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### Research Article

# **Catalytic Behaviour of Mesoporous Cobalt-Aluminum Oxides for CO Oxidation**

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Ordered mesoporous materials are promising catalyst supports due to their uniform pore size distribution, high specific surface area and pore volume, tunable pore sizes, and long-range ordering of the pore packing. The evaporation-induced self-assembly (EISA) process was applied to synthesize mesoporous mixed oxides, which consist of cobalt ions highly dispersed in an alumina matrix. The characterization of the mesoporous mixed cobalt-aluminum oxides with cobalt loadings in the range from 5 to 15 wt% and calcination temperatures of 673, 973, and 1073 K indicates that  $\mathrm{Co}^{2^+}$  is homogeneously distributed in the mesoporous alumina matrix. As a function of the Co loading, different phases are present comprising poorly crystalline alumina and mixed cobalt aluminum oxides of the spinel type. The mixed cobalt-aluminum oxides were applied as catalysts in CO oxidation and turned out to be highly active.

#### 1. Introduction

Supported metal oxide catalysts have attracted much attention in recent years due to their widespread applicability in industrially and academically important reactions. The extent and nature of the interaction, dispersion, and reducibility of the metal oxides depend on the synthesis method, loading, calcination temperature, and time. Cobalt supported on alumina is a typical catalyst, which is specially important for Fischer-Tropsch synthesis. Conventionally, the preparation of cobalt catalysts is performed by incipient wetness impregnation using suitable cobalt precursors on commercial alumina at low pH. Weak interaction is normally observed between the positively charged alumina carrier and the cobalt cations resulting in relatively large crystallite sizes [1-4]. Continuous efforts have been made in the last few decades by several groups [5-7] to synthesize porous alumina with high surface area by high-temperature dehydration of bulk powders [8], modified sol-gel synthesis in the presence of organic moieties [9, 10], different surfactants [3], block copolymers [11–14], or evaporation-induced self-assembly (EISA) with colloidal precursors and amine structural agents [15, 16]. These materials represent an active support, which may participate positively or negatively in the formation of the final catalysts. Moreover, the methods of hard templating [17] (carbon template) and microwave irradiation [18] in the presence of surfactants have been applied to synthesize alumina materials with crystalline, ordered, and uniform mesopores. However, this process is very time consuming and hardly scalable for industrial applications.

Ordered mesoporous materials are promising catalyst supports due to their favourable structural characteristics [11]. The presence of surface hydroxyl groups offers the opportunity to support metals and metal oxides with catalytic activity. Moreover, due to the large pores they provide less diffusion limitation for the reactants and products. Transition

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aluminas are mainly used as either catalysts or catalyst supports in various industrially relevant processes. Traditional alumina supports are nonporous or show disordered structures with wide pore-size distributions, which makes it difficult to differentiate which pores are involved in the reaction. After the discovery of well-ordered, periodically organized mesoporous silica materials (M41S family, Mobil [19]), extensive efforts have been made to extend the group of mesoporous materials to alumina systems [20].

The evaporation-induced self-assembly (EISA) process is a highly suitable approach to design functional mesoporous oxides with fine-tuned structural, compositional, and morphological properties [21]. The EISA technique can be considered liquid crystal template strategy. In this process, a homogeneous precursor solution is dispersed into fine droplets and subsequently dried and calcined, which results in the formation of mesostructured materials. The present contribution describes an improved synthesis methodology of mesoporous mixed cobalt-aluminum oxides with various cobalt loadings using the EISA process. The materials were thoroughly characterized by nitrogen physisorption, Xray diffraction (XRD), transmission and scanning electron microscopy (TEM, SEM), X-ray photoelectron spectroscopy (XPS), and ultra-high vacuum Fourier transformed infrared spectroscopy (UHV-FTIR) using CO as probe molecule. As a first catalytic test reaction to monitor the redox properties, the mixed metal oxides were applied in CO oxidation.

#### 2. Experimental

2.1. Synthesis. All solvents and chemicals were obtained from Aldrich Chemicals and used as received. The required amounts of cobalt nitrate and 6.0 g of (EO)20(PO)70(EO)20 triblock copolymer (Pluronic P123) were dissolved in 100 mL of ethanol. Additionally, 12 g of aluminium isopropoxide was dissolved in 10 mL of nitric acid (68%) and 100 mL of ethanol. Once dissolved, the two solutions were combined and allowed to stir for 5 h. The obtained materials were dried and calcined at the desired temperatures in a calcination furnace applying a heating rate of 2 K/min and holding the final temperature for 6 h. The obtained catalysts were denoted as xCo–Al<sub>2</sub>O<sub>3</sub>, where x is the Co loading in wt%.

2.2. Characterization. The prepared catalysts and the support were characterized by  $N_2$  physisorption measurements at 77 K using a slightly modified Autosorb 1C setup (Quantachrome). Prior to the measurements, the samples were degassed under vacuum for 2 h at 473 K. The specific surface areas were determined from the adsorption isotherms in the relative pressure  $(p/p_0)$  range from 0.06 to 0.20 applying the BET method. The pore-size distributions (PSDs) were calculated from the nitrogen desorption branch using the Barrett-Joyner-Halenda (BJH) method considering the maximum of the PSD as the average pore size. The pore volume was considered as the volume of liquid nitrogen adsorbed at  $p/p_0 \sim 1$ .

XRD patterns were recorded in the  $2\theta$  range from 0.5 to 5° using D8-Advance-Bruker-AXS diffractometer and 10 to 70° (step width of 0.0308°) with a Panalytical MPD diffractometer

using Cu  $K_{\alpha}$  radiation ( $\lambda=1.5418\,\text{Å}$ ) at 45 kV and 40 mA, 0.58 divergent and antiscatter slits, a 0.2 mm high receiving slit, incident and diffracted beam 0.04 rad soller slits, and a secondary graphite monochromator. Powder diffraction files (PDFs) from the International Centre of Diffraction Data (ICDD) combined with the X'Pert Line software (Panalytical, Almeno) were used for qualitative phase analysis.

TEM analysis was carried out using a Hitachi H-8100 transmission electron microscope ( $200\,\mathrm{kV}$ ,  $\mathrm{LaB}_6$  filament). The samples were prepared by dispersing the powder material in isopropanol and putting a drop of the solution on a carbon-coated Cu grid. SEM measurements of the powder materials were performed with a high-resolution thermally aided field SEM (Zeiss, LEO1530 Gemini).

X-ray photoelectron spectroscopy (XPS) measurements were carried out in an ultra-high vacuum (UHV) setup equipped with a monochromatic Al  $K_{\alpha}$  X-ray source (h $\nu$  = 1486.6 eV) operated at 14.5 kV and 35 mA and a highresolution Gammadata-Scienta SES 2002 analyzer. The base pressure in the measurement chamber was maintained at about  $7 \times 10^{-10}$  mbar. The measurements were carried out in the fixed transmission mode with a pass energy of 200 eV resulting in an overall energy resolution better than 0.5 eV. A flood gun was applied to compensate the charging effects. High-resolution C 1s, O 1s, Al 2p, and Co 2p spectra were recorded. The binding energy scales were recalibrated based on the C 1s line from adventitious hydrocarbons at 284.8 eV. The Casa XPS software [22] with a 70:30 Gaussian-Lorentzian product function and Shirley background subtraction was used for peak deconvolution. The Co 2p spectra were normalized to the corresponding Al 2p peak areas for better comparison.

In addition, the interaction of CO with Al<sub>2</sub>O<sub>3</sub> and Co-Al<sub>2</sub>O<sub>3</sub> nanoparticles was investigated employing UHV-FTIR spectroscopy. CO was used to probe the comparable substrates in order to get more information on the local structure of CO adsorbed on Al<sub>2</sub>O<sub>3</sub> and Co-Al<sub>2</sub>O<sub>3</sub> surfaces using a novel UHV apparatus combining a state-of-the-art vacuum IR spectrometer (Bruker, VERTEX 80v) with an UHV system (Prevac) [23, 24]. Pure alumina and mixed Co-Al oxide powder samples were first pressed on a goldcoated stainless steel grid and then mounted on a sample holder that was specially designed for the FTIR transmission measurements under UHV conditions. The base pressure in the measurement chamber was  $2 \times 10^{-10}$  mbar. The optical path inside the IR spectrometer and the space between the spectrometer and UHV chamber were also evacuated to avoid atmospheric moisture adsorption resulting in high sensitivity and stability. The samples were cleaned in the UHV chamber by heating to 850 K in order to remove adsorbed species (e.g., carbonate and hydroxyl groups) [24]. Prior to each exposure, the spectrum of clean powder was used as a background reference. All UHV-FTIR spectra were collected with 1024 scans at a resolution of 4 cm<sup>-1</sup> in the transmission mode.

2.3. Catalytic Testing. CO oxidation was performed in a glass-lined fixed-bed microreactor with an inner diameter of 4 mm coupled to a gas supply equipped with mass-flow controllers. Gases were obtained by Air Liquide with the

Sample	Surface area/m <sup>2</sup> g <sup>-1</sup>	Pore diameter/nm	Pore volume/cm <sup>3</sup> g <sup>-1</sup>
$Al_2O_3$	300	6.8	0.70
5Co/Al <sub>2</sub> O <sub>3</sub> (973)	287	8.8	0.82
10Co/Al <sub>2</sub> O <sub>3</sub> (973)	258	7.7	0.74
15Co/Al <sub>2</sub> O <sub>3</sub> (973)	258	5.6	0.66
5Co/Al <sub>2</sub> O <sub>3</sub> (673)	275	8.8	0.78
5Co/Al <sub>2</sub> O <sub>3</sub> (1073)	284	6.6	0.62

TABLE 1: N<sub>2</sub> physisorption results obtained with the Co–Al<sub>2</sub>O<sub>3</sub> oxides.

xCo-Al<sub>2</sub>O<sub>3</sub> (y) = cobalt loading (wt%) in Al<sub>2</sub>O<sub>3</sub> (calcination temperature, K).

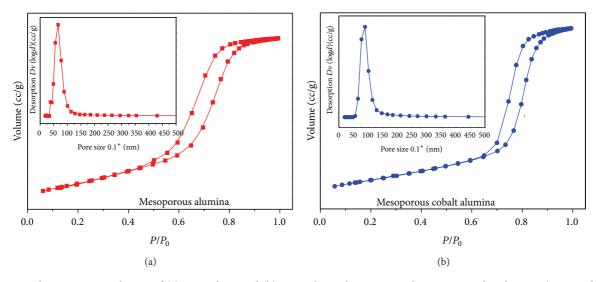


FIGURE 1:  $N_2$  physisorption isotherms of (a) pure  $Al_2O_3$  and (b)  $5Co-Al_2O_3$ ; the corresponding pore size distributions (BJH method) are shown in the insets.

following purities: 1.97%  $\rm H_2$  (99.9999%) in He (99.9999%), 1% CO (99.997%), and 20%  $\rm O_2$  (99.995%) in He (99.9999%), as well as pure He (99.9999%). The reactor was filled with 100 mg of the samples in the sieve fraction of 250–350  $\mu$ m. Prior to the reaction, the catalysts were reduced with 1.97%  $\rm H_2$  at 573 K. After cooling to room temperature, a flow of 1% CO and 20%  $\rm O_2$  in He was applied (55 Nml min<sup>-1</sup>) increasing the temperature with 5 K min<sup>-1</sup> up to 573 K. The concentrations of CO and CO<sub>2</sub> at the gas outlet were continuously detected by a nondispersive infrared analyzer, while the  $\rm O_2$  concentration was measured with a paramagnetic sensor analyzer (X-STREAM, Emerson).

#### 3. Results and Discussion

The obtained mixed oxides were investigated by  $N_2$  physisorption. The resulting isotherms for the  $Al_2O_3$  and the mesoporous  $Co-Al_2O_3$  oxides were found to be type IV isotherms with H1 hysteresis loop with a sharp increase in the amount of nitrogen adsorbed at a relative pressure  $(p/p_0)$  of about 0.6–0.9. The shape of the isotherm confirms the mesoporosity of  $Al_2O_3$  (Figure 1(a)) [11]. Moreover, even after the addition of cobalt (Figure 1(b)) the textural properties of  $Al_2O_3$  were maintained. The pure  $Al_2O_3$  sample

exhibited a maximum pore diameter of about 6.8 nm and a specific surface area of  $300 \, \text{m}^2 \, \text{g}^{-1}$  (Table 1). Adding more cobalt during the synthesis changed the pore size from 8.8 to 5.6 nm. The decrease in pore size could be due to formation cobalt oxide in the pores in case of higher loading and led to a slight decrease of the specific surface area.

The TEM images of the mixed  $Co-Al_2O_3$  samples (Figure 2) also provide strong evidence that the hexagonally ordered mesoporous structure of  $Al_2O_3$  is maintained. The pore diameters estimated from the micrographs were found to be 8-9 nm, which is in good agreement with the physisorption results.

The bulk structure of the  $\text{Co-Al}_2\text{O}_3$  samples was investigated by powder X-ray diffraction. The low angle XRD measurements (Figure 3) reveal a peak in the range between 0.5 and 5° which is in good agreement with the TEM image of the hexagonally ordered material. The XRD patterns show the presence of X-ray amorphous alumina and the formation of a crystalline spinel phase in the samples with higher Co loadings (Figure 4(a)) and higher calcination temperatures (Figure 4(b)), which is in good agreement with the results reported in the literature [25]. It is not possible to differentiate between  $\text{Co}_3\text{O}_4$  and a mixed  $\text{CoAl}_2\text{O}_4$  phase, because both phases crystallize in the cubic spinel structure (*Fd3m*) and the ionic radii of  $\text{Co}^{3+}$  and  $\text{Al}^{3+}$  are nearly of the same value.

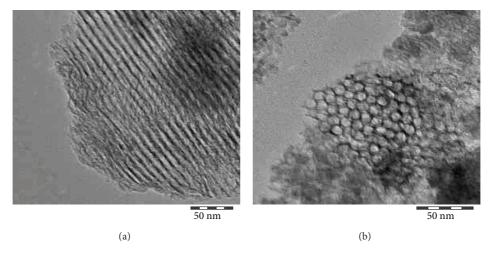


FIGURE 2: TEM images of the 5Co-Al<sub>2</sub>O<sub>3</sub> oxide calcined at 973 K.

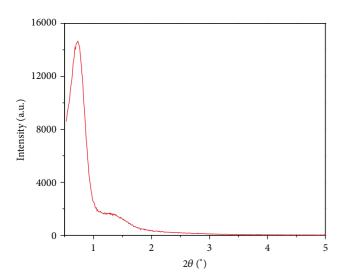


FIGURE 3: Low angle XRD of the 5Co-Al<sub>2</sub>O<sub>3</sub> oxide calcined at 973 K.

The morphology of the materials was further investigated by means of SEM. The micrograph of one  $Co-Al_2O_3$  sample is shown in Figure 5(a). It indicates that the mixed  $Co-Al_2O_3$  oxides consist of irregularly shaped agglomerates exhibiting a sponge-like structure. The homogeneous distribution of Co inside the alumina matrix is demonstrated by elemental mapping (Figure 5(b)).

Samples with different Co loadings and different calcination temperatures were analyzed by means of XPS. The Co 2p spectra of three mixed oxides with different Co loadings (5, 10, and 15 wt%) calcined ex situ at 973 K are shown in Figure 6. All spectra exhibit the same features consisting of the two main Co  $2p_{3/2}$  and  $2p_{1/2}$  peaks and two pronounced satellites at their high-energy side designated as sat1 and sat2. It is known that the occurrence of satellites is related to the shake-up process of  $Co^{2+}$  ions in a high-spin configuration, which is the case for  $Co-Al_2O_3$  [26]. The analysis of the peak energies results in a shake-up splitting of 4.9 eV for sat1 and a  $Co 2p_{3/2}$  binding energy of 781.4 eV that is in good agreement

Table 2: XPS-derived surface compositions (atom%) of the Co-Al<sub>2</sub>O<sub>3</sub> oxides.

Sample	Co/at%	Al/at%	sat1/Co 2p <sub>3/2</sub> *
5Co/Al <sub>2</sub> O <sub>3</sub> (973)	0.5	41.8	0.9
10Co/Al <sub>2</sub> O <sub>3</sub> (973)	0.9	43.1	0.8
15Co/Al <sub>2</sub> O <sub>3</sub> (973)	1.0	42.3	0.7

xCo/Al<sub>2</sub>O<sub>3</sub> (y) = cobalt loading (wt%) on Al<sub>2</sub>O<sub>3</sub> (calcination temperature,

with those reported for Co in the  $\mathrm{CoAl_2O_4}$  spinel structure [22, 26]. The surface concentrations in at% are summarized in Table 2.

Figure 7 shows the Co surface atomic concentration (left axis) and the sat1/Co  $2p_{3/2}$  area ratio (right axis) as a function of the Co loading. Comparing the atomic surface concentrations of Co with the respective sat1/Co  $2p_{3/2}$  area ratios, opposite trends are observed as a function of the Co loading. When the bulk Co loading is increasing from 5 to 10 wt%, the total Co atomic surface concentration increases from 0.50% to 0.94% indicating that the surface atomic concentration changes at about the same proportion as the bulk concentration. However, further addition of Co does not change the surface composition. Increasing the Co loading enhances the formation tendency of the pure cobalt oxide phase Co<sub>3</sub>O<sub>4</sub>, which has weak satellite peaks. This oxide with spinel structure is a mixture of two different Co oxidation states with one Co<sup>2+</sup> ion in a tetrahedral site and two Co<sup>3+</sup> ions in octahedral sites. While the former one is in a highspin state, the second is in a low-spin state and does not lead to a shake-up process [26]. When the XPS area ratio of sat1 to Co  $2p_{3/2}$  is analysed as a function of the Co loading, indeed a decreasing trend is observed. According to these results, it is not possible to rule out the existence of a small amount of Co in the form of  $Co_3O_4$  in the  $Co-Al_2O_3$  samples with high Co loading.

The UHV-FTIR spectra recorded after CO adsorption on the  $5\text{Co-Al}_2\text{O}_3$  sample at 100 K are presented in Figure 8.

<sup>\*</sup>Area ratios from the Co 2p region spectra.

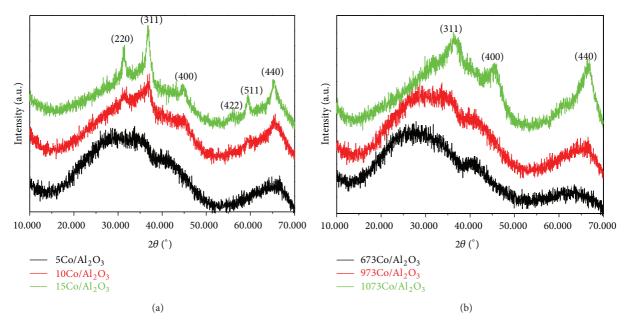


Figure 4: XRD patterns of the Co–Al $_2$ O $_3$  oxides with (a) different cobalt loadings: (A) 5 wt%, (B) 10 wt%, (C) 15 wt%, and (b) different calcination temperatures: (A) 673 K, (B) 973 K, and (C) 1073 K. The reflections originate from the spinel structure.

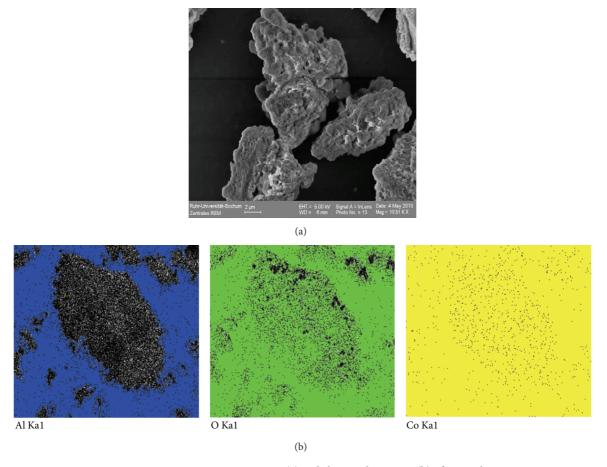


Figure 5: Representative SEM images (a) and elemental mapping (b) of  $5\text{Co-Al}_2\text{O}_3$ .

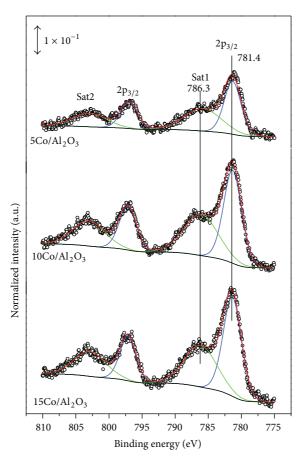


FIGURE 6: Co 2p XP spectra of the  $Co_xO_y/Al_2O_3$  composites with different Co loadings calcined at 973 K: (A) 5 wt% Co, (B) 10 wt% Co, and (C) 15 wt% Co.

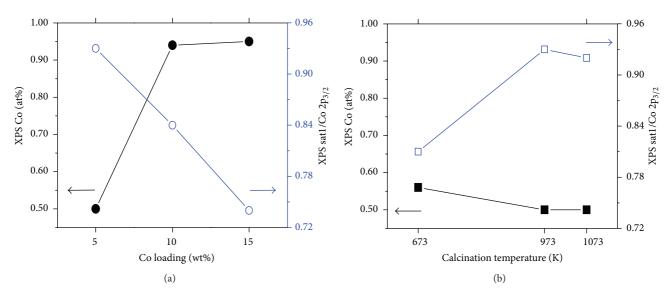


Figure 7: XPS Co atomic concentration (filled circles) and sat1/Co  $2p_{3/2}$  ratio (open circles) of mixed Co–Al<sub>2</sub>O<sub>3</sub> oxides calcined at 973 K with different Co loadings.

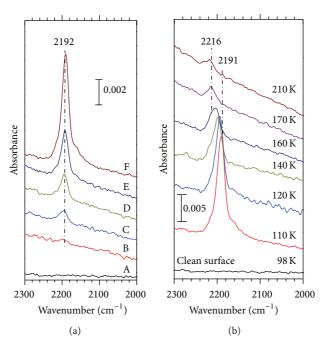


FIGURE 8: UHV-FTIR spectra obtained after exposing the clean  $\mathrm{Co_xO_y/Al_2O_3}$  composite to different doses of CO at 100 K in an UHV chamber; (a) (A) clean surface, (B)  $5 \times 10^{-7}$  mbar, (C)  $1 \times 10^{-6}$  mbar, (D)  $5 \times 10^{-6}$  mbar, (E)  $1 \times 10^{-5}$  mbar, (F)  $5 \times 10^{-5}$  mbar, and (G)  $1 \times 10^{-4}$  mbar CO; (b) further heating to the indicated temperatures under UHV.

In order to obtain a clean and adsorbate-free surface the sample was pretreated in UHV at 850 K (Figure 8(a)). After exposing the clean sample to CO at 100 K, a broad single CO stretching band is observed at  $2176\,\mathrm{cm}^{-1}$ , which is asymmetric to higher wavenumbers. This band appears at higher wavenumbers compared with the corresponding gas phase CO band ( $2143\,\mathrm{cm}^{-1}$ ), which is characteristic for CO adsorption on oxide surfaces. The interaction of CO with  $5\mathrm{Co}-\mathrm{Al_2O_3}$  was further investigated by varying the temperature. Figure 7(b) shows the UHV-FTIR spectra recorded after exposing the clean  $\mathrm{Co}-\mathrm{Al_2O_3}$  sample to CO at 100 K followed by subsequent heating. With increasing temperature the intensity of the CO band at  $2176\,\mathrm{cm}^{-1}$  decreases markedly and almost disappears at around  $240\,\mathrm{K}$ .

In order to identify the influence of the cobalt ions on CO adsorption, further UHV-FTIR experiments were carried out for a pure mesoporous Al<sub>2</sub>O<sub>3</sub> sample (Figure 9). After exposing the clean mesoporous Al<sub>2</sub>O<sub>3</sub> sample to CO at 110 K, a single CO stretching band appears at 2192 cm<sup>-1</sup>. This band is assigned to a CO species bound to the Al<sup>3+</sup> cations of the mesoporous Al<sub>2</sub>O<sub>3</sub> surface. Figure 8(b) shows the UHV-FTIR spectra recorded after the sample was heated subsequently to higher temperatures. Upon heating, the intensity of the CO band at 2192 cm<sup>-1</sup> decreases until the band completely disappears at around 210 K. Simultaneously, the band shifts slightly to higher frequencies. The blue shift of the CO band on mesoporous Al<sub>2</sub>O<sub>3</sub> is related to the decrease of CO coverage at higher temperatures, which is in line with the results for CO adsorption on other oxide surfaces such as ZnO [27].

In general, the blue shift of the CO band on both pure mesoporous  ${\rm Al_2O_3}$  and  ${\rm Co-Al_2O_3}$  with respect to the gas phase value can be explained by both the Stark effect and  $5\sigma$  donation from CO to the surface cations [23–31]. Importantly, for both the mesoporous  ${\rm Al_2O_3}$  and the  $5{\rm Co-Al_2O_3}$  sample only one dominating CO band was identified. In comparison to the band at 2192 cm<sup>-1</sup> for pure alumina, the band observed for  $5{\rm Co-Al_2O_3}$  at 2176 cm<sup>-1</sup> is clearly shifted. These findings provide further spectroscopic evidence for the incorporation of the  ${\rm Co^{2^+}}$  ions into  ${\rm Al_2O_3}$  during the synthesis instead of a mixture of separated Co and Al oxides.

In previous studies, UHV-FTIR has been used to monitor the coadsorption of CO and CO<sub>2</sub> on ZnO nanoparticles [32]. It was found that the preadsorption of CO<sub>2</sub> leads to a slight blue shift of the C-O vibrational band. This shift originates from the formation of tridentate carbonate species on the nonpolar ZnO(10-10) surface, which increases the Lewis acidity of neighboring Zn<sup>2+</sup> cations and shifts the CO band to higher wavenumbers [27]. The reverse scenario was observed for the Co-Al<sub>2</sub>O<sub>3</sub> samples. The presence of Co<sup>2+</sup> ions in the Al<sub>2</sub>O<sub>3</sub> structure led to a decrease of the Lewis acidity of the neighboring Al<sup>3+</sup> cations resulting in a decrease of the C-O stretching band for the mixed Co-Al<sub>2</sub>O<sub>3</sub> oxide compared with pure alumina. In addition, the observation of a significantly broader CO band on Co-Al<sub>2</sub>O<sub>3</sub> also implies the adsorption of CO molecules on different cationic sites. Further investigations are in progress to gain deeper insight into the interaction of CO with Co-Al<sub>2</sub>O<sub>3</sub>.

There are ample examples that have been found in current literature for application of mixed oxide for CO oxidation. The catalytic redox performance was investigated by applying

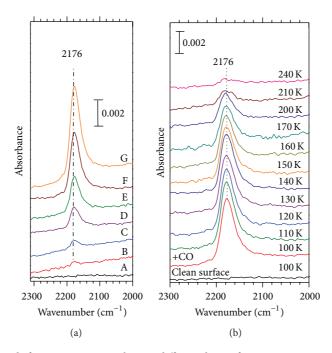


FIGURE 9: UHV-FTIR spectra obtained after exposing pure  $Al_2O_3$  to different doses of CO at 110 K in an UHV chamber; (a) (A) clean surface, (B)  $1 \times 10^{-6}$  mbar, (C)  $5 \times 10^{-6}$  mbar, (D)  $1 \times 10^{-5}$  mbar, (E)  $5 \times 10^{-5}$  mbar, and (F)  $1 \times 10^{-4}$  mbar CO; (b) further heating to the indicated temperatures under UHV.

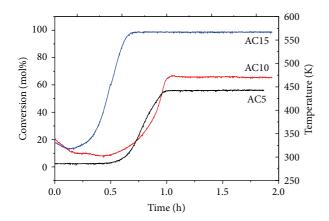


FIGURE 10: CO oxidation over the  $\text{Co-Al}_2\text{O}_3$  composites calcined at 973 K as a function of the Co loading.

the mesoporous mixed oxides in CO oxidation. The results are shown in Figure 10. Prior to reaction, the samples were reduced in 2% H<sub>2</sub> at 573 K. It is evident from the results that all the samples exhibited good CO oxidation activity, which strongly increases with increasing Co loadings. The sample 15Co–Al<sub>2</sub>O<sub>3</sub> reaches full conversion already at about 450 K. At 573 K, the degree of conversion of the catalysts remains stable for 1h time on stream. Cao et al. reported copper catalyst supported by ceria-zirconia and iron. The most active catalyst they observed 25% of CuO on ceria-zirconia and 15–20% of CuO on iron support [27, 32]; moreover, the report demonstrates that both the supports are active for CO oxidation without copper. We are using nearly an inert support alumina compared with highly active

not only used as support but also used catalyst phase  $Fe_2O_3$  and  $Ce0.8Zr0.2O_2$ . Moreover, we are using low amount of cobalt 5–15% age compared with 20–30% age of copper. These results demonstrate that EISA is a promising synthetic approach for catalytic applications.

#### 4. Conclusions

A simple and reproducible synthesis of mesoporous mixed cobalt aluminum oxides with well-ordered pore structure in a single-step approach has been successfully demonstrated for Co contents in the range from 5 to 15 wt%. The cobalt ions were found to be homogeneously dispersed in a poorly crystalline  $Al_2O_3$  matrix. The surface areas and the TEM results reflect the well-ordered mesoporosity of the mixed  $Co-Al_2O_3$  oxides. XPS and UHV-FTIR CO adsorption studies reveal the presence of  $CoAl_2O_4$ -like surface species for samples with low Co loading. The red shift of the CO band relative to pure  $Al_2O_3$  indicates a decrease of the surface Lewis acidity due to the presence of the  $Co^{2+}$  cations. The catalytic CO oxidation activity was found to increase with the Co loading. For the catalyst with a Co loading of 15 wt%, 50% CO conversion was reached at 429 K.

#### **Conflict of Interests**

The authors declare that there is no conflict of interests regarding the publication of this paper.

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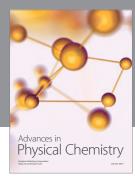
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