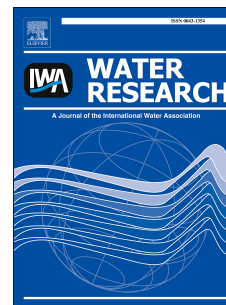


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Petroleomic analysis of the treatment of naphthenic organics in oil sands process-affected water with buoyant photocatalysts

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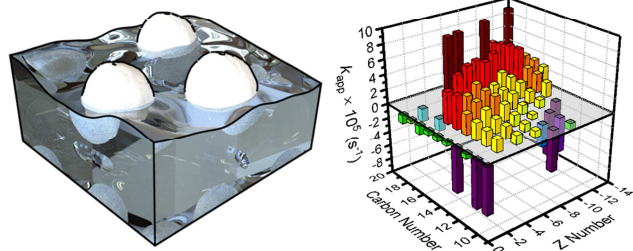
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Passive water treatment → Petroleomic-level kinetics



1 Petroleomic analysis of the treatment of
 2 naphthenic organics in oil sands process-
 3 affected water with buoyant photocatalysts

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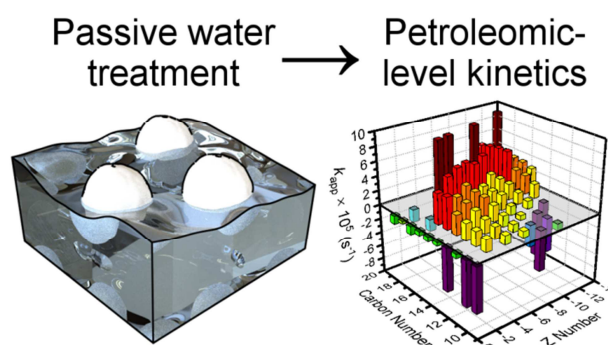
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11 Abstract

12 The persistence of toxicity associated with
 13 the soluble naphthenic organic compounds
 14 (NOCs) of oil sands process-affected water
 15 (OSPW) implies that a treatment solution
 16 may be necessary to enable safe return of
 17 this water to the environment. Due to recent advances in high-resolution mass spectrometry



18 (HRMS), the majority of the toxicity of OSPW is currently understood to derive from a subset of
19 toxic classes, comprising only a minority of the total NOCs. Herein, oxidative treatment of
20 OSPW with buoyant photocatalysts was evaluated under a petroleomics paradigm: chemical
21 changes across acid-, base- and neutral-extractable organic fractions were tracked throughout
22 the treatment with both positive and negative ion mode electrospray ionization (ESI) Orbitrap
23 MS. Elimination of detected OS^+ and NO^+ classes of concern in the earliest stages of the
24 treatment, along with preferential degradation of high carbon-numbered O_2^- acids, suggest that
25 photocatalysis may detoxify OSPW with higher efficiency than previously thought. Application
26 of petroleomic level analysis offers unprecedented insights into the treatment of petroleum
27 impacted water, allowing reaction trends to be followed across multiple fractions and
28 thousands of compounds simultaneously.

29 Keywords

30 naphthenic acid; titanium dioxide; floating; passive; positive ion; advanced oxidation process

31 Highlights

- 32 • Oil sands process-affected water (OSPW) is impacted by naphthenic organic compounds
33 (NOCs)
- 34 • Majority of OSPW toxicity attributed to only a subset of NOC classes
- 35 • Passive treatment of OSPW demonstrated with buoyant photocatalysts
- 36 • First time petroleomics used to study treatment kinetics across NOC fractions
- 37 • Preferential degradation of priority O_2^- , OS^+ and NO^+ NOC classes of concern

38 List of Acronyms

AEO	Acid extractable organics
AOP	Advanced oxidation process
BEO	Base extractable organics
BPCs	Buoyant photocatalysts
ESI	Electrospray ionization
ESI(-) MS	Negative ion mode ESI mass spectrometry
ESI(+) MS	Positive ion mode ESI mass spectrometry
HGMs	Hollow glass microspheres
HRMS	High resolution mass spectrometry
NAs	Naphthenic acids, of the general formula $C_cH_{2c+z}O_2$
NEO	Neutral extractable organics
NOCOCs	Naphthenic organic classes of concern
NOCs	Naphthenic organic compounds, of general formula $C_cH_{2c+z}N_nO_oS_s$
OSPW	Oil sands process-affected water
PC	Photocatalysis
WET	Whole effluent toxicity

39 Introduction

40 The Clark process used for extraction of bitumen in Canada's oil sands generates large volumes
41 of water as a by-product, referred to as oil sands process-affected water (OSPW), which is
42 stored on site in tailings ponds for water recycling. The oil sands mining companies are

43 obligated to eventually return this water to the environment (Martin, 2015; *Lower Athabasca*
44 *Region - Tailings Management Framework for the Mineable Athabasca Oil Sands*, 2015,
45 *Directive 085: Fluid Tailings Management for Oil Sands Mining Projects*, 2017). Currently,
46 however, they are operating on a zero-discharge policy, due in part to the water's toxicity,
47 which is primarily attributed to dissolved bitumen-derived organics.(Verbeek et al., 1994;
48 Hughes et al., 2017b; Brown and Ulrich, 2015; McQueen et al., 2017b) Fractions of these
49 organics are highly persistent,(Han et al., 2009; Quagraine et al., 2005) and remain potentially
50 toxic even after decades of aging.(Marentette et al., 2015) Thus treatment of OSPW may be
51 required to enable safe discharge, and the industry is currently exploring passive remediation
52 solutions.(“COSIA Challenge #0014: Passive Organics Treatment Technology,” 2015)

53 In the past, the organic constituents of OSPW were thought to simply comprise naphthenic
54 acids (NAs), of the classical formula $C_cH_{2c+z}O_2$, where Z indicates hydrogen deficiency from rings
55 or double bonds.(Clemente and Fedorak, 2005) However, with the advance of analytical
56 capabilities such as high-resolution mass spectrometry (HRMS), far more complexity has been
57 revealed (Barrow et al., 2015, 2010; Grewer et al., 2010). OSPW is now understood to contain
58 not only these conventional NAs, but also oxidized and heteroatomic classes,(Barrow et al.,
59 2014) and non-acid neutral and basic species,(Barrow et al., 2016) referred to collectively
60 herein as naphthenic organic compounds (NOCs, of general formula $C_cH_{2c+z}N_nO_oS_s$). While
61 classic NAs are known toxicants,(Hughes et al., 2017b) recent effects-directed analyses have
62 also shown these base-neutral organics contribute significantly to the toxicity of
63 OSPW,(Morandi et al., 2017, 2015) and may also be implicated in its endocrine disruptive
64 effects.(Rowland et al., 2011; Pereira et al., 2013) With the petroleomic level insights afforded

65 by such rich HRMS datasets,(Marshall and Rodgers, 2008; McKenna et al., 2013) it has even
66 been proposed recently that the whole effluent toxicity (WET) of OSPW may be predictable
67 simply through mass spectral analysis.(Morandi et al., 2016)

68 While many of these analytical advances have been driven by the goals of environmental
69 forensics,(Frank et al., 2014; Headley et al., 2013, 2011; C. Sun et al., 2017) it is important for
70 water treatment technologies to keep pace with the scientific progress and be evaluated with
71 the same analytical rigor, to provide validated remediation tools for emergent environmental
72 priorities. In terms of technologies studied for OSPW treatment, solar photocatalysis (PC) has
73 been shown to be particularly effective at eliminating NAs,(Headley et al., 2009; Leshuk et al.,
74 2016b, 2016a; Liu et al., 2016; McQueen et al., 2017a) and may be the only advanced oxidative
75 process (AOP) with the potential for deployment in passive treatment systems, given the vast
76 sunlight-exposed surface area of tailings ponds. However, the capacity of PC to treat base-
77 neutral fraction NOCs has not been previously studied.

78 The objective of this work was to evaluate the performance of buoyant photocatalysts (BPCs) to
79 degrade NOCs in OSPW, while tracking chemical changes across acid-, base- and neutral-
80 extractable organic fractions with HRMS. Through combining pH fractionation with both
81 positive and negative ion mode MS, we aimed to gain an unprecedented petroleomic
82 perspective of the PC treatment of OSPW, by following molecular transformations across
83 thousands of species simultaneously. While the photochemistry of petroleum has long been
84 studied with low mass resolution techniques (Payne and Phillips, 1985; Shankar et al., 2015;
85 Ziolli and Jardim, 2003; D'Auria et al., 2009; García-Martínez et al., 2006), and recently with FT-
86 ICR MS (Griffiths et al., 2014), this is the first time PC, as a water treatment method, has been

87 studied through the lens of petroleomics, not only capturing a more holistic picture of the
88 chemical changes occurring during NOC oxidation, but also exposing new insights into
89 treatment of emerging naphthenic organic classes of concern (NOCOCs). As not all OSPW
90 organics are equally toxic, (Hughes et al., 2017b; Morandi et al., 2015) tracking elimination of
91 specific NOCOCs in a complex mixture, rather than simply measuring reduction of bulk organic
92 metrics, may represent a new standard for evaluating treatment solutions for petroleum
93 impacted waters.

94 Experimental

95 Materials

96 OSPW was provided by an industrial producer operating in the Athabasca oil sands, and stored
97 in sealed polyethylene containers in the dark at 4 °C for 16 weeks prior to testing. The OSPW
98 was homogenized by stirring before each use, and then centrifuged (14,000 xg) or filtered
99 (Whatman 934-AH glass fiber filter) to remove suspended solids, depending on test volume
100 requirements.

101 A commercial mixture of naphthenic acids (technical grade, carbon numbers 6 – 20, Z numbers
102 0 to -4, as characterized by Damasceno et al. (Damasceno et al., 2014)), dichloromethane (DCM,
103 ≥99.9%, HPLC grade), NH₄OH (28-30%, ACS grade), HNO₃ (70%, ACS grade), HCl (37%, ACS
104 grade) tetraethylorthosilicate (TEOS, 98%) and Pluronic F127 were purchased from Sigma-
105 Aldrich and used as received. Sulfuric acid (95-98%, ACS grade, Fisher), ethanol (EtOH, ACS
106 grade) and TiO₂ nanoparticles (Aeroxide P25, ~10-50 nm particle diameter, 55 m² g⁻¹ surface
107 area, Acros) were used as received. Hollow glass microspheres (HGMs, 3M iM30k, soda-lime-

108 borosilicate glass, ~10-30 μm diameter, 0.6 g/cm^3 density) were washed by 1 mol/L HNO_3 or
109 H_2SO_4 before use (at 125 g/L microspheres), 3-5 times with deionized (DI) water by flotation,
110 then dried at 120 $^\circ\text{C}$ in air.

111 Buoyant photocatalyst (BPC) synthesis

112 A silica sol-gel solution was prepared as previously.(Allain et al., 2007) Briefly, an acidic
113 ethanolic TEOS solution of molar ratio TEOS:EtOH:H₂O:HCl = 1:4:10:0.01 was hydrolysed at 60
114 $^\circ\text{C}$ for 1 h, and then cooled to room temperature before use. TiO_2 nanoparticles and Pluronic
115 F127 were then dispersed into DI H₂O by probe sonication, after which silica sol-gel solution
116 and 1 mol/L HNO_3 were added to achieve a molar ratio of Ti:Si:F127 = 1:1:0.01, 0.1 mol/L HNO_3 ,
117 and 25 g/L TiO_2 . This TiO_2 suspension was then added to HGM powder at a 2:1 volume:mass
118 ratio, and dried at room temperature for ≥ 24 h. The dried cake was then crushed to a powder,
119 calcined for 6 h at 400 $^\circ\text{C}$ in air to remove the polymeric templates, and then washed with DI
120 H₂O by flotation and dried. Particle morphology was analyzed by SEM (Zeiss Merlin FESEM).

121 Photocatalytic experiments

122 Photocatalytic experiments were performed in a custom photoreactor enclosure, consisting of
123 an array of UVA fluorescent bulbs (Philips F20T12/BL, peak emission ~350 nm) suspended
124 above the samples.(Leshuk et al., 2016a) The UV intensity was measured to be ~36 W/m^2 with a
125 UVA/B light meter (Sper Scientific, NIST certified calibration), which is similar to the UV content
126 of the solar spectrum (46.6 W/m^2 , ASTM G173-03 global tilt). Our previous work demonstrated
127 equivalent photocatalytic treatment rate of OSPW in this photoreactor as under natural
128 sunlight (Leshuk et al., 2016b, 2016a).

129 For the principal treatment study (Figure 2-Figure 5), BPCs were added at 300 g/m^2 ($\approx 13.8 \text{ g/m}^2$
130 TiO_2) to 1 L of OSPW in a borosilicate glass beaker (11 cm I.D., sides wrapped with Al foil), which
131 was sealed with UV-transparent polyethylene film. Beakers were equilibrated in the dark for 1
132 h, then placed in the photoreactor and exposed to UV light while stirring at 300 rpm (PTFE
133 coated stir bar, $3.81 \times 0.95 \text{ cm l} \times \text{d}$), with periodically sampling (1 mL for UV_{220}) and addition of
134 DI H_2O (Millipore, $\geq 15 \text{ M}\Omega\cdot\text{cm}$) to correct for evaporation losses. Beaker temperatures
135 equilibrated at $\sim 23 \text{ }^\circ\text{C}$ during the exposure. Following the UV treatment, the OSPW mixture was
136 vacuum filtered (Whatman 934-AH glass fiber filter) to remove BPC particles, and the filtrate
137 retained for analysis (stored at $4 \text{ }^\circ\text{C}$ in the dark for $< 24 \text{ h}$ before extraction).

138 Preliminary experiments on the effect of depth, mixing intensity, catalyst concentration and
139 recyclability (Figure S2-Figure S5) were conducted in 500 mL PTFE beakers (7.2 cm I.D.) at a UV
140 intensity of $\sim 26 \text{ W/m}^2$, with typical levels (i.e., held constant when varying the other factors) of
141 125 g/m^2 ($\approx 5.8 \text{ g/m}^2 \text{ TiO}_2$) for BPC coverage, 300 mL OSPW, and 130 rpm stirring, with kinetics
142 measured by UV_{220} . OSPW UV absorbance has been previously shown to correlate with NOC
143 concentration (Mohamed et al., 2008), and 220 nm was monitored in this work as it provided
144 the highest signal-to-noise ratio. Depth was varied by testing different volumes of OSPW in the
145 same beakers. For the recyclability study, between UV exposures BPCs were separated by
146 flotation, rinsed thrice with DI H_2O , then added to fresh OSPW for another treatment cycle.

147 Liquid-liquid extraction (pH fractionation)

148 For organics extraction, 200 mL OSPW was adjusted with H_2SO_4 to either pH 2.0 (to ensure
149 protonation of carboxylic acids) for acid-extractable organics (AEO), or $\text{pH } 7.0 \pm 0.1$ for neutral-

150 extractable organics (NEO), or with NH_4OH to pH 10.5 for base-extractable organics (BEO), then
151 extracted with 100 mL DCM (40, 40, and 20 mL sequentially), after which the extract was dried
152 under N_2 . NEO and BEO were collected to investigate NOCs that may not be extractable under
153 acidic conditions thereby not appear in typical AEO analyses.

154 For total extractable organics (total EO), 400 mL OSPW was first adjusted to pH 10.5 with
155 NH_4OH and extracted with 100 mL DCM, then to pH 7.0 ± 0.1 with H_2SO_4 and again extracted
156 with 100 mL DCM, then to pH 2.0 with H_2SO_4 and again extracted with 100 mL DCM, after
157 which the extracts were combined and dried under N_2 . This extract was used to gravimetrically
158 prepare a standard curve for UV_{220} (Figure S1), and from the absorbance of OSPW prior to
159 extraction, extraction efficiency was determined to be 49.1%, based on extract mass.

160 Analysis

161 AEO_{FTIR} was measured by Fourier transform infrared spectroscopy (FTIR) according to the
162 standard method (Holowenko et al., 2001; Jivraj et al., 1995) with minor modifications (*viz.*, the
163 acidified samples were extracted thrice with DCM in a 1:12.5 solvent:sample volumetric ratio,
164 with $80 \pm 4\%$ total recovery), using the commercial NA mixture to prepare the calibration curve.
165 UV absorbance at 220 nm (UV_{220}) was measured with a spectrophotometer (BioTek
166 Epoch). (Mohamed et al., 2008) Chemical oxygen demand (COD) was measured with a test kit
167 (Hach, APHA 5220D). Total organic carbon (TOC, APHA 5310B), biochemical oxygen demand
168 (BOD, APHA 5210B), anion concentration by ion chromatography (EPA 300.1), alkalinity (as
169 CaCO_3 , EPA 310.2), and dissolved metals by inductively coupled plasma mass spectrometry
170 (ICPMS, APHA 3030B/6020A) were measured according to standard methods by ALS

171 Environmental (Waterloo, ON, Canada), a laboratory accredited by the Canadian Association for
172 Laboratory Accreditation (CALA) according to international standards (ISO 17025).

173 HRMS Analysis

174 Dried extracts from the pH fractionation liquid-liquid extractions as described above (AEO, NEO
175 and BEO) were each individually re-dissolved in DCM. Each DCM solution was split into two
176 equal portions (with the exception of the NEO extract, as no pH modifier was used for re-
177 dissolution for either ion mode) and again brought to dryness under a gentle stream of N₂. The
178 split dried extracts were then re-dissolved in a solvent system based on the corresponding
179 HRMS analysis listed below. For the AEO extract: one dried extract was re-dissolved in 50:50
180 acetonitrile (ACN):water with 0.1% NH₄OH, and run in negative ion mode with 50:50 ACN:H₂O
181 with 0.1% NH₄OH as the LC eluent; the second extract was re-dissolved in 50:50 ACN:H₂O with
182 no pH modifier, and run in positive ion mode with 0.1% formic acid (HCOOH) as the LC eluent.
183 For the BEO extract: one dried extract was re-dissolved in 50:50 ACN:H₂O with 0.1% HCOOH,
184 and run in positive ion mode with 50:50 ACN:H₂O with 0.1% HCOOH as the mobile phase; the
185 second extract was re-dissolved in 50:50 ACN:H₂O with no pH modifier, and run in negative ion
186 mode with 0.1% NH₄OH as the mobile phase. For the NEO extract: the dried extract was re-
187 dissolved in in 50:50 ACN:H₂O with no pH modifier, and run in positive ion with 50:50 ACN:H₂O
188 with 0.1% ACN:H₂O as the mobile phase, and again in negative ion mode with 50:50 ACN:H₂O
189 with 0.1% NH₄OH as the mobile phase.

190 Mass spectrometry analysis was performed using an LTQ Orbitrap Elite (Thermo Fisher
191 Scientific, San Jose, CA) operating in full scan in negative and positive ion mode. Mass
192 resolution was set to 240,000 with an *m/z* scan range of 100-600. For negative ion mode the ESI

193 source was operated as follows: sheath gas flow rate 10 (arbitrary units), spray voltage 2.90 kV,
194 auxiliary gas flow rate 5 (arbitrary units), S lens RF level 67 %, heater temperature 50 °C, and
195 capillary temperature 275 °C. For positive ion mode the ESI source was operated as follows:
196 sheath gas flow rate 10 (arbitrary units), spray voltage 3.00 kV, auxiliary gas flow rate 5
197 (arbitrary units), S lens RF level 63 %, heater temperature 50 °C, and capillary temperature 275
198 °C. As per Composer data analysis, the mass accuracy was < 2 ppm error for all mass
199 assignments.

200 For negative ion analysis, the mobile phase solvent used was 50:50 ACN:H₂O containing 0.1 %
201 NH₄OH, while positive ion analysis used 50:50 ACN:H₂O containing 0.1 % HCOOH. Given that
202 the same mobile phase was used for all samples in each ionization mode, class ionization
203 efficiency was assumed to be independent of extraction pH when comparing between the
204 different pH fractions. A flow rate of 200 µL min⁻¹ was used for both, delivered by an Accela
205 1250 solvent pump (Thermo Fisher Scientific, San Jose, CA). A volume of 5 µL was injected into
206 the mobile phase stream using a Thermo PAL-HTC Accela autosampler (Thermo Fisher
207 Scientific, San Jose, CA). Quantitation was performed using linear regression obtained from a 5
208 point external calibration. (Hughes et al., 2017b)

209 The software used for instrument control/data acquisition and molecular analysis was Xcalibur
210 version 2.1 (Thermo Fisher Scientific, San Jose, CA) and Composer version 1.5.2 (Sierra
211 Analytics, Inc., Modesto, CA), respectively. Pseudo-first order rate constants were fit to the O₂[±]
212 class data based on initial trends of when congeners were first detected in the reaction (since
213 some congeners displayed complex trends of intensity increasing initially, but decreasing later
214 in the treatment). For comparisons between the different pH fractions, it was assumed that the

215 ionization efficiency of a given class was independent of extraction pH, given that pH of the
216 mobile phase was the same.

217 Results and Discussion

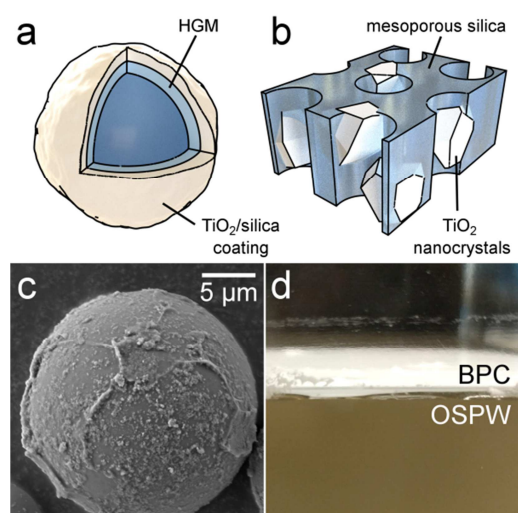
218 Buoyant photocatalyst (BPC) design

219 Previous OSPW treatment studies have evaluated nanoparticle photocatalysts dispersed as
220 slurries in the OSPW, (Headley et al., 2009; Leshuk et al., 2016b; Mishra et al., 2010) which,
221 while useful as performance benchmarks, are impractical for passive deployment due to the
222 requirement for vigorous mixing to keep the particles suspended, the challenge of catalyst
223 recovery, and concern of environmental release of nanoparticles. Since solar PC is driven by
224 sunlight absorption at the water surface, we hypothesized that by immobilization on buoyant
225 supports, photocatalysts could remain suspended in the illuminated zone without the
226 requirement for mixing, while enabling simple catalyst retention and separation following
227 treatment. Such a design should also result in more efficient materials utilization, since
228 photocatalyst particles are not dispersed in the dark zone below the water surface where they
229 are unreactive and result in catalyst oversupply, in contrast to slurry dispersions. BPCs have
230 been successfully demonstrated for treatment of simulated oil spills and dissolved
231 organics. (Berry and Mueller, 1994; Magalhães and Lago, 2009; Nair et al., 1993) Given their
232 proven potential, we thus sought to demonstrate BPCs for OSPW treatment.

233 BPC composite particles were synthesized by coating TiO₂ nanoparticles on hollow glass
234 microspheres, using mesoporous silica as a binder (Figure 1). Binding nanoparticles within
235 composite materials is a successful strategy to control the environmental release of free

236 nanoparticles (Froggett et al., 2014; Ging et al., 2014). Purely inorganic materials were selected
237 for the composites to resist photocatalytic attack, (Fabiya and Skelton, 2000; Shang et al., 2003;
238 Singh et al., 2013) and a porous silica binder was used to enhance nanoparticle adhesion to the
239 microsphere support, (Qiu and Zheng, 2007) while still allowing access of solution to the catalyst
240 via mesopores. (Allain et al., 2007) The synthesized BPC material was hydrophilic, and floated at
241 the surface of water as a frothy film (Figure 1d&e).

242



243

244 **Figure 1.** Schematic drawings of (a) BPC composite structure and (b) TiO₂ nanoparticles
245 immobilized in mesoporous silica, (c) SEM image of a BPC composite particle, and (d)
246 photograph of a BPC film floating on OSPW, from a side view.

247 The PC performance of the BPCs were evaluated in OSPW. Treatment rate diminished as a
248 function of water depth (Figure S2), consistent with a surface driven reaction, where >99% of
249 UV light was absorbed within the top cm of OSPW in previous photocatalytic experiments
250 (Leshuk et al., 2016b). Notably, the apparent rate of the BPCs ($\sim 4.3 \times 10^{-6} \text{ s}^{-1}$) was similar to that

251 of a TiO₂ nanoparticle slurry (P25) at low concentrations (<5 g/m² TiO₂, Figure S3) and gentle
252 mixing conditions (Re < 1000, Figure S4), although the TiO₂ slurry was more efficient under
253 vigorous mixing (Re > 1000) and at higher concentrations (>5 g/m² TiO₂). The BPCs were also
254 found to maintain their performance over 10 batch treatment cycles (Figure S5). Thus when
255 operating under non-turbulent flow regimes, BPCs match the performance of TiO₂ slurries,
256 while enabling easier retention and recycling than free nanoparticle dispersions (Chong et al.,
257 2010; Malato et al., 2009).

258 Overall treatment kinetics

259 Following these preliminary experiments, the transformation of NOCs during the photocatalytic
260 process was thoroughly investigated. The initial organics concentrations in the OSPW were
261 measured by several methods (Table 1; inorganic parameters given in Table S1; FTIR and MS
262 spectra given in Figure S6 and Figure S7-Figure S36, respectively). A relatively low BOD number
263 compared to the other metrics is typical for OSPW, and indicates the recalcitrance of the NOCs
264 to biodegradation (Leshuk et al., 2016b). The difference of AEO concentrations measured by
265 FTIR and MS is likely due to the use of a commercial NA mixture (with low average molecular
266 weight) as the calibration standard for the FTIR method. (Hughes et al., 2017a) The most
267 organics (by ESI(-) MS) were extracted at neutral pH with 113.5 mg/L NEO, ~42% more than the
268 acidic extract, and ~19-fold more than the basic extract. Previous studies have similarly
269 measured reduced extraction of negative ion species at high pH. (Huang et al., 2016; Klammerth
270 et al., 2015) This comparison assumes class response factors are independent of extraction pH
271 for a given ionization mode. The high NEO:AEO ratio may be evidence of polar non-acids
272 partitioning to the neutral fraction.

273

274 **Table 1.** Measures of dissolved organics in raw OSPW.

Parameter	Concentration (mg/L)
AEO _{FTIR}	40.9 ± 2.4
AEO _{MS} ^a	79.9
NEO _{MS} ^a	113.5
BEO _{MS} ^a	6.0
Total EO (UV ₂₂₀)	78.9 ± 1.9
TOC	54
COD	153
BOD	3.0

275 ^a Concentrations calculated only from negative ion MS data, assuming an extraction efficiency
 276 of 49.1%.

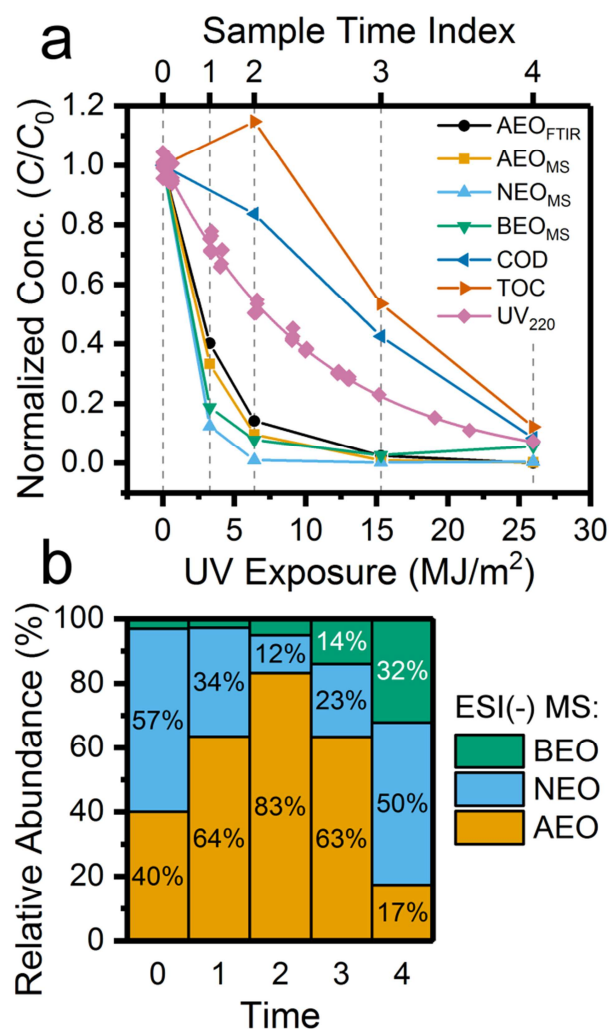
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278 During the photocatalytic reaction, FTIR was found to be a good surrogate measure for MS
 279 kinetics. The apparent pseudo-first order rate constant (k_{app}) of AEO_{FTIR} removal, $9.2 \pm 0.4 \times 10^{-6}$
 280 s^{-1} , matched closely to that of AEO_{MS} removal, $11.4 \pm 0.4 \times 10^{-6} s^{-1}$ (Figure 2a). (Hughes et al.,
 281 2017a; Islam et al., 2014) The NEO and BEO were eliminated significantly more quickly than the
 282 AEO, with $k_{app} = 25.1 \pm 0.7 \times 10^{-6} s^{-1}$ and $14.9 \pm 1.3 \times 10^{-6} s^{-1}$, respectively. This may be
 283 reasonable on the basis that ring-opening photocatalytic reactions form carboxylic acid
 284 groups, (Bui et al., 2011; Grabowska et al., 2012; Pichat, 1997; Soana et al., 2000) which would

285 be expected to lead to accumulation of originally base-neutral species in the AEO fraction over
286 the course of the treatment (Figure 2b). Continuation of photocatalytic exposure resulted in
287 final organics mineralization (reduced COD and TOC, Figure 2a), in contrast to weaker oxidation
288 processes such as ozonation, which have been shown to leave a toxic organic residual in OSPW
289 even after high O₃ doses (>30 mg/L). (Klamerth et al., 2015; Meshref et al., 2017; Scott et al.,
290 2008) Effective photocatalytic NOC mineralization may be due to the high oxidation potential of
291 TiO₂ valence band holes (~3.0 V vs. SHE), (Nosaka and Nosaka, 2013) or the involvement of
292 superoxide radicals, as hypothesized previously (de Oliveira Livera et al., 2018; Leshuk et al.,
293 2016b). Faster elimination of extractable organics compared to UV₂₂₀, COD, and TOC, may be
294 due to a process of photocatalytic oxidation initially increasing the polarity of the organics to
295 the point where they are no longer extractable by DCM at any pH, after which they are steadily
296 mineralized. AEO_{FTIR} was only reduced by 11% (4.6 mg/L) in a catalyst-free OSPW control
297 exposed to a UV fluence of 27.8 MJ m⁻², similar to previous observations of minimal photolytic
298 elimination in the absence of a catalyst (Leshuk et al., 2016b).

299

300



301
 302 **Figure 2.** (a) Photocatalytic treatment kinetics by various organics measures. Samples taken
 303 throughout the treatment were labelled by a sequential Time Index. (b) Ratios of AEO, NEO,
 304 and BEO negative ion concentrations throughout the photocatalytic reaction, with time indices
 305 corresponding to those labeled in (a).

306 Heteroatomic class transformations

307 Recently, heteroatomic and positive ion classes have been implicated in the toxicity of

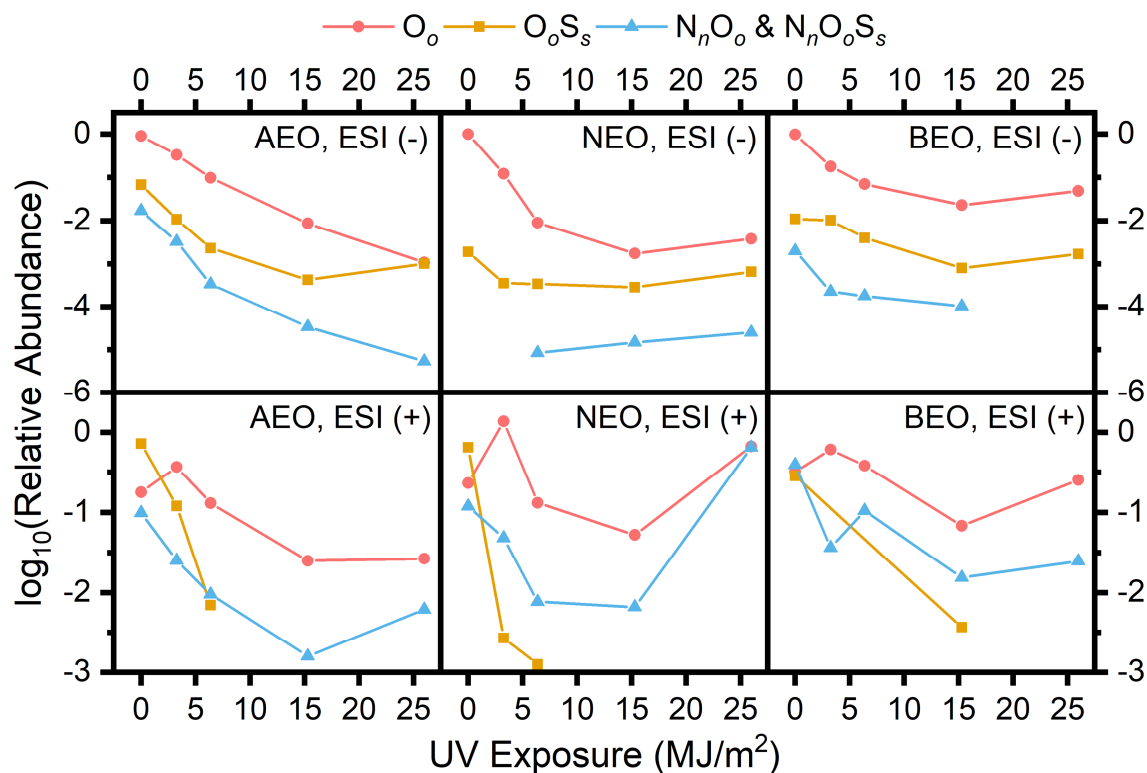
308 OSPW,(Alharbi et al., 2016; Morandi et al., 2017, 2015) therefore it is important to understand

309 their transformations during PC. In terms of initial speciation of negative ions, the neutral and
310 basic fractions were dominated by O_2^- (classic NAs), while the AEO additionally contained
311 minority O_3^- , O_4^- and O_3S^- classes (Figure S37). A high O_2^- ratio (relative to O_o^- classes with $o > 2$)
312 may indicate a relatively fresh OSPW sample, as o increases with environmental aging. (Han et
313 al., 2009) As observed previously, (Barrow et al., 2010) a greater diversity of heteroatomic
314 classes were detected in positive ion mode (Figure S38). The BEO was primarily characterized
315 by OS^+ (28%), O_8^+ (23%) and NO_8^+ (26%) classes, the AEO by SO_3^+ (59%), and the NEO by OS^+
316 (29%) and O_3S^+ (32%), along with minor NO^+ (3.8%), O_2^+ (7.7%), O_3^+ (4.2%), O_8^+ (5.8%) and O_2S^+
317 (3.6%).

318 In terms of environmental implications, O_2^- has been repeatedly confirmed as one of the most
319 acutely toxic negative ion classes, with a narcotic mechanism arising from the NAs' surfactant
320 properties (Hughes et al., 2017b; Morandi et al., 2015; Roberts and Costello, 2003; Yue et al.,
321 2015b). Higher oxygen numbered species are less acutely toxic. (Frank et al., 2009) O_3S^- may
322 comprise sulfonic acids, and thus impart similar surfactant modes of toxicity. (Quesnel et al.,
323 2015) O_o positive ions likely contain hydroxyl or ketone groups, and may be implicated in the
324 endocrine disrupting effects of OSPW. (Pereira et al., 2013; Rowland et al., 2011; Yue et al.,
325 2015a) The O_3S^+ class is thought to comprise thiophenic hydroxylated aldehydes, (Rowland et
326 al., 2014; J. Sun et al., 2017) and has previously been found in non-toxic NOC fractions. (Morandi
327 et al., 2017, 2015) The O_2^- , O^+ and OS^+ classes have among the highest measured membrane
328 partitioning ratios, with potential to bioaccumulate. (Zhang et al., 2015, 2016) While typically
329 measured at lower intensity than the O_2^- NAs, OS^+ and NO^+ species are also thought to be
330 potent toxicants, (Morandi et al., 2016) with potential to inhibit membrane transport proteins

331 and damage DNA through oxidative stress.(Alharbi et al., 2016; Morandi et al., 2017; J. Sun et
332 al., 2017)

333 During the photocatalytic treatment, both positive and negative ions of the heteroatomic O_oS_s
334 family were initially preferentially degraded (Figure 3), such that the class distributions shifted
335 to almost exclusively O_o at intermediate time points (Figure S39). The relative increase in O_o^+
336 intensity observed in all extracts from the first treated sample (3.3 MJ/m² UV exposure) could
337 be attributed to the appearance of oxidized intermediates. These changes in relative
338 composition of heteroatomic classes, especially in the positive ion data (where the O_o fraction
339 increases to ~90% from ~20% in the raw OSPW, Figure S39 ESI(+) trend), are much larger than
340 observed previously following OSPW treatment with O_3 , UV/ H_2O_2 and Fe(VI) (relative changes
341 of only ~20%) (Wang et al., 2016). This could potentially indicate a more selective oxidation
342 mechanism for PC, in accordance with previous observations.(de Oliveira Livera et al., 2018;
343 Leshuk et al., 2016b) In the final stages of the photocatalytic reaction, the abundance of $O_oS_s^-$
344 and $N_nO_o^+/N_nO_oS_s^+$ species relative to the O_o^\pm increased in the AEO and NEO extracts,
345 concurrently with the decreasing AEO fraction (Figure 2b). Under the assumption that
346 ionization efficiency of a given class is similar across all samples investigated, it is hypothesized
347 that while raw O_oS_s species are initially the most reactive NOCs, oxidized intermediates
348 produced during the photocatalytic process are more reactive still, possibly due to preferential
349 adsorption of acidic and catecholic moieties to TiO_2 .(Dobson and McQuillan, 1999; Janković et
350 al., 2009) If so, in the final stages of the treatment acidic O_o compounds could be preferentially
351 degraded over base-neutral heteroatomics.



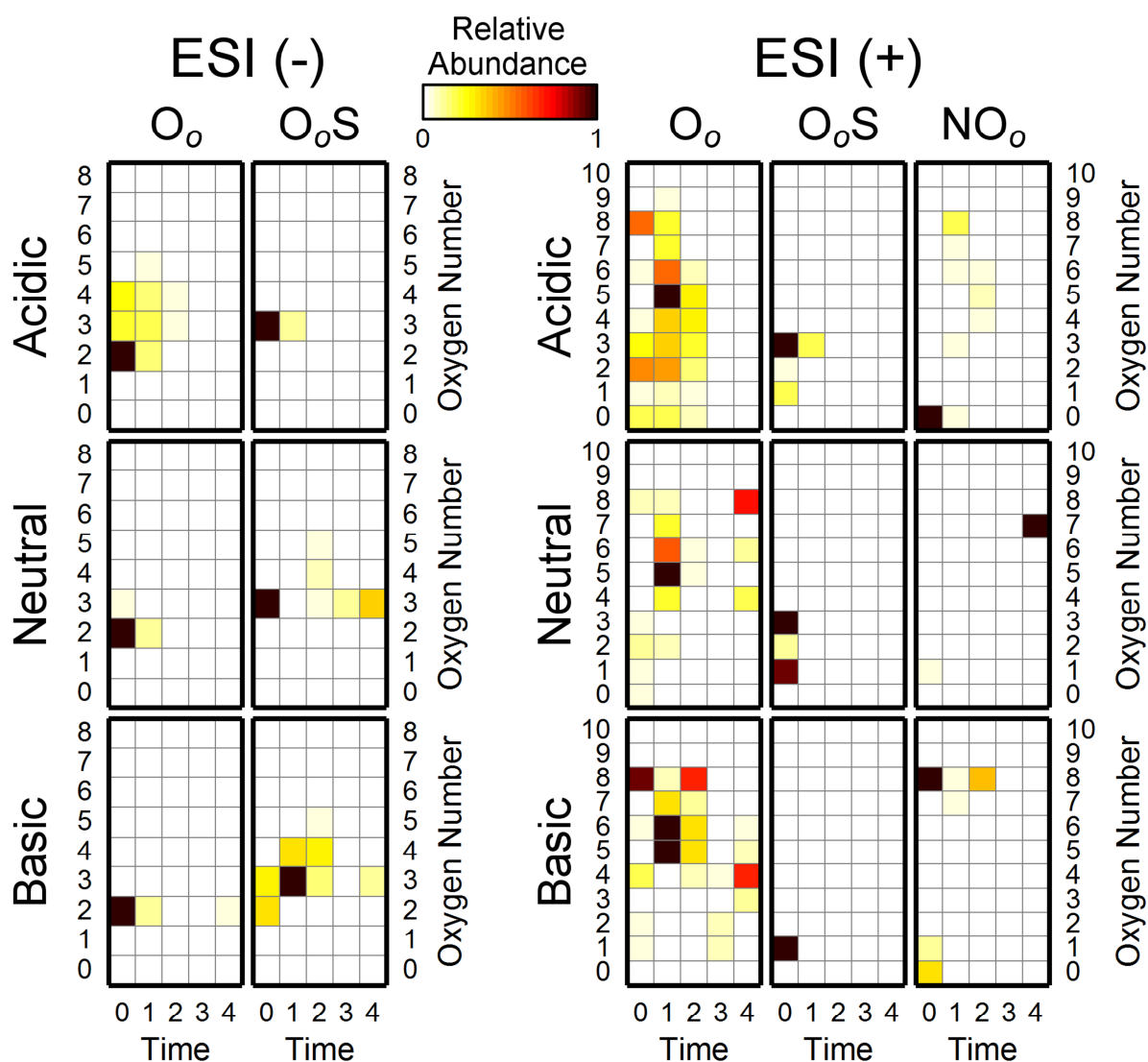
352
 353 **Figure 3.** Relative abundance of heteroatomic families throughout the photocatalytic
 354 treatment. Relative abundance was normalized within each extract and ion mode to the total
 355 intensity measured in the initial raw OSPW.

356

357 Class oxidation trends

358 Oxygen number $o > 2$ has been generally shown to be inversely correlated with acute toxicity
 359 for OSPW NOCs, as the polarity of added oxygen functionalities counteracts the molecules'
 360 surfactant properties. (Frank et al., 2008; Yue et al., 2015b) While the intensity of the negative
 361 ions was significantly diminished by the first sampling time point (Figure 4), clear trends of
 362 increasing o with time were observed in all extracts for both O_o^- and O_oS_s^- classes (Figure S40,

363 normalized with respect to time point to highlight the oxidation trends). In the AEO, average *o*
364 increased from 2.5 in the raw OSPW to 4.3 by the third time point of photocatalytic exposure.
365 This is once again a stronger shift than was reported for OSPW AEO oxidation using other
366 AOPs,(Wang et al., 2016) although a similarly large increase in *o* has been observed previously
367 for photocatalytic OSPW AEO oxidation.(Leshuk et al., 2016b) Apparent deviation from this
368 trend in some extracts at the final two time points may simply be due to poor DCM extraction
369 efficiency of highly polar, heavily oxidized compounds in the final stages of the treatment.
370



371
 372 **Figure 4.** Trends in oxygen number (o) with time for different heteroatomic classes. Relative
 373 abundance of species by oxygen number is presented normalized to the maximum intensity
 374 measured within each class, where time indices correspond to those labelled in Figure 2a.

375
 376 In positive ion mode, any trends in o with time were less clear: the broad distributions in O_o^+ in
 377 the acidic and neutral extracts may be attributed to the appearance of hydroxylated oxidation

378 intermediates.(J. Sun et al., 2017) Indeed, the increased O_o^+ intensity at Time 1 is correlated
379 with the reduction in O_o^- and O_oS^- abundance. Some single-class conclusions may also be drawn
380 from the ESI(+) data: the OS^+ NOCOC was eliminated by the first time point in the BEO and NEO.
381 Similarly, the NO^+ species in the neutral extract were eliminated by the first time point, along
382 with the O_2^+ and O_3^+ classes.

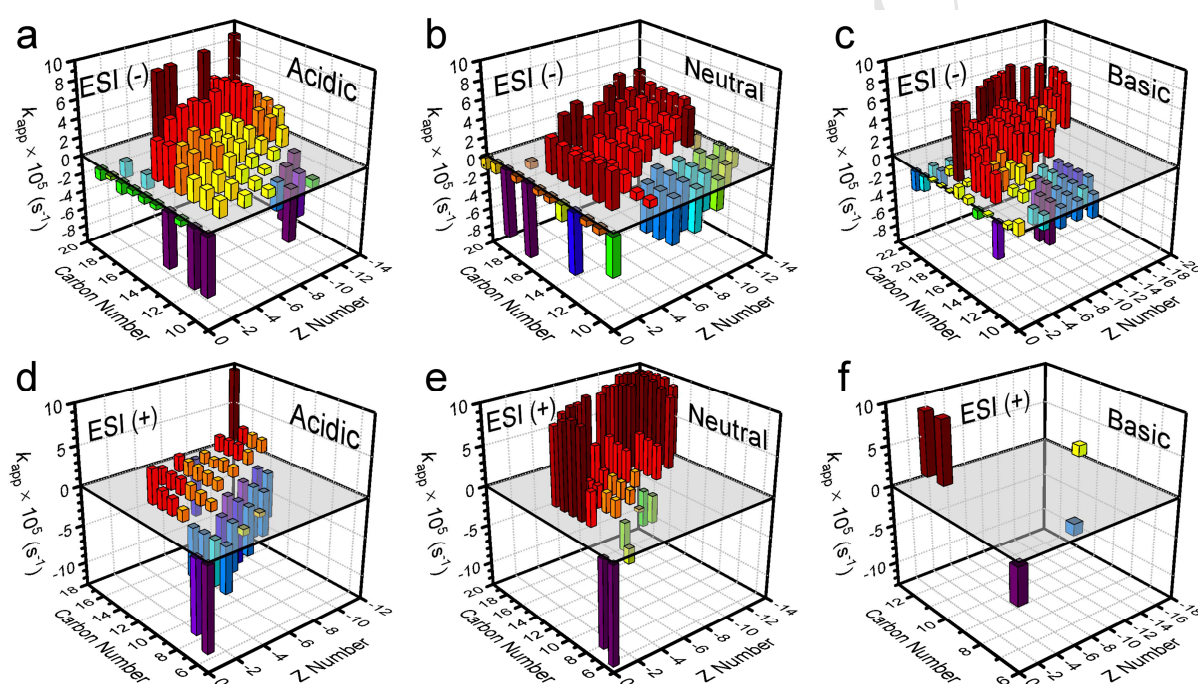
383 Thus the presumed most toxic NOCOCs (O_2^- , OS^+ and NO^+)(Morandi et al., 2015; J. Sun et al.,
384 2017) were rapidly transformed in the earliest stages of the treatment, when AEO_{FTIR} was still
385 measured as 40%. This is promising for the practicality of photocatalytic OSPW treatment, as
386 only a relatively short exposure may be needed to meet WET targets, rather than full organics
387 mineralization. This is supported by our previous finding that OSPW toxicity towards *Vibrio*
388 *fischeri* could be eliminated by solar PC prior to full organics mineralization,(Leshuk et al.,
389 2016b) although more rigorous toxicity testing of PC treated OSPW is warranted.

390 Previous studies have shown that oxidized NOCs are more readily biodegradable.(Brown et al.,
391 2013; Dong et al., 2015; Martin et al., 2010) Thus given the oxidation patterns observed herein,
392 supplementation of PC with biodegradation may be another promising strategy to increase
393 overall OSPW treatment efficiency, *e.g.*, by combination of solar PC with passive treatment
394 wetlands.(Araña et al., 2008; Chow et al., 2017; McQueen et al., 2017a)

395 Carbon and Z number kinetics

396 In addition to following chemical transformations between classes, through HRMS it was also
397 possible to investigate the molecular weight (carbon number *c*) and hydrogen deficiency (*Z*
398 number) distribution within any single class throughout the photocatalytic treatment. We thus

399 fit a pseudo-first order rate constant to each O_2^\pm species as a function c and Z (Figure 5). It
 400 should be emphasized that the O_2^+ species are likely hydroxylated NOCs rather than NAs, but
 401 they are still presented together with the O_2^- NAs for comparison of the relative reactivity of
 402 positive and negative ions within the same treatment. Furthermore, since very few O_2^+
 403 compounds were detected in the initial BEO (Figure S38), the data for Figure 5f is sparse.
 404



405
 406 **Figure 5.** Estimates of pseudo-first order rate constants (k_{app}) of photocatalytic degradation of
 407 (a)-(c) O_2^- and (d)-(f) O_2^+ species in the (a)&(d) AEO, (b)&(e) NEO and (c)&(f) BEO fractions.
 408 Positive k_{app} values indicate rates of disappearance, while rates of appearance of new species
 409 are plotted as negative values of k_{app} .

410 The initial raw OSPW profiles of O_2^\pm in each of the extracts are presented in Figure S41. For the
 411 O_2^- , the NEO and BEO were distributed to higher c and $|Z|$ relative to the AEO, which is as

412 expected, since only the most hydrophobic NAs (highest ratio of aliphatic carbon to the
413 carboxylate anion) should be extractable at higher pH values. In ESI(+), the O_2^+ distribution in
414 NEO was also shifted to slightly higher c and $|Z|$ numbers versus the AEO.

415 The photocatalytic kinetics show a clear trend, across all fractions, of reactivity increasing with
416 carbon number (Figure 5), up to $k_{app} \approx 10 \times 10^{-5} s^{-1}$ for congeners of highest c . Furthermore, new
417 species of lower c and $|Z|$ numbers, which did not appear in the initial profiles (Figure S41),
418 were produced over the course of the treatment (represented as negative values of k_{app} in
419 Figure 5). These smaller, more linear NOCs are likely generated from heavier, more cyclic
420 parent compounds through photocatalytic C-C bond scission, *e.g.*, via ring opening or
421 decarboxylative chain shortening. Indeed, it is likely that the true rate constants are
422 approximately equal across the O_2^- class and largely independent of c and Z , as would be
423 expected for a non-specific HO^\bullet directed AOP. The apparent dependence may thus simply result
424 from intermediate c and $|Z|$ numbered organics being simultaneously created from the
425 degradation of higher c and $|Z|$ numbered species. Similarly, if acid-extractable O_2^+ compounds
426 are indeed hydroxylated aldehydes or ketones (Rowland et al., 2014; J. Sun et al., 2017), the
427 relatively lower rate constants in Figure 5d could be interpreted as evidence of their formation
428 during PC. Indeed, this would be expected from multiple pathways of $O_2^{\bullet-}$ driven C-C
429 cleavage.(Cermenati et al., 2000; Lair et al., 2008; Soana et al., 2000)

430 The environmental significance of these results is that both the most toxic and environmentally
431 persistent NAs are preferentially eliminated during PC treatment. Hughes et al. reported that
432 NAs with $c \geq 17$ were the most acutely toxic constituents of OSPW to rainbow trout
433 (*Oncorhynchus mykiss*). (Hughes et al., 2017b) Likewise, Yue et al. found that NAs with $14 \leq c \leq$

434 18 and $-6 \leq Z \leq -4$ were those most correlated with acute toxicity towards *Vibrio fischeri*, (Yue et
435 al., 2015b) similar to the trend of increasing NA toxicity with c measured by Jones et al. (Jones et
436 al., 2011) Similarly, NOCs with high c and $|Z|$ numbers are known to be the most recalcitrant
437 fractions in OSPW, while smaller and less cyclic NAs are more readily biodegradable. (Han et al.,
438 2009, 2008; Holowenko et al., 2002) However, further research is merited to evaluate the
439 toxicity of the lower c and $|Z|$ numbered intermediates formed during the PC treatment
440 process.

441 Conclusions

442 With recent insights into the structure-activity relationships driving various modes of observed
443 OSPW toxicity, it is clear that specific classes of organics, comprising only a minority of the total
444 NOCs, constitute the majority of the toxicity associated with OSPW. (Hughes et al., 2017b;
445 Morandi et al., 2015) Through implementing a fractionated HRMS investigation, these NOCOs
446 could be individually tracked in the context of PC oxidation trends occurring in the NOCs as a
447 whole. Revelation that the OS^+ and NO^+ classes were eliminated in the earliest stages of the PC
448 reaction, and that the highest molecular weight O_2^- NAs were preferentially degraded, may
449 indicate that only relatively low solar doses would be required to detoxify OSPW. This could
450 result in more efficient treatments as compared to the solar exposures required for complete
451 NOCs oxidation or DOC mineralization. This study also demonstrates application of a buoyant
452 photocatalyst formulation as a passive treatment concept for oil sands remediation challenges.
453 Further studies to develop this paradigm of a passive AOP are ongoing in our lab.

454

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462 Conflict of Interest

463 The following authors, T.L. and F.G., declare involvement as co-founders (with stock ownership)
464 in H2nanO Inc., an organization with a financial interest in the subject matter and materials
465 discussed in this manuscript. The following authors, K.M.P, D.d.O.L., A.T., P.B., and J.V.H.
466 declare no competing financial interest.

467

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Highlights

- Oil sands process-affected water (OSPW) is impacted by naphthenic organic compounds (NOCs)
- Majority of OSPW toxicity attributed to only a subset of NOC classes
- Passive treatment of OSPW demonstrated with buoyant photocatalysts
- First time petroleomics used to study treatment kinetics across NOC fractions
- Preferential degradation of priority O_2^- , OS^+ and NO^+ NOC classes of concern