

## Potential to Use Sorghum Brewers Spent Grains as a Boiler Fuel

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The potential of using sorghum brewers spent grain (BSG) was examined for the production of bioelectricity. A local brewery company, with a production capacity of 24 tons per day of sorghum brewers spent grain as biomass waste, was used as a source of boiler fuel. After a full proximate analysis, the sorghum brewers spent grain had an average calorific value of 12.6 MJ/kg whilst coal had 19.9 MJ/kg. In addition, the BSG had a fixed carbon content of 41.6%. This indicated that it was feasible to generate electricity using sorghum brewers spent grain as a source of fuel just like coal; however the moisture content of the BSG must be controlled at minimum levels to attain high calorific values. An assumed feed rate of 1100 kg/h BSG being fed, operation at 86% efficiency, maximum pressure of 9 bars, and a steam output of 1689 kg/h were designed to supply a one megawatt (MW) turbine generator. An economic analysis was done with a total investment cost of USD\$ 3.4 million, a payback period of 3.7 years, and a return on investment of 27.4%. Sorghum BSG can be provided as an alternative source of bioelectricity for the brewery industry.

**Keywords:** Bioelectricity; Brewers spent grains; Direct combustion; Economic analyses

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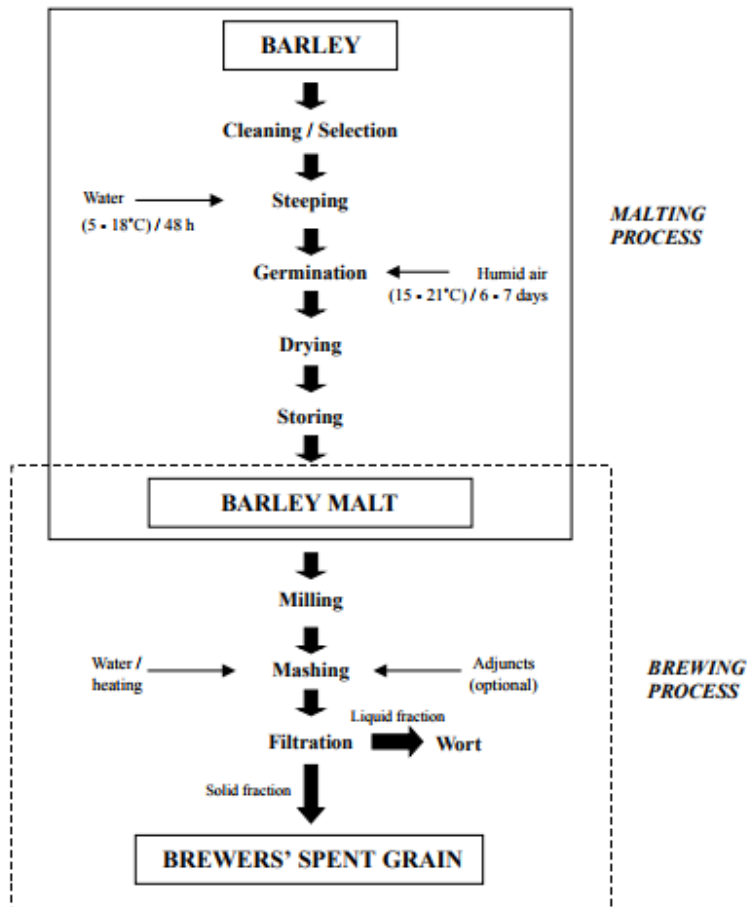
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### INTRODUCTION

Electricity is an important aspect of every nation's industrial growth and the economic development of any nation worldwide (Mbohwa, 2003; Mbohwa and Fukuda, 2003). A study by Attigah and Mayer-Tasch (2013) indicated that there is a strong correlation between reliable access to electricity and the overall productivity of an industry. This means that erratic electricity supplies often result in poor productivity indices. Hence there is a strong need for a constant and reliable electricity supply in any industry worldwide and particularly in developing countries like Zimbabwe. Due to the increased interest in the increased use of biomass in bio energy, there is need to explore alternative route for electricity generation, and brewers spent grains presents such an opportunity (Olagire 2012).

Conversely, the brewery industry is generating brewers spent grain (BSG) that has the potential for conversion into energy (Mussato *et al.* 2006; Weger *et al.* 2014; Buffington 2014). Huge amounts of brewers' waste are generated on a daily basis, and they contribute to about 85% of the bio waste produced, and this can end up at the landfills causing waste management problems (Mussato *et al.* 2006; Aliyu and Bala 2011; Olajire 2012). BSG being a lignocelluloses material contains 17% cellulose, 28% lignin, and 2% non-cellulosic materials, which are mainly polysaccharides (Mussato *et al.* 2006; Buffington 2014). Figure 1 shows the BSG generation process in the brewing industry.

52



53  
54 **Fig. 1.** BSG generation process from the brewery process (Mussato *et al.* 2006)  
55

56 Energy can be harnessed from the BSG either through combustion, anaerobic  
57 digestion, or gasification (IRENA 2012). BSG can also be a source of various energy  
58 including bioethanol, biogas, syngas, and biomass briquettes (Mussato *et al.* 2006). Figure  
59 2 shows a summary of the brewing process and potential uses of the BSG in bio energy  
60 generation.

61 In Zimbabwe, electricity is generated commercially through hydropower and  
62 thermal power. Zimbabwe has one hydropower station in Kariba, which has an installed  
63 capacity of 750 MW, but it is churning out **only** 694 MW. Four thermal power stations in  
64 Munyati, Bulawayo, Hwange, and Harare have a joint capacity of 1190 MW, but they are  
65 **producing just** 763 MW, giving a national total of 1457 MW against a **nominal** national  
66 capacity of 1940 MW. Electricity tariff comparative studies within the Southern African  
67 Development Community (SADC) region show that the Zimbabwe Electricity Supply  
68 Authority (ZESA) electricity tariffs (at around 9.86 US cents/KWh) are lower than those  
69 for Namibia (17.00 US cents /KWh) and Swaziland (10.30 US cents /KWh), while they  
70 are generally higher, as compared to information given by Briceño-Garmendia and  
71 Shkaratan (2011), for other SADC member states.  
72



## 104 **Methods**

105 The physicochemical characteristics of the BSG and the coal (total moisture on  
106 a dry basis, ash content, volatile matter, fixed carbon and calorific value) were  
107 measured in triplicate, and the variation was compared using histograms. A sensitivity  
108 analysis on the impact of varying moisture content of the BSG was done based on the  
109 assumption that each of the parameters interacted linearly. During the sensitivity  
110 analysis, moisture content values of up to 60% were considered using correlations  
111 reported in literature on the relationship between moisture content and the calorific  
112 value.

113

### 114 *Moisture content determination*

115 A Memmert UF55 moisture oven (Mermmet, Germany) was used to determine the  
116 moisture content of the brewery spent grains. The classic oven method of moisture  
117 determination uses the principle of calculating the percentage of weight loss of a sample after  
118 drying and assuming it to have been the percentage moisture content (Sanni and Fakunle,  
119 2016). For moisture determination, the Memmert UF55 oven was set at  $105 \pm 5$  °C using a  
120 multifunctional digital PID- microprocessor controller with a color display. The system uses  
121 a quiet air turbine to force air circulation within the oven so that there is an even temperature  
122 distribution within the oven. Its safety features are the presence of an oven temperature  
123 monitor that switches off heating when temperatures rise approximately 200 °C above the  
124 nominal temperature

125 The moisture content was determined in accordance with Eq. 1,

126

$$127 \text{Moisture content (\%)} = (M_2 - M_3) / (M_2 - M_1) \times 100 \quad (1)$$

128

129 where  $M_1$  is the mass of the empty dish (g),  $M_2$  is the mass of the dish + the wet spent grains  
130 sample (g), and  $M_3$  is mass of the dish + the dried spent grains sample (g).

131

### 132 *Calorific heat value determination*

133 The calorific values of a fuel express the amount of energy released during the  
134 complete combustion of a mass unit of a given fuel (Celaya *et al.* 2015). A Nenus Instruments  
135 (India) bomb calorimeter was used for the experiments, which is a device that measures heat  
136 energy transferred (enthalpy change) between products and reactants at 25 °C. Briggs *et al.*  
137 (1996) stated that the bomb calorimeter uses the concept of igniting the sample in a constant  
138 volume container (jacket) in water until complete combustion is achieved. The sample is  
139 ignited and the difference between the maximum and minimum temperatures of the water  
140 was used to compute the gross calorific value.

141 The brewery spent grains sample was ground to powder, and 1.00 g was measured  
142 using an analytical balance. The sample was placed in a bomb calorimeter for firing and the  
143 results were displayed. The gross calorific value displayed was then used to calculate the net  
144 calorific value.

145

### 146 *Volatile matter determination*

147 Volatile matter is any portion of the biomass that is released as volatile gases when  
148 heated to temperatures around 400 °C. The volatile matter content represents the percentage  
149 of the biomass that volatilizes as a gas; normally high volatile matter content indicates a high  
150 amount of the biomass (Celaya *et al.* 2015).

151 The sample was first oven dried as part of the sample preparation. Approximately 2  
152 g of the sample was weighed in a porcelain crucible and put in a muffle furnace at 550 °C

153 for 10 min. Next, it was cooled in a desiccator, and then weighed, and the percentage volatile  
154 matter was calculated as shown in Eq. 2,

$$156 \quad \text{Volatile matter (\%)} = 100 \times (A - B) / A \quad (2)$$

157  
158 where  $A$  is the mass of the oven dried sample (g) and  $B$  is the mass of the sample after 10  
159 min in the furnace (g).

160

#### 161 *Fixed carbon content determination*

162 The amount of fixed carbon in a sample gives a rough estimate of the calorific value  
163 of a substance. This is because carbon generates most of the heat during burning, so there is  
164 a higher probability that a sample with high carbon content would have a high calorific value.  
165 The determination of the ash content is shown in Eq. 3,

$$167 \quad \text{Fixed carbon content (\%)} = (M_3 - M_1) / (M_2 - M_1) \times 100 \quad (3)$$

168  
169 where  $M_1$  is mass of the empty crucible (g),  $M_2$  is the mass of the crucible + brewery spent  
170 grain sample (g), and  $M_3$  is the mass of the crucible + ash (g).

171

#### 172 *Ash content determination*

173 Ash is an inorganic material bound in the physical structure of the biomass that is left  
174 as a residue after dry oxidation at 575 °C (Senthilkumar *et al.* 2010). Its accumulation on  
175 heat transfer surfaces in boilers, and internal surfaces in gasifiers, normally causes an  
176 acceleration in the corrosion rate of such equipment and also reduces its efficiency, hence  
177 the need for an ash analysis. The determination of the ash content is shown in Eq. 4,

$$179 \quad \text{Ash content (\%)} = (M_3 - M_1) / (M_2 - M_1) \times 100 \quad (4)$$

180  
181 where  $M_1$  is the mass of the empty crucible (g),  $M_2$  is the mass of the crucible + brewery  
182 spent grain sample (g), and  $M_3$  is mass of the crucible + ash (g).

183

#### 184 *Economic assessment methodology*

185 A local brewery company with a production capacity of 24 tons per day of sorghum  
186 BSG as waste was used as a source of boiler fuel for this study and considered for an  
187 economic assessment. The cash discounted methodology, which is based on the total costs  
188 from the process, was used determining the economic feasibility of generating  
189 bioelectricity from BSG.

190

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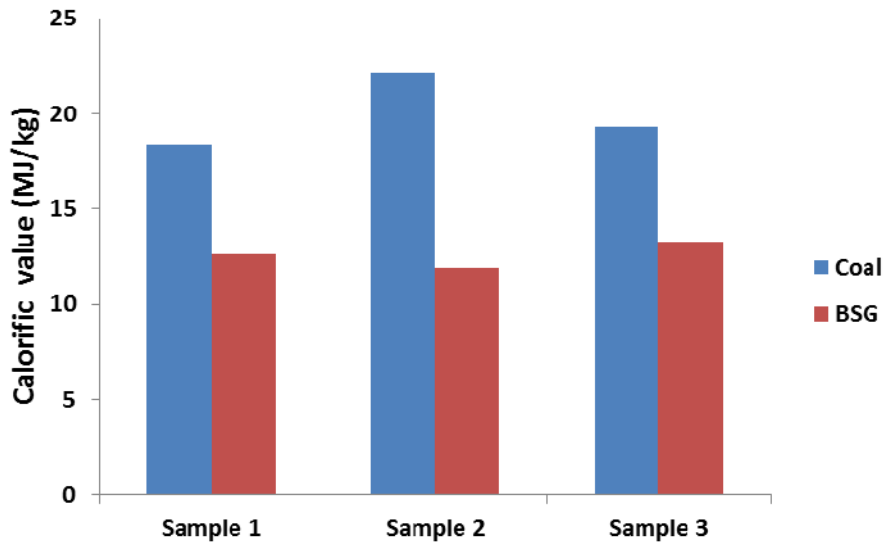
## 192 **RESULTS AND DISCUSSION**

193

### 194 **Potential to Use Brewers Spent Grains as a Combustion Fuel**

#### 195 *Calorific value*

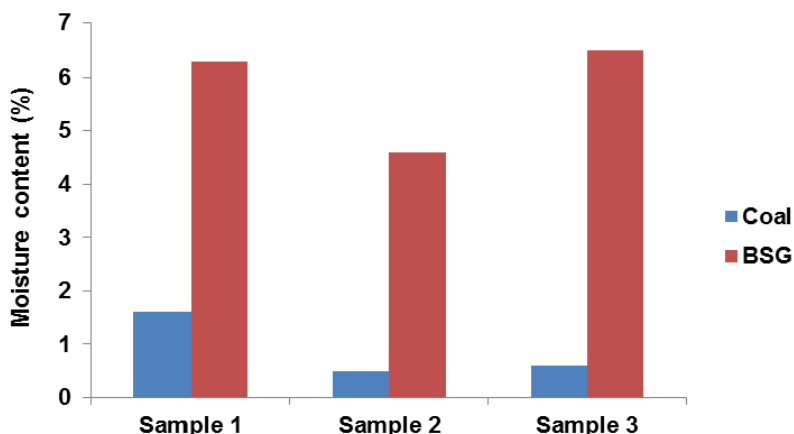
196 The analysis of the BSG's physicochemical characteristics indicated that the BSG  
197 had an average calorific value of 12.6±0.7 MJ/kg, which was approximately 37% less  
198 than that of coal, which was 19.9 ± 1.9 MJ/kg (Fig. 3). Irrespective of the fact that the  
199 calorific value of BSG was lower, this indicated that the BSG could be thermally  
200 converted into electricity (Veringa 2014). The results were compared to coal to check the  
201 feasibility of using BSG in bioelectricity generation or its potential to be used as a  
202 combustion fuel.



203  
204 **Fig. 3.** Comparison of the BSG and coal calorific values  
205

206 *Moisture content*

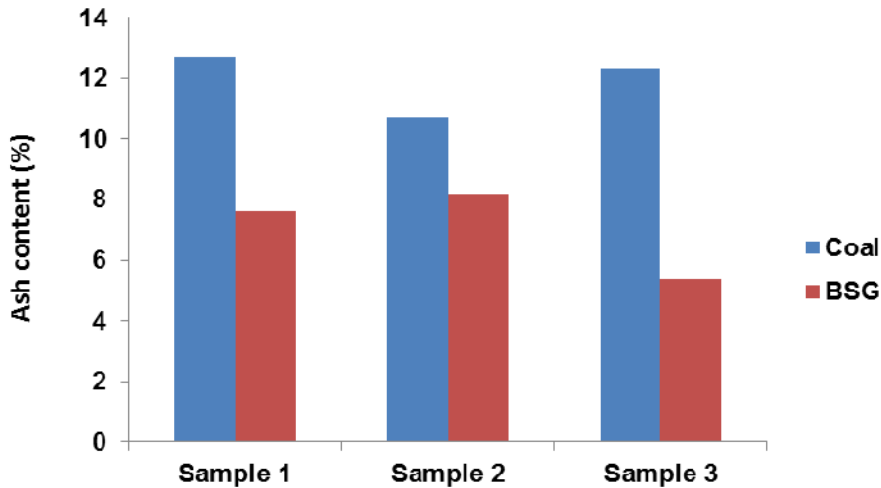
207 The average moisture content ( $5.8 \pm 1.0\%$ ) in the BSG was 84% as compared to the  
208 standard coal used for boiler combustion and electricity generation ( $0.9 \pm 0.6\%$ ), as indicated  
209 in Fig. 4. High moisture content values in the BSG are attributed to the fact that the brewing  
210 process is a wet process, and despite the BSG being sun dried for a while, the moisture  
211 content values were still very high. A high moisture content of the BSG has potential to  
212 lower the calorific value of the BSG, limiting its potential for being used in boiler  
213 combustion or bio electricity generation. The BSG must then be further dried using a rotary  
214 drier as proposed by Sani and Fakunle (2016) when they also observed moisture content  
215 values of 8.16 to 9.1% in spent brewers' grains.  
216



217  
218 **Fig. 4.** Comparison of the BSG and coal moisture content  
219  
220

221 *Ash content*

222 The average ash content in the BSG ( $11.9\pm 1.1\%$ ) was 40% as compared to the  
223 standard coal ( $7.1\pm 1.5\%$ ) used to fire the boilers and generate electricity (Fig. 5). The  
224 ash content in this study was on the higher side compared to values in literature as  
225 earlier reported by other researchers with values between 3 and 5% (Dong and Ogle  
226 2003; Senthilkumar *et al.* 2010). High ash content in the feedstock for combustion or  
227 electricity generation has a tendency to lower the energy efficiency as well as the  
228 calorific value.

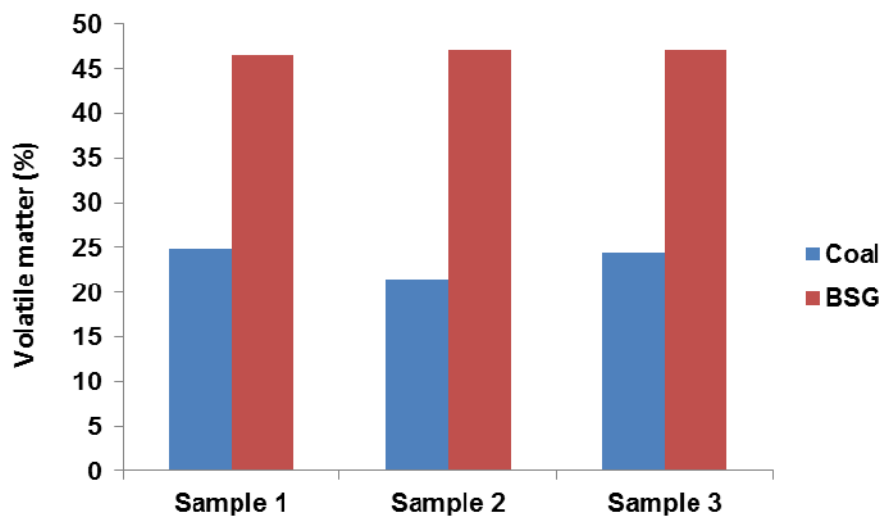


229  
230 **Fig. 5.** Comparison of the BSG and coal ash content

231  
232 *Volatile matter content*

233 The volatile matter in the BSG ( $47.0\pm 0.3\%$ ) was almost 50% higher as  
234 compared to the standard coal ( $23.6\pm 1.9\%$ ) used for boiler energy combustion and  
235 electricity generation (Fig. 6).

236



237  
238 **Fig. 6.** Comparison of the BSG and coal volatile content

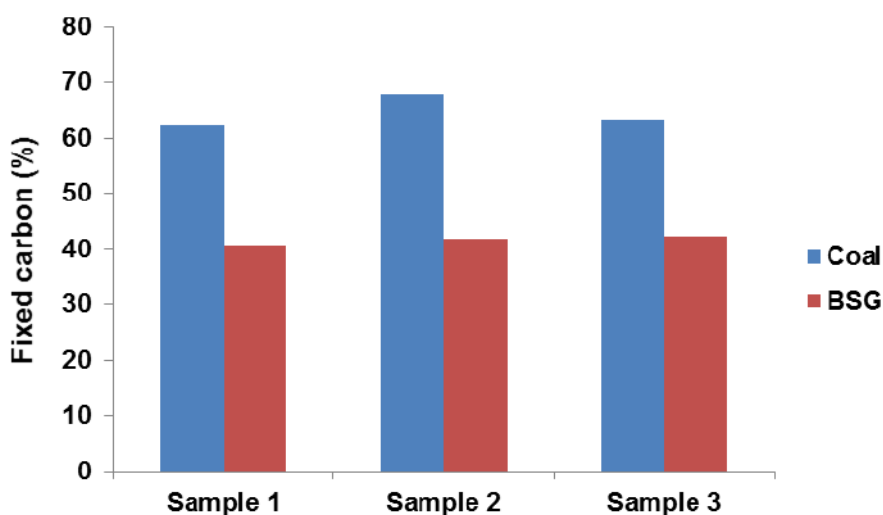
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240 The higher volatile content in the BSG was attributed to the high volatiles that  
 241 are available in the BSG, which results in lower calorific values as compared to coal  
 242 (Celaya *et al.* 2015). The high volatiles can be reduced by carbonizing the BSG to bio  
 243 char which can be pelletized to a coal like fuel effectively increasing the calorific value  
 244 of the BSG (Celaya *et al.* 2015).

245

#### 246 *Fixed carbon content*

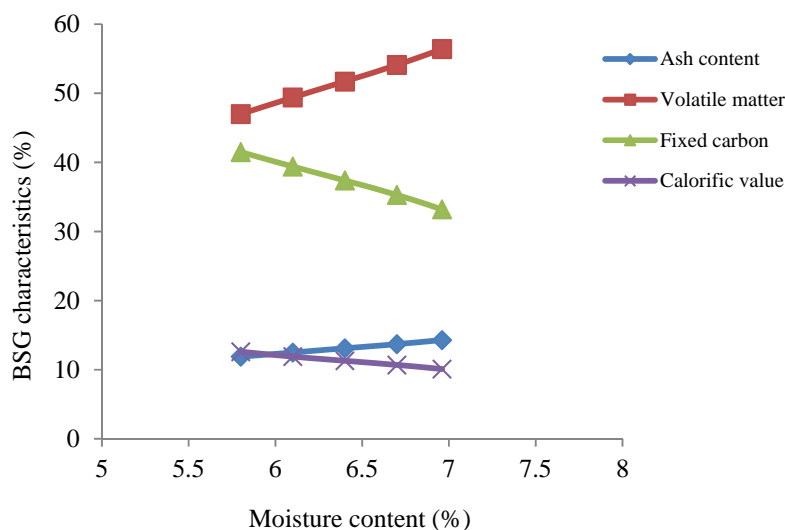
247 The fixed carbon content in the BSG ( $41.5 \pm 0.9\%$ ) was 36% lower as compared  
 248 to the fixed carbon content in the standard coal ( $64.5 \pm 3.0\%$ ), as indicated in Fig 7. The  
 249 fixed value observed in this study was slightly higher in comparison to a value of 35.6%  
 250 that was reported by Khidzir *et al.* (2010). The fixed carbon content is directly related  
 251 to the calorific value of a material. The fixed carbon of the BSG can probably be  
 252 increased through carbonization and then pelletizing to bio pellets (Celaya *et al.* 2015).  
 253



254

255 **Fig. 7.** Comparison of the BSG and coal fixed carbon content

256



257

258 **Fig. 8.** Summary of the BSG physicochemical properties against moisture changes



259 A sensitivity analysis on the effect of the moisture content on the BSG  
 260 physicochemical parameters indicated that moisture content is a critical parameter in the  
 261 potential use of BSG as a boiler fuel or electricity generation. Decreasing the moisture  
 262 content of the BSG to approximately 4.6% results in increased BSG calorific values up to  
 263 15.1 MJ/kg (Fig. 8). The increase in calorific value is attributed to an increase in the fixed  
 264 carbon content (49.8%) and a decrease in both ash content and the volatile matter (Fig. 8).  
 265 The converse is also true for an increase in the BSG moisture content, the calorific value  
 266 and the fixed carbon will significantly decrease.

267

### 268 Effect of Higher Moisture Content Values in the BSG

269 From this study, it can be assumed that moisture content has the greatest effect on  
 270 all the other BSG physicochemical properties and its potential to be used as a solid fuel.  
 271 The increase in the moisture content results in increased ash content and volatile matter,  
 272 which ultimately cause a decrease in the calorific value and fixed carbon content of the  
 273 BSG. Most BSG is not dried post the process and can have moisture contents as high as  
 274 60%; this has negative effects on the potential of using BSG as a solid fuel. Dewatering  
 275 and drying techniques must be employed to realise this potential. Several correlation on  
 276 the effect of moisture content on the biomass calorific value were adopted from the  
 277 literature, and the predicted effect of moisture content on the BSG calorific value quantified  
 278 in according to correlations 1, 2 (Ebeling and Jenkins 1985) and correlation 3 (Sheng and  
 279 Azevedo 2005).

280

281 Correlation 1: Calorific value = 20.067 - 0.234Ash content

282

283 Correlation 2: Calorific value = 26.601 - 0.304Ash content - 0.082Volatile matter

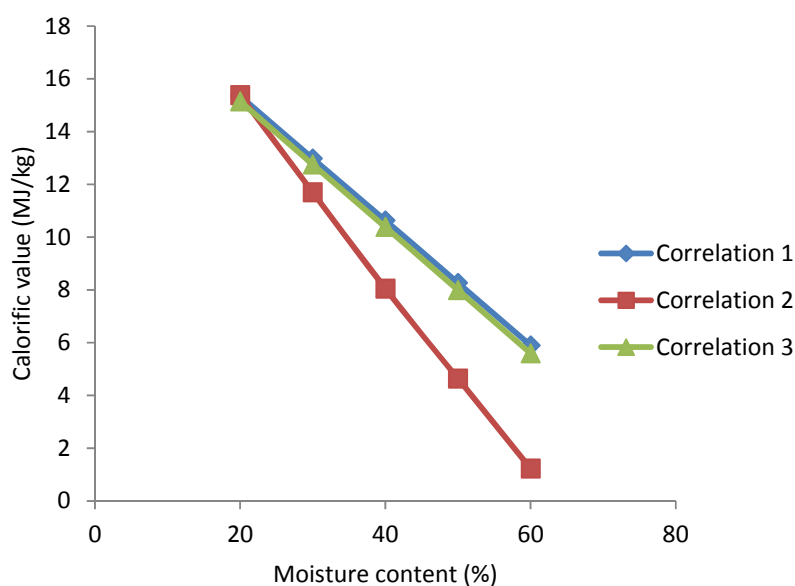
284

285 Correlation 3: Calorific value = 19.914 - 0.2324Ash content

286

287 All the three correlations indicated that as the moisture content increases up to 60%, the  
 288 calorific value also will significantly decrease, as indicated in Fig 9.

289



290

291

**Fig. 9.** Effect of moisture content increase on the BSG calorific value

## 292 Bioelectricity Production Process Design

293 An assumed feed rate of 1100 kg/h of sorghum BSG biomass feedstock, at 6%  
 294 moisture and a calorific value of 12.6 MJ/kg, was fed into a 1623 m<sup>3</sup> water capacity  
 295 biomass boiler unit producing a steam output of 1689 kg/h steam at a temperature of 573  
 296 °K and a pressure of 9 bars. As the superheated steam exited the boiler, it was directed to  
 297 the turbine unit, where a turning effect was induced on the turbine blades by the pressure  
 298 and velocity of the steam as mechanical shaft energy. The turbine blades, which were  
 299 connected to a turbo alternator electricity generator unit, then induced a rotational motion  
 300 on the series of coils in a magnetic field housed in the turbo alternator electricity generator  
 301 unit. This resulted in the formation of a voltage, using Faraday's law of electromagnetic  
 302 induction. The electricity generator unit has an output of 1 MW of electricity. The  
 303 vaporized steam, now at 343 °K, was then pumped back into the boiler unit using a  
 304 centrifugal pump. The electricity generated from the BSG can be utilized for refrigeration,  
 305 packaging, compressed air generation as well as used in the brew house and boiler house  
 306

## 307 Pre-Economic Analysis

308 This section clearly evaluated the cost of the project by using a pre-economic  
 309 feasibility study. Thus, the cost method that was used was the Lang factorial method. The  
 310 Lang factorial method is attributed to Lang (1948), as cited in Peters and Timmerhaus (1993),  
 311 and it expresses the fixed capital cost of the project as a function of the total purchase  
 312 equipment cost. A summary of the economic factors considered is given in Table 1.

313 The assumed feed rate of 1100 kg/h of BSG being fed, operating at 86% efficiency,  
 314 maximum pressure of 9 bars, and steam output of 1689 kg/h was designed to supply a one  
 315 megawatt turbine generator. An economic analysis was done with a total investment cost  
 316 of USD\$ 3.4 million, a payback period of 3.7 years, and a return on investment of 27.4%,  
 317 as shown in Table 1. The shorter payback period and return on investment are an indication  
 318 that it is feasible to use BSG either as a boiler fuel or a raw material for bioelectricity  
 319 generation. The economic indicators can also be greatly improved if the physicochemical  
 320 characteristics of the BSG are improved mainly the calorific value and the fixed carbon  
 321 content.  
 322

323 **Table 1.** Summary of Economic Analysis

Item	Cost (US\$)
Total purchase cost of equipment	841,144.00
Physical plant cost	2,186,974.00
Fixed capital	3,061,764.00
Working capital	306,176.40
Total investment cost	3,367,941.00
Fixed costs	201,106.00
Variable costs	817,581.00
Annual operating costs	1,018,687.00
Rate of return on investment	27.4%
Payback period	3.7 years
Breakeven point	780 KW

**CONCLUSIONS**

1. Sorghum brewers spent grains' physicochemical characteristics, as obtained in dry form from the subject brewery, were almost similar to that of coal. However, the moisture content of the BSG can be further decreased by further dewatering and drying before using as a fuel for increasing the calorific value of the BSG.
2. Sorghum brewers spent grains can be used as a boiler combustion fuel and possibly for bio electricity generation due to their calorific value
3. There is economic potential to generate bioelectricity using sorghum brewers spent grain as a source of fuel.
4. The BSG's calorific value can be enhanced by carbonizing the BSG to bio pellets as a future study which allows removal of volatile matter and increase of the fixed carbon.

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