

Metal removal from soil leachates using DTPA-functionalised maghemite nanoparticles, a potential soil washing technology

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14 Abstract

There is significant current interest in the application of magnetic (magnetite or maghemite) 15 16 nanoparticles functionalised with chelating agents for the environmental remediation of metal 17 contaminated waters and solutions. Whilst there is a body of knowledge about the potential remediation efficacy of such engineered nanoparticles from studies involving synthetic 18 19 solutions of single metals, there is relatively little data involving mixed-metal solutions and virtually no studies about nanoparticle performance in chemically complex environmental 20 solutions representing those to which a scaled-up nanoremediation process might eventually 21 be applied. Therefore, we investigated the ability of diethylenetriaminepentaacetic acid 22 (DTPA)-functionalised, silica-coated maghemite nanoparticles to extract potentially toxic (Cd, 23 Co, Cu) and "non-toxic" (Ca, Mg) metals from solution (initial [metal] = 10 mg L^{-1} ; pH range: 24 2-8) and to extract a wider range of elements (As, Ca, Cd, Co, Cr, Cu, Mg, Na, Pb, Zn) from 25 leachate obtained from 10 different contaminated soils with variable initial pH, (semi-)metal 26

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27 and dissolved organic carbon (DOC) concentrations. The functionalised nanoparticles could extract the potentially toxic metals with high efficiency (in general >70 %) from single metal 28 solutions and with efficiencies that were either unaffected or reduced from the soil leachates. 29 K_d values remained high (> 500 L kg⁻¹), even for the soil leachate extractions. Our findings 30 31 show that DOC and relatively high concentrations of non-toxic elements do not necessarily 32 reduce the efficiency of metal contaminant removal by DTPA-functionalised magnetic 33 nanoparticles and thus demonstrate the potential of this process when applied to chemically 34 complex soil-derived contaminated solutions.

35

36 **Keywords**: metals; soil; DTPA; adsorption; remediation; nanoparticles

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38 Introduction

39 The contamination of soils with toxic metals can potentially lead to significant health effects in humans, flora and fauna (Siegel, 2002). This occurs if a pathway of exposure to toxic 40 41 metals is established. Toxic metals are present in many different phases in the soil including being bound to organic matter, iron or manganese hydroxides and being incorporated within 42 43 the structure of mineral grains (Sahuquillo et al. 1999; Lei et al. 2010). However the most important fraction with regards to potential risk is the water soluble fraction as the metals 44 within this fraction are both mobile and bioavailable (Seguin et al. 2004). This means they 45 can be taken up by organisms and leach into rivers, lakes and groundwater thereby 46 providing a pathway for plant, animal and human exposure. When metal contamination of 47 soils poses a risk to the surrounding ecosystem and human health, remediation schemes 48 are often instigated. Soil washing is an established technology used for removing toxic 49 50 metals from soils, and aminocarboxylate chelating agents such as DTPA and EDTA are often used to enhance metal removal (Lestan et al., 2008). Whilst using chelating agents 51 52 improves the effectiveness of metal removal, the techniques currently used for removing the chelating agents from solution after use, such as membrane separation, electrochemical 53 54 treatment or precipitation via the addition of ferric chloride or calcium hydroxide can often

add to remediation costs as they require inputs of energy or chemical reagents (Lo and
Zhang, 2005; Finzgar and Lestan, 2008; Pochieca and Lestan, 2009).

57

58 The nanoparticle revolution has impacted on many areas of modern life. In the field of remediation perhaps most practical applications of nanotechnology have focussed on the 59 use of zero valent iron as a treatment of organic contaminants in ground water (e.g. Li et al, 60 2006; Varanasi et al., 2007; Kim et al., 2017; Zhang et al., 2009; Crane and Scott, 2012; Fu 61 et al., 2014). However, a challenge with the use of zero valent iron is the concern regarding 62 63 the environmental fate of nanoparticles post injection into aquifers (Oughton et al., 2017). Another promising application of nanotechnology in the field of remediation focusses on the 64 use of magnetic nanoparticles as there is the potential for recovery of the nanoparticles 65 using magnets following deployment. Many studies have now investigated the use of 66 magnetic nanoparticles, typically magnetite or maghemite, which are then functionalised with 67 chelating agents to enable the particles to adsorb metal contaminants in a highly efficient 68 69 way. The majority of these studies have currently been conducted in the laboratory using 70 ideal solutions of single (Liu et al., 2009; Wang et al., 2011; Zhang et al., 2011; Figueira et al., 2011; Koehler et al., 2009; Afsar et al., 2014; Yen et al., 2017; Chung et al., 2012; Wang 71 72 et al., 2015 Chen et al., 2014; Chen et al., 2016; Pan et al., 2016) or far less frequently, multiple (Zhang et al., 2011; Liu et al., 2008; Zeng et al., 2012; Hughes et al., 2017; Shan et 73 74 al., 2015) potentially toxic metals. To increase levels of realism some studies have 75 considered the impact of dissolved organic matter (DOM) on the efficiencies of metal 76 removal by such nanoparticles, either through additions of organic acids to metal solutions 77 (Zhang et al., 2012; Hughes et al., 2017) through the use of metal-amended natural waters 78 (Figueira et al., 2011; Liu et al., 2008) or, rarely, the use of actual metal contaminated environmental solutions (Bao et al., 2016). 79

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81 In our previous study we described a synthetic method for preparing DTPA-functionalised maghemite nanoparticles and tested the efficiency of the nanoparticles for Pb and Zn 82 83 removal from solution for both single and binary metal solutions and in the presence and 84 absence of fulvic acid as a model form of DOM. Metal-bearing solutions arising from soil 85 washing will contain a wider range of metals (both contaminant and non-contaminant) and a 86 more diverse range of forms of DOM. Therefore, the aims of the current study were to 87 consider the effectiveness of our nanoparticles for 1) adsorption of a wider range of metals 88 (Ca, Cd, Co, Cu and Mg) from solution and 2) extraction of metals from leachate obtained 89 from metal contaminated soils. Our study is novel in the following respects. Firstly, it uses 90 DTPA functionalised nanoparticles; despite the established chelating capacity of DTPA there 91 are hardly any reports of the synthesis and use of DTPA-functionalised magnetic 92 nanoparticles (Koehler et al., 2009; Zhao et al., 2015; Zhang et al., 2016; Hughes et al., 93 2017 to date that we are aware of). Secondly, and from the perspective of assessing the practical applications of this emerging technology more importantly, it uses soil leachate 94 95 from metal contaminated soils resulting in mixed metal solutions with relatively high DOM contents and the presence of "non-toxic" metals such as Ca and Mg. 96

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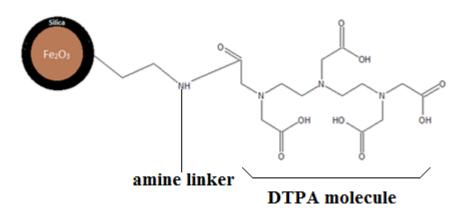
98 Methods

99 DTPA-functionalised maghemite nanoparticles

DTPA-functionalised maghemite nanoparticles were synthesised as previously described 100 (Hughes et al., 2017). In brief, the maghemite nanoparticles were synthesised by the 101 reaction of Fe²⁺ and Fe³⁺ ions present in FeCl₂ and FeCl₃ solutions in a 1:2 molar ratio in the 102 presence of 2 M NaOH as a base. The nanoparticles were given a silica coating by reacting 103 104 them in tetraethyl orthosilicate (TEOS) and an amine linker added to the surface via reaction with 3-aminopropyltriethoxysilane (APTES). The nanoparticles were washed in 105 106 dimethylformamide (DMF) and the diethylenetriaminepentaacetic acid (DTPA) added to the amine linker by reaction with triethylamine (TEA) and DTPA dianhydride to give the final 107 108 composite nanoparticle (Fig. 1). Finally the nanoparticles were washed four times in

methanol and stored in deionised water. The average diameter of the resulting particles was 47 \pm 6.9 nm (according to TEM). Full details of particle characterization are given in Hughes et al (2017).

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Fig. 1. Theoretical structure of the silica coated DTPA-functionalised maghemitenanoparticle.

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117 <u>Extraction tests</u>

The extraction tests (for both single metal solutions and soil leachates) followed the same 118 119 basic protocol detailed in Hughes et al (2017). 2 mL of an aqueous suspension of DTPA-120 functionalised nanoparticles (10 mg in total) were added to 8 mL of either a test solution 121 containing a background electrolyte of 0.1M NaNO₃, to maintain a constant ionic strength in the extraction solutions (Yang et al. 2006) or a soil leachate. For fixed pH experiments the 122 123 pH of the suspensions were adjusted by dropwise addition of 0.01M HCl and 0.1M NaOH. pH was measured using a Jenway 3310 pH meter with a Fisherbrand FB68793 glass 124 125 electrode. The pH meter was calibrated using pH 4 and pH 7 buffers. Calibration was 126 conducted at the start of analysis and after every 10 samples. Following addition of the 127 nanoparticles, each solution was shaken for 18 hours on an end-over-end shaker at constant temperature (20 °C). The nanoparticles were then removed from solution using a 128 129 neodymium permanent magnet and the solution analysed for the metal(s) of interest by 130 either a Perkin Elmer 100B Atomic absorption spectrometer (AAS) or a Perkin Elmer

131 OPTIMA 3000 inductively coupled plasma optimal emission spectrometer (ICP-OES). In the single metal experiments, to check for nanoparticle stability and / or remnant nanoparticles in 132 suspension, Fe in solution was also analysed by AAS or ICP-OES. In all cases Fe was 133 134 below detection in solution indicating that the nanoparticles were stable and removal of at 135 least 99.99% of the added nanoparticles (Hughes et al, 2017). Nanoparticle free controls 136 were also run. All experiments were performed in triplicate. Metal extraction efficiency was 137 calculated as the difference in concentration between the test and a control solution 138 expressed as a percentage of the control solution concentration. Partition coefficients (K_d) 139 were calculated as the ratio of metal concentration on the nanoparticles to the metal concentration remaining in solution. 140

141

142 Single metal solutions

143 In the first set of experiments, solutions containing 10 mg L⁻¹ of either Ca, Cd, Co, Cu or Mg were used (though note that results are expressed in terms of moles to allow comparison 144 between elements). The metals were introduced as nitrate salts and the pH was adjusted to 145 pH 2, 3, 4, 5, 6, 7 and 8. Metal concentrations were analysed by AAS. Detection limits were 146 147 0.02 mg L⁻¹ (Ca), 0.01 mg L⁻¹ (Cd), 0.007 mg L⁻¹ (Cu), 0.009 mg L⁻¹ (Co), 0.001 mg L⁻¹ (Fe), 0.001 mg L⁻¹ (Mg), 0.008 mg L⁻¹ (Pb) and 0.01 mg L⁻¹ (Zn), whilst precision was 3.16% (Ca), 148 4.62% (Cd), 2.99% (Cu), 3.71% (Co), 2.66% (Fe), 3.40% (Mg), 3.52% (Pb) and 3.08% (Zn). 149 Accuracy was 98% (Ca), 97% (Cd), 98% (Cu), 95% (Co) and 96% (Mg). 150

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152 Soil leachates

153 For a second set of experiments, soils were collected from metal contaminated sites:

Avonmouth (ST 532 803) a former Pb/Zn smelter, which was operational until 2003

155 (Nahmani et al. 2007); Barney Beck (SD 992 998), an episodically flooded pasture located

near a small tributary of the River Swale in North Yorkshire, an area that was extensively

- 157 mined for Pb from the Roman era up until the late 19th Century when the mine was
- abandoned (Dennis, 2005); Cwmystwyth (SN 804 747) a former Pb/Zn mine site located in

159 Ceredigion, central Wales that was mined from the beginning of the Roman era to 1950 (Hughes, 1981); Devon Great Consols (DGC) (SX 728 964) an abandoned Cu and As mine 160 which operated between 1844 and 1930 (Richardson, 1991); Graig Goch (SN 802 741) an 161 162 abandoned Pb mine located in Ceredigion, central Wales and a part of the central Wales 163 orefield (Palumbo-Roe, 2013); Redruth (SW 724 397) the former Tresavean Cu and Sn mine 164 site, which ceased operating in 1928 (Dines, 1956); Rookhope (NY 894 441) a former Pb and fluorspar mine (Sizmur et al. 2011); Scunthorpe (SE 893 108) the site of the 165 166 Buckingham allotments which have elevated soil As concentrations due to the underlying 167 geology of the area which consists of arsenic rich Jurassic ironstone (Palumbo-Roe et al. 2005); Shipham (ST 448 573) a former Zn mining site, active in the 18th and 19th centuries in 168 Somerset (Kiekens, 1995); and, Wisley (TQ 065 592) an uncontaminated sandy loam soil 169 that was spiked with lead nitrate, copper sulphate and zinc sulphate in 2005 (Alexander et al. 170 171 2006). These soils were used to generate leachates that were in turn used to investigate the ability of the DTPA-functionalised nanoparticles to remove metals from mixed-metal 172 solutions that also contained natural dissolved organic matter. This allowed an assessment 173 of the potential use of the nanoparticles as a component of soil washing remedial treatments 174 175 or to remediate metal-contaminated water courses. The soil leachates were prepared by adding 2.5 g of soil (air dried, 2mm sieved) to 50 mL of ultrapure H₂O. This ratio was based 176 on the 1:20 to 1:40 range of optimal ratios for extraction of metals from soil washing 177 solutions using EDTA (Papassiopi et al., 1999). The suspension was shaken on an end over 178 end shaker for 24 hours then centrifuged for 20 minutes at 3500 rpm. The supernatant was 179 decanted off, producing the final soil leachate. The pH of the leachate was measured and 180 then 10 mg of nanoparticles in 2mL of ultrapure water were added to 8 mL of leachate. After 181 182 removal of the nanoparticles, solutions were syringe filtered using 0.45µm cellulose nitrate filters before being analysed for a range of metals by ICP-OES (As, Ca, Cd, Co, Cr, Cu, Fe, 183 Mg, Na, Ni, P, Pb, Zn). Detection limits and precision were as follows: As (1.3 x 10⁻³ mg L⁻¹, 184 3.1 %), Ca (1.3 x 10⁻³ mg L⁻¹, 2.6%), Cd (8.9 x 10⁻⁵ mg L⁻¹, 2.9 %), Co (1.6 x 10⁻³ mg L⁻¹, 185 186 4.2%), Cr (3.2 x 10⁻⁴ mg L⁻¹, 3.9%), Cu (1.3 x 10⁻³ mg L⁻¹, 2.6 %), Fe (2.1 x 10⁻³ mg L⁻¹, 4.5

%), Mg (1.6 x 10⁻⁴ mg L⁻¹, 2.5%), Na (9.2 x 10⁻⁴ mg L⁻¹, 3.1 %), Ni (3.3 x 10⁻³ mg L⁻¹, 2.7%), P 187 (3.3 x 10⁻² mg L⁻¹, 2.7 %), Pb (1.2 x 10⁻² mg L⁻¹, 3.3 %), Zn (8.5 x 10⁻⁴ mg L⁻¹, 3.6 %). 188 Dissolved organic carbon (DOC) was measured using a Shimadzu TOC-L total carbon 189 analyser equipped with a non-dispersive infra-red (NDIR) detector. The detection limit for the 190 191 DOC was 1.31×10^{-4} mg L⁻¹ and the precision value for the 12 samples measured in 192 duplicate was ± 2.4 %. 193 194 Statistical analysis 195 Data were analysed using SigmaPlot 12 for Windows. 196 **Results and Discussion** 197 198 199 Single metal studies 200 Metal concentrations in the control and nanoparticle-treated mono-metallic solutions are 201 presented in Table 1 and calculated extraction efficiencies in Table 2. The decrease in 202 control solution concentrations with increasing pH for Cu and, to a lesser extent Cd and Co, 203 indicate that some precipitation occurred at higher pH values for these metals. However, differences in concentration between the control and nanoparticle-treated solution 204 concentrations at a given pH are indicative of adsorption as the metal removal process. K_d 205 values were calculated as the ratio of the concentration of metal on the nanoparticles at 206 equilibrium concentrations (mmol kg⁻¹) and the concentration of metal in solution at 207 equilibrium (mmol L⁻¹) for the extractions and are presented in Table 3. 208 209

Table 1. Concentrations (mmol L⁻¹) of metals in solution in control and nanoparticle treated solutions. Values are mean ± standard deviations (n

211 = 3).

	Ca		Cd		Co		Cu		Mg	
рН	Control	NP	Control	NP	Control	NP	Control	NP	Control	NP
2	0.232 ±0.004	$\textbf{0.223} \pm \textbf{0.001}$	0.086 ± 0.001	0.032 ± 0.003	0.173 ± 0.002	0.033 ± 0.013	0.163 ± 0.002	0.022 ± 0.00	0.406 ± 0.002	0.402 ± 0.006
3	$\textbf{0.233} \pm \textbf{0.003}$	0.161 ± 0.032	0.085 ± 0.001	$\textbf{0.010} \pm \textbf{0.000}$	0.171 ± 0.002	$\textbf{0.018} \pm \textbf{0.002}$	0.158 ± 0.001	$\textbf{0.017} \pm \textbf{0.000}$	$\textbf{0.416} \pm \textbf{0.004}$	0.348 ± 0.031
4	0.237 ± 0.003	0.090 ± 0.008	0.080 ± 0.000	0.006 ± 0.002	0.168 ± 0.001	$\textbf{0.017} \pm \textbf{0.001}$	0.150 ± 0.007	0.026 ± 0.002	0.407 ± 0.004	0.337 ± 0.026
5	0.227 ± 0.001	$\textbf{0.079} \pm \textbf{0.012}$	0.065 ± 0.001	0.006 ± 0.002	$\textbf{0.169} \pm \textbf{0.001}$	0.020 ± 0.002	0.154 ± 0.003	0.032 ± 0.000	$\textbf{0.410} \pm \textbf{0.002}$	0.336 ± 0.031
6	0.236 ± 0.001	0.080 ± 0.004	$\textbf{0.077} \pm \textbf{0.000}$	$\textbf{0.007} \pm \textbf{0.002}$	$\textbf{0.168} \pm \textbf{0.001}$	$\textbf{0.019} \pm \textbf{0.001}$	0.150 ± 0.002	0.026 ± 0.000	$\textbf{0.413} \pm \textbf{0.005}$	$\textbf{0.339} \pm \textbf{0.016}$
7	$\textbf{0.228} \pm \textbf{0.002}$	0.059 ± 0.005	$\textbf{0.077} \pm \textbf{0.003}$	0.006 ± 0.001	0.152 ± 0.001	$\textbf{0.019} \pm \textbf{0.000}$	0.067 ± 0.004	$\textbf{0.017} \pm \textbf{0.001}$	$\textbf{0.410} \pm \textbf{0.002}$	0.354 ± 0.014
8	0.231 ± 0.000	0.057 ± 0.007	$\textbf{0.079} \pm \textbf{0.000}$	$\textbf{0.006} \pm \textbf{0.000}$	0.152 ± 0.003	0.020 ± 0.000	0.058 ± 0.011	0.012 ± 0.002	0.402 ± 0.016	0.391 ± 0.008

212

Table 2. Percentage extraction efficiencies of Ca, Cd, Co, Cu, Mg, Pb and Zn from aqueous

solution by nanoparticles at pH 2 to 8. Values are mean \pm standard deviation, n = 3. Pb and

рН	2	3	4	5	6	7	8
Metal							
Ca	3.6 ± 0.54	31 ± 14	62 ± 3.3	65 ± 5.3	66 ± 1.9	74 ± 2.1	75 ± 3.0
Cd	62 ± 3.7	89 ± 0.57	92 ± 2.0	91 ± 2.8	91 ± 3.1	92 ± 1.4	92 ± 0.13
Co	81 ± 7.5	90 ± 1.2	90 ± 0.53	88 ± 1.2	89 ± 0.66	87 ± 0.23	87 ± 0.40
Cu	86 ± 0.17	90 ± 0.10	82 ± 1.5	79 ± 0.18	82 ± 0.060	75 ± 1.8	79 ± 3.2
Mg	1.0 ± 1.5	16 ± 7.4	17 ± 6.3	18 ± 7.6	18 ± 3.8	14 ± 3.5	2.7 ± 2.0
Pb	91 ± 2.8	97 ± 0.32	94 ± 0.78	95 ± 0.92	94 ± 1.6	62 ± 9.4	71 ± 8.1
Zn	76 ± 10	92 ± 2.6	92 ± 1.8	91 ± 1.4	91 ± 1.7	91 ± 0.53	88 ± 0.26

217 Zn data from Hughes et al. (2017).

218

Table 3. Metal partition coefficients (K_d / L kg⁻¹) for Cd, Co, Cu, Pb, Zn, Ca and Mg extraction by nanoparticles between pH 2 and 8. Values are mean ± standard deviation (n = 3). Pb and

221 Zn values taken from Hughes et al (2017).

рН	Cd	Со	Cu	Pb	Zn	Са	Mg
2	1680±250	5140±3190	6270±88.1	10800±4400	4050±2850	37.3±5.80	10.4±15.9
3	7780±441	8750±1070	8580±91.2	32800±3440	12000±3560	486±329	200±112
4	12100±2950	8630±483	4700±494	17300±2780	12000±2660	1650±222	212±95.6
5	11000±3290	7570±836	3810±40.9	18900±3760	10000±1720	1990±425	228±120
6	11100±3570	7870±520	4670±19.4	16000±4240	10900±2440	1960±171	220±57.5
7	11400±1950	6820±141	3060±281	1760±747	10100±636	2880±324	160±47.8
8	12300±234	6800±242	3890±706	2670±1140	7560±189	3120±499	28.4±21.7

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Of the potentially toxic metals, extraction efficiency of Cd, Co and Cu is in the same range as that of Pb and Zn in our previous experiments (Hughes et al., 2017) and as reported for a range of functionalised nanoparticles (e.g. Afsar et al., 2014; Liu et al., 2008; Liu et al., 2009; Koehler et al., 2009; Zhang et al., 2011; the review of Lofrano et al., 2016; Table S1 in the Supplementary Information). In depth comparison of extraction efficiencies found here and in other studies is compromised by differences in initial solution composition and solid/liquid 229 ratios. Two way Analysis of Variance (ANOVA) indicates that significant (p < 0.01) differences are present between metals and between pH for both extraction efficiencies and 230 K_{d} values and that there are significant interaction terms between the two. Extraction 231 efficiency is greater for Cd, Co, Cu, Pb and Zn than it is for Ca and Mg at all pH levels 232 233 except at pH 7 and 8 when extraction efficiency of Ca increases; relative to the other "toxic" metals Cd shows reduced extraction efficiency at pH 2 and Cu at pHs 4 – 6. Pb extraction 234 efficiency decreases at pH 7 and 8. In general K_ds of \geq 500 L kg⁻¹ are considered acceptable 235 236 and > 5000 mg/L very good (Fryxell et al., 2005). Thus the K_ds determined for our 237 nanoparticles across a range of potentially toxic metals are suggestive of them being a useful adsorbent. Ca and Mg always have the lowest Kds. Similar results are reported in 238 other studies using functionalised nanoparticles. 239

240

The iso-electric point of the nanoparticles is 6.74 (Hughes et al., 2017). Thus whilst our 241 242 previous data suggest that adsorption of the metals is most likely dominated by chelation 243 with the nitrogen atoms in the DTPA (Hughes et al., 2017) for $pH \le 6$ ion exchange with protons on the protonated functional groups of the DTPA and for pH > 7 electrostatic 244 adsorption to deprotonated functional groups of the DTPA is also likely to occur. The 245 246 differences in efficiencies and Kds between the different metals are due in part to the metal-247 DTPA complexation stability constants for the potentially toxic metals tested being higher 248 than those for Ca and Mg (e.g. Lindsay et al., 1979; Dojino, 2017; Liu et al., 2008). However, in addition, as initial concentrations in solutions for the single metal tests were equal for all 249 metals on a mg L⁻¹ basis the different atomic masses of the elements result in differing molar 250 concentrations which may also have an impact. For example, both Ca and Mg have lower 251 atomic masses than the toxic metals and therefore their molar concentrations are higher. 252 Adsorption sites on the nanoparticles are potentially closer to saturation in the Ca and Mg 253 254 extraction tests which may reduce extraction efficiency.

255 The reduced extraction efficiency of Cd at pH 2 compared to Cu and Pb (Hughes et al., 2017) is consistent with previous studies using EDTA-functionalised nanoparticles (Koehler 256 257 et al., 2009; Zhang et al., 2011) and is due to the lowering of the pH-dependent complex 258 formation constant (Anderegg et al., 1959). Reduced extraction efficiency of Cu relative to 259 Cd and Pb at similar concentrations to those used in our experiment has been previously 260 observed at pH 6 (Koehler et al., 2009) and pH 5 (Zhang et al. 2011) and attributed to the 261 lower molar concentration of Cd and Pb solutions relative to Cu for solutions of the same 262 concentration by mass leading to increased saturation levels of adsorption sites for the Cu. 263 The high extraction efficiency and K_d values for Pb at pH 2 – 6 are consistent with a number of other studies using a variety of functionalised nanoparticles (Koehler et al., 2009; Zhang 264 265 et al., 2011; Liu et al, 2009; Liu et al., 2008) and are related to high stability constants and the low molar concentration of Pb in the test solution relative to the other metals. We have 266 267 discussed the reduced extraction efficiency and K_d values of Pb at pH 7 and 8 previously (Hughes et al., 2017); it is consistent with previous studies on a variety of functionalised 268 nanoparticles and is attributed to changes in speciation at these pH values (Hughes et al., 269 2017; Wang et al., 2015; Weng, 2004; Liu et al., 2009). 270

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272 Similar to other studies on a variety of chelating agent functionalised magnetic nanoparticles (e.g. Chen et al., 2016; Liu et al., 2008; Liu et al., 2009; Shi et al., 2016; Zhang et al., 2012, 273 274 Zhang et al., 2011; Table S1 in Supporting Information) our single metal extraction experiments show that our functionalised nanoparticles can extract a range of contaminant 275 276 metals. This is to be expected as the chelating agents used to functionalise the nanoparticles are not specific for a single metal. This is encouraging for use of functionalised 277 nanoparticles in real world situations where mixed metal contamination is more likely than 278 single metal contamination. However, although previous studies have shown the capacity of 279 280 functionalised nanoparticles to maintain high extraction efficiencies in mixed metal solutions often containing high concentrations of nontoxic elements such as Ca and Mg (e.g. Hughes 281

282 et al., 2017; Liu et al., 2008; Shan et al., 2015; Zhang et al., 2012) extraction efficiency can be reduced relative to single metal solutions (e.g. Hughes et al., 2017; Liu et al., 2008; 283 Zhang et al., 2011). Ca and Mg often occur at high concentrations in soils (Ca = $1-200 \text{ g kg}^{-1}$; 284 $Mg = 0.1-28.6 g kg^{-1}$ (Bolan et al. 2004) and solutions and leachates from soil could 285 286 therefore contain higher concentrations of such elements than concentrations considered in 287 experiments to date. Similarly although previous studies have shown high levels of metal 288 extraction in the presence of DOC (Hughes et al., 2017; Liu et al., 2008; Shan et al., 2015; 289 Zhang et al. 2012) our previous experiments (Hughes et al., 2017) also showed significant reductions in extraction efficiency at concentrations of 2.1 mg L⁻¹ and 21 mg L⁻¹ DOC. Metal-290 291 rich extracts obtained by leaching soils with water may contain higher concentrations of DOC 292 than this which could potentially have an impact on the extraction efficiency of toxic metals 293 from such soils. Therefore to investigate further the potential use of our DTPA-functionalised 294 nanoparticles for removal of metal from the aqueous leachates of contaminated soils, we determined extraction efficiencies using leachates from soils containing a mixture of 295 296 inorganic contaminants and variable, native concentrations of DOC.

297

298 Soil extractions

The chemistry of the soil leachates in control and nanoparticle-present treatments is 299 300 presented in Tables 4 and 5. All the leachates were filtered to 0.45 μ m prior to use. 301 Operationally we have assumed that this filtration step results in the production of a pure 302 solution and that differences between control and nanoparticle-present treatments are therefore due to interactions between ions in solution and the added nanoparticles. We did 303 304 not analyse our filtered solutions for the presence of colloids but these may be present and 305 have an impact on our results. However, from a practical perspective the aim of our 306 investigation was to determine whether our nanoparticles were effective at removing metals from leachates obtained from metal contaminated soils regardless of whether colloidal 307 particles play a role or not. The leachates contain relatively low concentrations of metals 308

309 despite samples being taken from former mine sites with soils that have high total metal concentrations reported in the literature; this reflects the speciation of the metals in the soils 310 311 and highlights the important difference between concentrations of "total" metals compared to other fractions such as "bioavailable", "bioaccessible" and "mobile". The Scunthorpe soil is a 312 good example of this. Palumbo-Roe et al (2005) report elevated As concentrations in soils 313 314 taken from this sample locality but also that the majority of this As is not bio-accessible. 315 Further the pH of the leachate (c. neutral) lies in the range where As sorption to Fe oxides is 316 high which reduces the likelihood of As passing into solution (Dixit and Hering, 2003; Partey 317 et al. 2008). However, in this study we are not concerned with the issue of bioavailability of metals in soils. Rather, the contaminated soils were used to generate leachates containing 318 319 metals which could be used to determine the ability of the DTPA-functionalised nanoparticles 320 to remove metals from mixed metal solutions that also contained dissolved organic matter. 321 This allowed us to assess the potential use of the nanoparticles as a stage in soil washing remedial treatments and / or for remediating metal-contaminated natural waters. 322

323

The total concentration of "non toxic" elements (Ca, Mg, Na) in the control leachate was 324 325 significantly greater ($p \le 0.05$, Kruskal-Wallis analysis of variance on ranks) than that of the total concentration of potentially toxic elements (As, Cd, Co, Cr, Cu, Pb, Zn). Despite this the 326 nanoparticles removed significantly more toxic than non-toxic (either Ca+Mg or Ca+Mg+Na) 327 elements from solution ($p \le 0.05$, Kruskal-Wallis analysis of variance on ranks). Out of the 328 10 soils studied, where there are significant differences (p ≤ 0.05 ; t-tests) between the 329 concentrations in the nanoparticle-present and control treatments (As - 4 soils, Cd - 4 soils, 330 Cu – 4 soils, Pb – 5 soils, Zn – 6 soils), the nanoparticle-present treatments contain lower 331 332 concentrations of potentially toxic metals than the controls. Cd, Cu, Pb and Zn would be 333 present as cations under the solution conditions whereas As would be present as an oxyanion. As with the single element extractions, adsorption of the cations is most likely 334 335 dominated by chelation but will also involve, depending on pH, ion exchange or electrostatic

adsorption whilst adsorption of the As is most likely due to non-specific adsorption betweenthe As oxyanion and the protonated nanoparticle surface.

338

With respect to the effect of the nanoparticle treatment on concentrations of the major, non-339 340 toxic elements, Na usually has significantly higher concentrations in the nanoparticle-present treatments (7 out of 8 soils) whereas Mg was lower in the nanoparticle-present leachates for 341 two soils (Avonmouth and Cwmystwyth) and Ca showed no consistent trend in the two soils 342 (Avonmouth and Barney Beck) where there were significant differences. The production of 343 the nanoparticles involves precipitation of Fe oxide in 2 M NaOH. Despite subsequent 344 washing stages, the most obvious explanation for the increase in Na in solution on addition 345 of the nanoparticles to the leachates is that residual Na⁺ is still present associated with the 346 347 nanoparticles.

Table 4. Mean concentrations (µmol L⁻¹) of metals in control (cont) and nanoparticle (NP)-treated soil leachate. Values are mean ± standard

deviations (n = 3). BDL indicates concentration below detection limit. Bold italics indicate a significant difference ($p \le 0.05$; t-test) between

control and nanoparticle present solution element concentrations. For statistical analysis of solutions where concentrations were below
 detection limits, concentrations were fixed at the detection limit. Avon = Avonmouth, Barn = Barney Beck, Cwm = Cwmystwyth, DGC = Devon

352 Great Consols, Graig= Graig Goch, Red – Red Ruth, Rook = Rookhope, Scun = Scunthorpe, Ship = Shipham, Wis = Wisley.

Soil	Treatment	As	Ca	Cd	Co	Cr	Cu	Mg	Na	Pb	Zn
	cont	0.241 ± 0.075	415 ± 10.8	8.46 ± 0.380	0.167 ± 0.00348	0.151 ± 0.116	9.01 ± 0.997	145 ± 22.2	82.4 ± 11.1	7.89 ± 2.11	579 ± 22.8
Avon	NP	BDL	376 ± 15.7	6.48 ± 0.271	0.142 ± 0.0145	0.00900 ± 0.00417	1.19 <i>±</i> 0.213	1.70 ±2.30	119 ± 3.05	BDL	473 ± 19.9
Dorn	cont	BDL	118 ± 2.25	0.00226 ± 0.000111	BDL	0.0615 ± 0.0271	0.0197 ± 0.00143	$\textbf{16.4} \pm \textbf{2.06}$	$\textbf{47.1} \pm \textbf{0.415}$	0.686 ± 0.183	0.701 ± 0.204
Barn	NP	BDL	130 ± 5.39	BDL	BDL	0.0621 ± 0.0137	0.0241 ± 0.00388	$\textbf{17.3} \pm \textbf{1.91}$	104 ± 8.08	0.143 ± 0.0826	0.270 ± 0.213
Curr	cont	BDL	14.7 ± 4.65	$\begin{array}{c} 0.0150 \pm \\ 0.0000489 \end{array}$	$\begin{array}{c} 0.0293 \pm \\ 0.00361 \end{array}$	$\begin{array}{c} 0.0210 \pm \\ 0.0193 \end{array}$	0.132 ± 0.0470	10.2 ± 0.554	31.4 ± 2.54	1.53 ± 0.618	11.3 ± 0.704
Cwm	NP	BDL	10.2 ± 2.39	BDL	BDL	$\begin{array}{c} 0.00822 \pm \\ 0.00359 \end{array}$	$\begin{array}{c} 0.0663 \pm \\ 0.00695 \end{array}$	7.42 ± 1.00	78.5 ± 2.62	0.075 ± 0.000503	2.07 ± 1.45
DGC	cont	2.27 ± 0.101	107 ± 11.9	BDL	0.0755 ± 0.00810	BDL	11.7 ± 1.73	$\textbf{16.2} \pm \textbf{2.17}$	15.9 ± 1.20	BDL	1.44 ± 0.508
DGC	NP	1.129 ± 0.0449	111 ± 1.42	BDL	$\begin{array}{c} 0.0633 \pm \\ 0.00713 \end{array}$	BDL	0.247 ± 0.146	16.5 ± 0.304	66.1 ± 2.54	BDL	0.626 ± 0.285
Croig	cont	BDL	16.2 ± 0.683	0.157 ± 0.00535	0.109 ± 0.0183	$\begin{array}{c} 0.00676 \pm \\ 0.00105 \end{array}$	0.383 ± 0.00204	12.4 ± 0.656	28.3 ± 12.0	41.4 ± 0.591	75.9 ± 1.83
Graig	NP	BDL	18.0 ± 0.909	0.0946 ± 0.0107	0.0904 ± 0.00569	$\begin{array}{c} 0.00635 \pm \\ 0.000342 \end{array}$	0.0787 ± 0.0236	11.4 ± 0.293	71.3±3.15	0.228 ± 0.145	51.0 ± 7.39
Ded	cont	BDL	636 ± 47.5	BDL	BDL	BDL	$\begin{array}{c} 0.0384 \pm \\ 0.00696 \end{array}$	14.9 ± 0.842	90.4 ± 3.25	BDL	0.459 ± 0.212
Red	NP	BDL	681 ± 47.4	BDL	BDL	$0.0330 \pm$	0.0325 ± 0.0112	18.8 ± 2.75	35.4 ± 1.96	BDL	0.0404 ± 0.00485
Pook	cont	0.0764 ± 0.0124	308 ± 26.4	0.0181 ± 0.000750	0.166 ± 0.0701	$\begin{array}{c} 0.0600 \pm \\ 0.0476 \end{array}$	$\begin{array}{c} 0.0429 \pm \\ 0.0293 \end{array}$	53.4 ± 2.72	38.5 ± 2.54	$\textbf{3.38} \pm \textbf{1.46}$	8.59 ± 0.966
Rook	NP	0.0400 ± 0.00467	301 ± 3.37	BDL	0.126 ± 0.0141	$\begin{array}{c} 0.0200 \pm \\ 0.00547 \end{array}$	0.024 ± 0.0118	49.6 ± 0.820	85.7±5.68	0.952 ± 0.0782	1.50 ± 0.532
Sour	cont	0.181 ± 0.157	549 ± 403	0.00671 ± 0.00519	0.119 ± 0.0259	0.214 ± 0.250	0.135 ± 0.187	$\textbf{72.1} \pm \textbf{34.3}$	140 ± 72.2	BDL	0.718 ± 0.525
Scun	NP	0.230 ± 0.0552	$\textbf{335} \pm \textbf{35.8}$	$\begin{array}{c} 0.00792 \pm \\ 0.00413 \end{array}$	0.150 ± 0.0470	0.278 ± 0.0890	$\begin{array}{c} 0.0255 \pm \\ 0.00346 \end{array}$	$\textbf{73.5} \pm \textbf{11.9}$	129 ± 12.2	BDL	0.600 ± 0.101
Ship	cont	$\textbf{0.546} \pm \textbf{0.0948}$	337 ± 3.71	0.787 ± 0.0366	0.119 ± 0.0555	0.0407 ± 0.0212	0.0314 ± 0.00786	144 ± 4.93	61.9 ± 9.30	0.839 ± 0.284	177 ± 3.71
	NP	$\textbf{0.400} \pm \textbf{0.0501}$	343 ± 9.01	0.521 ± 0.0247	0.210 ± 0.0595	0.0126 ± 0.00593	0.0357 ± 0.00168	146 ± 3.83	111 ± 3.34	0.263 ± 0.288	148 ± 5.95
	cont	0.0666 ± 0.00387	417 ± 14.3	0.00435 ± 0.00125	0.166 ± 0.0266	0.0181 ± 0.00358	1.05 ± 0.0368	51.9 ± 1.31	35.6 ± 2.18	0.145 ± 0.0187	$\begin{array}{c} \textbf{2.04} \pm \\ \textbf{0.0316} \end{array}$
Wis	NP	0.0409 ± 0.00306	424 ± 2.57	0.00292 ± 0.00195	0.137 ± 0.0279	0.00839 ± 0.00388	0.828 ± 0.0336	50.6 ± 1.21	101 ± 3.33	BDL	1.24 ± 0.517
Detection	n Limit	0.0174	0.0324	0.0008	0.0272	0.0062	0.0205	0.0066	0.04	0.0579	0.013

Table 5. Leachate pH and dissolved organic carbon content / mg L⁻¹ in control (cont) and 354

355 nanoparticle (NP)-treated soil leachate. Soil names are as specified in the legend for Table

Soil	Treatment	рН	Dissolved
			organic carbon
Avon	cont	5.32 ± 0.20	9.16 ± 1.73
Avon	NP	$\textbf{5.17} \pm \textbf{0.07}$	$10.0\ \pm 0.375$
Barn	cont	$\textbf{6.94} \pm \textbf{0.40}$	22.1 ± 23.1^{1}
Dam	NP	$\textbf{6.78} \pm \textbf{0.09}$	23.6 ± 24.5^2
Cwm	cont	5.44 ± 0.05	15.5 ± 0.633
Cwill	NP	$\textbf{5.43} \pm \textbf{0.13}$	18.7 ± 0.522
DGC	cont	$\textbf{4.48} \pm \textbf{0.12}$	1.85 ± 0.233
DGC	NP	4.38 ± 0.05	$\textbf{2.66} \pm \textbf{0.206}$
Croig	cont	$\textbf{4.41} \pm \textbf{0.32}$	$\textbf{9.69} \pm \textbf{0.600}$
Graig	NP	$\textbf{4.44} \pm \textbf{0.18}$	10.8 ± 0.510
Red	cont	$\textbf{7.70} \pm \textbf{0.21}$	11.2 ± 0.576
Reu	NP	$\textbf{7.51} \pm \textbf{0.29}$	15.6 ± 2.25
Rook	cont	$\textbf{6.30} \pm \textbf{0.11}$	10.7 ± 0.924
RUUK	NP	5.90 ± 0.06	11.5 ± 0.454
Scun	cont	$\textbf{7.74} \pm \textbf{0.38}$	7.11 ± 3.63
Scuri	NP	$\textbf{7.71} \pm \textbf{0.31}$	$\textbf{7.56} \pm \textbf{2.09}$
Shin	cont	5.79 ± 0.06	$\textbf{30.9} \pm \textbf{2.42}$
Ship	NP	5.53 ± 0.12	$\textbf{30.9} \pm \textbf{5.13}$
W/ie	cont	$\textbf{6.98} \pm \textbf{0.33}$	19.2 ± 6.14
Wis	NP	$\textbf{6.52} \pm \textbf{0.23}$	20.9 ± 6.17

356 4. Values are means \pm standard deviation (n = 3).

 $\frac{1}{1}$ individual values were 48.8, 9.7 and 7.9 mg L⁻¹. The initial value is likely to be an error which would give a mean composition of 8.8 ± 1.3 mg L⁻¹ $\frac{1}{1}$ individual values were 51.9, 10.4 and 8.6 mg L⁻¹. The initial value is likely to be an error which would give a mean composition 357 358 359 360

of 9.5 ± 1.3 mg L⁻¹

The lower concentrations of Mg in the nanoparticle-present treatments seems most likely to be due to adsorption of Mg, despite the relatively low Mg-DTPA complexation stability constants (e.g. Lindsay et al., 979; Dojino, 2017; Liu et al., 2008) and adsorption efficiencies measured in our single metal experiments.

366

367 Extraction efficiencies (Table 6) were calculated for the metals that showed significant

368 reductions in concentration between the controls and the nanoparticle treatments.

369

370 Table 6. Percentage extraction efficiencies from soil solutions by nanoparticles where

371 nanoparticles cause a significant decrease in solution concentration. Values are mean \pm

372 standard deviations (n = 3). Soil names are as specified in the legend for Table 4.

373

Metal Soil	As	Cd	Cu	Pb	Zn
Avon	93 ± 0	23 ± 3.2	87 ± 2.4	97 ± 4.8	18 ± 3.4
Barn	-	62 ± 4.8	-	79 ± 12	-
Cwm	-	-	-	95 ± 0.033	82 ± 13
DGC	37 ± 16	-	97 ± 0.70	-	-
Graig	-	40 ± 6.8	79 ± 6.1	99 ± 0.35	33 ± 9.7
Red	-	-	-	-	91 ± 1.1
Rook	48 ± 6.1	91 ± 8.1	-	-	83 ± 6.2
Scun	-	-	-	-	-
Ship	-	-	-	-	16 ± 3.4
Wis	39 ± 4.6	-	21 ± 3.2	60 ± 0	39 ± 25

374

375 Extraction efficiencies are variable between soils (no significant differences for As, ANOVA 376 on Ranks; significant differences for Cd and Cu between all soils, ANOVA and Holm-Sidak multiple comparisons; between Graig Goch and Wisley for Pb and between Redruth and 377 Shipham for Zn, ANOVA on ranks and Tukey test multiple comparisons) and are similar or 378 379 lower to those obtained from the single metal solutions (Table 2). These results are 380 consistent with previous findings in which extraction efficiencies of metals from mixtures are high and either unaffected or reduced by the presence of multiple metals, presumably due to 381 competition for adsorption sites and preferential adsorption (Zhang et al., 2012; Liu et al., 382 2008; Zhang et al., 2011, Hughes et al., 2017; Shan et al., 2015) with precise trends 383

384 depending on a range of variables including the metal concentration, pH and nanoparticle concentration. Additionally there will be competition for metal binding between the adsorption 385 386 sites on the nanoparticles and complexation sites on the dissolved organic matter present in 387 solution. In our study Zn extraction efficiencies in particular appear to be depressed compared to the typical range (70 - 90%) found in single metal extraction experiments which 388 389 is consistent with our previous findings from mixed Pb-Zn solutions (Hughes et al., 2017). Pb 390 extraction efficiencies remain high except for from the Wisley soil which has a relatively high 391 pH. Reduced Pb extraction at high pH is consistent with our previous findings on the effect of 392 pH on Pb extraction (Hughes et al., 2017). Considering individual replicates rather than mean values the DOC content of the control leachate was in the range 2 – 49 mg L⁻¹ with no 393 394 significant differences (two-way ANOVA, $p \ge 0.05$) between the DOC content of the control and treated leachates. The maximum DOC values are higher than those in previous studies 395 396 (e.g. Zhang et al., 2012; Liu et al., 2008; Shan et al., 2015; Hughes et al., 2017) where extraction efficiencies have been found to remain high but have been reduced by the 397 presence of the DOC. Thus our results indicate that even in the presence of dissolved 398 organic matter, the nanoparticles could be used to remove metals from solution. There were 399 400 insufficient data to perform meaningful multiple regression analysis to determine any controlling variables for extraction efficiency. Correlation analysis between the extraction 401 efficiency of individual metals and the pH, DOC, individual metal concentration and total 402 metal concentration in controls for As, Cd, Cu, Pb and Zn only gave a significant correlation 403 for % Pb extraction and pH (r = -0.89, $p \le 0.05$). 404

405

K_d values were calculated for metals that showed a significant decrease in concentration
between the controls and nanoparticle treatments (Table 7). The K_d for specific metals
largely show no significant differences between soils. The K_d values for individual elements
determined from the soil samples were usually either significantly lower (16 out of 40 values)
or had no significant difference (21 out of 40 values) compared to the K_d values obtained on
single metal solutions at similar pH values. The lower K_d values relative to those obtained

412 from single metal solutions are consistent with the reduced extraction efficiencies observed 413 and again, reflect competition for adsorption sites and competition between adsorption on 414 the nanoparticles and complexation with the dissolved organic matter. Despite the reductions in K_d values, they are still typically > 500 L kg⁻¹ and many are > 5000 L kg⁻¹ 415 416 indicating the potential for the nanoparticles to be used as adsorbents (Fryxell et al., 2005). 417 As with the extraction efficiency data, there were insufficient data to carry out multiple linear regression to determine controlling variables on the K_d values. There were no correlations 418 419 between the K_d for a particular metal and the pH, DOC, individual metal concentration and 420 total metal concentration in the controls. The reduction in K_d values compared to singlemetal solutions and the lack of extraction of some elements from the leachates despite the 421 presence of those elements in solution indicates the importance for more studies such as 422 this one in which real, rather than synthetic, metal-bearing solutions are used to test the 423 424 potential of novel sorbents for remediation.

425

Due to the significant variation between the different soil leachates used in our study in 426 terms of pH, metal concentration, DOC and also the variations between this study and 427 428 others in the literature (again pH, metal concentration, DOC but also the nature of the chelating agent added to the magnetic nanoparticles), together with the paucity of multi-429 element studies using real solutions in the literature it is difficult to make comparisons that 430 431 are other than rather general as above. However, this study further demonstrates the potential for chelating agent functionalised magnetic nanoparticles to remove a range of 432 433 metal contaminants from contaminated solutions and indicates that dissolved organic carbon 434 and relatively high concentrations of non-toxic elements should not necessarily reduce the 435 efficiency of the process.

436

Although not considered in our study, an important consideration in the viability of
adsorbents for metal removal is their potential for reuse. There are various studies in the
literature where solutions including HCl, HNO₃, CH₃COOH, NaOH, EDTA and water are

440 used to desorb metals from sorbents including those that present DTPA, EDTA and other chelating agents at their surface (e.g. Huang et al., 2018; Alizadeh et al., 2018; Ma et al., 441 442 2017; Yuan et al., 2016; Zhao et al., 2015; Liu et al., 2009; Zhang et al., 2011; Yang and Hodson, In press; Kaur et al., 2013; Venkateswarlu and Yoon, 2015, Zhang et al. 2016 (and 443 444 references therein) and thus we are confident that reuse of the DTPA functionalised magnetic nanoparticles should be possible. Whilst that should be confirmed in laboratory studies, 445 more important requirements for future studies are further investigations using "real" rather 446 than synthetic test solutions and also the large scale application of this potential remediation 447 technology. Larger scale trials would address issues concerned with potential mixing of 448 nanoparticles in larger volumes of solution and also removal efficiencies of the nanoparticles 449 when, depending on the design of reactor vessels, the nanoparticles may be further from the 450 451 magnets required to collect the nanoparticles.

452

Table 7. Metal partition coefficients (K_d / L kg⁻¹) for As, Cd, Cu, Pb and Zn extraction by 454 nanoparticles from different soil leachates. Values are means \pm standard error (n = 3). 455 Where solution concentrations were below detection limits these were set at the detection 456 limits for the purposes of calculation. For each element, values with an alphabetic 457 458 superscript in common are not significantly different ($p \ge 0.05$) between soils as assessed by analysis of variance (ANOVA) and Holm Sidak pair wise comparisons (As) or ANOVA on 459 460 higher values than the K_d determined on a single metal solution at the nearest pH below (lo) 461 or above (hi) that of the soil experiment, =lo/hi indicates no significant difference (Analysis of 462 variance and Holm-Sidak pair wise comparisons except for Avon and DGC Cu and Avon, 463 Barn, Graig and Wis Pb which were analysed by ANOVA on ranks and Tukey tests). Soil 464 465 names are as specified in the legend for Table 4.

 Soil	As	Cd	Cu	Pb	Zn
 Avon	12900±0.00ª	308±55.1 ^{a<lo<hi< sup=""></lo<hi<>}	6750±1500 ^{ab>lo=hi}	93500±72200 ^{ab=lo=hi}	227±50.5 ^{ab<lo<hi< sup=""></lo<hi<>}
Barn		1670±313 ^{ab<lo<hi< sup=""></lo<hi<>}		4950±3086 ^{ab=lo=hi}	
Cwm				19400±137 ^{ab=lo=hi}	6680±5230 ^{ab=lo=hi}
DGC	1010±81.7 ^b		57100±27700 ^{a=lo>hi}		
Graig		674±202 ^{ab<lo<hi< sup=""></lo<hi<>}	4140±1390 ^{ab=lo=hi}	233000±128000 ^{a=lo=hi}	511±236 ^{ab<lo<hi< sup=""></lo<hi<>}
Red					10500±1470 ^{a>hi=lo}
Rook	927±230 ^{bc}	16090±10090 ^{b=lo=hi}			5420±2870 ^{ab=lo=hi}
Scun					
Ship					198±47.3 ^{b<lo<hi< sup=""></lo<hi<>}
Wis	633±118°		264±51.7 ^{b<lo<hi< sup=""></lo<hi<>}	$1500{\pm}0^{b=lo=hi}$	852±778 ^{ab<lo<hi< sup=""></lo<hi<>}

466

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476

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