

# Development of A Low Temperature Co-Fired Ceramic Fuel Processor for the Micro-scale Solid Oxide Fuel Cell System

B. Jiang<sup>1,2</sup>, A. J. Santis-Alvarez<sup>3</sup>, P. Muralt<sup>1</sup>, D. Poulikakos<sup>3</sup>, T. Maeder<sup>2</sup>

<sup>1</sup>Laboratory of Ceramics, EPFL Lausanne, CH-1015 Lausanne, Switzerland

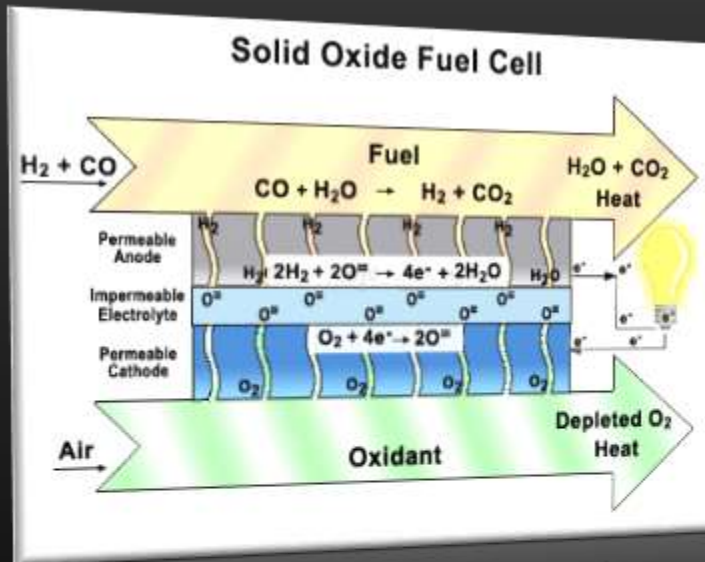
<sup>2</sup>Laboratory of Micro-engineering for Manufacturing, EPFL Lausanne, CH-1015 Lausanne, Switzerland

<sup>3</sup>Laboratory of Thermodynamics in Emerging Technologies, ETH Zurich, CH-8092 Zurich, Switzerland

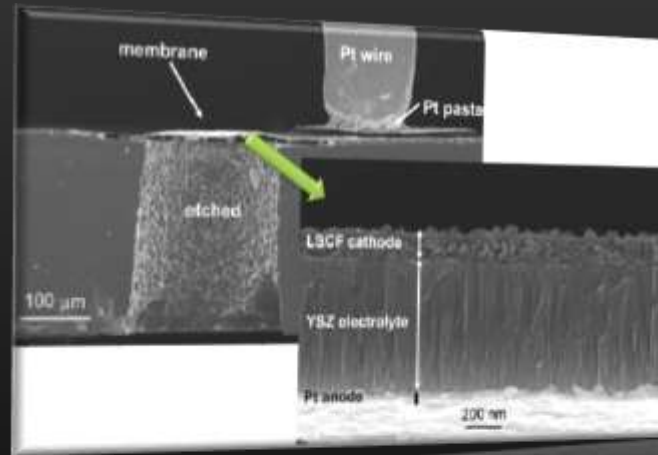
# Outline

- Introduction
  - Concept of the micro-scale solid oxide fuel cell system ( $\mu$ -SOFCs)
  - Concept of the  $\mu$ -SOFC fuel processor
  - Low temperature co-fired ceramic (LTCC) technology
- Design of LTCC fuel processor
- Fabrication process
- Fluidic, thermal and thermally self-sustain characterization
- Conclusion
- Outlook

# What are $\mu$ -SOFCs?



Principle of SOFC



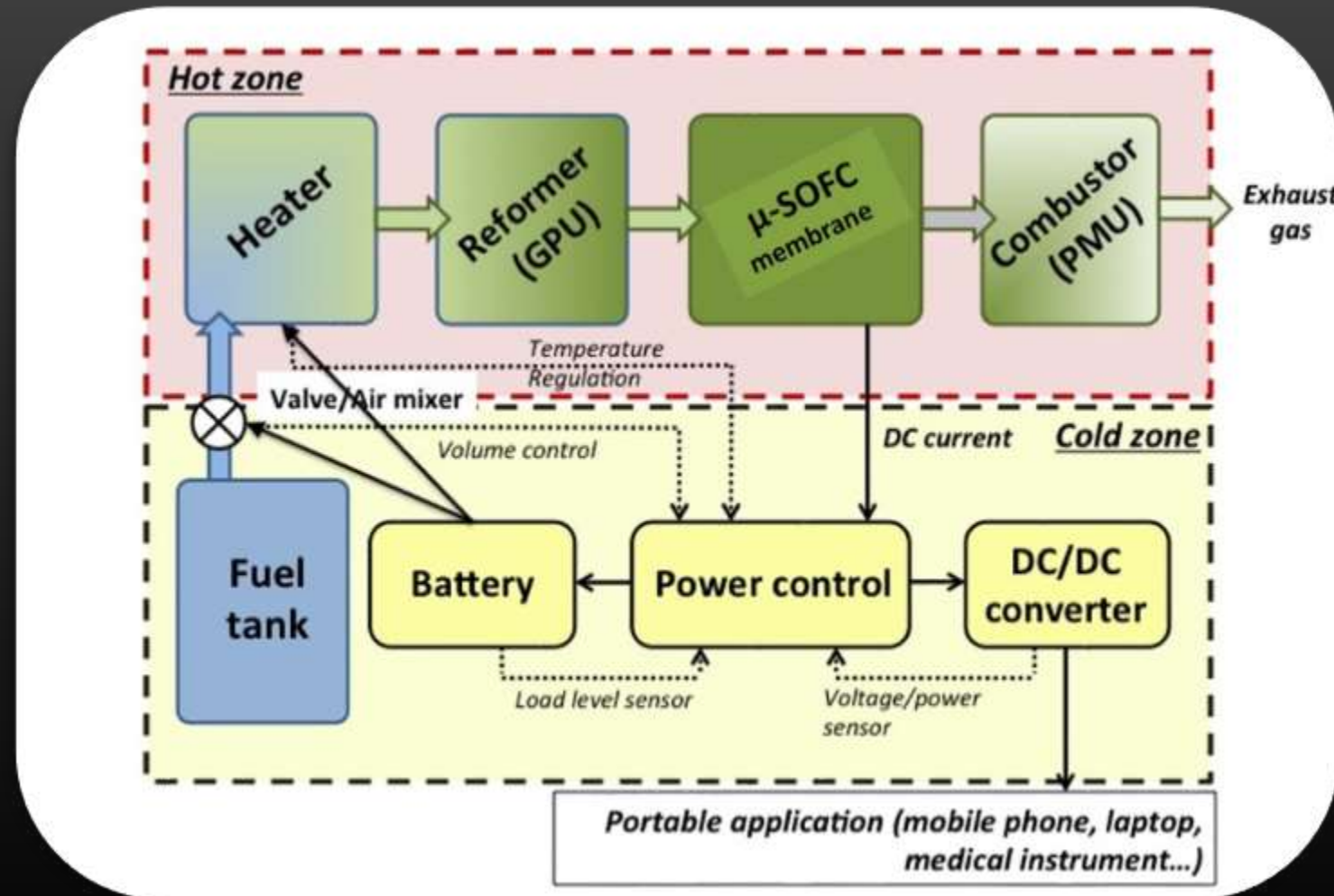
Silicon base  $\mu$ SOFC membrane  
*2008 Bieberle, J. Power Sources*



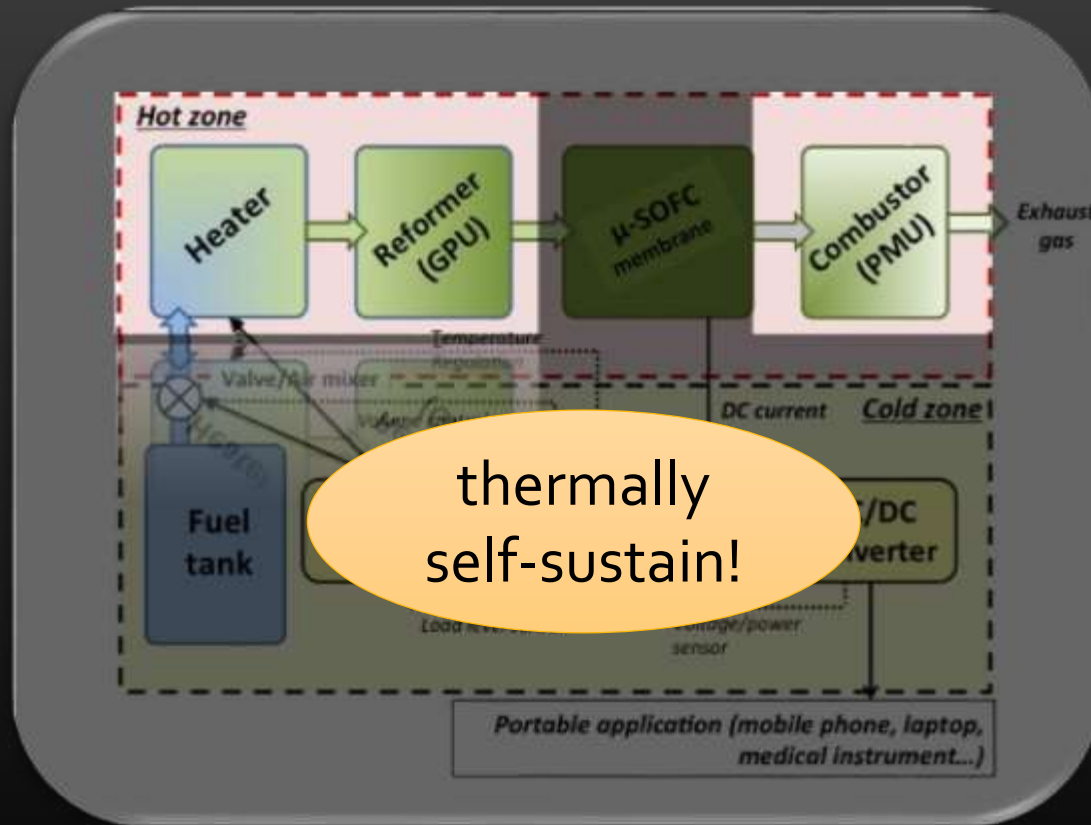
1<sup>st</sup> commercialized  $\mu$ -SOFC product  
*Lilliputian Systems, Inc.*

# What is a $\mu$ -SOFC fuel processor?

Concept of  $\mu$ -SOFCs system



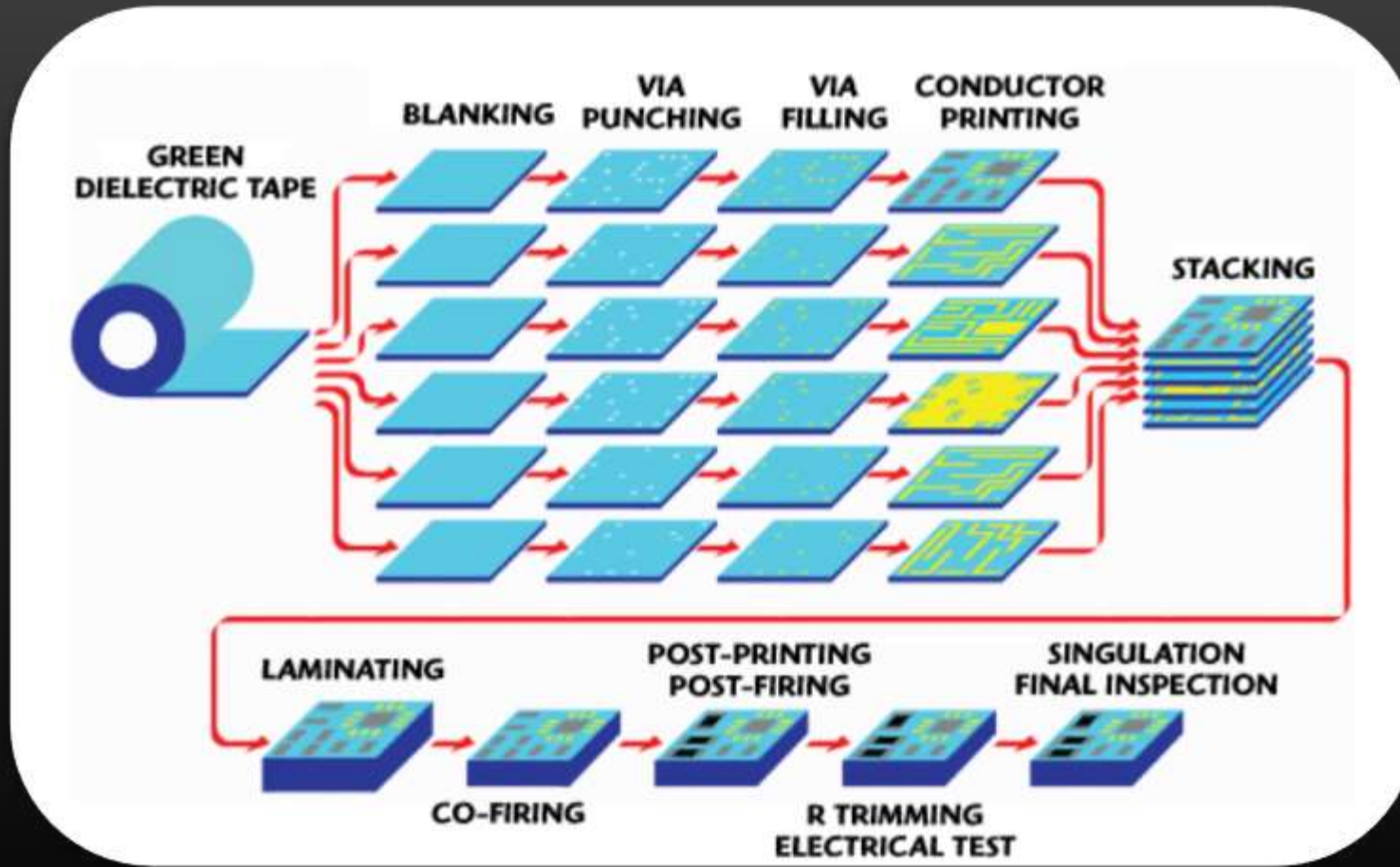
# What is a $\mu$ -SOFC fuel processor?



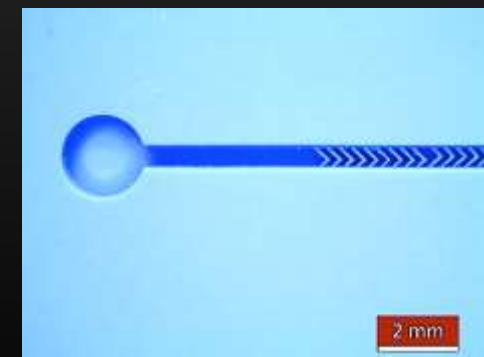
- The fuel processor is a vital component in the whole  $\mu$ -SOFC system
  - Heater – providing initial thermal energy for triggering the chemical reaction
  - reformer – converting hydrocarbon fuel mainly into hydrogen and carbon monoxide with a partial oxidation reaction route
  - combustor – totally oxidizing exhaust gas from the  $\mu$ -SOFC membranes
  - thermally independent operation for minimizing the power input to the system



# What is LTCC technology?



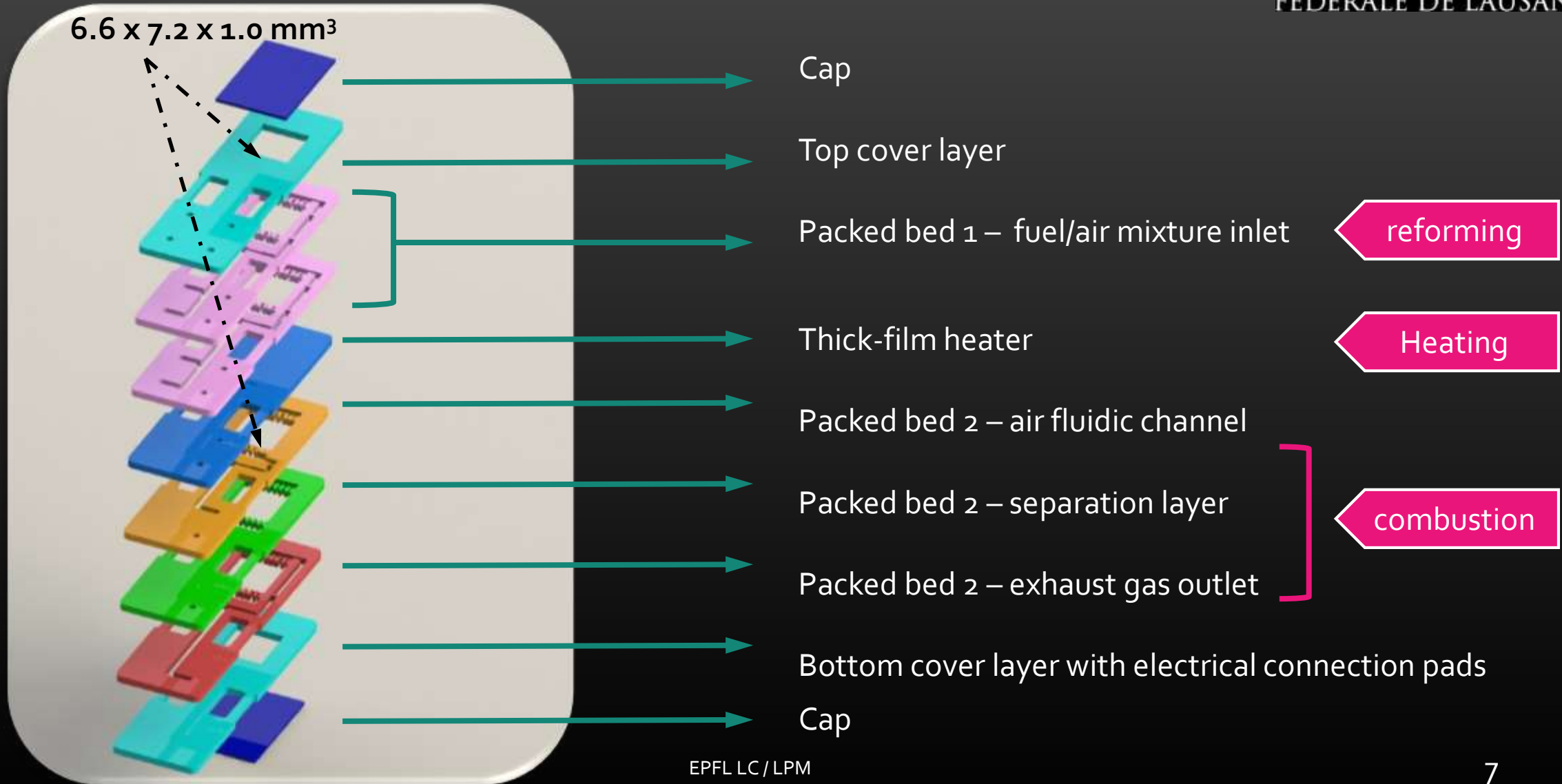
LTCC flow sensor



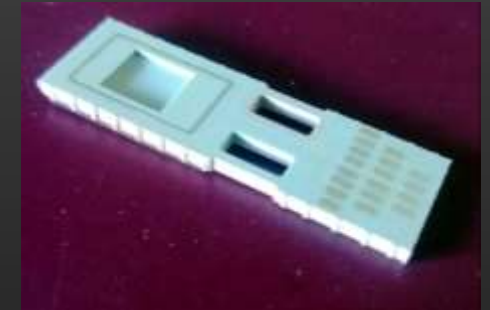
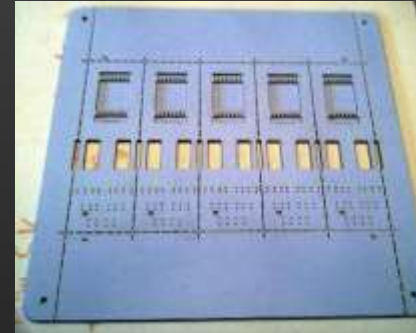
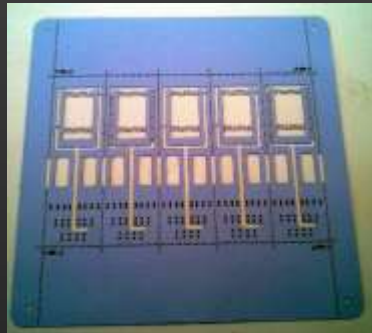
LTCC microreactor

<http://www.microwavejournal.com>

# Design of a LTCC fuel processor



# Fabrication of LTCC fuel processors



Laser ablation  
(a Nd-YAG laser, LS9000)



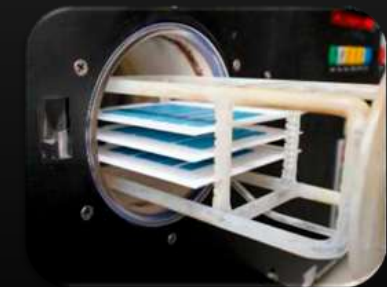
Screen printing  
(Aurel C900)



Uniaxial lamination  
(2 – 20 MPa  
25°C – 70°C)

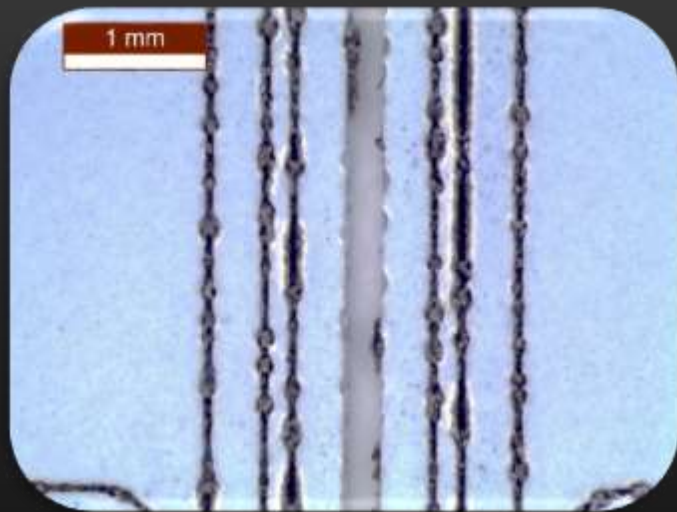


Sintering  
(ATV PEO-601 lamp furnace  
10 hours – 875°C – Air)

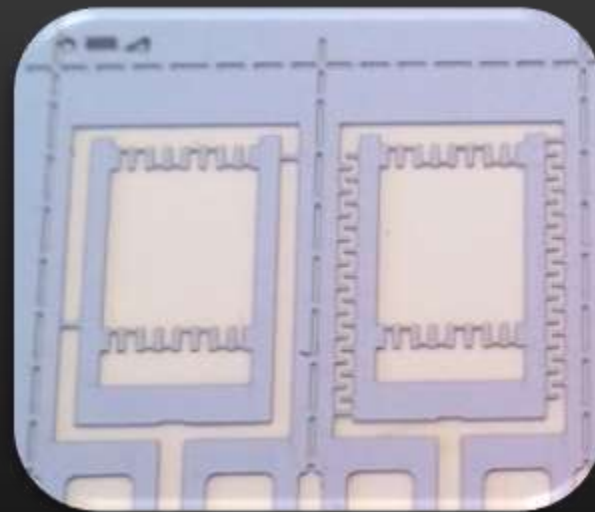




# Fabrication of LTCC fuel processors



Bad



Good

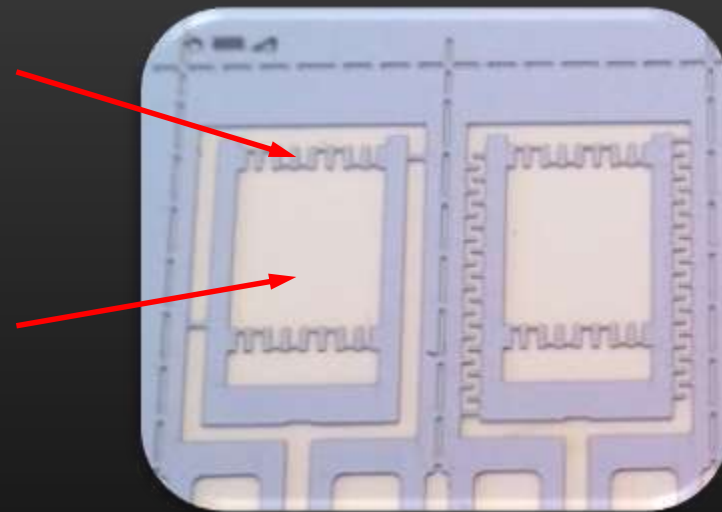
## Channel and cavity formation

- Laser cutting parameters
  - a.  $I$  - diode current (A)
  - b.  $f$  - frequency of the acoustic optical switch (kHz)
  - c.  $v$  - beam deflection velocity (mm/s)
- Inadequate laser parameters may result in channel sidewall bulging or heavy burnt of the cutting interface to destroy the fine fluidic structure on LTCC

# Fabrication of LTCC fuel processors

Strips for the  
catalyst barrier  
(200  $\mu\text{m}$ )

Cavities for the  
catalytic packed bed  
(6.6 x 7.2  $\text{mm}^2$ )



Good

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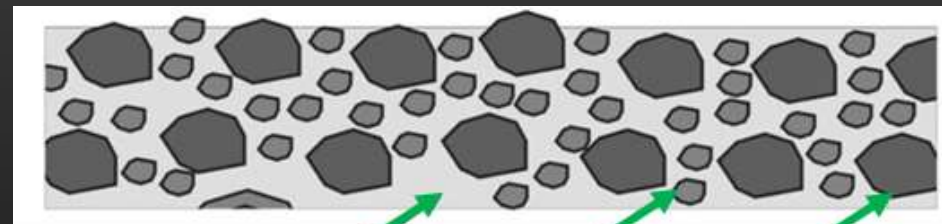


# Fabrication of LTCC fuel processors

## Lamination



Uniaxial lamination

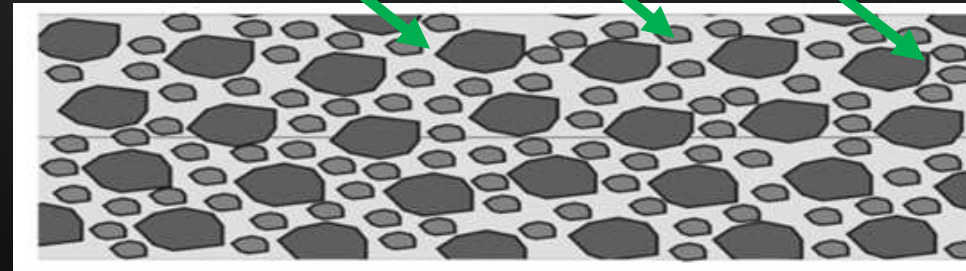


LTCC tape

Organic binder

Glass

Ceramic



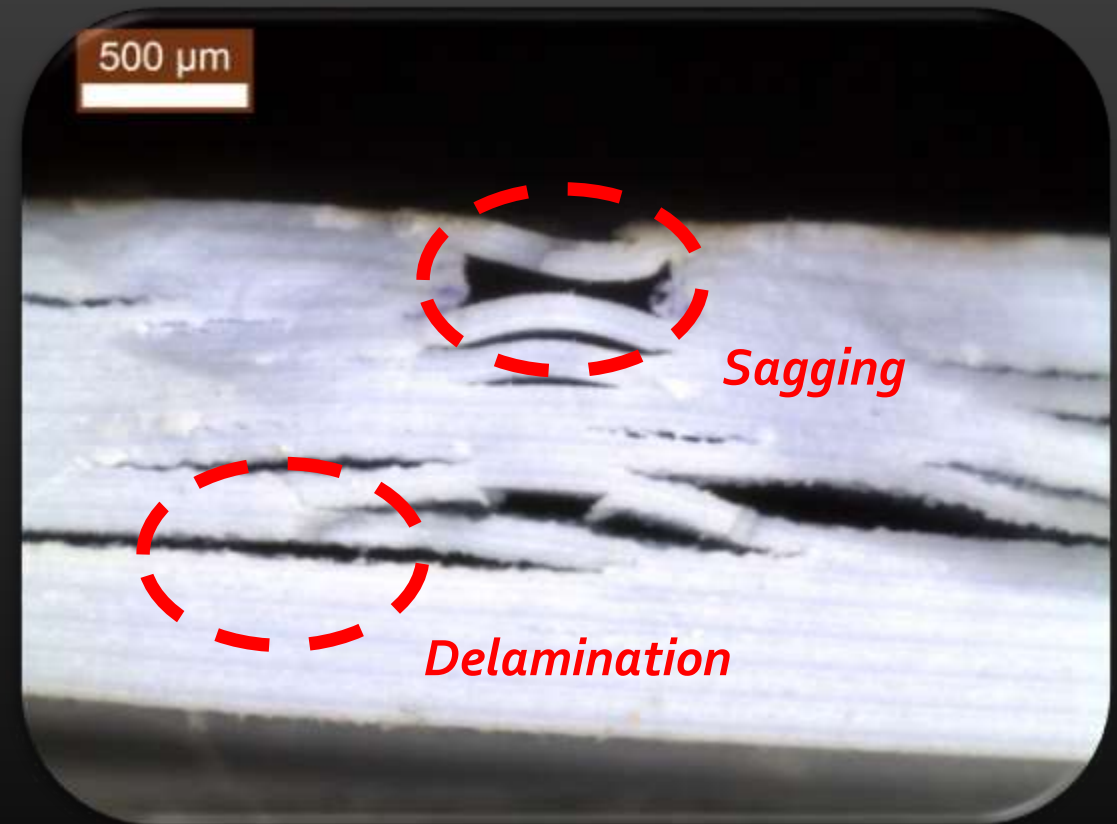
Interface between laminated tapes

*D. Jurków and L. Golonka, J. of the European Ceramic Society, 2012*

# Fabrication of LTCC fuel processors

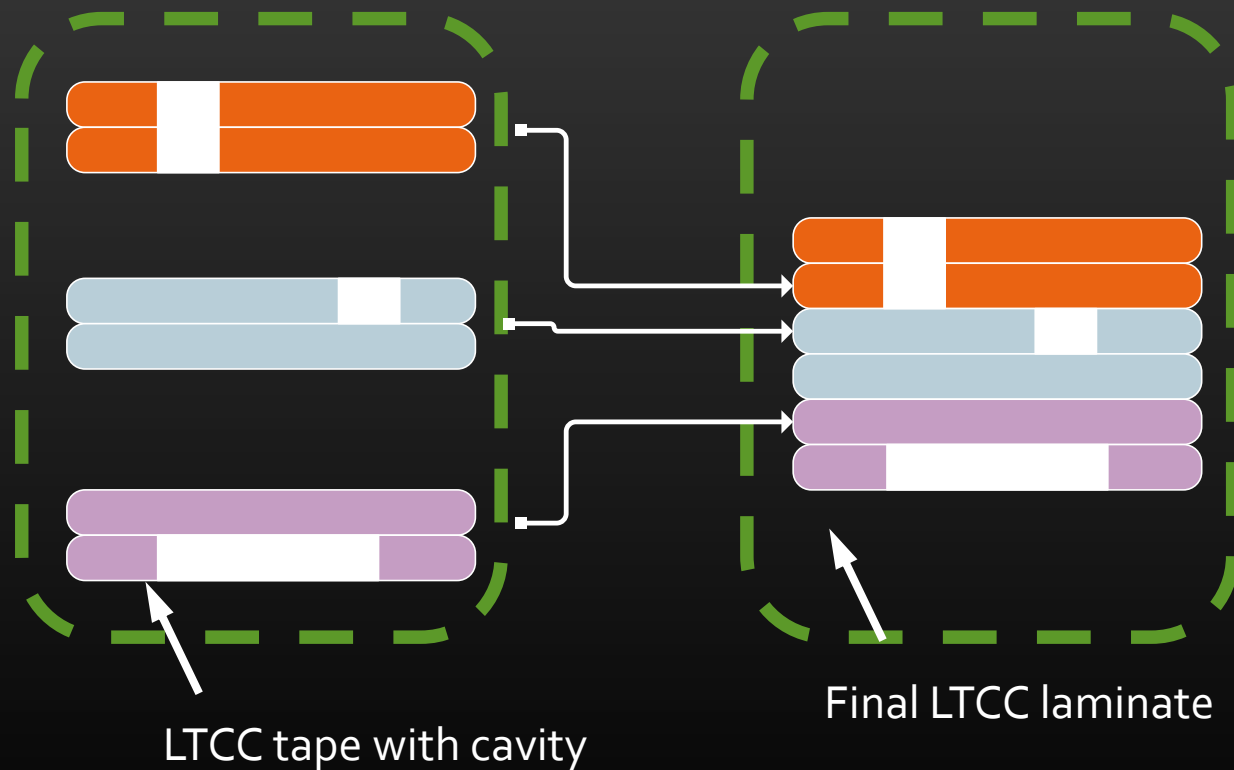
## Lamination

- improper lamination causes sagging of fluidic channel and delamination of fired samples
- Progressive lamination provides a good solution to the fine, complex fluidic structure formation in development of the LTCC fuel processor



# Fabrication of LTCC fuel processors

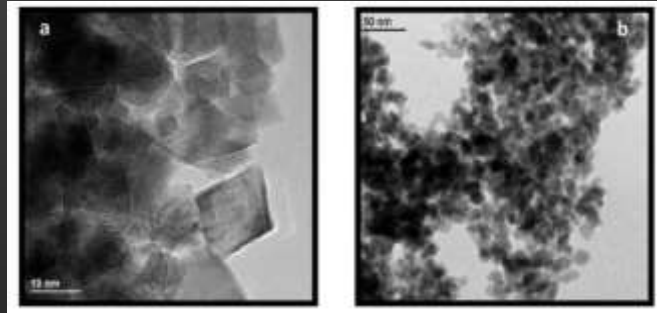
## Progressive lamination procedure



- For those tapes with same fluidic pattern are pre-laminated. The thickness of the fluidic structure was therefore built up by the lamination at room temperature with applied standard pressure (21 MPa)
- Each laminated functional layer were stacked and laminated together one by one with a applied low pressure ( $< 4\text{MPa}$ ) at  $70^\circ\text{C}$

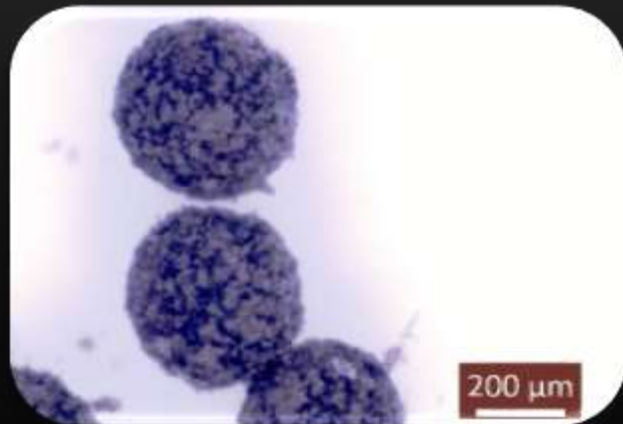


# Catalyst for the fuel reactions



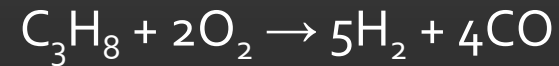
Transmission electron micrographs of the as-prepared Rh/(Ce,Zr)O<sub>2</sub> catalyst particles

2008 Hotz, *Chem. Eng. Sci.*



10 wt% of Rh/(Ce,Zr)O<sub>2</sub> on YSZ beads support

## Partial oxidation of propane



- Exothermic reaction
- High syngas (CO & H<sub>2</sub>) production possible with Rh-metal catalyst

YSZ beads (diameter: 100 – 200 μm) as catalyst supports for building up the packed bed in the processor

- 👍 homogenous packed bed & low pressure drop
- 👍 no solvent needed for the filling
- 👎 low thermal conductivity – improper to obtain isothermal bed condition (alternative: high temperature alloy felt as catalytic bed)

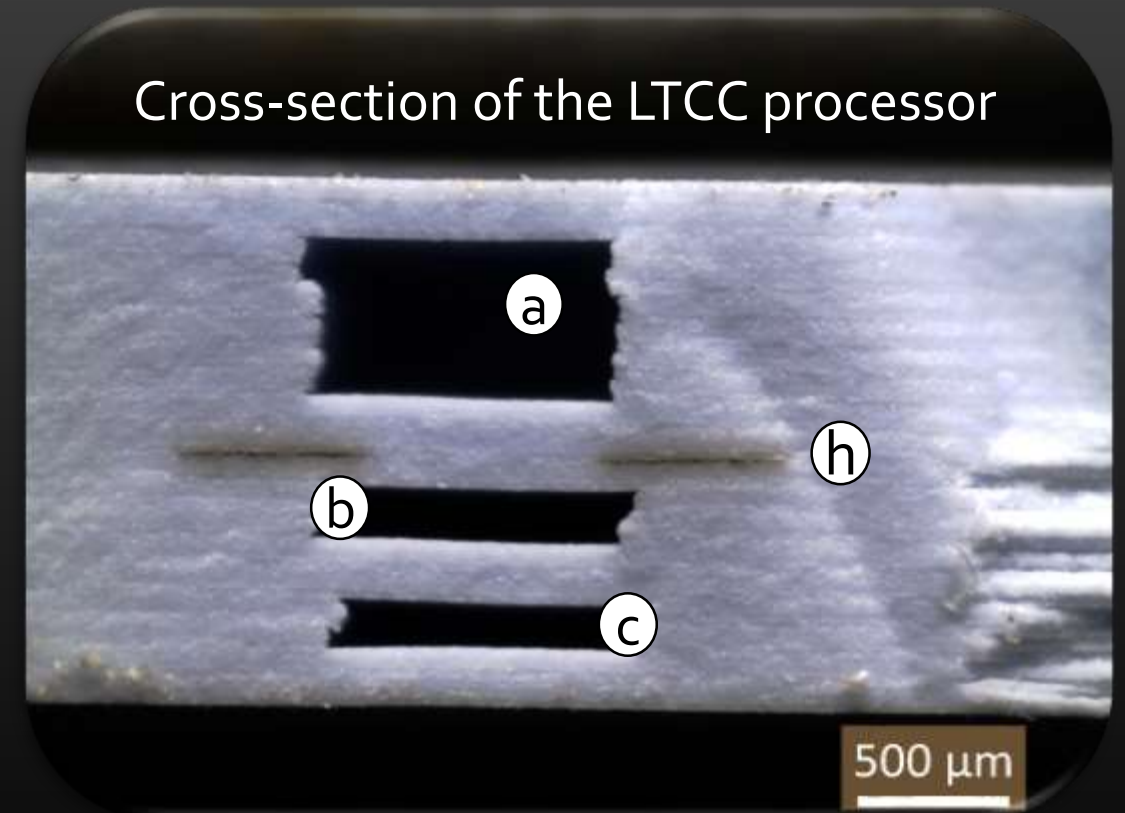
# Fluidic characterization

- Fluidic structure

- a. Cross section of exhaust channel:  $0.5 \times 0.96 \text{ mm}^2$
- b. Channel 1:  $0.95 \times 0.17 \text{ mm}^2$
- c. Channel 2:  $0.95 \times 0.14 \text{ mm}^2$

- Heater (h)

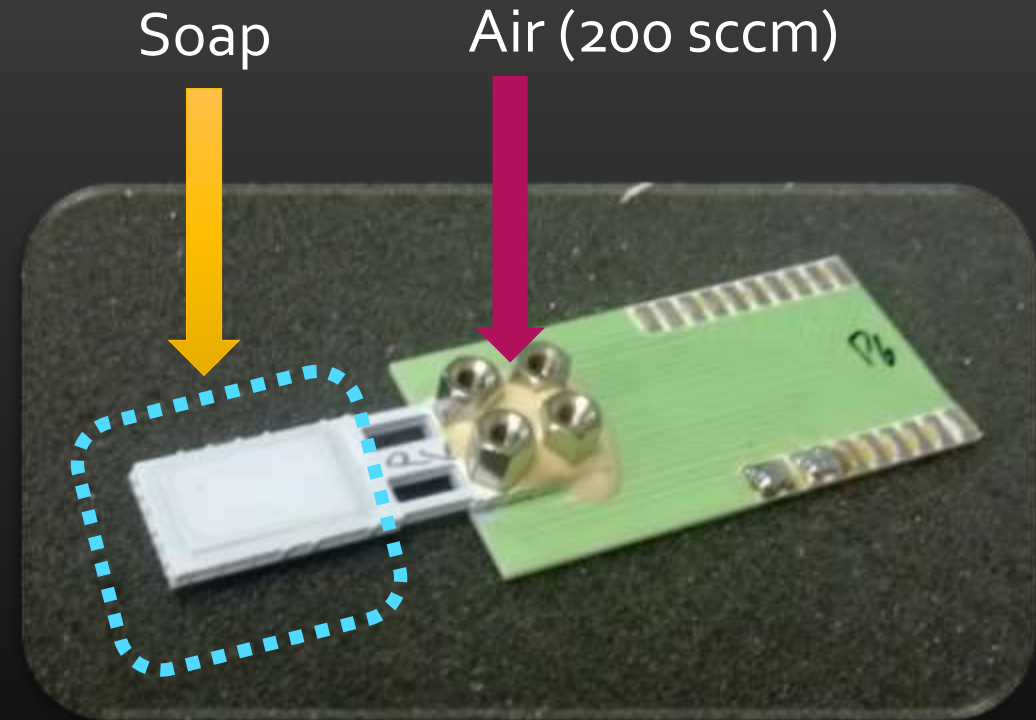
- a. screen printed thick-film platinum (CL11-6109 ,  
< 50 milliohms per square, Heraeus Inc.)
- a. Co-firing process
- b. fired thickness  $\approx 10 \text{ }\mu\text{m}$



# Fluidic characterization

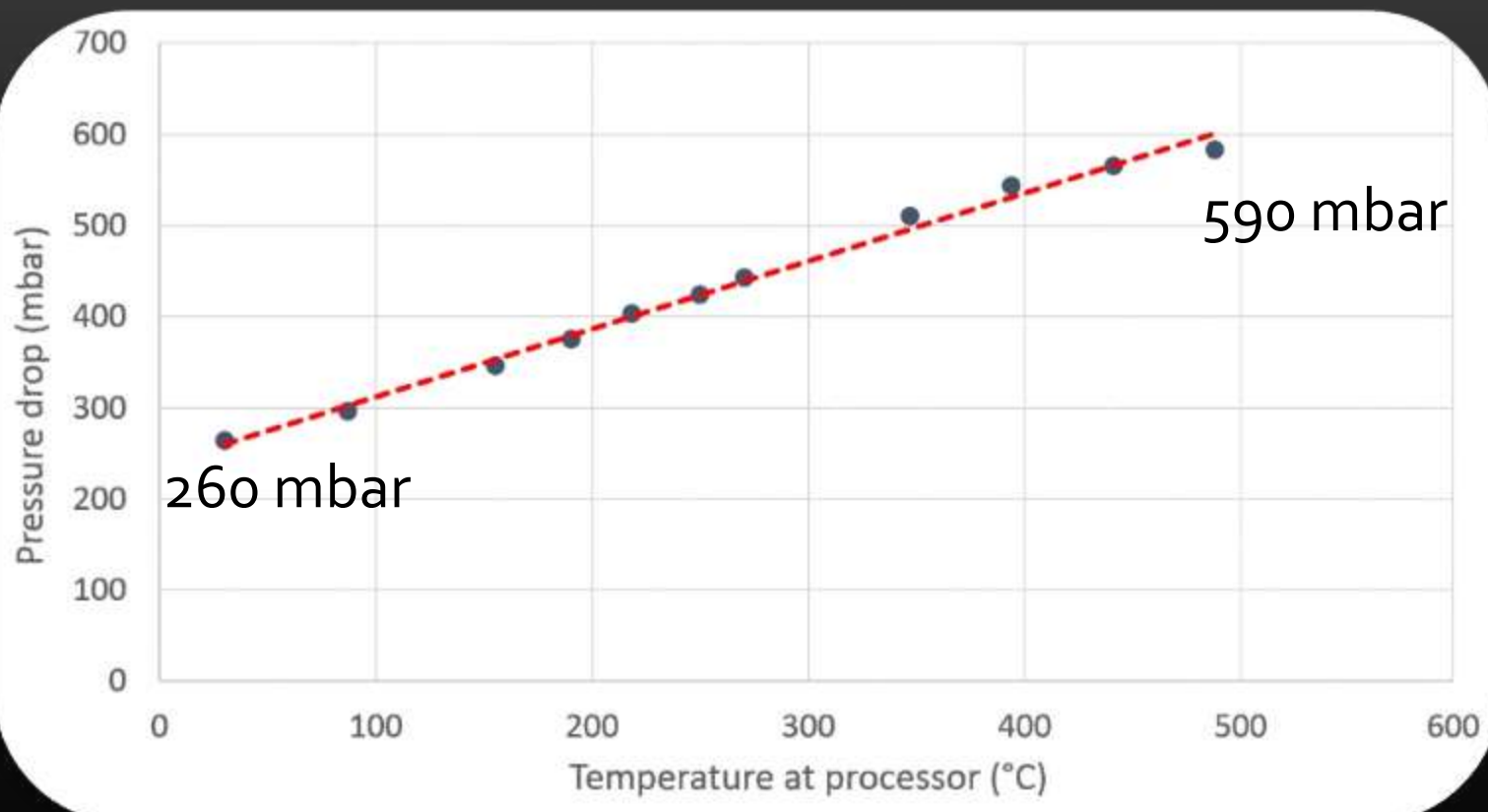
## Hermeticity of as-prepared MSR

- Using ESL 4026 sealing glass for the processor packaging
- Simply using soap solution to check the leakage of sealed LTCC fuel processor under apply 200 sccm of air flow at room temperature
- No leaking was observed on as-prepared fuel processor



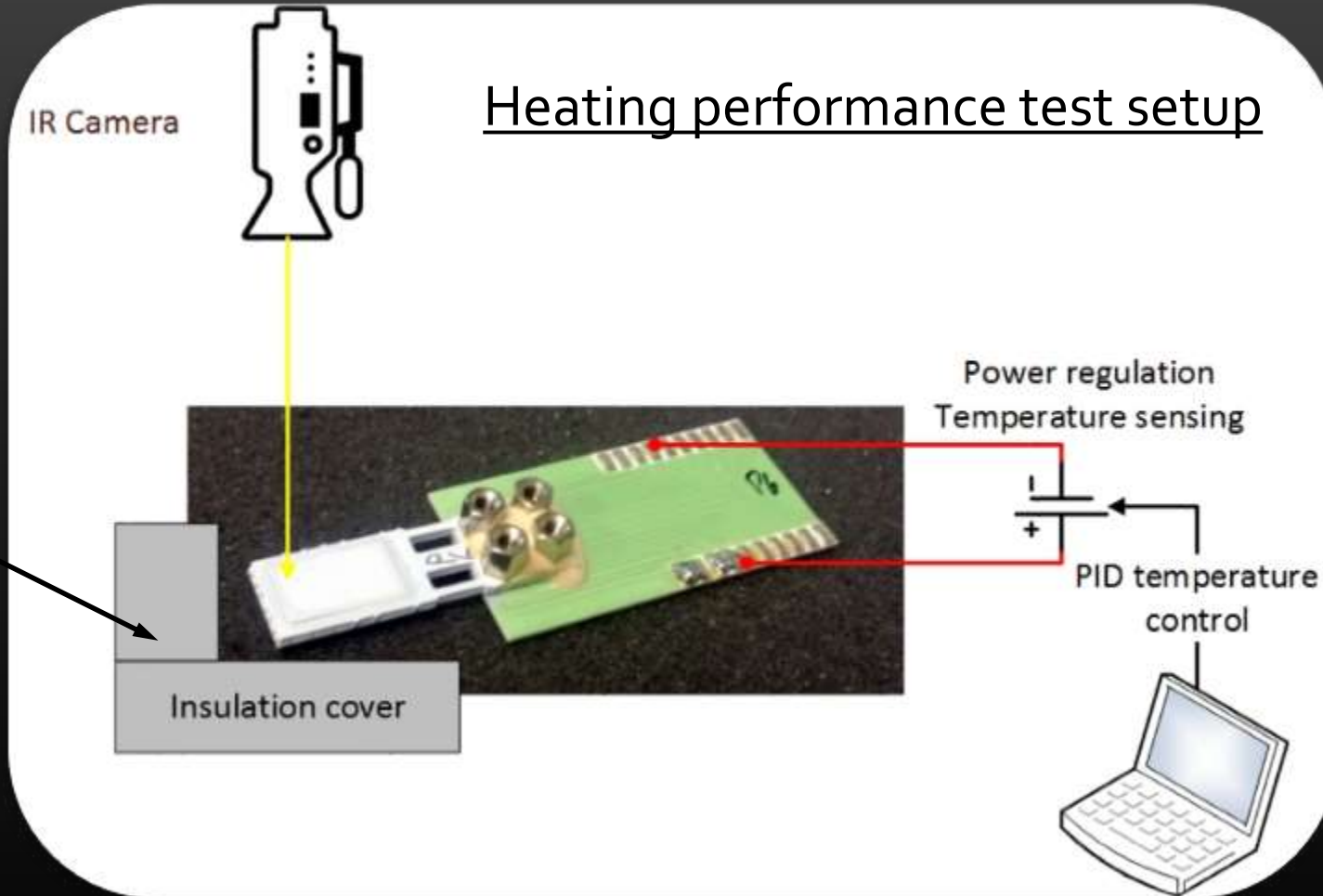
# Fluidic characterization

## Pressure drop



- Flow rate of air: 200 sccm
- Moderate pressure drop across the processor  
590 mbar @ 490°C

# Thermal characterization



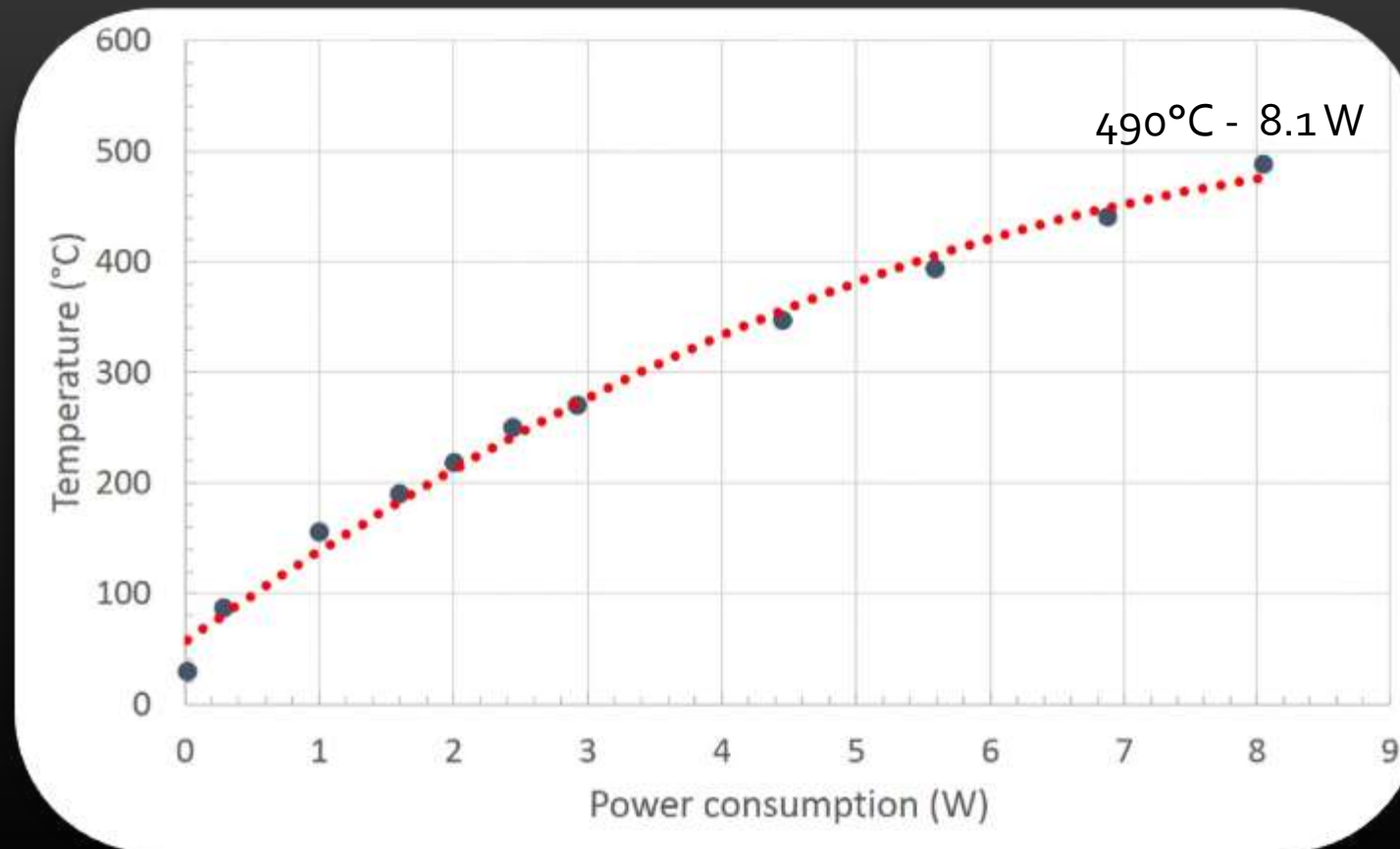
WDS© Ultra, thermal conductivity at 500° C: 0.027 W/m/K

Max. applied voltage: 24 V



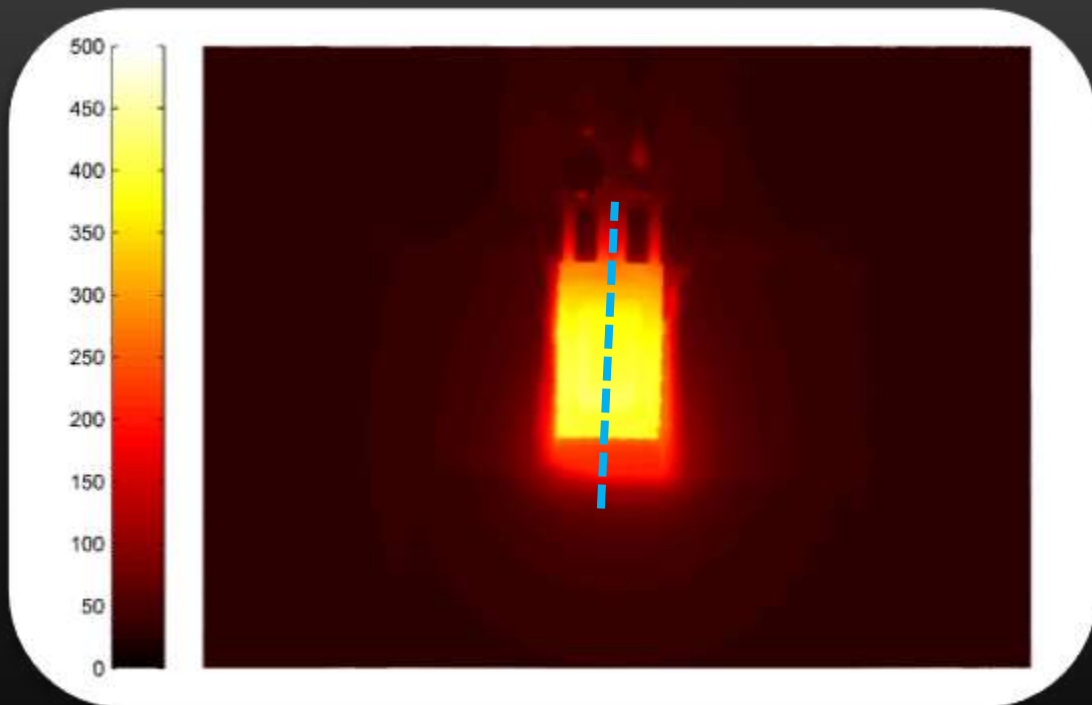
# Thermal characterization

## Power consumption vs. heating performance

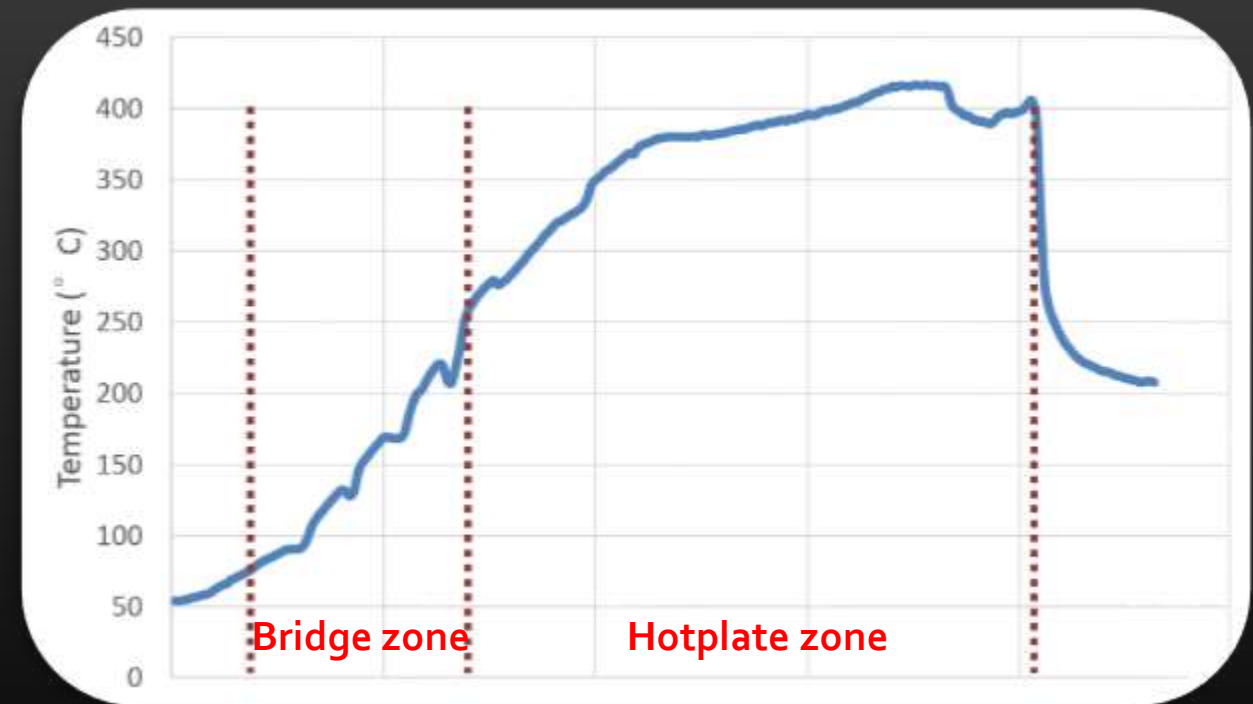


# Thermal characterization

An IR Image of LTCC fuel processor  
running at 400°C of temperature set point



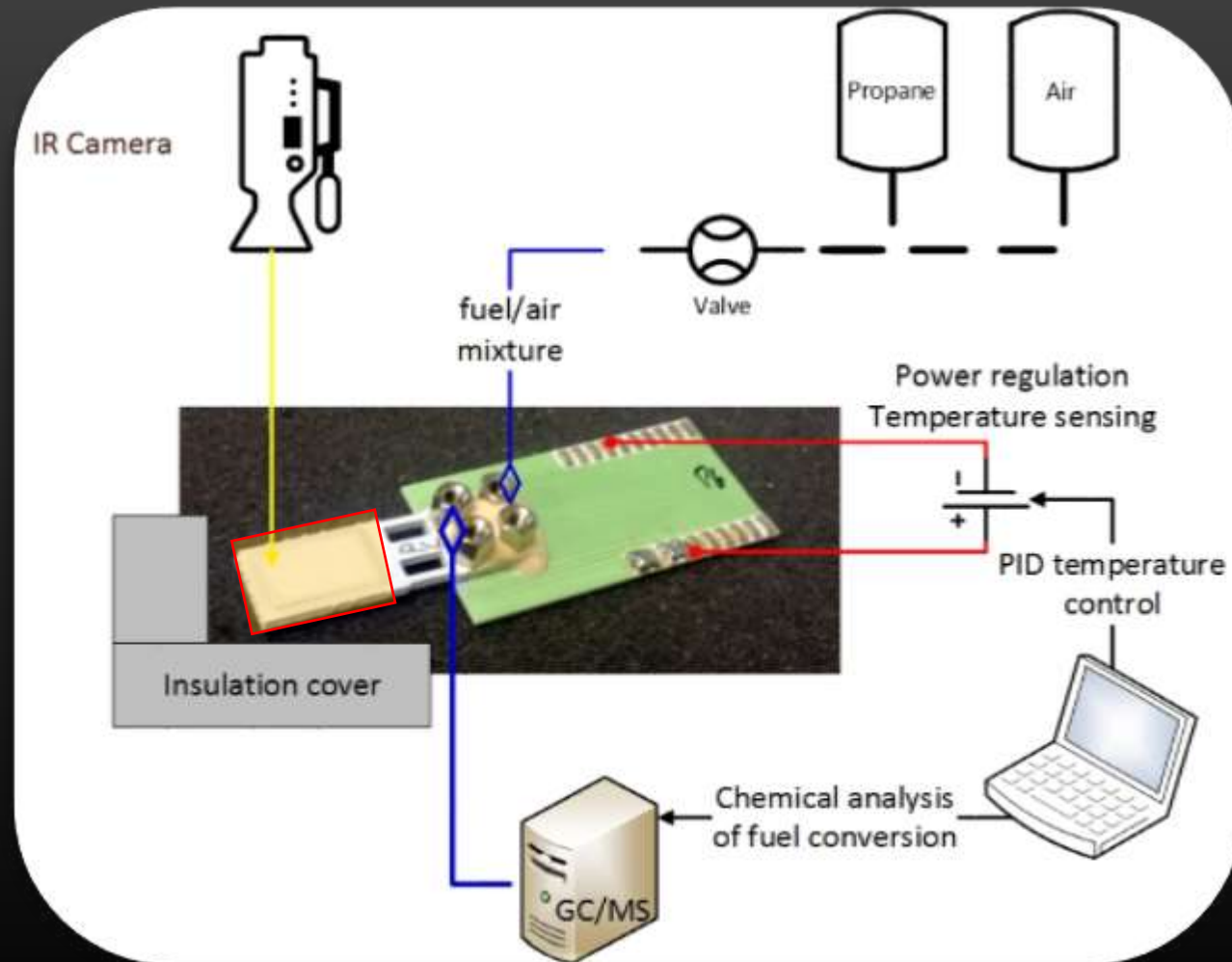
Temperature distribution profile



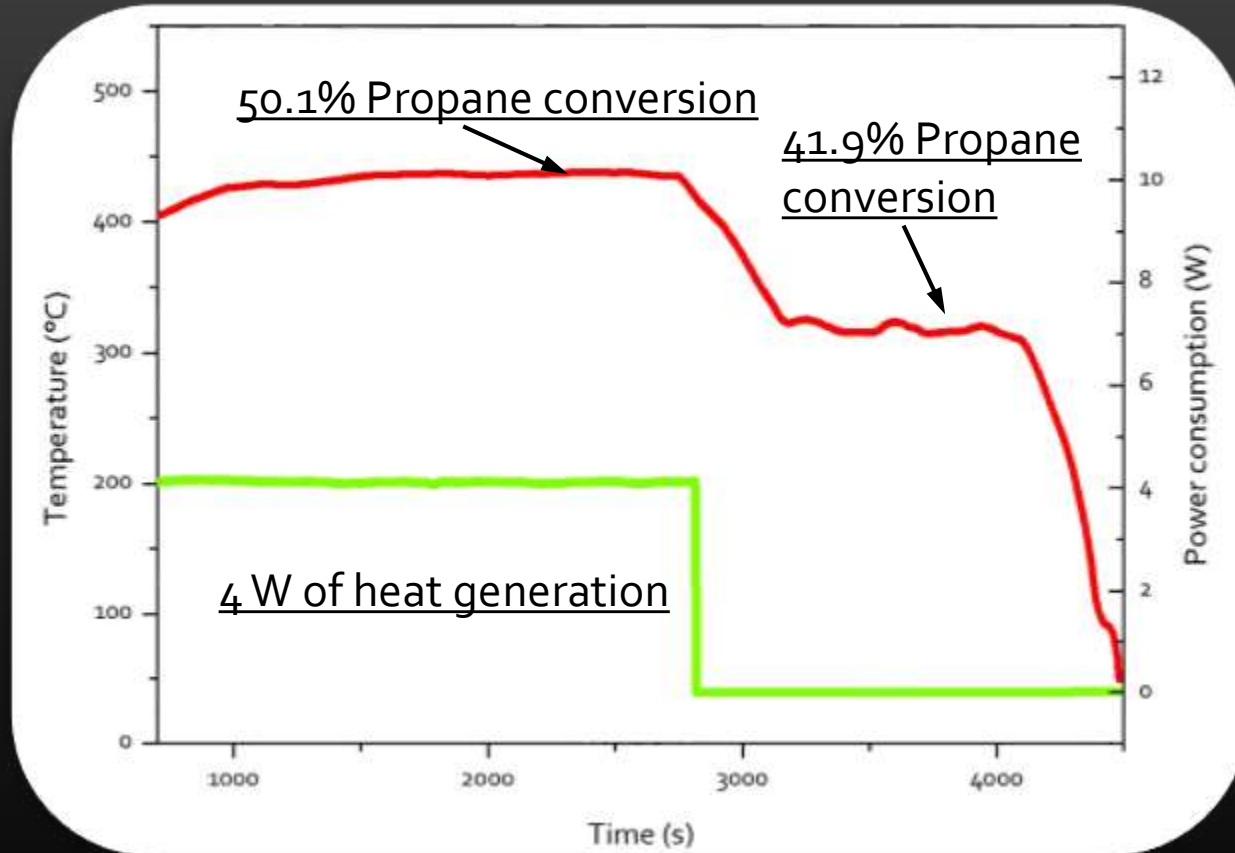
Bridge structure for efficient thermal isolation = convective fluidic and electrical connection available

# Self-sustain reaction characterization

Thermally self-sustain reaction testing setup



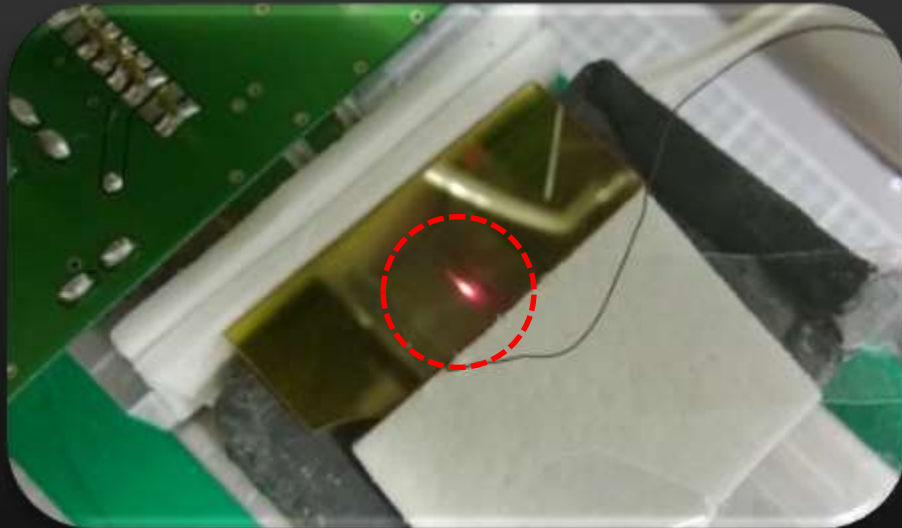
# Self-sustain reaction characterization



## Self-sustaining reaction

- C/O ratio = 1
- Flow rate = 200 sccm of air/propane mixture
- Starting temperature = 400°C
- Propane was able to partially oxidized in the LTCC fuel processor
- The exothermic reaction makes the thermally independent reactor operation possible

# Self-sustain reaction characterization



## Problem:

- unstable sealing caused the leakage after the exothermic reaction
- the leakage may result in propane's low conversion



# Conclusion

- A LTCC fuel processor was developed for the  $\mu$ -SOFCs system
- The micro-scale fine structuration was realized in LTCC fuel processor through a novel progressive lamination
- The catalyst packed bed with YSZ beads could provide moderate pressure drop across the LTCC fuel processor
- The novel bridge structure efficiently isolates the heating zone of the processor
- 70% of heating area at hot zone could maintain relatively homogenous thermal distribution
- The LTCC fuel processor achieved self-sustaining operation through the exothermic partial oxidation of propane at a feeding flow rate of 200 sccm and C/O ratio = 1

# Outlook

- Achieve reliable sealing for the LTCC fuel processor packaging
- Improve design of packed bed for avoiding hot spot
- Total oxidization process implementation in the LTCC fuel processor
- Thermal insulation enhancement



Thank you!

