

1                    **Bioremediation of aquaculture wastewater from *Mugil cephalus***  
2                    **(Linnaeus, 1758) with different microalgae species**

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**Abstract**

Current aquaculture practices have a detrimental impact on the environment, in particular due to the release of high concentration of nitrogen and phosphorus that can induce eutrophication. This study investigates and compares the capacity of three microalgae species *Tetraselmis suecica*, *Isochrysis galbana* and *Dunaliella tertiolecta*, in the bioremediation of grey mullet *Mugil cephalus* wastewater.

The experiment was conducted in batch conditions for 7 days using completely mixed bubble column photobioreactors. After two days, *T. suecica* and *D. tertiolecta* were able to remove more than 90% of Dissolved Inorganic Nitrogen (DIN) and Dissolved Inorganic Phosphorous (DIP), whereas *I. galbana* removed only 32% and 79% of DIN and DIP, respectively. A higher biomass yield resulted for *T. suecica* ( $0.60 \pm 0.03$  g/L, mean  $\pm$  SE).

This study confirms the potential to employ *T. suecica* in an Integrated Multi Trophic Aquaculture system for bioremediation of wastewater and identifies *D. tertiolecta* as another valid candidate species. Moreover, these species can growth in unsterilized culture media, and this reduces energy consumption, costs and efforts.

**Keywords:** phytoremediation, biotreatment, bioreactors, wastewater, algae.

## 42 **1.1 Introduction**

43 Aquaculture is one of the fastest-growing food producing sectors in the  
44 world, providing almost about 50% of all fish for human consumption;  
45 within 2030, this share is projected to rise to 62% (FAO, 2014). On the  
46 other hand, aquaculture represents one of the major contributors to the  
47 increasing levels of dissolved and particulate nutrients in the aquatic  
48 ecosystems (Lamprianidou et al., 2015). A high nutrient loading into the  
49 aquatic environment, in particular nitrogen and phosphorus may cause  
50 eutrophication, oxygen depletion and siltation (Burford et al., 2003).

51 With the aim to reduce the impacts of traditional aquaculture, several  
52 Countries around the world are developing Integrated Multi-Trophic  
53 Aquaculture (IMTA) systems, which re-uses the wastewaters for the growth  
54 of micro and macroalgae. Indeed, aquaculture wastewater provides nutrients  
55 (ammonia, nitrite, nitrate, dissolved organic nitrogen and phosphate)  
56 (Converti et al., 2006; Soletto et al., 2005; Abe et al., 2002) which can be  
57 used for the production of microalgae. The uptake of dissolved nutrients by  
58 microalgae is considered as the main way to remove nitrogen in aquaculture  
59 wastewaters (Attasat et al., 2013; Sirakov et al., 2013).

60 Previous studies showed that it is possible to remove nutrients from  
61 wastewater (fishes and shrimp production plants) employing microalgae and  
62 macroalgae as key elements in biological treatments (Gao et al., 2016;  
63 Michels et al., 2014; Sirakov and Velichkova, 2014; Bartoli et al., 2005;  
64 Borges et al., 2005; Lefebvre et al., 2004; Hussenot et al., 1998; Lefebvre et  
65 al., 1996; Hammouda et al., 1995; Shpigel et al., 1993).

66 This phycoremediation is an eco-friendly method that offers the advantage  
67 to be a low-cost way to nutrient removal (Mulbry et al., 2008). In addition,  
68 the biomass produced through bioremediation could have multi-purpose  
69 uses including fuels, fertilizers, fine chemicals production and feed in  
70 aquaculture (Mulbry et al., 2006; Vilchez et al., 1997).

71 One of the most common microalgae species employed in aquaculture  
72 bioremediation wastewater is *Tetraselmis* spp. (Michels et al., 2014; Sirakov  
73 and Velichkova, 2014; Borges et al., 2005). A recent study Michels et al.,  
74 (2014) showed for the first time that it is possible to use *Tetraselmis suecica*  
75 for the nutrient assimilation of fishfarm wastewater throughout its  
76 cultivation in controlled photobioreactors.

77 The aim of this study is to evaluate and compare the capability of *T.*  
78 *suecica*, *Isochrysis galbana* and *Dunaliella tertiolecta*, widely used in  
79 aquaculture as feed for rotifers (Mason 1963), echinoderms (Brundu et al.,  
80 2016a, 2016b; Paredes et al., 2015; De La Uz et al., 2013; Azad et al., 2011;  
81 Miller and Emlet 1999; Zamora and Stotz 1994;), filter feeders (Nevejan et  
82 al., 2003; Carboni et al., 2016) and fin fishes (Fabregas et al., 1986), for the  
83 removal of dissolved inorganic nutrients (nitrogen and phosphorous) of  
84 wastewater aquaculture. We evaluate the biomass yield of these species in  
85 controlled bubble column annular photobioreactors, by using untreated  
86 mullet wastewater as culture medium. Contrarily to previous studies that  
87 sterilized the wastewater before its use for bioremediation to eliminate  
88 zooplankton, bacteria and suspended solids (Michels et al., 2014), we  
89 avoided the use of expensive pre-treatment procedures as filtration and

90 sterilization, aiming to reduce the costs of seawater treatment and simulate  
91 more real operation conditions of a wastewater treatment system.

92

## 93 **2.1 Materials and methods**

### 94 **2.1.1 Aquaculture wastewater**

95 Aquaculture wastewater was provided by an experimental fish hatchery  
96 located in the International Marine Centre - IMC Foundation (Oristano,  
97 Sardinia, Italy). Juveniles of grey mullet *Mugil cephalus* (Linnaeus, 1758)  
98 were obtained in laboratory and reared in a recirculating aquaculture system  
99 (RAS) consisting of 4 tanks of 2000 L volume. In this system, the tanks  
100 were linked in a single biological (trickling filter) and cartridge mechanical  
101 filter (10 µm) and supplied with UV lamp (UVPE5, 80 W) and protein  
102 skimmer (Panaque). Temperature was maintained at  $23 \pm 2$  °C (mean  $\pm$  SE)  
103 with a chiller (TECO TR60, 0.91 Kw) and natural photoperiod (14/10 L/D)  
104 was adopted (Figure 1).

105 Natural seawater (NSW) at  $37.0 \pm 1.0$  ppt salinity was previously micro-  
106 filtered (0.5 µm) and UV lamp sterilized. Juveniles of  $0.35 \pm 0.43$  g body  
107 weight (BW) were fed at 3% BW per day with the commercial formulated  
108 feed for sea fish supplied by Skretting SpA (PERLA LARVA) composed of  
109 62% crude protein, 11% crude oils and fats, 9% crude ash, 0.8% crude fiber  
110 and 1.2% crude phosphorus. Fishes were stocked at an average density of  
111 0.5 g body weight/L.

112 Tanks were monitored daily for checking mortality; the uneaten food and  
113 faeces were siphoned out twice a week for maintaining good water quality.  
114 A 30% water exchange was weekly performed, and a part of this 30% was

115 employed as wastewater in our experiment. Wastewater was taken at the  
116 inlet of the tank, after UV lamp.

117

### 118 **2.1.2 Microalgae culture**

119 The microalgae species were provided by the Agency for Agricultural  
120 Research in Sardinia (AGRIS) and sourced from the Culture Collection for  
121 Algae and Protozoa (CCAP: Oban, Scotland). Pre-culture inocula were  
122 permanently kept in Erlenmeyer flasks in Pyrex glass with total capacity of  
123 2 L, closed with cotton and covered with gauze and aluminum foil. NSW  
124 was autoclaved at 121 °C for 30 min and enriched with Guillard F/2  
125 medium (Guillard 1975; Guillard and Ryther 1962). Cultures were exposed  
126 to a constant illumination ( $155 \mu\text{mol/s/m}^2$ ) provided by 4 fluorescent lamps  
127 (OSRAM type Natura). Continuous aeration 3 L/min was supplied by  
128 peristaltic pump (ECOH Air Pump) and temperature was maintained at 23  
129 °C by air conditioning.

130

### 131 **2.1.3 Experimental design**

132 Nutrient uptake and biomass production of *T. suecica*, *I. galbana* and *D.*  
133 *tertiolecta* were evaluated during seven days in batch conditions using two  
134 completely mixed bubble column photobioreactors of 6 L; five runs were  
135 done for a total of three replicates per treatment.

136 Lighting system was composed by four neon daylight lamp (four fluorescent  
137 lamps type cool daylight, OSRAM Lumilux FQ 24W/865), with light

138 intensity of 100  $\mu\text{mol/s/m}^2$ . This system was monitored with a  
139 Programmable Logic Controller (PLC) that it is a device that performs  
140 discrete or continuous control logic in process plant or factory environments  
141 (Figure 2). These controllers are hardware and software engineered  
142 microcomputers, used to provide industrial control operations (Netto et al.,  
143 2013). Reactors were equipped with temperature and aeration regulation  
144 control system; temperature was maintained at 23 °C, aeration was ensured  
145 by a blower at flow rate of 3 L/min. On the contrary, pH was not controlled  
146 and resulted at  $7.7 \pm 0.2$ . Phytoplankton laboratory-culture methods and  
147 photobioreactors operation were adopted according to Saiu et al., (2016).

148 Microalgae growth was measured as dry weight biomass (DW) (Clasceri *et*  
149 *al.* 1999). DW was measured once a day in 40 mL of water sample  
150 previously filtered through 0.45  $\mu\text{m}$  Whatman fiber-glass. After filtration,  
151 filters were washed with 20 mL of deionized water to remove salts and dried  
152 in an oven at 105 °C until constant weight, following Saiu et al., (2016). The  
153 supernatant liquid fraction obtained after filtration was used for nitrate,  
154 nitrite, ammonia and phosphorous analysis. In order to monitor the  
155 microalgae nutrient uptake, nutrients were daily analysed by an automatic  
156 chemical analyzer  $\mu\text{CHEM}$  based on Loop Flow Analysis (Systea, Italy).  
157 Microalgae removal efficiencies of Dissolved Inorganic Nitrogen (DIN) and  
158 Dissolved Inorganic Phosphorous (DIP) were calculated according to the  
159 method used by Michels et al., (2014), as follow:

160 N removal efficiency (%) =  $((\text{DIN influent} - \text{DIN effluent}) / \text{DIN influent}) \times$   
161 100

162 P removal efficiency (%) = ((DIP influent - DIP effluent / DIP influent) x  
163 100

164 DIN values were calculated as the sum of nitrite (NO<sub>2</sub><sup>-</sup>), nitrate (NO<sub>3</sub><sup>-</sup>) and  
165 ammonia (NH<sub>4</sub><sup>+</sup>), while DIP corresponded to the total dissolved phosphate  
166 (PO<sub>4</sub><sup>3-</sup>).

167

#### 168 **2.1.4 Statistical analysis**

169 Data were analyzed by Statistica 6.1 StatSoft, Inc. (2004). Differences in the  
170 removal efficiencies among phytoplankton species were analysed using  
171 analysis of variance (ANOVA). Shapiro Wilk's W test was used to verify  
172 the normality of the data distribution and Levene's test was used to verify  
173 the homogeneity of variances. Biomass was analyzed using repeated-  
174 measures ANOVA, with species as independent factor and days as repeated  
175 factor. Tukey's honestly-significant difference (HSD) test was used to  
176 evaluate all pair-wise treatment comparisons ( $p < 0.05$ ).

177

### 178 **3.1 Results**

179 The nutrient concentration of the wastewater was regularly measured before  
180 each experiments (Table 1). It was possible to observe that the composition  
181 of wastewater was very similar in each experiment, being nitrate the N  
182 species with the higher concentration.



### 183 **3.1.1 Nutrients removal efficiency**

184 At the end of the experiment a clearly higher DIN removal efficiency ( $p <$   
185  $0.001$ , two-way ANOVA) resulted for *T. suecica* ( $94.4 \pm 1.0\%$ , mean  $\pm$  SE)  
186 and *D. tertiolecta* ( $95.4 \pm 0.3\%$ ) in comparison with *I. galbana* ( $66.0 \pm$   
187  $1.5\%$ ). There were not statistical differences between the three species in the  
188 removal of DIP at the end of the experiments (Table 2).

189 *T. suecica* and *D. tertiolecta* showed a similar pattern of nutrient uptake  
190 (Figure 3 A, 3 C). Both species removed more than 90% of DIN and DIP  
191 after 2 and 1 day, respectively. On the contrary, *I. galbana* showed a slower  
192 nutrient uptake, lower than 35% and 80% removal for DIN and DIP,  
193 respectively, after 2 days (Figure 3 B). The nutrient uptake of DIN showed  
194 significant differences ( $p < 0.001$ ) between *I. galbana* and the other two  
195 phytoplankton species (Repeated-measures ANOVA).

196

### 197 **3.1.2 Biomass yield**

198 Ciliate protozoan *Paramecium* spp. was observed in all cultures through the  
199 duration of the experiment, but we did not evaluate the abundance of this  
200 species. This was mainly due to lack of the wastewater pre-treatment  
201 procedures (i.e. filtration and sterilization). We found a significant  
202 difference in biomass yield among the three species (Repeated measures  
203 ANOVA,  $p < 0.001$ ). *T. suecica* resulted in a higher DW ( $0.57 \pm 0.02$  g/L,  
204 mean  $\pm$  SE) than *I. galbana* ( $0.12 \pm 0.01$  g/L) from 3 days up to the end of  
205 the experiment,  $0.60 \pm 0.03$  g/L for *T. suecica* and  $0.16 \pm 0.02$  g/L for *I.*

206 *galbana*. We found no difference between *D. tertiolecta* and the other two  
207 species (Figure 4).

208

#### 209 **4.1 Discussion**

210 In this study, we tested the capability of three microalgae species to remove  
211 nutrients dissolved in the wastewater of a hatchery pilot rearing system of  
212 *M. cephalus*. We found two out of three species, *T. suecica* and *D.*  
213 *tertiolecta*, able to remove more than 90% of the DIN and DIP after two  
214 days of treatment. Differently, the phytoplankton species *I. galbana*  
215 employed 7 days to remove 92% of DIN, while DIP were not completely  
216 removed at the end of the experiment (66%).

217 This is the first time that the *D. tertiolecta* was used as aquaculture  
218 wastewater species, while previous studies obtained efficient results by  
219 using *T. suecica*. Michels et al., (2014) showed that with a biomass  
220 concentration of 0.5 g/L, *T. suecica* resulted in a removal efficiency of  
221 49.4% for N and 99.0% for P, after 15 days and using continuously operated  
222 tubular photobioreactor. Michels et al., (2014) obtained an higher N removal  
223 efficiency ( $95.7 \pm 1.0\%$ ) after addition of extra orthophosphate to  
224 compensate the insufficient amount of DIP in the wastewater. Culturing *T.*  
225 *suecica* under batch condition, on the contrary, Borges et al., (2005)  
226 obtained a maximum P removal of only 52-63% at 8 days, even after  
227 nutrient (+N) ratio correction.

228 The growth of microalgae is influenced by the culture medium composition  
229 and variables such as temperature, light intensity and pH (Molina *et al.*

230 1991). Moreover, it was previously observed that other factors are  
231 determinant for the growth of phytoplankton, as the N:P ratio. Once  
232 microalgae reaches the stationary phase, indeed, Molina *et al.* (1991)  
233 observed that the biomass concentration increases with the N:P ratio up to  
234 different levelling-off values, which depends upon temperature, with  
235 concentration remaining nearly constant for values beyond this point. At 25  
236 °C, the N:P levelling-off value registered by Molina *et al.* (1991) for  
237 *Tetraselmis* spp. (10) is lower than values registered in the wastewater used  
238 for this study, 18 for *D. tertiolecta*, 16.3 for *I. galbana* and 32 for *T.*  
239 *suecica*.

240 In this study, the highest biomass yield (DW) was obtained with *T. suecica*,  
241  $0.6 \pm 0.06$  g/L, while  $0.38 \pm 0.06$  and  $0.16 \pm 0.04$  g/L was recorded for *D.*  
242 *tertiolecta* and *I. galbana*, respectively, at the end of the experiment. We  
243 hypothesize that these differences were due to a diverse species-specific cell  
244 size; according to FAO (2004), indeed, *T. suecica* has the largest median  
245 cell volume ( $300 \mu\text{m}^3$ ), followed by *D. tertiolecta* ( $170 \mu\text{m}^3$ ) and *I. galbana*  
246 ( $40\text{-}50 \mu\text{m}^3$ ).

247 *I. galbana* is not suitable for the nutrient removal of *M. cephalus*  
248 aquaculture wastewater. According with Borges et al., (2005) *I. galbana*  
249 resulted in a low biomass yield and removal efficiency of DIN and DIP. We  
250 hypothesize that the ciliate *Paramecium* spp. influenced negatively the  
251 growth of *I. galbana*, because this organism effectively feeds on other live  
252 microorganisms (Wichterman 1986). *Paramecium* spp. was observed also in  
253 the cultures of *T. suecica* and *D. tertiolecta*, but the presence of this  
254 protozoan did not seem to affect the growth of these phytoplankton species.

255 *I. galbana* is smaller than the other two species, therefore it could be a more  
256 easy prey for the zooplankton. Moreover, it has been previously reported a  
257 large spectrum of antimicrobial activity and antibiotic substances of the  
258 genus *Tetraselmis* spp. (Austin et al., 1992; Austin and Day 1990) and  
259 *Dunaliella* spp. (Chang et al., 1993), which could limit the negative effects  
260 of *Paramecium* spp. on the growth of cultures. When aquaculture  
261 wastewater is used as a nutrient source for algae, sterilization may be  
262 necessary to minimize the negative effects of bacteria and other organisms  
263 on the algae growth (Cai et al., 2013; Stein 1979). However, sterilization  
264 process increases the capital cost of the algae cultivation system,  
265 representing a negative point for an efficient phytoplankton bioremediation  
266 system at large scale. Microalgae production, indeed, must be a low cost  
267 system, easily installable and maintainable (Cai et al., 2013). Avoiding to  
268 pre-treat and sterilize the wastewater, as in our experiment, reflects in a  
269 reduction of management costs, as manual labour and energy. Moreover, it  
270 was demonstrated that microalgae cultures with protozoans such as  
271 *Paramecium* spp. represent suitable diets for fish fries (FAO 1980).

272 During last decade, research efforts have been focused towards the  
273 development of more efficient, higher surface-to-volume ratio  
274 photobioreactors for microalgae cultivation (Tredici 2004; Rodolfi et al.,  
275 2008). This is the first study that compared the ability of these three  
276 microalgae species in nutrient removal of aquaculture wastewater by using  
277 controlled bubble column annular photobioreactors. Gao et al., (2016)  
278 recently tested *Chlorella vulgaris* and *Scenedesmus obliquus* cultivated in  
279 shrimp *Penaeus vannamei* Boone wastewater, in batch conditions and by  
280 using photobioreactors. A better performance in the biomass production was

281 recorded for *C. vulgaris* (7.3 mg/L/day) in comparison with *S. obliquus* (6.2  
282 mg/L/day).

283

## 284 **5.1 Conclusion**

285 This study confirms the potential of *T. suecica* in the assimilation of  
286 nutrients dissolved in aquaculture wastewater and in the production of  
287 biomass. *D. tertiolecta* also resulted suitable for bioremediation, removing  
288 more than 90% of dissolved inorganic nitrogen and phosphorous.  
289 Differently from *I. galbana*, *T. suecica* and *D. tertiolecta* are able to grow  
290 well in no sterilized culture media contaminated with bacteria and  
291 zooplankton (*Paramecium* spp.), reflecting in the potential to reduce manual  
292 labour and energy costs for pre-treatment of culture medium in a  
293 phytoplankton bioremediation system.

294 *T. suecica* and *D. tertiolecta* are valid candidate for the employment in  
295 IMTA systems. They can be cultivated for bioremediation of finfish or  
296 shrimp wastewater and biomass produced can be re-used as live-feed for  
297 hatchery-grown of herbivorous and filter feeders (Alsull and Omar 2012;  
298 Michels et al., 2014). Nevertheless, further studies will be needed to assess  
299 the biochemical composition of these phytoplankton species cultivated in  
300 aquaculture wastewater and to evaluate their effects as live-feed.

301

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**Table 1.** Nutrients dissolved in the *Mugil cephalus* wastewater. Values are expressed as mean  $\pm$  SE (n= 3).

	<i>Tetraselmis suecica</i>	<i>Dunaliella tertiolecta</i>	<i>Isochrysis galbana</i>
<b>NO<sub>3</sub><sup>-</sup> -N (mg/L)</b>	4.1 $\pm$ 0.4	4.2 $\pm$ 0.1	4.2 $\pm$ 0.4
<b>NO<sub>2</sub><sup>-</sup> -N (mg/L)</b>	0.2 $\pm$ 0.1	0.2 $\pm$ 0.1	0.1 $\pm$ 0.1
<b>NH<sub>4</sub><sup>+</sup> -N (mg/L)</b>	0.3 $\pm$ 0.1	0.3 $\pm$ 0.1	0.2 $\pm$ 0.1
<b>PO<sub>4</sub><sup>3-</sup> -P (mg/L)</b>	0.3 $\pm$ 0.1	0.6 $\pm$ 0.1	0.6 $\pm$ 0.1

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**Table 2.** Influent and effluent DIN and DIP values (mg/L) and removal efficiency (%) of *Tetraselmis suecica*, *Dunaliella tertiolecta* and *Isochrysis galbana*. Values are expressed as mean  $\pm$  SE (n= 3). Superscripts indicate significant differences among species.

	<i>Tetraselmis suecica</i>	<i>Dunaliella tertiolecta</i>	<i>Isochrysis galbana</i>
<b>DIN Influent (mg/L)</b>	4.5 $\pm$ 0.5	4.6 $\pm$ 0.1	4.6 $\pm$ 0.5
<b>DIN Effluent (mg/L)</b>	0.3 $\pm$ 0.1	0.2 $\pm$ 0.1	1.6 $\pm$ 0.1
<b>DIN %</b>	94.4 $\pm$ 1.0 <sup>a</sup>	95.4 $\pm$ 0.3 <sup>a</sup>	66.0 $\pm$ 1.5 <sup>b</sup>
<b>DIP Influent (mg/L)</b>	0.3 $\pm$ 0.1	0.6 $\pm$ 0.1	0.6 $\pm$ 0.1
<b>DIP Effluent (mg/L)</b>	0.1 $\pm$ 0.1	0.1 $\pm$ 0.1	0.1 $\pm$ 0.1
<b>DIP %</b>	96.0 $\pm$ 2.5	91.2 $\pm$ 2.3	91.9 $\pm$ 4.0

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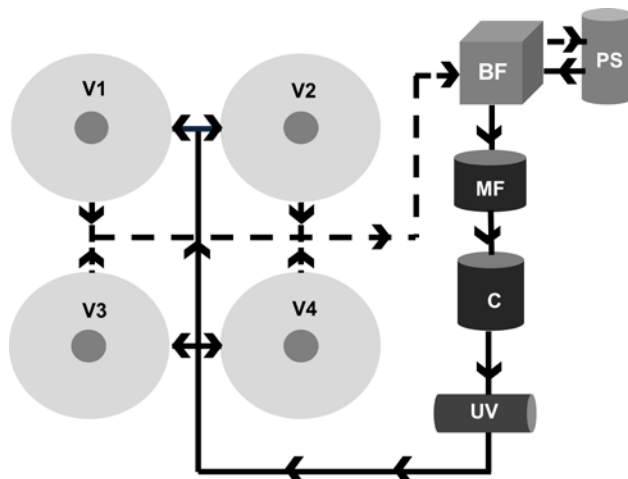
588 **Figure 1: Recirculating aquaculture system (RAS) for rearing of juvenile grey**  
589 **mulletts *Mugil cephalus*, consisting of four circular fiberglass tanks with 2000**  
590 **L volume (V1, V2, V3 and V4). The system was equipped with biological (BF)**  
591 **and mechanical filter (MF), protein skimmer (PS), chiller (C) and UV lamp**  
592 **(UV). Dotted arrow = seawater outlet; continuous arrow = seawater intake.**

593 **Figure 2: Bubble column annular photobioreactors of 6 L volume (R1 and**  
594 **R2) used for the growth of phytoplankton, supplied with LIGHT,**  
595 **Programmable Logic Controller (PLC), gentle aeration (AIR), probes for**  
596 **temperature (T) and pH (pH).**

597 **Figure 3: Nutrient uptake (%) of Dissolved Inorganic Nitrogen (DIN) and**  
598 **Dissolved Inorganic Phosphorous (DIP) for *Tetraselmis suecica* (A),**  
599 ***Isochrysis galbana* (B) and *Dunaliella tertiolecta* (C), during 7 days. Values are expressed**  
600 **as mean  $\pm$  SE (n= 3).**

601 **Figure 4: Microalgal growth curves as DW (g/L) of *Tetraselmis suecica*,**  
602 ***Isochrysis galbana* and *Dunaliella tertiolecta*, during 7 days. Values are**  
603 **expressed as mean  $\pm$  SE (n= 3). Superscripts indicate significant differences**  
604 **among species.**

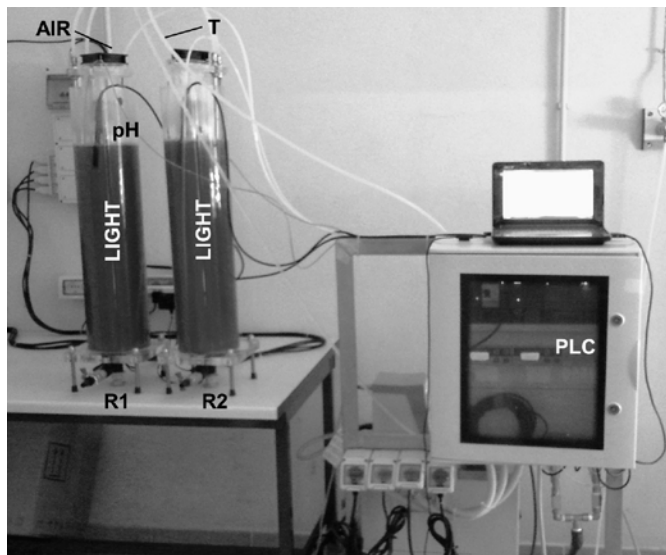
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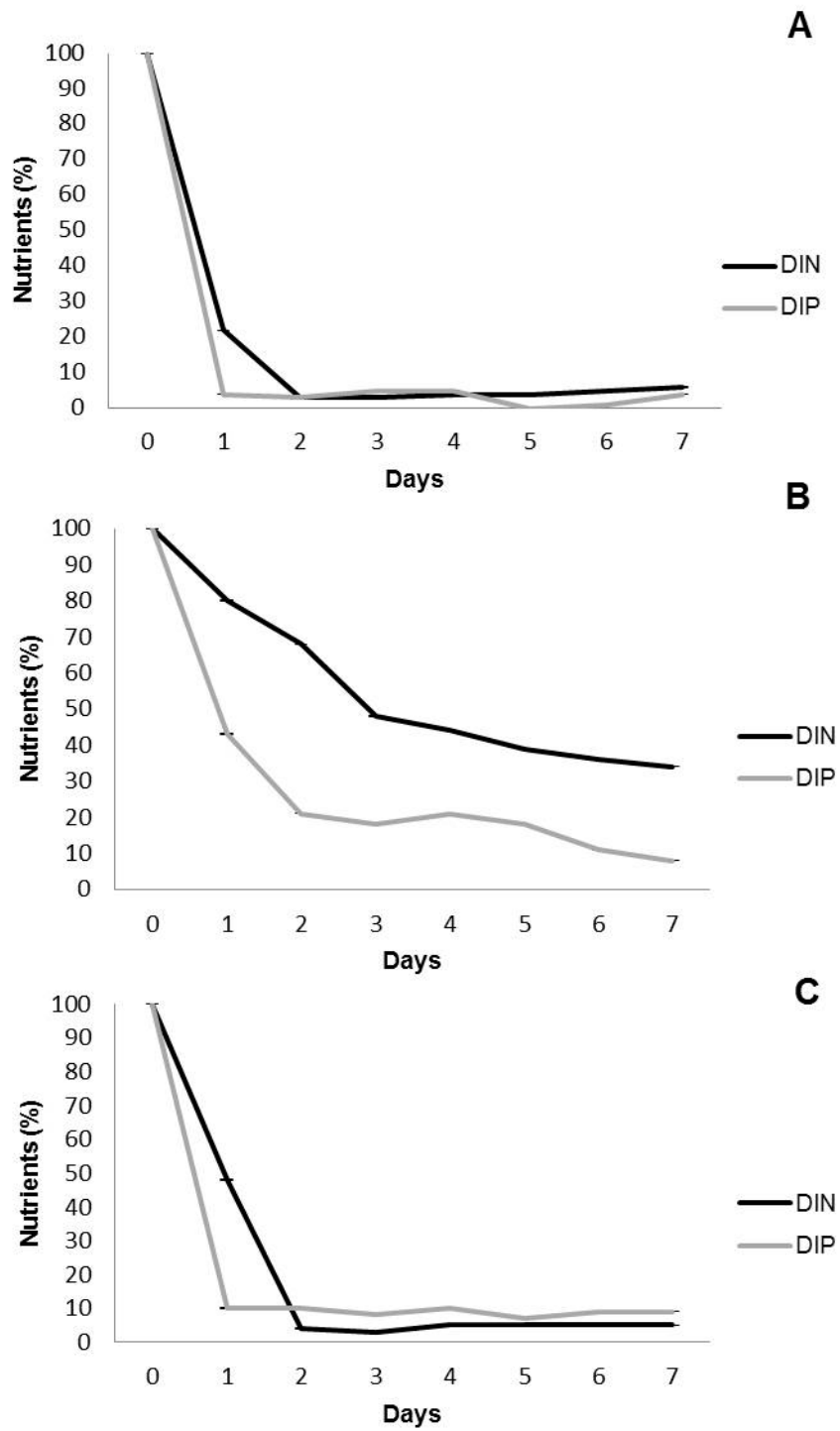
**Figure 2**





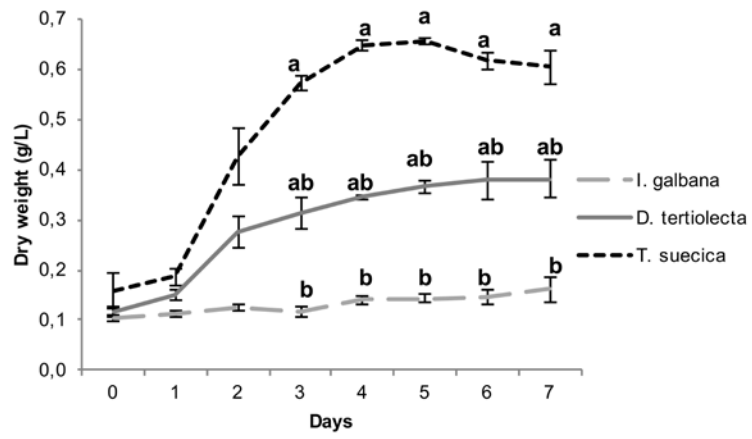
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**Figure 2**



**Figure 3**

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**Figure 4**