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1 **An Improved Modeling for Low-grade Organic Rankine Cycle**
2 **Coupled with Optimization Design of Radial-inflow Turbine**

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23 **Abstract**

24 Organic Rankine cycle (ORC) has been proven to be an effective and promising
25 technology to convert low-grade heat energy into power, attracting rapidly growing
26 interest in recent years. As the key component of the ORC system, turbine
27 significantly influences the overall cycle performance and its efficiency also varies
28 with different working fluids as well as in different operating conditions. However,
29 turbine efficiency is generally assumed to be constant in the conventional cycle design.
30 Aiming at this issue, this paper couples the ORC system design with the radial-inflow
31 turbine design to investigate the thermodynamic performance of the ORC system and
32 the aerodynamic characteristics of radial-inflow turbine simultaneously. The
33 constrained genetic algorithm (GA) is used to optimize the radial-inflow turbine with
34 attention to six design parameters, including degree of reaction, velocity ratio, loading
35 coefficient, flow coefficient, ratio of wheel diameter, and rotational speed. The
36 influence of heat source outlet temperature on the performance of the radial-inflow
37 turbine and the ORC system with constant mass flow rate of the heat source and
38 constant heat source inlet temperature is investigated for four kinds of working fluids.
39 The net electrical powers achieved are from few tens kW to one hundred kW. The
40 results show that the turbine efficiency decreases with increasing heat source outlet
41 temperature and that the decreasing rate of turbine efficiency becomes faster in the
42 high temperature region. The optimized turbine efficiency varies from 88.06% (using
43 pentane at the outlet temperature of 105 °C) to 91.01% (using R245fa at the outlet
44 temperature of 80 °C), which appears much higher compared to common values
45 reported in the literature. Furthermore, the cycle efficiency increases monotonously
46 with the growth of the heat source outlet temperature, whereas the net power output
47 has the opposite trend. R123 achieves the maximum cycle efficiency of 12.21% at the

48 heat source outlet temperature of 110 °C. Based on the optimized results, the
49 recommended ranges of the key design parameters for ORC radial-inflow turbine are
50 presented as well.

51 **Keywords**

52 Organic Rankine cycle; Radial-inflow turbine; Coupled modeling; Genetic algorithm

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70 **1. Introduction**

71 Nowadays, with rapidly increasing globalization and energy demands,
72 researchers are devoted to solving problems of energy shortage and environmental
73 pollution. Apart from the development of new energy sources, the recovery and
74 utilization of renewable energy, such as solar energy [1-3], biomass energy [4, 5],
75 geothermal energy [6-9] and waste heat [10-12], have attracted increasing attention.
76 Because of the advantages of low capital cost, small size and easy maintenance [13],
77 Organic Rankine cycle (ORC), which has the same configuration as conventional
78 steam Rankine cycle but uses organic fluid instead of water as working fluid, has been
79 proved to be an effective and promising technology for the low-grade heat recovery.

80 Over the past two decades, a large part of relevant research studies focuses on the
81 working fluid selection. Dry and isentropic fluids with positive slopes or infinitely
82 large slopes of vapor saturation curves in the temperature-entropy diagram are
83 preferable due to their convenience in the non-superheating ORC [14]. Additionally, a
84 suitable working fluid should also satisfy cycle and turbine performances, safety and
85 environmental criteria [15]. Wang et al. [16] evaluated R11, R141b, R123, R245fa and
86 R245ca as working fluids for engine waste heat recovery. R245fa and R245ca were
87 recommended as the most suitable working fluids for an engine waste heat-recovery
88 application. Rayegan and Tao [17] developed a procedure to compare 117 organic
89 fluids in solar ORC. R245fa and R245ca were selected for the medium temperature
90 level. Drescher and Bruggemann [18] investigated suitable working fluids for ORC in
91 biomass power plants. It was found that the family of alkylbenzenes showed the
92 highest cycle efficiencies. Qiu [19] proposed a preferable ranking of 8 mostly-applied
93 working fluids by means of spinal point method in micro-CHP (combined heat and
94 power) systems. In general, the selection of working fluids is a complex process,

95 which is affected by the heat source type and level, operating conditions, cycle
96 configuration, the turbine types and performance. The results of working fluid
97 selection do not have universality because of widely varying cycle operation
98 conditions, diverse cycle configurations, different aims for working fluid selection in
99 terms of different application background and so forth [20].

100 It is also noted that determination and optimization of the ORC system
101 parameters are another hot topic in the field of ORC. Peris et al. [21] studied the
102 performance of a regenerative ORC with heat source inlet temperature of 127-156 °C
103 experimentally. The inlet pressure of volumetric expander was about 14-20 bar and
104 the maximum electrical efficiency of 12.32% was obtained at the heat source inlet
105 temperature of 155 °C. Braimakis and Karellas [22] presented an integrated
106 thermoeconomic optimization approach of standard and regenerative ORCs. It was
107 concluded that for small scale ORCs the most important costs were related to heat
108 exchangers and the pump while for large scale ORCs screw expanders and turbines
109 were preferred and they had very high costs. Mehrpooya and Ashouri [23] performed
110 a thermoeconomic analysis of a regenerative two-stage ORC with solar energy as heat
111 source to minimize the product cost and maximize the exergy efficiency. The cycle
112 efficiency of 19.59% was reached and product cost rate was 3.88 million dollars per
113 year. Yang and Yeh [24] analyzed the ORC system for geothermal application with
114 heat source inlet temperature of 100 °C and mass flow rate of 80 kg/s and found that
115 the higher the operating pressures were, the larger the proportion of purchased cost
116 would be. Marion et al. [25] conducted theoretical and experimental studies on a solar
117 subcritical ORC and concluded that the net mechanical power strongly depended on
118 the fluid mass flow rate and that the optimum mass flow rate was a linear function of
119 the solar radiation. Apart from the standard ORC system, advanced ORC systems like

120 recuperative ORC [26, 27], regenerative ORC [22, 28], supercritical ORC [29-31],
121 zeotropic ORC [32, 33] and trilateral cycle [34, 35] also have been studied
122 extensively.

123 The turbine design is a critical step in the design of ORC systems since turbine
124 geometry and aerodynamic performance directly affect the overall cycle performance
125 and vice versa. Among kinds of ORC expanders, the radial-inflow turbine shows good
126 aerodynamic performance due to its capability of dealing with large enthalpy drops
127 with relatively low peripheral speeds [36]. The conventional turbine design method
128 used for gas turbine is also applicable to the design of an ORC turbine. Due to the
129 lack of extensive experimental data, the loss models are often based on the
130 experimental studies of gas turbine. Fiaschi et al. [36] discussed a 0-D model for the
131 design of radial turbine for 50 kW ORC applications and investigated the estimation
132 of the turbine losses and the main design parameters. The total-to-total efficiency of
133 the designed turbine ranged from 0.72 to 0.80 and backswept bladed rotors showed
134 1.5-2.5% higher efficiencies. Song et al. [37] proposed a 1-D aerodynamic analysis
135 model of the radial-inflow turbine and a performance prediction model of the heat
136 exchanger. The expansion ratio of the six working fluids in the radial-inflow turbine
137 was about 5-25 when the evaporation temperature was 360-430 K. Sauret and Gu [38]
138 performed preliminary steady-state 3-D computational fluid dynamics (CFD)
139 simulations of radial turbine for a number of operating conditions. The maximum
140 turbine efficiency was 88.45% with rotational speed of 25463.5 rpm and turbine inlet
141 temperature of 413 K. Kang [39] examined a two-stage radial turbine with the
142 expansion ratio of the high-pressure turbine as 2.67 and the expansion ratio of the
143 low-pressure turbine as 4.07. The maximum electric power, average cycle and turbine
144 efficiencies were found to be 39.0 kW, 9.8% and 58.4% when the evaporation

145 temperature was 116 °C. When it comes to the optimization design of fluid machinery,
146 the genetic algorithm (GA), simulated annealing algorithm, particle swarm
147 optimization (PSO) and ant colony optimization (ACO) are frequently used. Since the
148 GA can deal with complex optimization problems and is less sensitive to the initial
149 conditions, it is distinguished from other optimization methods with respect to the
150 optimization design of turbines for ORC systems, and is the most widely used method
151 to select parameters about the turbine size [13], stage geometry [15, 40] and turbine
152 performance.

153 In the conventional design of the ORC system, the turbine efficiency is a fixed
154 value. But in practical application, the turbine efficiency is directly related with the
155 selected working fluids and the system operating conditions. At the same time, the
156 system parameter determination is also influenced by the turbine performance. It's
157 necessary to couple the modeling of ORC system with the preliminary design of
158 radial-inflow turbine. Song et al. [41] presented a 1-D analysis model of the
159 radial-inflow turbine in the ORC system design with seven key parameters
160 determining the turbine geometry and aerodynamic performance as fixed values. Pan
161 and Wang [42] replaced the constant isentropic efficiency with the internal efficiency
162 of optimal radial turbine for each condition and analyzed the effects of evaporating
163 temperature on cycle performance. This study focused on the optimization of degree
164 of reaction, hub-diameter ratio and peripheral velocity ratio while remaining other
165 parameters constant. Jubori et al. [43] presented an integrated approach combining
166 ORC system modeling, mean-line design and 3-D CFD analysis for micro-scale axial
167 and radial-inflow turbines with the maximum total-to-total efficiency as 83.48% and
168 83.85%, respectively. It appears from the previous investigations that the existing
169 research aforementioned mainly focused on the study of ORC system or radial turbine

170 only. To the best of the authors' knowledge, however, the exploration of the coupled
171 design of the ORC system and its radial-inflow turbine has been far from complete
172 and there is still much room to be enhanced in this area. Moreover, the recommended
173 values of the key design parameters for the ORC radial-inflow turbine are not
174 extensively studied.

175 In this paper, an ORC model is built for the utilization of geothermal resource
176 with heat source inlet temperature of 120 °C. A coupled design of the ORC system
177 and the radial-inflow turbine is performed with the constrained GA to maximize the
178 turbine efficiency. The ORC systems with different heat source outlet temperatures
179 and working fluids are investigated by an original MATLAB code. The analysis of the
180 optimized parameters: degree of reaction, velocity ratio, loading coefficient, flow
181 coefficient, ratio of wheel diameter and rotational speed, is conducted. In addition,
182 this paper also provides references on the recommended ranges of the key design
183 parameters for ORC radial-inflow turbine based on the optimized results.

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Nomenclature

Symbol

W	work/power, W
Q	heat, J
h	specific enthalpy, J/kg
Δh_{actual}	actual enthalpy drop, J/kg
Δh_s	isentropic enthalpy drop, J/kg
Δh	enthalpy difference, J/kg
T	temperature, K
P	pressure, Pa
ρ	density, kg/m ³
c	absolute velocity, m/s
w	relative velocity, m/s
u	peripheral velocity, m/s
m	mass flow rate, kg/m ³
r	radius, m
d	diameter, m
b	blade height, m
τ	blockage factor
h_c	tip clearance, m
E	energy, factor
H	form factor
C	loss coefficient multiplier, 1
l	surface length, m
s	blade spacing at blade-row exit, m
A	area, m ²
t	trailing-edge thickness, m
Z	blade number
Ma	Mach number
$d_{2,s}$	diameter at the rotor shroud, m
$d_{2,h}$	diameter at the rotor hub, m
$d_{2,sh}$	mean diameter at the rotor outlet, m

Subscripts

wf	working fluid
0	nozzle inlet
1	nozzle outlet or rotor inlet
2	rotor outlet
$cond$	condenser
$evap$	evaporator
s	isentropic process
n	nozzle
r	rotor
m	meridional direction
u	peripheral direction
2-D	two dimensional
3-D	three dimensional
rel	relative
abs	absolute

Greek letters

η_{1st}	the first law efficiency of ORC system
$\eta_{turbine}$	turbine efficiency
α	absolute flow angle, degree
β	relative flow angle, degree
Ω	degree of reaction
φ	nozzle velocity coefficient
ψ	rotor velocity coefficient
Φ	flow coefficient
Ψ	loading coefficient
μ	dynamic viscosity, Pa · s
ξ	loss coefficient
ζ	energy loss coefficient
θ	momentum thickness, m
γ	flow angle, degree
ω	rotational speed, rpm

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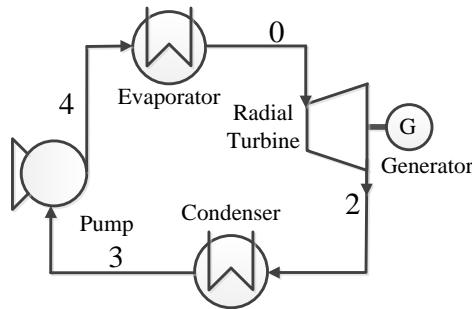
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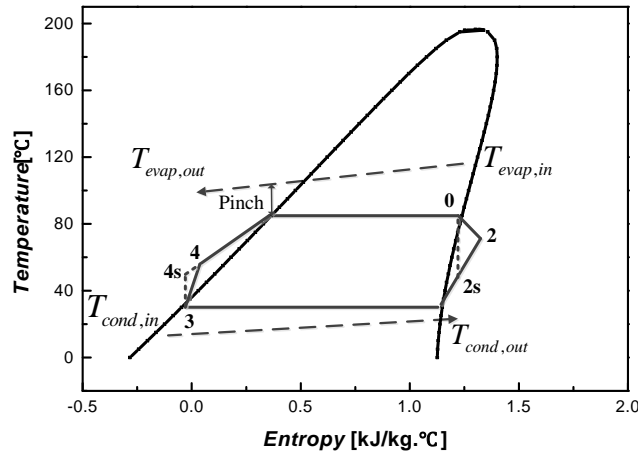
199 **2. ORC modeling and working fluid candidates**

200 2.1 ORC modeling

201 Fig. 1 shows the schematic diagram of a basic ORC system, which includes four
 202 main components: working fluid pump, evaporator, turbine and condenser. The
 203 temperature-entropy diagram of the basic ORC using pentane is shown in Fig. 2.



204 Fig.1. Schematic diagram of the basic ORC
 205



206 Fig.2. Temperature-entropy curve of the basic ORC (using pentane)
 207

208 The work consumed by the pump in the process 3 to 4 is expressed by:

209
$$W_{pump} = m_{wf}(h_4 - h_3) = m_{wf}(h_{4s} - h_3) / \eta_{pump} \quad (1)$$

210 The heat absorbed in the evaporator in the process 4 to 0 is expressed by:

211
$$Q_{evap} = m_{wf}(h_0 - h_4) = m_{evap}(h_{evap,in} - h_{evap,out}) \quad (2)$$

212 The work produced by the turbine in the process 0 to 2 is expressed by:

213
$$W_{turb} = m_{wf}(h_0 - h_2) = m_{wf}(h_0 - h_{2s}) \cdot \eta_{turbine} \quad (3)$$

214 The heat generated in the condenser in the process 2 to 3 is expressed by:

$$215 \quad Q_{cond} = m_{wf} (h_2 - h_3) = m_{cond} (h_{cond,out} - h_{cond,in}) \quad (4)$$

216 The net power output of the ORC system is expressed by:

$$217 \quad W_{net} = W_{turbine} - W_{pump} \quad (5)$$

218 The first law efficiency of the ORC system can be calculated by:

$$219 \quad \eta_{1st} = \frac{W_{net}}{Q_{evap}} = \frac{W_{turbine} - W_{pump}}{Q_{evap}} = \frac{(h_0 - h_2) - (h_4 - h_3)}{h_0 - h_4} \quad (6)$$

220 The conditions for the heat source, heat sink and ORC system are summarized in
 221 Table 1. The working conditions are applied to the utilization of geothermal resource
 222 with fixed heat source temperature and mass flow rate.

223 Table 1 Working conditions for the heat source, heat sink and cycle parameters

System	Parameters	Value
Heat source (water)	Inlet temperature (°C)	120
	Pressure (kPa)	500
	Mass flow rate (kg/s)	10
Heat sink (water)	Inlet temperature (°C)	25
	Outlet temperature (°C)	35
	Pressure (kPa)	250
ORC	Isentropic pump efficiency	0.8
	Pinch temperature in the evaporator (°C)	12
	Pinch temperature in the condenser (°C)	8

224 2.2 Working fluid candidates

225 Working fluid plays an important role in the design and performance analysis of
 226 an ORC system. It not only affects the turbine aerodynamic performance but also its
 227 geometry. Generally, the organic working fluids are divided into three categories: wet,
 228 dry and isentropic in terms of the slope of the saturated vapor line in the T-s diagram.
 229 Due to the low temperature of the heat source, this study selects four commonly used
 230 dry working fluids, pentane, R245fa, R365mfc and R123 [13, 36, 44]. This ensures

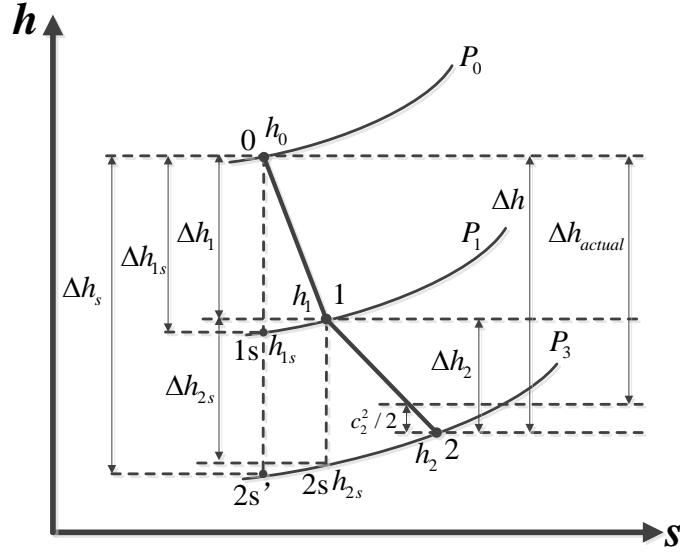
231 that there are no liquid working fluids existing in the rotor and thus there is no need to
 232 superheat the working fluids. Table 2 shows the properties of the selected working
 233 fluid candidates.

234 Table 2 Properties of the working fluid candidates

Fluid	Molecular weight (g/mol)	Critical pressure (kPa)	Critical temperature (°C)	Normal boiling point (°C)	GWP (100 yr)	ODP
Pentane	72.15	3370	196.55	36.06	20	0
R245fa	134.05	3651	154.01	15.14	950	0
R365mfc	148.07	3266	186.85	40.15	794-997	0
R123	152.93	3662	183.68	27.82	77	0.02

235 3. Turbine design

236 The preliminary design of the radial turbine is performed by the mean-line
 237 approach, which is on the basis of a one-dimensional assumption that there is a mean
 238 streamline through the stage [13]. Conservation of mass, momentum and energy
 239 together with velocity triangle equation, state equation and loss model are used to
 240 determine the parameters of basic geometry, velocity triangles, thermodynamic
 241 properties. In this paper, volute and expansion diffuser are ignored in order to simplify
 242 computational load. The simplified working procedure is shown in Fig. 3, where point
 243 0 represents the state of the working fluid at the nozzle inlet, point 1 represents the
 244 state at the nozzle outlet as well as the state at the rotor inlet, and point 2 represents
 245 the state at the rotor outlet. Δh_s is the isentropic enthalpy drop of the entire turbine
 246 and Δh_{actual} is the actually useful enthalpy drop which does not account for the
 247 energy of leaving velocity.



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Fig.3. $h-s$ diagram of the radial-flow turbine

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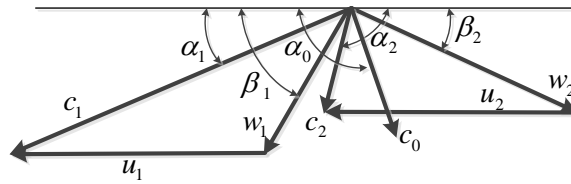
Absolute velocity, relative velocity and velocity angles at the nozzle outlet and

251

rotor outlet are determined according to velocity triangles of the radial-inflow turbine

252

as shown in Fig. 4.



253

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Fig.4. Velocity triangles of the radial-inflow turbine

255

As shown in Fig. 3, working fluid flows through the nozzle and rotor. From state

256

point 0 to state point 1, the flow equations of the working fluid can be expressed as

257

follows, where the subscripts 0, 1 and 2 represent the same state point in Fig. 3:

258

Mass continuity equation: $m_{wf} = \rho_1 c_{1m} b_{1n} d_{1n} \pi \tau_n$ (7)

259

Energy equation:
$$\begin{cases} \Delta h_{1s} = (1 - \Omega) \cdot \Delta h_s, h_{1s} = h_0 - \Delta h_{1s} \\ h_1 = h_{1s} + (c_{1s}^2 - c_1^2) / 2 = h_{1s} + c_{1s}^2 (1 - \varphi^2) / 2, c_1 = \varphi c_{1s} \end{cases}$$
 (8)

260

Equation of state: $P_1 = f(h_{1s}, s_0), T_1 = f(P_1, h_1), \rho_1 = f(P_1, h_1)$ (9)

261

Velocity triangle: $u_1 = (u_1 / c_s) \cdot c_s, c_{1m} = \Phi \cdot u_1, c_{1u} = \sqrt{c_1^2 - c_{1m}^2}$ (10)

262 where τ_n is the nozzle blockage factor. c_s ($=\sqrt{2\Delta h_s}$) is the ideal velocity of the
 263 working fluid at the turbine outlet. c_{1m} and c_{1u} are the absolute velocity in the
 264 meridional and peripheral directions at the nozzle outlet, respectively. ϕ is the nozzle
 265 velocity coefficient. u_1/c_s is the velocity ratio. Φ is the flow coefficient
 266 ($\Phi = c_{1m}/u_1$). Ω is the degree of reaction. b_{1n} is the nozzle blade height and d_{1n} is
 267 the nozzle outlet diameter.

268 From state point 1 to state point 2, the flow equations of the working fluid can be
 269 expressed as follows:

270 Mass continuity equation: $m_{wf} = \rho_1 c_{1m} b_1 d_1 \pi \tau_1 = \rho_2 c_{2m} b_2 \pi \cdot (d_{2,s} + d_{2,h}) / 2 \cdot \tau_2$ (11)

271 Energy equation:
$$\begin{cases} h_2 = h_{2s} + (w_{2s}^2 - w_2^2) / 2 + L_{df} + L_c \\ = h_{2s} + w_{2s}^2 (1 - \psi^2) / 2 + L_{df} + L_c, w_2 = \psi w_{2s} \end{cases}$$
 (12)

272 Equation of state: $T_2 = f(P_2, h_2), \rho_2 = f(T_2, h_2)$ (13)

273 Velocity triangle: $u_2 = \mu u_1, c_{2u} = (c_1 \cdot \cos \alpha_1 \cdot u_1 - u_1^2 \cdot \Psi) / u_2, c_{2m} = \sqrt{c_2^2 - c_{2u}^2}$ (14)

274 where τ_1 and τ_2 are the rotor inlet and outlet blockage factors, respectively. c_{2m}
 275 and c_{2u} are the absolute velocity in the meridional and peripheral directions at the
 276 rotor outlet, respectively. ψ is the rotor velocity coefficient. μ is the ratio of wheel
 277 diameter ($\mu = d_{2,sh} / d_1$). Ψ is the load coefficient ($\Psi = (u_1 c_{1u} - u_2 c_{2u}) / u_1^2$). b_1 is the
 278 nozzle blade height and d_1 is the nozzle outlet diameter. $d_{2,s}$ and $d_{2,h}$ are the
 279 diameter at the rotor shroud and hub, respectively. L_{df} and L_c are the disk-friction
 280 loss and tip clearance loss, respectively.

281 Five kinds of turbine loss are taken into consideration in the preliminary design,

282 including the nozzle passage loss, rotor passage loss, leaving velocity loss,
 283 disk-friction loss and tip clearance loss. The nozzle passage loss coefficient (ξ_n), rotor
 284 passage loss coefficient (ξ_r) and leaving velocity loss coefficient (ξ_e) are expressed
 285 as follows:

$$286 \quad \xi_n = (1 - \varphi^2)(1 - \Omega) \quad (15)$$

$$287 \quad \xi_r = (w_2 / c_s)^2 (1 / \psi^2 - 1) \quad (16)$$

$$288 \quad \xi_e = (c_2 / c_s)^2 \quad (17)$$

289 Disk-friction loss (L_{df}) and coefficient (ξ_{df}), tip clearance loss (ξ_c) and coefficient
 290 (L_c) are expressed as follows [45]:

$$291 \quad \xi_{df} = \frac{0.02125 \rho_1 u_1^3 r_1^2}{\left(\frac{\rho u r}{\mu} \right)_1^{0.2} \cdot m_{wf} \cdot \Delta h_s} \quad (18)$$

$$292 \quad L_{df} = \xi_{df} \cdot \Delta h_s \quad (19)$$

$$293 \quad \xi_c = \frac{h_c}{r_{2,s} - r_{2,h}} \quad (20)$$

$$294 \quad L_c = \xi_c \cdot \Delta h_s \quad (21)$$

295 where h_c is the tip clearance, specified as 0.3mm. This loss model assumes that the
 296 fractional loss due to tip clearance equals to the ratio of clearance to passage height at
 297 the rotor exit.

298 Turbine efficiency (total to static efficiency) is expressed as:

$$299 \quad \eta_{turbine} = \frac{\Delta h_{actual}}{\Delta h_s} = \frac{\Delta h - c_2^2 / 2}{\Delta h_s} \quad (22)$$

300 The power output is calculated as follows:

$$301 \quad W = \Delta h_{actual} m_{wf} \eta_{turbine} \quad (23)$$

302 **4. Coupled model of ORC and radial-inflow turbine with genetic algorithm**

303 4.1 Velocity coefficient

304 According to Eqs. (7)-(14), nozzle velocity coefficient (φ), rotor velocity
 305 coefficient (ψ), degree of reaction (Ω), velocity ratio (u_1/c_s), loading coefficient
 306 (Ψ), flow coefficient (Φ), ratio of wheel diameter (μ) are seven key dimensionless
 307 parameters when designing the radial-inflow turbine. In the preliminary design of
 308 conventional turbine, φ and ψ are estimated and specified according to the
 309 empirical formula since they are dependent on many factors, such as the blade profile,
 310 machining precision, fluid flow conditions and so forth. This study uses the loss
 311 models proposed by the Lewis Research Center [45] to calculate these two parameters
 312 iteratively. The relationships of φ and ψ with nozzle and rotor energy loss
 313 coefficients (ζ_n and ζ_r) are as follows:

$$314 \quad \varphi = \sqrt{1 - \zeta_n}, \quad \psi = \sqrt{1 - \zeta_r} \quad (24)$$

315 ζ_n and ζ_r can be expressed in a unified formula:

$$316 \quad \zeta_{3D} = \frac{EC \left(\frac{\theta_{tot}}{l} \right)_{ref} \left(\frac{Re}{Re_{ref}} \right)^{-0.2} \left(\frac{l}{s} \right) \left(\frac{A_{3D}}{A_{2D}} \right)}{\cos \gamma - \frac{t}{s} - HC \left(\frac{\theta_{tot}}{l} \right)_{ref} \left(\frac{Re}{Re_{ref}} \right)^{-0.2} \left(\frac{l}{s} \right)} \quad (25)$$

317 where E is the energy factor and H is the form factor, which presents the
 318 characteristics of boundary layer flow and can be calculated by empirical equations. C
 319 is the loss coefficient multiplier. Re is the Reynolds number. θ is the momentum

320 thickness. l is the surface length from leading edge to trailing edge. s is blade spacing
321 at blade-row exit. A_{3D}/A_{2D} represents the 3-D to 2-D area ratio. γ is the flow
322 angle from the throughflow direction. t is the trailing-edge thickness. All these related
323 factors are discussed in detail in [45] and can be calculated according to the
324 corresponding formulas. Some parameters need to be known in advance in order to
325 complete the preliminary design of the radial-inflow turbine and obtain some
326 parameters related to the geometry: the tip clearance value is fixed as 0.3mm
327 considering the manufacture technology; the radial clearance between nozzle and
328 rotor is specified as 1 mm [46]; the nozzle solidity is specified as 1.3 according to [47].
329 Nozzle blade uses the TC-4P blade profile which is a commonly used stator profile in
330 the ORC system and thus the nozzle inlet absolute flow angle α_0 can be obtained.
331 Initial φ and ψ are presupposed in advance to finish the preliminary design of the
332 radial-inflow turbine. Then ζ_n and ζ_r can be calculated by Eq. (25), after which φ
333 and ψ are updated by Eq. (24) to proceed to the next iteration until the differences in
334 velocity coefficients of two iteration are within a minimum range.

335 4.2 Optimization method

336 In addition to the other five dimensionless parameters (Ω , u_1/c_s , Ψ , Φ , μ),
337 rotational speed (ω) should also be optimized since its optimal value varies with
338 operating conditions. In this work, turbine efficiency is specified as the objective
339 function to optimize the radial-inflow turbine for each operating condition since under
340 this condition the optimized results of the power output as the optimization objective
341 are very similar to that of the turbine efficiency as the optimization objective.

342 The six optimized variables are limited by empirical values, as listed in Table 3.

343

Table 3 Recommended value ranges of the six optimized variables

Design variables	Range	Reference
Degree of reaction (Ω)	0.50-0.60	[48]
Velocity ratio (u_1 / c_s)	0.69-0.71	[36]
Loading coefficient (ψ)	0.85-1.00	[38]
Flow coefficient (ϕ)	0.15-0.30	[38]
Ratio of wheel diameter (μ)	0.50-0.60	[46]
Rotational speed (ω , <i>rpm</i>)	12000-25000	[38]

345 Some optimization constraints are implemented in this model to ensure the
 346 reasonable results of optimized turbine in terms of high aerodynamic performance and
 347 ease of manufacture.

348 • The nozzle outlet absolute blade angle α_1 is recommended between 12-30°
 349 and the rotor outlet relative blade angle β_2 is recommended between 20-45° [46].

350 These values are established with the trade-off between the high stage shaft power and
 351 low flow losses.

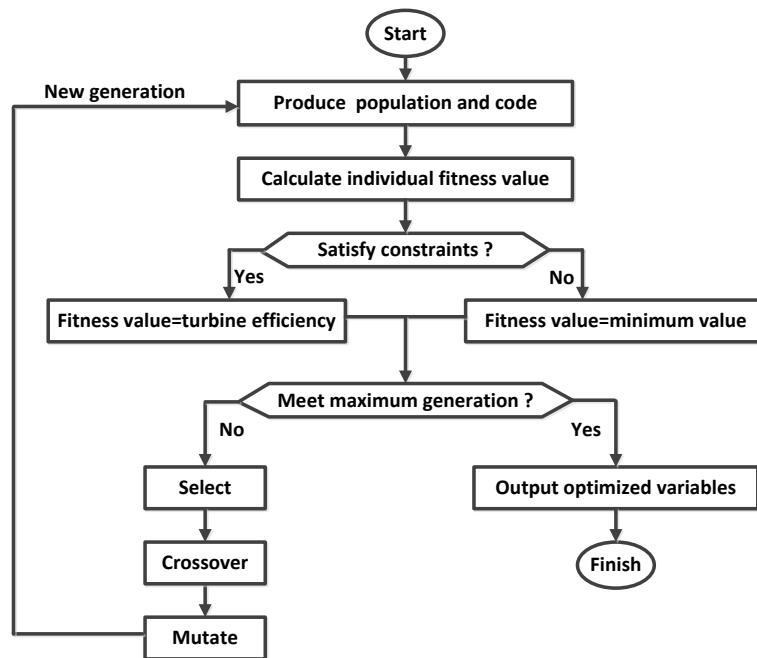
352 • The ratio of the rotor inlet blade height and diameter is considered to lie
 353 between 0.03 and 0.1 [46]. This value is set to limit the rotor tip clearance losses.

354 • The nozzle outlet Mach number is limited less than 1.5 to lower the supersonic
 355 loss at the rotor inlet.

356 • The hub ratio (rotor exit hub to inlet radius ratio, $d_{2,h} / d_1$) is set more than 0.2
 357 since the smaller hub ratio leads to great difficulty in assigning blades at the hub [44].

358 In this work, the genetic algorithm (GA) is used to complete the optimization of
 359 the six key design parameters. The GA is a global optimum algorithm based on the
 360 theory of biological evolution [49]. Compared with other optimization methods, the
 361 GA has many advantages. It can not only deal with complex optimization problems
 362 such as non-linear and multi-dimensional but also is less sensitive to the initial
 363 conditions. Therefore, the GA is widely used in many literatures about ORC systems

364 [13, 15, 40]. In the basic GA, the initial population of individuals is generated
 365 randomly from the prescribed range of optimization variables. All individuals in every
 366 generation are assessed in terms of their fitness values. A new generation of
 367 individuals is generated by selecting the current population according to their fitness
 368 values, crossovering the selected members according to the crossover rate and
 369 mutating certain individuals according to the mutation rate. Therefore, selection,
 370 crossover and mutation are the three main operations in GA. The flowchart of the
 371 constrained GA is shown in Fig. 5. The control operators of GA are listed in Table 4.



372

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Fig.5. Flowchart of the constrained GA

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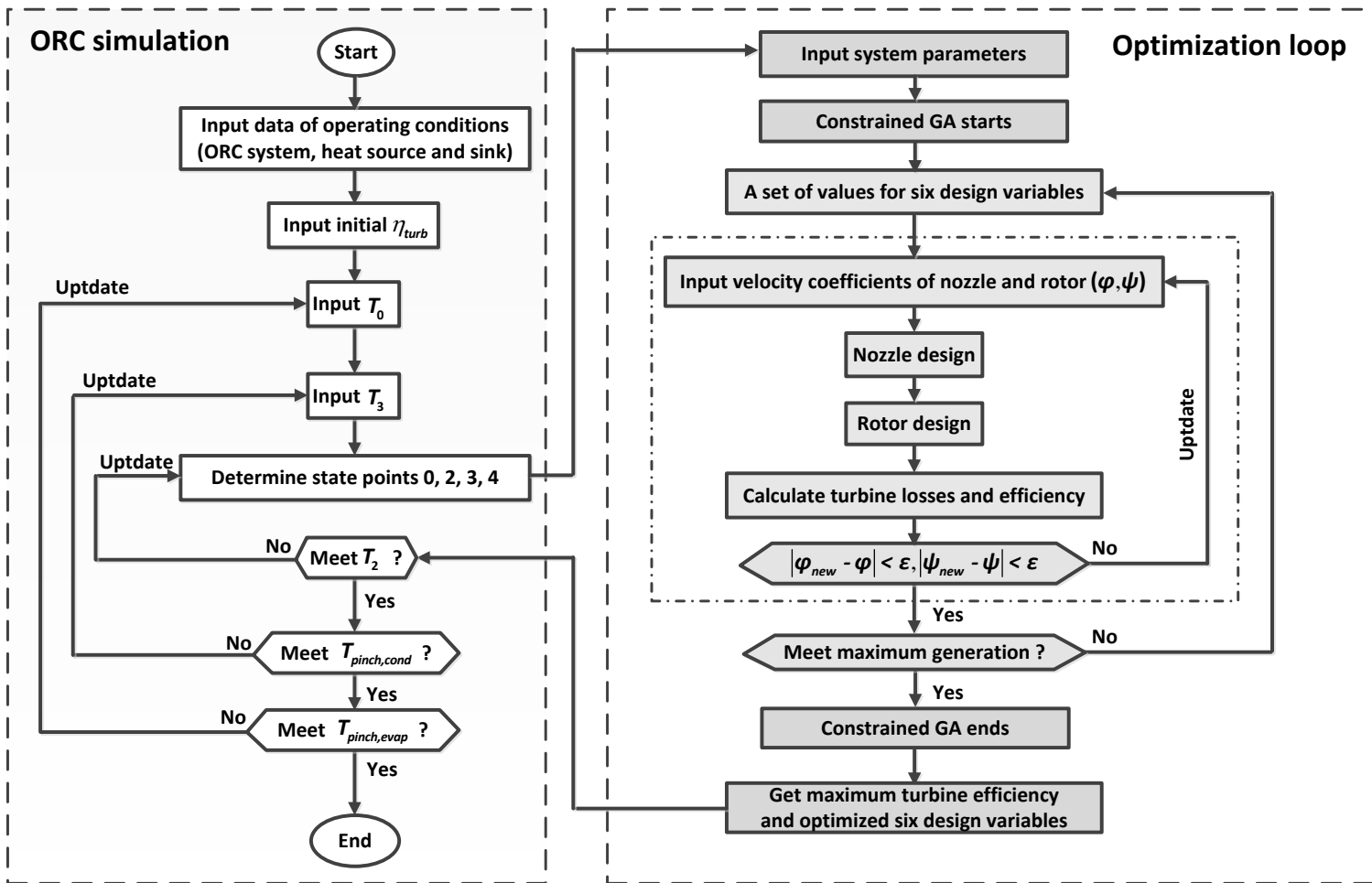
Table 4 Control operators of GA

Operator	Value
Maximum number of generations	200
Number of individuals	80
Selection rate	0.9
Crossover probability	0.7
Mutation rate	0.01

375 4.3 Simulation method

376 Fig. 6 shows the flowchart of the simulation process of the ORC system, in
377 which the optimization design of the radial-inflow turbine with constrained GA is
378 introduced. The pinch methodology is used here to simulate the ORC cycle. To
379 simplify the ORC modeling, the turbine inlet and condenser outlet are assumed to be
380 saturated vapor state and saturated liquid state, respectively. The turbine efficiency is
381 varying with the operation conditions of the ORC system instead of being constant in
382 the conventional ORC system design. Three initial input parameters, turbine inlet
383 temperature (T_0), condenser outlet temperature (T_3), and turbine efficiency ($\eta_{turbine}$)
384 are estimated as the initial input data to start the simulation. In the preliminary
385 optimization design, constrained GA optimizes six key parameters in the experience
386 value range as listed in Table 4, and the iterative solving process determines the
387 velocity coefficients of nozzle and rotor. After each loop, the newly obtained values of
388 the turbine inlet and outlet temperature as well as the condenser outlet temperature are
389 updated. If the requirements of the three parameters are not reached as shown in Fig. 6,
390 they are used again as the initial input data to continue the next loop. However,
391 initially turbine efficiency is estimated instead of the turbine outlet temperature. This
392 is because at the beginning it is difficult to estimate the turbine outlet temperature
393 while turbine efficiency can be estimated by experience. The process is repeated until
394 the requirements of the turbine outlet temperature, the pinch temperature in the
395 evaporation and condenser are met. Pinch point in the evaporation appears at the
396 saturated liquid state of the working fluids and pinch point in the condenser appears at
397 the saturated vapor state of the working fluids. An original MATLAB code is
398 programmed to simulate the described ORC system and optimization design of
399 radial-inflow turbine. The properties of working fluids are obtained from REFPROP

400 9.0 [50]. The simulation is assumed to operate at the steady state and to neglect the
 401 pressure and heat losses in the entire cycle.



402 Fig.6. Flowchart of the coupled ORC-turbine model

403 **5. Results and discussion**

404 5.1 Validation of the turbine design model

405 The turbine design model described in section 3 is validated by the comparison
 406 of the developed codes with other published codes: Glassman [45], commercial radial
 407 turbine design software RITAL from Concepts NREC [51] and Rahbar et al. [52]. The
 408 testing conditions are from Glassman case [45] and the results of different codes are
 409 shown in Table 5. The set of results from the developed model in this work shows a

410 good agreement with both the original one and literature in terms of flow
 411 characteristic, turbine principal geometry and overall performance. It should be
 412 noticed that the turbine total-to-static efficiency predicted by the developed code in
 413 this work is closer to the original efficiency than the other two kinds of codes.
 414 Therefore, the turbine design model is considered to be validated for the coupled
 415 modeling of ORC system and its radial-inflow turbine.

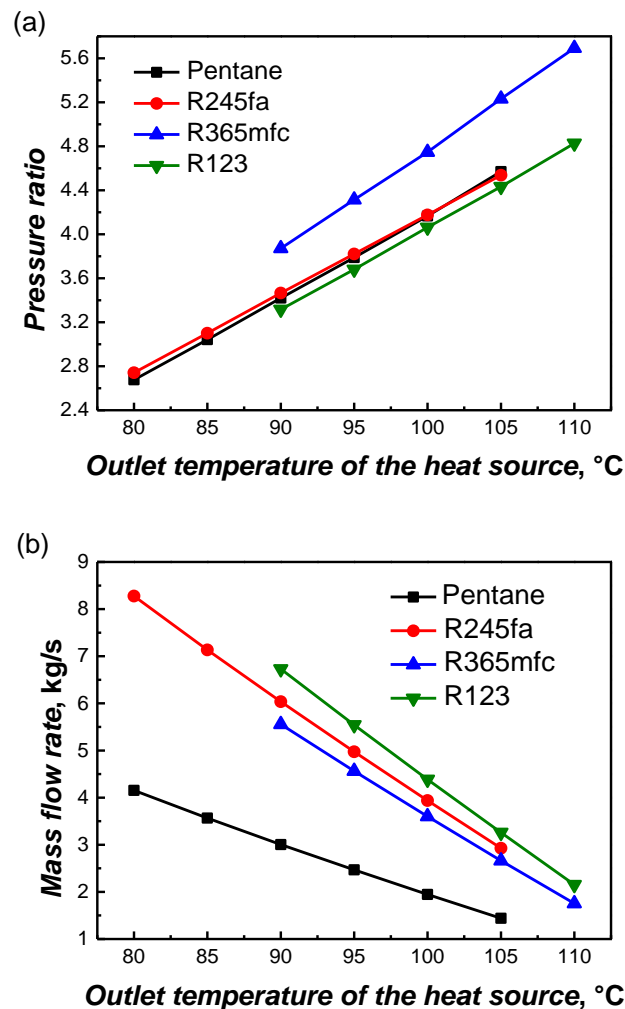
416 Table 5 Comparison of developed code with published codes

Paramter	Glassman [45]	RITAL [51]	Rahbar et al. [52]	Present code
Stator				
Inlet radius, m	0.09775	0.1033	0.09911	—
Outlet radius, m	0.07983	0.08268	0.08133	0.07795
Outlet absolute flow angle, deg.	18	26.61	21.89	18.09
Rotor				
Inlet radius, m	0.0777	0.07874	0.07888	0.07695
Outlet hub radius, m	0.01936	0.02362	0.02312	0.01995
Outlet shroud radius, m	0.05542	0.05591	0.05546	0.0546
Inlet absolute flow angle, deg.	18.08	26.87	26.49	18.09
Inlet relative flow angle, deg.	121.5	116.27	116.64	123.55
Outlet absolute flow angle, deg.	90	90.01	90	90.56
Outlet relative flow angle, deg.	35.10	34.42	36.24	35.1399
Total-to-static efficiency, %	82	79	78.8	79.45
Power, kW	22.371	—	—	21.52

417 5.2 Optimization results

418 The turbine design model validated in section 5.1 is used to study the coupled
 419 modeling of ORC system and its radial-inflow turbine, and to investigate the influence
 420 of heat source temperature. The overall examined range of the heat source outlet
 421 temperature is set from 110 °C to 80 °C. For pentane and R245fa the temperature
 422 range is 80-105 °C while for R365mfc and R123 the temperature range is 90-110 °C.
 423 Out of these ranges, certain design parameters of the radial-inflow turbine cannot

424 satisfy the constraints proposed in section 4 and thus there is no data at this point. The
 425 variations of pressure ratio and mass flow rate with the outlet temperature of the heat
 426 source are first shown in Fig. 7.



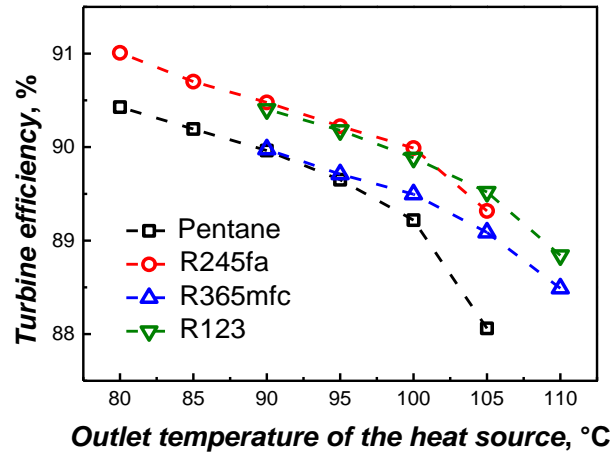
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429 Fig.7. Variations of (a) pressure ratio and (b) mass flow rate with the outlet temperature of the heat
 430 source

431 Under the condition of fixed mass flow rate for the heat source, as the outlet
 432 temperature of the heat source decreases, more heat load is absorbed by the ORC
 433 system and thus the mass flow rate of the working fluids increases. The cycle using
 434 R123 has the highest mass flow rate at any conditions while using pentane has the
 435 lowest mass flow rate. The lower outlet temperature of the heat source causes the
 436 evaporation temperature to decrease and thus to lower the pressure ratio. R365mfc has

437 the highest pressure ratio at each condition while for pentane, R245fa and R123 the
438 pressure ratios are similar.

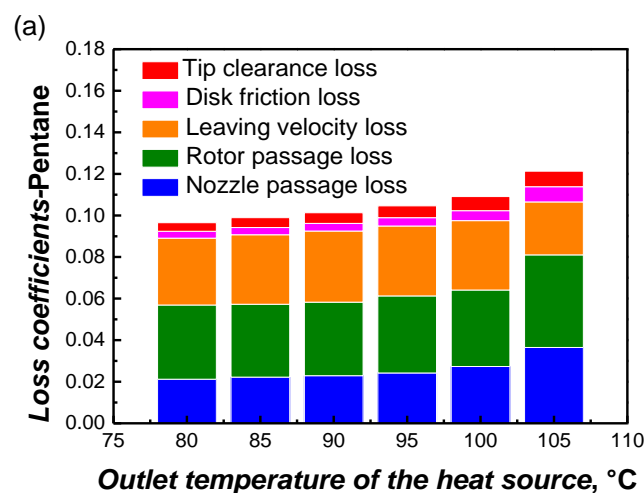


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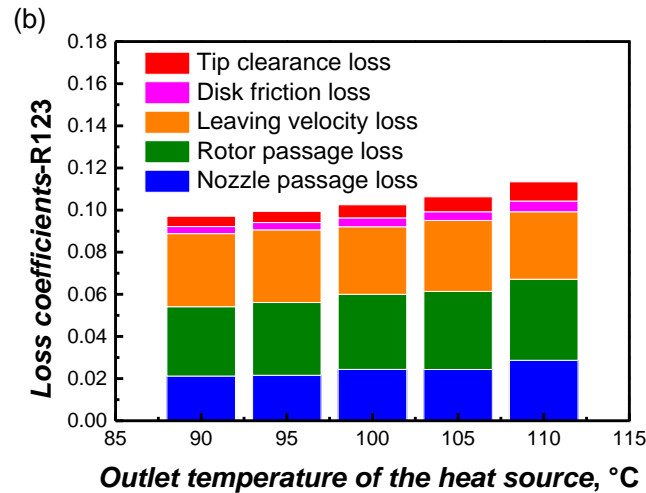
440 Fig.8. Variation of turbine efficiency with the outlet temperature of the heat source

441 The turbine efficiency depending on different working fluids and heat source
442 temperature conditions are shown in Fig. 8. The optimized turbine efficiency varies
443 from 88.06% using pentane at the heat source outlet temperature of 105 °C to 91.01%
444 using R245fa at the heat source outlet temperature of 80 °C. Fig. 8 also shows that the
445 turbine efficiency decreases with the increase of the heat source outlet temperature.
446 This indicates that smaller pressure ratio and larger mass flow rate enhance the turbine
447 efficiency. In addition, the decreasing rate of turbine efficiency becomes faster when
448 the heat source outlet temperature is greater than 100 °C, especially for pentane and
449 R245fa. R123 and R365mfc also have this similar trend but the decreasing rate is
450 respectively less intense. This can be explained by the loss distribution shown in Fig.
451 9, which illustrates the variations of five kinds of losses related with the heat source
452 outlet temperature using pentane and R123 as working fluids. Fig. 9 shows that the
453 rotor passage loss has the highest contribution for all the examined working fluids. As
454 the outlet temperature of the heat source increases, the rotor passage loss increases
455 gradually, especially violently when the heat source outlet temperature is greater than

456 100 °C. For pentane and R245fa, when the heat source outlet temperature increases
 457 from 100 °C to 105 °C, the increasing rate of the rotor passage loss coefficient is 20.92%
 458 and 17.05%, respectively. While for R365mfc and R123 the change rate is within
 459 4.5%. This great increase of the rotor passage loss accounts for the sudden drop of the
 460 turbine efficiency using pentane and R245fa. Since the pressure ratio increases with
 461 the higher outlet temperature of the heat source, the velocity at rotor becomes larger
 462 leading to higher rotor passage loss. In addition, the loss distribution is similar for all
 463 the examined working fluids with the rotor passage loss having the highest
 464 contribution, varying from 32.15% to 37.40% of the total losses. The nozzle passage
 465 loss, rotor passage loss and leaving velocity loss are diverse in the same order of
 466 magnitude. Disk-friction loss and tip clearance loss are one magnitude lower than the
 467 above three kinds of losses. As shown in Fig. 9, both the disk-friction loss and tip
 468 clearance loss increase with the rise of the heat source outlet temperature. This is
 469 consistent with the conclusion that high expansion ratio leads to high friction loss
 470 [42].



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Fig.9. Variations of the five kinds of losses with the outlet temperature of the heat source using pentane and R123

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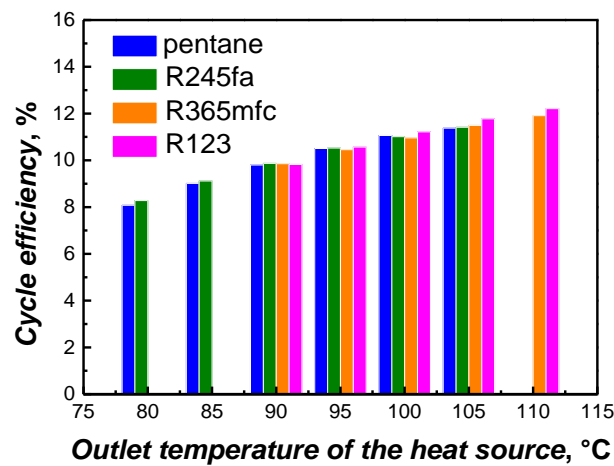
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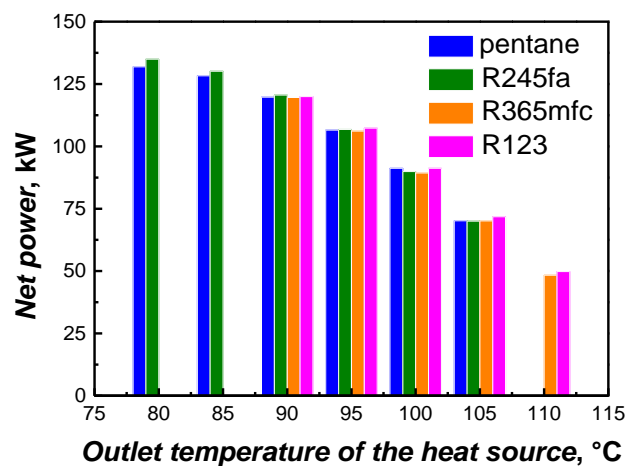
The simulated results of the cycle efficiency, net power output and specific net power per mass flow rate are successively plotted in Fig. 10, Fig. 11 and Fig. 12. Fig. 10 shows the cycle efficiency increases with the rise of the heat source outlet temperature while the net power has the opposite trend. This is due to the fact that the mass flow rate of the working fluids increases and enthalpy drop decreases with the lower heat source outlet temperature, but the increase degree of the mass flow rate is much larger than the decrease degree of the enthalpy drop, which accounts for the increase of the net power. Take R123 for example, the enthalpy drop is -23.23% while the increase of the mass flow rate is 212.60% when the outlet temperature of the heat source changes from 110 °C to 90 °C. Moreover, it can be noticed that the differences of both the cycle efficiency and the net power output among different working fluids at each condition are not substantial. As shown in Fig. 12, the specific net power per mass flow rate increases with the higher heat source outlet temperature. Though the turbine efficiency using pentane is the lowest at each condition presented in Fig. 8, the specific net power is much higher than the other three kinds of working fluids. This indicates that pentane has the highest enthalpy drop among the examined working

491 fluids. In the situation where the inlet temperature of the heat source rather than the
 492 absorbed heat load is fixed, the ORC cycle efficiency and the net power output change
 493 monotonously with the heat source outlet temperature, but their variation trends are in
 494 the opposite direction. From the perspective that the net power output is the main aim
 495 of the ORC system, the lower the outlet temperature of the heat source is, the better.
 496 Among the four examined working fluids, R123 achieves the maximum cycle
 497 efficiency of 12.21% together with the turbine efficiency of 88.84% at the heat source
 498 outlet temperature of 110 °C. R245fa achieves both the maximum net power output of
 499 138.74 kW and the maximum turbine efficiency of 91.01% at the heat source outlet
 500 temperature of 80 °C.



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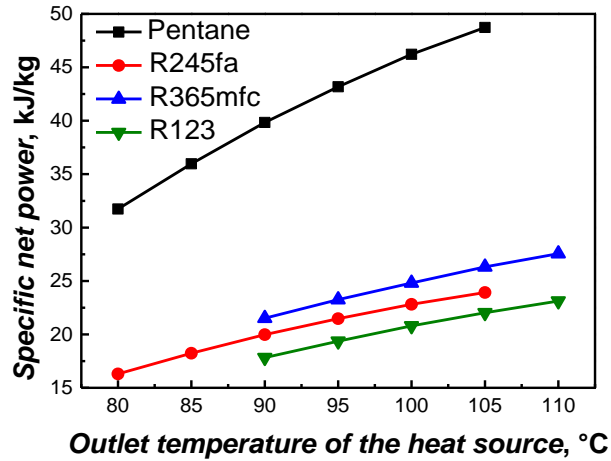
Fig.10. Variation of cycle efficiency with the outlet temperature of the heat source



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Fig.11. Variation of net power with the outlet temperature of the heat source



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Fig.12. Variation of specific net power with the outlet temperature of the heat source

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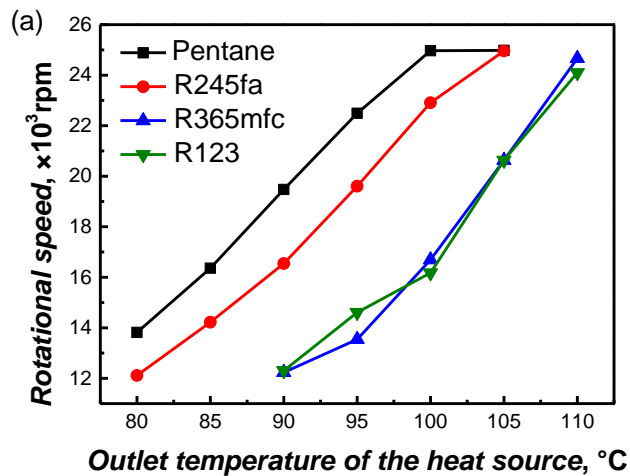
In the following section a thorough analysis of the optimized results of the six key design parameters is conducted to provide references for ORC radial-inflow turbine in the low temperature range. Fig. 13 shows the optimized results of rotational speed, overall diameter (d_0) and Mach number at the rotor inlet with the outlet temperature of the heat source.

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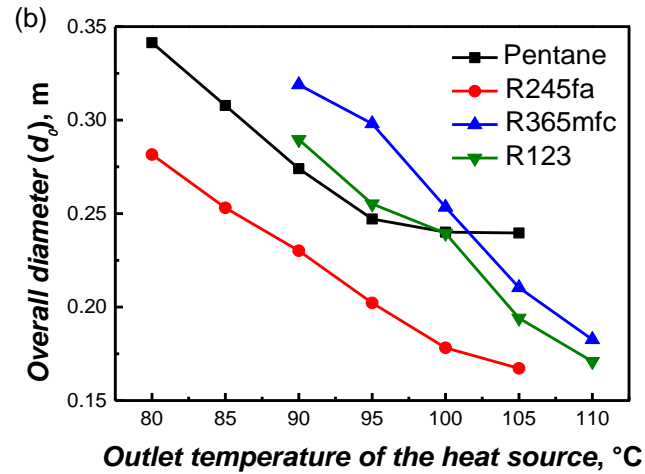
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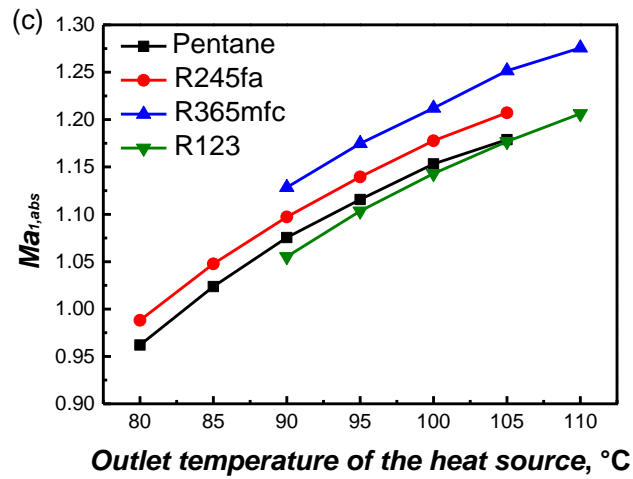
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515 Fig.13. Variation of rotational speed (a), overall diameter (b) and Mach number at the rotor inlet (c)
 516 with the outlet temperature of the heat source

517 As shown in Fig. 13, the rotational speed increases with the rise of the heat
 518 source outlet temperature. Since the enthalpy drop increases with the higher heat
 519 source outlet temperature, higher rotational speed is required to provide the larger
 520 peripheral speed and more wheel periphery work. Taking R245fa for example, the
 521 rotational speed increases from 12114 rpm to 24959 rpm when the heat source outlet
 522 temperature changes from 80 °C to 90 °C, which amounts to 106.03% growth rate. In
 523 addition, pentane has the highest rotational speed at each condition. This is expected
 524 because pentane has the largest enthalpy drop among the examined fluids discussed
 525 previously. Fig. 13 also indicates that pentane reaches its rotational speed constraint

526 when the heat source outlet temperature is more than 100 °C.

527 Considering the practicability of manufacture, some parameters related to the
528 turbine geometry, including the hub ratio ($d_{2,h} / d_1$), the inlet diameter of the turbine
529 (d_0) and the ratio of the rotor inlet blade height and diameter (b_1 / d_1), restrict the
530 upper and lower limits of the heat source outlet temperature. For the examined
531 working fluids, as the outlet temperature of the heat source increases, the inlet
532 diameter of the turbine decreases because of the reduction in the mass flow rate of the
533 working fluids. The minimum overall diameter d_0 is achieved by R245fa at the heat
534 source outlet temperature of 105 °C ($d_0=167.2\text{mm}$) while the largest size is achieved
535 by pentane at the heat source outlet temperature of 80 °C ($d_0=341.4\text{mm}$). The rotor
536 exit hub to inlet radius ratio is in the range of 0.2017-0.2785 and is consistent with the
537 literature [15, 44]. Fig. 13 shows the variation of Mach number at the rotor inlet
538 ($Ma_{1,abs}$) with the outlet temperature of the heat source. $Ma_{1,abs}$ increases with the
539 higher heat source outlet temperature and R365mfc has the highest $Ma_{1,abs}$ at all
540 conditions because of combined effect of the high peripheral speed and low density
541 while R123 has the lowest. Except the condition of heat source outlet temperature of
542 80 °C, all the examined working fluids have supersonic expansion at the rotor inlet,
543 which is undesirable. It indicates that it is appropriate to use the TC-4P blade profile
544 for nozzle since such kind of blade profile has lower loss in the transonic situation.

545 Based on the optimized results, the recommended ranges for the key six design
546 parameters can be made: the degree of reaction is recommended as 0.5-0.51; the
547 velocity ratio is recommended as 0.70-0.71; the loading coefficient is recommended
548 as 0.88-0.93; the flow coefficient is recommended as 0.26-0.29; the ratio of wheel
549 diameter is recommended as 0.51-0.6. Detailed results at the maximum turbine

550 efficiency condition are shown in Table 6.

551 Table 6 Optimized results of the preliminary design for the examined working fluids at the
 552 maximum turbine efficiency condition

Parameters	Pentane, 80 °C	R245fa, 80 °C	R365mfc, 90 °C	R123, 90 °C
d_0 (m)	0.3414	0.2816	0.3189	0.2896
$b_{1,n}$ (m)	0.0175	0.0135	0.0145	0.0138
$d_{1,n}$ (m)	0.2625	0.2166	0.2452	0.2227
d_1 (m)	0.2605	0.2146	0.2432	0.2207
b_1 (m)	0.0180	0.0139	0.0149	0.0142
b_1 / d_1	0.0690	0.0646	0.0614	0.0643
$d_{2,s}$ (m)	0.2106	0.1730	0.1962	0.1782
$d_{2,h}$ (m)	0.0637	0.0498	0.0523	0.0553
Z_r	12	12	12	12
$Ma_{1,rel}$	0.2780	0.2868	0.3267	0.3065
$Ma_{1,abs}$	0.9621	0.9882	1.1284	1.0553
$Ma_{2,rel}$	0.5947	0.5987	0.6973	0.6618
$Ma_{2,abs}$	0.2481	0.2402	0.3054	1.0553
α_0 (deg.)	79.21	79.16	79.26	79.21
α_1 (deg.)	16.38	16.43	16.33	16.37
α_2 (deg.)	99.63	99.67	99.28	99.20
β_1 (deg.)	102.58	102.90	103.84	103.90
β_2 (deg.)	24.29	23.29	25.61	25.02
$\beta_{2,s}$ (deg.)	18.10	17.26	18.96	18.72
$\beta_{2,h}$ (deg.)	51.09	51.16	56.72	51.21
$d_{2,h} / d_1$	0.2445	0.2322	0.2151	0.2505
$\eta_{turbine}$ (%)	90.428	91.008	89.977	90.404

553

554 6. Conclusions

555 This paper proposes a coupled modeling of the ORC system and the
 556 radial-inflow turbine, which is designed by the mean-line approach with constrained
 557 GA to maximize the turbine efficiency. This model allows for the dynamic design of
 558 the ORC system and its radial-inflow turbine based on a wide range of operating
 559 conditions and a reasonable range of aerodynamic and geometric parameters. The

560 influences of heat source outlet temperature on the performance of ORC and
561 radial-inflow turbine are investigated for pentane, R245fa, R365mfc and R123. It is
562 found that the turbine efficiency decreases as the outlet temperature of the heat source
563 increases with the minimum efficiency of 88.06% and maximum efficiency of 91.01%.
564 Moreover, the cycle efficiency increases monotonously with the increase of the heat
565 source outlet temperature while the net power output has the opposite trend. The
566 maximum turbine and cycle efficiencies of 91.01%, 12.18% are obtained by R245fa at
567 the heat source outlet temperature of 80 °C and R123 at the heat source outlet
568 temperature of 110 °C, respectively. In addition, the recommended ranges for the
569 degree of reaction, velocity ratio, loading coefficient, flow coefficient and ratio of
570 wheel diameter of radial-inflow turbine are 0.5-0.51, 0.70-0.71, 0.88-0.93, 0.26-0.29
571 and 0.51-0.6, respectively. The minimum overall diameter d_0 (=167.2mm) is
572 achieved by using R245fa at the heat source outlet temperature of 105 °C.

573 Compared with other coupled design for ORC and radial-inflow turbine, this
574 study introduces the constrained GA into the preliminary design of radial-inflow
575 turbine with the prediction models of the velocity coefficients of nozzle and rotor.
576 This coupled model is dynamic with the aim of achieving the maximum turbine
577 efficiency. This study highlights the potential and effectiveness of this coupled
578 modeling in design analysis for the ORC system and its radial-inflow turbine. Further
579 work will concentrate on the CFD simulation or experimental testing of an ORC
580 radial-inflow turbine.

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738 **Table and figure captions**

739 Fig.1. Schematic diagram of the basic ORC

740 Fig.2. Temperature-entropy curve of the basic ORC (using pentane)

741 Table 1 Working conditions for the heat source, heat sink and cycle parameters

742 Table 2 Properties of the working fluid candidates

743 Fig.3. h-s diagram of the radial-flow turbine

744 Fig.4. Velocity triangles of the radial-inflow turbine

745 Table 3 Recommended value ranges of the six optimized variables

746 Fig.5. Flowchart of the constrained GA

747 Table 4 Control operators of GA

748 Fig.6. Flowchart of the coupled ORC-turbine model

749 Table 5 Comparison of developed code with published codes

750 Fig.7. Variations of (a) pressure ratio and (b) mass flow rate with the outlet

751 temperature of the heat source

752 Fig.8. Variation of turbine efficiency with the outlet temperature of the heat source

753 Fig.9. Variations of the five kinds of losses with the outlet temperature of the heat

754 source using pentane and R123

755 Fig.10. Variation of cycle efficiency with the outlet temperature of the heat source

756 Fig.11. Variation of net power with the outlet temperature of the heat source

757 Fig.12. Variation of specific net power with the outlet temperature of the heat source

758 Fig.13. Variation of rotational speed (a), overall diameter (b) and Mach number at the

759 rotor inlet (c) with the outlet temperature of the heat source

760 Table 6 Optimized results of the preliminary design for the examined working fluids at
761 the maximum turbine efficiency condition