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Electrochemical Deposition and Dissolution of Aluminum in NaAlCl4 Melts

Influence of MnCl2 and Sulfide Addition

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Conclusions

Pyrolytic graphite electrodes subjected to anodic currents in an electrochemical bath change structurally in both the near-surface and surface layers. Currents of 2 mA/cm² for 2h produces little change in the surface, but after 24h changes in crystallite size and edge-plane density is seen. In contrast, 10 mA/cm² current for 2h produces noticeable changes and after 24h can cause severe damage. The changes in island formation, edge-plane density, defects, and lattice disorder may be detected by Raman spectroscopy and STM. General agreement between the results of both analytical methods indicate that complementary information may be gained from similar studies involving graphitic structures.

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Electrochemical Deposition and Dissolution of Aluminum in NaAICI₄ Melts

Influence of MnCl₂ and Sulfide Addition

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ABSTRACT

Effects of the additives MnCl₂, sulfide, and their combined influence on aluminum deposition and dissolution in NaAlCl₄ saturated with NaCl have been studied by polarization measurements, galvanostatic deposition, and current re-versal chronopotentiometry (CRC). The solubility of MnCl₂ was found to be 0.086 ± 0.006 m/o in the melt at 175°C. Alumi-num-manganese alloys can be deposited in NaAlCl₄ saturated with both NaCl and MnCl₂, resulting in a slight increase in cathodic overpotentials. The codeposition of the binary alloys at current densities below 4 mA/cm² gave rise to formation of deposite so compact that their specific average volumes are of the theoretical value. The content of manganese in the alloy deposits was found to be between 8-11 a/o. It was found that the manganese content in the deposits did not depend on the current efficiency. The presence of sulfide in NaAlCl₄ results in the formation of more spongy deposits at low cur-rent densities, and thus destroys the beneficial effects of MnCl₂ when both additives are present, but prevents formation of dendritic deposits at high current densities. Coulombic ratios of dissolution to deposition were found by CRC measurements to be affected by the nature of the substrate.

Aluminum electrodeposition from AlCl₃-based molten salts has been the subject of many investigators (1). In most cases the electrolysis has been performed in the following ranges: temperature 150°-180°C, current density 20-50 mA/cm², and concentration of AlCl₃ 56-64 mole percent (m/o). These melts have a high vapor pressure which may lead to a high evaporation of AlCl₃. At preferable concentrations, close to 50 m/o AlCl₃, with AlCl₃ bound as the stable complex AlCl4-, smooth aluminum layers could be deposited only in the current density range 2-10 mA/cm². At higher current densities aluminum was deposited in the form of dendrites or very porous powders. Surface-active components such as tetraalkylammonium halides (2-5) and urea (5) have been suggested as electroplating aiding

agents. In the case of rechargeable batteries, the oxidationreduction conditions are more demanding, and slow decomposition can make organic additives unfavorable (6). The effects of many inorganic additives have also been investigated. Among them, BaCl₂ (7) was found to have little effect, whereas $PbCl_2(3, 8)$, $SnCl_2(3, 9, 10)$, $MnCl_2(3, 11-13)$, NaBr, and NaI (3, 14) were found to have some beneficial effects on aluminum deposition. Iron chloride as an impurity in the chemicals, however, might make deposits even worse (15).

In our preliminary investigations (16), the effects of some inorganic additives on the morphology of aluminum were widely investigated. There were: GaCl₃, InCl₃, BiCl₃, HgCl₂, CdCl₂, PbCl₂, SnCl₂, and MnCl₂. Sulfide is of interest because it is present in the electrolyte of a newly developed battery having transition metal sulfides (e.g.,

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 Ni_2S_3) as cathode (17). $MnCl_2$, among others, was found to be the most favorable additive. In the present paper, the influences of manganese chloride, sulfide, and their combination on aluminum deposition and dissolution are presented.

Experimental

Chemicals.—The preparation of distilled aluminum chloride and dried NaCl has been described previously (18). NaAlCl₄ salts prepared from an equimolar mixture of distilled AlCl₃ and dried NaCl of analytic grade were further purified by zone refining (1). Manganese dichloride was prepared from analytical reagent $MnCl_2 \cdot 4H_2O$ by successively passing HCl gas over the solid salt at its dehydration temperatures (106° and 198°C) and then through the melt at 650°C. Finally, the melt was flushed with pure N₂ and filtered. Sulfide in form of NaAlSCl₂ was prepared stoichiometrically at 250°C according to the following equilibrium [19]

$$2NaCl + NaAlCl_4 + 3S + 2Al \rightarrow 3NaAlSCl_2$$

with extra NaAlCl₄ as solvent.

Electrode and cell assembly.—A glassy carbon electrode of 3 mm diam was used as the working electrode in the deposition experiments. Aluminum electrodes of 99.999% purity were used both as counter and reference electrodes. The cell assembly and the preparation of the electrodes were the same as described in the previous paper (1).

Instruments and measurements.—The solubility of manganese dichloride in NaAlCl₄ saturated with NaCl was measured by atomic absorption analysis in combination with visual observation. The melts with excessive MnCl₂ were charged, evacuated, and sealed in Pyrex ampuls. At the test temperatures, the melts were maintained for 100h and then filtered through a built-in ceramic filter by turning the cell upside down. The filtered solidified melts were then analyzed.

Cathodic polarization measurements were carried out by recording a steady-state potential with a X-t recorder after setting a constant current step by step.

The alloy samples were deposited onto a glassy carbon electrode. After deposition, the electrode was carefully removed from the melt, washed initially with dimethyl sulfoxide, then with thionyl chloride (>99%), and finally with distilled water. The composition of aluminum-manganese alloys was analyzed by EDX using a Philips SEM 505 equipped with an EDAX analyzer.

Current reversal chronopotentiometry (CRC) was performed by using a Keithley 224 Programmable Current Source. A Keithley 199 System DMM/Scanner was used to monitor the potential. All measurements were controlled by an IBM-compatible computer with a battery test program developed in this laboratory.

All handlings of chemicals were performed in a dry-airfilled glove box (dew point $< -50^{\circ}$ C). Most of the experiments, deposition, current reversal chronopotentiometry, and polarization measurements were performed in a seethrough oven (1). The deposits were observed by using a Zeiss Jena Technival 2 Stereo Microscope equipped with an Olympus OM-2 SLR camera and a Schott KL 1500 cold light source. The morphology of the deposits was examined by microphotography and the specific volumes of the deposits were measured as averages from the pictures.

In all melts containing $MnCl_2$, saturated concentration of $MnCl_2$ was used except for the melts containing sulfide, in the form of 1.5 m/o NaAlSCl₂. In the latter case the concentration of $MnCl_2$ when present was ~ 0.1 m/o.

Results and Discussion

Solubility of manganese dichloride.—Figure 1 shows the resulting solubility of $MnCl_2$ in the NaCl-saturated NaAlCl₄ melt. The solubilities increase with temperature and the following relationship is obtained by regression analysis

$$S(m/o) = \frac{1}{19.44 - 0.04436t}$$

Fig. 2. Cathodic polarization curves at 175°C on carbon and aluminum

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Fig. 1. Solubility of MnCl₂ in NaAlCl₄ also saturated with NaCl

where t is the temperature in °C. At 175°C the solubility is found to be 0.086 \pm 0.006 m/o MnCl₂. In addition, the solubility of MnCl₂ increases with the addition of sulfide and with increasing acidity of the melt, *i.e.*, with increasing AlCl₃ concentration (not shown in Fig. 1).

Effects of $MnCl_2$ on cathodic overpotentials.—A set of steady-state cathodic polarization curves obtained from NaCl-saturated NaAlCl₄ are shown in Fig. 2. In melts both with and without added $MnCl_2$, overpotentials for aluminum deposition on a glassy carbon electrode are significantly larger than that on an aluminum substrate, showing that aluminum is more easily deposited on its own base than on a foreign substrate. The presence of $MnCl_2$ in the melt results in an increase in the deposition overpotential. Stafford (13) and Hayashi (12) reported a similar increase of deposition overpotential of aluminum upon addition of $MnCl_2$ to the melt.

This phenomenon can be explained by a codeposition of manganese and aluminum. In measurements of the deposition potentials of some metals in molten NaCl-KCl-AlCl₃ at 156°C, Wade *et al.* (20) found, with a platinum reference and a platinum cathode, that the deposition potential for aluminum was -2.02V and for manganese -1.91V, respectively. Later they found, with an aluminum reference and a platinum cathode in the same melt, that the deposition potentials for aluminum and manganese were -0.02 and -0.06V, respectively (21). Such a small difference in deposition potentials clearly presents the possibility of codeposition of manganese and aluminum from the melt.

Analysis of the electrodeposits from NaAlCl₄ saturated with $MnCl_2$ reveals that the content of manganese in the alloy is high, especially when the mole ratio of Mn/Al in the melts is taken into account (approximately 1:10 in deposits compared with 1:500 in melts). The results are tabulated in Table I as a function of current density of deposition. The content of Mn in the deposits varied between 8 and 11 atom percent (a/o) when the current density varied from 0.29 to 2.86 mA/cm², which means that the manganese con-



Table I. Manganese content in electrodeposits from NaAlCl₄ saturated with NaCl and MnCl₂ at 175°C.

Current density (mA/cm ²)	Mn content (a/o Mn)
0.29	9.1 ± 0.5
0.43	7.8 ± 0.5
1.43	10.5 ± 1.5
2.86	8.3 ± 1.0

tent in the deposits is not very dependent on the current density.

Smith et al. (11) reported that binary aluminummanganese alloy deposits containing up to 28 a/o Mn could be obtained from chloroaluminate melts containing small amounts of MnCl₂. The manganese content of the electrodeposits was found to increase with increasing MnCl₂ and decreasing AlCl₃ concentration in the melts. Hayashi (12) found a similar increase in the manganese concentration of manganese-aluminum codeposits as well as an increase in the cathodic polarization when increasing the MnCl₂ concentration in the melt. The structures of the electrodeposited aluminum-manganese alloys have been investigated (22), and it was shown that the lowmanganese alloys consisted entirely of a supersaturated solid solution of manganese in aluminum, whereas the high-manganese alloys were comprised of two phases, a supersaturated solid solution and the intermetallic compound, MnAl₆, well known from the aluminum-manganese phase diagram (23). The results by Stafford (13) showed that the manganese content of the electrodeposited binary alloys was dependent upon deposition potential as well as the relative concentrations of Al₂Cl₇⁻ and Mn²⁺ ions in the melt.

Morphology of deposits.—Figure 3 shows the observed different morphologies that aluminum can have when it is deposited from NaAlCl₄ saturated with NaCl (first column, a-d), with added $MnCl_2$ (second column, e-h) at different



Fig. 3. Morphologies of electrodeposits achieved at current densities of 0.29 (a, e), 5.0 (b, f), 21.4 (c, g), and 42.9 mA/cm² (d, h) at 175°C; (a-d) in NaAlCl₄ (saturated with NaCl) (e-h) in NaAlCl₄ (saturated with NaCl) + MnCl₂(s).



Fig. 4. Morphologies of electrodeposits achieved at current densities of 0.29 (i, m), 5.0 (j, n), 21.4 (k, o), and 42.9 mA/cm² (1, p) at 175°C; (i-1) in NaAlCl₄ + 1.5 m/o NaAlSCl₂, (m-p) in NaAlCl₄ + 1.5 m/o NaAlSCl₂ + MnCl₂ (\sim 0.1 m/o).

current densities. Similarly, Fig. 4 shows the observed different morphologies that aluminum can have when it is deposited from NaAlCl₄ containing sulfide (first column, i-1) and containing both sulfide and $MnCl_2$ (second column, m-p) at different current densities.

It was found previously (1), at lower current densities (below 0.7 mA/cm²), that many precursors for aluminum dendrites were formed initially and spongy deposits were obtained finally due to difficulties in the electronucleation process of deposition (Fig. 3a). In the intermediate range of current densities $(1.0 < i < 10 \text{ mA/cm}^2)$, a smooth layer of aluminum deposits was achieved having *ca*. 5 times larger volume than the theoretical value (Fig. 3b). At higher current densities (>15 mA/cm²) dendritic or porous deposits often appeared (Fig. 3c and d).

With addition of a small amount of manganese chloride, the precursors and finally the spongy deposits could be completely avoided, and perfectly dense deposits were obtained at lower current densities (Fig. 3e). Smooth layers of deposits were obtained at current densities up to 20 mA/cm² (Fig. 3f); however, at current densities above ca. 25 mA/cm², dendritic or porous deposits were formed (Fig. 3g and h). These dendritic deposits seemed to be different in appearance from those obtained from pure NaAlCl₄. As previously demonstrated (1), spongy deposits of aluminum formed at lower current densities can be attributed to the slow rate of electronucleation involved in the deposition process. When MnCl₂ additions are present, codeposition of Al and Mn apparently promotes the nucleation, and therefore the formation of such spongy deposits is avoided

In the melt containing $1.5 \text{ m/o} \text{ NaAlSCl}_2$, aluminum deposits were even more spongy at lower current densities (0.285 mA/cm², Fig. 4i). This suggests that the nucleation process of aluminum deposition is more difficult in this case than in pure NaAlCl₄ melts. An interesting finding is that smooth aluminum deposits, though very porous in most cases, were formed at higher current densities (Fig. 4j and k), at which dendritic deposits would be formed from

NaAlCl₄ independent of any $MnCl_2$ addition. No dendrites were formed at current densities as high as 42.9 mA/cm² (Fig. 41).

The combination of $MnCl_2$ and sulfide as additives to NaAlCl₄ melts resulted in a slight improvement in the spongy deposits at lower current densities (Fig. 4m) compared with those from NaAlCl₄ with (Fig. 4i) or without (Fig. 3a) sulfide. However, the deposits were far from as smooth and condensed as the deposits from NaAlCl₄ containing only $MnCl_2$ (Fig. 3e). Hence, the presence of sulfide in the melt destroys the effect of manganese chloride. At higher current densities no dendritic deposits were formed (Fig. 4o and p).

Figure 5 shows specific average volumes of electrodeposits obtained from the NaCl-saturated NaAlCl₄ without any additives compared with melts containing manganese chloride, sulfide, and both manganese chloride and sulfide additives. Each point is the average value of at least two measurements. At low current densities, the high values of specific volumes of deposits from the NaAlCl₄ melts and melts containing sulfide indicate the formation of spongy deposits. The volumes of deposits from melts saturated with MnCl₂ were close to the theoretical value, indicating formation of perfectly compact deposits of aluminummanganese alloys.

At intermediate current densities, the volumes of deposits from NaAlCl₄ melts and melts containing sulfide and sulfide-manganese chloride in combination were approximately equal and were about five times larger than the theoretical value. Deposits from the melts containing only manganese chloride were significantly more compact, especially at lower current densities.

Current reversal chronopotentiometry.—Current reversal chronopotentiometry was used to investigate the reversibility of aluminum deposited in NaAlCl₄ melts with addition of MnCl₂, sulfide, and their combination. 1 C/cm² was applied in each deposition. In order to study the effects of the deposition current on the reversibility of aluminum deposition, an arbitrary constant current of 0.714 mA/cm² was used to reoxidize the aluminum deposited at different current densities. A set of chronopotentiograms at a current density of 0.714 mA/cm² for both deposition and reoxidation is shown in Fig. 6.

As can be seen from Fig. 6, overpotentials of reoxidation are much higher for the aluminum-manganese alloy than for pure aluminum. When aluminum or aluminummanganese alloy was being reoxidized upon reversal current, the electrode potential was almost constant or increased slightly. When this process was complete, the potential rose rapidly to that of chlorine evolution (at *ca.* 2.3V *vs.* aluminum reference). The transition time was determined from the potential-time curves by extrapolation of the maximum slope at the completion of reoxidization. The coulombic efficiency (charge ratio of reoxidization to deposition) was thus calculated, as shown in Fig. 7.



Fig. 6. Current reversal chronopotentiograms on a glassy carbon electrode at 0.714 mA/cm² for both deposition and oxidation. Vertical dash line indicates the reversing of current. (a) in NaAlCl₄, (b) in NaAlCl₄ + MnCl₂(s), (c) in NaAlCl₄ + 1.5 m/o NaAlSCl₂, and (d) in NaAlCl₄ + 1.5 m/o NaAlSCl₂ + MnCl₂ (\sim 0.1 m/o).

All values of coulombic efficiencies were less than unity. This has earlier, in both NaCl-AlCl₃ (24) and organic aluminum chloride (25-27), been attributed to the corrosion of aluminum by impurities. In the present study, it was found that this phenomenon was mainly dependent on the interfacial properties between deposits and the electrode, *i.e.*, the adhesion of deposits to the substrate. Through a microscope, it was observed that some forms of small aluminum pieces fell off into the melt during reoxidization, and small aluminum particles remained on the electrode surface during chlorine gas evolution, apparently not adhering well to the electrode.

It can be seen from Fig. 7 that coulombic efficiencies of more than 95% were obtained at low deposition current densities in NaAlCl₄ melts both with and without MnCl₂. The coulombic efficiency decreased with increasing deposition current density, more significantly in the melt containing manganese dichloride than in the pure NaAlCl₄ melt. Addition of sulfide resulted in much lower coulombic efficiencies (with a maximum at a current density of ca. 0.7 mA/cm²). The addition of MnCl₂ to the melts already containing sulfide considerably improved the cou-



Fig. 5. Specific average volume of deposits, in mm³/C, on a glassy carbon electrode as a function of current density.



Fig. 7. Coulombic efficiency as a function of current density of deposition. Current density of reoxidation: 0.714 mA/cm². Temperature: 175°C.

lombic efficiencies, although not as much as without sulfide. An investigation on the mechanism, using several different substrates such as copper, tungsten, nickel, etc., is underway (28).

Conclusions

The solubility of manganese dichloride was found to be 0.086 ± 0.006 m/o in NaAlCl₄ saturated with NaCl at 175°C. The addition of such a small quantity of MnCl₂ to NaAlCl₄ melts saturated with NaCl leads, upon electrolysis, to a codeposition of aluminum-manganese binary alloys, resulting in a formation of smooth, compact deposits at low current densities, below 6 mA/cm². Dendritic deposits of the alloy were formed at high current densities, above 25 mA/cm².

The presence of sulfide in NaAlCl₄ melts tends to cause spongy deposits, and therefore, when both additives are present, destroys the beneficial effects of MnCl₂ at lower current densities. At high current densities, however, it prevents dendrite formation.

Cathodic overpotentials of the codeposition of Al-Mn alloys are slightly higher than that of pure aluminum deposition, and overpotentials are ca. 60 mV higher at a glassy carbon electrode than at an aluminum electrode in melts both with and without MnCl₂.

Coulombic efficiencies by CRC measurements are high at lower current densities but decrease with increasing current density of deposition. In the melts containing sulfide, coulombic efficiencies are extremely low. In all cases, coulombic efficiencies were found to be less than unity, mainly due to the bad adhesion of the deposits to the substrate. Further investigations are planned by using different substrates.

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Flat porous electrodes are presently used in fuel cells, but they require careful porosity control, resulting in a complex production process. The development of a new type of electrode with a simpler structure as well as a larger effective area would be desirable.

This study proposes a three-phase fluidized bed electrode that can be used in simple electrode alkaline fuel cells. There are several publications on fluidized bed electrodes that combine two liquid phases or a solid and a liquid phase (1, 2). However, we have not found any publication on three-phase fluidized bed electrodes that combine solids, liquids, and gases. The electrode structure consists of a glass tube containing an electrolytic solution and catalytic particles. Hydrogen or oxygen gas is introduced into the tube from the bottom, while the solution and catalyst are agitated in the fluidized bed. Under these conditions,