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Published in:
Journal of Solid State Electrochemistry

Link to article, DOI:
[10.1007/s10008-012-1778-4](https://doi.org/10.1007/s10008-012-1778-4)

Publication date:
2012

[Link back to DTU Orbit](#)

Citation (APA):
Shao, J., & Kammer Hansen, K. (2012). Optimization of an electrochemical cell with an adsorption layer for NO_x removal. *Journal of Solid State Electrochemistry*, 16, 3331–3340. DOI: 10.1007/s10008-012-1778-4

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Optimization of an electrochemical cell with an adsorption layer for NO_x removal

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Abstract

The structure of a multilayer electrochemical cell with an adsorption layer was optimized by removing a yttria-stabilized zirconia cover layer. It was found that the NO_x removal properties of the electrochemical cell were dramatically enhanced through the optimization, especially under conditions of low voltage, intermediate temperature and high O₂ concentration. The pronounced increase in activity and selectivity for NO_x decomposition after removing the yttria-stabilized zirconia cover layer was attributed to the extensive release of selective reaction sites for NO_x species and a strong promotion for NO_x reduction from the interaction of the directly connected adsorption layer with both the Pt and catalytic layers. The optimized electrochemical cell may provide a promising solution for NO_x emission control.

Key words: NO_x removal, Electrochemical cell, Optimization, NO_x adsorption

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1. Introduction

Lean burn engines can greatly improve fuel economy, however, the amount of NO_x emission also increases under lean conditions and cannot be removed by the traditional three-way catalyst due to the O_2 rich environment [1]. NO_x is dangerous for both human beings and the environment, causing health problems [2], acid rain and depletion of the protective ozone layer [3, 4]. Government regulations to limit NO_x emission are becoming increasingly more stringent in many countries [5, 6]. Therefore, there is high demand to find an effective method to reduce NO_x emission from lean burn engine exhaust. The electrochemical reduction of NO_x using a solid oxide cell is an attractive technique for lean burn exhaust-gas after treatment because it requires no additional reducing agents other than electrons and has the potential to form only N_2 and O_2 [7, 8]. The challenge of this technique is to achieve both high selectivity and activity towards NO_x reduction in the presence of excess O_2 . Thus a lot of research effort has been made on searching suitable electrode materials and optimizing the cell structure [7, 8].

Recently, K. Hamamoto et al. proposed a new type of electrochemical cell with a multilayer cathode and a NO_x adsorption layer or a NO_x adsorbent for the NO_x removal [9-11]. It was reported that the introduction of a NO_x adsorption layer greatly improved both the activity and selectivity of the electrochemical cell towards NO_x reduction [9, 10]. Figure 1 shows a sketch of such a cell with an adsorption layer for NO_x decomposition [9]. During the cell operation, the external voltage was applied between the mesh-patterned Pt cathode and the Pt|YSZ (yttria stabilized zirconia) anode, which led to the polarization of the YSZ electrolyte and the reduction of NiO to nano Ni grains in the vicinity of NiO|YSZ interfacial regions in the catalytic layer [8, 9, 12-15]. Because the adsorption and decomposition of NO_x molecules occurs in preference to oxygen molecules on Ni grain surfaces [16-19], the self-assembled nano-pores and nano-Ni particles in the catalytic layer provide a highly selective reaction site for NO_x reduction [8, 9, 12-15] and also suppress the unwanted reaction of oxygen

decomposition [20, 21]. The adsorption layer, coated on the cathode side of the electrochemical cell, was made of a traditional NSR (NO_x storage and reduction) catalyst that is normally used to trap and reduce NO_x through a cyclic switch between lean and rich conditions [22]. It was previously proposed [9] that an additional adsorption layer could provide a NO_x -rich atmosphere to the reaction sites in the NiO|YSZ catalytic layer to promote NO_x reduction. A YSZ cover layer was deposited on the top of the catalytic layer in order to increase the NO_x selectivity, because it was stated that the YSZ upper layer led to inhibit the O_2 decomposition on the open surface of the catalytic layer and increase the amount of nano-Ni grains in the interface region of YSZ|NiO [8, 12, 13].

However, for the electrochemical cell itself, the cathode with a YSZ cover layer was developed before the adsorption layer has been introduced [8, 12-15, 20, 21]. Although on a cell without the adsorption layer, the deposition of a YSZ upper layer led to improve NO_x selectivity [8, 12, 13], after adding the adsorption layer, we believe the presence of the YSZ cover layer will be harmful to NO_x decomposition. First, the diffusion of NO_x gas from the adsorption layer to the reaction sites in the catalytic layer should be severely impeded by the intervening YSZ layer, which could in turn inhibit the desorption of the NO_x stored in the adsorption layer. Second, a promotion effect for NO_x removal may be generated at the interface of the adsorption layer and the Pt layer or catalytic layer because the adsorption and desorption properties of the NO_x adsorbent in the vicinity of the reaction site may play an important role in NO_x decomposition [9, 10]. But this positive effect cannot be utilized with the YSZ cover layer because it blocks the direct contact between the adsorption layer and the other layers. Therefore, in this study, we modified the structure of the electrochemical cell by removing the YSZ cover layer to make the cell better cooperate with the adsorption layer.

2. Experiment

2.1. Cell preparation

A schematic diagram of the electrochemical cell with a YSZ cover layer can be found in figure 1. The cell was supported on a 200- μm layer of YSZ (8% Y_2O_3 doped ZrO_2) electrolyte with a multilayer cathode and a Pt|YSZ anode. An adsorption layer was applied to the surface of the cathode. Here, two kinds of electrochemical cells were prepared and tested for comparison: one with a YSZ cover layer, named S1; the other one without a YSZ cover layer, named S2. Other than the YSZ cover layer, all the other parts of these two cells were fabricated in the same way. The preparation procedure of S1 is described below as an example.

The catalytic layer was made by screen printing a composite paste of 55 mol% NiO – 45 mol% YSZ (8% Y_2O_3 doped ZrO_2) on a 5 cm x 5 cm YSZ tape. Then, the NiO|YSZ layer was sintered at 1450 °C for 5 hours. A net-shaped Pt layer was screen printed over the NiO|YSZ layer and calcined at 1250 °C for 1 hour. A YSZ (8% Y_2O_3 doped ZrO_2) cover layer was later screen printed over the Pt layer and sintered at 1450 °C for 3 hours. The Pt|YSZ paste (TR-7070, Tanaka Kikinzoku) was subsequently screen printed on the other side of the YSZ tape and sintered at 1400 °C for 1 hour. Finally, the adsorption layer was coated by dripping several drops of an adsorbent solution on the top YSZ cover layer. The adsorbent solution was made by mixing 10 wt% adsorbent and 10 wt% Pluronic 123 surfactant (BASF) in water. The adsorbent was composed of 10 wt% K and 3 wt% Pt supported on Al_2O_3 powder. The adsorption layer was first dried at 110 °C for 12 hours, followed by heating at 600 °C for 1 hour. The preparation was similar to that of Hamamoto et al [9]. After the preparation, the large cell (5 cm x 5 cm) was laser-cut into several small round cells with diameters of 14 mm.

2.2. Electrochemical test

For the electrochemical test, S1 and S2 were examined under the same conditions. The cells were set in a quartz tube reactor [23] inside a furnace and connected to a Gamry Reference 600 potentiostat. The cells were polarized under -1.5 to -4.5 V for a certain period in the temperature range of 375 °C to

500 °C, with 25 °C intervals. The gas composition was 1000 ppm NO and 0%- 8% O₂ in a balance gas of Ar with a flow rate of 2 L/h, maintained by Brooks mass flow controllers. The outlet gas composition was monitored throughout the test. The NO, NO₂ and NO_x concentration were measured by chemiluminescence (Model 42i HL, Thermo Scientific). The N₂ and N₂O were measured by mass spectrometry (Omnistar GSD 301, Pfeiffer Vacuum). No N₂O was detected in all the tests.

2.3. Microstructure characterization

The microstructure and element composition of the cells before and after the test were investigated by scanning electron microscopy (Zeiss Supra 35) and EDS (energy dispersive spectroscopy). The cells were broken manually and the cross section was polished and coated with carbon. In order to distinguish different elements on the cross section, all the images were recorded with the backscattered detector.

3. Results

The performance of the electrochemical cell can be evaluated by its activity and selectivity toward NO_x reduction. The activity of the cell can be represented by the NO_x conversion rate, a percentage of the NO_x decomposed compared with the total NO_x content. The selectivity can be evaluated by current efficiency (CE), a ratio of the current consumed by NO_x reduction (I_{NO}) to the total current (I_{tot}) flowing through the cell. I_{NO} is calculated using Faraday's law, as shown in equation 1. The current consumed by O₂ reduction is calculated by subtracting I_{NO} from I_{tot} .

$$(1)$$

$$(2)$$

ΔNO_x is the amount of NO_x decomposition; z is the charge change of N from NO_x to N₂ (for NO, $z = 2$; for NO₂, $z = 4$); v is the total flow rate; and F is Faraday's constant. Because NO₂ concentration varies with

O₂ concentration and temperature and it is usually lower than 30% of the total NO_x concentration, we calculated CE as the minimum by assuming all of the NO_x were NO ($z = 2$), in order to simplify the calculation and compare our results with the literature [9].

3.1. Dependence of NO_x removal properties on O₂ concentration

The dependence of NO_x removal properties of S1 (with the YSZ cover layer) and S2 (without the YSZ cover layer) on O₂ concentration is shown in figures 2 and 3. The cells were polarized under -2.5 V at 450 °C in 1000 ppm NO and different O₂ concentrations with balance Ar. The concentration of O₂ was varied from 0% to 8%. The results reported by Hamamoto et al. [9] on an electrochemical cell with a YSZ cover layer, which has the same structure with S1, was also listed as a reference. The reference results, which were the best reported in the literature, were measured under the same polarization voltage (-2.5) but at a higher temperature (500 °C). It was observed that without O₂, both S1 and S2 could decompose NO_x with quite high activity and selectivity. After O₂ was introduced, the activity of S1 sharply fell to less than 40% while the activity of S2 only slightly decreased from 100% to greater than 85%; the current efficiencies of S1 and S2 both dropped to approximately 16%, but the CE of S2 became increasingly higher than that of S1 with increasing O₂ concentrations. Because S1 and S2 were prepared and tested under the same conditions, the difference in their performance could be ascribed to the presence of the YSZ cover layer, which strongly supported the great improvement in NO_x removal properties by removing the YSZ cover layer. In comparing the results of this work with that of the reference, the NO_x conversion rate of S1 was obviously lower than that of the reference cell. Because S1 should have the same structure as the reference cell, we assumed that the deviation might be caused by the difference of the raw material and some other preparation details, which have not yet been clearly identified. Other than the YSZ cover layer step, the cell S2 was prepared exactly in the same way as S1. Thus, if there was any negative effect on the structure brought by the preparation other than the YSZ cover

layer, it should be equally present on S2. However, S2, showed a much higher NO_x conversion rate than the reference cell. The current efficiency of S2 was slightly lower than that of the reference cell under low O₂ concentrations, but became increasingly higher than the latter with increasing O₂. Moreover, because the results of S2 were recorded at 50 °C lower than that in the reference [9], it indicated that by removing the YSZ cover layer, better performance could be achieved at a lower temperature, which further demonstrated that the modification of the structure was successful.

There was an unusual increase of the activity and selectivity of S2 in 8% O₂. The reason has not yet been identified, but it should not be ascribed to a measurement error because the result was reproducible. One possible reason for the promotion of NO_x conversion under higher O₂ concentration was the larger ratio of NO₂ to NO because NO₂ was a stronger oxidant and proposed as an intermediate for NO reduction on the LSM | CGO electrode [24]. However, it was unclear why the promotion was only revealed on S2 when 8% O₂ was present.

3.2. Dependence of NO_x removal properties on temperature

Figure 4 shows the performance of S1 and S2 for NO_x decomposition at different temperatures under - 2.5 V in 1000 ppm NO and 2% O₂ with balance Ar. It was observed that S2 gave a greatly higher activity for NO_x decomposition than S1 over the entire temperature range and completely removed all the NO_x at 475 °C and 500 °C. Meanwhile, S1 decomposed less than 50% NO_x under the same conditions. The selectivity of S2 was also markedly higher than that of S1 at lower temperatures, but fell close to that of S1 at 475 °C and slightly lower at 500 °C. S2 lost the advantage of selectivity over S1 at high temperature, as it was approaching the limit for NO_x conversion. At 450 °C, the NO_x conversion of S2 achieved 92%, so with additional temperature increases, there was little room for further increases in NO_x conversion. At 475 °C, S2 completely decomposed all the NO_x in the system. The current for reducing NO (I_{NO}) had reached the maximum and could not increase further at elevated temperatures. Under these conditions,

the increased activity of the system at high temperatures resulted in increased O₂ reduction rather than NO_x reduction. As a result, the decline in selectivity of S2 was magnified at high temperatures. This result indicated that S2 might have the potential to give a higher selectivity at high temperature when a larger amount of NO_x is presented. It is noteworthy that S2 showed a similar NO_x conversion (8.5% lower) and a far greater CE (48.5% higher) at as low as 425 °C compared with the reference cell at 500 °C [9].

3.3. Dependence of NO_x removal properties on polarization voltage

Figure 5 shows the NO_x removal properties at various voltages at 450 °C in 1000 ppm NO and 2% O₂ with balance Ar. S2 reduced near 50% NO_x under voltage as low as -1.5 V and completely removed all the NO_x from -3.5 V to -4.5 V, while the NO_x conversion of S1 was below 50% over the entire voltage range. The selectivity of S2 was increasingly higher than that of S1 with voltage decreasing below -2.5 V. Above -2.5 V, the CE of S2 decreased to values near that of S1. In the case of S2, the NO_x conversion increased rather linearly by increasing the voltage up to -2.5 V, while eventually reached a steady state above -3.5 V which behavior could be an evidence of a diffusion controlled process taking place. Specifically, in the range of -2.5 V and -3.5 V, the process could be likely a mixed controlled behavior, limited both by the mass transfer of NO_x species towards the electrode or product species from the electrode, and by charge transfer or surface adsorption/desorption processes depended on the change of voltage. However, it is needed to point out that the application of voltage higher than -3.5 V resulted in a 100% conversion of NO_x species present in the gas mixture. Therefore, even though the absolute value of the applied voltage increased, the NO_x conversion could not further be increased, since NO_x species in the system have been already completely reduced by S2. For sample S1, with YSZ cover layer, it seems not to be a simple diffusion controlled behavior, although the diffusion of NO_x species to the electrode should be seriously impeded by the YSZ cover layer. One possible explanation is that not only the

diffusion of NO_x species was impeded, but also the other processes related with the electrochemical reduction of NO_x were affected by the existence of YSZ cover layer.

3.4. Selectivity towards N_2 formation

On both S1 and S2, the amount of N_2 formation measured by mass spectrometer was quite close to that calculated from NO_x decomposition (see equation 4). The N_2 selectivity (η , see equation 3) was approximately 90% under all the test conditions. Taking into account the N_2 formation calculated for sample S2 at different O_2 concentrations as an example (table 1), it was found that the selectivity towards N_2 formation was as high as 91.5% without O_2 ; While in presence of O_2 , the N_2 selectivity decreased slightly below 90%. Besides, no N_2O was detected by mass spectrometry in all the tests. Therefore, it is concluded that both S1 and S2 have high selectivity towards N_2 formation.

In summary, compared with the sample with the YSZ cover layer, the sample without a YSZ cover layer gave much higher activity for NO_x decomposition under all the tested voltages, temperatures and O_2 concentrations, providing better selectivity at low voltage (-1.5 V to -2.75 V), intermediate temperature (375 °C to 450 °C) and high O_2 concentrations (4% to 8%). Therefore, by removing the YSZ cover layer, the NO_x removal properties of the electrochemical cell with an adsorption layer could be dramatically enhanced under harsh conditions.

4. Discussions

4.1. Reasons for activity enhancement

According to systematic research [8, 12-15] on the NiO|YSZ catalytic layer by Bredikhin and colleagues, it is believed that there are two reaction sites for NO and O_2 molecules in the catalytic layer. As schematically shown in figure 6, one is the F-center near the three phase boundaries of YSZ|Pt|gas or YSZ|Ni|gas, which is dominated by O_2 reduction in O_2 -rich environment. The other is the nano-sized Ni

particle generated by reducing NiO under cell operation, which can preferably adsorb and decompose NO in the presence of O₂ [16-19], thus providing an effective reaction site for the selective reduction of NO_x. The reaction mechanism can be modeled by the following equations.

For O₂ reduction:

(5)

For NO reduction:

(6)

(7)

(8)

In this study, one of the major reasons for the enhancement of NO_x reduction activity by removing the YSZ cover layer was thought to be the increase in active reaction sites for NO_x reduction. This assumption was corroborated by the microstructure observation and EDS analysis results of the NiO|YSZ layer.

Figure 7 shows the microstructure images for the cathodes of S1 and S2 before and after measurement. It can be clearly seen that there were nano-particles and nano-pores generated in the NiO|YSZ catalytic layer after measurement, which was due to the reduction of NiO to Ni by the cell operation. More importantly, it was found that there was a large amount of nano-Ni particles left on S1 compared to S2, which was confirmed by composition analysis by EDS in figure 8. It was previously demonstrated that because the oxidation of Ni by O₂ started at 350 °C [25], most of the unconsumed Ni would be re-oxidized by O₂ during the cooling period without the protection of applied voltage [26]. In this work, both S1 and S2 were held in 2% O₂ at 500 °C for approximately 10 hours before cooling down. Therefore,

the Ni particles should be almost fully re-oxidized unless they cannot be reached by O_2 . Significantly more residual Ni in the catalytic layer of S1 indicated that the gas path to the nano-Ni grains was severely impeded or even blocked compared with that of S2, which led to a large loss of active sites for NO_x reduction. By removing the YSZ cover layer, a significant number of reaction sites for NO_x reduction could be released, greatly enhancing the NO_x reduction activity of S2.

4.2. Reasons for selectivity increase

In addition to the activity enhancement for NO_x reduction, the O_2 reduction also increased after removing the YSZ cover layer, because the suppression of O_2 adsorption and decomposition on the open surface of the catalytic layer by the YSZ layer was lost as well. On an electrochemical cell without an adsorption layer, omitting the YSZ cover layer resulted in a lower selectivity for NO_x reduction. However, in the case with an adsorption layer, the cell without a YSZ cover layer showed much better selectivity under harsh conditions while simultaneously maintaining a high activity.

The difference was most likely due to the introduction of the adsorption layer. The adsorption layer on the electrochemical cell is made of an NSR catalyst (Pt-K- Al_2O_3) but is not used in the same way as an NSR catalyst [22]. The NSR catalyst is operated via cyclic switches between lean and rich conditions. NO_x gases are trapped and stored in the form of nitrate under lean condition. The nitrate is then induced to decompose by the switch to rich condition. The released NO_x species are reduced near the trapping sites by the reducing agents. While on the electrochemical cell, there is no gas switch to induce the decomposition of nitrate. The reduction of NO_x is not accomplished near the trapping sites in the adsorption layer, but rather inside the NiO|YSZ layer, which means the stored NO_x species has to be released by the decomposition of the nitrate (KNO_3 in this case) and then diffuse through the adsorption layer to the reaction sites in the NiO|YSZ layer. There are then two steps that likely become rather difficult by depositing an additional YSZ cover layer on the electrochemical cell.

One step is the diffusion of the released NO_x species from the storage sites to the reaction sites. With a YSZ cover layer in between, diffusion is severely impeded or even blocked, which has been demonstrated above. The other step is the decomposition of nitrate on the alkali component (KNO_3), which is the pre-step for NO_x release and, more importantly, regeneration of the NO_x storage sites to trap NO_x continuously. Thus, this step is vital to the overall efficiency of the adsorption layer. Because of missing the strong driving force from gas switch, the decomposition of KNO_3 on the electrochemical cell with the YSZ cover layer can only be driven by the concentration gradient of NO_x species along the adsorption layer, which should be comparatively weak and insufficient. Consequentially, the adsorption layer was incapable of trapping NO_x as effectively as possible.

Correspondingly, by removing the YSZ cover layer the aforementioned two steps can be significantly affected in a positive way. Firstly, the diffusion of NO_x species from the trapping sites to the reaction sites could become unobstructed, which would in turn benefit the adsorption and desorption of NO_x species inside the adsorption layer. Secondly, by removing the YSZ cover layer, the KNO_3 on the trapping sites near the interface between the adsorption layer and the Pt layer was able to be directly decomposed by the negative polarization applied during the operation, which was essentially impossible with the presence of YSZ cover layer because it covered nearly the whole interface between these two layers. According to the research on molten potassium nitrate (KNO_3), the decomposition of KNO_3 starts at a potential of -0.65 V (vs. $\text{Ag}|\text{Ag}^+|\text{NO}_3^-$) on a Pt cathode at $340\text{ }^\circ\text{C}$ [27]. Because the electrochemical cell was polarized under the voltage from -1.5 V to -4.5 V and operated above the melting point of KNO_3 , after removing the YSZ cover layer, the decomposition of KNO_3 on the interface should be easily achieved while the electrochemical cell is running. As a result, the trapped NO_x species could be effectively released and reduced on the reaction sites nearby. The trapping sites of the adsorption layer were able to be quickly regenerated near the interfacial area.

Figure 9 shows the microstructure pictures and EDS analysis results for the interface of the adsorption layer and cathode of S1 and S2 after testing. On S2, many tiny Pt particles accumulated around the Pt surface bared in the adsorption layer, and a thin Pt layer deposited on the open surface of the YSZ nearby. On S1, a similar phenomenon was only observed on the Pt surface exposed to the adsorption layer through a few narrow gaps of the dense YSZ layer. It was reported that in the molten KNO_3 with the cathodic potential increasing to greater than -1.5 V, Pt was extensively oxidized to Pt oxide by the potassium peroxide formed through the accumulation of O^{2-} under continuous KNO_3 decomposition [27]. On a solid state fuel cell, it was reported that Pt could migrate via PtO_2 gas vaporized from the Pt current collector and be deposited around the TPBs (three phase boundaries) because the volatility of PtO_2 was comparatively higher among the Pt species [28, 29]. Therefore, we concluded that the Pt particles accumulation and Pt layer deposition on our cells were caused by redistribution of Pt from the Pt layer through a mechanism of oxidation of Pt by the potassium peroxide, diffusion of gas phase Pt oxide and subsequent decomposition or reduction of Pt oxide to Pt under negative polarization. It must be noted that the oxidation of Pt was not likely due to the reaction between Pt and O_2 or NO because in that case, the oxidation should be much weaker and should only be able to result in an extremely small amount of Pt migration. The intensive redistribution of Pt provided an evidence for the decomposition of KNO_3 by polarization at the interface of the Pt layer and adsorption layer. However, such benefits for KNO_3 decomposition were negligible on the cell with the YSZ cover layer because the electronic insulated layer extensively broke the connection between the Pt layer and adsorption layer.

Moreover, it should be noted that by removing the YSZ cover, there was a possibility for the KNO_3 to be reduced directly to N_2 over the potassium trapping sites adjacent to Pt|YSZ|gas TPBs (three phase boundaries) under negative polarization. The reduction of NO_x through this short reaction path, as shown in equation 9, should be much more efficient than through a long path of KNO_3 decomposition, NO_x diffusion to nano-Ni grains and finally NO_x reduction to N_2 over the Ni grains. Thus, the Pt|YSZ|gas

TPBs could also work as the selective reaction sites for NO_x reduction rather than only being dominated by O_2 reduction if they remained connected with the adsorption layer. This effect might be one of the reasons for the selectivity improvement by removing the YSZ cover layer.

(9)

In summary, these two steps, diffusion of NO_x species and regeneration of NO_x trapping sites, which might limit the performance of the NSR adsorption layer on the electrochemical cell with a YSZ cover layer, were distinctly improved by removing the YSZ cover layer. These improvements gave rise to a much more efficient adsorption layer for NO_x trapping and smoother transport for the NO_x species to the reaction sites. Additionally, a short reaction path of direct reduction of KNO_3 to N_2 might be created at the interface of the Pt layer and adsorption layer. Combined, all of these positive effects could greatly promote the NO_x reduction and make it more pronounced than the increase of O_2 reduction. As a result, selectivity was not decreased, but rather increased by removing the YSZ cover layer.

5. Conclusions

By the optimization of removing the YSZ cover layer, the NO_x removal properties of an electrochemical cell with an adsorption layer was dramatically enhanced, especially under conditions of low voltage, intermediate temperature and high O_2 concentration.

The large increase of NO_x decomposition activity was due to the extensive release of the reaction sites for NO_x reduction by removing the YSZ cover layer. The improvement of selectivity for NO_x reduction in spite of the increase of O_2 reduction was attributed to the interaction of the adsorption layer with the Pt layer and the catalytic layer strongly promoting the reduction of NO_x , which was specified as the following:

1) The diffusion of NO_x species from the adsorption layer into the reaction sites on the NiO|YSZ catalytic layer was greatly enhanced after optimization.

2) The trapping sites of the adsorption layer in the interfacial area of the Pt layer and adsorption layer were quickly regenerated by the decomposition of nitrite under negative potential.

3) The direct reduction of KNO₃ to N₂ could be realized over the Pt|YSZ|gas TPBs adjacent to the NO_x storage sites of the adsorption layer.

Through the structure optimization of removing the YSZ cover layer, an electrochemical cell with an adsorption layer was able to give good performance under harsh conditions, may providing a promising solution for NO_x emission control.

Acknowledgements

The author would like to acknowledge the financial support of the Danish Strategic Research Council under contract no. 09-065186. We are grateful to our colleagues at the Fuel Cell and Solid State Chemistry Division, Risø-DTU for help and discussion.

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Table 1 Selectivity towards N₂ formation on sample S2, without YSZ cover layer, at various O₂ concentrations and 1000 ppm NO with balance Ar under -2.5 V at 450 °C

O ₂ concentrations / %	N ₂ formation (ΔN ₂) /ppm	NO _x decomposition (ΔNO _x) /ppm	N ₂ selectivity (η) ^a / %
0	455	995	91.5
1	403	919	87.7
2	396	899	88.1
4	388	869	89.3
8	411	939	87.5

^a N₂ selectivity (η) is calculated as in equation 3, according to the decomposition reaction of NO_x to N₂ as

showing in equation 4:

(3)

(4)

Figure 1 A sketch of the electrochemical cell with a multilayered cathode and a NO_x adsorption layer for removal of NO_x [9].

Figure 2 Activity of different cells toward NO_x decomposition at various O₂ concentrations and 1000 ppm NO with balance Ar under -2.5 V at 450 °C. (S1: with a YSZ cover layer; S2: without a YSZ cover layer)

Figure 3 Selectivity of different cells toward NO_x decomposition at various O₂ concentrations and 1000 ppm NO with balance Ar under -2.5 V at 450 °C. (S1: with a YSZ cover layer; S2: without a YSZ cover layer)

Figure 4 NO_x removal properties of different cells as a function of temperature under -2.5 V in 1000 ppm NO and 2% O₂ with balance Ar. (S1: with a YSZ cover layer; S2: without a YSZ cover layer)

Figure 5 NO_x removal properties of different cells as a function of voltage at 450 °C in 1000 ppm NO and 2% O₂ with balance Ar. (S1: with a YSZ cover layer; S2: without a YSZ cover layer)

Figure 6 Schematic representation of the reaction sites for NO and oxygen gases in the catalytic layer [8, 12-15].

Figure 7 Microstructure images for the cathodes of different cells before and after testing. The images show: A: S1 cathode before testing, B: S1 cathode after testing, C: S2 cathode before testing, D: S2 cathode after testing (S1: with a YSZ cover layer; S2: without a YSZ cover layer)

Figure 8 Microstructure image and EDS results for the NiO|YSZ catalytic layer of the cell (S1) with a YSZ cover layer after testing.

Figure 9 Microstructure images and EDS results for the Pt layer|adsorption layer interfaces of different cells after testing. (S1: with a YSZ cover layer; S2: without a YSZ cover layer)

Figure 1

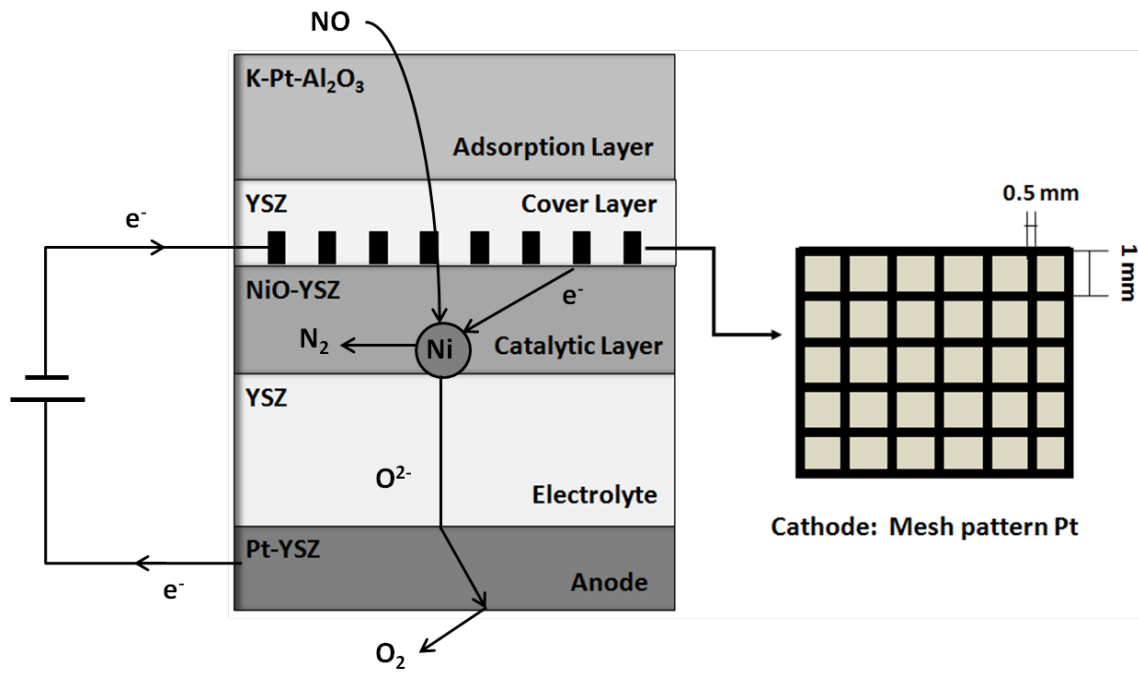


Figure 2

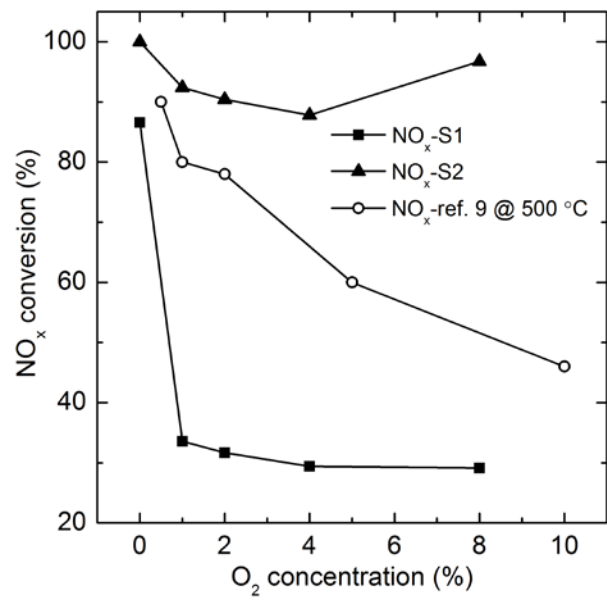


Figure 3

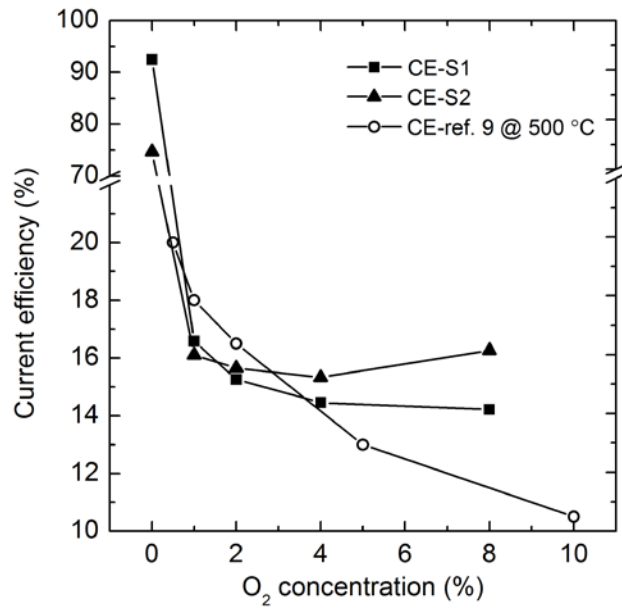


Figure 4

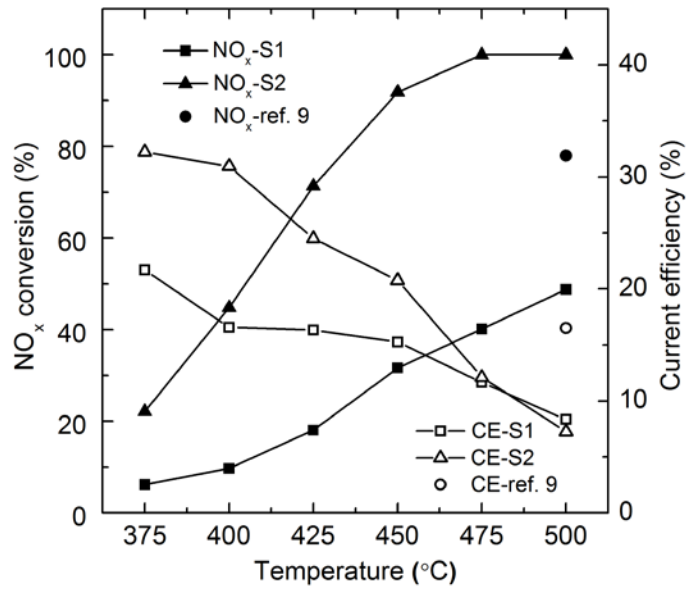


Figure 5

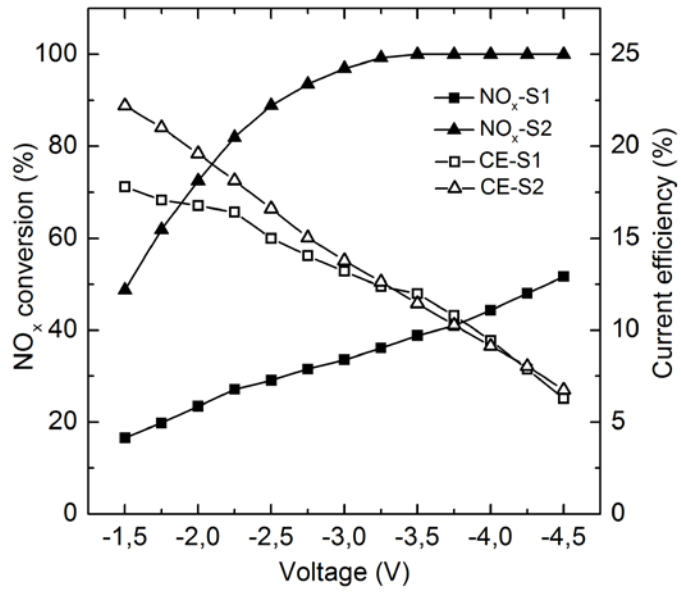


Figure 6

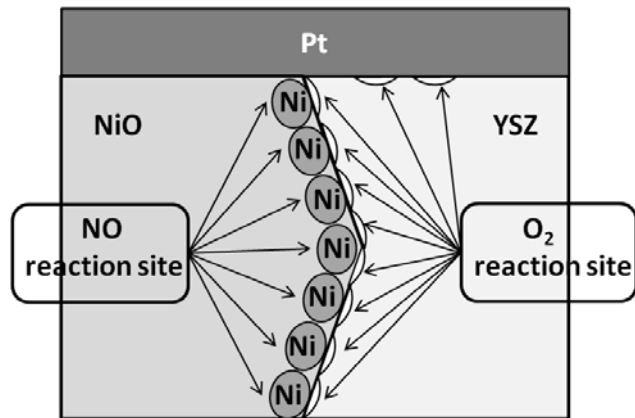


Figure 7

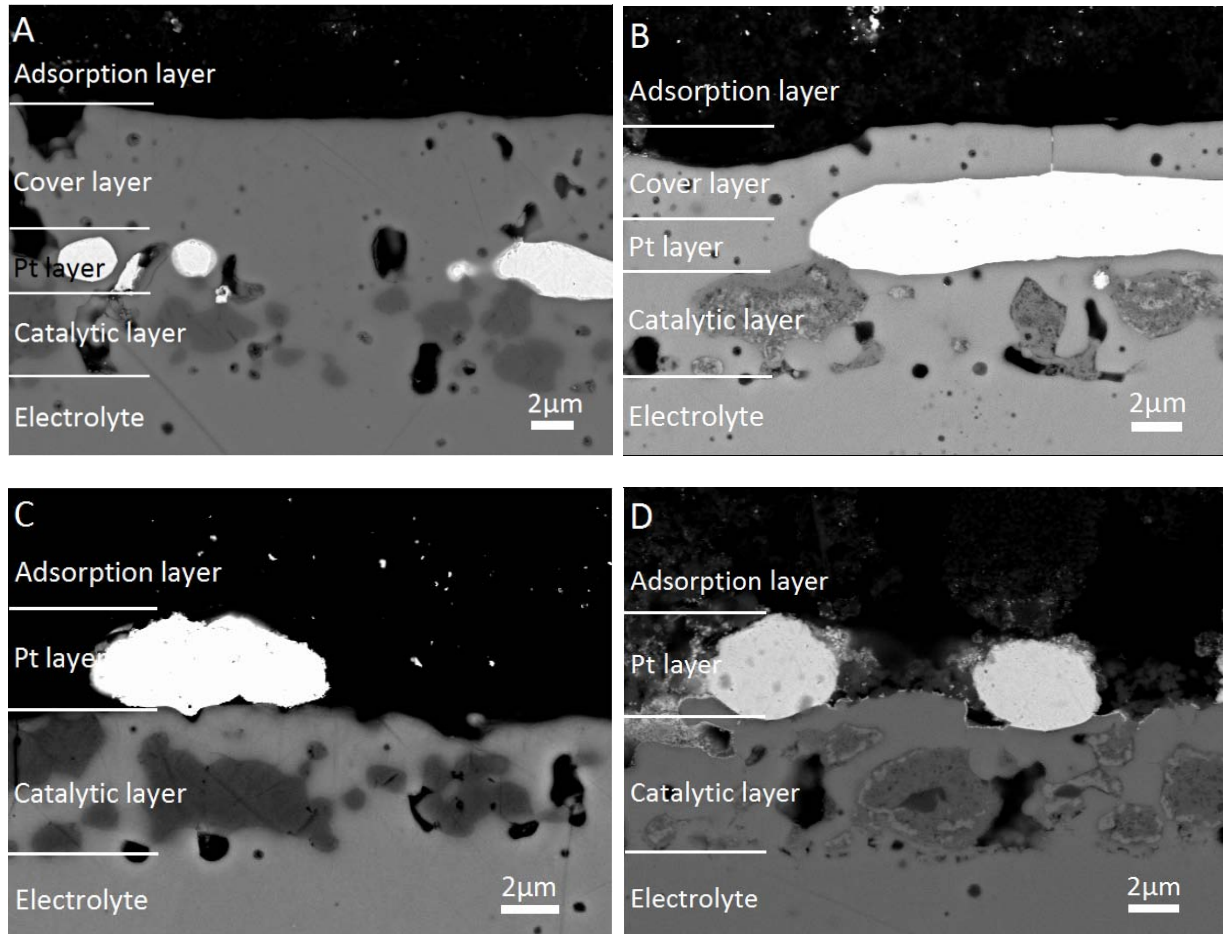


Figure 8

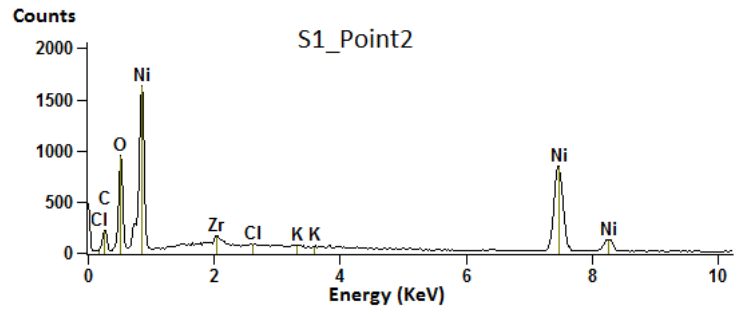
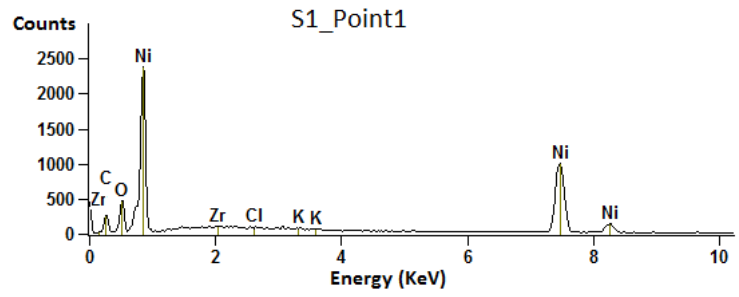
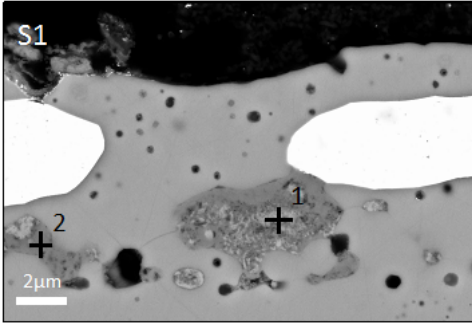


Figure 9

