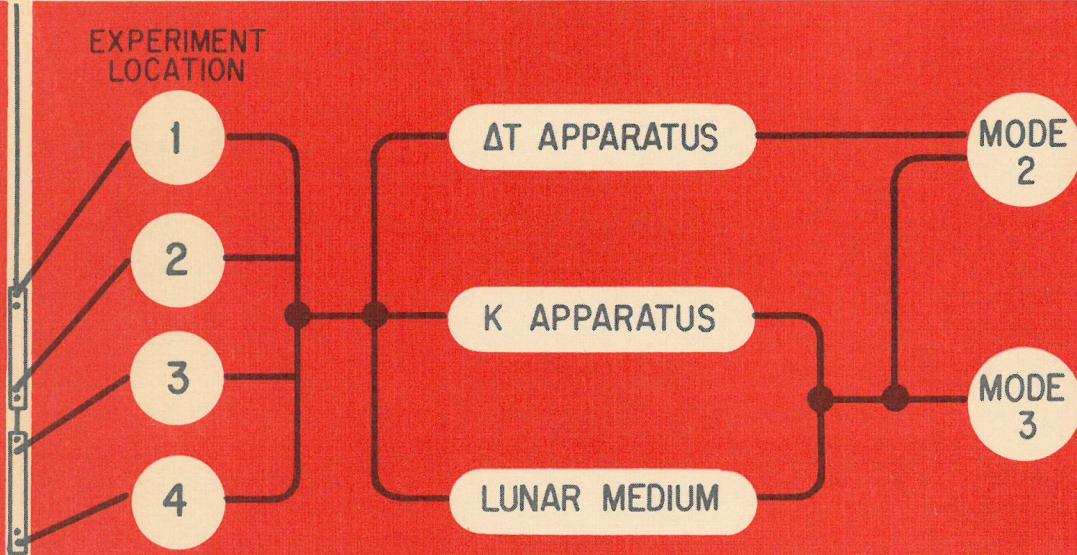


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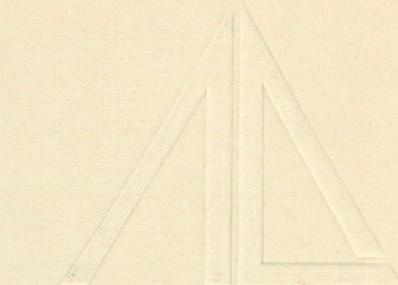
PERFORMANCE PREDICTION AND ANALYSIS OF THE LUNAR HEAT FLOW PROBES

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PREPARED FOR
LAMONT-DOHERTY
GEOLOGICAL OBSERVATORY

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OF THE LUNAR HEAT FLOW PROBES

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SUMMARY

The Heat Flow Experiment (HFE), part of the Apollo Lunar Scientific Experiment Package (ALSEP), when deployed on the moon, will provide in situ measurement of heat flow from the lunar interior. Each HFE, consisting of two heat flow probes emplaced by the astronaut at the bottom of a three-meter drilled hole, will measure the temperature gradient, the ambient temperature, and the thermal conductivity of the lunar surface layers--characteristics that in combination will provide a measure of the heat flow.

Thermal conductivity measurements will be made indirectly by monitoring the temperature response of sensors in the probes after appropriate heaters in the instrument are energized. Thermal conductivity data will be extracted from the temperature response of the sensors. The sensor response is related to the thermal conductivity of the lunar material surrounding the probe, the inherent thermal characteristics of the probe, the thermal interaction between the probe and the drill casing which will line the lunar bore hole, and the thermal characteristics of the interface between the drill casing and the surrounding lunar material. The interpretation of lunar temperature data and subsequent transformation of this data to conductivity predictions is influenced by these factors.

This report describes the mathematical modeling of the thermal behavior of the heat flow probes and surrounding medium. The computer models developed simulate the thermal performance of the conductivity experiments and will aid in the interpretation of lunar data. They provide a convenient means of examining experiment performance for any value of thermal conductivity or absolute temperature level existing in the lunar environment.

Predictions of probe performance in the lunar environment were made by the use of the mathematical models to aid the Principal Investigator of the HFE during a real-time data reduction, which is planned after emplacement of the experiment in the upcoming Apollo 13

lunar landing. The mathematical models will also be suitable as an aid to a refined data analysis during the post-flight period.

Other studies described in this report:

- 1) demonstrated that computer time was not excessive for solution of the finite-difference model of the probe and its surroundings;
- 2) led to an improved understanding of instrument performance during conductivity experiments; and
- 3) established the influence of certain environmental and physical uncertainties on probe thermal performance.

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- I COMPUTER SOLUTION OF HEAT FLOW MODELS
- II SAMPLE LISTING OF COMPUTER MODEL OF PROBE LOCATION 3 FOR MODE 3 OPERATION IN LUNAR ENVIRONMENT
- III FINITE-DIFFERENCE EQUATIONS AND BOUNDARY CONDITIONS FOR THERMAL MODELS OF LUNAR MEDIUM
- IV TABULATION OF PERFORMANCE PREDICTIONS IN THE LUNAR ENVIRONMENT

I. INTRODUCTION

With the guidance of Dr. M. Langseth of Lamont-Doherty Geological Observatory, Columbia University, Arthur D. Little, Inc., designed, developed, fabricated and tested lunar heat flow probes for the ALSEP^{*} Heat Flow Experiment.¹ The Lunar Heat Flow Experiment (HFE) is designed to measure both the temperature gradients in the subsurface of the moon and the thermal conductivity of the local lunar material. The purpose of the measurements is to provide a basis for calculating the heat flow from the lunar interior.

Thermal conductivity measurements are performed by energizing heaters in the probe and monitoring the temperature responses of two types of probe sensors. The relationship between the sensor responses and the thermal conductivity of the surrounding medium provides an indirect measurement of conductivity. Thermal responses of the probe sensors are also inherently related to the thermal properties of the probe and its structural elements, heat flow in the drill string which will line the lunar bore hole, the thermal coupling between the probe and the liner, the interface between the liner and the bore hole, and the absolute temperature level. These factors all complicate the calibration or interpretation of the experiment.

Subsequent to the construction and performance testing of the heat flow probes, an analysis of existing test data was conducted at Arthur D. Little, Inc., under Lamont-Doherty sponsorship. This work involved the use of simplified descriptions of the thermal behavior of the probe and lunar surroundings. The assumptions necessary to make the analytical solutions mathematically tractable limited the precision and generality of the results. One of the final recommendations of this work was the development of digital-computer thermal models which could include details of the heat flow probe and a comprehensive representation of the surrounding lunar material.

* Apollo Lunar Scientific Experiment Package.

¹ Superscript numerals refer to references listed in Section VII.

This report describes the development and use of computer mathematical models to describe the lunar probe and its surroundings. The main objectives of this work can be summarized as follows:

- Develop computer mathematical models capable of describing the details of heat flow in the probe and the lunar surroundings - and the interaction between them.
- Analyze the thermal performance of the heat flow probe in laboratory tests and investigate the relationship between sensor performance and experiment location.
- Predict the performance of the experiment after equilibration in the lunar environment (in an undisturbed medium), considering a drill string lining the lunar bore hole. The thermal response of the probe is to be related to the thermal conductivity of the surrounding lunar material as a function of time and absolute temperature.
- Provide information to the Principal Investigator of the HFE to aid in real-time data reduction of the experiment in the upcoming Apollo 13 lunar landing.
- Provide mathematical models of the probe and lunar surroundings for use in a refined data analysis during the post-flight period.

All the studies and predictions presented in this report relate to the performance of the heat flow probes in a homogeneous, thermally isotropic, and thermally equilibrated lunar environment. Analysis of diurnal variations in the lunar bore hole or of thermal perturbations and their effect on the conductivity experiments were beyond the scope of the subject work. The influence of diurnal variations and techniques

for correcting lunar data for their effects are being studied by Lamont-Doherty Geological Observatory for use during real-time data reduction and post-flight reduction of lunar data.

II. BRIEF REVIEW OF HEAT FLOW EXPERIMENT

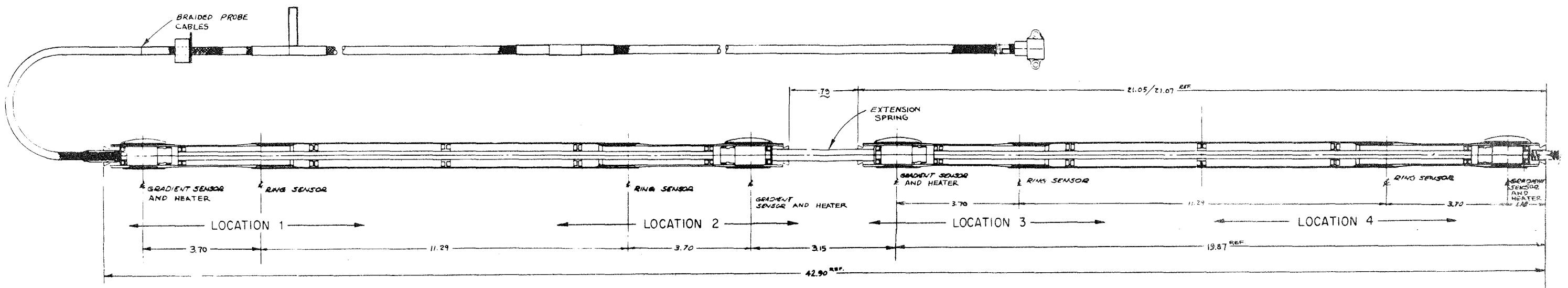
A. Introduction

Detailed documentation on the heat flow probe is available in Reference 1, which contains a comprehensive description of the probe design, fabrication and tests performed. A brief review of the general probe configuration and thermal sensors is presented below, primarily to define important thermal components and serve as a suitable reference for discussion contained in other sections of this report.

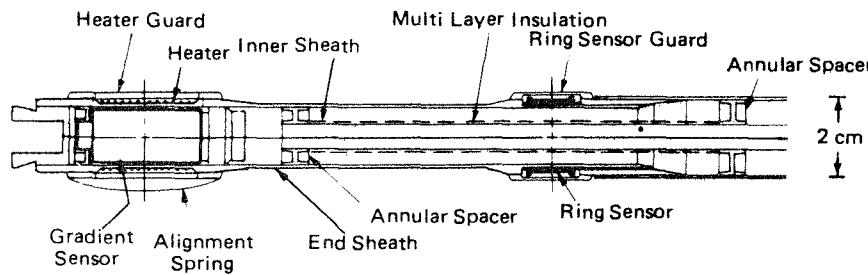
Each lunar heat flow probe is approximately 100 cm long and is comprised of two 50 cm-long static sections or half-probes. The two half-probes are connected by electrical wiring and an extension spring, so that one is directly above the other after installation at the bottom of a 3-meter, lined bore hole (Figure 1).

Each 50 cm section consists of a filament-wound, epoxy-fiber-glass structure which houses a "gradient"-sensor bridge, a "ring"-sensor bridge, and two heaters. The entire probe assembly contains four gradient sensors, four ring sensors and four heaters. It has been convenient to identify four experiment locations, each location comprising a heater winding, a gradient sensor, and a remote ring sensor approximately 10 cm from the heater. Experiment location number 1 is uppermost when the probe is emplaced inside the drill casing and number 4 is lowermost.

The gradient sensors shown in Figure 2a are platinum resistors. They are positioned concentric and internal to the heater windings at each of the four experiment locations. Each gradient sensor consists of a sealed enclosure formed by an outer platinum can and inner platinum mandrel. The enclosure is filled with helium. Lead wires from the sensor enclosure pass through an epoxy plug which is used to position the sensors.



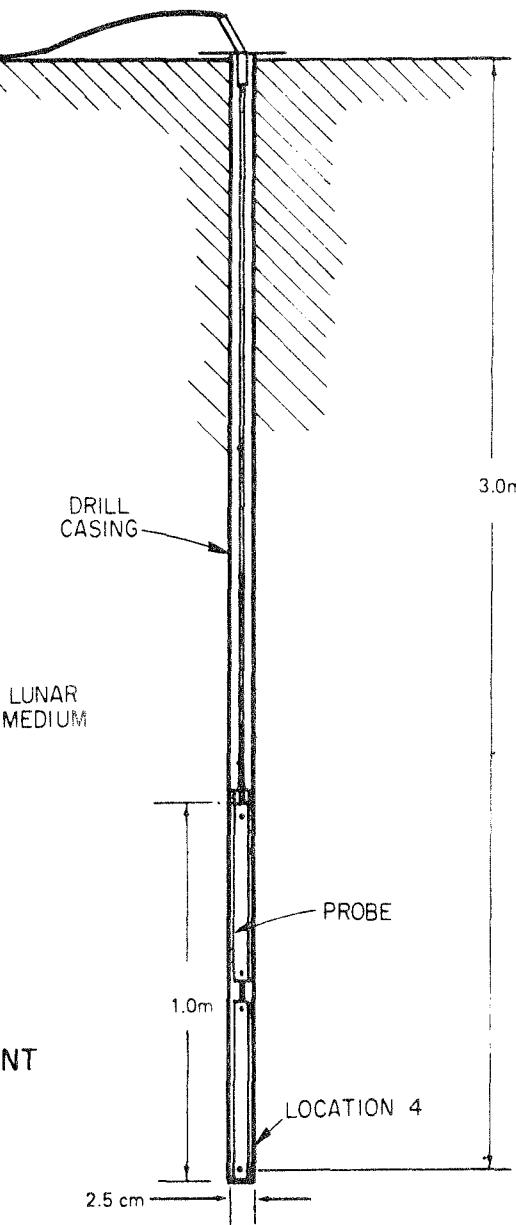
PROBE IN FULLY EXTENDED POSITION
FIGURE 1a

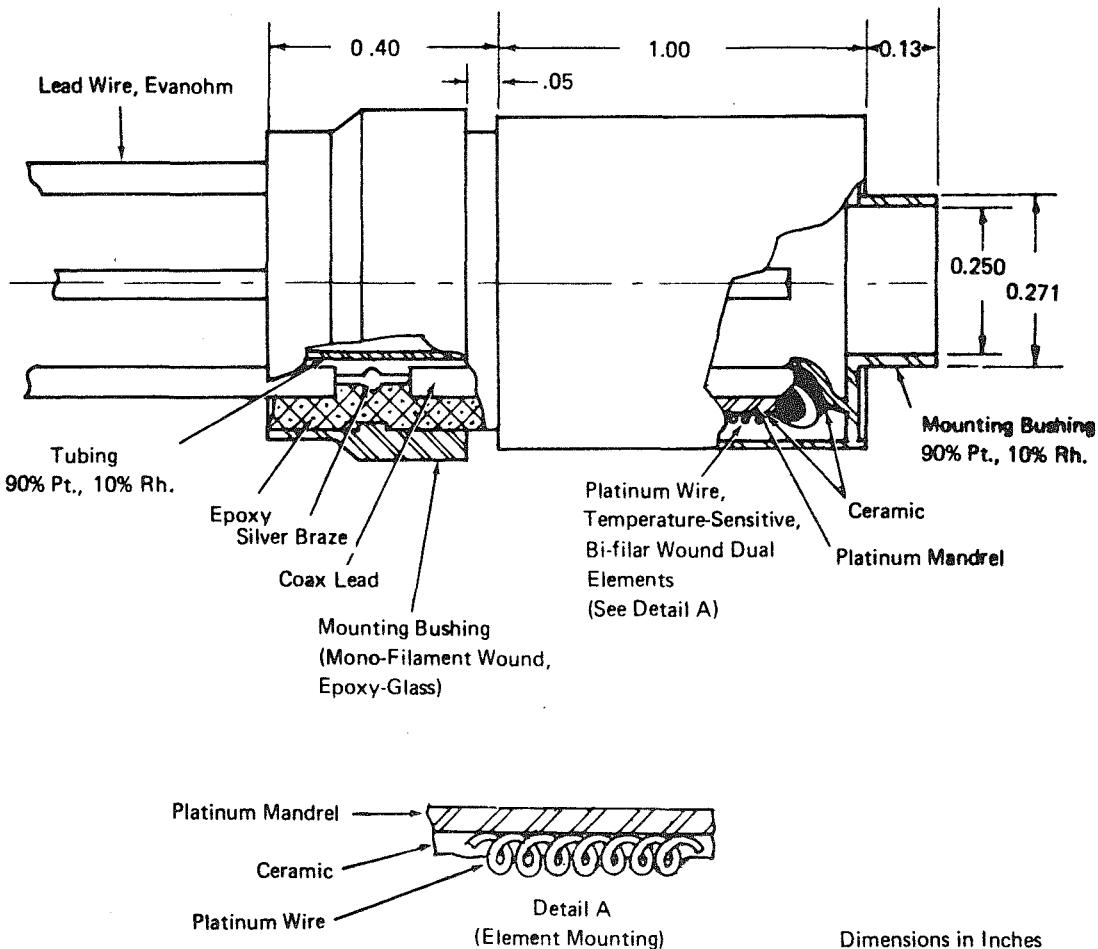


DETAIL OF TYPICAL EXPERIMENT LOCATION
(LEAD WIRES NOT SHOWN)
FIGURE 1b

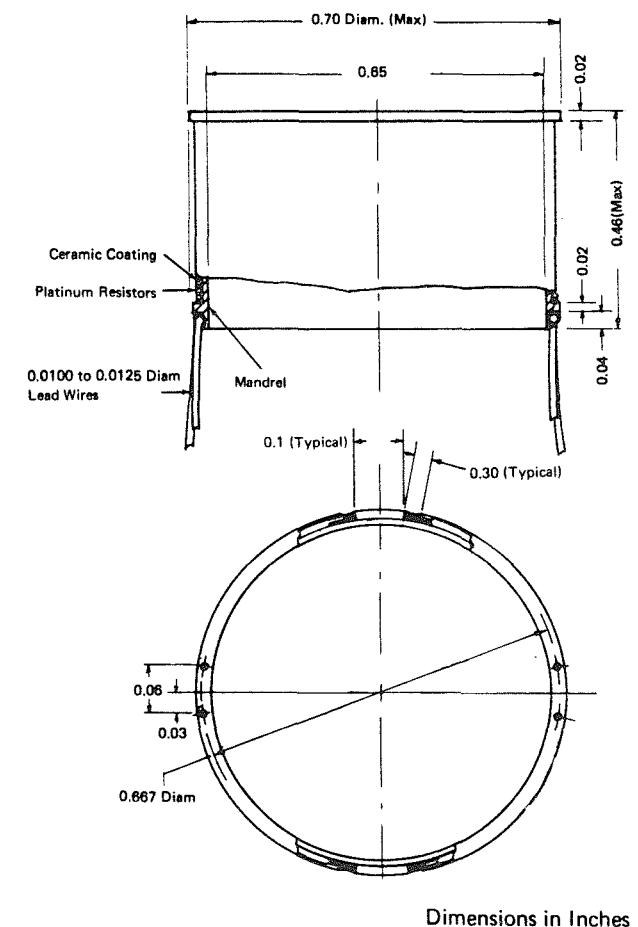
FIGURE 1 LUNAR HEAT FLOW PROBE

TYPICAL
PROBE EMBLACEMENT
FIGURE 1c





GRADIENT SENSOR
FIGURE 2a



RING SENSOR
FIGURE 2b

FIGURE 2 PROBE TEMPERATURE SENSORS

The ring sensors illustrated in Figure 2b consist of thin platinum bands on which are wound two resistors. The resistors are embedded in a blue-glaze ceramic coating on the external surface. A portion of the internal surface of the platinum band is cemented to a filler sheath which supports it and is, in turn, cemented to the outer sheath of the probe structure.

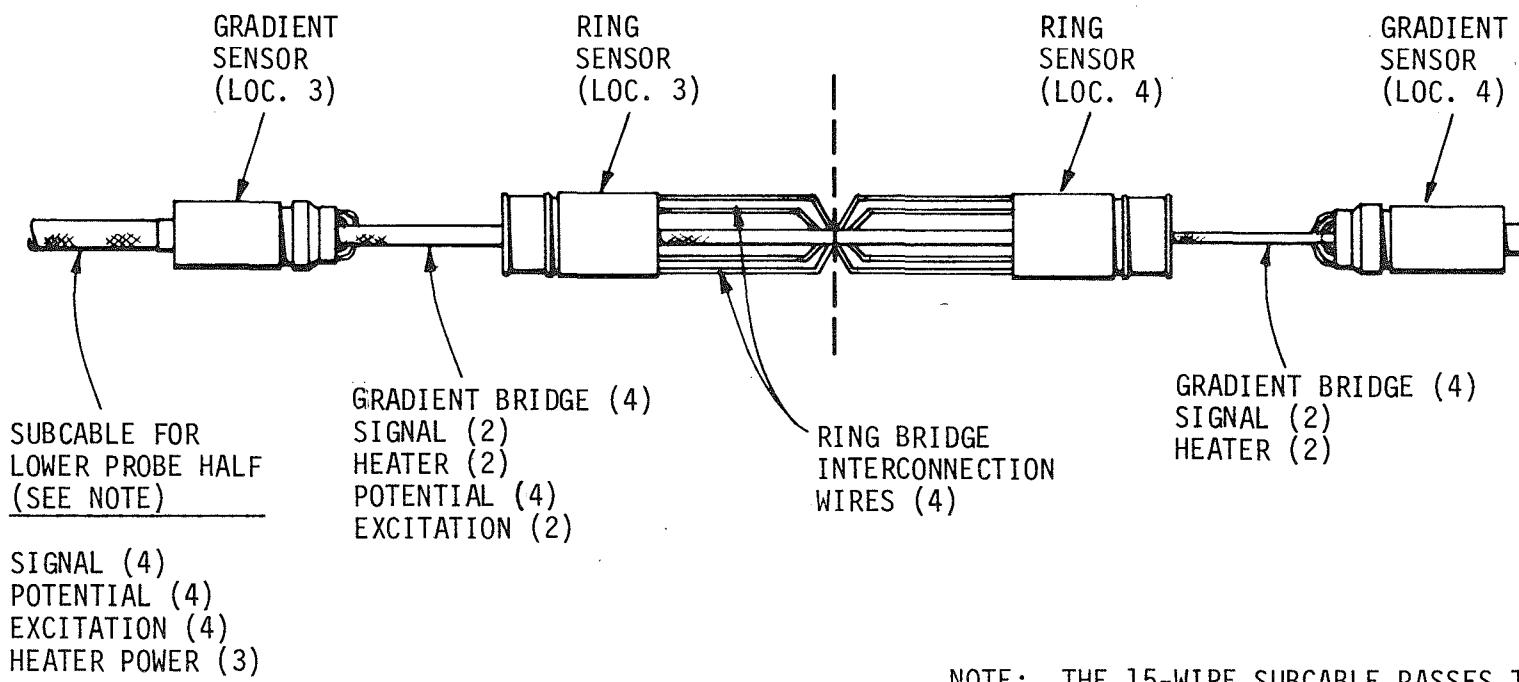
B. Operating Modes for Thermal Conductivity Measurement

In situ thermal conductivity measurements are to be made by one of two methods, depending upon whether the material surrounding the probes is in the low or high range of anticipated thermal conductivity.¹ In either mode, a heater is activated and the temperature response of probe sensors provides an indication of thermal conductivity of the surroundings. Thermal transients propagating from the lunar surface or due to instrument emplacement may be present in the lunar medium. These effects must be evaluated and corrections applied to the instrument response to interpret the conductivity experiments.

1. Low-Conductivity Range ($K < 2 \times 10^{-4}$ w/cm °K)

The low-range conductivity experiment, identified as the Mode 2 experiment, can be performed at any of the four locations along a probe by energizing the appropriate heater at a power level of 2 milliwatts and subsequently monitoring the temperature rise of the gradient sensor. (The other gradient sensor associated with the resistance bridge is unaffected by the heater and serves as a reference temperature.) The temperature rise of the gradient sensor at the location of the energized heater is related to the thermal conductivity of the lunar surroundings, absolute temperature level, thermal characteristic of probe structure and drill casing, and the conductive heat flow paths presented by lead wires and cables.

The lead wires in each probe half play an important role in the Mode 2 operation. The physical arrangement of lead wires in the lower probe half is depicted schematically in Figure 3. The influence



NOTE: THE 15-WIRE SUBCABLE PASSES THROUGH
 THE ENTIRE UPPER PROBE HALF, WHICH
 ALSO CONTAINS A WIRING CONFIGURATION
 IDENTICAL TO THAT SHOWN HERE.

FIGURE 3 SCHEMATIC ARRANGEMENT OF WIRING
IN LOWER PROBE HALF

of lead wires on thermal performance is least at location 4 where the fewest wires (8) are thermally coupled to the gradient sensor. In comparison, at location 3 a total of 29 wires provides thermal couplings to the gradient sensor. Similarly, in the upper probe half, which is not shown in Figure 3, 38 wires are thermally coupled to the gradient sensor at location 2. For the gradient sensor at location 1, heat flows along two 15-conductor subcables which are in radiative communication with the probe surroundings, and along 29 other wires routed in the direction of location 2.

Heat flow along the wires depresses the temperature of the gradient sensor associated with the energized heater. Therefore, the temperature rise of the gradient sensor is highest at location 4 and lowest at location 1.

2. High-Conductivity Range ($K > 2 \times 10^{-4}$ w/cm $^{\circ}$ K)

The Mode 3 experiment is designed for measurements in the high range of possible lunar conductivities. One of the heater windings is energized at a 0.5-watt level, and the temperature rise of the ring sensor - approximately 10 cm from the heater - is monitored as a function of time. The temperature response of the ring sensor is also dependent on the thermal characteristics of the probe. However, transient effects primarily related to the probe characteristics and absolute temperature level have short time constants and become small after approximately a three-hour period. Thereafter, the time rate of change of ring-sensor temperature ("slope") is controlled by the thermal conductivity of the surrounding lunar material.

III. DESCRIPTION OF THERMAL MODELS

A. Introduction

A computerized thermal analysis of a physical system, involving finite-difference procedures, requires the following steps:

- Subdividing the physical system into thermal zones or nodes.
- Preparing input data, which describe the heat-balance equations, for a computer program.
- Solving for the temperatures on a digital computer.

When finite-difference techniques are used in thermal analysis, the geometrical subdivision of the system being analyzed is important from the standpoints of accuracy and cost. If the subdivision is too fine (or the number of subdivisions too large), a large amount of computer time is required to formulate and solve the thermal models; if it is too coarse, excessive error will result in the computations.

Stringent requirements must be observed for computer simulation and numerical predictions of performance of the HFE. For example, in the Mode 2 operation, the thermal conductivity of the surrounding lunar medium is related to a small temperature rise of the gradient sensor - between 0.3 and 2°K. A 10% change in the signal can correspond to a 50% change in thermal conductivity, for values in the range of 2×10^{-5} to 4×10^{-5} w/cm °K. Therefore, accurate modeling of the lunar medium and proper simulation of the interplay between the probe and the medium are of prime importance.

Prior to the development of detailed models for the lunar heat flow probe and surrounding lunar medium, preliminary studies were made for the following purposes:

- 1) determine the finite-difference subdivision in the low-conductance probe sheath necessary

- to render an accurate description of the heat flow between sensor locations; and
- 2) develop finite-difference models and procedures for describing an infinite lunar medium.

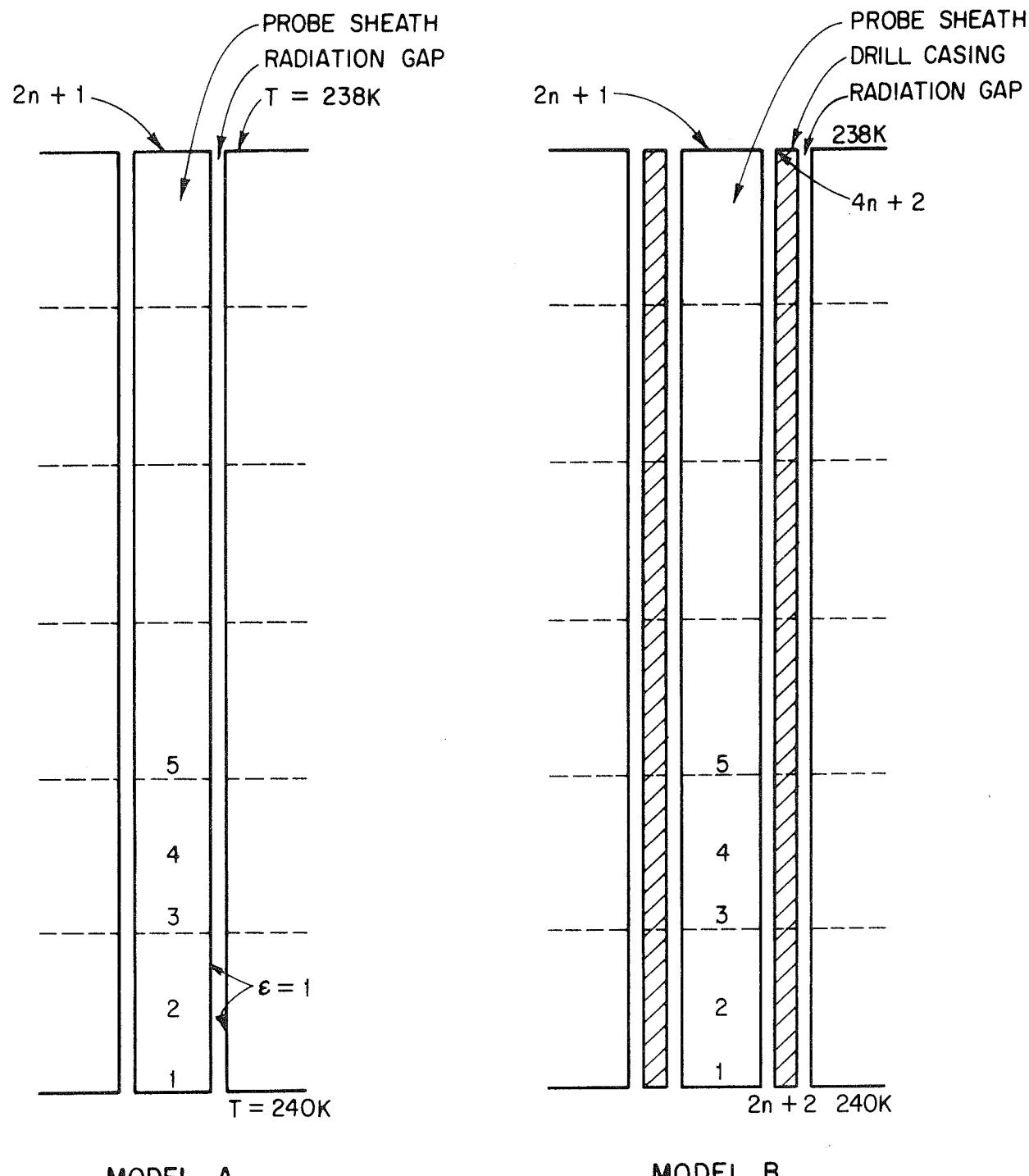
A discussion of these studies and the models developed for the probe and lunar medium is given in the following section. An evaluation of the models, performed prior to performance predictions in the lunar environment, is described in Section IV.

The heat flow equations for the thermal models were written in finite-difference form using the Zone Method of Strong and Emslie.⁴ Numerical solutions were obtained using an existing Arthur D. Little, Inc., Generalized-Thermal-Analyzer computer program (ADLGTA) discussed in Appendix I. Appendix II contains a complete input data listing for a typical thermal model of the probe and surroundings.

B. Modeling of Lunar Probe

1. Preliminary Study for Subdivision Requirements

Two thermal models, shown schematically in Figure 4, were used to examine the relationship between the number of subdivisions in the probe and the accuracy of the temperature predictions. Model A considers an epoxy-fiber-glass probe sheath 50-cm long, separated from a surrounding medium by a radiation gap. The surrounding medium has a specified temperature distribution which varies linearly from 240°K at the lower end to 238°K at the top end. The emittances of the outer surface of the probe sheath and the internal surface of the surrounding medium are taken as unity. Heat flow in the probe sheath is governed by radiation transfer at the outer surface and by conduction along the length. In this physical model, the internal and end boundaries are adiabatic. Model B considers a similar arrangement but with a drill casing (lunar drill string) between the probe sheath and the surrounding medium.



NOTE: DOTTED LINE DENOTES FINITE DIFFERENCE SUBDIVISION

$$\Delta T_{\text{probe}} = T_1 - T_{2n+1}$$

FIGURE 4 THERMAL MODELS FOR STUDY OF SUBDIVISION REQUIREMENTS IN LUNAR PROBE

The number of equal-length subdivisions in the probe sheath (and in both the probe sheath and drill casing for Model b) was varied from a minimum of 2 to a maximum of 40. The results of this study are shown in Figure 5 where the end-to-end ΔT in the probe is plotted as a function of the number of subdivisions (and subdivision size). The calculations show that a subdivision size of approximately 2.0 cm is adequate for an accurate description of both configurations. The calculations also demonstrate the possible influence of a conductive drill casing on the predicted temperature difference in the probe sheath. The 2°K temperature difference in the environment corresponded to a temperature difference along the probe of 1.94°K for Model A and 1.77°K for Model B.

Based on this work, the length of vertical subdivisions did not exceed 2 cm in thermal models of the lunar heat flow probe in the regions near the gradient and ring sensor. This requirement also applied to thermal models of the drill casing and lunar medium in the same region.

2. Models for Thermal Conductivity Experiments

Computer models were developed to describe the thermal performance of the heat flow probe at four experiment locations during the two modes of operation. These models were developed to enable simulation of the probe thermal performance during tests in the Temperature Gradient Apparatus and the Thermal Conductivity Test Apparatus^{1,3} and during operation in the lunar environment.

Many of the construction details in the gradient and ring sensor regions are similar at all four locations. However, certain details are specific to each experiment location, the most important of these being the wire harnesses. As an example of the approach used to model the four experiment locations, the overall configuration of the thermal model for experiment location 1 is shown in Figure 6. Details of the gradient-sensor and ring-sensor regions, which apply to all experiment locations, are illustrated schematically in Figures 7

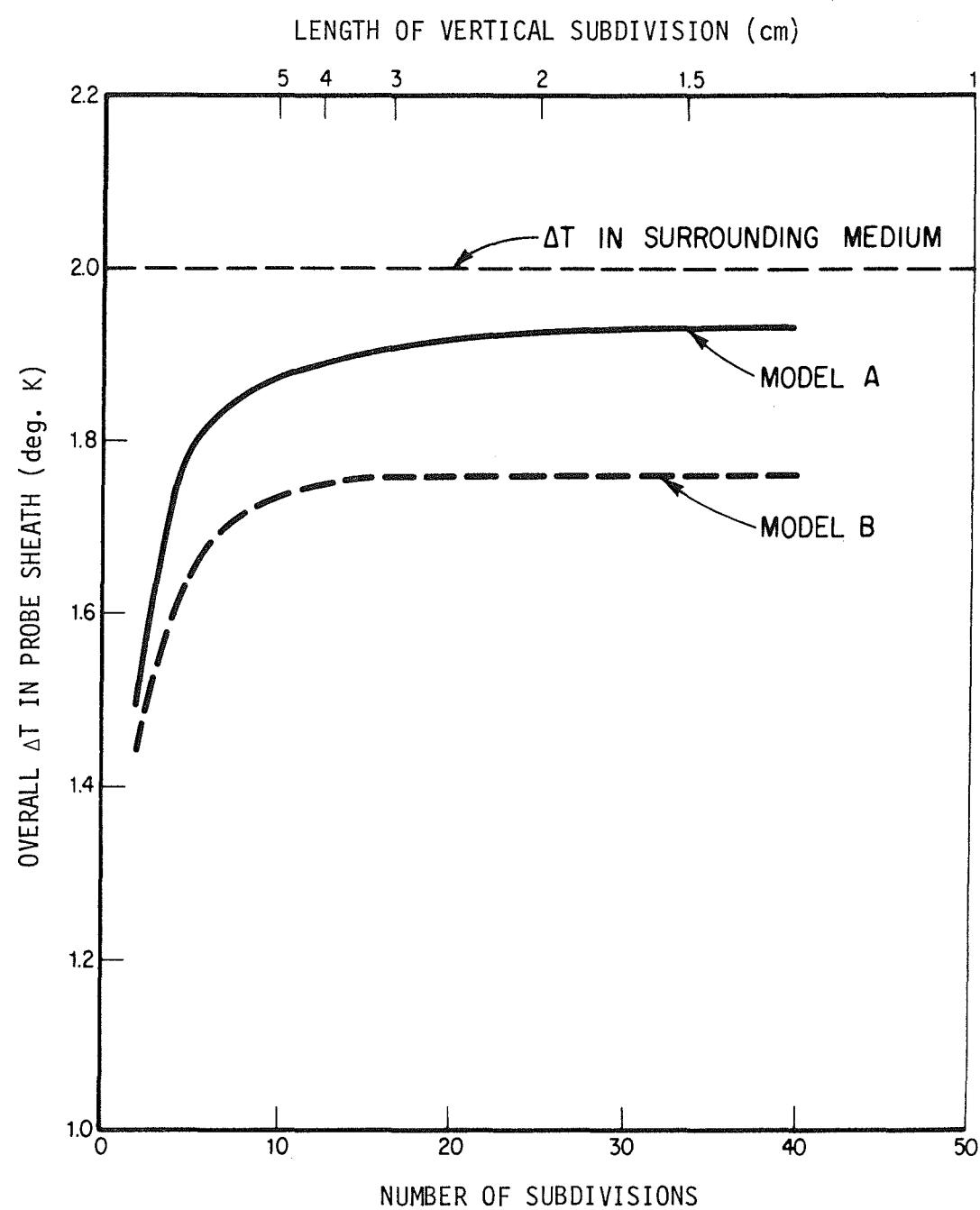
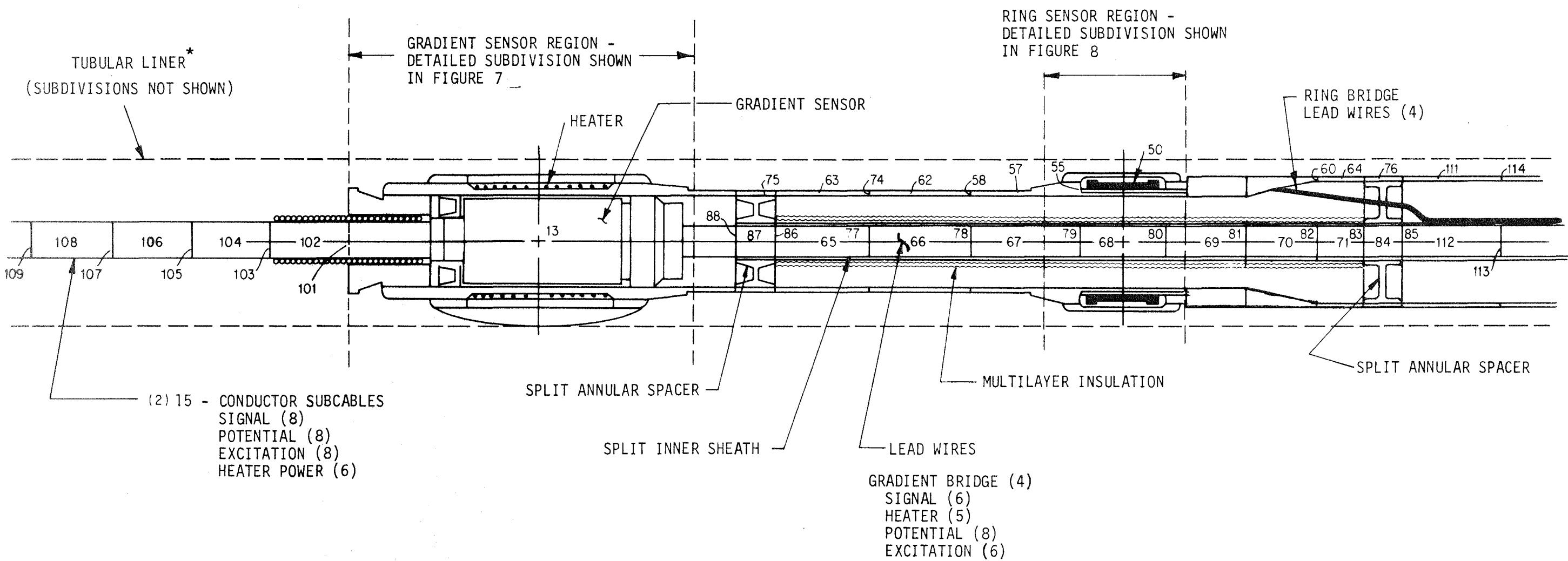


FIGURE 5 COMPUTED VERTICAL TEMPERATURE DIFFERENCE
IN PROBE SHEATH VERSUS NUMBER OF SUBDIVISIONS



* ALUMINUM TUBE IN AT TEST APPARATUS
 EPOXY-FIBER-GLASS TUBE IN K APPARATUS
 BORON-REINFORCED DRILL CASING IN
 LUNAR ENVIRONMENT.

FIGURE 6 OVERALL CONFIGURATION OF THERMAL MODEL FOR EXPERIMENT LOCATION 1

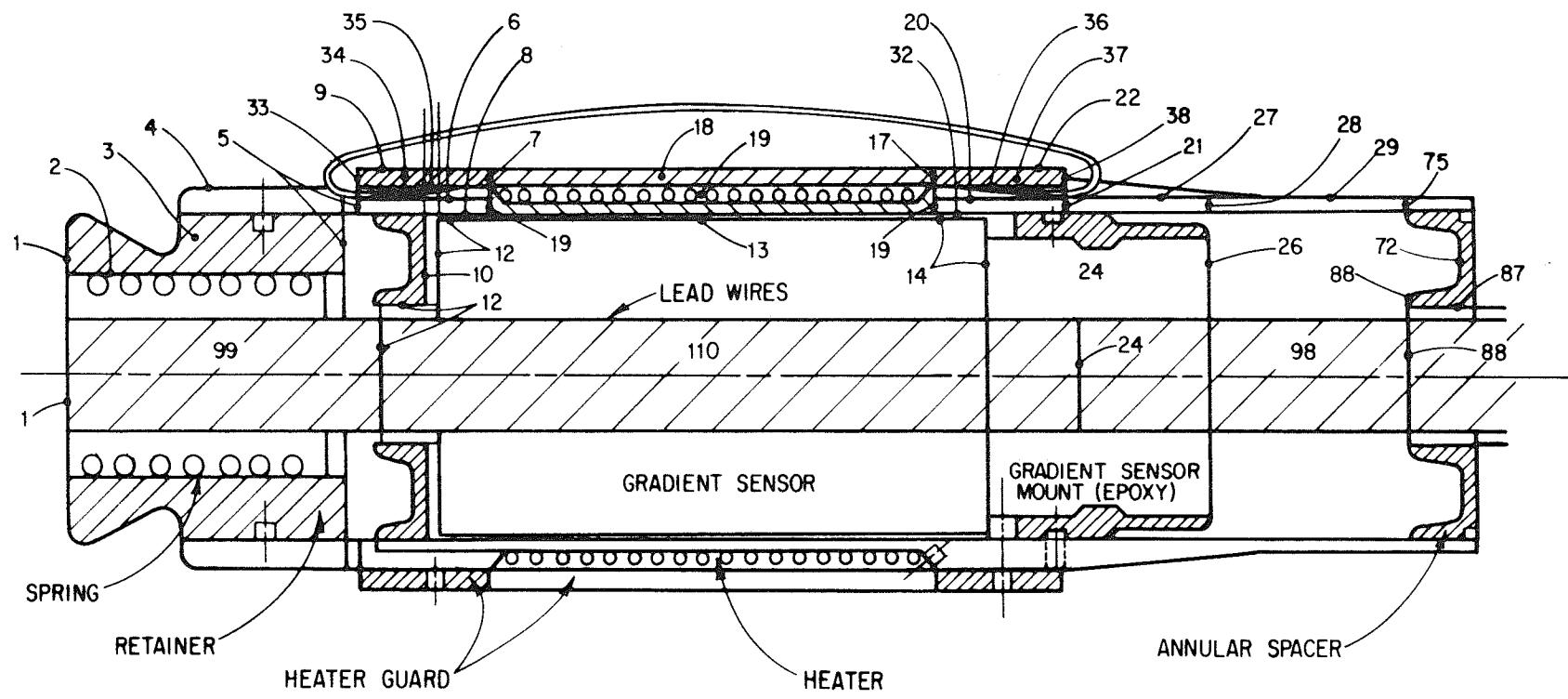


FIGURE 7 DETAIL OF GRADIENT SENSOR THERMAL MODEL

and 8. The numbers shown on Figures 6-8 are temperature subscripts identifying zones or boundaries in the thermal models of the probe. The dotted line shown in Figure 6 represents the environmental boundary which is in thermal communication with the external surface of the probe.

The arrangement of the thermal models for each of the experiment locations is shown schematically in Figure 9. Each model extends approximately 25 cm in length and includes the details of the gradient sensor, ring sensor, heater and thermal couplings at a given location. The subdivision in these models extends to regions which are essentially uninfluenced by the heater activation. The specification of boundary conditions at the ends of the models and the length of the probe chosen for modeling were checked out in early calculations.

a. Gradient Sensor

Approximately 40 equations were used to describe the heat flow in the region of a gradient sensor location (Figure 7). Most of the thermal conductances are well defined in terms of lengths and probe thermal properties. The most important parameters which determine the thermal behavior are the emittance of the heater wires, emittance of probe casing, thermal conductance of probe body, and conductance between lead wires and gradient sensor.

The model accounted for the following modes of energy interchange in the gradient sensor region:

- Conduction along epoxy probe casing -

Because of the high conductance as compared to radiant interchange between the heater sections and the gradient sensor, the major portion of heat is conducted through Zones 6, 30, 34 and 37.

- Conduction along lead wires -

Because of the snug fit between the lead wires and other elements in the gradient sensor

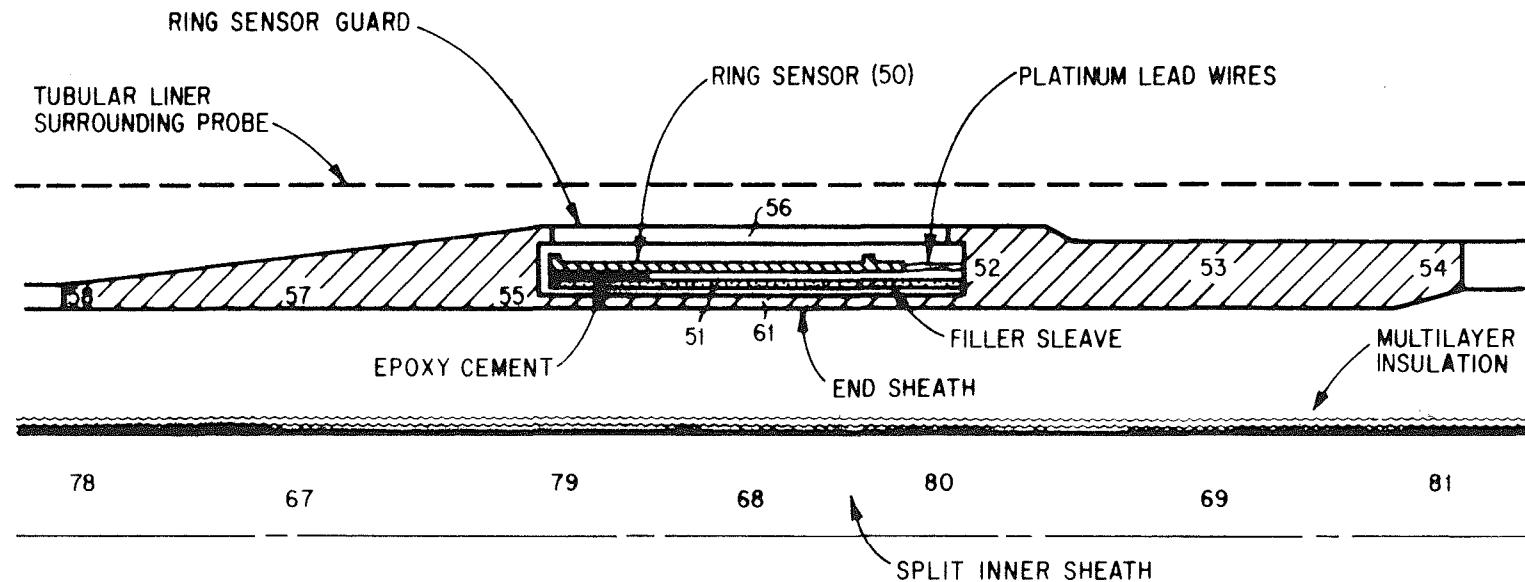


FIGURE 8 DETAIL OF RING SENSOR THERMAL MODEL

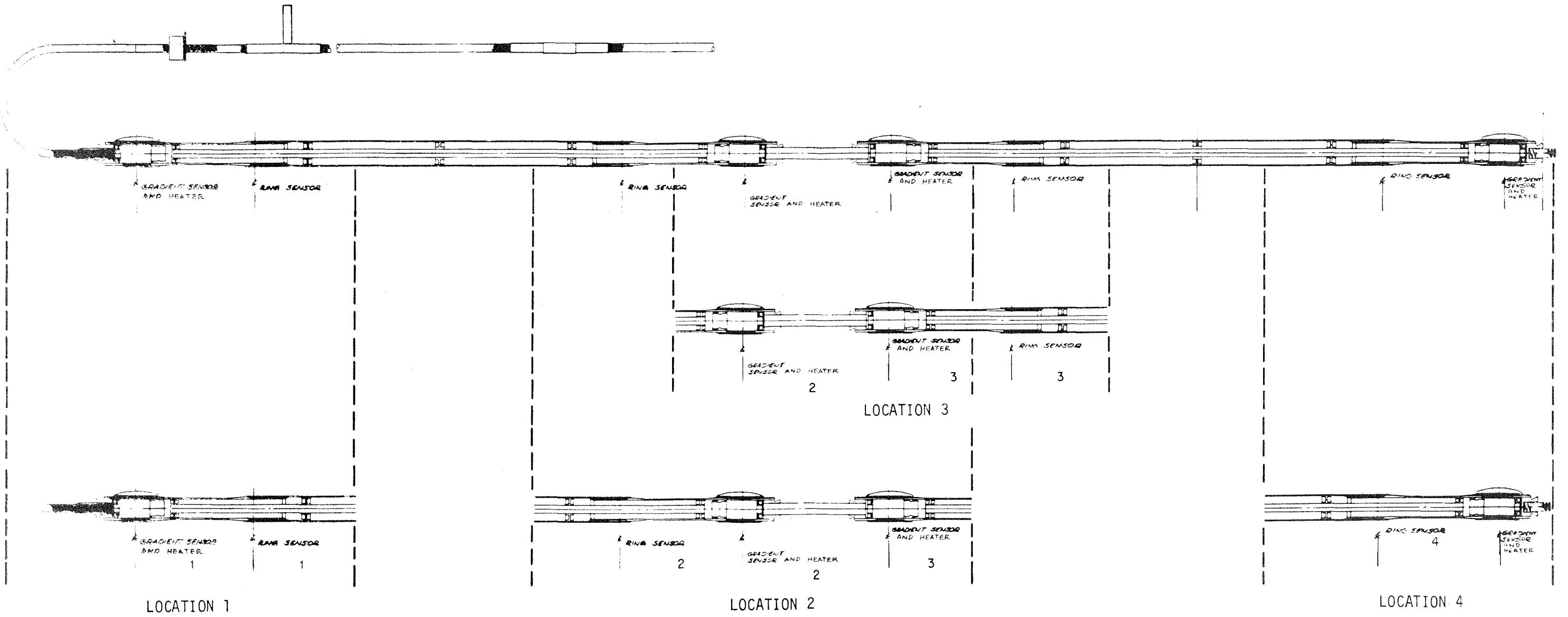


FIGURE 9 SCHEMATIC ARRANGEMENT OF THERMAL MODELS FOR THE FOUR EXPERIMENT LOCATIONS

region, the wires were considered to be heat stationed at several locations (1, 12, 24, 88). Lead wire conductance is most important in the region from the gradient sensor mount to the annular spacer.

- Radiation interchange within probe body

Zones within the probe body exchange energy with each other and with the lead wires by radiation.

b. Ring Sensor

Approximately 50 heat-balance equations described the heat flow in the ring sensor region (see Figures 6 and 8). The model description accounted for the following important characteristics which govern the thermal performance of the ring sensor:

- Radiation heat transfer between the ring sensor and the ring sensor guard, drill casing, and filler sleeve.

The ring sensor is radiatively coupled to the ring sensor guard. It is also radiatively coupled* and thermally coupled via four platinum lead wires to a filler sleeve which supports it.

- Radiant heat transfer between the filler sleeve and end sheath.

The filler sleeve, in the region of the ring sensor, is radiatively coupled to the end sheath.*

* Across a 1 1/2 to 3 1/2-mil radial clearance.

- Radiant heat transmission along the annular space formed by the internal surface of the end sheath and the external surface of the insulated split inner tube.
- Conduction heat transfer along probe body and lead wires (not shown on Figure 8).

Wire harnesses thermally coupled to the gradient sensor are routed inside and epoxied to the split inner tube. Bridge wires, spliced to the four platinum lead wires on the ring sensor, pass through the filler sleeve to the annular spacer beyond the ring sensor. The bridge wires continue along the outside surface of the split inner tube to another annular spacer midway between two heater locations on a half probe.

C. Modeling of Lunar Medium

Computer models were developed to represent the lunar medium surrounding the heat flow probe. The medium was constructed to be infinite in extent in all directions. The heat flow was assumed to be two-dimensional in the radial and vertical directions and to have radial symmetry, since the heat flow in the probe is radially symmetric.

The lunar medium surrounding the probe was modeled as many layers of concentric annuli of varying radial thickness and equal vertical length. Finite-difference equations written for the annular zones and the heat flow equations required at the boundaries of the medium are presented in Appendix III.

Figure 10 illustrates a typical annular element. The vertical height, λ , of each element was chosen to be a constant whose value depends on the thermal properties of the medium and the operating mode of the conductivity experiment. Studies showed that the accuracy of calculations could be enhanced if two separate models of the lunar medium were developed--one tailored for simulation of the Mode 2 experiment (low power, low conductivity) and the other for the Mode 3 experiment (high power, high conductivity).

Because of the rapid attenuation of a thermal wave within the medium, the thickness of each zone varies with the radial distance, r . The radial temperature distribution in a medium for analogous physical problems (point or spherical-surface heat sources in an infinite medium) varies approximately as $1/r$. Hence, in the finite-difference models the ratio of outer-to-inner radii (b/a) of a typical annular element was chosen to vary as r :

$$b = c_2 a$$

where c_2 is a parameter.

Figure 11 shows the model of the lunar medium surrounding a probe experiment location. The intersection of the horizontal and vertical centerlines of the medium coincide with the center of the heater at the experiment location. The number of vertical subdivisions M , the number of concentric annuli, N , and values of the quantities c_2 and λ define the geometrical configuration of the medium and the number of locations or nodes that require descriptive heat flow equations. The values of these parameters which were used to define the surrounding medium are summarized in Table I.

To assist in the preparation of data cards describing the lunar medium heat flow, an automatic numbering system was adopted for identifying each zone. Figure 12 illustrates this system. Each zone is identified by the indices I and J where the maximum value of J is an odd number so that the innermost element of the central layer surrounds the gradient sensor. In Figure 12 the plus signs represent

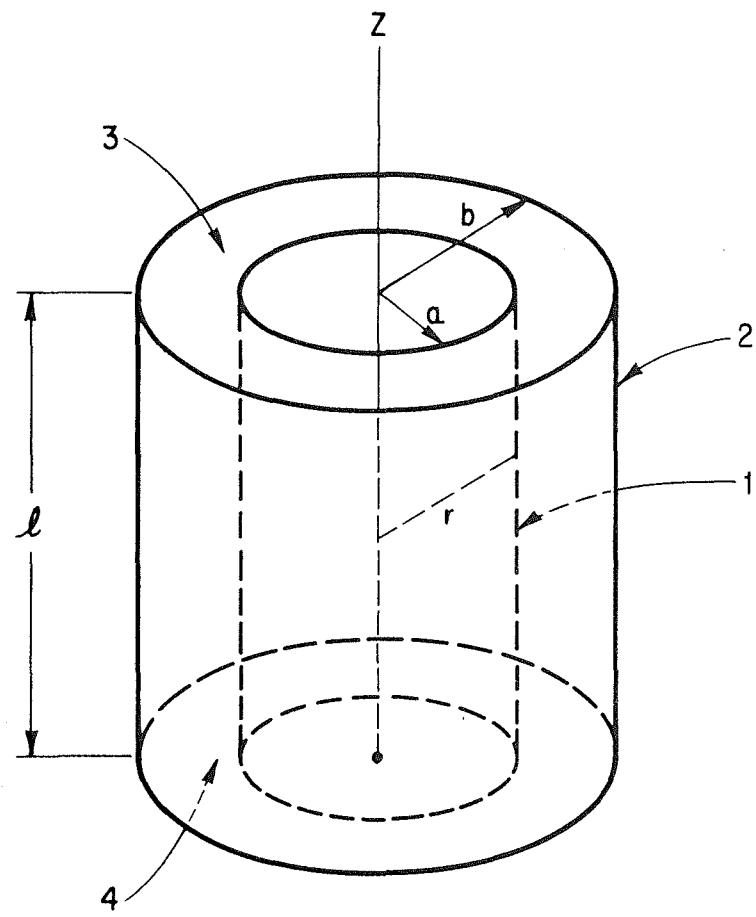


FIGURE 10 ANNULAR CYLINDER ELEMENT OF LUNAR MEDIUM

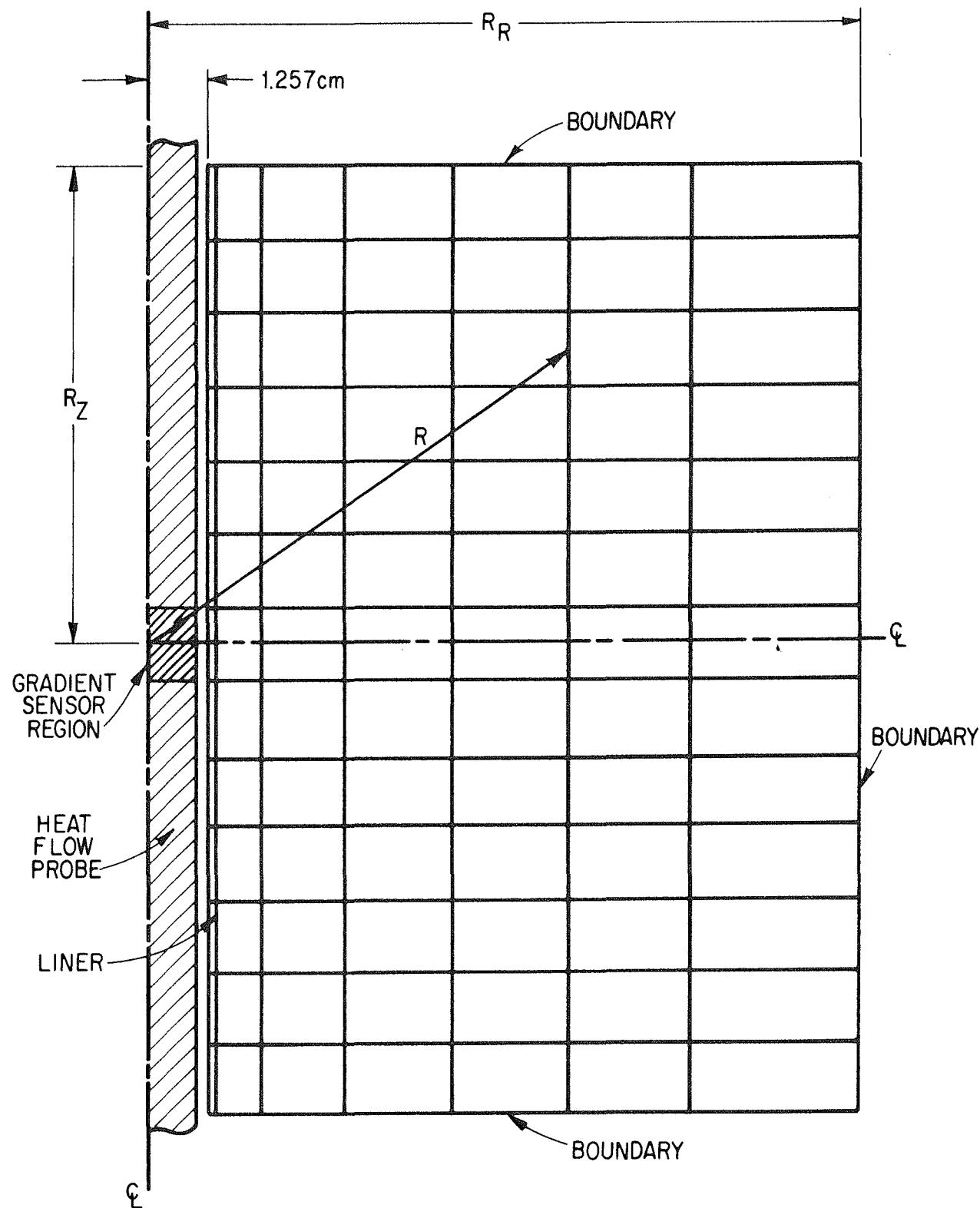


FIGURE 11 SCHEMATIC DIAGRAM OF FINITE-DIFFERENCE MODEL FOR 2-DIMENSIONAL MODEL OF LUNAR MEDIUM

TABLE I
SUMMARY OF PARAMETERS FOR
LUNAR SURROUNDINGS OF PROBE

<u>Quantity</u>	<u>Mode 2</u>	<u>Mode 3</u>
ℓ , length of vertical subdivision (cm)	1.091	1.846
M, number of vertical subdivisions	13	15
N, number of radial subdivisions	5	6
c_2 , ratio of outer-to-inner radius of each annulus	1.367	1.512
Number of finite-difference heat flow equations describing lunar medium	213	291

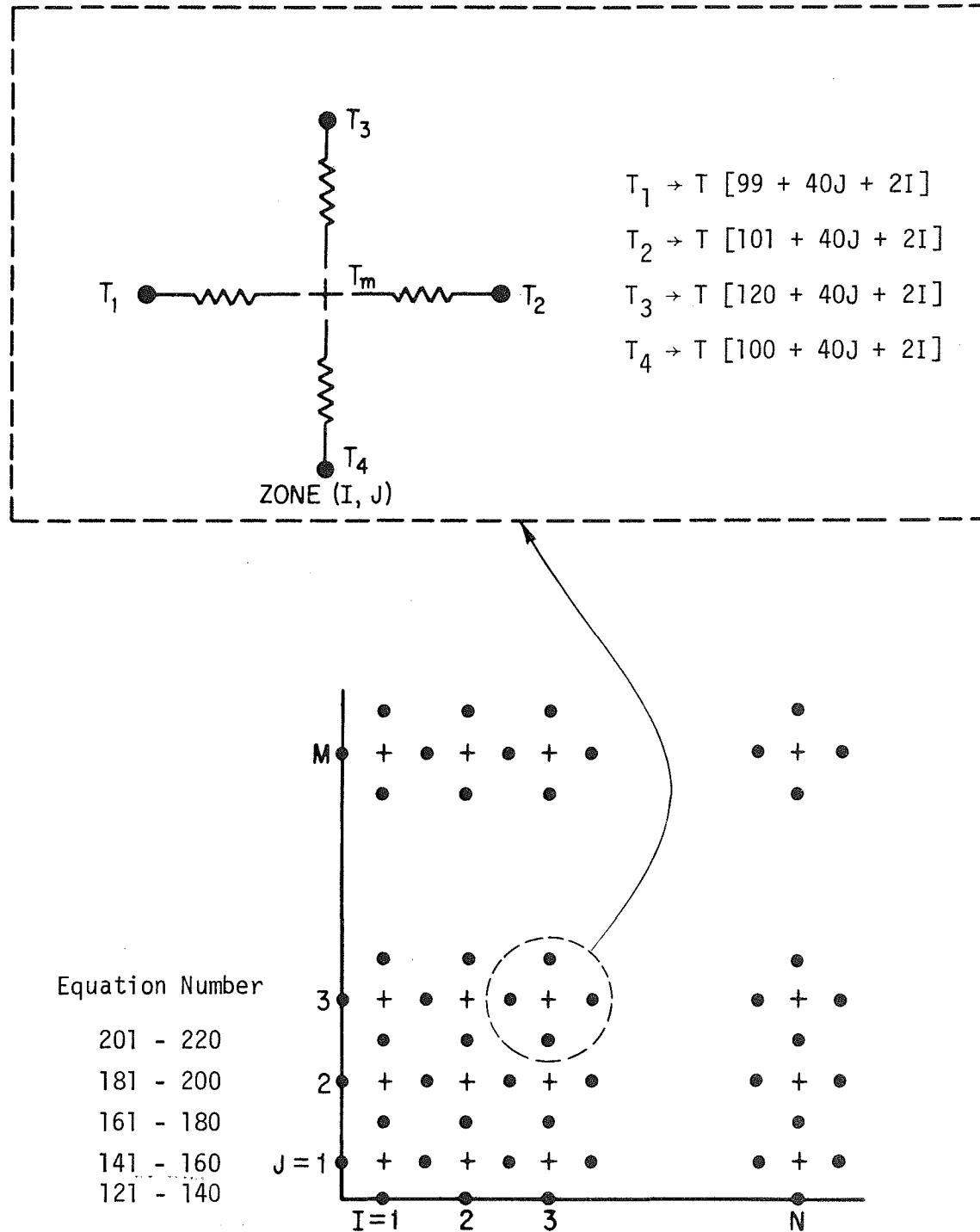


FIGURE 12 NUMBERING PATTERN FOR TEMPERATURE LOCATIONS (See Text)

the mean temperature node, while the dots represent the surfaces shown as 1 through 4 in Figure 10.

D. Tubular Liner

A description of the liner is required to complete the modeling of the conductivity experiments. The liner is important to the test performance of the probe and the performance in the lunar environment.

An epoxy-fiber-glass tube (called a bore tube in previous references) is imbedded in a medium of glass beads contained in the Thermal Conductivity Test Apparatus.³ It was assumed that the thermal coupling between the probe and the bore tube was purely radiative. This is consistent with the original conceptual design of the probe and the clearance provided by the 1-inch inside diameter of the bore tube.* Also, since the glass beads in the K Apparatus were compacted, it was assumed that the external surface of the tube and the inner boundary of the medium were well coupled thermally and were equal in temperature. Heat flow equations were written to describe the longitudinal conduction of heat along the tube and its radiative interchange with the heat flow probe. The vertical subdivisions in the tube were the same as those in the lunar model. Parameters and zone identification numbers associated with the model for the liner are summarized in Table II.

Although the configuration of the experiment in the lunar medium is apparently similar to that in the K Apparatus, there are some basic differences associated with the lunar drill casing. The drill casing is approximately four times as conductive as the bore tube. In addition, the 7/8-inch inside diameter of the drill casing is

* The validity of the assumption was also confirmed by the agreement between computer-predicted and test results when the probe was inserted in a 1" ID tube which was temperature-controlled.

TABLE II

DESCRIPTION OF PARAMETERS FOR
THERMAL MODELS OF TUBULAR LINER

<u>Parameter</u>	<u>Mode 2</u>	<u>Mode 3</u>
Number of vertical subdivisions	13	15
Length of vertical subdivisions (cm)	1.091	1.846
Identification numbers for thermal zones	141, 181, ... 621	141, 181, ... 701
Identification numbers for zone boundaries	123, 163, ... 643	123, 163, ... 723
Zone on centerline of probe heater	381	421

smaller than the corresponding dimension for the bore tube. This smaller dimension introduces some uncertainty in contact conductance to the three alignment springs situated at each heater location (see Figure 6). The overall diameter of the circular envelope defined by the extension springs exceeds 7/8-inch.* Contacting between the springs and the inside of the drill casing could provide another path for transfer of heat from the probe heater to the drill casing. There is also some uncertainty as to the exact nature of the thermal coupling at the interface between the external surface of the drill casing and the lunar material.

For the performance predictions in the lunar medium prepared to facilitate real-time data reduction, it was decided that the drill casing would be modeled according to the same guidelines developed for the bore tube. A limited number of parametric calculations were made to investigate the effect of the above-mentioned uncertainties on the thermal performance of the probe.

* No flight-configuration casings, or tubular liners with a 7/8-inch inside diameter have been used in probe performance tests.

IV. EVALUATION OF COMPUTER MATHEMATICAL MODELS

A. Surrounding Lunar Medium

The finite-difference method of modeling the thermal resistance of the lunar medium was evaluated by comparing computer predictions with available exact solutions for the line heat source problem and the spherical surface source problem. The formulation of these problems, and the results will be discussed separately in the present section.

1. One-Dimensional (Line Source) Problem

Finite-difference models were formulated for the problem of a thin, cylindrical heat source surrounded by a medium composed of concentric annular rings. Numerical calculations were compared with exact solutions for the problem of a line heat source in an infinite medium. The motivation for this study was to determine the requirements of radial subdivision in the lunar medium appropriate for accurate temperature predictions at regions close to the source of heat. For this purpose, the one-dimensional problem is more meaningful for the spherical-source model.

Figure 13 illustrates the radial subdivisions in the finite-difference model. Due to the differences in heat source power, thermal conductivity levels and important locations in the lunar medium, two finite-difference models were selected--one appropriate to each operating mode of the conductivity experiments. In the Mode 2 experiment accurate temperature predictions at locations near the source (i.e., near the heater and gradient sensor) are important. In the Mode 3 experiment accurate temperature predictions at remote locations from the source (i.e., near a ring sensor location) are important. Consequently, in the following discussion comparisons between exact and numerical solutions will be important at a radius of approximately 1.27 cm for the Mode 2 operation and at a radius of approximately 10 cm for the Mode 3 operation.

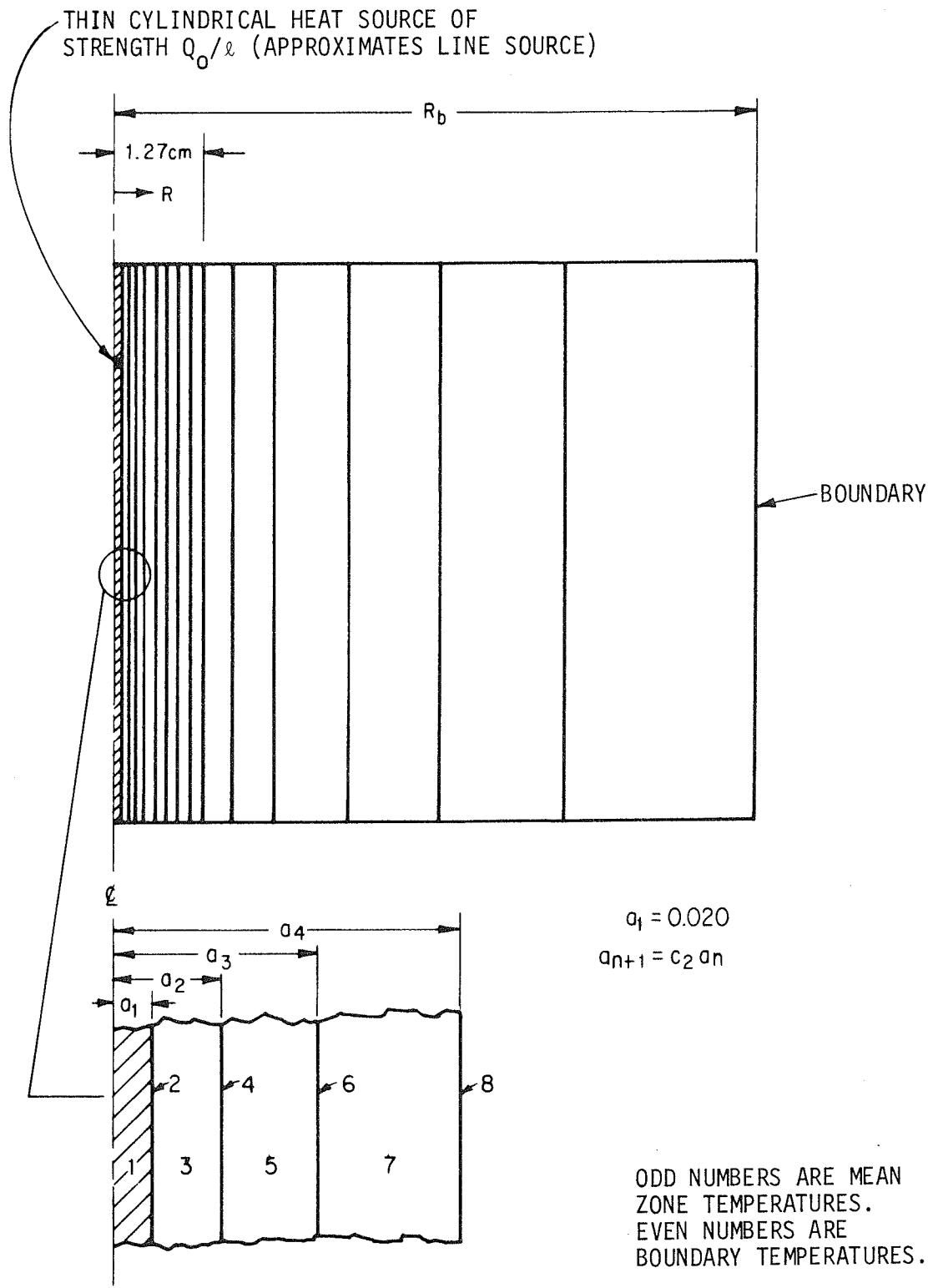


FIGURE 13 SCHEMATIC DIAGRAM OF FINITE-DIFFERENCE MODEL FOR LINE SOURCE PROBLEM

Figure 14 illustrates a comparison of temperature rise versus time for the Mode 2 finite-difference model and the exact model of the line source problem. The solid line corresponds to the exact solution at a radial location of 1.274 cm, and the circled symbols represent the values predicted with the computer program. The close agreement between exact and finite-difference models demonstrates that sufficient detail in the finite-difference model can be obtained using only five radial subdivisions.

Figure 15 illustrates exact and predicted values of temperature rise in the lunar medium at conditions corresponding to Mode 3 operation of the probe. The temperature rise at a distance of 10 cm from the heat source showed excellent agreement with the exact solution over the time span of solution. Six radial subdivisions were judged to give sufficient detail in the thermal model of the lunar medium.

2. Two-Dimensional Model of Lunar Medium

Two-dimensional, finite-difference representations of the lunar medium were made as described in Section (III-C). To evaluate these models, the lunar medium was considered to occupy the central core otherwise occupied by the heat flow probe and drill casing - see Figure 11 - with a cylindrical heat source located at the region corresponding to the gradient sensor. Calculations were performed for the temperature rise in an initially isothermal medium. These results were compared to analytical solutions for the spherical surface source.

In reviewing comparisons here between the computed results and the exact solution, it is important to consider the following:

- 1) In the finite-difference model, the heat source has the shape of a solid circular cylinder, while the exact solution applies to a spherical surface source. This difference should be most important at regions in the lunar medium close to the heat source. Checks on the

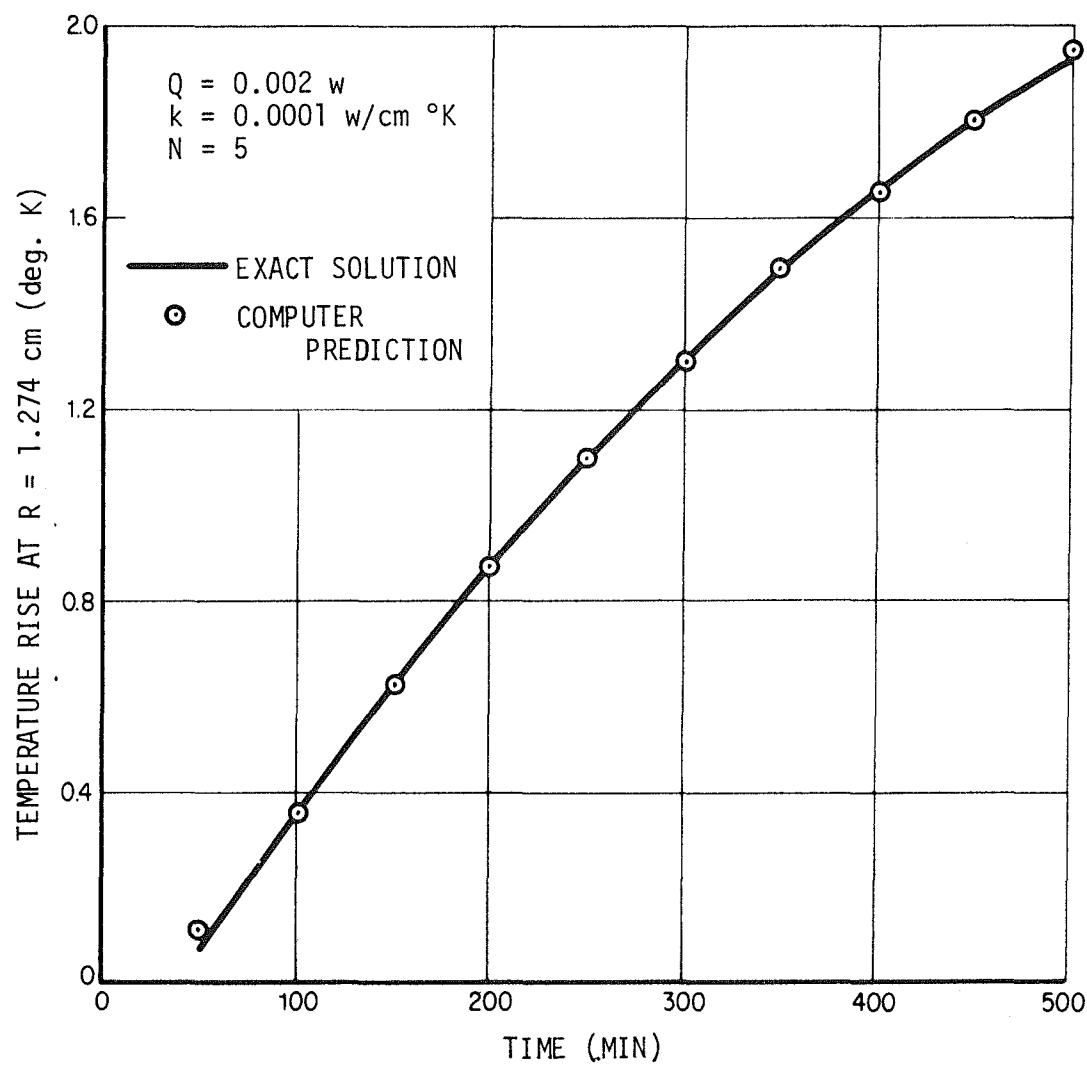


FIGURE 14 TEMPERATURE RISE VERSUS TIME FOR MODE 2 MODEL OF LINE SOURCE PROBLEM

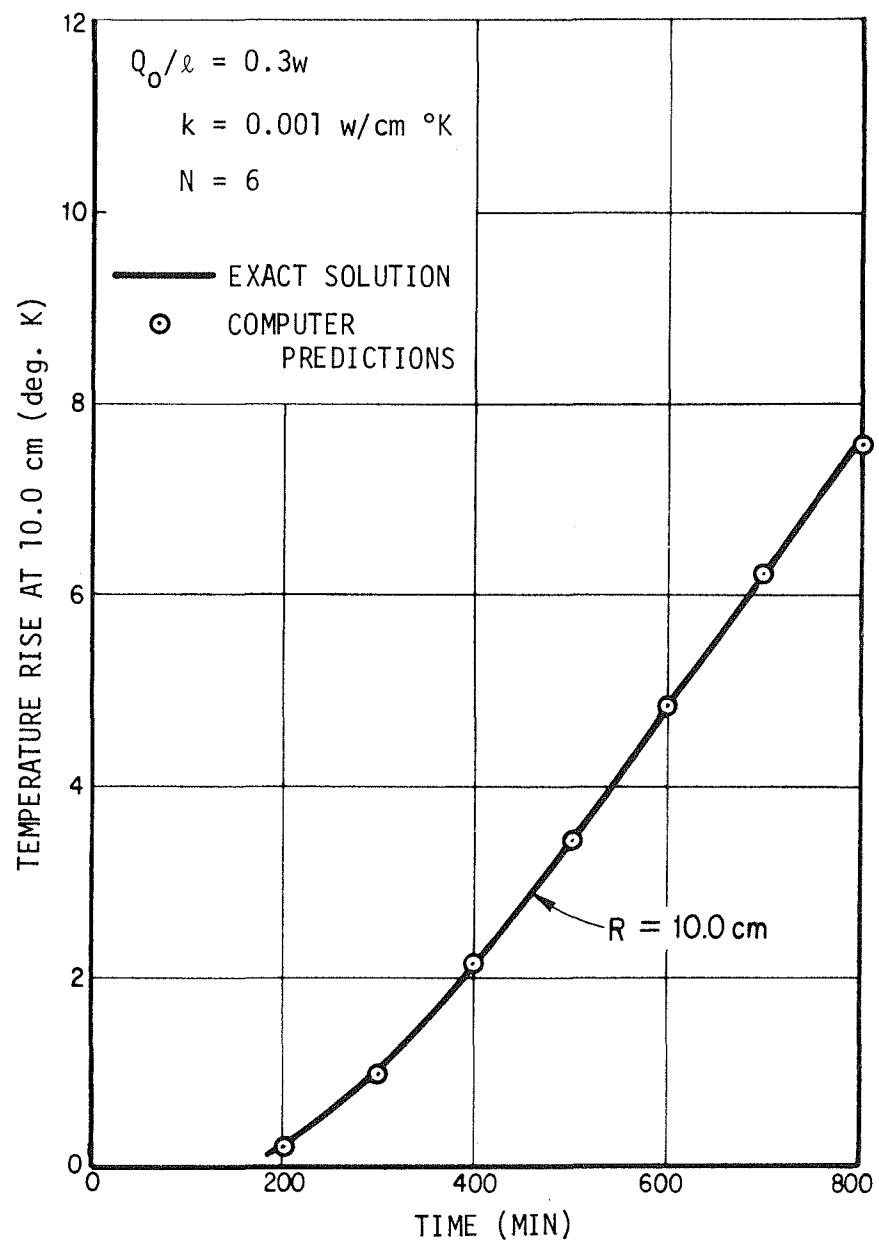


FIGURE 15 TEMPERATURE RISE VERSUS TIME FOR MODE 3 MODEL OF LINE SOURCE PROBLEM

subdivision close to the source were made in the work described above for a one-dimensional problem, where the geometrical difference between exact and finite-difference source is small.

- 2) Comparisons between exact and finite-difference models are made as a function of R , the distance from the center of the source to the location of interest in the lunar medium. We calculate R in the finite-difference model as the distance to the center of a radial boundary of an annular cylindrical zone. The computed temperature of this surface is the temperature averaged over the surface and is not necessarily equal to the center temperature of the surface.

Since the heat flows at the boundaries are determined as a function of the absolute distance from a spherical surface source, it is of interest to examine the computed results from the standpoint of radial symmetry. Figure 16 shows the radial temperature distribution in the lunar medium for a Mode 3 model at a time of 500 minutes. The solid curve corresponds to the values computed from the exact solution; the dotted symbols represent values computed using the finite-difference model. Values obtained from computer solution apply to position vectors extending in various angular directions to locations in the lunar medium. The close agreement between exact and computed values indicates that the Mode 3 model accurately predicts the radial temperature distribution in the lunar medium.

Figure 17 shows a comparison of exact and computed temperature rise at $R = 8.811$ cm, as a function of time up to 1,000 minutes. The computed values shown on this curve were obtained for several values of N , the number of radial subdivisions in the lunar medium, and α , an integration parameter used in the numerical solution of the

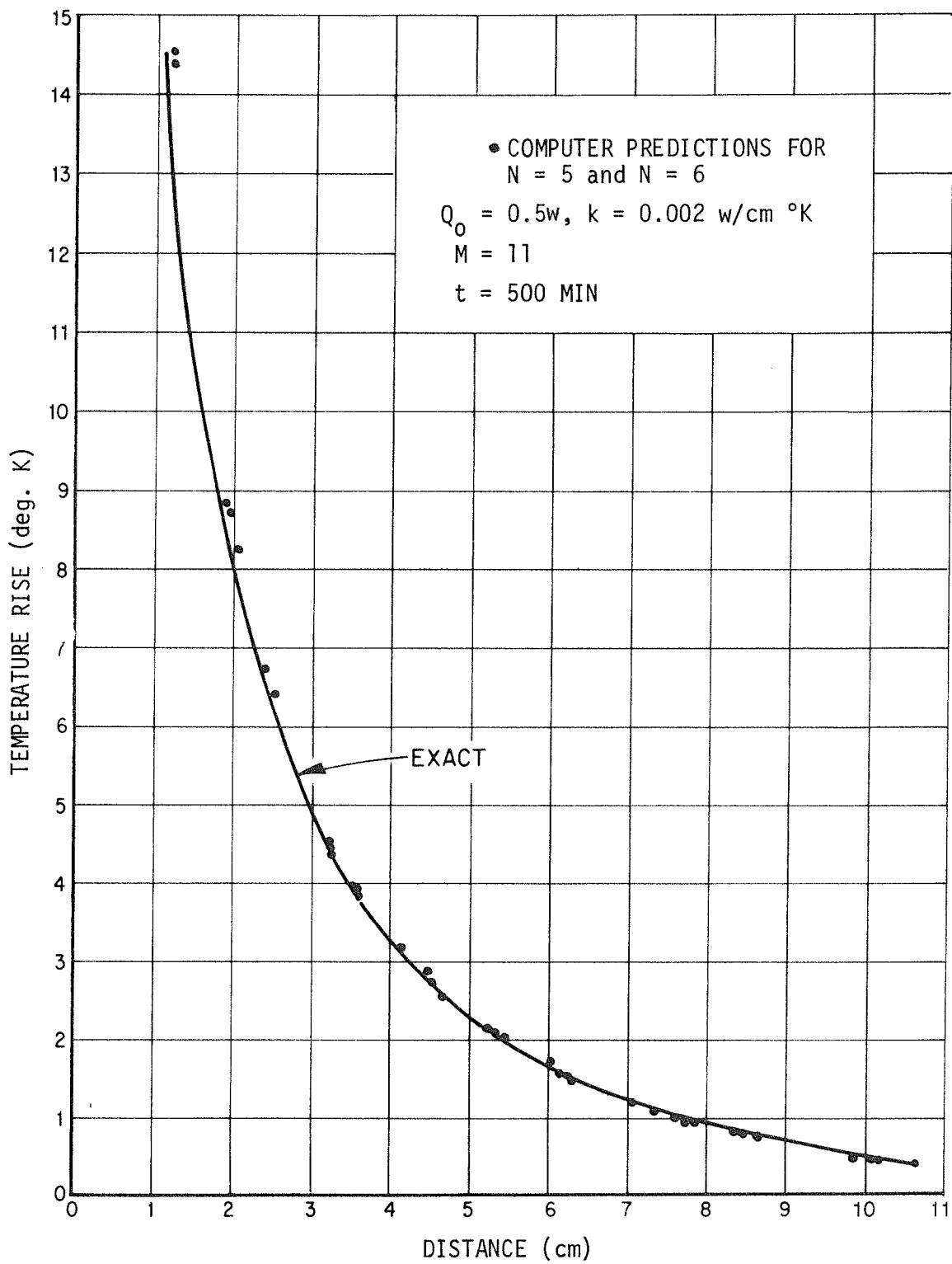


FIGURE 16 TEMPERATURE DISTRIBUTION IN MODE 3 MODEL OF LUNAR MEDIUM

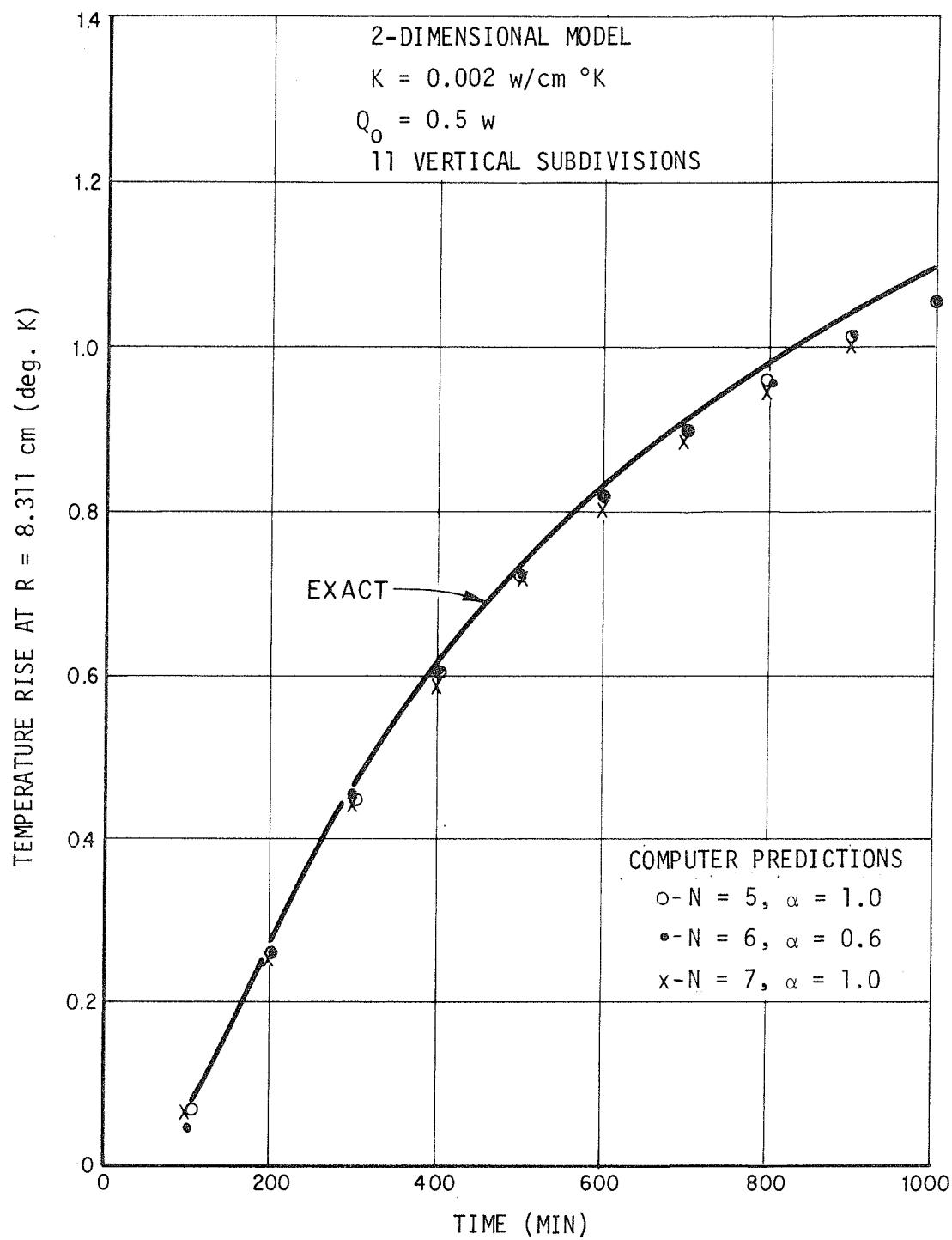


FIGURE 17 TEMPERATURE RISE VERSUS TIME FOR MODE 3 MODEL OF LUNAR MEDIUM

finite-difference equations by ADLGTA. (A discussion of the integration parameter α is included in Appendix I.)

The computed values of temperature rise show a slight but small dependence on the integration parameter. Results computed for other cases not shown here reveal that the most accurate solutions are obtained using large values of α . Subsequently, the calculations were performed using a value of $\alpha = 1.0$.

The agreement between exact and computed values of temperature rise is good up to times of 500 minutes. As time increases, the computed results begin to have a small deviation from the exact solution. It is believed that the deviation results from the difference in the source geometries discussed earlier. The uncertainties which arise because of this deviation are small compared to other uncertainties which can arise when analyzing the entire experiment.

B. Lunar Probe

The heat flow probes have built-in instrumentation for monitoring the temperature responses of gradient and ring sensors. Although tests were not designed or instrumented specifically for the purpose of providing detailed checks on the computer models, several tests were conducted for performance evaluation of the heat flow probes under other subcontracts.^{1,3} Available data for the responses of gradient and ring sensors at particular locations during performance tests were used as a check on the probe computer models, prior to performance predictions in the lunar environment.

Two types of tests which were performed in the Arthur D. Little, Inc., HFE Thermal Test Facility³ provided information useful for comparisons with predicted results. One series of tests was conducted in a Temperature Gradient Test Apparatus, where the probe was surrounded by a temperature-controlled, near-isothermal, aluminum tube. Another series of tests was performed in the Thermal Conductivity Apparatus where the probe was surrounded radially by a bore tube and a

medium comprising glass beads with interstitial gas. In this test procedure the pressure of the interstitial gas (helium or nitrogen) was varied between approximately 1μ and 1 atmosphere to simulate a range of thermal conductivity levels in the glass-beaded medium. An evacuated medium simulates a low thermal conductivity, in the range of Mode 2 operation, while a helium or nitrogen-filled medium simulates a high thermal conductivity, typical of the range for the Mode 3 operation of the experiment.

The tests in the ΔT apparatus provided a useful means for checking the ability of the computer models to predict Mode 2 performance of the probe. In these tests, one possible uncertainty was minimized--the thermal conductivity of the surrounding medium. The Mode 2 tests in the K Apparatus for low values of simulated conductivity provided only qualitative information and were not applicable for verification checks on the computer models. Interpretational difficulties with the Mode 2 tests in the K Apparatus are described in Reference 3.

Mode 3 tests in the K Apparatus for helium-filled and nitrogen-filled (at 1 atm) glass-bead beds were not subject to interpretational difficulties and were used for comparison with computer predictions.

1. Predicted Performance for Mode 2 Operation in the ΔT Apparatus

The computer model for the heat flow probe was evaluated by predicting gradient sensor temperature rises for Mode 2 operation in an isothermal environment and comparing them with corresponding measured values obtained from tests performed in the ΔT apparatus. Comparisons between experiment and theory were made for all six test conditions included in the Group I series of tests reported in Reference 3. The gradient sensor temperature rises were measured at all four experiment locations at one environmental temperature level; performance data for experiment location 2 was obtained at two additional temperature levels.

Table III presents test results and computer predictions for the gradient sensor temperature rise. At a temperature level of 224.4°K, the agreement between test and theory is within 4% for all locations. The maximum deviation between computer model predictions and experiments was obtained at the high temperature condition at location 2.

A comparison between predictions for the transient temperature response and test results from the ΔT apparatus is shown in Figures 18 and 19 for all four experiment locations and an environmental temperature level of 224.4°K. The agreement between experiment and theory is good over the total time to reach steady conditions.

Calculations were also made to evaluate the influences of uncertainties in probe thermal characteristics specified in the computer model. The influence of these uncertainties on the predicted gradient sensor temperature rise in an isothermal environment are summarized in Table IV.

The most important uncertainty affecting the computer predictions of probe performance is the radiation coupling between the probe body and the aluminum bore tube. A 1 percent uncertainty in the probe emittance corresponds to nearly a 1 percent change in steady-state temperature rise.

2. Predicted Performance for Mode 3 Operation in the K Apparatus

After the temperature calculations were performed for the Mode 3 experiment in the K Apparatus, slopes of the ring-sensor temperature were found using a simple curve-fitting technique. A parabolic equation was fitted to pass through the computed sensor temperature at a given time and through the temperatures computed in both the preceding and succeeding time intervals. The derivative of the curve then provided the slope of the temperature vs. time curve.

Figure 20 illustrates the predictions for rate of ring-sensor temperature rise versus time when the probe is surrounded by a

TABLE III
COMPARISON BETWEEN MEASURED AND PREDICTED
TEST PERFORMANCE IN ΔT APPARATUS

Experiment Location	Temperature Level °K	Temperature Rise of Gradient Sensor		Deviation %
		Test °K	Predicted °K	
1	224.4	0.1970	0.2004	1.7
	205.4	0.2640	0.2663	0.9
	224.4	0.2055	0.2127	3.5
	244.5	0.1596	0.1702	6.6
3	224.4	0.2168	0.2159	- 0.4
4	224.4	0.2248	0.2226	- 1.0

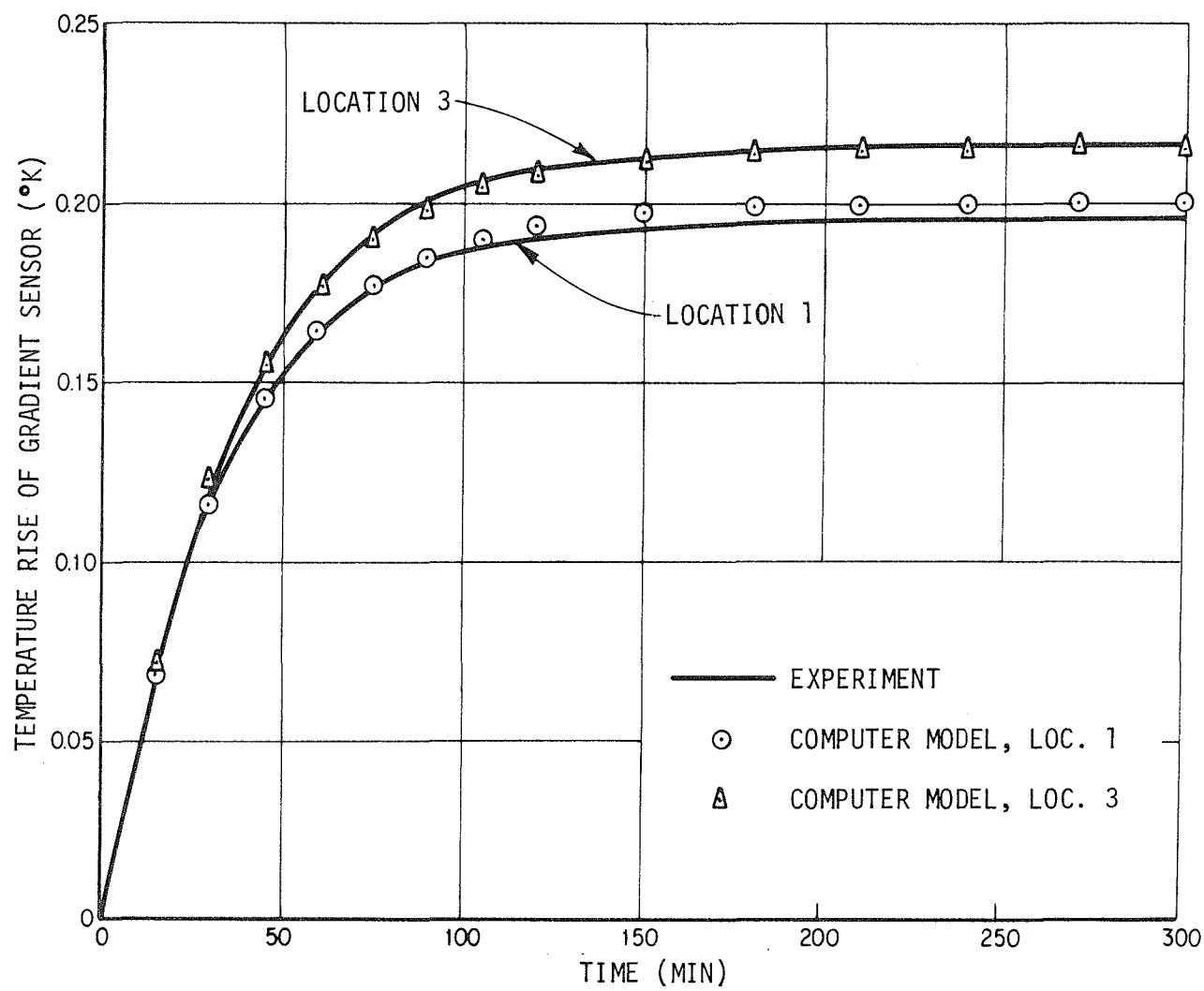


FIGURE 18 TRANSIENT TEMPERATURE RESPONSE FOR MODE 2 TESTS IN ΔT APPARATUS

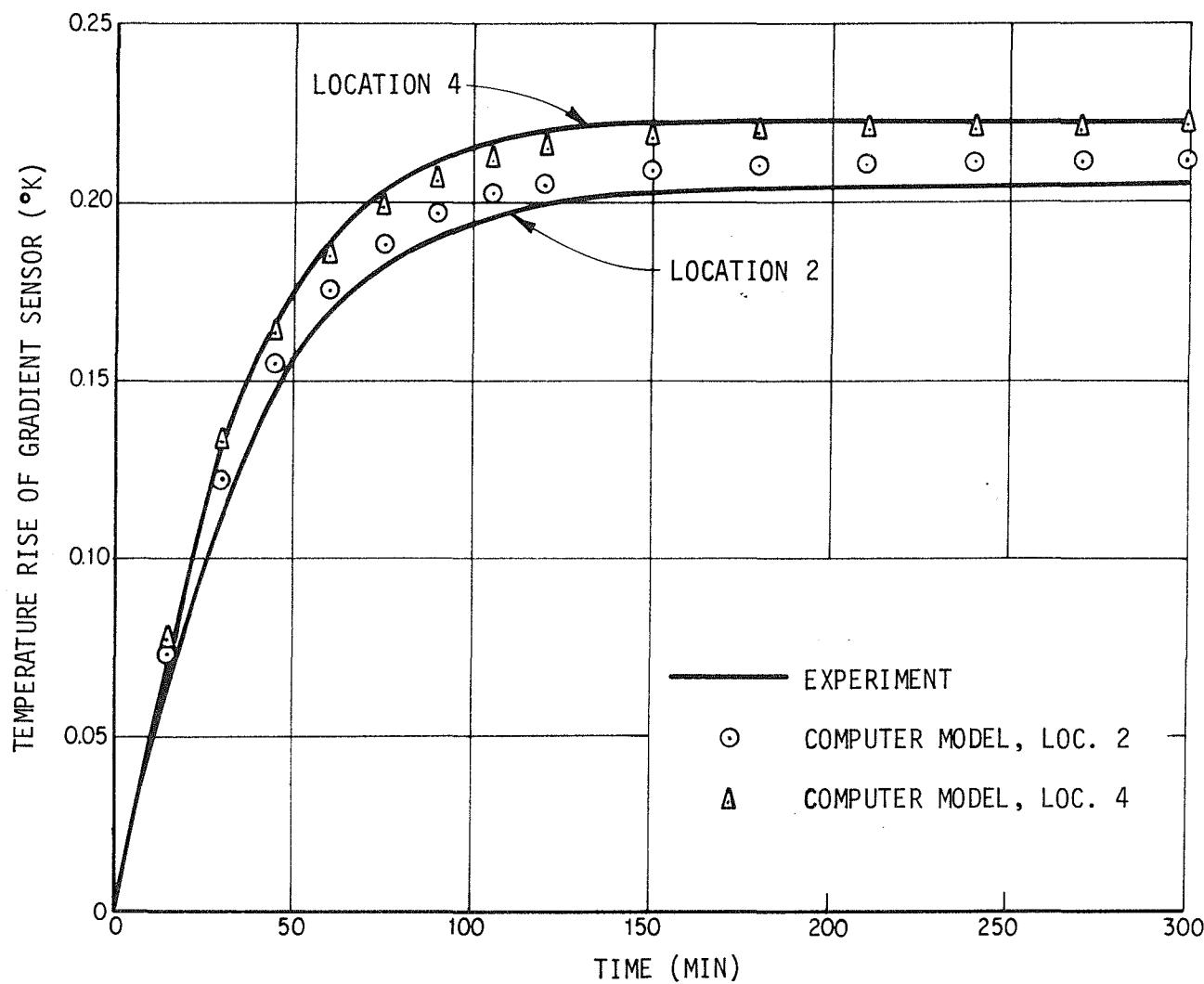


FIGURE 19 TRANSIENT TEMPERATURE RESPONSE FOR MODE 2 TESTS IN ΔT APPARATUS

TABLE IV

INFLUENCE OF UNCERTAINTIES ON PREDICTED
TEMPERATURE RISES IN THE ΔT APPARATUS

<u>Parameter</u>	<u>Change</u>	<u>Change in ΔT(%)</u>
1) Thermal conductance of probe body	Increase 10%	- 0.7%
2) Lead wire conductance	Decrease 21%	+ 0.7%
3) View area from heater to space	Increase 5%	- 1.1%
4) Emittance of sensor can	Decrease 43%	+ 0.2%
5) Emittance of probe body	Decrease 6%	+ 5.0%

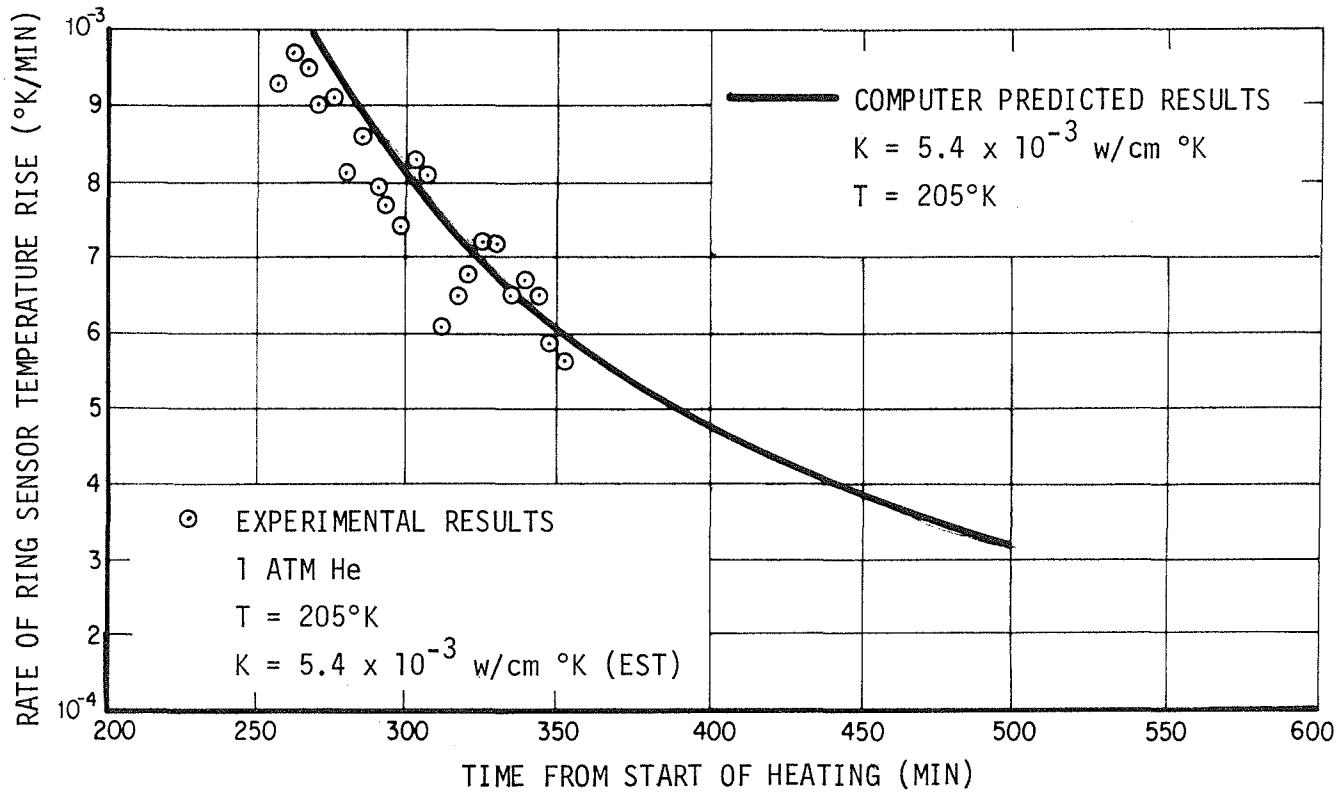


FIGURE 20 PREDICTED SLOPE OF RING-SENSOR TEMPERATURE DURING MODE 3 TEST IN K APPARATUS,
 $K = 5.4 \times 10^{-3} \text{ w/cm } ^{\circ}\text{K}$

medium having a thermal conductivity (K) of 5.4×10^{-3} w/cm °K. The rate of temperature rise is shown for times greater than 250 minutes; the values at earlier times are off-scale for the linear ordinate used. The circled points presented on Figure 20 represent test data for experiments performed in the K-1^{*} Apparatus. Close agreement is shown between computer-predicted and test results.

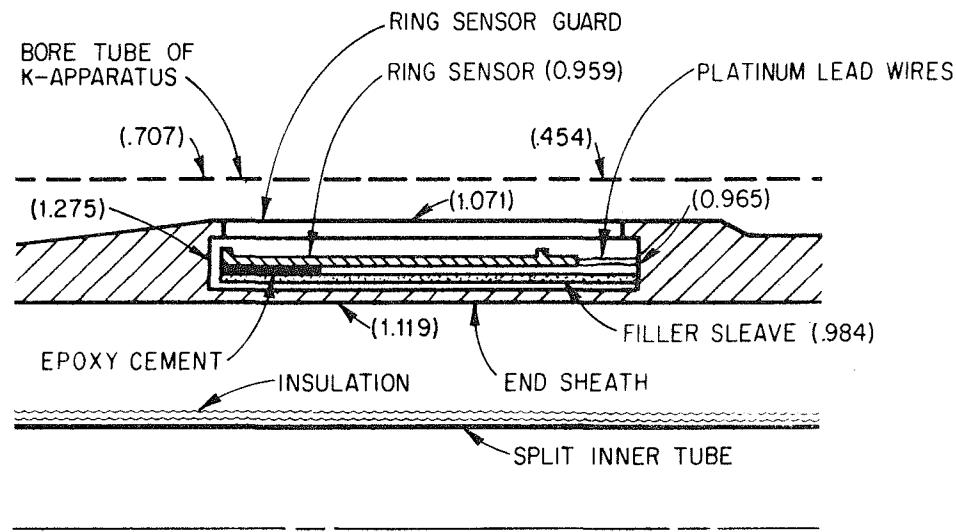
Several interesting details concerning the probe operation in a Mode 3 experiment were revealed by the computer calculations. They will be discussed here prior to the presentation of another comparison between computer predictions and test performance.

In particular, there is a net transfer of heat from the ring sensor to the bore tube. This condition indicates that heat transfer along the probe elements, between the gradient and ring sensors, is appreciable. Important heat flow paths to the ring sensor are provided by the probe sheath, lead wires and ring-bridge wires (see Figures 6 and 8).

Also, during the Mode 3 experiments, the ring sensor is surrounded by elements of the probe at slightly higher temperatures. An illustration is presented with the aid of Figure 21. The temperature rises shown for the ring sensor and other elements (filler sleeve, ring sensor guard and the end sheath) lie in a range of 0.959 to 1.119°K. For the corresponding test in the K Apparatus, the measured temperature rise of the ring sensor was 1.04°K. The radial clearance between the filler sleeve and the warmer end sheath is very small (1 1/2 to 3 1/2 mils). Contacting surfaces could provide conductive heat transfer across this apparent clearance and slightly raise the temperature of both the filler sleeve and the ring sensor.

In Figure 22 the predicted transient response of the ring sensor and the end sheath are shown in comparison with test points for the ring sensor. The test conditions ($K = 1.7 \times 10^{-3}$ w/cm °K, $T = 225$ °K) are the same as those referenced in Figure 21. The upper curve

* The Thermal Conductivity Apparatus having a 1-inch ID by 0.025-inch wall bore tube.



NOTE: NUMBERS IN PARENTHESES ARE COMPUTER-PREDICTED
VALUES OF TEMPERATURE RISE FOR THE FOLLOWING
CONDITIONS:

MODE 3, LOCATION 2 IN K APPARATUS

$$K = 1.7 \times 10^{-3} \text{ w/cm } ^\circ\text{K}$$

$$T_{\text{INITIAL}} = 225^\circ\text{K}$$

TIME AFTER START OF HEATING = 350 MIN

FIGURE 21 SCHEMATIC SKETCH OF RING SENSOR DETAIL

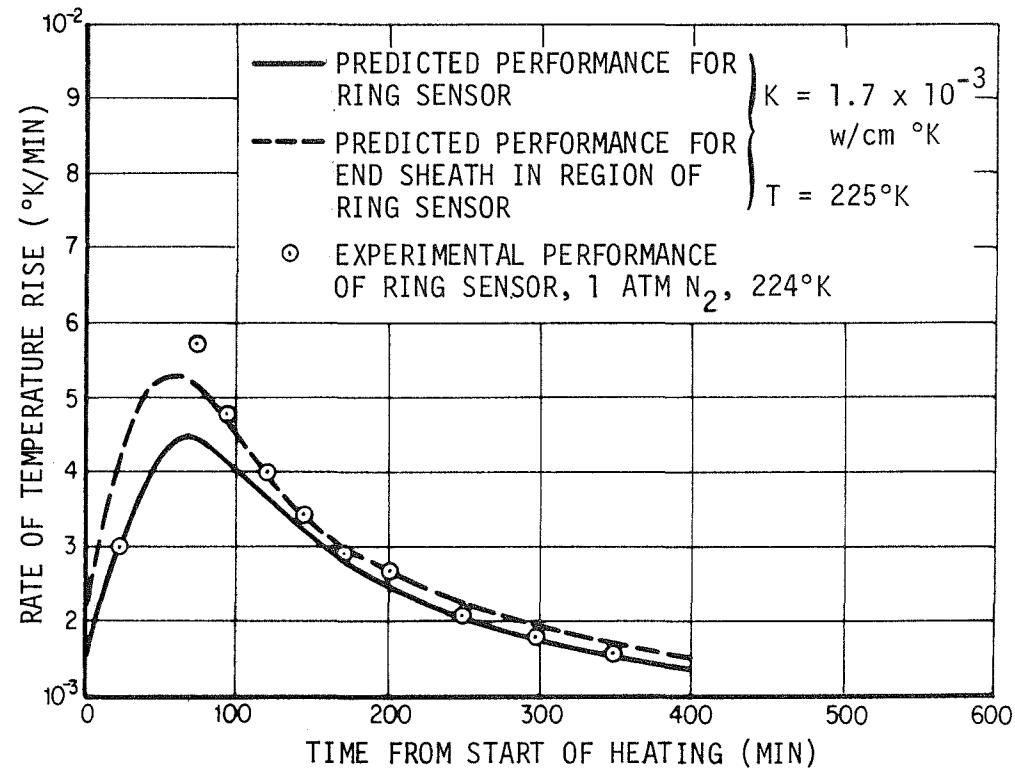
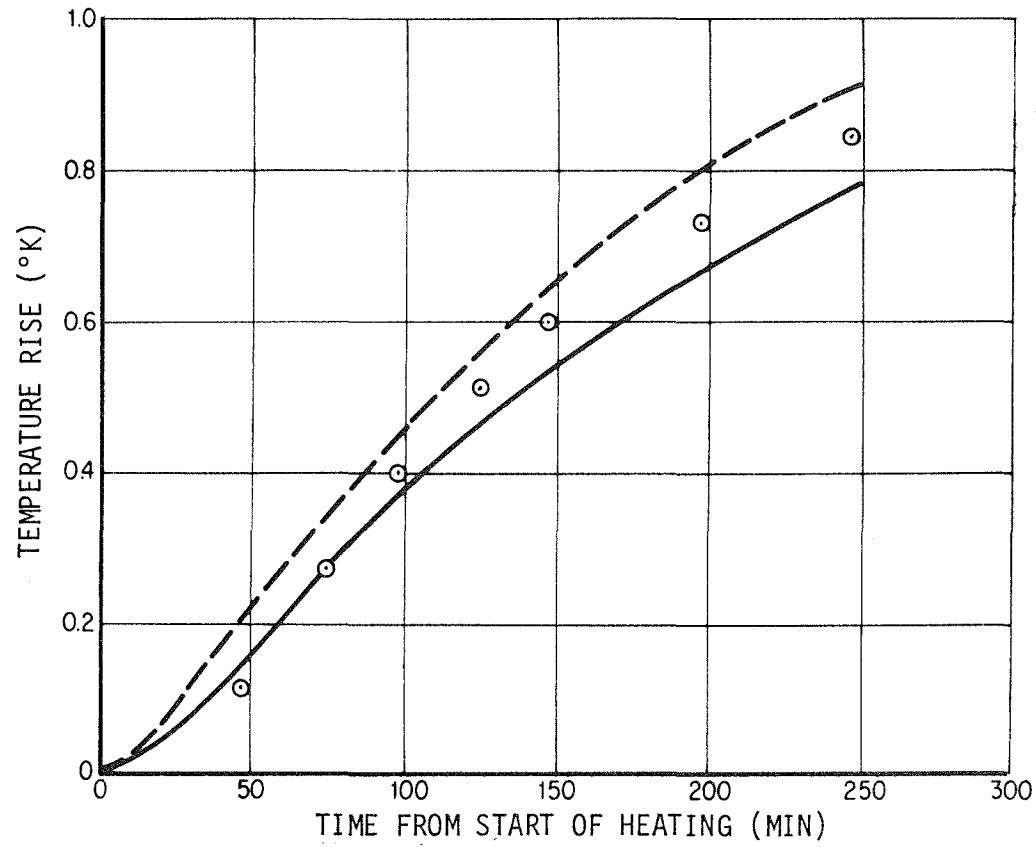


FIGURE 22 COMPARISON OF PREDICTED AND TEST RESULTS FOR MODE 3 EXPERIMENT IN K APPARATUS

in Figure 22 shows that the predicted temperature rises for the ring sensor and the end sheath bracket the ring sensor test results.

The rate of temperature rise for both the end sheath and the ring sensor are plotted in the lower curve and show close agreement with the test results.

The predictions for the Mode 3 operation of the probe indicate that the rate of ring-sensor temperature rise provides a good indication of thermal conductivity of the surrounding medium at times greater than three hours after the start of heating. At earlier times, the slope is sensitive to the thermal characteristics of the heat flow probes. A similar conclusion was drawn from results of performance tests of the probe.³

The predictions also show that the Mode 3 models of the probe and surroundings are accurate and agree with test results well within the limits of experimental accuracy. If contacting between the end sheath and filler sleeve occurs across the narrow clearance separating the two elements, it should not significantly affect the performance of the Mode 3 conductivity experiments.

V. PREDICTED PERFORMANCE IN THE LUNAR ENVIRONMENT

A. Introduction

An important objective of the performance predictions in the lunar environment was to prepare information for use as an aid to the Principal Investigator during the real-time data reduction of the Heat Flow Experiment. It was also of interest to compare the performance of conductivity experiments in the K Apparatus and the same experiment in the lunar medium.

As directed by the Principal Investigator, thermal performance was predicted at two experiment locations for the Mode 2 experiment - locations 2 and 4 - and at location 3 for the Mode 3 experiment. Gradient sensor temperature rise was computed as a function of time, thermal conductivity, and absolute temperature level for Mode 2 operation. In Mode 3 studies, both the temperature rise and rate of temperature rise (slope) of the ring sensor were computed as a function of time and thermal conductivity. The effect of temperature level and variations in several other parameters were investigated with the aid of the computer models. Runs were also made to investigate the decay behavior of the ring sensor and gradient sensor at location 2 after heater turn-off in a Mode 3 experiment.

All predicted data is presented in tabular form in Appendix IV to facilitate subsequent data processing by Lamont-Doherty Geological Observatory.

B. Mode 2 Experiment

Predicted data for gradient sensor temperature rise versus time is plotted in Figures 23 through 25 for experiment location 2. The predicted performance data for the gradient sensor at experiment location 4 (tabulated in Appendix IV) is similar, except that the temperature rises are approximately 10 to 20% higher at long times. As described earlier, the temperature rises of the gradient sensor at location 4 are higher than those at location 2 because of locational variations in the number of lead wires and their associated conductances.

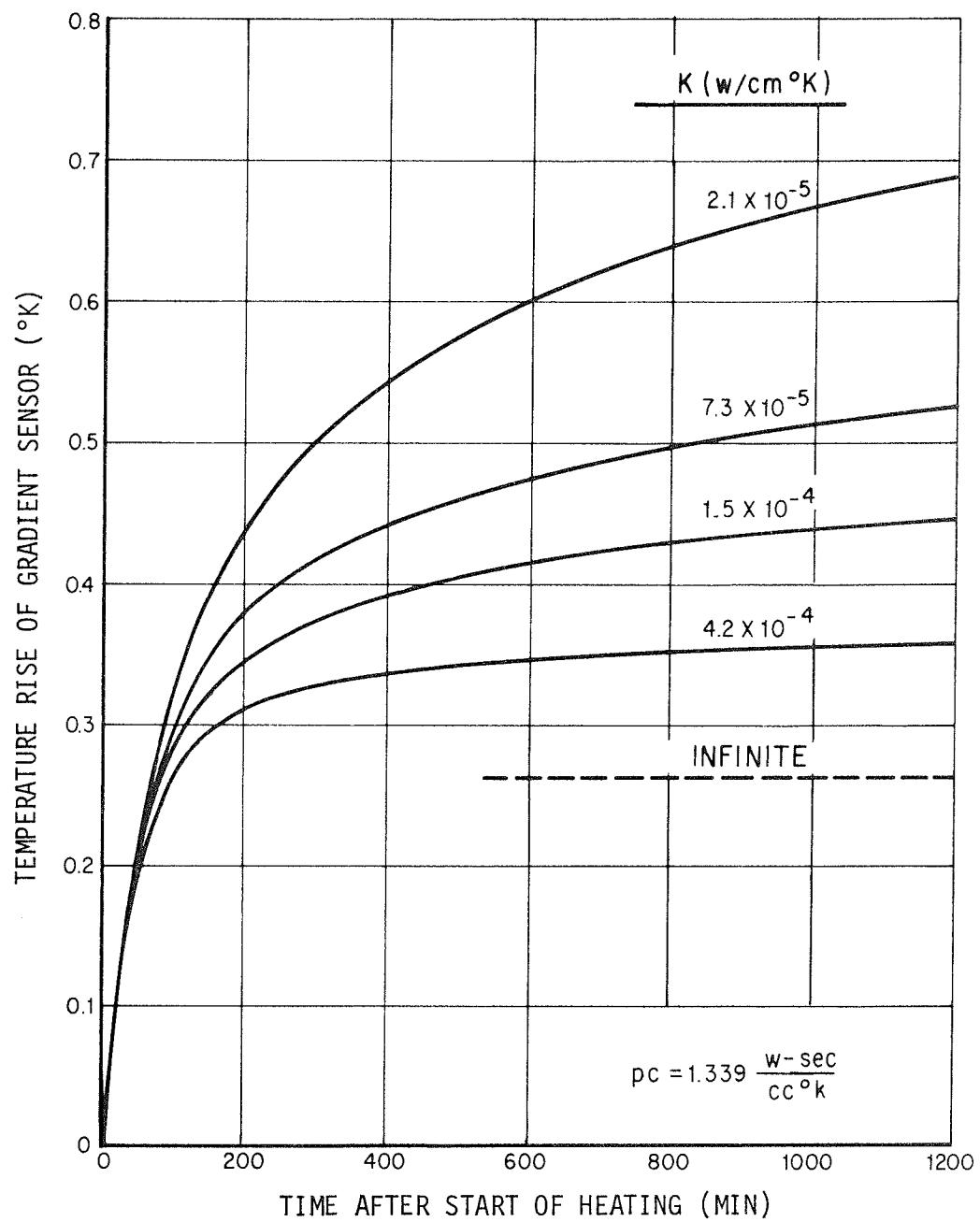


FIGURE 23 PREDICTED PERFORMANCE OF MODE 2 EXPERIMENT - LOCATION 2, $T = 205^{\circ}\text{K}$

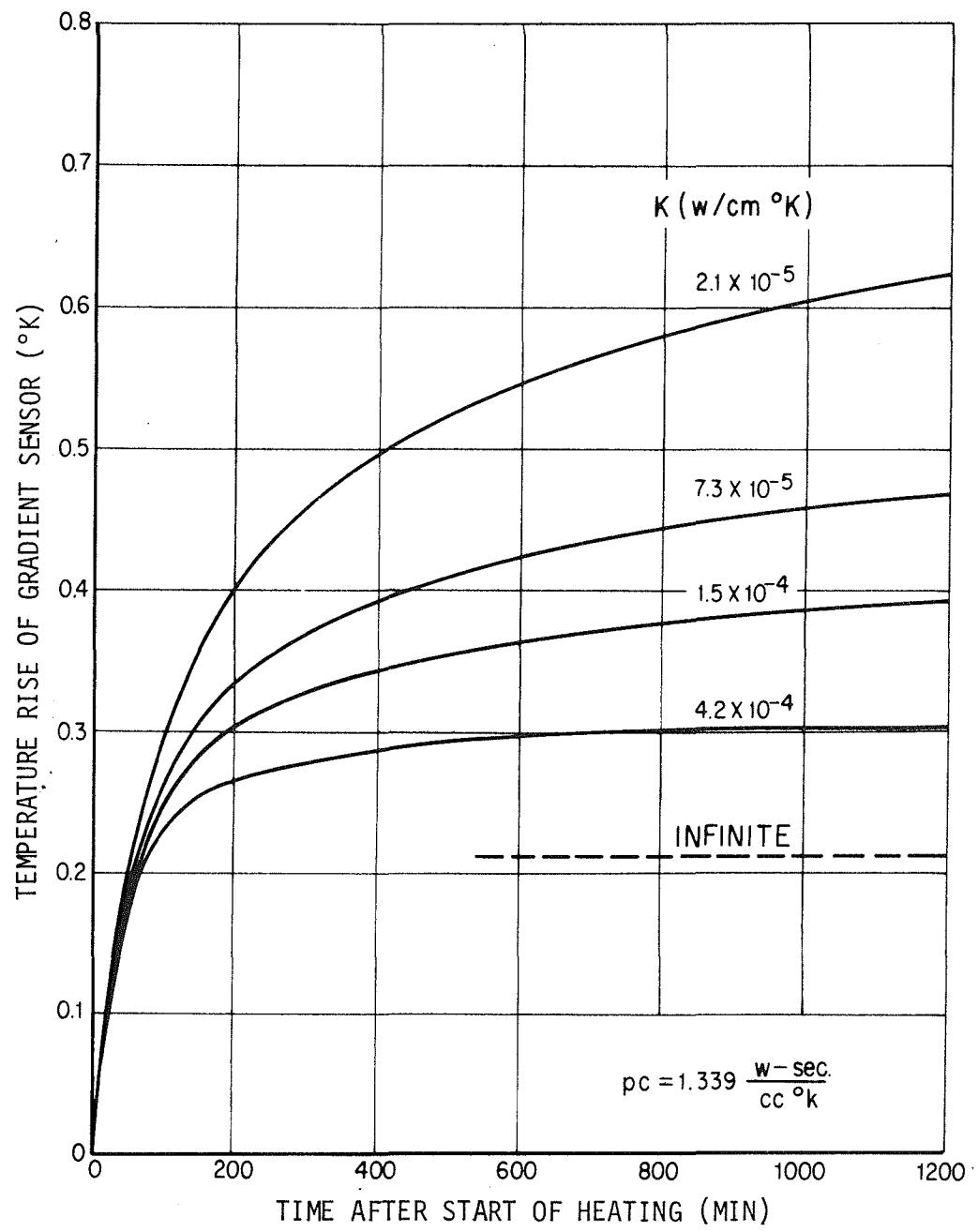


FIGURE 24 PREDICTED PERFORMANCE OF MODE 2 EXPERIMENT -
LOCATION 2, $T = 225^\circ K$

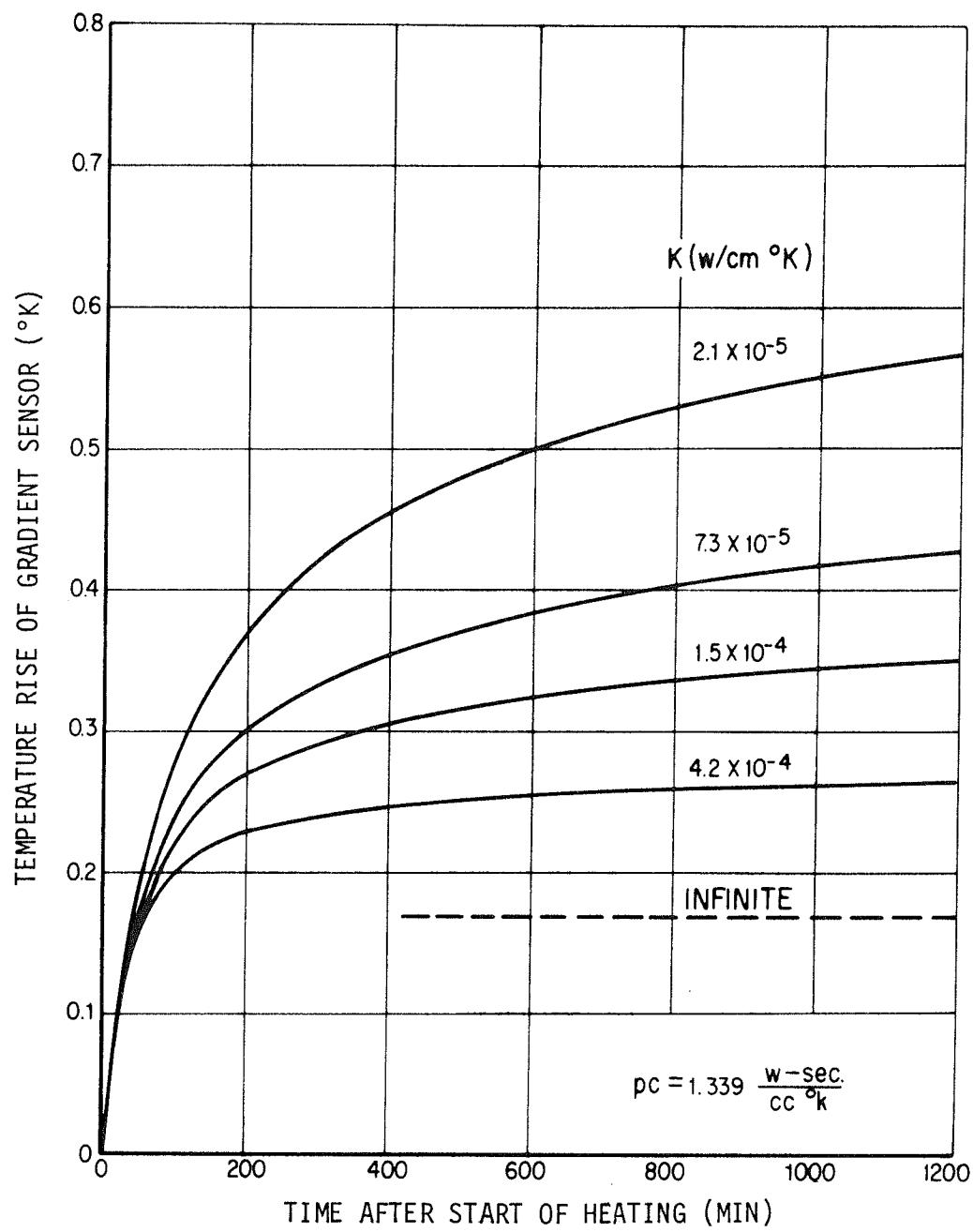


FIGURE 25 PREDICTED PERFORMANCE OF MODE 2 EXPERIMENT -
LOCATION 2, $T = 245^{\circ}\text{K}$

Several trends are obvious from an examination of the plots.

- 1) The temperature rise of the gradient is inversely proportional to both thermal conductivity and absolute temperature level;
- 2) The sensitivity of the Mode 2 experiment to changes in thermal conductivity decreases as thermal conductivity increases.

When the probe is surrounded by a medium having a near-infinite conductivity, the temperature rise is primarily governed by the inherent thermal resistance provided by the radiation gap between the probe and the drill casing. As the thermal conductivity of the medium decreases, the temperature rise of the gradient sensor increases. At low values of lunar conductivity the resistance provided by the medium becomes a major contributor to the temperature rise.

1. The Use of Slope Data to Supplement Evaluation of Mode 2 Data

Although not originally intended as a method of data interpretation, the use of the rate of change of gradient sensor temperature with time ("slope data") to determine the conductivity of the lunar medium surrounding the probe was investigated. This brief look was motivated by the successful use of slope data for interpreting Mode 3 data. In addition, a simple point-heat-source model⁶ suggests that the slope may be a more sensitive indication of the thermal conductivity than is the value of the temperature rise. For a point source, the steady-state temperature rise varies inversely with the thermal conductivity; whereas, the time rate of change (slope) varies inversely with the conductivity raised to the three-halves' power.

Table V provides a comparison between the two methods of interpreting Mode 2 data over a wide range of thermal conductivities. The calculations were made for experiment location 2 assuming an initial temperature of 225°K. Shown in the table are predicted values of

TABLE V

COMPARISON OF SENSITIVITIES OF TEMPERATURE RISE
AND SLOPE OF GRADIENT SENSOR, MODE 2 EXPERIMENT

	Thermal Conductivity of Medium w/cm °K	<u>Gradient Sensor</u> [*]		<u>Percentage Change in</u>			% Change in Slope % Change in ΔT
		Temperature Rise (°K)	Slope °K/min	Conductivity (%)	Temperature Rise (%)	Slope (%)	
55	2.1×10^{-5}	0.547	0.000203	+248	-23	-40	1.7
	7.3×10^{-5}	0.423	0.000121	+105	-14	-32	2.3
	1.5×10^{-4}	0.364	0.000082	+180	-19	-61	3.2
	4.2×10^{-4}	0.295	0.000032				

* Experiment Location 2
 T = 225
 $\rho c = 1.339$ w-sec/cc °K
 Time = 10 hours after start of heating

temperature rise and rate of temperature rise after 10 hours from start of experiment. From these values, the percent changes in temperature rise and in slope were determined as a function of the percent change in thermal conductivity. The results confirm that the slope data is two to three times more sensitive to the lunar thermal conductivity than is the temperature rise.

Figure 26 shows a plot of slope data versus time on log-log paper. For the case considered, the data very nearly fits a straight line after a heating time of only 50 minutes. The slope of the plot reveals a power law dependence on time of -1.35. Corresponding values for the point-source and line-source models are -1.5 and -1, respectively.

The behavior illustrated may be used to estimate the steady-state temperature rise and the time required to reach a given percentage of this value--on the basis of the temperature-time history at early times. The results may be fitted to the following simple model for the rate of change of temperature, T, with time, t:

$$\frac{\partial T}{\partial t} = \alpha t^{-\beta}$$

Once the parameters α and β are found from the data, the steady-state temperature rise can be estimated from:

$$T_{ss} = T_\tau + \int_{\tau}^{\infty} \frac{\partial T}{\partial t} dt$$
$$= T_\tau + \frac{\alpha \tau (1 - \beta)}{\beta - 1}$$

where

$$T_\tau = \text{temperature rise after some time } \tau.$$

Using the data shown in Figure 26, a steady-state temperature rise of 0.507 is estimated compared to a computed value of 0.481.

The model may also be used to predict the time required to reach X% of steady-state temperature rise:

$$t_{X\%} = \frac{T_{ss} (1-0.01X) (\beta - 1)}{\alpha}^{\frac{1}{1-\beta}}$$

For the results illustrated, the times to reach 80% and 90% of the final value of temperature rise are estimated to be 61.6 hours and 459.5 hours, respectively.

The simple extrapolation model presented here is speculative since it has not been thoroughly investigated in the present work. It is offered here as a potential means of supplementing the interpretation of Mode 2 data, and as an aid in planning the experiments to be performed.

C. Mode 3 Experiment

For the Mode 3 experiment, computations of ring sensor temperature rise and slope were performed during a six-hour heating period for the following thermal conductivities: 1.5×10^{-4} , 6×10^{-4} , 1×10^{-3} , 1.7×10^{-3} and 5.4×10^{-3} w/cm °K. As directed by the Principal Investigator, the absolute temperature level was 225°K and the density, ρ , and specific heat, c , were specified at 1.6 gm/cm^3 and $0.2 \text{ cal/gm } ^\circ\text{C}$, respectively ($\rho c = 1.339 \text{ w-sec/cc } ^\circ\text{K}$). At the end of the six-hour heating period, the heater was turned off and the temperatures of the ring sensor and the gradient sensor at location 2 were computed as a function of time during a decay period of approximately 18 hours.

The computer-predicted results for the temperature rise and slope of the ring sensor during the six-hour heating period and the temperature decay of the ring sensor and gradient sensor during the decay period are tabulated in Appendix IV.

Before discussing the Mode 3 results, it is appropriate to state the measurement ranges of the gradient and ring bridges. The gradient bridges are designed to operate over the range of 200 to 250°K and measure differential temperature within two distinct ranges:

1) $\pm 2^{\circ}\text{K}$, and 2) $\pm 20^{\circ}\text{K}$. The ring bridges are designed to operate over the same temperature range but measure differential temperature within one range: $\pm 2^{\circ}\text{K}$. This means that the slope of the ring sensor during a Mode 3 experiment cannot be used to measure a thermal conductivity which is sufficiently low to cause the ring-sensor temperature to rise more than 2°K . Similarly, the decay data of the gradient sensor can only be obtained when the temperature rise of the ring sensor is less than 20°K .

The predicted temperature rise of the ring sensor is shown in Figure 27 for a heating period of 6 hours and a decay period of 18 hours. The performance data for a conductivity of 1.5×10^{-4} is not plotted since the predicted temperature rise of the ring sensor exceeded the measurable maximum of 2°K during the early transient.

The relationship between ring sensor slope and time is presented in Figure 28 for all five values of thermal conductivity. The predicted slope for a conductivity of 1.5×10^{-4} is described by a dotted line for times greater than 120 minutes where the temperature rise lies outside of the measuring range of the ring bridge.

Referring to Figure 29, it is evident that the cooling behavior of the gradient sensor at location 2 is also related to the thermal conductivity of the surrounding lunar material. This behavior can serve several purposes. It can be used to provide an experimental check on the conductivity measurement indicated by the ring sensor response. The decay behavior can also be used to measure conductivities lying in the transition between the Mode 2 and Mode 3 ranges, where conductivities may be too low to be measured by a Mode 3 experiment, and where a Mode 2 experiment may be resolution-limited. For example, in the range of 6.0×10^{-4} to 1.5×10^{-4} w/cm $^{\circ}\text{K}$, the cooling behavior of the gradient sensor is quite sensitive to the thermal conductivity of the lunar medium.

The range limitations of the Mode 3 conductivity experiments are dependent upon the absolute temperature level of the moon, and the

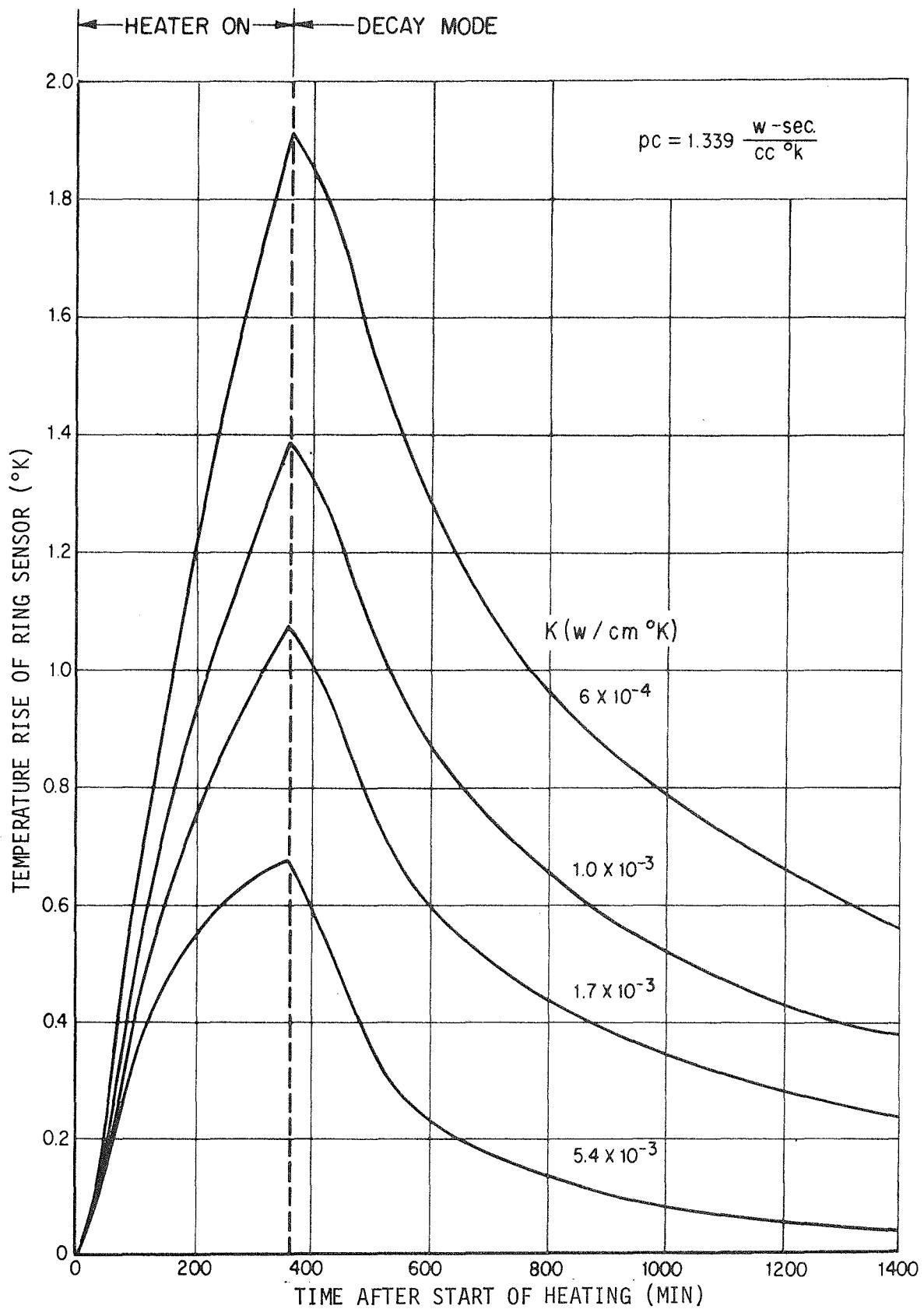


FIGURE 27 TEMPERATURE RISE OF RING SENSOR DURING HEATING AND DECAY PERIODS OF MODE 3 EXPERIMENT, LOCATION 2, $T = 225^\circ K$

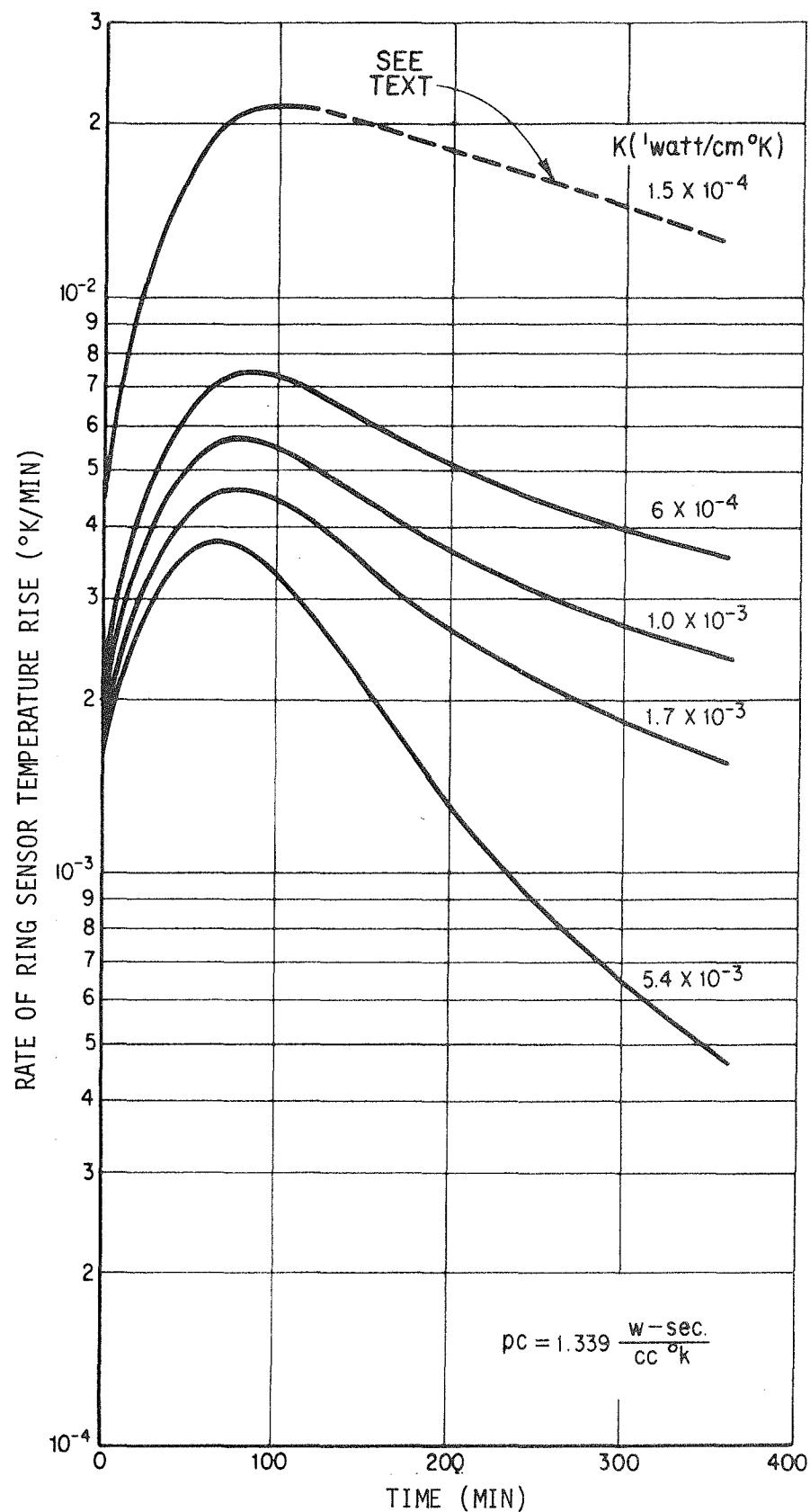


FIGURE 28 SLOPE OF RING-SENSOR TEMPERATURE DURING MODE 3 EXPERIMENT - LOCATION 2,
 $T = 225^{\circ}\text{K}$

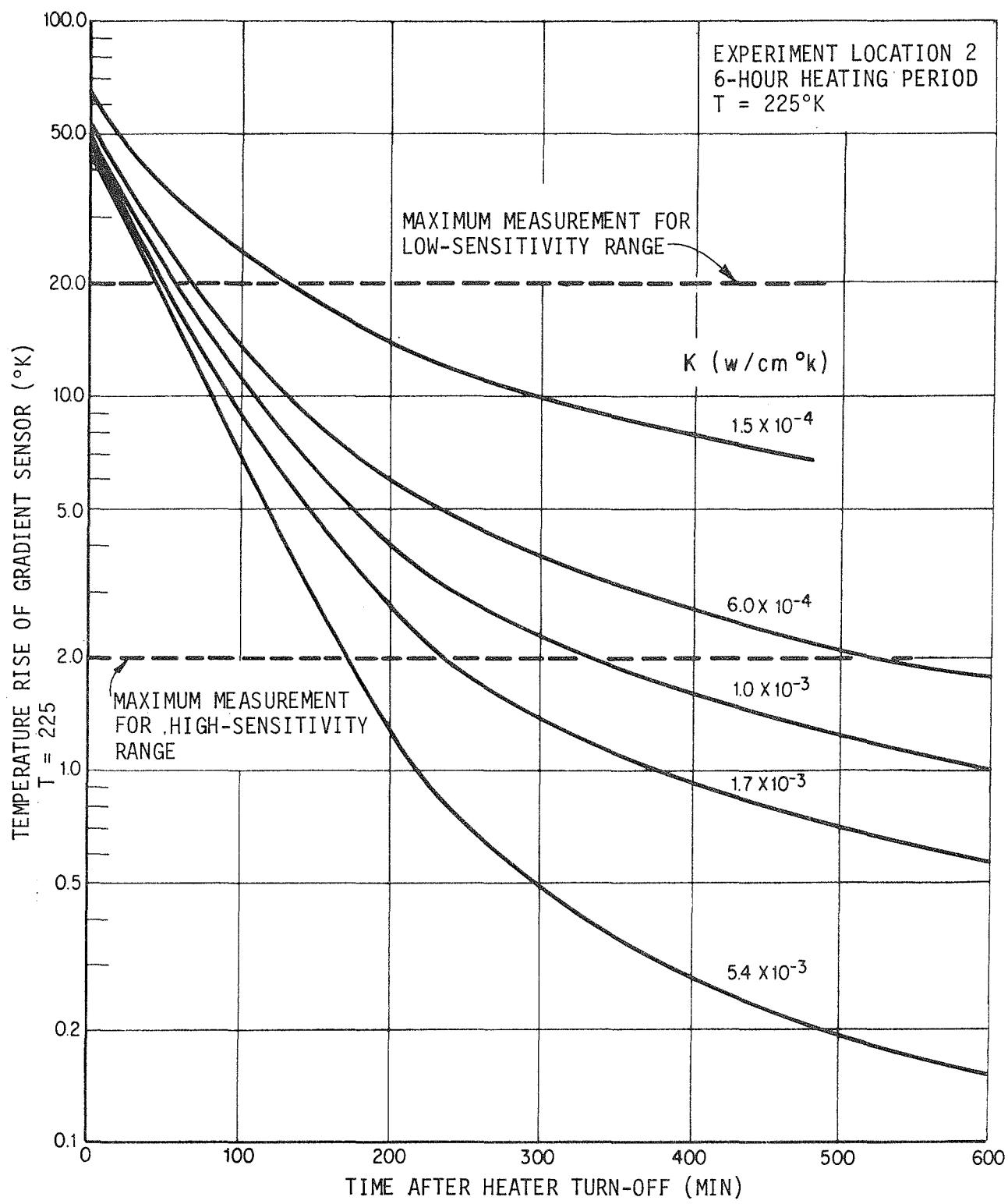


FIGURE 29 TEMPERATURE DECAY OF GRADIENT SENSOR
AFTER MODE 3 EXPERIMENT

duration of the heating period necessary to minimize the effect of probe-related transients. It is presently planned to operate the Mode 3 experiments for a minimum of five or six hours. Parametric computer predictions could be used to evaluate and define experimental limitations. An example is presented below.

D. Typical Performance of Conductivity Experiments in the Lunar Environment

Figure 30 summarizes the predicted performance of the heat flow probes for lunar conductivities ranging from 2×10^{-5} to 5.4×10^{-3} w/cm °K. The performance capabilities shown are for several specified conditions:

- Experiment location 2
- An absolute temperature of 225°K
- A Mode 2 heating period of at least 16 hours
- A Mode 3 heating period of at least 6 hours

For the Mode 2 performance, both the temperature rise and the slope of the gradient sensor are shown at a time of 16 hours. It is interesting to note that the slope of the gradient sensor is significantly more sensitive to thermal conductivity than is the temperature rise. Over the range of 2.1×10^{-5} to 4.2×10^{-4} w/cm °K, the slope changes by almost an order of magnitude. In contrast, the temperature rise varies between 0.6 at $K = 2.1 \times 10^{-5}$ and 0.3°K at $K = 4.2 \times 10^{-4}$. The limited resolution of the temperature rise at $K = 4.2 \times 10^{-4}$ is apparent, since 90 millidegrees, a 30% change in signal, separates a low and near-infinite prediction of thermal conductivity.

The data show that the Mode 3 experiment is limited to measuring a thermal conductivity of approximately 5.5×10^{-4} , which is sufficiently low to cause the ring sensor to rise 2°K. The decay behavior of the gradient and ring sensors can be used in the range of 1.5×10^{-4} to 5.5×10^{-3} w/cm °K to supplement the Mode 2 and Mode 3 experiments.

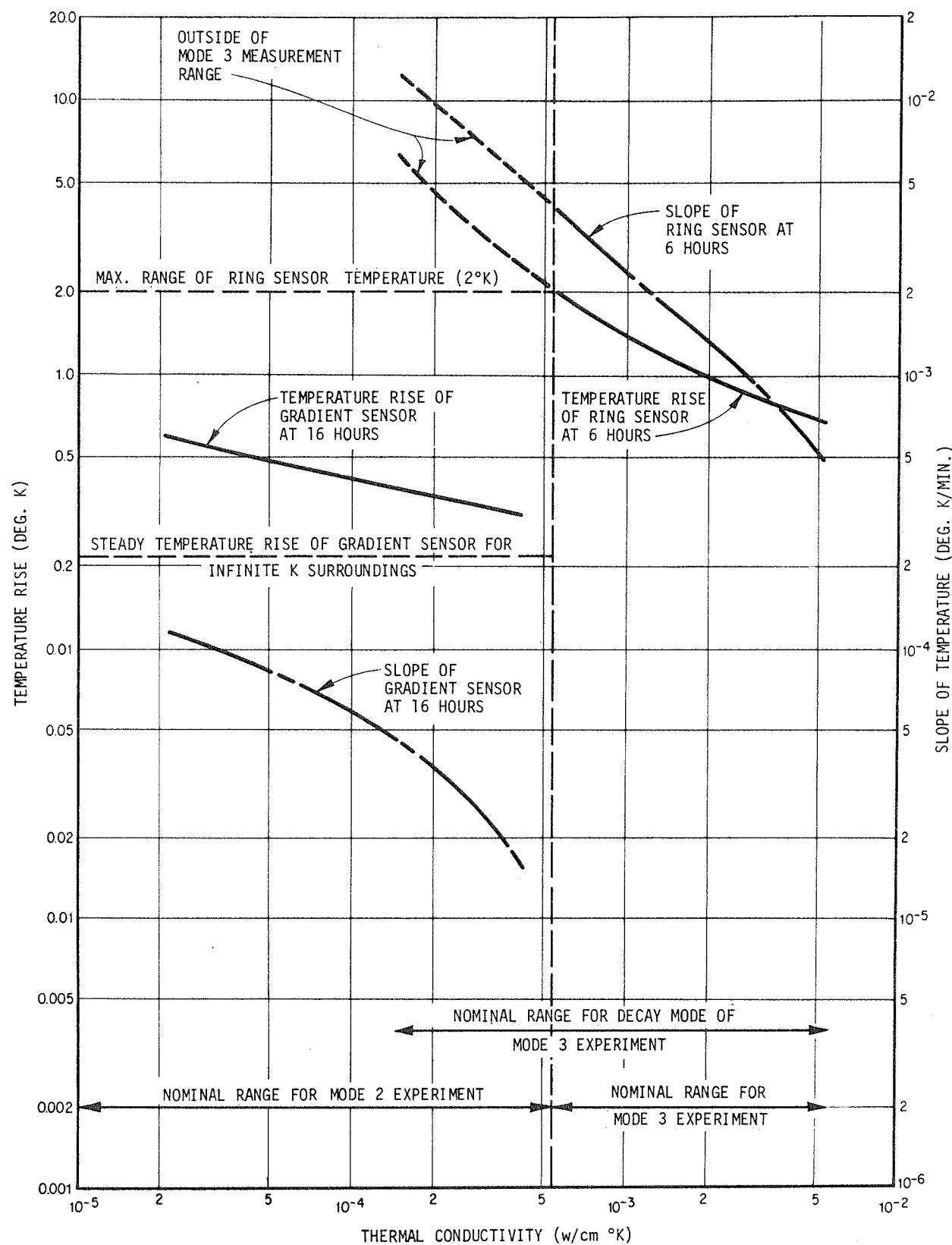


FIGURE 30 PREDICTED THERMAL PERFORMANCE OF EXPERIMENT LOCATION 2 AT A TEMPERATURE OF 225°K

It is important to note that these data are quite specific and apply to the conditions previously stated. Performance ranges will be different at other experiment locations and for other values of absolute temperature level. For example, calculations indicate that experiment location 4 will experience a smaller temperature rise at its ring sensor at given value of conductivity, although the slope behavior will be consistent with that of location 2. Therefore, the Mode 3 experiment at location 4 should be capable of measuring conductivities less than 5.5×10^{-4} w/cm °K. When the absolute temperature of the medium is less than 225°K (resulting in an increased temperature rise for the ring sensor), the Mode 3 limitation for location 2 will apply to thermal conductivities slightly higher than 5.5×10^{-4} .

E. Comparison of Experiment Performance in the K Apparatus and Lunar Environment

The physical differences between the bore tube in the K Apparatus and the lunar drill casing were discussed in Section III-D. The drill casing is approximately four times as conductive as the bore tube. Consequently, as shown in Table VI, probe performance in the K Apparatus and in the lunar environment differs for the same environmental conductivity.

For the Mode 2 experiments performed in the K Apparatus, the low-conductance bore tube permits less longitudinal heat transfer than the drill casing, resulting in a higher gradient sensor temperature rise. Therefore, the probe performs as if it were in a lunar environment having a conductivity 27 to 37% lower. The bore tube has the opposite effect on the response of the Mode 3 experiment. The low-conductance bore tube provides less longitudinal heat flow to the region of the bore tube near the ring sensor. In the Mode 3 test, the probe performed as if it were in a lunar medium having a conductivity 9% higher than the conductivity of the medium in the K Apparatus.

TABLE VI

COMPARISON OF EXPERIMENT PERFORMANCE IN THE
K APPARATUS AND LUNAR MEDIUM^{*}

	Lunar Environment (with boron-reinforced, epoxy fiber-glass, drill casing)	K Apparatus (with epoxy-fiber-glass bore tube)	% Deviation	Approximate Error in Conductivity Simulated by test (%)
Mode 2 experiment at 1200 minutes				
Temperature rise of ring sensor ($^{\circ}$ K)				
@ $K = 1.5 \times 10^{-4}$ w/cm $^{\circ}$ K	0.393	0.427	+ 8.6	-27
@ $K = 7.3 \times 10^{-5}$ w/cm $^{\circ}$ K	0.470	0.531	+13.0	-37
Mode 3 experiment at 301 minutes				
$K = 1.7 \times 10^{-3}$ w/cm $^{\circ}$ K				
Temperature rise of ring sensor ($^{\circ}$ K)	0.969	0.877	- 9.5	
Slope of ring sensor ($^{\circ}$ K/min)	0.00185	0.00175	- 5.4	+ 9

* Experiment location 2; absolute temperature = 225 $^{\circ}$ K

F. Parametric Studies of Experiment Performance

1. Parametric Studies for Mode 3 Experiment

The Mode 3 performance predictions already described are based upon nominal values of parameters which were included in the computer model description of experiment location 2. The computer model description was specifically related to the following operational conditions:

Experiment location:	2
Absolute temperature:	225°K
Density of lunar material:	1.6 gm/cm ³
Specific heat of lunar material:	0.2 cal/gm °K (i.e., $\rho c = 1.339 \text{ w-sec/cc } ^\circ\text{K}$)

Suppose the density or specific heat of the lunar material were not previously known at the time of the measurements, or that the data correlations were made on performance data at 225°K while the measured environmental temperature was 205°K: What uncertainty would be involved if predicted data for experiment location 2 were used to evaluate the performance at experiment location 4?

It is first of interest to examine the relationship between changes in thermal conductivity and changes in slope of the ring sensor. This relationship is indicated in the following tabulation considering the slope at a time of five hours after the start of heating. Changes in conductivity were made from a base value of 1.7×10^{-3} w/cm °K.

<u>Percent Change in Lunar Conductivity</u>	<u>Percent Change in Slope of Ring Sensor</u>
-41	45
+20	-13
+218	-65

The results of examining the influence of various uncertainties on the Mode 3 experiment are presented in Table VII. Also shown is a column for the estimated error in a conductivity prediction, since this is a more meaningful quantity than the percentage change in slope. It is assumed that: 1) the thermal conductivity in the surrounding lunar material, which is to be evaluated by the measurement, is 1.7×10^{-3} w/cm °K, and 2) an estimate of the lunar conductivity is made by correlating the slopes of the ring sensor with the data for experiment location 2 and the conditions already described.

The estimates for errors in conductivity predictions are approximate, and the relationships described in Table VII specifically relate to a lunar conductivity value of 1.7×10^{-3} w/cm °K. A comprehensive uncertainty analysis would involve computations at other values of conductivity and consideration of other potential uncertainties not described here.

Computer models of the lunar probe were developed describing the Mode 2 and Mode 3 performance at all four experiment locations. Therefore, uncertainties associated with the effect of absolute temperature level and experiment location can be minimized in a refined data analysis.

Detailed listings of ring sensor response versus time for the parametric studies described above are presented in Appendix IV.

2. Possible Uncertainties Associated with the Experiment Configuration

Two other conditions which relate to uncertainties in the experiment configuration were examined with the aid of the computer models. The purpose of these calculations was to estimate the maximum possible influence of these uncertainties on experiment performance. While it is not suggested that the uncertainty intervals examined actually exist, it is believed that an examination of their possible influence is appropriate.

TABLE VII

INFLUENCE OF UNCERTAINTIES ON MODE 3 PERFORMANCE
AT A THERMAL CONDUCTIVITY OF 1.7×10^{-3} w/cm °K

Time = 5 hours after start of heating

Parameter	Uncertainty Interval on Change	Influence on Response of Ring Sensor		Approximate * Error in Conductivity Prediction (%)
		% Change in Temperature Rise	% Change in Slope	
Thermal Mass of Lunar Material (ρc)	+ 20%	- 7.6	- 7.6	+ 8
Absolute Temperature	- 20°K (T = 205°K)	+ 27.0	+ 4.9	- 6
	+ 20°K (T = 245°K)	- 14.6	- 2.7	+ 3
Thermal Conductance of Drill Casing	+ 20%	+ 2.8	+ 1.7	- 2
Experiment Location	Location 1	- 1.5	- 2.2	+ 3
	Location 3	- 10.6	- 1.6	+ 2
	Location 4	- 10.7	- 0.5	less than 1

* Based on estimating conductivity by correlating the predicted slopes with the performance of experiment location 2 listed in Table VIII.

a. Interface between Probe Alignment Springs and Drill Casing

As previously mentioned in Section III.D, the fact that the 7/8-inch inside diameter of the drill casing lining the lunar bore hole is smaller than the corresponding 1-inch dimension for the bore tube in the K Apparatus could introduce some uncertainty in predicting experiment performance. Heat flow to the casing via the alignment springs at the heater locations, apparently insignificant in a 1" ID surrounding, could become important in a 7/8" ID surrounding environment because of contacting between the alignment springs and the drill casing.

The magnitude of the thermal coupling or contact conductance is not known at this time. The approach used here was to select a condition which would surely bound the effect of heat flow between the alignment springs and the drill casing. The interfacial surfaces of the three equally spaced alignment springs and the drill casing were assumed to be in good thermal contact, i.e., negligible contact resistance. A well-coupled condition was also assumed at the ends of the springs which are positioned between the heater guard and the probe sheath. Conductance couplings between the probe and the drill casing were then evaluated on the basis of the thermal conductivity and cross-sectional area of the beryllium-copper springs and the effective thermal path between the probe and the drill casing.

The results of the study for the Mode 2 experiment are tabulated below.

Mode 2 Experiment

(Location 4)

($T = 225^{\circ}\text{K}$, time = 20 hrs. after start of heating)

<u>Interface Condition</u>	K (w/cm $^{\circ}\text{K}$)	Temperature Rise of Gradient Sensor ($^{\circ}\text{K}$)
Thermally isolated	4.2×10^{-4}	0.333
Well-coupled	4.2×10^{-4}	0.193
Thermally isolated	Infinite	0.223

The results show that the interfacial thermal coupling between the alignment springs and the drill casing is important and could significantly influence the performance of the Mode 2 experiment. Understandably, there is a non-zero contact resistance between the alignment springs and the drill casing, and between the springs and the probe, which would tend to diminish the trend noted here. Further investigations would be required to evaluate the effect on performance of other assumptions for the contacting interface, and the potential of alternate modes of interpreting experiment performance.

A similar calculation for the Mode 3 experiment indicated that even the worst-case assumption for the spring coupling could be tolerated and would not seriously influence experiment performance. This calculation was performed at experiment location 2 at a conductivity of 1.7×10^{-3} w/cm °K. The results are summarized below:

Mode 3 Experiment

($K = 1.7 \times 10^{-3}$ w/cm °K, $T = 225$, Location 2,

Time = 6 hrs. after the start of heating)

<u>Interface Condition</u>	<u>Temperature Rise of Ring Sensor (°C)</u>	<u>Slope of Ring Sensor Temperature (°K/MIN)</u>
Thermally isolated	1.071	0.00157
Well-coupled	0.760	0.00149

The estimated error in the conductivity prediction, if it were based on predicted slope data for thermally isolated interfaces, is only +6%. However, further studies at other values of thermal conductivity would be appropriate before concern for the Mode 3 experiment could be dismissed entirely.

b. Radiation Coupling between the Drill Casing and the Moon

For performance predictions in the lunar environment, the drill casing was modeled according to the same guidelines developed

for the bore tube in the K Apparatus. That is, the external surface of the drill casing was treated to be in intimate thermal contact with the lunar medium. A computation was also made under the assumption of a pure radiative coupling between the drill casing and the surrounding lunar material. A Mode 3 experiment was chosen for study since this assumption is more reasonable in a high-conductivity or rock moon than in a low-conductivity, powder-type material. Computations were made for experiment location 2 considering a conductivity of 5.4×10^{-3} w/cm °K; results are summarized below at a time of 6 hours after the start of heating.

INFLUENCE OF DRILL CASING - MOON

INTERFACE ON MODE 3 PERFORMANCE

$$(K = 5.4 \times 10^{-3} \text{ w/cm } ^\circ\text{K})$$

<u>Interface between Drill Casing and Lunar Material</u>	<u>Temperature Rise of Ring Sensor (°K)</u>	<u>Slope of Ring Sensor °K/MIN</u>
1) Well-coupled	0.676	0.00047
2) Radiatively coupled	3.368	0.00066

For the radiatively coupled interface the predicted temperature rise of the ring sensor exceeds the maximum measurement range of the Mode 3 experiment. Consequently, the slope at six hours could not be obtained experimentally. Since the temperature rise of the ring sensor is inversely proportional to thermal conductivity of the moon, the limitation on temperature measurement would be more prevalent at lower values of conductivity.

For a conductivity of 5.4×10^{-3} , the temperature rise reaches 2°K approximately two hours after the start of heating, a time not favorable to the evaluation of the Mode 3 experiment. At this time, the transient response of the ring sensor is strongly influenced by transient responses in the probe. However, the decay

behavior of the ring and gradient sensors after heater turn-off could possibly be used in conjunction with the computer models to determine the lunar conductivity.

VI. CONCLUSIONS AND RECOMMENDATIONS

The results of this work showed that the thermal behavior of the lunar medium could be accurately simulated by a detailed finite-difference model.

The detailed mathematical model of the thermal characteristics of the probe was extremely accurate. The accuracy was determined by comparing computer prediction to certain probe test results when the test boundary conditions were well defined.* The accuracy of the computer predictions demonstrated that the extension of the predictions to a probe in a lunar environment is appropriate.

A source of locational variations in sensor response, particularly significant to the interpretation of the Mode 2 experiment, was shown to be due to the conductive effects of lead wires passing through the entire probe. The total number of lead wires for instrumentation, resistance-bridge measurements and heaters vary along the length of the probe and thereby induce a spatial variation of thermal conductance in the probe.

The bore tube which contains the glass-beaded medium in the Thermal Conductivity Apparatus has dimensions and thermal characteristics different from the boron-reinforced, epoxy-fiber-glass drill casing which will line the bore hole in the lunar environment. Computer predictions were made to compare the Mode 2 and Mode 3 performance in the moon and in the Thermal Conductivity Apparatus for the same specified values of thermal conductivity. The comparisons indicated that precise calibration of the experiment performance in the laboratory (relating temperature responses and thermal conductivity) and performance check-out could best be accomplished if the emplaced experiment configuration and the test simulation had the same tubular liners (or liners with the same thermal conductance and internal dimensions).

* All experimental data used in the evaluation of the computer models were obtained from test programs sponsored under other subcontracts.

The analytical results showed that the interfacial thermal coupling between the probe alignment springs (at the heater locations) and the internal surface of the drill casing is important and could influence the accuracy of the Mode 2 experiment. The magnitude of this thermal coupling is unknown at this time since no flight-configuration casings, or tubular liners with the same internal dimensions were used in performance tests. Further study is recommended to investigate the nature of the thermal coupling at the spring-casing interface. Additionally, in the lunar environment, there are uncertainties in the thermal coupling at the interface between the external surface of the drill casing and the surrounding lunar material. Additional computer studies are recommended to assure that Mode 3 conductivity data can be interpreted with existing data reduction procedures if this interfacial coupling is radiation dominated.

Other parametric studies indicated that the computer models developed in this work could be used to establish potential ranges of limitations of certain conductivity-experiment modes and the suitability of others. Interpretation of the conductivity data in the range of transition between the Mode 2 and Mode 3 experiments can be enhanced by the use of a decay mode. Computer studies and previous test work demonstrated that additional information about the thermal conductivity of the surroundings can be obtained after a Mode 3 experiment by turning off the heater and monitoring the temperatures of gradient and ring sensors. The computation of slopes from temperature data for the gradient sensor during a Mode 2 experiment also shows promise of aiding in the interpretation of data.

The computer modeling and related studies provided information leading to a better understanding of instrument performance and limitations. Consequently, it is recommended that investigative work with computer models be incorporated into the early phases of a program involving similar experiments (design definition, instrument design, design of test equipment, etc.).

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APPENDIX I

COMPUTER SOLUTION OF HEAT FLOW MODELS

I. FINITE-DIFFERENCE EQUATIONS

Within this section we will discuss the form in which the finite-difference equations--governing the system thermal behavior--must appear in order to be solved using the Generalized Thermal Analysis Program (ADLGTA). The purpose is twofold: to present the format of the difference equations written to describe the probe and surrounding lunar medium; and to describe a disk or tape-oriented procedure for modifying the original input data for a problem. Methods of modifying input data will be described in a later section of this appendix. It is useful to introduce here the concept of a system. Nodes (or zones and their boundaries in the Method of Zones technique) whose temperatures are unknown and are to be calculated are taken to comprise a thermal system. On the other hand, nodes where the temperature is known are considered outside the system. During solution, energy balances are performed on the system to allow checks on the accuracy of the solution.

The basic form of the heat-balance equations for the system nodes is:

$$\sum_j Q_{ij} + P_i(t) + M_i \frac{dT_i}{dt} = 0 \quad (I-1)$$

where

Q_{ij} = outward heat flow from node i in direction j (watts)

$P_i(t)$ = negative of power into node i (watts)

M_i = thermal mass of node i (Joule/°K)

The power term $P_i(t)$ may represent heat generated within the volume element represented by node i or may represent power into the volume element from some external source.

The outward heat flows Q_{ij} may be related to conductive and radiative interchange with other nodes in the system. In this case, the basic form of the energy equation becomes:

$$\sum_j C_{ij} T_j + \sum_j A_{ij} \sigma T_j^4 + P_i(t) + M_i \frac{dT_i}{dt} = 0 \quad (I-2)$$

where

C_{ij} = thermal conductance between nodes i and j (watts/ $^{\circ}$ K)

A_{ij} = radiative view area between nodes i and j (cm^2)

The energy Equation (I-2) relates the time rate of change in temperature at node i to the net energy transfer with surrounding nodal elements. An equation of the same form is written for each node within the system. The thermal mass M_i may be zero for any or all of the nodes in the system.

Similar equations can be written for the constant temperature nodes outside the system boundaries:

$$\frac{dT_i}{dt} = 0 \quad (I-3)$$

By convention, the thermal mass of such a node is taken to be unity, although any non-zero value will suffice. The solution to Equation (I-3) is that the temperature T_i is a constant.

To obtain a heat balance on the entire system, an equation can be written for the total heat flow across the system boundaries:

$$Q_{out} = \sum_i C_i T_i + \sum_i A_i \sigma T_i^4 \quad (I-4)$$

where

C_i = thermal conductance from node i to elements outside system boundary (watts/ $^{\circ}$ K)

A_i = radiative view area from node i to elements outside system boundary (cm^2)

and where the summation over index i includes the nodes outside the system boundary. The appropriate energy balance on the system may then be written:

$$\sum_i M_i \frac{dT_i}{dt} + \sum_i P_i(t) + Q_{out} = 0 \quad (I-5)$$

or, from Equation (I-4),

$$\begin{aligned} \sum_i M_i \frac{dT_i}{dt} + \sum_i C_i T_i + \sum_i A_i \sigma T_i^4 \\ + \sum_i P_i(t) = 0 . \end{aligned} \quad (I-6)$$

A sample problem illustrating the formulation of heat flow equations according to the format described above is given in Section VI of the Appendix.

II. INPUT DATA

A. Original Data

The input data consist mainly of a sequence of card images on magnetic tape. The data for several problems may be placed in succession on a single tape and followed by an end-of-file record. For the purpose of this description, we shall assume all data to be on cards as they might be before card-to-tape conversion.

A single problem consists of the following:

A. A heading card. This is an alphanumeric title to be printed on each sheet of output for identification and description.

B. A series of cards containing numerical information describing the differential equations to be solved. This series of cards is divided into sets, each of which describes a single equation. The format for all of these cards is the same, and in FORTRAN notation is I5, F20.9,

F20.9, I5, I5. A decimal point is customarily used in the two F-type fields so as to permit full flexibility. The first three fields contain the information needed to solve the problem, and the last two fields contain identification numbers. The identification in the fourth field is the equation number, and the identification in the fifth field is a serial number within the set of cards describing an equation. The information in the first three fields in a single set of cards is described below.

1. The first card contains the equation number i in the first field, the quantities A_{ij} and C_{ij} in the second and third fields, respectively, as required for use in Equation (I-4).

2. A series of cards comes next to give view areas, weighted conductances, and power inputs which determine A_{ij} , C_{ij} , and P_i for a single value of i in Equation (I-2). These cards are of two types:

a. The first type of card contains the quantities j , A_{ij} , and C_{ij} in the first three fields. The indices j may be in any order, and a single index may be repeated more than once if desired. If an index is repeated, the view areas and conductances given will be summed by the computer.

b. The second type of card is used when a power input is to be specified. A power input may be either constant or vary periodically. In the case of a constant power, a single card is needed: the first two fields are zero, and the third field contains the power. In all equations which contain input powers, it is required that the diagonal elements A_{ii} and C_{ii} be positive; otherwise, the conservation of energy check will fail. In case the power varies periodically, the power must be tabulated as a function of time over the period. The cards used for describing a periodic power are:

- A card which contains a zero in the first field, the period in suitable units of time in the second field, and the average power in the third field. The average power given will be used as a check when the data are read into the machine.

• A series of cards which tabulate the power as a function of time. The first field is zero, the second field contains the time, and the third field contains the power. The first time given must be zero, and the last time must be equal to the specified period. In case a discontinuity in power occurs, the time at which it occurs must be repeated, and the two values of power given.

3. The last card of each equation contains the negative of the equation number in the first field, the thermal mass M_i in the next field, and the starting temperature in the last field. The starting temperature may also be supplied in another way, and may be omitted in this card. This will be fully discussed later.

C. A blank card to terminate the data on the zones.

D. One or more control cards. The control cards contain ten fields whose format is, in FORTRAN notation, F5.2, E10.1, F10.3, I5, I5, F10.3, F10.3, I5, F5.2, I5. Decimal points are customarily used in all F-type and E-type fields.

The first field, F5.2, contains the acceleration factor used in solving the systems of simultaneous equations.

The second field, E10.1, contains a tolerance which determines when the iterations for solving the system of simultaneous equations are to be terminated.

The third field, F10.3, contains the time increment to be used in solving the differential equations.

The fourth field, I5, contains an integer which specifies the frequency of off-line print-out; the fifth field information is not used.

The sixth field, F10.3, contains the maximum value of time for which the problem is to be run before reading another control card.

The seventh field contains a starting temperature or zero. If a starting temperature is specified (and it must be on the first control card), this starting temperature will be used for all zones except for those which have already had a starting temperature specified under B-3

above. If the starting temperature punched in the second or later control card is zero, the computation will continue with the most recent temperatures as starting values but with any new parameters (e.g., time interval, acceleration factor, etc.) as specified by the new control card. If, on a second or later control card, the starting temperature is not zero, the computation will be restarted from time zero with the new parameters specified by the control card.

The eighth field, I5, specifies the largest value of the index i. Since some indices may be omitted, the number in the eighth field will be greater than or equal to the number of equations to be solved.

The ninth field, F5.2, contains the integration parameter α .

The tenth field, I5, contains a zero if the input data is expressed in watt, deg. K, cm., units, the integer 1 if the units are Btu, deg. R, ft., hr., or the integer 2 if the units are Btu, deg. R, ft., min.

E. The last card is a blank card which, when read in place of a normal control card, causes the computer to proceed to read in data for the next problem.

The data cards just described are read as card images from magnetic tape.

A sample problem with an illustration of the input data is presented in Section VI of this Appendix.

B. Data Modification Procedure

A problem description on magnetic tape can be used to generate a new tape which contains a modified version of the data on the original tape. This procedure could be used, for example, in a case where the geometrical subdivision and heat-balance equations for two problems are similar, but the boundary condition or surface properties are different. (A problem can be modified by changing the punched data cards which were described above. However, the tape modification procedure minimizes the chances of error inherent in manipulating large numbers of data cards.)

The input data for the modification procedure involves coded instructions for controlling logical units and instructions for storing the original data with modifications on another tape. The form of the data cards for these instructions are presented in Table I-1, and the general arrangement of the input data is described below.

The general arrangement of the input data to instruct the computer on generating a data tape from a problem using an original data tape is as follows:

- F. A card or series of cards commanding tape maneuvers required to start the data modification.
- G. A heading card. This is an alphanumeric title card to be printed on each sheet of output for identification and description.
- H. A series of cards containing numerical information describing the modifications to be made to the data on the original tape in generating the modified tape. The format for all these cards is the same; and in FORTRAN notation is I5, F20.9, F20.9, I5, I5, I5. A decimal point is customarily used in the two F-type fields to permit full flexibility. The first three fields contain information needed to solve the problem. The identification in the fourth field is the equation number, and the identification in the fifth field is a serial number within a set of cards describing an equation. The fifth field contains an integer which specifies the modification to be made.
- I. A card with the integer 9 in column 60 follows the last correction card and instructs the computer to copy the remainder of the reference tape without modification.
- J. A blank card.
- K. One or more control cards as described in II-D above.
- L. A card with instructions to rewind and end file on the generated tape.

TABLE I-1
CODED INSTRUCTIONS FOR DATA INSERTION AND MODIFICATION

Card Column							Operation Description	Instructions Referenced to Data Cards or Card Images on Tape
1	5	25	45	50	55	60		
				A	B	1	Copy through Equation A, Card B without correction.	
				A	B	2	Skip through Equation A, Card B.	
A	B	C	D	E		3	Insert this card which describes Equation D, Card E.	
A	B	C	D	E		4	Copy to Equation D, Card E and substitute this card for Equation D, Card E.	
-----							Multiply through Equation A, Card B by the terms on the following card.	
a	b		A	B	10		<u>a</u> multiplies radiation term, <u>b</u> multiplies conduction term (Note: If a radiation or conduction term is to remain unchanged, <u>a</u> or <u>b</u> , respectively, must be 1.0.)	
			A	B	0		Begin to copy problem to be modified from Tape A to Tape B.	
			A	B	5		Rewind Tape A and/or Tape B.	
			A	B	6		End of file on Tape A and/or B, then rewind same.	
			A	B	7		Copy problem from Tape A to Tape B without corrections. (If B = 0, skip problem on Tape A.)	
					8		End of copy program.	
								Instructions Referenced to Tape Drive Units

M. A card with the integer 8 in column 60 signifying that the copying procedure is completed.

III. DATA CHECK PROCEDURES

It is a laborious task to set up all of the numerical coefficients used in the equations describing the heat-balance conditions in a complicated problem, so that errors may frequently arise. Many of these errors can be detected by checks based on the principles of reciprocity and the conservation of energy. In general, the rows and columns of the matrices of conductances and view areas should add up to zero. This will be so if the equations are written in full exactly as prescribed by the method outlined in Section I with all diagonal elements positive. While it would make no difference to the final answer if various equations were multiplied by different constants, such manipulation would make it impossible to use the column sums to check the input data.

To test the consistency of the input data, row and column sum checks are made on the matrices $\{A_{ij}\}$ and $\{C_{ij}\}$. The row sums

$$S_R = \sum_j A_{ij} - A_i \quad (I-7)$$

$$S_C = \sum_j C_{ij} \quad (I-8)$$

are calculated for all values of i and tested to be small in magnitude. Any sums over tolerance (10^{-5}) are printed out. Also, the column sums

$$C_S R = \sum_i A_{ij} - A_j \quad (I-9)$$

$$C_S C = \sum_i C_{ij} - C_j \quad (I-10)$$

are calculated for each value of j and tested to be small in magnitude. Any column sums over tolerance are also printed. The signs in the

summations of Equations (I-9) and (I-10) are the same as the signs of the diagonal elements, A_{ii} or C_{ii} .

Certain complications may arise. When any part of the system (e.g., a boundary) has a fixed, preassigned temperature T , the equation for this temperature is simply

$$\frac{dT}{dt} = 0$$

The conductances and view areas of the rest of the system to this part are omitted, but not conversely, so that non-zero column sums will occur. As long as all the omitted conductances and areas are known, however, the non-zero sums can be checked.

It is to be noted that the method of solving the difference equations corresponding to the differential equation (I-2) requires that a diagonal element be in every row of the matrix $\{ |A_{ij}| + |C_{ij}| \}$, or if $\{ A_{ij} \}$ and $\{ C_{ij} \}$ have only zeros in a certain row, that the corresponding M_i be non-zero. The program checks to make sure that this requirement is satisfied and automatically omits the solution of the equations if the requirement is not satisfied.

The average power into each zone, \bar{P}_i , is also calculated and printed. In the case of periodically varying power inputs, the average power over a period is part of the input data, so that \bar{P}_i can be automatically checked. The total average power input is also calculated and printed.

IV. METHOD OF SOLUTION

A. Integration Scheme

The basic energy Equation (I-2) may be integrated with respect to time from t to $t + h$ where h is a small increment in time:

$$\sum_j C_{ij} \int_t^{t+h} T_j dt + \sum_j A_{ij} \sigma \int_t^{t+h} T_j^4 dt + \int_t^{t+h} P_i(t) dt$$

$$+ M_i T_i(t + h) - M_i T_i(t) = 0 \quad (I-11)$$

Where P_i is a constant, the integral term appearing in Equation (I-11) is simply $h P_i$. Where P_i is a function of time, $P_i = P_i(t)$, the integral is evaluated using the Trapezoidal rule:

$$\int_t^{t+h} P_i(t) dt \approx \frac{h}{2} [P_i(t+h) + P_i(t)] \quad (I-12)$$

where the values $P_i(t)$ are found from input data by linear interpolation. Note that where the time span t to $t+h$ encompasses a step change in power level P_i , the integral is evaluated in parts on either side of the discontinuity.

In order to obtain approximate expressions for the integrals of T_j and T_j^4 , we use the general linear two-point integration formula:

$$\int_t^{t+h} f(t) dt = h [(1 - \alpha) f(t) + \alpha f(t+h)] \quad (I-13)$$

where f is a function of time and α is any number between zero and one. It can be shown that the quadrature given by Equation (I-13) is of order h^2 --that is, the error in Equation (I-13) is proportional to h^2 as h approaches zero. Hence, the integration scheme is most accurate for small values of h .

The choice of the quantity α , which we call the integration parameter, influences the accuracy and stability of the numerical solution of the set of difference equations that has been derived.

Using the integration formula, the heat-balance equations become:

$$h \left\{ \sum_j C_{ij} [(1 - \alpha) T_j(t) + \alpha T_j(t+h)] + \sum_j A_{ij} \alpha [(1 - \alpha) T_j^4(t) + \alpha T_j^4(t+h)] \right\} \\ + \int_t^{t+h} P_i(t) dt + M_i [T_i(t+h) - T_i(t)] = 0 \quad (I-14)$$

Equation (I-14) is one of a set of non-linear simultaneous difference equations. This set of equations can be solved for $T_i(t + h)$ when the values $T_i(t)$ are given.

1. Stability of Integration Scheme

In order to investigate the factors which determine the optimum value of the integration parameter α , we will compare solutions of Equation (I-14) with solutions of Equation (I-2). In order to present this analysis as simply as possible, we investigate the conductive cooling of a lumped thermal mass M with an initial temperature T_0 connected by a conductance C to a sink at zero degrees. If the temperature is T at time t , Equation (I-2) becomes

$$CT + M \frac{dT}{dt} = 0 \quad (I-15)$$

with exact solution

$$T = T_0 e^{-t/\tau} \quad (I-16)$$

where

$$\tau = \frac{M}{C}. \quad (I-17)$$

The corresponding difference equation is

$$hC [(1 - \alpha) T(t) + \alpha T(t + h)] + M[T(t + h) - T(t)] = 0 \quad (I-18)$$

The solution to Equation (I-18) is

$$T(nh) = T_0 \left(\frac{1 - (1 - \alpha) \frac{h}{\tau}}{1 + \alpha \frac{h}{\tau}} \right)^n \quad (I-19)$$

The maximum discrepancy between the values of T calculated from (I-16) and (I-19) is dependent on α and the ratio h/τ as shown in Figures (I-1) and (I-2). The error is given as a percentage of T_0 .

The time at which the maximum error occurs is

$$t = h \quad \text{for } h > \tau \\ t = \tau \quad \text{for } h < \tau$$

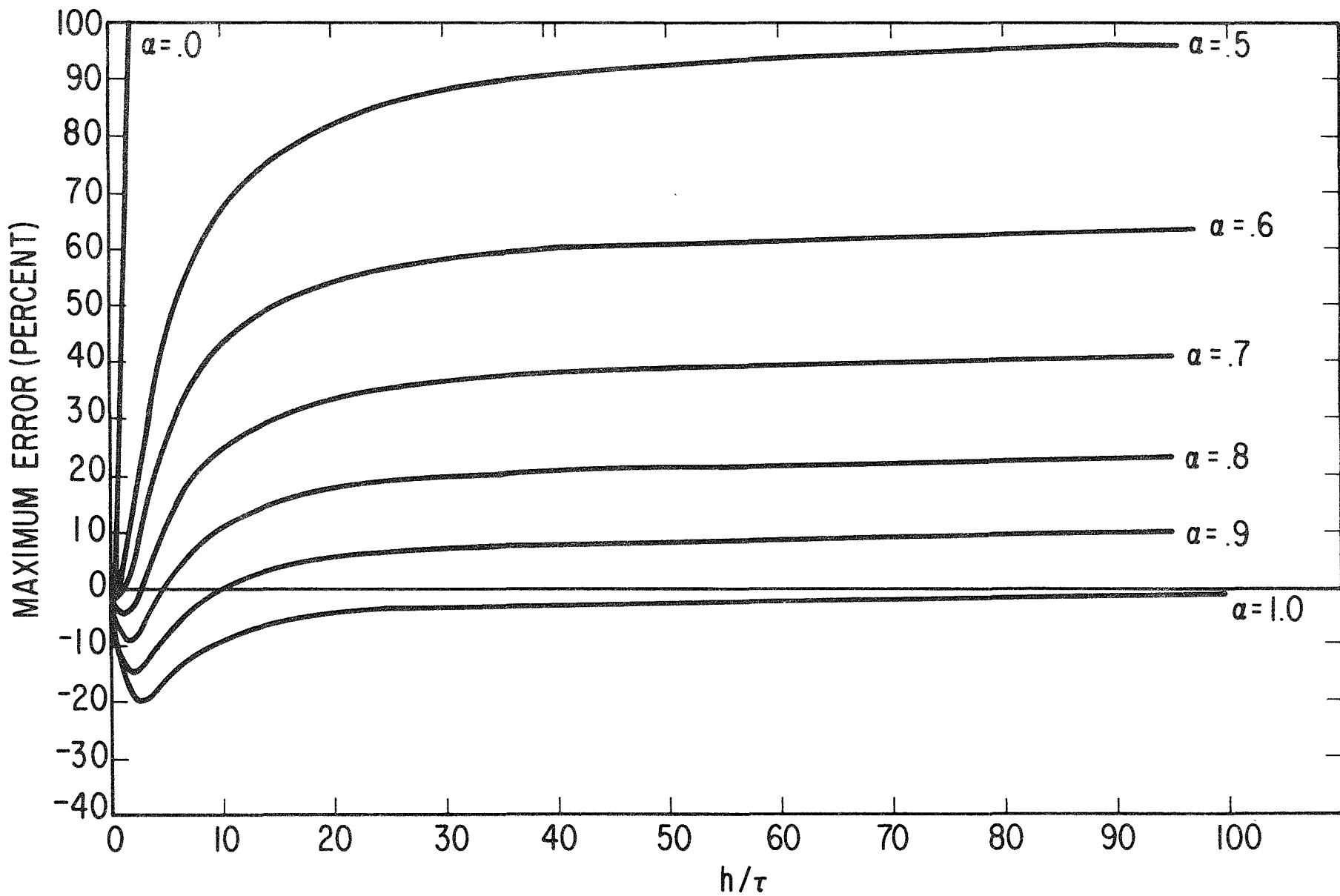


FIGURE I-1 MAXIMUM PERCENTAGE ERROR IN TEMPERATURE AS A FUNCTION OF THE RATIO OF TIME INCREMENT TO TIME CONSTANT FOR VARIOUS VALUES OF THE INTEGRATION PARAMETER α .

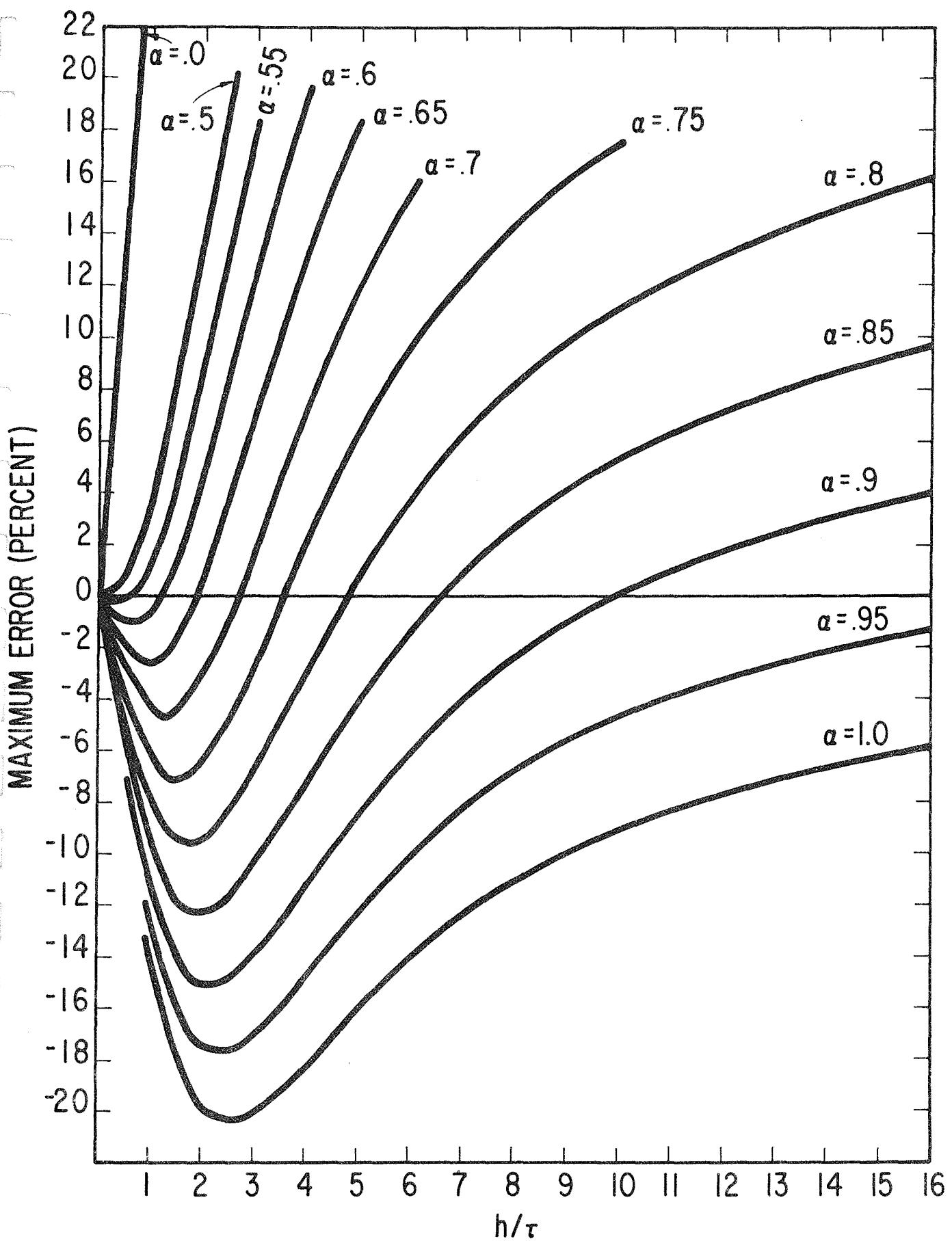


FIGURE I-2 DETAILS IN THE NEIGHBORHOOD OF THE ORIGIN OF FIGURE I-1

It will be seen from Equation (I-19) that if the quantity

$$\beta = \frac{1 - (1 - \alpha) \frac{h}{\tau}}{1 + \alpha \frac{h}{\tau}} \quad (I-20)$$

becomes greater than unity in absolute value, the temperature T_{nh} will tend to infinity instead of zero. This happens when

$$\frac{h}{\tau} > \frac{2}{1 - 2\alpha}, \quad \alpha < \frac{1}{2} \quad (I-21)$$

and never for $\alpha > \frac{1}{2}$. Thus, values of α greater than $\frac{1}{2}$ always lead to stable solutions.

2. Selection of the Integration Parameter

In order to simplify the discussion of problems involving many zones, we assume the terms in T_j^4 can be linearized. Then the entire set of differential equations (I-2) can be written in matrix notation as

$$CT + P + M \frac{dT}{dt} = -R \quad (I-22)$$

where

C - matrix of conductance, including radiative conductances

T - vector whose elements are the nodal temperatures

M - diagonal matrix of the thermal masses

P - vector whose elements are the power inputs

R - vector of the radiation powers which are the constant terms obtained in the linearization process.

The solution to Equation (I-22) is

$$T = F E + G(t) \quad (I-23)$$

where

F - matrix of constants depending on the initial conditions

E - vector whose components are e^{-t/τ_k}

G - vector representing the particular integral

τ_k - time constant

The time constants τ_k are found by setting the determinant of the matrix $C - \frac{1}{\tau} M$ equal to zero

$$|C - \frac{1}{\tau} M| = 0 . \quad (I-24)$$

The finite-difference equation corresponding to Equation (I-22) is

$$\begin{aligned} hC [(1 - \alpha) T(t) + \alpha T(t + h)] + \int_t^{t+h} P dt \\ + M [T(t + h) - T(t)] = -hR \end{aligned} \quad (I-25)$$

The solution to Equation (I-25) is

$$T = F B + H(t) . \quad (I-26)$$

where

F - the same matrix introduced in Equation (I-23)

B - vector with components $(\beta_k)^n$

H - vector representing the particular sum.

The quantities β_k are found by solving the equation

$$|C - \frac{1 - \beta}{h(1 - \alpha + \alpha\beta)} M| = 0 \quad (I-27)$$

Comparison of Equations (I-27) and (I-24) shows that

$$\frac{1}{\tau_k} = \frac{1 - \beta_k}{h(1 - \alpha + \alpha\beta_k)} \quad (I-28)$$

or

$$\beta_k = \frac{1 - (1 - \alpha) \frac{h}{\tau_k}}{1 + \alpha \frac{h}{\tau_k}} \quad (I-29)$$

If the quantities $\frac{h}{\tau_k}$ vary over a wide range, then it may be seen from Figure (I-1) that a value of α of about 0.87 minimizes the maximum percentage discrepancy between e^{-nh/τ_k} and $(\beta_k)^n$ over all values of $\frac{h}{\tau_k}$. If the quantities $\frac{h}{\tau_k}$ vary over a small range, however, a smaller value

of α gives the minimum error. Figure (I-3) shows the optimum value of α as a function of the maximum $\frac{h}{\tau_k}$. In practice, one often finds the optimum value of α by numerical experimentation.

3. Selection of the Time Increment

It is shown in Fig. (I-1) that the error introduced by the quadrature in time is reduced by making $\frac{h}{\tau}$ small. However, the time increment h must not be made too small because if a small error ϵ is made at each step in solving the difference equations for $T(t + h)$, this error may be highly magnified in succeeding steps. To show this most simply, we revert to the case of a single lumped mass. After we introduce the error ϵ , Equation (I-19) becomes

$$T(h) = T_0 \beta + \epsilon$$

$$T(2h) = T_0 \beta^2 + (1 + \beta)\epsilon \quad (I-30)$$

$$T(nh) = T_0 \beta^n + \frac{\epsilon}{1 - \beta}$$

We now substitute for β from Equation (I-20) and find

$$T(nh) = T_0 \beta^n + \left(\frac{\tau}{h} + \alpha\right)\epsilon \quad (I-31)$$

It is seen from Equation (I-31) that a correlated error will be magnified by the factor $(\frac{\tau}{h} + \alpha)$ which will be large if $\frac{h}{\tau}$ is small. A generalization of the argument shows that magnification factors $(\frac{\tau_k}{h} + \alpha)$ occur in multizone problems.

B. Solution of Integral Form of Heat-Balance Equations

For values of the integration factor α greater than zero, Equation (I-14) represents a set of implicit non-linear simultaneous equations. At each time increment, the simultaneous heat-balance equations are solved by a Gauss-Seidel procedure using the Newton-Raphson Iteration Method to solve for the individual nodal temperatures.

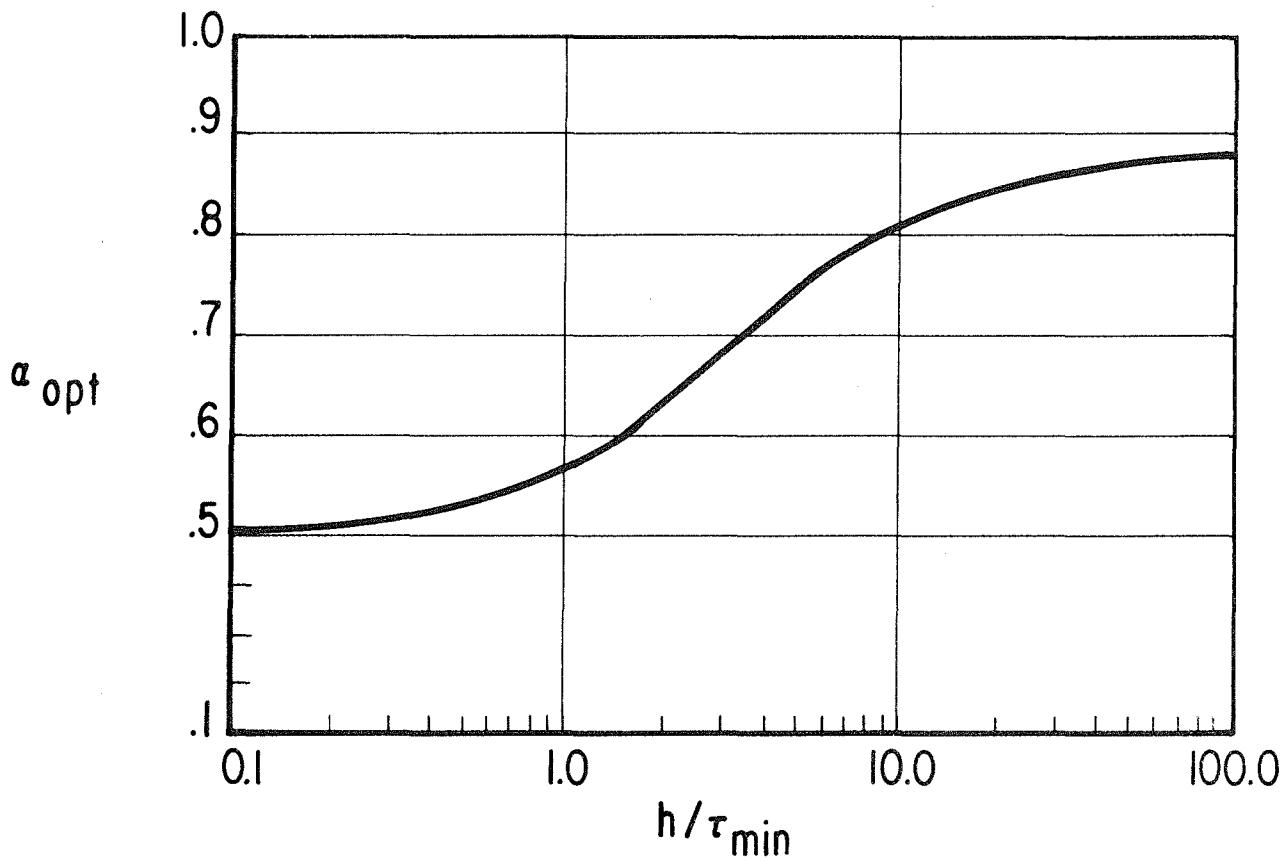


FIGURE I-3 THE OPTIMUM VALUE OF THE INTEGRATION PARAMETER AS A FUNCTION OF THE RATIO OF TIME INCREMENT TO SMALLEST TIME CONSTANT

The ordinary differential equations (I-1) can be solved only when starting temperatures $T_i(0)$ are given. In certain equations, however, the quantity M_i may be zero and the starting temperature unknown. In that case, the corresponding value of $T_i(0)$ must be calculated so that Equation (I-2) is satisfied initially as well as at all succeeding times. The program automatically carries out this calculation before proceeding with the main computation. During the iterative solution for the initial temperature of nodes with zero thermal mass, the sum of the residual errors is printed out after every 50 passes through the set of equations.

While the Gauss-Seidel procedure used to solve the difference Equation (I-14) is well known, it will be briefly described here for the sake of completeness.

To begin the process, the values of $T_i(t)$ are used as a starting approximation to $T_i(t + h)$. New approximations are obtained using the Newton-Raphson Iteration Method to solve:

$$A T_i(t + h) + B T_i^4(t + h) + C = F(T_i) = 0 \quad (I-32)$$

where

$$A = M_i + h \alpha C_{ii} \quad (I-33a)$$

$$B = h \alpha A_{ii} \sigma \quad (I-33b)$$

$$\begin{aligned} C = h \sum_{j \neq i} C_{ij} [(1 - \alpha) T_j(t) + \alpha T_j(t + h)] \\ + h \sum_{j \neq i} A_{ij} \sigma [(1 - \alpha) T_j^4(t) + \alpha T_j^4(t + h)] \\ + h C_{ii} (1 - \alpha) T_i(t) + h A_{ii} \sigma (1 - \alpha) T_i^4(t) \\ - M_i T_i(t) + \int_t^{t+h} P_i(t) dt \end{aligned} \quad (I-33c)$$

According to the Newton-Raphson procedure, the new value T_i ($t + h$) is found from:

$$T_i(t+h) - \frac{F(T_i)}{F'(T_i)} \rightarrow T_i(t+h) \quad (I-34)$$

where

$$F'(T_i) = A + 4BT_i^3(t+h) \quad (I-35)$$

This process continues until the solution to Equation (I-32) converges to within 10^{-5} . If the solution to Equation (I-32) is not found within 50 iterations, an error message is printed out:

CHECK YOUR DATA FOR EQUATION NO. i

and the solution is terminated.

When the root to Equation (I-32), $T_i^*(t+h)$, has been found, the old value of $T_i(t+h)$ is replaced by:

$$T_i'(t+h) = T_i(t+h) + \rho [T_i^*(t+h) - T_i(t+h)] \quad (I-36)$$

where ρ is a relaxation factor, and the next equation is set up and solved. The relaxation factor ρ is used to accelerate the solution of the simultaneous equations. At the end of one pass through the set of simultaneous equations (say iteration n), a residual error term is calculated:

$$\epsilon_n = \sum_i |T_i'(t+h) - T_i(t+h)| \quad (I-37)$$

This error term is compared with some tolerance value specified on the data control cards; if the residual error is larger than the tolerance, the process is repeated.

A further check is made at the end of each pass through the set of heat-balance equations to determine if the solution is convergent.

The residual error at iteration step n is compared with that at the previous time step. If the difference $\epsilon_n - \epsilon_{n-1}$ is positive, the method is considered divergent, and the solution is terminated, and the next control card is processed.

In principle, an optimum value of relaxation factor ρ exists for each problem. However, this value is generally not known ahead of time; in practice, one simply makes use of the fact that an optimum exists, and the best value of ρ is found by numerical experiments.

V. ENERGY BALANCES

At each time step in the program, an overall energy balance is made to allow an evaluation of the accuracy of the solution.

From the integral form of Equation (I-6), a quantity $E_s(t)$ called the System Energy Imbalance is defined:

$$E_s(t) = \sum_i M_i T_i(0) - \sum_i M_i T_i(t) \\ - \sum_i \int_0^t P_i(t) dt - \sum_i \int_0^t A_i \sigma T_i^4 dt \\ - \sum_i \int_0^t C_i T_i dt . \quad (I-38)$$

The current value of E_s is found from the value at the previous time step and the two-point integration formula (I-13):

$$E_s(t+h) = E_s(t) + \sum_i M_i [T_i(t) - T_i(t+h)] \\ - \sum_i \int_t^{t+h} P_i(t) dt - \sum_i \int_t^{t+h} A_i \sigma T_i^4(t) dt \\ - \sum_i \int_t^{t+h} C_i T_i(t) dt . \quad (I-39)$$

If the computation were perfectly accurate, E_s should be zero at all times. In practice, of course, one requires that E_s be small. Other quantities, such as:

STORED INTERNAL ENERGY:

$$E_p = \sum_i M_i T_i(t) \quad (I-40)$$

TOTAL ENERGY INTO SYSTEM:

$$E_{in} = \sum_i \int_0^t P_i dt , \quad (I-41)$$

are also printed in order to provide numbers that can be compared with E_s . The quantity E_p also serves to indicate when a system has reached the end of a transient, and E_{in} is to be used to check that the input power is correctly computed.

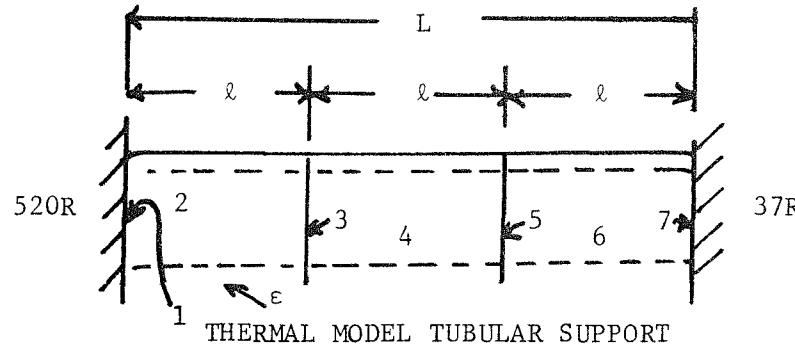
VI. SAMPLE PROBLEMS

A sample problem is presented to illustrate the procedure for coding the input data for ADLGTA. For the purpose of this illustration, the finite-difference thermal models are formulated using the Zone Method of Strong and Emslie.* The conventional nodal or lumped parameter finite-difference technique can also be used to formulate problems for solution with ADLGTA.

Consider the thermal model of a tubular support shown in the following figure. The support of length, ℓ , and cross-sectional area, A , is positioned between a high-temperature source at 520R and a sink at 37R. The temperature distribution is steady in time and varies spacially only in the longitudinal direction. The inner surface is

* P. F. Strong and A. G. Emslie, "The Method of Zones for the Calculation of Temperature Distribution," ASME Paper 65-WA/HT-47.

adiabatic; heat is radiated from the outer surface, to a zero temperature environment; and the support is subdivided into three zones of equal length, ℓ . ϵ is the total hemispherical emittance of the outer surface of the tubular support.



The temperature subscripts noted in the above figure represent the mean zone temperatures (T_2 , T_4 , and T_6) and the temperature of the zone boundaries (T_1 , T_3 , T_5 and T_7).

The following equations, which describe the heat flow and the boundary conditions, can be written according to the Zone Method:

$$\frac{dT_1}{dt} = 0; \quad T_1 = 520 \quad (I-42)$$

$$\frac{KA}{\ell} (12T_2 - 6T_1 - 6T_3) + \pi D\ell \epsilon \sigma T_2^4 = 0 \quad (I-43)$$

$$\frac{KA}{\ell} (6T_2 - 4T_3 - 2T_1) + \frac{KA}{\ell} (6T_4 - 4T_3 - 2T_5) = 0 \quad (I-44)$$

$$\frac{KA}{\ell} (12T_4 - 6T_3 - 6T_5) + \pi D\ell \epsilon \sigma T_4^4 = 0 \quad (I-45)$$

$$\frac{KA}{\ell} (6T_6 - 4T_5 - 2T_3) + \frac{KA}{\ell} (6T_6 - 4T_5 - 2T_7) = 0 \quad (I-46)$$

$$\frac{KA}{\ell} (12T_6 - 6T_5 - 6T_7) + \pi D\ell \epsilon \sigma T_6^4 = 0 \quad (I-47)$$

$$\frac{dT_7}{dt} = 0; \quad T_7 = 37 \quad (I-48)$$

Equations (I-43), (I-45) and (I-47) are the heat-balance equations for the mean zone temperatures; Equations (I-44) and (I-46) are joining equations necessary to describe the fluxes at the boundaries. The temperatures of boundaries 1 and 7 are constant and are specified in the statement of the problem.

For the sample problem, we assume $KA/\ell = 0.02 \text{ Btu/hr } ^\circ\text{R}$ and $\pi D\ell\varepsilon = 0.04 \text{ ft}^2$. The data for the above equations, in the form required by the program, are given in Table I-2.

The data on the first cards (A_i , C_i) for the sets describing the equations were determined by considering the following equation, which describes the net flux out of the system:

$$Q_{OUT} = 0.02 \left(6T_2 - 4T_1 - 2T_3 \right) + 0.04 (\sigma T_2^4 + \sigma T_4^4 + \sigma T_6^4) \\ + 0.02 (6T_6 - 4T_7 - 2T_5)$$

The output for the sample problem is shown in Table I-3.

VII. OUTPUT DATA

Table I-3 shows the output data for the sample problem discussed in the preceding Section. The bulk of the output consists of the time histories of the various temperatures. One page is printed off-line for each time interval specified on the control card. It consists of three lines of heading followed by pairs of index numbers and temperatures up to the highest number specified by the control card.

The first heading line is simply the alphanumeric heading information supplied on the heading card of input. The second line gives the contents of the last control card read. The third line shows the values of time, E_p , E_S , and E_{in} as defined in Equations (I-40), (I-38), and (I-41), respectively, as well as the total number of iterations used in solving the systems of equations since the last off-line print.

TABLE I-2
INPUT DATA FOR SAMPLE PROBLEM

Card column

5	25	45	50	55	60
			5	9	7
SAMPLE PROBLEM					
1 0.0	-0.08		1	1	
-1 1.0	520.0		1	99	
2 0.04	0.12		2	1	
2 0.04	0.24		2	2	
1 0.0	-0.12		2	3	
3 0.0	-0.12		2	4	
-2 0.0	0.0		2	99	
3 0.0	-0.04		3	1	
2 0.0	0.12		3	2	
3 0.0	-0.08		3	3	
1 0.0	-0.04		3	4	
4 0.0	0.12		3	5	
3 0.0	-0.08		3	6	
5 0.0	-0.04		3	7	
-3 0.0	0.0		3	99	
4 0.04	0.0		4	1	
4 0.04	0.24		4	2	
3 0.0	-0.12		4	3	
5 0.0	-0.12		4	4	
-4 0.0	0.0		4	99	
5 0.0	-0.04		5	1	
4 0.0	0.12		5	2	
5 0.0	-0.08		5	3	
3 0.0	-0.04		5	4	
6 0.0	0.12		5	5	
5 0.0	-0.08		5	6	
7 0.0	-0.04		5	7	
-5 0.0	0.0		5	99	
6 0.04	0.12		6	1	
6 0.04	0.24		6	2	
5 0.0	-0.12		6	3	
7 0.0	-0.12		6	4	
-6 0.0	0.0		6	99	
7 0.0	-0.08		7	1	
-7 1.0	37.0		7	99	
1.5 0.9E-02 1.0	1 10 1.0	300.0	7 1.0	1	
			9 6		
			8		

TABLE I-3
OUTPUT DATA FOR SAMPLE PROBLEM

SAMPLE PROBLEM

TEMPERATURE MEASURED IN DEGREES RANKINE, POWER IN Btu/HR

REL= 1.50 TOL= 9.0E-03 DT= 1.0 wF= 1 PF= 10 IMX= 1.0 TB= 300.0 SIZE= 7 ALPHA= 1.00
T1 = 1.00 EP = 5.5700000E+02 FS = -7.61205E-05 EIN = 0. NT= 1

1 520.0000 2 411.7004 3 319.8040 4 246.4164 5 175.1346 6 100.0312 7 37.0000

AVERAGE TIME FOR ONE PASS THROUGH ENTIRE SET OF EQUATIONS IS .01600 SECONDS

TIME PER REL TOL CARD = .06000 SECONDS

ELAPSED TIME IN TIA SOLUTION = .064SECONDS

TOTAL ELAPSED TIME IN TIA SOLUTION = 1.481 SECONDS

CHECKOUT = .144SECONDS

SOLUTION = .064SECONDS

Before the solution to the problem is printed, information about the input data is recorded. The off-line print consists of:

1. The heading;
2. The total average power for each equation (unless zero);
3. The equation number and sum of the elements of any rows whose sum is over tolerance. As shown in Equations (I-7) and (I-8), S_R is used to denote the sum of radiation terms and S_C is used to denote the sum of conduction terms;
4. A line of print which gives the number of equations read in, N_E , the number of row sum failures, N_R and N_C , for radiation and conduction, respectively, the number N_p , of periodic powers with incorrect average level, and P_T , the total average power to the system;
5. The column number and the sum of the elements of any columns whose sum is over tolerance. As shown in Equations (I-9) and (I-10), $C_S R$ is used to denote the sum of radiation terms, and $C_S C$ is used to denote the sum of conduction terms; and
6. A line of print giving N_{CSC} and N_{CSR} , which are the numbers of column sum failures for conduction and radiation, respectively.

ADLGTA uses logical unit numbers 5, 6, 7, 8 and 9. Logical units 5 and 6 are the system input and output units, respectively. The file output on unit 6 contains the computed solution. Logical units 7, 8 and 9 are used as scratch tapes; the final form of the data describing the problem solved by ADLGTA is ordinarily contained in the file of logical unit 9.

APPENDIX II

SAMPLE LISTING OF COMPUTER MODEL OF PROBE LOCATION 3 FOR MODE 3 OPERATION IN LUNAR ENVIRONMENT

This Appendix contains a complete computer listing of a typical computer model of the lunar heat flow probe in the lunar environment. The following tabulation indicates the descriptions appropriate to the eight computer models that were developed as a part of the subject work:

<u>Experiment Location</u>	<u>Conductivity Experiment</u>
1	Mode 2
2	Mode 2
3	Mode 2
4	Mode 2
1	Mode 3
2	Mode 3
3	Mode 3
4	Mode 3

The model shown was developed for Mode 3 operation at location 3 of the probe assuming an initial temperature of 225°K, and a lunar medium conductivity of $k = 0.0017 \text{ w/cm}^{-2}\text{K}$ and density - specific heat product of $\rho c = 1.339 \text{ w-sec/}^{\circ}\text{K}$. The identification numbers of the major components in the model are listed in Table II-1.

Table II-2 is a listing of the input data describing the model. The format of the input data has been discussed in Appendix I.

The units for the input data are:

Radiative couplings: $A_{ij} = \text{cm}^2$
Conductive couplings: $C_{ij} = \text{w/}^{\circ}\text{K}$
Power: $P_i = \text{w}$
Thermal mass: $M_i = \text{w-min/}^{\circ}\text{K.}$

TABLE II-1

IDENTIFICATION NUMBERS OF
MAJOR COMPONENTS IN THERMAL MODEL

<u>Components</u>	<u>Identification Number</u>	<u>Refer to</u>
Gradient Sensor	13	Figure 7
Ring Sensor	50	Figure 8
Heater	19	Figure 7
Probe Details	Remaining Nodes Between 1-121	Figure 6
Drill Casing	Zone: 141, 181, ..., 701 Boundaries: 123, 163, ..., 723	Figure 11 and Table II
Lunar Medium	Remaining Nodes Between 122-732	Figures 11 and 12 and Table I

TABLE II-2
COMPUTER LISTING OF EXPERIMENT LOCATION 3
FOR MODE 3 OPERATION IN THE LUNAR ENVIRONMENT

LOC	MODE	K ⁸	0.0017	T=225K	RHOC=1.339	LUNAR MEDIUM
1	3	0.000000000	0.000000000	1	1	
3		0.000000000	0.028440000	1	2	
1		-1.695063000	.018960000	1	3	
5		0.000000000	.009480000	1	4	
501		1.6950630		1	5	
3			0.06188	1	9	
1			-0.04125	1	10	
5			-0.02063	1	11	
99			0.01056	1	12	
1			-0.00839	1	13	
12			-0.00352	1	14	
115			0.00203	1	15	
116			-0.00068	1	16	
-1				1	99	
2	0.0			2	1	
3			0.13554	2	2	
2	-0.324		-0.08217	2	3	
4			-0.05337	2	4	
13	0.112			2	5	
24	0.013			2	6	
29	0.010			2	7	
72	0.009			2	8	
99	0.19			2	9	
-2				2	99	
3			0.48210	3	1	
1			-0.02844	3	2	
2			-0.16123	3	3	
4			-0.26394	3	4	
5			-0.02844	3	5	
3			0.12376	3	6	
1			-0.06188	3	7	
5			-0.06188	3	8	
-3	0.05106			3	9	
4	0.0			4	1	
3			0.28968	4	2	
2	-6.308845170		-210x20000	4	3	
2	0.000000000		-0.079060000	4	4	
461	5.14410117			4	5	
501	1.144744			4	6	
-4				4	99	
5			0.02844	5	1	
5	-1.10236		-0.03648	5	2	
1			-0.00948	5	3	
6			0.02628	5	4	
19			-0.00876	5	5	
10	1.10236			5	6	
3			0.06188	5	7	
6			-0.04125	5	8	
1			-0.02063	5	9	
-5				5	99	
6			1.28706	6	1	
5			-0.02628	6	2	
19			-0.02628	6	3	
8			-0.58391	6	4	
35			-0.65059	6	5	
-6	0.01178			6	6	
7				6	7	
34			0.01788	7	8	
7			-0.01192	7	9	
33			-0.00596	7	99	
18			0.00264	7	1	
7			-0.00176	7	2	
17			-0.00088	7	3	
+7				7	4	
R				7	5	
6			0.56724	7	6	
8	-0.10294		-0.40777	7	7	
35			-0.19674	7	8	
10			0.05124	7	9	
12			-0.01397	7	99	
12	0.10294			8	1	
-8	0.0			8	2	
34			1.20654	8	3	
9	-3.440338440		-813060000	8	4	
35	0.000000000		-393480000	8	5	
461	3.44033844			8	6	
-9				8	7	
10				8	8	
10	1.19493		0.07512	9	1	
R			-0.04668	9	2	
12			-0.02844	9	3	
12	-0.09357			9	4	
5	-1.10236			9	5	
-10	0.00452			9	6	
12				9	7	
13			0.39902	12	1	
12	-0.19651		-0.26601	12	2	
14			-0.13301	12	3	
10	0.09157			12	4	
6	0.10294			12	5	
99			0.01056	12	6	
12			-0.00704	12	7	
-1			-0.00352	12	8	
110			0.00168	12	9	
12			-0.00112	12	99	
24			-0.00056	12	1	
10			0.02388	12	2	
12			-0.01447	12	3	
4			-0.00941	12	4	
-12				12	5	
13				12	6	
13	0.66913		0.79804	13	7	
12			-0.39902	13	8	
14			-0.39902	13	9	
19	-0.66913			13	99	
13	0.191			13	1	
-2	-0.117			13	2	
24	-0.042			13	3	
26	-0.001			13	4	
29	-0.024			13	5	
72	-0.022			13	6	
-13	0.05833			13	7	
14			0.39902	14	8	
13			-0.45597	14	9	
14	-0.02873			14	10	

12	-0.13301	14	6
24	0.28495	14	5
26	-0.09499	14	6
32	0.02573	14	7
-14		14	99
17		17	1
37	0.01788	17	2
17	-0.01192	17	3
38	-0.00596	17	4
18	0.00264	17	5
17	-0.00176	17	6
7	-0.00088	17	7
-17		17	99
18	0.0	18	1
18	7.96270	18	2
7	-0.00264	18	3
19	-3.78118	18	4
421	-4.19152n	18	5
17	-0.00264	18	6
-18	0.01691	18	99
19		19	1
6	-0.02628	19	6
5	0.00876	19	7
20	-0.02628	19	8
21	0.00876	19	9
19	0.03504	19	10
19	11.74349	19	11
13	-0.64913	19	12
18	-3.78118	19	13
421	-7.3n318n	19	14
6	-0.01178	19	15
-19	0.01418	19	99
20		20	1
21	1.28706	20	2
19	-0.02628	20	3
21	-0.02628	20	4
32	-0.58391	20	5
36	-0.65059	20	6
-20	0.01178	20	99
21		21	1
20	0.02628	21	2
21	-0.02812	21	3
19	-0.00876	21	4
27	0.01590	21	5
28	-0.00530	21	6
21	-0.5	21	7
24	0.5	21	8
-21		21	99
22	0.0	22	1
37	1.20654	22	2
22	-3.440338440	22	3
36	0.000000000	22	4
381	3.44033844	22	5
-22		22	99
24		24	1
24	0.5699	24	2
14	-0.28495	24	3
26	-0.28495	24	4
24	1.81081	24	5
2	-0.013	24	6
13	-0.042	24	7
29	-0.039	24	8
72	-0.076	24	9
27	-1.59781	24	10
28	-0.0020	24	11
24	1.0	24	12
32	-0.5	24	13
21	-0.5	24	14
12	0.00056	24	15
110	-0.00168	24	16
24	0.00112	24	17
88	0.000000000	24	18
98	0.000000000	24	19
24	0.000000000	24	20
-24	0.0045	24	99
26		26	1
24	0.28495	26	2
26	-1.361	26	3
14	-0.18996	26	4
13	0.001	26	5
24	0.0002	26	6
29	0.001	26	7
72	0.330	26	8
87	0.114	26	9
65	0.002	26	10
26	-0.00136	26	11
88	0.00136	26	12
+26		26	99
27	0.0	27	1
27	4.67604	27	2
21	-0.01590	27	3
28	-0.01590	27	4
24	-1.59781	27	5
381	-2.97823n	27	6
-27	0.00716	27	99
28		28	1
27	0.01590	28	2
28	-0.01352	28	3
21	-0.00530	28	4
29	0.00438	28	5
75	-0.00146	28	6
-28		28	99
29	0.0	29	1
29	3.84437	29	2
28	-0.00438	29	3
75	-0.00438	29	4
29	1.979	29	5
2	-0.010	29	6
13	-0.024	29	7
24	-0.019	29	8
26	-0.001	29	9
72	-0.028	29	10
87	-0.067	29	11
65	-0.001	29	12
381	-2.04899n	29	13
29	0.83	29	14
98	-0.83	29	16
341	-1.87372	29	17
-29	0.00712	29	99
32		32	1
20	0.56724	32	2
32	-0.02573	32	3
36	-0.37050	32	4
14	0.02573	32	5
32	-0.5	32	6
24	0.5	32	7
-32	0.00015	32	99
33		33	1
34	0.01788	33	2
33	-4.10268510	33	3
7	0.000000000	33	4
501	0.410269	33	5

-33		33	99
34		34	1
34	2.34912	34	2
33	-0.01788	34	3
7	-0.01788	34	4
9	=1.18998	34	5
35	-1.12338	34	6
-34	0.00403	34	99
35		35	1
6	0.66726	35	2
8	-0.21341	35	3
34	1.10682	35	4
9	-0.37692	35	5
35	-1.18375	35	6
-35		35	99
36		36	1
20	0.66726	36	2
37	-0.21341	36	3
37	1.10682	36	4
22	-0.37692	36	5
36	-1.18375	36	6
-36		36	99
37		37	1
37	2.34912	37	2
17	-0.01788	37	3
38	-0.01788	37	4
22	=1.18998	37	5
36	-1.12338	37	6
-37	0.00403	37	99
38		38	1
37	0.01788	38	2
36	-4.10268510	38	3
17	0.00000000	38	4
38	0.410265	38	5
-38		38	99
50	0.0	50	1
181	-0.24818	50	2
56	-1.39446	50	3
51	-0.1857	50	4
61	-2.1662	50	5
51	-0.0032466	50	6
50	0.0021444	50	7
52	0.0010822	50	8
50	6.91178	50	9
221	-2.86724	50	10
50		50	11
52	-0.01	50	12
-50	0.02442	50	99
51	0.0	51	1
51	4.2589	51	2
50	-0.1857	51	3
61	-4.0732	51	4
51	0.0064932	51	5
50	-0.0032466	51	6
52	-0.0032466	51	7
51	0.003421	51	99
52	0.0	52	1
51	0.0032466	52	2
52	-0.0021444	52	3
50	-0.0010822	52	4
50	0.0179580	52	5
53	-0.0119720	52	6
52	-0.0119720	52	7
54	-0.0059460	52	8
51	0.0053440	52	9
52	-0.0035760	52	10
55	-0.0017880	52	11
56	0.0034968	52	12
52	-0.0023272	52	13
55	-0.0011636	52	14
51	0.00432	52	15
52	-0.00288	52	16
54	-0.00144	52	17
52	-0.01	52	18
50	0.0	52	99
-52	0.0	53	1
53	0.0	53	2
51	A.89453	53	3
181	-A.89453A	53	4
53	0.0359160	53	5
52	-0.0179580	53	6
54	-0.0179580	53	7
53	0.00864	53	8
52	-0.00432	53	9
54	-0.00432	53	10
53	7.039	53	11
53	-5.026	53	12
57	-1.032	53	13
59	-1.506	53	14
61	-1.809	53	15
64	-2.285	53	16
69	-1.050	53	17
73	-1.161	53	18
-53	0.04492	53	99
54	0.0	54	1
53	0.0	54	2
54	-0.0179580	54	3
52	-0.0119720	54	4
52	-0.0059460	54	5
59	0.0141000	54	6
54	-0.0094000	54	7
60	-0.0047000	54	8
53	0.00432	54	9
54	-0.00288	54	10
52	-0.00144	54	11
54	-0.000682	54	12
73	0.000682	54	13
-54	0.0	54	99
55	0.0	55	1
56	0.0	55	2
56	0.00349080	55	3
55	-0.00232720	55	4
52	-0.00116360	55	5
57	0.00885600	55	6
55	-0.00590400	55	7
58	-0.00295200	55	8
61	0.00536400	55	9
55	-0.00357600	55	10
52	-0.00178800	55	11
-55	0.0	55	99
56	0.0	56	1
56	0.0	56	2
56	4.32036	56	3
181	-0.248730	56	4
50	-1.39446	56	5
56	0.0069816	56	6
55	-0.0034908	56	7
52	-0.0034908	56	8
221	-2.64717n	56	99
56	0.00424	57	1
57	0.0	57	2
57	8.11104	57	3
261	-8.043070	57	4
57	0.017712	57	5
55	-0.008856	57	6
56	-0.008856	57	7

221	-3.022970	6.636	57	7
57		-.032	57	16
53		-4.739	57	17
57		.888	57	18
61		.728	57	19
52		.049	57	20
67			57	21
-57	0.020778	0.0	57	99
58	0.0	0.0	58	1
62		.00257982	58	2
58		-0.00171988	58	3
74		-0.00085994	58	4
57		.00885600	58	5
58		-0.00590400	58	6
55		-0.00295200	58	7
-54	0.0	0.0	58	99
59	0.0	0.0	59	1
59	3.774343290	0.000000000	59	2
141	-3.774343		59	3
59		.028200	59	4
54		-0.014100	59	5
60		-0.014100	59	6
59		2.979	59	16
53		-.596	59	17
59		-1.658	59	18
64		-.424	59	19
73		.261	59	20
-59	0.0066347	0.0	59	99
60	0.0	0.0	60	1
59		.01410000	60	2
60		-0.00940000	60	3
54		-0.00470000	60	4
64		.00871536	60	5
60		-0.00541024	60	6
74		-0.00290512	60	7
-60	0.0	0.0	60	99
61	0.0	0.0	61	1
61	5.2394		61	2
50	-2.1667		61	3
51	-4.0732		61	4
61		0.010728	61	5
52		-0.005344	61	6
55		-0.005344	61	7
61	5.720		61	16
53	-.889		61	17
57	-.888		61	18
61	-3.817		61	19
62	-.086		61	20
68	-.040		61	21
-61	0.009386	0.0	61	99
62	0.0	0.0	62	1
62	7.689086250	0.000000000	62	2
301	-3.94152025		62	3
62		.00515964	62	4
58		-0.00257982	62	5
74		-0.00257982	62	6
201	-3.727566		62	7
62	7.332		62	16
57	-.928		62	17
61	-.086		62	18
62	-5.093		62	19
63	-.999		62	20
66	-.052		62	21
72	-.174		62	22
-62	0.0032686	0.0	62	99
63	0.0	0.0	63	1
63	7.689086250	0.000000000	63	2
341	-3.549060		63	3
63		.00515964	63	4
74		-0.00257982	63	5
75		-0.00257982	63	6
301	-4.140026		63	7
63	7.318		63	16
62	-.999		63	17
63	-5.129		63	18
65	-.053		63	19
72	-1.137		63	20
-63	0.0032686	0.0	63	99
64	0.0	0.0	64	1
64		.01743072	64	2
60		-0.00871536	64	3
76		-0.00871536	64	4
64	3.369946020	0.000000000	64	5
141	-3.349946		64	6
64	2.656		64	16
53	-.285		64	17
59	-.424		64	18
64	-1.143		64	19
73	-.804		64	20
-64	0.0032686	0.0	64	99
65	0.0	0.0	65	1
65		.00193272	65	2
86		-0.00096636	65	3
77		-0.00096636	65	4
65	0.189		65	10
26	-0.009		65	11
29	-0.001		65	12
87	-0.184		65	13
65	.053		65	16
63	-.053		65	17
65	0.000000000	.013198848	65	18
86	0.000000000	-.006599424	65	19
77	0.000000000	-.006599424	65	20
-65	0.00594		65	99
66	0.0	0.0	66	1
66		.00193272	66	2
77		-0.00096636	66	3
78		-0.00096636	66	4
66	0.000000000	.013198848	66	5
77	0.000000000	-.006599424	66	6
78	0.000000000	-.006599424	66	7
66	.052		66	16
62	-.052		66	17
-66	0.0594		66	99
67	0.0	0.0	67	1
67		.00212718	67	2
79		-0.00106359	67	3
78		-0.00106359	67	4
67	0.000000000	.014436240	67	5
78	0.000000000	-.00218120	67	6
79	0.000000000	-.007218120	67	7
67	.049		67	16
57	-.049		67	17
-67	0.06540		67	99
68	0.0	0.0	68	1
68		.00246876	68	2
80		-0.00123430	68	3
79		-0.00123430	68	4
68	0.000000000	.016807900	68	5
79	0.000000000	-.008403954	68	6
80	0.000000000	-.008403954	68	7
68	.040		68	16

61	-0.040		68	17
-68	0.00465		68	99
69	0.0		69	1
69	0.00201324		69	2
80	-0.00106662		69	3
81	-0.00106662		69	4
69	0.0000000000	.013714428	69	5
80	0.0000000000	-.006857214	69	6
81	0.0000000000	-.006857214	69	7
69	.050		69	16
53	-.050		69	17
-69	0.00571		69	99
70	0.0	0.0	70	1
70	0.004743742		70	2
81	0.002361871		70	3
82	0.002361871		70	4
70	0.0000000000	.032461540	70	5
81	0.0000000000	-.016240770	70	6
82	0.0000000000	-.016240770	70	7
-70	0.00242		70	99
71	0.0	0.0	71	1
71	0.005394776		71	2
82	0.002642388		71	3
81	0.002642388		71	4
71	0.0000000000	.035987444	71	5
82	0.0000000000	-.0179493742	71	6
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75		-.04871	72	4
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13	-0.027		72	6
24	-0.016		72	7
26	-0.339		72	8
29	-0.978		72	9
87	-0.008		72	10
72	1.350		72	16
62	-.174		72	17
63	-1.137		72	18
72	-.039		72	19
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73	0.0	0.0	73	1
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76	-.02117		73	3
91	-.01165		73	4
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73	0.00187		73	7
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71	1.297		73	16
51	-.141		73	17
59	-.261		73	18
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67	-.01422		75	7
63	0.00257982		75	8
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74	-.000045994		75	10
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73	0.02358		76	4
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76	-.000092		76	11
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-76	0.0	0.0	76	99
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77	0.00064424		77	3
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66	0.00096636		77	5
77	0.00064424		77	6
78	0.00032212		77	7
65	0.008599424		77	8
77	0.004399616		77	9
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77	0.000000000	0.004399616	77	12
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78	0.000000000	-.0064812080	78	12
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78	0.002406040		79	10
68	0.0064812080		79	11
79	-.005662036		79	12
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79		-0.00041146	80	4
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85		-0.001761592	85	3
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113		-0.00014	85	10
112		0.00522	85	11
85		-0.00348	85	12
113		-0.00174	85	13
85		-0.00187	85	14
73		0.00187	85	15
-85	0.0	0.0	85	99
86	0.0	0.0	86	1
85		0.002642388	86	2
86		-0.001761592	86	3
84		-0.000880794	86	4
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86	0.000000000	-0.00654424	86	6
77		-0.00032212	86	7
87	0.000000000	.017993742	86	8
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88	0.000000000	.005997914	86	10
65	0.000000000	.006599424	86	11
86	0.000000000	-0.004399616	86	12
77	0.000000000	.002199808	86	13
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88		-0.002642388	87	4
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72	-0.003		87	18
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91		-0.00376	91	4
76		-0.00376	91	5
91	-3.255		91	6
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99		99	1
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2	-0.10	99	5
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100	0.0	100	1
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110		110	1
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111		111	1
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-147	0.000000000	0.000000000	147	99
148	0.000000000	0.000000000	148	1
148	0.000000000	1.423482833	148	2
147	0.000000000	.2507676729	148	3
149	0.000000000	-.329458231	148	4
168	0.000000000	-.421491557	148	5
128	0.000000000	.421491557	148	6
-148	3.142544637	0.000000000	148	99
149	0.000000000	0.000000000	149	1
148	0.000000000	.349376166	149	2
149	0.000000000	.300082236	149	3
147	0.000000000	-.104590299	149	4
150	0.000000000	.231068853	149	5
151	0.000000000	.084872424	149	6
-149	0.000000000	0.000000000	149	99
150	0.000000000	0.000000000	150	1
150	0.000000000	2.507625746	150	2
149	0.000000000	.2507676729	150	3
151	0.000000000	-.329458231	150	4
170	0.000000000	.963590394	150	5
130	0.000000000	-.963590394	150	6
-150	7.184305110	0.000000000	150	99
151	0.000000000	0.000000000	151	1
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151	0.000000000	.300082236	151	3
149	0.000000000	-.104590299	151	4
152	0.000000000	.231068853	151	5
153	0.000000000	-.084872424	151	6
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152	0.000000000	0.000000000	152	1
152	0.000000000	4.986257753	152	2
151	0.000000000	.2507676729	152	3
153	0.000000000	-.329458231	152	4
172	0.000000000	.2.20296397	152	5
132	0.000000000	-.2.20296397	152	6
-152	16.24365167	0.000000000	152	99
153	0.000000000	.0.149470900	153	1
152	0.000000000	.349376166	153	2
151	0.000000000	-.104590299	153	3
153	0.000000000	.259732896	153	4
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0	0.000000000	3.363098037	153	7
35	0.000000000	3.363098037	153	8
0	72.000000000	3.363098035	153	9
108	0.000000000	3.363097454	153	10
144	0.000000000	3.363099494	153	11
180	0.000000000	3.363052264	153	12
216	0.000000000	3.362964044	153	13
252	0.000000000	3.362812249	153	14
288	0.000000000	3.362597273	153	15
324	0.000000000	3.362328042	153	16
0	361.000000000	3.362117186	153	17
0	361.000000000	3.363098037	153	18
0	2000.000000000	3.363098037	153	19
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162	0.000000000	0.000000000	162	1
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122	0.000000000	.011758534	162	3
162	0.000000000	-.047034537	162	4
182	0.000000000	.035275942	162	5
202	0.000000000	-.011758534	162	6
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163	0.000000000	0.000000000	163	1
141	0.000000000	.038999982	163	2
163	0.000000000	-.025999988	163	3
123	0.000000000	.012999994	163	4
181	0.000000000	.038999982	163	5
163	0.000000000	-.025999998	163	6
203	0.000000000	.012999994	163	7
-163	0.000000000	0.000000000	163	99
164	0.000000000	0.000000000	164	1
144	0.000000000	.08045793	164	2
124	0.000000000	.024804931	164	3
164	0.000000000	-.167527723	164	4
184	0.000000000	.080645793	164	5
204	0.000000000	-.026881931	164	6
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126	0.000000000	-.061455965	166	3
166	0.000000000	.245823860	166	4
186	0.000000000	.184367895	166	5
206	0.000000000	-.061455965	166	6
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168	0.000000000	.561988742	168	4
188	0.000000000	.421491557	168	5
208	0.000000000	-.140497186	168	6
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130	0.000000000	-.321196798	170	3
170	0.000000000	-.1.284787191	170	4
190	0.000000000	.963590394	170	5
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172	0.000000000	-.2.937208529	172	4
192	0.000000000	.2.20296397	172	5
212	0.000000000	-.734321232	172	6
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162	0.000000000	.231068853	181	2
181	0.000000000	.146196429	181	3
183	0.000000000	.084872424	181	4
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53	8.894530000	0.000000050	181	7
56	2687.30000	0.000000050	181	8
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203	0.000000000	.038999982	181	10
163	0.000000000	.038999982	181	11
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181	0.000000000	-.2.20296397	182	3
183	0.000000000	.329458231	182	4
202	0.000000000	-.035275942	182	5
182	0.000000000	-.035275942	182	6
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182	0,000000000	.349376146	183	2
183	0,000000000	-.390942236	183	3
181	0,000000000	-.104590299	183	4
184	0,000000000	.231048853	183	5
185	0,000000000	-.084872424	183	6
-183	0,000000000	0,000000000	183	99
184	0,000000000	0,000000000	184	1
184	0,000000000	.781736545	184	2
183	0,000000000	-.250786729	184	3
185	0,000000000	-.329458231	184	4
204	0,000000000	-.080645793	184	5
164	0,000000000	-.080645793	184	6
-184	0,000000000	.601276545	184	99
185	0,000000000	0,000000000	185	1
184	0,000000000	.349376146	185	2
185	0,000000000	-.390942236	185	3
183	0,000000000	-.104590299	185	4
186	0,000000000	.231048853	185	5
187	0,000000000	-.084872424	185	6
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186	0,000000000	0,000000000	186	1
186	0,000000000	.949180749	186	2
185	0,000000000	-.250786729	186	3
187	0,000000000	-.329458231	186	4
206	0,000000000	-.184367895	186	5
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187	0,000000000	0,000000000	187	1
186	0,000000000	.349376146	187	2
187	0,000000000	-.390942236	187	3
185	0,000000000	-.104590299	187	4
188	0,000000000	.231048853	187	5
189	0,000000000	-.084872424	187	6
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188	0,000000000	1,423428073	188	2
187	0,000000000	-.250786729	188	3
189	0,000000000	-.329458231	188	4
208	0,000000000	-.421491557	188	5
168	0,000000000	-.421491557	188	6
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189	0,000000000	0,000000000	189	1
188	0,000000000	.349376146	189	2
189	0,000000000	-.390942236	189	3
187	0,000000000	-.104590299	189	4
190	0,000000000	.231048853	189	5
191	0,000000000	-.084872424	189	6
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190	0,000000000	0,000000000	190	1
190	0,000000000	2,507625746	190	2
189	0,000000000	-.250786729	190	3
191	0,000000000	-.329458231	190	4
210	0,000000000	-.963490394	190	5
170	0,000000000	-.963490394	190	6
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191	0,000000000	0,000000000	191	1
190	0,000000000	.349376146	191	2
191	0,000000000	-.390942236	191	3
189	0,000000000	-.104590299	191	4
192	0,000000000	.231048853	191	5
193	0,000000000	-.084872424	191	6
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191	0,000000000	-.250786729	192	3
193	0,000000000	-.329458231	192	4
212	0,000000000	-2,20296397	192	5
172	0,000000000	-2,20296397	192	6
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193	0,000000000	.015849327	193	1
192	0,000000000	.349376146	193	2
191	0,000000000	-.104590299	193	3
193	0,000000000	-.250655113	193	4
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0	36,100000000	3,570615167	193	8
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0	108,300000000	3,570599255	193	10
0	144,200000000	3,570575898	193	11
0	180,500000000	3,570493865	193	12
0	216,500000000	3,570325141	193	13
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0	288,800000000	3,56972536	193	15
0	324,900000000	3,569326556	193	16
0	361,000000000	3,568889089	193	17
0	361,000000000	3,57061567	193	18
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182	0,000000000	.035275962	202	2
162	0,000000000	-.011758324	202	3
202	0,000000000	.047034537	202	4
222	0,000000000	.035275962	202	5
242	0,000000000	-.011758324	202	6
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203	0,000000000	0,000000000	203	1
181	0,000000000	.038999982	203	2
203	0,000000000	.029999998	203	3
163	0,000000000	-.038999982	203	4
221	0,000000000	.038999998	203	5
203	0,000000000	-.029999998	203	6
243	0,000000000	-.012999994	203	7
-203	0,000000000	0,000000000	203	99
204	0,000000000	0,000000000	204	1
184	0,000000000	.080645763	204	2
164	0,000000000	.026881931	204	3
204	0,000000000	.10792773	204	4
224	0,000000000	.006649793	204	5
244	0,000000000	-.026881931	204	6
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205	0,000000000	0,000000000	205	1
185	0,000000000	.184367895	205	2
165	0,000000000	.001455945	205	3
205	0,000000000	.249823080	205	4
225	0,000000000	.184367895	205	5
245	0,000000000	.001455945	205	6
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206	0,000000000	0,000000000	206	1
186	0,000000000	.184367895	206	2
166	0,000000000	.001455945	206	3
206	0,000000000	.249823080	206	4
226	0,000000000	.184367895	206	5
246	0,000000000	.001455945	206	6
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207	0,000000000	0,000000000	207	1
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167	0,000000000	.001455945	207	3
207	0,000000000	.249823080	207	4
227	0,000000000	.184367895	207	5
247	0,000000000	.001455945	207	6
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208	0,000000000	0,000000000	208	1
188	0,000000000	.184367895	208	2
168	0,000000000	.001455945	208	3
208	0,000000000	.249823080	208	4
228	0,000000000	.184367895	208	5
248	0,000000000	.001455945	208	6
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209	0,000000000	0,000000000	209	1
189	0,000000000	.953390394	209	2
170	0,000000000	.321196798	209	3
210	0,000000000	-.284787191	209	4
230	0,000000000	.963590394	209	5
250	0,000000000	.321196798	209	6
-210	0,000000000	0,000000000	209	99

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192	0.000000000	2.20296397	212	2
172	0.000000000	-734302132	212	3
212	0.000000000	-2.937208529	212	4
232	0.000000000	2.20296397	212	5
252	0.000000000	.734302132	212	6
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221	0.000000000	-.146196429	221	3
223	0.000000000	-.084872424	221	4
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56	2.897240000	0.000000000	221	6
56	2.687170000	0.000000000	221	7
57	.022970000	0.000000000	221	8
221	0.000000000	.077999965	221	9
243	0.000000000	.038999982	221	10
203	0.000000000	.038999982	221	11
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222	0.000000000	.650998744	222	2
221	0.000000000	-.250786729	222	3
223	0.000000000	.329658231	222	4
224	0.000000000	-.035275942	222	5
202	0.000000000	-.035275942	222	6
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223	0.000000000	.030000000	223	1
222	.34937616	0.000000000	223	2
223	.390982236	0.000000000	223	3
221	.104590299	0.000000000	223	4
224	.231068853	0.000000000	223	5
225	.084872424	0.000000000	223	6
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224	.741736545	0.000000000	224	2
223	.250786729	0.000000000	224	3
225	.329658231	0.000000000	224	4
244	.080645793	0.000000000	224	5
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225	.390982236	0.000000000	225	3
223	.104590299	0.000000000	225	4
226	.231068853	0.000000000	225	5
227	.084872424	0.000000000	225	6
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225	.250786729	0.000000000	226	3
227	.329658231	0.000000000	226	4
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206	.184367855	0.000000000	226	6
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226	.34937616	0.000000000	227	2
227	.390982236	0.000000000	227	3
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226	.231068853	0.000000000	227	5
227	.084872424	0.000000000	227	6
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227	.250786729	0.000000000	228	3
229	.329658231	0.000000000	228	4
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208	.421491567	0.000000000	228	6
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228	.34937616	0.000000000	229	2
229	.390982236	0.000000000	229	3
227	.104590299	0.000000000	229	4
230	.231068853	0.000000000	229	5
231	.064872424	0.000000000	229	6
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230	0.000000000	0.000000000	230	1
230	.2507625746	0.000000000	230	2
229	.329658231	0.000000000	230	3
231	.963590394	0.000000000	230	4
250	.963590394	0.000000000	230	5
210	.963590394	0.000000000	230	6
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231	0.000000000	0.000000000	231	1
230	.34937616	0.000000000	231	2
231	.390982236	0.000000000	231	3
229	.104590299	0.000000000	231	4
232	.231068853	0.000000000	231	5
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232	0.000000000	0.000000000	232	1
232	.986257753	0.000000000	232	2
231	.250786729	0.000000000	232	3
233	.329658231	0.000000000	232	4
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0	.377981519	0.000000000	233	8
0	.3779815088	0.000000000	233	9
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0	.3778694455	0.000000000	233	14
0	.3778399472	0.000000000	233	15
0	.3777449158	0.000000000	233	16
0	.3777271459	0.000000000	233	17
0	.3779815189	0.000000000	233	18
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222	0.000000000	.035275902	242	2
202	0.000000000	-.011758634	242	3
242	0.000000000	.047034537	242	4
252	0.000000000	.035275902	242	5
282	0.000000000	-.011758634	242	6
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243	0.000000000	0.000000000	243	1
221	0.000000000	.038999982	243	2
243	0.000000000	-.025999988	243	3
203	0.000000000	.012999994	243	4
251	0.000000000	.038999982	243	5
243	0.000000000	.025999988	243	6
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244	0.000000000	0.000000000	244	1
224	0.000000000	.080645793	244	2

204	0,000000000	.026881931	244	3
244	0,000000000	.107527723	244	4
264	0,000000000	.080645793	244	5
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246	0,000000000	.000000000	246	1
226	0,000000000	.184347895	246	2
206	0,000000000	.041455945	246	3
246	0,000000000	.245473860	246	4
266	0,000000000	.184347895	246	5
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248	0,000000000	.000000000	248	1
228	0,000000000	.421491557	248	2
208	0,000000000	.140497186	248	3
248	0,000000000	.561988742	248	4
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230	0,000000000	.963590394	250	2
210	0,000000000	.321196798	250	3
250	0,000000000	.1284787191	250	4
270	0,000000000	.963590394	250	5
290	0,000000000	.321196798	250	6
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252	0,000000000	.293720859	252	4
272	0,000000000	.20296397	252	5
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261	0,000000000	.146196429	261	3
263	0,000000000	.084872924	261	4
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57	5,993070000	.000000000	261	6
62	3,727566000	.000000000	261	7
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293	0,000000000	.038999992	261	9
243	0,000000000	.038999992	261	10
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262	0,000000000	.45099674	262	2
261	0,000000000	.250746729	262	3
263	0,000000000	.329458231	262	4
282	0,000000000	.035275952	262	5
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262	0,000000000	.349376106	263	2
263	0,000000000	.390982236	263	3
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631	0,000000000	,3,777271499	633	11
632	0,000000000	,3,777171499	633	12
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663	0,000000000	,329658231	662	4
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665	0,000000000	-,104590299	667	4
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669	0,000000000	-,084n72424	667	6
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0	2000,000000000	.892n25215	726	19
-726	0.000000000	0,000000000	726	99
728	0.000000000	.008713955	728	1
708	0.000000000	.421491557	728	2
688	0.000000000	-.140497186	728	3
728	0.000000000	-.289708324	728	4
0	2000,000000000	1.959653597	728	6
0	0.000000000	1.9606411585	728	7
0	36,100000000	1.9606411584	728	8
0	72,200000000	1.960439885	728	9
0	108,300000000	1.960586542	728	10
0	144,*0000000	1.960399700	728	11
0	180,500000000	1.960664437	728	12
0	216,600000000	1.959624717	728	13
0	252,700000000	1.95911334n2	728	14
0	288,800000000	1.958630944	728	15
0	324,900000000	1.958143161	728	16
0	361,000000000	1.9576848546	728	17
0	361,000000000	1.9606411585	728	18
0	2000,000000000	1.9606411585	728	19
-728	0.000000000	0,000000000	728	99
730	0.000000000	.018394058	730	1
710	0.000000000	.963590394	730	2
690	0.000000000	-.3211n6798	730	3
730	0.000000000	-.660787654	730	4
0	2000,000000000	4.137322934	730	6
0	0.000000000	4.138666674	730	7
0	36,100000000	4.138666674	730	8
0	72,200000000	4.138665615	730	9
0	108,300000000	4.138629464	730	10
0	144,*0000000	4.138450223	730	11
0	180,500000000	4.138n54518	730	12
0	216,600000000	4.137458384	730	13
0	252,700000000	4.1367226n6	730	14
0	288,800000000	4.135911373	730	15
0	324,900000000	4.135075714	730	16
0	361,000000000	4.134251032	730	17
0	361,000000000	4.138666674	730	18
0	2000,000000000	4.138666674	730	19
-730	0.000000000	0,000000000	730	99
732	0.000000000	.036366261	732	1
712	0.000000000	.2,029n6397	732	2
692	0.000000000	-.1,734302132	732	3
732	0.000000000	-.1,504970576	732	4
0	2000,000000000	8,1814n3274	732	6
0	0.000000000	8,182415798	732	7
0	36,100000000	8,182415798	732	8
0	72,200000000	8,182415798	732	9
0	108,300000000	8,182410353	732	10
0	144,*0000000	8,182355594	732	11
0	180,500000000	8,182144860	732	12
0	216,600000000	8,18177336n5	732	13

0	252.700000000	8,181171268	732	14
0	288.800000000	8,180386975	732	15
0	324.900000000	8,179467093	732	16
0	361.000000000	8,178488972	732	17
0	361.000000000	8,182415798	732	18
0	2000.000000000	8,182415798	732	19
-732	0.000000000	0,000000000	732	99
		-0	-0	
1.85	1.0E-02 30.0	1 10 90.0	225.0	732 1.0
1.85	1.0E-03 1.0	1 10 91.0		732 1.0
1.85	1.0E-02 30.0	1 10 361.0		732 1.0
0.00			-0 -0 A	-0

APPENDIX III

FINITE-DIFFERENCE EQUATIONS AND BOUNDARY CONDITIONS FOR THERMAL MODELS OF LUNAR MEDIUM

Figure 10 in the body of the report illustrates a typical annular element used in the finite-difference representation of the lunar medium. Shown in the figure are the coordinate system and the dimensions of the ring. According to the Method of Zones, a parabolic temperature distribution is assumed within each element. Expressions for the net heat flow from faces 1 through 4 are found in terms of the average surface temperatures, T_1 through T_4 and the mean temperature of the element, T_m :

$$Q_1 = \frac{2\pi k \ell a}{b - a} \left(6T_m - \frac{3b + 5a}{b + a} T_1 - \frac{3b + a}{b + a} T_2 \right) \quad (\text{III-1})$$

$$Q_2 = \frac{2\pi k \ell b}{b - a} \left(6T_m - \frac{5b + 3a}{b + a} T_2 - \frac{b + 3a}{b + a} T_1 \right) \quad (\text{III-2})$$

$$Q_3 = \frac{k\pi(b^2 - a^2)}{\ell} \left(6T_m - 4T_3 + 2T_4 \right) \quad (\text{III-3})$$

$$Q_4 = \frac{k\pi(b^2 - a^2)}{\ell} \left(6T_m - 4T_4 + 2T_3 \right) \quad (\text{III-4})$$

The mean temperature of each annular zone is described by:

$$Q_1 + Q_2 + Q_3 + Q_4 + \rho \pi (b^2 - a^2) \ell C \frac{dT_m}{dt} = 0 \quad (\text{III-5})$$

where ρ is the density and C is the specific heat of the lunar medium.

Thermal connection between the zones is made by way of the net heat flows at the zone surfaces. For example, the heat flow from the outer surface of an element (surface 2 in Figure 10) is equal to the negative of the heat flow from the inside surface (1) of the surrounding annular ring.

At the outer boundaries, the heat flow from the surfaces are matched with the form of solution predicted for a spherical surface heat source:

$$Q'' = \frac{k}{R^*} T(R^*, t) - \frac{k}{R^*} T_\infty + f(Q_o, R^*, t) \quad (\text{III-6})$$

where

Q'' - heat flux at boundary surface

R^* - distance from center of source

Q_o - strength of heat source

T_∞ - initial temperature of lunar medium

and

$$f(Q_o, R^*, t) = \frac{Q_o}{8\pi R_o R^*} \left[\operatorname{erfc}\left(\frac{R_o - R^*}{2\sqrt{\alpha t}}\right) - \operatorname{erfc}\left(\frac{R_o + R^*}{2\sqrt{\alpha t}}\right) \right] \quad (\text{III-7a})$$

$$\operatorname{erfc}(z) = 1 - \frac{2}{\sqrt{\pi}} \int_0^z e^{-x^2} dx \quad (\text{III-7b})$$

Applying these equations over a boundary surface of area A_b , the total heat flow at the boundary is expressed as:

$$Q_b = A_b k T_b / R^* + P_b(R^*, t) \quad (\text{III-8a})$$

where

$$P_b(R^*, t) = A_b f(Q_o, R^*, t) - A_b k T_\infty / R^* . \quad (\text{III-8b})$$

The quantity P_b represents a negative power applied to the boundary surface (See Appendix I). The value used for R^* corresponds to the radial distance from the center of the gradient sensor to the center position on the boundary surface.

APPENDIX IV

TABULATION OF PERFORMANCE PREDICTIONS IN THE LUNAR ENVIRONMENT

Table No.

<u>Table No.</u>	<u>Description</u>
IV-1	Predicted Performance for Mode 2 Operation in Lunar Environment, Experiment Location 2
IV-2	Predicted Performance for Mode 2 Operation in Lunar Environment, Experiment Location 4
IV-3	Predicted Performance for Mode 3 Operation in Lunar Environment
IV-4	Temperature Decay of Ring Sensor after Heating Period in Mode 3 Experiment
IV-5	Temperature Decay of Gradient Sensor after Heating Period of Mode 3 Experiment
IV-6	Predicted Performance for Mode 3 Parametric Studies
IV-7	Influence of Interface between Probe Alignment Springs and Drill Case
IV-8	Influence on Radiation Coupling between Drill Casing and the Moon

TABLE IV-1
PREDICTED PERFORMANCE FOR MODE 2
OPERATION IN LUNAR ENVIRONMENT,
EXPERIMENT LOCATION 2
 $(\rho c = 1.339 \text{ w-sec/cc } ^\circ\text{K})$
 $K = 2.1 \times 10^{-5} \text{ w/cm } ^\circ\text{K}$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor ($^\circ\text{K}$)		
	T = 205 $^\circ\text{K}$	T = 225 $^\circ\text{K}$	T = 245 $^\circ\text{K}$
0	0.000	0.000	0.000
15	0.084	0.079	0.076
30	0.151	0.142	0.134
45	0.204	0.191	0.179
60	0.247	0.229	0.214
91	0.311	0.286	0.266
121	0.357	0.327	0.303
151	0.394	0.360	0.332
181	0.423	0.386	0.357
241	0.468	0.426	0.393
301	0.502	0.457	0.420
361	0.529	0.481	0.443
421	0.552	0.502	0.461
481	0.572	0.519	0.477
541	0.588	0.534	0.490
601	0.603	0.547	0.502
722	0.627	0.568	0.520
842	0.646	0.586	0.535
962	0.663	0.600	0.548
1082	0.677	0.612	0.558
1202	0.689	0.623	0.567

TABLE IV-1 - Cont'd.

$$K = 7.3 \times 10^{-5} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor ($^\circ\text{K}$)		
	T = 205°K	T = 225°K	T = 245°K
0	0.000	0.000	0.000
15	0.082	0.077	0.073
30	0.146	0.136	0.126
45	0.195	0.179	0.165
60	0.233	0.212	0.194
91	0.285	0.257	0.233
121	0.321	0.287	0.259
151	0.347	0.309	0.279
181	0.367	0.327	0.295
241	0.396	0.351	0.317
301	0.416	0.370	0.334
361	0.432	0.385	0.348
421	0.446	0.397	0.359
481	0.457	0.407	0.369
541	0.466	0.416	0.377
601	0.474	0.423	0.384
722	0.488	0.436	0.396
842	0.500	0.447	0.406
962	0.509	0.456	0.414
1082	0.517	0.463	0.421
1202	0.525	0.470	0.427

TABLE IV-1 - Cont'd.

$$K = 1.5 \times 10^{-4} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature $T = 205^\circ\text{K}$	Rise of Gradient Sensor $(^\circ\text{K})$ $T = 225^\circ\text{K}$	$T = 245^\circ\text{K}$
0	0.000	0.000	0.000
15	0.081	0.076	0.071
30	0.144	0.133	0.122
45	0.190	0.173	0.158
60	0.226	0.203	0.184
91	0.273	0.242	0.216
121	0.303	0.267	0.237
151	0.325	0.284	0.252
181	0.340	0.297	0.264
241	0.361	0.315	0.280
301	0.376	0.328	0.292
361	0.387	0.338	0.301
421	0.395	0.346	0.308
481	0.403	0.353	0.315
541	0.409	0.358	0.320
601	0.414	0.364	0.325
722	0.423	0.373	0.333
842	0.430	0.379	0.340
962	0.436	0.385	0.345
1082	0.441	0.389	0.350
1202	0.446	0.393	0.354

TABLE IV-1 - Cont'd.

$$K = 4.2 \times 10^{-4} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor		
	T = 205°K	T = 225°K	T = 245°K
0	0.000	0.000	0.000
15	0.080	0.075	0.069
30	0.141	0.129	0.117
45	0.185	0.166	0.149
60	0.217	0.192	0.171
91	0.258	0.224	0.196
121	0.282	0.242	0.210
51	0.298	0.254	0.219
181	0.308	0.262	0.226
241	0.321	0.272	0.235
301	0.329	0.278	0.241
361	0.335	0.283	0.245
421	0.339	0.287	0.249
481	0.342	0.290	0.252
541	0.345	0.293	0.254
601	0.347	0.295	0.256
722	0.350	0.298	0.259
842	0.353	0.301	0.261
962	0.355	0.303	0.263
1082	0.357	0.304	0.265
1202	0.358	0.305	0.266

TABLE IV-2

PREDICTED PERFORMANCE FOR MODE 2OPERATION IN LUNAR ENVIRONMENT,EXPERIMENT LOCATION 4

(ρc = 1.339 w-sec/cc °K)

$$K = 2.1 \times 10^{-5} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor T = 205 °K	T = 225 °K	T = 245 °K
0	0.000	0.000	0.000
15	0.090	0.085	0.081
30	0.163	0.153	0.144
45	0.176	0.206	0.193
60	0.268	0.248	0.232
91	0.339	0.312	0.290
121	0.392	0.360	0.333
151	0.435	0.398	0.368
181	0.470	0.430	0.398
241	0.524	0.480	0.446
301	0.568	0.521	0.484
361	0.605	0.556	0.517
421	0.636	0.586	0.546
481	0.664	0.612	0.571
541	0.688	0.636	0.593
601	0.711	0.657	0.613
722	0.749	0.694	0.648
842	0.781	0.725	0.678
962	0.810	0.753	0.704
1082	-	0.777	0.727
1202	-	-	-

TABLE IV-2 - Cont'd.

$$K = 1.5 \times 10^{-4} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor ($^\circ\text{K}$)		
	T = 205 $^\circ\text{K}$	T = 225 $^\circ\text{K}$	T = 245 $^\circ\text{K}$
0	0.000	0.000	0.000
15	0.087	0.082	0.076
30	0.155	0.143	0.132
45	0.206	0.187	0.170
60	0.245	0.219	0.198
91	0.297	0.262	0.234
121	0.330	0.289	0.256
151	0.354	0.308	0.273
181	0.372	0.323	0.286
241	0.395	0.343	0.303
301	0.412	0.357	0.317
361	0.425	0.369	0.328
421	0.435	0.378	0.337
481	0.443	0.386	0.344
541	0.450	0.393	0.351
601	0.457	0.399	0.357
722	0.467	0.410	0.367
842	0.476	0.418	0.375
962	0.483	0.425	0.382
1082	0.490	0.431	0.389
1202	0.495	0.437	0.394

TABLE IV-2 - Cont'd.

$$K = 7.3 \times 10^{-5} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor ($^\circ\text{K}$)		
	T = 205 $^\circ\text{K}$	T = 225 $^\circ\text{K}$	T = 245 $^\circ\text{K}$
0	0.000	0.000	0.000
15	0.088	0.083	0.078
30	0.158	0.146	0.136
45	0.211	0.193	0.178
60	0.252	0.229	0.209
91	0.310	0.278	0.252
121	0.350	0.312	0.281
151	0.379	0.337	0.303
181	0.402	0.357	0.321
241	0.435	0.385	0.347
301	0.459	0.408	0.368
361	0.478	0.425	0.385
421	0.494	0.440	0.399
481	0.508	0.453	0.412
541	0.520	0.465	0.423
601	0.531	0.475	0.433
722	0.549	0.493	0.449
842	0.564	0.507	0.463
962	0.576	0.520	0.476
1082	0.588	0.531	0.486
1202	0.598	0.541	0.496

TABLE IV-2 - Cont'd.

$$K = 4.2 \times 10^{-4} \text{ w/cm } ^\circ\text{K}$$

Time after Start of Heating (min)	Temperature Rise of Gradient Sensor ($^\circ\text{K}$)		
	T = 205 $^\circ\text{K}$	T = 225 $^\circ\text{K}$	T = 245 $^\circ\text{K}$
0	0.000	0.000	0.000
15	0.086	0.080	0.074
30	0.152	0.139	0.126
45	0.200	0.179	0.161
60	0.235	0.208	0.184
91	0.280	0.242	0.211
121	0.307	0.262	0.227
151	0.325	0.275	0.237
181	0.337	0.284	0.244
241	0.351	0.295	0.253
301	0.360	0.302	0.260
361	0.366	0.308	0.265
421	0.371	0.312	0.269
481	0.374	0.315	0.272
541	0.377	0.318	0.274
601	0.380	0.321	0.277
722	0.384	0.324	0.281
842	0.387	0.327	0.283
962	0.389	0.329	0.286
1082	0.391	0.331	0.288
1202	0.393	0.333	0.289

TABLE IV-3

PREDICTED PERFORMANCE FOR
MODE 3 OPERATION IN LUNAR ENVIRONMENT

MODE 3
 LOCATION 2
 $K = 0.0001500 \text{ W}/\text{CM-DEG K}$
 $RHO*C = 1.3390 \text{ W-SEC}/\text{CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K
 DURATION = 361.0 MIN.

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.004531
30.000	0.255900	0.012528
60.000	0.751700	0.018571
90.000	1.370200	0.021483
120.000	2.040700	0.021346
151.000	2.670300	0.020008
181.000	3.261800	0.019023
211.000	3.811700	0.017673
241.000	4.322200	0.016426
271.000	4.797300	0.015316
301.000	5.241200	0.014338
331.000	5.657600	0.013478
361.000	6.049900	0.012674

MODE 3
 LOCATION 2
 $K = 0.0010000 \text{ W}/\text{CM-DEG K}$
 $RHO*C = 1.3390 \text{ W-SEC}/\text{CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K
 DURATION = 361.0 MIN.

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001848
30.000	0.089100	0.004091
60.000	0.245500	0.005508
90.000	0.419600	0.005617
121.000	0.587800	0.005077
151.000	0.730000	0.004431
181.000	0.853700	0.003880
211.000	0.962800	0.003454
241.000	1.061000	0.003134
271.000	1.150900	0.002888
301.000	1.234300	0.002691
331.000	1.312400	0.002523
361.000	1.385700	0.002363

TABLE IV-3 - Cont'd.

MODE 3
 LOCATION 2
 $K = 0.0006000 \text{ W/CM-DEG K}$
 $\text{RHO*C} = 1.3390 \text{ W-SEC/CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K
 DURATION = 361.0 MIN.

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.002165
30.000	0.108900	0.005094
60.000	0.305700	0.007051
90.000	0.532000	0.007420
121.000	0.758100	0.006925
151.000	0.955200	0.006208
181.000	1.130600	0.005541
211.000	1.287700	0.004998
241.000	1.430500	0.004571
271.000	1.562000	0.004233
301.000	1.684500	0.003960
331.000	1.799600	0.003729
361.000	1.908300	0.003516

MODE 3
 LOCATION 2
 $K = 0.0017000 \text{ W/CM-DEG K}$
 $\text{RHO*C} = 1.3390 \text{ W-SEC/CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K
 DURATION = 361.0 MIN.

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001656
30.000	0.077600	0.003516
60.000	0.211000	0.004633
90.000	0.355600	0.004600
121.000	0.491200	0.004034
151.000	0.602400	0.003416
181.000	0.696200	0.002908
211.000	0.776900	0.002526
241.000	0.847800	0.002241
271.000	0.911400	0.002023
301.000	0.969200	0.001846
331.000	1.022200	0.001699
361.000	1.071200	0.001566

TABLE IV-3 - Cont'd.

MODE 3
 LOCATION 2
 $K = 0.0054000 \text{ W}/\text{CM-DEG K}$
 $\text{RHO*C} = 1.3390 \text{ W-SEC/CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K
 DURATION = 361.0 MIN.

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001533
30.000	0.068400	0.003026
60.000	0.181600	0.003814
90.000	0.297300	0.003540
121.000	0.396900	0.002815
151.000	0.469800	0.002118
181.000	0.524000	0.001581
211.000	0.564700	0.001206
241.000	0.596400	0.000953
271.000	0.621900	0.000775
301.000	0.642900	0.000646
331.000	0.660700	0.000551
361.000	0.676000	0.000468

TABLE IV-4

TEMPERATURE DECAY OF RING SENSOR AFTER
HEATING PERIOD OF MODE 3 EXPERIMENT

Experiment Location 2
 $\rho c = 1.339 \text{ w-sec/cc } ^\circ\text{K}$
 $T = 225^\circ\text{K}$

Time after Start of Heating (min)	Time after Heater Turn-Off (min)	Thermal Conductivity of Lunar Material (w/cm $^\circ\text{K}$)				
		5.4×10^{-3}	1.7×10^{-3}	1.0×10^{-3}	6.0×10^{-4}	1.5×10^{-4}
361	0	0.676*	1.071	1.386	1.908	(6.050) ⁺
421	60	0.551	0.971	1.291	1.811	(5.931)
481	120	0.405	0.819	1.125	1.607	(5.427)
541	180	0.298	0.692	0.978	1.417	(4.874)
601	24	0.229	0.598	0.866	1.266	(4.383)
721	360	0.161	0.483	0.721	1.065	(3.669)
841	480	0.120	0.406	0.617	0.921	(3.145)
961	600	0.092	0.350	0.539	0.811	-
1081	1720	0.071	0.308	0.477	0.723	-
1201	840	0.056	0.275	0.429	0.652	-
1321	960	0.043	0.248	0.389	-	-
1441	1080	0.034	0.225	0.357	-	-

* All values shown are temperatures in deg. K above an initial equilibrium value of 225°K.
⁺ Temperatures in parentheses are outside of the ring-bridge sensitivity range.

TABLE IV-5

TEMPERATURE DECAY OF GRADIENT SENSOR AFTER
HEATING PERIOD OF MODE 3 EXPERIMENT

Experiment Location 2
 $\rho c = 1.339 \text{ w-sec/cc } ^\circ\text{K}$
 $T = 225^\circ\text{K}$

Time after Start of Heating (min)	Heater Turn-Off (min)	Thermal Conductivity of Lunar Material (w/cm $^\circ\text{K}$)				
		5.4×10^{-3}	1.7×10^{-3}	1.0×10^{-3}	6.0×10^{-4}	1.5×10^{-4}
361	0	(43.633) ⁺	(46.702)	(49.160)	(55.324)	(65.271)
421	60	14.140 [*]	16.798	19.029	(21.945)	(33.896)
481	120	4.848	6.878	8.686	11.1105	(21.279)
541	180	1.839	3.339	4.762	6.727	15.255
601	240	0.813	1.933	3.059	4.664	11.882
721	360	0.343	1.073	1.853	3.020	8.586
841	480	0.209	0.736	1.306	2.199	6.685
961	600	0.154	0.569	1.005	1.715	-
1081	720	0.120	0.471	0.817	1.398	-
1201	840	0.096	0.406	0.690	1.175	-
1321	960	0.078	0.358	0.600	-	-
1441	1080	0.063	0.321	0.534	-	-

^{*}All values shown are temperatures in deg. K above an initial equilibrium value of 225°K.

⁺Temperatures in parentheses are outside of the range of the low-sensitivity gradient-bridge measurement ($\pm 20^\circ\text{K}$).

TABLE IV-6
PREDICTED PERFORMANCE FOR MODE 3 PARAMETRIC STUDIES

NOMINAL CASE

MODE 3
 LOCATION 2
 $K = 0.0017000 \text{ W}/\text{CM-DEG K}$
 $\text{RHO*C} = 1.3390 \text{ W-SEC/CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K
 DURATION = 361.0 MIN.

TIME(MIN)	<u>RING SENSOR RESPONSE</u>	
	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001656
30.000	0.077600	0.003516
60.000	0.211000	0.004633
90.000	0.355600	0.004600
121.000	0.491200	0.004034
151.000	0.602400	0.003416
181.000	0.696200	0.002908
211.000	0.776900	0.002526
241.000	0.847800	0.002241
271.000	0.911400	0.002023
301.000	0.969200	0.001846
331.000	1.022200	0.001699
361.000	1.071200	0.001566

Change: 20% increase in thermal mass of lunar material (RHO*C)

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001606
30.000	0.074100	0.003333
60.000	0.200000	0.004346
90.000	0.334900	0.004266
121.000	0.459800	0.003694
151.000	0.560900	0.003100
181.000	0.645800	0.002631
211.000	0.718800	0.002289
241.000	0.783200	0.002043
271.000	0.841400	0.001858
301.000	0.894700	0.001711
331.000	0.944100	0.001591
361.000	0.990200	0.001481

TABLE IV-6 - Cont'd.

Change: 20°K decrease in temperature level

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.002008
30.000	0.099700	0.004638
60.000	0.278300	0.006264
90.000	0.475600	0.006262
121.000	0.659700	0.005400
151.000	0.806100	0.004404
181.000	0.924000	0.003568
211.000	1.020200	0.002944
241.000	1.100700	0.002496
271.000	1.170000	0.002178
301.000	1.231400	0.001941
331.000	1.286500	0.001758
361.000	1.336900	0.001601

Change: 20°K increase in temperature level

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001421
30.000	0.063900	0.002838
60.000	0.170300	0.003684
90.000	0.285000	0.003683
121.000	0.394700	0.003320
151.000	0.488000	0.002926
181.000	0.570300	0.002598
211.000	0.643900	0.002338
241.000	0.710600	0.002128
271.000	0.771600	0.001951
301.000	0.827700	0.001803
331.000	0.879800	0.001674
361.000	0.928200	0.001551

Change: 20% increase in thermal conductance of drill casing

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001701
30.000	0.079700	0.003611
60.000	0.216700	0.004763
90.000	0.365500	0.004736
121.000	0.505200	0.004155
151.000	0.619700	0.003519
181.000	0.716400	0.002991
211.000	0.799200	0.002590
241.000	0.871800	0.002293
271.000	0.936800	0.002063
301.000	0.995600	0.001878
331.000	1.049500	0.001726
361.000	1.099200	0.001586

TABLE IV-6 - Cont'd.

Change: Experiment Location 1

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001478
30.000	0.071900	0.003314
60.000	0.198900	0.004473
90.000	0.340300	0.004544
121.000	0.475800	0.004048
151.000	0.587900	0.003448
181.000	0.682700	0.002933
211.000	0.763900	0.002524
241.000	0.834200	0.002216
271.000	0.896900	0.001990
301.000	0.953600	0.001808
331.000	1.005400	0.001628
361.000	1.051300	0.001431

Change: Experiment Location 3

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001236
30.000	0.060500	0.002796
60.000	0.167800	0.003813
90.000	0.289300	0.003949
121.000	0.408500	0.003617
151.000	0.510400	0.003176
181.000	0.599100	0.002774
211.000	0.676900	0.002449
241.000	0.746100	0.002193
271.000	0.808500	0.001990
301.000	0.865500	0.001823
331.000	0.917900	0.001681
361.000	0.966400	0.001551

Change: Experiment Location 4

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.001360
30.000	0.064100	0.002913
60.000	0.174800	0.003874
90.000	0.296600	0.003924
121.000	0.413900	0.003543
151.000	0.513200	0.003099
181.000	0.599900	0.002720
211.000	0.676400	0.002421
241.000	0.745200	0.002188
271.000	0.807700	0.001998
301.000	0.865100	0.001841
331.000	0.918200	0.001705
361.000	0.967400	0.001575

TABLE IV-7
INFLUENCE OF INTERFACE BETWEEN PROBE ALIGNMENT SPRINGS AND
DRILL CASE (SEE Text, Section V.F.2.a.)

MODE 2 EXPERIMENT WITH WELL-COUPLED INTERFACE
BETWEEN SPRINGS AND DRILL CASING

LOCATION 4
 $K = 0.0004200 \text{ W}/\text{CM-DEG K}$
 $\rho \cdot C = 1.3390 \text{ W-SEC}/\text{CC-DEG K}$
 TEMP LEVEL = 225.0 DEG K

TIME(MIN)	TEMP(DEG K)	GRADIENT SENSOR	
			SLOPE(DEG K/MIN)
0.000	0.000000		0.004166
15.000	0.052000		0.002766
30.000	0.083000		0.001633
45.000	0.101000		0.001033
60.000	0.114000		0.000741
91.000	0.129000		0.000390
121.000	0.138000		0.000266
151.000	0.145000		0.000216
181.000	0.151000		0.000177
241.000	0.159000		0.000116
301.000	0.165000		0.000083
361.000	0.169000		0.000066
421.000	0.173000		0.000058
481.000	0.176000		0.000050
541.000	0.179000		0.000041
601.000	0.181000		0.000033
722.000	0.185000		0.000029
842.000	0.188000		0.000020
962.000	0.190000		0.000016
1082.000	0.192000		0.000012
1202.000	0.193000		0.000004

TABLE IV-7 - Cont'd.

MODE 3 EXPERIMENT WITH WELL-COUPLED INTERFACE
BETWEEN SPRINGS AND CASING

LOCATION 2
K = 0.0017000 W/CM-DEG K
RHO*C = 1.3390 W-SEC/CC-DEG K
TEMP LEVEL = 225.0 DEG K

RING SENSOR

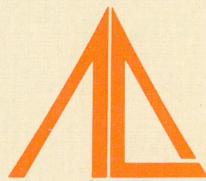
TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.000908
30.000	0.042800	0.001944
60.000	0.116700	0.002619
90.000	0.200000	0.002750
121.000	0.284400	0.002624
151.000	0.360300	0.002431
181.000	0.430300	0.002253
211.000	0.495500	0.002094
241.000	0.556000	0.001943
271.000	0.612100	0.001809
301.000	0.664600	0.001693
331.000	0.713700	0.001586
361.000	0.759800	0.001486

TABLE IV-8
INFLUENCE ON RADIATION COUPLING BETWEEN
DRILL CASING AND THE MOON
(SEE Text, Section IV.F.2.b)

MODE 3 EXPERIMENT WITH RADIATION COUPLING
BETWEEN CASING AND MOON

MODE 3
LOCATION 2
K = 0.0054000 W/CM-DEG K
RHO*C = 1.3390 W-SEC/CC-DEG K
TEMP LEVEL = 225.0 DEG K

TIME(MIN)	TEMP(DEG K)	SLOPE(DEG K/MIN)
0.000	0.000000	0.009794
30.000	0.422800	0.018391
60.000	1.103500	0.022531
90.000	1.774700	0.020084
121.000	2.324000	0.014990
151.000	2.694500	0.010265
181.000	2.939900	0.006731
211.000	3.098400	0.004341
241.000	3.200400	0.002813
271.000	3.267200	0.001866
301.000	3.312400	0.001286
331.000	3.344400	0.000929
361.000	3.368200	0.000656



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