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Development and Physicochemical Characterization of Acetalated Dextran Aerosol Particle Systems for Deep Lung Delivery

Zimeng Wang
University of Rhode Island

Sweta K. Gupta
University of Rhode Island

See next page for additional authors

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Authors

Zimeng Wang, Sweta K. Gupta, and Samantha A. Meenach

1 **Development and Physicochemical Characterization of Acetalated Dextran Aerosol**
2 **Particle Systems for Deep Lung Delivery**

3
4 Zimeng Wang¹, Sweta K. Gupta¹, Samantha A. Meenach^{1,2}
5
6
7

8 ¹University of Rhode Island, College of Engineering, Department of Chemical
9 Engineering, Kingston, RI 02881, USA

10
11 ²University of Rhode Island, College of Pharmacy, Department of Biomedical and
12 Pharmaceutical Sciences, Kingston, RI 02881, USA
13

14
15
16
17 **Corresponding Author:** Samantha A. Meenach, University of Rhode Island, 205
18 Crawford Hall, 16 Greenhouse Road, Kingston, RI, 02881, USA. Email:
19 smeenach@uri.edu
20
21

33 **ABSTRACT**

34 Biocompatible, biodegradable polymers are commonly used as excipients to
35 improve the drug delivery properties of aerosol formulations, in which acetalated dextran
36 (Ac-Dex) exhibits promising potential as a polymer in various therapeutic applications.
37 Despite this promise, there is no comprehensive study on the use of Ac-Dex as an
38 excipient for dry powder aerosol formulations. In this study, we developed and
39 characterized pulmonary drug delivery aerosol microparticle systems based on spray-
40 dried Ac-Dex with capabilities of (1) delivering therapeutics to the deep lung, (2)
41 targeting the particles to a desired location within the lungs, and (3) releasing the
42 therapeutics in a controlled fashion. Two types of Ac-Dex, with either rapid or slow
43 degradation rates, were synthesized. Nanocomposite microparticle (nCmP) and
44 microparticle (MP) systems were successfully formulated using both kinds of Ac-Dex as
45 excipients and curcumin as a model drug. The resulting MP were collapsed spheres
46 approximately 1 μm in diameter, while the nCmP were similar in size with wrinkled
47 surfaces, and these systems dissociated into 200 nm nanoparticles upon reconstitution in
48 water. The drug release rates of the Ac-Dex particles were tuned by modifying the
49 particle size and ratio of fast to slow degrading Ac-Dex. The pH of the environment was
50 also a significant factor that influenced the drug release rate. All nCmP and MP systems
51 exhibited desirable aerodynamic diameters that are suitable for deep lung delivery (e.g.
52 below 5 μm). Overall, the engineered Ac-Dex aerosol particle systems have the potential
53 to provide targeted and effective delivery of therapeutics into the deep lung.

54

55 **KEYWORDS:** Acetalated dextran, nanocomposite microparticles, microparticles,
56 pulmonary delivery, spray drying, controlled release

57

58 **1. INTRODUCTION**

59 Pulmonary drug delivery has exhibited promising potential in the treatment of
60 lung diseases, as it allows for the delivery of a wide range of therapeutics directly and
61 efficiently to the lungs, thereby increasing local drug concentration, reducing systemic
62 side effects, providing a rapid onset of pharmaceutical action, and avoiding the first-pass
63 metabolism associated with the liver (Belotti et al., 2015; Cui et al., 2011; Mansour et al.,
64 2009; Meenach et al., 2012). The deep lung (alveolar) region can be utilized as a route
65 for systematic drug delivery due to the enormous surface area available and nearby
66 plentiful capillary vessels that facilitate drug absorption, the very thin (approximately 0.1
67 μm) liquid layer over the alveoli that ensures rapid and unhindered drug absorption, and
68 low enzymatic activity, which enhances drug availability (Collier et al., 2016; Cui et al.,
69 2011; Hoang et al., 2014). As a result, various therapeutics such as antibiotics, proteins,
70 peptides, anti-cancer drugs (Wu et al., 2014), plasmid DNA (Takashima et al., 2007),
71 siRNA (Jensen et al., 2010), and anti-tuberculosis (TB) drugs have been employed in
72 inhalation formulations for the treatment of pulmonary diseases such as asthma, chronic
73 obstructive pulmonary disease (COPD), cystic fibrosis (CF)-related pulmonary
74 infections, and lung cancer (Meenach et al., 2013a; Wu et al., 2014).

75 Dry powders are a dosage formulation that delivers therapeutics to the lung, in the
76 form of particles, using a dry powder inhaler (Wu et al., 2014). Compared with liquid
77 aerosols, these formulations offer additional benefits such as enhanced stability of the

78 formulation, controllable particle size for targeting different regions of the lung, and
79 increased drug loading of hydrophobic payloads (Cohen et al., 2010; Meenach et al.,
80 2013a). Spray drying has proven to be a suitable technology in the preparation of dry
81 powder therapeutics (Meenach et al., 2013a), as it is capable of producing respirable
82 microparticles for deep lung delivery with acceptable aerosol dispersion properties
83 (Belotti et al., 2015). Properties of dry powder particles such as particle size, particle
84 shape, and surface morphology can be modified by controlling the spray drying
85 production process, thus providing desirable particle characteristics (Belotti et al., 2015;
86 Wu et al., 2014).

87 Biocompatible, biodegradable polymers such as poly(ϵ -caprolactone) (PCL) and
88 poly(lactic-co-glycolic acid) (PLGA) have been used as dry powder formulation
89 excipients to carry drug molecules, protect drugs from degradation, and impart sustained
90 release to aerosol formulations (Mansour et al., 2009). However, PLGA and PCL
91 delivery systems show significant burst release of their payloads due to bulk erosion of
92 the polymers and it is difficult to control the polymer degradation rate and modulate their
93 release profiles (Ulery et al., 2011). Acetalated dextran (Ac-Dex) is an acid-sensitive,
94 biodegradable, biocompatible polymer prepared via a one-step reaction by reversibly
95 modifying dextran with acetal groups. This modification reverses the solubility properties
96 of dextran from hydrophilic to hydrophobic, making it possible to form polymeric
97 particles using standard emulsion or nanoprecipitation techniques. In contrast to other
98 commonly used polymers such as PLGA, polylactic acid, and PCL, Ac-Dex exhibits
99 attractive properties suitable for the controlled release of therapeutic payloads. By
100 controlling the reaction time during the formation of Ac-Dex, the ratio of cyclic acetal

101 groups (with a slower degradation rate) to acyclic acetal groups (with a faster degradation
102 rate) can be adjusted. As a result, the degradation rate of the resulting Ac-Dex can be
103 tuned from hours to months to suit various applications. Moreover, the acid-sensitivity of
104 Ac-Dex enables it to degrade faster in lower pH environments, such as lysosomes in
105 macrophage or tumor cells, allowing for controlled release of drug within these cells.
106 Furthermore, Ac-Dex degrades into neutral by-products, which avoids undesirable
107 changes in the micro-environmental pH in the body. Finally, Ac-Dex offers the potential
108 of targeted delivery, due to the presence of dextran chains that can be further modified
109 with a variety of functional targeting moieties (Bachelder et al., 2008; Broaders et al.,
110 2009; Kauffman et al., 2012).

111 Owing to the aforementioned advantages, Ac-Dex has been widely applied in the
112 formation of polymeric carriers for drug delivery. Porous Ac-Dex microparticles loaded
113 with the chemotherapeutic camptothecin were developed for pulmonary delivery using
114 emulsion techniques. These systems exhibited a respirable fraction of 37% and
115 experimental mass mean aerodynamic diameters from 5.3 - 11.9 μm (Meenach et al.,
116 2012). Ac-Dex nanoparticle systems have been investigated in the application of protein
117 delivery for immunotherapy (Broaders et al., 2009), gene delivery to phagocytic and non-
118 phagocytic cells (Cohen et al., 2010), tandem delivery of peptide and chemotherapeutic
119 for controlled combination chemotherapy (Cui et al., 2011), delivery of the host-mediated
120 compound AR-12 (Arno Therapeutics; formerly known as OSU-03012) for the treatment
121 of *Leishmania donovani* (Collier et al., 2016), and the control of *Salmonella* infections
122 (Collier et al., 2016). Both Ac-Dex nanoparticles and microparticles loaded with

123 horseradish peroxidase have been evaluated to improve vaccine stability outside cold
124 chain conditions (Kanthamneni et al., 2012).

125 Despite this work, there is no comprehensive study on using Ac-Dex as an
126 excipient for dry powder aerosol formulations produced via spray drying. In this study,
127 we aimed to develop and characterize dry powder pulmonary delivery systems based on
128 spray-dried Ac-Dex particles with capabilities of (a) delivering therapeutics to the deep
129 lung, (b) targeting the particles to a particular location within the lungs, and (c) releasing
130 therapeutics at a controlled rate. Previous studies have shown that: (a) aerodynamic
131 diameter (d_a) determines the region of the lungs where particles will deposit, where
132 particles with an d_a of 1 - 5 μm tend to deposit in the deep lung region (Meenach et al.,
133 2013a); (b) geometric size plays an important role in the cellular uptake of particles,
134 where nanoscale particles (approximately 150 nm) tend to escape phagocytic uptake (He
135 et al., 2010), while particles larger than 1 μm will suffer from macrophage clearance in
136 the alveoli (Kho et al., 2010); and (c) the drug release rate of Ac-Dex particles can be
137 tuned by modifying the synthesis time of the Ac-Dex polymer (Kauffman et al., 2012;
138 Meenach et al., 2012).

139 To prepare the engineered particle systems, two types of Ac-Dex with rapid or
140 slow degradation rates were synthesized. Nanocomposite microparticle (nCmP) and
141 microparticle (MP) systems were formulated using both kinds of Ac-Dex as the
142 excipient. Curcumin was used as model drug owing to its high hydrophobicity (similar to
143 many other pulmonary therapeutics) and fluorescence (allowing for easy detection). The
144 nCmP were prepared by spray drying an aqueous suspension of CUR-loaded Ac-Dex
145 nanoparticles (NP, 200 nm) and the solid MP were formulated by spray drying a solution

146 of Ac-Dex and CUR in a solution of tetrahydrofuran (THF) and acetone. We hypothesize
147 that upon pulmonary administration, the nCmP will deposit in the deep lung, decompose
148 into free NP, and facilitate the sustained release of drug to the targeted site, while the MP
149 will remain the original size after deposition in the deep lung region. A schematic of the
150 described particle preparation and design is shown in **Figure 1**. Overall, the goal of the
151 described research was the initial development and physicochemical characterization of
152 dry powder Ac-Dex aerosol particle systems with the potential for effective delivery of
153 therapeutics.

154

155 **2. MATERIALS AND METHODS**

156

157 **2.1 Materials**

158 Dextran from *Leuconostoc mesenteroides* (9000-11000 MW), pyridinium p-
159 toluenesulfonate (PPTS, 98%), 2-methoxypropene (2-MOP, 97%), triethylamine (TEA, \geq
160 99%), anhydrous dimethyl sulfoxide (DMSO, \geq 99.9%), poly(vinyl alcohol) (PVA, MW
161 13,000-23,000, 87-89% hydrolyzed), dichloromethane (DCM, anhydrous, \geq 99.8%),
162 deuterium chloride (DCl, 35 weight % in D₂O, 99 atom % D), Tween[®] 80, curcumin,
163 sodium acetate (\geq 99%), acetic acid solution (1.0 N), acetone (\geq 99.8%), tetrahydrofuran
164 (THF, \geq 99%), and methanol (anhydrous, \geq 99.9%) were obtained from Sigma–Aldrich
165 (St. Louis, MO). Deuterium oxide (D₂O, 99.8% atom D) was obtained from Acros
166 Organics (Geel, Belgium). Phosphate buffered saline (PBS) was obtained from Fisher
167 Scientific (Somerville, NJ). Hydranal[®] KF reagent was obtained from Fluka Analytical.

168

169 **2.2 Synthesis and NMR Analysis of Acetalated Dextran (Ac-Dex)**

170 Ac-Dex was synthesized as described previously (Bachelder et al., 2008) with
171 minor modifications. 1 g of lyophilized dextran and 25 mg of PPTS were dissolved in 10
172 mL of anhydrous DMSO. The resulting solution was reacted with 5 mL of 2-MOP under
173 nitrogen gas for 5 minutes to prepare Ac-Dex with a rapid degradation rate (Ac-Dex-
174 5min) or for 3 hours to prepare Ac-Dex with a slower degradation rate (Ac-Dex-3h). The
175 reaction was quenched with 1 mL of TEA. The reaction mixture was then precipitated in
176 basic water (water and TEA, pH 9), vacuum filtered, and lyophilized ($-50\text{ }^{\circ}\text{C}$, 0.023
177 mbar) for 24 hours to yield a solid product.

178 The cyclic-to-acyclic (CAC) ratio of acetal coverage and degrees of total acetal
179 coverage per 100 glucose molecules was confirmed by ^1H NMR spectroscopy (Bruker
180 300 MHz NMR, MA). 10 mg of Ac-Dex was added to 700 μL of D_2O and was
181 hydrolyzed with 30 μL of DCl prior to analysis. The hydrolysis of one cyclic acetal group
182 produces one acetone molecule whereas one acyclic acetal produces one acetone and one
183 methanol molecule each. Consequently, from the normalized integration of peaks related
184 to acetone, methanol, and the carbon ring of dextran, the CAC ratio of acetal coverage
185 and degrees of total acetal coverage per 100 glucoses were determined.

186

187 **2.3 Formation of CUR-Loaded Ac-Dex Nanoparticles (CUR NP)**

188 Curcumin-loaded nanoparticles (CUR NP) were prepared via an oil/water
189 emulsion solvent evaporation using Ac-Dex-5min, Ac-Dex-3h, or a mixture of both types
190 of Ac-Dex (50 % w/w). 49 mg of Ac-Dex and 1 mg of CUR were dissolved in 1 mL of
191 DCM over an ice bath, establishing the organic phase. The aqueous phase was comprised

192 of 6 mL of 3% PVA in PBS and was added to the organic phase. The resulting mixture
193 was sonicated (Q500 Sonicator, Qsonica, Newtown, CT) for 30 seconds with a 1 second
194 on/off pulse at 70% amplitude. The emulsion was transferred to a spinning solution of
195 0.3% PVA in PBS and was stirred for 3 hours to allow for evaporation of the organic
196 solvent and particle hardening. The solution was then centrifuged at 19802 ×g for 20
197 minutes to collect the nanoparticles. Nanoparticles were washed once with DI water,
198 redispersed in 0.1% PVA, and lyophilized (−50 °C, 0.023 mbar) for 48 hours. The
199 resulting NP systems were: CUR NP-5min (made of Ac-Dex-5min only), CUR NP-3h
200 (made of Ac-Dex-3h only), and CUR NP-h (50 wt% Ac-Dex-5min and 50 wt% Ac-Dex-
201 3h).

202

203 **2.4 Formulation of CUR Nanocomposite Microparticles (CUR nCmP) via Spray** 204 **Drying**

205 CUR nCmP were prepared via the spray drying of an aqueous suspension of each
206 type of CUR NP (0.5%, w/v) using a Büchi B-290 spray dryer (Büchi Labortechnik, AG,
207 Switzerland) in open mode. The CUR NP suspension was sonicated for 10 minutes
208 before spray drying. The spray drying conditions were as follows: inlet temperature of 60
209 °C (outlet temperature of 32 ± 2 °C), 0.7 mm nozzle diameter, atomization gas flow rate
210 of 414 L/h using dry nitrogen, aspiration rate of 28 m³/h, pump rate of 0.9 mL/min, and
211 nozzle cleaner rate of 3. The resulting nCmP were separated in a high-performance
212 cyclone, dried for 15 minutes in the spray dryer for further removal of residual water,
213 collected in a sample collector, and stored in amber glass vials in a desiccator at −20°C.

214 nCmP comprised of each kind of NP described previously were produced: nCmP-5min,
215 nCmP-3h, and nCmP-h, correspondingly.

216

217 **2.5 Formulation of CUR Microparticles (CUR MP) via Spray Drying**

218 Solid curcumin-loaded microparticles (CUR MP) were prepared via the spray
219 drying of an organic solution comprised of Ac-Dex and CUR using a Büchi B-290 spray
220 dryer in closed mode. The organic solutions were prepared by dissolving CUR and Ac-
221 Dex (2:98 w/w) in an organic solvent comprised of 85% acetone and 15% THF (v/v) at a
222 solids concentration of 2% (w/v). The spray drying conditions were as follows: inlet
223 temperature of 60 °C (outlet temperature of 40 ± 2 °C), 0.7 mm nozzle diameter,
224 atomization gas flow rate of 414 L/h using UHP dry nitrogen, aspiration rate of 40 m³/h,
225 pump rate of 3 mL/min, and nozzle cleaner rate of 0. The resulting MP were separated in
226 a high-performance cyclone, dried for 15 minutes in the spray dryer for further removal
227 of residual solvent, collected in a sample collector, and stored in amber glass vials in a
228 desiccator at -20°C. The resulting MP were: MP-5min (from Ac-Dex-5min), MP-3h
229 (from Ac-Dex-3h), and MP-h (from 50 wt% Ac-Dex-5min and 50 wt% Ac-Dex-3h).

230

231 **2.6 Particle Size, Size Distribution, and Zeta Potential Analysis**

232 The average diameter, size distribution, and zeta potential of the original NP and
233 the NP released from the dispersion of nCmP in water were measured by dynamic light
234 scattering (DLS) using a Malvern Nano Zetasizer (Malvern Instruments, Worcestershire,
235 UK). The original NP and nCmP were dispersed in DI water (pH = 7, 0.3 mg/mL) prior

236 to analysis. All experiments were performed in triplicate with a scattering angle of 173°
237 at 25°C .

238

239 **2.7 Particle Morphology and Shape Analysis via Scanning Electron Microscopy** 240 **(SEM)**

241 The shape and surface morphology of the nCmP and MP were evaluated by SEM
242 using a Zeiss SIGMA VP Field Emission-Scanning Electron Microscope (FE-SEM)
243 (Germany). Particle samples were placed on aluminum SEM stubs (Ted Pella, Inc.,
244 Redding, CA) with double-sided adhesive carbon tabs. The samples were coated with a
245 thin film of a gold/palladium alloy using a BIO-RAD sputter coating system at $20\ \mu\text{A}$ for
246 60 seconds under argon gas. Images were captured at 8 kV at various magnifications. The
247 geometric mean diameter and standard deviation of the MP were measured digitally from
248 SEM images using ImageJ software (Rasband, 1997-2016). Representative micrographs
249 (5000x magnification) for each sample were analyzed by measuring the diameter of at
250 least 300 particles.

251

252 **2.8 Tapped Density Evaluation of nCmP and MP**

253 The tapped density of the particles was measured as described previously with
254 minor modifications (Tomoda et al., 2008). 35 - 40 mg of particles was weighed into a
255 glass tube. The tube was tapped 200 times to ensure efficient packing of the particles and
256 then the volume occupied by the particles was measured using calipers. The density of
257 the particles was then determined by the following equation:

258

259 $\rho = \frac{m}{V}$ (1)

260

261 where ρ is the tapped density, m is the particle mass, and V is the volume occupied by the
262 particles as determined by measuring the height of the particles in the tube with a known
263 diameter (5 mm). The theoretical mass median aerodynamic diameter ($MMAD_T$) of the
264 particles was then calculated using the following equation:

265

266 $MMAD_T = d \sqrt{\frac{\rho}{\rho^*}}$ (2)

267

268 where d is the geometric diameter determined by ImageJ, ρ is the tapped density of the
269 particles, and $\rho^* = 1 \text{ g/cm}^3$, which is the reference density of solid polymer.

270

271 **2.9 Drug Loading Analysis of nCmP and MP**

272 The drug loading and encapsulation efficiency of CUR nCmP and CUR MP were
273 determined via fluorescence spectroscopy (Biotek Cytation 3, Winooski, VT). All
274 particle samples were dissolved in DMSO and were evaluated at 420 nm (excitation) and
275 520 nm (emission). The CUR drug loading and encapsulation efficiency (EE) of the
276 particles were determined by the following equations:

277

278
$$\text{Drug loading} = \frac{\text{mass of CUR loaded in particles}}{\text{mass of particles}}$$
 (3)

$$\text{Encapsulation efficiency (EE)} = \frac{\text{mass of CUR loaded in particles}}{\text{initial mass of CUR in particles}} \times 100\% \quad (4)$$

279

280 **2.10 *In Vitro* Drug Release from nCmP and MP**

281 The *in vitro* release profiles of CUR from nCmP and MP were determined via the
282 release of suspended particles (0.5 mg/mL, 1.5 mL) in modified phosphate buffer (0.1 M,
283 pH = 7.4, 0.5 wt% Tween[®] 80) and modified acetate buffer (0.1 M, pH = 5, 0.5 wt%
284 Tween[®] 80). The particle suspensions were incubated at 37 °C and 100 rpm (Digital Heat
285 Block and ORBi shaker, Benchmark Scientific, Edison, NJ). At various time points,
286 particle samples were centrifuged at 23102 ×g for 5 minutes at 4 °C to isolate the NP.
287 200 µL of supernatant was withdrawn and replaced by the same amount of fresh modified
288 buffer in each sample. The withdrawn solutions were mixed with an equal volume of
289 DMSO and analyzed for CUR content via fluorescence spectroscopy using the same
290 method described for drug loading. The release data was fitted to several commonly
291 utilized drug release models (Supplemental Information **Section S.1**) to elucidate the
292 mechanism of drug release of Ac-Dex particles. The coefficient of determination (R^2)
293 was applied to test the applicability of the described release models.

294

295 **2.11 Differential Scanning Calorimetry (DSC)**

296 The thermal phase transitions of nCmP, MP, and their raw components were
297 determined via DSC using a TA Q10 DSC system (TA Instruments, New Castle, DE,
298 USA) equipped with an automated computer-controlled TA instruments DSC refrigerated
299 cooling system. 1 - 3 mg of sample was weighed into Tzero™ alodine-coated aluminum
300 pans that were hermetically sealed. The sealed pans were placed into the DSC furnace

301 along with an empty sealed reference pan. The heating range was 0 – 200 °C at a heating
302 rate of 10 °C/min.

303

304 **2.12 Powder X-Ray Diffraction (PXRD)**

305 The crystalline states of nCmP, MP, and its raw components were examined by
306 PXRD using a Rigaku Multiflex X-ray diffractometer (The Woodlands, TX) with a Cu
307 K α radiation source (40 kV, 44 mA). The samples were placed on a horizontal quartz
308 glass sample holder (3 mm) prior to analysis. The scan range was 5 – 60° in 2 Θ with a
309 step width of 0.1 and scan rate of 1 °/min.

310

311 **2.13 Karl Fischer Coulometric Titration**

312 The water content of nCmP and MP was quantified by Karl Fischer (KF) titration
313 using a 737 KF coulometer (Metrohm, Riverview, FL). 5 mg of powder was dissolved in
314 anhydrous methanol. The resulting solution was injected into the KF reaction cell filled
315 with Hydranal[®] KF reagent and then the amount of water was analyzed. Pure solvent was
316 also injected for use as a background sample.

317

318 **2.14 *In Vitro* Aerosol Dispersion Performance with the Next Generation Impactor** 319 **(NGI)**

320 *In vitro* aerosol dispersion performance of nCmP and MP was evaluated using a
321 Next Generation Impactor[™] (NGI[™], MSP Corporation, Shoreview, MN) equipped with
322 a stainless steel induction port (USP throat adaptor) attachment and stainless steel
323 gravimetric insert cups. The NGI[™] was coupled with a Copley TPK 2000 critical flow

324 controller, which was connected to a Copley HCP5 vacuum pump (Copley Scientific,
325 United Kingdom). The air flow rate (Q) was measured and adjusted to 60 L/min before
326 each experiment in order to model the flow rate in a healthy adult lung. Glass fiber filters
327 (55 mm, Type A/E, Pall Life Sciences, PA) were placed in the gravimetric insert cups for
328 stages 1 through 7 to minimize particle bounce or re-entrapment (Meenach et al., 2013a)
329 and these filters were weighed before and after the experiment to determine the particle
330 mass deposited on each stage. Approximately 10 mg of powder was loaded into a
331 hydroxypropyl methylcellulose (HPMC, size 3, Quali-V[®], Qualicaps[®] Inc., Whitsett, NC,
332 USA) capsule and the capsule was placed into a human dry powder inhaler device
333 (HandiHaler, Boehringer Ingelheim Pharmaceuticals, CT) attached to a customized
334 rubber mouthpiece connected to the NGI[™]. Three HPMC capsules were loaded and
335 released in each measurement and experiments were performed in triplicate. The NGI[™]
336 was run with a delay time of 10 s and running time of 10 s. For Q = 60 L/min, the
337 effective cutoff diameters for each stage of the impactor were given from the
338 manufacturer as: stage 1 (8.06 μm); stage 2 (4.46 μm); stage 3 (2.82 μm); stage 4 (1.66
339 μm); stage 5 (0.94 μm); stage 6 (0.55 μm); and stage 7 (0.34 μm). Our previous study on
340 the relationship between particle mass distribution and payload distribution showed that
341 no significant difference existed between the drug amount and particle mass in each
342 chamber of NGI ($p > 0.05$), indicating that the drug was uniformly dispersed in both
343 CUR-MP and CUR-nCmP (**Figure S1**). The fine particle fraction (FPF), respirable
344 fraction (RF), and emitted dose (ED) were calculated as follows:

345

$$\text{Fine particle fraction (FPF)} = \frac{\text{mass of particles on Stages 2 through 7}}{\text{initial particle mass loaded into capsules}} \times 100\% \quad (5)$$

346

$$\text{Respirable fraction (RF)} = \frac{\text{mass of particles on Stages 2 through 7}}{\text{total particle mass on all stages}} \times 100\% \quad (6)$$

347

$$\text{Emitted dose (ED)} = \frac{\text{initial mass in capsules} - \text{final mass remaining in capsules}}{\text{initial mass in capsules}} \times 100\% \quad (7)$$

348

349 The experimental mass median aerodynamic diameter (MMAD_E) and geometric
350 standard deviation (GSD) for the particles were determined using a Mathematica[®]
351 program written by Dr. Warren Finlay (Meenach et al., 2013a; W, 2008).

352 **2.15 Statistical Analysis**

353 All measurements were performed in at least triplicate. Values are given in the
354 form of mean ± standard deviation. The statistical significance of the results was
355 determined using analysis of variance (ANOVA) and student's t-test. A p-value of <0.05
356 was considered statistically significant.

357 **3. RESULTS AND DISCUSSION**

358 **3.1 Preparation and Characterization of Ac-Dex and Curcumin Nanoparticles**

359 *3.1.1 NMR Analysis of Ac-Dex*

360 Successful synthesis of Ac-Dex was confirmed by ¹H NMR (**Figure S2**). Ac-Dex-
361 5min exhibited 61.2% cyclic acetal coverage (CAC) and 71.6% total conversion of -OH

364 groups, while Ac-Dex-3h exhibited 82.5% CAC and 80.0% total conversion of -OH
365 groups, which matched our previous results (Wang et al., 2016; Wang and Meenach,
366 2016). The Ac-Dex with longer synthesis time (Ac-Dex-3h) exhibited a higher CAC,
367 which was in accordance with previous studies. An increase in CAC is known to decrease
368 polymer degradation and ultimately, the drug release rate, due to the slower degradation
369 of the cyclic acetal groups on the Ac-Dex backbone (Bachelder et al., 2008; Broaders et
370 al., 2009). Ac-Dex-3h also showed a higher total conversion of -OH groups, which could
371 be a result the longer reaction time. This higher total acetal coverage is favorable in the
372 enhancement of the stability of the PVA coating of nanoparticles (data not shown), thus
373 ensuring small particle size and narrow size distribution.

374

375 *3.1.2 Dynamic Light Scattering (DLS) Analysis of Original and Redispersed CUR NP*

376 Average nanoparticle size, size distribution/polydispersion index (PDI), and zeta
377 potential are shown in **Table 1**. No significant changes in NP size, PDI, or zeta potential
378 was found between the original and redispersed NP ($p < 0.05$), indicating that the CUR
379 NP maintained their properties after redispersion. The original and redispersed NP
380 exhibited an average diameter of approximately 200 nm, which is in the desirable range
381 to avoid macrophage clearance and mucus entrapment (Kho et al., 2010). The low PDI
382 value denotes a narrow size distribution of the NP, and the slightly negatively charged
383 surface of nanoparticles, as measured by zeta potential, is desirable in order to reduce the
384 interactions with negatively charged mucin fibers present in airway mucus (Lai et al.,
385 2009). According to our preliminary experiments (data not shown), a low total
386 conversion of -OH groups on the Ac-Dex results in NP with larger sizes and PDI due to

387 NP agglomeration. This phenomenon could be a result of the reduced hydrophobicity of
388 Ac-Dex with fewer -OH groups converted to acetal groups, which leads to insufficient
389 absorption of PVA on the NP surface. However, the Ac-Dex in this study was prepared to
390 produce NP with small sizes and low PDI, as the total conversion of -OH groups was
391 kept in a higher range to prevent NP agglomeration.

392

393 **3.2 Preparation and Characterization of Nanocomposite Microparticles (nCmP) and** 394 **Microparticles (MP)**

395

396 *3.2.1 Morphology, Sizing, and Size Distribution*

397 CUR nCmP displayed a wrinkled surface with visibly encapsulated NP as seen in
398 **Figure 2 and Figure S3**. The raisin-like morphology of the nCmP can be attributed to
399 the early formation of nanoparticle shells in the solution droplets during spray drying,
400 which determines the geometric size of nCmP. As the drying process proceeds, the
401 remaining solvent evaporates from the droplet center, resulting in hollow particles that
402 tend to shrink (Atalar and Dervisoglu, 2015; Gu et al., 2015).

403 CUR MP were collapsed, wrinkled spheres as seen in **Figures 2D-F**. Altering the
404 Ac-Dex composition of the particles had no impact on particle morphology. The
405 geometric diameters (d_g) of the CUR nCmP and MP systems are shown in **Table 2**. All of
406 the MP d_g were approximately 1 μm in size, which is reported to make the particles
407 vulnerable to macrophage uptake (Sung et al., 2009). In contrast, the NP released from
408 nCmP systems can escape macrophage clearance upon reaching the deep lung.

409

410 3.2.2 Analysis of Particle Density

411 The density of the particles was determined via tapped density measurements, as
412 shown in **Table 2**. CUR nCmP exhibited tapped density values around 0.12 g/cm^3 , while
413 the MP system showed values around 0.05 g/cm^3 . These density values are relatively low
414 compared with the raw materials ($\sim 1 \text{ g/cm}^3$), which can be attributed to the wrinkled
415 morphology and hollow structures of the particle systems. It has been reported that
416 particles $> 1 \text{ }\mu\text{m}$ in diameter with greater density will deposit in the lungs by
417 sedimentation (Heyder, 2004). Therefore, the increased density of CUR nCmP system as
418 compared to MP could enhance their rate of deposition into the deep lung.

419

420 3.2.3 Loading and In Vitro Release of CUR

421 CUR was successfully encapsulated into both the nCmP and MP systems as seen
422 in **Table 2**. The MP systems prepared via closed mode, organic spray drying exhibited
423 higher encapsulation efficiency (EE, $> 50\%$) than the nCmP systems (approximately
424 30%) prepared in open mode in aqueous solutions. The lower EE of the nCmP can be
425 attributed to the EE of the original CUR-loaded NP, which was also approximately 30%
426 (**Table S1**). The spray drying process had no influence on the CUR loading and EE for
427 the nCmP systems ($p < 0.05$), which indicates that the drug loading of nCmP systems can
428 be determined during NP preparation.

429 Results of the *in vitro* release of CUR from both nCmP and MP systems in
430 modified phosphate (pH 7.4) and acetate (pH 5) buffers at physiological temperature
431 (37°C) are reported in **Figure 3** as the percentage of cumulative drug released over time.
432 As shown in **Table S2**, the particle systems exhibited shorter release durations and

433 increased release of CUR ($p < 0.05$) at acidic pH with the exception of nCmP-5min,
434 which only exhibited a shorter release duration. These results are in accordance with
435 previous studies (Meenach et al., 2012; Vehring, 2008). The release profiles suggest that
436 the drug will be released at significantly higher rates once the carrier particles reach an
437 acidic environment. This can allow Ac-Dex particles the ability to provide controlled
438 release of a therapeutic payload in cells and tissue with lower pH values, such as tumor
439 cells and macrophages. In contrast, if the carrier particles remain in the extracellular or
440 neutral pH environments, the release rate can be reduced, which can minimize systemic
441 and local cytotoxicity (Meenach et al., 2012).

442 In addition, the nCmP systems exhibited faster release than the MP systems,
443 which is likely due to the larger surface area available in the nano-sized delivery systems.
444 Upon reaching an aqueous environment, the nCmP dissociate into nanoparticles with
445 large surface areas and a PVA coating that facilitates particle dispersity, while the MP
446 may agglomerate due to their highly hydrophobic, uncoated surfaces. As a result, the
447 nCmP systems undergo faster polymer degradation and drug diffusion, resulting in a
448 faster release of payloads than MP at both acidic and physiologic pH.

449 Particles comprised of Ac-Dex-3h exhibited slower release rates than those
450 comprised of Ac-Dex-5min, indicating that the drug release rate can be controlled by the
451 polymer reaction time. At pH 7.4, particles made of Ac-Dex-h exhibited a drug release
452 rate between Ac-Dex-5 min and Ac-Dex-3h, suggesting that the ratio of different types of
453 Ac-Dex can also act as an important factor in adjusting the release profiles of particle
454 systems. Nevertheless, the drug release rates of the Ac-Dex particles at pH 5 did not
455 follow this trend, which could be explained by one of the following: (1) the release

456 profile of Ac-Dex particles is polymer degradation controlled and the decomposition of
457 the Ac-Dex matrix is greatly impacted by the release buffer pH and (2) the release profile
458 of Ac-Dex particles is both polymer degradation and drug diffusion controlled. In
459 previous studies, drug release from Ac-Dex particles was associated with Ac-Dex
460 degradation (Bachelder et al., 2008; Kauffman et al., 2012; Meenach et al., 2012).
461 However, Ac-Dex degradation may result in the surface erosion of particles, formation of
462 large pores in the particles that facilitate drug diffusion, or both at the same time. As a
463 result, the drug release profile could be controlled by drug diffusion through water-filled
464 pores (diffusion controlled), polymer erosion on the particle surface (erosion controlled),
465 or both drug diffusion and surface erosion (diffusion and erosion controlled), respectively
466 (Broaders et al., 2009).

467 In order to further illustrate the mechanism of drug release of Ac-Dex particles,
468 we fitted the CUR release data to several commonly utilized drug release models,
469 including: (1) a first order model and (2) Hixson–Crowell model for drug dissolution-
470 controlled release, (3) Higuchi model modified to fit burst release at time 0, (4)
471 Korsmeyer–Peppas model and (5) Baker–Lonsdale for drug diffusion-controlled release,
472 (6) Hopfenberg model for surface erosion-controlled release, (7) Baker’s model for both
473 degradation and diffusion-controlled release, and (8) Weibull model as a general
474 empirical equation to describe a dissolution or release process (Bohrey et al., 2016; Costa
475 and Sousa Lobo, 2001; Kamaly et al., 2016; Seidlitz and Weitschies, 2012; Shuwisitkul,
476 2011). The coefficient of determinations (R^2) of the fit for the models are summarized in
477 **Table S3**. The modified Higuchi and Baker–Lonsdale models exhibited higher R^2
478 compared with other models, indicating that the drug release profiles of all Ac-Dex

479 particles at both acidic and neutral pH was due primarily to drug diffusion. For Baker's
480 model (Shuwisitkul, 2011) that describes a degradation and diffusion process, the optimal
481 coefficient k was 0, thus the equation of Baker's model exhibited the same form as the
482 equation for the Higuchi model. Since the degradation of Ac-Dex was observable during
483 the release experiments, the release profiles of Ac-Dex particles can be explained by the
484 mechanism of drug diffusion through water-filled pores (Kamaly et al., 2016). In the
485 process of drug diffusion through water-filled pores, water was absorbed by Ac-Dex
486 particles and filled in the pores of the polymer matrix, through which the drug diffused
487 into the buffer. As polymer degraded, both pore size and number increased, resulting in
488 enhanced drug release. Therefore, the reaction time of Ac-Dex affected the drug release
489 rate significantly by controlling the formation of pores of particle matrix but not polymer
490 degradation on the surface. Meanwhile, the water absorption into the particles may also
491 influence the drug release rate, which can be supported by the fact that Ac-Dex-3h had a
492 higher ratio of total hydrophobic acetalated group conversion than Ac-Dex-5min. The
493 fitted release curves using modified Higuchi model are shown in **Figure S4** along with
494 the original data points. The model was modified to fit the burst release at time 0 of the
495 particle systems, which can be attributed to CUR being initially available on the surface
496 of the particles. The nCmP systems exhibited a high release at time 0 because the
497 nanoparticle suspension was sonicated before spray drying to form a uniform dispersion,
498 which may cause CUR release in to the suspension.

499

500 3.3.4 Karl Fischer Titration

501 The residual water content of CUR nCmP and MP is shown in **Table 2**. The water
502 content of nCmP system was approximately 8%, while that of MP system was
503 approximately 6%. The lower water content of MP samples is likely due to the absence of
504 water during the closed mode spray drying process. All particle systems showed
505 acceptable water content for aerosol formulations. In general, reducing the water content
506 in inhalable dry powders can significantly improve their dispersion properties and
507 enhance the stability of the powders during storage (Hickey et al., 2007; Mohammadi et
508 al., 2010). Correspondingly, low water content in inhalable dry powders is highly
509 favorable for efficient dry powder aerosolization and effective particle delivery
510 (Mohammadi et al., 2010; Wu et al., 2013).

511

512 *3.3.5 Differential Scanning Calorimetry*

513 **Figure 4** shows DSC thermograms of the raw materials used in particle
514 preparation and the final CUR nCmP and CUR MP systems. Both the raw Ac-Dex-5min
515 and Ac-Dex-3h displayed endothermic phase transition peaks due to melting (T_m) near
516 170 °C. The peaks were broad because of the wide size distribution of Ac-Dex polymer
517 crystallites. None of the CUR nCmP systems exhibited a peak corresponding to Ac-Dex
518 melting, which indicates that the Ac-Dex was transformed in an amorphous state by rapid
519 precipitation during NP formation. The CUR MP systems exhibited broad phase
520 transition peaks near 160 °C, which corresponds to the melting of Ac-Dex. This phase
521 transition shifted to the lower temperature range, indicating a reduction in the
522 crystallinity of Ac-Dex after the spray drying process.

523

524 3.3.6 Powder X-ray Diffraction (PXRD)

525 X-ray diffraction diffractograms of the raw materials, physical mixture of Ac-Dex
526 and CUR, CUR nCmP, and CUR MP are shown in **Figure 5**. No peaks were present for
527 either raw Ac-Dex samples, suggesting an irregular distribution or lack of Ac-Dex
528 crystallites. The absence of diffraction peaks from Ac-Dex is quite different from
529 commercialized polymers such as PLGA, which exhibits strong XRD characterization
530 peaks (Mohammadi et al., 2010). This phenomenon is likely because the Ac-Dex was
531 collected by rapid precipitation in water, which prevents the formation of large polymer
532 crystallites. Strong peaks were present for raw CUR indicating that it was in crystalline
533 form prior to spray drying. XRD diffractograms of the physical mixture, CUR nCmP and
534 CUR MP were absent of any diffraction peaks corresponding to raw CUR, which was
535 due to the dilution effect of Ac-Dex. The results obtained from the XRD diffractograms
536 confirmed those from DSC thermograms, which show that raw CUR was converted to
537 amorphous forms during the particle manufacturing process.

538

539 3.3.7 In Vitro Aerosol Dispersion Performance Using Next Generation Impactor (NGI)

540 *In vitro* aerosol dispersion performance properties of the nCmP were evaluated
541 using a Next Generation Impactor™ coupled with a human DPI device (**Figure 6 and**
542 **Figure 7**). The results indicated that the formulated nCmP and MP are favorable for
543 efficient dry powder aerosolization and effective targeted pulmonary delivery. The
544 experimental mass mean aerodynamic diameter (MMAD_E) values of all particle systems
545 were approximately 2 μm, while the geometric standard deviation (GSD) values were 2 -
546 3 μm. The MMAD_E values were within the range of 1 - 5 μm that is required for

547 predominant deposition of particles into the deep lung region (Meenach et al., 2013b),
548 which would be desirable to deliver therapeutics for the treatment of both local and
549 systematic diseases through the lung. The theoretical mass mean aerodynamic diameter
550 ($MMAD_T$, **Table 2**), calculated using the geometric diameter and tapped density, was
551 lower than the experimental MMAD. This discrepancy is likely due to particle
552 agglomeration, which increased the geometric size of the dry powder particulates. All of
553 the particle systems exhibited low tapped density values, which supports the hypothesis
554 that the particles are likely hollow. This can also be attributed to their wrinkled surface
555 morphology, as seen in SEM analysis. The GSD values were within the range of those
556 previously reported and the respirable fraction (RF), fine particle fraction (FPF), and
557 emitted dose (ED) values were all higher than reports from similar systems (Meenach et
558 al., 2013a; Meenach et al., 2013b; Ungaro et al., 2006). The formulated Ac-Dex particle
559 systems are expected to achieve an improved therapeutic effect with a reduced amount of
560 payloads by effectively delivering drugs into the deep lung region.

561

562 **4. CONCLUSIONS**

563 Two types of pulmonary delivery systems were successfully formulated using Ac-
564 Dex with two different degradation rates. The resulting CUR MP were wrinkled spheres
565 (approximately 1 μm), while nCmP were similar in size with wrinkled surfaces that
566 showed the presence of nanoparticles. The variations in the drug release rates from the
567 Ac-Dex particles were influenced by the Ac-Dex reaction time, ratio of two types of Ac-
568 Dex, and the particle size, which could be easily tuned during the manufacturing process.
569 The pH value of the environment also had a significant influence on the release profiles,

570 allowing the Ac-Dex particles to release the payload in a controlled fashion. All nCmP
571 and MP systems exhibited desirable properties as dry powder inhalation formulations,
572 including small aerodynamic diameters, which is suitable for deep lung delivery, low
573 water content, which is favorable for particle storage, and amorphization of a crystalline
574 payload, which improves the efficiency of drug dissolution. Overall, the engineered Ac-
575 Dex aerosol particle systems have the potential for targeted delivery of therapeutics into
576 the deep lung.

577

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591

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593 No conflicts of interest exist.

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727

728

729 **TABLES AND FIGURES**

730

731 **Table 1.** Average diameter (as measured by dynamic light scattering), polydispersity
 732 index (PDI), and zeta potential (ZP) of CUR-loaded nanoparticles before spray drying
 733 (NP) and after redispersion from nanocomposite microparticles (nCmP) (mean \pm standard
 734 deviation, n = 3).

735

Particle System	Average Diameter (nm)	PDI	ZP (mV)
NP-5min	192.2 \pm 2.7	0.07 \pm 0.03	-8.4 \pm 4.1
NP-h	201.1 \pm 1.5	0.02 \pm 0.01	-8.0 \pm 3.7
NP-3h	206.1 \pm 1.3	0.03 \pm 0.03	-7.0 \pm 1.6
nCmP-5min	199.3 \pm 1.3	0.09 \pm 0.02	-14.5 \pm 1.0
nCmP-h	210.2 \pm 2.5	0.07 \pm 0.01	-13.3 \pm 1.9
nCmP-3h	213.5 \pm 2.4	0.02 \pm 0.00	-11.2 \pm 1.6

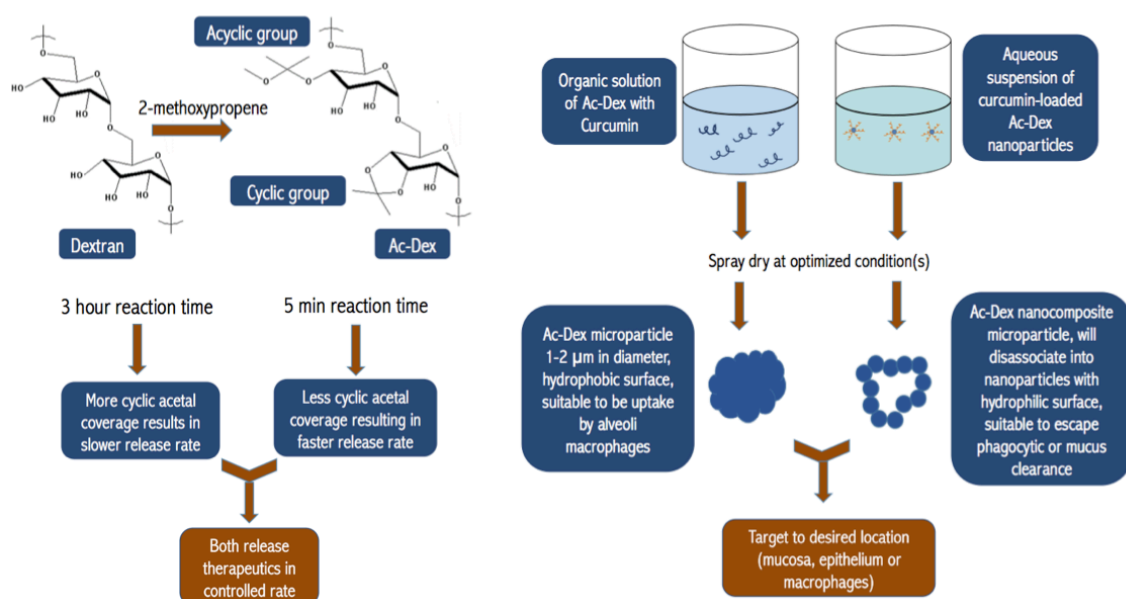
736

737 **Table 2.** Geometric diameter (as measured by SEM imaging and ImageJ analysis),
 738 experimental mass median aerodynamic diameter (MMAD_E), geometric standard
 739 deviation (GSD), water content, tapped density, theoretical mean mass aerodynamic
 740 diameter (MMAD_T), drug loading, and drug encapsulation efficiency (EE) of nCmP and
 741 MP (mean \pm standard deviation, n = 3).

Particle System	Geometric Diameter (μ m)	MMAD _E (μ m)	GSD (μ m)	Water Content (%)	Tapped Density (g/cm ³)	MMAD _T (μ m)	Drug Loading (mg/100 mg particle)	EE (%)
nCmP-5min	1.52 \pm 0.33	1.61 \pm 0.16	2.37 \pm 0.24	7.69 \pm 0.76	0.122 \pm 0.001	0.52 \pm 0.09	0.57 \pm 0.006	28.7 \pm 0.32
nCmP-h	1.77 \pm 0.46	2.05 \pm 0.09	2.62 \pm 0.17	7.89 \pm 1.56	0.115 \pm 0.004	0.60 \pm 0.09	0.58 \pm 0.008	28.4 \pm 0.42
nCmP-3h	1.72 \pm 0.39	1.89 \pm 0.09	2.70 \pm 0.13	7.86 \pm 0.43	0.133 \pm 0.002	0.64 \pm 0.12	0.62 \pm 0.013	31.2 \pm 0.63
MP-5min	0.89 \pm 0.30	2.38 \pm 0.06	2.14 \pm 0.14	6.12 \pm 1.33	0.050 \pm 0.001	0.21 \pm 0.03	1.33 \pm 0.092	66.3 \pm 4.62
MP-h	1.26 \pm 0.41	2.21 \pm 0.23	2.17 \pm 0.03	5.87 \pm 1.85	0.050 \pm 0.001	0.29 \pm 0.32	1.03 \pm 0.030	51.6 \pm 1.48
MP-3h	1.05 \pm 0.36	2.41 \pm 0.07	2.02 \pm 0.08	5.23 \pm 1.13	0.052 \pm 0.001	0.23 \pm 0.03	1.12 \pm 0.012	55.8 \pm 0.61

742

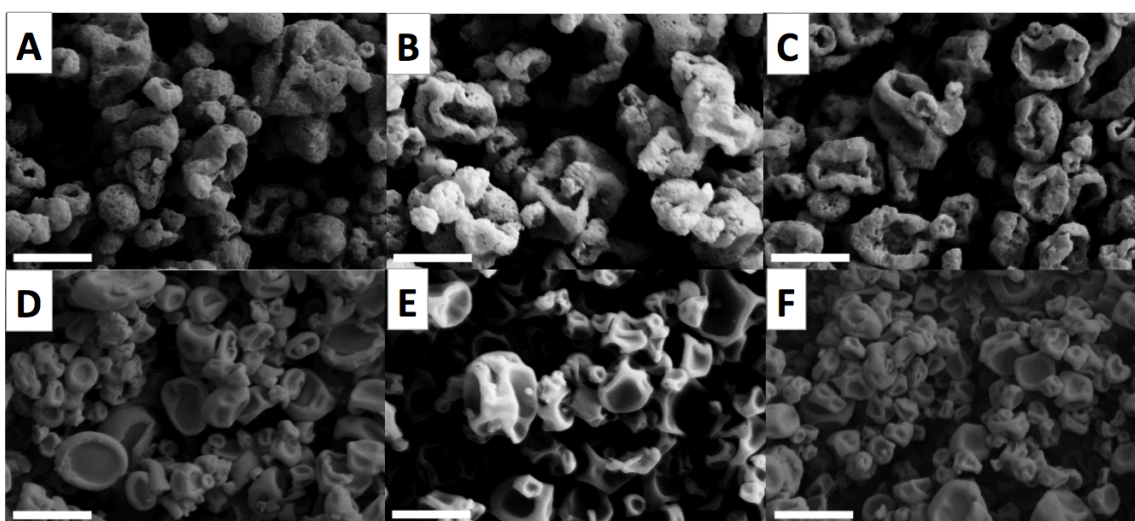
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745 **Figure 1.** Schematic depicting the synthesis of Ac-Dex (Left) and preparation of
746 nanoparticles and formation of nanocomposite microparticles (nCmP) and microparticles
747 (MP) (Right).

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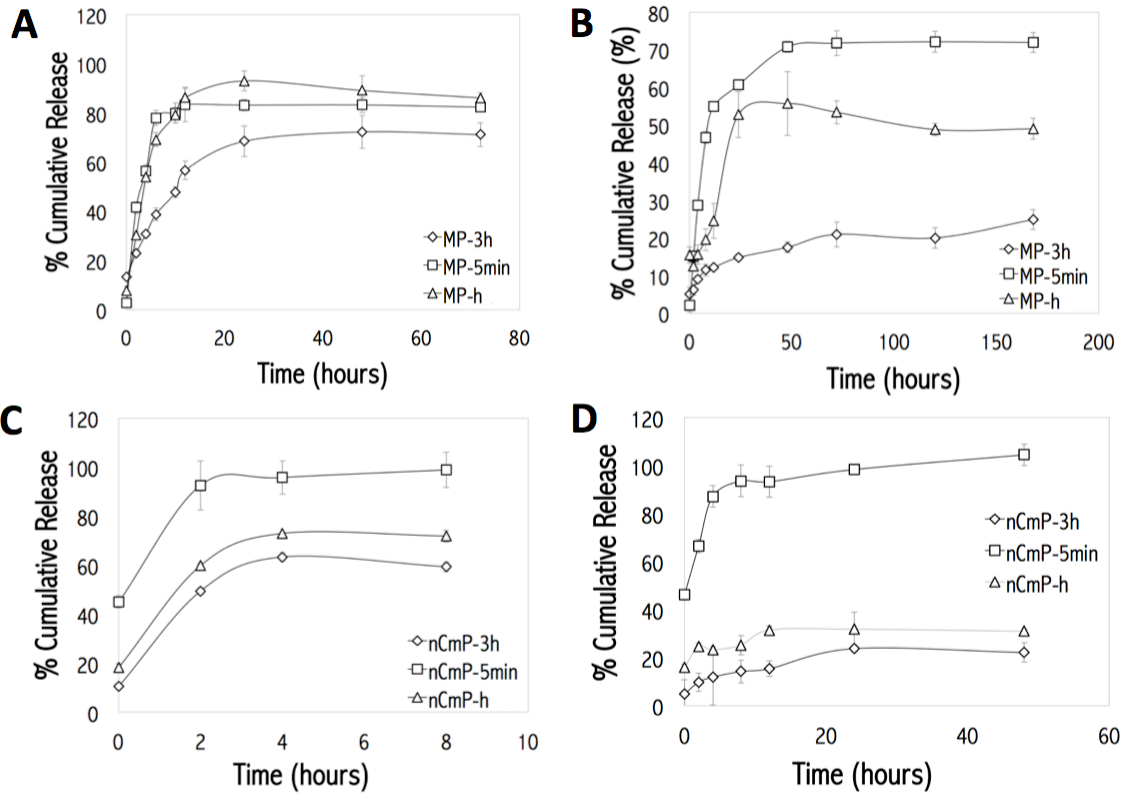


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750 **Figure 2.** SEM micrographs of curcumin-loaded nanocomposite microparticles (CUR
751 nCmP) and microparticles (CUR MP) including: (A) CUR nCmP-5min, (B) CUR nCmP-
752 h, (C) CUR nCmP-3h, (D) CUR MP-5min, (E) CUR MP-h, and (F) CUR MP-3h
753 systems. Scale bar = 2 μm .

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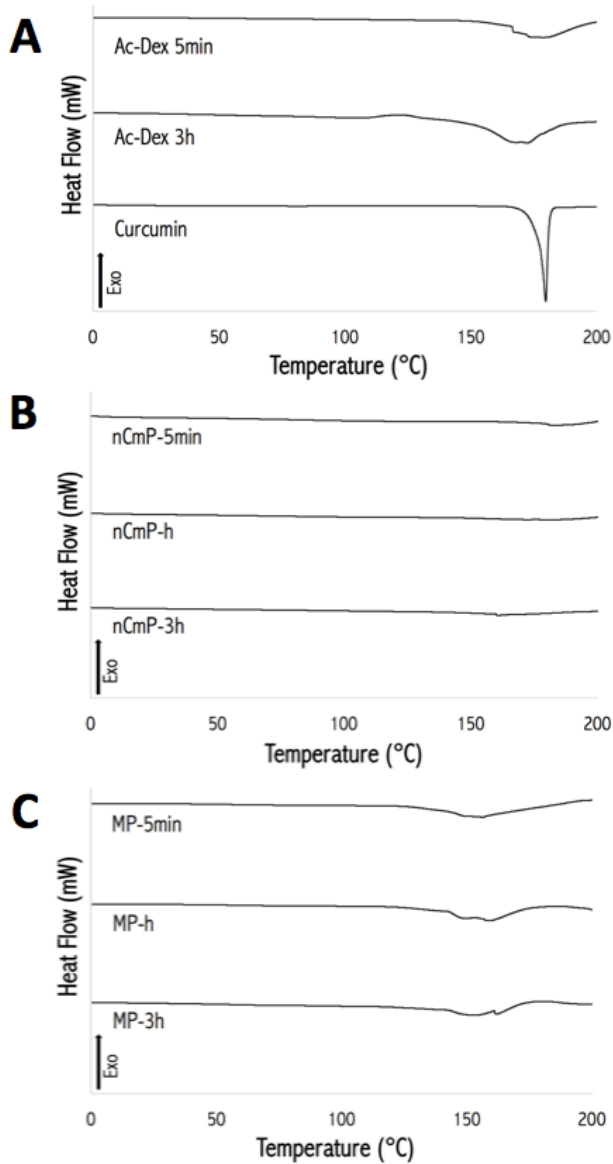
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757 **Figure 3.** *In vitro* drug release profiles for curcumin-loaded microparticle (MP) systems
758 at (A) pH 5 and (B) pH 7.4 and curcumin-loaded nanocomposite microparticle (nCmP)
759 system at (C) pH 5 and (D) pH 7.4.

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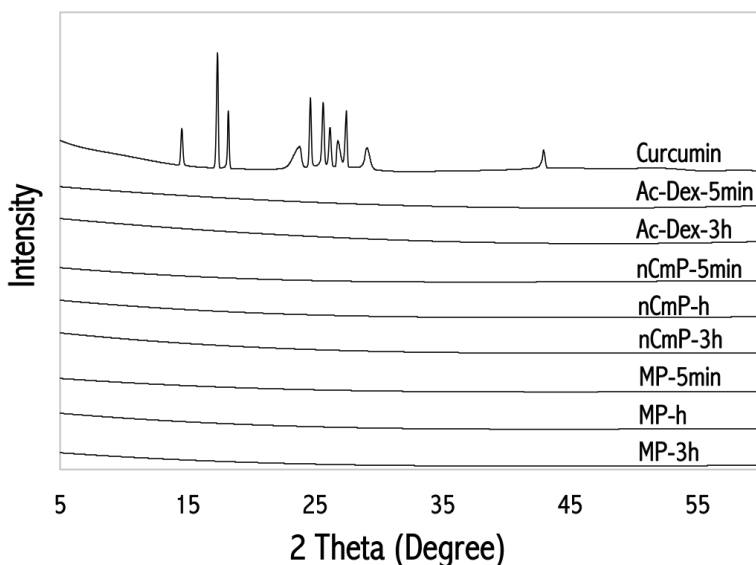


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762 **Figure 4.** Representative differential scanning calorimetry (DSC) thermograms of (A)
 763 raw curcumin (CUR), raw acetalated dextran-5min (Ac-Dex-5min), and raw acetalated
 764 dextran-3h (Ac-Dex-3h), (B) CUR nCmP-5min, CUR nCmP-h, and CUR nCmP-3h, and
 765 (C) CUR MP-5min, CUR MP-h, and CUR MP-3h.

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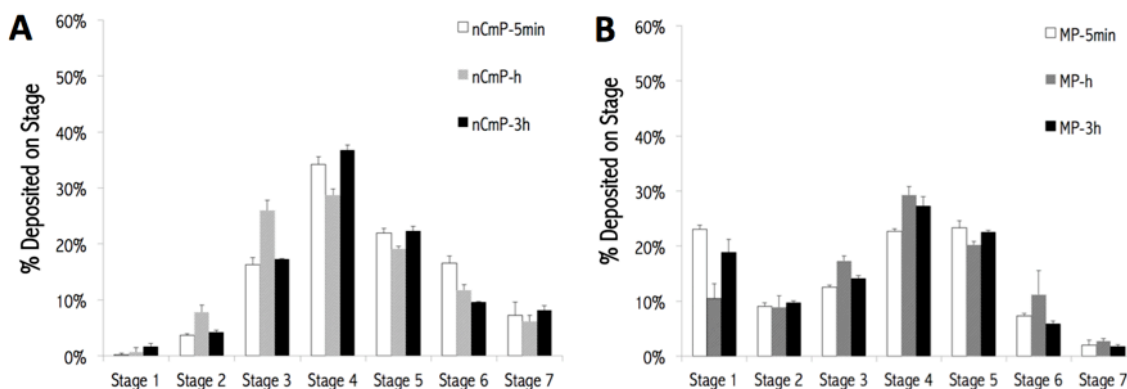


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769 **Figure 5.** Representative powder X-ray diffractograms (PXRD) of raw curcumin (CUR),
 770 raw acetalated dextran-5min (Ac-Dex-5min), raw acetalated dextran-3h (Ac-Dex-3h),
 771 CUR nCmP-5min, CUR nCmP-h, CUR nCmP-3h, CUR MP-5min, CUR MP-h, and CUR
 772 MP-3h.

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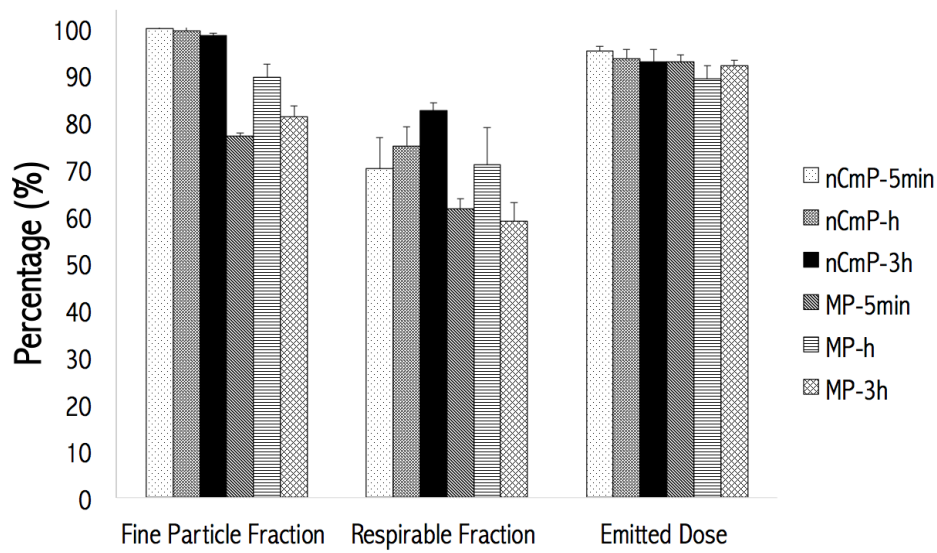
775

776 **Figure 6.** Aerosol dispersion performance of (A) curcumin-loaded nanocomposite
 777 microparticles (CUR nCmP) and (B) microparticles (CUR MP) as % particles deposited
 778 on each stage of the Next Generation Impactor™ (NGI™). For Q = 60 L/min, the
 779 effective cutoff diameters (D_{50}) for each impaction stage are as follows: stage 1 (8.06
 780 μm), stage 2 (4.46 μm), stage 3 (2.82 μm), stage 4 (1.66 μm), stage 5 (0.94 μm), stage 6
 781 (0.55 μm), and stage 7 (0.34 μm) (mean \pm standard deviation, n = 3).

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786 **Figure 7.** *In vitro* aerosol dispersion performance properties including fine particle dose
787 (FPD), fine particle fraction (FPF), respirable fraction (RF), and emitted dose (ED) for
788 curcumin loaded nanocomposite microparticles (CUR nCmP) and microparticles (CUR
789 MP) (mean \pm standard deviation, n = 3).

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806 **SUPPLEMENTAL INFORMATION**

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808 **S.1 Drug Release Model Descriptions**

809 The drug release data of the particle systems was fitted to several relevant models
810 (equations shown below) to aid in the determination of the type of release the systems
811 underwent. For the models that can be linearized (all except for Baker's model), the
812 coefficient of determination (R^2) was calculated to determine the applicability of the
813 release models. For Baker's model, Microsoft Excel with Solver add-in was applied to
814 determine the parameters that minimize the sum of squares of the residues of the model.
815 The models, equations, and their corresponding parameters are as follows:

816

817 First order model:
$$\log M_t = \log M_0 + \frac{K}{2.303} t \quad (S1)$$

818

819 where M_t is the amount of drug released at time t , M_0 is the initial amount of drug in the
820 solution, and K is the first order release constant.

821

822 Weibull model:
$$m = 1 - \exp\left(\frac{-(t - T_i)^b}{a}\right) \quad (S2)$$

823

824 where m is the accumulated fraction of the drug released at time t , a is the scale
825 parameter, which defines the time scale of the process, T_i is the location parameter, which
826 represents the lag time before the onset of the dissolution or release process, and b is the
827 shape parameter, which characterizes the shape of release curve.

828

829 Higuchi model: $M_t = Kt^{1/2} + b$ (S3)

830

831 where M_t is the amount of drug released at time t , K is the Higuchi dissolution constant,
832 and b is the amount of drug released at time 0.

833

834 Hixson–Crowell model: $W_0^{1/3} - W_t^{1/3} = Kt$ (S4)

835

836 where W_0 is the initial amount of drug in the particles, W_t is the remaining amount of
837 drug in the particles at time t , and K is a constant characterizing the surface to volume
838 relationship.

839

840 Korsmeyer–Peppas model: $m = at^n$ (S5)

841

842 where a is a constant characterizing the structural and geometric properties of the
843 particles, n is the release exponent, indicating the drug release mechanism, and m is the
844 accumulated fraction of the drug released at time t .

845

846 Baker–Lonsdale model: $\frac{3}{2}[1 - (1 - m)^{2/3}] - m = Kt$ (S6)

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848 where K is the release constant and m is the accumulated fraction of the drug released at
849 time t .

850

851 Hopfenberg model: $m = 1 - [1 - Kt(t-1)]^n$ (S7)

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853 where K is a constant equal to k_0/C_0a_0 , where k_0 is the erosion rate constant, C_0 is the
854 initial concentration of drug in the matrix, and a_0 is the initial radius for particles. m is the
855 accumulated fraction of the drug released at time t .

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857 Baker's model: $M_t = A(2P_0e^{kt}C_0t)^{1/2}$ (S8)

858

859 where M_t is the amount of drug released in time t , P_0 is the drug permeability, A is the
860 total area of the particle, C_0 is the drug concentration at the initial time, and k is the first-
861 order rate constant of bond cleavage of the polymer carrier.

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869 **Table S1.** Drug loading and encapsulation efficiency of curcumin NP including NP-
870 5min, NP-h, and NP-3h.

Particle System	Drug Loading (mg/100mg particle)	EE (%)
NP-5min	0.600 ± 0.059	30.0 ± 2.95
NP-h	0.621 ± 0.056	31.0 ± 2.82
NP-3h	0.617 ± 0.063	30.9 ± 3.15

871

872 **Table S2.** The release duration and total fraction of curcumin released from each particle
873 system at acidic and neutral pH.

Particle System	pH = 5		pH = 7.4	
	Release Duration (h)	Total Released (%)	Release Duration (h)	Total Released (%)
nCmP-5min	2	92.6	8	93.6
nCmP-h	2	63.4	12	31.5
nCmP-3h	4	73.0	24	23.7
MP-5min	6	78.0	24	60.6
MP-h	12	86.4	24	52.7
MP-3h	24	68.5	168	24.9

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883 **Table S3.** Summary of the coefficient of determinations (R^2) of all the fitted drug release
 884 models for all particle system. The model with relatively high R^2 for all particle systems
 885 was regarded as a viable fit for that system.

pH = 5						
Model	nCmP - 5min	nCmP - -h	nCmP - -3h	MP - 5min	MP -h	MP -3h
First order	0.7835	0.8549	0.8511	0.5730	0.4848	0.7517
Hixson- Crowell	0.8615	0.9571	0.9613	0.8470	0.8899	0.9490
Higuchi (modified)	0.9468	0.9968	0.9989	0.9867	0.9748	0.9715
Korsmeyer- Peppas	0.9998	0.6906	0.5050	0.8100	0.8843	0.9882
Baker- Lonsdale	0.8729	0.9945	0.9799	0.9065	0.9595	0.9753
Hopfenberg	0.5497	0.8743	0.9029	0.8925	0.849	0.9276
Weibull	0.9098	0.5773	0.2538	0.9387	0.9936	0.9353

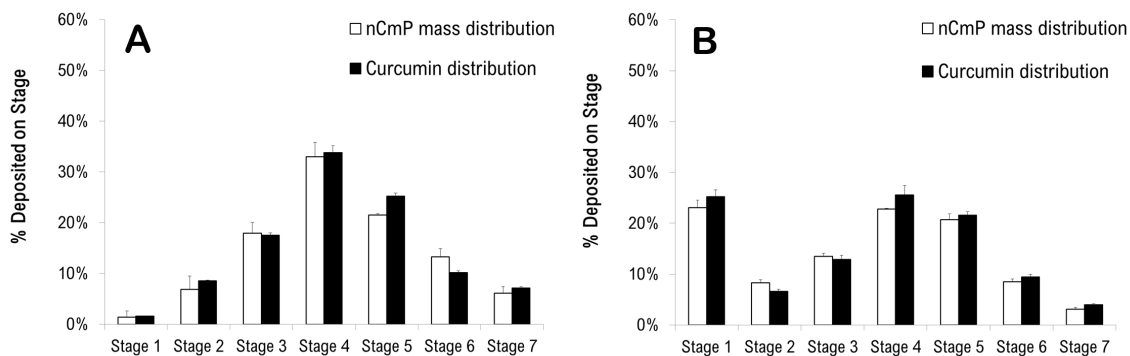
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pH = 7.4						
Model	nCmP - 5min	nCmP - -h	nCmP - 3h	MP - 5min	MP -h	MP -3h
First order	0.8084	0.7345	0.7574	0.3797	0.8290	0.6414
Hixson- Crowell	0.9312	0.8021	0.9482	0.7696	0.9117	0.8188
Higuchi (modified)	0.9573	0.8758	0.9732	0.9369	0.8288	0.9462
Korsmeyer- Peppas	0.8990	0.5374	0.9457	0.8828	0.9349	0.9708
Baker- Lonsdale	0.9709	0.8172	0.9089	0.9283	0.9141	0.9074
Hopfenberg	0.8493	0.8678	0.9685	0.7462	0.8241	0.8526
Weibull	1.0000	0.5235	0.7905	0.9783	0.8897	0.8963

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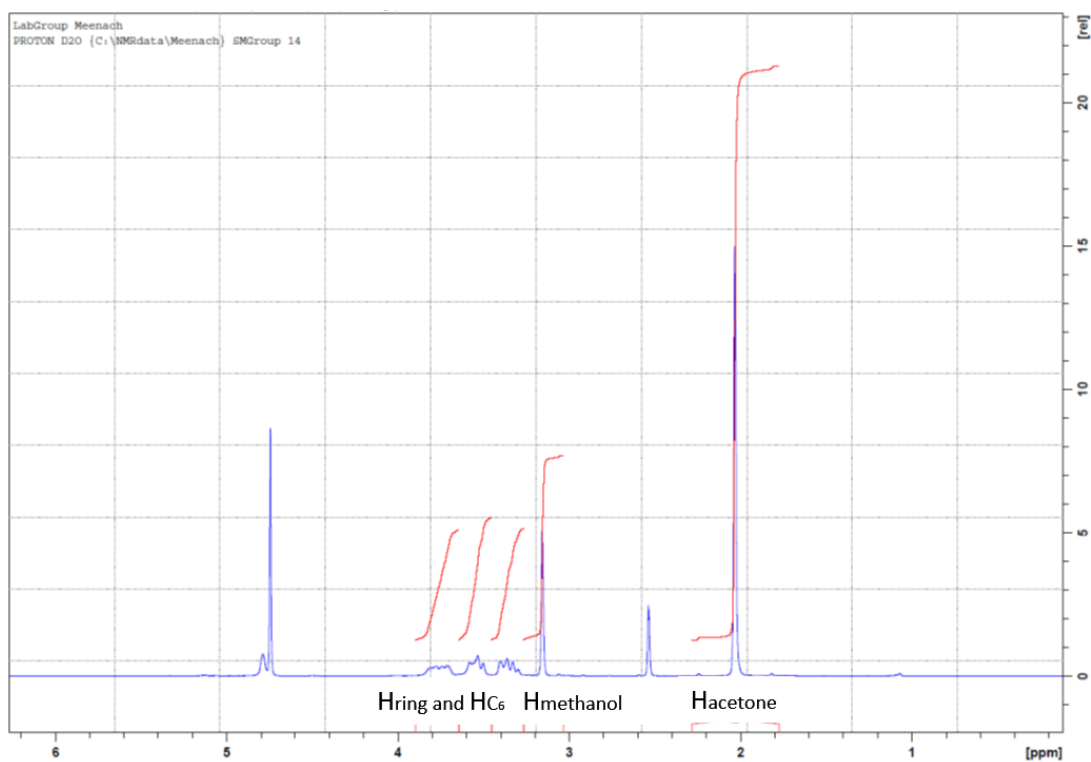
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Figure S1. Relationship between particle mass distribution and curcumin (CUR) distribution in all chambers of NGI for (A) CUR-nCmP and (B) CUR-MP.



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Figure S2. NMR analysis of Ac-Dex where peaks using during analysis include 3.4-4.0 ppm for dextran (H_{ring} and H_{C_6}), 3.36 ppm for methanol, and 2.08 ppm for acetone.

Cyclic acetal coverage (CAC) and total conversion of -OH group were calculated by the following equations:

$$\text{Normalization factor (NF)} = \frac{\text{Total area of 3 dextran peaks}}{6}$$

$$\text{Methanol per glucose} = \frac{\text{Methanol Peak Area}}{3 \times \text{NF}}$$

912

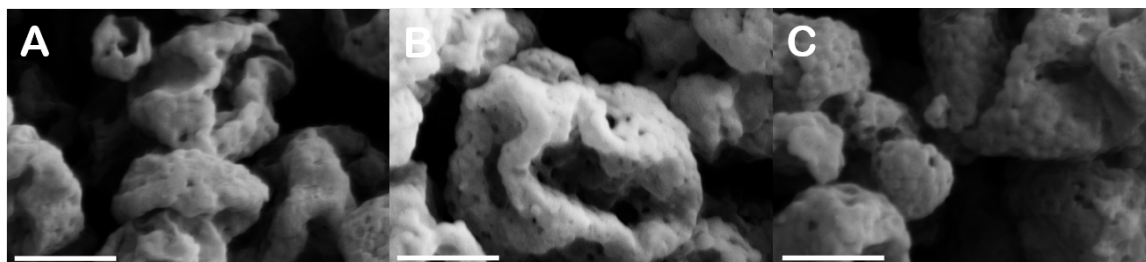
$$\text{Acetone per glucose} = \frac{\text{Acetone Peak Area}}{6 \times \text{NF}}$$

$$\text{Cyclic acetal coverage (CAC)} = (\text{Acetone per glucose} - \text{Methanol per glucose}) \times 100\%$$

$$\text{Total conversion of } -\text{OH groups} = \frac{(2 \times \text{Acetone per glucose} - \text{Methanol per glucose})}{3} \times 100\%$$

913

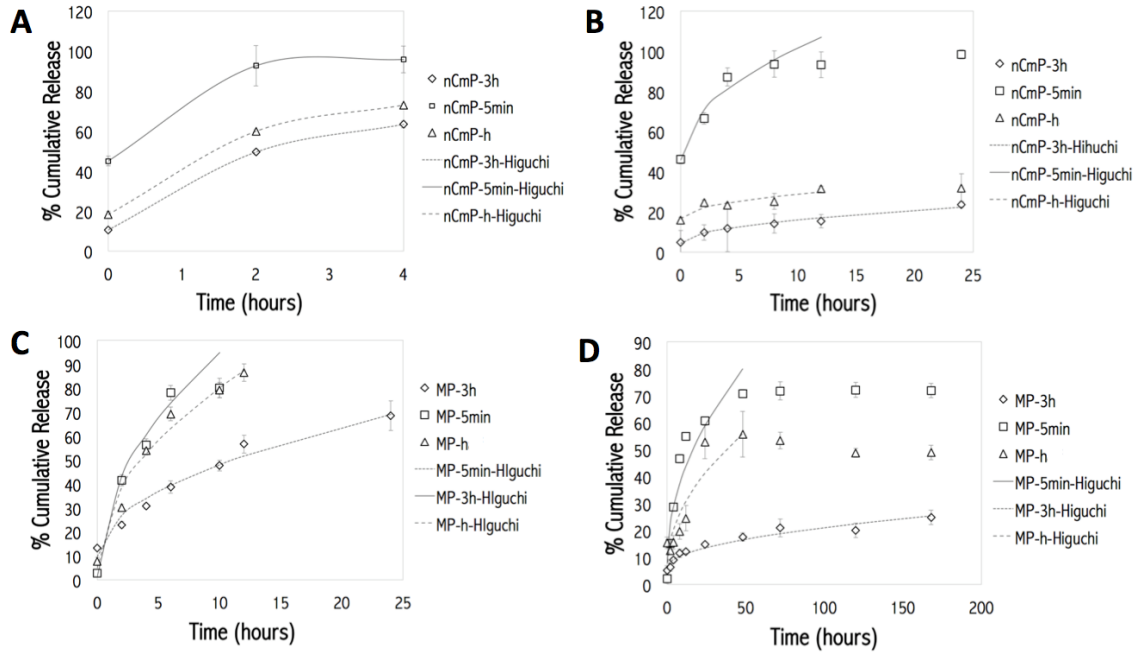
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916 **Figure S3.** Zoomed in images of CUR-nCmP including: (A) CUR nCmP-5min, (B) CUR
917 nCmP-h, (C) CUR nCmP-3h. Scale bar = 2 μm .

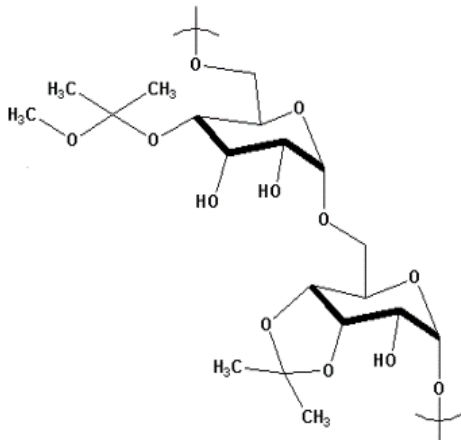
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920 **Figure S4.** Original data and fitted curves of *in vitro* drug release profiles for curcumin
 921 (CUR) nCmP (A and B) and MP systems (C and D) including CUR nCmP-5min, CUR
 922 nCmP-h, CUR nCmP-3h, CUR MP-5min, CUR MP-h, and CUR MP-3h at pH = 5 (A and
 923 C) and pH = 7.4 (B and D).

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926 **Figure S5.** Structure of acetalated dextran (Ac-Dex).

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