

Copyright is owned by the Author of the thesis. Permission is given for a copy to be downloaded by an individual for the purpose of research and private study only. The thesis may not be reproduced elsewhere without the permission of the Author.

# **A Study of the Importance of Secondary Reactions in Char Formation and Pyrolysis**

**A dissertation presented in partial fulfilment  
of the requirements for the degree of**

**Doctor of Philosophy  
in  
Process Engineering**

**at Massey University, Manawatū,  
New Zealand.**

**Georg Dietrich Ripberger**

**2016**



## Abstract

Anthropogenic climate change, caused primarily by excessive emissions of carbon dioxide, has led to a renewed interest in char, the solid product of pyrolysis. When applied to soil as biochar it can both sequester carbon and improve soil function. To make its manufacture environmentally friendly and economically viable it is important to maximise char yield, which can be done by promoting secondary reactions.

This research shows that secondary reactions, which are enhanced by prolonged vapour-phase residence time and concentration, not only increase the char yield but are the source of the majority of the char formed. All four biomass constituents (extractives, cellulose, hemicellulose and lignin) undergo secondary reactions concurrent with primary reactions over the entire pyrolysis range  $\approx 140$  to  $500$  °C, which makes it practically impossible to separate them. Secondary char formation was confirmed to be exothermic which affects the overall heat of pyrolysis. Impregnating the feedstock with the elements K, Mg and P, which are plant macro-nutrients naturally present in biomass, resulted in the catalysis of secondary char formation. The results reveal that a first order reaction model does not describe pyrolysis accurately when char formation is enhanced by catalysis and secondary reactions.

Secondary char can be enhanced by increasing the particle size but there is a limit due to increased cracking and fracturing of the pyrolysing solid. This limitation is overcome by pyrolysis in an enclosed vessel, termed autogenous pressure pyrolysis, which was discovered to cause significant changes in the volatile pyrolysis products; indicating the co-production of a high quality liquid. This process, however, negatively affects the char properties relevant for biochar like the surface area, similar to self-charring and co-carbonisation of condensed volatile pyrolysis products. To increase research capabilities a unique high temperature/ high pressure reactor ( $600$  °C at  $20$  MPa) was designed to allow the detailed characterisation of all three pyrolysis product classes under extreme pyrolysis conditions. This was demonstrated to be invaluable for understanding the underlying pyrolysis mechanism and physical processes at play.



## Acknowledgements

Doing research is a bit like a quest into the unknown. Over the past few years I embarked on my own journey to discover the unknown, and shed some light onto it. There are a few people who helped me along the way, who I would sincerely like to thank:

My principal supervisor Professor Jim Jones and co-supervisor Professor Tony Paterson whose guidance and mentorship throughout this journey has been invaluable. They helped me to conquer the seemingly ever-increasing mountain of research questions and provided me with many opportunities to further my knowledge and gain experience for the tasks ahead. I am grateful for their continuous support, ideas, and encouragement.

The fourth year students Fatima Bashir, Uchena Evanson, Craig Kirwan, Hani Mohd-Hanif, Saleh Alyami and Nadeem Caco who contributed with their final year research projects to the outcome of this quest.

John McDonald-Wharry from the University of Waikato, who I would like to thank for taking SEM images, doing Raman analysis, and the helpful discussions and comments about char chemistry and the nanostructural development.

Associate Professor Marta Camps, Roberto Calvelo Pereira, Tao Wang, Laura Munoz and everyone from the New Zealand Biochar Research Centre for assisting me with experiments, and helping me to understand the complexities of biochar and its intricate interplay with soil.

Professor Peter Buurman, Barry Scott and Bruce Fraser for their help with Py/GC-MS, and the team from DKSH New Zealand for their support with elemental analysis.

Rhonda Bridges for her help with experiments during her Masters, and for being a friend and running partner; keeping me physically fit for the challenges of this journey.

Clive Bardell, Bruce Collins, Ian Thomas, Anthony Wade, and all the workshop team from the School of Engineering and Advanced Technology that provided the specialised equipment needed for my PhD endeavour. Special thanks goes also to the

team from Worley Parsons New Zealand and Fitzroy Engineering Ltd for their expertise in designing the high temperature/ high pressure reactor.

The academic staff, in particular Professor John Bronlund, Professor Robert McLachlan, and Colin Brown for their assistance with modelling; Mike Bretherton, Ian Furkert, John Sykes, and all the technical staff that helped with the analytical equipment and its maintenance. A special thank you goes to John Edwards for always making time, organising all the bits-and-pieces, and for giving me ideas on how to tackle the problems encountered; Ann-Marie Jackson, the Lab Manager; Nick Look and Michael Lusby for IT support; Glenda Rosoman, Gayle Leader and all the administrative staff that were part of making this project possible.

I would also like to acknowledge my fellow explorers Eli, Grace, Ian, Julawit, Sadia, Shakti, Sureewan, Tawan, Tiyaporn and all the others in the postgraduate office not named here, who offered their friendship and company while embarking on their own journey.

Last but not least, many special thanks go to my family back in Germany and my New Zealand family. Their support and backing seems to have no boundaries, and they are the best cheerleaders one could ever ask for. Especially, I would like to thank my wife Amber Rose for being so understanding about the commitment such a task takes and sacrificing her personal time with me so I could immerse myself into the world of research.

Like an expedition into the wild, this journey was not a single person's effort. One can only be as good as the team that supports them; imparting their knowledge, wisdom, and insight along the way. Thus, journeys are not defined by reaching the finish line, but rather by the experiences we gain, the people we meet, and the friendships we develop. I have been privileged to be part of a great team that made this journey possible to whom I am greatly indebted.

# Statement of Contribution to Doctoral Thesis Containing Publications

## List of Publications

### Report:

Ripberger, G. D. (2012). *Biochar pyrolysis engineering* [PhD Confirmation Report]. Massey University, Palmerston North, New Zealand.

[PhD Confirmation Report]

### Conference presentations:

Ripberger, G. D., Jones, J. R., Paterson, A. H. J., & Holt, R. (2015, September/October). *Is it possible to produce biochar at different highest treatment temperatures in the pyrolysis range?—The exothermic nature of pyrolysis*. Paper presented at the APCChE 2015 Congress incorporating Chemeca 2015, Melbourne, Australia.

[Conference Oral Presentation & Peer Reviewed Paper; Speaker: Georg Ripberger]

Ripberger, G. D., Jones, J. R., Paterson, A. H. J., & Holt, R. (2013, September). *Temperature regime of secondary char forming reactions in the pyrolysis of radiata pine*. Paper presented at the Chemeca 2013: Challenging Tomorrow conference, Brisbane, Australia. Paper retrieved from <http://www.conference.net.au/chemeca2013/papers/25402.pdf>

[Conference Oral Presentation & Peer Reviewed Paper; Speaker: Georg Ripberger]

Ripberger, G. D., Kirwan, C., Jones, J. R., & Paterson, A. H. J. (2014, October). The intricate relationship between vapour phase residence time and biochar/biofuel yield properties. In R. Craggs (Chair), *Next generation liquid biofuels and co-products science symposium: Session three*. Symposium conducted at the meeting of the Advanced Biofuels Research Network (ABRN), Rotorua, New Zealand.

[Conference Oral Presentation; Speaker: Georg Ripberger]



Ripberger, G. D., Kirwan, C., Jones, J. R., & Paterson, A. H. J. (2014, September). The intricate relationship between vapour phase residence time and biochar/biofuel yield properties. In D. Elliott (Chair), *Symposium on thermal and catalytic sciences for biofuels and biobased products: Pyrolysis session 3*. Symposium conducted at the TCS2014 conference, Denver, CO.

[Conference Oral Presentation; Speaker: Georg Ripberger]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2014, May). The science of producing biochar effectively. In H. Ohtani (Chair), *Presentation Session 5: Applied Pyrolysis*. Symposium conducted at the Pyro2014 20th International Symposium on Analytical and Applied Pyrolysis, Birmingham, United Kingdom.

[Conference Oral Presentation; Speaker: Georg Ripberger]

McDonald-Wharry, J., Ripberger, G. D., Manley-Harris, M., & Pickering, K. (2013, July). Studying carbonisation with raman spectroscopy. In R. Calvelo Pereira (Chair), *Session 2: Formation, characterisation and monitoring of biochars*. Symposium conducted at the New Zealand 2013 Biochar Workshop, Palmerston North, New Zealand.

[Conference Oral Presentation; Speaker: J. McDonald-Wharry]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2013, July). Secondary char formation. Part 1. It's role, potential and limitations in the manufacture of biochar. In R. Calvelo Pereira (Chair), *Session 2: Formation, characterisation and monitoring of biochars*. Symposium conducted at the New Zealand 2013 Biochar Workshop, Palmerston North, New Zealand.

[Conference Oral Presentation; Speaker: Georg Ripberger]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2013, July). Secondary char formation. Part 2. Questions to be answered. In R. Calvelo Pereira (Chair), *Session 2: Formation, characterisation and monitoring of biochars*. Symposium conducted at the New Zealand 2013 Biochar Workshop, Palmerston North, New Zealand.

[Conference Oral Presentation; Speaker: Georg Ripberger]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2012, February). The necessity for a char formation model, In *Session 3: Production Technology*. Symposium conducted at the New Zealand 2012 Biochar Workshop, Palmerston North, New Zealand.

[Conference Oral Presentation; Speaker: Georg Ripberger]

**Conference posters:**

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2015, November). *Designing a pyrolysis reactor that creates new research capabilities*. Poster presented at tcbiomass2015: Technology for the Bioeconomy, Chicago, IL.

[Conference Poster; Presented by Georg Ripberger]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2015, September/October). *Designing a pyrolysis reactor that creates new research capabilities*. Poster presented at the APCCChE 2015 Congress incorporating Chemeca 2015, Melbourne, Australia.

[Conference Poster; Presented by Georg Ripberger]

Ripberger, G. D., Kirwan, C., Jones, J. R., & Paterson, A. H. J. (2014, September/October). *Effect of autogeneous pressure on volatile pyrolysis products*. Poster presented at Chemeca 2014: Processing excellence; Powering our future, Perth, Australia.

[Conference Poster; Presented by Georg Ripberger]

Ripberger, G. D., Kirwan, C., Jones, J. R., & Paterson, A. H. J. (2014, May). *Effect of autogeneous pressure on volatile pyrolysis products*. Poster presented at the Pyro2014 20th International Symposium on Analytical and Applied Pyrolysis, Birmingham, United Kingdom.

[Conference Poster; Presented by Georg Ripberger]

Ripberger, G. D., Jones, J. R., Paterson, A. H. J., & Holt, R. (2014, May). *The role of secondary char formation in the manufacture of biochar*. Poster presented at the Pyro2014 20th International Symposium on Analytical and Applied Pyrolysis, Birmingham, United Kingdom.

[Conference Poster; Presented by Georg Ripberger]

Ripberger, G. D., Jones, J. R., Paterson, A. H. J., & Holt, R. (2014, May). *Temperature regime of secondary char forming reactions in the pyrolysis of radiata pine*. Poster presented at the Pyro2014 20th International Symposium on Analytical and Applied Pyrolysis, Birmingham, United Kingdom.

[Conference Poster; Presented by Georg Ripberger]

Bridges, R. P., Jones, J. R., Ripberger, G. D., & Paterson, A. H. J. (2014, May). *Design and characterisation of a distributed biochar reactor*. Poster presented at the Pyro2014 20th International Symposium on Analytical and Applied Pyrolysis, Birmingham, United Kingdom.

[Conference Poster; Presented by Georg Ripberger]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2012, September). *Modelling secondary char formation reactions — Implication for the manufacture of biochar*. Poster presented at Chemeca 2012: Quality of life through chemical engineering, Wellington, New Zealand.

[Conference Poster; Presented by Georg Ripberger]

### **Seminars:**

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2014, June). *Die Wissenschaft von einer effektiven Herstellung von Biokohle (The science of producing biochar effectively)*. Oral presentation presented at the Leibniz-Institut für Agrartechnik Potsdam-Bornim e.V., Potsdam, Germany.

[Oral Presentation; Speaker Georg Ripberger]

Ripberger, G. D., Jones, J. R., & Paterson, A. H. J. (2014, May). *The science of producing biochar effectively*. Oral presentation presented at the UK Biochar Research Centre, Edinburgh, Scotland, United Kingdom.

[Oral Presentation; Speaker Georg Ripberger]

Ripberger, G. D., Jones, J. R., Paterson, A. H. J., & Holt, R. (2013, September). *Wood pyrolysis – Why size matters*. Oral presentation presented at Callaghan Innovation, Wellington, New Zealand.

[Oral Presentation; Speaker Georg Ripberger]

Ripberger, G. D. (2012, May). *Biochar pyrolysis engineering*. PhD confirmation seminar presented at Massey University, Palmerston North, New Zealand.

[Oral Presentation; Speaker Georg Ripberger]

## Statement of Contribution

These outputs were distributed over the time of Georg Ripberger's PhD study. They represent the state of knowledge at the time. The final opinions are contained in the thesis which, in some cases, are different to those expressed in the publications and presentations. In other words, the work has evolved over time. Georg had ownership of his PhD project and the work contained is entirely his. The role of the supervisors, Jim Jones and Tony Paterson, was to mentor him. A number of honours research projects were conducted alongside the PhD; these were supervised by Georg Ripberger and Jim Jones. We discussed many of the ideas presented in the publications, but emphasise that they are the work of Georg. Percentages are hard to ascribe, but as supervisors, we can only attribute ourselves a small percentage commensurate with mentoring.

Signed

Jim Jones, Principal Supervisor

# Table of Contents

Abstract .....	iii
Acknowledgements.....	v
Statement of Contribution to Doctoral Thesis Containing Publications.....	vii
List of Publications .....	vii
Statement of Contribution .....	xii
Table of Contents.....	xiii
List of Figures.....	xxiii
List of Tables .....	xli
Chapter 1 Project Overview .....	1-1
1.1 Introduction .....	1-2
1.1.1 Climate Change and Carbon Balance .....	1-2
1.1.2 Biochar and its Potential .....	1-3
1.2 Problem Definition .....	1-6
1.3 Concise Statement of Research Tasks and Questions .....	1-8
1.4 References .....	1-10
Chapter 2 Literature Review: Pyrolysis .....	2-1
2.1 Introduction .....	2-2
2.2 What is Pyrolysis? .....	2-3
2.2.1 Definition .....	2-3
2.2.2 Overview of Processes Involved .....	2-3
2.3 Products.....	2-11
2.3.1 Solid.....	2-11
2.3.2 Liquid.....	2-15
2.3.3 Gas .....	2-16
2.4 Pyrolysis Types/ Modes.....	2-17
2.5 Feedstock .....	2-19

2.5.1	Structure of Softwood/ Radiata Pine .....	2-19
2.5.2	Wood Composition .....	2-29
2.5.3	Transport Properties of Wood .....	2-39
2.5.4	Decomposition Behaviour of Wood Components .....	2-48
2.6	Effect of Pyrolysis Conditions.....	2-51
2.6.1	Heating Rate .....	2-51
2.6.2	Highest Treatment Temperature.....	2-52
2.6.3	Soak Time .....	2-54
2.6.4	Pressure and Vapour-phase Concentration .....	2-54
2.6.5	Vapour-phase Residence Time, Particle Size and Sample Loading.....	2-60
2.6.6	Moisture .....	2-61
2.6.7	Atmosphere .....	2-62
2.6.8	Thermal Pre-treatment .....	2-63
2.6.9	Summary .....	2-63
2.7	Proposed Pyrolysis Mechanism.....	2-65
2.7.1	Simple Schemes Applicable for Modelling .....	2-65
2.7.2	Complex Multistep Pyrolysis Mechanism .....	2-69
2.7.3	Empirical Approach.....	2-71
2.7.4	Summary and Conclusion .....	2-71
2.8	Pyrolysis Processes Involving or Closely Related to Autogenous Pressure Pyrolysis.....	2-72
2.8.1	Improved Batch Reactor for Charcoal Production .....	2-72
2.8.2	Deoxy-liquefaction .....	2-72
2.8.3	Hydrous Pyrolysis.....	2-74
2.8.4	Confined Medium Pyrolysis without the Addition of Water .....	2-75
2.8.5	Hydropyrolysis .....	2-77
2.8.6	Hydrothermal Processes.....	2-77
2.8.7	Summary .....	2-81
2.9	Conclusion.....	2-85
2.10	References .....	2-86
Chapter 3	Role of Secondary Char Formation in the Manufacture of Biochar.....	3-1
3.1	Introduction .....	3-2
3.2	Materials and Methods.....	3-3

3.2.1	Feedstock .....	3-3
3.2.1.1	Origin .....	3-3
3.2.1.2	Composition .....	3-3
3.2.1.3	Ultimate Analysis .....	3-6
3.2.1.4	Proximate Analysis .....	3-7
3.2.1.5	Higher Heating Value .....	3-12
3.2.1.6	Density and Porosity .....	3-14
3.2.2	Laboratory Scale Thermogravimetric Analysis .....	3-15
3.2.3	Macro-Thermogravimetric Analysis .....	3-19
3.2.4	Drum Pyrolyser .....	3-23
3.2.5	Hot Stage Experiments .....	3-24
3.2.6	Evolved Gas Analysis .....	3-24
3.2.7	Summary of Experimental Plan .....	3-26
3.3	Results and Discussion .....	3-28
3.3.1	Extraparticle Secondary Char Formation .....	3-28
3.3.2	Intraparticle Secondary Char Formation .....	3-43
3.3.3	Char Yield versus Fixed Carbon Yield .....	3-50
3.3.4	Structural Changes .....	3-52
3.3.5	Transfer Limitations .....	3-63
3.3.6	Torrefaction and Its Impact on Primary Char Formation .....	3-75
3.3.7	Temperature Regime of Secondary Char Forming Reactions .....	3-78
3.3.8	Biomass Components and their Behaviour during Primary and Secondary Pyrolysis Reactions .....	3-81
3.4	Conclusions .....	3-91
3.5	References .....	3-94
Chapter 4	Effect of Catalysts on Pyrolysis .....	4-1
4.1	Introduction .....	4-2
4.2	Material and Methods .....	4-3
4.2.1	Feedstock .....	4-3
4.2.2	Catalysts and Impregnation Procedure .....	4-3
4.2.3	Pyrolysis .....	4-5
4.2.4	Curve-fitting .....	4-6



4.2.5	Summary of Experimental Plan.....	4-7
4.3	Results and Discussion.....	4-8
4.3.1	Physical Addition versus Impregnation .....	4-8
4.3.2	Catalytic Effect of Impregnated Samples .....	4-11
4.3.3	Summary of Catalysts Performance .....	4-31
4.4	Conclusion.....	4-34
4.5	References .....	4-36
Chapter 5	Heat of Pyrolysis.....	5-1
5.1	Introduction .....	5-2
5.2	Material and Methods .....	5-3
5.2.1	Feedstock.....	5-3
5.2.2	Temperature Recording in Wood Cylinders .....	5-3
5.2.3	Heat Flow Analysis of TGA Experiments .....	5-4
5.3	Results and Discussion.....	5-8
5.3.1	Derivation of Reaction Heat Effects from Internal Temperature Recordings . .....	5-8
5.3.2	Heat Flow Analysis of TGA Experiments .....	5-19
5.4	Conclusions .....	5-32
5.5	References .....	5-34
Chapter 6	Effect of Autogenous Pressure on Volatile Pyrolysis Products .....	6-1
6.1	Introduction .....	6-2
6.2	Materials and Methods.....	6-3
6.2.1	Py-GC/MS .....	6-3
6.2.1.1	Evolved Gas Analysis .....	6-4
6.2.1.2	Open Crucible Experiments .....	6-4
6.2.1.3	Sealed Glass Capsule Experiments.....	6-7
6.3	Results and Discussion.....	6-9
6.3.1	Open Crucible Experiments .....	6-9
6.3.2	Sealed Glass Capsule Experiments.....	6-22
6.3.3	Comparison between Open Crucible and Sealed Capsule Experiments...	6-33
6.3.4	Possible Reaction Mechanisms from the Literature Explaining the Observed Results .....	6-41

6.4	Conclusions .....	6-51
6.5	References .....	6-54
Chapter 7	Tar-char/ Coke <i>versus</i> Wood-char/ Charcoal.....	7-1
7.1	Introduction .....	7-2
7.2	Material and Methods .....	7-3
7.2.1	Feedstock .....	7-3
7.2.2	Tar and Coke Production .....	7-3
7.2.3	Wood-char Production.....	7-5
7.2.4	Microscopy.....	7-5
7.2.5	Ultimate Analysis .....	7-5
7.2.6	Raman Analysis.....	7-5
7.2.7	Proximate Analysis.....	7-6
7.2.8	Electrical Conductivity and pH .....	7-6
7.2.9	True Density.....	7-6
7.2.10	Surface Area.....	7-7
7.2.11	Calorific Value .....	7-7
7.3	Results and Discussion .....	7-8
7.3.1	Appearance.....	7-8
7.3.2	Yield.....	7-14
7.3.3	Ultimate Analysis .....	7-21
7.3.4	Raman Analysis.....	7-26
7.3.5	Proximate Analysis.....	7-31
7.3.6	Electrical Conductivity and pH .....	7-39
7.3.7	True Density.....	7-42
7.3.8	Surface Area .....	7-43
7.3.9	Calorific Values.....	7-44
7.4	Conclusions .....	7-46
7.5	References .....	7-47
Chapter 8	High Temperature High Pressure Reactor .....	8-1
8.1	Introduction .....	8-2
8.2	Design Objectives.....	8-3
8.2.1	Principal Design Features .....	8-3

8.2.2	Pressure Envelope.....	8-4
8.2.3	Temperature Range and Heating Rate .....	8-4
8.2.4	Sample Size and Shape .....	8-5
8.2.5	Pyrolysis Environment/ Atmospheres.....	8-7
8.3	Final Design .....	8-9
8.3.1	Preliminary Considerations .....	8-9
8.3.2	P&ID .....	8-10
8.3.3	Process Description.....	8-13
8.3.4	Final Process Parameters.....	8-14
8.4	Proposed Experiments/ Research Capabilities .....	8-15
8.5	Conclusion.....	8-22
8.6	References .....	8-23
Chapter 9	Project Conclusion.....	9-1
9.1	Introduction .....	9-2
9.2	Pyrolysis Mechanism.....	9-3
9.3	Suggestions for Future Work .....	9-13
9.4	Conclusion.....	9-16
9.5	References .....	9-17
10.	Nomenclature .....	10-1
Appendix A	..... Project Overview	
	.....	A-1
A.1	Biochar: Potential and Concerns .....	A-2
A.2	References .....	A-5
Appendix B.....	Role of Secondary Char Formation in the Manufacture of Biochar	
	.....	B-1
B.1	TGA Proximate Analysis Results without Adjustment of Ash Content....	B-2
B.2	Matlab Code for Selecting Data Corresponding to Temperatures in the Range 30 to 700 °C.....	B-3
B.3	Binder Burner/Macro-TGA.....	B-4
B.3.1	Equipment Pictures.....	B-4

B.3.2	Extended Operating Procedure for Pyrolysis Experiments in the Binder Burnout Furnace .....	B-6
B.4	Drum Pyrolyser .....	B-11
B.4.1	Equipment Pictures.....	B-11
B.4.2	Modifications.....	B-11
B.5	Extraparticle Secondary Char Formation.....	B-13
B.5.1	Differences between Experiments with and without a Lid.....	B-13
B.5.2	Relationship between Yield, Lid/No Lid and Initial Dry Sample Mass..	B-19
B.5.3	Differences between Experiments with High and Low Initial Dry Sample Mass.....	B-20
B.6	Intraparticle Secondary Char Formation.....	B-24
B.6.1	Effect of Sample Size .....	B-24
B.6.2	Thermocouple Experiments .....	B-27
B.6.3	Macro-TGA Graphs.....	B-31
B.6.4	Comparison between Pyrolysis of Slices and Sawdust .....	B-33
B.7	Biomass Components and their Behaviour during Primary and Secondary Pyrolysis Reactions.....	B-34
B.7.1	Matlab Code .....	B-34
B.7.2	Curve-fitting .....	B-34
B.8	Torrefaction and Its Impact on Primary Char Formation .....	B-37
	References .....	B-39
	Appendix C.....Effect of Catalysts on Pyrolysis .....	C-1
C.1	Catalysis by Metallic Salts .....	C-2
C.1.1	Relationship between Yield, Lid/No Lid and Initial Dry Sample Mass of K Impregnated Samples.....	C-2
C.1.2	t-test Peak Temperatures of Derivative Weight-loss Curves of K Impregnated Sawdust Experiments With and Without a Lid.....	C-3
C.1.3	Derivative Weight-loss Curves of K Impregnated Samples .....	C-5
C.1.4	Curve-fitting of K Impregnated Samples.....	C-6
C.1.5	Magnesium Impregnation .....	C-7
C.1.6	Curve-fitting of Mg Impregnated Samples .....	C-10

C.2	Catalysis by Acid Treatment .....	C-14
C.2.1	TGA Data .....	C-14
C.2.2	Curve-fitting of P Impregnated Samples.....	C-17
Appendix D	.....Heat of Pyrolysis	
	.....	D-1
D.1	Derivation of Reaction Heat Effects from Internal Temperature Recordings	
	.....	D-2
D.2	Heat Flow Analysis of TGA Experiments .....	D-5
Appendix E	.....Effect of Autogenous Pressure on Volatile Pyrolysis Products	
	.....	E-1
E.1	Pyrograms of Open Crucible Experiments.....	E-2
E.2	Pyrograms of Sealed Glass Capsule Experiments.....	E-7
E.3	Compound Identification of Pyrograms.....	E-9
E.4	Record Numbers .....	E-10
Appendix F	.....Tar-char/ Coke <i>versus</i> Wood-char/ Charcoal	
	.....	F-1
F.1	SEM Micrographs.....	F-2
F.2	Yield.....	F-4
F.3	Temperature Profile .....	F-10
F.4	Ultimate Analysis .....	F-11
F.5	Proximate Analysis.....	F-17
F.6	Surface Area .....	F-23
F.7	References .....	F-24
Appendix G	..... High Temperature High Pressure Reactor	
	.....	G-1
G.1	Initially Proposed Reactor Designs.....	G-2
G.2	Tender Documents.....	G-4
G.2.1	Process Requirements and Description.....	G-4
G.2.2	General Specifications .....	G-4
G.2.3	Specification for Pressure Vessels.....	G-4
G.2.4	Datasheets.....	G-4

---

G.2.5	Supplier Data Instructions Form .....	G-4
G.3	Final Reactor Design .....	G-5
G.4	Process Description .....	G-6
G.4.1	Preparation Sequence.....	G-6
G.4.2	Mode 1: Autogenous Operation .....	G-9
G.4.3	Mode 2: Augmented Operation.....	G-10
G.4.4	Mode 3: Vacuum Operation.....	G-12
G.4.5	Mode 4: Steam/ Water Vapour Injection.....	G-13
G.4.6	Steam Cleaning Procedure .....	G-16



## List of Figures

<i>Figure 2-1.</i> Biomass pyrolysis steps and their interactions. ....	2-4
<i>Figure 2-2.</i> Charcoal produced in a retort kiln. ....	2-11
<i>Figure 2-3.</i> Structure of softwood. ....	2-20
<i>Figure 2-4.</i> Tracheids. ....	2-21
<i>Figure 2-5.</i> Detailed three dimensional softwood section of southern pine. ....	2-23
<i>Figure 2-6.</i> Types of pit pairs. ....	2-24
<i>Figure 2-7.</i> Bordered pits in radiata pine. ....	2-25
<i>Figure 2-8.</i> Cell wall structure ....	2-27
<i>Figure 2-9.</i> Partial structure of cellulose. ....	2-32
<i>Figure 2-10.</i> Formation of crystalline structure. ....	2-32
<i>Figure 2-11.</i> Partial structure of the two main softwood hemicelluloses. ....	2-35
<i>Figure 2-12.</i> Structure of starch. ....	2-36
<i>Figure 2-13.</i> Monomers that form lignin. ....	2-37
<i>Figure 2-14.</i> Section of a typical softwood lignin structure. ....	2-37
<i>Figure 2-15.</i> Values of the bound water diffusivity in the transverse direction ( $D_{BT}$ ) compared to the water vapour diffusion coefficient in air in the lumens ( $D_V$ ) as a function of the average moisture content ( $M$ ) and temperature $T$ . ....	2-44
<i>Figure 2-16.</i> Shrinkage and distortion of wood when dried below the FSP. ....	2-46
<i>Figure 2-17.</i> One-step global scheme. ....	2-65
<i>Figure 2-18.</i> Reaction scheme of a multi-component one-step model. ....	2-66
<i>Figure 2-19.</i> Commonly applied pyrolysis mechanism based on ....	2-67
<i>Figure 2-20.</i> Reaction scheme proposed by ....	2-68



<i>Figure 2-21.</i> Seven-step global reaction scheme proposed by.....	2-68
<i>Figure 2-22.</i> Cellulose pyrolysis mechanism proposed by .....	2-69
<i>Figure 2-23.</i> “Black box” approach.....	2-71
<i>Figure 2-24.</i> Phase diagram of water including the operating ranges of the different pyrolysis processes containing water as reviewed in 2.8. ....	2-82
<i>Figure 3-1.</i> Average derivative weight curve of the proximate analysis experiments with and without a lid. ....	3-9
<i>Figure 3-2.</i> Original positioning of cut pine shavings. ....	3-17
<i>Figure 3-3.</i> Final positioning of cut pine shavings. ....	3-17
<i>Figure 3-4.</i> Preparation of heartwood stripes containing resin. ....	3-18
<i>Figure 3-5.</i> Scheme of Macro-TGA with loaded sample.....	3-21
<i>Figure 3-6.</i> Thermocouple positioning. ....	3-22
<i>Figure 3-7.</i> Cutting direction of sample beams. ....	3-23
<i>Figure 3-8.</i> Weight-loss curves of the proximate analysis runs in section 3.2.1.4. ....	3-29
<i>Figure 3-9.</i> Weight-loss curve of pyrolysis experiments to 700 °C with and without a lid having approximately the same initial sample weight. ....	3-30
<i>Figure 3-10.</i> Average weight-loss curve of pyrolysis experiments with and without a lid to 700 °C. ....	3-31
<i>Figure 3-11.</i> Correlation plot between char yield at 695 °C and the initial dry sample mass. ....	3-32
<i>Figure 3-12.</i> Char yield at 695 °C of pyrolysis experiments with and without a lid as a function of the initial dry sample weight. ....	3-34
<i>Figure 3-13.</i> Difference between derivative weight curves of pyrolysis experiments with a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight. ....	3-36
<i>Figure 3-14.</i> Difference between derivative weight curves of pyrolysis experiments without a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight. ....	3-36

- Figure 3-15.* Comparison of derivative weight curves of planed heartwood strips containing resin with sawdust representative of the whole wood composition during pyrolysis without a lid. .... 3-38
- Figure 3-16.* Comparison of derivative weight curves of heartwood strips containing resin with sawdust representative of the whole wood composition during pyrolysis with a lid. .... 3-39
- Figure 3-17.* Char yield on a dry basis at 695 °C of pyrolysis experiments with and without a lid employing heartwood slices containing extractives as a function of the initial dry sample weight. .... 3-40
- Figure 3-18.* Differences between weight-loss and derivative weight curves of heartwood strips containing resin during pyrolysis with and without a lid... 3-42
- Figure 3-19.* Yield of char at 695 °C as a function of sample size..... 3-43
- Figure 3-20.* Example of placement of slices in “LTGA—EW; slices & cuboids” experiments in Figure 3-19..... 3-44
- Figure 3-21.* Placement of slices in experiments “LTGA—EW; slices 2” in Figure 3-19..... 3-44
- Figure 3-22.* Weight-loss curves of the slices in Figure 3-19 that employed a low stacking density..... 3-46
- Figure 3-23.* Derivative weight curves of the slices in Figure 3-19 that employed a low stacking density..... 3-47
- Figure 3-24.* Difference between derivative weight curves of a sample with small sample size compared to a sample with larger size showing a corresponding yield increase with size..... 3-49
- Figure 3-25.* Fixed carbon yield at 745 °C as a function of the char yield at 695 °C of lab scale TGA pyrolysis experiments..... 3-50
- Figure 3-26.* Fixed carbon yield of Macro-TGA experiments..... 3-51
- Figure 3-27.* Proximate analysis results of the Macro-TGA experiments in Figure 3-26. .... 3-52
- Figure 3-28.* Extent of cracking and fracturing in samples with increasing size. .... 3-53
- Figure 3-29.* Fracturing as a function of sample size, grain direction, and *HTT*. .... 3-54
- Figure 3-30.* Comparison of fracturing between saturated and dried samples. .... 3-55

- Figure 3-31.* Cracks and fractures in a cuboid sample beam with a length of approximately 175 mm and a cross section of 67 x 67 mm pyrolysed to  $\approx 400$  °C.....3-55
- Figure 3-32.* Shrinkage of samples pyrolysed to 700 °C.....3-57
- Figure 3-33.* Shrinkage of samples after drying, and pyrolysis to between 367 to 407 °C and 500 °C.....3-58
- Figure 3-34.* Change in relative pore area and sample width during pyrolysis as observed in a microscopic hot stage.....3-59
- Figure 3-35.* Light microscope micrograph of heartwood pyrolysed in nitrogen at a heating rate of 5 °C/min taken at 153 °C.....3-62
- Figure 3-36.* Derivative weight curves of a selection of experiments in Figure 3-19.....3-64
- Figure 3-37.* Peak temperature of the derivative weight curves of the runs in Figure 3-19 as a function of their characteristic dimension.....3-65
- Figure 3-38.* Results of thermocouple run 10 employing a cylinder with a diameter of 20 mm and a height of 60 mm.....3-68
- Figure 3-39.* Results of thermocouple run 3 employing a cylinder with a diameter of 30 mm and a height of 60 mm.....3-69
- Figure 3-40.* Results of thermocouple run 6 employing a cylinder with a diameter of 74 mm and a height of 60 mm.....3-70
- Figure 3-41.* Difference between plotting the derivative weight curve of the Macro-TGA experiments as a function of the heater temperature compared to the actual sample temperature.....3-72
- Figure 3-42.* Peak temperature of the extractive peaks in Figure 3-1 of the experimental runs without a lid.....3-74
- Figure 3-43.* Weight-loss and temperature profile of torrefaction experiments.....3-76
- Figure 3-44.* Char yield at 695 °C on a dry basis of pyrolysis experiments including a torrefaction step compared to pyrolysis without a torrefaction step with and without a lid as a function of the initial dry sample weight.....3-77
- Figure 3-45.* Derivative weight-loss of radiata pine in crucibles with and without lid compared to EGA of radiata pine.....3-78

- Figure 3-46.* Comparison between the difference in the derivative weight of sawdust pyrolysed in crucibles with and without lid in a laboratory TGA to the average time derivative of the temperature difference between the centre and heater temperature observed during the pyrolysis of cylinders with a diameter of 20 mm and a height of 60 mm in a Macro-TGA. .... 3-80
- Figure 3-47.* Conversion curves of the experimental and modelled data of run RP012 representing pyrolysis experiments without a lid. .... 3-86
- Figure 3-48.* Conversion curves of the experimental and modelled data of run RP013 representing pyrolysis experiments with a lid. .... 3-87
- Figure 4-1.* Comparison of weight-loss curves of pine sawdust with and without physically added KCl on a salt free basis. .... 4-9
- Figure 4-2.* Comparison of derivative weight-loss curves of pine sawdust with and without physically added KCl on a salt free basis. .... 4-9
- Figure 4-3.* Comparison of char yields at 695 °C on a dry basis of various pyrolysis experiments with and without a lid as a function of the initial dry sample weight. .... 4-10
- Figure 4-4.* Comparison of char yields at 695 °C of 2 % (wt/wt) K impregnated sawdust pyrolysed with and without a lid. .... 4-12
- Figure 4-5.* Comparison of average weight-loss curves of impregnated, 2 % (wt/wt) K, and non-impregnated pine sawdust pyrolysed in crucibles with and without a lid. .... 4-14
- Figure 4-6.* Comparison of the char yield obtained at 695 °C of 2 % (wt/wt) K impregnated pine sawdust pyrolysed with and without a lid with pine sawdust pyrolysed with and without a lid. .... 4-15
- Figure 4-7.* Comparison of average derivative weight-loss curves of impregnated, 2 % (wt/wt) K, and non-impregnated pine sawdust pyrolysed in crucibles with and without a lid. .... 4-16
- Figure 4-8.* Comparison of difference curves “no lid-lid” of derivative weight-loss curves of impregnated, 2 % (wt/wt) K, and non-impregnated pine sawdust samples. .... 4-18
- Figure 4-9.* Comparison of the average derivative conversion curves of untreated pine sawdust and pine sawdust impregnated with 2 % (wt/wt) K pyrolysed in crucibles without a lid. .... 4-20

- Figure 4-10.* Comparison of the average derivative conversion curves of untreated pine sawdust and pine sawdust impregnated with 2 % (wt/wt) K pyrolysed in crucibles with a lid. ....4-20
- Figure 4-11.* Comparison of average derivative weight-loss curves of pine sawdust impregnated with 2 and 5 % (wt/wt) Mg pyrolysed in crucibles with and without a lid. ....4-22
- Figure 4-12.* Comparison of average derivative weight-loss curves of pine sawdust impregnated with 1.75 and 4.25 % (wt/wt) P pyrolysed in crucibles with and without a lid. ....4-22
- Figure 4-13.* Comparison of the char yield obtained at 650 °C of Mg impregnated pine sawdust pyrolysed with and without a lid with pine sawdust pyrolysed with and without a lid. ....4-24
- Figure 4-14.* Comparison of the average derivative conversion curves of untreated pine sawdust and pine sawdust impregnated with 1.75 % (wt/wt) P pyrolysed in crucibles without a lid.....4-27
- Figure 4-15.* Comparison of the char yield obtained at 695 °C of P impregnated pine sawdust pyrolysed with and without a lid with pine sawdust pyrolysed with and without a lid. ....4-28
- Figure 4-16.* Conversion curves of the experimental and modelled data of 2 % (wt/wt) K impregnated sawdust pyrolysed without a lid. ....4-30
- Figure 4-17.* Conversion curves of the experimental and modelled data of 2 % (wt/wt) K impregnated sawdust pyrolysed with a lid. ....4-30
- Figure 4-18.* Comparison of the weight-loss rate of untreated pine sawdust and sawdust impregnated with K, Mg and P pyrolysed in crucibles with and without a lid.....4-32
- Figure 4-19.* Comparison of the total char yield obtained at 695 °C on a dry ash free basis of pine sawdust and sawdust impregnated with K, Mg and P pyrolysed in crucibles with and without a lid. ....4-33
- Figure 5-1.* Stainless steel perforated crucible with loaded sample in the case of the pyrolysis of large wood cylinders with a diameter of 120 mm and a height of 60 mm. ....5-3
- Figure 5-2.* Comparison of the time derivative conversion curves of pine sawdust and its pseudo-components pyrolysed in crucibles without a lid with the average time derivative of the temperature difference between the centre and heater

temperature observed during the pyrolysis of cylinders with a diameter of 20 mm and a height of 60 mm in a Macro-TGA. ....	5-9
<i>Figure 5-3.</i> Temperature profile including differential temperature change recorded in a large pine cylinder (d = 120 mm, h = 60 mm) undergoing pyrolysis. ....	5-10
<i>Figure 5-4.</i> Maximum temperature overshoot observed in the pyrolysis of pine cylinders with a height of 60 mm and varying diameter. ....	5-12
<i>Figure 5-5.</i> Comparison of the centre temperature profiles with the derivative weight-loss curves of large pine cylinders (d = 120 mm, h = 60 mm) undergoing pyrolysis. ....	5-13
<i>Figure 5-6.</i> Comparison of the centre temperature profiles with the derivative weight-loss curves of large pine cylinders (d = 120 mm, h = 60 mm) undergoing pyrolysis as a function of time. ....	5-14
<i>Figure 5-7.</i> Results of thermocouple run 10 (see Figure 3-38 in 3.3.5) employing a cylinder with a diameter of 20 mm and a height of 60 mm depicted as a function of time. ....	5-15
<i>Figure 5-8.</i> Time derivative of the difference between the centre temperature and the smoothed heater temperature of pine cylinders of various size being pyrolysed at $\approx 5.5$ °C/min in a Macro-TGA. ....	5-17
<i>Figure 5-9.</i> Raw heat flow data as obtained from the TGA analysis of pine sawdust pyrolysed in crucibles with and without a lid divided by the initial dry ash free feedstock weight. ....	5-19
<i>Figure 5-10.</i> Pyrolysis heat flow and its component heat flows in the case of pine sawdust pyrolysed in crucibles without a lid. ....	5-21
<i>Figure 5-11.</i> Offset corrected pyrolysis heat flows of pine sawdust pyrolysed in crucibles without a lid. ....	5-23
<i>Figure 5-12.</i> Offset corrected pyrolysis heat flows of pine sawdust pyrolysed in crucibles with a lid. ....	5-24
<i>Figure 5-13.</i> Heat of pyrolysis as a function of the char yield. ....	5-25
<i>Figure 5-14.</i> Raw heat flow data of heartwood slices pyrolysed in crucibles without a lid. ....	5-28
<i>Figure 5-15.</i> Raw heat flow data of heartwood slices pyrolysed in crucibles with a lid. ....	5-28

<i>Figure 5-16.</i> Raw heat flow data of pine sawdust impregnated with 2 % (wt/wt) Mg pyrolysed in crucibles without a lid. ....	5-30
<i>Figure 5-17.</i> Raw heat flow data of pine sawdust impregnated with 2 % (wt/wt) Mg pyrolysed in crucibles with a lid. ....	5-30
<i>Figure 6-1.</i> Py-GC/MS crucibles and glass capsule. ....	6-4
<i>Figure 6-2.</i> Experimental procedure for pyrolysis runs in open crucibles minimising the effect of secondary reactions.....	6-5
<i>Figure 6-3.</i> Experimental procedure for pyrolysis runs in sealed glass capsules.....	6-7
<i>Figure 6-4.</i> Pyrograms of pine sawdust heated in open crucibles from 40 to 240 °C. ....	6-10
<i>Figure 6-5.</i> Mass Ion Chromatograms consisting of $m/z$ 57+71 of the six pyrolysis zones in Figure 3-45.....	6-14
<i>Figure 6-6.</i> Pyrograms of the six pyrolysis zones in Figure 3-45. ....	6-17
<i>Figure 6-7.</i> Open crucible pyrograms of pine sawdust pyrolysed from 40 to 280 °C, 240 to 280 °C, and 40 to 240 °C. ....	6-18
<i>Figure 6-8.</i> Open crucible pyrograms of pine sawdust pyrolysed from 40 to 350 °C, 280 to 350 °C, and 40 to 280 °C. ....	6-18
<i>Figure 6-9.</i> Open crucible pyrograms of pine sawdust pyrolysed from 40 to 380 °C, 350 to 380 °C, and 40 to 350 °C. ....	6-20
<i>Figure 6-10.</i> Open crucible pyrograms of pine sawdust pyrolysed from 40 to 500 °C, 380 to 500 °C, and 40 to 380 °C. ....	6-20
<i>Figure 6-11.</i> Comparison of pyrograms obtained by heating samples of pine wood from 40 °C to a highest treatment temperature of 350, 380, 500, and 700 °C respectively. ....	6-21
<i>Figure 6-12.</i> Glass capsule pressure test.....	6-22
<i>Figure 6-13.</i> Pyrograms of pine sawdust heated in a sealed glass capsule from 60 to 240 °C.....	6-24
<i>Figure 6-14.</i> Comparison of pyrograms of pine sawdust heated in a sealed glass capsule from 60 to 240 °C, 60 to 280 °C, 60 to 350 °C, 60 to 380 °C, and 60 to 500 °C. ....	6-25

<i>Figure 6-15.</i> Mass Ion Chromatograms consisting of $m/z$ 57+71 of sealed capsule experiments “60-240-1”, “60-240-2”, “60-280-1”, “60-350-1”, and “60-350-2”. .....	6-29
<i>Figure 6-16.</i> Mass Ion Chromatograms consisting of $m/z$ 57+71 of sealed capsule experiments “60-380-1”, “60-380-2”, “60-500-1”, and “60-500-2”.....	6-30
<i>Figure 6-17.</i> Mass Ion Chromatograms consisting of $m/z$ 58+59 of sealed capsule experiments “60-350-1”, “60-350-2”, “60-380-1”, “60-380-2”, “60-500-1”, and “60-500-2”. .....	6-32
<i>Figure 6-18.</i> Comparison of pyrograms obtained by pyrolysing pine sawdust in sealed capsules and open crucibles in the temperature range 60 to 500 °C and 40 to 500 °C respectively. ....	6-33
<i>Figure 6-19.</i> Comparison of Mass Ion Chromatograms consisting of $m/z$ 57+71 of open crucible experiments “380-500-5” and “40-500-5” with the sealed capsule runs “60-240-1” and “60-500-2”. .....	6-35
<i>Figure 6-20.</i> Comparison of pyrograms obtained by pyrolysing pine sawdust in sealed capsules and open crucibles in the temperature range 60 to 380 °C and 40 to 380 °C respectively. ....	6-37
<i>Figure 6-21.</i> Bond energy in methoxyphenol. ....	6-41
<i>Figure 7-1.</i> Tar pyrolysis vessel with 10 ml beaker from Kimble®. ....	7-4
<i>Figure 7-2.</i> Conventional char from radiata pine pyrolysis. ....	7-9
<i>Figure 7-3.</i> Photographs of tar-char produced from radiata pine tar as viewed under a stereomicroscope.....	7-9
<i>Figure 7-4.</i> Photographs of Manuka bisquettes pyrolysed on a modified Bradley Smoker (Auckland, New Zealand) at 340 °C. ....	7-10
<i>Figure 7-5.</i> Comparison of SEM micrographs of pine-char and tar-char/ coke produced at a <i>HTT</i> of 600 °C. ....	7-14
<i>Figure 7-6.</i> Comparison of wood-char and tar-char yield on a dry ash free basis. ....	7-15
<i>Figure 7-7.</i> Coke yield of various tars pyrolysed at 300 and 600 °C as a function of their production temperature ( <i>HTT</i> of tar production). ....	7-16
<i>Figure 7-8.</i> Ash content of wood-char and tar-char produced at 300, 450 and 600 °C..... .....	7-17
<i>Figure 7-9.</i> Ash of wood-char and tar-char produced at 300, 450 and 600 °C.....	7-18



- Figure 7-10.* Yield of pine-char and tar-char pyrolysed at 300, 450 and 600 °C on a dry basis. .... 7-20
- Figure 7-11.* H/C ratio of tar-char produced at 300 and 600 °C as a function of the HTT of the tar collection process. .... 7-21
- Figure 7-12.* Comparison of carbon content of pine-char and tar-char as a function of the HTT of the pyrolysis process. .... 7-22
- Figure 7-13.* Comparison of atomic H/C ratio of pine-char and tar-char as a function of the HTT of the pyrolysis process. .... 7-23
- Figure 7-14.* Van Krevelen diagram of pine-char and tar-char produced at 300, 450 and 600 °C. .... 7-25
- Figure 7-15.* Measured G band positions of wood-chars and tar-chars with increasing *HTT*. .... 7-27
- Figure 7-16.* Comparison of  $I_D/I_G$  and  $I_N/I_G$  ratios of wood-chars and tar-chars with increasing *HTT*. .... 7-28
- Figure 7-17.* Comparison of  $I_V/I_G$  signals of wood-char and tar-char with increasing *HTT*. .... 7-29
- Figure 7-18.* Comparison of photoluminescence slope/ $I_G$  signals of wood-char and tar-char with increasing *HTT*. .... 7-31
- Figure 7-19.* Proximate analysis results of coke produced from tar pyrolysis with a *HTT* of 300 °C. .... 7-32
- Figure 7-20.* Effect of a lid on the proximate analysis of tar-char and pine-char. .... 7-34
- Figure 7-21.* Comparison of derivative weight-loss curves obtained by pyrolysis with and without a lid of pine, tar-char and pine-char. .... 7-36
- Figure 7-22.* Comparison between averaged pine-char and tar-char volatile matter content. .... 7-38
- Figure 7-23.* Comparison between pine-char and tar-char fixed carbon content. .... 7-38
- Figure 7-24.* pH of pine-char and tar-char in water solution as a function of *HTT*. ... 7-40
- Figure 7-25.* Electrical conductivity of pine-char and tar-char in water solution as a function of *HTT*. .... 7-41
- Figure 7-26.* True density of pine-char and tar-char as a function of *HTT*. .... 7-42

---

<i>Figure 7-27.</i> Higher heating values of pine, pine-char and tar-char as a function of the <i>HTT</i> .....	7-44
<i>Figure 9-1.</i> Modified pyrolysis mechanism based on .....	9-4
<i>Figure 9-2.</i> Proposed pyrolysis mechanism. ....	9-5
<i>Figure 9-3.</i> Proposed pyrolysis mechanism including the relevant physical processes, and the main parameters of influence.....	9-7
<i>Figure B-1.</i> Binder Burner (Macro-TGA) with peripheral equipment. ....	B-4
<i>Figure B-2.</i> Binder Burner furnace with stainless steel crucible and pyrolysed wood sample MTGA16.....	B-5
<i>Figure B-3.</i> Condenser for Binder Burner. ....	B-5
<i>Figure B-4.</i> Exhaust burner with air-inlet plate.....	B-6
<i>Figure B-5.</i> Drum pyrolyser.....	B-11
<i>Figure B-6.</i> Sample holder with samples for drum pyrolyser.....	B-11
<i>Figure B-7.</i> Weight-loss curve of proximate analysis PA2 and PA9. ....	B-13
<i>Figure B-8.</i> Weight-loss curve of proximate analysis PA3 and PA8. ....	B-14
<i>Figure B-9.</i> Average weight-loss curve of additional pyrolysis experiments with and without a lid. ....	B-14
<i>Figure B-10.</i> Average derivative weight curve of additional pyrolysis experiments with and without a lid.....	B-15
<i>Figure B-11.</i> Derivative weight curves of proximate analysis experiments with and without a lid inclusive an additional pyrolysis experiment to 700 °C for the cases lid and no lid. ....	B-15
<i>Figure B-12.</i> Derivative weight curves of additional pyrolysis experiments with and without a lid. ....	B-16
<i>Figure B-13.</i> Comparison of weight-loss curves of pyrolysis experiments with or without lid of heartwood strips containing resin.....	B-17
<i>Figure B-14.</i> Differences between weight-loss and derivative weight curves of heartwood strips containing resin during pyrolysis with and without a lid..	B-18

- Figure B-15.* Difference between derivative weight curves of pyrolysis experiments with a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight 1)..... B-20
- Figure B-16.* Difference between derivative weight curves of pyrolysis experiments with a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight 2)..... B-21
- Figure B-17.* Difference between derivative weight curves of pyrolysis experiments with a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight 3)..... B-21
- Figure B-18.* Difference between derivative weight curves of pyrolysis experiments without a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight 1)..... B-22
- Figure B-19.* Difference between derivative weight curves of pyrolysis experiments without a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight 2)..... B-22
- Figure B-20.* Difference between derivative weight curves of pyrolysis experiments without a lid that have differing initial sample weights correlating to yield differences caused by the varying feedstock weight 3)..... B-23
- Figure B-21.* Weight-loss curves of cuboid samples in Figure 3-19 compared to the weight-loss curve of a thick slice and a small cylindrical sample. .... B-24
- Figure B-22.* Derivative weight curves of cuboid samples in Figure 3-19 compared to the derivative weight curve of a thick slice and a small cylindrical sample. B-25
- Figure B-23.* Difference between derivative weight curves of a sample with small sample size compared to a sample with larger size showing a corresponding yield increase with size 1)..... B-25
- Figure B-24.* Difference between derivative weight curves of a sample with small sample size compared to a sample with larger size showing a corresponding yield increase with size 2)..... B-26
- Figure B-25.* Difference between derivative weight curves of a sample with small sample size compared to a sample with larger size showing a corresponding yield increase with size 3)..... B-26
- Figure B-26.* Results of thermocouple run 11 employing a cylinder with a diameter of 20 mm and a height of 60 mm. .... B-27

- Figure B-27.* Results of thermocouple run 12 employing a cylinder with a diameter of 20 mm and a height of 60 mm. .... B-28
- Figure B-28.* Results of thermocouple run 5 employing a cylinder with a diameter of 30 mm and a height of 60 mm. .... B-29
- Figure B-29.* Results of thermocouple run 2 employing a cylinder with a diameter of 74 mm and a height of 60 mm. .... B-30
- Figure B-30.* Results of Macro-TGA of cylinders with a diameter of 20 mm and a height of 60 mm. .... B-31
- Figure B-31.* Results of Macro-TGA of cylinders with a diameter of 30 mm and a height of 60 mm. .... B-32
- Figure B-32.* Results of Macro-TGA of cylinders with a diameter of 74 mm and a height of 60 mm. .... B-32
- Figure B-33.* Comparison of derivative weight curves of thin slices and sawdust that have been pyrolysed in the laboratory TGA. .... B-33
- Figure B-34.* Conversion curves of the experimental and modelled data of run RP012 representing pyrolysis experiments without a lid. .... B-34
- Figure B-35.* Conversion curves of the experimental and modelled data of run RP013 representing pyrolysis experiments with a lid. .... B-35
- Figure B-36.* Weight-loss of torrefaction experiments compared to pyrolysis without a torrefaction step. .... B-37
- Figure B-37.* Fixed carbon yield at a HTT of  $\approx 745$  °C of pyrolysis experiments including a torrefaction step compared to pyrolysis experiments without a torrefaction step with and without a lid as a function of the initial dry sample weight. .... B-38
- Figure C-1.* Derivative weight-loss curves of 2 % (wt/wt) K impregnated pine sawdust pyrolysed without a lid. .... C-5
- Figure C-2.* Derivative weight-loss curves of 2 % (wt/wt) K impregnated pine sawdust pyrolysed with a lid. .... C-6
- Figure C-3.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 2 % (wt/wt) Mg pyrolysed in crucibles without a lid. .... C-7
- Figure C-4.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 2 % (wt/wt) Mg pyrolysed in crucibles with a lid. .... C-8

- Figure C-5.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 5 % (wt/wt) Mg pyrolysed in crucibles without a lid. .... C-8
- Figure C-6.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 5 % (wt/wt) Mg pyrolysed in crucibles with a lid. .... C-9
- Figure C-7.* Conversion curves of the experimental and modelled data of 2 % (wt/wt) Mg impregnated sawdust pyrolysed without a lid. .... C-10
- Figure C-8.* Conversion curves of the experimental and modelled data of 2 % (wt/wt) Mg impregnated sawdust pyrolysed with a lid. .... C-10
- Figure C-9.* Conversion curves of the experimental and modelled data of 5 % (wt/wt) Mg impregnated sawdust pyrolysed without a lid. .... C-11
- Figure C-10.* Conversion curves of the experimental and modelled data of 5 % (wt/wt) Mg impregnated sawdust pyrolysed with a lid. .... C-11
- Figure C-11.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 1.75 % (wt/wt) P pyrolysed in crucibles without a lid. ... C-14
- Figure C-12.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 1.75 % (wt/wt) P pyrolysed in crucibles with a lid. .... C-15
- Figure C-13.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 4.25 % (wt/wt) P pyrolysed in crucibles without a lid. ... C-15
- Figure C-14.* Derivative weight-loss and weight-loss curves of pine sawdust impregnated with 4.25 % (wt/wt) P pyrolysed in crucibles with a lid. .... C-16
- Figure C-15.* Conversion curves of the experimental and modelled data of 1.75 % (wt/wt) P impregnated sawdust pyrolysed without a lid. .... C-17
- Figure C-16.* Conversion curves of the experimental and modelled data of 1.75 % (wt/wt) P impregnated sawdust pyrolysed with a lid. .... C-17
- Figure C-17.* Conversion curves of the experimental and modelled data of 4.25 % (wt/wt) P impregnated sawdust pyrolysed without a lid. .... C-18
- Figure C-18.* Conversion curves of the experimental and modelled data of 4.25 % (wt/wt) P impregnated sawdust pyrolysed with a lid. .... C-18
- Figure D-1.* Temperature profile including differential temperature change recorded in a large pine cylinder (d = 120 mm, h = 60 mm) undergoing pyrolysis. .... D-2
- Figure D-2.* Corresponding temperature profile to Figure 5-3 as a function of time. .D-3

- Figure D-3.* Corresponding temperature profile to Figure D-1 as a function of time. D-3
- Figure D-4.* Temperature profile as a function of time of a large pine cylinder (d = 120 mm, h = 60 mm) undergoing pyrolysis. .... D-4
- Figure D-5.* Recorded heat flows of blank runs employing crucibles with and without a lid..... D-5
- Figure D-6.* Heat flows used for determining the offset for the heat of pyrolysis in Figure 5-10..... D-6
- Figure D-7.* Weight-loss and derivative weight-loss of feedstock and subsequent char pyrolysis in crucibles without a lid. .... D-6
- Figure D-8.* Weight-loss and derivative weight-loss of feedstock and subsequent char pyrolysis in crucibles with a lid. .... D-7
- Figure D-9.* Recorded heat flows of blank runs without a lid..... D-8
- Figure D-10.* TG/DSC measurement of air-dried pine sawdust pyrolysed in a crucible without a lid. .... D-9
- Figure D-11.* Raw heat flow data of sapwood slices pyrolysed in crucibles without a lid..... D-9
- Figure D-12.* Raw heat flow data of pine sawdust impregnated with 5 % (wt/wt) Mg pyrolysed in crucibles without a lid. .... D-10
- Figure D-13.* Raw heat flow data of pine sawdust impregnated with 5 % (wt/wt) Mg pyrolysed in crucibles with a lid. .... D-10
- Figure D-14.* Raw heat flow data of pine sawdust impregnated with 2 % (wt/wt) K pyrolysed in crucibles without a lid. .... D-11
- Figure D-15.* Raw heat flow data of pine sawdust impregnated with 2 % (wt/wt) K pyrolysed in crucibles with a lid. .... D-11
- Figure D-16.* Raw heat flow data of pine sawdust impregnated with 1.75 % (wt/wt) P pyrolysed in crucibles without a lid. .... D-12
- Figure D-17.* Raw heat flow data of pine sawdust impregnated with 1.75 % (wt/wt) P pyrolysed in crucibles with a lid. .... D-12
- Figure D-18.* Raw heat flow data of pine sawdust impregnated with 4.25 % (wt/wt) P pyrolysed in crucibles without a lid. .... D-13

- Figure D-19.* Raw heat flow data of pine sawdust impregnated with 4.25 % (wt/wt) P pyrolysed in crucibles with a lid. .... D-14
- Figure E-1.* Pyrograms of pine sawdust volatile fraction released between 240 to 280 °C. .... E-2
- Figure E-2.* Pyrograms of pine sawdust heated in open crucibles from 40 to 280 °C. E-2
- Figure E-3.* Pyrograms of pine sawdust volatile fraction released between 280 to 350 °C. .... E-3
- Figure E-4.* Pyrograms of pine sawdust heated in open crucibles from 40 to 350 °C. E-3
- Figure E-5.* Pyrograms of pine sawdust volatile fraction released between 350 to 380 °C. .... E-4
- Figure E-6.* Pyrograms of pine sawdust heated in open crucibles from 40 to 380 °C. E-4
- Figure E-7.* Pyrograms of pine sawdust volatile fraction released between 380 to 500 °C. .... E-5
- Figure E-8.* Pyrograms of pine sawdust heated in open crucibles from 40 to 500 °C. E-5
- Figure E-9.* Pyrograms of pine sawdust volatile fraction released between 500 to 700 °C. .... E-6
- Figure E-10.* Pyrograms of pine sawdust heated in open crucible from 40 to 700 °C. E-6
- Figure E-11.* Pyrogram of pine sawdust heated in a sealed glass capsule from 60 to 280 °C. .... E-7
- Figure E-12.* Pyrograms of pine sawdust heated in a sealed glass capsule from 60 to 350 °C. .... E-7
- Figure E-13.* Pyrograms of pine sawdust heated in a sealed glass capsule from 60 to 380 °C. .... E-8
- Figure E-14.* Pyrograms of pine sawdust heated in a sealed glass capsule from 60 to 500 °C. .... E-8
- Figure F-1.* SEM micrographs of coke bubbles on Manuka bisquettes pyrolysed on a modified Bradley food smoker at 340 °C. .... F-2
- Figure F-2.* SEM micrographs of coke bubbles on Manuka bisquettes pyrolysed on a modified Bradley food smoker at 340 °C. .... F-2
- Figure F-3.* SEM micrographs of radiata pine wood. .... F-3

<i>Figure F-4.</i> SEM micrographs of pine-char produced at various HTT.....	F-3
<i>Figure F-5.</i> Comparison of wood-char and tar-char fixed carbon yields. ....	F-4
<i>Figure F-6.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 2 % (wt/wt) K and its char pyrolysed in crucibles without a lid.....	F-5
<i>Figure F-7.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 2 % (wt/wt) K and its char pyrolysed in crucibles with a lid. ....	F-5
<i>Figure F-8.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 2 % (wt/wt) Mg and its char pyrolysed in crucibles without a lid. ....	F-6
<i>Figure F-9.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 2 % (wt/wt) Mg and its char pyrolysed in crucibles with a lid. ....	F-6
<i>Figure F-10.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 5 % (wt/wt) Mg and its char pyrolysed in crucibles without a lid. ....	F-7
<i>Figure F-11.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 5 % (wt/wt) Mg and its char pyrolysed in crucibles with a lid. ....	F-7
<i>Figure F-12.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 1.75 % (wt/wt) P and its char pyrolysed in crucibles without a lid. ....	F-8
<i>Figure F-13.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 1.75 % (wt/wt) P and its char pyrolysed in crucibles with a lid. ....	F-8
<i>Figure F-14.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 4.25 % (wt/wt) P and its char pyrolysed in crucibles without a lid. ....	F-9
<i>Figure F-15.</i> Weight-loss and derivative weight-loss of pine wood impregnated with 4.25 % (wt/wt) P and its char pyrolysed in crucibles with a lid. ....	F-9
<i>Figure F-16.</i> Recorded furnace temperature profiles from Caco (2014).....	F-10
<i>Figure F-17.</i> Carbon content of tar-char produced at 300 °C as a function of the HTT of the tar collection process. ....	F-11
<i>Figure F-18.</i> Hydrogen content of tar-char produced at 300 °C as a function of the HTT of the tar collection process. ....	F-12
<i>Figure F-19.</i> Carbon content of tar-char produced at 600 °C as a function of the HTT of the tar collection process. ....	F-12
<i>Figure F-20.</i> Hydrogen content of tar-char produced at 600 °C as a function of the HTT of the tar collection process. ....	F-13



<i>Figure F-21.</i> Nitrogen content of tar-char produced at 300 °C as a function of the HTT of the tar collection process. ....	F-13
<i>Figure F-22.</i> Nitrogen content of tar-char produced at 600 °C as a function of the HTT of the tar collection process. ....	F-14
<i>Figure F-23.</i> Comparison of hydrogen content of pine-char and tar-char as a function of the HTT of the pyrolysis process. ....	F-15
<i>Figure F-24.</i> Comparison of nitrogen content of pine-char and tar-char as a function of the HTT of the pyrolysis process. ....	F-16
<i>Figure F-25.</i> Weight-loss recorded during proximate analysis of ground, dried and ground, non-dried coke in Figure 7-19.....	F-17
<i>Figure F-26.</i> Proximate analysis results of ground and non-ground coke produced from tar pyrolysis with a HTT of 600 °C.....	F-18
<i>Figure F-27.</i> Weight-loss and derivative weight-loss curves of pine-char proximate analysis performed with and without a lid.....	F-18
<i>Figure F-28.</i> Weight-loss and derivative weight-loss curves of tar-char proximate analysis performed with and without a lid.....	F-19
<i>Figure F-29.</i> Volatile matter content of pine-char and tar-char produced at various HTT's.....	F-20
<i>Figure F-30.</i> Fixed carbon content of pine-char and tar-char produced at various HTT's.....	F-21
<i>Figure F-31.</i> Weight-loss curves of proximate analysis of tar-char samples produced at a HTT of 450 °C.....	F-22
<i>Figure G-1.</i> Schematic of initially proposed apparatus for studying pyrolysis of pine shavings. ....	G-2
<i>Figure G-2.</i> Schematic of initially proposed apparatus for studying pyrolysis of pine shavings and cylindrical wood rods in one reactor. ....	G-2
<i>Figure G-3.</i> Schematic of initially proposed apparatus for studying pyrolysis of pine shavings and cylindrical wood rods in one reactor. ....	G-3

## List of Tables

<i>Table 1-1.</i> Concise statement of research tasks and questions.....	1-9
<i>Table 2-1.</i> Charcoal yields for conventional pyrolysis. ....	2-14
<i>Table 2-2.</i> Common pyrolysis classification. ....	2-17
<i>Table 2-3.</i> Radiata pine tracheid dimensions. ....	2-26
<i>Table 2-4.</i> Cellulose microfibril orientation and microfibril angle. ....	2-28
<i>Table 2-5.</i> Average moisture content in radiata pine sapwood and heartwood.....	2-29
<i>Table 2-6.</i> Chemical composition of radiata pine sapwood and mature bark. ....	2-30
<i>Table 2-7.</i> Major hemicelluloses in softwood. ....	2-34
<i>Table 3-1.</i> Extractive, carbohydrate and lignin analysis. ....	3-4
<i>Table 3-2.</i> Cellulose, hemicellulose, and lignin content of radiata pine. ....	3-5
<i>Table 3-3.</i> Ultimate analysis of radiata pine on a dry (dry ash free) basis.....	3-7
<i>Table 3-4.</i> Empirical formula and molar <i>H/C</i> and <i>O/C</i> ratio of radiata pine wood.....	3-7
<i>Table 3-5.</i> TGA procedure for proximate analysis. ....	3-8
<i>Table 3-6.</i> Proximate analysis with lid of air-dried radiata pine in % (wt/wt) on an air-dry basis.....	3-11
<i>Table 3-7.</i> Proximate analysis without lid of air-dried radiata pine in % (wt/wt) on an air-dry basis.....	3-11
<i>Table 3-8.</i> Moisture contained in air-dried radiata pine in % (wt/wt) on an air-dry basis as determined by oven-drying.....	3-11
<i>Table 3-9.</i> Higher heating value of radiata pine wood in MJ/kg measured and estimated.....	3-13
<i>Table 3-10.</i> Porosity, basic and apparent density of radiata pine wood. ....	3-14
<i>Table 3-11.</i> Temperature programme of pyrolysis experiments in the laboratory scale TGA.....	3-16

<i>Table 3-12.</i> Py-GC/MS parameters for EGA. ....	3-25
<i>Table 3-13.</i> Experimental plan. ....	3-26
<i>Table 3-14.</i> Correlation analysis. ....	3-32
<i>Table 3-15.</i> Regression statistics. ....	3-33
<i>Table 3-16.</i> Analysis of variance. ....	3-33
<i>Table 3-17.</i> Coefficient analysis. ....	3-33
<i>Table 3-18.</i> F-test for equality of variances.....	3-41
<i>Table 3-19.</i> t-test for equality of means assuming equal variances. ....	3-41
<i>Table 3-20.</i> F-test for equality of variances.....	3-66
<i>Table 3-21.</i> t-test for equality of means assuming equal variances. ....	3-67
<i>Table 3-22.</i> Initial values for $A_i$ , $E_i$ and $x_i$ . ....	3-85
<i>Table 3-23.</i> Fitted parameters, char yield of the biomass constituents and char composition of run RP012 representing pyrolysis without a lid.....	3-88
<i>Table 3-24.</i> Fitted parameters, char yield of the biomass constituents and char composition of run RP013 representing pyrolysis with a lid.....	3-88
<i>Table 4-1.</i> Ash content of impregnated radiata pine sawdust.....	4-5
<i>Table 4-2.</i> Experimental plan. ....	4-7
<i>Table 4-3.</i> Correlation analysis for 2 % (wt/wt) K impregnated sawdust.....	4-11
<i>Table 4-4.</i> F-test for equality of variances on data in Figure 4-4. ....	4-12
<i>Table 4-5.</i> t-test for equality of means assuming unequal variances. ....	4-13
<i>Table 4-6.</i> Characteristic temperatures of the derivative weight-loss curves in Figure 4-7.....	4-17
<i>Table 5-1.</i> Latent heat of moisture evaporation.....	5-22
<i>Table 6-1.</i> Py-GC/MS parameters for open crucible pyrolysis runs.....	6-6
<i>Table 7-1.</i> BET N <sub>2</sub> surface area of wood-char and tar-char. ....	7-43
<i>Table 8-1.</i> Proposed experiments.....	8-15

<i>Table A-1.</i> Potential/ benefits of biochar production and application. ....	A-2
<i>Table A-2.</i> Concerns and criticism of biochar.....	A-4
<i>Table B-1.</i> Proximate analysis with lid of air-dried radiata pine in % (wt/wt) on an air-dry basis.....	B-2
<i>Table B-2.</i> Proximate analysis without lid of air-dried radiata pine in % (wt/wt) on an air-dry basis.....	B-2
<i>Table B-3.</i> Char yields at 695 °C and dry feedstock weight of pyrolysis experiments with and without a lid.....	B-19
<i>Table B-4.</i> Fitted parameters, char yield of the biomass constituents and char composition of run RP012 representing pyrolysis without a lid in Figure B-34. ....	B-36
<i>Table B-5.</i> Fitted parameters, char yield of the biomass constituents and char composition of run RP013 representing pyrolysis with a lid in Figure B-35... B-36	
<i>Table C-1.</i> Char yields at 695 °C and dry feedstock weight of pyrolysis experiments of 2 % (wt/wt) K impregnated sawdust pyrolysed with and without a lid. ....	C-2
<i>Table C-2.</i> Peak temperatures of derivative weight-loss curves of K impregnated sawdust experiments with and without a lid.....	C-3
<i>Table C-3.</i> F-test for equality of variances on data in Table C-2.....	C-3
<i>Table C-4.</i> t-test for equality of means assuming equal variances.....	C-4
<i>Table C-5.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 2 % (wt/wt) K in Figure 4-16. ....	C-6
<i>Table C-6.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 2 % (wt/wt) K in Figure 4-17. ....	C-7
<i>Table C-7.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 2 % (wt/wt) Mg in Figure C-7. ....	C-12
<i>Table C-8.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 2 % (wt/wt) Mg in Figure C-8. ....	C-12

<i>Table C-9.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 5 % (wt/wt) Mg in Figure C-9. .....	C-13
<i>Table C-10.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 5 % (wt/wt) Mg in Figure C-10. .....	C-13
<i>Table C-11.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 1.75 % (wt/wt) P in Figure C-15. ....	C-19
<i>Table C-12.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 1.75 % (wt/wt) P in Figure C-16. ....	C-19
<i>Table C-13.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 4.25 % (wt/wt) P in Figure C-17. ....	C-20
<i>Table C-14.</i> Fitted parameters, resulting char yield of the biomass components and char composition of pine sawdust impregnated with 4.25 % (wt/wt) P in Figure C-18. ....	C-20
<i>Table D-1.</i> Char weight-loss during pyrolysis in crucibles without a lid from 30 to 700 °C. ....	D-7
<i>Table D-2.</i> Char weight-loss during pyrolysis in crucibles with a lid from 30 to 700 °C. .....	D-8
<i>Table G-1.</i> Preparation sequence. ....	G-6
<i>Table G-2.</i> Autogenous operation. ....	G-9
<i>Table G-3.</i> Augmented operation. ....	G-11
<i>Table G-4.</i> Vacuum operation. ....	G-12
<i>Table G-5.</i> Steam/ water vapour injection. ....	G-14
<i>Table G-6.</i> Steam cleaning procedure. ....	G-17