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Adsorption kinetics of ions
at Bi single crystal planes
from aqueous electrolyte solutions and
room- temperature ionic liquids



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to my dearest ones

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I. LIST OF ORIGINAL PUBLICATIONS

- I. **L. Siinor**, K. Lust and E. Lust, Impedance study of adsorption of iodide ions at Bi(001) electrode from the aqueous solutions with constant ionic strength, *Journal of Electroanalytical Chemistry*, Volume 601, Issues 1–2, 15 March 2007, Pages 39–46.
- II. **L. Siinor**, V. Ivaništšev, K. Lust, E. Lust, Impedance study of adsorption of iodide ions at Cd(0001) and Bi(111) electrode from various solutions with constant ionic strength, *Journal of Solid State Electrochemistry*, Volume 14, Number 4, April, 2010, Pages 555–563.
- III. **L. Siinor**, K. Lust, and E. Lust, Electrical Double Layer Structure at Bi(111)|1-ethyl-3-methyl-imidazolium Tetrafluoroborate Interface, *ECS Transactions*, Volume 16, Issue 49, October 2008, Pages 559–567.
- IV. **L. Siinor**, K. Lust, E. Lust, Electrical Double Layer Capacitance at Bi(111)|1-Ethyl-3-methylimidazolium Tetrafluoroborate Interface as a Function of the Electrode Potential, *Journal of Electrochemical Society*, Volume 157, Issue 7, 25 May 2010, Pages F83–F87.
- V. **L. Siinor**, K. Lust, E. Lust, Influence of anion composition and size on the double layer capacitance for Bi(111) | room temperature ionic liquid interface, *Electrochemistry Communications*, Article in Press.

Author's contribution:

- Paper I: Performed all electrochemical measurements, modeling of data and interpretation of results.
- Paper II: Performed all electrochemical measurements at Bi(111) electrode, modeling of data and interpretation of results.
- Paper III: Performed all electrochemical measurements, modeling of data and interpretation of results.
- Paper IV: Performed all electrochemical measurements, modeling of data and interpretation of results.
- Paper V: Performed all electrochemical measurements, modeling of data and interpretation of results.

2. ABBREVIATIONS AND SYMBOLS

A	CPE coefficient
A	area of the electrode
ac	alternating current
AFM	atomic force microscopy
c	analyte concentration
C_0	thermodynamic low-frequency capacitance
C_{ad}	adsorption capacitance
C_{dl}	“true” high-frequency differential double layer capacitance
c_{KI}	concentration of KI
CPE	constant phase element
C_s	differential capacitance
CV	cyclic voltammetry
D	diffusion coefficient
E	electrode potential
EC	equivalent circuit
edl	electrical double layer
EDLC	electrochemical double layer capacitor
EIS	electrochemical impedance spectroscopy
EMImBF ₄	1-ethyl-3-methylimidazolium tetrafluoroborate
EMImFAP	1-ethyl-3-methylimidazolium tris(pentafluoroethyl)trifluorophosphate
EMImTCB	1-ethyl-3-methylimidazolium tetracyanoborate
E_{min}	potential of minimum in C, E- curves
f	ac frequency
FMG	Frumkin-Melik-Gaikazyan model
j	imaginary unit, $j = \sqrt{-1}$
IL	ionic liquid
i_p	peak current
ISE	ion selective electrode
j	current density
n	number of moles
q	electrode charge density
R_{ad}	adsorption (or partial charge transfer) resistance
R_D	diffusion-like process resistance
R_{el}	high-frequency series resistance
R_p	parallel resistance
RTIL	room temperature ionic liquid
SCE	saturated calomel electrode
STM	scanning tunneling microscopy
Z	complex impedance
Z'	real part of the impedance
Z''	imaginary part of the impedance

Z_w	Warburg-like diffusion impedance
$Z_{W(oc)}$	open circuit finite length Warburg impedance
T	mass transfer frequency factor
v	potential scan rate
x	mole fraction of KI
χ^2	chi-square function
μ	chemical potential
Γ	Gibbs adsorption
α	CPE fractional exponent
σ_{ad}	Warburg constant
τ_D	diffusion relaxation time
τ_H	adsorption relaxation time
(hkl)	the notation of the Bi crystallographic plane (index)
$ Z $	impedance modulus
δ	phase angle
Δ^2	weighted sum of squares
ΔE	potential region of ideal polarizability

3. INTRODUCTION

Adsorption of various ions and molecules has been elaborately studied by several groups of electrochemists. Adsorption processes effect crucially characteristics of heterogeneous electrochemical processes such as anodic dissolution, electrochemical corrosion, electrodeposition, electrosynthesis and electroanalysis of ions and molecules and also processes in electric double layer capacitors and fuel cells. Nature of surface active substances as well as ingredients of solutions and crystallographic structure of electrode surface affect significantly the adsorption process in electrical double layer. Therefore the adsorption kinetics and thermodynamics of inorganic and organic ions, neutral molecules on metal electrodes (poly- and mono crystalline), as well as at the porous carbon electrodes from aqueous and nonaqueous solutions have been studied.

The reason of specific adsorption of anions is the strong interaction between partly desolvated anion and surface atoms of metal. At certain positive surface polarization it leads to the formation of covalent bond between anion and metal surface, which is the slow process and limiting stage is the charge transfer or adsorption step.

Formation of the compact adsorption layer of aromatic heterocyclic poly-functional compounds with specifically adsorbed cations can be used as an effective corrosion inhibitor. The process of electrosynthesis is strongly affected by the composition of surface inactive electrolyte selected as well as by presence of cations and anions that adsorb specifically.

To date, most electrochemical reactions have been carried out in the electrolytes of molecular solvents. Recently, however, a new class of electrolytes has emerged – ionic liquids. These electrolytes are fluid at room temperature, and consist mainly of ionic species. They have many fascinating properties which make them of fundamental interest to all chemists, since both the thermodynamics and kinetics of reactions carried out in ionic liquids are different to those in conventional electrolytes of molecular solvents. As they are made up of at least two components which can be varied (the anion and cation), these electrolytes can be designed with a particular end use in mind, or to possess a particular set of properties. The use of non-aqueous electrolytes and room temperature ionic liquids in electrochemical double layer capacitors (EDLC) was initiated by the wider region of ideal polarizability of nanoporous carbon | electrolyte interface in comparison with the traditional aqueous electrolyte solutions.

The main aim of this work was to establish the limiting stages for the adsorption process and to calculate the kinetic parameters describing iodide ions adsorption at Bi(111) and Bi(001) electrodes from aqueous binary electrolyte solutions as well as to analyze the electrical double layer structure at Bi(111) | ionic liquid interface.

4. LITERATURE OVERVIEW

4.1 Adsorption kinetics of ions on single crystal electrodes

Adsorption of the halide ions from aqueous and non-aqueous electrolyte solutions on single crystal plane electrodes of various metals has been investigated by several electrochemists for a long time [1–21]. However, there are only few works devoted to the adsorption kinetics of the halide and other anions on various single crystal plane electrodes – Au(*hkl*), Ag(*hkl*), Pt(*hkl*), Rh(111) – from aqueous electrolyte solutions and on Bi(*hkl*) from non-aqueous electrolyte solutions [1–6]. The adsorption of halide ions as well as other anions seems to be a rather complicated process [1–33] and the structure of the adsorption layer depends noticeably on the electrode potential, chemical composition and concentration of ions and on the nature of the metal as well as solvent studied [5,6]. At Au (111) | SO₄²⁻ aqueous solution interface the formation of the compact adsorption phase (layer) is possible, but comparatively slow process [1]. The so-called frequency dispersion discussed by Hamelin [7] has been explained later by low adsorption rates of specifically adsorbed anions on Au (*hkl*) [1,8]. For Ag(111) electrode the adsorption of Cl⁻ ions starts near -0.7 V (vs. sat. calomel electrode, SCE) while adsorption of Br⁻ ions starts at $E = -1.0$ V (SCE). A disordered adlayer is formed up to potential of -0.1 V and an ordered adlayer for the anions as an unrotated (1.38×1.38) structure and ($\sqrt{3} \times \sqrt{3}$) R 30° adlayer for Br⁻ ions has been observed, using ex situ reflection energy electron diffraction and in situ STM methods [10–17]. At electrode potentials more positive than the potential of sharp capacitance peak in the capacitance vs potential curves or the current density peak in the current density vs. potential curves, the more compressed adsorption overlayer structure has been observed [16,17]. However, the sum of the double layer and adsorption capacitances (independent of ac frequency) could be obtained only at very low frequency ($f < 2$ Hz) [2]. For real polycrystalline surfaces the situation is more complicated [2].

The strong adsorption of iodide and chloride ions was detected on Bi single crystal planes from aqueous and non-aqueous supporting electrolyte solutions [5,6,31–34]. Analysis of the impedance data can help to understand the complicated adsorption behavior of iodide ions at the Bi(*hkl*) planes within a wide potential region. The impedance data of I⁻ and Cl⁻ can be fitted with classical Frumkin–Melik-Gaikazyan (FMG) model.

The thermodynamics of the halides adsorption has been discussed and analyzed in detail by Parsons [18], Lipkowski et al.[19,20], Schmickler [21], Damaskin et al. [24–26], Vorotyntsev and Golub [27,28], as well as by Schultze and Vetter [29], Schmickler and Guidelli [30]. There are some differences in the thermodynamic data obtained using various measurement methods and it is

probably mainly caused by the slow adsorption rate of the halide anions as well as by the partial charge transfer process from the adsorbed halide ions to the metal surface depending on the chemical nature of the electrolyte studied [19–21,29–33]. For example, Lipkowski et al. [19] observed that the charge densities calculated by using differential capacitance, chronocoulometry and voltammetry methods differ each other even if the same method has been used for the surface preparation of the Au(*hkl*) electrode.

4.2 Ionic liquids

4.2.1 Physical properties of ionic liquids [35–36]

An ionic liquid (IL) is a salt in the liquid state, that consists of large organic cations and smaller inorganic anions or vice versa. Ionic liquids are usually liquid below 100 °C.

4.2.1.1 Viscosity

Ionic liquids are more viscous than common molecular solvents and high viscosity is determined by van der Waals forces and hydrogen bonding. Electrostatic forces may also play an important role. Viscosity of IL increases with the increase of alkyl chain's length because of stronger van der Waals forces between cations. Hydrogen bonding between anions also accrues viscosity.

4.2.1.2 Conductivity

Ionic liquids have relatively good ionic conductivity, based on the fact that they consist only of ions, but at room temperatures their conductivities are lower than in concentrated aqueous electrolyte solutions. Conductivity depends not only on the number of charge carriers but also on their mobility, it indicates that ionic liquids that consist of large ions have lower conductivity. Ionic liquids with higher viscosity leads to lower conductivity. Increase in temperature lowers viscosity and increases conductivity.

4.2.1.3 Density

Ionic liquids are denser than water with density from 1 to 1.6 g cm⁻³ and their densities decrease with increase in the length of the alkyl chain in the cation. Density of ionic liquids is also affected by identity of anions.

4.2.1.4 Melting point

Ionic liquids have low melting point below 100 °C and most of them are liquid at room temperature. Both anion and cation structures play an important role in low melting point of IL. If anion size increases, the melting point decreases and if cations are large and asymmetrically substituted, it reduces melting point.

4.2.1.5 Thermal stability

Ionic liquids are known for their good thermal stability up to 450 °C. The thermal stability of ionic liquids is limited by the strength of their heteroatom–carbon and heteroatom–hydrogen bonds, but ionic liquids can tolerate such high temperature only for short time, otherwise they decompose.

4.2.1.6 Electrochemical window

The role of the region of ideal polarizability, i.e. electrochemical window is significant using ionic liquids in electrochemical measurements (electrodeposition of metals, semiconductors and supercapacitors). Electrochemical stability of solvents and electrolytes determine the electrochemical window. The electrodeposition of elements and compounds from aqueous electrolyte solutions is limited by low electrochemical window, but in ionic liquids it is noticeable wider.

4.2.2 Ionic liquids in electrochemistry

Recent research activity of ionic liquids, initiated by their potential applications in various modern electrochemical power systems, created interest in the interface between ionic liquids and metal [37–49] as well as carbon, including nanoporous carbon electrodes [50–52]. They are increasingly being used in applications such as green synthesis [54,55], catalysis with transition metals [56,57], and in electrochemical applications such as electrodeposition of metals [58], as electrolytes in lithium-ion batteries [59–61], sensors [62–66], supercapacitors [67–69], solar cells [70], and fuel cells [71].

RTILs are currently being investigated as possible electrolytes for gas sensing applications [55], since their favorable properties (low-volatility and high thermal stability) means that the sensor does not dry out, and provides the possibility for gas sensing at high temperatures, which may be of use in the combustion industry and elsewhere. Potentiometry with ion selective electrodes (ISEs) is an accurate, fast, and inexpensive analytical method [63–66]. ISEs have provided the possibility to detect chemical species with reasonable selecti-

vity and low detection limit. ILs were found to be excellent materials to prepare membranes for ISEs due to their polymer plasticizing ability and ionic nature.

Electrochemical capacitors, based on the differential capacitance of the double layer formed at the carbon/electrolyte interface, have received considerable attention as they can be used as high power density energy storage devices. Both carbon materials as well as electrolytes have been developed for application in various systems. Many aqueous and organic liquid solutions of electrolytes have been used in electrochemical capacitors. Because of the superior properties of ionic liquids they have recently widely been studied as electrolytes in EDLC [67–69].

Ionic liquids have been used in lithium-ion batteries as novel candidates for electrolyte solvents [59–61]. EMImBF₄ (1-ethyl-3-methyl imidazolium) series RTILs have been widely used for battery applications since the discovery of EMImBF₄ because of their moderate viscosity and conductivity. Among many from the series of RTILs, quaternary ammonium cation-imide combinations are fairly interesting because of their higher electrochemical stability especially in the reduction reaction, but in this case graphitized carbon materials for Li-ion batteries have difficulty in obtaining the practical Li⁺ intercalation/deintercalation capacitance without additives. RTILs improve the safety of Li-ion batteries with carbon negative electrodes. To date, RTILs are the most promising electrolytes for improving the safety of Li-metal batteries which could be important for higher energy densities, i.e. for transportation applications.

Ionic liquids are good solvents for catalytic reactions [56–57]. The rational selection of the appropriate ionic liquid solvent for a particular reaction requires general knowledge about the properties of ionic liquids, and the details of some properties of the specific ionic liquid solvents being considered.

A fuel cell is an electrochemical device that converts a fuel into an electrical current. Fuel cells are made up of three segments: the anode, the electrolyte and the cathode. Brønsted acid-base ionic liquids, inorganic and organic ionic liquids have been investigated as the electrolyte candidates for fuel cells electrolytes [72–74]. Inorganic ammonium salt mixtures can actually be used in place of the commonly used organic ionic liquids as fuel cell electrolytes. The fuel cell electrodes can operate in the same temperature range as existing fuel cells, while the efficiencies at low current densities can be much better [75].

4.3 Electrochemical impedance spectroscopy

Electrochemical impedance spectroscopy (EIS) method is based on the system response to the application of a periodic small amplitude ac signal, and therefore these measurements are carried out at different ac frequencies. Analysis of the system response contains information about the interface, its structure and reactions taking place at the interfaces.

System impedance is a complex parameter and may be represented in Cartesian form as,

$$Z = Z' + jZ'' \quad [4.3.1]$$

where the real and imaginary parts of the impedance are: $Z' = R$ and $Z'' = -1/\omega C$, respectively.

$$\delta = \arctan \frac{|Z''|}{Z'} \quad [4.3.2]$$

δ is the phase-angle between the ac current and potential applied. The current has the same frequency as the applied potential but can be phase-shifted by the angle δ depending on the system characteristics.

On ideally polarizable solid electrodes the electrical equivalent model can be usually represented (including the monocrystalline electrodes in the case of absent adsorption) as a series connection of the solution resistance and double-layer capacitance. However, on solid electrodes frequency dispersion is observed, that is the observed impedances cannot be represented by connection of simple R - C elements. The impedances may often be represented by an equation without simple electrical representation, i.e. through the so-called distributed elements. The Warburg impedance is an example of a distributed element.

Experimental impedance data in this work were fitted by using the equivalent circuits shown in Fig. 1, where R_{el} is the high-frequency series resistance equal to the electrolyte solution resistance at $f \rightarrow \infty$; C_{dl} is the so-called “true” high-frequency differential double layer capacitance, obtained at $f \rightarrow \infty$ ($C_{dl} = (\partial q / \partial E)_{\Gamma, \mu}$, where q is the electrode charge density, Γ is the Gibbs adsorption and μ is the chemical potential); adsorption capacitance C_{ad} is equal to $(C_0 - C_{dl}) = (\partial q / \partial \Gamma)_E (\partial \Gamma / \partial E)_{\mu}$, where thermodynamic low-frequency capacitance $C_0 = (\partial q / \partial E)_{\Gamma, \mu} + (\partial q / \partial \Gamma)_E (\partial \Gamma / \partial E)_{\mu}$ is obtained at $f \rightarrow 0$; $Z_w = \sigma_{ad}(j\omega)^{-1/2}$ is Warburg-like diffusion impedance ($\sigma_{ad} = \tau_D^{1/2} C_{ad}^{-1}$ is the Warburg constant, where τ_D is the diffusion relaxation time); CPE is the constant phase element and the CPE impedance Z_{CPE} is equal to $A^{-1}(j\omega)^{-\alpha}$ (A is a CPE constant and α is fractional exponent; if $\alpha = 1$ then $A = C_{dl}$); R_{ad} is the adsorption (or partial charge transfer) resistance ($R_{ad} = \tau_H C_{ad}^{-1}$, where τ_H is adsorption relaxation time); and R_p is the parallel resistance, calculated according to the classical conception discussed in elsewhere [76-80]. The goodness of a fit is estimated by the value of the χ^2 – function, weighted sum of squares (Δ^2), and by the relative errors of each parameter in the equivalent circuit (EC) under analysis.

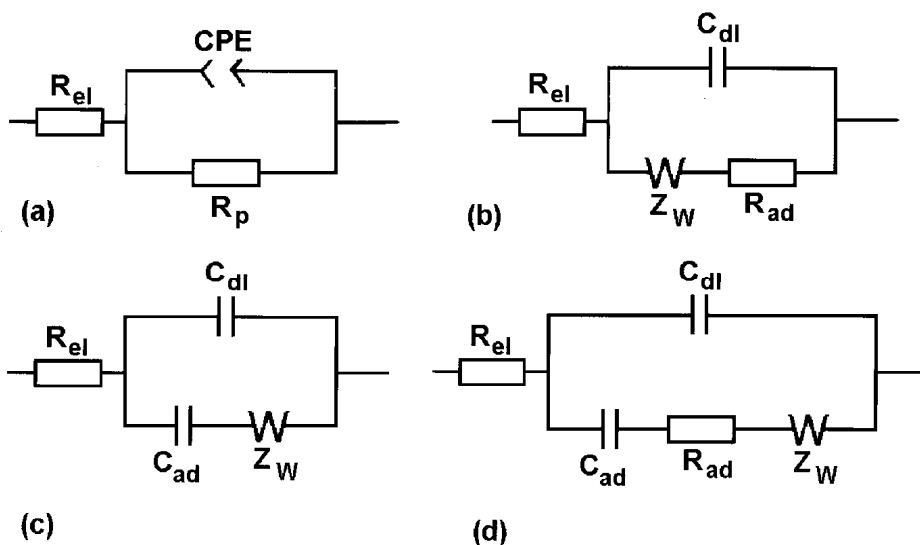


Fig. 1. Equivalent circuits used for fitting the experimental data. R_{el} is the electrolyte solution (high frequency) resistance, C_{dl} is the double layer capacitance at ac $f \rightarrow \infty$, C_{ad} is the adsorption capacitance, Z_w is the Warburg-like diffusion impedance defined as $Z_w = \sigma_{ad}(j\omega)^{-1/2}$, where σ_{ad} is the coefficient of the Warburg impedance. CPE is the constant phase element with impedance $Z_{CPE} = A^{-1}(j\omega)^{-\alpha}$ (A is a constant and α is a fractional exponent, $CPE = C_{dl}$ if $\alpha=1$). R_{ad} is the adsorption or partial charge transfer resistance and R_p is the parallel charge transfer resistance.

4.4 Cyclic voltammetry

Cyclic voltammetry is the most widely used technique for acquiring qualitative information about electrochemical reactions. In a typical cyclic voltammetry method, a solution component is electrolyzed (oxidized or reduced) by placing the solution in contact with an electrode surface, and then making that surface sufficiently positive or negative in voltage to initiate the electron transfer. It enables the electrode potential to be rapidly scanned in search of redox couples. Once located, a couple can then be characterized from the potentials of peaks on the cyclic voltammogram and from current changes caused by variation of the potential scan rate. CV analysis is often the first experiment or method performed in an electrochemical study. To obtain a cyclic voltammogram, the current at the working electrode is measured during the potential scan.

Usually the electrode potential is ramped linearly to a more negative potential, and then ramped in reverse back to the starting voltage. The forward scan produces a current peak for any analytes that can be reduced through the range of the potential scan. The current will increase as the potential reaches the reduction potential of the analyte, but then falls off as the concentration of the analyte is depleted close to the electrode surface. As the applied potential is

reversed, it will reach a potential that will reoxidize the product formed in the first reduction reaction, and produce a current of reverse polarity from the forward scan. This oxidation peak will usually have a similar shape to the reduction peak. The peak current, i_p , is described by the Randles-Sevcik equation:

$$i_p = (2.69 \times 10^5) n^{3/2} A c D^{1/2} \nu^{1/2} \quad [4.4.1]$$

where n is the number of moles of electrons transferred in the reaction, A is the area of the electrode, c is the analyte concentration (in moles/cm³), D is the diffusion coefficient, and ν is the scan rate of the applied potential.

5. EXPERIMENTAL

5.1 Measurements in aqueous solutions

The adsorption kinetics of iodide ions at electrochemically polished Bi(001) and Bi(111) single crystal planes from aqueous solutions with constant ionic strength $0.1x$ M KI + $0.1(1-x)$ M KF and $0.1x$ M KI + $0.033(1-x)$ M K_2SO_4 was studied by ac impedance spectroscopy (0.1 stands for the total concentration of solution and x is the mole fraction of KI in a solution). Measurements were carried out in the solutions with constant ionic strength to minimize the influence of the changes in the total solution concentration on the diffusion and adsorption steps. Solutions were prepared from KF, KI and K_2SO_4 (Aldrich Chemical Company, 99.998%) and Milli Q+ water (ultra purified water using the Milli Q+ purification system, resistance > 18.2 M Ω cm). Surface preparation of the electrodes was carried out before each experiment by electrochemical polishing in an aqueous solution of KI+HCl. After that the electrodes were rinsed carefully with Milli Q+ water and polarized at -1.2 V (vs. Ag | AgCl | 4M KCl aqueous solution) in surface-inactive electrolyte solution, which was previously saturated with the electrolytic hydrogen for minimum 2 hours. The quality of the Bi single crystal electrodes were tested by X-ray diffraction, in situ STM, AFM and ultra high vacuum STM methods. The experimental impedance spectra were measured using Autolab PGSTAT 30 FRA 2 ($0.1 < f < 10000$ Hz, 100 different frequencies).

5.2 Measurements in ionic liquids

Bi(111)|ionic liquid (1-ethyl-3-methylimidazolium tetrafluoroborate (EMImBF₄), $>99.0\%$, ≤ 200 ppm H₂O, Fluka; 1-ethyl-3-methylimidazolium tris(pentafluoroethyl)trifluoro-phosphate (EMImFAP), 99.9% , ≤ 100 ppm H₂O, Merck KGaA and 1-ethyl-3-methylimidazolium tetracyanoborate (EMImTCB), 99.9% , ≤ 100 ppm H₂O, Merck KGaA) interface has been studied by cyclic voltammetry (CV) (potential cyclation rate was varied from 0.5 to 500 mV s⁻¹) and impedance spectroscopy ($0.1 < f < 10000$ Hz, 100 different frequencies) using Autolab PGSTAT 30 FRA 2 at temperature 296 ± 0.1 K inside glove box (Labmaster sp, LMBraun; O₂ and H₂O concentrations < 0.1 ppm). The Bi(111) electrode was electrochemically polished before each experiment in the KI+HCl aqueous solution. After polishing the electrode was rinsed with Milli Q+ water, dried by Ar (99.99995%) and by ionic liquid. Ionic liquids were saturated for 24 hours with Ar (99.99995%) before submerging the electrochemically polished Bi (111) electrode into electrolyte. Electrochemically stable current densities have been established after at least 2 hours polarization of the electrode at -0.7 V (vs. Ag | AgCl | ionic liquid currently measured).

6. RESULTS AND DISCUSSION

6.1 Adsorption of iodide ions at Bi(111) and Bi(001) single crystal electrodes [I, II]

Cyclic voltammetry and electrochemical impedance spectroscopy have been applied for investigation of adsorption kinetics of iodide ions from aqueous electrolyte solutions at electrochemically polished Bi(*hkl*) electrodes. The cyclic voltammetry (*j* vs. *E*) curves show that the Bi(111) electrode is ideally polarizable within the regions of $-1.4 < E < -0.55$ V (vs. Ag|AgCl|4M KCl) in the aqueous solution with constant ionic strength $0.1x$ M KI + $0.033(1-x)$ M K₂SO₄ and Bi(001) is ideally polarizable within the potential region from -1.4 V to -0.5 V (vs. Ag|AgCl|4M KCl) in the aqueous solution of $0.1x$ M KI + $0.1(1-x)$ M KF. The electrochemical impedance spectroscopy method has been used for the quantitative study of I⁻ ions adsorption at bismuth single crystal planes.

The complex impedance plane $-Z''$, Z' – plots, i.e. Nyquist plots, where Z'' is an imaginary component ($Z'' = -\frac{1}{C_s\omega}$, C_s is the total series capacitance at fixed angular frequency $\omega = 2\pi f$, where *f* is ac frequency), and Z' is a real part of the impedance [76–85] at different electrode potentials and mole fractions of KI, are shown in Figs. 2 and 3, where points are experimental data and solid lines are fitting results (discussed later). The shape of a Z'' , Z' curve depends noticeably on the electrode potential applied (Fig. 2) and on the amount of the surface active electrolyte KI in the solution (Fig. 3). At fixed KI concentration, c_{KI} , and Z' , the absolute value of Z'' slightly decreases with the decrease of negative potential of the electrode from -1.2 to -0.5 V (vs. Ag|AgCl|4M KCl), which is explained by the weak adsorption and partial charge transfer from the adsorbed I⁻ anions to the Bi(001) and Bi(111) surface [23, 31–33, 76,77].

In the region of intensive increase of the differential capacitance C_s ($-0.7 < E \leq -0.5$ V) the impedance spectra for Bi(*hkl*) have a complicated shape (Fig. 2) and can be fitted by tilted non-linear curves rather than by the semicircles, characteristic of the true faradic process [76–85]. In this region of electrode potentials, the value of $|Z''|$ increases with increasing the mole fraction of KI in the solution (Fig. 3) because of the noticeable adsorption and partial charge transfer process. In the region of more negative potentials than -1.4 V the slight increase in the current density can be observed and the impedance spectra become a shape of slightly depressed semicircles, which indicate the beginning of the faradic process (hydrogen evolution from KF + KI aqueous solutions) or can be explained by the slow adsorption of K⁺ ions following by the partial charge transfer process. These parts of the $-Z''$, Z' spectra have not analyzed in detail in this work.

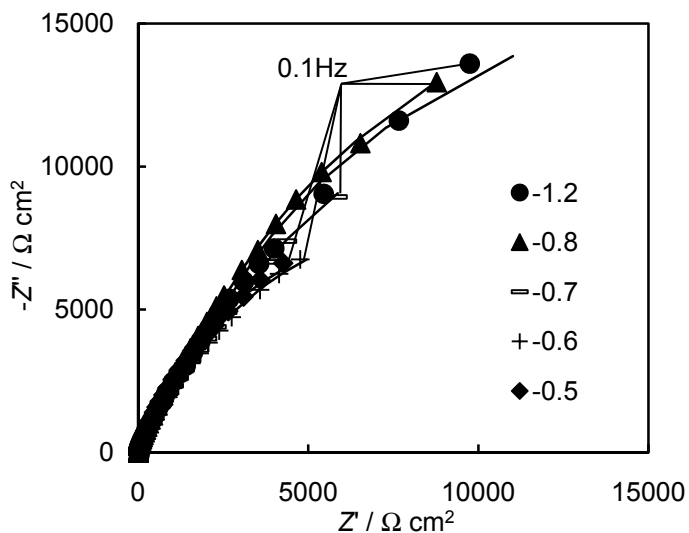


Fig. 2. Complex impedance plane plots for the Bi(001) electrode in 0.1 M KI aqueous solution at different electrode potentials E (V vs. Ag | AgCl), noted in figure. Marks – experimental data, and solid lines – fitting according to the Frumkin-Melik-Gaikazyan equivalent circuit (c in Fig. 1).

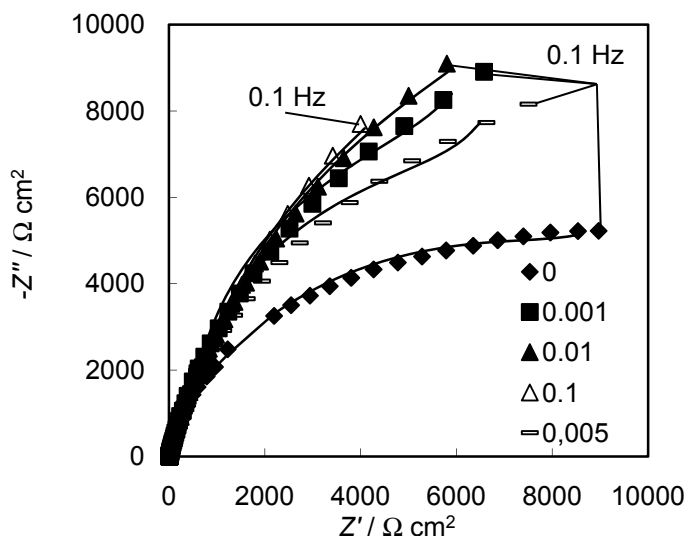


Fig. 3. Complex impedance plane plots for the Bi(001) electrode at -0.5 V in $0.1x \text{ M KI} + 0.1(1-x) \text{ M KF}$ aqueous solutions at different mole fractions of KI, x (M), noted in figure. Marks – experimental data, and solid lines – fitting according to the FMG equivalent circuit (c in Fig. 1).

The dependence of the phase angle δ ($\delta = \arctan(|Z''|/Z')$) on $\log f$ is presented in Figs. 4, because the Z''/Z' plots do not indicate the all needful information. Differently from the non-aqueous LiI solution | Bi(*hkl*) interface the shape of the δ , $\log f$ curves is nearly independent of KI concentration if $E < -0.8$ V and $c_{\text{KI}} < 0.05\text{M}$ (Ag | AgCl) (Fig. 4 a).

In the low- frequency range from 0.1 to 1 Hz, δ values change from -58 to -60° , indicating the kinetically mixed process (i.e. the total rate of the process becomes limited by the rates of diffusion-like and adsorption steps as well as partial charge transfer). The high absolute values of $|\delta| \approx 80^\circ$ obtained in the moderate ac frequency region from 10 to 100 Hz show that the adsorption of the solution components at Bi(001) and Bi(111) planes is limited mainly by the rate of adsorption step [5,6,78–83].

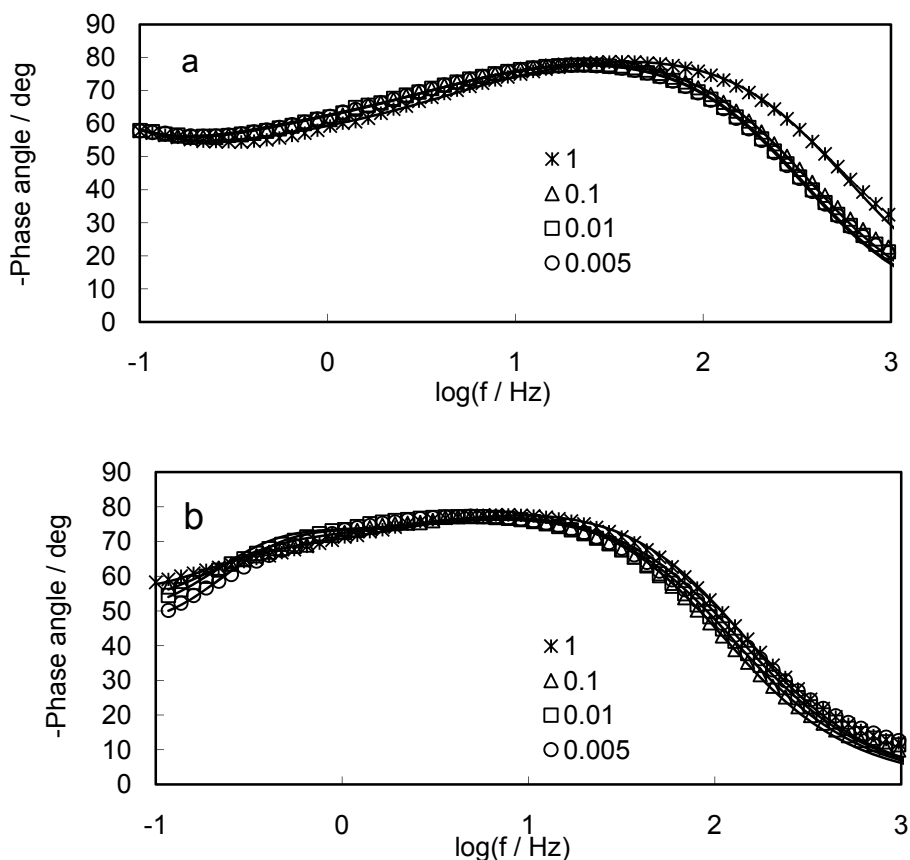


Fig. 4. Dependence of the phase angle (δ) on ac frequency for the Bi(111) electrode in 0.1x M KI + 0.033(1-x) M K_2SO_4 aqueous solutions at the various fixed electrode potentials -1.2 V (a), -0.5 V (b) at the mole fractions of KI, x (M), noted in figure.

In the region of less negative potentials ($E \geq -0.8$ V vs. Ag | AgCl | 4M KCl) there is a certain dependence of the phase angle on the concentration of KI at ac frequency $f < 1$ Hz as well as at $f > 10$ Hz. In ac frequency range from 1 Hz to 10 Hz the experimental data show that the main limiting stage is the adsorption step $|\delta| > 75^\circ$ (Fig. 4b). In the high- frequency range $f > 100$ Hz the absolute values of phase angle increase with c_{KI} , indicating the rise of the role of the adsorption step in the adsorption kinetics, but the limiting stage is still mixed kinetics (diffusion, adsorption and partial charge transfer) with $|\delta| > 45^\circ$. Thus, in the potential region of intensive adsorption of the Γ^- ions (near -0.5 V vs. Ag | AgCl) (Fig. 4b), there is a considerable dependence of δ on the concentration of KI, the limiting stage is the mixed kinetic step (slow adsorption, diffusion as well as partial charge transfer steps, discussed in [31–33]). At $f < 1$ Hz the absolute values of phase angle $|\delta|$ decrease from 50° to 60° , hence, they are closer to $|\delta| = 45^\circ$, which is characteristic of the semi- infinite diffusion step limited processes [76–85]. A noticeable dependence of the phase angle on c_{KI} in the region of ac frequency from 100 Hz to 1000 Hz indicates the dependence of the inner layer structure of the electrical double layer on c_{KI} . In the high ac frequency region there is no dependence of $|\delta|$ on the electrode potential in the case of 0.1 M KF as it was established for LiClO_4 solutions in ethanol [5] as well as for KI containing solutions in this work, which indicates that, contrary to the weakly solvated ClO_4^- and Γ^- ions in ethanol [5,6] and Γ^- in water, the F^- ions are unable to enter into the inner part of the electrical double layer. Thus, the solvated F^- ions are practically surface inactive at the $\text{Bi}(001)|$ aqueous solution interface. The same is valid for the K_2SO_4 aqueous solution as base electrolyte (Fig 4b).

6.1.1 Analysis of impedance data

The theoretical impedance data were calculated based on the equivalent circuits shown in Fig. 1 using the non-linear least squares fitting with the experimental impedance data. The best fitting results were obtained with the modified Frumkin-Melik-Gaikazyan equivalent circuit (FMG EC) (circuit c in Fig. 1). The results of fitting show that the values of the fractional exponent, α_w , for the Warburg like diffusion impedance are close to 0.5 (Fig. 5), demonstrating that the deviation of $\text{Bi}(111)|\text{KI}+\text{H}_2\text{O}$ interface from the traditional semi-infinite diffusion model is weak [76–80, 84,85].

According to the data measured at $\text{Bi}(001)$, the electrolyte resistance R_{el} (fitting error $\approx 1\%$) is independent of electrode potential (Fig. 6a), but there is a weak dependence of R_{el} on the concentration of the surface active component (KI) because the molar conductivity of KI is somewhat higher than that for KF.

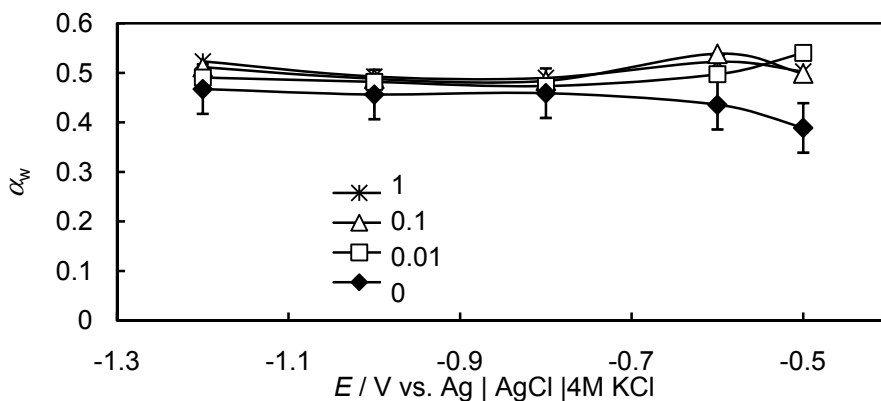


Fig. 5. Dependence of fractional exponent α_w on the electrode potential for Bi(001) in 0.1x M KI + 0.1(1-x) M KF aqueous solutions at various mole fractions of KI, x (M), noted in figure. Statistical error bars obtained using five independent experiments are given in figure.

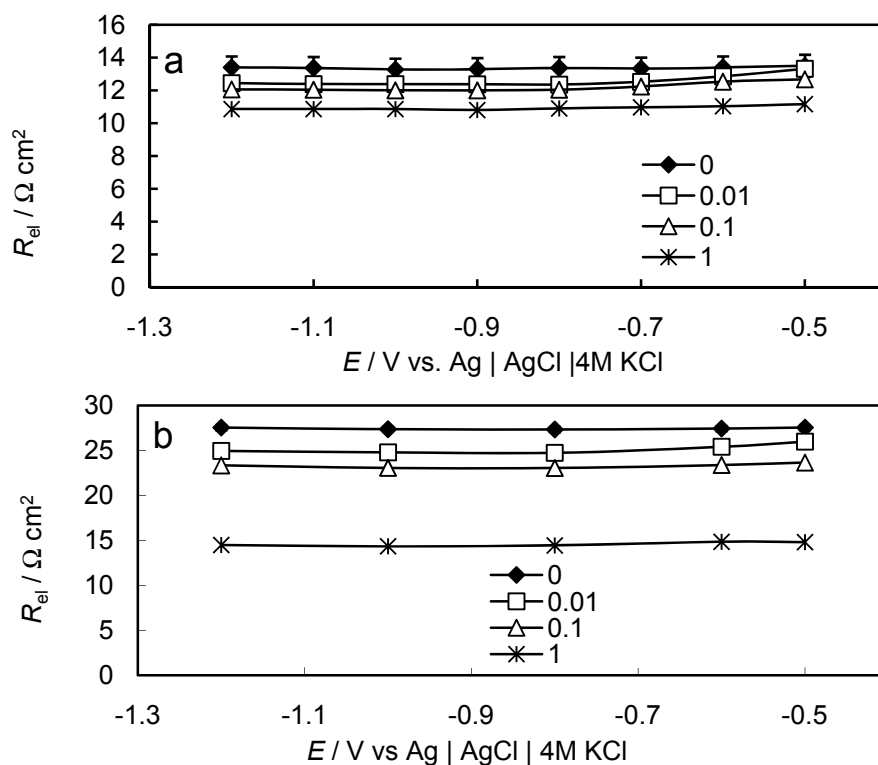


Fig. 6. Dependence of the electrolyte resistance R_{el} on the electrode potential for Bi(001) in 0.1x M KI + 0.1(1-x) M KF (a) and for Bi(111) in 0.1x M KI + 0.033(1-x) M K₂SO₄ (b) aqueous solutions at various mole fractions of KI, x (M), noted in figure. Statistical error bars obtained using five independent experiments are given in figure.

It is caused by fact that the Γ^- ions are less solvated than F^- ions and the resistance of the electrolyte solution decreases with increasing c_{KI} in the mixed electrolyte solution. In Fig. 6b it can be seen that for Bi(111)| K_2SO_4 electrolyte interface as for surface inactive electrolyte there is no dependence of R_{el} on electrode potential.

The ‘true’ double layer capacitance (Fig. 7), C_{dl} , considerably depends on the concentration of KI in the potential range from -1.0 to -0.5 V (vs. Ag | AgCl) and C_{dl} increases with c_{KI} . It can be explained with the specific adsorption of Γ^- at the Bi(001) and Bi(111) electrode surfaces at less negative electrode potentials [23, 31–33]. The dependence of C_{dl} on the mole fraction of KI indicates that the inner layer structure depends on the values of Gibbs adsorption Γ of the Γ^- ions.

The values of C_{ad} , adsorption capacitance, indicate that the adsorption process of Γ^- ions takes place at Bi(hkl) electrodes. The values of C_{ad} show some expansion in both ends of the region of ideal polarizability (Fig. 8). At $E > -0.7$ V, the weak increase in the values of C_{ad} with increasing c_{KI} has been observed, which can be explained by the intensive specific adsorption of iodide ions at the Bi(hkl) electrode surface. However, there is no noticeable dependence of C_{ad} on c_{KI} at $E < -1.2$ V where the adsorption of Γ^- ions is negligible.

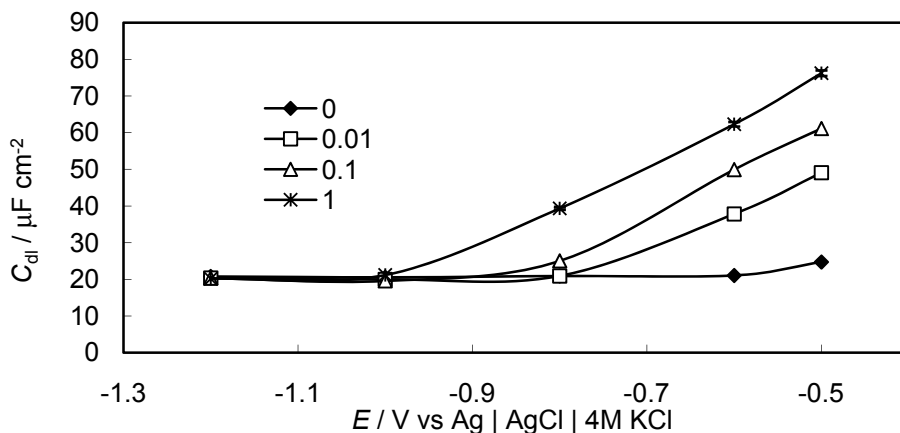


Fig. 7. Dependence of ‘true’ double layer capacitance C_{dl} on the electrode potential for Bi(111) in $0.1x$ M KI + $0.033(1-x)$ M K_2SO_4 aqueous solutions at various mole fractions of KI, x (M), noted in figure. Statistical error bars obtained using five independent experiments are given in figure.

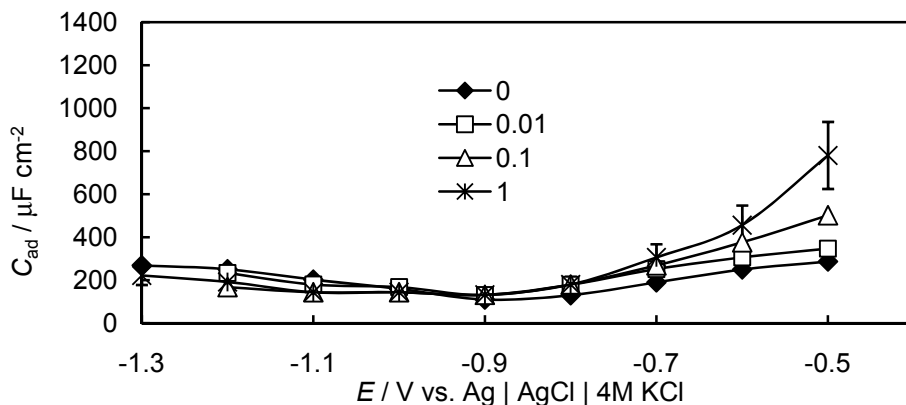


Fig. 8. Dependence of adsorption capacitance C_{ad} on the electrode potential for Bi(001) in $0.1x$ M KI + $0.1(1-x)$ M KF aqueous solutions at various mole fractions of KI, x (M), noted in figure. Statistical error bars obtained using five independent experiments are given in figure.

The diffusion resistance R_D has maximum values in the region of potentials (Fig. 9), where the specific adsorption of Γ ions at Bi(hkl) starts, i.e. in the region of intensive increase of the differential capacitance in the C,E curves. The same effect has been established for Bi(hkl) | non-aqueous surface active electrolyte systems (LiI) [31–33]. The decrease in R_D at $E > -0.9$ V can be explained by the specific adsorption of the Γ ions [5,6, 31–33]. Taking into account the relative error obtained from various experiments as well as fitting errors, there is no clear dependence of R_D on the concentration of KI. The so-called mass transfer frequency factor (T) also depends on the electrode potential and somewhat increases with c_{KI} at $E > -0.7$ V (Fig. 10).

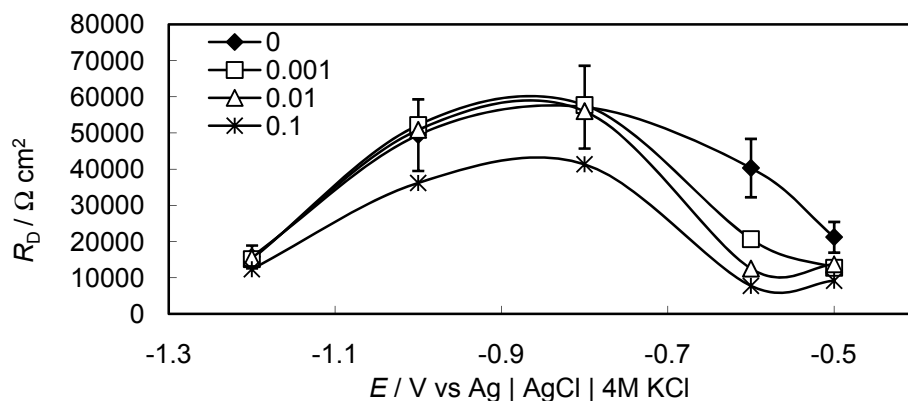


Fig. 9. Dependence of diffusion resistance R_D on the electrode potential for Bi(111) in $0.1x$ M KI + $0.033(1-x)$ M K_2SO_4 aqueous solutions at various mole fractions of KI, x (M), noted in figure. Statistical error bars obtained using five independent experiments are given in figure.

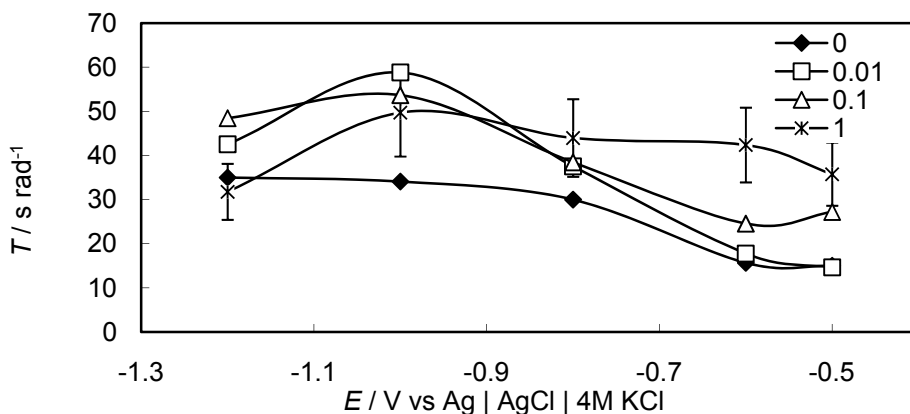


Fig. 10. Dependence of mass transfer frequency factor (T) on the electrode potential for Bi(001) in $0.1x$ M KI + $0.1(1-x)$ M KF aqueous solutions at various mole fractions of KI, x (M), noted in figure. Statistical error bars obtained using five independent experiments are given in figure.

For conclusion the electrical double layer capacitance, adsorption capacitance, diffusion resistance and other adsorption characteristics depend on the electrode potential applied. However, there is no noticeable dependency of these parameters on the mole fraction of the surface active Γ anion in the electrolyte solution at moderate negative potentials (i.e. in the region where there is no specific adsorption of anions). At $E > -1.0$ V for Bi(111) and Bi(001), there is a noticeable dependence of C_{ad} and C_{dl} on the mole fraction of KI, thus, if the intensive specific adsorption of the Γ ions starts. Analysis of complex impedance plane and phase angle vs. ac frequency curves shows that adsorption of Γ anions is limited by mixed kinetics (slow adsorption and diffusion-like steps), but the rate of adsorption step is limiting at moderate frequencies.

6.2 Properties of electrical double layer at Bi(111) | ionic liquid interface [III–V]

Cyclic voltammetry and electrochemical impedance spectroscopy have been applied for investigation of the electrochemically polished Bi(111) electrode in 1-ethyl-3-methyl imidazolium tris(pentafluoroethyl)trifluorophosphate (EMImFAP), 1-ethyl-3-methyl imidazolium tetracyanoborate (EMImTCB) and 1-ethyl-3-methyl imidazolium tetrafluoroborate (EMImBF₄) ionic liquids. These RTILs were chosen to investigate the influence of the chemical composition, structure and possible dependence of the closest approach of ions, i.e. specific adsorption of the ionic liquid anions on the electrical double layer

capacitance (well-known for halide, CN^- and SCN^- ions from the aqueous and non-aqueous electrolytes).

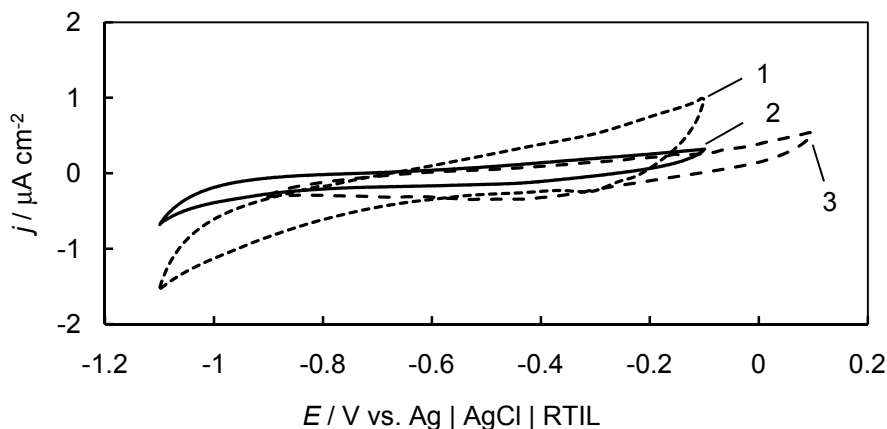


Fig. 11. Cyclic voltammograms for Bi(111) in EMImTCB (1); EMImBF₄ (2) and EMImFAP (3) at potential scan rate 10 mVs⁻¹.

Analysis of current density (j) vs. electrode potential (E) dependences (Fig. 11) show that the Bi(111) electrode is ideally polarizable (current density lower than 10^{-6} A cm⁻²) from -0.9 to 0.1 V in EMImFAP and from -1.1 to 0.0 V in EMImBF₄ and EMImTCB. The increase in j outside these potential regions is caused by the faradic reduction and oxidation of residual water and oxygen as well as BF₄⁻ anions. At small negative or positive electrode potentials an anodic oxidation of metal takes place.

The width of the ideal polarizability region is in a good correlation with the data in impedance plane plots (Nyquist plots) — for Bi(111)|EMImBF₄ interface there are only weak deviations from the adsorption limited process mechanism within the region of $-0.9 < E < -0.2$ V (Fig.12a). For Bi(111)|EMImTCB and Bi(111)|EMImFAP, both adsorption and diffusion determine the rate of the total adsorption process similarly to the Bi(111)|LiClO₄ aqueous solution interface [86,87].

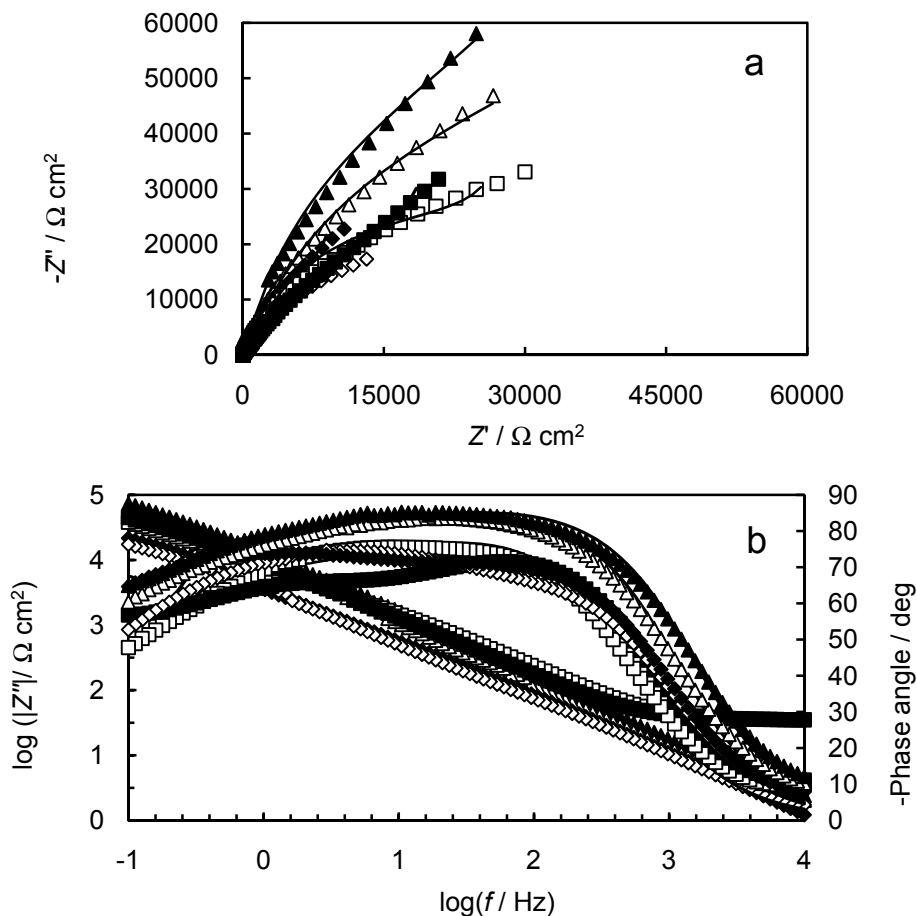


Fig. 12. Nyquist plots (a), impedance complex plane and phase angle plots (b) for Bi(111) in EMImBF₄ (triangles), EMImFAP (squares) and EMImTCB (rhombuses) at -0.7 (filled marks) and -0.1 V (open marks) (vs. Ag|AgCl|IL) (dots – exp. data, lines – fitting by Frumkin – Melik-Gaikazyan electrical circuit (EC) (c) in Fig.1).

Also the phase angle, δ ($|\delta| > 83^\circ$ at $f < 10^2 \text{ Hz}$) (Fig. 12b) and impedance modulus ($|Z|$) vs. frequency dependences for Bi(111)|EMImBF₄ confirm these conclusions. Only at very low ac frequency the small decrease in the negative values of phase angle has been established, which could be explained by occurring of the very slow first layer reorganization process of edl or partial charge transfer from ions to the electrode surface [88–90].

The experimental total series differential capacitance C_s (Fig. 13) has been calculated from the Nyquist dependences presented in Fig. 12a. The potential of the slight minimum in the constructed C_s vs. E plots, E_{\min} , being located at -0.7 V , has found to be independent of ac frequency. The values of C_s for EMImFAP at E_{\min} are noticeably lower than those for EMImBF₄, and especially for EMImTCB, and C_s for EMImFAP at $E > E_{\min}$ is even lower than at $E < E_{\min}$.

The lower capacitance values for EMImFAP can be explained by the larger molar volume (bigger diameter) for FAP^- compared with BF_4^- or TCB^- .

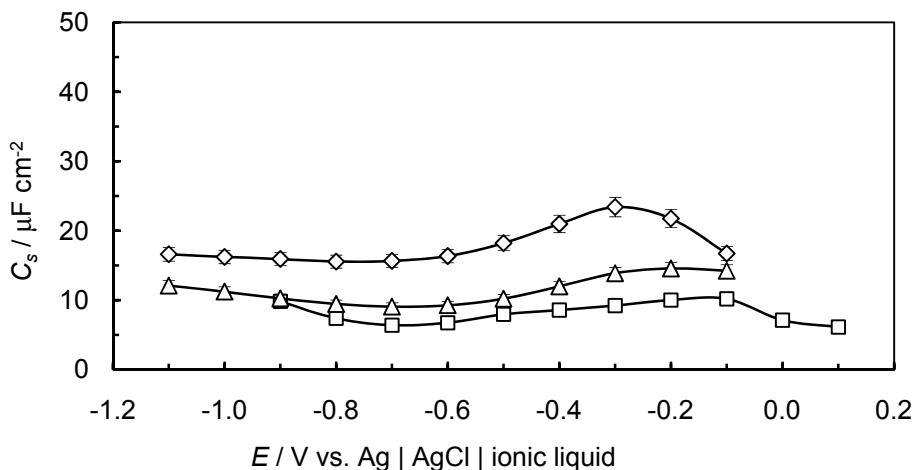


Fig. 13. Dependences of series capacitance vs. electrode potential curves for Bi(111)|EMImBF₄ (triangles), EMImFAP (squares) and EMImTCB (rhombuses) interface.

For Bi(111)|EMImBF₄ and EMImTCB (i.e. for RTILs with noticeable asymmetry of ions) the bell-shaped C_s, E curve has been found, but for EMImFAP (higher symmetry of molar volumes of ions) there is only a wide and low maximum at $E > E_{\min}$. However, it seems that, in addition to the asymmetry of ions, the difference in surface activity, i.e. in the closest approach of anions to the electrode surface is also important, obtaining mainly the asymmetric shape of the inner layer capacitance vs. potential curve for BF_4^- and TCB^- containing RTILs. The surface activity for EMImTCB seems to be noticeably higher than that for EMImFAP, explaining higher capacitance value for EMImTCB within the all potential region applied. Thus, the influence of second layer ions on C_s values, discussed by Kornyshev et al. [91–93] has been established. The same shape of “hump” in the C, E curve has been found to be characteristic of Hg in LiBF_4 or LiClO_4 and Bi(hkl) in LiBF_4 , LiClO_4 and LiSCN aqueous and non-aqueous solutions [86,87].

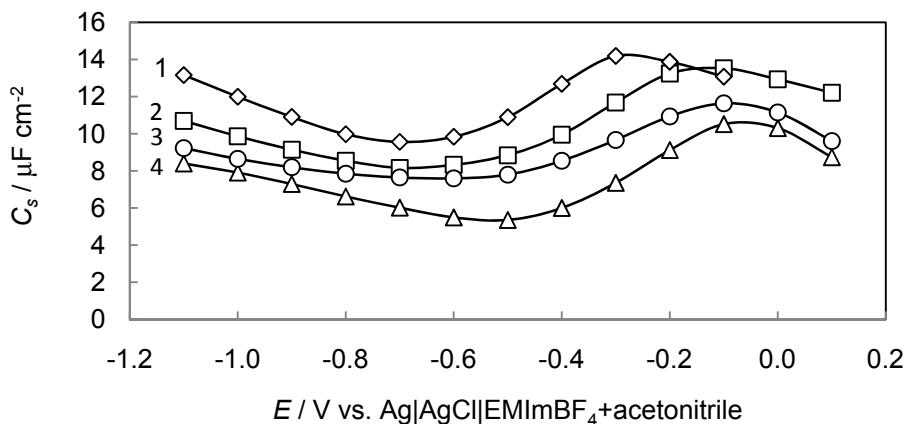


Fig. 14. Series capacitance vs. electrode potential curves for Bi(111)| x M EMImBF₄ + acetonitrile solution interface at 210 Hz and for x (M): 1 – pure; 2 – 0.5; 3 – 0.05; 4 – 0.005 EMImBF₄).

To analyze the influence of EMImBF₄ concentration on the capacitance and E_{\min} values, the EMImBF₄ solutions in acetonitrile ($H_2O < 0.003\%$, Riedel-de Haën) were studied using impedance method. For Bi(111)|acetonitrile (AN) + x M EMImBF₄ interface the decrease in series capacitance with dilution of the electrolyte has been observed and the well developed capacitance minimum has been established at $E = -0.5$ V vs. Ag|AgCl|EMImBF₄ in acetonitrile (Fig. 14). However, differently from LiClO₄ + AN solutions [86,87] the location of the minimum in the capacitance vs. potential curve for EMImBF₄ + AN solution depends strongly on the concentration of EMImBF₄ in acetonitrile. Thus, on the basis of Grahame electrical double layer model, the remarkable shift of E_{\min} toward less negative potentials with the decrease of EMImBF₄ concentration indicates that the surface activity of BF₄⁻ anions is higher than that for EMIm⁺ cations [86,87,89].

6.2.1 Simulation of impedance data

For calculation of the high-frequency double layer capacitance, C_{dl} , and equilibrium adsorption capacitance, C_{ad} , the equivalent circuit (EC) modeling method has been applied [85,88,89,94]. The non-linear least squares fitting shows that the more adequate fit of calculated with experimental spectra for Bi(111)|ionic liquid interface can be obtained by the modified Frumkin – Melik-Gaikazyan EC (Fig. 1(c)) where the classical semi-infinite diffusion impedance has been replaced by the open circuit finite length Warburg impedance $Z_{W(oc)}$ [86,87,95–97]. Thus, the values of series capacitance (C_s) within the region of ideal polarizability can be divided into C_{dl} and C_{ad} (Fig. 15). Based on the fitting data, C_{dl} weakly depends of RTIL studied, corresponding to the edl structure, if there

is no specific adsorption of anions with partial charge transfer [90] between the negatively charged electrode surface and RTIL anion. However, in the all potential region applied, C_{ad} is somewhat higher than C_{dl} , being higher for Bi(111)|EMImTCB compared with Bi(111)|EMImFAP interface, indicating the dependence of closest approach of anions onto the Bi(111) surface on the chemical structure of anions studied [13].

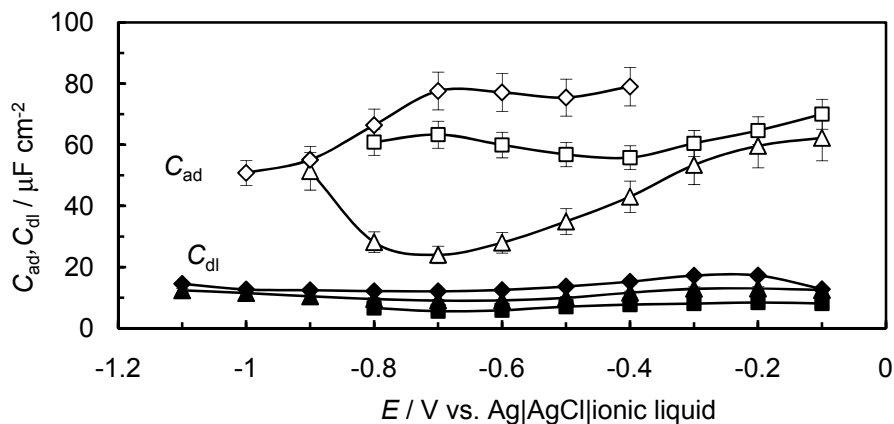


Fig. 15. Dependences adsorption capacitance C_{ad} and double layer capacitance C_{dl} vs. electrode potential curves for Bi(111) EMImBF₄ (triangles), EMImFAP (squares) and EMImTCB (rhombuses).

The diffusion-like process resistance R_D (Fig. 16) depends on RTIL studied, being higher for EMImBF₄. The values of fractional exponent of the Warburg-like diffusion impedance, α_w , are nearly 0.5 for EMImBF₄, thus the semi-infinite diffusion-like edl reorganization process takes place similarly to the Bi(111)|KF + KI aqueous solution interface (Fig. 16) [88]. Only for EMImTCB|Bi(111) interface the values of $\alpha_w > 0.5$ indicates the formation of ordered layer of adsorbate at the electrode surface.

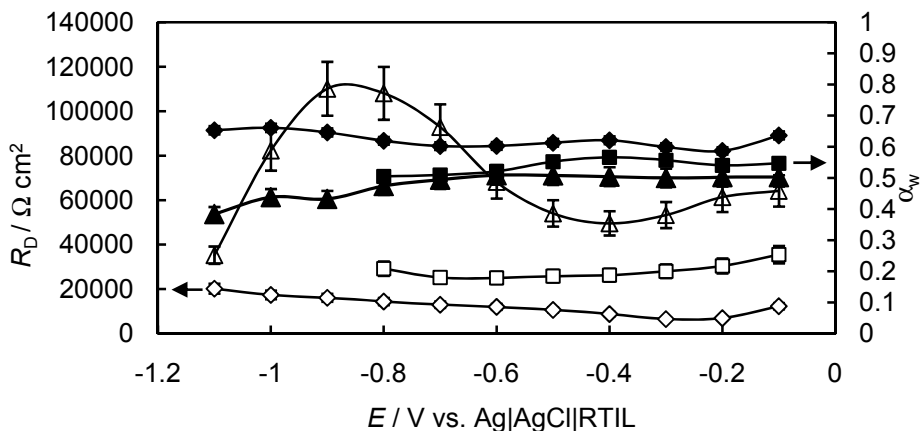


Fig. 16. Dependences of adsorption resistance R_D and fractional exponent in the generalized finite length Warburg impedance (α_w) on electrode potential for Bi(111) in EMIImBF₄ (triangles), EMIImFAP (squares) and EMIImTCB (rhombuses).

For conclusion, cyclic voltammetry and impedance data show the strong dependence of electrical double layer capacitance, i.e. structure of Bi(111)|RTIL interface on the chemical composition, ion size asymmetry and surface activity.

6.3 Comparison of limiting stages of adsorption and some characteristic parameters of ionic liquids and aqueous solutions of KI at Bi(111) and Bi(001)

6.3.1 Analysis of limiting stages of adsorption

At cathodic potentials $E < -1.2\text{V}$ (vs. Ag|AgCl|4M KCl) for systems Bi(001)|0.1x M KI+0.1(1-x) M KF; Bi(111)|0.1x M KI+0.033(1-x) M K₂SO₄ and at $E < -0.7\text{V}$ (vs. Ag|AgCl|ionic liquid) (it should be noted that the potential difference between Ag|AgCl in 4M KCl+H₂O electrolyte and Ag|AgCl|RTIL reference electrodes is near -0.29V) for system Bi(111)|ionic liquid dependencies of the phase angle δ on $\log f$ plots are similar and a needful information of limiting stages of adsorption process can be expected. The shape of δ , $\log f$ curves is practically independent of KI concentration at both Bi electrodes measured. In the low-frequency range from 0.1 Hz to 1 Hz δ changes from -60° in aqueous solution of KI to $-60-70^\circ$ in ionic liquids, indicating that the kinetically mixed process (the total rate of process is limited by diffusion-like, adsorption and partial charge transfer steps) prevail at the Bi(*hkl*)|electrolyte interface. In the moderate ac frequency region from 10Hz to 100Hz δ , $\log f$ -curves demonstrate maximum values from -70° to -84° in ionic liquids and $\delta \cong$

-80° in aqueous solutions of KI indicating that the adsorption of solution components (i.e. ions) is mainly limited by the rate of adsorption step [5,6, 80–83].

At less negative potential, i.e. near to the end of ideal polarizability $E \geq -0.5V$ (vs. Ag|AgCl|4M KCl) for systems Bi(001)|0.1x M KI+0.1(1-x) M KF; Bi(111)|0.1x M KI+0.033(1-x) M K₂SO₄, there is a noticeable dependence of capacitance on the concentration of KI at low frequency range. At $E \geq -0.1V$ (vs. Ag|AgCl|ionic liquid) for Bi(111)|ionic liquid systems there can be seen also dependence of capacitance on the concentration of RTIL ions in acetonitrile solutions. Phase angle values increase with c_{KI} from -50° to -65° on both Bi single crystal planes studied, indicating the rise of the role of the adsorption step in the adsorption kinetics, but the limiting stage has still a mixed kinetic nature (diffusion, adsorption and partial charge transfer). At low ac frequency range the phase angle values depend on the ionic liquid chemical composition and the values of phase angle change from -48° (EMImFAP) to -60° (EMImBF₄). Thus, the adsorption is likewise limited by mixed kinetics. The slow adsorption stage is observed only in the medium ac frequencies – in frequency range from 1Hz to 100Hz.

6.3.2 Similarity and analysis of Nyquist plots

Analysis of experimentally measured Nyquist plots show that the impedance data for Bi(*hkl*) electrode in both electrolytes, i.e. in the electrolyte aqueous solutions and ionic liquids can be fitted with the modified Frumkin – Melik-Gaikazyan (FMG) equivalent circuit (Fig. 1 (c)), which takes into account the adsorption and diffusion-like mass transfer limited processes at Bi(*hkl*)|electrolyte interfaces.

The electrolyte resistance R_{el} calculated is independent of the electrode potential in the cases of ionic liquids and iodide adsorption at Bi(111) from aqueous solution. There is only a weak dependence of R_{el} on the concentration of the surface active component (KI) at Bi(*hkl*) in the mixed electrolyte solution with constant ionic strength, because the limiting molar conductivity of KI is somewhat higher than that for KF.

The limiting diffusion resistance, R_D , has maximum values in the potential region where the specific adsorption of iodide ions starts in the case of adsorption of iodide ions at Bi(111) and Bi(001) single crystal electrodes or where adsorption of BF₄⁻ or TCB⁻ anions from ionic liquid takes place. It can be explained by the reversible partial charge transfer from ions to the electrode surface [5,6, 31–33]. R_D values are independent of the concentration of KI, but there is a dependence of R_D on the crystallographic structure of Bi planes studied. R_D values are lower for more active Bi(001) plane. R_D for Bi(111)|ionic liquid interface depends on the ionic liquid studied and has higher values for EMImBF₄ than these for EMImFAP or EMImTCB ionic liquids.

The double layer capacitance C_{dl} depends noticeably on the system studied. In the case of iodide adsorption at Bi(*hkl*) there is a considerable dependence of

the electrical double layer capacitance on the electrode potential where the specific adsorption of Γ starts. C_{dl} increases with the concentration of KI in the electrolyte solution with constant ionic strength [23, 31–33]. In ionic liquid systems C_{dl} is practically independent of the electrode potential, because there is no remarkable specific adsorption at Bi(111) single crystal electrode in the high frequency ac region investigated.

Adsorption capacitance C_{ad} values measured in ionic liquids at Bi(111) plane are noticeably lower than these in aqueous solutions, containing KI and KF. The values of C_{ad} show some expansion at less negative electrode potentials for 0.1x M KI+0.1(1-x) M KF and 0.1x M KI+0.033(1-x) M K_2SO_4 systems, which can be explained by the intensive adsorption of iodide ions at Bi(*hkl*) surface. At Bi(001) and at $E > -0.7$ V, the dependence on c_{KI} can be seen, contrary to Bi(111), which is a less active electrode surface.

7. SUMMARY

Cyclic voltammetry and impedance spectroscopy methods have been applied for investigation of the adsorption kinetics of Γ^- ions at Bi(001) and Bi(111) single crystal plane electrodes in aqueous solutions with constant ionic strength. Electrical double layer structure at Bi(111) in 1-ethyl-3-methyl imidazolium tris(pentafluoroethyl)trifluorophosphate (EMImFAP), 1-ethyl-3-methyl imidazolium tetracyanoborate (EMImTCB) and 1-ethyl-3-methyl imidazolium tetrafluoroborate (EMImBF₄) ionic liquids has been studied as well. Experimental data show that the reproducible data in aqueous solution and in ionic liquids can be obtained in the range of ac frequencies from 0.1 to 10000 Hz. It was demonstrated that the Bi(001) electrode is ideally polarizable within the potential region from -1.4 V to -0.5 V (vs. Ag|AgCl|4M KCl) in the aqueous solution with constant ionic strength $0.1x$ M KI + $0.1(1-x)$ M KF. The Bi(111) single crystal electrode is ideally polarizable in the region from -0.9 to 0.1 V in EMImFAP, from -1.1 to 0.0 V in EMImBF₄ and EMImTCB and from -1.4 to -0.55 V (vs. Ag|AgCl|4M KCl) in the aqueous solution of $0.1x$ M KI + $0.033(1-x)$ M K₂SO₄.

Calculated Nyquist plots by using the various equivalent circuits were fitted to the experimental ones, but the best results were obtained with the modified Frumkin- Melik- Gaikazyan model, where general finite-length diffusion impedance has been introduced into the equivalent circuit. The electrical double layer capacitance, adsorption capacitance, diffusion resistance and other adsorption characteristics depend on the electrode potential applied, as well as on the composition of electrolyte studied.

Analysis of phase angle vs. ac frequency curves shows that adsorption of ions from aqueous medium is limited by mixed kinetics (slow adsorption, diffusion and partial charge transfer steps) at very low ac frequency, as well as from ionic liquids measured. However, mainly the rate of adsorption step is limiting at moderate frequencies from 10 to 200 Hz and electrode potentials, where the specific adsorption of anions starts.

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9. SUMMARY IN ESTONIAN

Ioone adsorptsioonikineetika Bi monokristalli tahkudel vesilahustes ja ioonsetes vedelikes

Antud töös uuriti elektrokeemilise impedantspektroskoopia meetodiga jodiidiooni adsorptsioonikineetikat järgmistes süsteemides: Bi(001) | 0.1 xM KI + 0.1 (1-x) M KF, kus x on KI moolmurd, mille puhul elektrood on ideaalselt polariseeritav potentsiaalvahemikus -1.4V kuni -0.5 V (vs. Ag|AgCl|4M KCl), Bi(111) | 0.1x M KI+0.033(1-x) M K₂SO₄, kus x on KI moolmurd ning ideaalse polariseeritavuse ala on -1.3V kuni -0.5V (vs. Ag|AgCl|4M KCl). Ioonse vedeliku ja Bi(111) püripinnale tekkiva elektrilise kaksikkihi parameetreid uuriti lisaks elektrokeemilisele impedantspektroskoopiale ka tsüklilise voltamperomeetria meetodiga järgmistes ioonsetes vedelikes: 1-etüül-3-metüül-imidasoolium tetrafluoroboraat (EMImBF₄), 1-etüül-3-metüül-imidasoolium tris(pentafluoroetüül)trifluorofosfaat (EMImFAP), 1-etüül-3-metüül-imidasoolium tetraatsüaanoboraat (EMImTCB). Bi(111) on EMImBF₄ and EMImTCB korral ideaalselt polariseeritav -1.1 kuni 0.0 V (vs. Ag|AgCl|RTIL) ning EMImFAP puhul -0.9 kuni 0.1 V (vs. Ag|AgCl|RTIL). Enne iga eksperimendi poleeriti vismutelektrood elektrokeemiliselt KI+HCl lahuses. Mõõtmised ioonsetes vedelikes viidi läbi kuivkapis (Labmaster sp, LMBraun; O₂ and H₂O concentrations <0.1 ppm) argooni (99.99995%) keskkonnas.

Ekspérimentaalselt mõõdetud reaktiivtakistuse Z'' ja aktiivtakistuse Z' sõltuvuste mittelineaarne regressioonanalüüs näitas, et kõigi mõõdetud süsteemide puhul andis paremaid modelleerimistulemusi klassikalise Frumkin- Melik-Gaikazyani mudel, kuigi andmeid modelleeriti ka teiste ekvivalentskeemidega. Modelleerimistulemuste kokkulangevust eksperimendialsete andmetega analüüsi mittelineaarse regressioonanalüüsi abil määratud χ^2 - funktsiooni ja kaalutud ruutkeskmise hälbe põhjal ning üksikute parameetrite väärtuste ja nende standardhälvete põhjal. Faasinurga vahelduvvoolu sagedusest sõltuvused näitasid, et jodiidiooni adsorptsiooni kiirust määravad staadiumid (vahetu adsorptsioon, osakeste difusioon pinnale ning osaline laenguülekanne) on võrreldavate kiirustega ning suuremal osal uuritud vahelduvvoolu sageduste alas allub Γ adsorptsiooniprotsess segakineetika seaduspärasustele. Tehti kindlaks, et KF ega K₂SO₄ vesilahuste korral ei sõltu vahelduvvoolu faasinurk elektroodipotentsiaalst, küll aga on näha faasinurga sõltuvust potentsiaalst KI lahuses nii vahelduvvoolu kõrgsageduslikus kui ka madalsageduslikus alas, mis näitab, et jodiidioonid adsorbeeruvad Bi(001) ning Bi(111) elektroodil spetsiifiliselt ning adsorptsiooniprotsess on uuritud potentsiaalide vahemikus kiire ning pöörduv. Bi(111) ioonne vedelik süsteemides oli näha sarnast käitumist, ehk siis suuremal osal uuritud sageduste alas protsess on limiteeritud segakineetika poolt (vahetu adsorptsioon, osakeste difusioon pinnale ning osaline laenguülekanne), kuigi faasinurga vahelduvvoolu sagedusest sõltuvuste kuju on mõnevõrra erinev ioonsete vedelike puhul, mida antud töös uuriti.

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List of publications

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