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Comparison of ultra high temperature (UHT) stability of high protein milk dispersions prepared from milk protein concentrate (MPC) and conventional low heat skimmed milk powder (SMP)

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1 **Title: Comparison of ultra high temperature (UHT) stability of high protein milk dispersions**
2 **prepared from milk protein concentrate (MPC) and conventional low heat skimmed milk**
3 **powder (SMP)**

4
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26 **Abstract:** This study compared the UHT (145 °C for 5 s) stability and fouling behavior of high
27 protein milk dispersions prepared from reconstituted low heat skimmed milk powder (RSMP) and
28 milk protein concentrate powder (RMPC). It was found that RMPC at 10 and 14% protein content
29 was more UHT stable as compared to lower protein content RSMP (3.25, 6.5, 7, 7.5, 8 %).
30 Matching the total solids and mineral composition of 7.5-RMPC with 7.5-RSMP by addition of
31 minerals and lactose markedly reduced its UHT stability (UHT run-time reduced to 66 min from
32 >120 min). The RP-HPLC analysis showed increased casein dissociation but similar whey protein
33 aggregation in 7.5-RSMP as compared to 14-RMPC. UHT processing lead to formation of larger
34 particles in case of 7.5-RSMP (1.84 μm D(0.9)) as compared to 14-RMPC (0.23 μm D(0.9)). It was
35 observed that mineral environment affected protein interactions leading to the differences in UHT
36 behavior of RSMP and RMPC.

37

38 **Keywords:** Milk powders; ultra high temperature processing; milk proteins; fouling; milk minerals

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1 Introduction

51
52 Increased consumer awareness towards benefits of protein in diet and its positive effects on weight
53 loss and muscle building has surged the demand for high protein weight loss diets (Friedman,
54 2004). There are various formats of high protein processed foods available in the market, but ready-
55 to-drink (RTD) high protein beverages are notable departure from typical powder type sports
56 supplements specifically targeted at body builders and sports people (Baxter et al., 2011). Due to
57 their convenience, high protein beverages are also appealing to health conscious ordinary
58 consumers. RTD high protein beverages based on milk proteins are processed liquid food products.
59 Manufactures combine high protein dairy powders along with other ingredients to obtain a ready to
60 drink product with desired protein, fat and carbohydrate content, amino acid profile and sensory
61 attributes (Jelen, 2011, Baxter et al., 2011). The RTD high protein beverages are required to contain
62 high protein levels without compromising product stability and quality. Food and drug
63 administration (FDA) of the United States requires adding minimum 10 g protein per 240 ml of
64 drink (~ 4.2%) to claim high protein beverage (Etzel, 2004).

65
66 There are several types of milk protein ingredients available in the market. Skim milk powder
67 (SMP), whole milk powder, milk protein concentrate powders (MPC), casein and whey protein
68 concentrate powders are widely produced and used as ingredients in a range of milk protein based
69 beverages. MPCs are complete dairy proteins, containing casein and whey proteins in their original
70 proportions found in milk and in their native state. Much of the caseins in concentrates are in
71 micellar form and whey proteins are largely undenatured (Agarwal et al., 2015). The protein content
72 of MPC varies from 42 to 85%, which is indicated by the number following MPC, e.g. MPC85.
73 MPCs find application in the manufacture of food emulsions, cheese, yogurt, ice cream, health
74 related products and various other dairy products (Kelly, 2011). There is growing popularity of
75 MPC as a protein source in neutral pH RTD high protein beverages due to the fact that it is an
76 excellent source of protein and can provide a milky flavor and opacity to the drink (Agarwal et al.,

77 2015). MPC are manufactured from skim milk by ultrafiltration and diafiltration process, followed
78 by spray drying the retentate (Havea, 2006). The filtration process also partially removes lactose
79 and mineral salts from the milk. Due to the significant differences in the composition of non-protein
80 constituents of MPC and SMP, reconstituted MPC (RMPC) can provide more protein per total
81 solids as compared to reconstituted SMP (RSMP) (Deeth and Hartanto, 2009). However, RMPC
82 contains altered mineral environment as compared to RSMP due to ultrafiltration and diafiltration
83 process used to concentrate milk proteins during MPC manufacturing process. MPC contains more
84 calcium than SMP, however per unit of protein MPC contains less calcium (Kelly, 2011).

85

86 Generally, There are two types of high protein beverages based on milk protein ingredients: neutral
87 pH (pH~6.8) and low pH acidic beverages (Beecher et al., 2008). MPC based beverages are mostly
88 neutral pH beverages due to its high casein content (Agarwal et al., 2015). Neutral pH beverages are
89 required to be commercially sterilized to make them shelf-stable for a longer storage period. UHT is
90 a commonly used technology for thermally processing these products. There are less colour and
91 flavour changes and minimal losses of nutrients during UHT due to very short holding time and
92 faster heat transfer as compared to retort sterilisation (Burton, 1994). However, thermal processing
93 of dairy products causes formation of deposit layers on heat transfer surfaces, which is known as
94 fouling (Sadeghinezhad et al., 2013). Fouling is a result of heat-induced destabilisation of milk
95 constituents during processing which can limit the processing time and incur costs of cleaning and
96 processing down times. Fouling may also adversely affect product quality due to dislodgement of
97 deposits and mixing with product. Fouling deposits has very low heat conductivity as compared to
98 process surfaces and fouling layers can reduce the heat flow, which causes insufficient processing
99 of product (Prakash et al., 2005). In addition, increased obstruction to fluid flow can cause pressure
100 drops across the processing line. These issues may increase the energy requirements due to
101 increased energy costs to maintain adequate processing condition. In a worst scenario UHT
102 processing plant may also be required to be shut down for cleaning (Bansal and Chen, 2006). There

103 are several factors affecting fouling of heat transfer surfaces which can be broadly classified as
104 product and processing factors (Deeth, 2010). Understanding the behaviour of a milk product
105 during UHT processing can be of great importance in controlling fouling and increasing run-time of
106 processing plant. Milk protein system consists of different types of proteins and a complex mixture
107 of native whey proteins, whey protein aggregates and whey protein-casein complexes can be
108 formed during heating of milk protein dispersions (Wijayanti et al., 2014).

109
110 The heat stability of milk proteins and their susceptibility to denaturation and aggregation and final
111 composition of this mixture depends on the temperature and time of heating, pH, relative abundance
112 of other proteins and salts in the food system (Singh, 2004). Difference in thermal stability of
113 proteins coming from different milk protein ingredients can play an important role in determining
114 UHT stability of the final product (Sikand et al., 2010). In case of high protein beverages,
115 improved UHT stability can be achieved by choosing a milk protein powder based on knowledge
116 about their heat stability. The differences in composition of SMP and MPC can cause these two
117 protein dispersions to behave differently during UHT processing. A lot of research has been
118 conducted on UHT stability of normal strength and concentrated RSMP, but not sufficient work has
119 been previously reported on UHT processability of RMPC. More research is required on UHT
120 stability of RMPC because of its increasing usage in formulation of UHT processed RTD high
121 protein beverages (Agarwal et al., 2015).

122
123 The present work is focused on understanding the behavior of high protein milk dispersions
124 prepared from MPC and compare with conventional low heat SMP during UHT processing. An
125 understanding of UHT stability and fouling behavior of RMPC can be beneficial for controlling and
126 minimizing heat induced fouling during use of MPC in commercially sterilized high milk protein
127 beverages, and other UHT treated products.

128 **2 Materials and Methods**

129 **2.1 Materials**

130 Commercial MPC and low heat SMP (purchased from Real Dairy Australia Pty. Ltd, Australia)
131 were used in the preparation of reconstituted milk protein dispersions for all but one experiment for
132 which MPC-G from a different manufacturer was purchased from Maxum Foods, Queensland,
133 Australia for comparison purposes. Lactose was procured from Bio-Strategy Laboratory Products
134 Pty. Ltd., Queensland, Australia. Standards for pure proteins were bought from Bio-Rad, Australia.
135 Other chemicals and reagents were purchased from Sigma-Aldrich Pty. Ltd., NSW, Australia unless
136 otherwise stated. Simulated milk ultrafiltrate (SMUF) was prepared according to the recipe by
137 Jenness and Koops (1962).

138

139 **2.2 Compositional and quality analysis of milk powders**

140 MPC and SMP were analyzed for total protein content and lactose content using Kjeldahl method
141 (AOAC, 2005) and titrimetric method (AS, 1994), respectively. MPC and SMP were also analyzed
142 for mineral composition using Inductively Coupled Plasma-Optical Emission Spectrometric (ICP-
143 OES) analysis as described by Martinie and Schilt (1976).

144

145 MPC was also analyzed for its solubility according to Bansal et al. (2017). MPC solubility was
146 analysed at rehydration temperature of 50°C, which was the temperature used for reconstitution of
147 samples throughout this study. The solubility of each sample was calculated as follows:

148

149 Solubility (%) = (total solids per g of filtrate/ total solids per g of suspension) * 100

150

151 **2.3 Undenatured whey proteins and electrophoresis of milk powders**

152 Undenatured whey proteins were quantified by adjusting the pH of RMPC and RSMP to 4.6 using
153 2M HCl or 2M NaOH, followed by centrifugation at 4500 g at 20⁰C for 15 min to precipitate serum
154 caseins and denatured soluble whey proteins (García-Risco et al., 1999). Supernatants were
155 analyzed for protein content using Kjeldahl method (AOAC, 2005). All measurements were
156 performed in duplicates. Undenatured whey protein content was reported as percentage of total
157 protein content of RMPC and RSMP.

158
159 Sodium Dodecyl Sulphate–Polyacrylamide Gel Electrophoresis (SDS-PAGE) analysis was
160 performed under reducing (R SDS-PAGE) and non-reducing (NR SDS-PAGE) conditions
161 following the method of Laemmli (1970). Precast polyacrylamide gels (4-20%), sample buffer and
162 Precision Plus Protein™ Dual Xtra molecular weight standard were obtained from Bio-Rad
163 Laboratories Pty. Ltd, NSW, Australia. All other preparations for SDS-PAGE analysis were based
164 on the standard guidelines in the Bio-Rad manual (Catalog number 161-0993. Samples were mixed
165 1:1 with 2X sample buffer for NR SDS-PAGE analysis. For R SDS-PAGE analysis, samples were
166 mixed with sample buffer containing 10% β-mercaptoethanol and heated at 95⁰C for 5 min. 10 μg
167 protein was loaded onto each well. Electrophoresis was carried out at 80 V for 30 min and then at
168 100 V. Bio-Rad Mini Protean Tetra Cell system (Bio-Rad Laboratories Pty. Ltd, NSW, Australia)
169 was used to run the gels. The gels were stained overnight with a solution of 0.04% Coomassie
170 Brilliant blue G250, 25% methanol and 10% acetic acid in water. The gels were scanned and
171 analyzed using Bio-Rad GS-800 Calibrated Densitometer (Bio-Rad Laboratories Pty. Ltd, NSW,
172 Australia).

173

174 **2.4 Preparation of reconstituted milk protein dispersions**

175 Calculated amounts of milk powders, lactose, SMUF and distilled water were mixed to achieve
176 required (w/w) protein content (PC) and total solids (TS) of RMPC and RSMP. Table 1 shows
177 different samples and sample codes used in this study. Suffix UN and UHT were used to denote
178 unheated and UHT heated samples, respectively. Reconstituted protein dispersions were prepared
179 by reconstituting milk powders in distilled water at 50 ± 2 °C. The protein dispersions were kept
180 under refrigeration overnight (~14 h) to ensure complete hydration of all powder particles. Protein
181 dispersions were then allowed to reach room temperature. pH of protein dispersions were analyzed
182 and adjusted to 6.8 using 2M NaOH or 2M HCl, if required. Milk protein dispersions were filtered
183 to remove any undissolved particles.

184

185 **2.5 Ethanol stability of reconstituted milk protein dispersions**

186 Ethanol stability was determined by mixing equal volume (2 mL) of milk and a range of ethanol
187 solutions (50 to 100% at 2% intervals) and carefully examining the sample for clotting when poured
188 in a petri dish. The highest concentration of ethanol, which did not cause coagulation, was reported
189 as ethanol stability for the sample.

190

191 **2.6 Ionic Ca activity in reconstituted milk protein dispersions**

192 Ca-ion activity in milk protein dispersions was measured using LAQUAtwin calcium ion meter
193 (Horiba Instruments, Japan). The calcium ion meter was calibrated using 3.74 mM (150 ppm) and
194 49.90 mM (2000 ppm) Ca-ion activity standard solution before each experiment, according to
195 manufacturer instructions. All measurements were performed at room temperature (23°C).

196

197 **2.7 UHT processing of reconstituted milk protein dispersions**

198 The samples were UHT processed using a bench top UHT plant as shown in Fig 1. The product
199 temperature at inlet and outlet of sterilization section was measured by T-type thermocouples,
200 which were connected to a data logger and the temperature data was recorded in a Microsoft
201 Windows based data acquisition system, VISIDAQ (PCLD-8115, Advantech Co., Ltd., Taiwan). A
202 complete description of bench top UHT plant can be found in Prakash (2007). The product was
203 preheated to 95°C and held at this temperature for 8 s in the holding tube before heating to 145°C in
204 sterilization section and held at this temperature for 5 s. The volumetric flow rate of the product in
205 the beginning of the trial was 150 mL/min (2.5×10^{-6} m³/s).

206
207 Indicators used to end the UHT run due to deposit formation were as described by Prakash (2007).
208 The UHT run was stopped if the back pressure could not be maintained at 0.4 MPa and high back
209 pressure triggered the over pressure valve. The experiment was also stopped in case the outlet
210 temperature of sterilization section dropped below 120 °C. The other unlikely scenario to stop UHT
211 run was blockage of product channel due to severe fouling. Unless otherwise stated, if none of the
212 above factors stopped UHT processing, the experiment was terminated after 120 min has elapsed
213 into the UHT run. All experiments were performed in duplicate and their average value is reported.

214 **2.8 Fouling measurements**

215 Changes in overall heat transfer coefficient (OHTC) were used to monitor fouling. The plot of
216 OHTC versus run time of UHT plant from the start to the end run was used to monitor development
217 of fouling during the UHT run. Equation 3.1 was used to calculate OHTC.

$$\text{OHTC} = \frac{GC_p\Delta\theta}{A\Delta T_{lm}} \quad \text{eq (1)}$$

218 Where, G is the mass flow rate of the product in kg/s; C_p is the specific heat of product in J/kg⁰C;
219 $\Delta\theta$ is the temperature difference between the inlet and outlet of the UHT section, in °C; A is the

220 heat exchanging surface area of the tubing in m^2 ; ΔT_{lm} is the log mean temperature difference
221 (LMTD) in $^{\circ}C$ calculated using the equation 3.2.

$$\Delta T_{lm} = \frac{(T_o - T_{mo}) - (T_o - T_{mi})}{\ln[(T_o - T_{mo}) / (T_o - T_{mi})]} \quad \text{eq (2)}$$

222

223 Where T_o is the temperature of oil bath in $^{\circ}C$; T_{mi} and T_{mo} are temperatures of milk at the inlet and
224 outlet of the sterilisation section in $^{\circ}C$.

225

226 Specific heat and density of reconstituted milk powders were calculated using the specific heat and
227 density of protein, carbohydrate, fat, ash and water and mass fraction of these major components in
228 the dispersion (Singh, 2006, Choi, 1986).

229

230 **2.9 Heat coagulation time measurements**

231 Heat coagulation time (HCT) of samples was measured at the temperature similar to UHT
232 sterilization ($145^{\circ}C$) using the method described by Davies and White (1966). Glass vials (22.6 x
233 75.5 mm) containing 2 mL of sample were placed on a rocker and immersed in a temperature
234 controlled oil bath for heating. The rocker speed was kept at ~8 revolutions per min. HCT was
235 reported as time elapsed between putting the samples in the oil bath and appearance of first visible
236 signs of coagulation.

237

238 **2.10 Particle size distribution**

239 Particle size distribution (PSD) of unheated and UHT processed protein dispersions were measured
240 by dynamic light scattering (DLS) using a Malvern Mastersizer 2000MU-A (Malvern Instruments
241 Ltd, Malvern, United Kingdom) as described by Dumpler and Kulozik (2016). The refractive index
242 of protein was set at 1.41 and for dispersant (distilled water) was 1.33. Particle absorption index

243 was kept as 0.001. Stirrer speed was set at 2000 rpm and laser obscuration was maintained between
244 10 and 11 during measurement. All measurements were performed at room temperature (23 °C).

245

246 **2.11 Viscosity measurements**

247 The apparent viscosity of unheated and UHT processed protein dispersions was measured using an
248 AR-G2 Rheometer (TA Instruments Ltd., USA) equipped with 60 mm parallel plate geometry with
249 interplate gap set at 300 µm during measurements. The temperature of Peltier plate was set at 20°C
250 and viscosity measurements were performed after samples were allowed temperature equilibration
251 for 1 min. Apparent viscosity at a shear rate of 300 s⁻¹ was analyzed because it normally falls under
252 the typical range of shear rate encountered during pipe flow, mixing and stirring of liquid food
253 products (Steffe, 1996).

254

255 **2.12 Whey protein denaturation and heat induced dissociation of caseins**

256 Unheated and UHT processed samples were ultra-centrifuged (Avanti JXN-30, Beckman Coulter,
257 Australia Pty. Ltd., NWS, Australia) at 100,000g for 1 h at 20 °C. The supernatant was removed
258 carefully and analyzed for non-sedimentable protein (NSP) content using Kjeldahl method (AOAC,
259 2005). The supernatants were further analyzed to quantify individual non-sedimentable proteins of
260 interest using Reverse Phase-High Performance Liquid Chromatography (RP-HPLC) (RP-HPLC-
261 UV, Agilent 1100, Agilent Technologies Australia, Victoria, Australia) using method adopted from
262 Wijayanti et al. (2013).

263 **2.13 Statistical analysis**

264 The data was analyzed using Microsoft Excel and Minitab 16 software package. Significant
265 differences between average values of replicate measurements on each data point was analyzed by
266 analysis of variance (ANOVA) using Tukey's HSD post hoc test at 95% confidence level.

267

268 **3 Results and discussion**

269 **3.1 Compositional and quality analysis of milk powders**

270 MPC contained on average $81.95 \pm 1.77\%$ (w/w) total protein and $6.26 \pm 0.13\%$ (w/w) lactose. The
271 total protein and lactose contents of SMP on average were $32.64 \pm 0.53\%$ and $55.37 \pm 0.53\%$,
272 respectively. Amount of undenatured whey proteins in MPC ($18.85 \pm 0.55\%$ w/w) and SMP (22.52
273 $\pm 0.21\%$ w/w) were similar. This was also confirmed with SDS-PAGE analysis. Which showed that
274 β -lactoglobulin (β -lg) and α -lactoalbumin (α -la) were present in their native form in the milk
275 powders as shown in Fig 2. Total calcium content of MPC ($2.19 \pm 0.05\%$ w/w) was significantly
276 higher than that of SMP ($1.46 \pm 0.05\%$ w/w), presumably due to the higher protein (casein) content
277 of MPC binding higher amount of colloidal calcium. Solubility of MPC was found to be $85.19 \pm$
278 1.61% , which reached 100% at 50°C . This ensured that the temperature used for reconstitution
279 during this study was sufficient for complete rehydration of samples.

281 **3.2 UHT processing of milk protein dispersions**

282 Firstly, a UHT processing trial was conducted with 3.25-RSMP to establish baseline performance of
283 the bench-top UHT plant. The run-time for this sample was very long and UHT run was terminated
284 after 300 min elapsed and ~ 50 kg sample was exhausted. The samples did not show any excessive
285 pressure development and UHT temperature was maintained at $145 \pm 2^{\circ}\text{C}$. After that UHT stability
286 of concentrated milk protein dispersions (RMPC and RSMP at different protein concentrations) was
287 analysed. 10-RMPC and 14-RMPC were also very stable during UHT processing and average run-
288 times of bench-top UHT plant exceeded 300 min for 10-RMPC and averaged 280 min for 14-
289 RMPC. These samples were processed without any major temperature drops or pressure
290 fluctuations. The RMPC sample with 16% PC was not UHT processed due to high viscosity and gel
291 like consistency before processing. For further experiments, to be able to process multiple samples
292 in a day, the UHT run was terminated after 120 min has elapsed, if fouling did not interrupt

293 processing. Fig 3 and 4 shows average run times and changes in OHTC during UHT run,
294 respectively, for all the milk protein dispersions used in this study.

295

296 For RSMP samples containing 6.5, 7 and 7.5% proteins, the UHT run lasted for 88, 72 and 23 min,
297 respectively before fouling was observed. Excessive back pressure developed after this time, which
298 triggered the over pressure valve and the milk was pumped back into the balance tank of the UHT
299 plant. Sample containing 8% proteins could not be processed through the UHT plant, because
300 excessive back pressure developed as soon as 8-RSMP passed through the UHT section of plant.
301 This suggested that 8-RSMP was highly unstable under UHT conditions and fouled immediately.
302 These results showed that total protein content in RSMP influenced its ability to be UHT processed.
303 The UHT run decreased with increasing protein content. Although other studies do not report the
304 effect of increased total protein directly, similar results were obtained by Kastanas (1996), Prakash
305 (2007), when the total solids of milk were increased.

306

307 The RSMP containing 3.25% protein showed high OHTC values as compared to 6.5, 7 and 7.5-
308 RSMP during UHT processing (Fig 4A). This can be attributed to low TS and high amount of water
309 in the sample, which in turn leads to high values of specific heat (C_p) (Singh, 2006, Toledo, 2007,
310 Choi, 1986). OHTC values are directly proportional to C_p as shown in eq. 3.1. On average, values of
311 OHTC during processing of 6.5-RSMP, 7-RSMP and 7.5-RSMP were lower than 3.25-RSMP. This
312 also suggests that increased total solids and increased viscosity play a role in decreasing turbulence
313 and heat transfer during UHT processing.

314

315 The OHTC vs run-time graph (Fig. 4A) shows that the OHTC remained almost constant for 3.25-
316 RSMP throughout the run, whereas, for concentrated RSMP samples there was a gradual decrease
317 in OHTC with increasing run-time after an induction period. The observations for 3.25-RSMP were
318 consistent with results previously reported by Prakash (2007). This OHTC vs run-time behavior of

319 concentrated RSMPs was due to gradual fouling of heat transfer surfaces with milk solids, which
320 offered more resistance to heat transfer as compared to clean surfaces, causing lower UHT
321 temperatures. A fouling induction period of 25, 14 and 8 min was observed for 6.5-RSMP, 7-RSMP
322 and 7.5-RSMP, respectively suggesting that fouling started faster in samples containing higher
323 protein and higher total solids

324

325 In concentrated RSMPs milk proteins are relatively densely packed as compared to 3.25-RSMP.
326 Increased protein content in concentrated RSMPs increases the chances of interactions between
327 protein molecules leading to increase in amount of higher molecular mass β -lg aggregates (Bon et
328 al., 1999). This can result in increased amount of voluminous Type A deposits (Tissier, 1984).
329 These deposits will cause temperature drops and excessive fluctuations in back pressure to a point
330 where back pressure could not be maintained at 0.4 kPa and UHT run had to be terminated. As 8-
331 RSMP was extremely unstable to UHT processing, effect of protein content higher than 8% could
332 not be studied using RSMP.

333

334 Further, RMPCs were processed to observe the effect of increased protein content on UHT behavior
335 of high protein milk dispersions. RMPC samples showed high UHT stability as compared to
336 concentrated RSMPs at much higher protein levels. RMPC with 8% protein was very stable during
337 UHT processing (data not shown), therefore the amount of protein in samples was increased further.
338 10-RMPC and 14-RMPC samples showed no signs of fouling throughout the run-time of 120 min
339 and there was an insignificant drop in OHTC (Fig 4B). The ethanol stability of 14-RMPC (86%)
340 was significantly higher than that of 7.5-RSMP (54%) (Table 2). Heat stability behavior of milk
341 protein dispersions when measured by HCT was also in agreement with their UHT stability. HCT
342 for sample 7.5-RSMP (1.77 min) was low as compared to 14-RMPC (2.54 min) (Table 2). The
343 UHT behavior of 14-RMPC-G prepared from MPC85 obtained from a different supplier showed
344 similar UHT stability results. This was done to eliminate the possibilities of any differences

345 between UHT stability of reconstituted samples prepared from MPC85 manufactured by different
346 manufacturers.

347

348 A distinguishing difference between RMPC and RSMP samples may be that RMPC samples had
349 much lower TS (Table 1) than RSMP samples, which can lead to better heat stability under UHT
350 conditions. High viscosities of concentrated samples can shift the fluid flow behavior from turbulent
351 to laminar; which can cause low flow rates for layers of process fluid adjacent to the heat transfer
352 surface, resulting in larger volume of material in contact with heating surface for longer period of
353 time. This can lead to formation of larger volume of fouling deposits (Burton, 1994). However, 14-
354 RMPC showed high UHT stability even though its viscosity was significantly ($P<0.05$) higher than
355 7.5-RSMP (Table 2). Therefore in order to look into the effect of total solids on UHT heat stability
356 of milk protein dispersions, lactose was added to 7.5-RMPC (7.5-RMPC-LAC) to match TS of 7.5-
357 RSMP.

358

359 7.5-RMPC-LAC showed a UHT run time of greater than 120 min (Fig 3). Also, the OHTC over the
360 run time of 7.5-RMPC-LAC was similar to 14-RMPC and much higher than 7.5-SMP (Fig 4C).
361 Ethanol stability and HCT of 7.5-RMPC-LAC were significantly ($P<0.05$) higher than that of 7.5-
362 SMP (Table 2) and were similar to that of 14-RMPC. Hence, it could be concluded that 7.5-RMPC-
363 LAC had much higher UHT stability than 7.5-SMP at same TS content and could be processed
364 without fouling.

365

366 The results suggested that milk constituents other than proteins, such as milk minerals (in particular
367 calcium), may be responsible for the differences in UHT stability and susceptibility to fouling of
368 RMPCs and RSMPs. High calcium ion activity has been associated with decreased UHT stability of
369 milk products (Singh, 2004). However, 14-RMPC had significantly ($P<0.05$) higher ionic calcium
370 activity as compared to 7.5-RSMP (Table 2), which does not correlate with UHT stability of these

371 two high protein samples. Hence, calcium ion activity alone could not be the dominating factor
372 explaining the differences between the UHT stability of these samples. Similar results on ionic
373 calcium and heat stability behavior of milk protein concentrate suspensions (MPC80) was reported
374 by Crowley et al. (2015) .

375

376 To investigate the synergetic effect of milk proteins, lactose and milk minerals on UHT stability of
377 RMPC, an MPC dispersion (7.5-RMPC-LAC-SMUF) containing same amount of proteins, lactose
378 and mineral salts as 7.5-RSMP was prepared. The amount of SMUF used in 7.5-RMPC-LAC-
379 SMUF was calculated on the basis of matching total calcium of this sample to 7.5-RSMP, which
380 also closely matched the amount of lactose and other milk minerals such as magnesium,
381 phosphorous etc. in these two samples (Table 2). The calcium ion activity of 7.5-RMPC-LAC-
382 SMUF was found to be 1.30 mM, which was very close to that of 7.5-RSMP (1.36 mM). During
383 UHT processing, 7.5-RMPC-LAC-SMUF showed 66 min run-time on average (Fig 3). The sample
384 showed an induction time of 21 min, after which frequent temperature and back pressure
385 fluctuations were observed (Fig 4C) and the UHT run had to be terminated after 66 min due to
386 fouling. The induction period of 21 min showed by 7.5-RMPC-LAC-SMUF was very close to total
387 run-time of 23 min observed for 7.5-RSMP.

388

389 Ethanol stability and HCT of RMPC reduced markedly after addition of milk minerals; 7.5-RMPC-
390 LAC-SMUF showed ethanol stability (59%) and HCT (1.51 min) similar to 7.5-SMP (Table 2). The
391 study conducted by Crowley et al. (2015) on heat stability behavior of RMPCs containing 8.5%
392 protein also showed that HCT of reconstituted MPC35 (composition closely matching to an SMP)
393 at pH 6.8 was lower than that of reconstituted MPC80; however, UHT stability was not studied.
394 Ethanol stability test is used to determine casein micelle stability. Ethanol collapses the κ -casein
395 hairy layer on the casein micelle surface and its function of steric stabilization is lost, leading to

396 casein micelles coagulation (Horne, 1984). The ethanol stability results were similar to UHT
397 stability of milk protein dispersions studied.

398

399 PSD data (performed on whole sample) of UHT processed samples demonstrated formation of
400 larger size particles in 7.5-RSMP as compared to 14-RMPC (Fig 5). Almost all the particles in UHT
401 processed 14-RMPC were of sub-micron size ($0.23 \mu\text{m D}(0.9)$) as compared to 7.5-RSMP ($1.84 \mu\text{m}$
402 $\text{D}(0.9)$) as shown in Table 3. These differences in particle size were significant and were possibly
403 due to the differences the mineral environment of the samples. The large particles could be formed
404 from whey protein interactions amongst themselves and or with caseins to form whey protein-casein
405 aggregates. The differences in the mineral environment can affect the size of whey protein
406 aggregates formed during UHT treatment and can lead to formation of larger aggregates in case of
407 RSMP and RMPC-LAC-SMUF (Havea et al., 2002, Crowley et al., 2015).

408

409 We further investigated the effect of mineral environment on protein dissociation in samples before
410 and after UHT processing. RP-HPLC analysis was performed on supernatants of unheated and UHT
411 processed 7.5-RSMP, 14-RMPC and 7.5-RMPC-LAC-SMUF samples (Fig 6). The RP-HPLC data
412 showed that in all three samples, β -lg was completely aggregated after UHT processing (Fig 6A)
413 and was absent from the non-sedimentable fraction. Additionally more than 75% of α -la was
414 aggregated in all three samples (Fig 6B). Crowley et al. (2015) also showed that the difference in
415 amount of non-sedimentable whey proteins in heated reconstituted MPC80 and MPC35 was not
416 significant. But it is possible that the types of aggregates formed from these non-sedimentable whey
417 proteins upon heating are responsible for differences in UHT stability of RMPC and RSMP samples
418 as described above.

419

420 Significant differences were observed in the non-sedimentable caseins between 14-RMPC, 7.5-
421 RSMP-UHT and 7.5-RMPC-LAC-SUMF before and after UHT treatment. This is interesting

422 because the stability of casein micelles during UHT processing could be another factor governing
423 UHT stability of RMPC samples. It was observed from RP-HPLC data that unheated samples of 14-
424 RMPC had significantly ($P<0.05$) higher amounts of dissociated caseins as compared to 7.5-RSMP
425 and 7.5-RMPC-LAC-SMUF (Fig 6C-E).

426

427 Non-sedimentable protein content in all three samples was similar after UHT processing, however,
428 when comparing unheated samples to UHT treated samples, it slightly increased in 7.5-RSMP and
429 significantly ($P<0.05$) increased 7.5-RMPC-LAC-SMUF after UHT processing whereas it
430 significantly ($P<0.05$) decreased in 14-RMPC (Fig 6F). This may suggest that casein micelles in
431 7.5-RSMP and 7.5-RMPC-LAC-SUMF were more unstable to UHT treatment than in 14-RMPC. It
432 could be possible that in 14-RMPC the initially dissociated caseins might have deposited on heated
433 surfaces initially (Santos et al., 2003), but there was not much further dissociation of caseins during
434 UHT processing to participate in formation of large aggregates. In 7.5-RSMP higher dissociation of
435 casein micelles during UHT treatment might have happened, bringing its post UHT non-
436 sedimentable protein content almost similar to heated 14-RMPC. These UHT induced dissociated
437 caseins might have led to formation of large aggregates due to whey-casein aggregation via κ -
438 casein- β -Ig interactions or aggregation of unstable casein micelles (Anema and Li, 2003, Ono et al.,
439 1999). Smaller protein aggregates formation observed in UHT processing of MPC could be related
440 to its altered mineral environment during manufacturing (Crowley et al., 2015).

441

442 The ethanol stability data (Table 2) also showed that 14-RMPC had higher ethanol stability than
443 7.5-RSMP, implying higher casein micelle stability in 14-RMPC. As RP-HPLC results (Fig 6E)
444 showed that κ -casein content in all three UHT processed samples was similar it can be concluded
445 that either electrostatic interactions between caseins or extent of collapse of κ -casein hairy layer and
446 loss of steric stabilization during UHT processing of these protein dispersions were influenced by
447 soluble salts in the serum phase (Horne, 2016). As stated above, mineral environment of RSMP
448 appeared to be favorable to start rapid interactions of casein micelles as observed by Horne (1984),

449 Horne and Parker (1981) and indicated by low ethanol stability shown by RMPC with added
450 SMUF (7.5-RMPC-LAC-SMUF).

451

452 It was observed that milk proteins behaved differently in different mineral environments. Milk
453 protein dispersions prepared from RMPC formed submicron particles after UHT treatment as shown
454 by PSD and dissociation of caseins was limited in RMPC mineral environment as compared to
455 RSMP as shown by RP-HPLC and ethanol stability data. The similarity in UHT behavior of 7.5-
456 RSMP and 7.5-RMPC-LAC-SMUF and drop in UHT stability of RMPC after addition of minerals
457 was an indicator that total milk mineral environment plays a crucial role in UHT stability of high
458 protein dispersions. Effect of UHT temperatures on milk protein stability, changes in protein state
459 and their interactions with milk minerals during heating of milk protein dispersions prepared from
460 these two different milk protein powders can be an important factor in determining their fouling
461 behavior. This suggest that difference in mineral composition of MPC powder from SMP due to
462 ultrafiltration process can be an important factor causing its high heat stability. During SMP
463 manufacturing all the milk minerals are retained in the final product, however during membrane
464 filtration process employed during manufacturing of MPC, free ions pass through the membrane
465 and protein is retained, which increases the volume fraction of caseins and changes ratio between
466 soluble and colloidal minerals (Dalglish and Corredig, 2012). This also alters the casein inter-
467 micelle interactions. Mineral composition of aqueous phase has also been found to have a
468 significant role on physicochemical properties and heat stability of reconstituted casein micelles (Le
469 Ray et al., 1998). The higher instability of 7.5-RMPC-LAC-SMUF compared to 7.5-SMP is being
470 further investigated.

471

472 **4 Conclusion**

473 MPC is an important ingredient of milk protein based beverages, however, there is little known
474 about their UHT stability. MPC reconstituted to 14% protein showed significantly higher UHT

475 stability as compared to SMP reconstituted at 7.5% protein, although the ionic calcium activity and
476 viscosity of the former was higher than the later. The lower UHT stability of RSMP can be related
477 to larger protein aggregate formation and destabilization of casein micelles in 7.5-RSMP at UHT
478 temperatures. High UHT stability of milk protein dispersions made from high protein milk powder,
479 such as MPC85, can be due to the ultrafiltration processing used during their manufacturing, which
480 causes them to have a modified mineral composition as compared to SMP. The UHT instability of
481 mineral readjusted MPC85 even at 7.5% protein concentration suggested that the total mineral
482 composition is responsible for fouling of high protein SMP suspension. Further investigation is
483 underway to explore the effect of changes in mineral composition on UHT behavior of MPC
484 powders at different protein concentrations.

485

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489

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491

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Figure Captions

Figure 1: Flow diagram of bench top UHT plant

Figure 2: SDS-PAGE analysis of milk powders, Lane: 1. Molecular weight standards, 2. Low Heat SMP (Non-Reduced SDS-PAGE), 3. MPC (Non-Reduced SDS-PAGE), 4. Low Heat SMP (Reduced SDS-PAGE) and 5. MPC (Reduced SDS-PAGE)

Figure 3: The average UHT run times on a bench top UHT tubular heat exchanger during processing of milk protein dispersions. Error bars represent standard deviation, n=2. Means with different letters are significantly different (P<0.05). Samples with † did not foul in 120 min.

Figure 4: Variation in OHTC with run time for milk protein dispersions, (A) milk protein dispersions prepared using RSMP, (B) milk protein dispersions prepared using RMPC, (C) comparison of 7.5-RSMP with 7.5-RMPC with added lactose and SMUF. Representative data of duplicate runs is presented here.

Figure 5: Particle size distribution of UHT processed milk protein dispersions. Representative data of four measurements.

Figure 6: Effect of UHT processing of milk protein dispersions on non-sedimentable milk proteins (data shown as percentage of non-sedimentable protein of total individual milk protein present in the sample) . (A) β -lg , (B) α -1a, (C) α s1-casein, (D) β -casein (E) κ -casein and (F) Total non-sedimentable protein. Error bars represent standard deviation, n=2. UN= unheated sample, UHT= UHT treated sample.

Table 1: Description of reconstituted milk protein dispersions used

Sample	Ingredients	Protein content (%w/w)	Total solids (% w/w)
3.25-RSMP	SMP	3.25	10.00
6.5-RSMP	SMP	6.50	20.00
7-RSMP	SMP	7.00	21.53
7.5-RSMP	SMP	7.50	23.07
8-RSMP	SMP	8.00	24.61
10-RMPC	MPC	10.00	12.27
14-RMPC	MPC	14.00	17.17
16-RMPC	MPC	16.00	19.63
14-RMPC-G	MPC-G	14.00	17.17
7.5-RMPC-LAC	MPC and Lactose	7.5	23.07
7.5-RMPC-LAC-SMUF	MPC, lactose and mineral salts	7.5	23.07

Table 2: Calcium ion activity, ethanol stability, viscosity, HCT, lactose and major milk minerals of selected samples

Sample	Calcium	Ethanol	Viscosity* (mPa.s)		HCT*	Lactose	Ca [#]	P [#]	Mg [#]	Cl [#]	K [#]
	ion activity* (mM)	Stability* (%)	UN	UHT	(min)	(% w/w)	(% w/w)	(% w/w)	(% w/w)	(% w/w)	(% w/w)
7.5-RSMP	1.36±0.01 ^b	54.00±0.00 ^d	6.79±0.64 ^c	12.97±1.66 ^b	1.77±0.16 ^c	12.69	0.34	0.24	0.03	0.14	0.30
14-RMPC	1.98±0.02 ^a	86.00±0.00 ^b	32.43±0.89 ^a	34.74±4.36 ^a	2.54±0.11 ^b	0.86	0.38	0.25	0.02	0.03	0.06
7.5-RMPC-LAC	2.00±0.13 ^a	88.00±0.00 ^a	8.85±0.49 ^c	5.50±0.03 ^c	2.82±0.16 ^a	14.73	0.20	0.14	0.01	0.01	0.03
7.5-RMPC- LAC-SMUF	1.30±0.02 ^b	59.00±0.89 ^c	19.20±2.82 ^b	7.53±0.46 ^{bc}	1.51±0.10 ^d	12.56	0.36	0.28	0.04	0.35	0.58

* All results are expressed as the mean ± standard deviation (n = 4). Means in a single column with different superscripts are significantly different (P<0.05)

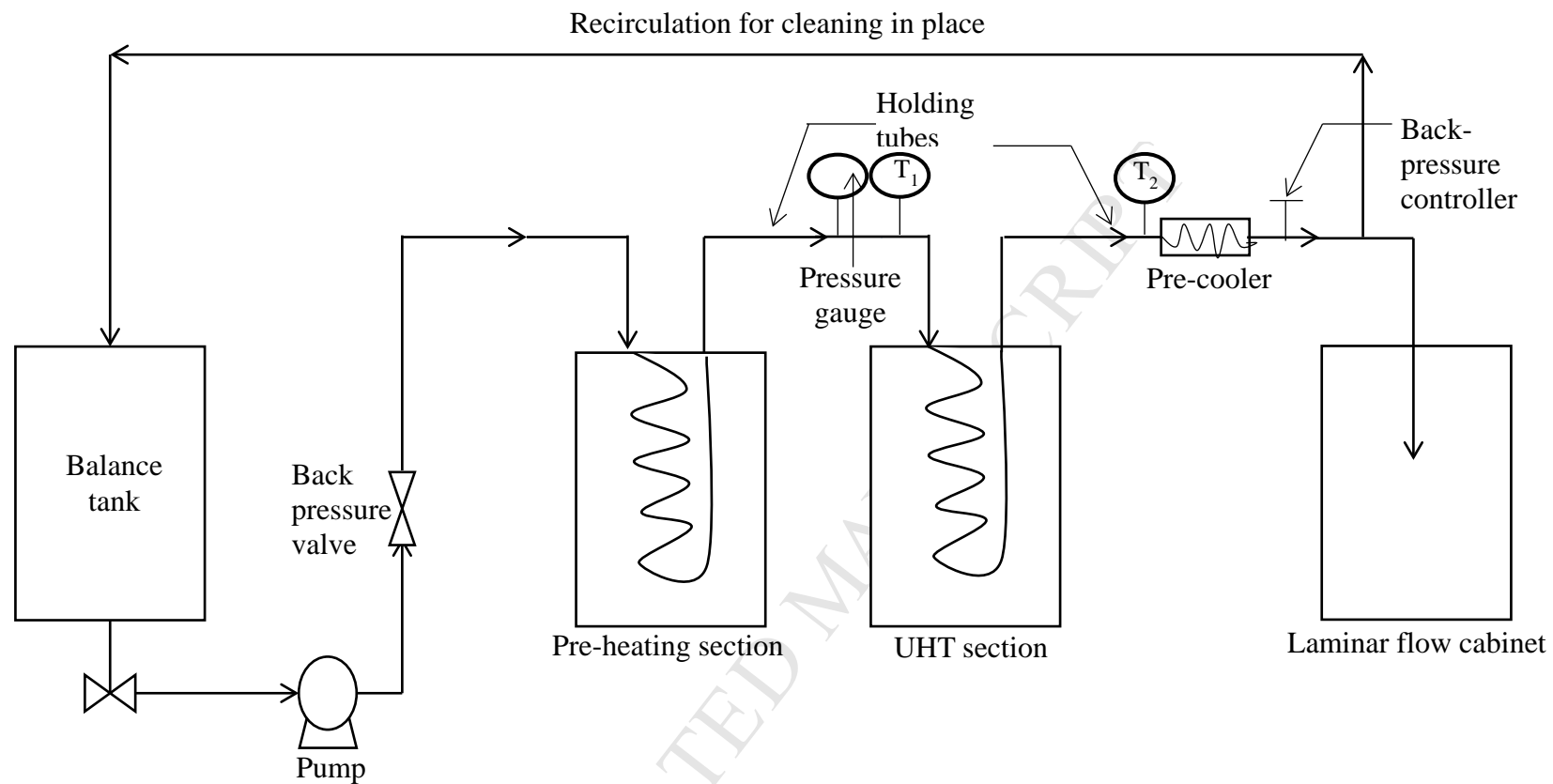
[#]Values derived from mineral composition of milk powders used to prepare the samples. (except for sample 7.5-RMPC-LAC-SMUF values measured using ICP-OES)

UN= unheated sample, UHT= UHT treated sample

Table 3: Comparison of volume weighted mean diameter, Surface weighted mean diameter and particle size distribution for 7.5RSMP and 14-RSMPC

Sample	D[4,3] (μm)	D[3,2] (μm)	D(0.1) (μm)	D(0.5) (μm)	D(0.9) (μm)
7.5-RSMP	1.12 \pm 0.50	0.16 \pm 0.01	0.08 \pm 0.00	0.19 \pm 0.01	1.84 \pm 1.38
14-RMPC	0.50 \pm 0.17	0.12 \pm 0.00	0.08 \pm 0.00	0.13 \pm 0.00	0.23 \pm 0.00
7.5-RMPC- LAC-SMUF	22.43 \pm 2.99	1.40 \pm 0.30	0.62 \pm 0.10	1.39 \pm 0.29	74.71 \pm 4.49

All results are expressed as the mean \pm standard deviation (n = 4). Means in a single column with different superscripts are significantly different (P<0.05).



T_1 - Thermocouple at the inlet of UHT section

T_2 - Thermocouple at the outlet of UHT section

Figure 1: Flow diagram of bench top UHT plant

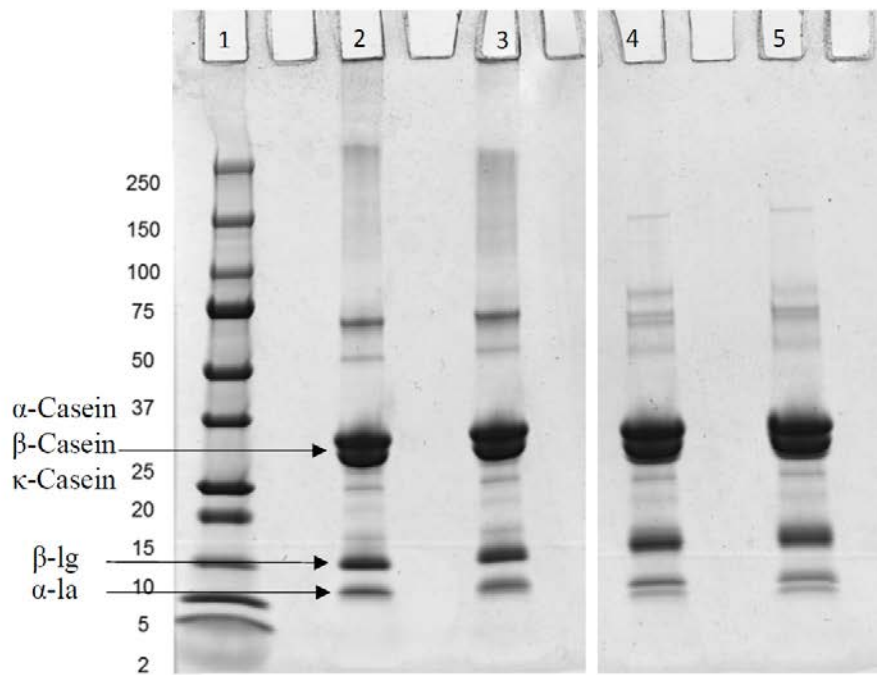


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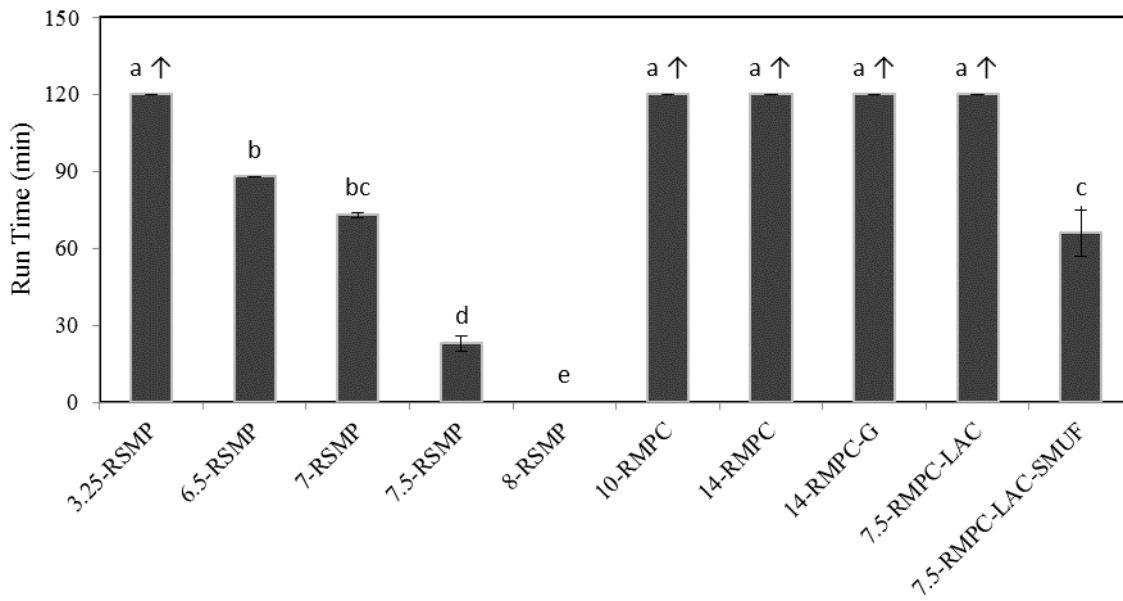


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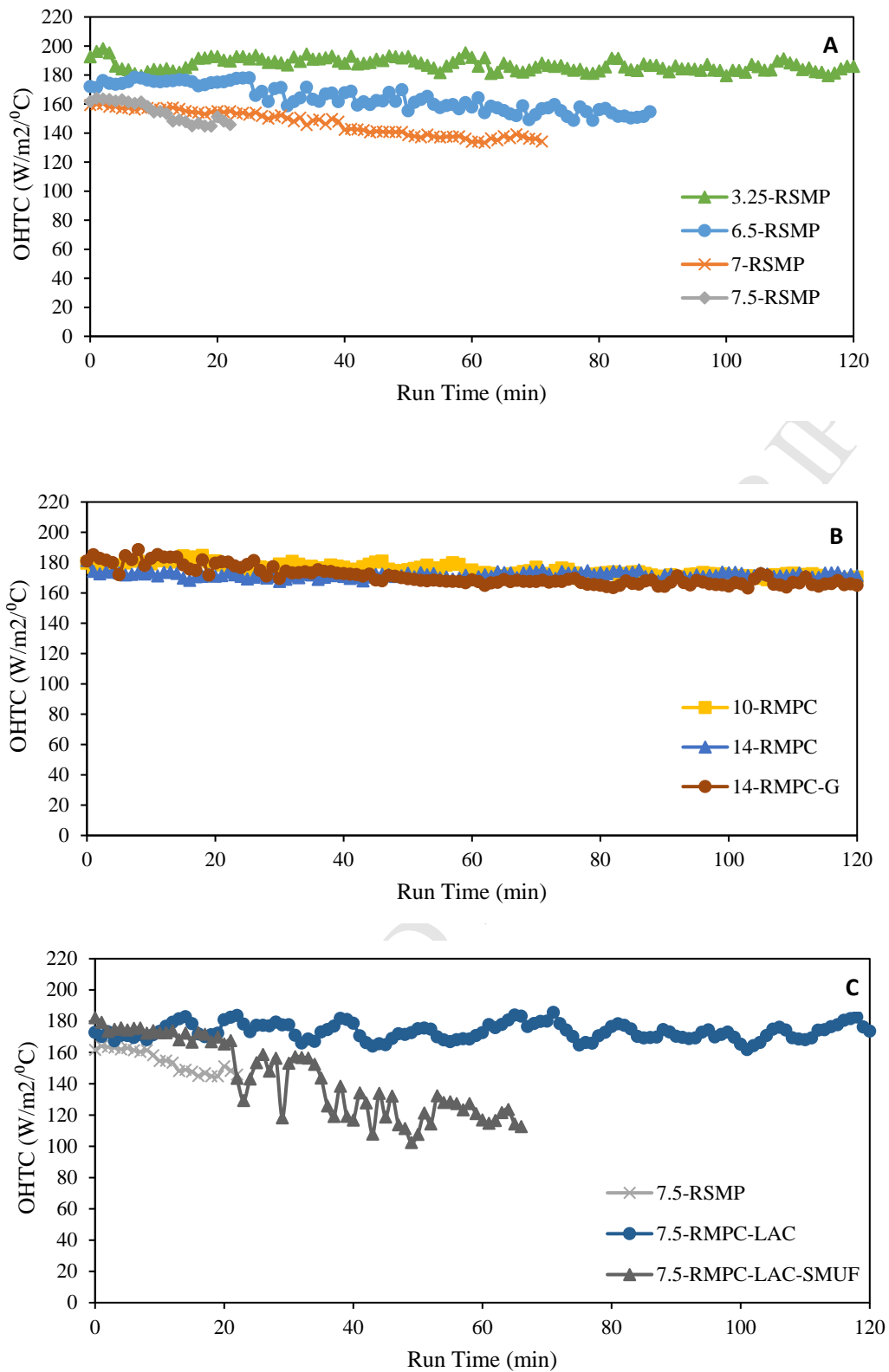


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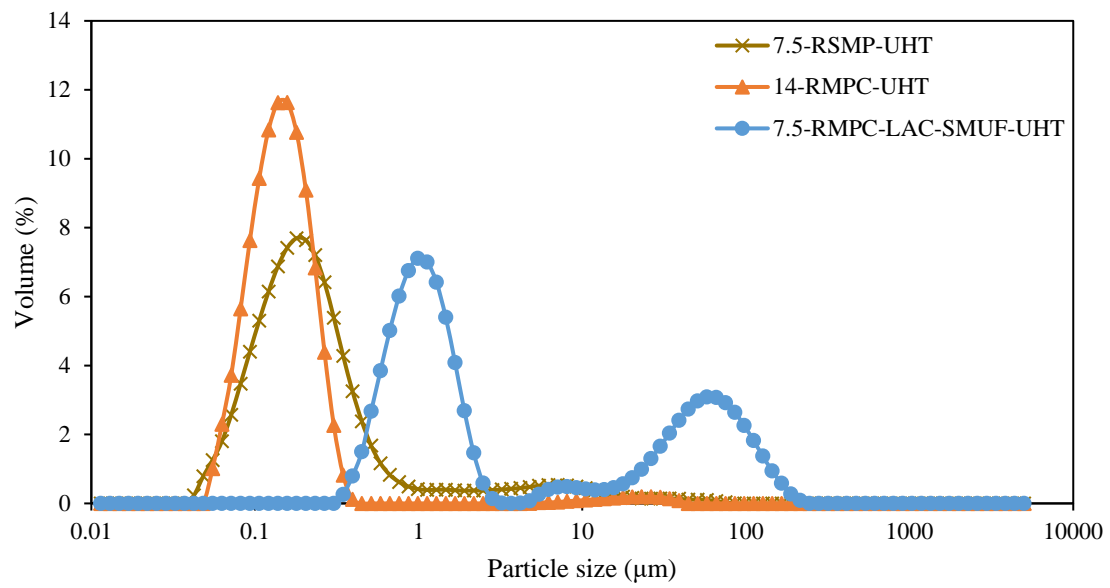


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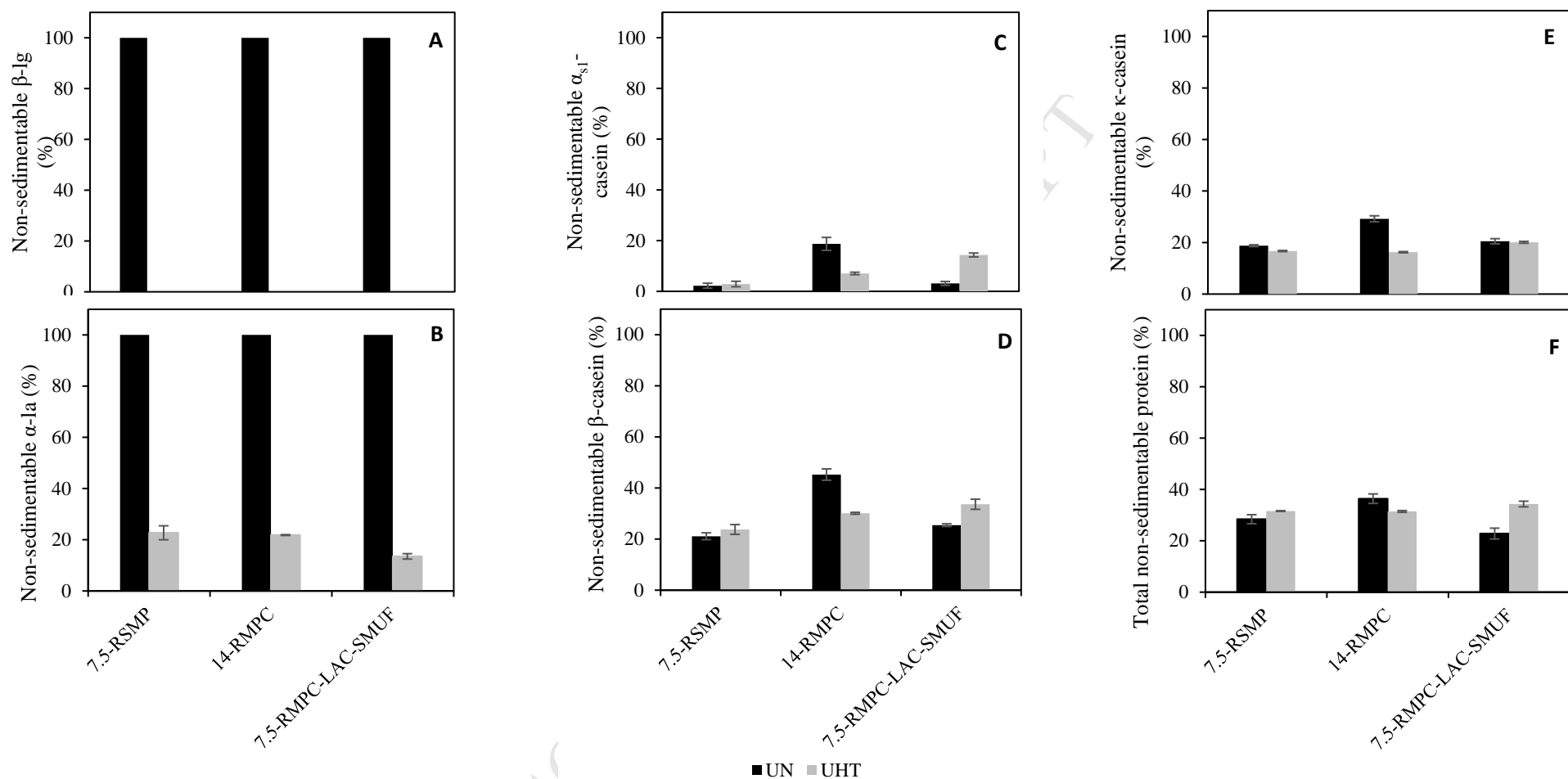


Figure 6: Effect of UHT processing of milk protein dispersions on non-sedimentable milk proteins (data shown as percentage of non-sedimentable protein of individual and total milk protein present in the sample) . (A) β -Ig , (B) α -la, (C) α s1-casein, (D) β -casein (E) κ -casein and (F) Total non-sedimentable protein. Error bars represent standard deviation, n=2. UN= unheated sample, UHT= UHT treated sample.

Highlights:

- MPC has higher UHT stability than SMP even at higher protein content.
- Higher viscosity and higher ionic Ca did not cause fouling in MPC.
- Total mineral balance affected the UHT behaviour of high protein milk dispersions.
- Larger protein aggregates caused lower UHT stability of SMP.