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25 detecting both minor changes in effluent quality and issues with treatment process  
26 performance.

27 **Keywords:** real-time monitoring, fluorescence spectroscopy, wastewater treatment  
28 plant, organic matter

## 29 **Introduction**

30 The most significant energy usage in wastewater treatment plants (WwTPs) arises from  
31 the vigorous aeration of settled sewage in the activated sludge process (ASP, an aerobic  
32 system involving entrainment of air for microbial degradation of organic matter - OM). This  
33 process contributes to over 55% of the energy budget associated with wastewater treatment  
34 (Environmental Knowledge Transfer Network 2008). Due to the diurnal variations in  
35 wastewater flow and load, and lack of rapid and reliable effluent monitoring (Bourgeois et al.  
36 2001; Jouanneau et al. 2014), treatment plants often over-aerate the settled sewage to be  
37 certain of achieving regulatory compliance, leading to excessive energy consumption and  
38 unnecessary operating costs.

39 In the past two decades, several studies have demonstrated, through off-line monitoring  
40 experiments, the potential of fluorescence spectroscopy for treatment process control (Ahmad  
41 and Reynolds 1995; Bridgeman et al. 2013; Cohen et al. 2014; Murphy et al. 2011; Ou et al.  
42 2014; Singh et al. 2012, 2015; Tartakovsky et al. 1996). The technique offers practical  
43 advantages, such as: fast measurements, cost-effectiveness, lack of need for reagents, and  
44 high sensitivity (Coble et al. 1990; Yang et al. 2015). However, no on-line fluorescence  
45 monitoring studies have been performed at WwTPs. To date, Galinha et al. (2011) have  
46 undertaken the only real-time monitoring study of wastewater on a pilot scale membrane  
47 bioreactor system to predict performance parameters. They found that fluorescence was able  
48 to describe influent and effluent chemical oxygen demand (COD), but could not predict other  
49 performance parameters. Singh et al. (2015) obtained promising results from an online

50 monitoring study on two water recycling sites. Using a single-wavelength fluorescence  
51 sensor, they were able to prove the robustness of the technique in detecting reverse osmosis  
52 membrane fouling and integrity. Moreover, Singh et al. (2015) showed that the sensor was  
53 sufficiently sensitive to identify underperformance issues. Real-time monitoring of treated  
54 wastewater at WwTPs has been hampered by numerous factors that can interfere with the  
55 fluorescence signal: fouling, pH, inner filter effects, temperature and metal ion presence  
56 (Henderson et al. 2009; Reynolds 2002). To counteract these issues, regular, time consuming  
57 cleaning of contact surfaces or subsequent data corrections are recommended.

58 Here, we report the first *in-situ* and on-line monitoring of treated wastewater, using  
59 three fluorescence portable devices, to test the robustness of the technique and the hypothesis  
60 that we can obtain valuable results from a 1-month monitoring experiment without major  
61 device cleaning or subsequent data correction. In addition, a laboratory scale activated sludge  
62 system was constructed to establish, before the in-situ experiment, the relationship between  
63 fluorescence and BOD.

#### 64 **Methodology**

65 The real-time experiment was undertaken for 29 days, from the 10<sup>th</sup> of August until the  
66 7<sup>th</sup> of September 2015, at a WwTP located in the West Midlands, UK. The treatment plant  
67 serves a region of 450,000 population equivalent and collects on average 120 ML/day of  
68 wastewater from various types of sources: household, surface runoff, industrial (soluble oil,  
69 chemical laboratory waste, engine cleaning, painting wastes, laundering, meat processing,  
70 slaughterhouse, print waste etc.). In addition, the WwTP receives activated sludge mixed  
71 liquor from a nearby sewage sludge facility at periodic intervals. During the experiment,  
72 liquor was pumped, before noon, on the: 13<sup>th</sup>, 15<sup>th</sup>, 21<sup>st</sup> and 24<sup>th</sup> of August 2015.

73 The treatment process train consists of coarse and fine screens at the inlet, six primary  
74 sedimentation tanks, 3 activated sludge reactors and 12 final settlement tanks. The primary

75 treatment step removes solids as well as oil and grease, after which, the remaining wastewater  
76 is delivered to the ASP, comprising three basic components: 1) a reactor in which  
77 microorganisms are kept in suspension, aerated, and in contact with the wastewater they are  
78 treating; 2) liquid-solid separation; and 3) a sludge recycling system for returning activated  
79 sludge back to the beginning of the process.

## 80 ***Real-time monitoring***

### 81 *Laboratory scale ASP experiment*

82 Before the in-situ measurements were undertaken, a laboratory scale ASP was  
83 constructed to check the feasibility of the method and the relationship with BOD. Settled  
84 sewage and returned activated sludge (RAS) were collected twice a week from the WwTP and  
85 stored at 4<sup>0</sup> C prior to use. The setup consisted of a feed primary tank (30 L volume), aeration  
86 tank (10 L volume) and final settling tank (4 L volume) (Fig. S1). The settled sewage was  
87 pumped into the aeration tank at a rate of 11 mL/min. Two aquarium air stones were inserted  
88 in the aeration tank to replicate the aeration process and two stirrers ensured a greater degree  
89 of mixing. A stirrer was inserted in the final settling tank to ensure settlement of the sludge  
90 flocs. The settled sludge was returned to the aeration tank via a peristaltic pump at a rate of 11  
91 mL/min. An average mixed liquor suspended solids (MLSS) concentration of 3,300 mg/l was  
92 maintained in the aeration tank. When the quantity of MLSS decreased, additional RAS was  
93 added without changing the volume of liquor in the aeration tank. The health and population  
94 of microorganisms in the activated sludge reactor were checked regularly via microscope. The  
95 experiment ran for six weeks and samples were collected daily for fluorescence, BOD<sub>5</sub>, COD  
96 and total organic carbon (TOC) analyses. Dissolved oxygen concentration and pH were  
97 monitored every 30 min in the ASP tank.

### 98 *In situ measurements*

99 Three portable fluorescence instruments were installed and left unattended at the WwTP

100 final effluent discharge point, before the discharge to the river. Specifically, these were two  
101 submersible probes (Cyclops 7, Turner Designs; EXO1 sonde, YSI Xylem) and a cuvette-  
102 based (DuoFluor; designed and manufactured at the University of Birmingham) (Bridgeman  
103 et al. 2015). The Cyclops 7 and EXO1 were inserted directly into the final effluent channel.  
104 Proprietary protective caps were placed over the two submersible sensors and they were not  
105 cleaned for the duration of the experiment. The sensors were also secured with ropes to  
106 prevent excessive movement caused by the fluid flow.

107 The cuvette-based DuoFluor device was installed in an adjacent shed for power  
108 connection and protection from rainfall (Fig. S2). The final effluent was pumped to the  
109 fluorimeter at a flow-rate of 340 mL/min. A mesh covered the pump end tube to prefilter the  
110 water and prevent debris from entering the cuvette. However, biofilm growth was observed  
111 with time on the cuvette walls and on the tubing. Consequently, the cuvette was washed (10  
112 % nitric acid) and rinsed with de-ionised water on a weekly basis, and the tubing was replaced  
113 after two weeks.

114 The measurement frequency was set at 15 min for all instruments. Cyclops 7 was  
115 initially set up to measure every 30 min, however the number of data points was insufficient  
116 to obtain an adequate assessment of water quality fluctuations. No problems occurred with the  
117 submersible devices. However, operation of the DuoFluor ceased one week before the end of  
118 the experiment due to power failure.

## 119 ***Measurements***

### 120 *Fluorescence peaks*

121 This study focused on specific fluorescence components, assigned to spectral regions T  
122 ( $\lambda_{\text{ex}}/\lambda_{\text{em}} - \sim 280 \text{ nm} / 350 \text{ nm}$ ) and C ( $\lambda_{\text{ex}}/\lambda_{\text{em}} - \sim 330 \text{ nm} / 425 \text{ nm}$ ), which can be used to  
123 assess the quality of wastewater (Carstea et al. 2016). Peak T is generally associated with  
124 living and dead cellular material and their exudates and indicates microbial activity

125 (Bridgeman et al. 2013). Peak T is also widely associated with material derived from  
126 anthropogenic activities (Yu et al. 2014). Several fluorophores could contribute to these  
127 regions (Carstea et al. 2016; Coble et al. 2014). Considering the variety of wastewater  
128 discharges received by the WwTP and the wavelengths used by the devices, the following  
129 components could fluoresce in the peak T region: lignins, aromatic hydrocarbons and indoles  
130 originating from domestic waste (partially degraded foods, undigested dietary fibre, toilet  
131 paper, proteins and peptides), petrochemical, pharmaceutical and paper industries. Peak C is  
132 defined as reduced quinone-like and was identified in OM from a wide variety of aquatic  
133 systems, especially those dominated by terrestrial and microbial inputs (Ishii and Boyer  
134 2012). Potential contributors to the fluorescence of peak C could be: lignin breakdown  
135 products, quinones, flavonoids, humic acids and fluorescent whitening agents (FWAs)  
136 originating from municipal wastewater (food, plants, microbes, fungi, laundry detergents,  
137 sanitary products, toilet paper and tissues) and paper making industry (Carstea et al. 2016). In  
138 a recent study, it was shown that the removal rates of peaks T and C correlated with the  
139 removal of pharmaceuticals, such as gemfibrozil, ibuprofen and naproxil, and with personal  
140 care products, such as triclosan or caffeine (Sgroi et al. 2016). Thus, the exact composition of  
141 fluorophores cannot be determined by the measurement of peaks T and C, however, these  
142 peaks are highly effective in showing the removal of wastewater OM. Apart from these two  
143 peaks, the common fluorescence regions reported for FWAs, at excitation wavelength 370 nm  
144 and 400 nm (Coble et al. 2014), were also considered, due to the proximity of EXO1  
145 excitation wavelength to one of the FWAs peaks. Past studies (Assaad et al. 2014; Chandler  
146 and Lerner 2015; Graham et al. 2015), proposed FWAs as indicators of human faecal  
147 contamination, sewer misconnections and landfill leachates.

#### 148 *Fluorescence measurements*

149 Fluorescence was measured with three portable fluorimeters. Cyclops 7 measures the

150 fluorescence intensity at the excitation / emission wavelengths of 285 nm / 350 ± 55 nm, with  
151 a limit detection range of 3 ppb to 5,000 ppb tryptophan standard. EXO1 sonde houses three  
152 sensors: fDOM (fluorescence dissolved OM), conductivity/temperature and pH. The fDOM  
153 sensor records at 365 ± 5 / 480 ± 4 nm (excitation / emission wavelength pair). The detection  
154 range is 0 ppb - 300 ppb quinine sulphate units. DuoFluor is capable of detecting fluorescence  
155 in real time at 280/350 nm (Peak T) with minimum limit of detection 1.5 ppb of L-tryptophan  
156 and at 330/425 nm (Peak C) with minimum limit of detection 1.5 ppb of quinine sulphate. The  
157 linearity between the portable devices and a benchtop spectrofluorimeter (Varian Cary  
158 Eclipse) was checked with a series of dilutions of L-tryptophan and quinine sulphate  
159 standards (Fig. S3). L-tryptophan solutions were varied between 50 ppb and 250 ppb, while  
160 quinine sulphate was prepared in concentrations of 10 ppb to 700 ppb. The linearity of the  
161 EXO1 was checked up to 400 ppb of quinine sulphate, as recommended by the manufacturer.  
162 R<sup>2</sup> values exceeded 0.98 for all instruments.

163 Excitation-emission matrices were produced using the benchtop spectrofluorimeter: by  
164 scanning excitation wavelengths from 200 to 400 nm in 5 nm steps, and detecting the emitted  
165 fluorescence in 2 nm steps between 280 and 500 nm. Excitation and emission slit widths were  
166 set to 5 nm. Instrument stability was checked by recording the Raman values (at excitation  
167 wavelength 348 nm and emission wavelength 395 nm) before each set of measurements. The  
168 average Raman value was 9.94 a.u. with a standard deviation of 0.24. The fluorescence peaks  
169 were extracted using the peak-picking method, in accordance with previous studies (Coble et  
170 al. 2014).

#### 171 *Ancillary analyses*

172 Rainfall, temperature, total phosphorus, iron, ammonia and suspended solids were  
173 measured daily on-site at the WwTP outfall. In addition, samples were collected twice a week  
174 for BOD<sub>5</sub>, COD, TOC, nitrate and turbidity (Table S1). Low values were observed for all



175 parameters, indicating effective treatment of the wastewater. BOD<sub>5</sub> was measured based on  
176 the standard method for wastewater testing using a HQ40d portable meter (Hach) with an  
177 IntelliCAL LBOD101 LDO probe. The accuracy of the BOD<sub>5</sub> measurements was checked  
178 using a 300 mg/L glucose-glutamic acid standard, and a coefficient of variation of 3.6 % was  
179 observed. COD and nitrate were measured using a DR890 Hach colorimeter, following  
180 standard procedures: *viz.* Reactor Digestion Method (USEPA) for COD, and Chromophoric  
181 Acid Method (high range, Test 'N Tube) for water and wastewater for nitrate. Turbidity was  
182 recorded using a Hach 2100N turbidimeter. TOC measurements were undertaken using a  
183 Shimadzu TOC-Vcpn analyser, using the non-purgeable organic carbon determination  
184 method.

## 185 **Results and discussion**

### 186 ***Laboratory scale ASP***

187 Before the *in-situ* study, a laboratory-based experiment was undertaken replicating the  
188 ASP to establish the relationship with BOD and to determine the potential of using  
189 fluorescence spectroscopy for real-time measurements. WwTPs measure BOD on a daily  
190 basis; however, a qualitative method is used, which provides ranges of BOD values and the  
191 result cannot be compared with fluorescence intensity. The regulatory 5-day BOD test is  
192 performed only once per month. Therefore, the laboratory scale ASP was designed to identify  
193 this fluorescence/BOD relationship.

194 Figure 1 shows the fluorescence intensity of peaks T and C measured with the benchtop  
195 fluorimeter plotted against BOD. The Kendall correlation coefficients with BOD<sub>5</sub> are: 0.71  
196 ( $p < 0.001$  – 2-tailed test of significance,  $N=87$ ) for peak T; and 0.43 ( $p < 0.001$  – 2-tailed test of  
197 significance,  $N=87$ ) for peak C. The correlation between BOD and fluorescence is  
198 challenging to identify at low BOD concentrations (Hudson et al. 2008), thus the values  
199 quoted above were determined using a combination of data from final effluent and settled

200 sewage samples. An improved correlation was observed for BOD with peak T compared to  
201 the peak C/BOD relationship was reported in other studies (Bridgeman et al. 2013; Hudson et  
202 al. 2007). The various types of fluorophores that contribute to the peaks T and C fluorescence  
203 region explain the difference in correlation values. In addition, Reynolds (2002) found that  
204 peak T is more representative for the biodegradable organic matter than peak C. Considering  
205 the strong correlation between peak T and BOD, obtained in this study, and the relationship  
206 reported in other studies (Bridgeman et al. 2013; Carstea et al. 2016; Coble et al. 2014;  
207 Hudson et al. 2008), it is clear that peak T fluorescence can detect some of the components  
208 measured with BOD. Furthermore, fluorescence spectroscopy provides more information on  
209 the nature of OM than the BOD test does and may be used as an independent indicator test for  
210 the presence of bioavailable OM (Hudson et al. 2008).

211 Similar relationships were obtained between fluorescence and COD and TOC. The  
212 Kendall correlation coefficients with COD are: 0.72 ( $p < 0.001$  – 2-tailed test of significance,  
213  $N=87$ ) for peak T; and 0.44 ( $p < 0.001$  – 2-tailed test of significance,  $N=87$ ) for peak C. While,  
214 the Kendall correlation coefficients with TOC are: 0.82 ( $p < 0.001$  – 2-tailed test of  
215 significance,  $N=81$ ) for peak T; and 0.49 ( $p < 0.001$  – 2-tailed test of significance,  $N=81$ ) for  
216 peak C. The good correlation between peak T and TOC may be attributed to the sugars and  
217 lignin (Baker 2002) degraded from sanitary products. However, the relationship between  
218 fluorescence peaks and BOD, TOC and COD varies depending on the ratio of fluorescent to  
219 non-fluorescent OM in a sample (Henderson et al. 2009).

#### 220 *In situ measurements*

221 Peaks T and C data provided by the 3 devices are shown in Figure 2. Kendall  
222 correlation analysis showed an association between EXO1 data and DuoFluor peaks T and C  
223 ( $R^2=0.49$  &  $0.48$ ,  $p < 0.001$ ), while Cyclops 7 data presented a slight correlation with the  
224 DuoFluor peak T ( $R^2=0.28$ ,  $p < 0.001$ ) (Table 1). The analysis also revealed that the EXO1 and

225 the DuoFluor data correlated with peaks T, C and FWAs measured with the Varian benchtop  
226 spectrofluorimeter. The variation in correlation coefficients might be explained by the  
227 differences in excitation and emission wavelengths used by the devices. For instance, the  
228 EXO1 excitation wavelength is closer to the optical region of FWAs, compared to the region  
229 where peak C is generally reported (Coble et al. 2014), and compared to the peak C excitation  
230 wavelengths measured with the DuoFluor and Varian Cary Eclipse. In addition, the  
231 correlations with Varian Cary Eclipse data were established using a small sample size (N=8),  
232 a larger dataset being needed to obtain statistically significant correlations. However, the  
233 results are sufficient to provide an indication of devices potential to measure peaks T and C *in*  
234 *situ*.

235 During the experiment, the DuoFluor system recorded a constant decrease in peak C  
236 fluorescence intensity (Fig. 2D) due to biofilm formation on the cuvette. Regular cuvette  
237 cleaning (twice per week) was required to ensure adequate DuoFluor fluorescence results.  
238 The EXO1 and the Cyclops 7 sensors were not cleaned during the entire experiment and no  
239 substantial reduction in fluorescence intensity was observed. However, further studies are  
240 needed to test the time span until fouling interferes with the fluorescence signal. This  
241 experiment shows that submersible instruments are more practical at WwTPs. The advantages  
242 of needing less frequent cleaning (no cleaning for at least 1 month) and being battery powered  
243 make them preferable for effluent monitoring. Fluorescence data were not corrected for  
244 thermal quenching as little impact was expected for a decrease of 0.5<sup>0</sup> C from day to night and  
245 of 3<sup>0</sup> C change over the entire period (Fig. S4A). Based on previous work (Carstea et al.  
246 2014), it is estimated that the fluorescence intensity would increase by 0.3 % for a decrease in  
247 temperature of 0.5<sup>0</sup> C and by 2.6 % for a 3<sup>0</sup> C temperature change. Temperature correction  
248 may be needed in areas with high seasonal variation. Inner filter effect is also known to  
249 impact the fluorescence measurements. However, Henderson et al. (Henderson et al. 2009)

250 showed that the inner filter effect is unlikely to occur in surface and wastewater samples with  
251 a TOC concentration below 25 mg/l. The final effluent TOC concentrations measured within  
252 the current experiment varied between 6.29 mg/L and 9.28 mg/L. Moreover, the same  
253 samples showed absorbance values below 0.20 at 254 nm, this being the threshold  
254 recommended by Aiken (Coble et al. 2014) for optically dilute samples. Metal ions have been  
255 shown to affect the fluorescence intensity and peak position of OM components (Coble et al.  
256 2014). The average iron concentration measured at the WwTP final effluent discharge point  
257 was 0.30 mg/L (Table 2). Poulin et al. (Poulin et al. 2014) found that an iron:organic carbon  
258 ratio of 0.3 would reduce the fluorescence intensity between 7 % and 23 % depending on the  
259 type of water sample. In this study, an average value of 0.03 for the iron:organic carbon ratio  
260 was observed. Suspended solids have been shown to influence the results from in situ  
261 fluorimeters (Coble et al. 2014). However, Belzile et al. (2006) found a strong correlation  
262 between a submersible fluorimeter and a benchtop spectrofluorimeter, at unfiltered samples  
263 with suspended solids concentrations below 35 mg/L. In the current study, the effluent  
264 suspended solids concentrations varied from 4.5 mg/L to 20.7 mg/L. Filtration, which would  
265 reduce the quantity of suspended solids, may also contaminate the sample and remove a large  
266 fraction of fluorescent components that are found in particulate or colloidal form (Coble et al.  
267 2014). Furthermore, one aim of this study was to test the robustness of fluorescence  
268 spectroscopy to monitor effluent quality without major intervention during or after  
269 measurement. For this purpose, a qualitative analysis of effluent OM, i.e. without correction  
270 for inner filter effect or extensive calibration, was sufficient to detect changes in effluent  
271 water quality.

272 Peaks T and C displayed a diurnal variation with a cycle of approximately 12 h, the  
273 highest intensity being recorded around midnight and the lowest intensity at noon (Fig. 2).  
274 During dry weather days, peak T displayed a decrease in fluorescence intensity of < 9 % for

275 the Cyclops 7 and 16 % for the DuoFluor between midnight and noon, while peak C  
276 decreased by < 10 % for the EXO1 sensor and 17 % for the DuoFluor over the same period.  
277 The diurnal variation in fluorescence intensity was consistent with the changes in effluent  
278 flow rate, conductivity and pH (Fig. S4 (B) and (C), and Fig. S5). However, fluorescence  
279 intensity was not directly proportional to the degree of increase in flow rate. The effluent flow  
280 rate presented 2 peaks, every day, of almost equal intensity (Fig. S5). We also observed two  
281 peaks in the fluorescence data; the first peak being recorded at midnight and the second peak  
282 at approximately 2 pm (Fig. 3). This 2 pm peak was substantially lower in intensity compared  
283 with the midnight peak, although high flow rate was recorded. It is concluded that these  
284 midnight and 2 pm peaks correspond to intensive household water use during the mornings  
285 and evenings. Considering the total wastewater retention time within the WwTP from inlet to  
286 discharge point (12-16h) and the additional retention time in the sewerage network from  
287 household to the WwTP, it is believed that the high values of peaks T and C observed at  
288 midnight correspond to the previous day morning high wastewater input, while the 2 pm peak  
289 represents the previous evening water usage.

290 Several rainfall periods, of different intensity and duration, were recorded during the  
291 real-time experiment (Table 1). We divided the precipitation days into 4 events: event I – 13<sup>th</sup>  
292 to 14<sup>th</sup> of August; event II – 19<sup>th</sup> of August; event III – 23<sup>rd</sup> to 27<sup>th</sup> of August; event IV – 30<sup>th</sup>  
293 of August to 3<sup>rd</sup> of September. The WwTP is served by a combined sewerage system and  
294 therefore rainfall increases the influent flow and modifies the properties of the influent  
295 affecting process performance and effluent quality (Wilén et al. 2006). Therefore, it is  
296 believed that the amount and frequency of precipitation affects most of the measured water  
297 quality parameters, depending on the catchment and sewerage system. Rain events were seen  
298 to trigger high ammonia and iron values (Table 2). Precipitation also increased the  
299 concentration of total phosphorus; the highest value being recorded during or after the first

300 day of the rain event. Conductivity and pH decreased after each rain event, depending on the  
301 intensity of the event (Fig. S4). Conductivity showed a significant decrease after events I and  
302 IV, while pH was the parameter least affected by precipitation.

303 A decrease in fluorescence intensity was observed one day after the beginning of each  
304 precipitation event (Fig. 2). Precipitation events I and IV generated the greatest decrease in  
305 Peak C (32 % & 42 % respectively) measured using the EXO1. Cyclops 7 recorded Peak T  
306 reductions of 25 % (event I) and 28 % (event IV). DuoFluor measured a 26 % decrease in  
307 peak C and 25 % in peak T following event I. The full impact of event IV was not assessed  
308 with the DuoFluor due to data loss following a power outage at the WwTP. However, the  
309 same effect is observed on peaks T and C after the other rain events. Overall, the decrease in  
310 fluorescence intensity is consistent with the quantity of rain per event. After each rain event  
311 the fluorescence intensity increased progressively until the next rainfall. Previous studies on  
312 urban river monitoring (Carstea et al. 2009) showed that peaks T and C intensity increased  
313 after precipitation events, due to the release of higher quantities of OM with surface runoff  
314 compared to the receiving water. Here, a dilution of the wastewater's heavily concentrated  
315 OM was observed. Others (Mines et al. 2007) also reported a dilution effect, reflected in a  
316 decrease in BOD values. Since BOD correlates with fluorescence (Bridgeman et al. 2013), a  
317 rainfall-generated decrease in fluorescence intensity is anticipated.

318 In addition to the daily variation and impact from precipitation, two data anomalies  
319 were identified on the 24<sup>th</sup> of August and 3<sup>rd</sup> of September, both immediately after midnight  
320 (Fig. 2– circled with red). These anomalies are most evident from the EXO1 sensor data. The  
321 data are higher than the normal daily variation, with or without precipitation, and may be  
322 associated with changes in influent quality or treatment processes. The first anomaly is  
323 explained by the release of liquor from the sewage sludge facility on the 24<sup>th</sup> of August at  
324 12:00pm. The WwTP managers report that silt is occasionally released with the liquor,

325 resulting in elevated concentrations of ammonia in the effluent. Unusually high ammonia was  
326 recorded at the same time as the high fluorescence intensity (Fig. S5). The high fluorescence  
327 intensity during the first anomaly could indicate the production of autochthonous OM from  
328 the sewage sludge liquor (Cohen et al. 2014; Riopel et al. 2014), as peak C components  
329 increase in the soluble microbial products with increasing retention times (Yu et al. 2015).  
330 Also, condensed polymerized humic-like material may form during biodegradation (Saadi et  
331 al. 2006). Therefore, liquor may carry large quantities of autochthonous OM, some of it  
332 biologically resistant, produced during the long retention times, along the stages of the  
333 sewage sludge facility.

334 The second anomaly (Fig. 2) is a result of the power issues that occurred at the WwTP.  
335 On the 3<sup>rd</sup> of September, low power caused the aeration tank air blowers to fail. Fluorescence  
336 data can be used to identify the process failure. The increase of peak C fluorescence from the  
337 second anomaly may represent FWAs present in the sewage. Peak C wavelengths coincide  
338 with the fluorescence regions of FWAs (Henderson et al. 2009). However, FWAs were also  
339 measured in the excitation/emission wavelengths region of 250 nm / 344 nm and 422 nm  
340 (Boving et al. 2004). Almost 80 % of FWAs are removed after the biological treatment and  
341 these compounds may be used as molecular markers of less effective treatment processes  
342 (Hayashi et al. 2002). Therefore, temporary interruption of the ASP tanks would have led to  
343 the presence of untreated FWAs, as seen in the second anomaly.

344 Thus, real-time, *in situ* analysis demonstrated the ruggedness of fluorescence  
345 spectroscopy and the ability to detect minor changes in effluent quality. Fluorescence  
346 spectroscopy could be used to identify underperformance issues, albeit with a time lag  
347 between the failure and the feedback information. However, fluorescence spectroscopy still  
348 represents a fast and effective control method, and a reliable alternative to BOD. The benefits  
349 of improved treatment control via fluorescence spectroscopy go beyond CO<sub>2</sub> reductions and

350 climate change mitigation, as they will also facilitate environmental improvements, reduce  
351 operating costs and improve the financial performance of the global wastewater industry.

## 352 **Conclusions**

- 353 • This study reported the first real-time monitoring of effluent wastewater using  
354 fluorescence spectroscopy. Results show that fluorescence spectroscopy is a  
355 robust technique for monitoring changes in effluent quality. It also shows that  
356 portable devices can run continuously, for 1 month, without any cleaning  
357 procedure in the case of submersible systems (or with limited regular cleaning  
358 for cuvette-based fluorimeters). Further studies are needed to test the time span  
359 until fouling interferes with the fluorescence signal. In addition, multiple sites  
360 should be considered in future studies to account various peculiarities of  
361 wastewater input.
- 362 • Fluorescence peaks T and C showed that OM varied diurnally depending on the  
363 flow rate. Precipitation decreased the fluorescence intensity of both peaks due to  
364 dilution of wastewater with runoff. The degree of decrease in fluorescence  
365 intensity was found to be proportional to the quantity of rainfall.
- 366 • 15 min measurement frequency yielded sufficient data to obtain a detailed  
367 assessment of daily variation, precipitation impact on influent quality and  
368 treatment process.
- 369 • A qualitative analysis of effluent OM, i.e. without correction for inner filter  
370 effect or extensive calibration can detect changes in effluent water quality.  
371 However, temperature correction may be needed in areas with high seasonal  
372 variation. Inner filter effect correction may be required when quantitative  
373 measurements are needed.
- 374 • Submersible instruments proved to be a more practical tool for *in situ*



375 measurement compared to the cuvette-based device. The advantages of reduced  
376 cleaning frequency (no cleaning for at least 1 month) and battery operation make  
377 them preferable for effluent OM monitoring.

378 • Results showed that fluorescence intensity of peaks T and C was capable of  
379 detecting minor changes in influent OM quantity and issues with treatment  
380 process. The substantial impact on peak C fluorescence intensity with changes in  
381 the system was attributed to the input of autochthonous OM from sewage sludge  
382 liquor and the presence of untreated FWAs. Although the variation in  
383 fluorescence was more clearly observed at peak C compared to peak T, it is  
384 recommended that both peaks are monitored due to variations in wastewater  
385 composition.

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### 394 **Supplemental Data**

395 Figs. S1-S5 and Table S1 are available online in the ASCE Library ([ascelibrary.org](http://ascelibrary.org)).

### 396 **References**

397 Ahmad, S. R., and Reynolds, D. M. (1995). "Synchronous fluorescence spectroscopy of  
398 wastewater and some potential constituents." *Water Research*, 29(6), 1599–1602.  
399 Assaad, A., Pontvianne, S., and Pons, M. N. (2014). "Photodegradation-based detection of

400 fluorescent whitening agents in a mountain river.” *Chemosphere*, Elsevier Ltd, 100, 27–  
401 33.

402 Baker, A. (2002). “Fluorescence excitation-emission matrix characterization of river waters  
403 impacted by a tissue mill effluent.” *Environmental Science and Technology*, 36(7),  
404 1377–1382.

405 Belzile, C., Roesler, C. S., Christensen, J. P., Shakhova, N., and Semiletov, I. (2006).  
406 “Fluorescence measured using the WETStar DOM fluorometer as a proxy for dissolved  
407 matter absorption.” *Estuarine, Coastal and Shelf Science*, 67(3), 441–449.

408 Bourgeois, W., Burgess, J. E., and Stuetz, R. M. (2001). “On-line monitoring of wastewater  
409 quality: A review.” *Journal of Chemical Technology and Biotechnology*, 76(4), 337–348.

410 Boving, T. B., Meritt, D. L., and Boothroyd, J. C. (2004). “Fingerprinting sources of bacterial  
411 input into small residential watersheds: Fate of fluorescent whitening agents.”  
412 *Environmental Geology*, 46(2), 228–232.

413 Bridgeman, J., Baker, A., Brown, D., and Boxall, J. B. (2015). “Portable LED fluorescence  
414 instrumentation for the rapid assessment of potable water quality.” *Science of the Total  
415 Environment*, Elsevier B.V., 524–525, 338–346.

416 Bridgeman, J., Baker, A., Carliell-Marquet, C., and Carstea, E. (2013). “Determination of  
417 changes in wastewater quality through a treatment works using fluorescence  
418 spectroscopy.” *Environmental Technology*, 34(23), 3069–3077.

419 Carstea, E. M., Baker, A., Bieroza, M., Reynolds, D. M., and Bridgeman, J. (2014).  
420 “Characterisation of dissolved organic matter fluorescence properties by PARAFAC  
421 analysis and thermal quenching.” *Water Research*, 61, 152–161.

422 Carstea, E. M., Baker, A., Pavelescu, G., and Boomer, I. (2009). “Continuous fluorescence  
423 assessment of organic matter variability on the Bournbrook River, Birmingham, UK.”  
424 *Hydrological Processes*, 23(13), 1937–1946.

425 Carstea, E. M., Bridgeman, J., Baker, A., and Reynolds, D. M. (2016). "Fluorescence  
426 spectroscopy for wastewater monitoring: A review." *Water Research*, 95, 206–219.

427 Chandler, D. M., and Lerner, D. N. (2015). "A low cost method to detect polluted surface  
428 water outfalls and misconnected drainage." *Water and Environment Journal*, 29(2), 202–  
429 206.

430 Coble, P. G., Green, S. A., Blough, N. V., and Gagosian, R. B. (1990). "Characterization of  
431 dissolved organic matter in the Black Sea by fluorescence spectroscopy." *Nature*,  
432 348(6300), 432–435.

433 Coble, P. G., Spencer, R. G. M., Baker, A., and Reynolds, D. M. (2014). "Aquatic Organic  
434 Matter Fluorescence." *Aquatic Organic Matter Fluorescence*, P. G. Coble, J. Lead, A.  
435 Baker, D. M. Reynolds, and R. G. M. Spencer, eds., Cambridge University Press, New  
436 York, 75–125.

437 Cohen, E., Levy, G. J., and Borisover, M. (2014). "Fluorescent components of organic matter  
438 in wastewater: Efficacy and selectivity of the water treatment." *Water Research*, Elsevier  
439 Ltd, 55, 323–334.

440 Environmental Knowledge Transfer Network. (2008). *Energy Efficient Water and*  
441 *Wastewater Treatment*.

442 Galinha, C. F., Carvalho, G., Portugal, C. A. M., Guglielmi, G., Oliveira, R., Crespo, J. G.,  
443 and Reis, M. A. M. (2011). "Real-time monitoring of membrane bioreactors with 2D-  
444 fluorescence data and statistically based models." *Water Science and Technology*, 63(7),  
445 1381–1388.

446 Graham, P. W., Baker, A., Andersen, M. S., and Acworth, I. (2015). "Field Measurement of  
447 Fluorescent Dissolved Organic Material as a Means of Early Detection of Leachate  
448 Plumes." *Water, Air, and Soil Pollution*, 226(7).

449 Hayashi, Y., Managaki, S., and Takada, H. (2002). "Fluorescent whitening agents in Tokyo

450 Bay and adjacent rivers: Their application as anthropogenic molecular markers in coastal  
451 environments.” *Environmental Science and Technology*, 36(16), 3556–3563.

452 Henderson, R. K., Baker, A., Murphy, K. R., Hambly, A., Stuetz, R. M., and Khan, S. J.  
453 (2009). “Fluorescence as a potential monitoring tool for recycled water systems: A  
454 review.” *Water Research*, Elsevier Ltd, 43(4), 863–881.

455 Hudson, N., Baker, A., and Reynolds, D. (2007). “Fluorescence analysis of dissolved organic  
456 matter in natural, waste and polluted waters—a review.” *River Research and  
457 Applications*, 23(6), 631–649.

458 Hudson, N., Baker, A., Ward, D., Reynolds, D. M., Brunson, C., Carliell-Marquet, C., and  
459 Browning, S. (2008). “Can fluorescence spectrometry be used as a surrogate for the  
460 Biochemical Oxygen Demand (BOD) test in water quality assessment? An example from  
461 South West England.” *Science of the Total Environment*, 391(1), 149–158.

462 Ishii, S. K. L., and Boyer, T. H. (2012). “Behavior of reoccurring parafac components in  
463 fluorescent dissolved organic matter in natural and engineered systems: A critical  
464 review.” *Environmental Science and Technology*, 46(4), 2006–2017.

465 Jouanneau, S., Recoules, L., Durand, M. J., Boukabache, A., Picot, V., Primault, Y., Lakel,  
466 A., Sengelin, M., Barillon, B., and Thouand, G. (2014). “ScienceDirect Methods for  
467 assessing biochemical oxygen demand ( BOD ): A review.” *Water Research*, Elsevier  
468 Ltd, 49, 62–82.

469 Mines, R. O., Lackey, L. W., and Behrend, G. H. (2007). “The Impact of Rainfall on Flows  
470 and Loadings at Georgia’s Wastewater Treatment Plants.” *Water, Air, and Soil  
471 Pollution*, 179(1), 135–157.

472 Murphy, K. R., Hambly, A., Singh, S., Henderson, R. K., Baker, A., Stuetz, R., and Khan, S.  
473 J. (2011). “Organic matter fluorescence in municipal water recycling schemes: Toward a  
474 unified PARAFAC model.” *Environmental Science and Technology*, 45(7), 2909–2916.

475 Ou, H. S., Wei, C. H., Mo, C. H., Wu, H. Z., Ren, Y., and Feng, C. H. (2014). “Novel insights  
476 into anoxic/aerobic1/aerobic2 biological fluidized-bed system for coke wastewater  
477 treatment by fluorescence excitation-emission matrix spectra coupled with parallel factor  
478 analysis.” *Chemosphere*, Elsevier Ltd, 113, 158–164.

479 Poulin, B. A., Ryan, J. N., and Aiken, G. R. (2014). “Effects of iron on optical properties of  
480 dissolved organic matter.” *Environmental Science and Technology*, 48(17), 10098–  
481 10106.

482 Reynolds, D. M. (2002). “The differentiation of biodegradable and non-biodegradable  
483 dissolved organic matter in wastewaters using fluorescence spectroscopy.” *Journal of*  
484 *Chemical Technology and Biotechnology*, 77(8), 965–972.

485 Riopel, R., Caron, F., and Siemann, S. (2014). “Fluorescence Characterization of Natural  
486 Organic Matter at a Northern Ontario Wastewater Treatment Plant.” *Water, Air, & Soil*  
487 *Pollution*, 225(9), 2126.

488 Saadi, I., Borisover, M., Armon, R., and Laor, Y. (2006). “Monitoring of effluent DOM  
489 biodegradation using fluorescence, UV and DOC measurements.” *Chemosphere*, 63(3),  
490 530–539.

491 Sgroi, M., Roccaro, P., Korshin, G. V., Greco, V., Sciuto, S., Anumol, T., Snyder, S. A., and  
492 Vagliasindi, F. G. A. (2016). “Use of fluorescence EEM to monitor the removal of  
493 emerging contaminants in full scale wastewater treatment plants.” *Journal of Hazardous*  
494 *Materials*.

495 Singh, S., Henderson, R. K., Baker, A., Stuetz, R. M., and Khan, S. J. (2012).  
496 “Characterisation of reverse osmosis permeates from municipal recycled water systems  
497 using fluorescence spectroscopy: Implications for integrity monitoring.” *Journal of*  
498 *Membrane Science*, Elsevier, 421–422, 180–189.

499 Singh, S., Henderson, R. K., Baker, A., Stuetz, R. M., and Khan, S. J. (2015). “Online

500 fluorescence monitoring of RO fouling and integrity: analysis of two contrasting  
501 recycled water schemes.” *Environ. Sci.: Water Res. Technol.*, Royal Society of  
502 Chemistry, 1, 689–698.

503 Tartakovsky, B., Lishman, L. A., and Legge, R. L. (1996). “Application of multi-wavelength  
504 fluorometry for monitoring wastewater treatment process dynamics.” *Water Research*,  
505 30(12), 2941–2948.

506 Wilén, B.-M., Lumley, D., Mattsson, A., and Mino, T. (2006). “Rain events and their effect  
507 on effluent quality studied at a full scale activated sludge treatment plant.” *Water Science  
508 and Technology*, 54(10), 201–208.

509 Yang, L., Han, D. H., Lee, B. M., and Hur, J. (2015). “Characterizing treated wastewaters of  
510 different industries using clustered fluorescence EEM-PARAFAC and FT-IR  
511 spectroscopy: Implications for downstream impact and source identification.”  
512 *Chemosphere*, Elsevier Ltd, 127, 222–228.

513 Yu, H., Qu, F., Sun, L., Liang, H., Han, Z., Chang, H., Shao, S., and Li, G. (2015).  
514 “Relationship between soluble microbial products (SMP) and effluent organic matter  
515 (EfOM): Characterized by fluorescence excitation emission matrix coupled with parallel  
516 factor analysis.” *Chemosphere*, Elsevier Ltd, 121, 101–109.

517 Yu, H., Song, Y., Liu, R., Pan, H., Xiang, L., and Qian, F. (2014). “Identifying changes in  
518 dissolved organic matter content and characteristics by fluorescence spectroscopy  
519 coupled with self-organizing map and classification and regression tree analysis during  
520 wastewater treatment.” *Chemosphere*, Elsevier Ltd, 113, 79–86.

521  
522

523 **Figure captions**

524 **Fig. 1.** Relationship between BOD and fluorescence. (A) peak T and (B) peak C (N=87).

525 **Fig. 2.** In situ fluorescence measurements. Peak T measured with (A) Cyclops 7 and (B)  
526 DuoFluor. Peak C measured with (C) EXO1 and (D) DuoFluor. Rainfall events I-IV are  
527 marked with blue and anomalies are circled with red. The DuoFluor stopped recording during  
528 rain event IV due to a power failure at the WwTP. The large differences in the fluorescence  
529 intensity observed at graph (D) for the dates Aug 17, Aug 20, Aug 24 and Aug 28 were  
530 caused by cuvette cleaning on the DuoFluor.

531 **Fig. 3.** Examples of daily fluorescence variation for the 3 portable devices. (A) peak T  
532 fluorescence and (B) peak C fluorescence. The 2 pm peak is marked with a blue square.

533 **Table 1.** Kendall Correlation Between the Data from Portable Devices and Varian Benchtop  
 534 Spectrofluorimeter.

Device		Cyclops 7	EXO1	DuoFluor		Varian		FWA 370	FWA 400
				Peak T	Peak C	Peak T	Peak C		
Cyclops 7		1	<b>0.19</b>	<b>0.28</b>	0.02	0.21	0.21	0.29	0.36
EXO1		-	1	<b>0.49</b>	<b>0.48</b>	0.64	0.64	0.86	<b>0.93</b>
DuoFluor	Peak T	-	-	1	-	0.33	0.20	0.47	0.47
	Peak C	-	-	-	1	0.60	0.47	0.73	0.73

535 Note: Correlation coefficients in bold have p values below 0.001 (p-values < 0.001 are considered significant).



536 **Table 2.** Standard Parameters Measured by the WwTP.

Date	Precipitation (mm)	Temperature (°C)	Total Phosphorus (mg/L)	Iron (mg/L)	Ammonia (mg/L)
10.08	0.0	19.5	0.57	0.31	0.06
11.08	0.0	18.9	0.73	0.29	0.06
12.08	0.0	18.8	0.70	0.33	0.21
13.08	33.0	19.4	0.44	0.34	0.21
14.08	3.0	18.5	0.98	0.49	2.37
15.08	0.0	19.2	0.47	0.35	0.35
16.08	0.0	19.7	0.30	0.28	0.30
17.08	0.0	18.5	0.62	0.28	0.06
18.08	0.0	18.2	0.50	0.33	0.06
19.08	8.0	18.9	0.44	0.37	0.08
20.08	0.0	19.2	0.61	0.33	0.30
21.08	0.0	19.5	0.46	0.25	0.06
22.08	0.0	19.7	0.38	0.35	0.35
23.08	9.0	20.1	0.37	0.46	0.32
24.08	9.0	18.9	0.55	0.27	0.06
25.08	7.0	18.4	0.66	0.30	1.81
26.08	0.5	18.7	0.38	0.26	0.06
27.08	0.5	18.3	0.48	0.25	0.06
28.08	0.0	18.4	0.39	0.21	0.06
29.08	0.0	18.9	0.49	0.24	0.06
30.08	18.0	19.2	0.51	0.17	0.06
31.08	12.0	18.3	0.39	0.25	0.06
01.09	25.0	17.0	0.51	0.20	0.10
02.09	4.0	17.0	0.30	0.19	0.27
03.09	1.0	17.3	0.37	0.23	0.07
04.09	0.0	17.1	0.50	0.40	0.68
05.09	0.0	17.1	0.37	0.25	0.40
06.09	0.0	17.4	0.49	0.24	0.30
07.09	0.0	17.7	0.54	0.34	0.15

537

## Supplementary data

### Online fluorescence monitoring of effluent quality in wastewater treatment plants

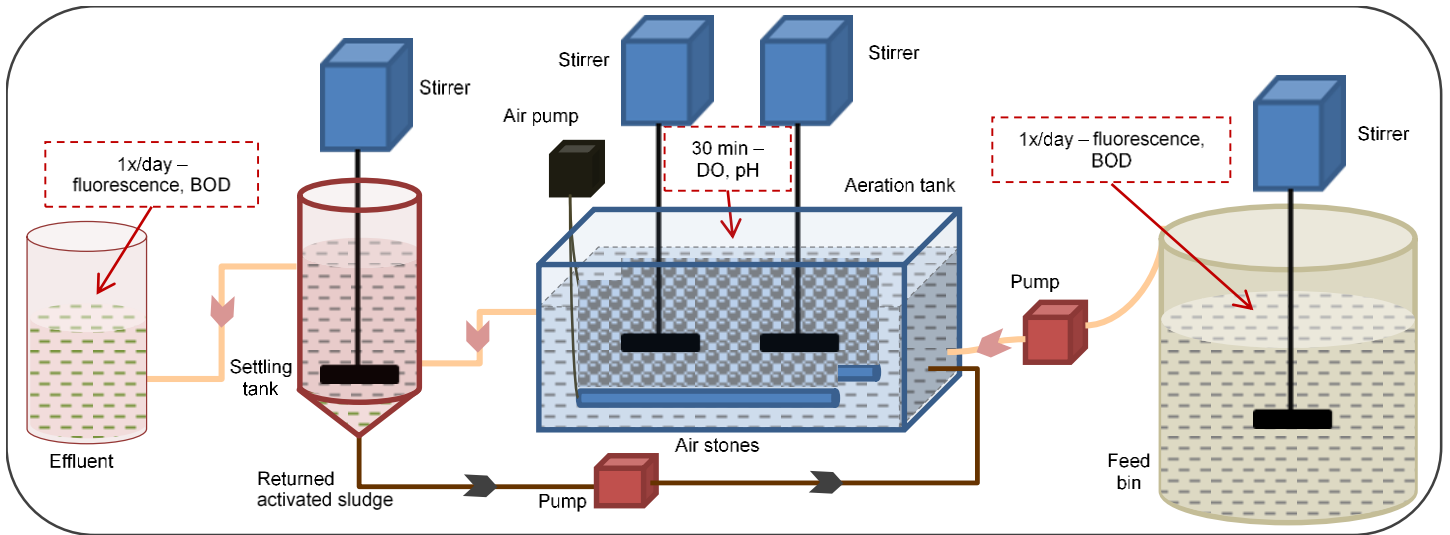
Elfrida M. Carstea<sup>1,2\*</sup>, Yulia S. Zakharova<sup>3</sup> and John Bridgeman<sup>4</sup>

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077125, Magurele, Romania; [elfrida.carstea@inoe.ro](mailto:elfrida.carstea@inoe.ro)*

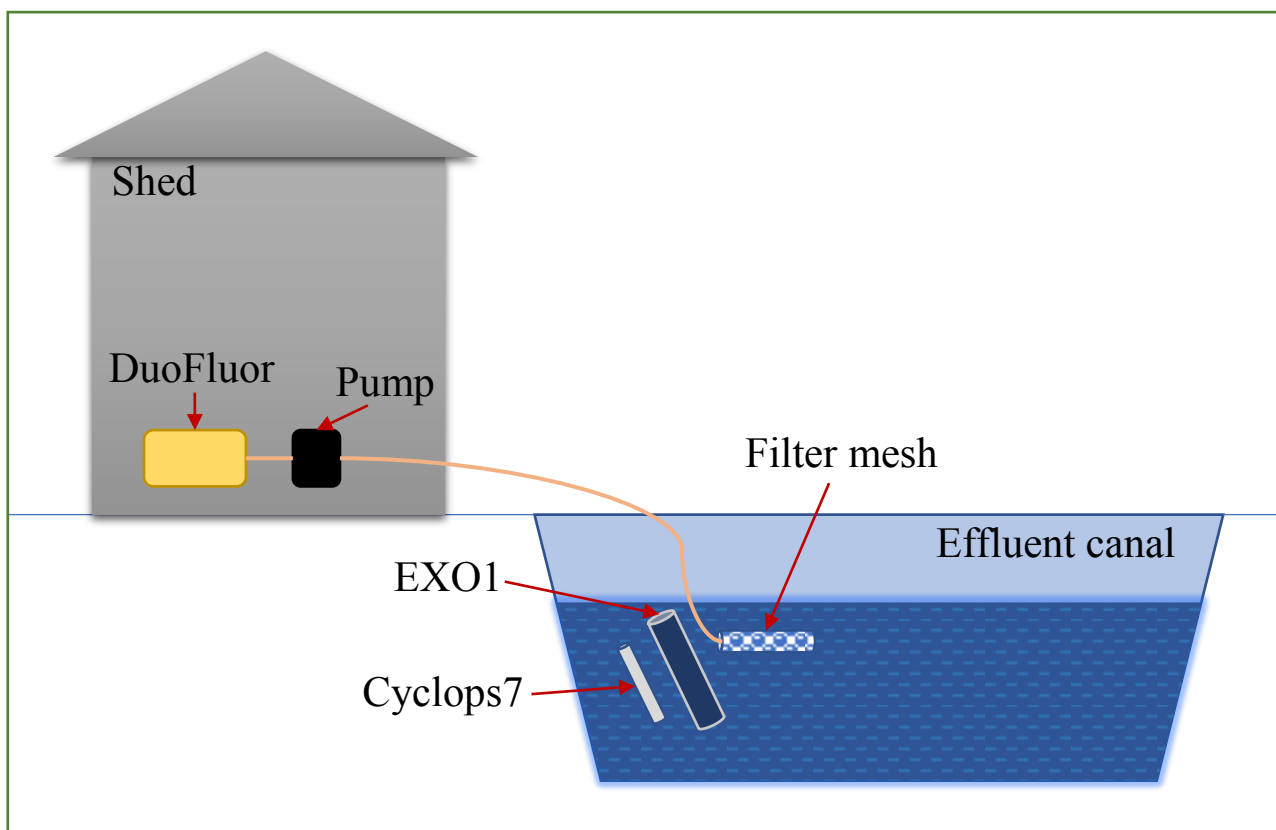
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Birmingham, B15 2TT, UK*

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2TT, UK, [julia\\_ripe@hotmail.co.uk](mailto:julia_ripe@hotmail.co.uk)*

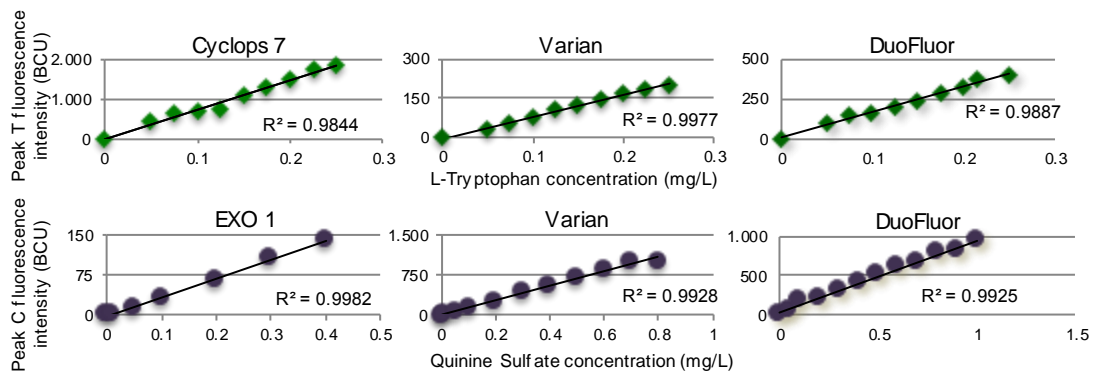
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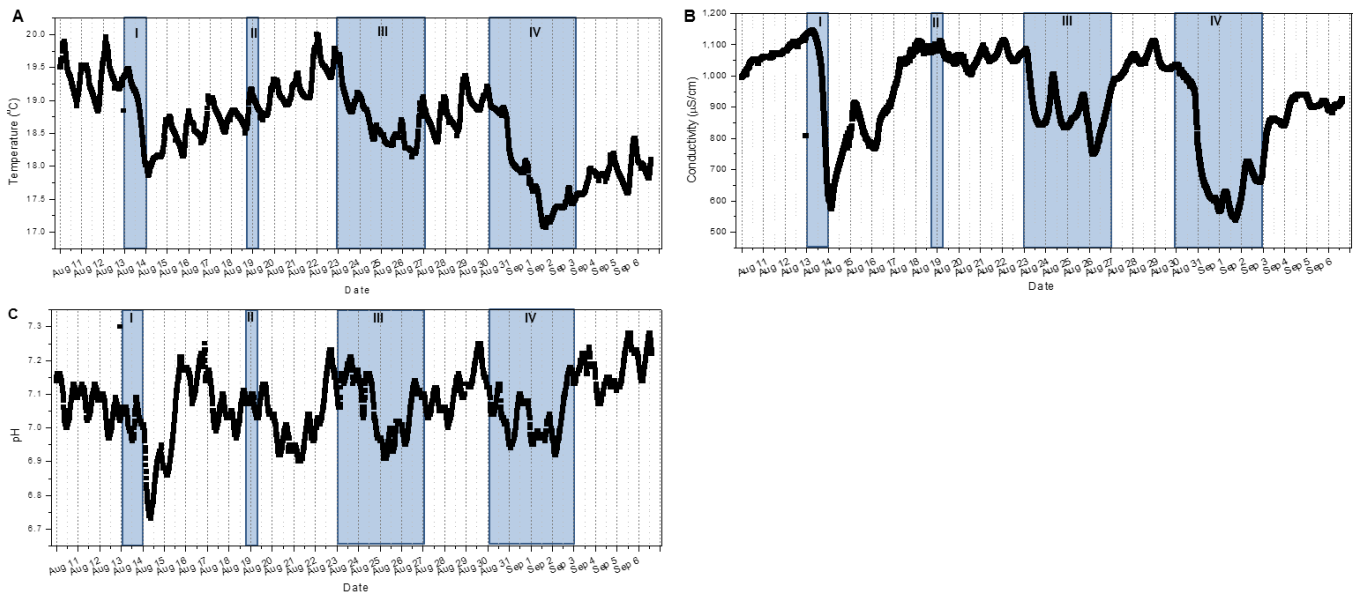
**Fig. S1.** The setup for the laboratory scale activated sludge process. BOD – biochemical oxygen demand; DO – dissolved oxygen. The orange and black arrows indicate the direction of the flow.



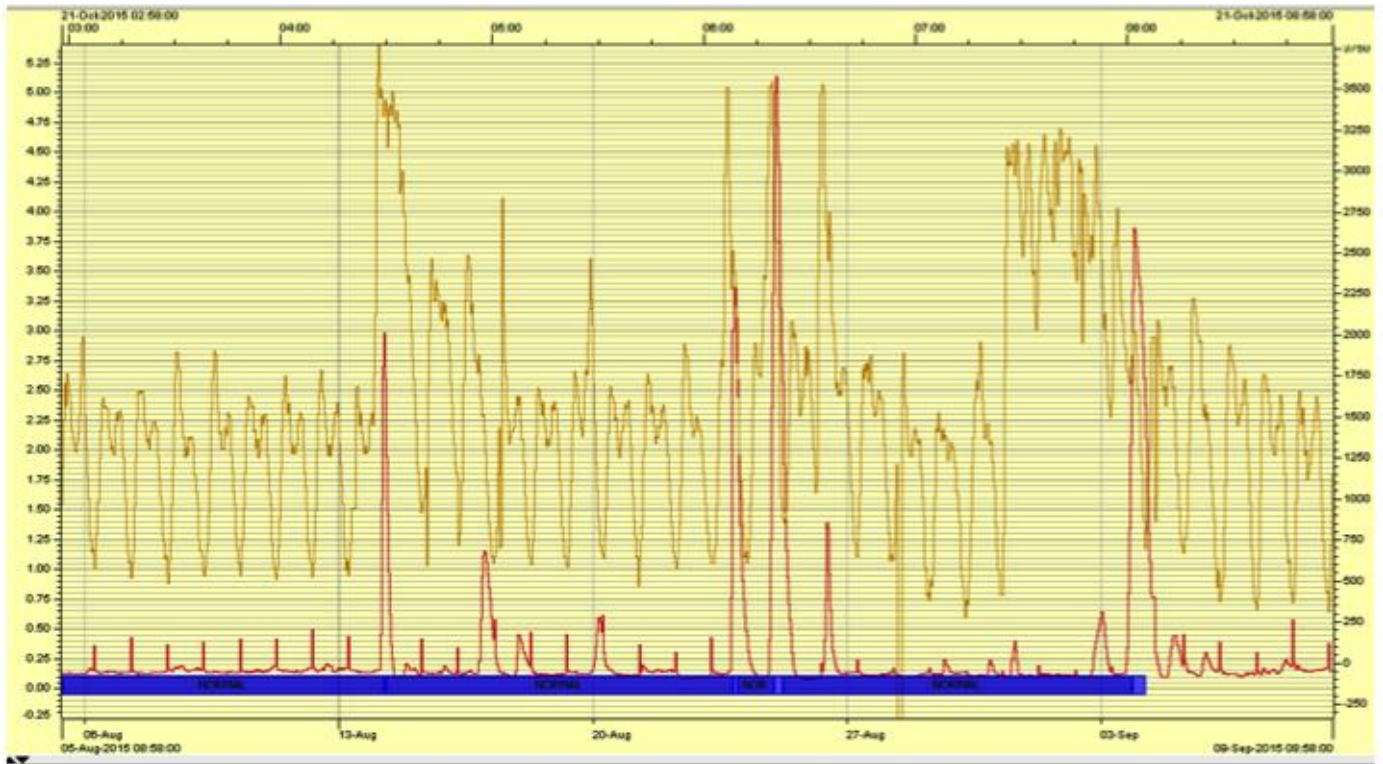
**Fig. S2.** The setup for the *in-situ* fluorescence measurements. The EXO1 and Cyclops 7 were connected to handheld devices and tightened with ropes to the cover grid above the effluent channel.



**Fig. S3.** Linearity check of the three portable devices and comparison with a benchtop spectrofluorimeter. The fluorescence intensity was corrected by extracting the blank spectrum.



**Fig. S4.** In situ measurements with the EXO1 sonde. (A) temperature, (B) conductivity and (C) pH.



**Fig. S5.** Flow rate (brown line) and quantity of ammonia (red line) at the effluent. Graph provided by the WwTP.

**Table S1.** Standard parameters and peak T and peak C fluorescence for grab samples of final effluent. The fluorescence peaks were measured with a benchtop spectrofluorimeter.

Date	BOD	COD	TOC	Nitrates	Turbidity	Fluorescence intensity			
						Peak T	Peak C	FWA 370*	FWA 400*
	(mg/L)				(NTU)	(a.u.)			
13.08.2015	1.6	27	8.9	30.7	N/A	106	178	80	58
17.08.2015	2.9	23	8.5	23.8	2.18	100	166	68	51
20.08.2015	1.9	24	9.3	28.8	1.90	104	189	79	56
25.08.2015	3.0	30	7.9	19.0	1.85	94	148	67	50
28.08.2015	1.7	32	N/A	27.3	1.54	107	168	68	50
01.09.2015	2.7	15	6.3	14.9	2.18	76	129	58	38
03.09.2015	3.0	18	7.2	16.5	2.67	81	148	66	39
07.09.2015	1.7	17	8.5	22.1	1.96	97	159	68	48

\* Fluorescence whitening agents' excitation wavelength