

Copyright is owned by the Author of the thesis. Permission is given for a copy to be downloaded by an individual for the purpose of research and private study only. The thesis may not be reproduced elsewhere without the permission of the Author.

Growth of *Streptococcus bovis* and a
Butyrivibrio in batch and continuous
culture and the relationship of molar
growth yield to intermicrobial
competition

A thesis presented in partial fulfillment
of the requirements for the degree of
Master of Science in Microbiology at
Massey University

Roderick Vincent Asmundson

1974

ABSTRACT

Cell growth yield of Streptococcus bovis and Butyrivibrio were determined in batch cultures where growth was separately limited by glucose, CO₂ and trypticase. With S. bovis, glucose limited growth, and a Y_g of 39.6 g / M in the presence of excess CO₂ was determined. S. bovis grew in the absence of CO₂, but the Y_g was reduced to 16.5 g / M. In the presence of excess CO₂, the Y_g determined for Butyrivibrio was 55 g / M. Butyrivibrio was strictly limited by CO₂ and the Y_{CO₂} was equal to Y_g. This led to the suggestion that CO₂ metabolism allows the generation of at least two additional ATP when combined with glucose metabolism for both organisms.

Monod growth constants were determined for both organisms in continuous culture under glucose limitation. K_s and μ_{\max} for S. bovis were 0.429 mM / l and 2.47 hr⁻¹, respectively. For Butyrivibrio, K_s and μ_{\max} were 0.332 mM / l and 0.704 hr⁻¹, respectively. The cell growth yields for S. bovis and Butyrivibrio were determined to be 39.6 g / M and 69.1 g / M, respectively. At growth rates less than 0.2 hr⁻¹ colony forming units and total cell counts of S. bovis decreased, but cell yield did not. Colony forming units, total counts and cell growth yield of Butyrivibrio did not decrease at low growth rates.

When S. bovis and Butyrivibrio were grown in continuous mixed culture, Butyrivibrio dominated at growth rates below 0.5 hr⁻¹ and growth of S. bovis was strongly depressed. That Butyrivibrio dominated mixed cultures supports the proposition that an organism deriving more ATP per mole of substrate than another will dominate in environments comparable with continuous culture. The roles of maintenance energy, K_s and μ_{\max} and cell yield in competition are considered.

ACKNOWLEDGEMENTS

Dr. B. D. W. Jarvis, for much useful advice

Mr. A. G. McCulloch for all methods of scintillation
counting and autoradiography

Dr. R. T. Clarke, for providing the bacterial
cultures

Mr. P. P. Roche, for assistance with the glassblowing
and entertainment

Table of Contents

Abstract	ii
Acknowledgements	iii
Table of Contents	iv
List of Figures	vii
List of Tables	viii
List of Plates	ix
Section I: Introduction and Statement of Purpose	1
Section II: Methods	6
1. Medium: Constituents and Preparation	6
1.1. Standard Medium	6
1.2. Preparation of Medium for Continuous Culture	7
2. Batch Culture Apparatus	8
2.1. Standard Roll Tubes	8
2.2. Nephelometer Flasks	8
2.3. Large Batch Culture Flasks	8
3. Continuous Culture Apparatus	11
3.1. Carbon Dioxide System	11
3.2. Medium Reservoir	14
3.3. Pump	14
3.4. Temperature Control	15
3.5. Growth Vessel	16
4. Analytical Methods	18
4.1. Glucose	18
4.2. Lactic Acid	18
4.3. Volatile Fatty Acids	22
3.1. Thin Layer Chromatography	22
3.2. Steam Distillation	22
4.4. Determination of Dry Weight	23
4.5. Determination of Colony Forming Units	23
4.6. Direct Microscopic Counts of Cells	24

II.4.7.	Radiometric Methods	25
7.1.	Scintillation Counting and Method of Correcting Counts (CPM to DPM)	25
7.2.	Methods of Sample Collection	26
2.1.	Collection of Cells	26
2.2.	Collection of Gasses	26
2.3.	Collection of Spots from Thin Layer Chromatography	26
7.3.	Scintillation Fluid: Composition and Sample Mixing	27
4.8.	Autoradiography	28
8.1.	Acid Hydrolysis of Cells	27
8.2.	Thin Layer Chromatography of Acid Hydrolysates	28
Section III: Results		
III.1.	Batch Culture Results	
1.1.	Batch Culture of Sbl	
1.1.	Cultural Characteristics	29
1.2.	Growth Yield of Sbl with Glucose	33
1.3.	Growth Yield of Sbl with Trypticase	38
1.4.	Growth Yield of Sbl with CO ₂	43
5.1.	Retention of ¹⁴ C Glucose and ¹⁴ CO ₂	47
5.2.	Account of Total Label of ¹⁴ C Glucose and ¹⁴ CO ₂ fed cells	48
1.2.	Batch Culture of W1	
2.1.	Cultural Characteristics	55
2.2.	Growth Yield of W1 with Glucose	55
2.3.	Growth Yield of W1 with Trypticase	58
2.4.	Growth Yield of W1 with CO ₂	58
2.5.	Retention of ¹⁴ C Glucose and ¹⁴ CO ₂ by W1	62

III.2.	Continuous Culture Results	
2.1.	Continuous Culture of <u>Streptococcus bovis</u>	
1.1.	Initiation of Continuous Culture	70
1.2.	Determination of Equilibration Time	70
1.3.	Equilibrium Results for Sb1	71
1.4.	Cell Dry Weight Results for Sb1	78
1.5.	Determination of Monod Constants for Sb1	78
2.2.	Continuous Culture of Butyrivibrio	
2.1.	Equilibrium Results for W1	78
2.3.	Cell Dry Weight Results for W1	83
2.4.	Determination of Monod Constants for W1	83
2.3.	Continuous Mixed Culture of Sb1 and W1	
3.1.	Inoculation Procedure and Results of Growth at $D = 0.36 \text{ hr}^{-1}$	92
3.3.	Mixed Continuous Culture at Low Growth Rates	95
Section IV: Discussion and Conclusions		
IV.1.	Culture Identities	112
IV.2.	Batch Culture	112
IV.3.	Continuous Monocultures	116
IV.4.	Continuous Mixed Cultures	118
IV.5.	Conclusions	119

.....

Bibliography

List of Figures

- Figure 1: Diagrams of Batch & Continuous Culture Fittings
- Figure 2: Diagram of Continuous Culture Apparatus
- Figure 3: Standard Curve for Glucose Estimation
- Figure 4: Standard Curve for Lactate Estimation
- Figure 5: Batch Growth of Sbl: Cell Yield with Glucose
- Figure 6: Batch Growth of Sbl: Cell Yield and Other Parameters of Growth with Glucose
- Figure 7: Visible Light Absorption Spectrum of Pigment Produced by Sbl
- Figure 8: Batch Growth of Sbl: Cell Yield with Trypticase
- Figure 9: Batch Growth of W1: Cell Yield with Glucose
- Figure 10: Batch Growth of W1: Cell Yield with Trypticase
- Figure 11: Continuous Culture of Sbl: Summary of CFU with D
- Figure 12: Continuous Culture of Sbl: Summary of Total Counts
- Figure 13: Continuous Culture of Sbl: Summary of Cell Yield
- Figure 14: Continuous Culture of Sbl: Lineweaver-Burke Plot
- Figure 15: Continuous Culture of W1: Summary of CFU and Total Cell Counts
- Figure 16: Continuous Culture of W1: Summary of Cell Yield
- Figure 17: Continuous Culture of W1: Lineweaver-Burke Plot
- Figure 18: Continuous Culture of W1: Summary of Glucose Determination
- Figure 19: Continuous Mixed Cultures of Sbl and W1: $D = 0.36 \text{ hr}^{-1}$
- Figure 20: " " " " " " " " 0.34 "
- Figure 21: " " " " " " " " 0.36 "
- Figure 22: " " " " " " " " 0.018 "
- Figure 23: " " " " " " " " 0.058 "
- Figure 24: " " " " " " " " 0.058 "
- Figure 25: " " " " " " " " 0.057 & 0.58 hr^{-1}

List of Tables

Table 1: Growth of Sb1 and W1 with a Variety of Substrates

Table 2: Growth of Sb1 with CO₂ at 3 mM PO₄

Table 3: Growth of Sb1 with CO₂ at 25 mM PO₄

Table 4: ¹⁴C glucose Retention by Sb1 at Differing Initial Levels of
Glucose

Table 5: ¹⁴C Labelled Glucose and CO₂ Retention by Sb1

Table 6: ¹⁴C Labelled Glucose and CO₂ Retention by Sb1

Table 7: TLC of Steam Distillate of Culture Supernatant of Sb1

Table 8: TLC of Supernatant of ¹⁴C Labelled Cultures of Sb1.

Table 9: Autoradiogram of Sb1 Labelled With ¹⁴C Glucose

Table 10: Growth of W1 with CO₂ at 3 mM PO₄

Table 11: Growth of W1 with CO₂ at 25 mM PO₄

Table 12: Retention of ¹⁴C-labelled Glucose and CO₂ by W1

Table 13: TLC of Steam Distillate of Culture Supernatant of ¹⁴C labelled
Cultures of W1

Table 14: TLC of Supernatant of ¹⁴C Labelled Cultures of W1

Table 15: Autoradiogram of W1 Labelled with ¹⁴C Glucose

List of Plates

Plate 1: Surface and Sub-surface Colony of SB1

Plate 2: Capsule of Sbl

Plate 3: Sbl Grown Without CO₂

Plate 4: Sbl Grown With CO₂

Plate 5: Sub-surface Multi-lobed Colony of WV1

Plate 6: Complete Surface Colony of WV1

Plate 7: Rhizoid Surface Colony of WV1

Plate 8: WV1 Grown on Low CO₂

Plate 9: WV1 Grown on High CO₂

Plate 10: Continuous Culture of Sbl, Pigment Production

Plate 11: Cells From Continuous Mixed Culture at Low Dilution Rate

Introduction

The bovine rumen is a semi-continuously fed culture which contains a wide variety of protozoa and bacteria. These microorganisms obtain their energy and nutrients by fermenting the food eaten by the animal and the animal in turn obtains energy by absorbing the end products of the microbial fermentation and digests the microorganisms themselves. Volatile fatty acids which cannot be metabolized anaerobically in the rumen are absorbed by the ruminant and metabolized aerobically to provide energy for the synthesis of glucose (Hungate, 1966). The microorganisms are digested in the abomasum and duodenum and constitute a major source of protein for the animal.

The stoichiometry of the rumen fermentation has been a topic of interest because of its direct implications in the bovine nutrition. Approximately 75 % of the available carbohydrate is converted to fatty acids, which are utilized by the animal (Barcroft, et al, 1944). That microbial protein synthesis is capable of supporting ruminant growth has been shown (Loosli, et al, 1949; Virtanen, 1966). The actual amount of protein available to the cow in the form of microbial cells has been estimated by a number of means but the precise amount remains indefinite, chiefly due to the difficulty of separating the microbes from the other rumen contents (Walker & Nader, 1968). The 10 g of microbial protein synthesized per 100 g of carbohydrate estimated as maximum by Hungate (1966) has been increased by later authors using label incorporation (Walker and Nader, 1968; Al-Rabbat et al, 1971; Pilgrim, et al, 1970) and phospholipid synthesis (Bucholtz & Bergen, 1973). From these increases has come the suggestion that the average yield of cell material per hexose, and hence the number of ATP derived from each hexose, in the rumen should be increased.

Butyrivibrio fibrisolvens is a rumen organism that ferments carbohydrates to

CO₂, H₂, ethanol, and acetic, butyric, formic and lactic acids (Hungate, 1966). It is a common rumen organism which usually occurs in the rumen at a concentration of at least 10^8ml^{-1} (Bryant & Burkey, 1953). The production of significant quantities of butyric acid and the numbers present in the rumen indicate that Buyrivibrio contributes significantly to metabolism in the rumen (Bryant & Small, 1956).

Streptococcus bovis is also a rumen organism, which is not normally found in the ruminant diet. Although S. bovis can always be isolated from rumen contents, its numbers seldom exceed 10^7ml^{-1} , and its main fermentation product is lactate (Hungate, 1966). It has been shown that the lactate pool in rumen contents is normally small and turns over slowly (Jayasuriya & Hungate, 1959). Consequently, S.bovis has been considered an organism not contributing greatly to ruminant metabolism (Hungate, 1966). However, conversion of lactate to volatile fatty acids in whole rumen contents has been demonstrated (Nakamura & Takahashi, 1971) and lactate may be considered a normal intermediate in the rumen fermentation.

Under certain conditions, when the ruminant diet is shifted from low to high carbohydrate, the production of lactic acid can increase to such an extent that acid indigestion results due to the inability of the digesta to metabolize lactic acid as rapidly as it is produced. When this occurs, the concentration of S.bovis is found to have increased to the vicinity of $5 \times 10^9 \text{ml}^{-1}$ and is considered one of the most significant contributors to acid indigestion. The ability of S.bovis to generate such high numbers appears to be due to its high maximum specific growth rate (a doubling time of 20 minutes).

The fact that S.bovis has a high maximum rate of growth and yet normally exists in low numbers has been explained in two ways. In animals shifted to high grain diets, high concentrations of S.bovis occur for a period of time, but in well adapted animals, the numbers are similar to those found in animals receiving a low grain diet. This has been

attributed to the establishment of a new equilibrium population in which it is possible that the S. bovis serve as food for an enlarged protozoan population. An alternative suggestion for the normally low concentration of S. bovis has been its poor ability to compete due to its relatively inefficient energy yielding metabolism in contrast to other rumen bacteria.

It has been generally accepted that established pathways of energy metabolism generate predictable yields of high energy intermediates, such as ATP, and that these are used to synthesize new cell material with constant efficiency. This constant, as determined by Bauchop & Elsdon (1960) is 10.5 g per mole of ATP. This constant has been verified for a variety of microorganisms (Forrest & Walker, 1971) and used widely for its predictive value. In 1966, Hungate suggested that "... in the competition to achieve maximum growth, selection is against lactic acid and ethanol production. Formation of each of these products entails loss of available ATP. Conversion of pyruvate to acetyl CoA and the reduction of acetyl CoA to ethanol similarly entails loss of a potential ATP. The acetyl-CoA can yield an ATP unless it must be used for hydrogen disposal... according to this view, the propionate formed in the rumen represents additional synthesis of ATP. This is also true for acetate on the hypothesis that pyruvate is split to acetyl CoA. A production of ATP in butyrate formation has been surmised, but efforts to demonstrate it have been unsuccessful. If there is a selection for maximum biochemical work, butyrate should also represent an end product accompanying additional energy conservation by the cell.

According to these views, the carbon dioxide, methane, acetate, propionate and butyrate, final products in the rumen fermentation, are formed because pathways leading to them provide the most efficient conversion of fermentable substrate into microbial cells."

The purpose of the research reported in this thesis was to test the proposition that an organism which derives a relatively low yield of two ATP per mole of glucose fermented will not be able to compete with an organism which can derive additional ATP by metabolism of pyruvate to acetate, propionate or butyrate. Two organisms were chosen for the experiments, S. bovis, which is a homofermenter and was expected to derive only two ATP per mole of glucose (Hungate, 1966) and Butyrivibrio fibrisolvens, which produces primarily formic and butyric acid and was expected to derive a larger number of ATP per mole of glucose fermented.

Continuous culture must be used to study competition based on substrate utilization because the outcome in batch culture will depend simply on the maximum specific growth rate and the duration of the lag phase for each organism. The organism with the larger maximum specific growth rate and shorter lag phase will always dominate if growth of both organisms is limited by the same substrate. Continuous culture in a chemostat allows this type of competition to be studied by limitation of the culture to a specific growth rate. Both organisms will have the same specific growth rate, and assuming equal affinity for substrate, dominance will depend on the efficiency with which the organism utilizes the substrate to synthesise new cell material.

The equations of continuous culture were originally derived by Monod (1950) and subsequently by Herbert et al (1956). Equations of significance to the work in this thesis are the following:

A. Dependence of specific growth rate on substrate concentration

$$\mu = \mu_{\max} S / (K_S + S) \quad \text{equation (1)}$$

μ = specific growth rate

μ_{\max} = maximum specific growth rate

K_S = substrate concentration at which $\mu = \frac{1}{2} \mu_{\max}$

S = substrate concentration

B. The inverse of equation (1) provides a graphical means of determining the constants μ_{\max} and K_S . A plot of equation (2) is called a Lineweaver-Burke plot.

$$1 / \mu = 1 / \mu_{\max} + (K_S / \mu_{\max}) 1 / S \quad \text{equation (2)}$$

C. Molar growth yield

$$Y_g = x / (S_r - S) \quad \text{equation (3)}$$

Y_g = grams cells produced per mole of substrate consumed

x = dry weight of cells in grams per liter

S_r = original or reservoir concentration of substrate

S = final or growth vessel concentration of substrate

Variations on these equations (Van Uden, 1969; Powell, 1967) due to the inconstancy of Y_g and the occurrence of maintenance metabolism will be considered in the discussion in regard to the results shown in Section III of this thesis. Awareness that these variations can occur led me to measure parameters necessary for the determination of viability (total and colony forming units (CFU) counts) and yield (dry weight) in continuous culture experiments.