

## Article

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# Antibacterial Electrospun PVA/Enzymatic Synthesized Poly(catechol) Nanofibrous Mid- Layer Membrane for Ultrafiltration

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**KEYWORDS:** poly(vinyl alcohol), catechol, silver nitrate, electrospinning, membrane,  
water filtration.

**ABSTRACT:** Two different nanofibrous antibacterial membranes containing enzymatically synthesized poly(catechol) (PC) or silver nitrate (AgNO<sub>3</sub>, positive control) blended with poly(vinyl alcohol) (PVA) and electrospun onto a poly(vinylidene fluoride) (PVDF) basal disc to generate thin-film composite mid-layers were produced for water ultrafiltration applications. The developed membranes were thoroughly characterized in terms of morphology, chemical composition and general mechanical and thermal features, antimicrobial activity and ultrafiltration capabilities. The

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2  
3 electrospun blends were recognized as homogeneous. Data revealed relevant  
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5 conformational changes in the PVA side groups, attributed to hydrogen bonding, and  
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7 high thermal stability and residual mass. PVDF+PVA/AgNO<sub>3</sub> membrane displayed  
8  
9 100% growth inhibition of both Gram-positive and Gram-negative bacteria strains,  
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11 despite the wide range of fiber diameters generated, from 24 to 125 nm, formation of  
12  
13 numerous beads and irregular morphology. The PVDF+PVA/PC membrane showed a  
14  
15 good growth inhibition of *Staphylococcus aureus* (92%) and revealed a smooth  
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17 morphology, with no relevant bead formations and diameters ranging from 68 to 131  
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19 nm. The ultrafiltration abilities of the membrane containing PVA/PC were tested in a  
20  
21 dead-end high-pressure cell (4 bar) using a reactive dye in distilled water and seawater.  
22  
23 After 5 cycles, a maximum rejection of  $\approx 85\%$  with an average flux rate of  $70 \text{ L m}^{-2} \text{ h}^{-1}$   
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25 for distilled water and  $\approx 64\%$  with an average flux rate of  $62 \text{ L m}^{-2} \text{ h}^{-1}$  for seawater were  
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27 determined with an overall salt rejection of  $\approx 5\%$ .  
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## 35 1. INTRODUCTION

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38 Catechols are small colorless molecules usually applied for the synthesis of food,  
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40 pharmaceuticals or agrochemical ingredients. They occur naturally in trace amounts in  
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42 fruits or vegetables but can also be found in insects, teas and even poisons. Catechols  
43  
44 are versatile electroactive species that undergo a variety of chemical reactions, and are  
45  
46 capable of establishing interactions with both organic and inorganic substrates.  
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48 Catechols possess a pivotal role as adhesive interfaces and effective anchoring groups,  
49  
50 giving rise to a large range of polymeric materials with fascinating structures and  
51  
52 properties.<sup>1-2</sup> Most importantly, catechols have shown to display antibacterial and  
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54 antifungal effects against various microorganisms.<sup>3-4</sup>  
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3 For many years, the polymeric synthesis of phenol-derived compounds, including  
4 catechol, was a challenge and only accomplished through the conventional  
5 formaldehyde-based high-temperature process. Enzymatic polymerization has provided  
6 a new strategy for the synthesis of phenols and aromatic amine-based polymers.<sup>5</sup>  
7 Enzymatic polymerization is defined as “the *in vitro* polymerization of artificial  
8 substrate monomers catalyzed by an isolated enzyme via non biosynthetic (non  
9 metabolic) pathways”.<sup>1, 6</sup> The enzymes laccase, lipase and peroxidase have been  
10 recognized as capable of catalyzing phenols, including catechol into poly(catechol)  
11 (PC).<sup>7-10</sup> This strategy possesses many advantages over conventional processes, as  
12 requiring only mild reaction conditions (e.g. temperature, pressure and pH) and being  
13 non-toxic.<sup>5, 11-12</sup> Although the literature has pointed some of the uses for PC,<sup>1</sup> its  
14 application in nanofibrous porous supports for thin-film composite (TFC) membranes  
15 for water ultrafiltration applications has not yet been exploited.

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33 TFC asymmetric membranes are composed of a top selective layer and a bottom  
34 porous substrate that can be independently controlled and optimized to achieve desired  
35 selectivity and permeability, while offering excellent mechanical strength. Over the  
36 years, a large variety of polymers has been successfully used as porous supports for  
37 TFC membrane fabrication.<sup>13</sup> Poly(vinylidene fluoride) (PVDF), a fluorinated-derived  
38 polymer with great chemical, thermal, and mechanical stabilities, has been a material of  
39 choice. Still, the use of PVDF as support layers in TFC membranes comes with  
40 limitations, namely is its high surface hydrophobicity, which complicates adhesion of  
41 other materials on the surface.<sup>14</sup> Modification of the PVDF support layer is therefore  
42 recommended. In the present research, enzymatically synthesized PC blended with  
43 poly(vinyl alcohol) (PVA) were electrospun onto a PVDF basal membrane to overcome  
44 this limitation.

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3 Electrospinning is broadly used for polymer fiber production of thinner diameters,  
4 from 2 nm to several micrometers.<sup>15</sup> It is a simple and straightforward method, in which  
5 a single polymer or polymeric blend is pumped at constant rate through a syringe or  
6 capillary tube connected to a high DC voltage source.<sup>16-18</sup> PVA membranes produced by  
7 electrospinning are very common. As a biodegradable, non-toxic or non-carcinogenic,  
8 biocompatible synthetic polymer with good mechanical properties, PVA is desirable for  
9 many applications.<sup>19-22</sup> Also, PVA can reduce the repulsive forces within the charged  
10 polymer solution to facilitate fiber electrospinning.<sup>23</sup> Its flexibility and swelling  
11 capability in aqueous environments are in particular cases of great interest, however  
12 may also represent a downside, affecting its stability. Blends of PVA with other  
13 polymers are, therefore, frequent.<sup>24-26</sup> Son et al. has shown PVA and catechol, oxidized  
14 and polymerized with amines in the form of polydopamine, to work in harmony to  
15 improve the electrospun surfaces stability as well as to increase binding of silver  
16 nanoparticles (Ag NPs) and, with that, the surface antimicrobial features.<sup>27</sup> To the  
17 authors knowledge, the PVA and PC potentialities have yet to be explored in the form  
18 of an ultra-thin and defect-free selective barrier for TFC membranes.

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39 In the present investigation, PVDF basal membranes were electrospun with PVA/PC  
40 blends to generate a mid-layer nanofibrous porous support for TFC membranes used in  
41 water ultrafiltration applications. PC was synthesized by enzymatic polymerization  
42 catalyzed by laccase. This is the first time an enzymatically synthesized PC is used in  
43 the production of electrospun nanofibers. A nanofibrous antibacterial membrane  
44 containing silver nitrate (AgNO<sub>3</sub>) blended with PVA was also produced and used as  
45 positive control. The two membranes were thoroughly characterized in terms of  
46 morphology, chemical composition and general mechanical and thermal features, using  
47 scanning electron microscopy (SEM), energy-dispersive X-ray spectroscopy (EDS), X-  
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3 ray photoelectron spectroscopy (XPS), dynamic mechanical analysis (DMA),  
4 thermogravimetry (TGA), and differential scanning calorimetry (DSC). The membrane  
5 antimicrobial properties were evaluated against *Escherichia coli* (*E. coli*) and  
6 *Staphylococcus aureus* (*S. aureus*) bacteria. The PVDF+PVA/PC ultrafiltration  
7 capabilities (e.g. flux) were established with distilled water (dH<sub>2</sub>O) and synthetic  
8 seawater.  
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## 20 2. EXPERIMENTAL SECTION

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23 **2.1. Materials.** PVA 87-90 % hydrolyzed (wt 30,000-70,000), AgNO<sub>3</sub> and catechol  
24 were purchased from Sigma Aldrich (USA), and the PVDF basal disc filter (5 cm in  
25 diameter and porosity of 0.02 μm) from Sterlitech (USA). Laccase from  
26 *Myceliophthora thermophila* (NS51003, Novozymes, Bagsvaerd, Denmark) was kindly  
27 provided by Professor Diego Moldes' Group from University of Vigo, Spain. Bacteria  
28 were acquired from the American Type Culture Collection (ATCC) company: *E. coli*  
29 (ATCC 25922) and *S. aureus* (ATCC 6538). The remainder materials were all  
30 purchased from Sigma-Aldrich and used without further purification.  
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42 **2.2. Enzymatic Polymerization Catalyzed by Laccase.** PC was obtained from a 50  
43 mM catechol solution incubated with 5 mg of laccase at 0.5 U/mg. Polymerization  
44 reaction was carried out overnight in a stirring system (0.1 M acetate buffer, pH 5.0) at  
45 50° C, as described in<sup>28</sup>.  
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52 **2.3. Electrospinning.** The electrospinning experiments were performed in a Nanon  
53 NF-103 (MECC, Japan) at room temperature (RT), using a 10 mL syringe with a needle  
54 of 0.5 mm inner diameter. An electric field of 27 kV was applied to all solutions. The  
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3 feed rate was 0.2 mL/h. The nanofibres were deposited on a collecting plate at the  
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5 controlled distance of 120 mm. The solutions viscosity and conductivity were measured  
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7 using a viscometer (Fungilab Smart Series Rotational Viscometer) and a  
8  
9 conductivimeter (Thermo Scientific), respectively. Solutions containing AgNO<sub>3</sub> were  
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11 prepared in a 60/40 ratio of PVA (12%, w/w) and AgNO<sub>3</sub> (1.5%, w/w) in dH<sub>2</sub>O, while  
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13 the solution containing catechol was prepared by dissolving PVA (12%, w/w) directly  
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15 in the enzymatically synthesized PC solution (60/40 ratio). The mixed solutions were  
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17 electrospun onto a PVDF basal microfiltration disc filter. Since PVA has poor stability  
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19 in water, the electrospun membranes were further cross-linked by glutaraldehyde (GA)  
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21 to maintain its morphology and prevent dissolution. GA has two active sites and can  
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23 promote intramolecular and intermolecular nonspecific bindings between PVA  
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25 molecules, decreasing membranes hydrophilicity without the need of thermal treatment.  
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27 Electrospun membranes were immersed in a 5 mM GA and 0.01 N HCl water solution  
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29 for 6 h, washed several times, and kept in water until use.<sup>29</sup> After electrospinning, the  
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31 porosity was calculated through the relationship between volume and density. The used  
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33 equation was  $P = (1 - (\rho/\rho_0))$ , where P is the porosity,  $\rho$  is the density of the electrospun  
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35 membrane, and  $\rho_0$  is the density of the bulk polymer.  
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42 **2.4. Scanning Electron Microscopy (SEM) and Energy Dispersive X-ray**  
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44 **Spectroscopy (EDS).** Morphology analyses of the prepared nanofibres were carried out  
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46 with an Ultra-High Resolution Field Emission Gun SEM, NOVA 200 Nano SEM, FEI  
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48 Company. Secondary electron images were acquired with an acceleration voltage of  
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50 5 kV, while backscattering electron images were obtained with an acceleration voltage  
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52 of 15 kV. To improve conductivity, the tested surfaces were covered with a film of Au-  
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54 Pd (80-20 weight %) using a high-resolution sputter coater, 208HR Cressington  
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56 Company, coupled to a MTM-20 Cressington high resolution thickness controller. The  
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3 membranes atomic compositions were examined with an EDS (coupled to the SEM  
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5 equipment) using an EDAX Si(Li) detector and an acceleration voltage of 5 kV.  
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8 **2.5. X-Ray photoelectron spectroscopy (XPS).** XPS measurements were performed  
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10 on a VG Scientific ESCALAB 200A equipment with PISCES software for data  
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12 acquisition and analysis. For analysis, an achromatic Al (K $\alpha$ ) X-ray source operating at  
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14 15 kV (300 W) was used, and the spectrometer, calibrated with reference to Ag 3d $_{5/2}$   
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16 (368.27 eV), was operated in CAE mode with 20 eV pass energy. Data acquisition was  
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18 conducted with a pressure lower than 1E-6 Pa. Deconvolution into sub-peaks was  
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20 performed by least-squares peak analysis software, XPSPEAK version 4.1, using the  
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22 Gaussian/Lorentzian sum function and Shirley-type background subtraction (or linear  
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24 consideration of the data).  
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29 **2.6. Thermogravimetric Analysis (TGA).** TGA was carried out on a Pyris 1 TGA  
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31 (Perkin Elmer, USA) according to the standard ISO 11358:1997(E). The TGA trace was  
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33 obtained in the range of 40-900 °C under nitrogen atmosphere, with a flow rate of  
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35 20 mL/min and heating rate of 10 °C/min. Samples were dried at 60 °C for 1 h and  
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37 placed into a porcelain sample pan before analysis. Data was plotted as weight  
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39 (percentage) vs. temperature.  
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43 **2.7. Differential Scanning Calorimeter (DSC) Analysis.** DSC was carried out on a  
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45 Power compensation Diamond DSC (Perkin Elmer, USA) with an Intracooler ILP,  
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47 based on the standards ISO 11357-1:1997, ISO 11357-2:1999 and ISO 11357-3:1999.  
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49 Samples were dried at 60 °C for 1 h and placed in an aluminum sample pan before  
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51 testing. The analysis was carried out in nitrogen atmosphere with a flow rate of  
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53 20 mL/min and heating rate of 10 °C/min. The thermogram was obtained in the range of  
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55 -50 °C to -200 °C. This upper limit for DSC was selected since this was the temperature  
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3 in which all the tested polymers started decomposition, as seen by TGA. Data was  
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5 plotted as heat flow vs. temperature.  
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8 **2.8. Dynamic Mechanical Analysis (DMA).** DMA analysis was performed on a  
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10 DMA 8000 (Perkin Elmer, USA) in tension mode according to an internal method  
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12 based on standard ASTM D4065-01. The temperature dependence of the storage  
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14 modulus and loss tangent was measured from -50 to 120 °C at a 2 °C/min rate.  
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18 **2.9. Antimicrobial Testing.** The antimicrobial activity was assessed according to the  
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20 standard shake flask method (ASTM-E2149-01). This method provides quantitative  
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22 data for measuring the reduction rate in number of colonies formed, converted to the  
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24 average colony forming units per milliliter of buffer solution in the flask (CFU/mL). *E.*  
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26 *coli* (ATCC 25922) and *S. aureus* (ATCC 6538) were expanded from a single colony.  
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28 The culture was then inoculated 24 h in sterile nutrient broth (NB, Sharlab, Spain) at 37  
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30 °C and 230 rpm. The inoculated bacterial culture was harvested by centrifugation and  
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32 washed twice with a 0.9 % solution of NaCl at pH 6.5. Thereafter, the samples were  
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34 incubated with 5 mL of bacterial suspension (previously diluted 10 fold with NaCl 0,9  
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36 % pH 6.5) at 37 °C and 100 rpm. For determination of the inoculum cell density the  
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38 suspensions were withdrawn before contact with the sample and after 1 h contact. The  
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40 withdrawn suspensions were serially diluted in sterile buffer solution, plated on a plate  
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42 count agar (VWR) and further incubated at 37 °C for 24 h to determine the number of  
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44 surviving bacteria. Antimicrobial activity, defined by equation (1), was reported in  
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46 terms of percentage of bacteria reduction calculated as the ratio between the number of  
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48 surviving bacteria before and after the contact with the electrospun membranes:  
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55 Bacteria reduction (%) =  $\left[ \frac{A-B}{A} \right] \times 100,$   
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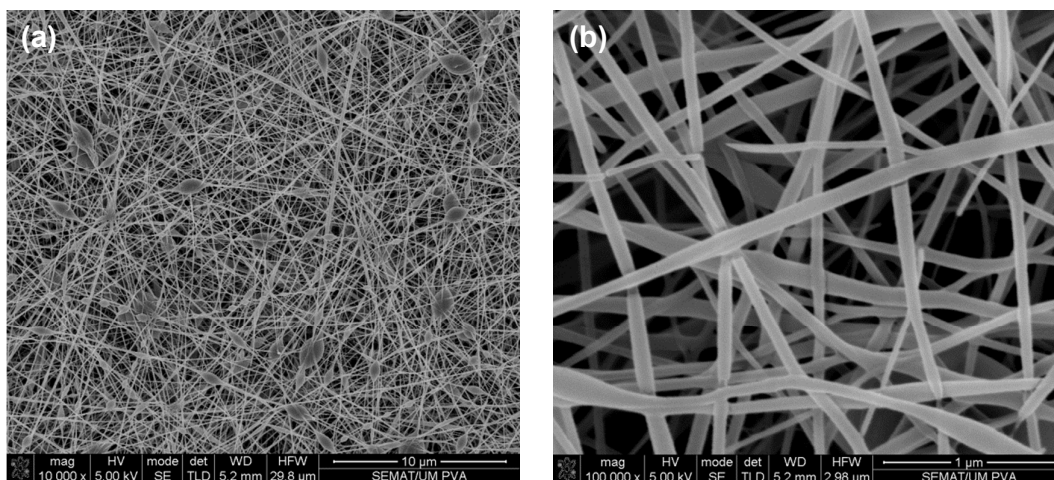
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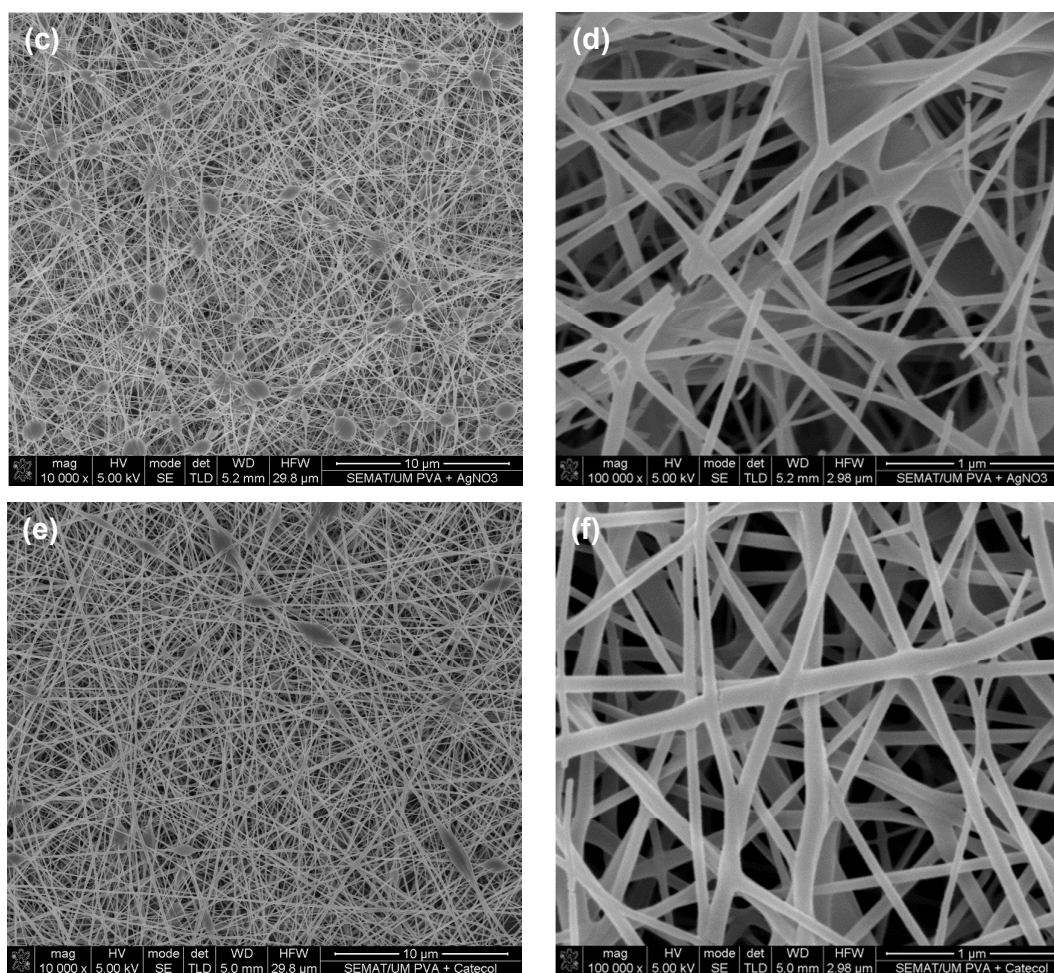
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3 where A and B are the average number of bacteria before and after the contact with the  
4 samples, respectively. All experiments were conducted in triplicate with data being only  
5 considered if the error between measurements was smaller than 15%.  
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10 **2.10. Ultrafiltration.** The ultrafiltration experiments were carried out at 25 °C using a  
11 C.I. Reactive Red 66 monoazo dye (0.1 g/L - 629.37 MW –  $\lambda$  max 570 nm) at 4 bar  
12 dispersed in 50 mL of dH<sub>2</sub>O and synthetic seawater using the ASN-III<sub>0</sub> medium. The  
13 system consisted of a 300 mL bench stainless steel tangential flow stirred cell  
14 (Sterlitech, HP4750, active membrane area, 14.6 cm<sup>2</sup>) pressurized with air. The solution  
15 in the chamber was stirred with a teflon-coated magnetic bar at 300 rpm. All  
16 membranes were preconditioned by filtering the solutions at 4 bar of pressure until a  
17 steady flux was guaranteed. At the end of filtration, the feed, permeate and retentate,  
18 were collected and the concentration and solute rejection were determined using UV/vis  
19 spectrophotometry. The membrane flux, defined as the volume of solvents and solutes  
20 that pass through the membrane unit area per unit time, was calculated dividing the  
21 volume of permeate by the membrane active area and filtration time. The overall salt  
22 rejection was calculated using a conductivimeter and expressed as percentage of  
23 reduction using the seawater mother solution as reference (44 mS cm<sup>-1</sup>). A calibration  
24 curve was established using the UV/vis spectrophotometry. Each experiment was  
25 conducted in triplicate.  
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### 3. RESULTS

**3.1. Membrane Characterization.** The nanofibrous membranes morphology, chemical composition and general mechanical and thermal features were characterized using SEM, EDS, XPS, DMA, TGA and DSC techniques. SEM micrographs of the PVA, PVA/AgNO<sub>3</sub> and PVA/PC electrospun nanofibers onto the PVDF basal membrane were taken (Figure 1). Beads and discontinuous fibers within the PVA nanofibrous membranes were detected. Fibers were classified as heterogeneous in size varying between 36 and 147 nm, with an average diameter of  $\approx 81$  nm, and porosity of  $\approx 88\%$  (Table 1). Beads within the nanofibers produced from the PVA/AgNO<sub>3</sub> blend were very frequent. Here, the nanofibers diameter varied between 24 and 125 nm with a porosity of  $\approx 90\%$ . The integrity of the fibers was as well compromised, with discontinuous and very thin nanofibers being detected. To the contrary, very little beads and smooth nanofibers were observed using the PVA/PC blend. Nanofibers were relatively homogeneous in shape and diameter compared to the other blends; average diameter and porosity were established at  $\approx 98$  nm (69-131 nm) and 51%, respectively.





**Figure 1** - SEM of the (a, b) PVA nanofibres and PVA blended with (c, d) AgNO<sub>3</sub> and (e, f) PC at magnifications x10,000 and x100,000.

**Table 1.** Porosity and average fiber diameter of the PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers electrospun onto a PVDF basal membrane.

Membranes	Porosity (%)	Fiber Diameter (nm)
PVDF+PVA	87.8	81.4 ± 32.4
PVDF+PVA/AgNO <sub>3</sub>	90.3	63.8 ± 31.7
PVDF+PVA/PC	51.3	98.2 ± 20.3

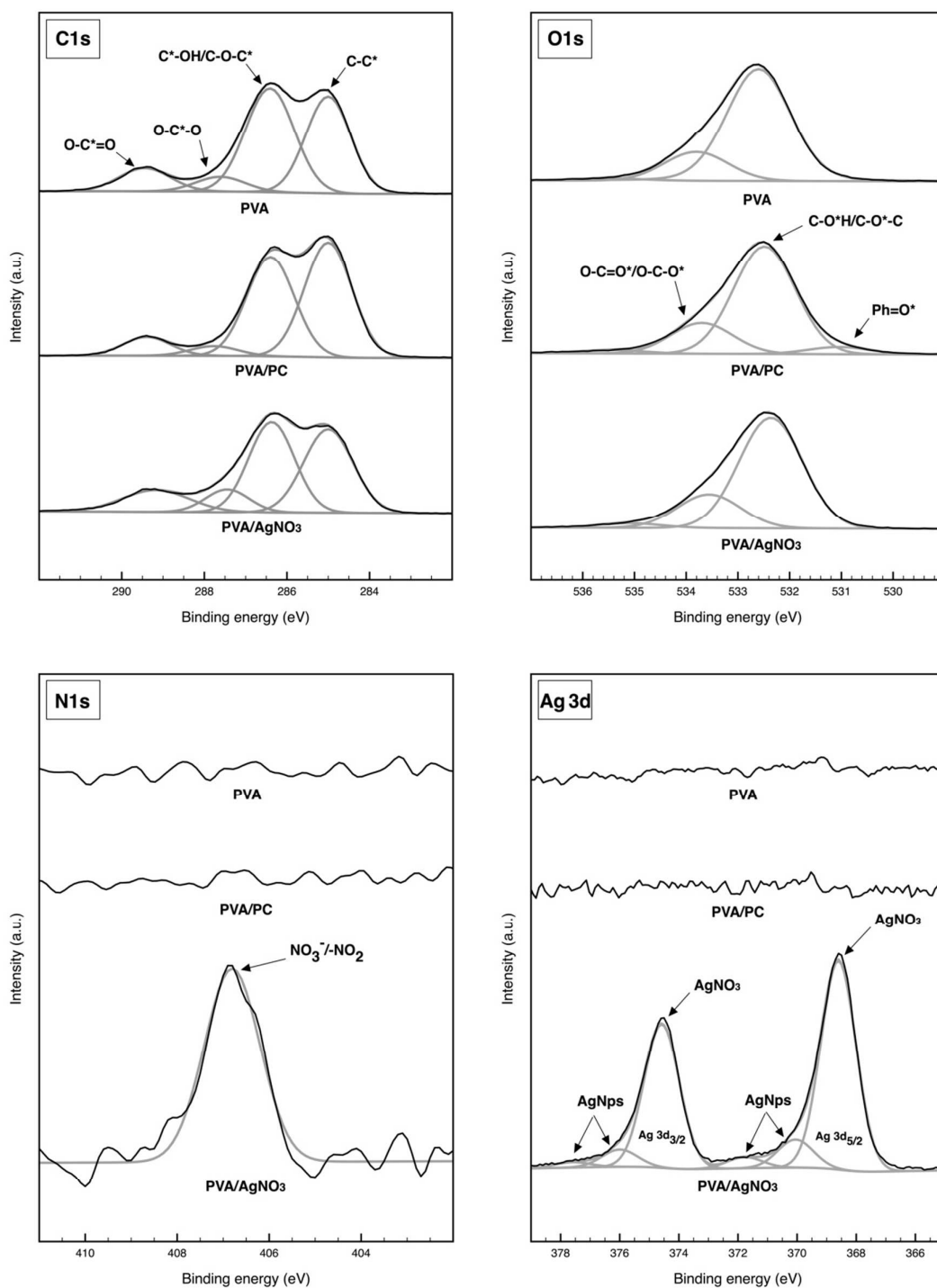
By EDS and XPS, the relative atomic composition of the PVA, PVA/AgNO<sub>3</sub> and PVA/PC electrospun nanofibers on the PVDF membrane was determined (Table 2, Figure S1 in Supporting Information). As expected, only on the PVA/AgNO<sub>3</sub> blend other elements aside from C and O were observed. Here, N and Ag from the AgNO<sub>3</sub> were detected confirming an efficient blending. Between the PVA and the PVA/PC blend, as the chemical composition of PVA is (C<sub>2</sub>H<sub>4</sub>O)<sub>n</sub> and catechol is C<sub>6</sub>H<sub>6</sub>O<sub>2</sub> and, thus, only C and O can be detected, no significant differences would be expected from this analysis (the condensed formula of the main chemicals used in this investigation can be depicted in Figure S2 in Supporting Information). EDS and XPS techniques differ significantly on the specimen excitation, size of the excitation area (0.5-4 μm of EDS vs. 15-500 μm of XPS), and depth resolution (500-3000 nm of EDS vs. 1-10 nm of XPS). However, since XPS is characterized by a lower planar but a higher vertical resolution than EDS, it is able to create deeper profiles of the chemical structure of the materials. Moreover, XPS analysis is generally free of matrix effects, which is the cause of a lower quantitative accuracy in EDS. The main difference between the two techniques, in this case, is the fact that the amount of Ag observed by XPS is higher with a concomitant lower concentration of the counter ion than the observed by EDS. This suggests a good availability of Ag ions on the surface of the nanofibers (Figure S3 and S4 in Supporting Information).

**Table 2.** Relative chemical composition and atomic ratio determined by EDS and XPS of PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers electrospun onto a PVDF basal membrane.

Membranes	At (%)					Atomic Ratio
	C	O	N	Ag	Imp.	O/C

	PVDF+PVA	62.56	37.06	-	-	0.38	0.59
EDS	PVDF+PVA/AgNO <sub>3</sub>	53.19	40.42	2.93	3.46	-	0.76
	PVDF+PVA/PC	62.01	36.82	-	-	1.17	0.59
	PVDF+PVA	70.00	30.00	-	-	-	0.43
XPS	PVDF+PVA/AgNO <sub>3</sub>	66.57	31.38	0.62	1.43	-	0.47
	PVDF+PVA/PC	70.76	29.24	-	-	-	0.41

The XPS high-resolution deconvoluted spectra and the corresponding atomic compositions are shown in Figure 2 and Table 3. Deconvolution of the C1s core level of the PVDF+PVA, PVDF+PVA/AgNO<sub>3</sub> and PVDF+PVA/PC show the expected stoichiometric ratios of the individual C components as shown in Table 3. The O1s XPS spectra of the three samples are similar and the ratio of O species is in accordance with the stoichiometric O content for each sample (Table 3). The PVDF+PVA/AgNO<sub>3</sub> sample shown a peak in the N1s core at 406.8 eV level typically attributed to the NO<sub>3</sub><sup>-</sup> and NO<sub>2</sub><sup>-</sup> anions.<sup>30</sup> The Ag 3d<sub>5/2</sub> component was deconvoluted in three subpeaks, a main peak at 368.6 eV attributed to AgNO<sub>3</sub> and two small peaks at higher binding energies attributed to the presence of small amount of nanoparticles formed during the electrospinning procedure. However, no nanoparticles can be observed in the SEM analysis because the electrospun PVA/AgNO<sub>3</sub> fibers were not produced with the intent to improve the Ag reduction on the PVA matrix.



**Figure 2** - High-resolution XPS C1s, O1s, N1s and Ag 3d spectra of PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers electrospun onto a PVDF basal membrane.

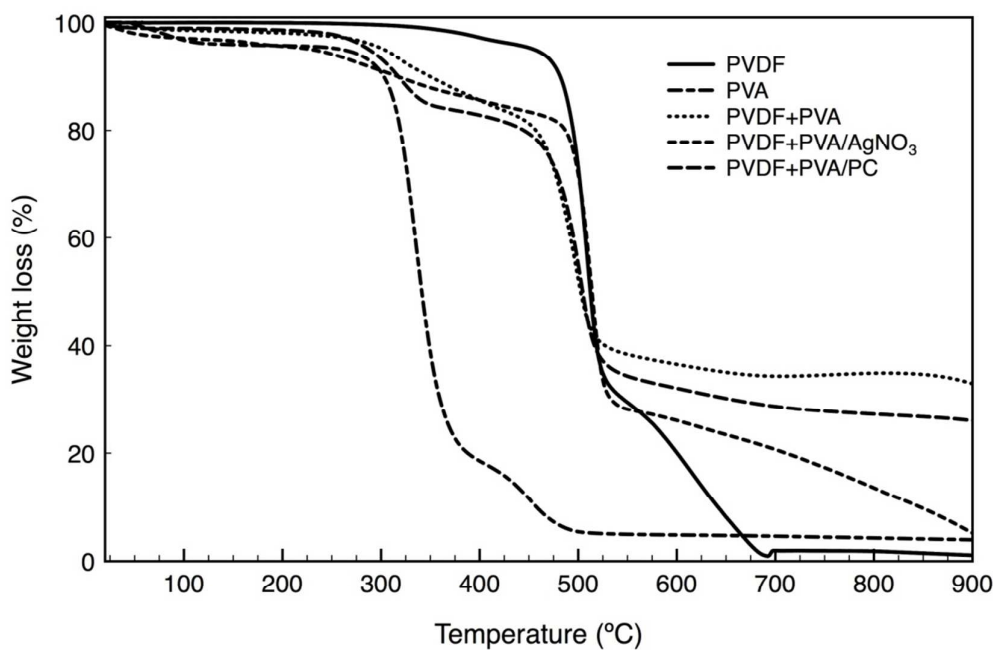
**Table 3.** Different chemical functional groups and represented by the deconvolution C1s, N1s, O1s and Ag d3 XPS peaks of PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers electrospun onto a PVDF basal membrane.

Binding energy (eV)	Functional group	Relative area of deconvoluted peaks (%)		
		PVDF+PVA	PVDF+PVA/AgNO <sub>3</sub>	PVDF+PVA/PC
285.0	C-C*	38.3	38.4	47.3
286.4	C-O*H/C-O-C*	44.8	38.6	41.0
287.6	O-C*-O	6.4	9.3	4.0
289.4	O-C*=O	10.5	13.7	7.7
368.6	Ag 3d <sub>5/2</sub> AgNO <sub>3</sub>	-	50.4	-
370.1/371.8	Ag 3d <sub>5/2</sub> AgNPs	-	9.5	-
374.6	Ag 3d <sub>3/2</sub> AgNO <sub>3</sub>	-	34.7	-
376.0/377.6	Ag 3d <sub>3/2</sub> AgNPs	-	5.5	-
406.8	NO <sub>3</sub> <sup>-</sup> /-NO <sub>2</sub>	-	100	-
532.5	C-O*H	79.3	74.1	72.2
533.7	O-C=O*/O-C-O*	20.7	25.9	22.9
531.0	Ph=O*	-	-	4.8

TGA analysis of the PVDF, PVA, PVDF+PVA, PVDF+PVA/AgNO<sub>3</sub> and PVDF+PVA/PC membranes (Figure 3) put in evidence three well-differentiated steps of degradation. For all combinations, the first step corresponds to the initial weight loss in water. PVDF sample is very stable until temperatures as high as 400 °C, after those it begins to degrade with a 70% mass loss,  $T_{max}$  at 510 °C. After the main degradation, a second weight loss step occurs and the residue obtained is  $\approx$  2%, at  $\approx$  700 °C. Also in the case of PVA, decomposition occurs mainly in two degradation steps. The first starts at  $\approx$  300 °C,  $T_{max}$  at 350 °C, representing a loss in mass of  $\approx$  80%. In the end of step 2, at 500 °C, only  $\approx$  5 % of residual mass was observed. By electrospinning PVA or the



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3 tested blends onto PVDF the weight loss behavior with time alters. Three well-  
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5 differentiated steps can be depicted. The first smallest step at  $\approx 350$  °C corresponds to  
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7 the PVA nanofibers degradation while the second step at  $\approx 500$  °C corresponds to the  
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9 PVDF membrane degradation. The third degradation step evolves at a slower rate and  
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11 continues until temperature reaches 900 °C, remaining  $\approx 38\%$ ,  $\approx 5\%$  and  $\approx 30\%$  of  
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13 residual mass on the PVDF+PVA, PVDF+PVA/AgNO<sub>3</sub> and PVDF+PVA/PC  
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15 membranes, respectively.  
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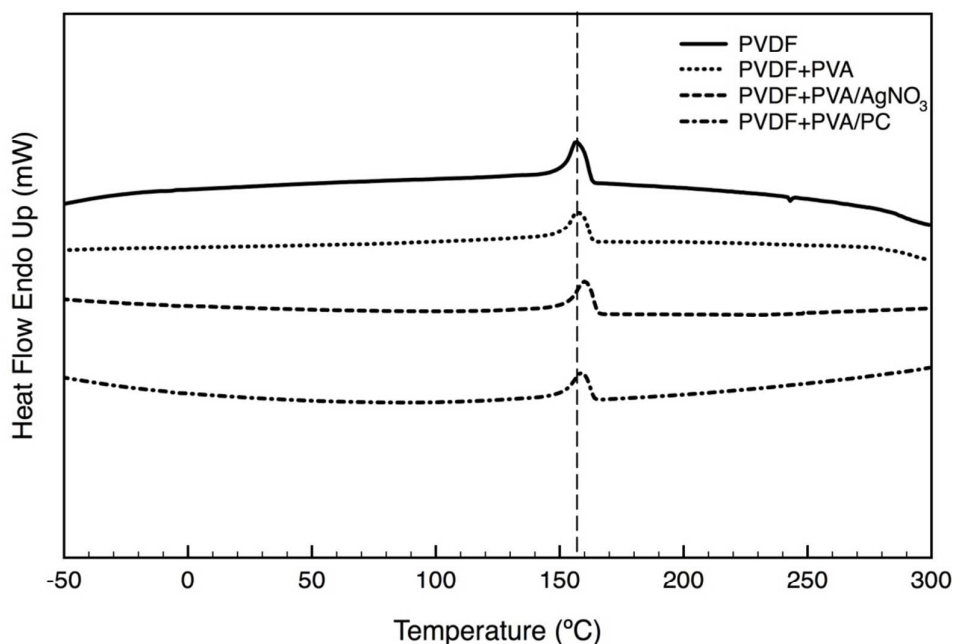


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**Figure 3** - TGA of the PVDF basal membrane and the PVDF electrosun with PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers from 35 °C to 900 °C, performed at a heating rate of 10 °C/min, in a nitrogen atmosphere.

The DSC analysis (Figure 4) detected the melting temperature of PVDF and PVDF+PVA at  $\approx 158$  °C, the PVDF+PVA/AgNO<sub>3</sub> at  $\approx 161$  °C and the PVDF+PVA/PC

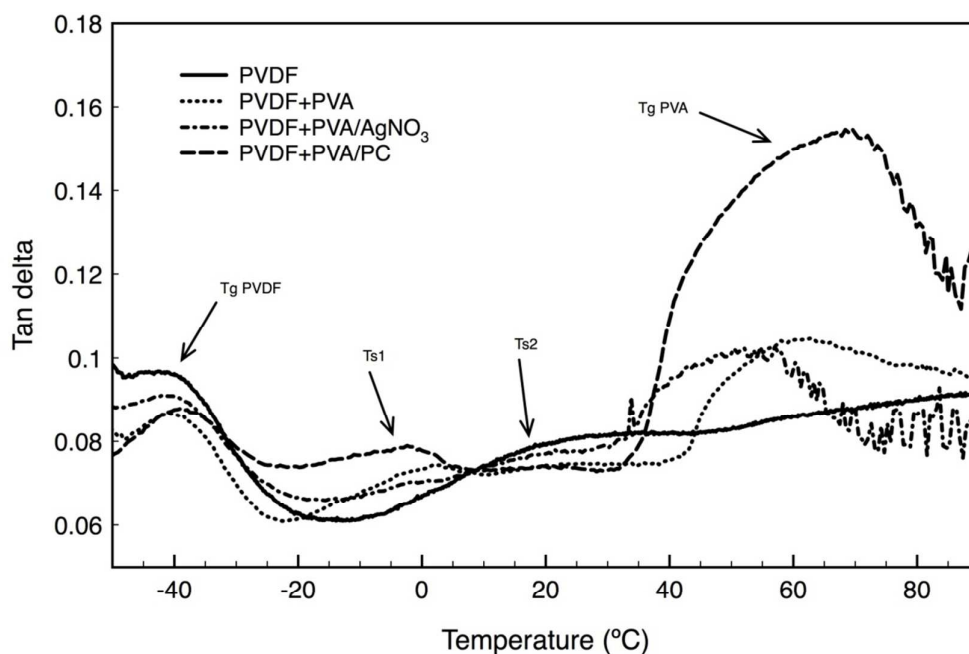
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3 membranes at  $\approx 159$  °C. As only one peak was detected for each sample, the blends  
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5 were recognized as homogeneous. Despite DSC being able to easily recognize the  
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7 melting point of the generated composite, it is not always accurate enough in identifying  
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9 Tg transitions.  
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38 **Figure 4** - DSC thermograms of 2<sup>nd</sup> heating of PVDF basal membrane and the PVDF  
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40 electrospun with PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibres in a temperature range of  
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42 -50 to 300 °C at 10 °C/min.  
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46 Since these data was inconclusive, the DMA technique, which is a more sensitive  
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48 method in terms of relaxation behavior, was used. Data was reported in terms of loss or  
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50 damping factor ( $\tan \delta$ ), which relates the loss modulus with the storage modulus and  
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52 provides information on the relative contributions of the viscous and elastic components  
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54 of a viscoelastic material.<sup>29</sup> The DMA analysis (Figure 5) was conducted on the PVFD,  
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56 PVDF+PVA, PVDF+PVA/AgNO<sub>3</sub> and PVDF+PVA/PC membranes. Electrospinning of  
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3 PVA and its blends was directly done on the PVDF membranes being, therefore,  
4 impossible to separate the PVA electrospun layer from the latter and analyze it  
5 individually. Four regions with different elastic behavior were detected, two secondary  
6 and two main relaxation peaks. The two main relaxation peaks were observed at  $\approx 40$  °C  
7 and  $\approx 65$  °C, while the secondary were found at  $\approx -5$  °C and  $\approx 20$  °C. The T<sub>g</sub> peak at 65  
8 °C is attributed to PVA and does not appear in the bare PVDF. After the addition of  
9 AgNO<sub>3</sub> the PVA peak clearly shifted to lower temperatures while PC shifted to higher.  
10 It may be difficult to identify precisely a single temperature peak for each sample, still  
11 the shift is significant even if the peak is calculated from a range of temperatures in the  
12 curve plateau (55-65 °C for PVDF+PVA, 65-75 °C for PVDF+PVA/PC and 45-55 °C  
13 for PVDF+PVA/AgNO<sub>3</sub>). Moreover the PVDF+PVA/PC peak showed a higher tan  $\delta$   
14 than the other membranes, reducing significantly its elastic modulus (more viscous  
15 material).  
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**Figure 5** - Tan  $\delta$  curves versus temperature of the membranes PVDF and PVDF electrospun with PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers.

**3.2. Antimicrobial Activity.** The membranes antimicrobial activity was measured against *E. coli* and *S. aureus* using the standard shake flask method. After 1 h contact, the number of viable microorganisms was counted and the percentage of reduction determined. Data collected (Table 4) established the PVDF+PVA/AgNO<sub>3</sub> as the most promising to prevent bacterial immobilization (100% reduction). PVDF+PVA/PC was also very important against *S. aureus* (92% reduction), however was only capable of reducing *E. coli* activity in 13%. PVDF and PVDF+PVA had little to none influence on the bacteria response.

**Table 4.** Antimicrobial activity of the filtration membranes using *E. coli* and *S. aureus*.

Membranes	Bacterial reduction (%)	
	<i>E. coli</i>	<i>S. aureus</i>
PVDF	17%	-2%
PVDF+PVA	-3%	-23%
PVDF+PVA/AgNO <sub>3</sub>	100%	100%
PVDF+PVA/PC	13%	92%

**3.3. Ultrafiltration.** The ultrafiltration performance of the developed PVDF+PVA/PC membrane was established by direct measurement of the C.I. Reactive Red 66 monoazo dye in dH<sub>2</sub>O and synthetic seawater solution at 4 bar. The maximum

removal dye efficiency was determined at  $\approx 85\%$  in dH<sub>2</sub>O after 5 cycles (Table 5). With this solution, a relative high filtration flux was also observed. In the presence of salts, a decrease in both rejection and flux was evidenced. The overall salt rejection was calculated using a conductivimeter and expressed as percentage reduction using the seawater mother solution as reference (44 mS cm<sup>-1</sup>). The results showed an overall salt reduction of 5% after 5 cycles.

**Table 5.** Ultrafiltration experiments in Reactive Red 66 dissolved in dH<sub>2</sub>O and seawater using a PVDF membrane electrospun with a PVA/PC.

Solution	Rejection (%)	Flux (L m <sup>-2</sup> h)	Overall salt rejection (%)
dH <sub>2</sub> O	85 ± 2	70 ± 4	-
Seawater	64 ± 2	62 ± 3	5 ± 1

#### 4. DISCUSSION

Electrospinning of single PVA solutions has been reported by many.<sup>31-33</sup> Yet, combinations of PVA with AgNO<sub>3</sub> or PC are less common. The solution parameters, including concentration, viscosity and conductivity, are determinant to the success of the final product. For that reason, optimization processes are usually conducted with the individual polymers prior to the formulation of blends. Since nanofibers could not be generated from pure AgNO<sub>3</sub> or PC solutions, only PVA required further testing. Using data from a previous work, in which detailed analyses of the effects of different processing conditions on the formation of PVA nanofibers is given,<sup>29</sup> an optimal concentration for PVA, suitable even in blends, was established at 12% w/w. Also, it

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3 should be mentioned that because of its solubility in water, PVA-based electrospun  
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5 nanofibers (in single or blend forms) require an extra step during fabrication. Its unique  
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7 nanofibrous structure is quickly lost in aqueous environments, becoming inappropriate  
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9 for water ultrafiltration applications. Crosslinking of PVA polymer with GA is,  
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11 therefore, necessary to stabilize the electrospun nanofibers. Their morphology, chemical  
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13 composition and mechanical and thermal properties were then characterized.  
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17 Nanofibers resultant from single PVA, PVA/AgNO<sub>3</sub> and PVA/PC blends displayed  
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19 very important features (Figure 1). Presence of beads within the nanofibers and  
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21 detection of discontinuous and thin nanofibers within the mesh were expected using  
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23 single PVA due to the low conductivity and viscosity of the solution at 12% w/w.<sup>29</sup>  
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25 Still, the occurrence of beads and the presence of discontinuous fibers were more  
26  
27 prevalent when AgNO<sub>3</sub> was present. Beads may stick to fibers changing pore size, they  
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29 may agglomerate to form larger beads that can obstruct other pores and may also  
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31 fragilize neighboring nanofibers. It has been reported that the addition of AgNO<sub>3</sub> to  
32  
33 polymeric solutions increases the charge density in the ejected jets and, thus, stronger  
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35 elongation forces are imposed, resulting in a morphology change of the e-spun fibers  
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37 from a bead-on-fiber structure to a uniform fiber structure with straighter shape and  
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39 smaller diameter.<sup>34-35</sup> Here, however, only the fibers smaller diameter was attained (63.8  
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41 ± 31.7 nm, Table 1). The formation of beads was not avoided nor the presence of  
42  
43 discontinuous fibers. As the PVA/AgNO<sub>3</sub> solution contacts with the metal needle tip  
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45 and is ejected, Ag oxides are susceptible to be formed and to grow on the surface of the  
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47 tip forming precipitates that can both difficult the exit of the electrospun solution and  
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49 lead to the formation of beaded fibers.<sup>36</sup> By combining PC with PVA, formation of  
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51 beads, thin and discontinuous nanofibers was overcome. The resulting fibers were more  
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53 homogeneous both in size and shape. Due to its electroactive versatility which allows  
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3 PC to undergo a variety of chemical reactions and interact with both organic and  
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5 inorganic substrates, the repulsive forces between the ionic groups within the polymer  
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7 backbones may be reduced and, thus, uniform fiber structures can be produced.<sup>1-2</sup> To  
8  
9 confirm the homogeneity of the blends and both the presence of AgNO<sub>3</sub> and PC on the  
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11 nanofibers, XPS and EDS analyses were conducted (Table 2). The atomic composition  
12  
13 of PVA was found consistent with the literature.<sup>37</sup> Presence of AgNO<sub>3</sub> on the  
14  
15 PVA/AgNO<sub>3</sub> blend was easily demonstrated by the detection of Ag and N at ≈ 3% each.  
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17 As expected, the ratio O/C also increased (more important in the EDS data). The atomic  
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19 composition of PVA/PC altered very little from single PVA, since both PVA and PC  
20  
21 exhibit equal chemical elements (C and O) and the amount of PC added to the blend  
22  
23 was not significant enough to alter the O/C ratios. Impurities, most likely resultant from  
24  
25 sample handling, were only detected by EDS on PVA and PVA/PC.  
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30 The deconvolution of the XPS C1s envelope (Figure 2, Table 3) shows a peak at  
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32 285 eV attributed to aliphatic carbon atoms (–C–C–) of the main chain of PVA.<sup>38</sup> The  
33  
34 peak at 286.4 eV can be attributed to the C-O-H bond of the hydroxyl group of PVA  
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36 structure. It is expected that C-O-C groups to be formed between PVA chains during the  
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38 electrospinning process and after the GA crosslinking.<sup>39</sup> This is confirmed by the  
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40 presence of the peak at 287.6 eV representing the bond of O-C-O. The oxidation effect  
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42 of GA on the PVA explains the presence of the peak at 289.4 eV attributed to the  
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44 carboxyl acid group (O-C=O).<sup>40</sup> The deconvolution of the O1s peak of PVDF+PVA and  
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46 PVDF+PVA/AgNO<sub>3</sub> gave two contributions: the peak at 532.5 eV which is assigned to  
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48 the C-OH bonds in the PVDF+PVA, and the peak at 533.7 eV which corresponds to the  
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50 C–OH bond in the carboxylic acid as observed in the C1s core level of the  
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52 PVDF+PVA.<sup>38, 41</sup> The PVDF+PVA/PC displayed a supplementary peak at 531.0 eV  
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54 attributed to the carbonyl oxygen of quinones of the catechol oxidized structure.<sup>42</sup>  
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3 The Ag3d<sub>5/2</sub> shows the main peak at 368.6 eV that corresponds to AgNO<sub>3</sub> proving  
4 that most of the metal in the nanofibers is still in the form of salt.<sup>43</sup> The two small peaks  
5 at 370.1 and at 371.8 eV suggest the presence of small amount of Ag NPs interacting  
6 with the PVA surface.<sup>44</sup> When Ag NPs chemically interacts with polymer moiety a  
7 positive shift in binding energy is usually observed.<sup>45-47</sup> As reported, decreasing the size  
8 of the Ag NPs leads to an increase in the positive shift of the Ag 3d<sub>5/2</sub> core electron  
9 binding energy.<sup>48</sup> The positive shift in binding energy may be attributed to the size  
10 effects (change in the electronic structure) of the noble metals in composite films.<sup>49</sup> The  
11 preparation of Ag NPs in an electrospun polymeric matrix is usually achieved by  
12 chemical or physical reduction.<sup>50-51</sup> It is important to stress that the main goal of this  
13 research was the use of AgNO<sub>3</sub> as positive control to establish the antimicrobial  
14 efficiency of PVDF+PVA/PC and not to produce nanoparticles. In fact, the  
15 electrospinning was performed in a way that the synthesis of nanoparticles was kept to a  
16 minimum. Light exposure inevitably creates some reductive conditions which may also  
17 explain the presence of silver in the metallic state. The two small peaks suggest the  
18 formation of two Ag NPs size distributions lower than 10 nm. This size in addition to  
19 the low content could explain the absence of visible NPs in the SEM analysis.  
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40 The steps of membrane degradation were defined and characterized by TGA (Figure  
41 3). PVDF was used as commercial control and base substrate for the single PVA,  
42 PVA/AgNO<sub>3</sub> and PVA/PC electrospun blends. The first step at ≈ 100 °C refers to the  
43 initial weight loss resultant from the evolution of moisture from the polymer matrix.  
44 However, still less than 10%, this was more important on the PC-containing membrane,  
45 suggesting the presence of more water molecules per repeat unit of the polymer. The  
46 PVDF membrane starts to degrade at 400°C continuously until it becomes residual at  
47 700 °C leading to the formation of hydrogen fluoride, the monomer and small amounts  
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3 of  $C_4H_3F_3$ .<sup>52</sup> Previous reports have shown, the thermal decomposition of pure PVDF to  
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5 be more important at  $\approx 500$  °C.<sup>53</sup> Our data is consistent with those findings. The second  
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7 weight loss step between 500 °C and 700 °C may be due to the presence of additives  
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9 introduced during commercial polymer processing, such as lubricants and plasticizers.<sup>54</sup>  
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11 PVA decomposition occurs mainly in the second degradation step which starts at  $\approx 300$   
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13 °C, representing a loss in mass of  $\approx 80\%$ , in which the PVA side chain is lost.<sup>55</sup> The  
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15 PVA main chain starts degrading after that point<sup>56</sup> and continues throughout step 3,  
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17 until 900 °C, at which point only  $\approx 5\%$  of residual mass remains. The combination of  
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19 the tested blends (PVA, PVA/AgNO<sub>3</sub> and PVA/PC) with PVDF, alters the  
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21 thermogravimetric profile of the membrane with time. Indeed, the pattern of  
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23 degradation only becomes more significant at the second step, after  $\approx 500$  °C. During  
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25 step 1, at  $\approx 350$  °C, degradation refers mostly to PVA, while at step 2 the PVDF  
26  
27 membrane is lost. Degradation of PC occurs throughout both the first and second steps.  
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29 Studies have shown the PC degradation rate to start at  $\approx 180$  °C and to evolve very  
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31 slowly with the increase in temperature. As the temperature rises, internal  
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33 rearrangements of the PC structure occur providing great thermal stability to the  
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35 catechol units.<sup>10</sup> Still, once reached 900 °C,  $\approx 30\%$  of residual mass remains from the  
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37 PVDF+PVA/PC membrane. The high solid residue content observed at 900 °C might be  
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39 due to the higher crystalline molecular configuration of the nanofibers containing PVA  
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41 or to the presence of cations ( $Na^+$ ,  $K^+$ ,  $Ca^{2+}$ ), which acted like a bridge between  
42  
43 different polymer chains.<sup>57</sup> These cations derive from the enzyme preparation which  
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45 requires several buffers and stabilizers. The presence of silver salt clearly interferes with  
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47 the nanofibres thermal resistance leading to a slow but gradual mass loss between 550  
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49 °C and 900 °C. TGA data suggests that the maximum running temperature that can be  
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51 used during filtration should not exceed 150 °C since after this value the PVA/PC blend  
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3 starts degrading. Without considering the high resistance of the PVDF basal membrane,  
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5 this temperature is a clear improvement over commercially available filtration  
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7 membranes that stand no more than 100 °C.  
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10 DSC analyses (Figure 4), which established the membranes melting temperatures,  
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12 provided important information about the homogeneity of the blends. DSC spectra  
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14 revealed only one endothermic peak, corresponding to the melting point, but did not  
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16 provide information about the different crystalline phases in which the elements  
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18 composing the membrane would be found. The PVDF melting temperature was  
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20 consistent with the literature.<sup>58</sup> Although the melting temperature of PVA ranges 200  
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22 °C,<sup>59</sup> the molecular interactions established with PVDF seems to have decreased its  
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24 melting point. According to the literature, the melting point of AgNO<sub>3</sub> is at ≈ 212 °C  
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26 and the PC at ≈ 125 °C.<sup>10, 60</sup> The addition of these elements to the PVA blends altered  
27  
28 slightly the position of the peaks as new molecular interactions (different from PVDF  
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30 and single PVA) were formed. However, data acquired from DSC was inconclusive. For  
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32 that reason, DMA technique was also used (Figure 5). Four regions with different  
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34 elastic behavior were detected on all tested membranes, two secondary and two main  
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36 relaxation peaks. The two main relaxation peaks were detected at ≈ -40 °C and ≈ 65 °C  
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38 and correspond to the glass transition temperatures (T<sub>g</sub>) of PVDF and PVA,  
39  
40 respectively.<sup>61-62</sup> The T<sub>g</sub> peak at 65 °C was exclusive of PVA and does not appear in the  
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42 bare PVDF. PVA electrospun nanofibers could not be analyzed individually, since PVA  
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44 was electrospun directly onto the PVDF membranes, thus making it impossible to  
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46 separate them. The secondary peaks were found at ≈ -5 °C (T<sub>s1</sub>) and ≈ 20 °C (T<sub>s2</sub>) and  
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48 are associated with the secondary relaxation temperature of PVA and with local  
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50 molecular motions or conformational changes of the PVA side groups, respectively.<sup>61</sup>  
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52 After the addition of AgNO<sub>3</sub>, the PVA peak clearly shifted to lower temperatures, while  
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3 PC shifted to a higher. It may be difficult to identify precisely a single temperature peak  
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5 for each sample, still the shift is significant even if the peak is calculated from a range  
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7 of temperatures in the curve plateau (55-65 °C for PVDF+PVA, 65-75 °C for  
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9 PVDF+PVA/PC and 45-55 °C for PVDF+PVA/AgNO<sub>3</sub>). This happens in response to  
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11 molecular interactions (hydrogen bonding) that occur between the elements in the blend  
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13 that promote conformational changes in the structure of the PVA side groups. The same  
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15 has been reported by Young et al. with chitin and PVA blends, and Sudhamani et al.  
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17 with Gellan and PVA blends.<sup>59, 63</sup> Also, we have shown chitosan and cyanobacterial  
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19 extracellular polymeric substances blended with PVA and electrospun onto PVDF  
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21 surfaces to promote equal effects.<sup>29</sup>  
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25 The addition of AgNO<sub>3</sub> is responsible for the decrease of the tan  $\delta$  peak temperature  
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27 from  $\approx 60$  °C to  $\approx 50$  °C. This leads to lower interactions between PVA polymer chains  
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29 and to higher free volume inside the lattice.<sup>64</sup> Despite the shift in temperature, the values  
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31 of the Tan  $\delta$  remained very similar. This seems to indicate that the thermoplastic PVA  
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33 network is not perturbed by the non-thermoplastic inorganic filler (AgNO<sub>3</sub>) in terms of  
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35 its viscoelastic properties.<sup>68</sup> The PVDF+PVA/PC peak showed a remarkably higher tan  
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37  $\delta$  and a slightly higher T<sub>g</sub> temperature than the other membranes, indicating a  
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39 significant reduction of its elastic modulus (more viscous material). The shift towards  
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41 higher T<sub>g</sub> could be attributed to the intermolecular interactions between PVA and PC in  
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43 the form of hydrogen bonding, indicating that the system is very close to being  
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45 miscible.<sup>65</sup> The DSC and DMA analyses provides important information about the  
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47 stability of the membrane in terms of operative temperature and pressure. DSC  
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49 confirmed the TGA data showing that the maximum temperature before filter  
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51 degradation is about 150 °C. DMA, which is a more sensitive technique, established that  
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53 to maintain a constant porosity and consequently promote an effective filtration, it  
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3 should be performed between -20 and 30 °C. This is because after the PVA T<sub>g</sub> the  
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5 nanofibers can be deformed under the ultrafiltration pressure (e.g. 4 bar) changing the  
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7 pore sizes.  
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10 The membranes antimicrobial activity was measured against *E. coli* and *S. aureus*  
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12 using the standard shake flask method (Table 4). PVDF+PVA/AgNO<sub>3</sub> was determined  
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14 as the most promising to prevent bacterial immobilization (100% reduction), regardless  
15  
16 the bacteria type (Gram-positive or Gram-negative). Ag-based compounds are currently  
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18 being used to control bacterial growth in a variety of applications. They are highly toxic  
19  
20 to microorganisms, showing strong biocidal effects on as many as 12 species of  
21  
22 bacteria, including *E. coli* and *S. aureus*.<sup>66-67</sup> In addition, Ag-based compounds, like  
23  
24 AgNO<sub>3</sub>, are capable of retaining its effective inhibitory activity against various  
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26 microorganisms even at very low concentrations,<sup>68</sup> which explains its enhanced  
27  
28 performance when blended with PVA and electroposited onto PVDF. PVDF+PVA/PC  
29  
30 was also very important against *S. aureus* (92% reduction) but showed a low activity  
31  
32 against *E. coli* (13% reduction). PC has also been used as a binding agent to improve  
33  
34 the antimicrobial and biocidal features of coatings against *E. coli* and *S. aureus* by  
35  
36 orienting its phenyl groups on the substrate surface and promoting an adhesive or cross-  
37  
38 linking functionality that discourages leaching and allows the tuning of activity.<sup>4, 27</sup> PC  
39  
40 was also reported in literature to display great antibacterial performance against  
41  
42 *Pseudomonas putida*, *Pseudomonas pyocyanea* and *Corynebacterium xerosis*, when  
43  
44 used individually.<sup>3</sup> To the authors knowledge, this is the first time the antimicrobial  
45  
46 features of PC blended with PVA have been tested against *E. coli* and *S. aureus*.  
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52 The different behavior for Gram-positive and Gram-negative bacteria may be  
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54 explained by the differences in the cell walls structure and composition. The cell wall of  
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56 Gram-positive bacteria is composed of a thick peptidoglycan layer composed of linear  
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3 polysaccharide chains cross-linked by short peptides to form a 3D rigid structure. On  
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5 the other hand, the cell wall of Gram-negative species is more structurally and  
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7 chemically complex with a thin peptidoglycan layer adjacent to the cytoplasmic  
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9 membrane and a lipopolysaccharidic outer membrane.<sup>69</sup> The higher antimicrobial  
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11 resistance of Gram-negative bacteria to PC is related to the hydrophilic surface of the  
12  
13 outer membrane and could be also associated with periplasmic-space enzymes capable  
14  
15 of degrading molecules introduced from the outside.<sup>70</sup> The enzymes produced in the  
16  
17 periplasmic space could be secreted through the outer membrane reaching the external  
18  
19 environment using a type II secretion system or the PC could be able to destabilize the  
20  
21 outer membrane allowing the direct access to the periplasmic space enzymes. The  
22  
23 absence of membrane bound periplasm in the Gram-positive bacteria allows a higher  
24  
25 permeability due to the hydrophilic porous structure of the cell wall that can be easily  
26  
27 destabilized by PC or poly(quinones).<sup>71</sup> There are several hypotheses on the  
28  
29 antibacterial activity of polyphenols. It has been suggested that polyphenols could  
30  
31 inhibit or kill the bacteria physically by direct adsorption onto the surface of the  
32  
33 bacterial cell wall. It has also been proposed that oxidative polyphenols could mediate  
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35 antibacterial activity by the generation of hydrogen peroxide. Yet, so far, there is no  
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37 consensus concerning these mechanisms.<sup>72</sup>  
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43 In a side experiment, an electrospun membrane was also synthesized using resorcinol  
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45 as precursor instead of catechol. Poly(resorcinol) (PR)-containing membranes showed  
46  
47 no antimicrobial activity even though their chemical, morphology and thermo-  
48  
49 mechanical properties were similar to those of PC (Figure S5 in Supporting  
50  
51 Information). These data revealed the importance of the chemical structure and  
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53 molecular interactions established between PC and PVA, which may be of extreme  
54  
55 importance to gain potent biocidal activity. Because they are not endowed with  
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3 antimicrobial properties, PVDF and PVDF+PVA had little to none influence on the  
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5 bacterial response.  
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8 The ultrafiltration capability of the PVDF membranes with assembled PVA/PC  
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10 electrospun thin-layers was evaluated (Table 5). Maximum removal dye efficiency was  
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12 established at 85% in dH<sub>2</sub>O, after 5 cycles. This indicates medium rejection ability, an  
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14 outcome from the irregular sponge-like thin-layer generated, however with relative high  
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16 filtration flux. In the presence of salts, a decrease in rejection is observed. This can be  
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18 explained by the Gibbs-Donnan effect, in which charged particles near a semi-  
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20 permeable membrane may fail in achieving an evenly distribution across the two sides  
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22 of the membrane.<sup>73</sup> With time the membranes suffered from flux decline due to its  
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24 sensitivity to scaling and osmotic pressure that resulted from the presence of salts. In the  
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26 dead-end filtration, the particles accumulated easily on the top surface of the  
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28 membranes and form a “cake layer”, which reduced the effective pore size of the  
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30 membrane and increased the resistance to flow with time. The observed flux rates were  
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32 slightly superior to the commercial TFC membranes ( $\approx 50 \text{ L m}^{-2} \text{ h}$ ). The overall salt  
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34 rejection was determined at 5%, after 5 cycles. Typically ultrafiltration salt rejection is  
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36 not measured, thus comparing these results with commercially available membranes is  
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38 very difficult. Still, 5% is a remarkable result in view of the high amount of mono-  
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40 cations present in the seawater solution compared to the average porosity of the basal  
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42 membrane (0.02  $\mu\text{m}$ ). Considering the good filtration rate and rejection performance,  
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44 the PVDF electrospun membrane with a Gram-positive antimicrobial enzymatically  
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46 synthesized PVA/PC thin-film has definitely the potential to be considered a candidate  
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48 for seawater pre-treatment applications, at relatively low cost.  
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## 57 **5. CONCLUSION**

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3 This study introduced a new mid-layer nanofibrous porous support containing a  
4 blend of PVA and PC for thin-film composite membranes used in water ultrafiltration  
5 applications. Characterization techniques recognized the electrospun blends as  
6 homogeneous, confirmed the presence of both AgNO<sub>3</sub> and PC, and established the  
7 fashioned membranes as thermally stable. Relevant conformation changes on the PVA  
8 structure were observed as the testing temperature raised and additives were combined  
9 in blends. PVDF+PVA/AgNO<sub>3</sub> membrane exhibited 100% growth inhibition of both  
10 Gram-positive and Gram-negative bacteria strains despite its irregular morphology and  
11 numerous bead formations. The PVDF+PVA/PC membrane was most effective against  
12 *S. aureus* (92%). Contrary to the PVDF+PVA/AgNO<sub>3</sub>, this membrane revealed a  
13 homogeneous morphology with very few bead formations. The ultrafiltration abilities of  
14 the membrane PVDF+PVA/PC were tested with dH<sub>2</sub>O and seawater. After 5 cycles, a  
15 maximum rejection of  $\approx 85\%$  with an average flux rate of  $70 \text{ L m}^{-2} \text{ h}^{-1}$  for dH<sub>2</sub>O and  $\approx$   
16  $64\%$  with an average flux rate of  $62 \text{ L m}^{-2} \text{ h}^{-1}$  for seawater were determined with an  
17 overall salt rejection of  $\approx 5\%$ . The efficacy of this PVDF electrospun membrane with a  
18 Gram-positive antimicrobial enzymatically synthesized PVA/PC thin-film has been  
19 established and its potential for seawater pre-treatment applications has been  
20 demonstrated.  
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## 48 ASSOCIATED CONTENT

### 49 Supporting Information.

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54 Wide XPS spectra of PVA, PVA/AgNO<sub>3</sub> and PVA/PC nanofibers electrospun onto a  
55 PVDF basal membrane were added. Wide XPS spectra of PVDF+PVA/AgNO<sub>3</sub> taken in  
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3 three different places of the same sample, covering an area of 1 mm<sup>2</sup> each. Condensed  
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5 formulas of PVDF, PVA, resorcinol and catechol. EDS spectrum of  
6  
7 PVDF+PVA/AgNO<sub>3</sub> taken at a depth probe of 5 μm. TGA, DSC and DMA spectra of  
8  
9 PVDF+PVA/PC and PVDF+PVA/PR membranes. This material is available free of  
10  
11 charge via the Internet at <http://pubs.acs.org>.  
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### 24 Author Contributions

25  
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28  
29 approval to the final version of the manuscript.  
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47  
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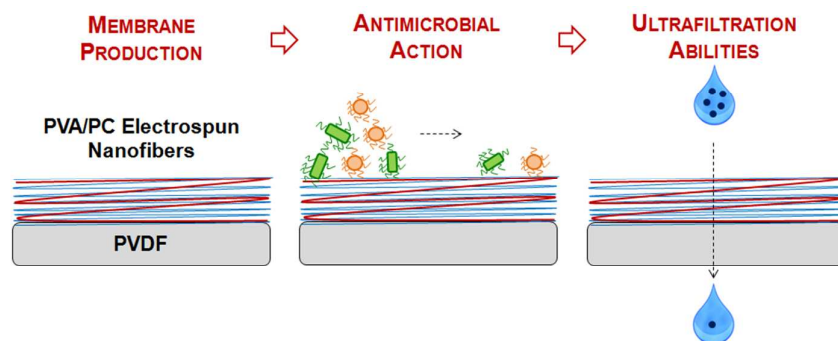
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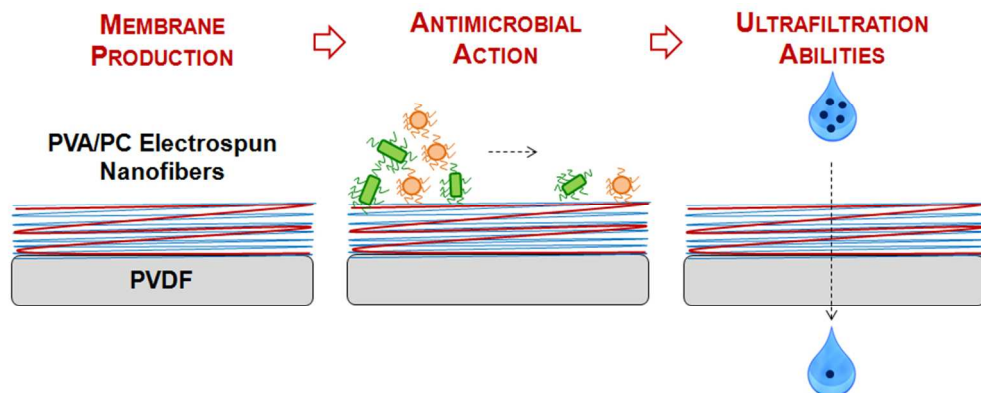
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### Table of Contents Graphic (TOC)





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