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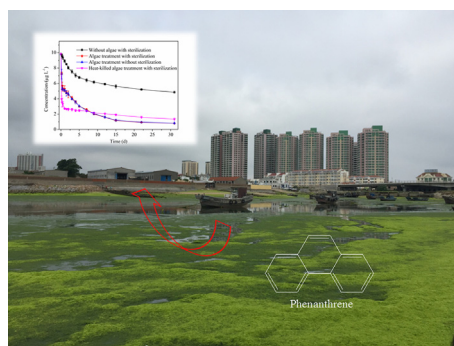
Removal of phenanthrene from coastal waters by green tide algae *Ulva prolifera*

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HIGHLIGHTS

- Phenanthrene was removed efficiently by green tide algae *Ulva prolifera*.
- Nutrient and temperature had positive influence on the removal of phenanthrene.
- 91.3% of phenanthrene was removed under the initial concentration of $5 \mu\text{g L}^{-1}$.
- New phenanthrene attenuation process associated with green tide was confirmed.

GRAPHICAL ABSTRACT



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ABSTRACT

Ulva prolifera (*U. prolifera*) has been frequently involved in terrible algal proliferation in coastal areas. Although it is known to be associated with green tide, its contribution to the natural attenuation of the polycyclic aromatic hydrocarbons (PAHs) in seawater has not been evaluated. In this study, the removal of phenanthrene using *U. prolifera* collected from coastal water with green tide blooming was investigated. The results showed that phenanthrene could be removed efficiently in the presence of both the live and heat-killed *U. prolifera*. The phenanthrene concentrations of the live algae treatment decreased smoothly from 10.00 to $0.80 \mu\text{g L}^{-1}$ through the whole process, while those of the heat-killed algae treatment decreased sharply from 10.0 to $2.71 \mu\text{g L}^{-1}$ in one day and kept constantly after that. The in situ monitoring and visualizing using laser confocal scanning microscopy (LCSM) confirmed the accumulation of phenanthrene in *U. prolifera*. The increase in nutrient and temperature led to the increase of phenanthrene removal rate, while the salinity had less influence on the removal of phenanthrene. The removal efficiency by *U. prolifera* had a good linear relationship with phenanthrene initial concentration ($r^2 = 0.999$) even at $100 \mu\text{g L}^{-1}$ which was higher than its environmentally relevant concentrations. High removal efficiency (91.3%) was observed when the initial phenanthrene concentration was set at environmental relevant concentration ($5 \mu\text{g L}^{-1}$). Results of this study demonstrate a potential new natural attenuation process for typical PAHs in coastal water during the outbreak of green tide. These findings indicate that the outbreak of harmful green tide algae may bring positive environmental benefits in the terms of the removal of harmful organic pollutants from coastal waters.

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1. Introduction

Algal blooms have become a global problem, resulting in loss of water clarity, production of bad taste and odor and toxins that lead to adverse effects on aquatic organism (Wu et al., 2010a; Wu et al., 2011; Wu et al., 2010b). In every spring and early summer since 2007, green tides persistently flourish along the coastal regions of the northern Yellow Sea, Jiangsu Province of China (Shi et al., 2015), and then floated northward until landed on seashore of Shandong Province with 6 million kg algae biomass, which brought negative effects on local economy and coastal ecosystems (Zhang et al., 2011). As a kind of dominant species, *Ulva prolifera* (*U. prolifera*) can inhabit in the inshore and estuaries as well as brackish and fresh waters which contain enriched nutrients from agriculture and animal aquaculture (Li et al., 2016). These algae consist of filamentous shoots with monostromatic hollow cylinders and have higher ratio of surface to volume (S/V), which endows them with high nutrient (nitrogen and phosphorus) uptake capability and the potential to remove pollutants when exposed to contaminated aquatic environment (Gao et al., 2016). Many laboratory experiments have indicated that *U. prolifera* can fast uptake nitrogen and phosphorus (Fan et al., 2014; Luo et al., 2012; Xu et al., 2016). It is also suggested that during the mid- to late period of the macroalgal blooms, *U. prolifera* can continue to remove nutrients such as N and P from seawater (Li et al., 2016; Zhu et al., 2016). However, few reports are available on the removal of organic toxic contaminants by *U. prolifera* during the macroalgal blooms.

Polycyclic aromatic hydrocarbons (PAHs) are a major group of persistent organic contaminants, which can exist for a long time and undergo long-range transport in the environment (Zhao et al., 2015). So far >100 PAH congeners have been identified and 16 PAH congeners are classified as priority pollutants by the European Union and US Environmental Protection Agency (US EPA) (Xia et al., 2012). PAHs enter into the environment through diverse natural and anthropogenic activities such as forest fires, incomplete combustion of fossil fuels, waste incineration, industrial effluent, urban runoff, oil spills, and atmospheric fallout (Augusto et al., 2010; Suman et al., 2016; Wang et al., 2012). PAHs in marine environments have triggered extensive public concerns and scientific interests owing to its carcinogenicity, mutagenicity, and teratogenicity (Kim et al., 2013). These pollutants not only pose risk to fish and other aquatic organisms, but also bioaccumulate in marine organisms with possible transfer to humans via food chains (Luo et al., 2014; Zhang et al., 2017). PAHs may undergo many natural attenuation processes including adsorption, volatilization, photolysis, and chemical degradation (Haritash and Kaushik, 2009). Among these processes, biodegradation has been suggested as the major pathway for the decontamination of PAHs in nature (Haritash and Kaushik, 2009; Juhasz and Naidu, 2000). Besides bacteria (Pugazhendi et al., 2017; Wang et al., 2017), PAHs can also be biodegraded by algae (Chan et al., 2010; Diaz et al., 2015; Luo et al., 2014). An integrated approach of physical, chemical, and biological degradation may be adopted to get synergistically enhanced PAHs removal rates and to treat/remediate the contaminated sites in an ecologically favorable process (Haritash and Kaushik, 2009). Although bioremediation is capable of delivering long-lasting and low-cost solutions for PAHs pollution control, the remediation of coastal water polluted with PAHs at large scale is still a challenge.

Among the PAHs, phenanthrene (PHE) which has three aromatic rings per molecule, is known as a highly reactive compound, a human skin photosensitizer and mild allergen, and a potent inhibitor of gap junction intercellular communications (Sinha et al., 2012). Although *U. prolifera* is known to be associated with green tide, its ability to remove typical PAHs has not been evaluated. In this study, the removal of typical PAHs (PHE) using green tide algae *U. prolifera* was firstly investigated. The influence of different environmental factors on the removal of PHE was also evaluated. The final goal was to obtain initial information on the potential positive environmental benefit in the terms of the removal of harmful organic pollutants from coastal waters

during the outbreak of harmful green tide algae. PHE was chosen as a representative compound of PAHs to discuss *U. prolifera*'s environmental effects because 1) it is difficult to be bioremoved due to its low water solubility (1.29 mg L^{-1}) (Pedetta et al., 2013); 2) it has been detected with high frequency and concentration, ranging from ng L^{-1} in surface water or groundwater (Zhu et al., 2014) to $\mu\text{g L}^{-1}$ in several oil spill area (D'Sa et al., 2016); and 3) it is a model carcinogenic PAHs containing both "bay-region" and "K-region" (Muratova et al., 2015).

2. Material and methods

2.1. Reagents and materials

Phenanthrene (PHE, purity > 99%) was purchased from Aladdin (Shanghai, China). Phenanthrene- d_{10} purchased from Dr. Ehrenstorfer GmbH (Augsburg, Germany) was used as internal standard in GC-MS analysis. Methanol, acetonitrile, acetone, and dichloromethane used for ultra high performance liquid chromatography (UHPLC) and gas chromatography-mass spectrometry (GC-MS) were HPLC grade. Sodium nitrate, sodium hypochlorite, and sodium hydrogen phosphate were analytical reagents and used without further purification. Anhydrous sodium sulfate was analytical reagents and dried in a muffle furnace at $450 \text{ }^\circ\text{C}$ for 4 h prior to use. The stock solution of PHE (1 g L^{-1}) was weekly prepared by dissolving an appropriate amount of PHE in methanol in a volumetric flask and diluted with sterile sea water to target concentration before use.

2.2. *U. prolifera* and seawater for experiments

U. prolifera was collected in July 2016 from the coastal water (Rushan City, China) where there was an outbreak of green tide. In the laboratory, these algae were washed several times with sterile seawater, sterilized with 1% sodium hypochlorite for 2 min, and then rinsed with autoclaved seawater. *U. prolifera* was pre-cultured in plastic case with natural seawater without additional nutrients. *U. prolifera* was incubated at $10 \text{ }^\circ\text{C}$ with a dark/light cycle of 12/12 under an irradiance of $100 \mu\text{mol photons m}^{-2} \text{ s}^{-1}$ in GXZ-380B-LED temperature controlled incubator (Ningbo Jiangnan Inc., China), and transferred to an experimental incubator at a constant temperature of $20 \text{ }^\circ\text{C}$ under the same incubation condition for 72 h before running experiments. The incubated medium was completely renewed every week. Seawater was obtained from the coast of Yantai, China. Natural seawater was filtered through glass fiber papers (Whatman GF/C, $0.22 \mu\text{m}$ pore size) to eliminate organic particles and debris of organisms. This seawater was used for culture macroalgae in all experiments of this study.

2.3. Experimental setup

The removal efficiency of PHE from the solution by *U. prolifera* under different environmental factors was investigated in 500 mL beaker containing 400 mL sterilized seawater with relevant concentrations of PHE and algae. Each beaker was covered with sealing film to minimize the abiotic loss of PHE but allowed sufficient gas exchange during the experiment. All beakers were shaken twice at a set time every day to promote the mass transfer process.

For live treatment, the algae (4.0 g L^{-1}) were added into beaker. For the heat-killed treatment, algae with the same mass as the live treatment were autoclaved at $121 \text{ }^\circ\text{C}$ for 20 min before the assay. The beakers without any algae were used as the abiotic controls for monitoring any abiotic loss of PHE. The initial concentration of PHE ($10 \mu\text{g L}^{-1}$) were obtained by diluting the stock solution of PHE (1 g L^{-1}) with sterile sea water. Water and algae samples were collected at given time intervals, and the residual amounts of PHE in the media and the algal cells were determined. 0.5 mL aliquots were put into centrifuge tube containing 0.5 mL acetonitrile and centrifuged at 12,000 rpm for 6 min before UHPLC analysis.

Intertidal macroalgae are subject to fluctuations in physicochemical variables such as high light intensities, high (or low) salinity, temperature, nutrient deficiency, and desiccation (Cabello-Pasini et al., 2011), which may influence the uptake of organic pollutant in the algae. To explore the effect of different light regimes, the algae were exposed to darkness, a photoperiod 12:12 (light:darkness) and continuous light, i.e., a 24 h photoperiod. In order to evaluate the effect of salinity on the removal of PHE, the salinity of seawater was set as 16, 24, and 32 g L⁻¹. Seawater with lower salinity was prepared by diluting seawater with salinity of 32 g L⁻¹ with corresponding volume of distilled water. To investigate the influence of nutrient, a certain amount of sodium nitrate and sodium hydrogen phosphate stock solution (20 mM NO₃⁻/2 mM PO₄²⁻) was added to reach nutrient concentration of 0 μM (NO₃⁻)/0 μM (PO₄²⁻), 50 μM (NO₃⁻)/5 μM (PO₄²⁻) and 150 μM (NO₃⁻)/15 μM (PO₄²⁻). In addition, temperature was adjusted by temperature controlled incubator to 10 °C, 20 °C and 30 °C to observe the PHE removal efficiency by *U. prolifera*. To evaluate the influence of PHE initial concentration on removal efficiency, various initial concentrations of PHE were obtained by diluting the stock solution of PHE (1 g L⁻¹) with sterile sea water to 5, 10, 20, 50, and 100 μg L⁻¹. Algae-free controls experiments were also performed when evaluating the effect of abiotic factors (temperature, salinity, and nutrients) and there was no significant difference between these algae-free controls under different abiotic factors and none-algae with sterilization control group (CK₁) (not shown in results).

2.4. Extraction of PHE in macroalgae

To perform the extraction procedure, 2 g of fresh algae sample was powdered and homogenized with 5 μL internal standard solution (phenanthren-*d*₁₀, 100 mg L⁻¹), and then ultrasonically extracted with 30 mL methylenechloride/acetone (1:1 v/v) at room temperature for 15 min. The extracted liquid was cleaned using 2 g of anhydrous sodium sulfate and concentrated with a nitrogen evaporator until nearly dry, then reconstituted with 1.0 mL of dichloromethane prior to GC-MS analysis.

2.5. Analytical methods

The residual concentrations of PHE in water samples were monitored by a ACQUITY UHPLC system (Waters, Milford, USA) equipped with a C18 reverse phase column (2.1 × 50 mm, 1.7 μm) with H₂O/acetonitrile (20/80, v/v %) as the mobile phase at a flow rate of 0.3 mL min⁻¹. The injection volume was 10 μL, and the fluorescence of eluted compounds was monitored at 388 nm with excitation at 242 nm using a fluorescence detector (Waters, Milford, USA).

Algae samples acquired through extraction were analyzed by Agilent 7820A GC system (Agilent technologies Inc., Palo Alto, CA, USA) with a M7 single quadrupole MS system from Persee Co. (Beijing, China), equipped with a 30 m × 0.25 mm I.D. DB-5MS column (Agilent J&W Scientific, Palo Alto, CA, USA) coated with 5% diphenylpoly dimethyl siloxane (film thickness 0.25 μm). The injector was operated at 280 °C in splitless mode. Helium (>99.999% pure) was used as carrier gas at 1.0 mL min⁻¹ during the whole run. The temperatures of the transfer line and ion source were held at 280 °C and 230 °C. The column oven temperature program started at 100 °C for 1 min, then programmed to 200 °C at a 20 °C min⁻¹ and held for 1 min, finally to 290 °C at 30 °C min⁻¹ rate, and held for 5 min to comprise a total runtime of 14.57 min, including a 6 min solvent cut for all analyses. All target compounds were identified by full scan mode (*m/z* 50–400) based on their mass spectra and GC retention times. Subsequent acquisition and quantification was performed by a time scheduled selective ion monitoring (SIM) program. The quantitative and qualitative ions for PHE are *m/z* 176, 178, and 179, and that of phenanthren-*d*₁₀ are *m/z* 187, 188, and 189. The recovery for PHE was 81%.

To visualize the locations of PHE in live and heat-killed algae, the algae samples were observed with a laser scanning confocal microscope (LCSM, Olympus Fluoview FV1000, 40× objective lens). The laser wavelength of the LCSM was set at 405 nm. Images of PHE in/on the tissues of *U. prolifera* were collected and processed using the Olympus Fluoview Ver.2.1c Viewer software.

2.6. Data analysis

All experiments were performed in triplicate with independent replication of data (*n* = 3). The results were analyzed by using Origin 8.5 and SPSS 20.0. One-way ANOVA and Tukey's multiple comparisons were employed to compare the differences in the PHE removal efficiency among various treatments. The significance level was set at 0.05.

3. Results and discussion

3.1. The removal of PHE using *U. prolifera*

The removal of PHE by *U. prolifera* was observed during the incubation period (Fig. 1). After 31 days incubation, the concentrations of PHE in the culture medium of the none-algae with sterilization control group (CK₁), heat-killed *U. prolifera* (CK₂), the algae-added with sterilization (T₁), and algae-added without sterilization (T₂), reduced from 10.00 μg L⁻¹ to 4.84, 1.34, 0.80, and 0.82 μg L⁻¹, respectively. The removal efficiencies were 51.6%, 86.6%, 92.0%, and 91.8% for CK₁, CK₂, T₁, and T₂, respectively. The removal of PHE in the control treatment showed that the abiotic loss of PHE (mainly through photodegradation and volatilization) (Luo et al., 2014; Shang et al., 2015) could beyond 50%. The removal efficiency of PHE in the *U. prolifera* treatment was much higher than that in the control treatment, indicating that *U. prolifera* was engaged in the removal of PHE. PAHs could undergo many natural attenuation processes including biodegradation, adsorption, volatilization, photolysis, and chemical degradation (Haritash and Kaushik, 2009). The high removal efficiency of PHE in the presence of green tide algae *U. prolifera* demonstrated a potential new natural attenuation process for typical PAHs in coastal water during the outbreak of green tide. LCSM, which was a real-time tool for direct observation of organic pollutant within plant (Wang et al., 2012), was used in this study. PHE fluorescence was clearly observed in both live and heat-killed *U. prolifera* (Fig. 2), confirming the engagement of *U. prolifera* in PHE removal. The removal efficiency of PHE in the live algae treatments under both sterilization (T₁) and without sterilization (T₂) were similar, indicating that plant accumulation but not the microbial biodegradation was the main removal process in the presence of *U. prolifera*.

The PHE contents in live (T₁) and heat-killed algae (CK₂) were detected as 0.26 μg g⁻¹ and 0.76 μg g⁻¹, respectively, confirming the

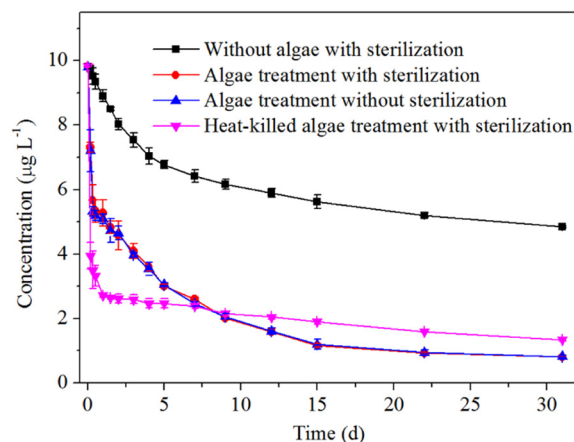


Fig. 1. Changes in phenanthrene concentrations in seawater during incubation.

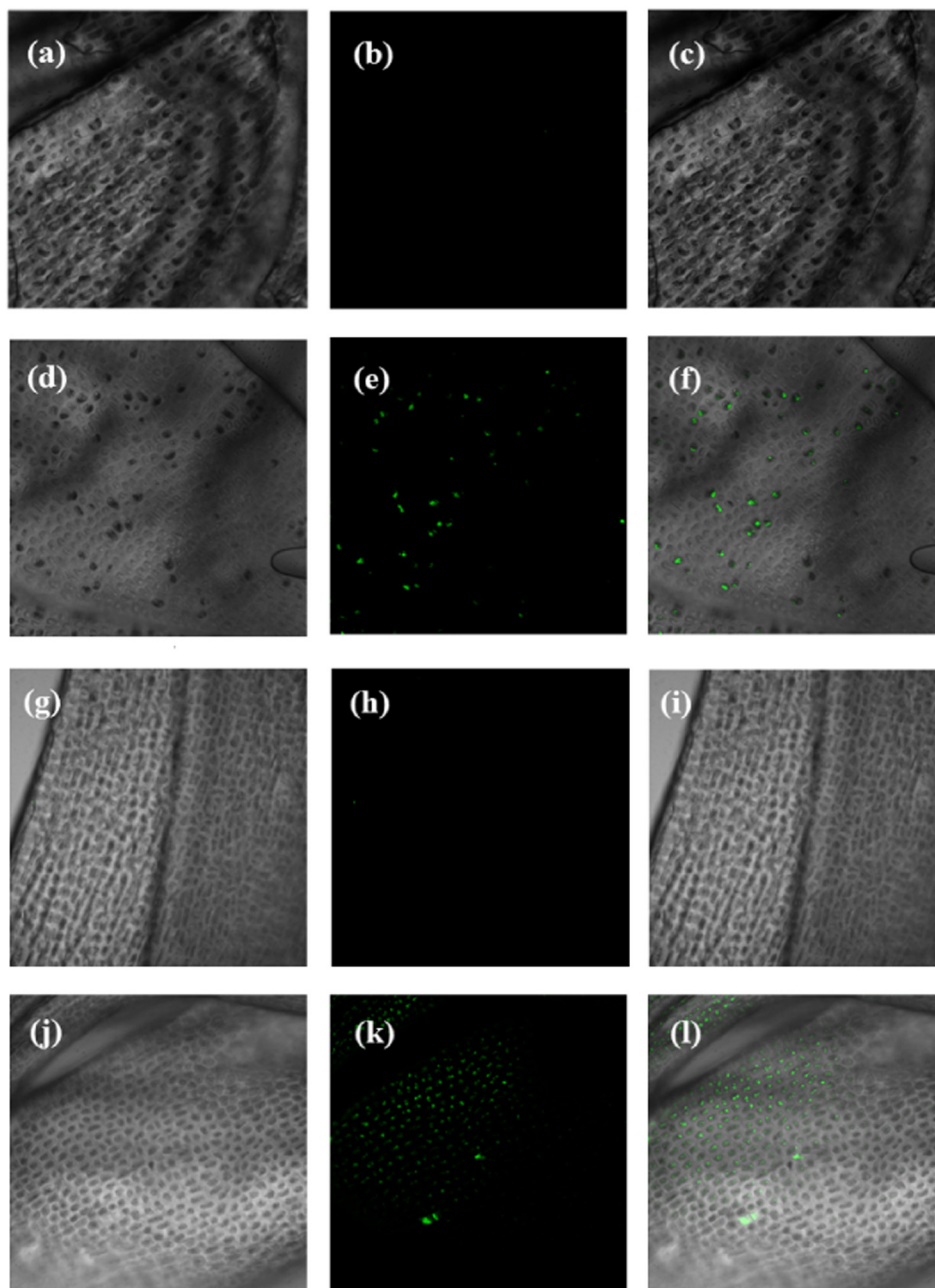


Fig. 2. Laser confocal scanning microscopy (LCSM) image of control group without phenanthrene in both live (a, b, c) and heat-killed (g, h, i) *U. prolifera* and phenanthrene distributed in both live (d, e, f) and heat-killed (j, k, l) *U. prolifera* under brightfield image (a, d, g, j), green fluorescence image (b, e, h, k) and overlay image (c, f, i, l) ($\times 10$, $\lambda_{\text{ex}} = 405 \text{ nm}$).

engagement of algae in the removal of PHE. According to the mass balance, 30.4% of the PHE was detected in the algae biomass in the heat-killed algae treatment (CK_2) while 10.4% of the PHE was detected in the live algae treatment (T_1). Since PHE was readily degraded in algae (Chan et al., 2010), the rational explanation was that the degradation of PHE in algae was also an important approach for the removal of PHE besides the abiotic loss ($> 50\%$) (mainly through photodegradation and volatilization) (Haritash and Kaushik, 2009).

Compared with the control without algae (CK_1), rapid removal of PHE occurred in the treatments with algae (CK_2 and T_1). According to Fig. 1, the PHE concentration decreased rapidly from $10.00 \mu\text{g L}^{-1}$ to $2.71 \mu\text{g L}^{-1}$ within one day in the presence of heat-killed *U. prolifera* (CK_2). Investigations have shown that dead algae possess impressive adsorptive removal for pollutants (Javadian et al., 2013). Luo et al. (2014) reported that Benz[a]anthracene and benzo[a]pyrene were highly transformed in both live and dead microalgae (*Selenastrum*

capricornutum), and dead cells displayed greater transformation levels than live cells. Dead *Selenastrum capricornutum* also showed a good performance on the removal of phenanthrene, fluoranthene, and pyrene (Chan et al., 2010). Similar rapid removal of PHE occurred first from day 0 to day 1 in the living algae treatments (T_1), followed with another rapid removal process occurring from day 1 to day 15, indicating that there were two-stage rapid removal processes in the living algae treatment. One reasonable explanation was that the PHE was mainly removed through a rapid adsorptive removal process and then followed a plant uptake process in the live algae treatments. The principle mechanism involved appears to be physico-chemical adsorption which is metabolism independent (Tam et al., 2002). Algae provided many potential binding sites to pollutants due to the presence of polysaccharides, proteins or lipid on their cell wall surfaces, thus the adsorptive removal process was similar for live and dead algal biomass (Avery et al., 1998). The process of heat-killing can increase the permeability of the cell wall of

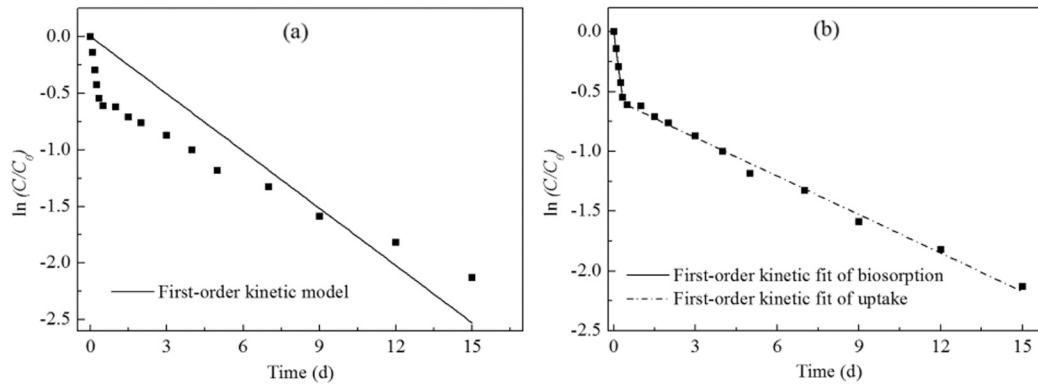


Fig. 3. (a) First-order kinetic equation fitting curves of the experimental data, and (b) two-stage first-order kinetic equations fitting curves of the adsorptive removal process and uptake process.

algae, and thereafter additional binding sites might become more available in dead algal cell in certain cases (Avery et al., 1998), which leads to the relatively high adsorptive removal efficiency in the heat-killed algae control (CK₂).

3.2. Removal kinetics

To better know the removal behaviors of PHE in the presence of *U. prolifera*, the removal kinetics was investigated. In this study, first-order kinetic (Eq. (1)) was used to correlate the experimental data:

$$\ln C_t = \ln C_0 - kt \quad (1)$$

where C_0 and C_t are PHE concentration at time 0 and t days, respectively; k (d^{-1}) is the first-order degradation rate constant.

The removal data did not fit first-order kinetic model well ($R^2 < 0.900$) (Fig. 3a). According to the removal data of the live algae treatment (T₁), it was supposed that the PHE was mainly removed through a rapid adsorptive removal process (process I) and then followed by a plant uptake process (process II) in the live algae treatment. Based on this hypothesis, two-stage first-order model was applied for the removal process (Fig. 3b). The constant k for the rapid adsorptive removal (k_a) was $1.69 d^{-1}$ ($R^2 = 0.999$), while that of the second-stage plant uptake process (k_u) was $0.11 d^{-1}$ ($R^2 = 0.993$).

3.3. Effect of photoperiod on PHE removal

According to Fig. 4, the light had influence on the removal of PHE. During the 31-day exposure with different photoperiod, the removal

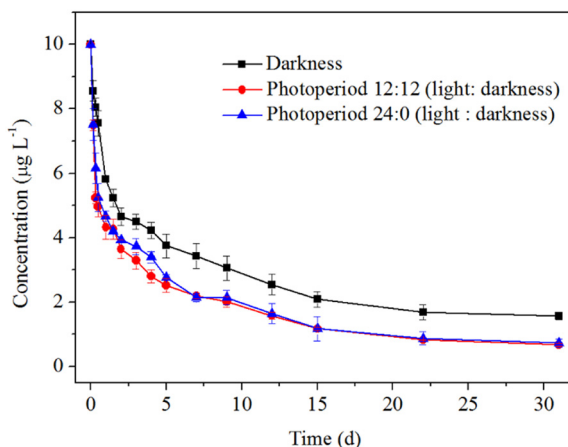


Fig. 4. Effect of photoperiod on the removal of phenanthrene by *U. prolifera*.

efficiency in the darkness treatment, photoperiod 12:12 (light: darkness) treatment, and photoperiod 24:0 (light:darkness) treatment were 84.2%, 91.8%, and 91.3%, respectively. The complete darkness had lower removal efficiency, confirming that PHE removal efficiency was influenced by light irradiation. According to Neumann et al. (2003), the complete darkness has lower algae Se removal rate compared with treatment with a 16 h light period. Algae need light for photosynthesis to convert light energy into chemical energy used for further metabolic activities (Singh and Singh, 2015). The complete darkness might inhibit the metabolic activities of *U. prolifera*, which subsequently led to the decrease in the removal efficiency of PHE. The removal of PHE in the photoperiod 12:12 (light:darkness) treatment was similar to that of the photoperiod 24:0 (light:darkness) treatment, indicating that the exposure time with light has no obvious influence on PHE removal.

3.4. Effect of salinity on PHE removal

In the case of salinity, an increase in salinity did not have a significant effect on the removal efficiency of PHE. The removal rate was found to be similar as the salinity increased from $16 g L^{-1}$ to $32 g L^{-1}$ (Fig. 5). Being an intertidal species, *U. prolifera* has wide salinity tolerance (Mou et al., 2013). For this reason, there was no effect of salinity on the removal of PHE.

3.5. Effect of nutrient on PHE removal

According to the experimental results (Fig. 6), the removal of PHE from the culture system was accomplished through two periods. At the first 7 days, PHE removal rate showed a tendency to increase as the nutrient concentration increased. The removal efficiencies under nutrient concentration of $0 \mu M (NO_3^-)/0 \mu M (PO_4^{2-})$, $50 \mu M (NO_3^-)/5 \mu M (PO_4^{2-})$, and $150 \mu M (NO_3^-)/15 \mu M (PO_4^{2-})$ were 73.5, 75.4, and 80.2%, respectively. The tendency of removal rate became similar during the last 24 days exposure because the added nutrient was depleted. The results of kinetic fitting showed that the k_a values were similar among these three treatments, while the k_u values could increase from $0.56 d^{-1}$ to $0.83 d^{-1}$ with the nutrient content increasing (Fig. 6). Thus, withdrawal of nutrients by *U. prolifera* in eutrophic water appeared to greatly enhance the removal rates of PHE.

3.6. Effect of temperature on PHE removal

Temperature strongly influences the cellular chemical composition, uptake of nutrients, and the growth rates of algae (Singh and Singh, 2015), which might have great influence on the removal of PHE in the presence of *U. prolifera*. Fig. 7 showed that the removal efficiency of PHE by *U. prolifera* was greatly influenced by temperature. The removal constant k_a at adsorption stage increased from $1.41 d^{-1}$ to $1.91 d^{-1}$, while

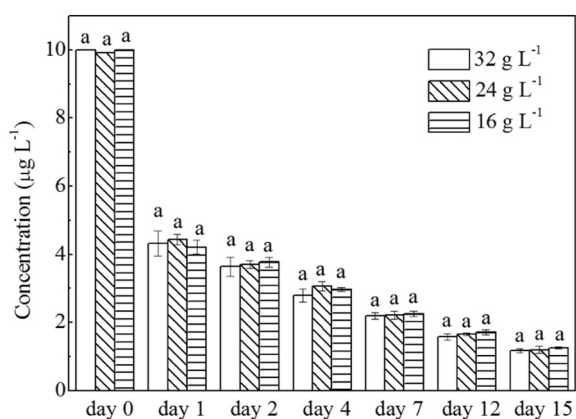


Fig. 5. Effect of salinity on the removal of phenanthrene by *U. prolifera*. Same letters on top of the bar indicate the means are not significantly different at $P \leq 0.05$ according to one-way ANOVA test.

the uptake constant k_{ii} increased slightly from 0.06 d^{-1} to 0.11 d^{-1} when the temperature increased from $10 \text{ }^\circ\text{C}$ to $30 \text{ }^\circ\text{C}$. The increase in temperature led to the increase in the removal efficiency of PHE, which was similar with other report on the removal of remazol black B dye using green alga *Chlorella vulgaris* (Aksu and Tezer, 2005).

3.7. Effect of initial concentration of PHE on PHE removal

Average removal rate as a function of initial concentration was shown in Fig. 8. Increase in the initial concentration of PHE resulted in increased average removal rate, accompanying with a linear relationship between initial concentration and the average removal rate ($R^2 = 0.999$) (Fig. 8). The maximum average removal rate could reach $5.77 \mu\text{g d}^{-1}$. It is generally accepted that the removal rate increases in linear proportion to the substrate concentration only at very low substrate concentrations while high initial concentration might have possible toxicity which would subsequently inhibit the removal efficiency by organisms (Lu et al., 2008). However, in our study, this linear relationship maintained even at relatively high initial concentration, indicating that the toxic effect had not occurred even at very high initial concentrations. According to previous investigation, the concentration of PAHs in water over the East China Sea ranges from 0.01 to about $2 \mu\text{g L}^{-1}$ (Men et al., 2009; Qiu et al., 2009; Wang et al., 2007). High PHE removal efficiency (91.3%) was achieved when the initial PHE concentration was set at environmental relevant concentration ($5 \mu\text{g L}^{-1}$), indicating that *U. prolifera* might efficiently remove PHE

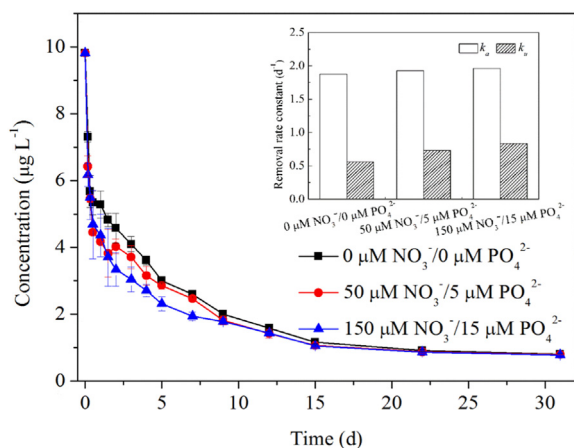


Fig. 6. Effect of nutrient on the removal of phenanthrene by *U. prolifera*. Inset: First-order rate constant for adsorptive removal (k_a), and plant uptake removal (k_{ii}) at different nutrient concentration.

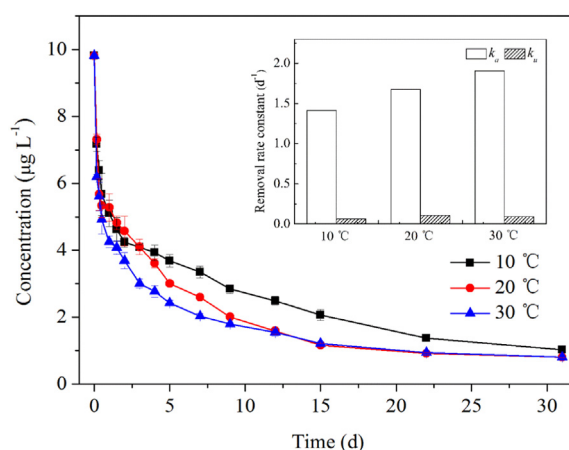


Fig. 7. Removal of phenanthrene by *U. prolifera* at different temperatures. Inset: First-order rate constant for adsorptive removal (k_a), and plant uptake removal (k_{ii}) at different temperatures.

from coastal water within its floating area during the outbreak of green tide.

4. Conclusions

Results of this study demonstrate a potential new natural attenuation process for typical PAHs in coastal water during the outbreak of green tide. The efficient removal of PHE in the presence of *U. prolifera* collected from the coastal water during the outbreak of green tide was observed. The nutrient and temperature had positive influence on the removal efficiency of PHE. The ability of *U. prolifera* on contaminant removal can be effective in coastal water under various saline conditions since the salinity had no significant effect on PHE removal efficiency. The removal efficiency by *U. prolifera* had a good linear relationship with PHE initial concentration even at $100 \mu\text{g L}^{-1}$ which was higher than its environmentally relevant concentrations. High removal efficiency was observed even when the initial PHE concentration was set at environmental relevant concentration, indicating that *U. prolifera* might efficiently remove PHE from coastal water within its floating area during the outbreak of green tide. These findings indicate that the outbreak of harmful green tide algae may bring positive environmental benefit in the terms of removing harmful organic pollutants from the coastal waters.

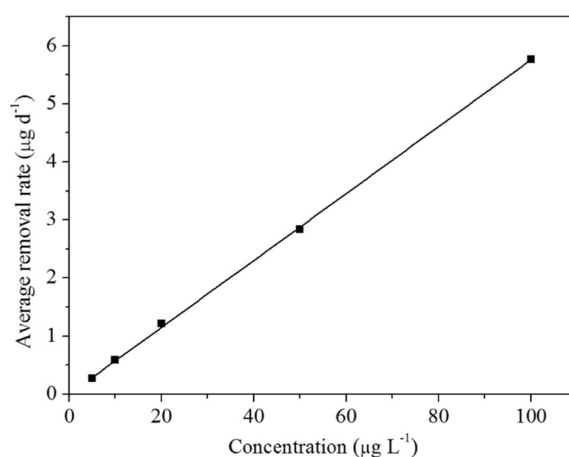


Fig. 8. Average removal rate as a function of the initial concentration of phenanthrene ($R^2 = 0.999$).

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