their electrochemical reaction mechanisms, the anode materials are categorized into three groups: intercalation-, alloy- and conversion reaction-based anode materials. [44]

#### 1.2.3.1. Intercalation-based anode materials

The electrochemical reaction occurring at this type of anode is based on the intercalation of  $\text{Li}^+$  into the structure of active materials, *e.g.*, layered, cylindrical and spinel structures. [45-47] These materials enable fast  $\text{Li}^+$  diffusion by providing the effective ionic transport channels during lithiation/de-lithiation, which are either one dimensional (1D) path or two dimensional (2D) planes. [36] However, they offer low specific capacities because the intercalation of  $\text{Li}^+$  is mostly limited by the intrinsic redox reactions of materials, *e.g.*, number of exchanged electrons. [48, 49] Presently, graphite is the primary choice and has been commercialized as the most successful intercalation-based anode material. [2] Graphite has a layered structure of carbon hexagon network in an orderly arrangement, as shown in Figure 1.5. In fact, when the layers are stacked, the different graphitic structures occur. The ABAB stacking results in the more common hexagonal graphite, whereas a stacking order of ABCABC gives the rhombohedral graphite. [50] The structure of graphite allows  $\text{Li}^+$  transport between its inter-spacing layers without the considerable volume change (the expansion and contraction in volume of material during lithiation which cause structural degradation), resulting in high coulombic efficiency, reaching 99.9 %. [51] Moreover, graphite has advantages of low-cost, high electrical conductivity ( $\sim 3 \times 10^5 \text{ S m}^{-1}$ ), [52] high  $\text{Li}^+$  diffusivity ( $10^{-11} - 10^{-7} \text{ cm}^2 \text{ s}^{-1}$ ), [20] compared to other intercalation-based anode materials, *e.g.*,  $\text{TiO}_2$ ,  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  and  $\text{Li}_{1.03}\text{V}_{0.97}\text{O}_2$ . [20, 53] However, the most Li-enriched intercalation of graphite has a stoichiometry of  $\text{LiC}_6$ , meaning one  $\text{Li}^+$  per 6 carbon atoms,

resulting in a theoretical specific capacity of  $372 \text{ mAh g}^{-1}$  (see equation 1.2). [2] This is a major drawback associated with commercial graphite-based LIBs, especially for applications, such as EVs and HEVs, which require high energy and power density, see equation 1.10. Hence, the use of graphite as anode is still limited to low-power devices like smart watches, mobile phones and laptops. [20]

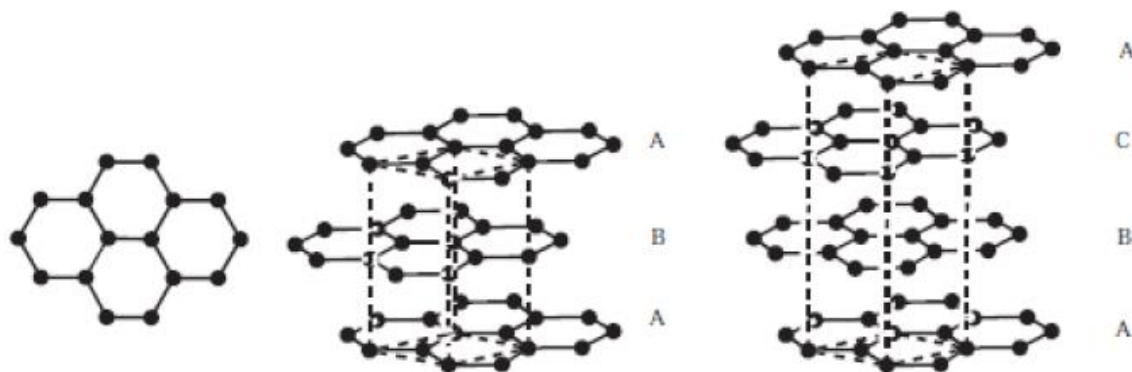


Figure 1.5. *The structure of a carbon layer, hexagonal and rhombohedral graphite.* [50]

### 1.2.3.2. Alloy-based anode materials

This type of materials is associated with elements which are able to electrochemically alloy and form compound phases with lithium. [44] Alloy forming compounds have higher theoretical specific capacity compared to that of commercial graphite ( $372 \text{ mAh g}^{-1}$ ), *e.g.*, Si, Ge, Sn, etc. with capacity values of 4200, 1600, 999  $\text{mAh g}^{-1}$ , respectively through an alloying product of  $\text{Li}_{4.4}\text{N}$  ( $\text{N} = \text{Si, Ge and Sn}$ ). [54, 55] The role of N is to provide the matrix of the alloy electrode to support the strain generated during the lithiation and de-lithiation process, as well as to improve the electrical conductivity. [56] Beside their high theoretical specific capacities, the alloy-based materials gained tremendous attention thanks to their abundance and low-cost. [57] Thus, it is believed that these materials will result in high enhancement in the overall energy density of LIBs, making them eligible for EVs and HEVs. However, the alloy-based anode materials suffer from slow lithium reaction kinetics and poor intrinsic conductivities which cause low rate capability of the LIBs. [36] Moreover, the critical challenge of this kind of anode materials relies on their large volume changes due to the reaction with  $\text{Li}^+$ . For example, the alloy of lithium with Si results in 440% increase in number of atoms in the alloyed Li-Si particle with respect to the initial Si particle, inducing a large volume change of  $\sim 300\%$ , see Figure 1.6. [58] This dramatically introduces a mechanical stress in the material during cycling of LIBs, leading to the pulverization of the electrode. [59] Consequently, this cause the electrical contact loss between Si particles and the current collector, [20, 60] resulting in severe capacity fading of the electrodes. [59, 61] Various strategies, such as carbon coating on the surface active materials and the size

reduction of the active materials, have been adopted to alleviate volume change without significantly compromise the specific capacity. [62, 63] Very recently, Sn and Si have been allowed to be used as anode in commercial LIBs with improved capacity up to 30%, along with better rate performance, compared to that of traditional graphitic anode.

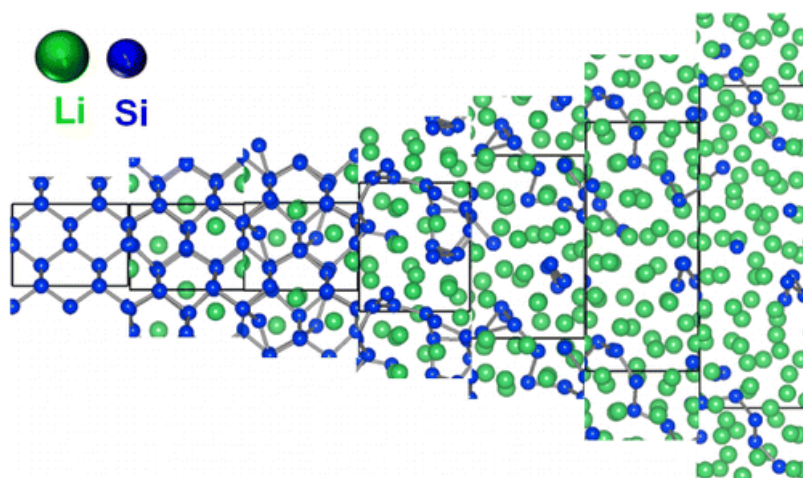


Figure 1.6. *The volume change of silicon during lithiation.* [58]

### 1.2.3.3. Conversion reaction-based anode materials

This type of material is mainly transition metal compounds ( $M_aX_b$ ,  $M$  = transition metal,  $X$  = O, S, F, P, N etc.), [64] which store the  $Li^+$  through a conversion reaction. In this reaction,  $Li^+$  reacts with metal ions to form  $Li_nX$  and reduces metal ions to their zero oxidation state, as shown in Figure 1.7. [65] During the conversion reaction, the structure and composition of electrode materials have completely changed. Therefore, an ideal conversion-based electrode material is expected to have the ability to regenerate their initial structure and composition during charging/discharging processes. [65] Anodes based on these compounds exhibit high reversible capacities ( $500 - 1000 \text{ mAh g}^{-1}$ ) owing to the participation of a high number of electrons in the conversion reactions. [66] One of the most typical conversion-based anode materials is TMOs, *e.g.*,  $CoO$ ,  $FeO$ ,  $NiO$  and  $Cu_2O$ , which were firstly introduced in LIBs by Poizot *et al.* [67] and then intensively studied, thanks to their high specific capacities and capacity retentions.

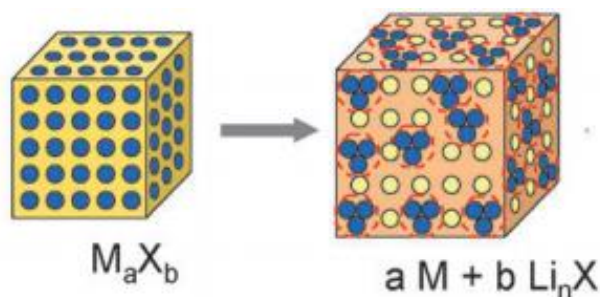
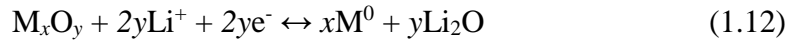


Figure 1.7. *Conversion reaction-based anode material.* [68]

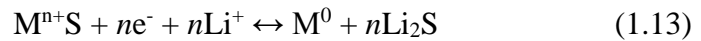
During lithiation process, the TMOs react with  $\text{Li}^+$  and yield metal nanoparticles in the matrix of  $\text{Li}_2\text{O}$  via a conversion reaction, as shown in equation 1.12. During de-lithiation process a reverse reaction occurs. [69]



in which M is Co, Ni, Fe, Cu, Mn, etc.

However, there are also drawbacks that limited the application of such materials in LIBs. Firstly, the hysteresis in voltage (a difference between lithiation and de-lithiation voltage) increases with ongoing conversion reactions, leading to a decrease in operating voltage of LIBs and consequently to a poor energy efficiency. Secondly, the  $\text{Li}^+$  stored per formula unit of TMOs through a conversion reaction, causing a volume change of active materials. Most conversion-based TMOs have much higher theoretical capacities than graphite ( $372 \text{ mAh g}^{-1}$ ), such as iron oxides ( $1007 \text{ mAh g}^{-1}$ ), [64] manganese dioxide ( $1223 \text{ mAh g}^{-1}$ ) [64] and cobalt oxide ( $890 \text{ mAh g}^{-1}$ ). [64] Despite the high theoretical specific capacity, conversion reaction-based TMOs should be further optimized to overcome other unsatisfactory electrochemical properties including volume change and voltage hysteresis. [67, 70]

TMSs, another important class of conversion reaction-based anode materials, follow similar mechanism for  $\text{Li}^+$  storage as that of TMOs. In general, the chemical reaction of metal sulfides with  $\text{Li}^+$  can be represented by equation 1.13. [71]



in which, M is Mo, W, Zr, V, Sn, Mn, etc.

During lithiation process, TMSs react with  $\text{Li}^+$  and yield metal nanoparticles in the matrix of  $\text{Li}_2\text{S}$  via a conversion reaction, whereas the reverse reaction occurs during de-lithiation process.

TMSs are considered as promising candidate for anode of LIBs thanks to their good thermal stability and conductivity along with high theoretical specific capacities, *e.g.*,  $\text{MoS}_2$  ( $670 \text{ mAh g}^{-1}$ ). [72] However, capacity fading is one of the critical issues for TMSs and it arises from two reasons. One is related to the voltage hysteresis that causes poor energy efficiency of LIBs. [65] The other is related to the  $\text{Li}^+$  transport in electrolyte hindered by the polysulfide anions, *e.g.*,  $\text{Li}_2\text{S}_x$  ( $6 < x \leq 8$ ), which are produced from the conversion reaction (equation 1.13). These polysulfide anions tend to breakdown to smaller  $\text{Li}_2\text{S}_x$  ( $2 < x \leq 6$ ) with continuous charging/discharging processes, [65] and then develop a barrier for  $\text{Li}^+$  diffusion and charge transport by depositing an insulating sulfur layer on electrode surface. [73, 74]

The blockage of  $\text{Li}^+$  diffusion can not only causes capacity fading, but also creates an increase in the internal temperature of battery and results in the thermal explosion. [75]

#### 1.2.4. Cathodes of lithium ion batteries

Plenty of promising materials have been explored as cathode materials for LIBs. The cathode materials can be categorized based on their operating voltage versus lithium (from 2.5 to 5V). Typically, 3-Volt cathode materials are  $\text{MnO}_2$  and  $\text{V}_2\text{O}_5$ ; [24] 4-Volt cathode materials are LCO,  $\text{LiNiO}_2$  with layered structure, three dimensional (3D) spinel  $\text{LiMn}_2\text{O}_4$ , and olivine  $\text{LiFePO}_4$  (LFP), tavorite  $\text{LiVPO}_4\text{F}$ ; [24] 5-Volt cathode materials are olivine  $\text{LiMnPO}_4$ ,  $\text{LiCoO}_4$  and 3D spinel  $\text{Li}_2\text{Fe}_x\text{Mn}_4\text{O}_8$  structure. [24] Generally, high operating voltage cathode is desirable because the operating voltage of cathode is proportional to the cell operating voltage, which could help to increase the energy density.

In order to optimize the performance of cathode, we also need to consider the structure of materials which is one the most important factors for the cyclability of the cathode. For examples, the 3D spinel structures exhibit high operating voltage (4-5 V), but they are still facing the issue of fast capacity fading due to the phase transition during cycling, which is related to mechanical stress in material. [76-78] Currently, layered LCO and olivine LFP are most widely used in commercial LIBs because of their good cycle life (> 500 cycles). [24]

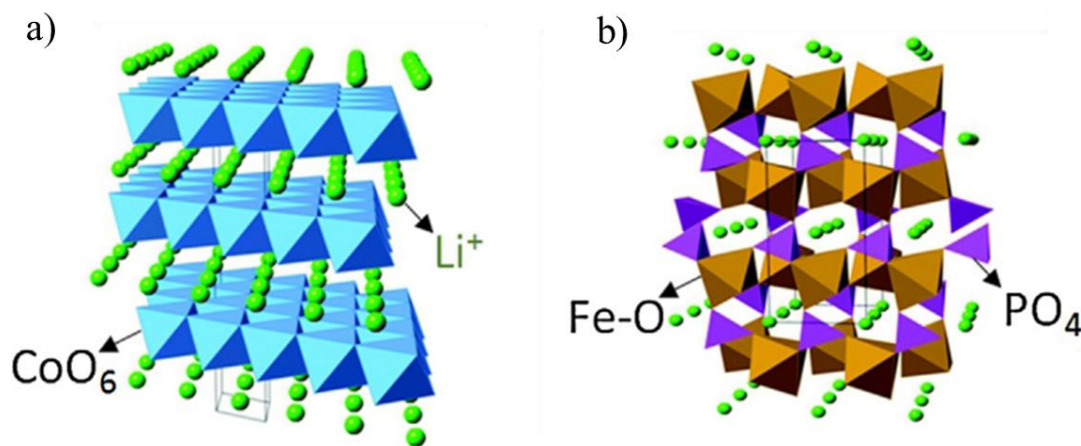


Figure 1.8. Crystal structure of typical cathode materials: (a) layered  $\text{LiCoO}_2$ , (b) olivine  $\text{LiFePO}_4$ . [20]

LCO exhibits the layered structure with Co and Li located in octahedral sites, as shown in Figure 1.8a, occupying alternating layers and forming a hexagonal symmetry. LCO is attractive for industrial production because it has high theoretical specific capacity ( $274 \text{ mAh g}^{-1}$ ) and can be easily manufactured in large scale, being also stable in air. [79] However, the major limitation of LCO relies on its high cost and toxicity of Co. Also, low thermal stability



is a major concern of this material. LCO typically experience thermal runaway past  $\sim 200\text{ }^{\circ}\text{C}$  due to an exothermic reaction between the released oxygen and organic materials in electrolyte. [24] Moreover, LCO can suffer from the lattice distortion from hexagonal to monoclinic symmetry at the de-lithiation voltage  $\sim 4.2\text{V}$  (approximately  $> 50\%$  if  $\text{Li}^+$  extract from LCO lattice), inducing capacity fading. [80] For these reasons, various types of metals, *e.g.*, Ni, Mn, Al, Fe and Cr, were studied with the aim to substitute Co. [81-83] Among the aforementioned materials, spinel  $\text{LiNi}_{0.5}\text{Mn}_{1.5}\text{O}_4$  (LNMO) was found to be attractive material because it can exhibit the similar electrochemical performance as LCO, while reducing cost and toxicity. Also, the presence of Ni allows higher de-lithiation capacity to be achieved with respect to original LCO due to the continuous reaction of  $\text{Ni}^{2+/3+/4+}$  with lithium, resulting in high operating voltage (4.6 to 4.8V vs.  $\text{Li}/\text{Li}^+$ ). This makes LNMO as a potential candidate of cathode for LIBs to power EVs and HEVs. Moreover, the presence of  $\text{Mn}^{3+}$  exhibit better rate performance in LNMO with respect to the  $\text{Co}^{3+}$  in LCO due to a higher electronic and ionic conductivity. However,  $\text{Mn}^{3+}$  is unstable and may be turned into:  $\text{Mn}^{2+}$  and  $\text{Mn}^{4+}$ . The produced  $\text{Mn}^{2+}$  then dissolves into the electrolyte, leading to a capacity fading during charging/discharging process [84, 85]. In the LNMO products,  $\text{Li}_x\text{Ni}_{1-x}\text{O}$  usually appears as impurity phase, lowering the capacity and hindering  $\text{Li}^+$  transport in the material. Therefore, it is crucial to investigate the reaction mechanism of  $\text{Mn}^{3+}$  and control their content of impurity in the spinel product. [86, 87]

Another type of commercial cathode, olivine structure LFP, is attracting much attention in the past decade due to its low-cost and low-toxicity. In LFP, Li and Fe atoms are located in octahedral sites, whereas P occupies tetrahedral sites in a hexagonal close-packed oxygen array, see Figure 1.8b. Compared to LCO, LFP also offers a number of advantages, such as stability, excellent cycle life, and temperature tolerance ( $-20$  to  $70^{\circ}\text{C}$ ). However, LFP has issues of poor electronic and ionic conductivity of  $10^{-10}\text{ S cm}^{-1}$  and  $10^{-8}\text{ cm}^2\text{ sec}^{-1}$ , respectively, as well as relatively low theoretical capacity ( $170\text{ mAh g}^{-1}$ ). [88] The other issue is that  $\text{Li}^+$  diffusion can easily be blocked by defects and impurities in the material. [89] In order to overcome this issue, synthesizing nano-sized LFP has been considered as a promising strategy by reducing  $\text{Li}^+$  diffusion paths during lithiation and de-lithiation in LIBs. [90]

### 1.2.5. Electrolyte, separator and current collectors

The *electrolytes* in LIBs act as an ionic media for  $\text{Li}^+$  transport back and forth between anode and cathode as the battery are charged and discharged. [42] Currently, the *liquid electrolyte*, solution containing lithium salts and organic solvents, is common used in commercial LIBs. [24] These organic solvents in liquid electrolytes are required to have high ionic mobility in a

wide temperature range and good chemical/thermal stability. [91] In order to meet these requirements, the content of solvents are typically formulated and mixed to effectively dissolve the lithium salts selected for practical application in LIBs. Over the past two decades, alkyl carbonates have been found to be the most suitable solvents for LIBs, thanks to their electrochemical stability, non-toxicity and low-cost. [15] However, the electrolytes are not only determined by the solvents, but also highly dependent on the properties of lithium salts. [24] Therefore, various lithium salts have been explored, including lithium hexafluorophosphate ( $\text{LiPF}_6$ ), lithium tetrafluoroborate ( $\text{LiBF}_4$ ), lithium hexafluoroarsenate(V) ( $\text{LiAsF}_6$ ) and lithium perchlorate ( $\text{LiClO}_4$ ). [24] Among these,  $\text{LiPF}_6$  is the most suitable lithium salt to make electrolyte (using alkyl carbonates as solvent), from the perspective of safety, high ionic conductivity and high solubility in organic solvents. [24] So far, the widely used commercial liquid electrolyte, as shown in Figure 1.9, is 1M  $\text{LiPF}_6$  in a 50:50 w/w mixture of ethylene carbonate (EC) and dimethyl carbonate (DMC). [91, 92] The mixture of EC/DMC allows high solubility of  $\text{LiPF}_6$  to form an electrolyte with high ionic conductivity with respect to the electrolytes formed by other alkyl carbonates. [93] Besides the liquid electrolyte, other types of electrolytes have also been developed and proposed for LIBs, such as *polymer, gel and ceramic electrolyte*. [42] *Polymer electrolyte* is solvent-free because it is formed by the mixing of high molecular-weight polymers (HMWPs) with lithium salts. [94] The advantage of polymer electrolyte with respect to liquid electrolyte is the low volatility, flexible design thanks to the high flexibility of HMWPs. [95] Moreover, the polymer electrolyte can also function as a potential to eliminate separators in LIB configuration, due to high ion permeability and electrochemical inert of HMWPs. [96] *Gel electrolyte* is formed by absorbing a solution of lithium salt and polar solvents into a network of HMWP. [97] Because the solvent containing lithium salt is fully absorbed within the polymers, the solvent leakage issue, which happened in LIB using liquid electrolyte and causes safety problems, can be avoided. *Ceramic electrolytes* have long been explored for fuel cells, and recently attracting increasing interest for the application in LIBs. [98, 99] The most obvious property of ceramic electrolyte is the robust mechanical strength of ceramic materials which make them more suitable for rigid battery designs as in, for example, thin-film-based devices. [98] The ionic conduction in ceramic compounds occurs by movement of ionic point defects, which requires energy, so the conductivity of ceramic electrolyte increases with increasing temperature. Therefore, the batteries with ceramic electrolyte can find applications in high temperature environment, including handheld orthopedic tools and powered medical devices that need to be sterilized in autoclaves under high temperature conditions.

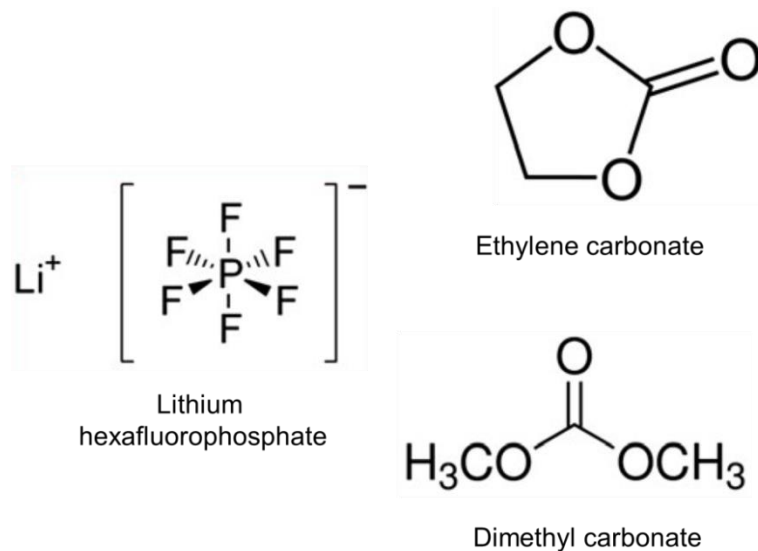


Figure 1.9. Chemical structures of common components in commercial electrolyte: lithium hexafluorophosphate as the lithium salt and the solvent composed of ethylene carbonate and dimethyl carbonate [24]

The *separator* is a porous membrane placed between electrodes, which is permeable to ionic flow, but prevents electric contact between the two sides of electrodes. [100] The separator must be chemically and electrochemically stable towards the electrolyte and electrode materials. In term of structure, the separator should have sufficient porosity with pore size  $< 1 \mu\text{m}$  to absorb sufficient liquid electrolyte for the high ionic conductivity. [24] However, the presence of separator increases the electrical resistance and takes space inside the battery, negatively affecting the battery performance. [101] Up to date, battery separators can be categorized into three types: *microporous polymer membranes*, *non-woven fabric mats* and *inorganic composite membranes*. [102] Among them, the microporous polymer membranes have been most widely used in batteries with liquid electrolyte due to their low-cost, light weight and facile manufacturing. Nevertheless, the main issues of these separators are poor mechanical strength and low melting point ( $\sim 100 \text{ }^\circ\text{C}$ ). [103, 104] Thus, for the development of future LIBs for high temperature applications inorganic composite membranes, *e.g.*,  $\text{Al}_2\text{O}_3$ , as separators are highly attractive, thanks to their excellent thermal stability and mechanical property. [105]

The *current collector* works as an electrical conductor between the electrode and external circuits and a support for the deposition of the electrode materials. [106] To completely form the electrode, the electrode materials are coated onto current collectors. The main requirements for current collector material are light weight, electrochemical stable at battery operation voltage and high electrical conductivity. For most commercial LIBs, Cu is the choice for anode because it is electrochemically stable in the range below 3 V vs.  $\text{Li/Li}^+$ ,

while aluminum is extensively used for cathode due to its electrochemical stability for higher voltages between 3-5 V vs. Li/Li<sup>+</sup>. [107] However, with extensive cycling, the adhesion of active materials to the current collector is reduced due to the structural degradation of active materials upon lithiation/de-lithiation. [108, 109] Especially for the alloying- and conversion-based anode materials, the contact between active material and current collector is easily lost upon cycling due to volume change. Recent research has focused on the use of a 3D micro-porous current collector to improve the mechanical stability of the electrodes.[110] Such current collectors offer a high porosity, which can accommodate the volume change of the active materials. [111]

### **1.3. Current challenges and opportunities of anodes in lithium ion batteries**

Although LIBs have been commercialized for about two decades and are dominating the portable electronic device market, the increasing demand for energy storage requires further improvements in the existing LIBs. Next generation LIBs with lower-cost, higher power and energy density is highly expected to power HEVs and EVs, without compromising vehicle performances, such as driving distances, speed, and safety. The main challenge of current LIBs is their low energy density which highly depends on specific capacity and operating voltage of electrode materials. Hence, the choice of electrode material is one of the crucial factors determining the performance of LIBs. Present commercial LIBs utilize graphite anode and LCO cathode, which only have power density of  $\sim 387 \text{ W kg}^{-1}$  and energy densities of  $\sim 120\text{--}150 \text{ Wh kg}^{-1}$  due to the following reasons: (i) the theoretical capacity of graphite anode (is low  $372 \text{ mAh g}^{-1}$ ), (ii) the practical capacity of LCO cathode ( $\sim 140 \text{ mAh g}^{-1}$ ) only reached 50% of its theoretical value ( $274 \text{ mAh g}^{-1}$ ) and (iii) the operating voltage of LCO is limited at 4.2 V vs Li/Li<sup>+</sup>. [112, 113] In order to increase energy and power density of LIBs, it is desirable to find anodes with high specific capacities (Figure 1.10), *e.g.*, TMOs ( $600\text{--}1200 \text{ mAh g}^{-1}$ ), TMSs ( $1000\text{--}1200 \text{ mAh g}^{-1}$ ) [44] and cathodes with high operating voltage, *e.g.*, LNMO, LiMnPO<sub>4</sub> ( $> 4.5 \text{ V}$ ). [24] There are a large numbers of anode candidates that could increase the specific capacities with respect to graphite, as shown in Figure 1.10. It should be noticed that the groups of conversion materials and alloying materials are highly attractive due to their large specific capacities, see section 1.2.3.3. Although the alloying materials can provide extremely large capacities, *e.g.*, Si ( $3579 \text{ mAh g}^{-1}$ ), their alloying process involves large volume expansion which results in substantial capacity loss upon cycling. The conversion materials, such as TMOs, TMSs are still under development due to volume changes ( $\sim 100\%$ ) and large voltage hysteresis, resulting in capacity fading and low energy density. Hence, tremendous efforts on the production and design of anode materials have been carried out to enable the application of anode materials.

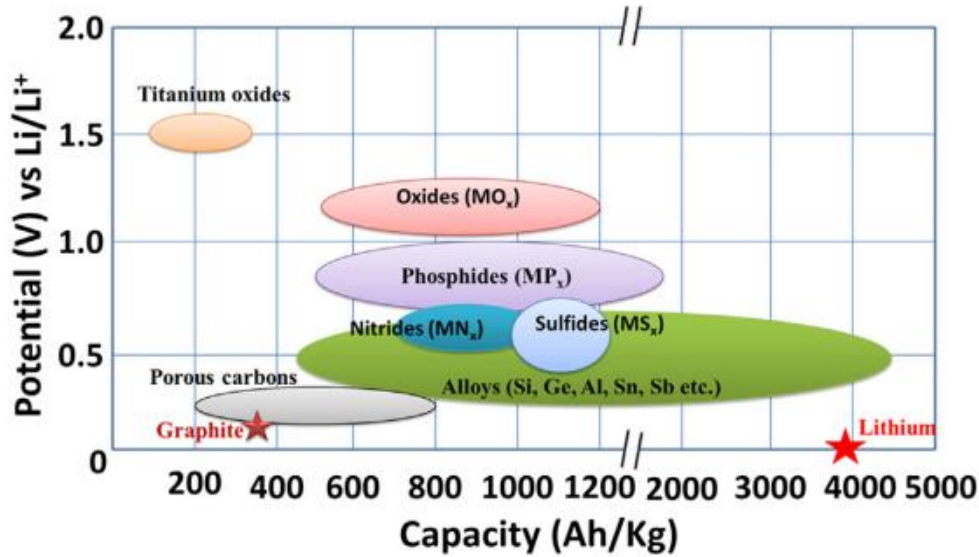


Figure 1.10. Schematic illustration of active anode materials for the next generation of LIBs. Potential vs.  $\text{Li/Li}^+$  and the corresponding specific capacity are shown. [44]

To date, there are two promising strategies for the development of anode materials: (i) *nanostructured anode materials* and (ii) *composite anode materials*. [44]

On one hand, nanostructured anode material, respect to the bulk one, can dramatically reduce the length of the paths for  $\text{Li}^+$  and electron transport, mitigating the volume change during charging/discharging process. [114] The alloying anode materials, *e.g.*, Sn, Si, and Ge, have shown evidence for the existence of a critical size below  $\sim 150$  nm which the fracture of a particle may not occur. [115] Using nanomaterials for LIB electrode, it can decrease the  $\text{Li}^+$  diffusion length and the  $\text{Li}^+$  diffusion time constant (see equation 1.14), consequently resulting in the improvement of rate capability. [116, 117] Furthermore, small particle size allows efficient mixing of the active material with other components such as the conductive carbon additive. However, the high specific surface area of nanomaterials leads to a large irreversible capacity in the first cycle due to the formation of *solid electrolyte interface (SEI)*, formed by the decomposition of the electrolyte. [24]

$$\tau = \frac{L^2}{D} \quad (1.14)$$

in which  $\tau$  the diffusion time constant,  $L$  is diffusion length and  $D$  is the diffusion coefficient.

Additionally, the shape of the nanomaterials plays a very important role in the electron and ion transport within electrode. Therefore, recent developments in nanostructured anode materials for LIBs have been based on zero dimensional (0D) (nanoparticles), 1D (nanowires, nanotubes), 2D (nanosheets, nanoplates) materials, as well as 3D porous framework, see

Figure 1.11. [118] Although 0D nanoparticles, *e.g.*, nanoparticles of Si and Sn, have been expected as the promising active materials in LIBs, their performances are limited by various factors. Firstly, 0D materials create the random pathways that can restrict the electron and  $\text{Li}^+$  transport. [36] Secondly, the grain boundaries and voids in between the nanoparticles hinder electron transport, limiting the LIB performance. [119, 120] Thirdly, the extremely high surface area of the 0D nanoparticles and access of the electrolytes trigger side reactions of electrolyte decomposition, forming SEI film. [120] The formation of SEI film consumes excessive charge supplied by the cathode, exhibiting low coulombic efficiency and capacity loss. [44, 119] In the case of 1D material, it is considered to be superior to 0D nanoparticles because its directional channels facilitate efficient electronic and ionic transport. [121] Moreover, 1D structure also provides mechanical stability during lithiation/de-lithiation. [61] For the 3D structured materials, *e.g.*, 3D graphene aerogels with porous frameworks, it can provide excellent properties of large specific surface area, rapid  $\text{Li}^+$  diffusion, excellent mechanical strength as well as multidimensional continuous electron-transport. However, the complexity in designing such nano-architecture is still a challenge that requires great efforts to reach practical LIB anode applications. [122, 123]

On the other hand, the synthesis of composite materials, combining active materials with inactive materials which can compensate for the limited properties of active material, *e.g.*, buffering the volume change and enhancing the conductivity of electrode. For instance, the composite of alloying materials and carbon-based materials (CNTs, graphene, etc.) can increase the ionic and electronic transport of the electrode. [124] Furthermore, carbon can form network to buffer the volume change of active material during charging/discharging processes. [125-127] Besides, developing a layer of inactive materials between electrolyte and active materials can prevent the direct contact between electrolyte and active material, hindering the side reactions between electrolyte and active materials, and then limiting the irreversible capacity. [128, 129] However, thickness of the inactive layer highly influences the electrochemical performance. In fact, if this layer is too thin, it might be collapsed with volume changes and bring electrode surface in contact with electrolyte. In contrast, if the inactive layer is too thick, the diffusion of  $\text{Li}^+$  will be hindered, resulting in a low performance of composite with respect to that of pristine active material. Thus, the thickness of inactive materials in the composites should be properly controlled to provide the ultimate performance of anodes. [130]

Furthermore, nanomaterials enable the facile synthesis of composite materials [131-133] Therefore, the nanostructured composite anode materials have been developed by the growth of various nanostructures of active materials along with inactive materials to build

hybrid/composite structures. This is a good strategy of exploiting the novel properties of inactive materials, *e.g.*, high conductivity, robust mechanical strength to support the limited properties of active materials, *e.g.*, low conductivity, volume change (see Figure 1.11). [134, 135] For instance, multiple nanostructures, *e.g.*, core-shell ( $\text{SnO}_2/\text{carbon}$ ) and hollow sphere ( $\text{SnO}_2$ ,  $\text{Fe}_2\text{O}_3$ ) structures have been designed/produced with the aim to improve the conductivity, protect the surface and limit volume changes of active materials. [134]

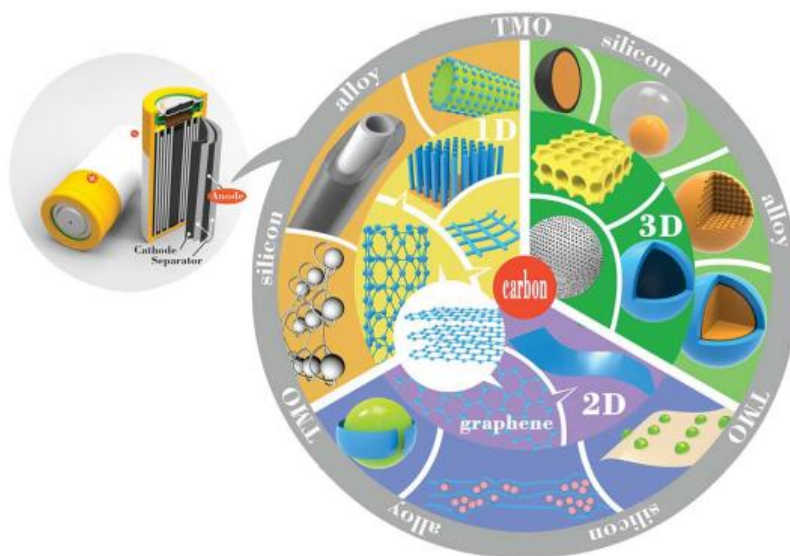


Figure 1.11. Schematic diagram of the recent anode materials for lithium ion batteries. [118]

#### 1.4. Graphene and other two dimensional materials: the promising anode materials for lithium ion batteries

Since the success in the exfoliation of graphite in 2004, [136] new classes of 2D materials, such as TMOs, [137] TMSs, [138] transition metal carbides/nitrides (Mxenes) [139], BP and elemental analogues of graphene (silicene, phosphorene, and borophene), [140] (Figure 1.12), have been successfully exfoliated or synthesized for many applications. In recent years, significant advances have been made in 2D materials, having the potential to bring unprecedented functionality to next-generation LIBs. [141] In general, 2D materials are defined as the free-standing atomic crystals that are strictly 2D and can be viewed as individual atomic planes exfoliated from bulk layered crystals or as unrolled single-wall nanotubes. [142] This structure provides the efficient ion transport channels between the layers, facilitating the diffusion of  $\text{Li}^+$ . Moreover, the large surface areas provide a large number of active site for  $\text{Li}^+$  storage. [143-146] It has been clearly shown in section 1.3 (see Figure 1.10) that graphene, layered TMOs and TMSs are the most promising materials which can replace graphite to become the future anode materials for LIBs. Additionally, BP has recently stimulated research interests to develop the extremely high specific capacity anode

due to its high theoretical capacity of 2596 mAh g<sup>-1</sup> [147-149] with respect to that of graphene, layered TMOs and TMSs.

Up to date, there are plenty of production techniques, including bottom-up and top-down approaches, [150] to produce graphene, 2D TMOs, TMSs and BP for LIBs applications. [150] However, most of the productions methods are still facing with the issues of high-cost, [151, 152] toxicity, [153, 154] time-consuming synthesis and low-yield of mass production [155, 156] which are the current challenges towards practical industrial application. For example, the chemical vapor deposition (CVD) method can be used to grow graphene, [157] TMOs [151] and TMSs. [158] However, this method is still facing with the issue of high-cost and low-yield in term of mass production, hindering the large-scale application for commercial LIBs. Hence, the low-cost processes via chemical solution methods have been proposed to overcome the issues of CVD. Large efforts have been devoted to the exploitation of chemically modified graphene (CMGs) such as graphene oxide (GO) and reduced GO (RGO). [159, 160] However, the chemical solution process is time-consuming and the CMGs suffer from limited conductivity and slow diffusion of Li<sup>+</sup> due to the defects on the basal planes. [5, 161] Concerning the growth of TMOs and TMSs, *e.g.*, MoO<sub>3</sub> and MoS<sub>2</sub>, the most frequently used approach for their producing is hydrothermal, [162, 163], solvothermal [164, 165] and template assisted techniques. [166, 167] However, these approaches involves toxic precursors, *e.g.*, (NH<sub>4</sub>)<sub>2</sub>MoS<sub>4</sub> or Na<sub>2</sub>MoO<sub>4</sub>, [168-171] and time-consuming synthesis, [172, 173] resulting in unresolved issues, *e.g.*, safety and scalability. [174-176] Furthermore, the TMSs and TMOs produced by these methods usually have an amorphous structure and contains defects, [177] which requires annealing at high temperature (700-800 °C) to obtain the layered structure of TMOs and TMSs, severely impacting on the production cost. [168, 178-182] Apart from the production of graphene, TMOs and TMSs, the production of 2D BP flakes can be performed using micromechanical cleavage (MC), [183, 184] which consists of consecutively peeling off crystal layers by using adhesive tape. [142] However, this technique is only suitable for research activities due to both the scalability limitation and morphological heterogeneity of the exfoliated flakes. [142] The other exfoliation technique, *e.g.*, ball-milling (BM), [185, 186] has been applied to synthesis BP flakes because it can meet the requirement of scalable production. However, ball milling usually introduces impurities in the obtained products. [145, 187]

In this context, LPE has been recognized as a potential method to produce graphene, TMO and TMS flakes thanks to its low-cost, simplicity and scalability, which can reach the industrial-scale production. [188-190] Therefore, the scope of this thesis is to provide the



insight-into study on production of graphene, MoO<sub>3</sub> and MoS<sub>2</sub> via LPE, as the representatives for 2D carbon, TMO and TMS materials, respectively, for LIB anodes.

#### 1.4.1. Graphene

Graphene, a defect-free carbon monolayer, is considered the mother material of a family of 2D carbon forms. [191] The novel properties of graphene, such as large surface to mass ratio (2600 m<sup>2</sup> g<sup>-1</sup>), [192] high electrical conductivity [193] and high mechanical strength [194], make it a promising material as electrodes in LIBs. Differently from graphite, in which Li<sup>+</sup> are intercalated between the stacked layers, [195] single-layer graphene (SLG) can theoretically store Li<sup>+</sup> on both surfaces, reaching the theoretical capacity of 744 mAh g<sup>-1</sup>. [196, 197] Also, the edges in graphene nanoflakes (< 100 nm) are able to offer the considered active sites for Li<sup>+</sup> storage. [198] However, both theoretical and experimental studies have evidenced that Li<sup>+</sup> storage is not thermodynamically favored in SLG, where only low Li<sup>+</sup> occupancy levels can be achieved. [160, 199, 200] Meanwhile, graphene nanoplatelets (GNPs) have demonstrated some appealing features for niche applications, *e.g.*, low temperature and high power), but no considerable gain in maximum specific capacity with respect to graphite. [201] This raises a natural question. What about what lies in between? Is there a critical flakes size where both beneficial properties of graphite, *e.g.*, low operating voltage and graphene, *e.g.*, high conductivity and short diffusion length, are found? Is few-layer graphene a good active material for next-generation LIBs? Despite the fact that it is well accepted that dimension (lateral size and thickness) of the flakes, [202] as well as their edges, [198] are expected to play key roles on the Li<sup>+</sup> storage mechanisms, [198, 202] the link between these morphological properties, and electrochemical performances has not been established yet. The answer for these questions will be unveiled in **chapter 4**.

#### 1.4.2. Molybdenum trioxide

MoO<sub>3</sub>, especially  $\alpha$ -MoO<sub>3</sub> with the stable orthorhombic phase, exhibits a very high theoretical capacity of 1117 mAh g<sup>-1</sup> as LIB anodes. [203, 204] Additionally, the interlayer spacing as large as 0.69nm of  $\alpha$ -MoO<sub>3</sub> compared to 0.34 nm of graphite, guarantees its Li<sup>+</sup> host capability. [205] Moreover, its higher intercalation voltages (1.5-2.3V Vs Li/Li<sup>+</sup>), with respect to that of graphite (< 0.4V Vs Li/Li<sup>+</sup>), could reduce the safety problems caused by the decomposition of electrolyte, especially for the utilization in HEVs. [64] However, the main drawbacks of bulk MoO<sub>3</sub> for LIB application is its low ionic [206] and electrical conductivity (10<sup>-5</sup> S m<sup>-1</sup>) [155] as well as volume change during charging/discharging processes. [64] In this regard, to enable MoO<sub>3</sub> for LIB application, the nanostructured design and synthesizing composite, including nano-sized MoO<sub>3</sub> and carbon-based materials, *e.g.*, amorphous carbon

[207, 208], CNTs [209, 210] and graphene [211, 212] are the highly promising strategies to overcome the aforementioned drawbacks of MoO<sub>3</sub>. In this thesis, the MoO<sub>3</sub> nanoflakes are firstly produced by LPE of bulk MoO<sub>3</sub>. A simple solution mixing process of SWNTs and MoO<sub>3</sub> flakes allows forming a hybrid structure of MoO<sub>3</sub>/SWNTs for LIB anode. The nano-sized MoO<sub>3</sub> reduces the Li<sup>+</sup> diffusion length, promoting fast Li<sup>+</sup> transport, whereas the SWNTs play a role of conductive agent to improve the conductivity of electrode and a buffer layer to accommodate the volume change. The synthesis of MoO<sub>3</sub>/SWNTs hybrid and its electrochemical properties as anode material for LIBs will be reported in **chapter 3 and 5**.

### 1.4.3. Molybdenum disulfide

Molybdenum disulfide (MoS<sub>2</sub>) with the 2H phase possesses sandwich-like layered structure in which the S and Mo atoms are covalently bonded forming 2D layers, and the layers are held together through weak van der Waals interactions. [213] The inter-layer spacing of MoS<sub>2</sub> (0.62 nm) [72] is more favourable for Li<sup>+</sup> intercalation [214, 215] with respect to that of graphite (0.34 nm). Notably, MoS<sub>2</sub> is able to deliver the theoretical capacity of 670 mAh g<sup>-1</sup>. [72] Moreover, the high insertion voltage of MoS<sub>2</sub> anode (~ 0.5-1.1 V vs. Li/Li<sup>+</sup>) can make itself as a safer anode than graphite (< 0.4 V vs. Li/Li<sup>+</sup>), because the Li dendrite formation, a layer progressively formed during the cycling process on the surface of electrode, is less likely to occur at higher insertion voltage. [216] Nevertheless, there are following issues that need to be solved: (i) the fast capacity fading of the bulk MoS<sub>2</sub> because of the volume change during lithiation/de-lithiation; [72, 217, 218] (ii) the low rate performance due to the low electrical conductivity of 2H phase MoS<sub>2</sub> (200 cm<sup>2</sup> V<sup>-1</sup> s<sup>-1</sup>). [214, 219-221] Therefore, many efforts have been devoted to develop nanostructure of MoS<sub>2</sub>, and to the synthesis of hybrid of MoS<sub>2</sub> and carbon-based materials. In particular, the composites of MoS<sub>2</sub>/GO, [222] MoS<sub>2</sub>/rGO [223, 224] and MoS<sub>2</sub>/CNTs [225] have been synthesized and demonstrated the significant improvement in LIB performance with respect to the individual components.

This thesis presents the hybrid structure of MoS<sub>2</sub> flakes (produced via LPE of bulk MoS<sub>2</sub>) and amorphous carbon, prepared by a thermal decomposition of a carbon source, *e.g.*, PAA. The presence of carbon network in the hybrid structure is expected as a conducting agent to improve the electrical conductivity of electrode and a buffer layer for active materials to hinder its pulverization during lithiation and de-lithiation. The synthesis of MoS<sub>2</sub>/C hybrid and its electrochemical properties for LIB anode will be introduced in **chapter 3 and 5**.

### 1.4.4. Black phosphorous

Black phosphorus (BP), a layered crystal, having an orthorhombic phase, with puckered layers [186] held together by interlayer van der Waals interactions. [186] This structure allows BP to uptake three  $\text{Li}^+$  to reach a composition of  $\text{Li}_3\text{P}$ , [149] leading to a very high theoretical specific capacity of  $2596 \text{ mA h g}^{-1}$  [147-149]. Also, the puckered structure is able to promote fast  $\text{Li}^+$  diffusion ( $10^4$  times faster than that in graphite), [226] resulting in its outstanding rate-capability. Moreover, when exfoliated into single layer (phosphorene) or FL-BP flakes, the increased available surface area can further enhance the electrochemical activity, [186] which is beneficial for energy storage applications. [147, 202] Therefore, exfoliated BP is a promising candidate for the next generation of LIB anodes. The exfoliation of bulk BP into FL-BP flakes can be performed by many methods, e.g., MC, BM and LPE. [186] However, the MC has the issues of scalability limitation [142] and morphological heterogeneity of the BP flakes, [150] whereas the drawback of BM is the presence of impurities in the BP flakes. [145, 187] In this regard, LPE has been recognized as a strategic route for the large-scale production of less defective phosphorene and FL-BP flakes. [226] However, current approaches for the LPE of BP present several issues especially in aqueous environment, where the chemical integrity of the exfoliated flakes is compromised due to the oxidation promoted by the presence of  $\text{O}_2/\text{H}_2\text{O}$ . [227-229] The formation of phosphorus-oxide species, *i.e.*  $\text{P}_2\text{O}_5$  and  $\text{P}_2\text{O}_4$ , [230] has been reported when the BP is exposed to air. These processes accelerate the degradation of BP. [231] Performing the LPE in pure organic solvents can solve this issue, since the presence of water and  $\text{O}_2$  is avoided. The organic solvents that commonly used to exfoliate BP are generally toxic (Health code  $\geq 2$  NFPA704), [232] and have a b.p. usually above  $100^\circ\text{C}$ , *e.g.* N-methyl-2-pyrrolidone (NMP, b.p. =  $202^\circ\text{C}$ ), [233] N,N-dimethylformamide (DMF, b.p. =  $153^\circ\text{C}$ ) [234] N-cyclohexyl-2-pyrrolidone (CHP, b.p. =  $284^\circ\text{C}$ ) [235] or formamide (b.p.  $210^\circ\text{C}$ ). [236] The solvent b.p. is critical for LIB technology because the solvent removal is of paramount importance for the realization of high performance electrodes of batteries.

In this thesis, the bulk BP is exfoliated by LPE using 14 different solvents, which were selected after having considered the different values of surface tension ( $\gamma$ ), b.p. and/or Hansen and Hildebrand solubility parameters of each solvent. A stability analysis of BP on the diverse solvents provides information about the solubility parameters of BP, *e.g.*,  $\gamma$ , Hansen and Hildebrand solubility parameters. These BP solubility parameters give me a clue on the adequate solvent selected to exfoliate and/or store exfoliated BF flakes. Ideally, the solvent should have a low-b.p., which would allow a fast deposition, especially useful for the aim of designing LIB anodes. This thesis firstly presents the analysis of dispersability and stability of exfoliated BP flakes in various solvents to determine the ideal solvent, *e.g.*, acetone, for the

LPE of BP. Then the feasibility and up-scalability of this approach is demonstrated by designing homogeneous films of FL-BP flakes exfoliated in acetone and used as anodes for LIBs. The details of solvent selection for LPE of BP and the study of electrochemical properties FL-BP based anode will be described in **chapter 3 and 6**.

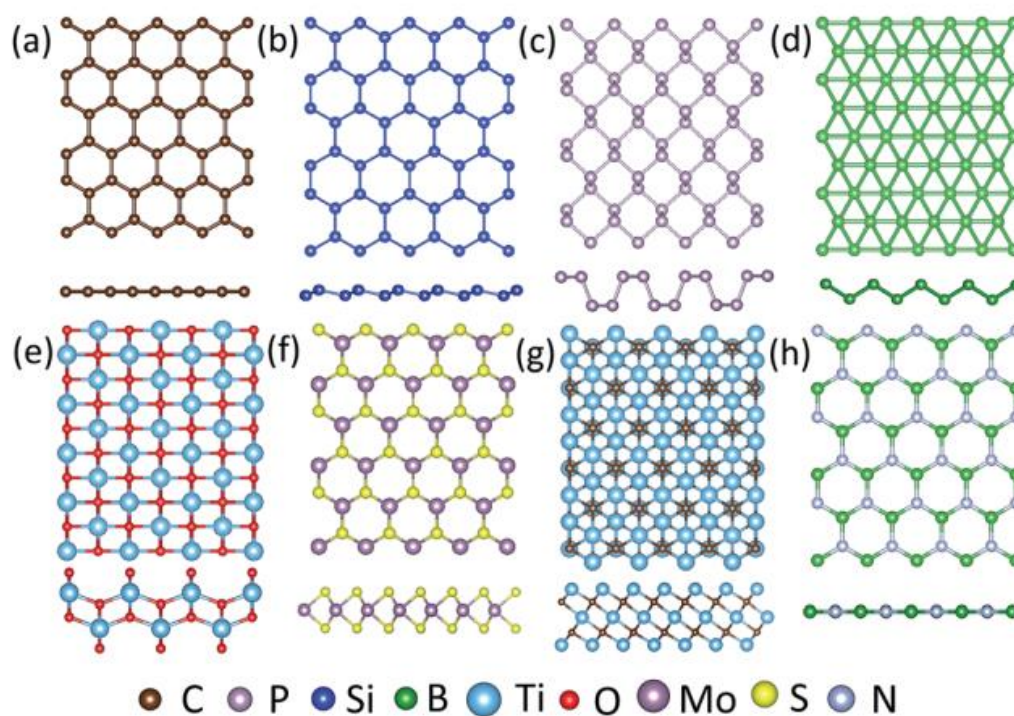


Figure 1.12. Top and side view of the atomic structure of 2D single layered: (a) graphene, (b) silicene, (c) phosphorene, (d) borophene, (e)  $\text{TiO}_2$ , (f)  $\text{MoS}_2$ , (1H) (g)  $\text{Ti}_3\text{C}_2$  and (f) h-BN. [145]

# Chapter 2:

## Experimental procedure

### 2.1. Production and processing of graphene and other two dimensional materials

In this thesis, LPE [237, 238] is exploited to produce graphene and other 2D materials, e.g., MoO<sub>3</sub> and MoS<sub>2</sub> owing to its low-cost, simplicity and high throughput, which can be scalable at the industrial level. [188-190] In particular, the LPE graphene exhibits a low level of basal plane defects and high crystallinity, [188, 189, 202, 239] which is an important feature for the electron transport within electrode in LIB application. [129]

#### 2.1.1. Liquid phase exfoliation of graphite and other layered materials

The LPE (Figure 2.1) [240] process typically involves three steps: (1) dispersion of bulk materials in solvents, (2) exfoliation and (3) purification. [150]

In the first step, bulk material is dispersed in a solvent. Then the exfoliation of bulk materials in the solvent is realized by ultra-sonication in the second step. During the ultra-sonication process, propagation of cavitation, [202] e.g., the growth and subsequent collapse of bubbles or voids in solvents due to pressure fluctuations, [150] creates hydrodynamic shear-force which acts on bulk materials, inducing exfoliation. [241] After exfoliation, the solvent–2D flakes interaction needs to balance the inter-sheet attractive forces. [150] Solvents ideal to stably disperse 2D flakes are those that minimize the interfacial tension between the liquid and graphene flakes, e.g., the force that minimizes the area of the surfaces in contact). [242] Therefore, the good dispersions of 2D flakes require the solvents having  $\gamma$  as close as the surface energy of 2D flakes. [243] For instance, NMP has a  $\gamma$  of 41.2 mN m<sup>-1</sup> [244] close to the value of surface energy of graphene (46.7 mN m<sup>-1</sup>). [241] Thus, NMP is the good solvent to disperse graphene. However, the exfoliation process produces a heterogeneous dispersion of thin/thick and small/large 2D flakes. Therefore, the purification step is necessary to separate exfoliated from un-exfoliated flakes, and is usually carried out via ultracentrifugation. [240] In this step, thick flakes can be removed by ultracentrifugation in a uniform medium, so called SBS. [245] The SBS is the most common separation strategy and, to date, flakes ranging from few nanometers to a few microns have been produced, with concentrations up to a few mg ml<sup>-1</sup>. [246]

The SBS is applied generally to particles (in this case flakes) dispersed in a medium (solvent) under a force field. [247] The forces acting on particles dispersed in a solvent during

centrifugation are (i) the centrifugal force  $F_c = m_p \omega^2 r$ , proportional to the mass of the particle itself ( $m_p$ ), the distance from the rotational axes ( $r$ ), and to the square of the angular velocity ( $\omega$ ); (ii) the buoyant force  $F_b = -m_s \omega^2 r$ , e.g., the force deriving from the Archimedes' principle that is proportional to the mass of the displaced solvent ( $m_s$ ) times the centrifugal acceleration; and (iii) the frictional force  $F_f = -fv$ , e.g., the force acting on the particles while moving with a sedimentation velocity ( $v$ ) in a fluid. This force is proportional to the friction coefficient ( $f$ ) between the solvent and the particle itself. The sum of the forces acting on the dispersed flakes is represented as: [247]

$$F_c - F_b - F_f = F_{tot} \quad (2.1)$$

The ratio of sedimentation or sedimentation coefficient ( $S$ ) can be defined as the ratio between the sedimentation velocity and the particle acceleration, e.g, the centrifugal acceleration ( $\omega^2 r$ ) in this case:

$$S = \frac{v}{\omega^2 r} = \frac{m_p - (1 - \frac{\rho_s}{\rho_p})}{f} \quad (2.2)$$

in which  $\rho_s$  and  $\rho_p$  are the density of the solvent and the particle, respectively. Following equation 2.2, the  $S$  increases according to the mass of the 2D flakes, while decreases with their physical dimensions (lateral size and thickness). The un-exfoliated bulk flakes, as well as large and thick ones, have a larger mass than the thin and small flakes, thus  $S$  of the un-exfoliated flakes is higher than that of thin and small flakes. By tuning centrifugal force, it is possible to obtain dispersions with flakes of different lateral size and thickness.

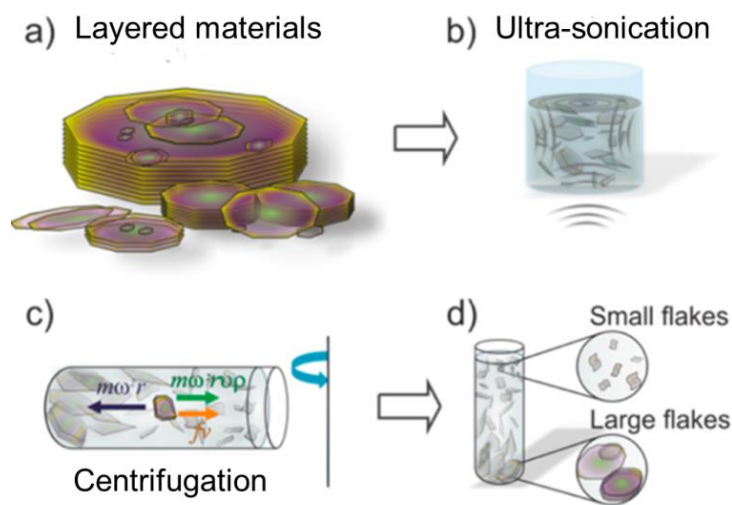


Figure 2.1. *Liquid phase exfoliation of bulk layered materials* [240]

### 2.1.2. Solvent exchange processes

It has been reported that liquids with  $\gamma$  of  $\sim 40 \text{ mN m}^{-1}$ , such as NMP, DMF, benzyl benzoate, etc., are the proper solvents for the dispersion of graphene and other 2D flakes, *e.g.*, MoS<sub>2</sub>, WS<sub>2</sub>. [150] Among these, NMP has been found to be one of the most effective solvents for the exfoliation of graphene and other 2D materials [150, 248]. However, NMP is not an environmentally friendly solvent, which is a considerable issue in development of 2D layered materials-based LIB technology. [3, 249, 250] Besides, due to the high b.p. (202° C), [3] the evaporation of NMP after electrode fabrication requires high temperature ( $> 150^\circ \text{C}$ ) [3, 249] and vacuum to avoid the oxidation of active materials. [251] To address these limitations, a solvent exchange process [252] is exploited to eliminate NMP. Moreover, the solvent exchange process allows recycling over 90% of NMP, decreasing production costs, waste disposal and pollution. Besides, the direct exfoliation of bulk 2D materials in an environmental friendly solvent is considered as a promising strategy to produce exfoliated 2D flakes.

### 2.1.3. Experimental

In this thesis, the LPE of graphite in NMP is exploited to firstly produce graphene. A solvent exchange process from NMP to a low b.p. and environmentally friendly solvent such as ethanol (EtOH), is deployed to obtain graphene flakes dispersion. Also, graphene flakes with different lateral size and thickness are sorted by means of SBS.

Concerning MoO<sub>3</sub> and MoS<sub>2</sub>, the exfoliation of bulk MoO<sub>3</sub> and MoS<sub>2</sub> is directly carried out in 2-propanol (IPA) in order to avoid the use of NMP. Then the SBS process is carried out to eliminate the bulk counter parts from the exfoliated MoO<sub>3</sub> and MoS<sub>2</sub>. More importantly, the LPE of BP is carried out in 14 different solvents in order to serve for the study on the effects of solvent properties on the exfoliation of BP. The productions of four materials are as following:

#### 2.1.3.1. Liquid phase exfoliation of graphite

1 g of graphite flakes (Sigma-Aldrich) is dispersed in 100 mL of NMP (Sigma-Aldrich) and exfoliated by ultra-sonication in a sonic bath (Branson®5800) for 6 hours. The resulting dispersion is then ultra-centrifuged at 10000 rpm (17100 g) (in a Beckman Coulter Optima™ XE-90 with a SW32Ti rotor) for 30 min at 15 °C, to remove thick flakes and un-exfoliated graphite. After the ultracentrifugation process, 80% of the supernatant is collected by pipetting, thus delivering a graphene dispersion in NMP. This dispersion is filtered through a Millipore® filter with 0.2 mm pore size by vacuum filtration to obtain the graphitic flakes.

Meanwhile 1 L of EtOH (Sigma-Aldrich, 99.8%) is added in batches of 100 mL each to the filtration flask in order to remove the residual NMP in graphitic flakes. Finally, 5 mL of EtOH are used to recover the graphitic flakes from the filter and 10 mins of sonication is then applied to re-disperse the graphitic flakes in EtOH.

### ***2.1.3.2. The sorting of graphene flakes by size and thickness via sedimentation-based separation***

Four batches of 10 g of graphite flakes (Sigma Aldrich) are dispersed in 1 L of NMP (Sigma Aldrich, biotech grade) by ultra-sonication (USC-2600 THD, VWR®) for 6 hours at a frequency of 40 kHz and power of 300W (10 g of graphite are distributed in 20 vials with 0.5 g graphite and 50 ml NMP in each vial). The obtained dispersions are settled for 12 hours, and then 80% of their supernatants are collected by pipetting, followed by an ultracentrifugation step at 2000 rpm (769 g) for 30 min using a Sigma 3-16P centrifuge with an 11180 rotor (S3-16P). Afterwards, the precipitate is collected and named as Sample #1. The supernatant is then collected and used for a second round of centrifugation at 4000 rpm (3076 g) for 30 mins; the precipitate is collected and named as Sample #2. Next, the supernatant is ultra-centrifuged at 10000 rpm (17100 g) for 50 mins using a Beckman Coulter Optima™ XE-90 ultracentrifuge with a SW32Ti rotor for the third round of ultracentrifugation to collect the precipitate and named as Sample #3. With the same rotor, a fourth round of ultracentrifugation is performed at 30000 rpm (153700 g), and the precipitated part is named Sample #4. To eliminate the presence of NMP in the 4 samples, we carried out the solvent exchange process, as outlined in the following procedure. Each sample in NMP is dispersed in 100 ml of EtOH (99.8%, Sigma Aldrich), namely in an environmentally friendly solvent having a much lower b.p. than NMP (78 °C vs 204.3 °C), ultra-sonicated for 15 min, and then left to sediment for 72 h. Afterward, the sediments of 4 samples are collected (the supernatant discarded) and stored in EtOH.

### ***2.1.3.3. Liquid phase exfoliation of molybdenum trioxide***

MoO<sub>3</sub> powder (240 mg) is added to IPA (80 mL) in a 100 mL open top, flat bottomed beaker. The dispersion is ultra-sonicated using a horn probe sonic tip (VibraCell CVX, 750W, 25% amplitude) for 5 h. The sonic tip is pulsed for 9 sec on and 2 sec off to avoid damage to the processor and reduce any solvent heating. To minimize heating effects, an external cooling system circulated cooled water at 5 °C around the beaker during ultra-sonication. To remove any un-exfoliated material the ultra-sonicated dispersion is filled in glass vials (~30 ml) and centrifuged at 1000 rpm (~100 g) for 30 mins. The supernatant is decanted (~20 ml) and



further centrifuged at 1000 rpm for 105 mins to remove small flakes. The supernatant is decanted (containing small flakes) and discarded while the sediment is re-dispersed in IPA.

#### ***2.1.3.4. Liquid phase exfoliation of molybdenum disulfide***

100 mg of MoS<sub>2</sub> are dispersed in 10 mL of IPA and ultra-sonicated (USC-2600 THD, VWR®) for 6 h at a frequency of 40 kHz and power of 300W. The obtained dispersion is centrifuged at 4000 rpm (3076 g) for 30 mins using a Sigma 3-16P centrifuge with an 11180 rotor (S3-16P), to remove thick and un-exfoliated MoS<sub>2</sub> flakes. After the centrifugation process, the upper 80% of the supernatant is collected by pipetting.

#### ***2.1.3.4. Liquid phase exfoliation of black phosphorous***

Black Phosphorus (500 mg, from Smart Elements) is pulverized with a mortar and pestle. The selected solvents (*i.e.* acetone, toluene, chloroform, IPA, trichloroethylene, methanol, ethylene glycol, acetonitrile, EtOH, n-hexane, NMP, CHP, DMF and diethyl carbonate) have different  $\gamma$ , b. p. and/or Hansen solubility parameters (see Table 3.3). All the solvents are of anhydrous grade and were purchased from Sigma Aldrich.

For the analysis of the dispersability and stability of exfoliated BP, 20 mg of pulverised BP and 20 mL of solvents are mixed using a sonic bath (VWR®, USC2600THD) for 6 hours, followed by centrifugation at 900 g for 60 min in order to promote the precipitation of the thicker and un-exfoliated flakes. The precipitation of thick or un-exfoliated flakes promotes the enrichment of BP flakes in dispersion with a specific lateral size and thickness. The centrifugation is carried out in a Sigma 2-16K centrifuge (11170-bucket 2x13299 rotor). After the centrifugation, the supernatant is collected and subjected to another centrifugation run at 900 g for 30 min to further purify the BP dispersions. The pulverization and weighting of the BP crystals and the balancing and sealing of the centrifuge tubes are carried out in a nitrogen-filled glovebox.

For the aging analysis, the samples are stored for three months at room temperature in a closed transparent glass vial. Note that after the LPE process, all the other experimental processes for the material production are conducted outside the glove box.

## **2.2. Preparation of single wall carbon nanotube-bridged molybdenum trioxide and molybdenum disulfide/amorphous carbon hybrids**

### **2.2.1. Preparation of single wall carbon nanotube-bridged molybdenum trioxide hybrid**

Single wall carbon nanotubes have displayed great potential as anode materials for lithium ion batteries due to their unique 1D structural, high electrical conductivity ( $10^6 \text{ S m}^{-1}$ ). [167, 253] Thus, the combination of SWNTs into the hybrid structure with 2D materials, *e.g.*,  $\text{MoO}_3$ , can improve the electrochemical performance of electrodes. SWNTs play a role as (i) a conducting agent, promoting electronic charge transport, [254] (ii) an active anode material, offering extra capacity thanks to its  $\text{Li}^+$  storage capability by surface and/or inside individual nanotubes. [254]

In this thesis, the P3 SWNTs (carbon solution) are dispersed in IPA at a concentration of  $0.1 \text{ g L}^{-1}$  and sonicated in both a horn sonic probe and a sonic bath to achieve a homogeneous dispersion. The procedure involves horn probe ultra-sonication (30 mins) followed by 1h in a sonic bath and an additional 30 min in the horn probe tip. After that, The as-produced  $\text{MoO}_3$  (as reported in section 2.1.3.3), SWNTs and carbon black super-P (CB) dispersions are mixed, without centrifugation, to form hybrid structures of known wt% ( $\text{MoO}_3$  : SWNTs = 9:1, 8:2 and 7:3, respectively). Accurate weighing of an alumina membrane (pore size 25nm) before and after filtration of  $\text{MoO}_3$  dispersion allowed determining the concentration.

## 2.2.2. Preparation of molybdenum disulfide/amorphous carbon hybrid

The aim of synthesizing  $\text{MoS}_2/\text{C}$  hybrid is to overcome drawbacks of  $\text{MoS}_2$  for LIB anode, *e.g.*, low conductivity and volume change. The carbon network is expected to improve the electrical conductivity of electrode [168, 169] and buffer the volume change of active materials upon cycling. [168, 169]

In the present work, PAA is used as a carbon source to form carbon network. The exfoliated  $\text{MoS}_2$  flakes (as reported in section 2.1.3.4) are mixed with PAA in IPA with various weight ratios of  $\text{MoS}_2$  : PAA, *e.g.*, 1:1, 1:2 and 1:4 wt%, followed by magnetic stirring for 60 min. Then the mixtures of  $\text{MoS}_2$  and PAA ( $\text{MoS}_2/\text{PAA}$ ) are dried at  $40^\circ \text{C}$  under vacuum overnight in order to remove the IPA, obtaining the  $\text{MoS}_2/\text{PAA}$  powders. These powders are annealed at  $500^\circ \text{C}$  for 30 minutes under argon atmosphere in order to carbonize the PAA. The pyrolysis forms a  $\text{MoS}_2/\text{C}$  hybrid. The  $\text{MoS}_2/\text{C}$  powders are named as  $\text{MoS}_2/\text{C}$ -1,  $\text{MoS}_2/\text{C}$ -2, and  $\text{MoS}_2/\text{C}$ -3 corresponding to the different weight ratios of  $\text{MoS}_2/\text{PAA}$  as 1:1, 1:2 and 1:4 wt%, respectively. These powders are used as active material in the LIB anodes.

## 2.3. Material characterization techniques

### 2.3.1. Optical absorption spectroscopy

The Optical absorption spectroscopy (OAS) is carried out in a Cary Varian 5000UV-vis spectrophotometer. For the OAS measurements, the graphene samples are diluted 1:10 (v/v) in NMP and the MoO<sub>3</sub> and MoS<sub>2</sub> samples are diluted 1:100 (v/v) in IPA and the SWNTs sample is diluted 1:10 in IPA. The absorption spectra are acquired using a 1 mL quartz glass cuvette. The absorption spectra of the solvents used are subtracted to each spectrum.

### **2.3.2. Thermogravimetric analysis**

Thermogravimetric analysis (TGA) (TG-Q500) is carried out in air. The temperature ramp started from room temperature (RT) to 900°C at a heating rate of 10°C min<sup>-1</sup>. 5 mg of each MoS<sub>2</sub> and MoS<sub>2</sub>/carbon composite samples are used for TGA.

### **2.3.3. Powder X-ray diffraction**

Powder X-ray diffraction (XRD) measurement is performed on a PANalytical X-ray powder diffractometer with monochromatic CuK<sub>α</sub> radiation ( $\lambda = 1.5418 \text{ \AA}$ ). The  $2\theta$  range used in the measurements is from 10 ° to 65 °. Samples (MoS<sub>2</sub> and MoS<sub>2</sub>/carbon MoS<sub>2</sub>/C hybrid powders) are prepared on quartz substrate.

### **2.3.4. Raman spectroscopy**

Raman spectroscopy (Renishaw inVia confocal Raman microscope) is performed with laser excitation wavelength of 514.5, 532, 633 and 785 nm (incident power of ~1 mW on the samples) and a 100× objective. The graphene samples are dispersed in NMP and EtOH, whereas the SWNTs, MoO<sub>3</sub> and MoS<sub>2</sub> samples are dispersed IPA and the BP sample are dispersed in CHP and acetone by sonication. All samples are drop-casted on a Si/SiO<sub>2</sub> (300 nm SiO<sub>2</sub>) (Si-Mat Silicon Materials) substrate and dried under vacuum overnight.

### **2.3.5. Transmission electron microscopy**

Transmission electron microscopy (TEM) images of samples are acquired with a JOEL JEM-1011 microscope, operated at 100 kV. The high-resolution TEM (HRTEM) and high angular annular dark field - scanning TEM ((HAADF)-STEM) images are obtained on a JEOL JEM-2200FS microscope, operating at 200 kV, which is equipped with a CEOS objective corrector, and an in-column filter ( $\Omega$ -type). The energy dispersive X-ray spectroscopy (EDS) and energy filtered (EFTEM) elemental mapping were acquired by a Bruker Quantax 400 system with a 60 mm<sup>2</sup> XFlash 6T silicon drift detector (SDD) on the same microscope. The electron energy loss spectroscopy (EELS) data are collected in TEM mode using a FEI Tecnai F20 TEM operating at 200 kV and equipped with Gatan Enfimum SE spectrometer. The EEL spectra are acquired with a collection semi-angle of 100 mrad. The SWNTs, MoS<sub>2</sub> and MoO<sub>3</sub> samples are

dispersed in IPA, graphene samples are dispersed of NMP and EtOH and BP are dispersed of CHP and acetone by sonication. 100  $\mu\text{L}$  of the resulting inks are drop-casted at RT onto carbon coated Cu TEM grids (300 mesh), and subsequently dried under vacuum overnight.

### **2.3.6. Scanning electron microscopy**

Scanning electron microscopy (SEM) images of all electrodes are taken using a field-emission scanning electron microscope FE-SEM (Jeol JSM-7500 FA) at the operating voltage of 10 kV without any metal coating, for all samples.

### **2.3.7. Atomic Force Microscopy**

Atomic Force Microscopy (AFM) images are acquired with Bruker Innova AFM in tapping mode using silicon probes ( $f = 300$  kHz,  $k = 40$  N/m). Intermittent contact mode AFM images of  $5 \times 5 \mu\text{m}^2$  were collected with 512 data points per line and the working set point was kept above 70% of free oscillation amplitude and measurements were taken at scan rate of 0.7 Hz. Thickness statistic is performed measuring  $\sim 100$  flakes from AFM images. Statistical analyses are fitted with log-normal distributions. The graphene,  $\text{MoS}_2$  and BP samples are diluted 1:100 (v/v) in EtOH. 100  $\mu\text{L}$  of the dilutions are drop-cast onto Si/SiO<sub>2</sub> wafers.

### **2.3.8. X-ray Photoelectron Spectroscopy**

X-ray Photoelectron Spectroscopy (XPS) analysis is carried out for all samples, using a Kratos Axis Ultra spectrometer. The samples are drop-casted onto silicon (Si-Mat Silicon Materials) wafers. The XPS spectra are acquired using a monochromatic Al  $K_\alpha$  source operated at 20 mA and 15 kV. The analyses are carried out on a  $300 \mu\text{m} \times 700 \mu\text{m}$  area. High-resolution spectra are acquired at pass energy of 10 eV and energy step of 0.1 eV. The photoelectrons are detected at a take-off angle (i.e., the angle defined by the sample surface normal and the position of the detector)  $\phi = 0$  with respect to the surface normal. The pressure in the analysis chamber is maintained below  $10^{-6}$  Pa for data acquisition.

### **2.3.9. Specific surface-area measurements**

Specific surface-area measurements are carried out by nitrogen physisorption at 77 K in a Quantachrome equipment, model autosorb iQ. The graphene-based anodes deposited onto the Cu support substrates ( $\sim 1.0$  mg) are cut into pieces fitting into the **BET** (Brunauer – Emmett – Teller) measurement chamber. The specific surface area is calculated using the multi-point BET model, considering 11 equally spaced points in the P/P 0 range from 0.05 to 0.30. Prior to measurements, the sample is degassed for 2 hours at 200  $^\circ\text{C}$  under vacuum to eliminate adsorbates.

### **2.3.10. Optical extinction spectroscopy**

The optical extinction spectroscopy (OES) is carried out by a Cary Varian 5000UV-Vis. In order to measure the extinction spectra, FL-BP dispersions in the different solvents are diluted 1:25 with the respective pure solvents. The dispersions in acetone are diluted at different ratios in order to determine the extinction coefficient of FL-BP. The dilutions prepared are: 1:1, 1:2, 1:5, 1:10; 1:20, 1:50 and 1:100. For each sample, the extinction spectra (absorbed plus scattered light) of their corresponding pure solvents are subtracted from the sample spectrum. After the extinction measurement, the samples that are dispersed in acetone are dried and the residue powder is weighted. The initial volume of the solvent and the mass of the dried powder gave the exact concentration for each dilution. The optical extinction coefficient is determined by using the Beer-Lambert law ( $E = \alpha C_{Ph} l$ , in which E is the optical extinction at 600 nm,  $\alpha$  is the extinction coefficient,  $C_{Ph}$  is the concentration of the exfoliated BP and  $l$  is the path length, 0.01 m).

## **2.4. Electrode fabrication and battery assembling**

### **2.4.1. Electrode fabrication**

#### ***2.4.1.1. Graphene electrodes***

The Cu foil with (Sigma-Aldrich) is cut into round shaped disks with a diameter of 1.5 cm and cleaned with acetone (Sigma-Aldrich) in an ultrasonic bath for 10 minutes. Then, the Cu foils are dried at 80 °C and  $10^{-3}$  bar for 2 hours in a glass oven (BÜCHI, B-585) and weighted (Mettler Toledo XSE104); the preparation of Cu foils is applied for all electrodes in this thesis. Subsequently, 250 mL of graphene ink in EtOH is drop-cast on Cu foil under air atmosphere at RT and then dried at 120 °C and  $10^{-3}$  bar for 30 min in an oven (BUCHI, B-585). The graphene mass loading (1 mg) for each anode is calculated by subtracting the weight of bare Cu foil from the total weight of the electrodes.

#### ***2.4.1.2. MoO<sub>3</sub> and MoO<sub>3</sub>/SWNTs hybrid electrodes***

50 mg of MoO<sub>3</sub> flakes (section 2.1.3.3) and MoO<sub>3</sub>/SWNTs hybrid (section 2.2.1) samples are dried and re-dispersed in 5ml EtOH via ultra-sonication for 15 min. Subsequently, the aforementioned samples are drop-cast on the Cu foils as supporting substrates in a circular shape with a diameter of 1.5 cm at 40 °C in air. Then, the as deposited films are dried at 120 °C and  $10^{-3}$  bar pressure for 12 hours in oven (BÜCHI, B-585). The mass loading of the active materials are calculated by subtracting the average weight (obtained with balance of Mettler Toledo XSE104) of bare Cu foil with the same area, from the total weight of the electrodes.

#### **2.4.1.3. MoS<sub>2</sub> and MoS<sub>2</sub>/amorphous carbon hybrid electrodes**

The MoS<sub>2</sub> flakes (see section 2.1.3.4) or MoS<sub>2</sub>/C powders (see section 2.2.2) are mixed with CB and PAA with a weight ratio of 8:1:1 in IPA to form the slurries. The slurries are pasted onto Cu disks with diameter of 1.5 cm. The disks are then dried in an oven (BÜCHI, B-585) at 60 °C and 10<sup>-3</sup> bar pressure for 12 hours. The mass loading of active materials (~1.0 mg) for each anode is calculated by subtracting the weight of bare Cu disks (using an analytical balance of Mettler Toledo XSE104) from the total weight of the electrode. The mass loading of the active materials are calculated by subtracting the average weight (obtained with balance of Mettler Toledo XSE104) of bare Cu foil with the same area, from the total weight of the electrodes.

#### **2.4.1.4. Few-layer black phosphorous electrodes**

The round copper disks (99.98% trace metals basis, Sigma-Aldrich) with a diameter of 1.5 cm cleaned with acetone and then dried for 2 hours in a glass vacuum oven (BÜCHI, B-585) at 80 °C with a 10<sup>-3</sup> bar pressure. The FL-BP dispersions in CHP and acetone are mixed with carbon black (CB, super-P) and Polyvinylidene fluoride (PVdF, Sigma-Aldrich), with a mass ratio of 3:1:1, then drop-cast onto the cleaned copper substrates inside the glove box at room temperature. The resulting FL-BP coated electrodes are subsequently dried in a vacuum oven at 120 °C for acetone, and to 180 °C for CHP dispersed sample, at a 10<sup>-3</sup> bar pressure for 30 mins. The average mass loading of FL-BP (not including CB or PVdF) that is obtained from both the CHP and acetone dispersions is 0.6 mg cm<sup>-2</sup> for both samples.

#### **2.4.2. Assembling of half- and full-cells**

All electrodes are assembled in half-cell configuration to characterize the electrochemical properties of each material. Half-cells are assembled in coin cells (2032, MTI) in an argon filled glove box (O<sub>2</sub> and H<sub>2</sub>O < 0.1 ppm) at 25 °C, using 1M LiPF<sub>6</sub> in a mixed solvent of ethylene carbonate/dimethylcarbonate (EC/DMC, 1:1 volume ratio) (Sigma Aldrich, CAS 21324-40-3) as electrolyte (LP30, BASF), and a glass-fibre as separator (Whatman GF/D). For the half-cell configuration, the anodes are tested against Li foil) as the counter and reference electrodes (two electrodes system).

In case of binder-free graphene electrode, the full-cell configurations are assembled with the commercial LNMO powder as active material for cathode (NEI Corporation). The cathode composition is 80 wt% of LNMO, 15 wt% of CB (TIMCAL) and 5 wt% Polyvinylidene fluoride (PVdF) (Sigma-Aldrich). The three components, in the form of powders, are mixed with NMP using a ball mill at 250 rpm for 2 hours. To promote a better adhesion between the

cathode slurry and the current collector, the roughness of Al foils is increased by an etching procedure in KOH. For this propose, the Al foils are immersed for 1 min in 5 wt% KOH aqueous solution, and afterward washed with distilled water and dried at 60 °C for 4 hours. The PVdF/LNMO/CB slurry is deposited, by using a doctor-blade, on KOH-etched Al foils. After the drying process, the electrodes are shaped in a circular form by a cutting procedure followed by a pressing process at ~ 2 MPa for 1 min. Before full-cell assembling, the anode is pre-lithiated by placing the graphitic film in direct contact with a Li foil wet by using the electrolyte solution (LP30) for 30 minutes.

## 2.5. Electrochemical characterizations

### 2.5.1. Cyclic Voltammetry

Cyclic voltammetry (CV) is a useful technique for acquiring qualitative information about electrochemical process occurring within electrode. A typical electrode reaction involves the transfer of charge between an electrode and a species in solution. [255] The CV technique can detect the charge transfer process of electrode reaction through recording the current response in a certain potential range when the fixed voltage scan rate is applied. In CV measurements the current response is plotted as a function of voltage.

The electrochemical reaction of electrode in the case of LIB can be described by CV, as shown in Figure. 2.2. As the voltage is initially swept from  $V_1$ , the equilibrium at the electrode surface begins to alter and the current begins to flow. The current rises as the voltage is swept further toward to  $V_2$  from its initial value equilibrium position ( $V_1$ ) due to the continuous reduction of  $\text{Li}^+$  in to Li, see equation 1.2, on the electrode surface (lithiation process). [256] Thus more active material is lithiated by the reduction of  $\text{Li}^+$ , resulting in the increase in the flux of  $\text{Li}^+$  to electrode surface. [255] This leads to the increase in Li concentration at electrode surface. The peak ( $i_c$ ) occurs once the concentration of Li is sufficient on the electrode surface. At this moment the flux of  $\text{Li}^+$  reduces, reaching the subsequent depletion of  $\text{Li}^+$  on electrode surface, therefore, the current begins to drop. When the scan is reversed, voltage is swept back from  $V_2$  to  $V_1$ , the reversible electrochemical reactions, e.g., the oxidation of Li into  $\text{Li}^+$  (de-lithiation), is observed which is evidenced by the peak  $i_a$ .

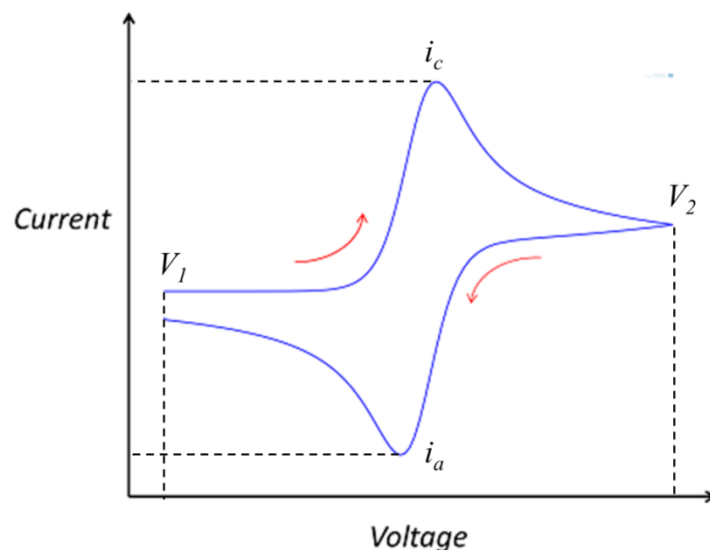


Figure 2.2. Schematic of cyclic voltammetry of lithium ion battery electrode [257]

In this thesis, the CV measurement is performed at a scan rate of  $50 \mu\text{Vs}^{-1}$  between 3 V and 5 mV vs Li/Li<sup>+</sup> with a Biologic MPG2 potentiostat/galvanostat for all electrodes in half-cell configurations against Li foils (Sigma-Aldrich) as the counter and reference electrodes (two electrodes system). All electrochemical measurements are performed at room temperature.

### 2.5.2. Galvanostatic charge/discharge cycling measurement

Galvanostatic charge/discharge cycling measurement, so called the constant current method, is considered to be a very useful method to characterize the electrochemical performance of an electrode. It measures the amount of charge stored within an electrode (capacity) under a constant current load over increasing cycle numbers. In order to characterize an electrode of LIB, a current pulse is applied to the electrode and its resulting potential is measured against a reference electrode (Li foil) as a function of time, see Figure 2.3a. In order to calculate the capacity, the duration of a single charge or discharge step has been multiplied by the current applied during that step, see Figure 2.3b. The plot of potential vs. capacity is called *voltage profile*.

In the galvanostatic charge/discharge cycling measurement, the constant current applied to the electrode causes the active materials, *e.g.*, graphite, to be oxidized/ reduced at a constant rate. [255] The electrode potential accordingly varies with time as the concentration ratio of active material, to lithiated-active material, *e.g.*, ratio of C/LiC<sub>6</sub>) changes at the electrode surface. After the concentration of active material drops to zero at the electrode surface (fully charged), the active material might be insufficiently supplied to the surface to accept all of the electrons being forced by the application of a constant current. The electrode potential will then sharply change to more negative/positive values. The fixed potential range with the cut-



off potentials, *e.g.*,  $E_1$  and  $E_2$ , is always set according to the working voltage of electrode to avoid side reactions, see Figure 2.3. When the voltage reaches the  $E_2$ , the electrode process, *e.g.*, charging/discharging, will stop. Then the new electrode process will start and the voltage will change back to the  $E_1$ .

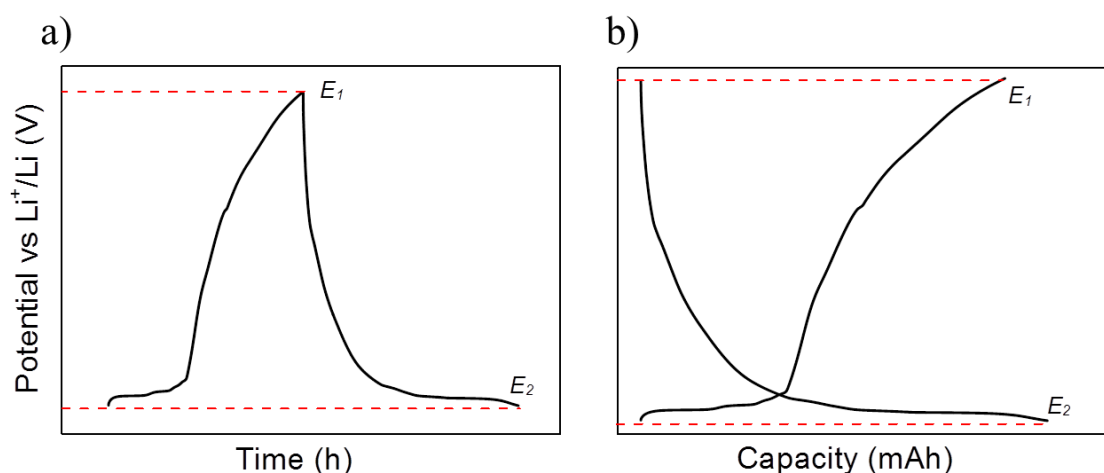


Figure 2.3. Schematics of galvanostatic charge/discharge curves of lithium ion battery electrode: (a) potential versus time and (b) potential versus capacity plots.

In this thesis, the galvanostatic charge/discharge cycling tests of all electrodes are performed at a constant current density, using a battery analyser BCS-805 (BioLogic). The charge/discharge cycling tests are performed at different rates (C-rate) by battery analyser BCS-805 (BioLogic). All electrochemical measurements are performed at room temperature.

### 2.5.3. Electrochemical impedance spectroscopy

In electrochemical impedance spectroscopy (EIS), the system under investigation is excited by a small amplitude AC sinusoidal signal of potential or current in a wide range of frequencies and the response of the current or voltage is measured. Since the amplitude of the excitation signal is small enough for the system to be in the (quasi-) equilibrium state, the EIS measurements can be used to effectively evaluate the system properties without significantly disturbing them. Frequency sweeping in a wide range from high-to low-frequency enables the reaction steps with different rate constants, such as mass transport, charge transfer, and chemical reaction, to be separated.

In the EIS measurement, a sinusoidal potential applied to the system leads to a sinusoidal current output at the same frequency which cause the exponential increase in output current with the applied potential. [255] In case an excitation signal with large amplitude is applied, the system is deviated from linearity; the current output to the sinusoidal potential input

contains the harmonics of the input frequency. Because the system excitation caused by the time-dependent, the impedance is expressed as [255]

$$Z(t) = \frac{E(t)}{I(t)} = \frac{Z_0 \cos(\omega t)}{\cos(\omega t - \phi)} \quad (2.3)$$

in which  $Z(t)$  is the impedance of the system,  $E(t)$  is the applied potential at time  $t$ ,  $Z_0$  is the impedance amplitude, and  $\omega$  is the angular frequency that is defined as the number of vibrations per unit time (frequency, Hz) multiplied by  $2\pi$ . The output current signals  $I(t)$  has is shifted in phase by  $\phi$ . By using Euler's relationship, [255] the system impedance is expressed as a complex function of

$$Z(\omega) = Z_0 \cos \phi + Z_0 j \sin \phi = Z_{Re} + jZ_{Im} \quad (2.4)$$

When the real part of the impedance ( $Z_{Re}$ ) is plotted on the axis of the abscissa and the imaginary ( $Z_{Im}$ ) part is plotted on the axis of the ordinate, a "Nyquist plot" is obtained, [258] see Figure 2.4.

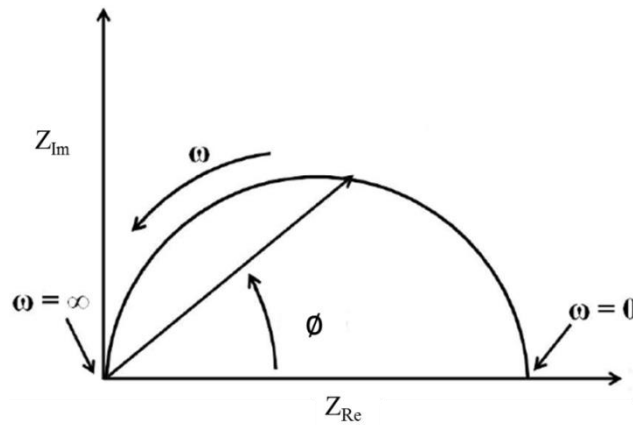


Figure 2.4. Nyquist plot, representing phase angle ( $\phi$ ), and angular frequency ( $\omega$ ) dependence of the impedance. [258]

In the case of LIBs, it can be seen that the electrode composition changes during lithiation/de-lithiation processes due to electrode reactions which is related to  $\text{Li}^+$  transport process, the electron transport process, and the charge transfer process. [259] Because the time constants of each process are different, the EIS is a suitable technique to investigate these reactions and can allow us to separate most of these processes. Therefore, using EIS to analyze the kinetic parameters related to lithiation/de-lithiation materials such as the SEI film resistance, charge transfer resistance ( $R_{CT}$ ), is essential to understand the reaction mechanism of  $\text{Li}^+$  with active material, to study degradation effects, to facilitate further electrode optimization, and to improve the charge/discharge cycle performance of LIBs. At present, the common electrode processes, especially for intercalation electrode, in LIBs are

represented by several steps, [258] as shown in Figure 2.5: (i)  $\text{Li}^+$  transport in an electrolyte; (ii)  $\text{Li}^+$  migration through the SEI film; (iii) electrochemical reaction on the interface of active material particles including electron transfer; (iv)  $\text{Li}^+$  diffusion in the solid phase and (v) phase-transfer in cases where several phases are presented in active material and a capacitive behavior that is related to the occupation of  $\text{Li}^+$ , which give a semicircle and straight line perpendicular to  $Z_{Re}$  axis in the Nyquist plot (commonly below  $10^{-2}$  Hz), respectively.

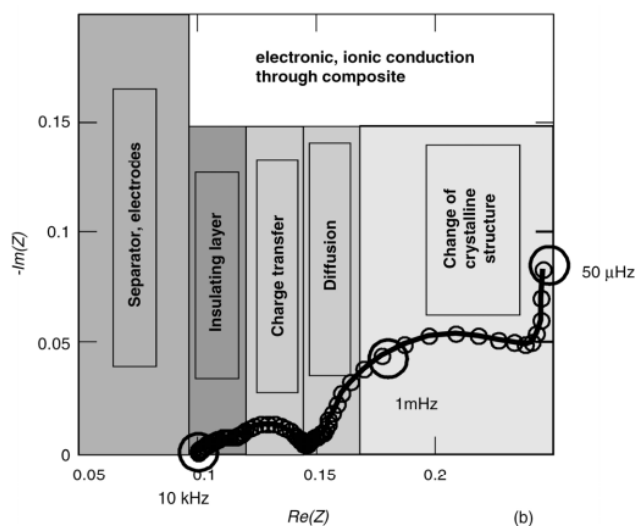


Figure 2.5. Typical electrochemical impedance spectra of intercalation electrode. [258]

In this thesis, the EIS of the half-cells (two electrode system) is performed at a bias voltage of 5 mV at room temperature with a VMP3 (BioLogic) in the frequency range of 10 kHz-10 mHz. Galvanostatic charge/discharge cycling tests are performed at a constant current density, using a battery analyser BCS-805 (BioLogic). The charge/discharge cycling tests are performed at different rates (C-rate) by battery analyser BCS-805 (BioLogic). All electrochemical measurements are performed at room temperature.

## Chapter 3:

# Characterizations of graphene and other two-dimensional materials

This chapter provides the detailed characterization of graphene, MoO<sub>3</sub>, MoS<sub>2</sub> flakes, SWNTs, MoO<sub>3</sub>/SWNTs, MoS<sub>2</sub>/C hybrids and BP. Different techniques are used in order to probe the physical and chemical properties of the samples. Optical absorption spectroscopy and OES is applied to estimate the concentration of graphene flakes in NMP and concentrations of BP in different solvents, respectively. The morphologies of the samples are characterized by using TEM (flake size), and AFM (thickness of flakes). The structural properties of all samples are revealed by Raman spectroscopy (diameter of SWNTs, thickness of flakes), high resolution-TEM (HRTEM) (inter-spacing of layers), and XRD (phase, orientation and thickness of flakes). In addition, XPS is carried out to assess the surface chemical composition of graphene after the solvent exchange process as well as to determine the oxidation stage of elements (Mo and S) in MoS<sub>2</sub> flakes after LPE process. TGA is performed to quantify the content of carbon on the MoS<sub>2</sub>/C hybrid. To measure the specific surface area of graphene flakes, I exploited BET. The energy dispersive X-ray spectroscopy is carried out to analyse the composition of BP flakes, whereas the EFTEM and EELS is exploited to evaluate the aging of BP flakes after exfoliation. The information obtained from the characterization techniques listed above enables a comprehensive evaluation of the material properties, which provide an insightful understanding of their electrochemical properties for applications in LIBs.

### 3.1. Graphene flakes

#### 3.1.1. Characterizations of graphene flakes in N-Methyl-2-pyrrolidone and ethanol

As mentioned in **chapter 2**, the graphene flakes are produced by LPE of graphite in NMP, followed by the exchange of graphene flakes from NMP to EtOH (section **2.1.3.1**). The graphene flakes in NMP and EtOH are characterized by means of OAS, TEM, Raman spectroscopy and XPS. Figure 3.1 plots the OAS of the graphene-based NMP ink. The absorption peak located at ~275 nm is attributed to inter-band electronic transitions from the unoccupied  $\pi^*$  states at the M point of the Brillouin zone. [260, 261] The concentration of the dispersions is determined according to the Beer Lambert law, as shown in equation 3.1: [241, 262]

$$A = \alpha cl \quad (3.1)$$

in which  $A$  is the absorbance;  $\alpha$  is the optical absorption coefficient ( $\text{L g}^{-1}\text{m}^{-1}$ );  $c$  is the concentration of the dispersed flakes;  $l$  is the path length of the cuvette in which the sample is contained.

Using the experimentally derived absorption coefficient of  $1390 \text{ L g}^{-1}\text{m}^{-1}$  at 660 nm, [202, 241] a concentration of graphitic flakes is estimated to be  $\sim 0.18 \text{ g L}^{-1}$ . Besides, the exchange of graphene flakes from NMP into EtOH [263] promotes the precipitation of the graphene flakes due to its low  $\gamma$  ( $22 \text{ mN m}^{-1}$ ) [241] with respect to the surface energy of graphene, [241] resulting in a metastable ink in EtOH. For the estimation of the concentration of the graphitic flakes in the EtOH-based ink, the average mass loading of the graphitic film (1 mg), after solvent evaporation at room temperature, is divided by a known volume ( $250 \mu\text{L}$ ) of the drop-cast EtOH-based ink onto the Cu foil. Following this procedure, a concentration of graphitic flakes is calculated to be  $\sim 5.6 \text{ g L}^{-1}$  in the EtOH-based ink. The low  $\gamma$  of EtOH ( $22 \text{ mN m}^{-1}$ ) [241] with respect to the surface energy of graphene ( $46.7 \text{ mN m}^{-1}$ ), [241] promotes the precipitation of the graphene flakes, resulting in a metastable ink in EtOH. The high concentration of the graphitic flakes in the EtOH-based ink enables the fabrication of anodes using a simple one-step process for LIB anode fabrication by directly drop-casting the as-obtained graphitic flakes onto a Cu foil followed by drying at room temperature.

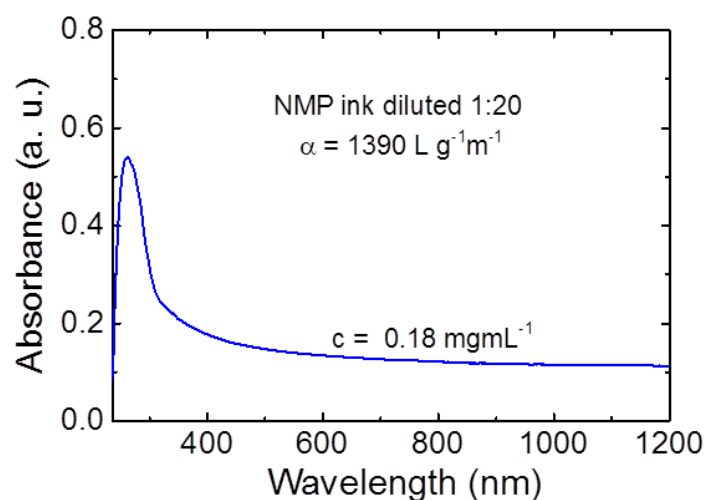


Figure 3.1. *Optical absorption spectra of the graphene ink in NMP.*

The morphological properties of the graphitic flakes dispersed in the NMP-based ink and in the EtOH-based ink are characterized by means of TEM and Raman spectroscopy. Transmission electron microscopy bright field images of the graphitic flakes before (NMP) and after the solvent exchange (EtOH) process are reported in Figure 3.2a and b, respectively. Both samples are formed by graphitic flakes with a lateral size ranging from 100 to 600 nm (see Figure 3.2c and d for statistical analysis). The statistical analysis demonstrates that the

solvent exchange process does not induce modification in the lateral size of the graphitic flakes. Electron diffraction patterns, shown in the insets of Figure 3.2a and b, collected on aggregated flakes indicate that the flakes are crystalline in both samples. All the rings are indexed as  $h, k, -h -k$ , and 0 reflections of a hexagonal lattice with  $a = 0.244(1)$  nm, in agreement with the graphite structure. [261]

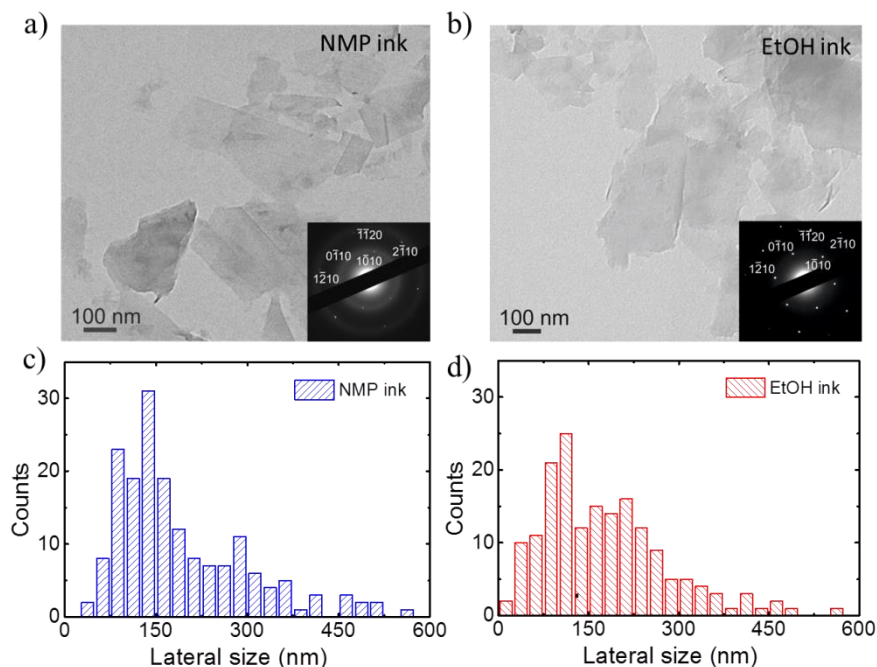


Figure 3.2. Bright- field TEM image of graphene flakes dispersed from the (a) NMP ink and (b) EtOH ink; the insets show the electron diffraction patterns collected on an area of 2 mm in diameter with the peaks labelled by Miller – Bravais indices. (c) and (d) are lateral size distribution, extracted by statistical analysis on TEM images, of graphitic flakes dispersed in NMP (blue) and after solvent exchange in EtOH (red).

Raman analysis is carried out in order to gain insight into the number of layers in the flakes and presence of defects. [264, 265] Figure 3.3a plots the typical Raman spectra of the graphite/graphene flakes deposited on Si/SiO<sub>2</sub> for both the NMP-based and the EtOH-based inks. In a typical Raman spectrum of graphene, the G peak corresponds to the E<sub>2g</sub> phonon at the Brillouin zone center; [265] the D peak is due to the breathing modes of the sp<sup>2</sup> rings and requires a defect for its activation by double resonance; [266-269] the 2D peak is the second order of the D peak. [266] For pristine graphene, the 2D peak has a single Lorentzian component, whereas it splits (upshifting also in position) for multi-layer graphene (MLG), reflecting the evolution of the band structure. [266, 270, 271] An estimation of the number of layers of the flakes can be derived from a statistical Raman analysis (based on 20 measurements for both NMP- and EtOH-based inks) of the full width at half maximum of the 2D peak (FWHM(2D)), see Figure 3.3b, the average position of the 2D peak (Pos(2D))

(Figure 3.3c) and the  $I(2D)/I(G)$  ratio (Figure 3.3d). For more details, the Raman spectra of both NMP and EtOH based-inks show that an average value of  $FWHM(2D)$  lower than  $70\text{ cm}^{-1}$ ,  $Pos(2D)$  around  $2700\text{ cm}^{-1}$  and the  $I(2D)/I(G)$  ratio higher than 0.5 (the value for graphite), [266] indicate that both samples are composed of a combination of SLG and FLG flakes. [202, 241, 262, 272] Additionally, the high  $I(D)/I(G)$  ratio (Figure 3.3e) is attributed to the edges of sub-micrometer flakes, [267] (see Figure 3.2) rather than to the presence of a large amount of structural defects within the flakes, otherwise the D peak would be much broader, and G and D' would merge in a single band. [265] Indeed,  $FWHM(G)$  always increases with defects. [265] As detailed in ref. [119, 273, 274] the lack of a clear correlation between  $I(D)/I(G)$  and  $FWHM(G)$  in both samples (Figure 3.3e) further supports the absence of structural defects also after the solvent exchange process.

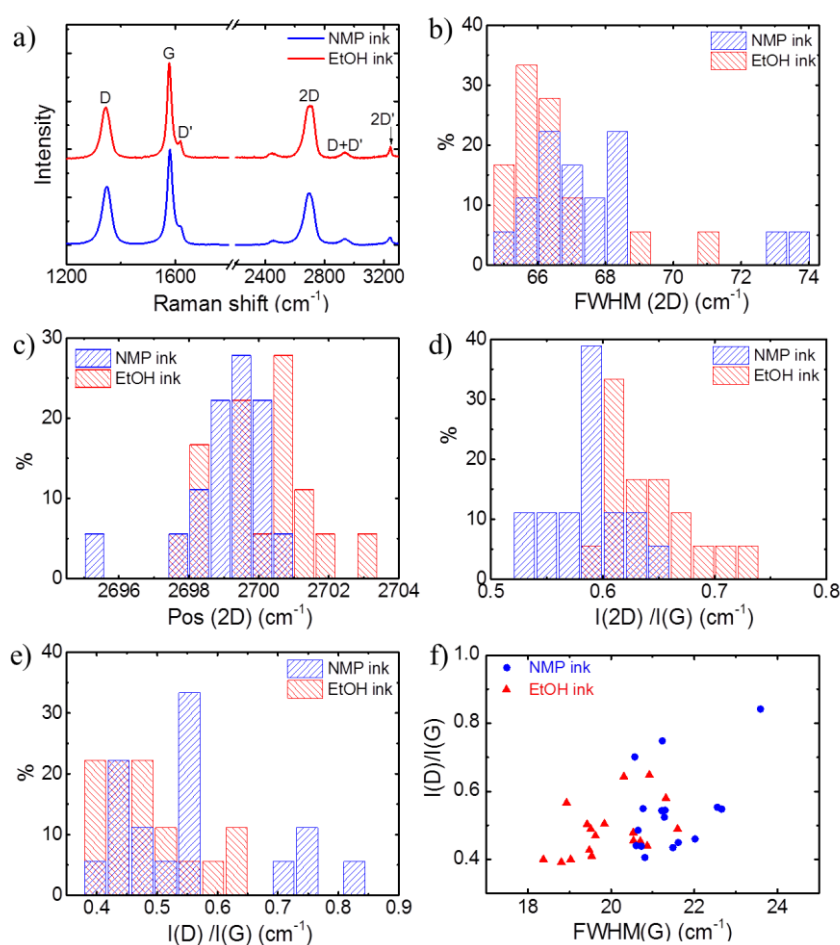


Figure 3.3. (a) Raman spectra at a  $532\text{ nm}$  excitation wavelength for representative flakes in the NMP ink (blue curve) and EtOH ink (red curve). Distribution of (b)  $FWHM(2D)$ , (c)  $Pos(2D)$ , (d)  $I(2D)/I(G)$ , and (e)  $I(D)/I(G)$ , and (f) distribution of  $I(D)/I(G)$  as a function of  $FWHM(G)$ , for the NMP ink (blue dashed histograms and dots) and EtOH ink (red dashed histograms and triangles), respectively.

In order to obtain information about the surface chemistry of the SLG/FLG-based films deposited before and after the solvent exchange process, the NMP and EtOH-based inks are investigated by XPS. The signal of C 1s and N 1s core-levels are focused to obtain information on the chemical state and the atomic bonding of the two elements (Figure 3.4).

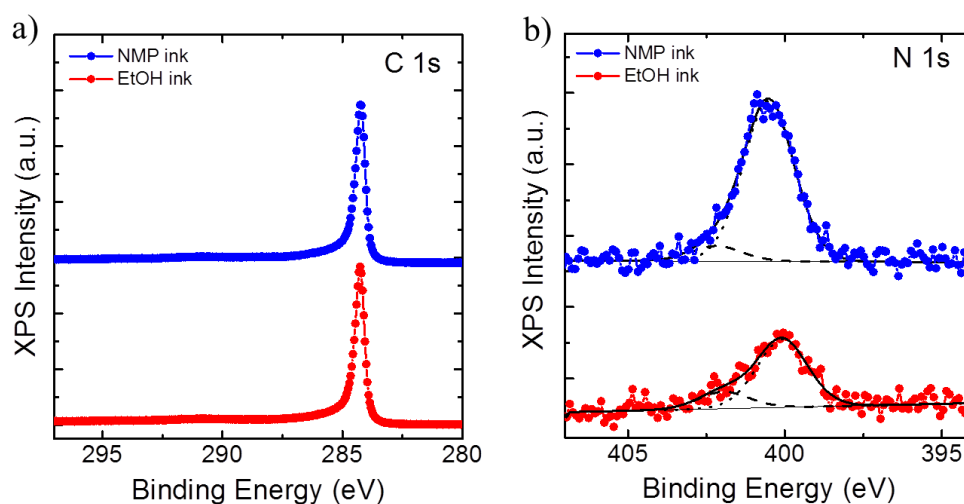


Figure 3.4. XPS data of the (a) C 1s and (b) N 1s core-levels acquired on graphene films obtained from NMP (blue curve) and EtOH (red curve) inks.

Indeed, the shape and position of the C 1s peak can provide information on the local environment and oxidation states of graphene, since binding energies are sensitive to the chemical environment. [3] The C 1s profiles collected on the two samples are reported in Figure 3.4a; in both cases, C 1s has an asymmetric shape with the C – C component centred at  $\sim 284.3$  eV, as typically reported for pristine graphene and graphite flakes. [275] The peak shape and the absence of a C – O component, usually centred at  $\sim 286.2$  eV, prove that the SLG and FLG flakes have not undergone oxidation during neither the exfoliation nor the solvent exchange process. [241, 276] As shown in Figure 3.4b, the N : C atomic ratio is 0.8 : 100 for the NMP ink, while it decreases to 0.4 : 100 after the solvent exchange process. For both NMP- and EtOH-based inks, the N 1s signal can be fitted with two components (Figure 3.4b). The main component (dotted profiles) is centred at  $400.3 \pm 0.3$  eV for both samples and can be assigned to pyrrolic N (*i.e.*, N coordinated as in the pyrrole molecule), [268] consistent with the presence of NMP molecules, [270, 277] likely trapped between the SLG and FLG flakes. [241] The pyrrolic N component accounts for  $\sim 90\%$  and  $\sim 80\%$  of the total N content of the SLG and FLG flakes in the NMP-based ink and in the EtOH-based ink, respectively. The second, minor component (dashed profiles) is centred at  $402.2 \pm 0.3$  eV, close to the position of the N peak observed in the related system of trimethylamine when adsorbed onto an electron acceptor substrate. [278] Therefore, this component is assigned to the N of the



NMP molecules adsorbed onto the SLG and FLG flakes. [279] In summary, the XPS analysis indicates that from one hand the solvent exchange process does not induce oxidation of the SLG and FLG flakes and from the other hand, it allows the removal of 50% of the NMP molecules adsorbed onto the SLG and FLG flakes, see Figure 3.4b. Such a small amount of residual NMP (less than 3.2 wt%, calculated from the N : C atomic ratio) demonstrates the feasibility of the proposed solvent exchange process for the NMP removal.

Briefly, the characterizations of graphene flakes in NMP and EtOH confirms that the solvent exchange process does not affect to the physical and chemical properties of the exfoliated flakes. Importantly, the Raman results indicate that both samples are composed of SLG and FLG flakes without defects on the basal planes. The high crystallinity of LPE graphene flakes is the key feature for assuring fast electron transport within LIB electrode.

### **3.1.2. Characterizations of graphene flakes having different lateral size and thickness**

The graphene flakes dispersion is firstly prepared via LPE of graphite in NMP, which contains a heterogeneous distribution of thin/thick and small/large lateral size graphitic flakes. [159, 280] A set of FLG and MLG flakes is obtained by means of SBS in centrifugal field, which are then used to prepare binder-free anodes. As reported in section 2.1.3.2, the obtained graphene flakes dispersions in NMP are ultra-centrifuged with different centrifugal speed, *e.g.*, 2000 rpm (769 g), 4000 rpm (3076 g), 10000 rpm (17100 g) and 30000 rpm (153700 g) corresponding Sample #1, #2, #3, and #4, respectively. Taking the advantage of the solvent exchange process, the NMP solvent in the four samples are exchanged by EtOH resulting in the four EtOH-based dispersions. The four NMP-based dispersions are firstly characterized by OAS to estimate the concentrations of the four samples before the exchange solvent process. As mentioned in section 3.1.1, the solvent exchange process does not affect to the physical and chemical properties of graphene flakes, so the four EtOH-based dispersions are characterized by TEM, AFM, XPS and Raman spectroscopy to observe the change in dimension of the graphene flakes according to the different centrifugal speeds. Figure 3.5 plots the OAS of the four NMP-based dispersions. The UV absorption peak located at ~268 nm is attributed to inter-band electronic transitions from the unoccupied  $\pi^*$  states at the M point of the Brillouin zone. [262] The concentration of the four dispersions in NMP are determined by OAS, using the experimentally derived absorption coefficient of  $1390 \text{ L g}^{-1}\text{m}^{-1}$  at 660 nm (considering that the scattering is negligible). [202, 241, 262] From Figure 3.5, the concentrations of the dispersions in Sample #1, #2, #3 and #4 in NMP are calculated to be 4.0, 2.4, 1.1 and  $0.1 \text{ g L}^{-1}$ , respectively. [241] The concentrations of the four dispersions decrease with the increase in centrifugal speed used for the preparation of the four samples.

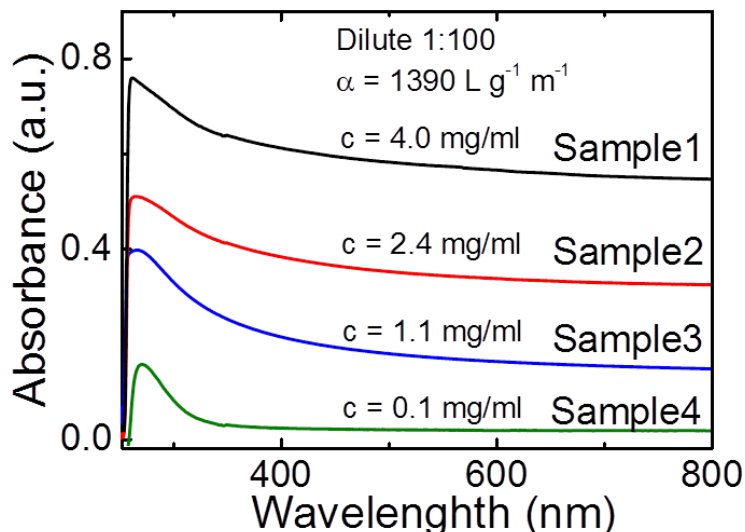


Figure 3.5. Room temperature optical absorption spectra of the FLG and MLG graphene dispersions. For the measurements the samples are diluted 1:100 with NMP.

The morphology of the samples is characterized by TEM and AFM analyses. The TEM images in Figure 3.6a and b show that the lateral size mode of the graphitic flakes decreases with the increase of the centrifugal force, passing from 380 nm to 75 nm, see Table 3.1. The XPS data of O 1s peaks and C 1s peaks is shown in Figure 3.7, giving surface chemical information for the FLG and MLG samples. As the flakes get smaller and thinner from

Table 3.1. Analysis of the four samples prepared at different ultracentrifugation speeds

	Centrifuge speed (rpm)	Average lateral size (nm)	Average thickness (nm)	Surface area (m <sup>2</sup> g <sup>-1</sup> )	O/C ratio
<b>Sample#1</b>	2000	380	20	114 ± 11	0.045
<b>Sample#2</b>	4000	180	10	236 ± 24	0.059
<b>Sample#3</b>	10000	120	5	317 ± 32	0.085
<b>Sample#4</b>	30000	75	2	414 ± 41	0.110

The AFM results shown in Figure 3.6c and d, demonstrate that both Sample#3 and #4 have narrower thickness distributions with respect to sample#1 and #2, *e.g.*, centered at 5 nm and 2 nm, respectively, (see Table 3.1). Accordingly, Sample#1 and #2 are mostly constituted by thick (20–50 layers) MLG flakes, while Sample#3 is composed of thinner MLG (10–15 layers) and Sample#4 comprised of FLG flakes. As also presented in Table 3.1, the surface area (SA) data obtained from BET measurement clearly demonstrate an increment of their

values (SA from  $114 \pm 11$  to  $414 \pm 41 \text{ m}^2 \text{ g}^{-1}$ ) passing from Sample#1 to Sample#4, respectively.

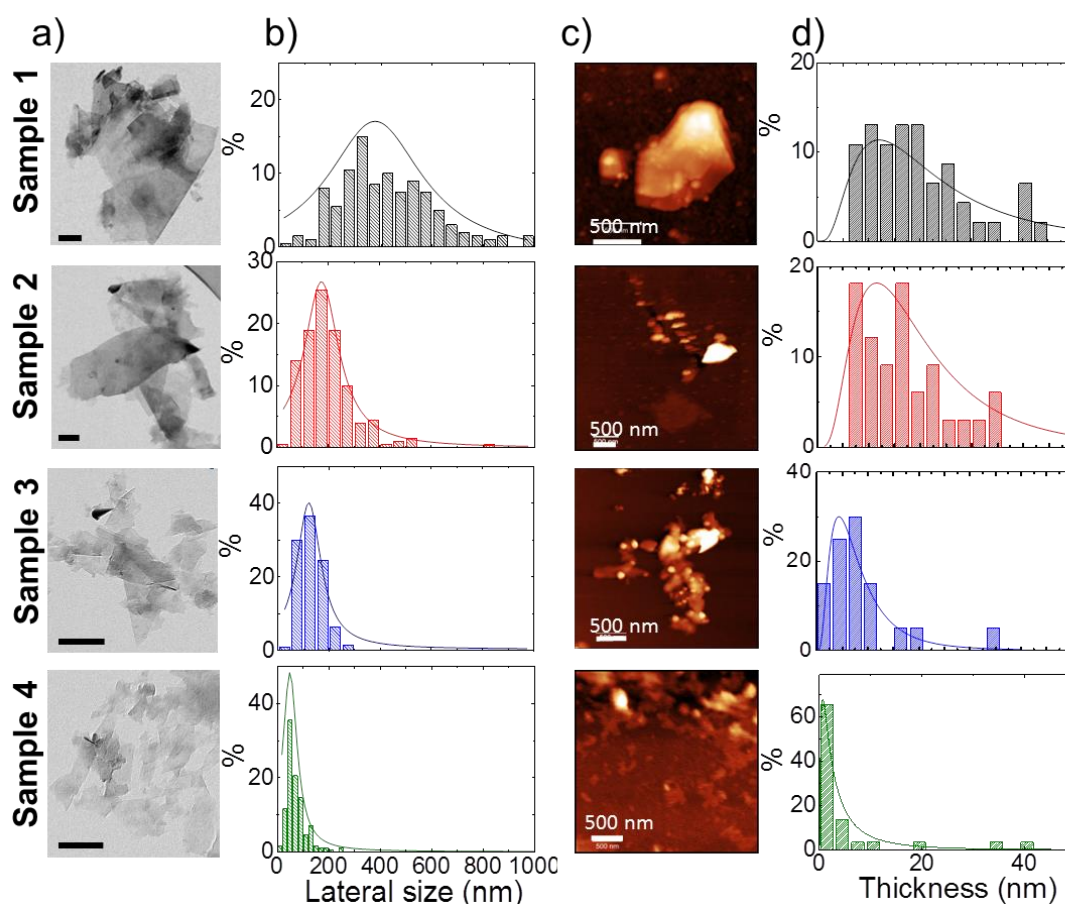


Figure 3.6. Morphological analysis of the four samples, (a) Representative TEM images and (b) lateral size distribution of graphene flakes (black, Sample #1), (red, Sample #2), (blue, Sample #3), (green, Sample #4) showing a decreasing average distribution with maxima at 380 nm, 180 nm, 120 nm and 75 nm, respectively. The TEM scale bars are 100 nm. (c) Representative AFM images and (d) thickness distribution of the four as-produced samples.

Sample #1 to Sample #4, the intensity of the oxygen peak on the O 1s region is increasing. The increase of oxygen presence in the smaller/thinner samples (Sample #3 and Sample #4), with respect to the larger/thicker ones (Sample #1 and Sample #2) is linked with the morphology of the flakes: Sample #3 and Sample #4 having more edges than Sample #1 and Sample #2 have consequently more active sites for the O attachment. The position of the XPS O 1s peak is at  $532.1 \pm 0.2 \text{ eV}$ , assigned to C-O moieties, in agreement with data reported in NIST XPS database (version 4.1). [281] Concerning the C 1s region, the four samples show similar C profile, characterized by an intense asymmetric peak centered at  $284.5 \pm 0.2 \text{ eV}$ . [3] It is worth to notice that C 1s profiles of the four samples differ in the 285~287 eV region, see inset in Figure 3.7b. In this region, the contribution of C-O moieties is expected (usually reported at  $286.2 \pm 0.2 \text{ eV}$ ). [282] In agreement with the O 1s results, the C signal in this

region is increasing from Sample #1 to Sample #4. The O/C ratio is calculated from XPS analysis, demonstrating that the increase in dimension of graphene flakes results in the increase in O/C ratio, see Table 3.1.

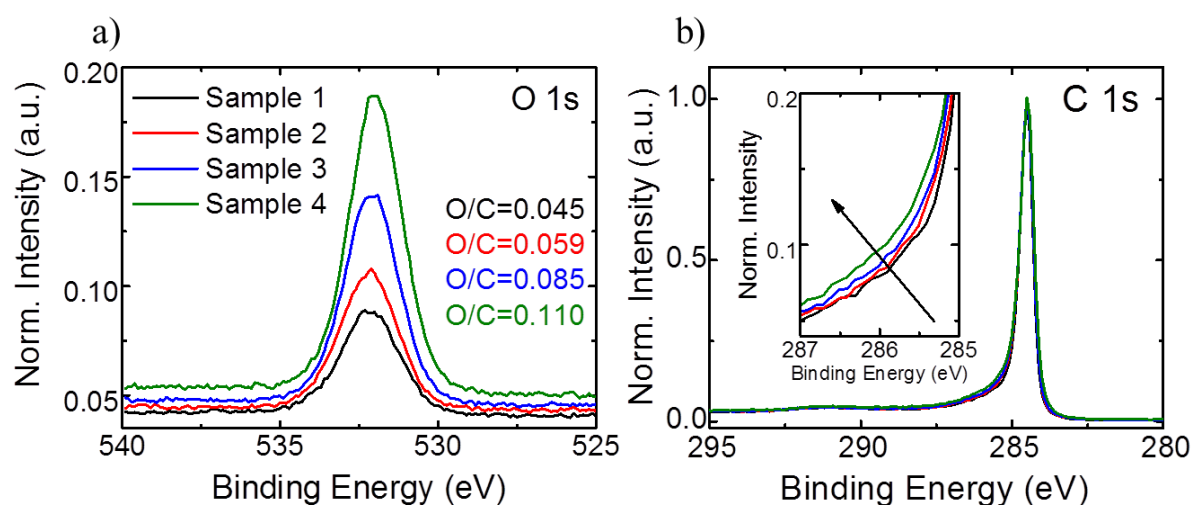


Figure 3.7. XPS spectra of the four samples deposited onto a Cu substrate after normalization of the carbon signal. (a) O 1s peaks and (b) C 1s peaks. Inset: close up of the 285-287 eV range.

The comparison of the Raman spectra of the as-prepared samples with that of graphite (Figure 3.8a) illustrates the evolution of the G, D and 2D peaks. There is an increase of both D and D' peaks intensity when passing from Sample #1 to Sample #4, which could be explained assuming an increase of defects, coupled with the reduction of FWHM(2D). The reduction of FWHM(2D) in turn indicates a decrease in the thickness of the flakes, [283] namely in the reduction of the number of layers of the initial graphite flakes. To corroborate these data, a statistical analysis is carried out. Figure 3.8b shows that the FWHM(2D) varies from 71 to 89  $\text{cm}^{-1}$  (Sample #1), 65 to 80  $\text{cm}^{-1}$  (Sample #2), 65 to 78  $\text{cm}^{-1}$  (Sample #3) and 65 to 75  $\text{cm}^{-1}$  (Sample #4), demonstrating the thickness reduction with the increase in centrifugal force.

The distribution between the  $I(2D)/I(G)$  is reported in Figure 3.8c, with integral intensity ratios, which range from 0.53-0.59 for Sample #1, 0.55-0.62 for Sample #2, 0.59-0.65 for Sample #3 and 0.63-0.77 for Sample #4. The progressive increase of the ratios, combined with the narrowing of FWHM(2D), suggests that the thickness of the flakes effectively decreases with the increase of the centrifugal force. The statistical analysis shows that Samples #1, #2 and #3 are composed by MLG, while Sample #4 mostly contains FLG flakes, in agreement with AFM data reported in Figure 3.5c-d. Besides, the analysis of  $I(D)/I(G)$  as a function of FWHM(G), and  $\text{Disp}(G)$ , shown in Figure 3.8d and Figure 3.9, respectively, allows to discriminate between disorder localized at the edges and disorder in the bulk. [265]

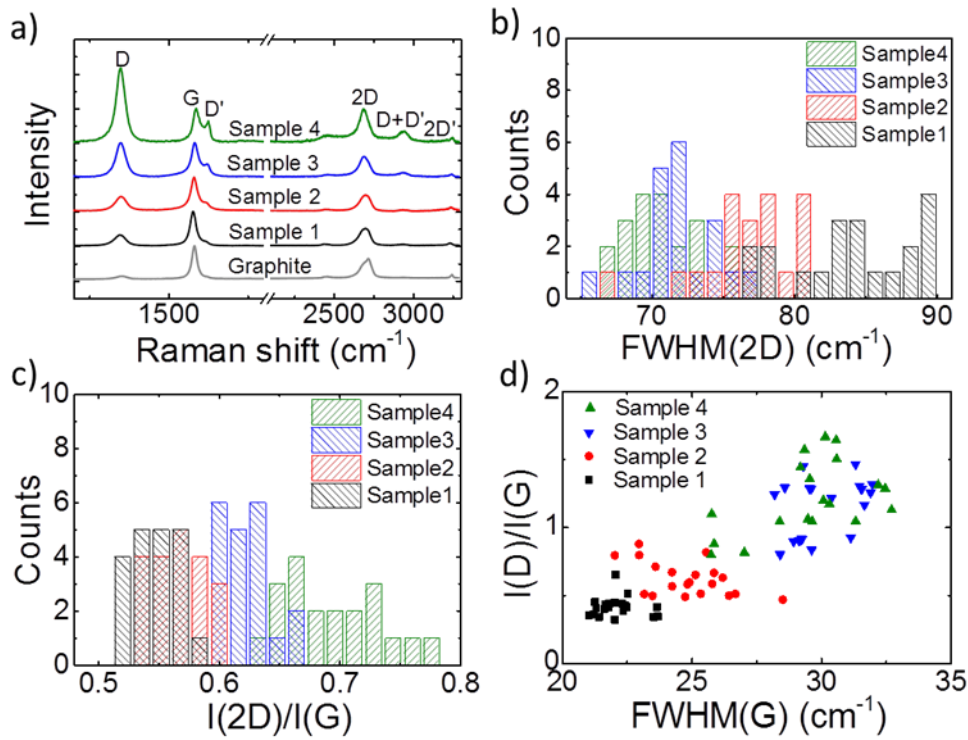


Figure 3.8. Representative Raman spectra excited at 532 nm excitation wavelength for (a) the four graphene-based samples. Statistical distribution of (b) FWHM(2D), (c)  $I(2D)/I(G)$  and (d)  $I(D)/I(G)$  vs. FWHM(G) are also shown.

In the latter case, a higher  $I(D)/I(G)$  would correspond to higher FWHM(G) and dispersion of the G peak (Disp(G)). Figure 3.8d and Figure 3.9 show that  $I(D)/I(G)$  is not correlated with both FWHM(G) and Disp(G). Moreover, the Disp(G) values (Figure 3.9) for all the samples are lower than  $0.1 \text{ cm}^{-1} \text{ nm}^{-1}$ , *e.g.*, the value expected for disordered carbons. [265] This is a proof that there is no in-plane defect caused during the exfoliation treatment, and the major contribution to the D peak comes from the sample edges, confirming that the LPE procedure does not introduce defects on the basal plane of the flakes.

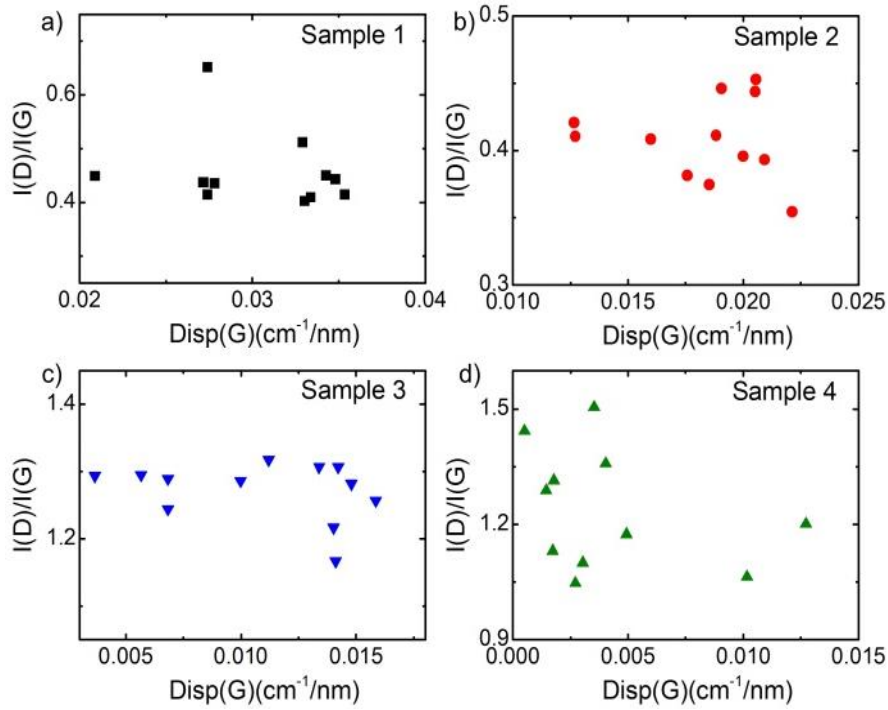


Figure 3.9.  $I(D)/I(G)$  as a function of  $Disp(G)$ . (a) Sample #1, (b) Sample #2, (c) Sample #3 and (d) Sample #4.

In summary, the characterizations of the four samples confirm the efficient SBS process to sort defect-free graphene flakes by lateral size (from 380 to 75 nm) and thickness (from MLG to 2 nm FLG). The obtained results are essential for the further explanations of the electrochemical behaviors of graphene anodes based on FLG and MLG flakes, which will be reported in **chapter 4**.

### 3.2. Single wall carbon nanotubes

The dispersion of SWNTs in IPA is firstly characterize by optical absorption spectroscopy to point out various properties of SWNTs dispersions such as transition energies, [284, 285] bundling, [286] and concentration. [287] The OAS measurements of SWNT samples are carried out in the 400-1300 nm range. This range is sufficient to cover the second and third excitonic transitions of semiconducting SWNTs (s-SWNTs), i.e.,  $eh_{22}$  and  $eh_{33}$ , respectively, and the first of the metallic SWNTs (m-SWNTs), i.e.,  $M_{11}$ . [288, 289] The assignment of the optical transitions is based on the empirical Kataura plot. [290] This gives values of optical transition frequencies versus chirality for SWNTs in IPA dispersions, and is more appropriate than Kataura plots theoretically derived from tight binding and other models. [291] The OAS of SWNTs (Figure 3.10a) shows the  $M_{11}$ , the  $eh_{22}$  and  $eh_{33}$  regions.

Raman spectroscopy can be used to probe SWNTs structure within dispersions, see Figure 3.10b. In the low frequency region, the Radial Breathing Modes (RBMs) are observed. [292]

Their position,  $Pos(RBM)$ , is inversely related to the SWNTs diameter,  $d$ , [293-295] as given by Equation 3.2:

$$Pos(RBM) = \frac{C_1}{d} + C_2 \quad (3.2)$$

Combining  $Pos(RBM)$ , with excitation wavelength and the Kataura plot, [288] it is, in principle, possible to derive the SWNTs chirality. [296, 297]

Matching the diameter with excitation wavelength in the Kataura plot also gives information on the semiconducting or metallic character. A variety of  $C_1$  and  $C_2$  have been proposed for this relation. [285, 286, 288, 297] Here, we use the  $C_1=214.4 \text{ cm}^{-1} \text{ nm}$  and  $C_2=18.7 \text{ cm}^{-1}$ , from Ref. [298]. These were derived by plotting the resonance energy as a function of inverse RBM frequency without additional assumptions. The results are validated by using the parameters proposed in Refs. [284, 287, 299]

Raman spectroscopy also probes possible damage via the  $D$  peak. [283] The latter is due to the breathing modes of  $sp^2$  rings and requires a defect for its activation by double resonance. [266, 300] The typical Raman spectrum of SWNTs in the  $1500\text{-}1600 \text{ cm}^{-1}$  region consists of the  $G^+$  and  $G^-$  bands. In s-SWNTs, they originate from the longitudinal (LO) and tangential (TO) modes, respectively, derived from the splitting of the  $E_{2g}$  phonon of graphene at the Brillouin zone centre. [265, 301] The positions of the  $G^+$  and  $G^-$  peaks,  $Pos(G^+)$ ,  $Pos(G^-)$ , are diameter dependent and their separation increases with decreasing diameter. [302, 303] In m-SWNTs, the assignment of the  $G^+$  and  $G^-$  bands is the opposite, and the FWHM of the  $G^-$  peak,  $FWHM(G^-)$ , is larger and  $Pos(G^-)$  down-shifted with respect to the semiconducting counterpart. [292, 304] Thus, a wide, low frequency  $G^-$  is a fingerprint of m-SWNTs. The absence of such a feature does not necessarily imply that only s-SWNTs are present, but could signify that m-SWNTs are off-resonance.

Doping could also modify positions and FWHMs. [305, 306] In m-SWNTs, a  $Pos(G^-)$  blue-shift, accompanied by a  $FWHM(G^-)$  decrease is observed with electron or hole doping. [271, 307] In s-SWNTs, doping upshifts  $Pos(G^+)$ , but does not affect  $FWHM(G^+)$ . [290, 295] Thus, a large number of excitation wavelengths are necessary for a complete characterization of SWNTs. [262, 305] Nevertheless; useful information can be derived even with few excitation wavelengths.

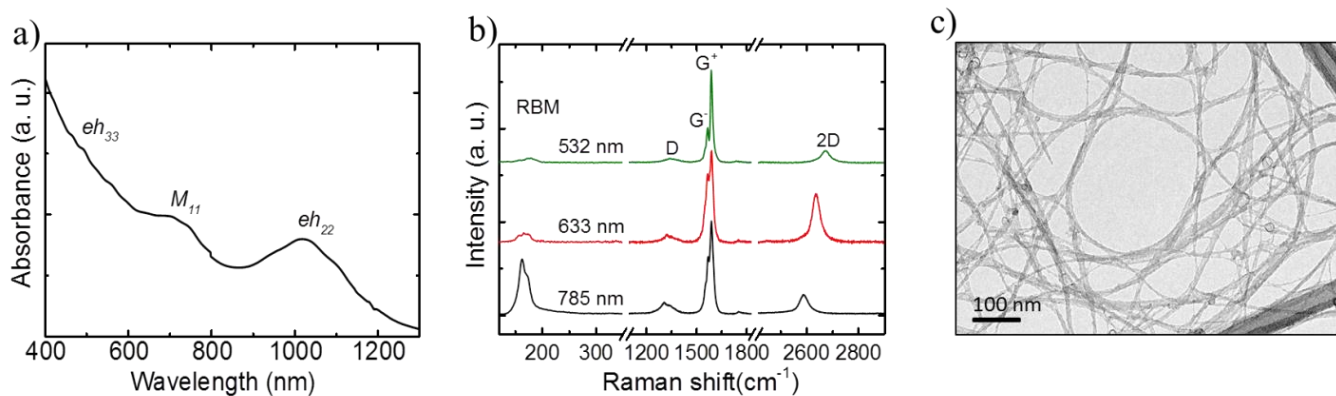


Figure 3.10. (a) Absorption spectrum of SWNTs. The labels  $eh_{22}$ ,  $eh_{33}$  and  $M_{11}$  refer to the second and third semiconducting and the first metallic excitonic transition. The spectra are normalized for a clear visualization. (b) Raman spectrum of pristine SWNTs. (c) Bright-field TEM images of pristine SWNTs.

The Raman spectra of the SWNTs in the RBM region reported in Figure 3.10b show a distribution in the  $100\text{--}200\text{ cm}^{-1}$  range. This RBM range corresponds to SWNTs with  $\sim 1.37\text{--}1.45\text{ nm}$  diameter. The Raman spectra in the D and G region of SWNTs, show a weak D band (*i.e.*,  $I(D)/I(G) \sim 0.05$ ), indicating a low number of defects, which could be linked with residual amorphous carbon from the synthesis process. [289, 291, 308]

The morphology of SWNTs is analysed by TEM. As shown in Figure 3.10c, from the TEM image of pristine SWNTs sample, it is possible to see the SWNTs aggregated in bundles, having a length exceeding the micrometre.

The characterizations of SWNTs provide the fundamental understanding about their physical properties, *e.g.*, diameters, defects and types of SWNTs (metallic or semiconducting) so that we can apply SWNTs for the proper applications. In this thesis, the SWNTs are used not only to improve the electrical conductivity of  $\text{MoO}_3/\text{SWNTs}$  electrode but also to buffer the volume change of  $\text{MoO}_3$  flakes during lithiation and de-lithiation. The detail information of  $\text{MoO}_3/\text{SWNTs}$  electrodes will be provided in section 3.3.

### 3.3. Molybdenum trioxide nanosheets and single wall carbon nanotube-bridged molybdenum oxide hybrid

The synthesis of the  $\text{MoO}_3/\text{SWNTs}$  hybrids for LIB anode starts with the solution processing of the two materials. The  $\text{MoO}_3$  flakes obtained by LPE of bulk  $\text{MoO}_3$ , see section 2.1.3.3, are characterized by TEM and Raman spectroscopy. The as-produced  $\text{MoO}_3$  and SWNTs dispersions are then mixed to form hybrid structures of known weight percentage. The morphology of as-prepared  $\text{MoO}_3/\text{SWNTs}$  hybrid is characterized by TEM.



The structural properties of MoO<sub>3</sub> flakes are further carried out by Raman spectroscopy. As shown in Figure 3.11a, the Raman spectrum shows all typical peaks of MoO<sub>3</sub> in the 100-1200 cm<sup>-1</sup> range. The peak at 995 cm<sup>-1</sup> is attributed to terminal oxygen stretching mode (Mo=O) which results from unshared oxygen, [309] whereas the peak at 818 cm<sup>-1</sup> is assigned to the intermediate bridging O–Mo–O bonds, [310] which results from corner-shared oxygens in common to two MoO<sub>6</sub> octahedral. This peak shows a shift of 7 cm<sup>-1</sup> with respect to other MoO<sub>3</sub> reports. [311, 312] This shift is attributed to the coordination of oxygen atoms with other atoms *e.g.*, hydrogen. [210, 310]

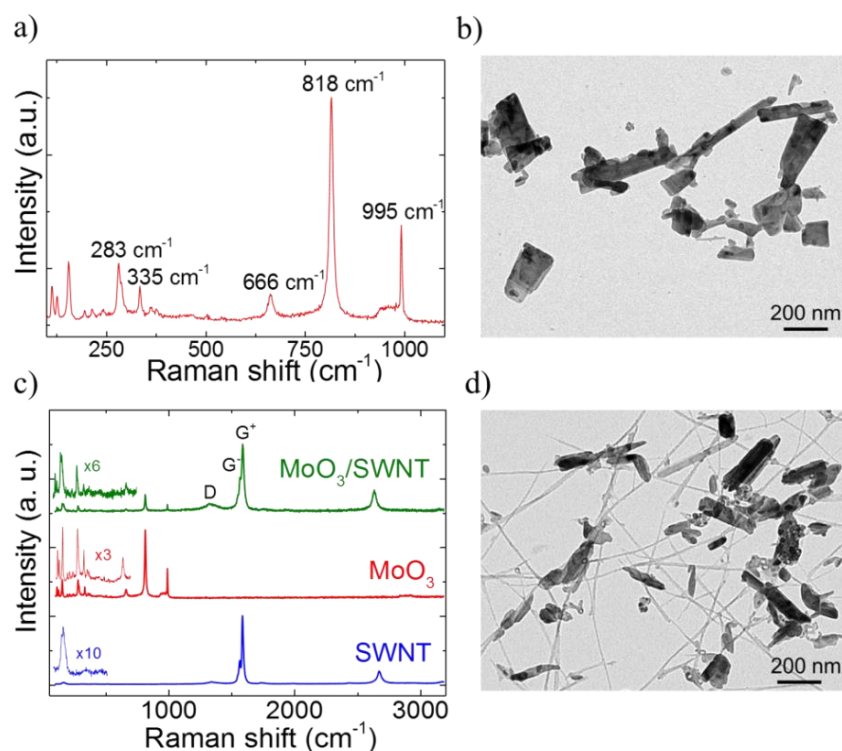


Figure 3.11. (a) Raman spectrum of MoO<sub>3</sub>, (b) Bright-field TEM image of MoO<sub>3</sub> flakes dispersed in IPA, (c) Raman spectrum of SWNTs, MoO<sub>3</sub> flakes and MoO<sub>3</sub>/SWNTs hybrid and (d) Bright-field TEM image of MoO<sub>3</sub>/SWNTs hybrid dispersed in IPA.

The peak at 666 cm<sup>-1</sup> is assigned to Mo<sub>3</sub>–O stretching mode caused by edge-shared oxygen atoms. [310, 313] The peaks located in the 200 - 400 cm<sup>-1</sup> range are attributed to the bending modes of MoO<sub>3</sub>. [4] In particular, the peaks at 375 and 365 cm<sup>-1</sup> are scissor modes of O–Mo–O, the peak at 335 cm<sup>-1</sup> is a bending mode of O–Mo–O, and the 283 cm<sup>-1</sup> and 244 cm<sup>-1</sup> peaks are due to the wagging and twisting modes of O=Mo=O, respectively. [310-313] Finally, the peak at 156 cm<sup>-1</sup> is due to the translation of the ridged chains along the z axis. [314] The morphology of the as-produced MoO<sub>3</sub> are analyzed by TEM. Figure 3.11b shows MoO<sub>3</sub> flakes with lateral sizes ranging from 50 to 300 nm. The Raman spectra of MoO<sub>3</sub>, SWNTs and MoO<sub>3</sub>/SWNTs samples are shown in Figure 3.11c. The spectra are normalized to the signal of G<sup>+</sup> peak of the SWNTs. The spectrum of MoO<sub>3</sub>/SWNTs sample shows the

intensities of Raman peaks of MoO<sub>3</sub> in the region of 200-1000 cm<sup>-1</sup> decrease with respect to the G<sup>+</sup> peak of the SWNTs due to their high Raman cross section. [315-317] The TEM image of hybrid MoO<sub>3</sub>/SWNTs sample (see Figure 3.11d), clearly shows the bundles of SWNTs acting as bridges to connect isolated MoO<sub>3</sub> flakes, forming an interconnected network in the mixture material of MoO<sub>3</sub>/SWNTs. This structure is expected to bring the benefits of SWNTs to improve the electrical conductivity of electrode and prevent the volume change of MoO<sub>3</sub>.

In short, the brief characterizations of morphology properties of MoO<sub>3</sub> flakes and MoO<sub>3</sub>/SWNTs hybrid have shown the promising role of SWNTs in the hybrid structure. The network formed by SWNTs is expected to improve the electrical conductivity of electrode as well as to prevent the volume change of MoO<sub>3</sub> flakes. Also, the LPE of bulk MoO<sub>3</sub> is able to produce the MoO<sub>3</sub> flakes with lateral size ranging from 50-300 nm, bringing the benefit of nanostructure for LIB anode (as mentioned in section 1.3).

### **3.4. Molybdenum disulfide flakes and molybdenum disulfide/amorphous carbon hybrids**

#### **3.4.1. Molybdenum disulfide flakes**

Similar to LPE graphene, NMP is found to be one of the most effective solvents for LPE of MoS<sub>2</sub>, [150, 248]. However, as mentioned in section 2.1.2, NMP shows issues related to environment and electrode fabrication, which can limit the development of LIB technology. In the case of MoS<sub>2</sub>, the exfoliation of bulk MoS<sub>2</sub> in NMP results in the presence of superficial oxidized Mo species because the self-oxidation of NMP creates the formation of hydro peroxides, which oxidize MoS<sub>2</sub>. [239] These oxidized Mo species can change the composition of electrode materials, leading to side electrochemical reactions during the cycling of battery. To address these limitations and implement MoS<sub>2</sub> flakes in the fabrication of LIB anode, the LPE of bulk MoS<sub>2</sub> is carried out in an environmentally friendly and low-b.p. solvent, *e.g.*, IPA, see section 2.1.3.4.

The TEM images (Figure 3.12a) and the statistical analysis of the size distribution (the inset in Figure 3.12a) indicate that the exfoliated MoS<sub>2</sub> has lateral size mode of ~ 90 nm. The HR-TEM (Figure 3.12b) reveals the presence of few-layer MoS<sub>2</sub> flakes. The thickness of exfoliated MoS<sub>2</sub> flakes is characterized by AFM, see Figure 3.12b and c. The thickness distribution of MoS<sub>2</sub> flakes exfoliated in IPA peak at 3 nm, corresponding to ~ 4 stacked MoS<sub>2</sub> layers, see Figure 3.12c. To probe the structural property of exfoliated MoS<sub>2</sub>, Raman spectroscopy is carried out on bulk and exfoliated MoS<sub>2</sub>. Figure 3.12e shows the Raman spectra of bulk MoS<sub>2</sub>, the two dominant peaks centered at ~ 379 cm<sup>-1</sup> and 405 cm<sup>-1</sup>, corresponding to the E<sup>1</sup><sub>2g</sub> (in-plane vibration of Mo-S bonds) and A<sub>1g</sub> (out-plane vibration of

Mo-S bonds) modes, respectively. [318, 319] For the exfoliated MoS<sub>2</sub>, the E<sub>2g</sub><sup>1</sup> and A<sub>1g</sub> modes appear at ~ 382 cm<sup>-1</sup> and 407 cm<sup>-1</sup>, respectively. The Raman shift differences between these two peaks are 26 and 25 cm<sup>-1</sup> for bulk MoS<sub>2</sub> and exfoliated samples, respectively. [319-321] The decrease in MoS<sub>2</sub> layers is associated to the red-shift of the A<sub>1g</sub> peaks because the van der Waals force between two MoS<sub>2</sub> layers facilitate the atom vibration. The E<sub>2g</sub><sup>1</sup> peak exhibits blue-shift due to the long-range coulombic interlayer interactions. Therefore, Raman shift difference between E<sub>2g</sub><sup>1</sup> and A<sub>1g</sub> peaks in the case of MoS<sub>2</sub> (25 cm<sup>-1</sup>) is lower than that of bulk MoS<sub>2</sub>, suggesting the decrease in number of MoS<sub>2</sub> layers. [318, 319] Interestingly, the E<sub>2g</sub><sup>1</sup> and A<sub>1g</sub> peaks blue-shifts with respect to the bulk MoS<sub>2</sub>. This observation is similar to the cases of chemical-assisted exfoliation of MoS<sub>2</sub>, which is attributed to the adsorption of surfactants, intercalation agents or solvent molecules on the surface of MoS<sub>2</sub> flakes. [322-324] The crystalline structures of bulk MoS<sub>2</sub> and the exfoliated MoS<sub>2</sub> are also studied by XRD analysis (Figure 3.12f). The diffraction patterns of the bulk MoS<sub>2</sub> and exfoliated MoS<sub>2</sub> show strong, sharp peaks at 2θ = 14.4°, 32.7°, 39.6°, 44.2°, 49.8°, 58.4°, 60.4°, which correspond to the (002), (100), (103), (006), (105), (110) and (008) planes of the hexagonal MoS<sub>2</sub> phase, respectively (JCPDS 37-1492). [163, 325] In particular, the distinct diffraction peak (002) at 2θ = 14.4° is characteristic of the ordered stacking of S-Mo-S layers, so the change in intensity of this peak can be associated with the thickness of MoS<sub>2</sub>. [218, 326] However, the exfoliation of bulk MoS<sub>2</sub> does not affect the intensity of various peaks of MoS<sub>2</sub> flakes, *e.g.*, (100), (103), (105), (110) planes, which are not orientated along the c-axis. Thus, the change in intensity of (002) can be evaluated by calculating the intensity ratio of (002) and (100) diffraction peaks (I<sub>(002)</sub>/I<sub>(100)</sub>). [218, 327] The XRD patterns of both materials are normalized according to the (002) diffraction peak for the realization of the change in intensity of (002) diffraction peak of exfoliated MoS<sub>2</sub> flakes with respect to bulk MoS<sub>2</sub>. The I<sub>(002)</sub>/I<sub>(100)</sub> ratios are calculated to be 4.94 and 2.08 for bulk MoS<sub>2</sub> and exfoliated MoS<sub>2</sub>, respectively. It confirms the decrease in the crystallite size in the z direction (thickness). [172, 328, 329] Moreover, the size of crystallites is inversely proportional to the FWHM of the diffraction peaks according to Scherrer equation, see equation 3.3. [215, 221] The FWHM of (002) diffraction peak of exfoliated MoS<sub>2</sub> (0.44°) is wider than that of bulk MoS<sub>2</sub> (0.30°), suggesting that thickness of MoS<sub>2</sub> flakes are decreased after the LPE process. [218, 221, 329] These indications from XRD patterns are in agreement with the TEM, HR-TEM, AFM and Raman analysis (Figure 3.12a, b, c and d), confirming the LPE process provides smaller and thinner MoS<sub>2</sub> flakes with respect to its bulk counterpart.

$$\tau = \frac{K \lambda}{\beta \cos \theta} \quad (3.3)$$

where  $\tau$  is the mean size of the crystallites,  $K$  is the dimensionless shape factor (0.9),  $\lambda$  is the X-ray wavelength;  $\beta$  is the line broadening at FWHM and  $\theta$  is the Bragg angle (in degrees).

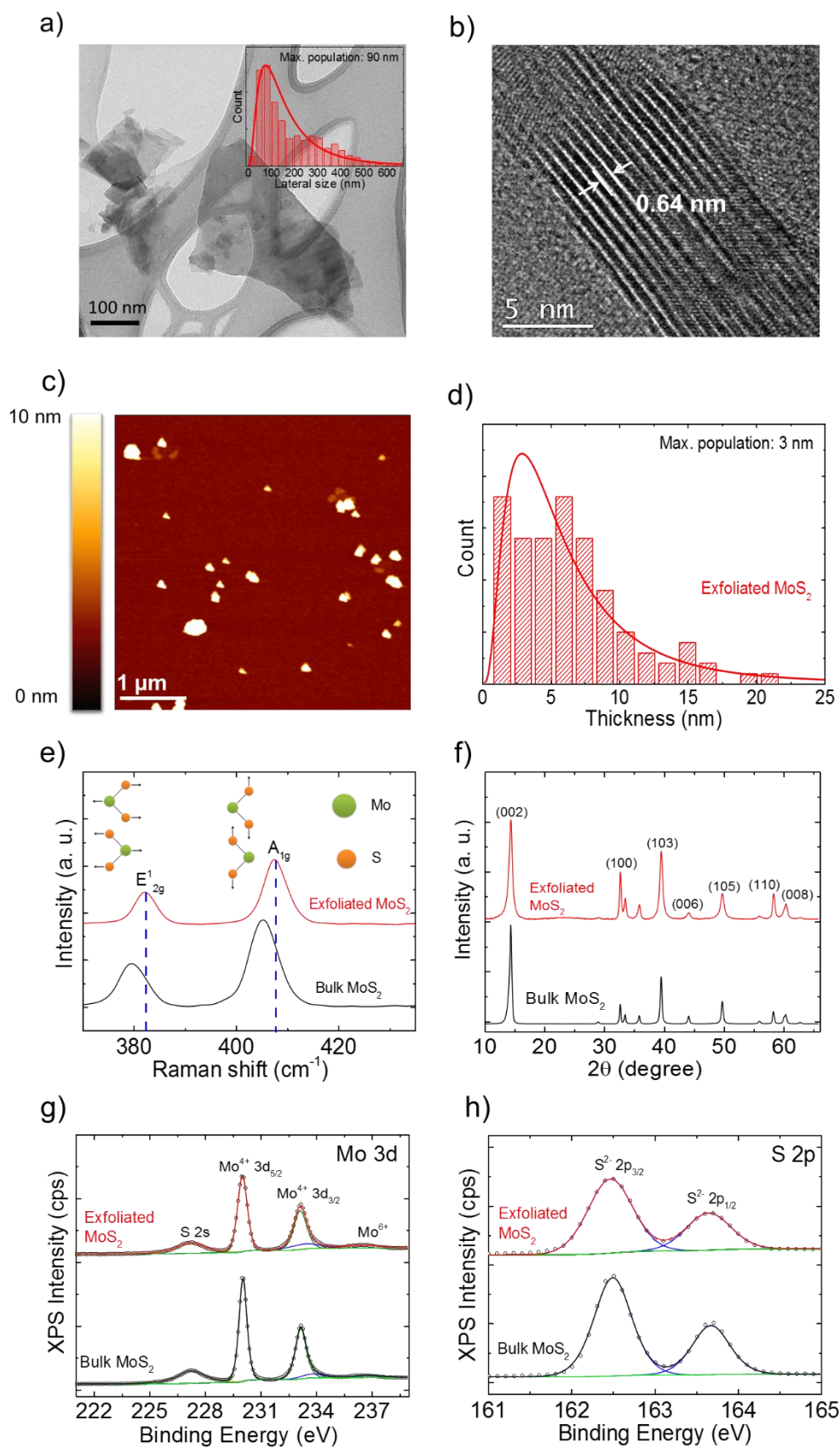


Figure 3.12. (a) Transmission electron microscopy image of exfoliated MoS<sub>2</sub>; the inset shows lateral size distribution, (b) High resolution-TEM image of exfoliated MoS<sub>2</sub>, (c) Atomic force microscopy images of exfoliated MoS<sub>2</sub> and (d) its corresponding thickness distribution, (e) Raman spectra of bulk and exfoliated MoS<sub>2</sub>, (f) X-ray diffraction patterns of bulk and exfoliated MoS<sub>2</sub>, high resolution-XPS spectra for (g) Mo 3d and (h) S 2p of bulk and exfoliated MoS<sub>2</sub>.

The chemical content in MoS<sub>2</sub> before and after LPE process is analyzed by the XPS. In the XPS spectra of Mo 3d in bulk and exfoliated MoS<sub>2</sub> samples (Figure 3.12g), two peaks at 229.5 and 232.7 eV, are assigned to 3d<sub>5/2</sub> and Mo 3d<sub>3/2</sub> binding energies of Mo<sup>4+</sup>, respectively, confirming the composition of MoS<sub>2</sub>. [215, 330] The peak at 227.2 eV is ascribed to the 2s binding energies of S atoms in the MoS<sub>2</sub>. [330, 331] The peak of Mo<sup>6+</sup> is observed in both XPS spectra of bulk and exfoliated MoS<sub>2</sub>, the presence of which in case of bulk MoS<sub>2</sub> can be caused by partial surface oxidation of bulk MoS<sub>2</sub> by oxygen/water in air. Additionally, there is no change in intensity of the Mo<sup>6+</sup> peaks in both XPS spectra of bulk and exfoliated MoS<sub>2</sub>, suggesting that the chemical structure of MoS<sub>2</sub> is not affected by the LPE process. [239] Figure 3.12h shows the XPS spectra of S 2p bulk and exfoliated MoS<sub>2</sub> samples, in which two peaks located at 162.5 and 163.7 eV correspond to 2p<sub>3/2</sub> and 2p<sub>1/2</sub> binding energies of S<sup>2-</sup> in MoS<sub>2</sub>, respectively.[215, 332] By quantitative analysis of the XPS data over binding energy regions of Mo 3d and S 2p in both bulk and exfoliated MoS<sub>2</sub> samples, the Mo:S ratios in the two samples are estimated to be 1:1.9. This result indicates that the influence of the exfoliation process on the stoichiometry MoS<sub>2</sub> is negligible.

### 3.4.2. Molybdenum disulfide/amorphous carbon hybrids

As reported in section 2.2.2, the MoS<sub>2</sub>/PAA mixtures are formed by solution mixing of the exfoliated MoS<sub>2</sub> flakes and PAA in IPA. The MoS<sub>2</sub>/C samples are formed by a thermal decomposition process of PAA. The MoS<sub>2</sub>/C powders named as MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2, and MoS<sub>2</sub>/C-3 corresponding to the different weight ratios of MoS<sub>2</sub>/PAA as 1:1, 1:2 and 1:4, respectively.

The electrical conductivity and thickness of the carbon network are adjusted by either tuning the carbon source content, or the annealing temperature and time. [333] The amount of carbon in MoS<sub>2</sub>/C samples is quantified by TGA in air. As shown in Figure 3.13a, the derivative weight curve of MoS<sub>2</sub> sample (red dash-curve) shows the first weight loss mainly occurring from ~ 350°C to 470°C, which is attributed to oxidation of MoS<sub>2</sub> to MoO<sub>3</sub>. [334] Thus, the weight loss of MoS<sub>2</sub> is calculated ~ 11.2 wt%. The second weight loss at ~ 760 °C is attributed to the sublimation of MoO<sub>3</sub>. [335] For the MoS<sub>2</sub>/C samples, the derivative curves

show a peak at  $\sim 360$  °C corresponding to the first weight loss that is caused by the oxidation of MoS<sub>2</sub> to MoO<sub>3</sub>. [335, 336] The second peak at  $\sim 420$  °C is attributed to the combustion of carbon to form CO<sub>2</sub>. [327, 337] The weight loss of these two processes is calculated approximately  $\sim 21.3$ ,  $27.3$  and  $41.1$  wt% for the MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2, MoS<sub>2</sub>/C-3 sample, respectively. Therefore, the carbon contents in MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2, and MoS<sub>2</sub>/C-3 samples are estimated to be  $\sim 10.1$ ,  $16.1$  and  $29.9$  wt% by subtracting the first weight loss of MoS<sub>2</sub> from the total weight loss of MoS<sub>2</sub> sample, see Table 3.2 for details. The weight loss of MoS<sub>2</sub>/C samples at  $\sim 730$  °C is attributed to the sublimation of MoO<sub>3</sub>.

The structure of the MoS<sub>2</sub>/C samples is further investigated by XRD and Raman measurements. Figure 3.13b shows the XRD patterns of the exfoliated MoS<sub>2</sub> and MoS<sub>2</sub>/C samples, all the diffraction peaks are normalized according to (002) peak. The typical diffraction peaks of hexagonal MoS<sub>2</sub> phase are detected in the XRD patterns of MoS<sub>2</sub>/C samples, suggesting the preservation of MoS<sub>2</sub> phase after the annealing process. The (002) diffraction peak is representative for the preferential orientation of MoS<sub>2</sub> layers along the z axis. The intensities of the (100), (103), (105) and (110) diffraction peaks significantly increase with the rise of carbon content. This indicates that the incorporation of amorphous carbon creates more disordered orientations of MoS<sub>2</sub> flakes, as reported in literatures. [163, 334, 337] In addition, there is no diffraction peak related to graphitic carbon, demonstrating that the carbon has amorphous nature. [163, 327] As shown in the Raman spectra of the MoS<sub>2</sub> and MoS<sub>2</sub>/C samples (Figure 3.13c), the characteristic peaks of MoS<sub>2</sub> (E<sub>12g</sub><sup>1</sup> and A<sub>1g</sub>) are observed in all samples and there are no shifts of these peaks in MoS<sub>2</sub>/C with respect to the starting MoS<sub>2</sub> sample. These results suggest that the presence of carbon neither affect the crystalline structure of MoS<sub>2</sub>, nor induces defects in the flakes. [163, 337] Compared to MoS<sub>2</sub> sample, the Raman spectra of MoS<sub>2</sub>/C samples show two additional peaks at  $\sim 1360$  and  $\sim 1599$  cm<sup>-1</sup> corresponding to the D band and G band of carbon materials, respectively. The D band is attributed to A<sub>1g</sub> breathing mode of sp<sup>3</sup>-hybridized disordered carbon or defective graphitic carbon, whereas the G band is associated with E<sub>2g</sub> stretching mode of the sp<sup>2</sup>-hybridized graphitic carbon. [338] The presence of D and G band features the formation of amorphous carbon in MoS<sub>2</sub>/C samples. [168, 169] To provide further insight into the morphology and structure of the amorphous carbon and MoS<sub>2</sub> flakes, HR-TEM measurement is performed. From HR-TEM images (Figure 3.13d, e and f), the interlayer distance of MoS<sub>2</sub> layers in MoS<sub>2</sub>/C samples is  $\sim 0.64$  nm, having similar value to the one of the exfoliated MoS<sub>2</sub> sample (Figure 3.12b). Also, the amorphous phase of carbon is observed in HR-TEM images of MoS<sub>2</sub>/C samples. The HR-TEM images show that the thickness of carbon layer of MoS<sub>2</sub>/C-1 ( $\sim 0.8$  nm) is smaller than that on MoS<sub>2</sub>/C-2 ( $\sim 2.4$  nm) and MoS<sub>2</sub>/C-3 ( $\sim 13.8$  nm).

Moreover, the carbon layer in MoS<sub>2</sub>/C-1 sample does not cover completely the MoS<sub>2</sub> flakes due to the insufficient amount of initial PAA.

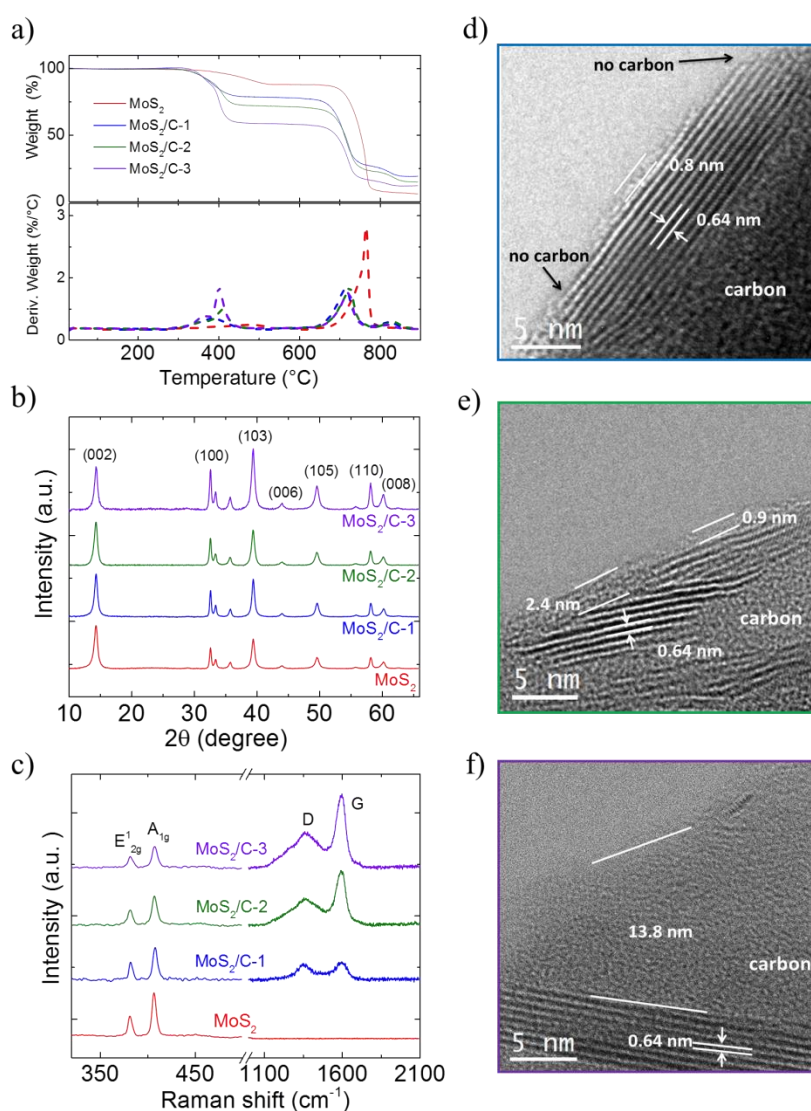


Figure 3.13. (a) TGA and Derivative Weight curves, (b) X-ray diffraction patterns, (c) Raman spectra at 514.5 nm excitation wavelength exfoliated MoS<sub>2</sub>, MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 samples. High resolution-TEM images of (d) MoS<sub>2</sub>/C-1, (e) MoS<sub>2</sub>/C-2 and (f) MoS<sub>2</sub>/C-3 samples.

Table 3.2. Calculation of wt% of carbon based on TGA measurement

Samples	Wt% of MoS <sub>2</sub> : PAA	Mass loss of Sulfur and Carbon (%)	Mass of carbon (%)
MoS <sub>2</sub> /C-1	1 : 1	21.22	<b>10.00</b>
MoS <sub>2</sub> /C-2	1 : 2	27.33	<b>16.11</b>

In conclusion, the characterization of exfoliated MoS<sub>2</sub> flakes confirm that the LPE process is able to produce the nano-sized MoS<sub>2</sub> flakes (lateral size mode of ~ 90 nm) without any change in the structural phase and chemical composition. Moreover, the characterizations of MoS<sub>2</sub>/C hybrids reveal the important information about the correlation between carbon content and the thickness of carbon layer in the MoS<sub>2</sub>/C hybrid. The obtained results contribute to the further understanding of the electrochemical properties of MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes in **chapter 5**.

### 3.5. Few-layer black phosphorous flakes

#### 3.5.1. Solvent analysis

In order to exfoliate and stabilize BP in a solvent, the Gibbs free energy of the mixture solvent/layered material must be minimized. [188, 241] This condition can be endorsed if the  $\gamma$  of the solvent is equivalent to the surface free energy of the material: [241]

$$\gamma = E_{Surface}^{Solvent} - TS_{Surface}^{Solvent} \quad (3.4)$$

in which  $E$  is the solvent surface energy,  $T$  is the absolute temperature and  $S$  is the solvent surface entropy (which generally takes a value of  $10^{-3} \text{ J m}^{-2} \text{ K}^{-1}$  [241, 339, 340]). Moreover, the matching of the Hansen or Hildebrand parameters of the solvent with the ones of the layered material facilitates the exfoliation process. [341-343] The Hildebrand parameter ( $\delta_T$ ) is widely used in polymer science, and is defined as the square root of the cohesive energy density: [344, 345]

$$\delta_T = \sqrt{\frac{\Delta H_v - RT}{V_m}} \quad (3.5)$$

in which  $\Delta H_v$  is the enthalpy of vaporization,  $R$  is the ideal gas constant, and  $V_m$  the molar volume. The Hildebrand parameter is used to evaluate the solubility or “dispersibility” of a material in a known solvent. [346, 347] However, in some specific cases, the Hildebrand parameter is not sufficient to describe and evaluate the dispersability of a material in a solvent. For example, the Hildebrand parameter of graphene is ~23 MPa<sup>1/2</sup>, [348] according to the solubility theory. A solvent with this  $\delta_T$  value, *e.g.* IPA with  $\delta_T \approx 23.8$ , [341] should form a stable dispersion of graphene which, however, has not been experimentally demonstrated. The reason lies in the fact that the Hildebrand parameter does not consider the hydrogen bonding and polar interactions. [341] In contrast, the Hansen solubility parameter splits the



cohesive energy ( $\delta_T^2$ ) into three components: the polar contribution ( $\delta_p$ ), the dispersive component ( $\delta_d$ ) and the hydrogen-bonding ( $\delta_h$ ) [341]

$$\delta_T^2 = \delta_d^2 + \delta_p^2 + \delta_h^2 \quad (3.6)$$

The  $\gamma$ , Hildebrand and Hansen parameters of the majority of solvents are reported in literature. [341] In contrast, the surface energy and the Hildebrand and Hansen parameters of the materials that are under consideration need an experimental estimation. A common way to obtain these data is to disperse the material in different solvents with a known  $\gamma$ , Hildebrand and Hansen parameters. The dispersed material is quantified either directly by evaporating the solvent and weighting the solid fraction, or indirectly by measuring the optical extinction of the material dispersed in the supernatant. Finally, when the solvent parameter value, e.g. the Hildebrand parameter, is plotted against the optical extinction, the maximum of the data distribution indicates the Hildebrand parameter of the dispersed material. The same analysis can be performed to estimate the Hansen parameters or to obtain the surface energy (see Equation 3.4).

Following this approach, the exfoliation of BP in different solvents (see section 2.1.3.4) is tested, most of which had been previously used for the LPE of other layered crystals. [188, 241] Subsequently, the known values of  $\gamma$  and the Hansen and Hildebrand solubility parameters of the solvents (see Table 3.3) as well as the optical extinction of BP dispersed on each solvent allow estimating the surface energy, and the Hansen and Hildebrand parameters of the exfoliated BP flakes.

Table 3.3. *List of solvents with their corresponding surface tension, Hildebrand and Hansen parameters, and boiling points*

Solvent	Surface Tension (mNm <sup>-1</sup> )	Hildebrand parameter (MPa <sup>1/2</sup> )	Hansen	Hansen	Hansen	Boiling point ( °C)
			parameter. Dispersive force (MPa <sup>1/2</sup> )	parameter. Polar force (MPa <sup>1/2</sup> )	parameter. Hydrogen bonding force (MPa <sup>1/2</sup> )	
Acetone	22.2	19.9	15.5	10.4	7.0	56.0
Toluene	28.4	18.2	18.0	1.4	2.0	110.6
Chloroform	25.8	18.9	17.8	3.1	5.7	61.2
2-Propanol	20.6	23.6	15.8	6.1	16.4	82.6
Trichloroethylene	28.7	19.0	18.0	3.1	5.3	87.2

<b>Methanol</b>	21.8	29.8	15.1	12.3	22.5	64.7
<b>Ethylene glycol</b>	47.0	33.0	17.0	11.0	26.0	197.3
<b>Acetonitrile</b>	27.7	24.4	15.3	18.0	6.1	82.0
<b>Ethanol</b>	21.1	26.5	15.8	8.8	19.4	78.4
<b>n-Hexane</b>	18.7	14.9	14.9	0.0	0.0	68.0
<b>N-Methyl-2-pyrrolidone</b>	40.1	23.0	18.0	12.3	7.2	202.0
<b>Dimethylformamide</b>	37.1	24.9	17.4	13.7	11.3	153.0
<b>Diethyl carbonate</b>	28.1	18.7	15.5	3.9	9.7	144.7
<b>N-Cyclohexyl-2-pyrrolidone</b>	43.2	20.5	18.2	6.8	6.5	284.0

Figure 3.14 shows the OES of BP flakes in 14 different solvents. By taking the value of the extinction at 680 nm of the dispersion in different solvents, and plotting them against the Hildebrand parameters and  $\gamma$  of each solvent, it is possible to estimate the Hildebrand parameter and  $\gamma$  of the dispersed material, respectively.

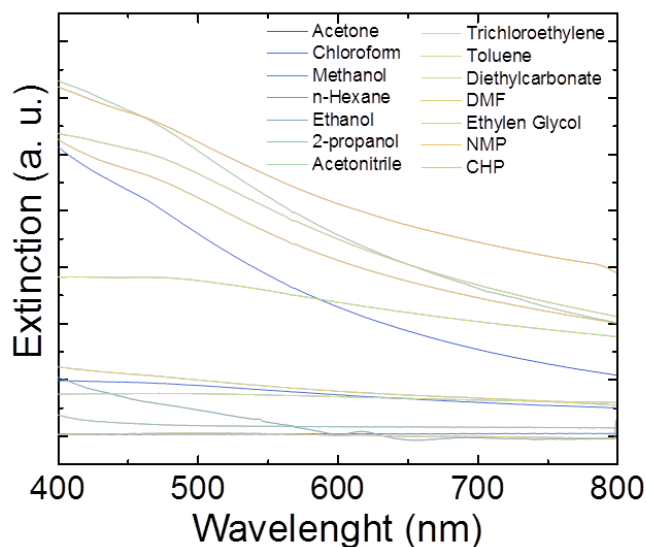


Figure 3.14. Optical extinction spectra of BP after LPE in different solvents.

Figure 3.15a and b show the solvent/BP dispersability analysis in terms of the Hildebrand parameter and  $\gamma$ , respectively. The dot distribution in Figure 3.15a fits a curve that peaks at a value close to  $21 \text{ MPa}^{1/2}$ . This value indicates the Hildebrand parameter of the BP, [343-345] which is in agreement with the previously report. [349] The data distribution in Figure 3.15b shows that the solvents that are able to exfoliate bulk BP have a  $\gamma$  in the range of 25-40  $\text{mN m}^{-1}$ . By applying equation 3.4, these values give a BP surface energy in the range of 50-65  $\text{mJ m}^{-2}$ .

<sup>2</sup>. The Hansen parameters of BP, shown in Figure 3.15c, d and e, provide  $\delta_p$ ,  $\delta_h$  and  $\delta_d$  values in the range of 5-12 MPa<sup>1/2</sup>, 5-10 MPa<sup>1/2</sup> and 15-18 MPa<sup>1/2</sup>, respectively. This means that a solvent with these Hansen parameters should be able to exfoliate and suspend the FL-BP. In summary, the solvent analysis (Figure 3.14 and 3.15) demonstrates that from the selected solvent, seven solvents are able to exfoliate/disperse BP: CHP, NMP, DMF, diethyl-carbonate, acetonitrile, trichloroethylene and acetone. In particular, three of these solvents have a low-b.p. (< 100 °C), *i.e.* trichloroethylene, acetonitrile and acetone, from which acetone the only non-toxic solvent is (Health code  $\leq 1$  NFPA704). [231] Thus, in the following part of this section, the exfoliated flakes in acetone and in CHP are fully characterized, the latter being used as a reference solvent.

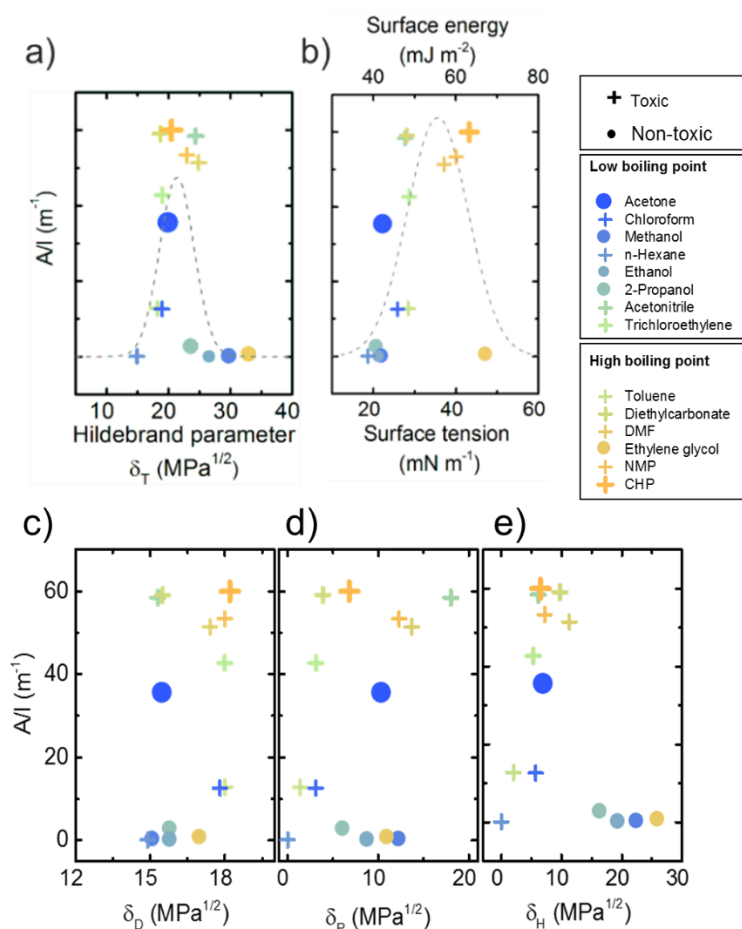


Figure 3.15. The extinction coefficient of BP dispersed in different solvents after the LPE process, plotted as a function of (a) Hildebrand parameter, and (b) surface tension (lower axis) and surface energy (upper axis). Dots represent the low/non-toxic solvents (Health code  $\leq 1$  NFPA704), crosses denote the highly toxic solvents ((Health code  $\geq 2$  NFPA704). Dots and crosses with colours from blue to light-green represent the solvents with b.p. < 100° C, while the ones from turquoise to orange represents solvents with b.p. > 100° C. Estimation of the Hansen parameters of FL-BP, giving approximated parameters of (c) dispersive force: 15-18 MPa<sup>1/2</sup>; (d) polar force: 5-12 MPa<sup>1/2</sup> and (e) hydrogen bonding force: 5-10 MPa<sup>1/2</sup>.

Figure 3.16a shows vials with the BP exfoliated in CHP (vial on the left) and the BP exfoliated in acetone at different dilution ratios (from the second left to right: no-dilution, 40%, 30%, 20%, 10% and 5%). Their corresponding extinction spectra are reported in Figure 3.16b, with the extinction coefficient for BP flakes dispersed in acetone being shown as an inset. The slope of this curve indicates that the extinction coefficient is  $600 \text{ L g}^{-1} \text{ m}^{-1}$ .

There is discrepancy between the extinction coefficient measured in this work and the previous values reported in literature, see Table 3.4. This difference is due to the diverse particle size distributions (thickness/lateral size), the refraction indexes of the solvents, and the wavelength at which the measurement is carried out. [350] The concentration of the FL-BP flakes in CHP (FL-BP<sub>CHP</sub>) is obtained using extinction coefficient at  $465\text{nm} = 1500 \text{ L g}^{-1} \text{ m}^{-1}$ , [235] attaining  $0.6 \text{ g L}^{-1}$ , and the concentration of BP flakes in acetone is obtained with the estimated extinction coefficient at  $660\text{nm} = 600 \text{ L g}^{-1} \text{ m}^{-1}$ , indicating a concentration of  $0.35 \text{ g L}^{-1}$ .

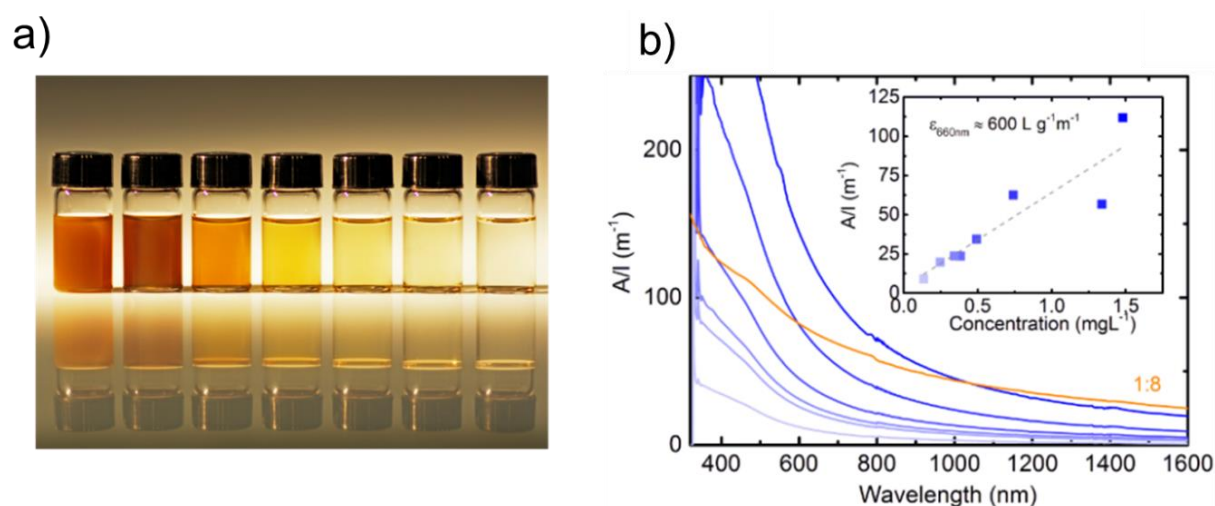


Figure 3.16. (a) Photograph of the FL-BP dispersions in CHP (first from the left) and acetone at different concentrations (from the second left to right). (b) Extinction spectra of the FL-BP dispersions in acetone at different concentrations, in different blue tones, and FL-BP dispersions in CHP, in orange. The inset shows the calibration curve according to the Beer-Lambert law, yielding an extinction coefficient of  $\sim 600 \text{ L g}^{-1} \text{ m}^{-1}$ , at  $660 \text{ nm}$ .

Table 3.4. Reported extinction coefficients for liquid phase exfoliated FL-BP in diverse solvents.

Solvent	Thickness (nm)	Lateral size (nm)	Wavelength (nm)	Extinction coefficient ( $\text{L g}^{-1} \text{ m}^{-1}$ )	Ref.
DMF	10	200*	1176	4819	[234]
DMSO	20	400*	1176	5373	[234]

<b>NMP</b>	10	100	660	263	[351]
<b>H<sub>2</sub>O</b>	5	100	660	209	[352]
<b>CHP</b>	6	100	465	1500 <sup>§</sup>	[235]
<b>Acetone</b>	5	30	660	600	This work

\* Lateral size estimated by dynamic light scattering. <sup>§</sup> Value of absorption coefficient.

### 3.5.2. Morphological characterization of BP flakes in CHP and acetone

Raman spectroscopy gives important information about the vibrational modes of exfoliated crystals. The Raman spectra of BP consists of three peaks, one out-of-plane mode ( $A_g^1$ , located at  $365\text{ cm}^{-1}$ ) and two in-plane modes ( $A_g^2$  and  $B_{2g}$ , located at  $471\text{ cm}^{-1}$  and  $440\text{ cm}^{-1}$  respectively, Figure 3.17). [353, 354] The positions and the intensity ratios between these peaks change depending on the T, [355] oxidation, [356, 357] strain, [358, 359] and number of layers. [352, 360]

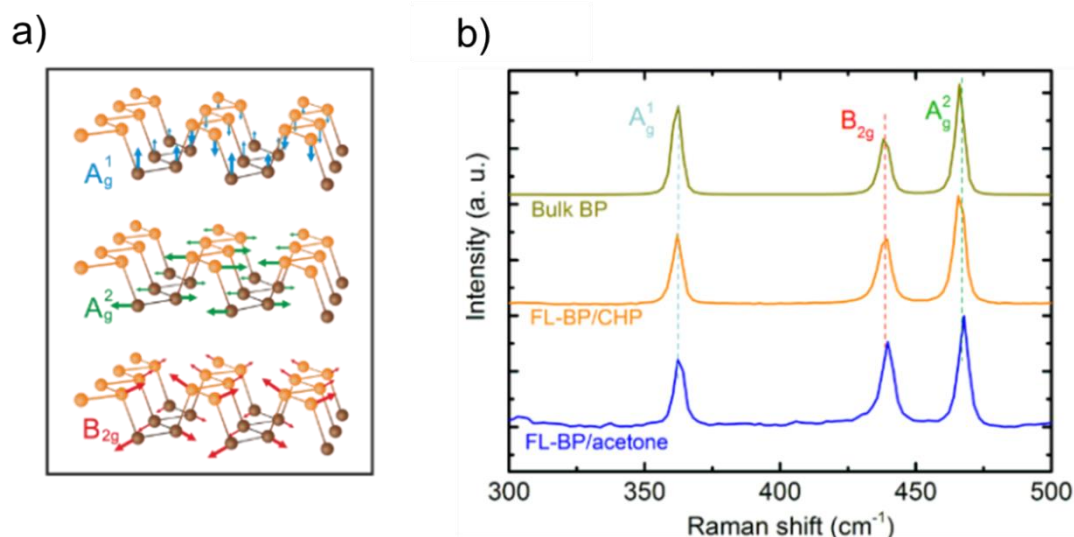


Figure 3.17. (a) Scheme of the FL-BP Raman active modes. (b) Raman spectra of the Bulk BP (dark yellow line), of the FL-BP cast from a CHP dispersion (orange line) and of FL-BP cast from a dispersion in acetone (blue line).

Figure 3.17b shows the Raman spectra of the starting bulk material (dark yellow), the BP exfoliated in CHP (orange) and the one in acetone (blue). The exfoliated samples display  $A_g^1$  at  $\sim 362.0\text{ cm}^{-1}$ ,  $B_{2g}$  at  $\sim 434\text{ cm}^{-1}$  and  $A_g^2$  at  $\sim 467\text{ cm}^{-1}$ , which is consistent with previous studies on liquid phase exfoliated BP, obtaining FL-BP. [235, 351] The Raman spectra on both samples, compared with the one of bulk material, suggest that the LPE process does not damage the BP structure and the number of layers is reduced with respect to bulk BP. [357]

The TEM characterization provides a detailed insight into the morphology and structure of the exfoliated BP flakes. The lateral size distribution analysis indicates that the FL-BP flakes exfoliated in acetone are smaller, with a lateral size of 30 nm (Figure 3.18a and 3.18b), compared with the ones exfoliated in CHP, which are 60 nm (Figure 3.18c and 3.18d). The FL-BP flakes thickness distribution, estimated by AFM analysis, indicates that the BP flakes exfoliated in acetone peak at 7 nm (~13 staked phosphorene layers, Figure 3.18e and f), while the ones in CHP peak at 8.1 nm (~16 staked phosphorene layers, Figure 3.18g and h). The TEM and AFM analysis indicates that FL-BP can be produced either using CHP or acetone.

Figures 3.19a and 3.19f report the STEM analysis of FL-BP produced in acetone and CHP (FL-BP<sub>acetone</sub> and FL-BP<sub>CHP</sub>, respectively). The compositional mapping by EDS, (Figure 3 b-d and g-i) shows that flakes are composed of P with no appreciable presence of O. Moreover, after the FL-BP<sub>acetone</sub> and FL-BP<sub>CHP</sub> production, both samples retained the crystal structure of FL-BP, as shown by HRTEM images in Figs. 3.19e and j.

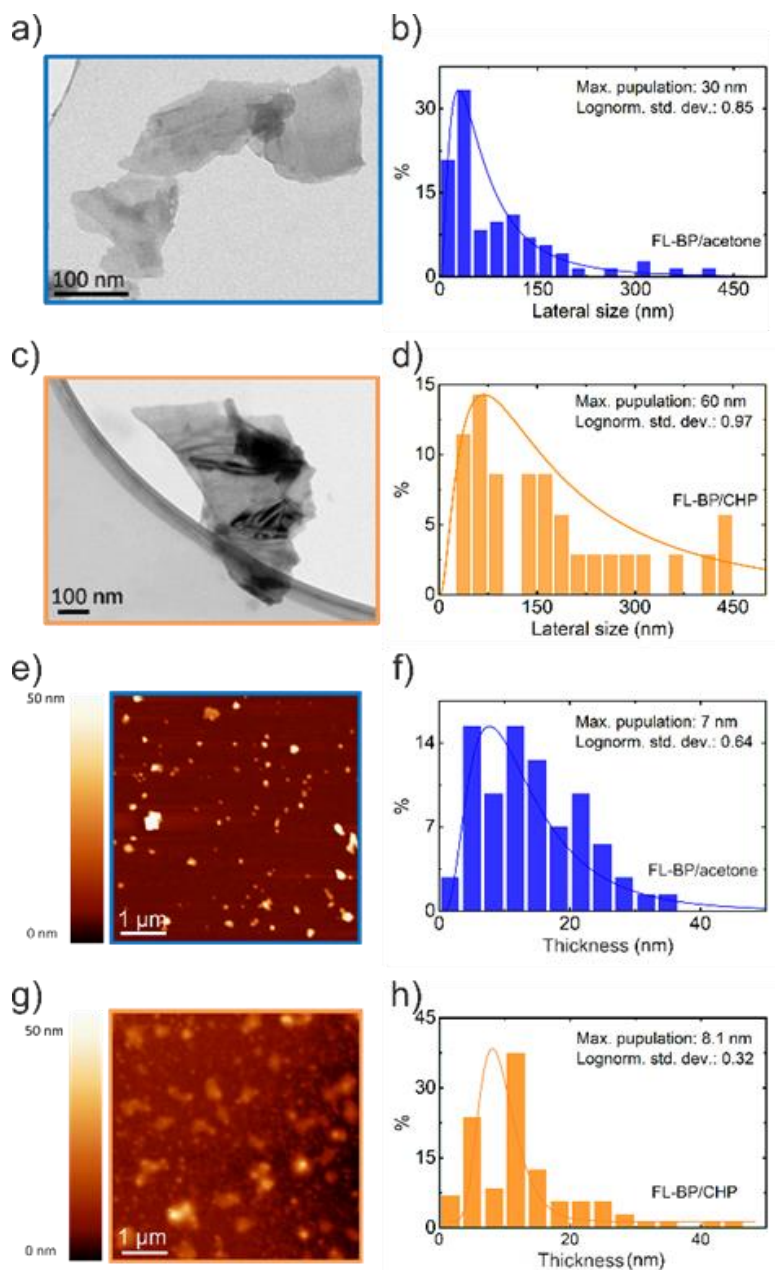


Figure 3.18. *Transmission electron microscopy of FL-BP in (a) acetone and (c) CHP, and their corresponding lateral size distributions (b and d). Atomic force microscopy images of (e) FL-BP<sub>acetone</sub> and (g) FL-BP<sub>CHP</sub>, and (f and h) their corresponding thickness distributions.*

The structural analysis of the exfoliated flakes is a challenging task due to the crystalline degradation of the thinnest flakes upon exposure to ambient conditions. [357] The degradation of FL-BP flakes is due to the presence of oxygen groups favouring the formation of PO groups. [228, 234, 235] In the case of LPE-BP, it has been reported that CHP and NMP form solvation shells adjacent to the BP surface, which prevents oxidation. [235]

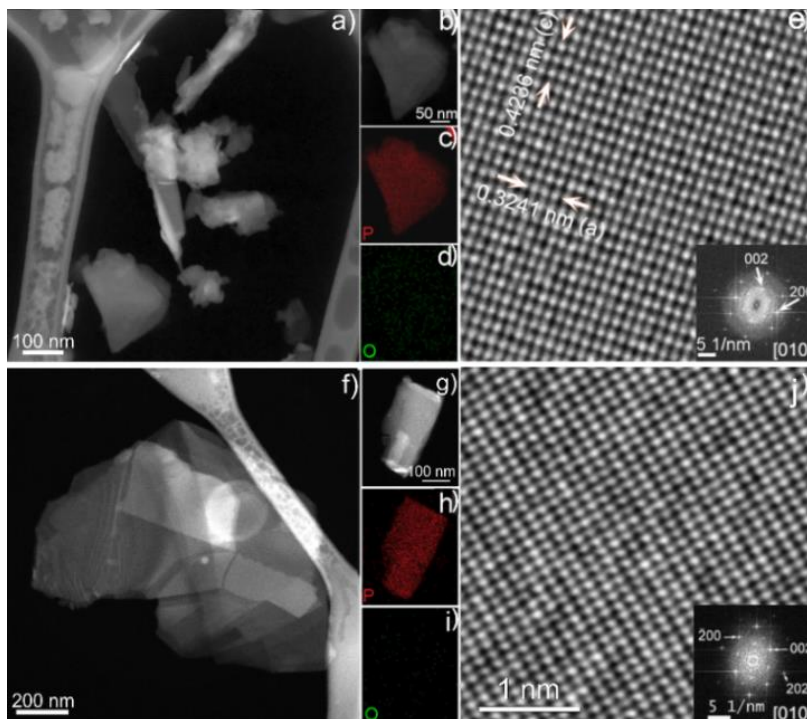


Figure 3.19. (a) STEM image of FL-BP<sub>acetone</sub> sheets. (b) STEM image of a selected FL-BP<sub>acetone</sub> sheet and corresponding d) EDS maps showing the distribution of P (c) and O (d). e) HRTEM image of an FL-BP<sub>acetone</sub> sheet oriented in its 010 axis with the FT reported as an inset. (f) STEM image of several overlapping FL-BP<sub>CHP</sub> sheets, g) STEM image of an FL-BP<sub>CHP</sub> sheet with the EDS maps showing the distribution of P (h) and O (i). (j) HRTEM of the FL-BP<sub>CHP</sub> sheet in the 010 orientation with the FT as an inset.

In light of this, an ageing study comparing FL-BP<sub>acetone</sub> with FL-BP<sub>CHP</sub> is performed. Electron energy loss spectroscopy (EELS) analysis is performed to determine the chemical bonding in the samples, at different storage times during a three months period. The comparison of the EELS collected from the flakes after different storage times in CHP (Figure 3.20a) and in acetone (Figure 3.20b) indicates that both samples undergo gradual oxidation over a three months period following the exfoliation process. This is evident from the rise of the peak at ~136 eV, in addition to the P L<sub>2,3</sub>-edge at ~130 eV (labelled as P<sup>0</sup>) which corresponds to elemental P (Figure 3.20a and b). The peak at ~136 eV (labelled as P<sub>x</sub>O<sub>y</sub>) has previously been attributed to oxidation of BP flakes [227, 361, 362] and is also a dominant feature in the P L<sub>2,3</sub>-edge from P<sub>2</sub>O<sub>5</sub>. [227, 361, 362] The corresponding EEL spectra focused on the oxygen K-edge region (Figure 3.20c) from the two samples following more than three months of ageing, exhibit weak but distinguishable signals associated with the presence of oxygen (arrowed). In contrast, no clear signal in the same energy range is observed in the spectra from the as-exfoliated samples.



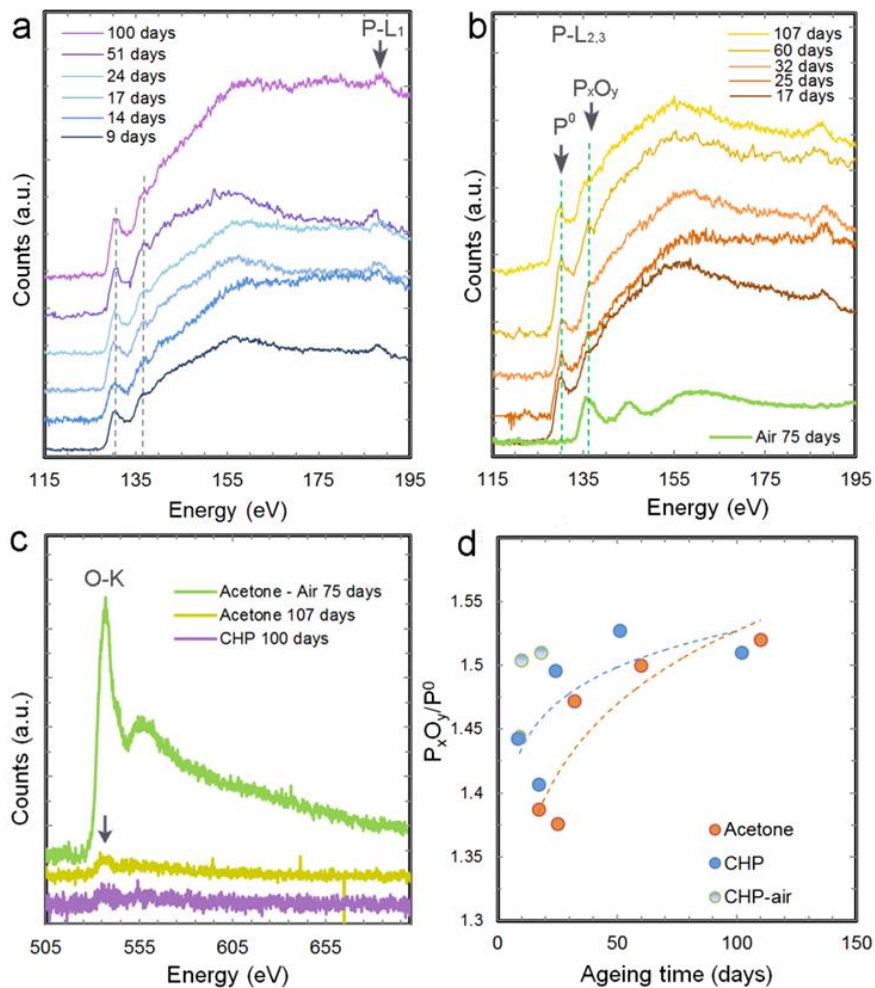


Figure 3.20. The EELS characterization of the FL-BP degradation in acetone and in CHP. EEL spectra exhibiting the phosphorus L-edge, collected from the FL-BP flakes stored in (a) CHP and in (b) acetone for different time, indicated in the graphs, following the exfoliation in the respective solvents. An EEL spectrum from the flakes stored in air for 75 days following the exfoliation in acetone is included for comparison in (b). The P L<sub>2,3</sub>-edge at ~130 eV corresponds to elemental P (P<sup>0</sup>), while the appearance of this edge at higher energies indicates that P is in a higher oxidation state. The additional peak observed here at ~136 eV has been attributed to oxidation of FL-BP flakes, [227, 361, 362] hence it is labelled P<sub>x</sub>O<sub>y</sub>. (c) EEL spectra in the oxygen K-edge region collected from the FL-BP flakes stored in CHP and in acetone for 100 and 107 days, respectively. The oxygen K-edge signal from the flakes after storage in the respective solvents is considerably weaker than the oxygen signal from the acetone-exfoliated flakes stored in air for 75 days, included for comparison in (c). (d) Evolution of the intensity ratio of the P<sub>x</sub>O<sub>y</sub> to P<sup>0</sup> signals in the EEL spectra collected after different storage times in CHP (blue circles) and in acetone (orange circles). Additional data from the CHP-exfoliated sample stored in air up to two weeks are also included for comparison in (d) (open blue circles). Each data point is an average of six measurements. The dashes lines are power-law fits to the experimental data points.

Although no significant differences are immediately visible between the EEL spectra from the two samples after comparable storage times in their respective solvents, the intensity ratio of the  $P_XO_Y$  signal at 136 eV versus the  $P^0$  signal at 130 eV, plotted in Figure 3.20d, is slightly but consistently higher in the spectra collected from the FL-BP<sub>CHP</sub> over the initial two months. After more than three months of storage (~100 days of storage in the respective solvents), both samples reach a similar level of oxidation (1.52  $P_XO_Y$  to  $P^0$  ratio, Figure 3.20d). The rate of oxidation of the FL-BP in both solvents is nevertheless significantly lower than in air (additional data points from the FL-BP<sub>CHP</sub> left in air for two weeks are included for comparison; light blue circles in Figure 3.20 d). This is evident from the prominent oxygen K-edge in the spectrum from the acetone-exfoliated sample left in air for 75 days (the topmost spectrum in Figure 3.20c) compared to the oxygen signals from flakes stored in the two solvent for more than three months.

The FL-BP flakes exposed to air in the present work retained their crystalline structure and most of the phosphorous in the elemental form within the initial couple of weeks, however the prolonged exposure to air gradually lead to their oxidation and structural degradation. The EEL spectrum from the acetone-exfoliated sample left in air for 75 days included in Figure 3.20b (green line) indicates a chemical shift from 130 eV to ~136 eV and exhibits additional features at higher energies, both consistent with the formation of phosphorus oxide. [227, 361, 362] The oxidation is accompanied by a significant structural transformation. What are initially fine crystalline FL-BP flakes in aggregates (Figure 3.21a), after exposure to air for 75 days transformed into amorphous clusters (Figure 3.21b), similar to droplet-like features reported previously. [227, 361-363] The compositional analysis based on EELS indicates that the composition of the amorphous clusters is approximately  $P_{54}O_{46}$  (expressed in at%; Figure 3.21c). The compositional analysis is based on the P L-edge found here at 136 eV and O K-edge at ~532 eV, both extracted from the raw spectra by removing the background fitted according to a power law model and using the Hartree-Slater model for the cross-section calculation.

After 12 weeks of aging time, both FL-BP<sub>acetone</sub> and FL-BP<sub>CHP</sub> samples retain their crystallinity, as is evident from the HRTEM image of an FL-BP<sub>acetone</sub> flake, shown in the 110 zone axis (Figure 3.22a). However, the degradation of the flakes is visible as a surface-localized amorphous coating which is 2 to 5 nm thick, as can be appreciated from the side-view image of the flake reported in Figure 3.22b.

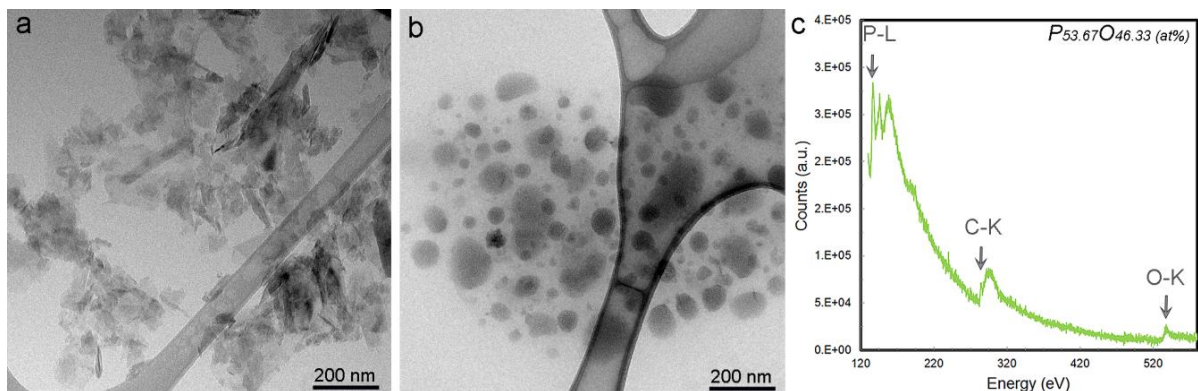


Figure 3.21. The degradation of the FL-BP flakes in air. (a) An aggregate of flakes after exfoliation in acetone and (b) a similar aggregate after exposure to air for 75 days. (c) An EEL spectrum from the flakes after oxidation in air for 75 days exhibiting prominent phosphorus and oxygen edges used for quantification. The carbon K-edge at 284 eV originates from the amorphous carbon TEM grid support.

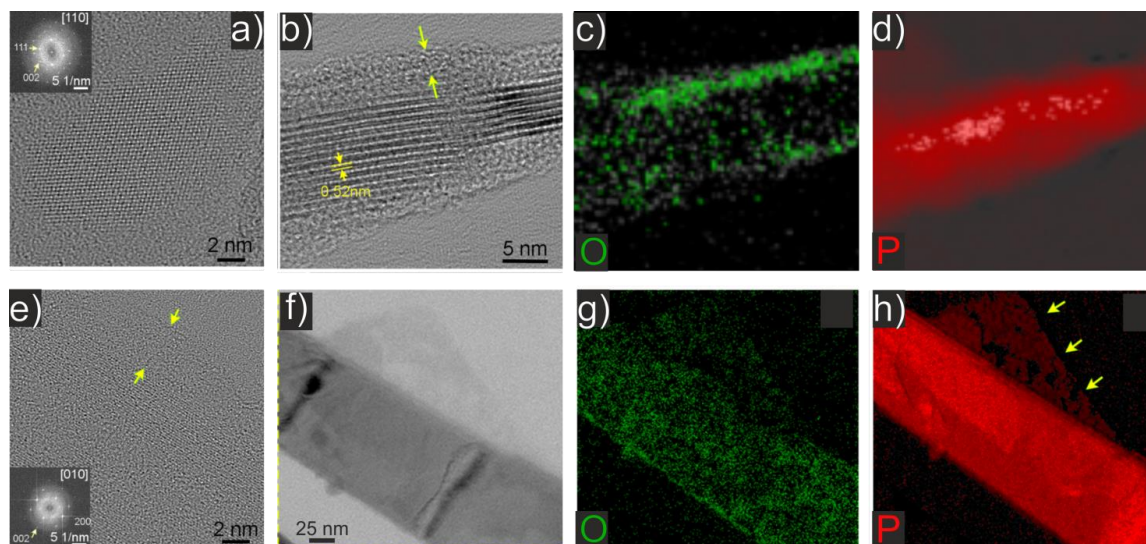


Figure 3.22. Study on the structural degradation of FL-BP<sub>acetone</sub> (a to d) and FL-BP<sub>CHP</sub> (e to h) flakes after 12 weeks of storage in the respective solvents. (a) A FL-BP<sub>acetone</sub> flake in the 110 zone axis exhibiting the structure of bulk BP. The corresponding FT is shown as an inset to (a). (b) An 8 layered thick flake shown edge-on, in which the individual phosphorene monolayers of  $\sim 0.52$  nm in thickness within the flake can be clearly resolved. The same flake also exhibits an amorphous layer on the surface (see yellow arrow) and the corresponding (c) oxygen and (d) phosphorus EFTEM elemental maps indicate that this layer is oxygen-rich. A thick amorphous layer is also present on the FL-BP<sub>CHP</sub> flakes (see arrows in e). The flake shown in (e) is in the 010 zone axis, with the corresponding FT shown as an inset. Additionally, a thinner (brighter in contrast in TEM image in (f)) flake overlapping the flake shown in (e) exhibits clear signs of structural degradation. The corresponding (g) oxygen and in particular (h) phosphorus EFTEM elemental maps clearly indicate the fragmentation of the thinner flake (yellow arrows in h).

The distance between two adjacent BP layers is 0.52 nm, [364] as is shown by the arrows (see Figure 3.22b). The compositional analysis of this flake (Figure 3.22c and d) by EFTEM indicates that the amorphous surface layer is oxygen-rich (Figure 3.22c), while the central crystalline part of the flake remains phosphorus-rich (Figure 3.22d). The presence of a thick amorphous layer is also evident on the FL-BP<sub>CHP</sub> (see arrows in Figure 3.22e). Fragmentation accompanying oxidation is also observed with thin flakes, such as the one shown in Fig 3.22f and g, overlapping the thicker (darker in contrast) flake. The degradation of the thinner flake (light contrast) is clearly visible from the EFTEM map of phosphorus (see arrows in Figure 3.22h).

The spectroscopic and morphological characterizations show that the exfoliation of bulk BP can be performed in acetone as successfully as in high-b.p. solvents such as CHP. Detailed structural and compositional characterization of the exfoliated material also demonstrates that the oxidation by aging FL- BP<sub>acetone</sub> is similar to aging FL-BP<sub>CHP</sub>. The exfoliation of BP in acetone is therefore an affordable alternative to the exfoliation process carried out exploiting high-b.p. and toxic solvents, offering a safe and sustainable route for the exfoliation, storage and deposition processes of FL-BP flakes.

In conclusion, it is demonstrated the exfoliation of bulk black phosphorus with acetone, creating a new way to formulate functional inks to be exploited for the designing of few-layers BP-based devices. The exfoliation of BP and its dispersion in 14 different solvents give us the possibility to evaluate the dispersability properties of few-layers BP. It has been estimated: (i) the surface energy to be in the range of 55-70 mJm<sup>-2</sup>; (ii) the Hildebrand parameter to be 21 MPa<sup>1/2</sup> and (iii) the Hansen parameters to be 15-18 MPa<sup>1/2</sup> for a dispersive force, 5-12 MPa<sup>1/2</sup> for a polar force and 5-10 MPa<sup>1/2</sup> for a hydrogen bonding force. Among the different trials, it has been found that exfoliation in acetone leads to exfoliated FL-BP flakes with average lateral size of 30 nm and thickness of 7 nm (corresponding to 13 layers). Additionally, The EELS and Raman spectroscopies demonstrates that the exfoliated BP flakes in acetone show an aging (oxidation and degradation) that is comparable with the one obtained by using high-b.p. solvents, *e.g.*, CHP. These results will give an opportunity for the exploitation of FL-BP flakes in acetone as an active material for the realization of LIB anodes which will be reported in **chapter 6**.

## Chapter 4:

# Application of graphene for lithium ion batteries

### 4.1. Introduction

Graphene flakes, obtained from the LPE of pristine graphite, represent an ideal yet not fully explored material platform for LIB anodes. [202] Besides all the properties of graphene that are beneficial for LIB applications, such as large surface to mass ratio ( $2600 \text{ m}^2/\text{g}$ ), [192] high electrical conductivity, [193] and high mechanical strength, [194] the LPE graphene flakes have high crystallinity, [159] a key feature for promoting fast electron transport in the electrode. [129] Moreover, the high specific surface area [192] of graphene flakes could allow  $\text{Li}^+$  uptake on both basal planes and at the edges, providing more active sites for  $\text{Li}^+$  storage. [196] Thus, graphene flakes prepared by LPE of graphite are emerging as a promising anode material for LIB. [198] As mentioned in **chapter 2**, LPE exploited the ultra-sonication process to exfoliate 2D flakes from their bulk counterparts in a specific solvent, having the  $\gamma$  as close as to the surface energy of 2D flakes. [188, 365] So far, NMP has been considered as one of the most-effective solvents for the production of graphene flake via LPE because its  $\gamma$  is  $41.2 \text{ mN m}^{-1}$ , which is close to graphene's surface energy ( $46.7 \text{ mN m}^{-1}$ ). (detailed discussion in section **2.1.2**). However, NMP is not an environmentally friendly solvent. [249, 250] Moreover, NMP has high b.p. ( $202 \text{ }^\circ\text{C}$ ), [3] therefore its evaporation process usually requires high temperature, ( $>150 \text{ }^\circ\text{C}$ ) [67, 249] coupled with high vacuum conditions to avoid the oxidation of the graphene flakes. [159, 249] These issues limit the LPE graphene based ink obtained in NMP for the application of energy conversion and storage devices. [159] Non-toxic and low-b.p. solvents such as water [243, 366, 367] and some alcohols, [368] which would be crucial to develop a fully environmentally compatible deposition/coating process, [159, 249] require the addition of stabilizing agents, *e.g.*, polymers or surfactants, [287, 367] for the optimal dispersion of the flakes. Unfortunately, the presence of such stabilizers in the ink compromises the graphene flake electrochemical properties once deposited onto the current collector. [272] A viable strategy to overcome the aforementioned issues relies in the exploitation of co-solvents, *e.g.*, water/EtOH, [249, 369] and water/isopropanol, [251, 370] to tune the rheological properties of low-b.p. solvents for the formulation of graphene flake-based inks. However, the concentration of the as-produced ink is still low ( $< 1 \text{ g L}^{-1}$ ), [249, 251] thus not ideal for applications where highly concentrated ink is needed, *e.g.*, the production of battery electrodes.

Besides the issues on the development of novel and high-performance anode materials, advances in the electrode fabrication processes are also important. In fact, the electrode preparation [371-376] is time-consuming and expensive with a strong impact on the cost of the LIB technology. [377-379] Additionally, the composition and morphology of the electrode are critical for LIB operation, because both composition and morphological inhomogeneity can hinder the diffusion of  $\text{Li}^+$  throughout the electrode itself, resulting in a high charge transfer resistance of electrode materials during lithiation/de-lithiation process. [380] Finally, the weight of the binder, being a material not involved in the lithiation/de-lithiation processes, has a negative effect on the electrochemical performance of the anode, limiting both the specific capacity and the energy density of LIBs. [381] For instance, PVdF is reported to swell, *e.g.*, the PVdF binder in a Si battery has shown a 20% thickness change in the electrolyte during the charge/discharge process) [382] in contact with electrolytes based on carbonate solvents. This phenomenon causes solvent decomposition, resulting in capacity fading of LIBs during operation. [382-384] Moreover, PVdF requires the use of toxic and expensive organic solvents, coupling with extra steps to mix and combine with active materials to form a complete electrode material. [371, 385] In this regard, tremendous efforts have been made to develop binder-free electrodes for LIBs, [377] mostly exploiting the direct deposition of the active materials onto the current collectors. [371-374] However, most of the proposed methods such as electrophoretic deposition of hollow  $\text{Co}_3\text{O}_4$ , [371] sputtering of Ge embedded in carbon matrix, [372] CVD of CNT and Si nanowire, [373, 374] have not met the requirements in terms of scalability and low-cost production. Another route, *e.g.*, vacuum filtration, has been reported as promising method for low-cost and mass production of the binder-free carbon-based anodes, without any current collector support substrate. Nevertheless, the anodes are still facing limitation of large irreversible capacity and low reversible capacity. For example, the binder-free SWNTs anode shows an irreversible capacity of  $1000 \text{ mAh g}^{-1}$ , while the RGO and CNT/GO free-standing anodes show the capacity of 300 and  $330 \text{ mAh g}^{-1}$ , respectively.

Besides the issues of solvent and electrode fabrication, the performance of graphene-based LIBs is still controversial. In fact, graphene and its derivatives, such as GO [386-388] and RGO, [117, 160, 389] are widely investigated for the realization of LIB electrodes. Recently, RGO, GO and their hybrids/composites with electrochemically active material have been the most investigated materials as promising choices of anodes for LIB. [117, 160, 389-391] Although RGO can provide large initial capacity value ( $> 2000 \text{ mAh g}^{-1}$ ), [392] it suffers large irreversible capacity and high voltage hysteresis upon lithiation/de-lithiation. This phenomena is due to the heteroatoms/functional groups, *e.g.*, O- and H-containing in

functional groups, and the presence of defects, *e.g.*, micro-pores, vacancies, etc., which diminish the conductivity and act as Li<sup>+</sup> traps during lithiation/de-lithiation. [393, 394] In order to avoid such negative effects of the functional groups and defects, pristine graphene flakes produced by the LPE of graphite, [202] are a viable replacement for graphite, GO and RGO as anode active material. The anode composed by pristine SLG flakes have shown a promising specific capacity of 744 mAh g<sup>-1</sup>, with the assumption of Li<sup>+</sup> adsorbed on both sides of graphene, forming a Li<sub>2</sub>C<sub>6</sub> stoichiometry. [196] However, the Li<sup>+</sup> storage is thermodynamically unstable in pristine SLG electrode during lithiation/de-lithiation, where only low Li<sup>+</sup> occupancy levels can be achieved. [157, 395] In contrast, MLG has shown several improvements in terms of electrochemical and thermal stability within the LIBs operational temperature range (-20/60° C), [201, 396] as well as mechanical stability of the electrode. [397] However, there are no considerable gains in specific capacity of MLG-based anode with respect to that of graphite anode. [5, 396] This raises a natural question. What about what lies in between? Is there a critical flakes size where both beneficial properties of graphite, *e.g.*, low operating voltage, and graphene (high conductivity and short diffusion paths) are found? Is FLG a good active material for next-generation Li-ion batteries? Despite the fact that it is well accepted that dimensions (lateral size and thickness) of the flakes [202] as well as their edges, [198] are expected to play key roles on the Li<sup>+</sup> storage mechanisms [36, 44, 198, 202, 398] the link between these morphological properties, and electrochemical performances has not been established yet, neither for RGO, [159, 392, 399-402] nor with the less investigated un-functionalized flakes.

This chapter presents the investigation on the electrochemical performance of binder-free single SLG/ FLG flakes based anode for LIB and the study on the role of graphene flake dimensionality on the electrochemical performance of anodes based on FLG and MLG flakes. The graphene flakes are obtained by LPE of graphite in NMP. A solvent exchange process is exploited to first remove the NMP and then to re-disperse the exfoliated SLG/FLG flakes in EtOH. The binder-free SLG/FLG flakes based anode is successfully formed via a one-step fabrication of LIB anodes (drop-casting an environmentally friendly graphene flake-based ink on a Cu substrate at room temperature), without the addition of conductive additives. The anode is assembled in half-cell configuration, achieving a reversible specific capacity of 503 mA h g<sup>-1</sup> after 100 cycles. Moreover, the full LIB configuration using binder-free SLG/FLG flakes anode and commercial LNMO cathode, exhibits the reversible specific capacity of ~100 mA h g<sup>-1</sup>. This process is able to avoid the conventional time-consuming preparation and deposition of the anode electrodes, promoting a novel strategy to produce graphene based electrodes in fast and efficient way. Additionally, the binder-free anodes based on FLG and

MLG flakes are fabricated to explore the role of flake dimensionality on the lithiation/delithiation processes and electrochemical properties. The electrochemical results show that decreasing graphene flake dimension (lateral size and thickness) leads to an increase of the initial specific capacity from  $\sim 590$  to  $\sim 1270$  mAhg<sup>-1</sup> which is however linked with a significant increase of the irreversible capacity. Especially, the Li<sup>+</sup> storage by adsorption is predominant compared with intercalation for the Li<sup>+</sup> storage in the case of anodes composed of small flake size (< 100 nm). In this thesis, the study of the role of graphene flakes dimension on its Li<sup>+</sup> storage ability provides insightful guidelines for the practical exploitation of graphene-based electrodes.

## **4.2. Graphene-based binder-free anode for lithium ion batteries**

This section provides a protocol to design binder-free graphene-based anodes for LIBs, starting from LPE of pristine graphite, solvent exchange process and drop-casting, opening the way to the optimization of energy/power densities and lifetime environmentally friendly LIBs. Briefly, graphite is exfoliated in NMP via ultra-sonication process, [260, 403] producing a heterogeneous dispersion of thin/thick and small/large graphitic flakes. [159] The obtained dispersion is subsequently ultra-centrifuged (10000 rpm), exploiting the SBS process, [202, 261] result in an ink enriched in SLG and FLG flakes. A solvent exchange process is exploited to replace NMP with EtOH, in order to obtain an environmentally friendly graphene ink for the deposition onto the current collector (see section **2.1.3.1**). Comparing the structural analysis by TEM and Raman (Figure 3.2a and b) characterizations of graphene flakes in both NMP and EtOH (see section **3.1.1**), it is demonstrated that the solvent exchange process does not affect the structural and morphological properties of the graphene flakes. Then, the graphene-based ink in EtOH is drop-casted onto Cu substrate under air atmosphere at room temperature and then dried at 120 °C and 10<sup>-3</sup> bar for 30 min in a vacuum oven. The as-produced binder-free electrodes have a mass loading of SLG and FLG flakes of 1 mg. The film covers homogeneously the Cu substrate, both at macroscopic (Figure 4.1a) and microscopic (Figure 4.1b) levels, with a thickness of 15 μm (inset to Figure 4.1b).



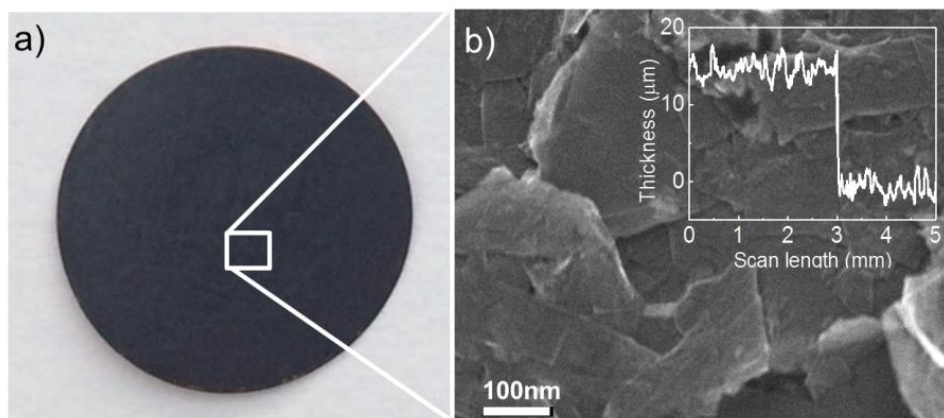


Figure 4.1. (a) Photograph of the Cu-supported SLG- and FLG-based electrode. (b) SEM image of the graphene electrode. The inset shows the thickness of the SLG- and FLG-based electrode measured by using a profilometer.

The as-produced anode is also characterized by Raman spectroscopy in order to evaluate the quality of the flakes composing the electrode. Figure 4.2a shows typical Raman spectra of grapheme flakes (in EtOH) deposited onto the SiO<sub>2</sub> substrate and binder-free graphene anode. Besides, Figure 4.2b exhibits no correlation in the distributions of the I(D)/I(G) vs. FWHM(G) in the both cases of graphene ink and graphene anode, indicating that no additional defects on SLG and FLG flakes are caused by the deposition process. [277, 404, 405] Moreover, the 2D peak still shows a Lorentzian line-shape distinctly different from that of graphite. In fact, the statistical analysis of I(2D)/I(G) (Figure 4.2c) and Pos(2D) (Figure 4.2d) of the as-prepared electrode indicates that the electrode is composed of a collection of SLG and FLG flakes,[202, 262] which, also if stacked together, are however electronically decoupled.

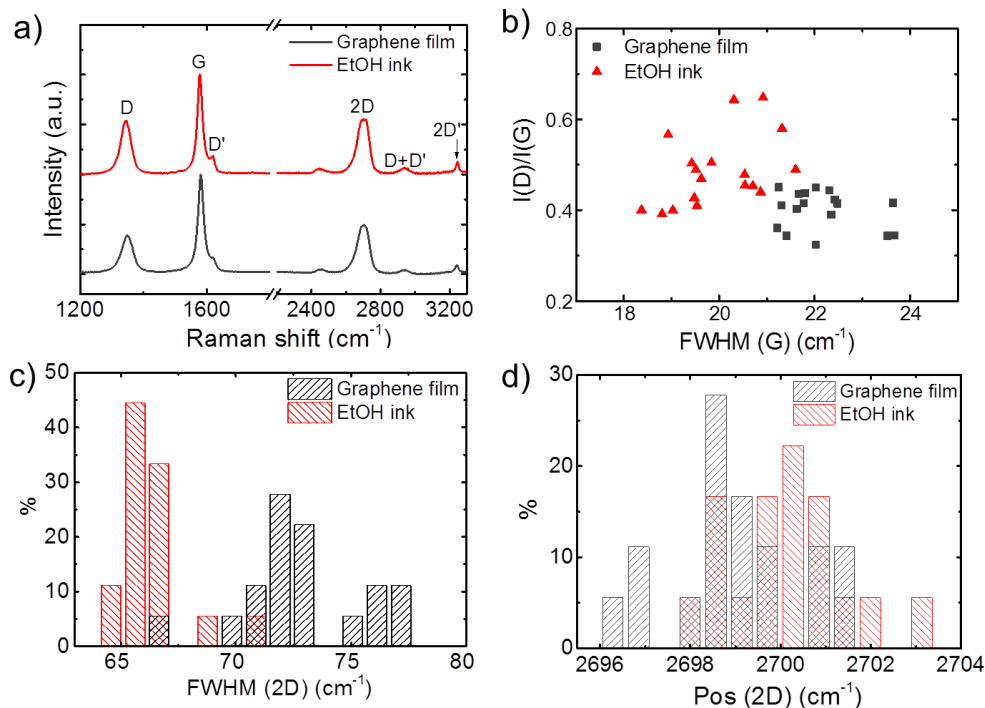


Figure 4.2. (a) Raman spectra of the graphene EtOH ink (red) and the graphene electrode (dark gray), (b)  $I(D)/I(G)$  ratios as a function of  $FWHM(G)$ , and histograms of (c)  $I(2D)/I(G)$  and (d)  $Pos(2D)$ .

The anode based on SLG and FLG flakes are tested against metallic Li in a half-cell configuration. Figure 4.3a reports the CVs performed at a scan rate of  $50 \mu\text{V s}^{-1}$ , carried out to get a complete electrochemical response for the Li ion transfer. [406] The scan range is from 1 V to 5 mV vs.  $\text{Li/Li}^+$ , covering the formation of the SEI [407] and the lithiation/de-lithiation process for carbon materials. [408] The first CV scan shows a broad reduction peak with a maximum at 0.55 V and an onset at 0.8 V, which is associated with the SEI formation due to side reactions or the reduction of the electrolyte at the surface of the electrode. [407] The absence of this peak in the following scans indicates that the SEI formation is stable, which guarantees a good cycle life of the anode, without further decomposition reactions. [407] Additionally, there is a current increase ( $\sim 20\%$ ) in the 0.1 – 0.3 V range passing from the 1<sup>st</sup> to the 5<sup>th</sup> cycle. This electrochemical behavior can be associated with a slow activation of the lithiation/de-lithiation processes that gradually enhance the capacity of the SLG/FLG-based anode over cycling. [396]

The binder-free electrode based on SLG and FLG flakes shows a specific capacity of  $503 \text{ mA h g}^{-1}$  at a current density of  $0.1 \text{ A g}^{-1}$  after the 100<sup>th</sup> charge/discharge cycle in the range from 50 mV to 3 V vs.  $\text{Li/Li}^+$  and a coulombic efficiency of 99.5% (Figure 4.3b). Moreover, the half-cell cycled at different current densities presents excellent charge/discharge cyclability as well. In fact, a specific capacity of  $610 \text{ mA h g}^{-1}$  is reached when the graphene-based anode is

cycled at  $0.05 \text{ A g}^{-1}$ . Additionally, specific capacity values of  $260 \text{ mA h g}^{-1}$  and  $150 \text{ mA h g}^{-1}$  have been reached after 20 cycles at current densities of  $0.5 \text{ A g}^{-1}$  and  $1 \text{ A g}^{-1}$ , respectively. Figure 4.3b and c, presents the voltage profiles of the electrodes during the 1<sup>st</sup>, 10<sup>th</sup>, 50<sup>th</sup> and 100<sup>th</sup> galvanostatic charge/discharge cycles. The latter are performed at a current density of  $0.1 \text{ A g}^{-1}$  between 5 mV and 3 V vs. Li/Li<sup>+</sup>, in order to complete the lithiation/de-lithiation (charge/discharge) process in the SLG/FLG-based anode during each cycle. From the first voltage profile, the irreversible specific capacity is calculated to be  $500 \text{ mA h g}^{-1}$ , which represents about half of the total charge capacity. Such a high irreversible charge capacity value is typical for graphene-based anodes and it is presumably due to the large surface area [195, 396] ( $325 \text{ m}^2 \text{ g}^{-1}$ , measured by BET) and edge reactivity of the SLG/FLG flakes compared to graphite-based anodes. [392]

The voltage profiles show that more than 50% of the electrode capacity is delivered at a potential lower than 0.25 V vs. Li /Li<sup>+</sup> with a flat plateau up to the 100<sup>th</sup> cycle (Figure 4.3c). Such a low potential is comparable to the values obtained using graphite (0 – 0.4 V vs. Li/Li<sup>+</sup>), leading to a high energy efficiency of batteries. [396] In order to understand the effect of voltage cut-off on both the specific capacity and coulombic efficiency of the graphene-based anode, we tested the electrode cycled at two different cut-off voltages, one between 50 mV and 2 V and the other one between 50 mV and 3 V. As shown in Figure 4.3d, the specific capacities of the electrode tested in these two different voltage ranges are similar, with a capacity loss lower than 5% for the first 50 cycles for both test conditions. Also the coulombic efficiency is quite similar, with a value >99% achieved after 8 and 5 cycles for the electrode cycled up to 2 V and 3 V, respectively. Moreover, the electrode cycled up to 2 V shows no gradual increase of the specific capacity upon cycling as instead shown by the electrode cycled up to 3 V. As mentioned before, this specific capacity increase is linked to the slow activation of the anode. [396] It indicates that a small quantity of irreversible capacity, which may be related to the edge effects of the graphene flakes, [202] requires high voltage (2 – 3 V) to be completed.

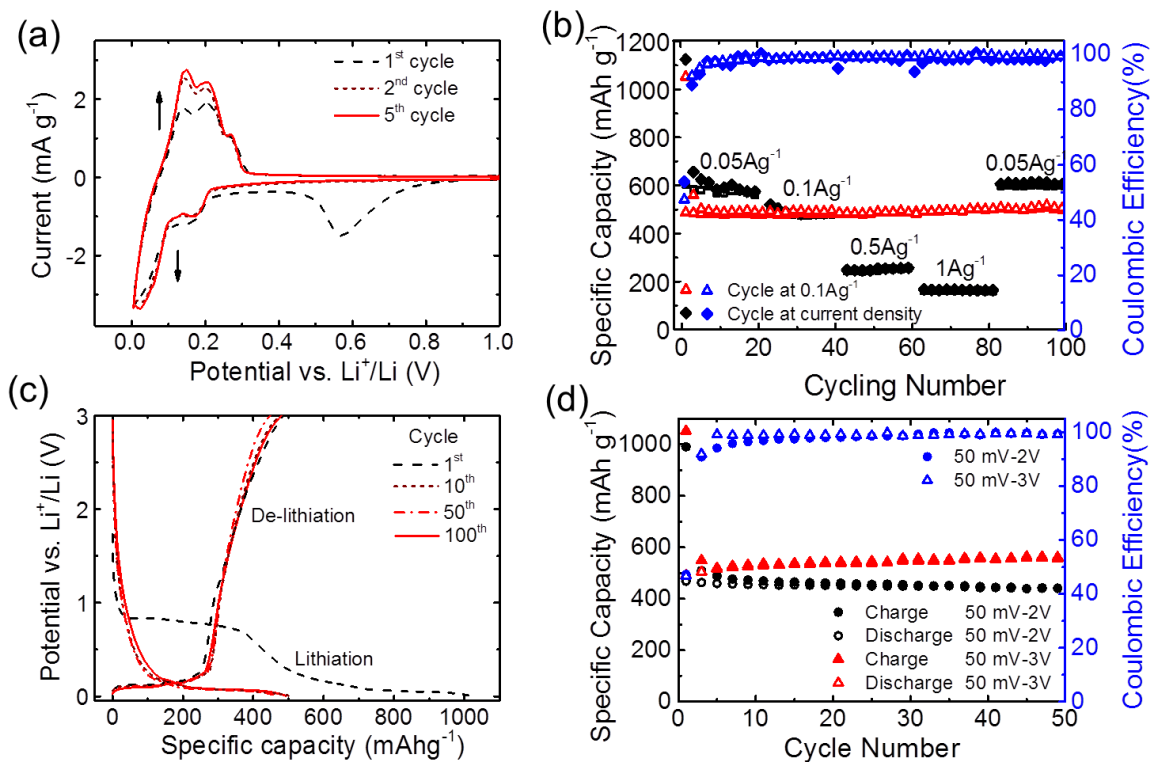


Figure 4.3. (a) Cyclic voltammograms at a scan rate of  $50 \mu\text{Vs}^{-1}$ . (b) Specific capacity and Coulombic efficiency over charge/discharge galvanostatic cycles between 50mV and 3V. The galvanostatic cycling at  $0.1 \text{ A g}^{-1}$  (triangles) is compared with the one at different current densities (diamond). (c) Voltage profile upon galvanostatic charge/discharge of graphene electrodes at  $0.1 \text{ A g}^{-1}$  between 50mV and 3V. (d) Specific capacity and Coulombic efficiency over galvanostatic cycles at current density of  $0.1 \text{ A g}^{-1}$  between 50 mV and 2 V (circle) and between 50 mV and 3 V (triangles), respectively.

The binder-free SLG/FLG-based anode is further studied in LIB configuration, coupling it with a commercial cathode material, *e.g.*, LNMO. The latter is considered as one of the most promising candidates in the development of high energy/power LIBs, [409, 410] thanks to its high theoretical specific capacity ( $146.7 \text{ mAh g}^{-1}$ ) [411] and high working voltage (around 4.7 V vs.  $\text{Li}/\text{Li}^+$ ). [412] Before the full LIB assembly, the pre-lithiation step is carried out on the anode to improve the working voltage and the energy density as well as to reduce the irreversible capacity loss, increasing the  $\text{Li}^+$  concentration of the electrolyte. [413] The aforementioned properties positively contribute to the cell cycling stability. [414] The reason behind the choice for the pre-lithiation process of the anode only for the full battery configuration and not for the half-cell configuration, relies on the fact that the LNMO cathode has limited  $\text{Li}^+$  source compared to the metallic Li foil (used for the half-cell configuration tests). [413] Thus, the LNMO cathode is not able to provide sufficient  $\text{Li}^+$  for the formation of SEI film without negatively affecting the cell cycling stability. [413] Moreover, in designing the battery, it is of paramount importance to reach an optimal balance of cathode and anode

electrodes both in term of weight and electrochemical properties. [413-415] The weight ratio we used in trying to optimize the anode/cathode balancing is 1/3.5, which takes into account the difference in specific capacity of the two electrodes. As shown in Figure 4.4a, the SLG/FLG-LNMO full battery operates at a high voltage ( $\sim 4.5$  V) with a voltage profile similar to the typical LNMO one, [411] confirming appreciable anode performance with a substantially constant working voltage lower than 0.20 V vs. Li/Li<sup>+</sup>. [412] The plot of the specific capacity as a function of the galvanostatic charge/discharge cycles (Figure 4.4b) shows a rather stable specific capacity of  $\sim 100$  mAh g<sup>-1</sup> with respect to the mass of LNMO, and a coulombic efficiency of  $\sim 99$  % achieved after 5 cycles. A major drawback of the LNMO-based batteries is their capacity fade, [416, 417] which is caused by the decomposition of the electrolyte at the electrode/electrolyte interface at the high working voltage ( $\sim 4.7$  V). [416] The capacity and the stability of SLG-FLG/LNMO full battery are comparable to those of state of the art LNMO-based batteries. [418-421] Although further research needs to be done on the optimization of LNMO cathodes and electrolyte, the results obtained by using the binder-free SLG/FLG-based electrodes, both in half- and full-cell configuration, strongly encourage their exploitation as advanced and high performance anode in LIBs.

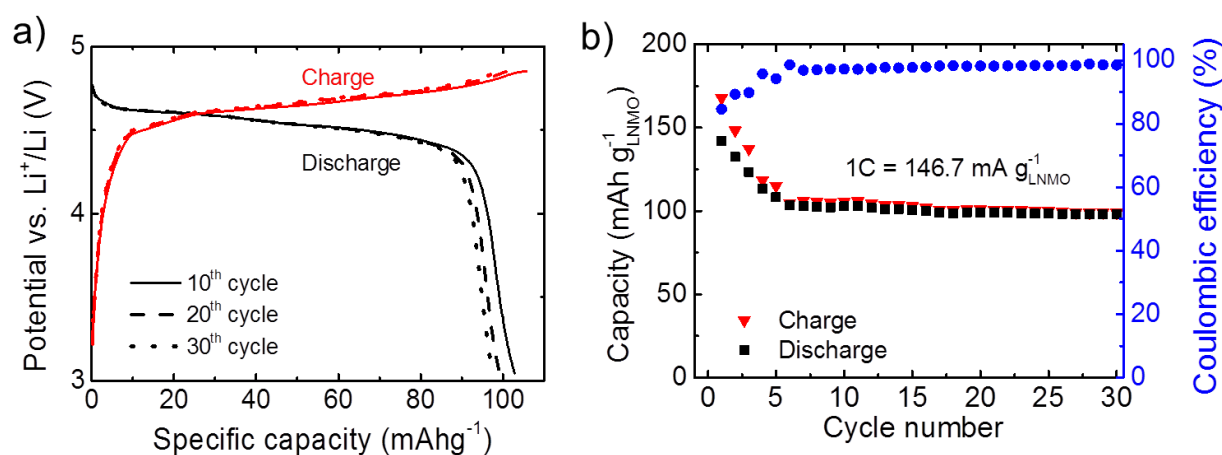


Figure 4.4. (a) Voltage profile upon galvanostatic charge/ discharge of graphene/LNMO full battery. 10th, 20th and 30th cycle at 1 C (146 mA g<sup>-1</sup> vs. LNMO). (b) Specific capacity and coulombic efficiency over charge/discharge galvanostatic cycles at 1 C between 3 V and 5 V of graphene/LNMO full battery.

### 4.3. The influence of graphene flake morphology on electrochemical properties of graphene based anode in lithium ion batteries

This section brings out the answers for the questions about the role of graphene flake morphology (i.e., lateral size and thickness) on the electrochemical properties of anodes based on FLG and MLG flakes, as mentioned in section 4.1. As reported in section 3.1.2, a set of

FLG and MLG flake dispersions (in NMP) are obtained and marked as Sample #1, #2, #3 and #4, corresponding to the lateral size (ranging from 75 to 380 nm) and thickness (from 2 to 20 nm), see Figure 3.6. The Raman results of these samples in Figure 3.8 confirm that Samples #1, #2 and #3 are composed of MLGs, while Sample #4 mostly contains FLG. In order to meet the requirements of fast deposition and non-toxicity, [150, 249] the sediments of the four samples are collected and dispersed in EtOH, allowing the simple one-step fabrication of binder-free electrodes. [3] The electrodes do not contain any additional conductive carbon, *e.g.*, carbon black, which is widely used in literature, [422] in order to avoid interfering with the electrochemical response of the graphene flakes, *e.g.*, by contributing to the Li<sup>+</sup> storage capacity. The graphene dispersions deposited onto the Cu substrates are characterized by SEM, see Figure 4.5.

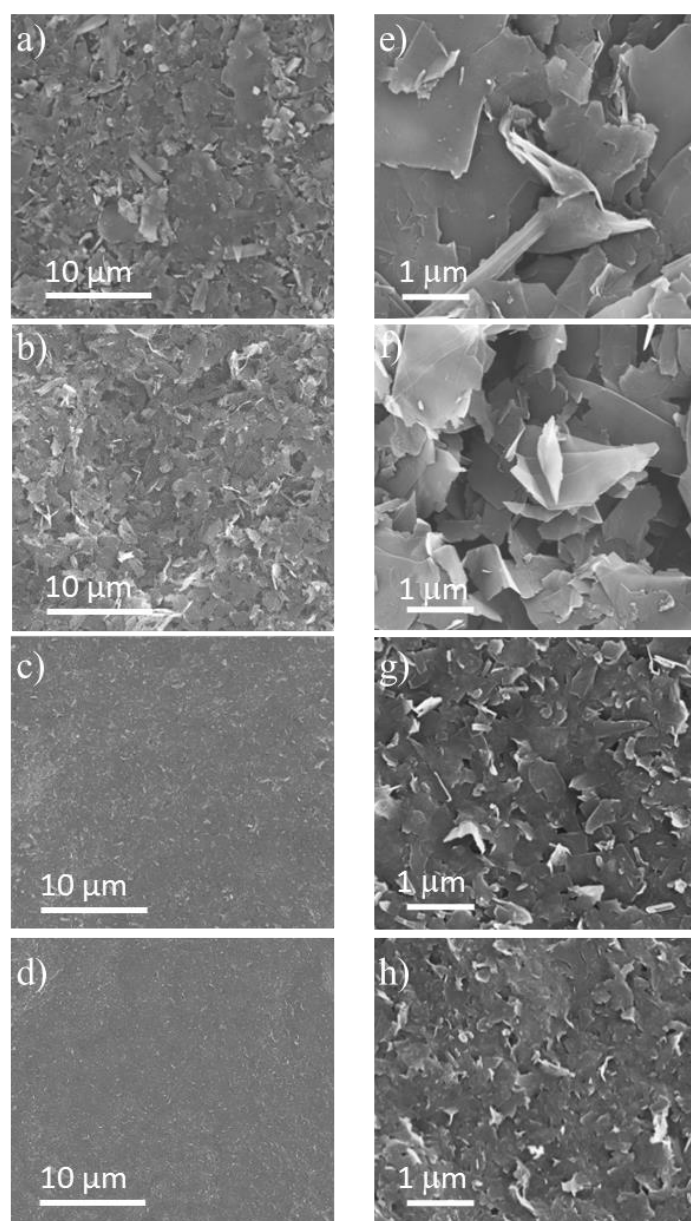


Figure 4.5. (a), (b), (c), (d) Low resolution SEM images and (e), (f), (g), (h) high resolution SEM images of Sample #1, #2, #3 and #4 deposited onto a Cu substrate, respectively.

The micrographs recorded at low magnification (Figure 4.5a, b, c and d), and representative for the whole area, testify the homogeneity of the binder-free electrodes, independently from the flake size. Higher magnification images (Figure 4.5e, f, g and h) reveal that, as the flake dimension decreases, the electrodes surface becomes more flat and compact, which from one hand could improve the electronic transport amongst the flakes, but, on the other hand, may not be beneficial for the lithium storage capacity and transport. The lateral sizes and thickness of the graphene flakes are expected to have a significant influence on their  $\text{Li}^+$  storage characteristics. [5, 195] The voltage profiles of Figure 4.6a show that upon the first lithiation, the specific capacity of the electrode increases from  $591 \text{ mAh g}^{-1}$  to  $1267 \text{ mAh g}^{-1}$  as the average lateral size and thickness of the flake decreases from Sample #1 to Sample #4. However, in the following opposite process,  $\text{Li}^+$  ions are released only to a certain extent, revealing a significant irreversible capacity, *e.g.*, 40% for Sample #1. As the flakes get smaller in both lateral size and thickness, more amount of charge is irreversibly consumed in the first cycle, resulting in only 35% coulombic efficiency for Sample #4, see Figure 4.6a. Accordingly, the loss of capacity may be ascribed to the irreversible electrolyte decomposition process leading to the formation of a solid electrolyte interphase (SEI) on the electrode surface. As previously discussed, changes in dimensions naturally leads to changes in surface area and edge defects (see Table 3.1 and Figure 3.7), and thus in turn, of electrode reactivity. [423] In fact, as confirmed by the evident plateau evolving in all samples below 0.9 V (Figure 4.6a), the charge associated to such irreversible process increases with decreasing flake sizes.

From the 2<sup>nd</sup> cycle onward, the specific capacity of Sample #1 and Sample #2 rapidly stabilizes without considerable fade, setting on values of  $341$  and  $366 \text{ mAh g}^{-1}$ , respectively, at the 20th cycle. The higher capacity provided by the smaller/thinner flakes appears to be partially lost upon cycling (Fig 6b). The flake size has a noticeable influence on the potential window in which the capacity is delivered. During lithiation and de-lithiation cycles, Samples #1 and Sample #2 provide more stable capacities, mainly delivered at low potentials in the  $0.005\text{-}0.2 \text{ V}$  and  $0.005\text{-}0.25 \text{ V}$  range for lithiation and de-lithiation, respectively), compared to Samples #3 and Sample #4 (Figure 4.6b). As the flakes dimension decreases, larger contributions arise from the more positive potential range instead (namely,  $0.2\text{-}3 \text{ V}$  and  $0.25\text{-}3 \text{ V}$  for lithiation and de-lithiation). Such behavior suggests that adsorption of  $\text{Li}^+$  (on the flakes' surface or edges) is the mechanism primarily responsible for charge storage in small lateral size FLG flakes, [202, 394] whereas, intercalation of  $\text{Li}^+$  (in between the layers) is the main process occurring in MLG flakes. By analyzing the capacity evolution upon the first 20

cycles (see Figure 6b), the  $\text{Li}^+$  adsorption mechanism (between 0.2/0.25-3 V) appears to be rather stable, and does not affect the electrodes cyclability in the case of big flake size based anodes (Samples #1 and Sample #2). Differently, it is evident that the decay observed for small flakes arises, for the largest extent, from the low potential region (below 0.25/0.2 V). This suggests that Li intercalation in small size MLG (sample #3) and FLG (sample #4) is somehow less reversible than in larger graphene flakes.

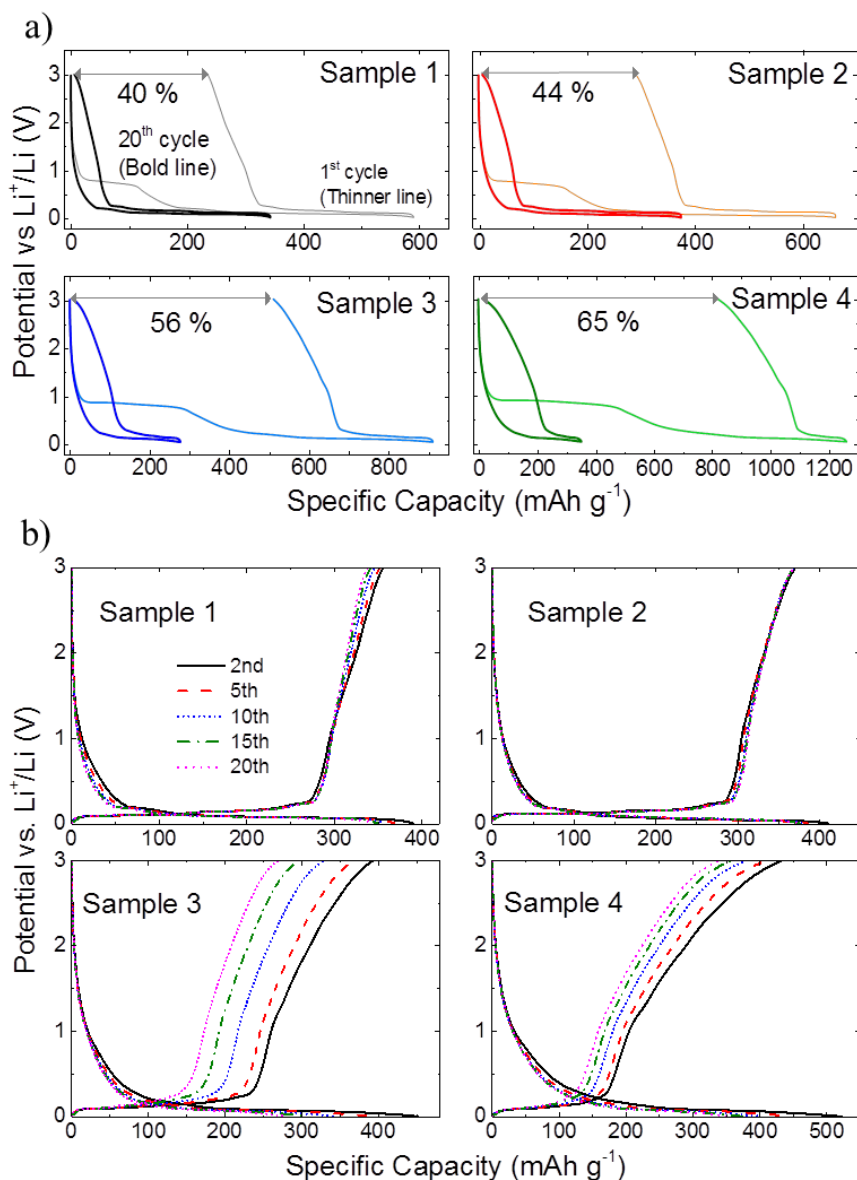


Figure 4.6. (a) Voltage profiles (1<sup>st</sup> cycle and 20<sup>th</sup> cycle) and (b) Voltage profiles evolution (in the cycle range 2-20) of the electrodes based on Sample #1, Sample #2, Sample #3, and Sample #4 (current density:  $0.1 \text{ A g}^{-1}$ ).

In order to get further understanding in the  $\text{Li}^+$  storage process in FLG- and MLG-based electrodes, a differential capacity analysis is carried out in the 0.005-0.3 V potential range, see Figure 4.7. For Samples #1 and #2 the  $\text{Li}^+$  storage process evolves with a series of very sharp peaks, demonstrating fast kinetics and high reversibility. As extensively reported in literature,



[424-426] the voltage peak sequence may be explained with the co-existence of phases, similar to those observed for graphite (*four-stage* or *staging mechanism*). [425] From the more diluted phase (>IV) to the fully lithiated one (I), all the main intercalation stages can be clearly detected in the samples with larger flakes (Samples #1 and #2). The different lithiation/de-lithiation stages are still detectable in Sample #3, however with weaker peaks for the IV to III and III to II stage-transitions. The former transition almost completely vanishes by further reducing the dimension of the flakes, *e.g.*, for Sample #4, suggesting that the majority of the flakes possesses a thickness lower than six layers, as indeed confirmed by the AFM (Figure 3.6 c and d) and Raman results (see Figure 3.8). The good news here is that the polarization associated with each intercalation stage, which is a kinetic parameter associated to the energy required to expand the van der Waals gap across two adjacent graphene layers by contrasting the repulsive interactions between guest species, [425] is not affected by the flake size. However, while large and thick flakes (Samples #1 and #2) show stable and highly reversible intercalation behavior, Samples #3 and #4 display a loss of such feature upon the first 20 cycles, which accounts for the aforementioned capacity fading (see Figure 4.6).

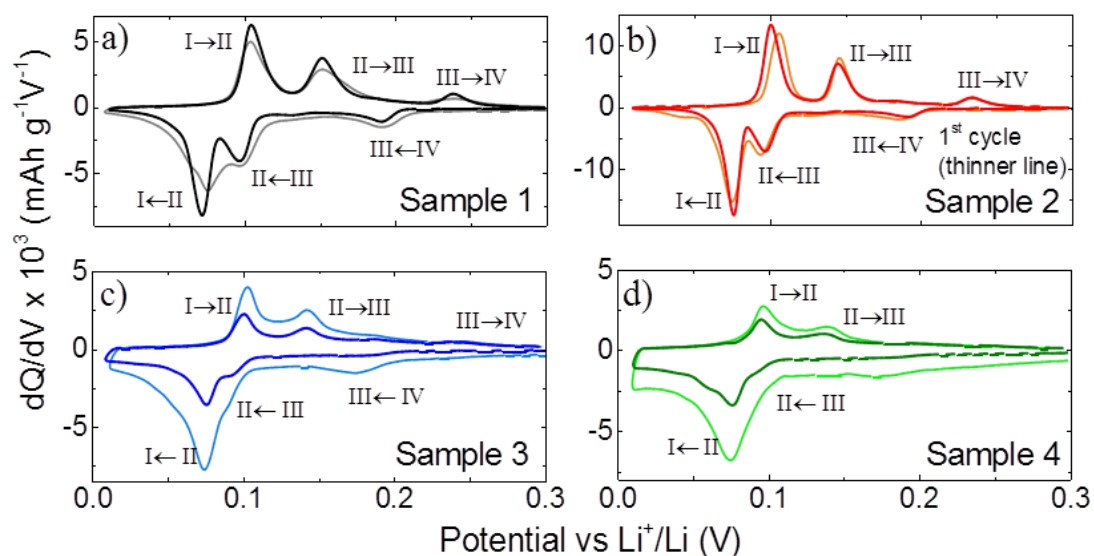


Figure 4.7. Differential capacity plots for the 1<sup>st</sup> (dash) and 20<sup>th</sup> (solid) cycle (current rate: 0.1 Ag<sup>-1</sup>) of the electrodes based on Sample #1, Sample #2, Sample #3, and Sample #4.

Small lateral size MLG- and FLG-flakes (Samples #3 and #4) would be expected to enable faster Li<sup>+</sup> diffusion due to the shorter diffusion lengths for ion transport compared to the large lateral size flakes. However, the rate capability test in Figure 4.8a shows that the capacities of Samples#3 and #4 are inferior to those of Samples#1 and #2 under all different current loads (0.1 to 10 A g<sup>-1</sup>). Noteworthy, Samples#1 and #2 provide good capacity retention up to 2 A g<sup>-1</sup> with respect to Samples #3 and #4. Unexpectedly, Sample#3 shows anomalously poor (but

reproducible) rate performance, whose cause remains unknown and will be investigated further. After the rate capability test, the electrodes based on Samples#1 and #2 show a full capacity recovery at  $0.1 \text{ A g}^{-1}$ , with a coulombic efficiency approaching 100%, whereas Samples#3 and #4 show a steeper capacity fading, *e.g.*, only 74% capacity retention for Sample#3).

A further contribution to a deeper understanding of the  $\text{Li}^+$  storage mechanism of MLG- and FLG-based electrodes is provided by EIS, see Figure 4.8b, c, d and e, which shows the typical signature of insertion electrodes, *e.g.*, a redox reaction which involves charge transfer resistance ( $R_{\text{CT}}$ ) coupled with insertion of guest ions contained in an electrolyte into the physical structure of a solid host). [195] The first feature, occurring at high frequency expressed for a phenomena such as  $\text{Li}^+$  diffusion through the SEI and/or with particle-particle and particle-collector contact resistances [427] both of which might indeed be in force in this study, with FLG- and MLG-flakes taking the role of the aforementioned particles. In fact, the slightly distorted shape of the semicircle suggests a scattered distribution of time constants, which makes it difficult to separate each contribution, as the sub-semicircles are highly overlapped due to very similar time constants.

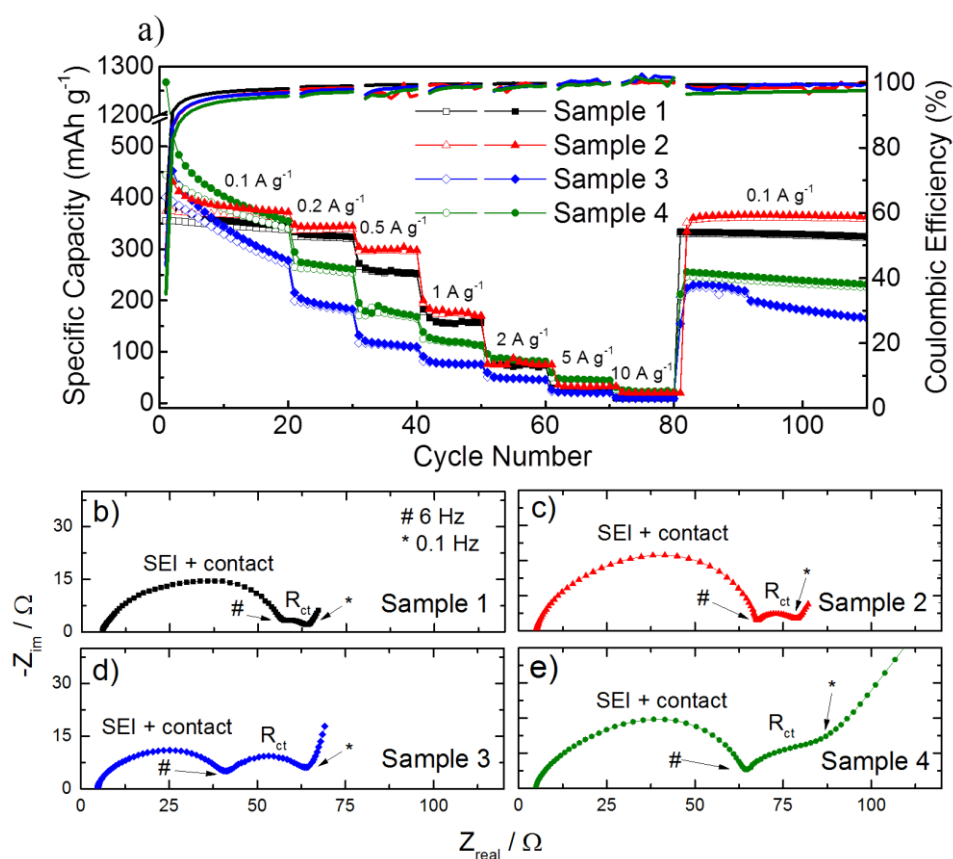


Figure 4.8. (a) Rate capability test of the graphene flake electrode samples. (b)-(e) Nyquist plots of partially lithiated graphene flake electrode samples (collected at 0.075 V) with the main contributions of SEI, contact, and charge transfer resistances are highlighted.

Moreover, both SEI and contact resistances are influenced by the flake dimension in a complex manner. Remarkably, the resistance of the mid-frequency semi-circle (from ca. 6-10 Hz to 0.1 Hz), attributed to the  $R_{CT}$  of the  $Li^+$  uptake process in the FLG- and MLG-based electrodes, displays a significant increase upon the decrease in the flake dimensions. This behavior is in agreement with several literature reports, [195, 428-430] where both theoretical and experimental results have in fact demonstrated that, as the (defect-free) graphene thickness approaches the single-layer limit, the lower Li-to-C binding energy and the stronger coulombic repulsions amongst  $Li^+$  may hinder high occupancy. [157, 430] It is evident that changes in dimensions can have great influences on the  $Li^+$  storage capability of FLG- and MLG- flakes. However, besides looking at the bare capacity values, we should not forget other parameters, which are equally important for practical application in LIBs. As the flakes size decreases, more capacity is delivered at high potentials. As a matter of fact, high lithiation/de-lithiation potential and sloping voltage profiles, however, might result in reduced and non-constant voltage output from the battery. The normalized charge and discharge cycles reported in Figure 4.9a and b clearly highlight to which extent the intercalation ( $< 0.2$  and  $< 0.25$  V) and adsorption ( $> 0.2$  and  $> 0.25$  V) storage contribute to the total state of charge (SOC) or depth of discharge (DOD) of the FLG- and MLG-based anodes. As summarized in Figure 4.9c, the intercalation is predominant in large and thick flakes, while it becomes less evident in the smaller and thinner ones. The contribution of adsorption in small and thin flakes is particularly relevant during  $Li^+$  extraction, where it can account for up to 65% of the whole delivered capacity, *e.g.*, in Sample#4). Such discrepancy between charge and discharge gives rise to a voltage hysteresis, common for carbonaceous materials. [408, 431] As shown in Figure 4.9d, the higher de-lithiation potentials, associated with the reduction in dimensions of the flakes, do increase considerably the electrode average voltage during discharge. This has a detrimental effect on the voltage efficiency which, ultimately, is reduced from 40% (Sample#1 and #2) to 25% (Sample#4).

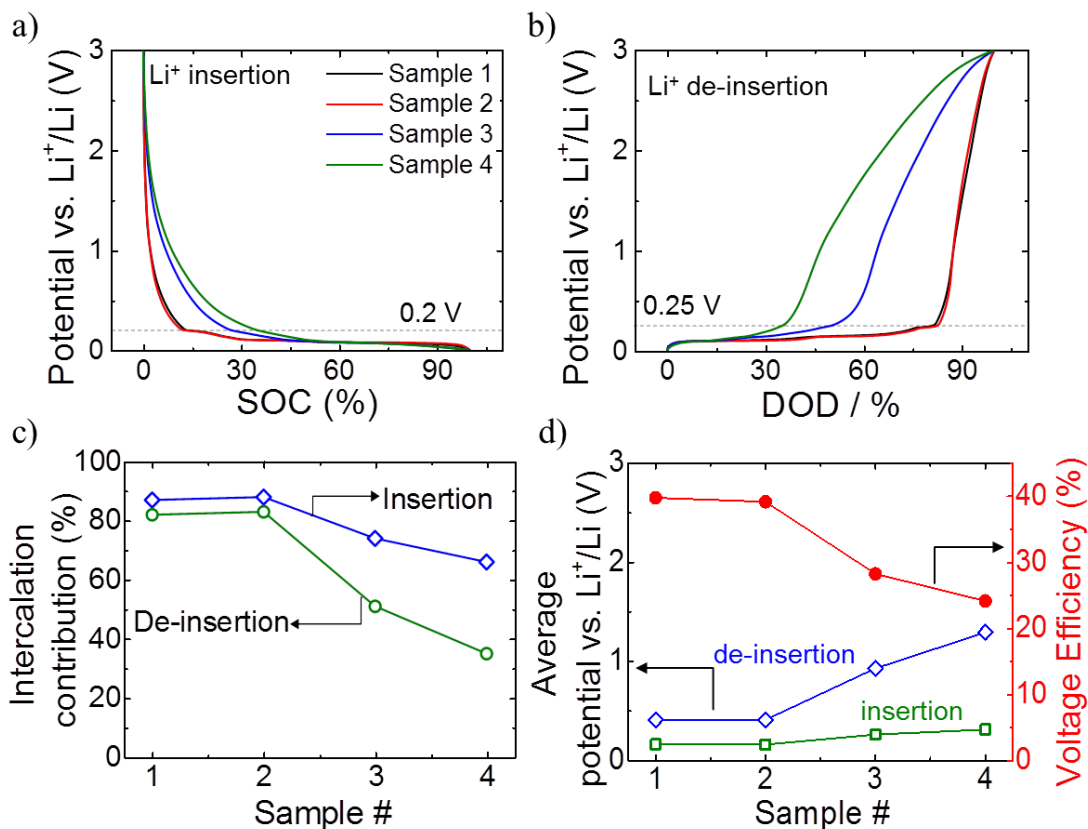


Figure 4.9. Normalized voltage profiles of the four graphene-based samples in terms of (a) SOC and (b) DOD (obtained from the 20th cycle at  $0.1 \text{ A g}^{-1}$ ). (c) Contribution of the intercalation mechanism to the total charge (calculated as the percentage of charge stored below 0.2 V or delivered above 0.25 V for lithiation and de-lithiation, respectively). (d) Effect of lithiation and de-lithiation average potentials on the voltage efficiency of the graphene anodes (the average potentials are obtained by the integral of the voltage profiles divided by the specific gravimetric capacity. The voltage efficiency is calculated as the ratio between de-lithiation and lithiation average potentials).

#### 4.4. Conclusion

In this chapter, graphene flakes (SLG/FLG) obtained by LPE of graphite in NMP and then followed by a solvent exchange process to re-disperse in environmentally friendly solvent, *e.g.*, EtOH, are used to fabricate a binder-free SLG/FLG-based anode for LIBs. This approach has several advantages in the production of anode for lithium ion batteries. First of all, the solvent exchange process can be considered as a fast, efficient and low-cost method to remove NMP from the graphene flakes, prior the deposition on the current collector. The solvent changes from NMP to EtOH can reduce the pollution and also facilitate the electrode deposition, leading to recycle the solvent (NMP) and then use for another LPE process of graphite. Secondly, the absence of any conductive agent and binder allows using a simple,

one-step process to deposit the SLG/FLG-based film onto the Cu substrate, avoiding time-consuming and costly preparation procedures. The binder-free SLG/FLG-based anode exhibits a reversible specific capacity of 503 mA h g<sup>-1</sup> after 100 cycles at a current density of 100 mA g<sup>-1</sup> with a coulombic efficiency > 99.5% (Figure 4.3b). Moreover, this anode is also used in a full-cell configuration (commercial LNMO as cathode), exhibiting a working voltage around 4.7 V and a reversible specific capacity of 100 mA h g<sup>-1</sup>. The one-step fabrication of binder-free SLG/FLG-based anode is paving the way to produce high energy/power density electrodes for LIBs through a facile coating process, with consequent reduction of the environmental impact and production costs.

Taking the advantages of the fabrication of binder-free graphene anode, a systematic and comprehensive study on the role of the morphology of MLG- to FLG-flakes on their electrochemical properties as anode for LIB is carried out. The results demonstrate that changes in the flakes dimension have indeed a significant impact into their capability of Li<sup>+</sup> storage. The decrease in flake lateral size/thickness does enable higher specific capacity values in the first cycle. Nevertheless, the capacity loss due to the SEI formation dramatically increases with the decrease in flake lateral size/thickness. Smaller flakes also show slower charge transfer kinetics attributable to lower Li-to-C binding energies and stronger coulombic repulsion among Li<sup>+</sup>, with respect to the larger counterparts. It should be noted that the staging behavior of graphite, the typical “fingerprint” of the intercalation mechanism, is always observed in all samples (Figure 4.7). However, the intercalation mechanism becomes less reversible with the shrinking of flake sizes. This phenomenon arises from surface passivation, trapping of Li<sup>+</sup> due to defects, or other effects that still need to be clarified by further studies. Furthermore, a larger contribution of Li<sup>+</sup> adsorption to the overall storage capacity can be clearly noticed passing from MLG to FLG flakes. This has a detrimental effect on the average de-lithiation voltage, which substantially increases with decreasing the flake dimension, resulting on lower voltage efficiency with respect to anodes based on MLG layer graphene. In general, the results in section 4.3 demonstrate that the mission of finding the ultimate anode material for LIBs is still on-going. Graphene is probably a part of it, but, may not be the main character for the task. Fully exploiting the advantages of graphene, *e.g.*, high conductivity and large surface area, to composite with other types of anode materials, *e.g.*, Si, TMOs and TMSs, can be more promising than graphene alone.

## Chapter 5:

# Application of molybdenum trioxide and molybdenum disulfide for lithium ion batteries

### 5.1. Introduction

Since graphene has been recognized more suitable as a supporting material in anodes for LIBS, the ever-increasing efforts have been devoted toward seeking promising 2D materials as active material in anodes to replace graphite. As discussed in **Chapter 1**, TMOs and TMSs are found to be the potential substitutions for graphite due to their very high specific capacity with respect to graphite. However, the issues of poor rate-capability and fast capacity fading, resulting from volume change and low intrinsic conductivity, are still limiting these materials for practical application in LIB anode. To overcome these issues, the strategies of nanostructure and composite/hybrid are proposed. This chapter introduces the studies on the production, processing and electrochemical properties of layered MoO<sub>3</sub> and MoS<sub>2</sub>, which are the typical representatives of TMOs and TMSs, respectively, for LIB anode.

In the field of LIBs, orthorhombic MoO<sub>3</sub> ( $\alpha$ -MoO<sub>3</sub>), the most thermodynamically stable phase of MoO<sub>3</sub>, [432, 433] has been demonstrated as a very promising anode material, thanks to its high theoretical specific capacity of 1117 mAh g<sup>-1</sup>. [203, 204] Additionally, the interlayer spacing as large as 0.69 nm of  $\alpha$ -MoO<sub>3</sub> with respect to that of graphite (0.34 nm) guarantees its Li<sup>+</sup> host capability. [434, 435] Moreover, its higher intercalation voltages (1.5 – 2.3V vs. Li/Li<sup>+</sup>) compared to that of graphite (< 0.4 vs Li/Li<sup>+</sup>) could reduce the safety problems caused by the electrolyte decomposition, especially for the utilization in EVs, HEVs. [436] Similar to  $\alpha$ -MoO<sub>3</sub>, MoS<sub>2</sub> has drawn significant interest as promising substitutes for the graphite thanks to its high theoretical capacity (670 mAh g<sup>-1</sup>), [437] large interlayer spacing (0.62 nm) [72] and high intercalation voltages (~ 0.5-1.1 V vs. Li/Li<sup>+</sup>). [216] Nevertheless, there are issues that still need to be solved for these materials: (i) the fast capacity fading of the bulk MoO<sub>3</sub> and MoS<sub>2</sub> because of the volume change during lithiation/de-lithiation, [72, 217, 218] (ii) the low rate-capability due to the low electrical conductivity of MoO<sub>3</sub> and MoS<sub>2</sub>. [214, 219-221] To overcome these issues, one of the most encouraging strategies for these 2D materials are reducing the lateral size of their bulk counterpart by nanostructuring, [4, 182, 438-441] and mixing the resulting nanostructures of MoO<sub>3</sub> and MoS<sub>2</sub> with carbon-based nanomaterials, such as amorphous carbon, [330, 442, 443] CNTs [167, 209, 444] and graphene, [211, 241, 445] to form composite/hybrid materials. Recently, the exploitation of various nanostructures

of both MoO<sub>3</sub> and MoS<sub>2</sub> composite/hybrid material as anode materials have demonstrated significant improvements, with respect to the bulk MoO<sub>3</sub> and MoS<sub>2</sub>, in term of specific capacity [446-449] and electrochemical stability. [438, 442, 450] Nevertheless, the costly production processes used, [438, 439, 442, 445] *e.g.*, CVD [206, 438, 451] or hydrothermal methods, [168, 330, 439, 440, 442] pose scalability challenges towards practical industrial application. [155, 206, 452] Additionally, the use of toxic materials [306, 453, 454] as well as binders [4, 455, 456] are also limiting factors for practical use.

This chapter firstly presents the investigation on production of nano-sized MoO<sub>3</sub>, MoS<sub>2</sub> flakes and their carbon-based hybrid/composite. Secondly, the insightful studies on their electrochemical performances are carried out to demonstrate the effects of carbon-based nanomaterials on the electrochemical performances of MoO<sub>3</sub> and MoS<sub>2</sub>. The LPE processes [237, 238] of bulk MoO<sub>3</sub> and MoS<sub>2</sub> in IPA are exploited as a facile and effective method for producing nano-sized MoO<sub>3</sub> and MoS<sub>2</sub> flakes, see section 2.1.3.3 and 2.1.3.4 for the detailed procedures. The hybrid structure of SWNTs-bridged MoO<sub>3</sub> is synthesized by mixing multilayer MoO<sub>3</sub> flakes with solution processed SWNTs and used as an active binder-free material for LIBs. Both the MoO<sub>3</sub> exfoliation process and the SWNTs dispersing are carried out in isopropanol, allowing a simple deposition onto the Cu substrate. The designed binder-free solution processed hybrid MoO<sub>3</sub>/SWNTs anode displays a specific capacity of 865 mAhg<sup>-1</sup> at 100 mA g<sup>-1</sup> after 100 cycles, with a columbic efficiency of 99.7%. The SWNTs addition determines a network structure with the MoO<sub>3</sub> providing (i) long channels for electronic charge transport; (ii) an active anode material, instead of polymeric binder, offering extra capacity for Li<sup>+</sup> storage; (iii) a buffer frame in the electrode, which reduces the capacity fading caused by the volume variation of MoO<sub>3</sub> flakes during the lithiation/delithiation process. To further confirm the essential roles of SWNTs, the electrochemical properties of the multilayers MoO<sub>3</sub> combined with CB nanoparticles are characterized. This structure is not able to create the network structure seen with SWNTs, yielding a significant capacity fading of the resulting battery. These results set the basis for the exploitation of exfoliated 2D MoO<sub>3</sub> sheets as anodic materials in LIBs. Meanwhile, the MoS<sub>2</sub>/C hybrids with three different weight ratios of carbon are formed by thermal decomposition of PAA (as carbon source) in Ar atmosphere. The hybrid structures consist of exfoliated MoS<sub>2</sub> flakes incorporated in carbon network. The as-prepared MoS<sub>2</sub>/C hybrids are deposited onto Cu substrate, in order to investigate the effect of different carbon contents on the electrochemical properties of MoS<sub>2</sub>. The MoS<sub>2</sub>/C electrode with optimized carbon content features a high reversible specific capacity of 521 mAh g<sup>-1</sup> after 100 cycles, with a columbic efficiency of 99.7%. The results confirm that carbon network not only improves the electrical conductivity of electrode by

facilitating the electron transport, but also acting as a buffer layer for active materials to avoid its volume change upon cycling. Through the optimization of the electrochemical properties, our study demonstrates a process that is promising for a production of MoS<sub>2</sub>/C hybrid for Li<sup>+</sup> storage application.

## **5.2. Carbon nanotubes-bridged MoO<sub>3</sub> hybrid structure as high performance anode for lithium ion batteries**

This section provides a simple, low-cost, non-toxic method to fabricate binder-free hybrid MoO<sub>3</sub>/SWNTs electrode, by a solution processing of SWNTs, and then mixing with MoO<sub>3</sub> flakes and depositing the mixture on Cu substrate. This is a promising strategy for exploiting the exfoliated MoO<sub>3</sub> flakes in LIB anodes, delivering high energy and power densities as well as long lifetime. As discussed in section 2.1.3.3, the MoO<sub>3</sub> flakes in dispersion are obtained by LPE of pristine MoO<sub>3</sub> in IPA, while the SWNTs and CB are dispersed in IPA by sonication. The diameter of SWNTs is estimated to be in the ~1.37–1.45 nm range by Raman spectroscopy whereas the diameter of the SWNTs bundle is ~10 nm according to TEM images and the corresponding statistical analysis, see Figure 3.10. The TEM images of Figure 3.11b display the MoO<sub>3</sub> flakes with lateral sizes ranging from 50 to 300 nm. The hybrid MoO<sub>3</sub>/SWNTs shown in Figure 3.11d clearly demonstrates that the bundles of SWNTs act as bridges to connect isolated MoO<sub>3</sub> flakes, forming an interconnected network in the mixture of these two materials. The as-prepared samples are then exploited for the realization of electrodes, *e.g.*, anodes, for LIBs. In particular, solution processed MoO<sub>3</sub> flakes and the hybrid MoO<sub>3</sub>/SWNTs mixed with ratio of 9:1 are deposited onto Cu substrates. A reference sample, *e.g.*, MoO<sub>3</sub> mixed with 10% CB, is also prepared by using the same process. The mass loading of MoO<sub>3</sub>, MoO<sub>3</sub>/SWNTs and MoO<sub>3</sub>/CB in the corresponding electrodes has been calculated as 0.80 mg, 0.74 mg and 0.75 mg, respectively. The morphology of the MoO<sub>3</sub>/SWNTs and MoO<sub>3</sub>/CB electrodes is characterized by SEM. The SEM image of the MoO<sub>3</sub> electrode (Figure 5.1a) shows MoO<sub>3</sub> flakes with regular polygonal shapes, which are homogeneously distributed onto the Cu substrate. Figure 5.1b shows how the morphology of the hybrid MoO<sub>3</sub>/SWNTs is dominated by the MoO<sub>3</sub> flakes inserted in the mesoporous network of SWNTs bundles. In contrast, the morphology of the MoO<sub>3</sub>/CB electrode is dominated by large aggregates of CB, ~ 400 nm in diameter, with a few MoO<sub>3</sub> flakes observed and pointed with white arrows in the image of Figure 5.1c. In order to corroborate the presence of SWNTs, MoO<sub>3</sub> or CB, Raman spectroscopy is performed on the three electrodes of MoO<sub>3</sub>, MoO<sub>3</sub>/SWNTs and MoO<sub>3</sub>/CB samples deposited onto Cu substrates. In Figure 5.1d, the typical Raman features of MoO<sub>3</sub>, which has been shown in Figure 3.11a, [310, 457, 458] can be observed in all three samples. However, it is worth to mention that the



Raman signals of SWNTs and CB dominates the Raman spectra of the MoO<sub>3</sub>/SWNTs and MoO<sub>3</sub>/CB electrodes, respectively.

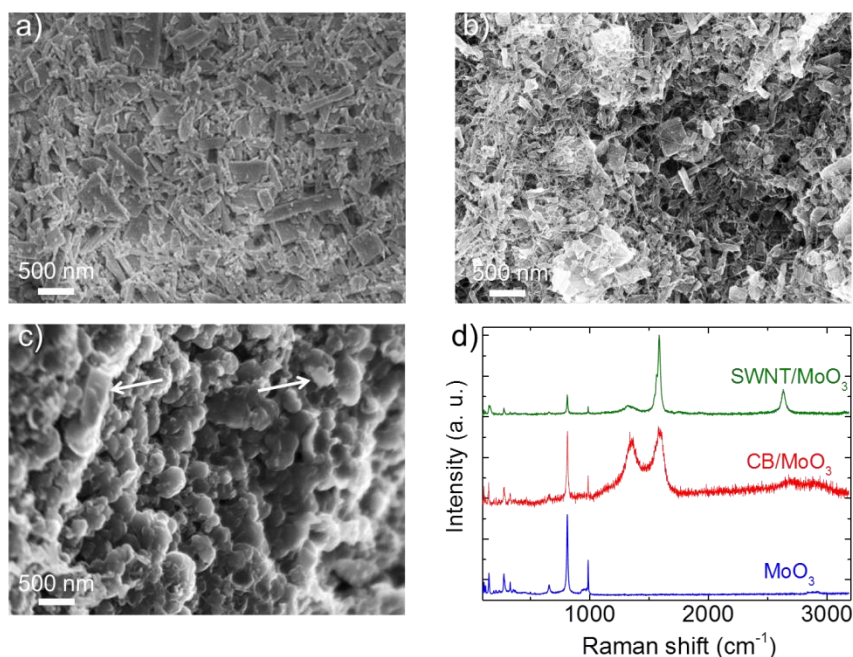
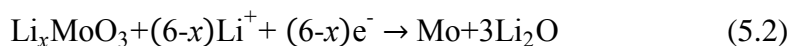
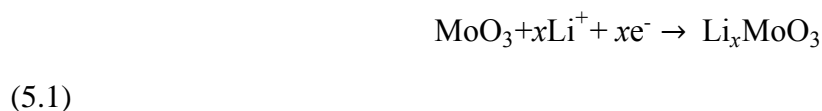


Figure 5.1. Scanning electron microscope images of (a) MoO<sub>3</sub>, (b) MoO<sub>3</sub>/SWNTs and (c) MoO<sub>3</sub>/CB deposited onto Cu substrates. (d) Raman spectra of the MoO<sub>3</sub>/SWNTs (green), MoO<sub>3</sub>/CB (red) and MoO<sub>3</sub> (blue) electrodes, deposited onto Cu substrates.

The CV results (Figure 5.2a) of the three samples, *e.g.*, MoO<sub>3</sub>, MoO<sub>3</sub>/CB and MoO<sub>3</sub>/SWNTs are collected at a scan rate of 50  $\mu\text{Vs}^{-1}$  starting from 5 mV vs Li/Li<sup>+</sup> potential, to cover the lithiation processes in both MoO<sub>3</sub> and SWNTs. [459] In the first reduction sweep, the MoO<sub>3</sub> exhibits two peaks at 2.3 and 2.7 V, which can be linked with the insertion of Li ions into the interlayers of the MoO<sub>3</sub> structure to form Li<sub>x</sub>MoO<sub>3</sub>, and another peak at 0.4 V, which corresponds to the conversion reaction of Li<sub>x</sub>MoO<sub>3</sub> into Mo and Li<sub>2</sub>O. [210, 460] The two processes determine, the accommodation of six Li ions in each MoO<sub>3</sub>, reaching theoretical specific capacity of 1117 mAhg<sup>-1</sup>, [203, 204] as summarized by equation 5.1 and 5.2. [210, 460]



In the reverse oxidation process, metallic Mo is converted into amorphous MoO<sub>2</sub> in the 1.0 V to 2.2 V range. [210] From the 2<sup>nd</sup> cycle onward, a clear shift is observed in the conversion reaction peak at 0.4 V, which is consistent with the formation, upon oxidation, of MoO<sub>2</sub> with

lower reactivity with respect to  $\text{MoO}_3$ . [171] Furthermore, in the second cycle a new peak, at 1.5 V, appears which can be assigned to the lithium insertion into amorphous  $\text{MoO}_2$ . [171, 461] For the  $\text{MoO}_3$  and the hybrid  $\text{MoO}_3/\text{CB}$  samples, the reduction peaks at 1.5 V and 0.4 V rapidly disappear during the following 8 cycles. On the contrary, in the case of  $\text{MoO}_3/\text{SWNTs}$  sample the intensity of these two peaks is maintained from cycle 2 to cycle 10, leading to a remarkable improvement on its electrochemical stability with respect to the other two samples.

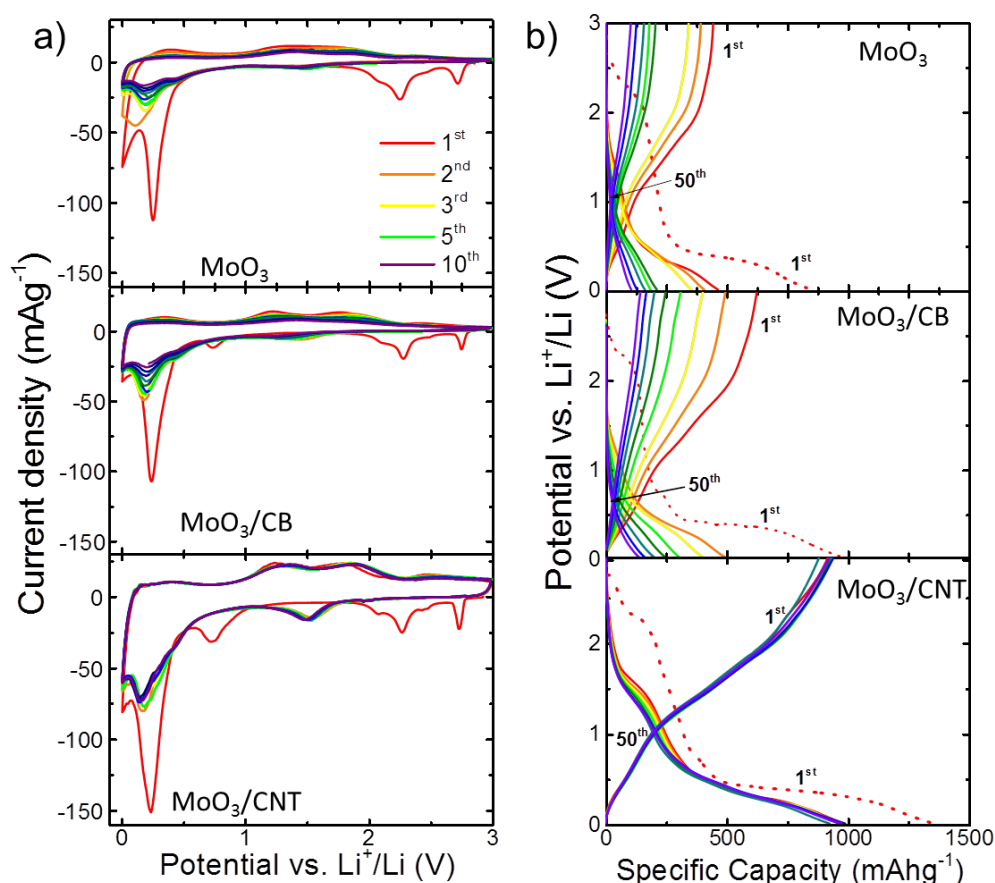


Figure 5.2. (a) Cyclic voltammograms and (b) Charge/discharge voltage profiles of  $\text{MoO}_3$ ,  $\text{MoO}_3/\text{CB}$  and  $\text{MoO}_3/\text{SWNTs}$  as anodes against Li foil in half cell configuration.

Figure 5.2b shows the charge/discharge voltage profiles of bulk  $\text{MoO}_3$  at  $100 \text{ mA g}^{-1}$ , in order to get a complete electrochemical response for the Li ion transfer, [462] during the lithiation/de-lithiation process at the anode. In the 1<sup>st</sup> charge (lithiation) process, two plateaus at 2.3 V and 0.4 V are observed in all the three samples. These two plateaus have already been attributed to the formation of  $\text{Li}_x\text{MoO}_3$  and its following conversion reaction into metallic Mo and  $\text{LiO}_2$ , respectively. [210, 460] These reactions have also contribution on the large initial specific capacity obtained in the three samples, e.g.,  $864 \text{ mAh g}^{-1}$  for  $\text{MoO}_3$ ,  $1332 \text{ mAh g}^{-1}$  for  $\text{MoO}_3/\text{CB}$ , and  $1357 \text{ mAh g}^{-1}$  for  $\text{MoO}_3/\text{SWNTs}$ . The higher initial specific capacity shown by

both the MoO<sub>3</sub>/SWNTs and MoO<sub>3</sub>/CB samples, compared with the MoO<sub>3</sub> sample, can be associated to the enhanced electrical conductivity in the hybrid electrodes due to the presence of the carbon nanomaterials. [439, 463] On the contrary, significant differences for the three samples are shown by the specific capacities obtained at the 1<sup>st</sup> discharge (de-lithiation) process. In fact, initial specific capacities of 481, 625 and 962 mAhg<sup>-1</sup> are achieved for the MoO<sub>3</sub>, MoO<sub>3</sub>/CB, and MoO<sub>3</sub>/SWNT samples, respectively. For all the 3 samples, the capacity drop between the 1<sup>st</sup> charge and discharge processes (Figure 5.3a), is caused by the combination of several irreversible processes, including: (i) the SEI formation; [155] (ii) the structural modulation during Li<sup>+</sup> insertion/extraction into the inter-layers and intra-layers of MoO<sub>3</sub>; [171] (iii) the conductivity loss caused by the electrode pulverization upon lithiation/de-lithiation. [464]

For the MoO<sub>3</sub> and MoO<sub>3</sub>/CB samples, a coulombic efficiency as low as 55.7% and 46.9% is observed at the 1<sup>st</sup> cycle, respectively, see Figure 5.3a. Moreover, both samples show capacity fading upon cycling, which is the main drawback of MoO<sub>3</sub> anodes due to the pulverization of the electrode, [439] with capacity loss of 84% and 64%, respectively, after 60 cycles. Alternatively, the MoO<sub>3</sub>/SWNTs sample shows a coulombic efficiency as high as 70.9% at the 1<sup>st</sup> cycle, a value which is significantly enhanced compared to the MoO<sub>3</sub> and MoO<sub>3</sub>/CB samples. Additionally, the MoO<sub>3</sub>/SWNTs sample shows a tangible improvement on the stability of the electrochemical performance, delivering reversible capacity of ~950 mAh g<sup>-1</sup> at 50<sup>th</sup> cycle, with only a 1.2% capacity loss from the 1<sup>st</sup> cycle.

In order to further understand the different electrochemical performance of the three MoO<sub>3</sub>-based electrodes, the EIS for all the three samples at charged state, after 60 cycles are carried out. The Nyquist plots of the electrodes are presenting a semi-circle at high-to-medium frequency, [465] demonstrating the different interface resistances in the three samples. The interface resistance occurring at high frequency is associated with phenomena such as Li<sup>+</sup> ion diffusion through the SEI film and/or in the active material, and the contact layer between the electrode and current collector. [427, 466, 467] As obtained from Figure 5.3b, the interface resistance of the MoO<sub>3</sub> sample is ~160 Ω, which is significantly reduced to ~80 Ω for the MoO<sub>3</sub>/CB sample. The MoO<sub>3</sub>/SWNTs hybrid structure gives the lowest value of interface resistance, *e.g.*, ~40 Ω, which is one fourth and one half with respect to the ones shown by the MoO<sub>3</sub>- and MoO<sub>3</sub>/CB-based electrodes, respectively. The reduction of the interface resistance upon the addition of carbon additives, especially SWNTs, compared with the MoO<sub>3</sub>, might be attributed to the different structural morphology of the electrodes after lithiation/de-lithiation processes. [439, 465]

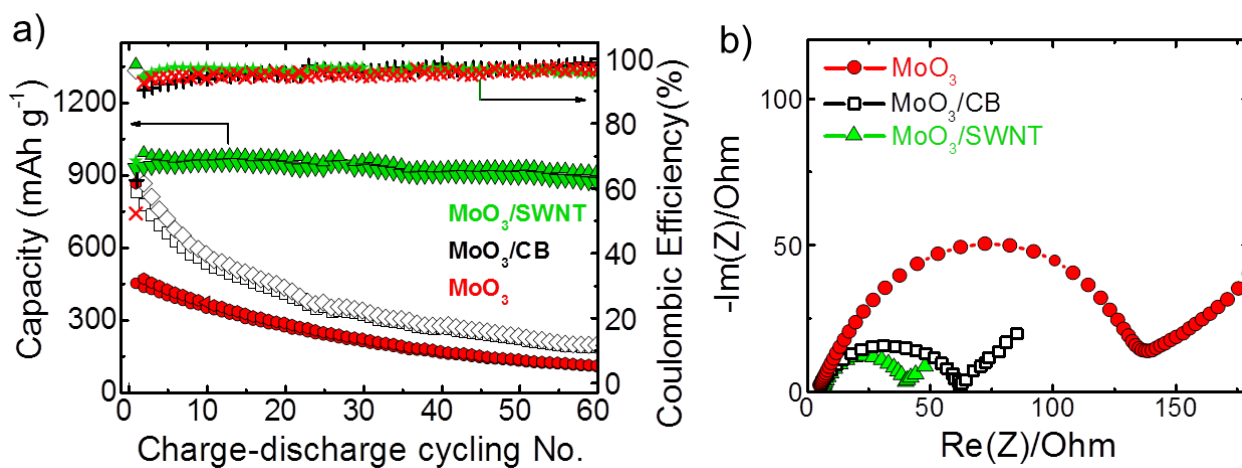


Figure 5.3. (a) Specific capacity and coulombic efficiency over charge/discharge galvanostatic cycles, and (b) Electrochemical impedance spectroscopy of MoO<sub>3</sub> (red), MoO<sub>3</sub>/SWNTs (green) and MoO<sub>3</sub>/CB (black) as anodes against Li foil in half cell configuration.

Therefore, in order to understand the relation between the electrochemical performance of the three samples and their structural morphology after charge-discharge cycles, the post-mortem SEM measurements on MoO<sub>3</sub>, MoO<sub>3</sub>/CB and MoO<sub>3</sub>/SWNTs electrodes after 60 charge/discharge cycles are carried out. As shown in Figure 5.4a, the MoO<sub>3</sub> electrode clearly presents cracks and fractures with width of 200-400 nm, likely caused by the volume change during the charge/discharge cycles. These cracks determine a drop in the electrical conductivity, with consequent capacity fading, [204, 468] as clearly presented in Figure 5.3. As shown in Figure 5.4b, large cracks over 1  $\mu\text{m}$  are observed in the MoO<sub>3</sub>/CB electrode as well.

Even if, compared to free MoO<sub>3</sub>, the presence of CB seems able to furnish better electrical conductivity during the first cycles, the MoO<sub>3</sub>/CB electrodes still suffer a remarkable capacity fading upon cycling. This is likely due to the inability of CB to keep the anode material in continuous contact with the current collector. [468, 469] Although the MoO<sub>3</sub>/SWNTs sample shows cracks after 60 cycles, the cracks are much narrower with respect to the ones presented by the MoO<sub>3</sub> and MoO<sub>3</sub>/CB electrodes. Moreover, the carbon network of nanotubes ensures high electrical conductivity upon the expansion/contraction processes of MoO<sub>3</sub>. This conductive framework is therefore beneficial for both mechanical stability [470] and the specific capacity of the anodes.

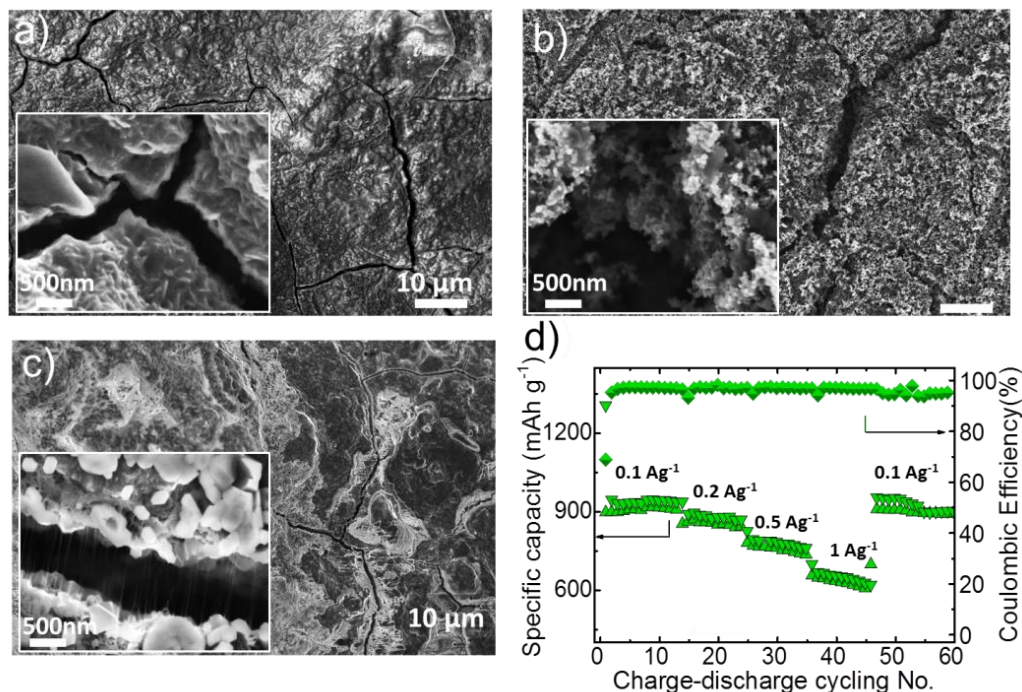


Figure 5.4. SEM images of (a) MoO<sub>3</sub>, (b) MoO<sub>3</sub>/CB, (c) MoO<sub>3</sub>/SWNTs electrodes after 60 charge/discharge galvanostatic cycles and (d) Specific capacity at different current densities of MoO<sub>3</sub>/SWNTs anodes measured against Li foil in half cell configuration.

In order to further investigate the electrochemical activities of the MoO<sub>3</sub>/SWNTs hybrid electrode at fast charge/discharge processes, the MoO<sub>3</sub>/SWNTs electrode is charged/discharged at different specific currents. As shown in Figure 5.4d, the specific capacities of MoO<sub>3</sub>/SWNTs electrode after 10 cycles at each specific current have been recorded as ~956 mAh g<sup>-1</sup>, to ~863 mAh g<sup>-1</sup>, ~757 mAh g<sup>-1</sup>, ~645 mAh g<sup>-1</sup>, when the specific currents varies from 0.1 to 0.2, 0.5 and 1 A g<sup>-1</sup>, respectively. A drop of ~30% with the specific current rising from 0.1 to 1 A g<sup>-1</sup>, and a coulombic efficiency of ~99 % strongly suggested that the MoO<sub>3</sub>/SWNTs hybrid electrode is very promising for the application of fast charge-discharge devices.

From the obtained results of MoO<sub>3</sub>, MoO<sub>3</sub> CB and MoO<sub>3</sub>/SWNTs electrodes, it is clear that the SWNTs addition (10% with respect to the MoO<sub>3</sub> flakes) is beneficial for the electrochemical properties of the as-produced electrodes. Thus, in order to further investigate the contribution of the SWNTs to the MoO<sub>3</sub>/SWNTs hybrid anode, another two electrodes with weight ratios of 20% and 30% for SWNTs, are prepared following the preparation processes described in section 2.4.1.2. As shown in Figure 5.5a, b and c, the three MoO<sub>3</sub>/SWNTs hybrid anodes show a homogenous coverage of SWNTs and MoO<sub>3</sub> flakes onto the Cu substrates. The presence of the hybrids SWNTs and MoO<sub>3</sub> flakes is confirmed by the

Raman spectra of the three samples shown in Figure 5.5d. The spectra are normalized to the signal of  $G^+$  peak of the SWNTs. The spectra show the Raman peaks of the  $\text{MoO}_3$  in the region of  $200\text{-}1000\text{ cm}^{-1}$ , which decrease in intensity, with respect to the  $G^+$  peak of the SWNTs, as the percentage of SWNTs increases in the  $\text{MoO}_3/\text{SWNTs}$  hybrid. For the  $\text{MoO}_3/\text{SWNTs}$ -30% hybrid anode the Raman spectrum is dominated by the SWNTs signal due to their high Raman cross section. [29, 471, 472]

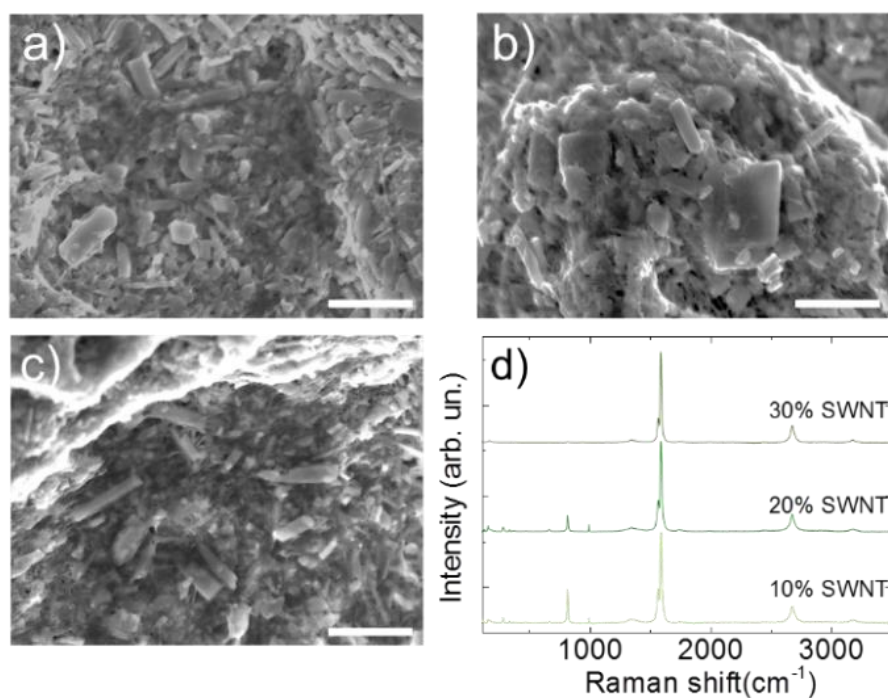


Figure 5.5. Scanning electron microscope images of  $\text{MoO}_3/\text{SWNTs}$  hybrids coated onto Cu substrates with SWNTs weight ratio of (a) 10%, (b) 20% and (c) 30%, with respect to the  $\text{MoO}_3$  flakes. All scale bars are  $1\ \mu\text{m}$ . (d) Raman spectra, acquired with an excitation wavelength of  $514.5\text{ nm}$ , of  $\text{MoO}_3/\text{SWNTs}$  hybrids with 10% (light green), 20% (green), and 30% (dark green) SWNTs relative content with respect to  $\text{MoO}_3$ .

The CV, galvanostatic charge/discharge and EIS measurements are carried out to understand the effects of SWNTs/ $\text{MoO}_3$  weight ratio on the electrochemical performances of the  $\text{MoO}_3/\text{SWNTs}$  hybrid anodes. As shown in Figure 5.6a, the CV curves of the three  $\text{MoO}_3/\text{SWNTs}$  hybrid samples have clearly demonstrated the insertion of Li ions into the interlayers of the  $\text{MoO}_3$  structure to form  $\text{Li}_x\text{MoO}_3$  at  $2.3\text{ V}$ . Additionally, the irreversible reduction peak at  $0.4\text{ V}$  observed in all the three samples can be attributed to the conversion reaction of  $\text{Li}_x\text{MoO}_3$  into Mo and  $\text{LiO}_2$ . A new peak at  $1.5\text{ V}$  is appearing from the second cycle onward, representing the Li ion insertion into amorphous  $\text{MoO}_2$ . Moreover, the intensity of the aforementioned peak drops significantly at the second cycle, due to the lower reactivity of  $\text{MoO}_2$  compared to the one of  $\text{MoO}_3$ . [3, 473] However, the intensity drop of this peak (at

0.4 V) is reducing with the increase of the SWNTs percentage in the MoO<sub>3</sub>/SWNTs, as a result of the decreasing contribution from MoO<sub>3</sub> reaction in the hybrid structure. Moreover, two peaks at 1.5 V and 0.4 V in all three samples are observed without any shift or intensity drop in the following cycles from 2 to 10, leading to the stable electrochemical performance of the MoO<sub>3</sub>/SWNTs hybrid anodes.

The post-mortem SEM images of the three MoO<sub>3</sub>/SWNTs electrodes shown in Figure 5.6b, c and d clearly demonstrate that the SWNTs in the MoO<sub>3</sub>/SWNTs electrode create a network between the cracked “islands” following the MoO<sub>3</sub> volume change during charge/discharge cycles. [439, 465] Notably, the width of the cracks is reducing with the percentage increase of SWNTs in the MoO<sub>3</sub>/SWNT hybrids. A possible explanation could be linked with the fact that the increasing amount of SWNTs, as buffer between the MoO<sub>3</sub> flakes, can efficiently attenuate the volume change during charge/discharge cycles, reducing the mechanical degradation of the electrodes and leading to stable electrochemical performances.

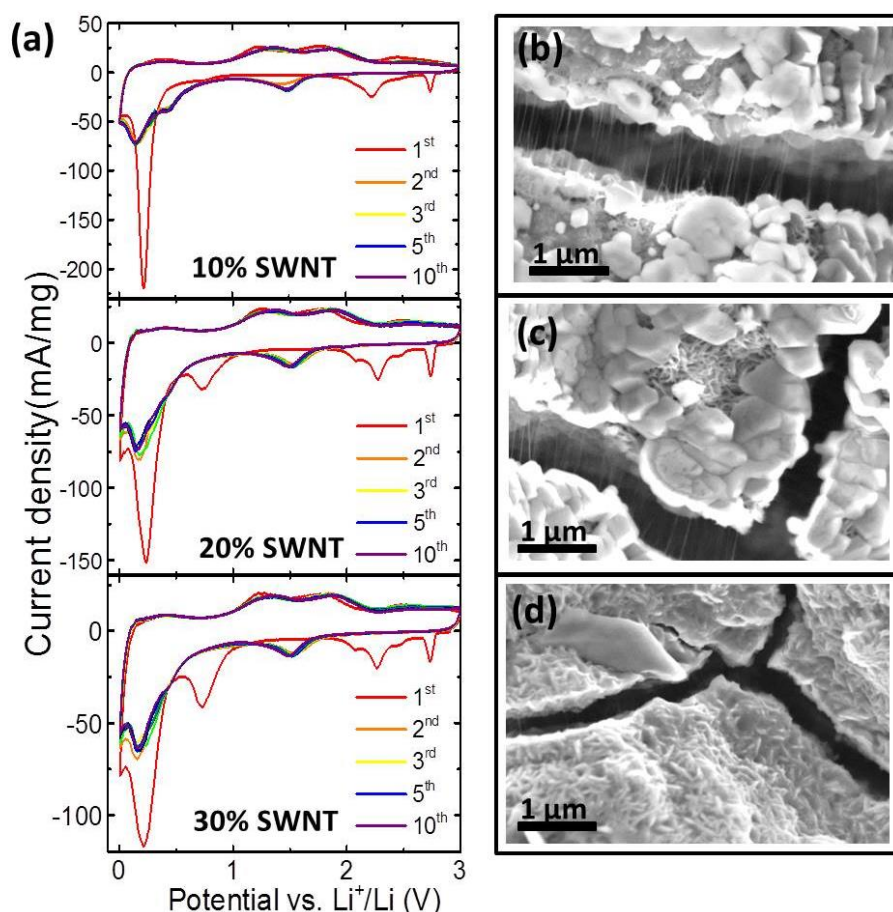


Figure 5.6. (a) Cyclic voltammograms of MoO<sub>3</sub>/SWNTs hybrids with different SWNT weight ratios as anodes against Li foil in half cell configuration. Scanning electron microscope images of (b) MoO<sub>3</sub>/10%SWNTs, (c) MoO<sub>3</sub>/20%SWNTs and (d) MoO<sub>3</sub>/30%SWNTs electrodes after 100 charge/discharge galvanostatic cycles.

As shown in Figure 5.7a, while the percentage of SWNTs in the MoO<sub>3</sub>/SWNT electrodes rises from 10% to 30%, the initial capacities of the three samples reach 1357, 1161 and 1044 mAhg<sup>-1</sup>, with corresponding discharge capacity at the first cycle of 927, 675, and 566 mAhg<sup>-1</sup>, respectively. The specific capacity and coulombic efficiency (Figure 5.6a) demonstrate that all the hybrid electrodes with different mixed ratios show remarkable stable cyclability up to 50 cycles, if compared with the MoO<sub>3</sub> anode.

The EIS results of the 3 samples shown in Figure 5.7b, demonstrates how the higher is the percentage of SWNTs in the hybrid MoO<sub>3</sub>/SWNTs electrodes, the lower is their R<sub>CT</sub>. In fact, R<sub>CT</sub> values of ~40 Ω, ~30 Ω and ~17 Ω have been obtained for the sample with 10%, 20% and 30% of SWNTs with respect to the MoO<sub>3</sub> flakes, respectively. However, although higher percentage of SWNTs, *e.g.*, 20-30%, in the hybrid structure can provide better electrical conductivity, *e.g.*, R<sub>CT</sub> of 30 Ω and 17 Ω for the electrodes containing 20% and 30% of SWNTs with respect to the MoO<sub>3</sub> flakes) this is not directly associated to an increase of the electrode specific capacity. In fact, the increasing percentage of SWNTs has determined a tangible decrease of the specific capacity with respect to the total loading of MoO<sub>3</sub>/SWNT hybrid electrodes. This could be linked with the high irreversible capacity that affect CNTs-based anode for LIBs. [254] In fact, the irreversible capacity increases from 32% for the 10% MoO<sub>3</sub>/SWNTs sample to 46% in the case of 30% MoO<sub>3</sub>/SWNTs one. Moreover, the 10% MoO<sub>3</sub>/SWNTs sample shows the highest capacity retention (71.6% after 50 cycles) over charge/discharge cycles, obtained by dividing the charge-capacity to the initial capacity (Figure 5.2a), amongst the electrodes, *e.g.*, the hybrids MoO<sub>3</sub>/SWNTs and the MoO<sub>3</sub> one.

Moreover, the specific capacity of each electrode is calculated, as shown in Figure 5.7d, labeled by different SWNTs content from 0 to 30%. The specific capacities are calculated using the mass loading of MoO<sub>3</sub> and MoO<sub>3</sub>/SWNTs, respectively. In both cases, the 10% SWNTs sample reaches the highest specific capacity of 1028 mAhg<sub>MoO<sub>3</sub></sub><sup>-1</sup> and 926 mAhg<sub>MoO<sub>3</sub>/SWNTs</sub><sup>-1</sup>, see Figure 5.7d, which represent the 92% and 82%, respectively, of the theoretical specific capacity of MoO<sub>3</sub>. [203, 204] The MoO<sub>3</sub>/SWNTs binder-free anode in this work favorably compares with state of the art MoO<sub>3</sub>-based LIB, as reported in literature. [154, 211, 432, 439, 474, 475] The reported electrochemical analysis indicates that the addition of 10% SWNTs in the hybrid structure with MoO<sub>3</sub> flakes represents the best compromise in term of mechanical and electrochemical properties of the as-produced anodes.



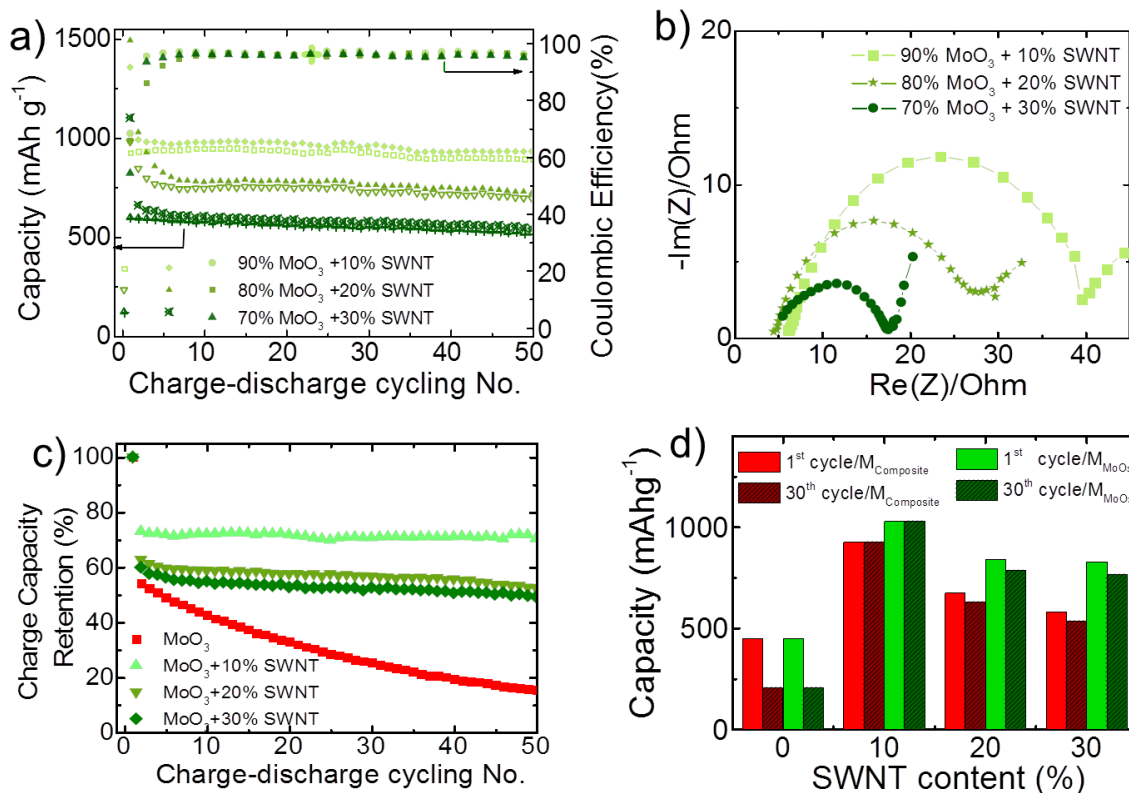


Figure 5.7. (a) Specific capacity and coulombic efficiency over charge/discharge galvanostatic cycles, and (b) Electrochemical impedance spectroscopy of MoO<sub>3</sub>/SWNTs hybrid electrodes with different SWNTs weight ratios as anodes against Li foil in half cell configuration. (c) Capacity retention of MoO<sub>3</sub>/SWNTs hybrid anodes and d) Specific capacity of MoO<sub>3</sub>/SWNTs hybrid anode calculated with respect the weight of MoO<sub>3</sub> (red) and the hybrid structures, respectively (green).

### 5.3. Molybdenum disulfide flakes/amorphous carbon hybrid as anode for lithium ion batteries

Similar to MoO<sub>3</sub>/SWNTs hybrid system, the goal of MoS<sub>2</sub>/C in MoS<sub>2</sub> based anode is to exploit the key features of amorphous carbon in improving the electrical conductivity of electrode and accommodating the volume change of MoS<sub>2</sub> during lithiation/de-lithiation. The production of MoS<sub>2</sub> flakes via LPE and the synthesis of MoS<sub>2</sub>/C hybrid via thermal decomposition of a carbon source (PAA) provide a promising strategy to obtain 2D crystals/carbon hybrid for LIB anode. In this work, the MoS<sub>2</sub> flakes obtained by LPE of bulk MoS<sub>2</sub> having an average lateral size of ~ 90 nm, see Figure 3.12a, which is advantageous for Li<sup>+</sup> diffusion due to the decrease in diffusion length. The AFM analysis, XRD and Raman spectroscopy (Figure 3.12c, d, e and f) demonstrate the reduction in thickness of MoS<sub>2</sub> layers without any change in crystal structure, with respect to its bulk counterpart, whereas the XPS results (Figure 3.12g and h) confirm the stable chemical structure of MoS<sub>2</sub> flakes after the LPE process. These results suggest that the physical and chemical properties of the obtained

MoS<sub>2</sub> flakes are not affected by the LPE process. As reported in section 2.2.2, The MoS<sub>2</sub>/C hybrids obtained by the thermal decomposition of MoS<sub>2</sub>/PAA mixtures are named as MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2, and MoS<sub>2</sub>/C-3, corresponding to the different mixing ratios of MoS<sub>2</sub> and PAA by weight at 1:1, 1:2 and 1:4, respectively. The carbon content in MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2, and MoS<sub>2</sub>/C-3 samples is estimated to be ~ 10.1, 16.1 and 29.9 wt% with respect to the total weights of hybrid samples by TGA results (Figure 3.13a). The HR-TEM images (Figure 3.13d, e and f) demonstrate that the thickness of carbon layer in MoS<sub>2</sub>/C hybrids increase with the increase in carbon content.

The MoS<sub>2</sub> flakes and MoS<sub>2</sub>/C powders are mixed with CB, and a binder (PAA) in IPA, forming the slurry. The electrodes are made by depositing the slurry onto Cu disks, see section 2.2.2. The surface morphology of the electrodes is evaluated by HR-SEM, Figure 5.8. In the case of MoS<sub>2</sub> electrode, the MoS<sub>2</sub> flakes are distributed in random orientations, as indicated by the arrows in Figure 5.8a. This feature is favorable for Li<sup>+</sup> storage due to the increase in active sites at the surface of electrode. [327] The SEM images of MoS<sub>2</sub>/C electrodes show the formation of particles, suggesting the covering of carbon onto the MoS<sub>2</sub> flakes, see Figure 5.8b, c and d.

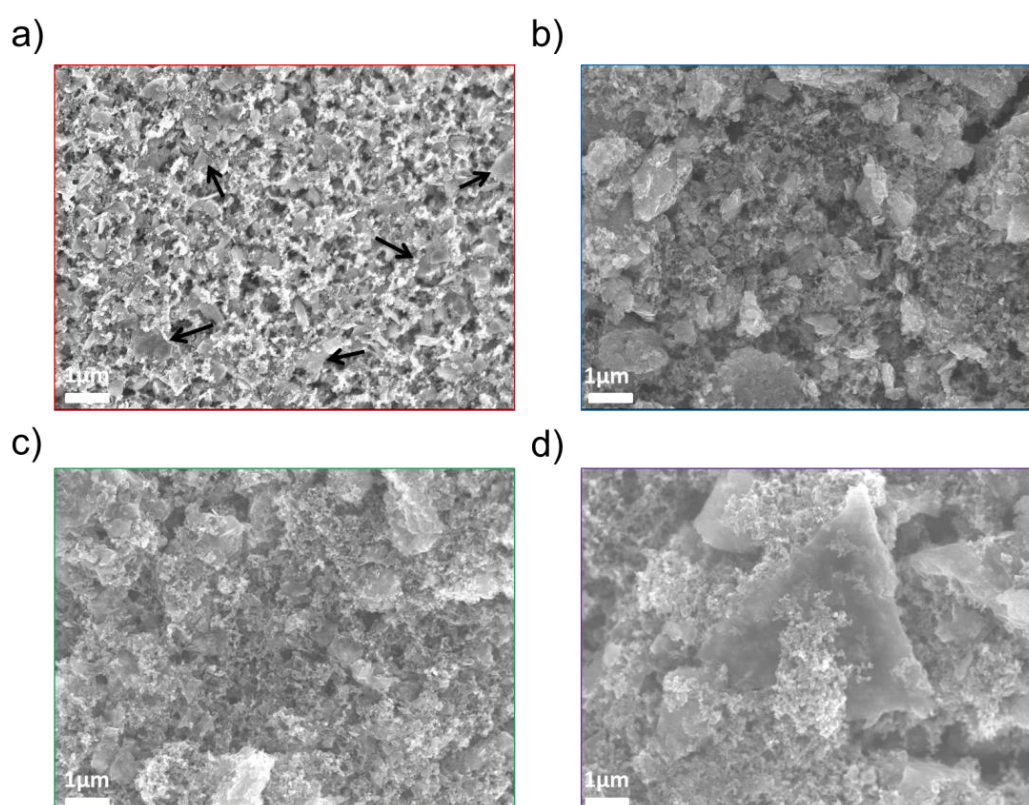
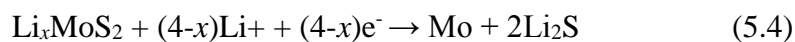
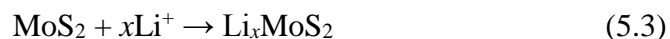


Figure 5.8. High-Resolution-SEM of (a) MoS<sub>2</sub>, (b) MoS<sub>2</sub>/C-1, (c) MoS<sub>2</sub>/C-2 and (d) MoS<sub>2</sub>/C-3 electrodes.

The covering of carbon onto the MoS<sub>2</sub> flakes is expected to form an electrical conductive network, which acting as a buffer prevents the volume change of MoS<sub>2</sub> during lithiation/delithiation. However, a large amount of carbon content also increases the thickness of carbon layer onto the MoS<sub>2</sub> flakes (Figure 5.8d), hindering the diffusion of Li<sup>+</sup> during lithiation/delithiation. [163, 337] Therefore, the appropriate portion of carbon on MoS<sub>2</sub> flakes need to be optimized in order to not only provide an effective conductive network between the MoS<sub>2</sub> flakes, but also allow a facile Li<sup>+</sup> diffusion during cycling process. The electrochemical properties of MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes as anode for LIBs assembled in a half-cell configuration are firstly investigated by means of CV technique. The CV measurement is carried out with the scan rate of 50 μVs<sup>-1</sup> over the potential range from 3.00 to 0.005 V vs Li/Li<sup>+</sup>. Figure 5.9a shows the CV curves of MoS<sub>2</sub> electrode. In the 1<sup>st</sup> cycle, the first reduction peak at ~1.03 V links to the formation of Li<sub>x</sub>MoS<sub>2</sub> by the intercalation of Li<sup>+</sup> into MoS<sub>2</sub> layers. The small reduction peak at ~0.70 V may be caused by the formation of SEI onto the surface of the MoS<sub>2</sub> electrode. [72] The reduction peak at ~ 0.46 V is instead associated to the formation of Li<sub>2</sub>S and metallic Mo nanoparticles via a conversion reaction of Li<sub>x</sub>MoS<sub>2</sub>. [72, 334, 476] The oxidation peak at ~ 2.32 V is attributed to oxidation of Li<sub>2</sub>S into Li<sup>+</sup> and sulphur (S). [72, 334, 476] Meanwhile, the broad and weak peak at ~ 1.63 V indicates the partial oxidation of metallic Mo to form MoS<sub>2</sub>. [214, 327] The CV result of MoS<sub>2</sub> electrode shows a new reduction peak at ~ 1.90 V in the 2<sup>nd</sup> cycle, which corresponds to the reduction of S to form Li<sub>2</sub>S. Besides, the oxidation peak observed at ~ 2.32 V is attributed to oxidation of Li<sub>2</sub>S. The two reduction and oxidation peaks in 2<sup>nd</sup> cycle constitute a reversible redox couple. [72, 334, 476] From the 2<sup>nd</sup> cycle, the electrochemical mechanism of MoS<sub>2</sub> is mainly dominated by the reversible conversion reaction of S to Li<sub>2</sub>S. [477] In general, the redox processes of MoS<sub>2</sub> can be summarized according to the following reactions: [72]



However, the intensities of two reduction peaks (at ~ 1.03 and ~ 0.45 V) drastically decrease in the 2<sup>nd</sup> and 3<sup>rd</sup> cycles because of the consumption of residual MoS<sub>2</sub>, which is not completely reduced during the 1<sup>st</sup> cycle. From 3<sup>rd</sup> cycle, the intensity of reduction peak at ~ 1.90 V is slightly increased (24.9 mA g<sup>-1</sup>) with respect to the 2<sup>nd</sup> cycle, which is attributed to an activation process of the electrode materials. [478] Importantly, in the case of MoS<sub>2</sub> and

MoS<sub>2</sub>/C-1 electrodes, it is observed that the intensities of oxidation peaks at ~ 2.32 V significantly decrease with the increasing of cycle number. In specific, the intensity differences of these peaks between 1<sup>st</sup> and 2<sup>nd</sup> cycles are 45 mA g<sup>-1</sup> and 18 mA g<sup>-1</sup> for MoS<sub>2</sub> and MoS<sub>2</sub>/C-1 electrodes, respectively. These CV behaviors suggest that in the case of MoS<sub>2</sub> electrode, irreversible electrochemical processes take place due to irreversible redox reactions during lithiation/de-lithiation, see equations 5.3 and 5.4. [327] These irreversible redox reactions progressively produce insulated S, see equation 5.5 and 5.6, which can hinder the electron transport of MoS<sub>2</sub> electrode during cycling, resulting in its irreversible electrochemical processes. [479] The irreversible electrochemical processes are alleviated in the case of MoS<sub>2</sub>/C-1 electrode due to the support of carbon network. However, these processes are still observed because the insufficient carbon content cannot completely cover all the MoS<sub>2</sub> flakes in the case of MoS<sub>2</sub>/C-1 electrode (see HR-TEM image in Figure 3.13d), which still cannot completely improve the electron transport within the electrode.

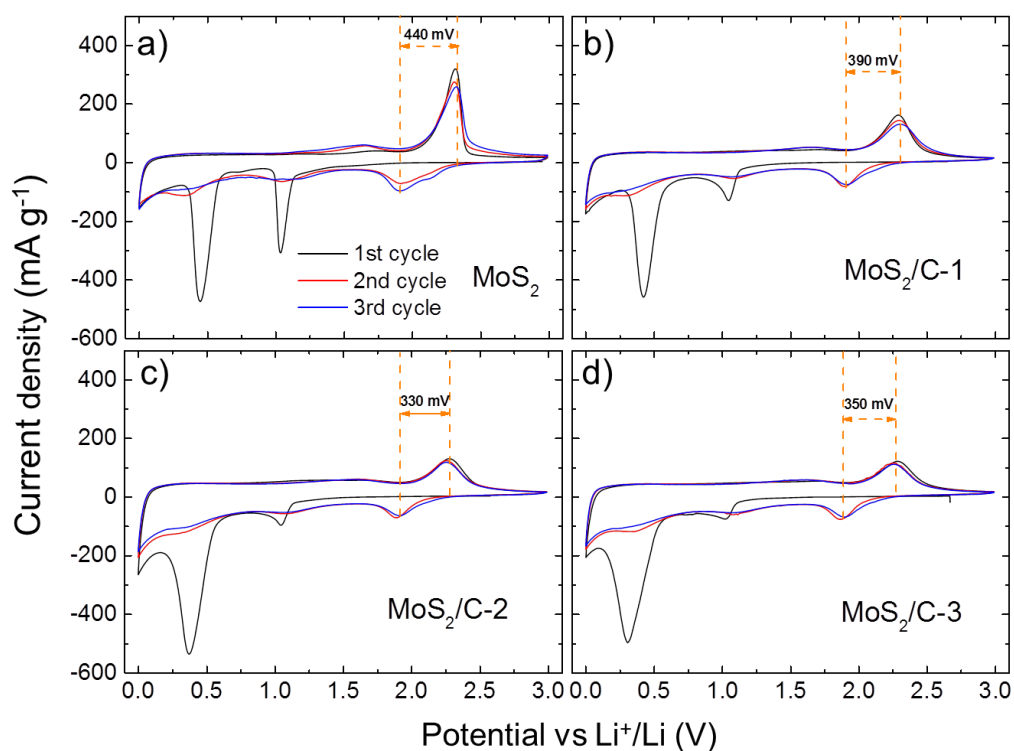


Figure 5.9. Cyclic voltammograms of (a) MoS<sub>2</sub>, (b) MoS<sub>2</sub>/C-1, (c) MoS<sub>2</sub>/C-2 and (d) MoS<sub>2</sub>/C-3 electrodes at a scan rate of 50  $\mu\text{V s}^{-1}$ .

For MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrodes (Figure 5.9c and d), the intensities of oxidation peaks at ~ 2.32 V in the initial three cycles are overlapped. The MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrodes exhibit a reversible electrochemical process, in contrast to MoS<sub>2</sub> and MoS<sub>2</sub>/C-1 electrodes which do not present this process, indicating that the sufficient carbon content improves the electrical conductivity of MoS<sub>2</sub>. It is noteworthy to mention that the potential differences

between redox peaks at  $\sim 1.92$  and  $2.32$  V, after 3 cycles, is 440, 390, 330 and 350 mV, for MoS<sub>2</sub>, MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrodes, respectively. This fact confirms that MoS<sub>2</sub>/C electrodes have lower overall resistance and better electrochemical reversibility than in the MoS<sub>2</sub> electrode. [215, 480] As the carbon content increase, a broadening of the reduction peak set at  $\sim 0.46$  V Li/Li<sup>+</sup>, together with a slight decrease in the peak current, is observed. This modification finds its explanation in kinetics limitation, *e.g.*, Li<sup>+</sup> diffusion through carbon thickness, of Li<sub>x</sub>MoS<sub>2</sub> – Li<sub>2</sub>S conversion buffered by carbon matrix. [481]

Galvanostatic charge/discharge cycling measurements are carried out at a current density of 100 mA g<sup>-1</sup> over the potential range from 3.00 to 0.005 V vs Li/Li<sup>+</sup> in order to fully investigate the electrochemical response for the Li<sup>+</sup> storage of the MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes. In Figure 5.10, the charge/discharge voltage profiles of MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes show similar electrochemical behaviours. They clearly indicate two distinct voltage plateaus at  $\sim 1.05$  and  $0.54$  V in the 1<sup>st</sup> charge process (lithiation), which correspond to the Li<sup>+</sup> intercalation and conversion reaction of Li<sub>x</sub>MoS<sub>2</sub> to metallic Mo and Li<sub>2</sub>S, respectively, see equations 5.3 and 5.4. [336, 482, 483] Simultaneously, a severe reduction in the 1.05 V plateau length happens. This is because the Li<sup>+</sup> intercalation reaction (equation 1), corresponding to 1.05V plateau, is progressively limited as the thickness of carbon layers increase ( $\sim 0.8$ ,  $2.4$  and  $13.8$  nm for MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3, respectively), see Figure 3.13c, d and f. Carbon matrix tortuosity and thickness might be responsible for the limited lithium diffusion and the direct switch to a conversion mechanism yielding metallic Mo and Li<sub>2</sub>S. Thus, the increase in thickness of carbon layer can be considered as a drawback for the intercalation of Li<sup>+</sup> into MoS<sub>2</sub> layers.

A voltage plateaus at  $\sim 2.25$  V is observed in the 1<sup>st</sup> discharge process (de-lithiation), the voltage plateaus at  $\sim 1.92$  V in the 2<sup>nd</sup> charge process, associated with the reversible redox reaction of Li<sub>2</sub>S/S couple, which always appears in the subsequent cycles. [218, 336, 482, 483] The voltage plateaus in the charge/discharge voltage profiles are consistent with the reduction and oxidation peaks in the CV results of the MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes (Figure 5.9). Nevertheless, the MoS<sub>2</sub>/C electrodes exhibit a good overlapped charge and discharge potential curves, upon 100 cycles with respect to MoS<sub>2</sub> electrode, a sign of a good reversible reaction during lithiation/de-lithiation. The initial irreversible capacities (the capacity difference between 1<sup>st</sup> charge and discharge) of the MoS<sub>2</sub>, MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrodes are 295, 338, 416 and 444 mAh g<sup>-1</sup>, respectively. The rise of the initial irreversible capacities with the increasing of carbon content could be due to the fact that the amount of amorphous carbon offers more active sites, *e.g.*, defects, for irreversible Li<sup>+</sup> storage in the 1<sup>st</sup> lithiation. [162, 168, 169, 484]

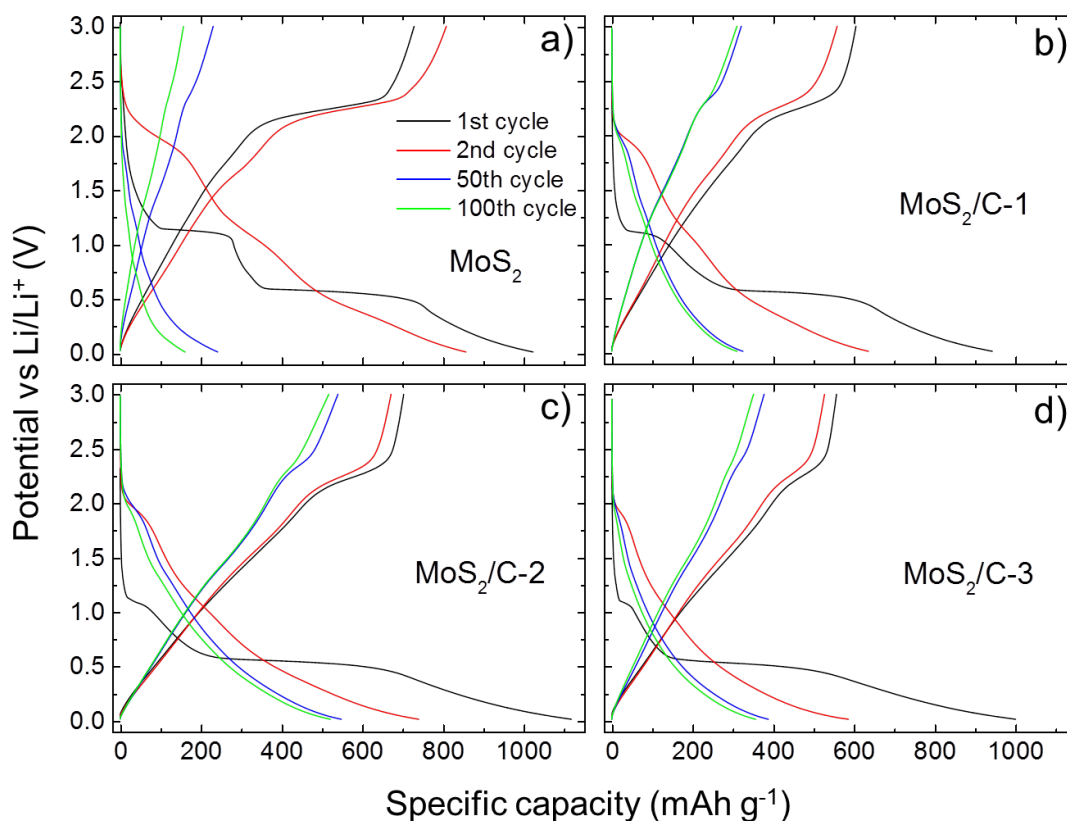


Figure 5.10. Voltage profiles upon galvanostatic charge/discharge of (a)  $\text{MoS}_2$ , (b)  $\text{MoS}_2/\text{C-1}$ , (c)  $\text{MoS}_2/\text{C-2}$  and (d)  $\text{MoS}_2/\text{C-3}$  electrodes at  $0.1 \text{ A g}^{-1}$  between 3.00 to 0.005 V vs  $\text{Li/Li}^+$ .

In order to clarify the  $\text{Li}^+$  storage capability of carbon network which may contribute to the irreversible specific capacity of  $\text{MoS}_2/\text{C}$  electrodes, the galvanostatic charge/discharge measurement of amorphous carbon electrode is carried out at a current density of  $0.1 \text{ A g}^{-1}$  over the potential range from 3.00 to 0.005 V vs  $\text{Li/Li}^+$ . The amorphous carbon is obtained by the thermal decomposition of PAA, and the preparation of amorphous carbon electrode is following the preparation steps of  $\text{MoS}_2$  and  $\text{MoS}_2/\text{C}$  electrodes reported in section 2.4.1.3. As shown in Figure 5.11a, the charge/discharge voltage profile of amorphous carbon electrode shows the specific capacity of  $\sim 285 \text{ mAh g}^{-1}$  in the initial charge process. From subsequent charge processes, the electrode exhibits the continuously capacity fading of  $\sim 145$ , 117 and 94  $\text{mAh g}^{-1}$  corresponding to the 2<sup>nd</sup>, 5<sup>th</sup> and 20<sup>th</sup> cycles, respectively. The capacity fading during cycling suggests the irreversible  $\text{Li}^+$  storage process of amorphous carbon electrode, associated to the presence of active sites, *e.g.*, defects, in amorphous carbon. [162, 168, 169, 484] The irreversible  $\text{Li}^+$  storage in amorphous carbon contributes to the increase in irreversible capacities of  $\text{MoS}_2/\text{C}$  electrodes, as shown in Figure 5.10.

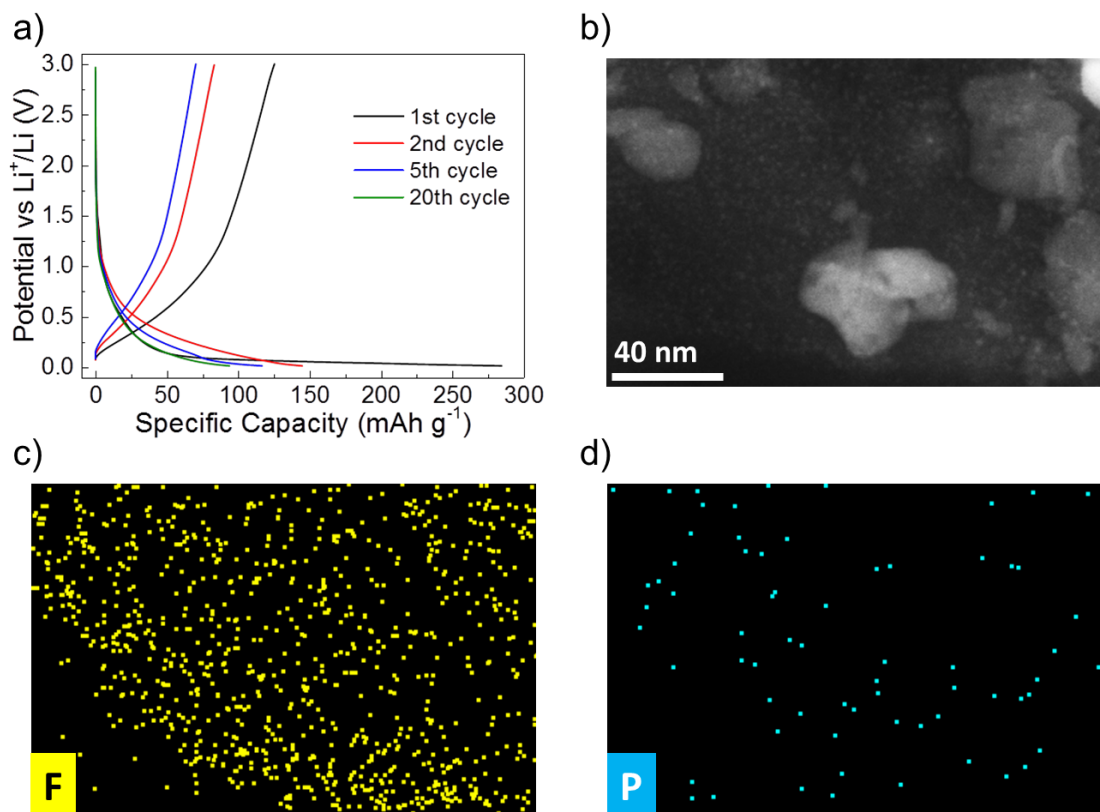
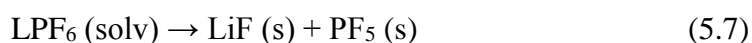


Figure 5.11. (a) Voltage profiles upon galvanostatic charge/discharge of amorphous carbon electrode at  $0.1 \text{ A g}^{-1}$  between  $5 \text{ mV}$  and  $3 \text{ V}$ ; (b) HAADF-STEM image of  $\text{MoS}_2$  electrode after 100 charge/discharge galvanostatic cycles and elemental maps of (c) F and (d) P acquired by STEM-EDS.

A further contribution to the initial irreversible capacity can be attributed to the formation of SEI on the surface of the electrodes. To confirm the formation of SEI, the elemental mapping of  $\text{MoS}_2$  electrode after 100 charge/discharge cycles is carried out by STEM-EDS measurements. Figure 5.11b shows a high angular annular dark field - scanning TEM (HAADF)-STEM image of  $\text{MoS}_2$  electrode materials, for which the corresponding elemental maps are demonstrated in Figure 5.11c and d. The distribution of fluorine (F) and phosphorus (P) on the electrode can be used to identify the formation of SEI. The components of SEI are always contributed from the reduction and decomposition of the electrolyte. In this work, the  $\text{LiPF}_6$  is used as the lithium salt (see section 2.4.2), which decomposes into  $\text{LiF}$  and a small portion of  $\text{PF}_5$  through the reactions 5.7 and 5.8, see the equation 5.7. [485, 486] The presence of F confirms the formation of  $\text{LiF}$ , while P is barely visible probably due to small amount of  $\text{PF}_5$  in the observed area.



The formation of SEI in MoS<sub>2</sub> electrode is in agreement with the small broad peak at ~ 0.7 V in the first cycle of its CV curve (see Figure 5.9a). In the cases of MoS<sub>2</sub>/C electrodes, the increase in irreversible capacity with higher content of carbon can be attributed to the excessive interphase between MoS<sub>2</sub>/amorphous carbon and electrolyte, leading to considerable side reactions of SEI formation on MoS<sub>2</sub>/amorphous carbon. [330, 483, 487]

To further understand the mechanism for the effect of carbon content on the electrochemical performance of the MoS<sub>2</sub>/C electrode, the EIS of MoS<sub>2</sub>, MoS<sub>2</sub>/C electrodes are acquired from a frequency of 10 kHz to 10 mHz. The Nyquist plots of all electrodes, Figure 5.12, consist of a depressed semi-circle in the high frequency region and a sloping straight line in the low-frequency region. The semi-circles are described by means of a generalized RC-circuit (the inset in Figure 5.12a) with electrolyte resistance R<sub>E</sub> (resistance caused by the mass transport of Li<sup>+</sup> through electrolyte), R<sub>CT</sub> (including the electron transfer to the reactive center MoS<sub>2</sub>), and a constant phase element (CPE) for the electrode/electrolyte interface. [162, 488] The high frequency region is associated with the R<sub>CT</sub>, whereas the low-frequency line is descriptive of the Li<sup>+</sup> diffusion impedance within the electrode which is described by the Warburg circuit element (Z<sub>W</sub>) in RC-circuit. [337, 488-490] Figure 5.12a shows the Nyquist plots of MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes after the 1<sup>st</sup> lithiation/de-lithiation, at charged state. The R<sub>CT</sub> values are ~ 85, 37, 29 and 70 Ω for MoS<sub>2</sub>, MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrodes, respectively. The R<sub>CT</sub> of the MoS<sub>2</sub>/C electrodes are thus lower than that of the MoS<sub>2</sub> electrode. This clearly indicates that the electrical conductivity of the MoS<sub>2</sub>/C electrodes is higher than that of MoS<sub>2</sub> electrodes. This fact confirms that the incorporation of carbon improves the electrical conductivity of the MoS<sub>2</sub>/C electrodes by constructing a conductive network between MoS<sub>2</sub> flakes, and thus greatly enhance electron transport within electrode during the lithiation/de-lithiation process. [306, 327] The MoS<sub>2</sub>/C-2 electrode shows the lowest value of R<sub>CT</sub> with respect to MoS<sub>2</sub>/C-1 and MoS<sub>2</sub>/C-3 electrodes, suggesting that MoS<sub>2</sub>/C-2 is endowed with the proper amount of carbon content so that a reasonable compromise between improved electrical conductivity of the electrode and the limited Li<sup>+</sup> diffusion through the carbon is obtained. [327, 491] Besides, among the three MoS<sub>2</sub>/C electrodes, the MoS<sub>2</sub>/C-3 electrode exhibits the highest R<sub>CT</sub> value. The increase in carbon content results in the increase in the thickness of carbon layer covering the flakes (Figure 3.13d, e and f). This feature prolongs the pathway for electron transfer across the MoS<sub>2</sub>/C in the MoS<sub>2</sub>/C electrode with respect to that of MoS<sub>2</sub>/C-1 and MoS<sub>2</sub>/C-2 electrodes, leading to the increase of the R<sub>CT</sub>. The Nyquist plots of MoS<sub>2</sub> and MoS<sub>2</sub>/C electrodes after the 100 cycles, at charged state in Figure 5.12b shows the same trend as the plots in Figure 5.12a. The R<sub>CT</sub> value of MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrodes exhibit the values of ~ 26, 21,



and 58  $\Omega$ . The decrease in the  $R_{CT}$  values of  $\text{MoS}_2/\text{C}$  electrodes after 100 cycles with respect to the 1<sup>st</sup> cycle can be explained based on the CV data and voltage profiles, as shown in Figure 5.9 and 5.10. According to the voltage profiles of  $\text{MoS}_2/\text{C}$  electrodes, the voltage plateaus at  $\sim 1.05$  and 0.54 V related to the intercalation and conversion reactions (equation 5.3 and 5.4), are observed at the 1<sup>st</sup> charge process, see Figure 5.10b, c and d. From the 2<sup>nd</sup> charge, these voltage plateaus are still observed as the sloping curves. This is because the  $\text{MoS}_2$  has not been completely consumed after the 1<sup>st</sup> charge process, therefore, the residual  $\text{MoS}_2$  continuously contribute to the intercalation and conversion reactions at the 2<sup>nd</sup> charge process. These features can also be observed by the broadened shape of reduction peaks at  $\sim 1.03$  and 0.45 V in the 2<sup>nd</sup> cycle of CV data with respect to that of 1<sup>st</sup> cycle (Figure 5.9b, c and d). Compare to the 1<sup>st</sup> charge process, the diminished voltage plateau at  $\sim 1.05$  and 0.54 V are diminished at the 100<sup>th</sup> charge process, (Figure 5.10b, c and d) suggesting the complete consumption of residual  $\text{MoS}_2$  via the intercalation and conversion reactions. [492-494] Thus, the high  $R_{CT}$  values after the 1<sup>st</sup> cycle compared to that of the 100<sup>th</sup> cycle in  $\text{MoS}_2/\text{C}$  electrodes are attributed to the formation of residual  $\text{MoS}_2$  which can limit the electron transfer across  $\text{MoS}_2/\text{C}$ . However, the  $R_{CT}$  value of the  $\text{MoS}_2$  electrode increases strictly after 100 cycles ( $\sim 174 \Omega$ ) because of structural destruction of the active material upon cycling. The EIS results confirm the effects of carbon on the electrochemical performances of the  $\text{MoS}_2/\text{C}$  electrodes after cycling.

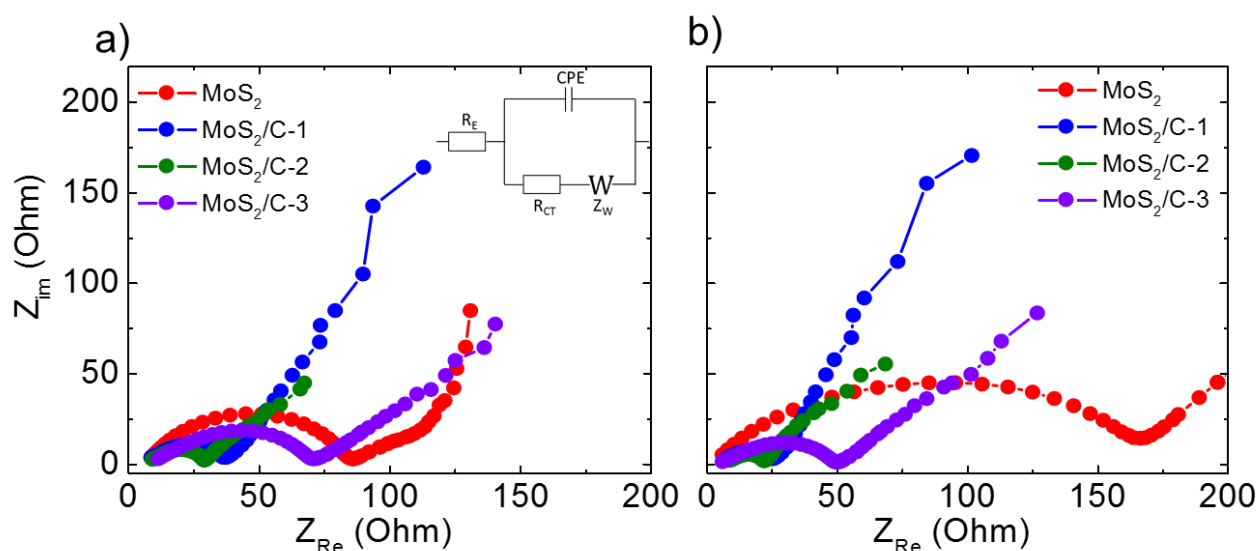


Figure 5.12. *Electrochemical impedance spectroscopy of  $\text{MoS}_2$ ,  $\text{MoS}_2/\text{C}-1$ ,  $\text{MoS}_2/\text{C}-2$  and  $\text{MoS}_2/\text{C}-3$  electrodes at charge state (a) after the 1<sup>st</sup> cycle and (b) after the 100<sup>th</sup> cycles.*

The specific capacity and coulombic efficiency over charge/discharge galvanostatic cycles at 100 mA  $\text{g}^{-1}$  of  $\text{MoS}_2$ ,  $\text{MoS}_2/\text{C}$  electrodes are shown in Figure 5.13a. Remarkably, the specific capacity of the  $\text{MoS}_2$  electrode increases from 859 to 939 mAh  $\text{g}^{-1}$  from 2<sup>nd</sup> to 9<sup>th</sup> cycle, but

rapidly decrease to  $161 \text{ mAh g}^{-1}$  after 100 cycles. The increase in specific capacity of  $\text{MoS}_2$  electrode in the few initial cycles is due to the continuous conversion reactions of  $\text{Li}_x\text{MoS}_2$ , recognized also in the reduction peaks at  $\sim 1.03$  and  $0.45 \text{ V}$  in CV data (Figure 5.9a). These reactions trigger the volume change of  $\text{MoS}_2$ , leading to the electrode pulverization, resulting in the introduction of defect sites. These sites may serve to trap more  $\text{Li}^+$  during subsequent lithiation processes, and could explain the gradual increase in specific capacity. [163, 168, 174, 495] However, this phenomenon takes place in the initial cycles because the electrode pulverises rapidly, resulting in an electrical contact loss between  $\text{MoS}_2$  and current collector, leading to a significant capacity fading in the following cycles. [72, 489] It is notable that the cyclability and specific capacities of the  $\text{MoS}_2/\text{C}$  electrodes is superior to that of the  $\text{MoS}_2$  electrode. This demonstrates that carbon network not only hinders the capacity fading of  $\text{MoS}_2$  flakes by buffering the volume change, but also enhances the electrical conductivity of electrode, by forming the carbon matrix as a conductive network. [334, 478, 491] The  $\text{MoS}_2/\text{C-1}$ ,  $\text{MoS}_2/\text{C-2}$  and  $\text{MoS}_2/\text{C-3}$  electrodes retain stable specific capacities of 310, 521,  $356 \text{ mAh g}^{-1}$ , with a coulombic efficiency of  $\sim 99.6$ ,  $99.7$  and  $98.2 \%$ , respectively, after 100 cycles. It is notable that the  $\text{MoS}_2/\text{C-1}$  electrode exhibits a low specific capacity with respect to that of  $\text{MoS}_2/\text{C-2}$  and  $\text{MoS}_2/\text{C-3}$  electrodes. This result is attributed to the partial carbon covering on  $\text{MoS}_2$  flakes, due to the insufficient carbon content, which is confirmed by HR-TEM image (Figure 3.13d). The incomplete embedding of  $\text{MoS}_2$  flakes into carbon network is associated to capacity loss of  $\sim 698 \text{ mAh g}^{-1}$  ( $\sim 80\%$  of initial capacity) after 100 cycles, due to the structural failure by pulverization. However, the  $\text{MoS}_2/\text{C-1}$  electrode is still able to preserve the reversible capacity ( $\sim 310 \text{ mAh g}^{-1}$ ), as shown in Figure 5.13a. [336, 483] In contrast, the  $\text{MoS}_2/\text{C-2}$  electrodes exhibits a significant higher specific capacities ( $521 \text{ mAh g}^{-1}$ ) with respect to  $\text{MoS}_2/\text{C-1}$  and  $\text{MoS}_2/\text{C-3}$  electrodes, demonstrating the high reversible  $\text{Li}^+$  storage ability and good structural stability of  $\text{MoS}_2/\text{C-2}$ , due to the sufficient carbon content providing the complete conductive carbon network which can effectively accommodate the volume change as a buffered layer, and also improve the electrical conductivity of the electrode. However, although the  $\text{MoS}_2/\text{C-3}$  electrode shows a stable cycling performance, its specific capacity ( $356 \text{ mAh g}^{-1}$ ) is drastically lower than that of  $\text{MoS}_2/\text{C-2}$  electrode ( $521 \text{ mAh g}^{-1}$ ). The thickness of carbon layer induces an elongated diffusion pathway of  $\text{Li}^+$ , leading to low specific capacity. [166, 337]

The electrochemical characterization at varying current densities are performed (Figure 5.13b) to investigate the rate capabilities of the  $\text{MoS}_2/\text{C}$  electrodes. The  $\text{MoS}_2/\text{C-2}$  achieves the best rate capability among the three  $\text{MoS}_2/\text{C}$  electrodes, with  $\sim 546 \text{ mAh g}^{-1}$  at  $100 \text{ mA g}^{-1}$  and  $\sim 272 \text{ mAh g}^{-1}$  at  $2000 \text{ mA g}^{-1}$ . The specific capacity restores to  $\sim 500 \text{ mAh g}^{-1}$  when the

current rate is changed back to  $100 \text{ mA g}^{-1}$ , featuring capacity retention of  $\sim 91.6 \%$ . The  $\text{MoS}_2/\text{C-3}$  electrode exhibits a specific capacity of  $\sim 402 \text{ mAh g}^{-1}$  at  $100 \text{ mA g}^{-1}$  and  $\sim 156 \text{ mAh g}^{-1}$  at  $2000 \text{ mA g}^{-1}$ . The specific capacity restores to  $\sim 371 \text{ mAh g}^{-1}$  when the current rate is changed back to  $100 \text{ mA g}^{-1}$ , displaying capacity retention of  $\sim 92.3 \%$ . The high values of capacity retention of  $\text{MoS}_2/\text{C-2}$  and  $\text{MoS}_2/\text{C-3}$  electrodes confirm the role of carbon in structural preservation of  $\text{MoS}_2$  flakes, protecting the electrode from pulverization during lithiation/de-lithiation. [337] On the contrary,  $\text{MoS}_2/\text{C-1}$  electrode shows rapid capacity decay as the current density increases, indicating a capacity retention of  $32.6 \%$  when the current rate is reset from  $2000 \text{ mA g}^{-1}$  to  $100 \text{ mA g}^{-1}$ . This is attributed to the insufficient carbon content, which is in agreement with the galvanostatic charge/discharge cycling test (Figure 5.13a).

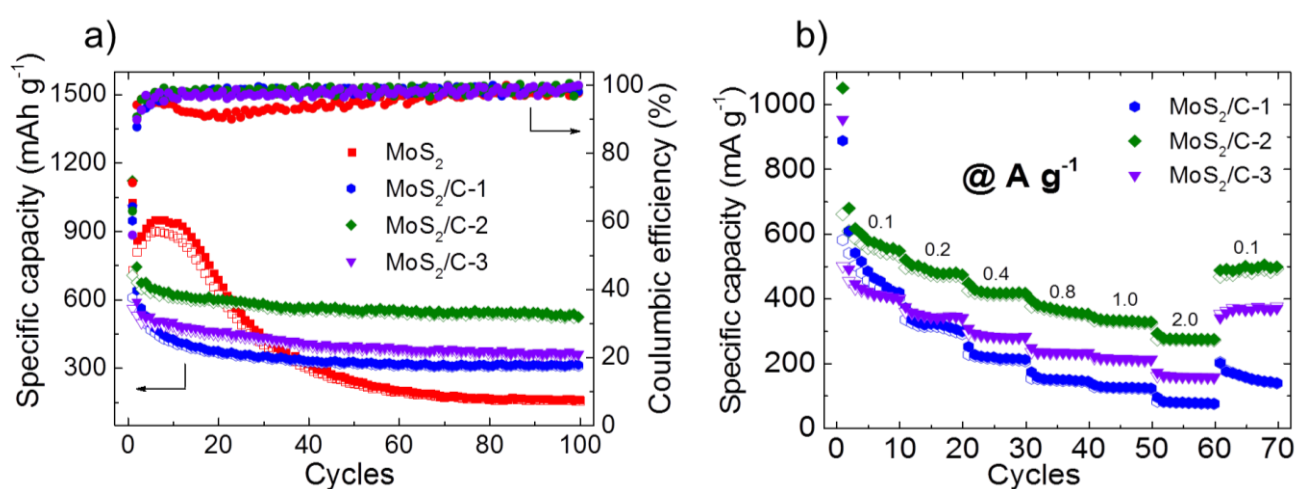


Figure 5.13. (a) Specific capacity and Coulombic efficiency over charge/discharge galvanostatic cycles at  $100 \text{ mA g}^{-1}$  and (b) rate performance at different current densities from  $0.1$  to  $2.0 \text{ A g}^{-1}$  of  $\text{MoS}_2$ ,  $\text{MoS}_2/\text{C-1}$ ,  $\text{MoS}_2/\text{C-2}$  and  $\text{MoS}_2/\text{C-3}$  electrodes. The specific capacity capacities are normalized by the mass of  $\text{MoS}_2/\text{C}$  hybrids.

To further study the effect of carbon content on the electrochemical behaviors of the electrodes, the morphologies of  $\text{MoS}_2$ ,  $\text{MoS}_2/\text{C-1}$ ,  $\text{MoS}_2/\text{C-2}$  and  $\text{MoS}_2/\text{C-3}$  electrodes after 100 charge/discharge cycles are examined by post-mortem SEM. As shown in Figure 5.14a, the  $\text{MoS}_2$  electrode clearly exhibits fractures with width of  $\sim 3 \mu\text{m}$  (indicated by arrows), likely caused by the volume change during the charge/discharge cycles. These fractures contribute to the decrease in electrical conductivity (Figure 5.12b), and the significant capacity fading of the electrode (Figure 13a) [468, 496, 497]. On the surface of  $\text{MoS}_2/\text{C-1}$  electrode the small fractures with the width of  $\sim 800 \text{ nm}$  are observed as shown in Figure 5.14b. This apparently shows that the pulverization of  $\text{MoS}_2/\text{C-1}$  electrode is less severe than that of the  $\text{MoS}_2$  electrode. These small fractures in  $\text{MoS}_2/\text{C-1}$  electrode are caused by partial

pulverization during cycling due to lacking of carbon covered on flakes which is confirmed by HR-TEM images (Figure 3.13d) and galvanostatic charge/discharge cycling test (Figure 5.13a). By contrast, the surface of MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3 electrode show a homogenous morphology and the presence of fractures mostly cannot be observed, demonstrating that the pulverization is hindered by carbon network. Thanks to the structure stability, both electrical conductivity and reversible specific capacity of MoS<sub>2</sub>/C electrodes are improved if compared with the MoS<sub>2</sub> electrode, as clearly shown in Figure 5.12 and 5.13a, respectively.

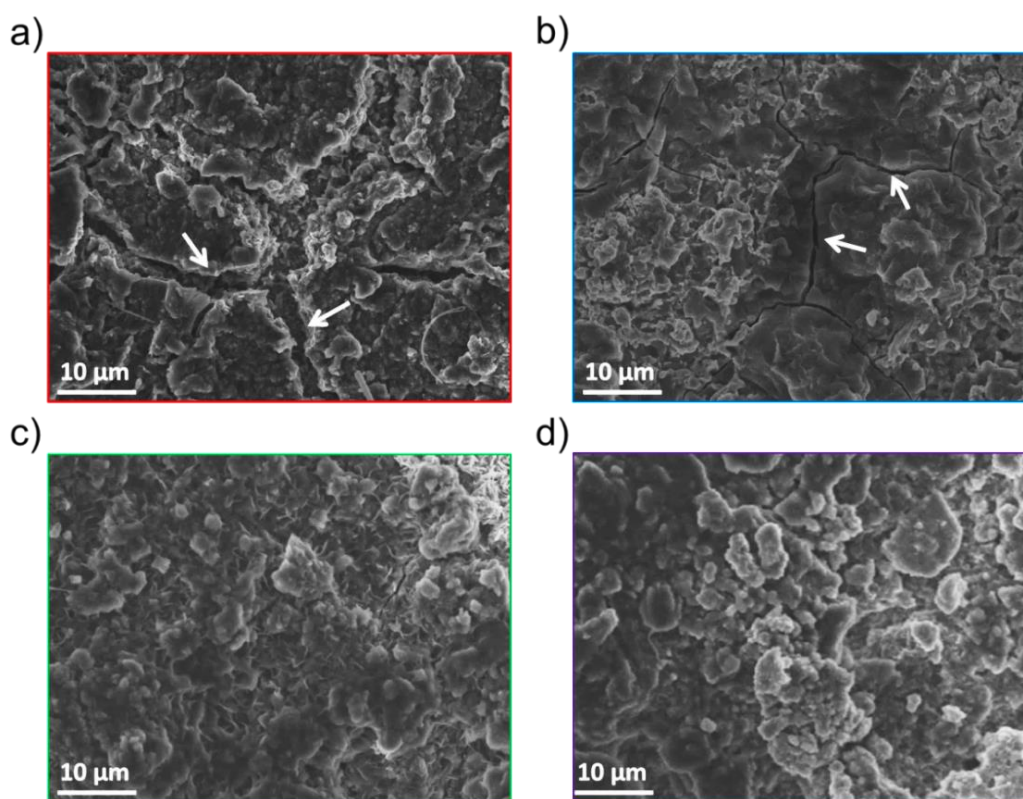


Figure 5.14. High resolution SEM images of (a) MoS<sub>2</sub>, (b) MoS<sub>2</sub>/C-1, (c) MoS<sub>2</sub>/C-2 and (d) MoS<sub>2</sub>/C-3 electrodes after 100 charge/discharge galvanostatic cycles.

#### 5.4. Conclusion

In this chapter, I described the experimental procedure for the realization of a high performance binder-free MoO<sub>3</sub>/SWNTs hybrid anode for LIBs, based on MoO<sub>3</sub> flakes obtained via LPE method, combined with solution processed SWNTs. Contrary to CB nanoparticles, the SWNTs addition determines a network structure with the MoO<sub>3</sub>, which is beneficial for the mechanical and electrochemical performances of the as-produced anode by providing (i) long channels for electronic charge transport; (ii) an active anode material, instead of polymeric binder, offering extra capacity for Li ions storage; (iii) a buffer frame in the electrode, which reduce the capacity fading caused by the volume expansion of MoO<sub>3</sub> flakes during the lithiation process. The designed binder-free solution processed hybrid

MoO<sub>3</sub>/SWNTs (90:10) anode has demonstrated a specific capacity of 865 mAhg<sup>-1</sup> at 100 mA g<sup>-1</sup> after 100 cycles, with a coulombic efficiency of 99.7% and a capacity fading of 0.02% per cycle. This work exhibits that the low-cost, non-toxic, binder-free hybrid MoO<sub>3</sub>/SWNTs can boost the development of high-performance anodes for LIBs.

The LPE process of bulk MoS<sub>2</sub> in IPA is also used to produce MoS<sub>2</sub> flakes with lateral size of ~ 90 nm. A subsequent thermal composition of PAA in the mixture with MoS<sub>2</sub> flakes successfully created the MoS<sub>2</sub>/C hybrids for LIB anodes. The MoS<sub>2</sub>/C electrodes exhibited high capacity, an improved cyclability, and high rate cycling compared with MoS<sub>2</sub> electrode. In particular, MoS<sub>2</sub>/C-2 electrode, with a ~16.11% wt of carbon content delivers a reversible specific capacity of 521 mAh g<sup>-1</sup> at 100 mA g<sup>-1</sup> after 100 charge/discharge cycles. These aspects unveiled an optimum value of carbon content in effectively embedding MoS<sub>2</sub> flakes. With respect to that of MoS<sub>2</sub> electrode (~ 174 Ω) after 100 cycles, the low R<sub>CT</sub> value of MoS<sub>2</sub>/C-2 electrode (~ 26 Ω), confirms that the proper carbon portion provides an effective conductive network. These results are ascribed to (i) a conductive network of carbon connecting the MoS<sub>2</sub> flakes, and facilitating the Li<sup>+</sup> diffusion and the electron transport; (ii) the carbon network acts as a buffer layer, easing the volume change of MoS<sub>2</sub> flakes during the lithiation/de-lithiation process. Therefore, the MoS<sub>2</sub>/C hybrid fabrication protocol is a promising tool for the production of MoS<sub>2</sub>/carbon hybrids and also can be easily extended to the construction of other 2D nano-crystals dispersed in amorphous carbon networks for LIB application.

## Chapter 6:

# Application of black phosphorous for lithium ion batteries

### 6.1. Introduction

Black phosphorous (BP) has recently attracted a great deal of interest because of its extremely high theoretical specific capacity of  $2596 \text{ mA h g}^{-1}$ . [147-149] This high theoretical specific capacity can be achieved thanks to the puckered structure of BP which allows uptaking three  $\text{Li}^+$  to form  $\text{Li}_3\text{P}$  compounds. [186] Additionally, the BP can exhibit outstanding charge/discharge rate because the puckered structure allows the fast  $\text{Li}^+$  diffusion is  $10^4$  times faster than it is in graphene [226], *e.g.*, the diffusion energy barrier in BP is  $0.09\text{eV}$  [498] and in graphene is  $0.327\text{eV}$  [198]. Moreover, when exfoliated into single layer (phosphorene) or into FL-BP flakes, the increased available surface area can further enhance the electrochemical activity, which is beneficial for energy storage applications. [186]

The exfoliation of bulk BP into single- or few-layer flakes can be achieved by several strategies, such as MC, BM and LPE [183, 184] methods. The MC method exfoliate BP based on consecutively peeling off crystal layers by using adhesive tape, [142] but it is only suitable for research activities due to both the limited scalability and morphological heterogeneity of the exfoliated flakes. [142] The other exfoliation technique, *e.g.*, BM [185, 186] can meet the requirement of scalable production, but usually introduces impurities in the obtained products. [145, 187] In contrast, LPE [150, 241, 499] is an affordable and scalable alternative to MC. [183, 184] The LPE of BP in both aqueous [500] and organic solvents [235, 360, 369] has been recently demonstrated which opened up possibilities to use the exfoliated BP in applications as light absorbers, [501, 502] and energy storage devices. [500, 503] However, current approaches for the LPE of BP present several issues especially in aqueous environment, where the chemical integrity of the exfoliated flakes is compromised due to the oxidation promoted by the presence of  $\text{O}_2/\text{H}_2\text{O}$ . [227-229] The formation of phosphorus-oxide species, *i.e.*  $\text{P}_2\text{O}_5$  and  $\text{P}_2\text{O}_4$ , [230] has been reported when the BP is exposed to air. These processes increase the roughness of the flakes and accelerate their degradation. [231] Performing the LPE in pure organic solvents solves this issue, since the presence of water and  $\text{O}_2$  is avoided. The organic solvents that commonly used to exfoliate BP are generally toxic (Health code  $\geq 2$  NFPA704), [232] and have a b.p. usually above  $100^\circ\text{C}$ , *e.g.* NMP, b.p. =  $202^\circ\text{C}$ , [233] DMF, b.p. =  $153^\circ\text{C}$  [234] CHP, b.p. =  $284^\circ\text{C}$  [235] or formamide (b.p. =

210 °C). [236] The solvent b.p. is critical for several applications because the solvent removal is of paramount importance for the realization of high performance anodes of batteries, [3, 504] and it is also relevant for the development of electronic, [249, 505] and optoelectronic devices. [161, 502] In general, the solvent removal is performed by heating the deposited sample or device above the solvent b.p. However, annealing procedures always run the risk of either degrading the material or damaging the device. Furthermore, in some cases the solvent degrades when heated, i.e. NMP, [506] thus it leaves contaminants or impurities on the as-prepared devices, [507] which are detrimental to their performance. [508] A possible solution for these problems is to use an easy-to-remove solvent, preferably one that is not toxic, not degrading with the annealing temperature. To date, however, a clear solution to overcome such an issue has not been found.

As discussed in section 3.5, the importance of the solvent selection, which is of paramount importance for the ink storage, treatment, deposition and drying, crucial for the application as anodes for LIBs. In specific, the selected solvent should be able to: (i) exfoliate BP; (ii) keep a stable dispersion of the exfoliated flakes, i.e. the exfoliated flakes should not flocculate or precipitate; (iii) prevent the degradation of the exfoliated flakes by oxidation; (iv) be easily removed without leaving impurities. Interestingly, the exfoliation is also possible in acetone (see section 3.5.1), a well-known non-toxic solvent with a low-b.p. [231] The exfoliation in acetone is attractive for real applications, e.g. polymer composites and functional inks, for both of which the drying time and toxicity are key factors to be considered. The exfoliation of BP in acetone is a feasible and up-scalable approach which allows fast deposition of homogeneous films of FL-BP flakes onto Cu substrate as anodes for LIBs. The study on electrochemical properties of FL-BP exfoliated in acetone indicates that it is promising with regards to the fast charge/discharge LIBs. Overall, the presented process is a step forward towards the fabrication of phosphorene-based devices.

## 6.2. Few-layer black phosphorous as anode for lithium ion batteries

The successful exfoliation of BP in acetone exploiting a low-b.p. solvent, not toxic, not degrading with the annealing temperature, offers the possibility to scale-up the production, [150, 241] for applications in the energy storage sector. To further highlight this point, this section will analyse the electrochemical properties of FL-BP<sub>acetone</sub>-based anode, comparing to the one based on FL-BP<sub>CHP</sub>. To this end, both dispersions are mixed with a conductive agent and a binding material, i.e. CB and PVdF, respectively, then deposited onto Cu substrates (see section 2.4.1.4). The SEM images of the samples show the mixture of the FL-BP, PVdF and CB, covering the copper substrates (see Figure 6.1a and b, obtained from acetone and CHP

dispersions, respectively). The optical pictures, reported as insets in Figure 6.1a and b, show the copper substrate coated with the FL-BP/CB/PVdF. These images demonstrate that a complete and uniform coverage of the substrate is achieved with the FL-BP<sub>acetone</sub> sample. In contrast, for the deposited FL-BP<sub>CHP</sub>, the substrate is not uniformly coated. This inhomogeneous material distribution is attributed to the slow drying/evaporation of the CHP (hours timescale), and the temperature required to dry the electrode (~180°C). The heterogeneity in terms of material distribution, *e.g.*, FL-BP and CB/PVdF, on the electrodes is also analysed by using EDS and Raman mapping. The presence of FL-BP is characterized by means of EDS, analysing the K<sub>α</sub> energy of phosphorus (2.013 eV), while the presence of CB or PVdF is identified by investigating the K<sub>α</sub> energy of carbon (0.277 eV). In the FL-BP<sub>acetone</sub> sample, the EDS mapping (Figure 6.1c) shows that the phosphorus, in red, is homogeneously distributed onto the substrate and evenly spread with the carbon, in cyan. On the contrary, for the FL-BP<sub>CHP</sub> sample (Figure 6.1d), the phosphorus distribution suggests that the FL-BP is aggregated, while the carbon is uniformly distributed. The Raman mapping of the film-like deposited samples further support the different distribution of FL-BP in the two samples by monitoring the signal to baseline ratio of the A<sub>g</sub><sup>1</sup> peak. The Raman mappings of FL-BP<sub>acetone</sub> and FL-BP<sub>CHP</sub> are shown in Fig. 6e and Fig. 6f, respectively. The Raman mapping of FL-BP<sub>acetone</sub> shows the homogenous presence of the A<sub>g</sub><sup>1</sup> peak, with an average intensity of 0.5, which confirms the uniform distribution of FL-BP crystals onto the substrate. On the contrary, the FL-BP<sub>CHP</sub> Raman mapping presents preferential areas where the A<sub>g</sub><sup>1</sup> peak is concentrated (intensity 1) and others where the A<sub>g</sub><sup>1</sup> peak is not present (intensity 0), indicating aggregation of the FL-BP flakes.

The FL-BP-based anodes are then tested against a Li foil in a half-cell configuration, as described in the methods section. The electrochemical results of the FL-BP anodes are summarized in Figure 6.2. The CV measurement (Figure 6.2a) are performed at a rate of 30 μVs<sup>-1</sup> in order to get an electrochemical response for the Li ion transfer from the Li foil to the FL-BP-based anodes. [509, 510] The CV scan ranges from 0.05 V to 3 V vs Li<sup>+</sup>/Li, which is within the reaction range of both the formation of the solid-electrolyte interface (SEI) and the lithiation/de-lithiation processes for the BP material. [147] The first CV reduction cycle shows multiple peaks around 0.6-1.0 V, which are attributed to the phase change from BP → Li<sub>x</sub>P → LiP → Li<sub>2</sub>P → Li<sub>3</sub>P. [147]



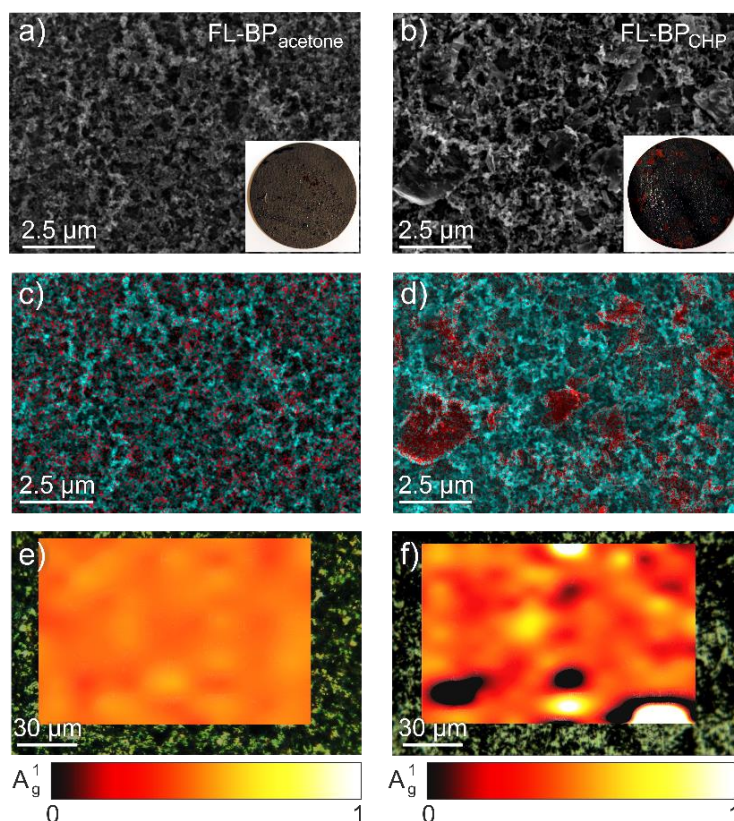


Figure 6.1. Scanning electron microscopy images of electrodes made of a)  $FL-BP_{acetone}$  and b)  $FL-BP_{CHP}$ , mixed with CB and PVdF deposited onto copper substrates. c) Energy-dispersive X-ray spectrometry elemental mapping of carbon (cyan) and phosphorus (red) of  $FL-BP_{acetone}$  and d)  $FL-BP_{CHP}$ . Raman mapping on the electrodes plotting the signal to baseline intensity of the  $A_g^1$  peak of e)  $FL-BP_{acetone}$  and f)  $FL-BP_{CHP}$ .

The voltage profiles of the FL-BP electrodes during the 1<sup>st</sup>, and 20<sup>th</sup> galvanostatic charge/discharge cycles are performed at a specific current of  $100 \text{ mA g}^{-1}$  between 50 mV and 3 V vs  $\text{Li}^+/\text{Li}$ , in order to complete the lithiation/de-lithiation (charge/discharge) process during each cycle (Figure 6.2b). From the first voltage profile of the  $FL-BP_{acetone}$  anode, an initial capacity of  $1732 \text{ mAh g}^{-1}$  and a discharge capacity of  $\sim 510 \text{ mAh g}^{-1}$  are measured. Such a high irreversible capacity ( $\sim 1220 \text{ mAh g}^{-1}$ ) is typical of nanoflake size-based anodes, [5, 511] and similar behaviour has already been reported for BP-based anodes. [148, 234] The high irreversible capacity is associated to the large quantity of Li ions that are consumed for the SEI formation on the FL-BP large surface area and trapped by the high energy binding on the edges. [5, 511] The voltage profiles of both FL-BP anodes show that more than 80% of the electrode capacity is delivered at a potential that is lower than 1 V vs  $\text{Li}^+/\text{Li}$  over the 20 cycles. Such a low potential is beneficial for the application of the FL-BP anode material to target high energy-efficiency LIBs. [191]

As shown in Figure 6.2c, both FL-BP anodes present a significant capacity which fades within the first 10 cycles. This could be caused by the large volume change that originates from the lithiation/de-lithiation processes during different  $\text{Li}_x\text{P}$  phases. [147] However, the  $\text{FL-BP}_{\text{acetone}}$  anode stabilizes at a specific capacity of  $\sim 480 \text{ mAh g}^{-1}$ , with a coulombic efficiency of 99.6% after 100 charge/discharge cycles, taken at a current density of  $0.1 \text{ A g}^{-1}$ . Meanwhile, the anode based on  $\text{FL-BP}_{\text{CHP}}$ , tested under the same experimental conditions, shows a specific capacity of  $\sim 200 \text{ mAh g}^{-1}$  with a coulombic efficiency of 99.6%. To get further insights on the performances, the two FL-BP electrodes are cycled between 50 mV to 3 V vs  $\text{Li}^+/\text{Li}$  at specific currents ranging from  $0.1$  to  $1 \text{ A g}^{-1}$  in order to investigate the electrochemistry activities of the samples during fast lithiation/de-lithiation (charge/discharge) processes. The results, presented in Figure 6.2d, demonstrate that the  $\text{FL-BP}_{\text{acetone}}$  electrode presents stable discharge cyclability with a specific capacity of  $447 \text{ mAh g}^{-1}$  at a specific current of  $0.2 \text{ A g}^{-1}$  after the 20<sup>th</sup> charge/discharge and a coulombic efficiency of 99.7%. On the other hand, under the same experimental conditions, the  $\text{FL-BP}_{\text{CHP}}$  electrode reaches a specific capacity of  $185 \text{ mAh g}^{-1}$  and a coulombic efficiency of 99.4% (Figure 6.2c and d).

Furthermore, for the  $\text{FL-BP}_{\text{acetone}}$  based anode, specific capacities of  $382 \text{ mAh g}^{-1}$  and  $345 \text{ mAh g}^{-1}$  are reached at current densities of  $0.5 \text{ A g}^{-1}$  and  $1 \text{ A g}^{-1}$ , respectively. Only less than a 30% drop in the specific capacities (from  $480 \text{ mAh g}^{-1}$  to  $345 \text{ mAh g}^{-1}$ ) is observed for the  $\text{FL-BP}_{\text{acetone}}$  anode which was tested at both a low ( $0.1 \text{ A g}^{-1}$ ) and a high current density ( $1 \text{ A g}^{-1}$ ), indicating that the  $\text{FL-BP}_{\text{acetone}}$  based battery is a promising option for fast charge/discharge devices. [149, 195, 512] Although the specific capacity of the  $\text{FL-BP}_{\text{CHP}}$  anode also presents a drop of 10% with the specific current varying from  $0.1$  to  $1 \text{ A g}^{-1}$ , its specific capacity still remains below  $200 \text{ mAh g}^{-1}$ , *i.e.* 50% lower than the one based on  $\text{FL-BP}_{\text{acetone}}$ . Moreover, the  $\text{FL-BP}_{\text{acetone}}$ -based anode outperforms previously reported anodes based on solution processed BP (*i.e.*  $\sim 200 \text{ mAh g}^{-1}$  at  $0.1 \text{ A g}^{-1}$  after the second discharge cycle, [500] and  $\sim 250 \text{ mAh g}^{-1}$  at  $0.1 \text{ A g}^{-1}$  after the first discharge cycle [234]). The difference in the electrochemical performances of the two different anodes, *i.e.* the specific capacity, is attributed to the aggregation of the  $\text{FL-BP}_{\text{CHP}}$  after the deposition, as demonstrated by both the SEM and Raman mappings reported in Figure 6.1. In contrast, the  $\text{FL-BP}_{\text{acetone}}$  flakes do not aggregate after the deposition onto the copper substrate.

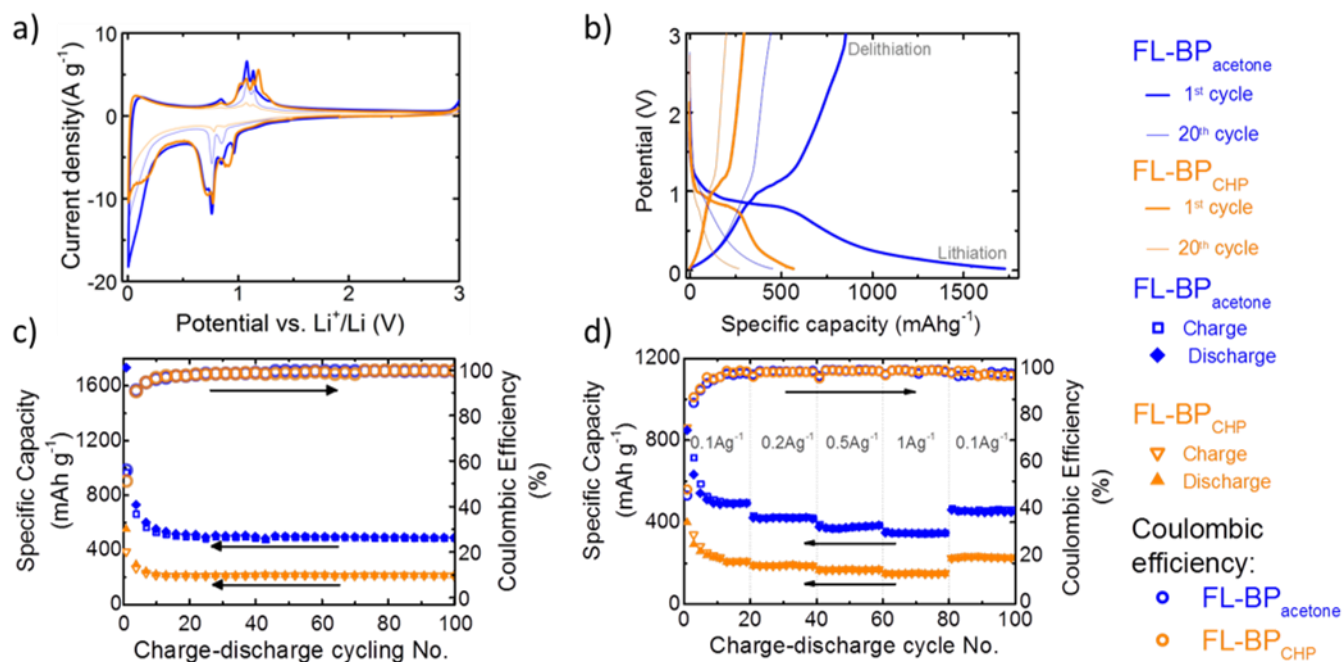


Figure 6.2. The electrochemical analysis of the FL-BP film (acetone exfoliated sample data points shown in blue; CHP exfoliated sample data points shown in orange). (a) Cyclic voltammograms at a scan rate of  $30 \mu\text{Vs}^{-1}$  and (b) voltage profile upon galvanostatic charge/discharge of BP-based electrodes at  $0.1 \text{ A g}^{-1}$  between  $50 \text{ mV}$  and  $3 \text{ V}$ . Thick and thin lines correspond to  $1^{\text{st}}$  and  $20^{\text{th}}$  cycle, respectively. (c) Specific capacity and coulombic efficiency over galvanostatic charge/ discharge and cycling between  $50 \text{ mV}$  and  $3 \text{ V}$  at  $0.1 \text{ A g}^{-1}$  (d) and different specific currents, for both the FL-BP<sub>acetone</sub>- and FL-BP<sub>CHP</sub>-based electrode

### 6.3. Conclusion

In conclusion, the exfoliation of bulk BP in acetone has been exploited for the realization of LIB anodes. The FL-BP<sub>acetone</sub> flakes are homogeneously distributed onto the current collector substrate thanks to the fast solvent removal. The FL-BP<sub>acetone</sub> based anodes, tested in half-cell configuration, achieved a specific capacity of  $480 \text{ mA h g}^{-1}$  at a current density of  $0.1 \text{ A g}^{-1}$ , with a coulombic efficiency of  $99.6\%$  after 100 charge/discharge cycles. The FL-BP<sub>acetone</sub>-based anode outperformed the FL-BP<sub>CHP</sub>-based one ( $\sim 200 \text{ mA h g}^{-1}$  after 100 cycles at  $0.1 \text{ A g}^{-1}$ , achieving a coulombic efficiency of  $\sim 99.0\%$ ). The proposed liquid phase exfoliation process can also be scaled-up since the use of acetone does not present environmental risks, whereas both CHP and NMP do. Finally, the exfoliation of BP in acetone can be further improved by the addition of acetone-soluble polymers, thus enabling the large-scale production of FL-BP/polymer composites.

# Chapter 7:

## Conclusion and outlook

Up to date, the search for novel materials is still one of the crucial quests for the development of high-performance lithium ion batteries (LIBs). In this context, two dimensional materials (2D) have been recognized as promising candidates for future LIB applications because their unique structure not only provides the efficient ion transport channels between the layers, facilitating the diffusion of  $\text{Li}^+$ , but also offers the large surface area for  $\text{Li}^+$  storage. Graphene, transition metal oxides (TMOs) and transition metal sulfides (TMSs) and black phosphorous (BP) have been recognized as promising materials for future LIB technology. Therefore, this thesis focused on the production of graphene,  $\text{MoO}_3$  (as a representative for TMOs) and  $\text{MoS}_2$  (as a representative for TMSs) and BP by liquid phase exfoliation (LPE) of their bulk counterparts for LIB anodes. The study of graphene anode provides a fast and simple preparation route to fabricate binder-free graphene anode for the improvement of specific capacity with respect to commercial graphite anode. Moreover, the study on the effects of flakes dimensions (lateral size and thickness) on the electrochemical performance of graphene flakes as anode material provides the guidelines for the practical exploitation of graphene-based electrodes. In addition to graphene, the understanding of the electrochemical properties of  $\text{MoO}_3$  and  $\text{MoS}_2$  provides a strategy in material synthesis, *e.g.*, single wall carbon nanotube bridge- $\text{MoO}_3$  flakes ( $\text{MoO}_3/\text{SWNTs}$ ) hybrid and  $\text{MoS}_2$  flakes/amorphous carbon hybrid ( $\text{MoS}_2/\text{C}$ ), to overcome the current issues of these materials for LIB anode, *e.g.*, volume change upon cycling, low electrical conductivity. Furthermore, the activity on the exfoliation of BP in different solvents offers the opportunity to understand the role of solvent parameters on exfoliation and dispersability of BP flakes. Based on this, we can determine the ideal solvent which can meet the requirement for the exfoliation of BP and the realization of LIBs. The aim of this chapter is to summarize the most relevant results achieved on graphene,  $\text{MoO}_3$ ,  $\text{MoS}_2$  and BP based anodes. In addition, the future developments for each of these materials in LIB technology are discussed.

### 7.1. Graphene-based anode for lithium ion batteries

The aim of my research on graphene based LIB anode relied on the exploitation of LPE to produce graphene flakes from graphite (LPE graphene) because the LPE graphene flakes have high crystallinity, that is, a key feature for assuring fast electron transport to the electrode support. In this work, the obtained graphene ink after LPE process is enriched in single-layer (SLG) and few-layer (FLG) graphene flakes. However, the drawback of LPE graphene is the

use of high boiling-point, toxic solvent, *e.g.*, N-Methyl-2-pyrrolidone (NMP) which is a critical issue both for the electrode deposition and the health and environment. Therefore, the solvent-exchange process of graphene flakes by using vacuum filtration was exploited to exchange NMP into a low-b.p. and environmental-friendly solvent, *e.g.*, ethanol (EtOH). In addition, it is important to evaluate the influence of solvent exchange process on the physical and chemical properties of the graphene flakes. To this aim, transmission electron microscopy (TEM), X-ray photoelectron spectroscopy (XPS) and Raman spectroscopy have been used. In particular, comparing the TEM and Raman characterizations of graphene flakes in NMP and EtOH, it is clearly demonstrated that the solvent exchange process does not affect the structural and morphological properties of the graphene flakes. Besides, the XPS analysis indicates that from one hand the solvent exchange process does not induce oxidation of the graphene flakes and from the other hand, it allows the removal of ~50% of the NMP molecules adsorbed onto the graphene flakes. Briefly, the solvent exchange process allows obtaining high crystallinity graphene flakes in EtOH, which enables the fast electrode fabrication at room temperature with respect to graphene flakes in NMP.

Taking the advantage of solvent exchange process, I fabricated the binder-free graphene anode via drop-casting graphene flakes in EtOH at room temperature (one-step fabrication) and studied its electrochemical properties. The graphene electrode in half-cell configuration exhibits remarkable electrochemical performance and stability, a charge/discharge specific capacity of 503 mA hg<sup>-1</sup> after 100 cycles at a current density of 100 mA g<sup>-1</sup> with a coulombic efficiency > 99.5%. Moreover, the graphene anode shows its functionality also in a full-cell configuration, exploiting commercial LiNi<sub>0.5</sub>Mn<sub>1.5</sub>O<sub>4</sub> (LNMO) as cathode, with a reversible specific capacity of ~ 100 mAh g<sup>-1</sup>. The results obtained by using the binder-free graphene electrodes, both in half- and full-cell configuration, provides useful guidelines for the practical exploitation not only for graphene but also for other 2D materials as stand-alone anode materials in LIBs. Moreover, compared to the commercial graphite anode the one-step preparation route of binder-free graphene anode is opening the way to the improvement of capacity (by utilizing 100% the weight of active material) through a low-cost, facile coating process (drop-casting of graphene dispersion at room temperature), with consequent reduction of the environmental impact (using environmental friendly solvents).

The dimension (lateral size and thickness) of the graphene flakes has an important role in the Li<sup>+</sup> storage mechanisms, but the link between these morphological properties, and electrochemical performances were not established yet. Therefore, the sorting of graphene flakes after the exfoliation of graphite with various dimensions by means of sedimentation based separation (SBS) has been carried to clarify the roles of graphene flakes dimension on

electrochemical performance of LIB anode. The SBS exploiting different centrifugal speeds, coupling with the solvent exchange process allows producing four dispersions of graphene flakes in NMP. The TEM and AFM measurements have been exploited for the characterization of the flakes morphology of the four samples. In particular, the graphene flakes dimension decreases, from Sample#1 to #4, with the increase in centrifugal speed. The Raman spectroscopies of graphene flakes in the four samples show that Sample#1 and #2 are mostly formed of thick (20–50 layers) MLG flakes, while Sample#3 is composed of thinner multi-layer graphene (MLG) (10–15 layers) and Sample#4 comprised of FLG flakes. Importantly, the obtained electrochemical results demonstrate that the MLG flakes (20–50 layers) having average lateral size ranging from 180–380 nm, have not yet demonstrated considerable gain in maximum specific capacity ( $\sim 341\text{--}366 \text{ mAh g}^{-1}$ ) compared to the theoretical specific capacity of graphite ( $372 \text{ mAh g}^{-1}$ ). Meanwhile, more capacity is delivered at high potentials ( $> 0.2 \text{ V vs Li/Li}^+$ ) upon graphene flake size reduction, due to the preferential  $\text{Li}^+$  storage by adsorption rather than intercalation in small lateral size ( $\sim 100 \text{ nm}$ ) and thin ( $< 15$  layers) flakes, resulting in reduced and non-constant voltage output, which is a detrimental factor for voltage efficiency. This study demonstrates that graphene might be still involved in the list of ultimate LIB electrode materials, but it may not be considered as the active materials. Nevertheless, graphene can be used as a supporting platform for other types of active materials in composite or hybrid structures, *e.g.*, conductive agent, buffered layer for volume change of active material, etc.

## **7.2. Molybdenum oxides- and molybdenum disulfide-based anode for lithium ion batteries**

In the second part of my PhD program, I started to investigate the electrochemical properties of  $\text{MoO}_3$ ,  $\text{MoS}_2$  flakes and their carbon-based hybrid structures with the aim to contribute in the understanding on the effects of carbon materials on  $\text{Li}^+$  storage ability of  $\text{MoO}_3$  and  $\text{MoS}_2$ . Although  $\text{MoO}_3$  and  $\text{MoS}_2$  exhibit high theoretical capacity with respect to that of graphite, these materials are still commonly facing the issues of volume change upon cycling and low electrical conductivity. Thus, nanostructuring and hybrid synthesis were proposed to be the viable strategies to overcome the current issues of  $\text{MoO}_3$  and  $\text{MoS}_2$ . In particular, the nano-sized  $\text{MoO}_3$  and  $\text{MoS}_2$  flakes reduce the length for  $\text{Li}^+$  diffusion and mitigate the volume change during charging/discharging process with respect to their bulk counterparts. In addition to nanostructuring, the synthesis of  $\text{MoO}_3/\text{SWNTs}$  and  $\text{MoS}_2/\text{C}$  hybrid is an effective strategy to exploit the preminent properties of carbon-based materials, *e.g.*, high electrical conductivity and mechanical strength, to compensate for the limited properties of active materials, *e.g.*, buffering the volume change and enhancing the conductivity of electrodes.

In the case of MoO<sub>3</sub> flakes-based anode, the MoO<sub>3</sub>/SWNTs hybrid was formed by exploiting a simple solution mixing process. The SWNTs in MoO<sub>3</sub>/SWNTs hybrid play a role of bridging the isolated MoO<sub>3</sub> flakes, forming an interconnected network in the mixture of MoO<sub>3</sub>/SWNTs. This structure enables long channels for electron transport and a buffered frame for accommodating the volume change of active material during lithiation/de-lithiation process. Indeed, the surface morphology of the MoO<sub>3</sub>/SWNTs hybrid electrode after 100 charge/discharge cycles demonstrates that the SWNTs in the MoO<sub>3</sub> /SWNT electrode create a network between the cracked ‘islands’ following the MoO<sub>3</sub> volume change during charge/discharge cycles. Hence, the MoO<sub>3</sub>/SWNTs hybrid anode displays a high specific capacity of ~ 865 mAh g<sup>-1</sup> at 100 mA g<sup>-1</sup> after 100 cycles, with a columbic efficiency of ~99.7%. This study set the basis for the exploitation of exfoliated MoO<sub>3</sub> flakes as anode materials in high LIB. Moreover, the binder-free MoO<sub>3</sub>/SWNTs hybrid anode prepared by a simple method can boost the development of high performance anodes for LIBs.

Taking advantages of the knowledge on the use of carbon based material in MoO<sub>3</sub>/SWNTs hybrid, I successfully synthesized the amorphous carbon/MoS<sub>2</sub> flakes hybrid. The hybrid structure consists of MoS<sub>2</sub> flakes incorporated in an amorphous carbon network. The carbon in the MoS<sub>2</sub>/C hybrid plays the role of conductive network, promoting the electron transport and also acts as a buffer layer for the active material, accommodating its volume variation upon cycling. However, controlling the carbon content (wt%) in MoS<sub>2</sub>/C hybrids is also an important task because it determines the thickness of carbon layer which highly influence to the Li<sup>+</sup> diffusion in the electrode. To do so, I synthesized three MoS<sub>2</sub>/C hybrids with different carbon contents of ~10.00%, 16.11% and 29.86% corresponding to sample MoS<sub>2</sub>/C-1, MoS<sub>2</sub>/C-2 and MoS<sub>2</sub>/C-3, respectively. The thickness of the carbon layer is found to increase with the increase in carbon content in the MoS<sub>2</sub>/C hybrids. Especially in the MoS<sub>2</sub>/C-1 hybrid, the low carbon content is unable to completely cover the MoS<sub>2</sub> flakes. The electrochemical performance of MoS<sub>2</sub>/C hybrids demonstrates that all hybrid electrodes feature a stable reversible capacity and low charge transfer resistances (R<sub>CT</sub>) upon 100 charge/discharge cycles with respect to that of pristine MoS<sub>2</sub>. This indicates the role of carbon in improving the electrode conductivity and buffering volume change of MoS<sub>2</sub>. Indeed, the morphology of the electrode surface after 100 cycles show that with the increase in carbon content, the formation of fractures gradually disappears on the surface of hybrid electrodes, confirming the role of carbon network in the structural preservation, avoiding pulverization of electrodes. Moreover, it has been observed that the insufficient carbon content in MoS<sub>2</sub>/C-1 sample leads to the pulverization of electrode, whereas the excess carbon content in MoS<sub>2</sub>/C-3 sample limits the Li<sup>+</sup> diffusion. As a result, both MoS<sub>2</sub>/C-1 and -3 electrodes exhibit lower reversible specific

capacity than that of the MoS<sub>2</sub>/C-2 one, which features a proper amount of carbon covering on MoS<sub>2</sub> flakes. The improved electrochemical performance of MoS<sub>2</sub>/C-2 sample with respect to MoS<sub>2</sub>/C-1 and -3 ones indicates that proper carbon content not only improves the electrical conductivity of the electrode by facilitating the electron transport, but also acts as a buffer layer for active materials to avoid its volume change upon cycling.

In summary, the electrochemical performances of MoO<sub>3</sub>/SWNTs and MoS<sub>2</sub>/C electrodes demonstrate an effective strategy in hybrid/composite synthesis to produce high performance LIB anode. Both the MoO<sub>3</sub>/SWNTs and MoS<sub>2</sub>/C hybrids are produced by facile fabrication protocols that can also be easily extended to the construction of hybrid structures of other 2D nano-crystals in carbon-based material networks for LIB application.

### **7.3. Black phosphorous based anode for lithium ion batteries**

In the last activity of my thesis, the production of FL-BP was carried out via LPE to investigate the solvent parameters which are relevant to the selection of an ideal solvent for the exfoliation of BP. In specific, the selected solvent should be able to: (i) exfoliate BP; (ii) keep a stable dispersion of the exfoliated flakes, *i.e.* the exfoliated flakes should not flocculate or precipitate; (iii) prevent the degradation of the exfoliated flakes by oxidation; (iv) be easily removed without leaving impurities. The exfoliation of BP in 14 different solvents were carried out and then the dispersability properties of few-layers BP (FL-BP) were evaluated, based on  $\gamma$ , Hansen solubility and Hildebrand parameters. Among the different trials, although the N-Cyclohexyl-2-pyrrolidone (CHP) is the solvent that promotes the highest concentration compared with all the other solvents, but it still showing the drawbacks of toxicity and high-boiling point (b.p.), the detrimental factors in LIB technology. Importantly, it has been recognized that the BP exfoliation is also possible in acetone, a well-known non-toxic solvent with a low-b.p. The morphological and structural characterization reveals that the exfoliated BP flakes in acetone are undamaged by the LPE process, and have an average lateral size of ~30 nm and an average thickness of ~7 nm. More importantly, by using electron energy loss (EEL) and Raman spectroscopies, it is demonstrated that the aging of exfoliated BP flakes in acetone is comparable with the one obtained by using high-b.p. solvent, *e.g.*, CHP. The successful exfoliation of BP in acetone creates the feasible and up-scalable approach for fast electrode deposition in LIB technology. The FL-BL<sub>acetone</sub>-based anode outperformed the FL-BP<sub>CHP</sub> - based one. These findings indicate that the FL-BP<sub>acetone</sub> - based LIB anode is promising with regards to the design of fast charge/discharge devices. Overall, the presented process is a step forward towards the fabrication of phosphorene-based devices.



#### 7.4. Future development

Liquid phase exfoliation of layered material is an effective strategy to produce 2D materials with low-cost, simplicity and high output, which can be applied for LIBs to reach the industrial-scale. This method can not only be used for MoO<sub>3</sub> and MoS<sub>2</sub>, but can also be extended to other 2D crystals. The key parameter of LPE is the solvent used in the process which determines the production yield. The current solvents to exfoliate 2D crystal are mostly high-b.p. and toxic organic solvents, *e.g.*, NMP, DMF, CHP, benzyl benzoate, etc. which are not favourable for future LIB technology. Therefore, the searching and the new solvents and modifying the composition of solvents to meet the requirements of exfoliation of 2D crystals, *e.g.*, the surface energy of solvents have to be close to the surface tension ( $\gamma$ ) of 2D flakes, the solvents have to be non-toxic, low-b.p., etc., is one of the future missions for research community to further develop the industrial-scale production of LIB materials.

In this thesis, the solvent exchange process of graphene flakes via vacuum filtration technique was explored as a promising route to the processing of environmentally friendly graphene ink, which allows one step fabrication of binder-free electrode for LIBs. This approach should be further exploited for other 2D materials, *e.g.*, TMOs, TMSs for the realization of LIB anode with high capacity. However, the vacuum filtration technique still has a drawback of losing material in filtering membrane. Thus, the solvent exchange process can be realized by other techniques, which should be further investigated for the realization of the simple, fast, effective and low-cost electrode fabrication.

Furthermore, the understanding of the role of graphene flakes dimension on their Li<sup>+</sup> storage ability provides the guidelines for the practical exploitation of graphene-based electrodes. One of the potential future directions in graphene-based LIB is exploiting hybrid structures of graphene with an active material with high theoretical capacity, *e.g.*, alloying materials, TMOs and TMSs, to fully utilize the novel properties of graphene, *e.g.*, high electrical conductivity, large surface area and high mechanical strength for the improvement of the Li<sup>+</sup> storage ability. As discussed in section 1.2.3, although exhibiting the large theoretical capacities, Si, TMOs, TMSs alone are still facing with the issues of low conductivity and large volume change. Owing to the impressive electrical conductivity, graphene was proposed as a conductive agent to improve the conductivity of these electrodes. [513] Moreover, the large surface area of graphene can buffer the volume change of active materials in Si, TMOs and TMSs electrodes. Besides, superior thermal conductivity of graphene can be advantageous for dissipating the heat generated in LIBs in the case of high current loads. [514] Recently, six models of graphene-based composites have been reported: encapsulated,

mixed, wrapped, anchored, sandwich-like and layered models [513], see Figure 7.1. The uses of each model depend on the design of active materials. For example, the graphene/nanoparticles based composites are commonly described by the encapsulated, mixed, wrapped and anchored models, whereas sandwich-like and layered models are associated to the composites of graphene and other 2D materials. In the case of LPE graphene flakes, the mixed model can be the ideal case for designing LIB anode material. [515]

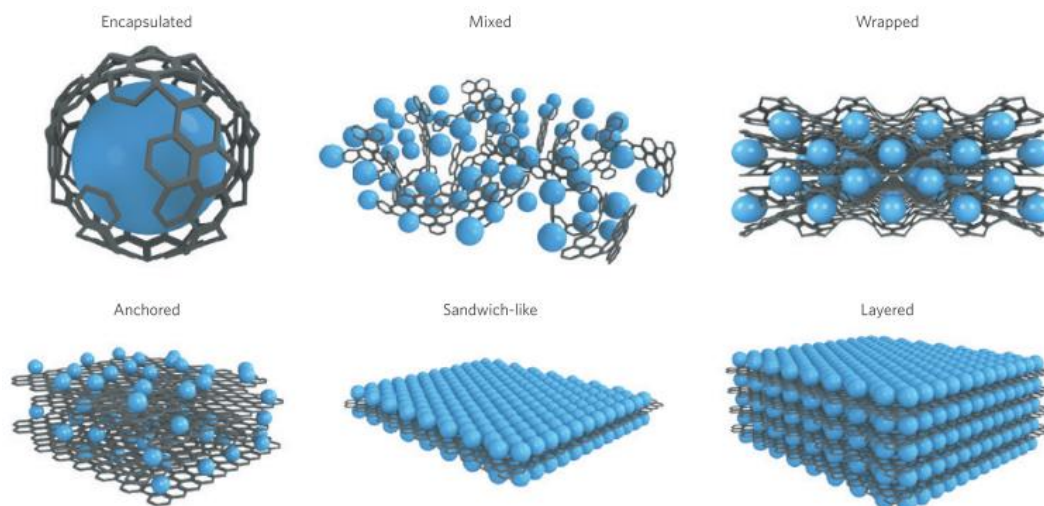


Figure 7.1. *Structural models of graphene composites.* [191]

The activities on  $\text{MoO}_3$  and  $\text{MoS}_2$  based anodes enable the use of carbon based materials in improving the electrochemical performance of anodes based on 2D materials. It should be noted that the electrochemical performances of  $\text{MoO}_3/\text{SWNTs}$  and  $\text{MoS}_2/\text{C}$  highly depend on the characteristics of adopted carbon based materials, such as the structure, morphology and content. Hence, optimization of the carbon network and synthesis of novel hybrid/composite structures, are the critical strategies for the future development of  $\text{MoO}_3$  and  $\text{MoS}_2$  for high performance LIB anodes. The choice of carbon-based materials for hybrid/composite structure with  $\text{MoO}_3$  or  $\text{MoS}_2$  is not limited to SWNTs and amorphous carbon. For example, the hybrid structures of  $\text{MoO}_3/\text{graphene}$  or  $\text{MoS}_2/\text{graphene}$  should be exploited for the realization of high performance LIB anode. Moreover, the development of well-designed architectures based on  $\text{MoO}_3$  and  $\text{MoS}_2$  materials could bring a new way to develop advanced TMOs- and TMSs-based electrodes with high energy density, high power density, and long cycle life for LIBs. Also, it is necessary to further develop and optimize the protocols for large-scale and environmentally friendly production of TMOs, TMSs and their hybrid/composites for LIBs applications. In addition, the control of lateral size and thickness of layered TMOs and TMSs via SBS can provide an enhanced specific surface area, increased number of active sites, and a faster ion transport, which could generate electrode materials for high rate electrochemical energy storage. The electrochemical properties of the 2D flakes can

be further improved by a rational structure design based on nanoscale manipulation of 2D flakes, such as aligning 2D nanosheets or constructing 3D nanosheets interconnected networks. To some extent, although the rechargeable performance of TMO- and TMSs-based materials has been studied, the correspondence between structure and performance is needed to be further clarified. The actual mechanism underlying these electrochemical properties is somewhat unclear to researchers. Further investigations into the trigger origin of electrochemical reaction and the principle of capacity retention need to be carried out. In this regard, in-situ TEM observation and operando X-ray techniques combined with cyclic voltammetry technology are strong tools for researches of electrochemical mechanism. The above proposed studies will pave a way for the innovative design of high performance LIB anodes based on TMOs and TMSs.

As for BP exfoliation, the LPE of BP in acetone still can be further improved by the addition of acetone-soluble polymers which can scale-up the production. Thus, formulating the acetone-based solvents is one of the essential works for future development of large-scale production of FL-BP based anode for LIBs and other applications. In the field of LIBs, the low-b.p. of acetone allows fast fabrication of FL-BL<sub>acetone</sub> based anode which exhibiting the stable specific capacity. However, the anode also shows large irreversible capacity during the first few cycles before getting a stable performance, resulting in a relatively low specific capacity with respect to the report from Cui *et al.* [149] In this regard, further studies need to be realized to investigate the morphology of BP flakes which is able to play a very important role in irreversible Li<sup>+</sup> storage. The defects on the flakes edges may trap the Li<sup>+</sup> producing the observed capacity loss. Besides, the FL-BP flakes in this thesis have favorable panel structure with controllable dimension can not only fully exploit the large inter-layer space for the fast charge-discharge approaching, but also minimize the damage caused by its volume change during cycles. Moreover, its high rate capacity and stability is attractive for industrial applications. Therefore, I believe that the FL-BL<sub>acetone</sub> based anode is promising and can be further improved for high-performance LIBs. Several strategies have been considered to improve BP batteries. For instance, by coating or bonding the BP flakes surface/edges with carbon materials and increasing the percentage of BP flakes in the electrode. In this way the battery is expected to exhibit better performances in terms of capacity and energy density. However, the additives have to be selected properly. The 2D or 3D structured additives, such as CNTs and graphene networks, are also expected to improve the conductivity of the anode materials and prevent the volume change. Binder materials with high elastic property may also take into the further investigation list.

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