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Effect of Schmidt number on mass transfer across a sheared gas-liquid interface in a wind-driven turbulence

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The mass transfer across a sheared gas-liquid interface strongly depends on the Schmidt number. Here we investigate the relationship between mass transfer coefficient on the liquid side, k_L , and Schmidt number, Sc , in the wide range of $0.7 \leq Sc \leq 1000$. We apply a three-dimensional semi direct numerical simulation (SEMI-DNS), in which the mass transfer is solved based on an approximated deconvolution model (ADM) scheme, to wind-driven turbulence with mass transfer across a sheared wind-driven wavy gas-liquid interface. In order to capture the deforming gas-liquid interface, an arbitrary Lagrangian-Eulerian (ALE) method is employed. Our results show that similar to the case for flat gas-liquid interfaces, k_L for the wind-driven wavy gas-liquid interface is generally proportional to $Sc^{-0.5}$, and can be roughly estimated by the surface divergence model. This trend is endorsed by the fact that the mass transfer across the gas-liquid interface is controlled mainly by streamwise vortices on the liquid side even for the wind-driven turbulence under the conditions of low wind velocities without wave breaking.

Mass transfer phenomena across gas-liquid interfaces are often seen in geophysical and industrial processes, and such mass transfer is believed to be enhanced by wind-driven turbulence (i.e., surface-renewal motions) near the interface on the liquid side (e.g., Jähne *et al.*¹⁻³, Komori *et al.*^{4,5}, Takagaki *et al.*⁶, Kurose *et al.*⁷). In order to clarify the mass transfer mechanism and precisely evaluate the amount of the mass transferred across the wind-driven wavy gas-liquid interface, direct numerical simulations (DNSs) of gas-liquid two-phase turbulent flows with wind-driven wavy interfaces were carried out by some researchers (Komori *et al.*⁵, Takagaki *et al.*⁶, Kunugi *et al.*⁸, Lakehal *et al.*⁹⁻¹¹, Banerjee¹², Banerjee *et al.*¹³). One of the most important properties to globally predict the amount of mass transferred across such gas-liquid interfaces is the mass transfer coefficient, k_L , and therefore a precise model for it is necessary. Here, k_L is defined as:

$$k_L = \frac{F}{\Delta C}, \quad (1)$$

where F is the mass flux at the gas-liquid interface per unit area, ΔC the mass concentration difference between the interface and the bulk liquid. The value of k_L is often correlated with the Schmidt number, $Sc (= \nu_L/D_L)$, on the liquid side, where ν_L and D_L are the kinematic viscosity and molecular diffusivity on the liquid side, respectively. However, the evaluations of k_L are limited for $Sc \leq 1600$ in previous experiments (e.g., Jähne *et al.*¹⁻³, Komori *et al.*⁴, Liss¹⁴, Broecker *et al.*¹⁵, Wanninkhof¹⁶, Iwano *et al.*^{17,18}) and limited for $Sc \leq 100$ in previous numerical simulations (e.g., Komori *et al.*⁵, Takagaki *et al.*⁶, Banerjee *et al.*¹³). Also, since the flow and mass conditions are different among these previous experimental and numerical studies, the universal relation between k_L and Sc has not been clarified yet, even in these Sc ranges.

In this paper, we aim to present the relationship between k_L and Sc in the wide range of $0.7 \leq Sc \leq 1000$ by applying a SEMI-DNS, in which the mass transfer is solved based on an approximated deconvolution model (ADM) scheme proposed by Stolz and Adams¹⁹, to a gas-liquid two-phase turbulent flow with a wind-driven wavy interface.

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Methods

The numerical procedure of the DNS used here was the same as in the study by Komori *et al.*⁵ and Takagaki *et al.*⁶. In the procedure, the wind-driven wavy gas-liquid interface was captured by the arbitrary Lagrangian-Eulerian (ALE) method with boundary-fitted coordinates (BFC) on moving grids (Komori *et al.*^{5,20}, Takagaki *et al.*⁶, Lakehal *et al.*^{9–11}, Banerjee *et al.*¹³, Fulgosi *et al.*²¹, Lin *et al.*²², Guo and Shen²³, Tsai *et al.*²⁴). The non-dimensional governing equations for an incompressible Newtonian fluid flow with mass transfer are given by the equation of continuity, Navier-Stokes (N-S) equation, and transport equations of mass using the Einstein summation convention:

$$\frac{\partial U_i}{\partial x_i} = 0, \quad (2)$$

$$\frac{\partial U_i}{\partial t} + U_j \frac{\partial U_i}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{1}{Re} \frac{\partial^2 U_i}{\partial x_j \partial x_j} + \frac{1}{Fr} \delta_{i3}, \quad (3)$$

$$\frac{\partial c}{\partial t} + U_j \frac{\partial c}{\partial x_j} = \frac{1}{Re \cdot Sc} \frac{\partial^2 c}{\partial x_j \partial x_j}, \quad (4)$$

where U_i is the i th component of the velocity vector ($i = 1, 2$, and 3 denote the streamwise, spanwise and vertical directions, respectively), p the pressure, δ_{ij} the Kronecker's delta, and c the mass concentration. Here, equation (4) is solved only on the liquid side. The non-dimensional parameters, Reynolds number Re , Schmidt number Sc and Froude number Fr are defined as:

$$Re = \frac{U_0 L_0}{\nu}, \quad Sc = \frac{\nu}{D}, \quad Fr = \frac{U_0^2}{gL_0}, \quad (5)$$

where L_0 and U_0 are the reference length and velocity, respectively, ν the kinematic viscosity, D_L the molecular diffusivity of mass on the liquid side, and g the acceleration due to gravity. On the gas-liquid interface, two boundary conditions should be satisfied. One is the kinematic boundary condition that describes the Lagrangian behavior of the fluid particle on the mobile gas-liquid interface, and the other is the dynamic boundary condition, which is determined from the balance of stresses acting on the gas-liquid interface in the normal and tangential directions (Komori *et al.*⁵, Takagaki *et al.*⁶).

Since a high Sc mass causes a smaller Batchelor scale (Hasegawa and Kasagi^{25–27}, Kurose *et al.*^{28,29}), the mass transfer was solved based on ADM scheme proposed by Stolz and Adams¹⁹ and modified by Mathew *et al.*³⁰. The model based on DNS of flow field and ADM of mass field is proposed by Schwertfirm and Manhart³¹ and is called as SEMI-DNS. The ADM method is briefly explained here, and see more details in Schwertfirm and Manhart³¹. When a mass concentration field, f , is predicted with meshes coarser than the Batchelor scale, the mass concentration field is like a filtered mass concentration field, \bar{f} . Now, by the filtering function, G , the relation between f and \bar{f} are $\bar{f} = G^* f$, where $*$ is the filtering procedure. On the ADM method, without any LES model, the mass concentration field is predicted using the inverse filtering function, Q . Generally, under the assumption of the existence of the inverse matrix, G^{-1} , the Taylor expansion of G^{-1} is shown as:

$$G^{-1} = \sum_{\nu=0}^{\infty} (1 - G)^{\nu}. \quad (6)$$

By equation (6), Stolz and Adams¹⁹ defines Q as:

$$Q = \sum_{\nu=0}^n (1 - G)^{\nu}, \quad (7)$$

and, therefore, Q has the property of inverse matrix, that is, $Q^* G = G^* Q \sim I$ and $Q \sim G^{-1}$. Therefore, \bar{f} can be restored by Q shown as:

$$Q^* \bar{f} = Q^* G^* f \sim f, \quad (8)$$

where they defines \tilde{f} as $\tilde{f} \equiv Q^* \bar{f}$. In this study, the simple filtering shown as:

$$G^* f = \frac{1}{2} f_i + \frac{f_{i-1} + f_{i+1}}{4}, \quad (9)$$

is used. Using equation (8), equation (4) is rewritten (see the details in Schwertfirm and Manhart³¹) as:

$$\frac{\partial \tilde{c}}{\partial t} + \frac{\partial \tilde{u}_j \tilde{c}}{\partial x_j} = \frac{1}{Re \cdot Sc} \frac{\partial^2 \tilde{c}}{\partial x_j \partial x_j}. \quad (10)$$

The computational domain was $8\delta \times 3.92\delta \times 3\delta$ ($\delta = 1.25 \times 10^{-2}$ m) in the streamwise (x), spanwise (y) and vertical (z) directions. The origin ($x = y = z = 0$) was located at the height of 2δ from the bottom, and the initial

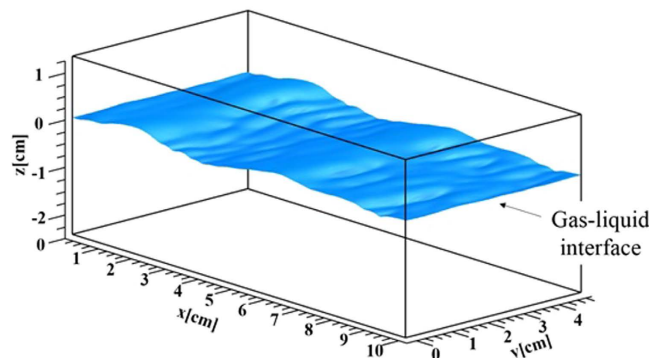


Figure 1. Instantaneous configuration of wind-driven wavy gas-liquid interface at $t = 5.0$ s.

flat gas-liquid interface which divides the two-phase flow between upper gas and lower liquid streams was placed on the plane of $z = 0$. The grid points used in the streamwise (x), spanwise (y) and vertical (z) directions were $200 \times 98 \times 60$ on the gas side and $200 \times 98 \times 120$ on the liquid side, respectively. The grid spacing was equidistant in the streamwise (x) and spanwise (y) directions, and to get high resolution the nonuniform meshes clustered in the gas-liquid-interface region were used in the vertical (z) direction. Periodic boundary conditions were applied in the streamwise (x) and spanwise (y) directions, and slip boundary conditions were applied at the top and bottom boundaries. As initial conditions of flow field, a fully developed wall turbulent flow and a quiescent flow were given on the gas and liquid sides of the initial flat interface, respectively. For the computation of the mass transfer on the liquid side, the boundary conditions of the passive mass at the gas-liquid interface and the bottom boundary were given by $C = 1.0$ and Neumann condition, respectively. The marker and cell (MAC) (Harlow and Welch³²) method was used to solve the Navier-Stokes equations. In order to induce the realistic deformation of the gas-liquid interface, a fully developed wall turbulence for an initial free stream wind speed of $U_{\infty,ini} = 4.8$ m/s and an initial friction velocity of $u_{*,ini} = 0.242$ m/s was given on the gas side over a flat quiescent liquid. The gas flow was driven by pressure gradient imposed in the streamwise direction. The Reynolds number based on $U_{\infty,ini}$ and δ , Re_{ini}^* , was 3960 and that based on $u_{*,ini}$ and δ , Re_{ini}^* , was 200. The density ratio of the gas and liquid was 830, which corresponds to the value for the air-water two phase flow at about 20 °C. The Schmidt number, Sc , on the liquid side ranged from 0.7 to 1000 (11 cases). For comparison, the computations for a forced flat gas-liquid interface were also carried out in the same conditions as for the wind-driven wavy gas-liquid interface (11 cases). Each computation was performed until the flow field on the liquid side reaches statistically steady state. The CPU times for the wind-driven wavy and flat interfaces were about 3900 hours (10 days of wall-clock time using 16 cores) and 5200 hours (14 days of wall-clock time using 16 cores) for 2,400,000 steps and 6,400,000 steps (6.0 seconds and 16.0 seconds) on the super computer NEC: SX-ACE, respectively. Figure 1 shows the instantaneous configuration of the wind-driven gas-liquid interface at a fully-developed time.

Results and Discussion

The mass transfer coefficient on the liquid side, k_L , (Eq. (1)) is calculated as:

$$k_L = \frac{F}{\Delta C} = \frac{1}{(C_i - C_b)} \frac{1}{A} \int_{\text{interface}} D_L \frac{\partial C}{\partial n} dS, \quad (11)$$

where $\Delta C = C_i - C_b$ (here, C_i and C_b are the mass concentrations of the interface and bulk liquid, respectively, and C_b is set to be zero in this study), n the normal direction with respect to the gas-liquid interface, A the surface area of the interface, and D_L the molecular diffusivity of the mass on the liquid side. For both the wind-driven wavy and flat interfaces, the statistics were taken after the flows fully develop and the values of k_L indicate statistically steady values. That is, in the wind-driven wavy interface, we started the wind-water simulation with initial flat air-water interface, defined as $t = 0$ s. We started to solve the mass concentration field also at $t = 0$ s. We calculated a time-averaged k_L by use of the mass concentration field during the time period $t = 5.0$ s to 6.0 s. In flat interface condition, we similarly started the wind-water simulation at $t = 0$ s, but we did not start to solve the mass concentration field until $t = 10$ s, and we calculated a time-averaged k_L by use of the mass concentration field from $t = 15.0$ s to 16.0 s. The statistics of wind and waves are also taken in the same manner as Komori *et al.*⁵ and Takagaki *et al.*⁶, and the values are listed in Table 1. Here, the uniform velocity on the gas side, U_{∞} , is defined as the velocity on the upper wall of the computational domain. The wind speed at 10 m height above the gas-liquid interface, U_{10N} , drag coefficient, C_{DN} , and surface current, U_{SURFB} , are estimated in the same manner as Komori *et al.*⁵ and Takagaki *et al.*⁶. Each wind wave is determined by applying the zero-up cross method to the spatial fluctuation of the water level. First of all, we obtained the streamwise distribution of surface elevation (Fig. 2). Using the zero-up cross method, we detected locations with zero-up cross (see positions A, B, and C in Fig. 2). Then, for example, a wave is defined as being in the area between positions of A and B in Fig. 2. From those waves, we selected the largest one-third waves, and defined the significant waves as the largest one-third waves. The significant wave height, H_s , and significant wave length, L_s , are defined as the mean wave height and length, respectively, for the largest one-third waves. The phase speed of the significant wind-waves, C_p , is measured by analyzing the propagation of the significant wind-waves.

Case	t	U_∞	u^*	U_{10N}	C_{DN}	U_{SURF}	H_S	L_S	C_P
	[s]	[m/s]	[m/s]	[m/s]	[-]	[m/s]	[m]	[m]	[m/s]
FLAT	15.0–16.0	4.87	0.241	8.86	7.40×10^{-4}	0.143	—	—	—
WAVE	5.0–6.0	3.13	0.243	7.21	1.14×10^{-3}	0.0667	0.00654	0.0488	0.313

Table 1. Predicted characteristics of gas flow and wind waves. t : elapsed time, U_∞ : free stream wind speed, u^* : friction velocity on the gas side, U_{10N} : wind speed at 10-m height, C_{DN} : drag coefficient, U_{SURF} : surface current, H_S : significant wave height, L_S : significant wave length, C_P : phase speed of significant wind waves.

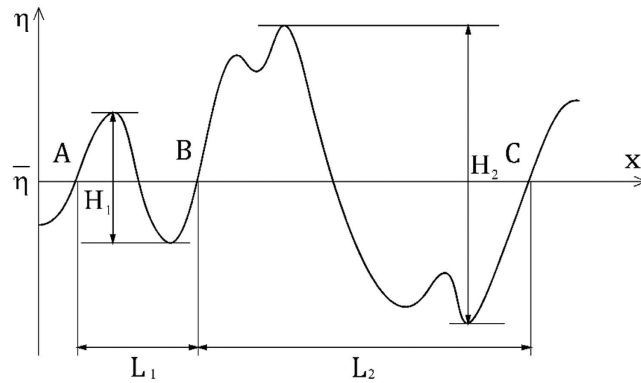


Figure 2. Sketch of zero-up cross method.

Figure 3 shows the relationship between distributions of instantaneous local mass flux on the gas-liquid interface and the mass concentration on the liquid side (y - z and z - x planes) for the wind-driven wavy interface for $Sc = 1.0$ and 1000 at $t = 5.0$ s. Here, the local mass flux, F_{local} , on the gas-liquid interface is estimated by:

$$F_{local} = D_L \frac{\partial C}{\partial n}. \quad (12)$$

It should be noted that the color ranges of F_{local} and the mass concentration for $Sc = 1.0$ and 1000 are different in this figure. The distributions of F_{local} and the mass concentration on the liquid side for $Sc = 1.0$ and 1000 are observed to be similar, namely, streaky motions of the mass flux on the gas-liquid interface are strongly associated with the streamwise vortices related to downward bursting motions appearing beneath the interface. The mass transfer mechanism across the wind-driven wavy interface is illustrated in Figure 24 in Komori *et al.*⁵. In summary, a pair of streamwise vortices causes downward bursting motions beneath the streaky regions with both low-mass flux and high streamwise velocity of the gas-liquid interface, and the peeling process happens between the downward bursting motions. Due to this process, the surface layer thickness is reduced and the gradient of the mass concentration increases, and then the mass flux is enhanced. It is evident that the distribution of F_{local} is streaky and the amount of the mass entrained into the liquid side is lower for $Sc = 1000$ than those for $Sc = 1.0$ due to the lower diffusivity, although the locations of the low- F_{local} streaks on the gas-liquid interface are identical between them. It is also confirmed, from the figure, that high Sc mass ($Sc = 1000$) induces a smaller scale structure than low Sc mass ($Sc = 1.0$).

Figure 4 shows the relationship between the mass transfer coefficient, k_L^+ , normalized by the friction velocity on the liquid side and Sc , together with those obtained by previous experiments (Jähne *et al.*³, Iwano *et al.*^{17,18}, Hanratty³³) and computations for the wind-driven wavy interface (Komori *et al.*⁵, Takagaki *et al.*⁶, Banerjee *et al.*¹³) and the flat interface (Hasegawa and Kasagi^{27,34,35}, Calmet and Magnaudet³⁶). Here, Hanratty's³³ range is obtained using the experimental data of Jähne *et al.*², Liss¹⁴, Broecker *et al.*¹⁵, and Merlivat and Memery³⁷. Similar to the previous studies, the predicted k_L^+ for both the wind-driven wavy and flat interfaces tend to be proportional to $Sc^{-0.5}$ (see Jähne *et al.*¹), except in the low Sc range. It is interesting to recognize that the trends of k_L^+ against Sc are similar between the wind-driven wavy and flat interfaces. This is due to the fact that the mass transfer across the gas-liquid interface is controlled by streamwise vortices on the liquid side even for the wind-driven turbulence under the conditions of low wind velocities without wave breaking (Komori *et al.*⁵). On the other hand, there appear discrepancies in k_L^+ between the present computations for the wind-driven wavy and flat interfaces and between the present computations and the previous experiments for the wind-driven wavy interfaces. The former discrepancies in k_L^+ predicted by the present computations between the wind-driven wavy and flat interfaces are considered to be due to the presences of the gravity/capillary waves with Langmuir circulations based on the discussions in Komori *et al.*⁵ and Takagaki *et al.*⁶, in which the mass flux distributions on the gas-liquid interfaces between the wind-driven wavy and flat interfaces are compared. The latter discrepancies in k_L^+ between the present computations and the previous experiments for the wind-driven wavy interfaces are considered to be due to the presence of surface contamination in the experiments, based on the discussions in Komori *et al.*⁴ and Komori and Shimada³⁸. As shown in Fig. 4, the predicted k_L^+ for the wind-driven wavy interface for $Sc = 600$ is 100–200% larger than the measured values in Iwano *et al.*^{17,18} where the free stream wind

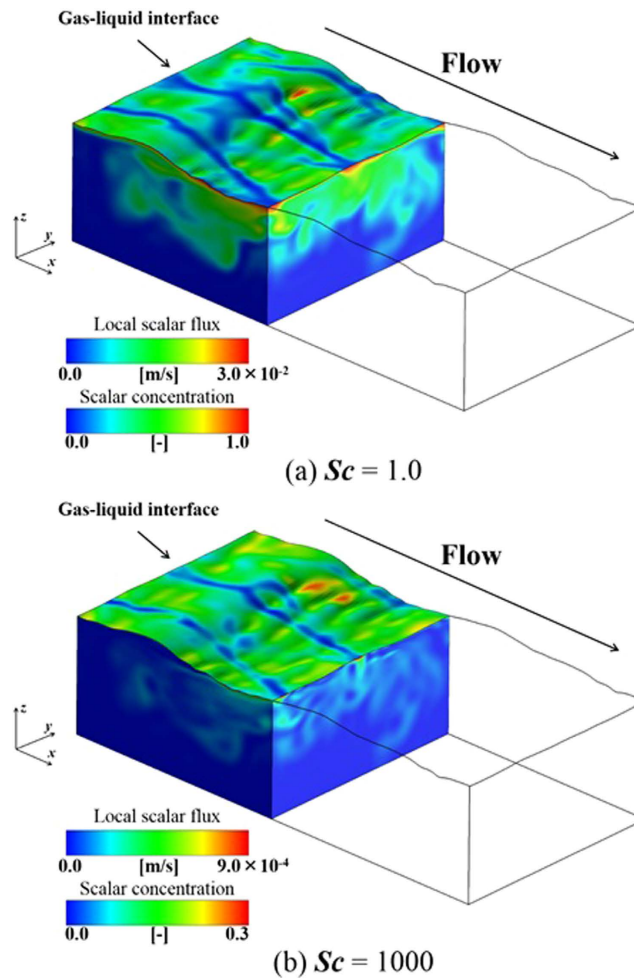


Figure 3. Relationship between distributions of instantaneous local mass flux on the gas–liquid interface, F_{local} and mass concentration on the liquid side (y - z and z - x planes) for the wind-driven wavy gas–liquid interface at $t = 5.0$ s for (a) $Sc = 1.0$ and (b) $Sc = 1000$. Only liquid sides are shown. It should be noted that the color ranges of F_{local} and mass concentration for $Sc = 1.0$ and 1000 are different.

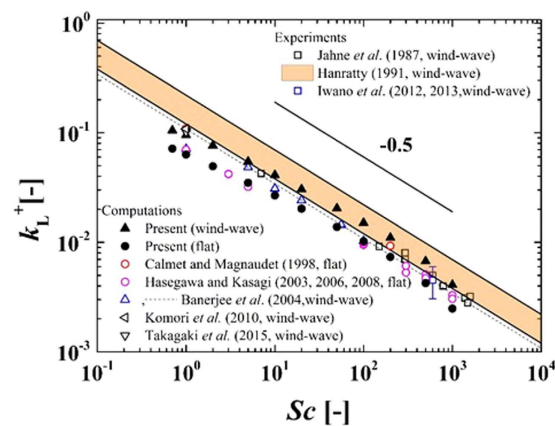


Figure 4. Relationship between k_L^+ and Sc together with previous studies.

speed ranges as $U_\infty = 3.4\sim 9.5$ m/s. Similarly, the present values of k_L^+ for the wind-driven wavy interface tend to be larger than the measured values in Jähne *et al.*³ as a whole. These results agree well with the statement in Komori *et al.*⁴ and Komori and Shimada³⁸ that the predicted value of k_L^+ becomes higher than that in experiments

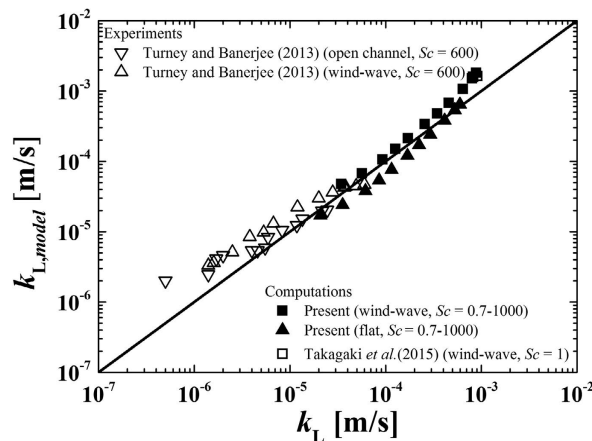


Figure 5. Relationship between measured and modeled values of mass transfer coefficients on both gas and liquid sides. Present values of $k_{L,model}$ are estimated using equation (8).

due to the presence of surface contamination in the experiments. It also confirmed that the filtering difference (equation (9)) is negligibly small on present results (e.g. Fig. 4).

The surface divergence model is considered as one of the models suitable for estimating the gas-liquid mass transfer coefficients (e.g. Banerjee *et al.*¹³, McCready *et al.*³⁹). McCready *et al.*³⁹ proposed an empirical model for the mass transfer coefficient on the liquid side, $k_{L,model}$ as:

$$k_{L,model} = 0.25\sqrt{\beta_{RMS}D_L}, \quad (13)$$

where D_L is the molecular diffusivity of mass on the liquid side, and β_{RMS} is the root-mean-square (RMS) value of the surface divergence, β . Here, β is defined as:

$$\beta = -\left.\frac{\partial w'}{\partial z}\right|_{z=0} = \left.\left(\frac{\partial u'}{\partial \hat{x}} + \frac{\partial v'}{\partial \hat{y}}\right)\right|_{z=0}, \quad (14)$$

where \hat{x} and \hat{y} are the tangential directions, and \hat{z} is the normal direction. In addition, u' and v' are the tangential fluctuating velocities in the streamwise and spanwise directions, respectively, and w' is the normal fluctuating velocity. The time-averaged RMS values of β_{RMS} are 36.5 s^{-1} (wind-wave) and 4.6 s^{-1} (flat). Figure 5 shows the relationship between mass transfer coefficients, k_L , and the values $k_{L,model}$ estimated from equations (13). Here, the vector spacings for calculating the surface divergence are 0.5 mm as in the study by Takagaki *et al.*⁶, and 0.5~0.7 mm and 0.7 mm in the study by Turney and Banerjee⁴⁰ on an open-channel gas-liquid interface, and on a wind-sheared gas-liquid interface, respectively. We can see moderately good agreements between our modeled data and the empirical data of previous studies (Turney and Banerjee⁴⁰). Slight disagreement of equation (13) with experimental and simulated k_L exists at low and high Sc , as seen in Fig. 5, and the coefficient of 0.25 is likely to depend on details of the flow field. Turney and Banerjee⁴⁰ showed that at wind conditions from approximately 4.0 to 10 m/s the capillary waves present in the capillary-gravity mixed wave field will not contribute toward both k_L due to dynamics of the advection-diffusion equation. This causes the needs for a combination of concepts from the surface renewal model and surface divergence model⁴⁰. For the purposes of this present paper, Fig. 5 shows surface divergence is an approximate proxy for gas-liquid mass transfer in a wide range of Schmidt number ($0.7 \leq Sc \leq 1000$).

Conclusions

In this study, a three-dimensional SEMI-DNS method was applied to a wind-driven turbulence with mass transfer across a sheared wind-driven wavy gas-liquid interface, and the relationship between mass transfer coefficient, k_L , and Schmidt number, Sc , was investigated in the wide range of $0.7 \leq Sc \leq 1000$. In order to capture the deforming gas-liquid interface, an arbitrary Lagrangian-Eulerian formulation (ALE) method was employed. The results showed that similar to the cases for flat gas-liquid interfaces, the mass transfer coefficient normalized by friction velocity on the liquid side, k_L^+ for the wind-driven wavy gas-liquid interface is generally proportional to $Sc^{-0.5}$. This trend is endorsed by the fact that the mass transfer across the gas-liquid interface is controlled mainly by streamwise vortices on the liquid side even for the wind-driven turbulence under the conditions of low wind velocities without wave breaking. In addition, the present study showed that k_L can be roughly estimated by the surface divergence model. For the higher wind velocity conditions, spanwise vortices due to gravity and capillary waves may affect the mass transfer across the interface. The details should be clarified using more powerful supercomputers in a future study.

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Author Contributions

N.T. analyzed the data and wrote this paper with R.K. R.K. designed the project including earning of research fund and framed this paper. A.K. conducted numerical simulations for mass transfer. S.K. supervised the overall project.

Additional Information

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