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## POSTBO, a time dependent one dimensional post-burnout heat transfer code

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Risø - M -

Title and author(s)		Date Maj 1971
<p>POSTBO A time dependent one dimensional post-burnout heat transfer code. by Janos Valko.</p>		Department or group Reactor Physics Department
<p>pages +      tables +      illustrations</p>		Group's own registration number(s)
<p><b>Abstract</b></p> <p>The program described calculates the heat transfer in a boiling water channel up to and after the point where a given burn out condition is reached.</p> <p>Guide to use the program is included together with a test case.</p>		Copies to Standard distribution.
		Abstract to
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## 1. INTRODUCTION.

If the heat input to a boiling water channel exceeds a certain value the heat transfer coefficient between wall and coolant suddenly decreases to fractions of its original value. This phenomenon can be called, among other names, occurrence of burnout. The main characteristic of the burnout region is the absence of good contact between the surface and liquid phase, the latter being present only in the form of droplets dispersed in the steam.

In ref. /1/ a physical model is suggested for the description of burnout region and steady state calculations using the model are compared with experimental values. Ref. /3/ reports on a reproduction of these calculations.

The present work uses the model proposed in ref. /1/ for the calculation of transients in the burnout region. In the following this model is very briefly outlined, and in the subsequent Sections the basic equations, the numerical method and the preparation of data and running of the program are described. A test case is given.

The essence of the proposed model is the assumption that in the burnout region there is no direct heat transfer from wall to droplets since the droplets do not wet the wall (radiation has been ignored). There is, however, an indirect heat transfer, because the droplets evaporate in the superheated steam atmosphere thus removing heat from the steam. This evaporation is enhanced by ventilation due to the relative velocity between steam and droplets. The size of the droplets change by this evaporation, but their number passing a given cross section per second remains the same. The droplets are also accelerated by the drag force of the passing steam. The initial size of the droplets is arbitrarily determined being a somewhat fictitious quantity in the model, as a kind of best fit to experiments.

In the time dependent calculation described below, a tubular channel with no burnout at inlet and/or at zero time is considered and continuity of the appropriate quantities is preserved.

Throughout the report and in the input/output of the program the MKS system of units is used.

## 2. BASIC EQUATIONS.

The flow in the boiling channel is represented by a one dimensional model. We consider the one dimensional mass continuity equation and the equation of energy conservation.

$$\frac{\partial \rho}{\partial t} + \frac{\partial G}{\partial z} = 0 \quad (1)$$

$$\frac{\partial E}{\partial t} + \frac{\partial L}{\partial z} = Q \quad (2)$$

where  $\rho$  is the coolant density,

$G$  is the mass flow rate (or momentum density),

$E$  is the internal energy density,

$L$  is the enthalpy flow rate (or enthalpy flux density),

$Q$  is the incoming heat per unit volume per second.

(In the following we consider an open channel rather than a closed loop therefore, the equation of momentum conservation is not needed.) In the two phase flow we have

$$\rho = \rho_w(1-f) + \rho_s f \quad (3)$$

$$G = v_w \rho_w(1-f) + v_s \rho_s f \quad (4)$$

$$E = \rho_w h_w(1-f) + \rho_s h_s f \quad (5)$$

$$L = \rho_w v_w h_w(1-f) + \rho_s v_s h_s f \quad (6)$$

where  $f$  is the void fraction and indices  $w$  and  $s$  refer to water and steam, respectively. The assumption of  $\partial p / \partial t = 0$  ( $p$  is pressure) has been made and kinetic energy terms have been neglected. In the boiling region

$$d\rho_w = d\rho_s = dh_s = dh_w = 0 \quad (7)$$

however, in the post-burnout region only

$$d\rho_w = dh_w = 0 \quad (8)$$

will be assumed

### 2.1. Region below burnout.

The procedure under burnout closely follows that of ref. /2/. The slip correlation due to Bankoff and Jones (see /2/) is used. Because the present program is directed to post-burnout regions, no subcooled region is included. For determining the point where burnout occurs the critical heat flux from Becker's burnout correlation /4,6/ is compared with the actual heat flux.

### 2.2. Burnout region.

The equations (1) and (2) are now valid with simplifying conditions (8) only, and thereby the number of unknown quantities becomes larger. Additional equations are obtained by formulating the physical model described in Section 1. concerning the formation, acceleration and evaporation of entrained liquid droplets.

The evaporation of water results in a change of droplet diameter,  $D$ .

$$\frac{\partial D}{\partial t} + v_w \frac{\partial D}{\partial z} = - \frac{4 k_s}{\rho_w D} (T - T_s) \cdot F \quad (9)$$

$$\frac{\partial D}{\partial t} + v_w \frac{\partial D}{\partial z} = - \frac{4 D_{\text{diff}}}{\rho_w R T D} (p_s - p) \cdot F \quad (10)$$

Where  $T_s$ ,  $p_s$  are the temperature and pressure inside the droplet,  $k_s$  is the thermal conductivity of steam,

$$D_{\text{diff}} = \frac{k_s (\gamma-1)}{\rho_s R} \quad \text{is mass diffusion coefficient}$$

( $\gamma$  being the index of isentropic expansion), and  $F$  is a ventilation factor

$$F = 1 + 0.276 \text{ Re}_d^{\frac{1}{2}} \left( \frac{\rho_s}{D \rho_w} \right)^{1/3} \quad (11)$$

$$\text{where } \text{Re}_d = \frac{(v_w - v_s) \rho_s D}{\mu_s} \quad (12)$$

is the droplet Reynolds number, and

$\mu_s$  is viscosity of steam.

Saturation condition is assumed inside the droplets thus  $p_s$  and  $T_s$  are related by

$$\frac{p_s}{p_{s1}} = \frac{\lambda}{R} \left[ \frac{1}{T_s} - \frac{1}{T_{s1}} \right] \quad (13)$$

where  $p_{s1}$  and  $T_{s1}$  are a corresponding pair of values in some other saturation state.

The velocity of droplets change according to the following equation

$$\frac{\partial v_w}{\partial t} + v_w \frac{\partial v_w}{\partial z} = \frac{3 C_d \rho_s (v_s - v_w)^2}{4D \rho_w} \quad (14)$$

$$\text{where } C_d = \frac{27}{Re_d} \cdot 0.84$$

Denoting by  $N$  the number of droplets passing through unit cross section area of the channel per second, the following relation holds

$$f = 1 - \frac{ND^2}{6} \frac{1}{v_w} \quad (15)$$

Before the solution of the system of Eqs. (1), (2), (9), (10), (14) can proceed, it should be noted, that

$$\frac{\partial \rho_s}{\partial T} = a - b \cdot \frac{\partial h_s}{\partial T} \quad (16)$$

$$\text{and } \frac{\partial f}{\partial T} = c \frac{\partial D}{\partial T} + g \frac{\partial v_w}{\partial T} \quad (17)$$

where  $a = \frac{\partial \rho_s}{\partial T}$  and  $b = \frac{\partial h_s}{\partial T}$  are table functions,

while  $c$  and  $g$  are obtained by differentiating Eq. (15).

### 2.3. Superheated steam only.

If the water flow rate in the channel becomes negligible due to the evaporation of droplets, a one phase region with superheated steam is considered. Eqs. (1) and (2) are used with steam quantities alone and  $f=1$ , together with (16).

### 2.4. Heat transfer coefficients.

In the boiling region we use Eq. (3, 2) of ref. /2/, while in the burnout region we use the Heiseman correlation following ref. /3/, in the form

$$h = 0.0133 \left( \frac{\rho_s v_w D_e}{\mu_f} \right)^{0.84} \cdot Pr_f^{1/3} \cdot \frac{k_f}{D_e} \quad (18)$$

where  $Pr_f = \frac{\mu_f C_p}{k_f}$ , and  $f$  denotes quantities at temperature  $t_f$ ,  
 $t_f = \frac{T + T_{wall}}{2}$

$D_e$  = channel diameter.

### 1. NUMERICAL METHOD.

The equations are solved by finite differences method. Because of non-linearities nearly all but the simplest differencing schemes lead to implicit systems solved only by iteration. To avoid this further complexity the following scheme is used.

$$\left. \begin{aligned} \frac{\partial Y}{\partial t} &\text{ is approximated by } \frac{Y_k^{j+1} - Y_k^j}{\Delta t} \\ \frac{\partial Y}{\partial z} &\sim \frac{Y_{k+1}^{j+1} - Y_k^{j+1}}{\Delta z} \end{aligned} \right\} \quad (19)$$

$$\text{and } Y \rightarrow Y_k^{j+1}$$

where  $k$  is referring to space mesh  $x_k$ , and  $j$  to time step  $t_j$ .  
 $k = 1$  for all values of  $j$  in the given (time dependent) boundary condition and  $j = 0$  refers to initial values for all  $k$ .

The resulting equations are

$$\Delta c \frac{1}{\Delta t} (D_k^{j+1} - D_k^j) + \Delta g \frac{1}{\Delta t} (v_{w_k}^{j+1} - v_{w_k}^j) - f_{ab} \frac{1}{\Delta t} (h_{s_k}^{j+1} - h_{s_k}^j) - \\ w_7 c \frac{1}{\Delta z} (D_{k+1}^{j+1} - D_k^{j+1}) + (w_7 g + \rho_w (1-f)) \frac{1}{\Delta z} (v_{w_{k+1}}^{j+1} - v_{w_k}^{j+1}) \quad (20)$$

$$+ \rho_s f \frac{1}{\Delta z} (v_{s_{k+1}}^{j+1} - v_{s_k}^{j+1}) + v_s f_{ab} \frac{1}{\Delta z} (h_{s_{k+1}}^{j+1} - h_{s_k}^j)$$

and

$$\Delta e \frac{1}{\Delta t} (D_k^{j+1} - D_k^j) + \Delta g \frac{1}{\Delta t} (v_{w_k}^{j+1} - v_{w_k}^j)$$

$$- (\rho_s f + h_s f_{ab}) \frac{1}{\Delta t} (h_{s_k}^{j+1} - h_{s_k}^j) + q =$$

$$[ \rho_w h_w (1-f) + v_8 g ] \frac{1}{\Delta z} (v_{w_{k+1}}^{j+1} - v_{w_k}^{j+1})$$

$$+ (\rho_s v_s f + v_s h_s f_{ab}) \frac{1}{\Delta z} (h_{s_{k+1}}^{j+1} - h_{s_k}^{j+1}) \quad (21)$$

$$+ \rho_s h_s f \frac{1}{\Delta z} (v_{s_{k+1}}^{j+1} - v_{s_k}^{j+1}) + v_8 c \frac{1}{\Delta z} (D_{k+1}^{j+1} - D_k^{j+1})$$

where

$$v_{w_{k+1}}^{j+1} = \frac{\Delta z}{v_{w_k}^{j+1}} \left( k_1 - \frac{v_{w_k}^{j+1} - v_{w_k}^j}{\Delta t} \right) + v_{w_k}^{j+1} \quad (22)$$

$$D_{k+1}^{j+1} = \frac{\Delta z}{v_{w_k}^{j+1}} \left( k_2 - \frac{D_k^{j+1} - D_k^j}{\Delta t} \right) + D_k^{j+1} \quad (23)$$

The unindexed quantities are to be taken at  $t^{j+1}$ ,  $z_k$ , and the following notations were used

$$A = \rho_w - \rho_s$$

$$B = \rho_w h_w - \rho_s h_s$$

$$w_7 = \rho_s v_s - \rho_w v_w$$

$$w_8 = \rho_s v_s h_s - \rho_w v_w h_w$$

$$k_1 = \frac{\mu_s^{0.84} \rho_s^{0.16} (v_s - v_w)}{\nu^{1.84} \rho_w}^{1.16}$$

$$k_2 = - \frac{1 \cdot k_1}{\rho_w \lambda D_k^{j+1}} (T - T_s) \cdot F$$

In the course of the computation transcendental equations are solved by iteration in connection with the Bankoff Jones slip correlation (for void fraction,  $f$ ), the temperature inside the droplet,  $T_s$ , and the wall temperature satisfying the Heineman correlation.

In the burnout region the droplet acceleration mechanism virtually replaces the slip correlation used before burnout. The water velocity,  $v_w$ , at the point of burnout is the initial value for calculation in the burnout region so to ensure continuity. The adopted numerical scheme, however, seemed to be insufficient to cope with the sudden increase of this velocity, therefore, a somewhat arbitrary limitation had to be used.

There is no obvious way of deciding on the number and size of the droplets at the point of burnout. It seemed advantageous to keep the initial droplet size arbitrarily determined as in the originally proposed model. It should be noted, however, that the relative insensitivity of the results to this initial quantity as observed by 1, 3/ holds only to a much lesser extent if steam quality vs. position downstream from burnout is considered.

The difference scheme used is clearly not unconditionally stable. The condition for stability appears to be in the form of  $\Delta z / \Delta t < \delta$ , where  $\delta$  depends also on the actual problem considered. Physically unrealistic oscillatory tendencies should be regarded as signs of instability.

#### 4. PREPARATION OF DATA AND USE OF THE PROGRAM.

In the present form of the program a round tube is considered with given inside wall heat flux, but this heat flux is assumed to appear immediately as a volume heat flux in the coolant. No pressure loss along the channel is accounted for. A case should be characterised by the geometrical data of the tube, pressure, inlet mass flow rate, inlet quality, as functions of time, and wall heat flux as a function of time and position. The time function can be given as discrete points and / or linear variation between points. The heat flux as a function of position is given by a fourth order polynomial.

To facilitate numerical experiments and series of runs a special routine ALTER is provided which can easily be coded to perform alterations of the data if only some values are to be changed from one case to an other. Data formats are as follow.

##### Card 1. Format (1)A6)

TITLE (I)	Title. (LAST in the first 4 columns terminates the run.)
-----------	--

##### Card 2. Format (I12)

NFULL	Full printout at every NFULL-th time-step, short printout (one line) in between.
-------	--

##### Card 3. Format (E12.5, I12, 3E12.5)

ZLENG	Length of channel (m).
XN	No. of mesh points.
DEQUIV	Equivalent diameter of channel (m).
AREA	Cross section area of channel ( $m^2$ ).
PSYS	Pressure ( $N/m^2$ ).

##### Card 4. Format(2E12.5)

G	Inlet mass flow rate ( $kg/m^2sec$ )
I	Inlet quality

##### Card 5. Format(5E12.5)

Q1	Coefficients for wall heat flux polynomial $Q(K) = Q1 + Q2 z + Q3 z^2 + Q4 z^3 + Q5 z^4$ ( $W/m^2$ )
Q2	
Q3	
Q4	
Q5	

##### Card 6. Format( I12, E12.5)

NTS	No. of time steps. (if zero, no time dependent calculation.)
DT	$\Delta t$ (sec)

##### Card 7. Format(3(E12.5,2I6))

CG(I)	Inlet mass flow rate ( $kg/m^2sec$ ) between time steps LG(I) and NG(I).
LG(I)	(If $LG(I+1) = NG(I)$ , $LG(I+1)$ need not be punched.) If $LG(I+1) > NG(I)$ linear variation between points NG(I) and LG(I+1) is assumed. Maximum number of values is 24. As many cards of type 7. as needed.)
NG(I)	

##### Card 8. Format(3(E12.5,2I6))

IIX(I)	Inlet quality.
LX(I)	(Same rules as for card 7)
MX(I)	

Card 9. Format(5E12.5,2I6)

Q1Q(I)  
Q2Q(I)  
Q3Q(I)  
Q4Q(I)  
Q5Q(I)  
LQ(I)  
HQ(I) }      Coefficients for wall heat flux polynomial.  
  
(Same rules as for card 7.)

Card 10. Format(3I12,3E12.5)

L      Standard ALTER card.  
  
GO TO(1,2,3,...,10),L in ALTER routine.  
  
If L = 0, no alteration is performed and no  
further data are needed.  
  
To be used freely in accordance with the sub-  
section of subroutine ALTER selected by L.  
  
K1  
K2  
A1  
A2  
A3 }     

5. TEST CASE.

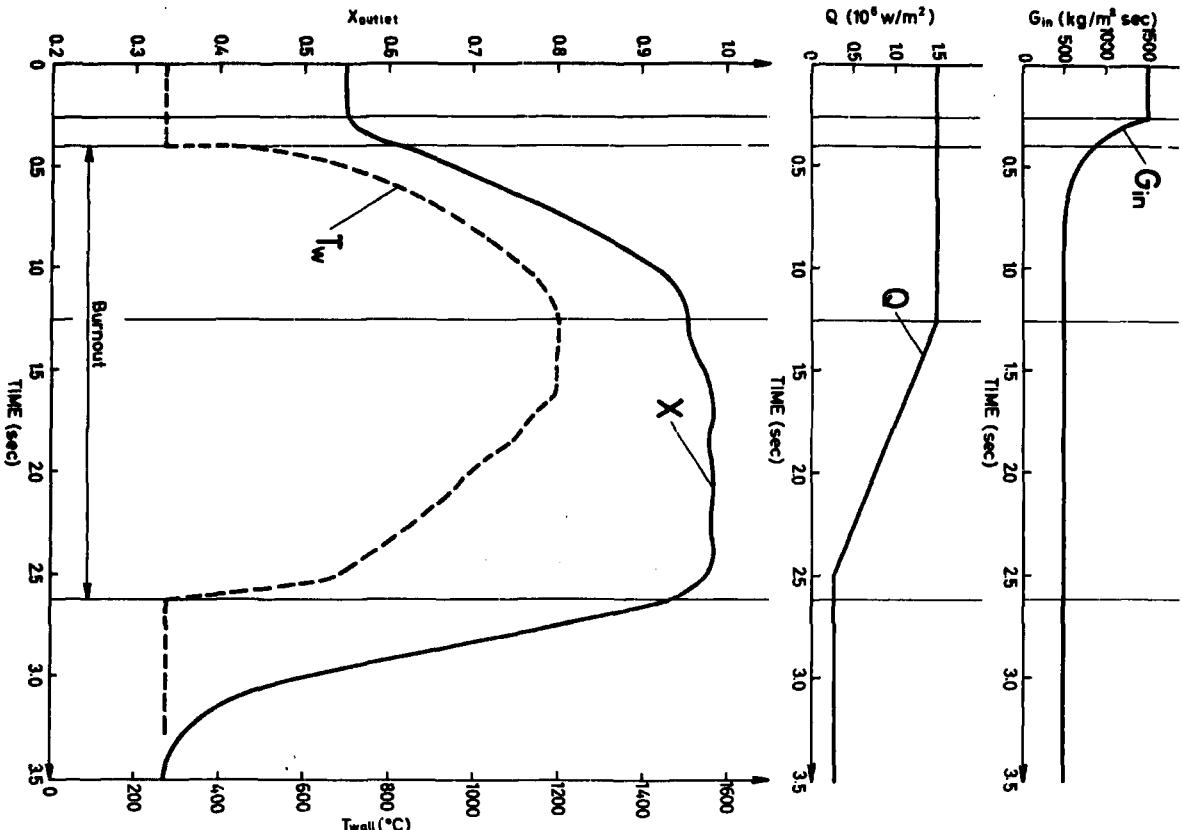
In the POSTBO report testcase there is no burnout in the initially calculated steady state. The disturbances in  $G_{inlet}$  and  $Q$  are shown in Fig. 1. The resulting transient in terms of the parameters,  $x$ , and  $T_{wall}$  at outlet are also shown in Fig. 1.

To save space, Full Printout is at every 10th time step only.

The running time of this case on the BURROUGHS computer was 175 sec. (processing time 119 sec.).

REFERENCES.

1. A.W.Bennett et al. Heat transfer to steam-water mixtures flowing in uniformly heated tubes in which the critical heat flux has been exceeded. AERE-R 5373. (1967).
2. D.Moxon. SLIP - A dynamics programme for the thermal-hydraulic behaviour of boiling water loops. AEEW-R 448 (1968).
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4. K.M.Becker. An analytical and experimental study of burnout conditions in vertical round ducts. AE-178 (1965).
5. M.Hjelm-Hansen. Polynomial approximation of thermodynamic properties of light water. Risø-M-669 (1967).
6. O.Rathmann. Survey of material procedures for light and heavy water in saturated state, for superheated steam of light water and procedures of two phase flow correlations for boiling water reactors. RD-Memo 34 (1970).



PROGRAM POSTBU

POSTBU REPORT TESTCASE (PUMP TRIP - POWER LINEAR DECREASE) 6

PAGE 1

#### INPUT DATA

LENGTH OF CHANNEL (M) 2.0000E 00  
 NO. OF MESH POINTS 41  
 COUPLING DIAMETER (M) 9.0000E-03  
 CRUSH SECT. AREA (M<sup>2</sup>) 6.3600E-05  
 PRESSURE (N/M<sup>2</sup>) 4.9050E 06

#### STEADY STATE CALCULATION

INLET MASS FLOW RATE (KG/M<sup>2</sup>S) 1.5000E 03  
 INLET QUALITY 1.0000E-02  
 COEFFICIENTS FOR HEAT FLUX POLYNOMIAL  
 1.5000E 06  
 0.0000E 00  
 0.0000E 00  
 0.0000E 00  
 0.0000E 00

#### TRANSIENT CALCULATION

NO. OF TIME STEPS 70  
 DELTA T 5.0000E-02  
 INLET MASS FLOW DATA  
 1.5000E 03 0 5 1.1300E 03 0 6 9.4000E 02 0 7  
 8.0000E 02 0 8 7.2000E 02 0 9 6.4000E 02 0 10  
 5.8000E 02 0 11 5.5000E 02 0 12 5.3000E 02 0 13  
 3.5000E 02 0 70  
 INLET QUALITY DATA  
 1.0000E-02 0 70

HEAT FLUX COEFFICIENTS DATA  
 1.5000E 06 0.0000E 00 0.0000E 00 0.0000E 00 0.0000E 00 0 25  
 3.0000E 05 0.0000E 00 0.0000E 00 0.0000E 00 0.0000E 00 50 70









## POSTBO REPORT TESTCASE (PUMP TRIP - POWER LINEAR DECREASE) G

PAGE 10

TIME STEP	TU	TIME (SEC)	0.35000E 01	INLET CONDITIONS	G= 0.50000E 03	X= 0.10000E-01
-----------	----	------------	-------------	------------------	----------------	----------------

POINT	Z (M)	HEAT FLUX (W/M3)	QUALITY	VOID FR.	V=WATER (M/S)	V=STEAM (M/S)	DROP.DIAM. (M)	BURN	T=STEAM (GRAD C)	T=WALL (GRAD C)
1	0.000E 00	1.334E 06	1.000E-02	1.865E-01	7.804E-01	1.079E 00	0.000E 00	F	2.627E 02	2.712E 02
2	5.000E-02	1.334E 08	1.810E-02	2.046E-01	8.802E-01	1.280E 00	0.000E 00	F	2.627E 02	2.712E 02
3	1.000E-01	1.334E 08	2.621E-02	3.568E-01	9.710E-01	1.478E 00	0.000E 00	F	2.627E 02	2.712E 02
4	1.500E-01	1.334E 08	3.432E-02	4.128E-01	1.055E 00	1.673E 00	0.000E 00	F	2.627E 02	2.712E 02
5	2.000E-01	1.334E 08	4.242E-02	4.577E-01	1.132E 00	1.865E 00	0.000E 00	F	2.627E 02	2.712E 02
6	2.500E-01	1.334E 08	5.053E-02	4.948E-01	1.205E 00	2.055E 00	0.000E 00	F	2.627E 02	2.712E 02
7	3.000E-01	1.334E 08	5.863E-02	5.262E-01	1.274E 00	2.242E 00	0.000E 00	F	2.627E 02	2.712E 02
8	3.500E-01	1.334E 08	6.673E-02	5.532E-01	1.339E 00	2.427E 00	0.000E 00	F	2.627E 02	2.712E 02
9	4.000E-01	1.334E 08	7.482E-02	5.767E-01	1.402E 00	2.611E 00	0.000E 00	F	2.627E 02	2.712E 02
10	4.500E-01	1.334E 08	8.292E-02	5.975E-01	1.461E 00	2.793E 00	0.000E 00	F	2.627E 02	2.712E 02
11	5.000E-01	1.334E 08	9.102E-02	6.160E-01	1.518E 00	2.974E 00	0.000E 00	F	2.627E 02	2.712E 02
12	5.500E-01	1.334E 08	9.912E-02	6.327E-01	1.573E 00	3.153E 00	0.000E 00	F	2.627E 02	2.712E 02
13	6.000E-01	1.334E 08	1.072E-01	6.479E-01	1.626E 00	3.331E 00	0.000E 00	F	2.627E 02	2.712E 02
14	6.500E-01	1.334E 08	1.153E-01	6.617E-01	1.677E 00	3.507E 00	0.000E 00	F	2.627E 02	2.712E 02
15	7.000E-01	1.334E 08	1.234E-01	6.744E-01	1.727E 00	3.683E 00	0.000E 00	F	2.627E 02	2.712E 02
16	7.500E-01	1.334E 08	1.315E-01	6.862E-01	1.775E 00	3.858E 00	0.000E 00	F	2.627E 02	2.712E 02
17	8.000E-01	1.334E 08	1.396E-01	6.970E-01	1.821E 00	4.032E 00	0.000E 00	F	2.627E 02	2.712E 02
18	8.500E-01	1.334E 08	1.477E-01	7.072E-01	1.867E 00	4.205E 00	0.000E 00	F	2.627E 02	2.712E 02
19	9.000E-01	1.334E 08	1.558E-01	7.166E-01	1.910E 00	4.377E 00	0.000E 00	F	2.627E 02	2.712E 02
20	9.500E-01	1.334E 08	1.640E-01	7.255E-01	1.953E 00	4.548E 00	0.000E 00	F	2.627E 02	2.712E 02
21	1.000E 00	1.334E 08	1.721E-01	7.339E-01	1.995E 00	4.718E 00	0.000E 00	F	2.627E 02	2.712E 02
22	1.050E 00	1.334E 08	1.802E-01	7.417E-01	2.035E 00	4.888E 00	0.000E 00	F	2.627E 02	2.712E 02
23	1.100E 00	1.334E 08	1.884E-01	7.493E-01	2.074E 00	5.057E 00	0.000E 00	F	2.627E 02	2.712E 02
24	1.150E 00	1.334E 08	1.965E-01	7.563E-01	2.113E 00	5.226E 00	0.000E 00	F	2.627E 02	2.712E 02
25	1.200E 00	1.334E 08	2.048E-01	7.631E-01	2.150E 00	5.393E 00	0.000E 00	F	2.627E 02	2.712E 02
26	1.250E 00	1.334E 08	2.129E-01	7.695E-01	2.187E 00	5.561E 00	0.000E 00	F	2.627E 02	2.712E 02
27	1.300E 00	1.334E 08	2.210E-01	7.756E-01	2.223E 00	5.727E 00	0.000E 00	F	2.627E 02	2.712E 02
28	1.350E 00	1.334E 08	2.293E-01	7.814E-01	2.257E 00	5.893E 00	0.000E 00	F	2.627E 02	2.712E 02
29	1.400E 00	1.334E 08	2.374E-01	7.870E-01	2.292E 00	6.059E 00	0.000E 00	F	2.627E 02	2.712E 02
30	1.450E 00	1.334E 08	2.455E-01	7.923E-01	2.325E 00	6.224E 00	0.000E 00	F	2.627E 02	2.712E 02
31	1.500E 00	1.334E 08	2.537E-01	7.974E-01	2.358E 00	6.389E 00	0.000E 00	F	2.627E 02	2.712E 02
32	1.550E 00	1.334E 08	2.618E-01	8.024E-01	2.390E 00	6.553E 00	0.000E 00	F	2.627E 02	2.712E 02
33	1.600E 00	1.334E 08	2.700E-01	8.071E-01	2.422E 00	6.716E 00	0.000E 00	F	2.627E 02	2.712E 02
34	1.650E 00	1.334E 08	2.782E-01	8.117E-01	2.452E 00	6.879E 00	0.000E 00	F	2.627E 02	2.712E 02
35	1.700E 00	1.334E 08	2.864E-01	8.162E-01	2.482E 00	7.042E 00	0.000E 00	F	2.627E 02	2.712E 02
36	1.750E 00	1.334E 08	2.947E-01	8.205E-01	2.511E 00	7.204E 00	0.000E 00	F	2.627E 02	2.712E 02
37	1.800E 00	1.334E 08	3.030E-01	8.247E-01	2.540E 00	7.366E 00	0.000E 00	F	2.627E 02	2.712E 02
38	1.850E 00	1.334E 08	3.113E-01	8.287E-01	2.567E 00	7.527E 00	0.000E 00	F	2.627E 02	2.712E 02
39	1.900E 00	1.334E 08	3.197E-01	8.327E-01	2.594E 00	7.687E 00	0.000E 00	F	2.627E 02	2.712E 02
40	1.950E 00	1.334E 08	3.281E-01	8.365E-01	2.621E 00	7.848E 00	0.000E 00	F	2.627E 02	2.712E 02
41	2.000E 00	1.334E 08	3.366E-01	8.403E-01	2.646E 00	8.007E 00	0.000E 00	F	2.627E 02	2.712E 02

T-STEP	TIME	INLET G	INLET X	ABOVE BD	MAX X (POINT,X)	MAX TSTEAM (P,TS)	MAX TWALL (P,TW)
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